April 24, 2020

Rhonda Romero
New Mexico Environment Department
Air Quality Bureau
525 Camino de los Marquez, Suite 1
Santa Fe, New Mexico, 87505

RE: Significant Revision to NSR Permit 7877
Cowboy CDP
XTO Energy Inc.

Dear Ms. Romero:

XTO Energy Inc. is submitting the attached application for a significant revision to NSR Permit 7877. See Section 3 for details regarding the nature of the permit revisions. Please note Tab 24 of the permit application contains information XTO Energy Inc. deems Confidential Business Information. Two copies of the application have been provided, along with two copies of the confidential information, which are provided in a manila folder.

Also included are CDs containing the electronic and modeling files, as well as a check for the filing fee. If you have any questions regarding these applications, please contact me at (865) 850-2007 or etullos@pei-tx.com.

Sincerely,

Evan Tullos

Evan Tullos
Vice President

Cowboy CDP

Eddy County, New Mexico

NSR Modification Permit Application

PREPARED BY:
Benjamin Schneider
Environmental Engineer

04/08/2020

Cowboy CDP

NSR Modification Permit Application

Table of Contents

Tab 1

UA1 Form - Company and Facility Information

Mail Application To:		For Department use only:
New Mexico Environment Department Air Quality Bureau Permits Section 525 Camino de los Marquez, Suite 1 Santa Fe, New Mexico, 87505 Phone: (505) 476-4300 Fax: (505) 476-4375 www.env.nm.gov/aqb		AIRS No.:

Universal Air Quality Permit Application

Use this application for NOI, NSR, or Title V sources.

Use this application for: the initial application, modifications, technical revisions, and renewals. For technical revisions, complete Sections, 1-A, 1-B, 2-E, 3, 9 and any other sections that are relevant to the requested action; coordination with the Air Quality Bureau permit staff prior to submittal is encouraged to clarify submittal requirements and to determine if more or less than these sections of the application are needed. Use this application for streamline permits as well. See Section 1-I for submittal instructions for other permits.

This application is submitted as (check all that apply)**:** ☐ Request for a No Permit Required Determination (no fee)
☐ **Updating** an application currently under NMED review. Include this page and all pages that are being updated (no fee required).
Construction Status: ☐ Not Constructed ☑ Existing Permitted (or NOI) Facility ☐ Existing Non-permitted (or NOI) Facility
Minor Source: ☐ a NOI 20.2.73 NMAC ☑ 20.2.72 NMAC application or revision ☐ 20.2.72.300 NMAC Streamline application
Title V Source: ☐ Title V (new) ☐ Title V renewal ☐ TV minor mod. ☐ TV significant mod. TV Acid Rain: ☐ New ☐ Renewal
PSD Major Source: ☐ PSD major source (new) ☐ minor modification to a PSD source ☐ a PSD major modification

Acknowledgements:

☑ I acknowledge that a pre-application meeting is available to me upon request. ☐ Title V Operating, Title IV Acid Rain, and NPR applications have no fees.
☑ $500 NSR application Filing Fee enclosed OR ☐ The full permit fee associated with 10 fee points (required w/ streamline applications).
☑ Check No.: 1301 in the amount of $500
☑ I acknowledge the required submittal format for the hard copy application is printed double sided 'head-to-toe', 2-hole punched (except the Sect. 2 landscape tables is printed 'head-to-head'), numbered tab separators. Incl. a copy of the check on a separate page.
☐ This facility qualifies to receive assistance from the Small Business Environmental Assistance program (SBEAP) and qualifies for 50% of the normal application and permit fees. Enclosed is a check for 50% of the normal application fee which will be verified with the Small Business Certification Form for your company.
☐ This facility qualifies to receive assistance from the Small Business Environmental Assistance Program (SBEAP) but does not qualify for 50% of the normal application and permit fees. To see if you qualify for SBEAP assistance and for the small business certification form go to https://www.env.nm.gov/aqb/sbap/small_business_criteria.html).

Citation: Please provide the **low level citation** under which this application is being submitted: **20.2.72.219.B.1.d NMAC**
(e.g. application for a new minor source would be 20.2.72.200.A NMAC, one example for a Technical Permit Revision is 20.2.72.219.B.1.b NMAC, a Title V acid rain application would be: 20.2.70.200.C NMAC)

Section 1 – Facility Information

Section 1-A: Company Information		AI # if known (see 1st 3 to 5 #s of permit IDEA ID No.):384481	Updating Permit/NOI #: 7877
1	Facility Name: Cowboy Central Delivery Point (CDP)	Plant primary SIC Code (4 digits): 1311 Plant NAIC code (6 digits): 211120	
a	Facility Street Address (If no facility street address, provide directions from a prominent landmark): See 1-D.4.		
2	Plant Operator Company Name: XTO Energy Inc.	Phone/Fax: (832) 624-4426	
a	Plant Operator Address: 22777 Springwoods Village Parkway, W4.6B.374, Spring, TX 77389		
b	Plant Operator's New Mexico Corporate ID or Tax ID: 1522747		

3	Plant Operator Company Name: XTO Energy Inc.	Phone/Fax: (832) 624-4426
a	Plant Owner(s) Mailing Address(s): 22777 Springwoods Village Parkway, W4.6B.374, Spring, TX 77389	
4	Bill To (Company): XTO Energy Inc.	Phone/Fax: (832) 624-4426
a	Mailing Address: 22777 Springwoods Village Parkway, W4.6B.374, Spring, TX 77389	E-mail: Benjamin_Schneider@xtoenergy.com
5	☐ Preparer: ☑ Consultant: Evan Tullos	Phone/Fax: (865) 850-2007
a	Mailing Address: 5 Cardinal Court; Edwardsville, IL 620205	E-mail: etullos@pei-tx.com
6	Plant Operator Contact: Benjamin Schneider	Phone/Fax: (832) 624-2768
a	Mailing Address: 22777 Springwoods Village Parkway, W4.6B.374, Spring, TX 77389	E-mail: Benjamin_Schneider@xtoenergy.com
7	Air Permit Contact: Benjamin Schneider	Title: Environmental Engineer
a	E-mail: Benjamin_Schneider@xtoenergy.com	Phone/Fax: (832) 624-2768
b	Mailing Address: 22777 Springwoods Village Parkway, W4.6B.374, Spring, TX 77389	
c	The designated Air permit Contact will receive all official correspondence (i.e. letters, permits) from the Air Quality Bureau.	

Section 1-B: Current Facility Status

1.a	Has this facility already been constructed? ☐ Yes ☑ No	1.b If yes to question 1.a, is it currently operating in New Mexico? ☐ Yes ☐ No
2	If yes to question 1.a, was the existing facility subject to a Notice of Intent (NOI) (20.2.73 NMAC) before submittal of this application? ☐ Yes ☐ No	If yes to question 1.a, was the existing facility subject to a construction permit (20.2.72 NMAC) before submittal of this application? ☐ Yes ☐ No
3	Is the facility currently shut down? ☐ Yes ☑ No	If yes, give month and year of shut down (MM/YY):
4	Was this facility constructed before 8/31/1972 and continuously operated since 1972? ☐ Yes ☑ No	
5	If Yes to question 3, has this facility been modified (see 20.2.72.7.P NMAC) or the capacity increased since 8/31/1972? ☐Yes ☐No ☐N/A	
6	Does this facility have a Title V operating permit (20.2.70 NMAC)? ☐ Yes ☑ No	If yes, the permit No. is: P-
7	Has this facility been issued a No Permit Required (NPR)? ☐ Yes ☑ No	If yes, the NPR No. is:
8	Has this facility been issued a Notice of Intent (NOI)? ☐ Yes ☐ No	If yes, the NOI No. is:
9	Does this facility have a construction permit (20.2.72/20.2.74 NMAC)? ☑Yes ☐ No	If yes, the permit No. is: 7877
10	Is this facility registered under a General permit (GCP-1, GCP-2, etc.)? ☐ Yes ☑ No	If yes, the register No. is:

Section 1-C: Facility Input Capacity & Production Rate

1	What is the facility's maximum input capacity, specify units (reference here and list capacities in Section 20, if more room is required)			
a	Current	Hourly: 33.3 MMSCF and 62,500 Barrels	Daily: 800 MMSCF and 1.5 MM Barrels	Annually: 2.92 BSCF and 547.5 MM Barrels
b	Proposed	Hourly: 41.7 MSCF Natural Gas 25,000 Barrels Condensate Barrels Natural Gas Liquids	Daily: 1 MMSCF Natural Gas 600,000 Barrels Condensate 190,000 Barrels Natural Gas Liquids	Annually: 356 MMSCF Natural Gas 219 MM Barrels Condensate 69.35 MM Barrels Natural Gas Liquids
2	What is the facility's maximum production rate, specify units (reference here and list capacities in Section 20, if more room is required)			
a	Current	Hourly: 33.3 MMSCF and 62,500 Barrels	Daily: 800 MMSCF and 1.5 MM Barrels	Annually: 2.92 BSCF and 547.5 MM Barrels
b	Proposed	Hourly: 41.7 MSCF Natural Gas 25,000 Barrels Condensate Barrels Natural Gas Liquids	Daily: 1 MMSCF Natural Gas 600,000 Barrels Condensate 190,000 Barrels Natural Gas Liquids	Annually: 356 MMSCF Natural Gas 219 MM Barrels Condensate 69.35 MM Barrels Natural Gas Liquids

Section 1-D: Facility Location Information

1	Section: 1	Range: 30E	Township: 25S	County: Eddy	Elevation (ft):
2	UTM Zone: ☐ 12 or ☑ 13			Datum: ☐ NAD 27 ☐ NAD 83 ☑ WGS 84	
a	UTM E (in meters, to nearest 10 meters): 609230			UTM N (in meters, to nearest 10 meters): 3558750	
b	**AND** Latitude (deg., min., sec.): 32º 09' 36"			Longitude (deg., min., sec.): -103º 50' 30"	
3	Name and zip code of nearest New Mexico town: Malaga - 88263				
4	Detailed Driving Instructions from nearest NM town (attach a road map if necessary): Head W on Duarte Rd. for 1.3 mi. to R on McDonald Rd. Drive 11.2 mi. to R on Twin Wells Rd. In 0.6 mi. take slight left to stay on Twin Wells Rd. Drive 1.4 mi. to R on Buck Jackson Rd. Site will be of L in 0.6 mi.				
5	The facility is 14 (distance) miles SE (direction) of Malaga (nearest town).				
6	Status of land at facility (check one): ☐ Private ☐ Indian/Pueblo ☑ Federal BLM ☐ Federal Forest Service ☐ Other (specify)				
7	List all municipalities, Indian tribes, and counties within a ten (10) mile radius (20.2.72.203.B.2 NMAC) of the property on which the facility is proposed to be constructed or operated: Lea				
8	**20.2.72** NMAC applications **only**: Will the property on which the facility is proposed to be constructed or operated be closer than 50 km (31 miles) to other states, Bernalillo County, or a Class I area (see www.env.nm.gov/aqb/modeling/class1areas.html)? ☑ Yes ☐ No (20.2.72.206.A.7 NMAC) If yes, list all with corresponding distances in kilometers: Texas - 17				
9	Name nearest Class I area: Carlsbad Caverns				
10	Shortest distance (in km) from facility boundary to the boundary of the nearest Class I area (to the nearest 10 meters): 49900				
11	Distance (meters) from the perimeter of the Area of Operations (AO is defined as the plant site inclusive of all disturbed lands, including mining overburden removal areas) to nearest residence, school or occupied structure: > 5				
12	Method(s) used to delineate the Restricted Area: Fencing "**Restricted Area**" is an area to which public entry is effectively precluded. Effective barriers include continuous fencing, continuous walls, or other continuous barriers approved by the Department, such as rugged physical terrain with steep grade that would require special equipment to traverse. If a large property is completely enclosed by fencing, a restricted area within the property may be identified with signage only. Public roads cannot be part of a Restricted Area.				
13	Does the owner/operator intend to operate this source as a portable stationary source as defined in 20.2.72.7.X NMAC? ☐ Yes ☑ No A portable stationary source is not a mobile source, such as an automobile, but a source that can be installed permanently at one location or that can be re-installed at various locations, such as a hot mix asphalt plant that is moved to different job sites.				
14	Will this facility operate in conjunction with other air regulated parties on the same property? ☒ No ☐ Yes If yes, what is the name and permit number (if known) of the other facility?				

Section 1-E: Proposed Operating Schedule (The 1-E.1 & 1-E.2 operating schedules may become conditions in the permit.)

1	Facility **maximum** operating ($\frac{hours}{day}$): 24	($\frac{days}{week}$): 7		($\frac{weeks}{year}$): 52	($\frac{hours}{year}$): 8760	
2	Facility's maximum daily operating schedule (if less than 24 $\frac{hours}{day}$)?	Start:	☐AM ☐PM	End:		☐AM ☐PM
3	Month and year of anticipated start of construction: Already started					
4	Month and year of anticipated construction completion: Train 1 – May 2020, Train 2 – February 2021, Train 3 – June 2021					
5	Month and year of anticipated startup of new or modified facility: Train 1 – May 2020, Train 2 – February 2021, Train 3 – June 2021					
6	Will this facility operate at this site for more than one year? ☑ Yes ☐ No					

Section 1-F: Other Facility Information

1	Are there any current Notice of Violations (NOV), compliance orders, or any other compliance or enforcement issues related to this facility? ☐ Yes ☑ No If yes, specify:

a	If yes, NOV date or description of issue:		NOV Tracking No:
b	Is this application in response to any issue listed in 1-F, 1 or 1a above? ☐ Yes ☐ No If Yes, provide the 1c & 1d info below:		
c	Document Title:	Date:	Requirement # (or page # and paragraph #):
d	Provide the required text to be inserted in this permit:		
2	Is air quality dispersion modeling or modeling waiver being submitted with this application? ☐ Yes ☑ No		
3	Does this facility require an "Air Toxics" permit under 20.2.72.400 NMAC & 20.2.72.502, Tables A and/or B? ☐ Yes ☑ No		
4	Will this facility be a source of federal Hazardous Air Pollutants (HAP)? ☑ Yes ☐ No		
a	If Yes, what type of source? ☑ **Major** (☑ ≥10 tpy of any single HAP **OR** ☐ ≥25 tpy of any combination of HAPS) **OR** ☐ **Minor** (☐ <10 tpy of any single HAP **AND** ☐ <25 tpy of any combination of HAPS)		
5	Is any unit exempt under 20.2.72.202.B.3 NMAC? ☐ Yes ☑ No		
a	If yes, include the name of company providing commercial electric power to the facility: ___________________________ Commercial power is purchased from a commercial utility company, which specifically does not include power generated on site for the sole purpose of the user.		

Section 1-G: Streamline Application

(This section applies to 20.2.72.300 NMAC Streamline applications only)

1	☐ I have filled out Section 18, "Addendum for Streamline Applications."	☑ N/A (This is not a Streamline application.)

Section 1-H: Current Title V Information - Required for all applications from TV Sources

(Title V-source required information for all applications submitted pursuant to 20.2.72 NMAC (Minor Construction Permits), or 20.2.74/20.2.79 NMAC (Major PSD/NNSR applications), and/or 20.2.70 NMAC (Title V))

1	Responsible Official (R.O.) (20.2.70.300.D.2 NMAC):	Phone:
a	R.O. Title:	R.O. e-mail:
b	R. O. Address:	
2	Alternate Responsible Official (20.2.70.300.D.2 NMAC):	Phone:
a	A. R.O. Title:	A. R.O. e-mail:
b	A. R. O. Address:	
3	Company's Corporate or Partnership Relationship to any other Air Quality Permittee (List the names of any companies that have operating (20.2.70 NMAC) permits and with whom the applicant for this permit has a corporate or partnership relationship):	
4	Name of Parent Company ("Parent Company" means the primary name of the organization that owns the company to be permitted wholly or in part.):	
a	Address of Parent Company:	
5	Names of Subsidiary Companies ("Subsidiary Companies" means organizations, branches, divisions or subsidiaries, which are owned, wholly or in part, by the company to be permitted.):	
6	Telephone numbers & names of the owners' agents and site contacts familiar with plant operations:	
7	Affected Programs to include Other States, local air pollution control programs (i.e. Bernalillo) and Indian tribes: Will the property on which the facility is proposed to be constructed or operated be closer than 80 km (50 miles) from other states, local pollution control programs, and Indian tribes and pueblos (20.2.70.402.A.2 and 20.2.70.7.B)? If yes, state which ones and provide the distances in kilometers:	

Section 1-I – Submittal Requirements

Each 20.2.73 NMAC (**NOI**), a 20.2.70 NMAC (**Title V**), a 20.2.72 NMAC (**NSR** minor source), or 20.2.74 NMAC (**PSD**) application package shall consist of the following:

Hard Copy Submittal Requirements:

1) One hard copy **original signed and notarized application package** **printed double sided** **'head-to-toe'** **2-hole punched** as we bind the document on top, not on the side; except Section 2 (landscape tables), which should be head-to-head. Please use **numbered tab separators** in the hard copy submittal(s) as this facilitates the review process. For NOI submittals only, hard copies of UA1, Tables 2A, 2D & 2F, Section 3 and the signed Certification Page are required. Please include a copy of the check on a separate page.

2) If the application is for a minor NSR, PSD, NNSR, or Title V application, include one working hard **copy** for Department use. This copy should be printed in book form, 3-hole punched, and **must be double sided**. Note that this is in addition to the head-to-to 2-hole punched copy required in 1) above. Minor NSR Technical Permit revisions (20.2.72.219.B NMAC) only need to fill out Sections 1-A, 1-B, 3, and should fill out those portions of other Section(s) relevant to the technical permit revision. TV Minor Modifications need only fill out Sections 1-A, 1-B, 1-H, 3, and those portions of other Section(s) relevant to the minor modification. NMED may require additional portions of the application to be submitted, as needed.

3) The entire NOI or Permit application package, including the full modeling study, should be submitted electronically. Electronic files for applications for NOIs, any type of General Construction Permit (GCP), or technical revisions to NSRs must be submitted with compact disk (CD) or digital versatile disc (DVD). For these permit application submittals, two CD copies are required (in sleeves, not crystal cases, please), with additional CD copies as specified below. NOI applications require only a single CD submittal. Electronic files for other New Source Review (construction) permits/permit modifications or Title V permits/permit modifications can be submitted on CD/DVD or sent through AQB's secure file transfer service.

Electronic files sent by (check one):

☐ CD/DVD attached to paper application

☑ secure electronic transfer. Air Permit Contact Name Benjamin Schneider

Email benjamin_schneider@xtoenergy.com

Phone number (832) 624-2768

a. If the file transfer service is chosen by the applicant, after receipt of the application, the Bureau will email the applicant with instructions for submitting the electronic files through a secure file transfer service. Submission of the electronic files through the file transfer service needs to be completed within 3 business days after the invitation is received, so the applicant should ensure that the files are ready when sending the hard copy of the application. The applicant will not need a password to complete the transfer. **Do not use the file transfer service for NOIs, any type of GCP, or technical revisions to NSR permits.**

4) Optionally, the applicant may submit the files with the application on compact disk (CD) or digital versatile disc (DVD) following the instructions above and the instructions in 5 for applications subject to PSD review.

5) If **air dispersion modeling** is required by the application type, include the **NMED Modeling Waiver** and/or electronic air dispersion modeling report, input, and output files. The dispersion modeling ***summary report only*** should be submitted as hard copy(ies) unless otherwise indicated by the Bureau.

6) If the applicant submits the electronic files on CD and the application is subject to PSD review under 20.2.74 NMAC (PSD) or NNSR under 20.2.79 NMC include,
   a. one additional CD copy for US EPA,
   b. one additional CD copy for each federal land manager affected (NPS, USFS, FWS, USDI) and,
   c. one additional CD copy for each affected regulatory agency other than the Air Quality Bureau.

   If the application is submitted electronically through the secure file transfer service, these extra CDs do not need to be submitted.

Electronic Submittal Requirements [in addition to the required hard copy(ies)]:

1) All required electronic documents shall be submitted as 2 separate CDs or submitted through the AQB secure file transfer service. Submit a single PDF document of the entire application as submitted and the individual documents comprising the application.

2) The documents should also be submitted in Microsoft Office compatible file format (Word, Excel, etc.) allowing us to access the text and formulas in the documents (copy & paste). Any documents that cannot be submitted in a Microsoft Office compatible format shall be saved as a PDF file from within the electronic document that created the file. If you are unable to provide

Microsoft office compatible electronic files or internally generated PDF files of files (items that were not created electronically: i.e. brochures, maps, graphics, etc,), submit these items in hard copy format. We must be able to review the formulas and inputs that calculated the emissions.

3) It is preferred that this application form be submitted as 4 electronic files (3 MSWord docs: Universal Application section 1 [UA1], Universal Application section 3-19 [UA3], and Universal Application 4, the modeling report [UA4]) and 1 Excel file of the tables (Universal Application section 2 [UA2]). Please include as many of the 3-19 Sections as practical in a single MS Word electronic document. Create separate electronic file(s) if a single file becomes too large or if portions must be saved in a file format other than MS Word.

4) The electronic file names shall be a maximum of 25 characters long (including spaces, if any). The format of the electronic Universal Application shall be in the format: "A-3423-FacilityName". The "A" distinguishes the file as an application submittal, as opposed to other documents the Department itself puts into the database. Thus, all electronic application submittals should begin with "A-". Modifications to existing facilities should use the core permit number (i.e. '3423') the Department assigned to the facility as the next 4 digits. Use 'XXXX' for new facility applications. The format of any separate electronic submittals (additional submittals such as non-Word attachments, re-submittals, application updates) and Section document shall be in the format: "A-3423-9-description", where "9" stands for the section # (in this case Section 9-Public Notice). Please refrain, as much as possible, from submitting any scanned documents as this file format is extremely large, which uses up too much storage capacity in our database. Please take the time to fill out the header information throughout all submittals as this will identify any loose pages, including the Application Date (date submitted) & Revision number (0 for original, 1, 2, etc.; which will help keep track of subsequent partial update(s) to the original submittal. Do not use special symbols (#, @, etc.) in file names. The footer information should not be modified by the applicant.

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Tab 2
UA2 Form - Application Tables

Cross reference table of all units in both permits

Unit numbers must correspond to unit numbers in the previous permit unless a complete cross reference table of all units in both permits is provided. This table completes that requirement.

Previous Unit Number	Previous Source Description	New Unit Number	New Source Description
1	Hot Oil Heater 1	SHTR1	Stabilization Hot Oil Heater (58.93 MMBtu/hr)
2	Hot Oil Heater 2	SHTR2	Stabilization Hot Oil Heater (58.93 MMBtu/hr)
3	Hot Oil Heater 3	SHTR3	Stabilization Hot Oil Heater (58.93 MMBtu/hr)
4	Hot Oil Heater 4	SHTR4	Stabilization Hot Oil Heater (58.93 MMBtu/hr)
5	Hot Oil Heater 5	SHTR5	Stabilization Hot Oil Heater (58.93 MMBtu/hr)
6	Hot Oil Heater 6	SHTR6	Stabilization Hot Oil Heater (58.93 MMBtu/hr)
7	Hot Oil Heater 7	SHTR7	Stabilization Hot Oil Heater w/ SCR catalyst (58.93 MMBtu/hr)
8	Hot Oil Heater 8	SHTR8	Stabilization Hot Oil Heater w/ SCR catalyst (58.93 MMBtu/hr)
9	Hot Oil Heater 9	SHTR9	Stabilization Hot Oil Heater w/ SCR catalyst (58.93 MMBtu/hr)
10	Hot Oil Heater 10	SHTR10	Stabilization Hot Oil Heater w/ SCR catalyst (58.93 MMBtu/hr)
		SHTR11	Stabilization Hot Oil Heater w/ SCR catalyst (58.93 MMBtu/hr)
12	Hot Oil Heater 1	CHTR1	Cryo Hot Oil Heater (94.54 MMBtu/hr)
13	Hot Oil Heater 2	CHTR2	Cryo Hot Oil Heater (94.54 MMBtu/hr)
14	Hot Oil Heater 3	CHTR3	Cryo Hot Oil Heater w/ SCR Catalyst (94.54 MMBtu/hr)
15	Hot Oil Heater 4	CHTR4	Cryo Hot Oil Heater w/ SCR Catalyst (94.54 MMBtu/hr)
16	Regen Heater 1	RHTR1	Regen Heater (35.25 MMBtu/hr)
17	Regen Heater 2	RHTR2	Regen Heater (35.25 MMBtu/hr)
18	Regen Heater 3	RHTR3	Regen Heater (35.25 MMBtu/hr)
19	Regen Heater 4	RHTR4	Regen Heater (35.25 MMBtu/hr)
20	Emergency Flare 1	FL2	Cryo Flare 1 (Dual Tip Flare)
21	Emergency Flare 2	FL1	Stabilizer Flare 2 (Dual Tip Flare)
22	Emergency Flare 3	FL3	Backup SSM/Emergency Flare 3 (Dual Tip Flare)
23	Tank 1 - RVP 9 (50,000 bbl)	IFR1	Oil Storage Tank 1 (50,000 bbl)
24	Tank 2 - RVP 9 (50,000 bbl)	IFR2	Oil Storage Tank 2 (50,000 bbl)
25	Tank 3 - RVP 10.4 (50,000 bbl)	IFR3	Oil Storage Tank 3 (50,000 bbl)
26	Tank 3 - RVP 10.4 (50,000 bbl)	IFR4	Oil Storage Tank 4 (50,000 bbl)
27	Tank 5 - RVP 9 (250,000 bbl)	IFR5	Oil Storage Tank 5 (250,000 bbl)
28	Tank 6 - RVP 9 (250,000 bbl)	IFR6	Oil Storage Tank 6 (250,000 bbl)
29	Tank 7 - RVP 9 (250,000 bbl)	IFR7	Oil Storage Tank 7 (250,000 bbl)
30	Tank 8 - RVP 9 (250,000 bbl)	IFR8	Oil Storage Tank 8 (250,000 bbl)
35	Combustor	ECD1	Combustor
36	TO-1	TO1	Thermal Oxidizer
37	TO-2	TO2	Thermal Oxidizer
38	TO-3	TO3	Thermal Oxidizer
39	TO-4	TO4	Thermal Oxidizer
42	Fugitives	FUG	Fugitives
43	MSS Floating Roof Landing 250 KBBL Tanks	SSM	SSM Emissions
44	MSS Misc	SSM	SSM Emissions
43	MSS Floating Roof Landing 50 KBBL Tanks	SSM	SSM Emissions
46	MSS Blowdowns	FL1-FL3OVHD-SSM	FL1-FL3 Stabilizer Overhead SSM Gas
46	MSS Blowdowns	FL1-FL3CRYO-SSM	FL1-FL3 Cryo Blowdown SSM Gas
47	Haul Road Fugitives	ROAD	Haul Road Fugitives
48	Amine Sweetener 1	AU1	Amine Sweetener 1
49	Amine Sweetener 2	AU2	Amine Sweetener 2
50	Amine Sweetener 3	AU3	Amine Sweetener 3
51	Amine Sweetener 4	AU4	Amine Sweetener 4
52	Amine Make Up Tank		Insignificant source moved to table 2-B
53	Gun Barrel Tank	GBS1	Gunbarrel Tank
54	Produced Water Tanks	PWTK1	Produced Water Tank 1
54	Produced Water Tanks	PWTK2	Produced Water Tank 2
55	Slop Oil Tank	SOTK1	Slop Oil Tank
		SOTL	Slop Oil Truck Loading
		GNE1	Generator 1
		GEN2	Generator 2
		GEN3	Generator 3
		GEN4	Generator 4

Table 2-A: Regulated Emission Sources

Unit and stack numbering must correspond throughout the application package. If applying for a NOI under 20.2.73 NMAC, equipment exemptions under 2.72.202 NMAC do not apply.

Unit Number[1]	Source Description	Make	Model #	Serial #	Manufacturer's Rated Capacity[3] (Specify Units)	Requested Permitted Capacity[3] (Specify Units)	Date of Manufacture[2] / Date of Construction/ Reconstruction[2]	Controlled by Unit # / Emissions vented to Stack #	Source Classification Code (SCC)	For Each Piece of Equipment, Check One	RICE Ignition Type (CI, SI, 4SLB, 4SRB, 2SLB)[4]	Replacing Unit No.
SHTR1	Stabilization Hot Oil Heater (58.93 MMBtu/hr)	THM	SHO5000	PK-6010 H-6012	58.93 MMBtu/hr	58.93 MMBtu/hr	2019 / 2019	N/A / SHTR1	31000403	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
SHTR2	Stabilization Hot Oil Heater (58.93 MMBtu/hr)	THM	SHO5000	PK-6020 H-6022	58.93 MMBtu/hr	58.93 MMBtu/hr	2019 / 2019	N/A / SHTR2	31000403	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
SHTR3	Stabilization Hot Oil Heater (58.93 MMBtu/hr)	THM	SHO5000	PK-6030 H-6032	58.93 MMBtu/hr	58.93 MMBtu/hr	2019 / 2019	N/A / SHTR3	31000403	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
SHTR4	Stabilization Hot Oil Heater (58.93 MMBtu/hr)	THM	SHO5000	TBD	58.93 MMBtu/hr	58.93 MMBtu/hr	TBD / TBD	N/A / SHTR4	31000403	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
SHTR5	Stabilization Hot Oil Heater (58.93 MMBtu/hr)	THM	SHO5000	TBD	58.93 MMBtu/hr	58.93 MMBtu/hr	TBD / TBD	N/A / SHTR5	31000403	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
SHTR6	Stabilization Hot Oil Heater (58.93 MMBtu/hr)	THM	SHO5000	TBD	58.93 MMBtu/hr	58.93 MMBtu/hr	TBD / TBD	N/A / SHTR6	31000403	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
SHTR7	Stabilization Hot Oil Heater w/ SCR catalyst (58.93 MMBtu/hr)	THM	SHO5000	TBD	58.93 MMBtu/hr	58.93 MMBtu/hr	TBD / TBD	SHTR7-CAT / SHTR7	31000403	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
SHTR8	Stabilization Hot Oil Heater w/ SCR catalyst (58.93 MMBtu/hr)	THM	SHO5000	TBD	58.93 MMBtu/hr	58.93 MMBtu/hr	TBD / TBD	SHTR8-CAT / SHTR8	31000403	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
SHTR9	Stabilization Hot Oil Heater w/ SCR catalyst (58.93 MMBtu/hr)	THM	SHO5000	TBD	58.93 MMBtu/hr	58.93 MMBtu/hr	TBD / TBD	SHTR9-CAT / SHTR9	31000403	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
SHTR10	Stabilization Hot Oil Heater w/ SCR catalyst (58.93 MMBtu/hr)	THM	SHO5000	TBD	58.93 MMBtu/hr	58.93 MMBtu/hr	TBD / TBD	SHTR10-CAT / SHTR10	31000403	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A

Table 2-A: Regulated Emission Sources

Unit and stack numbering must correspond throughout the application package. If applying for a NOI under 20.2.73 NMAC, equipment exemptions under 2.72.202 NMAC do not apply.

Unit Number[1]	Source Description	Make	Model #	Serial #	Manufact-urer's Rated Capacity[3] (Specify Units)	Requested Permitted Capacity[3] (Specify Units)	Date of Manufacture[2] Date of Construction/ Reconstruction[2]	Controlled by Unit # Emissions vented to Stack #	Source Classi-fication Code (SCC)	For Each Piece of Equipment, Check One	RICE Ignition Type (CI, SI, 4SLB, 4SRB, 2SLB)[4]	Replacing Unit No.
SHTR11	Stabilization Hot Oil Heater w/ SCR catalyst (58.93 MMBtu/hr)	THM	SHO5000	TBD	58.93 MMBtu/hr	58.93 MMBtu/hr	TBD TBD	SHTR11-CAT SHTR11	31000403	☐ Existing (unchanged) ☐ To be Removed ☑ New/Additional ☐ Replacement Unit ☐ To Be Modified ☐ To be Replaced	N/A	N/A
CHTR1	Cryo Hot Oil Heater (94.54 MMBtu/hr)	THM	TBD	PK-6110 H-6112	94.54 MMBtu/hr	94.54 MMBtu/hr	2019 TBD	N/A CHTR1	31000403	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
CHTR2	Cryo Hot Oil Heater (94.54 MMBtu/hr)	THM	TBD	TBD	94.54 MMBtu/hr	94.54 MMBtu/hr	TBD TBD	NA CHTR2	31000403	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
CHTR3	Cryo Hot Oil Heater w/ SCR Catalyst (94.54 MMBtu/hr)	THM	TBD	TBD	94.54 MMBtu/hr	94.54 MMBtu/hr	TBD TBD	CHTR3-CAT CHTR3	31000403	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
CHTR4	Cryo Hot Oil Heater w/ SCR Catalyst (94.54 MMBtu/hr)	THM	TBD	TBD	94.54 MMBtu/hr	94.54 MMBtu/hr	TBD TBD	CHTR4-CAT CHTR4	31000403	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
RHTR1	Regen Heater (35.25 MMBtu/hr)	THM	SHO2500	H-3132	35.25 MMBtu/hr	35.25 MMBtu/hr	TBD TBD	N/A RHTR1	31000405	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
RHTR2	Regen Heater (35.25 MMBtu/hr)	THM	SHO2500	TBD	35.25 MMBtu/hr	35.25 MMBtu/hr	TBD TBD	N/A RHTR2	31000405	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
RHTR3	Regen Heater (35.25 MMBtu/hr)	THM	SHO2500	TBD	35.25 MMBtu/hr	35.25 MMBtu/hr	TBD TBD	N/A RHTR3	31000405	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
RHTR4	Regen Heater (35.25 MMBtu/hr)	THM	SHO2500	TBD	35.25 MMBtu/hr	35.25 MMBtu/hr	TBD TBD	N/A RHTR4	31000405	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
FL1	Stabilizer Flare 1 (Dual Tip Flare)	Zeeco, Inc.	N/A	FS 6810 S.O # 35284	20 MMscfd	20 MMscfd	2018 2019	N/A FL1	31000160	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
FL2	Cryo Flare 2 (Dual Tip Flare)	Zeeco, Inc.	N/A	FS 6960 S.O # 38126	20 MMscfd	20 MMscfd	2019 2019	N/A FL2	31000160	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A

Table 2-A: Regulated Emission Sources

Unit and stack numbering must correspond throughout the application package. If applying for a NOI under 20.2.73 NMAC, equipment exemptions under 2.72.202 NMAC do not apply.

Unit Number[1]	Source Description	Make	Model #	Serial #	Manufact-urer's Rated Capacity[3] (Specify Units)	Requested Permitted Capacity[3] (Specify Units)	Date of Manufacture[2] Date of Construction/ Reconstruction[2]	Controlled by Unit # Emissions vented to Stack #	Source Classi-fication Code (SCC)	For Each Piece of Equipment, Check One	RICE Ignition Type (CI, SI, 4SLB, 4SRB, 2SLB)[4]	Replacing Unit No.
FL3	Backup SSM/Emergency Flare 3 (Dual Tip Flare)	Zeeco, Inc.	N/A	TBD	20 MMscfd	20 MMscfd	TBD TBD	N/A FL3	31000160	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
FL1-FL3OVHD-SSM	FL1-FL3 Stabilizer Overhead SSM Gas	Zeeco, Inc.	N/A	N/A	250 MMscfd	250 MMscfd	N/A N/A	FL1-FL3 FL1-FL3OVHD-	31000160	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
FL1-FL3CRYO-SSM	FL1-FL3 Cryo Blowdown SSM Gas	Zeeco, Inc.	N/A	N/A	250 MMscfd	250 MMscfd	N/A N/A	FL1-FL3 FL1-FL3CRYO-	31000160	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
IFR1	Oil Storage Tank 1 (50,000 bbl)	Advance Tank	N/A	TK-4201	50,000 bbl	50,000 bbl	2019 2019	N/A IFR1	40400331	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
IFR2	Oil Storage Tank 2 (50,000 bbl)	Advance Tank	N/A	TK-4202	50,000 bbl	50,000 bbl	2019 2019	N/A IFR2	40400331	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
IFR3	Oil Storage Tank 3 (50,000 bbl)	Advance Tank	N/A	TK-4203	50,000 bbl	50,000 bbl	2019 2019	N/A IFR3	40400331	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
IFR4	Oil Storage Tank 4 (50,000 bbl)	Advance Tank	N/A	TK-4204	50,000 bbl	50,000 bbl	2019 2019	N/A IFR4	40400331	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
IFR5	Oil Storage Tank 5 (250,000 bbl)	TBD	N/A	TBD	250,000 bbl	250,000 bbl	TBD TBD	N/A IFR5	40400331	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
IFR6	Oil Storage Tank 6 (250,000 bbl)	TBD	N/A	TBD	250,000 bbl	250,000 bbl	TBD TBD	N/A IFR6	40400331	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
IFR7	Oil Storage Tank 7 (250,000 bbl)	TBD	N/A	TBD	250,000 bbl	250,000 bbl	TBD TBD	N/A IFR7	40400331	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
IFR8	Oil Storage Tank 8 (250,000 bbl)	TBD	N/A	TBD	250,000 bbl	250,000 bbl	TBD TBD	N/A IFR8	40400331	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
ECD1	Combustor	Zeeco, Inc.	N/A	TBD	N/A	N/A	TBD TBD	N/A ECD1	31000209	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A

Table 2-A: Regulated Emission Sources

Unit and stack numbering must correspond throughout the application package. If applying for a NOI under 20.2.73 NMAC, equipment exemptions under 2.72.202 NMAC do not apply.

Unit Number[1]	Source Description	Make	Model #	Serial #	Manufact-urer's Rated Capacity[3] (Specify Units)	Requested Permitted Capacity[3] (Specify Units)	Date of Manufacture[2] / Date of Construction/ Reconstruction[2]	Controlled by Unit # / Emissions vented to Stack #	Source Classi-fication Code (SCC)	For Each Piece of Equipment, Check One	RICE Ignition Type (CI, SI, 4SLB, 4SRB, 2SLB)[4]	Replacing Unit No.
TO1	Thermal Oxidizer	Zeeco, Inc.	N/A	TO-6980 SO # 35595	25 MMbtu/hr	25 MMbtu/hr	2019 / 2019	N/A / TO1	31000209	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
TO2	Thermal Oxidizer	Zeeco, Inc.	N/A	TBD	25 MMbtu/hr	25 MMbtu/hr	TBD / TBD	N/A / TO2	31000209	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
TO3	Thermal Oxidizer	Zeeco, Inc.	N/A	TBD	25 MMbtu/hr	25 MMbtu/hr	TBD / TBD	N/A / TO3	31000209	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
TO4	Thermal Oxidizer	Zeeco, Inc.	N/A	TBD	25 MMbtu/hr	25 MMbtu/hr	TBD / TBD	N/A / TO4	31000209	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
FUG	Fugitives	N/A	N/A	N/A	N/A	N/A	TBD / TBD	N/A / FUG	31088811	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
SSM	SSM Emissions	N/A	N/A	N/A	N/A	N/A	TBD / TBD	N/A / SSM	31088811	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
ROAD	Haul Road Fugitives	N/A	N/A	N/A	N/A	N/A	TBD / TBD	N/A / ROAD	31088811	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
AU1	Amine Sweetener 1	N/A	N/A	N/A	250 MMSCFD	250 MMSCFD	TBD / TBD	TO1 / TO1	31000305	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
AU2	Amine Sweetener 2	N/A	N/A	N/A	250 MMSCFD	250 MMSCFD	TBD / TBD	TO2 / TO2	31000305	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
AU3	Amine Sweetener 3	N/A	N/A	N/A	250 MMSCFD	250 MMSCFD	TBD / TBD	TO3 / TO3	31000305	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
AU4	Amine Sweetener 4	N/A	N/A	N/A	250 MMSCFD	250 MMSCFD	TBD / TBD	TO4 / TO4	31000305	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
GBS1	Gunbarrel Tank	Angelina Tank	N/A	TK-7001	1,000 bbl	1,000 bbl	2019 / 2019	ECD1 / ECD1	31000506	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A

Table 2-A: Regulated Emission Sources

Unit and stack numbering must correspond throughout the application package. If applying for a NOI under 20.2.73 NMAC, equipment exemptions under 2.72.202 NMAC do not apply.

Unit Number[1]	Source Description	Make	Model #	Serial #	Manufact-urer's Rated Capacity[3] (Specify Units)	Requested Permitted Capacity[3] (Specify Units)	Date of Manufacture[2] / Date of Construction/ Reconstruction[2]	Controlled by Unit # / Emissions vented to Stack #	Source Classi-fication Code (SCC)	For Each Piece of Equipment, Check One	RICE Ignition Type (CI, SI, 4SLB, 4SRB, 2SLB)[4]	Replacing Unit No.
PWTK1	Produced Water Tank 1	Alliance Tank Services	N/A	TK-7005	750 bbl	750 bbl	2019 2019	ECD1 ECD1	40400315	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
PWTK2	Produced Water Tank 2	Alliance Tank Services	N/A	TK-7006	750 bbl	750 bbl	2019 2019	ECD1 ECD1	40400315	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
SOTK1	Slop Oil Tank	Alliance Tank Services	N/A	TK-6895	500 bbl	500 bbl	2019 2019	ECD1 ECD1	40400311	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
SOTL	Slop Oil Truck Loading	TBD	N/A	N/A	210 bbl/day	210 bbl/day	N/A N/A	ECD1 SOTL	40400250	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced	N/A	N/A
GEN1	Emergency Generator	Caterpillar	G3520H	TBD	3063 HP	3063 HP	TBD TBD	N/A GEN1	20200254	☐ Existing (unchanged) ☐ To be Removed ☑ New/Additional ☐ Replacement Unit ☐ To Be Modified ☐ To be Replaced	4SLB	N/A
GEN2	Emergency Generator	Caterpillar	G3520H	TBD	3063 HP	3063 HP	TBD TBD	N/A GEN2	20200254	☐ Existing (unchanged) ☐ To be Removed ☑ New/Additional ☐ Replacement Unit ☐ To Be Modified ☐ To be Replaced	4SLB	N/A
GEN3	Emergency Generator	Caterpillar	G3520H	TBD	3063 HP	3063 HP	TBD TBD	N/A GEN3	20200254	☐ Existing (unchanged) ☐ To be Removed ☑ New/Additional ☐ Replacement Unit ☐ To Be Modified ☐ To be Replaced	4SLB	N/A
GEN4	Emergency Generator	Caterpillar	G3520H	TBD	3063 HP	3063 HP	TBD TBD	N/A GEN4	20200254	☐ Existing (unchanged) ☐ To be Removed ☑ New/Additional ☐ Replacement Unit ☐ To Be Modified ☐ To be Replaced	4SLB	N/A

Table 2-A: Regulated Emission Sources

Unit and stack numbering must correspond throughout the application package. If applying for a NOI under 20.2.73 NMAC, equipment exemptions under 2.72.202 NMAC do not apply.

Unit Number[1]	Source Description	Make	Model #	Serial #	Manufact-urer's Rated Capacity[3] (Specify Units)	Requested Permitted Capacity[3] (Specify Units)	Date of Manufacture[2] / Date of Construction/ Reconstruction[2]	Controlled by Unit # / Emissions vented to Stack #	Source Classi-fication Code (SCC)	For Each Piece of Equipment, Check One	RICE Ignition Type (CI, SI, 4SLB, 4SRB, 2SLB)[4]	Replacing Unit No.
EOOSCOMP1-7	7 Electric Oil Overhead Stabilizer Compressors	Ariel	JGT/2	TBD	450 HP	450 HP	N/A / N/A	N/A / N/A	N/A	☐ Existing (unchanged) ☐ To be Removed ☑ New/Additional ☐ Replacement Unit ☐ To Be Modified ☐ To be Replaced	N/A	N/A
ECOSCOMP1-7	7 Electric Condenstate Overhead Stabilizer Compressors	Ariel	JGH/2	TBD	750 HP	750 HP	N/A / N/A	N/A / N/A	N/A	☐ Existing (unchanged) ☐ To be Removed ☑ New/Additional ☐ Replacement Unit ☐ To Be Modified ☐ To be Replaced	N/A	N/A
ERESCOMP1-18	18 Electric Residue Gas Compressors	Ariel	KBZ/6	TBD	6500 HP	6500 HP	N/A / N/A	N/A / N/A	N/A	☐ Existing (unchanged) ☐ To be Removed ☑ New/Additional ☐ Replacement Unit ☐ To Be Modified ☐ To be Replaced	N/A	N/A
CRYO1-4	4 Cryogenic Trains	N/A	N/A	N/A	N/A	N/A	N/A / N/A	N/A / N/A	N/A	☐ Existing (unchanged) ☐ To be Removed ☑ New/Additional ☐ Replacement Unit ☐ To Be Modified ☐ To be Replaced	N/A	N/A
MOL1-4	4 Molecular Sieve Dehydrators	N/A	N/A	N/A	N/A	N/A	N/A / N/A	N/A / N/A	N/A	☐ Existing (unchanged) ☐ To be Removed ☑ New/Additional ☐ Replacement Unit ☐ To Be Modified ☐ To be Replaced	N/A	N/A
Malfunction	Malfunction Emissions	N/A	N/A	N/A	N/A	N/A	N/A / N/A	N/A / N/A	31088811	☐ Existing (unchanged) ☐ To be Removed ☑ New/Additional ☐ Replacement Unit ☐ To Be Modified ☐ To be Replaced	N/A	N/A

[1] Unit numbers must correspond to unit numbers in the previous NOI unless a complete cross reference table of all units in both NOIs is provided.
[2] Specify dates required to determine regulatory applicability.
[3] To properly account for power conversion efficiencies, generator set rated capacity shall be reported as the rated capacity of the engine in horsepower, not the kilowatt capacity of the generator set.
[4] "4SLB" means four stroke lean burn engine, "4SRB" means four stroke rich burn engine, "2SLB" means two stroke lean burn engine, "CI" means compression ignition, and "SI" means spark ignition

Table 2-B: Insignificant Activities[1] (20.2.70 NMAC) OR Exempted Equipment (20.2.72 NMAC)

All 20.2.70 NMAC (Title V) applications must list all Insignificant Activities in this table. All 20.2.72 NMAC applications must list Exempted Equipment in this table. If equipment listed on this table is exempt under 20.2.72.202.B.5, include emissions calculations and emissions totals for 202.B.5 "similar functions" units, operations, and activities in Section 6, Calculations. Equipment and activities exempted under 20.2.72.202 NMAC may not necessarily be Insignificant under 20.2.70 NMAC (and vice versa). Unit & stack numbering must be consistent throughout the application package. Per Exemptions Policy 02-012.00 (see http://www.env.nm.gov/aqb/permit/aqb_pol.html), 20.2.72.202.B NMAC Exemptions do not apply, but 20.2.72.202.A NMAC exemptions do apply to NOI facilities under 20.2.73 NMAC. List 20.2.72.301.D.4 NMAC Auxiliary Equipment for Streamline applications in Table 2-A. The List of Insignificant Activities (for TV) can be found online at http://www.env.nm.gov/aqb/forms/InsignificantListTitleV.pdf . TV sources may elect to enter both TV Insignificant Activities and Part 72 Exemptions on this form.

Unit Number	Source Description	Manufacturer	Model No. / Serial No.	Max Capacity / Capacity Units	List Specific 20.2.72.202 NMAC Exemption (e.g. 20.2.72.202.B.5) / Insignificant Activity citation (e.g. IA List Item #1.a)	Date of Manufacture /Reconstruction[2] / Date of Installation /Construction[2]	For Each Piece of Equipment, Check Onc
FFT	1000 bbl Firefighting Foam Tank	TBD	N/A N/A	N/A N/A	20.2.72.202.B.5 Units with PTE < 0.5 tpy	TBD TBD	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced
48A	1000 bbl Raw Water Tank	TBD	N/A N/A	N/A N/A	20.2.72.202.B.5 Units with PTE < 0.5 tpy	TBD TBD	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced
48B	1000 bbl Raw Water Tank	TBD	N/A N/A	N/A N/A	20.2.72.202.B.5 Units with PTE < 0.5 tpy	TBD TBD	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced
49	1000 bbl Demineralized Water Tank	TBD	N/A N/A	N/A N/A	20.2.72.202.B.5 Units with PTE < 0.5 tpy	TBD TBD	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced
50	Amine Makeup Tank	TBD	N/A N/A	N/A N/A	20.2.72.202.B.5 Units with PTE < 0.5 tpy	TBD TBD	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced
51A	100 bbl Lube Oil Make-Up Tank	TBD	N/A N/A	N/A N/A	20.2.72.202.B.5 Units with PTE < 0.5 tpy	TBD TBD	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced
51B	100 bbl Lube Oil Make-Up Tank	TBD	N/A N/A	N/A N/A	20.2.72.202.B.5 Units with PTE < 0.5 tpy	TBD TBD	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced
55	Utility Water Tank	TBD	N/A N/A	N/A N/A	20.2.72.202.B.5 Units with PTE < 0.5 tpy	TBD TBD	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced
VTank01	Varsol Tank	TBD	N/A N/A	N/A N/A	20.2.72.202.B.5 Units with PTE < 0.5 tpy	TBD TBD	☐ Existing (unchanged) ☐ To be Removed ☐ New/Additional ☐ Replacement Unit ☑ To Be Modified ☐ To be Replaced

[1] Insignificant activities exempted due to size or production rate are defined in 20.2.70.300.D.6, 20.2.70.7.Q NMAC, and the NMED/AQB List of Insignificant Activities, dated September 15, 2008. Emissions from these insignificant activities do not need to be reported, unless specifically requested.

[2] Specify date(s) required to determine regulatory applicability.

Table 2-C: Emissions Control Equipment

Unit and stack numbering must correspond throughout the application package. Only list control equipment for TAPs if the TAP's maximum uncontrolled emissions rate is over its respective threshold as listed in 20.2.72 NMAC, Subpart V, Tables A and B. In accordance with 20.2.72.203.A(3) and (8) NMAC, 20.2.70.300.D(5)(b) and (e) NMAC, and 20.2.73.200.B(7) NMAC, the permittee shall report all control devices and list each pollutant controlled by the control device regardless if the applicant takes credit for the reduction in emissions.

Control Equipment Unit No.	Control Equipment Description	Date Installed	Controlled Pollutant(s)	Controlling Emissions for Unit Number(s)[1]	Efficiency (% Control by Weight)	Method used to Estimate Efficiency
FL2	Flare 1	TBD	VOC, HAP	Plant Inlet & SSM Activities	98%	Mnf. Guarantee
FL1	Flare 2	TBD	VOC, HAP	Plant Inlet & SSM Activities	98%	Mnf. Guarantee
FL3	Flare 3	TBD	VOC, HAP	Plant Inlet & SSM Activities	98%	Mnf. Guarantee
ECD1	Combustor	TBD	VOC, HAP	GBS1, PWTK1-PWTK2, SOTK1,SOTL	99%	Mnf. Guarantee
TO1	Thermal Oxidizer	TBD	VOC, HAP	AU1	99%	Mnf. Guarantee
TO2	Thermal Oxidizer	TBD	VOC, HAP	AU2	99%	Mnf. Guarantee
TO3	Thermal Oxidizer	TBD	VOC, HAP	AU3	99%	Mnf. Guarantee
TO4	Thermal Oxidizer	TBD	VOC, HAP	AU4	99%	Mnf. Guarantee
SHTR7-CAT	SCR Catalytic Reduction	TBD	NOx	SHTR7-CAT	NO_x - 75%	Mnf. Guarantee
SHTR8-CAT	SCR Catalytic Reduction	TBD	NOx	SHTR8-CAT	NO_x - 75%	Mnf. Guarantee
SHTR9-CAT	SCR Catalytic Reduction	TBD	NOx	SHTR9-CAT	NO_x - 75%	Mnf. Guarantee
SHTR10-CAT	SCR Catalytic Reduction	TBD	NOx	SHTR10-CAT	NO_x - 75%	Mnf. Guarantee
SHTR11-CAT	SCR Catalytic Reduction	TBD	NOx	SHTR11-CAT	NO_x - 75%	Mnf. Guarantee
CHTR3-CAT	SCR Catalytic Reduction	TBD	NOx	CHTR3-CAT	NO_x - 80%	Mnf. Guarantee
CHTR4-CAT	SCR Catalytic Reduction	TBD	NOx	CHTR4-CAT	NO_x - 80%	Mnf. Guarantee

[1] List each control device on a separate line. For each control device, list all emission units controlled by the control device.

Table 2-D: Maximum Emissions (under normal operating conditions)

Maximum Emissions are the emissions at maximum capacity and prior to (in the absence of) pollution control, emission-reducing process equipment, or any other emission reduction. Calculate the hourly emissions using the worst case hourly emissions for each pollutant. For each pollutant, calculate the annual emissions as if the facility were operating at maximum plant capacity without pollution controls for 8760 hours per year, unless otherwise approved by the Department. List Hazardous Air Pollutants (HAP) & Toxic Air Pollutants (TAPs) in Table 2-I. Unit & stack numbering must be consistent throughout the application package. Fill all cells in this table with the emission numbers or a "-" symbol. A "-" symbol indicates that emissions of this pollutant are not expected. Numbers shall be expressed to at least 2 decimal points (e.g. 0.41, 1.41, or 1.41E-4).

Unit No.	NOx		CO		VOC		SOx		PM[1]		PM10[2]		PM2.5[2]		H_2S		Lead	
	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
SHTR1	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.48	2.12	-	-	-	-
SHTR2	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.48	2.12	-	-	-	-
SHTR3	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.48	2.12	-	-	-	-
SHTR4	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.48	2.12	-	-	-	-
SHTR5	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.48	2.12	-	-	-	-
SHTR6	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.48	2.12	-	-	-	-
SHTR7	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.48	2.12	-	-	-	-
SHTR8	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.48	2.12	-	-	-	-
SHTR9	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.48	2.12	-	-	-	-
SHTR10	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.48	2.12	-	-	-	-
SHTR11	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.48	2.12	-	-	-	-
CHTR1	3.47	13.83	1.70	6.75	0.67	2.65	0.23	1.00	0.77	3.39	0.77	3.39	0.77	3.39	-	-	-	-
CHTR2	3.47	13.83	1.70	6.75	0.67	2.65	0.23	1.00	0.77	3.39	0.77	3.39	0.77	3.39	-	-	-	-
CHTR3	3.47	13.83	1.70	6.75	0.67	2.65	0.23	1.00	0.77	3.39	0.77	3.39	0.77	3.39	-	-	-	-
CHTR4	3.47	13.83	1.70	6.75	0.67	2.65	0.23	1.00	0.77	3.39	0.77	3.39	0.77	3.39	-	-	-	-
RHTR1	1.04	4.12	0.63	2.52	0.25	0.99	0.09	0.37	0.29	1.27	0.29	1.27	0.29	1.27	-	-	-	-
RHTR2	1.04	4.12	0.63	2.52	0.25	0.99	0.09	0.37	0.29	1.27	0.29	1.27	0.29	1.27	-	-	-	-
RHTR3	1.04	4.12	0.63	2.52	0.25	0.99	0.09	0.37	0.29	1.27	0.29	1.27	0.29	1.27	-	-	-	-
RHTR4	1.04	4.12	0.63	2.52	0.25	0.99	0.09	0.37	0.29	1.27	0.29	1.27	0.29	1.27	-	-	-	-
FL1-FL3[2]	1.40	6.14	2.80	12.26	0.29	1.29	0.00	0.00	0.08	0.33	0.08	0.33	0.08	0.33	-	-	-	-
FL1-FL3OVHD-SSM	Not operating during normal operating conditions																	
FL1-FL3CRYO-SSM	Not operating during normal operating conditions																	
IFR1	--	--	--	--	0.98	4.27	--	--	--	--	--	--	--	--	-	-	-	-
IFR2	--	--	--	--	0.98	4.27	--	--	--	--	--	--	--	--	-	-	-	-
IFR3	--	--	--	--	0.98	4.27	--	--	--	--	--	--	--	--	-	-	-	-
IFR4	--	--	--	--	0.98	4.27	--	--	--	--	--	--	--	--	-	-	-	-
IFR5	--	--	--	--	2.59	11.36	--	--	--	--	--	--	--	--	-	-	-	-
IFR6	--	--	--	--	2.59	11.36	--	--	--	--	--	--	--	--	-	-	-	-
IFR7	--	--	--	--	2.59	11.36	--	--	--	--	--	--	--	--	-	-	-	-
IFR8	--	--	--	--	2.59	11.36	--	--	--	--	--	--	--	--	-	-	-	-
ECD1[2]	0.03	0.11	0.05	0.22	0.01	0.03	0.00	0.00	0.00	0.01	0.00	0.01	0.00	0.01	-	-	-	-

Table 2-D: Maximum Emissions (under normal operating conditions)

Maximum Emissions are the emissions at maximum capacity and prior to (in the absence of) pollution control, emission-reducing process equipment, or any other emission reduction. Calculate the hourly emissions using the worst case hourly emissions for each pollutant. For each pollutant, calculate the annual emissions as if the facility were operating at maximum plant capacity without pollution controls for 8760 hours per year, unless otherwise approved by the Department. List Hazardous Air Pollutants (HAP) & Toxic Air Pollutants (TAPs) in Table 2-I. Unit & stack numbering must be consistent throughout the application package. Fill all cells in this table with the emission numbers or a "-" symbol. A "-" symbol indicates that emissions of this pollutant are not expected. Numbers shall be expressed to at least 2 decimal points (e.g. 0.41, 1.41, or 1.41E-4).

Unit No.	NOx		CO		VOC		SOx		PM[1]		PM10[2]		PM2.5[2]		H_2S		Lead	
	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
TO1²	0.33	1.45	0.20	0.89	0.36	1.58	0.00	0.00	0.18	0.79	0.18	0.79	0.18	0.79	-	-	-	-
TO2²	0.33	1.45	0.20	0.89	0.36	1.58	0.00	0.00	0.18	0.79	0.18	0.79	0.18	0.79	-	-	-	-
TO3²	0.33	1.45	0.20	0.89	0.36	1.58	0.00	0.00	0.18	0.79	0.18	0.79	0.18	0.79	-	-	-	-
TO4²	0.33	1.45	0.20	0.89	0.36	1.58	0.00	0.00	0.18	0.79	0.18	0.79	0.18	0.79	-	-	-	-
FUG	--	--	--	--	33.82	148.15	--	--	--	--	--	--	--	--	-	-	-	-
SSM	--	--	--	--	--	10.00	--	--	--	--	--	--	--	--	-	-	-	-
ROAD	--	--	--	--	--	--	--	--	2.76	0.01	0.70	0.00	0.07	0.00	-	-	-	-
AU1	--	--	--	--	80.16	351.11	--	--	--	--	--	--	--	--	-	-	-	-
AU2	--	--	--	--	80.16	351.11	--	--	--	--	--	--	--	--	-	-	-	-
AU3	--	--	--	--	80.16	351.11	--	--	--	--	--	--	--	--	-	-	-	-
AU4	--	--	--	--	80.16	351.11	--	--	--	--	--	--	--	--	-	-	-	-
GBS1	--	--	--	--	15.80	69.21	--	--	--	--	--	--	--	--	-	-	-	-
PWTK1	--	--	--	--	2.68	11.75	--	--	--	--	--	--	--	--	-	-	-	-
PWTK2	--	--	--	--	2.68	11.75	--	--	--	--	--	--	--	--	-	-	-	-
SOTK1	--	--	--	--	57.70	252.73	--	--	--	--	--	--	--	--	-	-	-	-
SOTL	--	--	--	--	53.34	0.58	--	--	--	--	--	--	--	--	-	-	-	-
GEN1	3.38	0.17	12.69	0.63	4.54	0.23	0.04	0.00	0.18	0.01	0.18	0.01	0.18	0.01	-	-	-	-
GEN2	3.38	0.17	12.69	0.63	4.54	0.23	0.04	0.00	0.18	0.01	0.18	0.01	0.18	0.01	-	-	-	-
GEN3	3.38	0.17	12.69	0.63	4.54	0.23	0.04	0.00	0.18	0.01	0.18	0.01	0.18	0.01	-	-	-	-
GEN4	3.38	0.17	12.69	0.63	4.54	0.23	0.04	0.00	0.18	0.01	0.18	0.01	0.18	0.01	-	-	-	-
Malfunction	--	--	--	--	--	10.00	--	--	--	--	--	--	--	--	-	-	-	-
Totals	53.33	160.36	75.37	101.90	529.07	2022.37	2.99	12.42	13.85	45.45	11.79	45.45	11.16	45.45	-	-	-	-

[1]**Condensable Particulate Matter:** Include condensable particulate matter emissions for PM10 and PM2.5 if the source is a combustion source. Do not include condensable particulate matter for PM unless PM is set equal to PM10 and PM2.5. Particulate matter (PM) is not subject to an ambient air quality standard, but PM is a regulated air pollutant under PSD (20.2.74 NMAC) and Title V (20.2.70 NMAC).

[2] Only includes pilot/purge gas/assist gas emissions, other emissions not considered normal operating conditions.

Table 2-E: Requested Allowable Emissions

Unit & stack numbering must be consistent throughout the application package. Fill all cells in this table with the emission numbers or a "-" symbol. A "-" symbol indicates that emissions of this pollutant are not expected. Numbers shall be expressed to at least 2 decimal points (e.g. 0.41, 1.41, or 1.41E^{-4}).

Unit No.	NOx		CO		VOC		SOx		PM[1]		PM10[1]		PM2.5[1]		H_2S		Lead	
	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
SHTR1	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.48	2.12	-	-	-	-
SHTR2	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.48	2.12	-	-	-	-
SHTR3	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.48	2.12	-	-	-	-
SHTR4	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.48	2.12	-	-	-	-
SHTR5	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.48	2.12	-	-	-	-
SHTR6	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.48	2.12	-	-	-	-
SHTR7	0.43	1.73	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.48	2.12	-	-	-	-
SHTR8	0.43	1.73	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.48	2.12	-	-	-	-
SHTR9	0.43	1.73	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.48	2.12	-	-	-	-
SHTR10	0.43	1.73	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.48	2.12	-	-	-	-
SHTR11	0.43	1.73	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.48	2.12	-	-	-	-
CHTR1	3.47	13.83	1.70	6.75	0.67	2.65	0.23	1.00	0.77	3.39	0.77	3.39	0.77	3.39	-	-	-	-
CHTR2	3.47	13.83	1.70	6.75	0.67	2.65	0.23	1.00	0.77	3.39	0.77	3.39	0.77	3.39	-	-	-	-
CHTR3	0.70	2.77	1.70	6.75	0.67	2.65	0.23	1.00	0.77	3.39	0.77	3.39	0.77	3.39	-	-	-	-
CHTR4	0.70	2.77	1.70	6.75	0.67	2.65	0.23	1.00	0.77	3.39	0.77	3.39	0.77	3.39	-	-	-	-
RHTR1	1.04	4.12	0.63	2.52	0.25	0.99	0.09	0.37	0.29	1.27	0.29	1.27	0.29	1.27	-	-	-	-
RHTR2	1.04	4.12	0.63	2.52	0.25	0.99	0.09	0.37	0.29	1.27	0.29	1.27	0.29	1.27	-	-	-	-
RHTR3	1.04	4.12	0.63	2.52	0.25	0.99	0.09	0.37	0.29	1.27	0.29	1.27	0.29	1.27	-	-	-	-
RHTR4	1.04	4.12	0.63	2.52	0.25	0.99	0.09	0.37	0.29	1.27	0.29	1.27	0.29	1.27	-	-	-	-
FL1-FL3	1.40	6.14	2.80	12.26	0.29	1.29	0.00	0.00	0.08	0.33	0.08	0.33	0.08	0.33				
IFR1	--	--	--	--	0.98	4.27	--	--	--	--	--	--	--	--	-	-	-	-
IFR2	--	--	--	--	0.98	4.27	--	--	--	--	--	--	--	--	-	-	-	-
IFR3	--	--	--	--	0.98	4.27	--	--	--	--	--	--	--	--	-	-	-	-
IFR4	--	--	--	--	0.98	4.27	--	--	--	--	--	--	--	--	-	-	-	-
IFR5	--	--	--	--	2.59	11.36	--	--	--	--	--	--	--	--	-	-	-	-
IFR6	--	--	--	--	2.59	11.36	--	--	--	--	--	--	--	--	-	-	-	-
IFR7	--	--	--	--	2.59	11.36	--	--	--	--	--	--	--	--	-	-	-	-
IFR8	--	--	--	--	2.59	11.36	--	--	--	--	--	--	--	--	-	-	-	-
ECD1	0.44	1.16	0.87	2.31	1.30	3.49	0.00	0.00	0.02	0.03	0.02	0.03	0.02	0.03	-	-	-	-
TO1	3.56	15.59	2.17	9.49	0.79	3.51	0.88	3.87	0.22	0.95	0.22	0.95	0.22	0.95	-	-	-	-
TO2	3.56	15.59	2.17	9.49	0.79	3.51	0.88	3.87	0.22	0.95	0.22	0.95	0.22	0.95	-	-	-	-
TO3	3.56	15.59	2.17	9.49	0.79	3.51	0.88	3.87	0.22	0.95	0.22	0.95	0.22	0.95	-	-	-	-
TO4	3.56	15.59	2.17	9.49	0.79	3.51	0.88	3.87	0.22	0.95	0.22	0.95	0.22	0.95	-	-	-	-

Table 2-E: Requested Allowable Emissions

Unit & stack numbering must be consistent throughout the application package. Fill all cells in this table with the emission numbers or a "-" symbol. A "-" symbol indicates that emissions of this pollutant are not expected. Numbers shall be expressed to at least 2 decimal points (e.g. 0.41, 1.41, or $1.41E^{-4}$).

Unit No.	NOx		CO		VOC		SOx		PM[1]		PM10[1]		PM2.5[1]		H_2S		Lead	
	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
FUG	--	--	--	--	16.44	72.00	--	--	--	--	--	--	--	--	-	-	-	-
ROAD	--	--	--	--	--	--	--	--	2.76	0.01	0.70	0.00	0.07	0.00	-	-	-	-
AU1	Emissions are represented at TO1																	
AU2	Emissions are represented at TO2																	
AU3	Emissions are represented at TO3																	
AU4	Emissions are represented at TO4																	
GBS1	Emissions are represented at ECD1																	
PWTK1	Emissions are represented at ECD1																	
PWTK2	Emissions are represented at ECD1																	
SOTK1	Emissions are represented at ECD1																	
SOTL	Emissions are represented at ECD1																	
GEN1	3.38	0.17	12.69	0.63	4.54	0.23	0.04	0.00	0.18	0.01	0.18	0.01	0.18	0.01	-	-	-	-
GEN2	3.38	0.17	12.69	0.63	4.54	0.23	0.04	0.00	0.18	0.01	0.18	0.01	0.18	0.01	-	-	-	-
GEN3	3.38	0.17	12.69	0.63	4.54	0.23	0.04	0.00	0.18	0.01	0.18	0.01	0.18	0.01	-	-	-	-
GEN4	3.38	0.17	12.69	0.63	4.54	0.23	0.04	0.00	0.18	0.01	0.18	0.01	0.18	0.01	-	-	-	-
Malfunction	--	--	--	--	--	10.00	--	--	--	--	--	--	--	--	-	-	-	-
Totals	54.6	170.0	84.0	138.4	61.8	197.0	6.5	27.9	14.0	46.1	12.0	46.1	11.3	46.1	-	-	-	-

[1] **Condensable Particulate Matter:** Include condensable particulate matter emissions for PM10 and PM2.5 if the source is a combustion source. Do not include condensable particulate matter for PM unless PM is set equal to PM10 and PM2.5. Particulate matter (PM) is not subject to an ambient air quality standard, but it is a regulated air pollutant under PSD (20.2.74 NMAC) and Title V (20.2.70 NMAC).

[2] For all pollutants except VOC/HAP, the hourly emission rate excludes the generators and overhead SSM stream as they cannot occur at the same time and the cryo SSM stream has a higher emission rate. For VOC, the overhead SSM stream is included with the highest hourly rate. For HAP, the generators have the highest hourly rate.

Table 2-F: Additional Emissions during Startup, Shutdown, and Routine Maintenance (SSM)

☐ This table is intentionally left blank since all emissions at this facility due to routine or predictable startup, shutdown, or scehduled maintenance are no higher than those listed in Table 2-E and a malfunction emission limit is not already permitted or requested. If you are required to report GHG emissions as described in Section 6a, include any GHG emissions during Startup, Shutdown, and/or Scheduled Maintenance (SSM) in Table 2-P. Provide an explanations of SSM emissions in Section 6 and 6a.

All applications for facilities that have emissions during routine our predictable startup, shutdown or scheduled maintenance (SSM)[1], including NOI applications, must include in this table the Maximum Emissions during routine or predictable startup, shutdown and scheduled maintenance (20.2.7 NMAC, 20.2.72.203.A.3 NMAC, 20.2.73.200.D.2 NMAC). In Section 6 and 6a, provide emissions calculations for all SSM emissions reported in this table. Refer to "Guidance for Submittal of Startup, Shutdown, Maintenance Emissions in Permit Applications (https://www.env.nm.gov/aqb/permit/aqb_pol.html) for more detailed instructions. Numbers shall be expressed to at least 2 decimal points (e.g. 0.41, 1.41, or 1.41E-4).

Unit No.	NOx		CO		VOC		SOx		PM[2]		PM10[2]		PM2.5[2]		H_2S		Lead	
	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
SSM	--	--	--	--	--	10.00	--	--	--	--	--	--	--	--	--	--	--	--
FL1-FL3OVHD-SSM	165.59	3.31	330.57	6.61	1,093.54	21.87	0.00	0.00	8.94	0.18	8.94	0.18	8.94	0.18	--	--	--	--
FL1-FL3CRYO-SSM	323.31	6.47	645.44	12.91	517.03	10.34	0.00	0.00	54.81	1.10	54.81	1.10	54.81	1.10	--	--	--	--
Totals	488.90	9.78	976.02	19.52	1610.57	42.21	0.00	0.00	63.75	1.28	63.75	1.28	63.75	1.28	-	-	-	-

[1] **For instance**, if the short term steady-state Table 2-E emissions are 5 lb/hr and the SSM rate is 12 lb/hr, enter 7 lb/hr in this table. If the annual steady-state Table 2-E emissions are 21.9 TPY, and the number of scheduled SSM events result in annual emissions of 31.9 TPY, enter 10.0 TPY in the table below.

[2] **Condensable Particulate Matter:** Include condensable particulate emissions for PM10 and PM2.5 if the source is a combustion source. Do not include condensable particulate matter for PM unless PM is set equal to PM10 and PM2.5. Particulat matter (PM) is not subject to an ambient air quality standard, but it is a regulated air pollutant under PSD (20.2.74 NMAC) and Title V (20.2.70 NMAC).

Table 2-G: Stack Exit and Fugitive Emission Rates for Special Stacks

☑ I have elected to leave this table blank because this facility does not have any stacks/vents that split emissions from a single source or combine emissions from more than one source listed in table 2-A. Additionally, the emission rates of all stacks match the Requested allowable emission rates stated in Table 2-E.

Use this table to list stack emissions (requested allowable) from split and combined stacks. List Toxic Air Pollutants (TAPs) and Hazardous Air Pollutants (HAPs) in Table 2-I. List all fugitives that are associated with the normal, routine, and non-emergency operation of the facility. Unit and stack numbering must correspond throughout the application package. Refer to Table 2-E for instructions on use of the "-" symbol and on significant figures.

Stack No.	Serving Unit Number(s) from Table 2-A	NOx		CO		VOC		SOx		PM		PM10		PM2.5		☐ H_2S or ☐ Lead	
		lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
N/A - This facility does not have Special Stacks																	
Totals:																	

Table 2-H: Stack Exit Conditions

Unit and stack numbering must correspond throughout the application package. Include the stack exit conditions for each unit that emits from a stack, including blowdown venting parameters and tank emissions.

Stack Number	Serving Unit Number(s) from Table 2-A	Orientation (H-Horizontal V=Vertical)	Rain Caps (Yes or No)	Height Above Ground (ft)	Temp. (F)	Flow Rate (acfs)	Flow Rate (dscfs)	Moisture by Volume (%)	Velocity (ft/sec)	Inside Diameter (ft)
SHTR1	SHTR1	V	No	33.0	488	441	NA	0	35.1	4.0
SHTR2	SHTR2	V	No	33.0	488	441	NA	0	35.1	4.0
SHTR3	SHTR3	V	No	33.0	488	441	NA	0	35.1	4.0
SHTR4	SHTR4	V	No	33.0	488	441	NA	0	35.1	4.0
SHTR5	SHTR5	V	No	33.0	488	441	NA	0	35.1	4.0
SHTR6	SHTR6	V	No	33.0	488	441	NA	0	35.1	4.0
SHTR7	SHTR7	V	No	33.0	488	441	NA	0	35.1	4.0
SHTR8	SHTR8	V	No	33.0	488	441	NA	0	35.1	4.0
SHTR9	SHTR9	V	No	33.0	488	441	NA	0	35.1	4.0
SHTR10	SHTR10	V	No	33.0	488	441	NA	0	35.1	4.0
SHTR11	SHTR11	V	No	33.0	488	441	NA	0	35.1	4.0
CHTR1	CHTR1	V	No	76.9	599	820	NA	0	65.3	4.0
CHTR2	CHTR2	V	No	76.9	599	820	NA	0	65.3	4.0
CHTR3	CHTR3	V	No	76.9	599	820	NA	0	65.3	4.0
CHTR4	CHTR4	V	No	76.9	599	820	NA	0	65.3	4.0
RHTR1	RHTR1	V	No	28.7	470	292	NA	0	52.3	2.7
RHTR2	RHTR2	V	No	28.7	470	292	NA	0	52.3	2.7
RHTR3	RHTR3	V	No	28.7	470	292	NA	0	52.3	2.7
RHTR4	RHTR4	V	No	28.7	470	292	NA	0	52.3	2.7
FL2	FL2	V	No	130.0	1832	139	NA	0	65.6	0.4
FL1	FL1	V	No	170.0	1832	139	NA	0	65.6	0.7
FL3	FL3	V	No	170.0	1832	139	NA	0	65.6	0.7

Table 2-H: Stack Exit Conditions

Unit and stack numbering must correspond throughout the application package. Include the stack exit conditions for each unit that emits from a stack, including blowdown venting parameters and tank emissions.

Stack Number	Serving Unit Number(s) from Table 2-A	Orientation (H-Horizontal V=Vertical)	Rain Caps (Yes or No)	Height Above Ground (ft)	Temp. (F)	Flow Rate		Moisture by Volume (%)	Velocity (ft/sec)	Inside Diameter (ft)
						(acfs)	(dscfs)			
ECD1	ECD1	V	No	40.0	1450	529	NA	0	39.5	8.4
TO1	TO1	V	No	58.0	1700	782.5	NA	0	58.6	4.1
TO2	TO2	V	No	58.0	1700	782.5	NA	0	58.6	4.1
TO3	TO3	V	No	58.0	1700	782.5	NA	0	58.6	4.1
TO4	TO4	V	No	58.0	1700	782.5	NA	0	58.6	4.1
GEN1	GEN1	V	No	14.0	736	260.3	NA	0	331.4	1.0
GEN2	GEN2	V	No	14.0	736	260.3	NA	0	331.4	1.0
GEN3	GEN3	V	No	14.0	736	260.3	NA	0	331.4	1.0
GEN4	GEN4	V	No	14.0	736	260.3	NA	0	331.4	1.0

Table 2-I: Stack Exit and Fugitive Emission Rates for HAPs and TAPs

In the table below, report the Potential to Emit for each HAP from each regulated emission unit listed in Table 2-A, only if the entire facility emits the HAP at a rate greater than or equal to one (1) ton per year For each such emission unit, HAPs shall be reported to the nearest 0.1 tpy. Each facility-wide Individual HAP total and the facility-wide Total HAPs shall be the sum of all HAP sources calculated to the nearest 0.1 ton per year. Per 20.2.72.403.A.1 NMAC, facilities not exempt [see 20.2.72.402.C NMAC] from TAP permitting shall report each TAP that has an uncontrolled emission rate in excess of its pounds per hour screening level specified in 20.2.72.502 NMAC. TAPs shall be reported using one more significant figure than the number of significant figures shown in the pound per hour threshold corresponding to the substance. Use the HAP nomenclature as it appears in Section 112 (b) of the 1990 CAAA and the TAP nomenclature as it listed in 20.2.72.502 NMAC. Include tank-flashing emissions estimates of HAPs in this table. For each HAP or TAP listed, fill all cells in this table with the emission numbers or a "-" symbol. A "-" symbol indicates that emissions of this pollutant are not expected or the pollutant is emitted in a quantity less than the threshold amounts described above.

Stack No.	Unit No.(s)	Total HAPs		n-Hexane ☑ HAP or ☐ TAP		Benzene ☑ HAP or ☐ TAP		Toluene ☑ HAP or ☐ TAP		Ethylbenzene ☑ HAP or ☐ TAP		Xylene ☑ HAP or ☐ TAP		Formaldehyde ☑ HAP or ☐ TAP		H2SO4 ☐ HAP or ☑ TAP		Ammonia ☐ HAP or ☑ TAP		Provide Pollutant Name Here ☐ HAP or ☐ TAP	
		lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
SHTR1	SHTR1	0.12	0.48	0.11	0.46	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.02	--	--	--	--		
SHTR2	SHTR2	0.12	0.48	0.11	0.46	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.02	--	--	--	--		
SHTR3	SHTR3	0.12	0.48	0.11	0.46	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.02	--	--	--	--		
SHTR4	SHTR4	0.12	0.48	0.11	0.46	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.02	--	--	--	--		
SHTR5	SHTR5	0.12	0.48	0.11	0.46	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.02	--	--	--	--		
SHTR6	SHTR6	0.12	0.48	0.11	0.46	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.02	--	--	--	--		
SHTR7	SHTR7	0.12	0.48	0.11	0.46	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.02	--	--	--	--		
SHTR8	SHTR8	0.12	0.48	0.11	0.46	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.02	--	--	--	--		
SHTR9	SHTR9	0.12	0.48	0.11	0.46	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.02	--	--	--	--		
SHTR10	SHTR10	0.12	0.48	0.11	0.46	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.02	--	--	--	--		
SHTR11	SHTR11	0.12	0.48	0.11	0.46	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.02	--	--	--	--		
CHTR1	CHTR1	0.19	0.76	0.18	0.73	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.01	0.03	--	--	--	--		
CHTR2	CHTR2	0.19	0.76	0.18	0.73	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.01	0.03	--	--	--	--		
CHTR3	CHTR3	0.19	0.76	0.18	0.73	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.01	0.03	--	--	--	--		
CHTR4	CHTR4	0.19	0.76	0.18	0.73	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.01	0.03	--	--	--	--		
RHTR1	RHTR1	0.07	0.28	0.07	0.27	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.01	--	--	--	--		
RHTR2	RHTR2	0.07	0.28	0.07	0.27	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.01	--	--	--	--		
RHTR3	RHTR3	0.07	0.28	0.07	0.27	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.01	--	--	--	--		
RHTR4	RHTR4	0.07	0.28	0.07	0.27	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.01	--	--	--	--		
FL1-FL3[1]	FL1-FL3[1]	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	--	--	--	--		
FL1-FL3[1]	FL1-FL3OVHD-	15.67	0.31	6.81	0.14	5.15	0.10	3.16	0.06	0.00	0.00	0.56	0.01	0.00	0.00	--	--	--	--		
FL1-FL3[1]	FL1-FL3CRYO-	1.62	0.03	1.45	0.03	0.16	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	--	--	--	--		
IFR1	IFR1	0.05	0.21	0.02	0.09	0.01	0.06	0.01	0.04	0.00	0.00	0.00	0.02	0.00	0.00	--	--	--	--		
IFR2	IFR2	0.05	0.21	0.02	0.09	0.01	0.06	0.01	0.04	0.00	0.00	0.00	0.02	0.00	0.00	--	--	--	--		
IFR3	IFR3	0.05	0.21	0.02	0.09	0.01	0.06	0.01	0.04	0.00	0.00	0.00	0.02	0.00	0.00	--	--	--	--		
IFR4	IFR4	0.05	0.21	0.02	0.09	0.01	0.06	0.01	0.04	0.00	0.00	0.00	0.02	0.00	0.00	--	--	--	--		
IFR5	IFR5	0.12	0.53	0.06	0.24	0.03	0.15	0.02	0.10	0.00	0.00	0.01	0.03	0.00	0.00	--	--	--	--		
IFR6	IFR6	0.12	0.53	0.06	0.24	0.03	0.15	0.02	0.10	0.00	0.00	0.01	0.03	0.00	0.00	--	--	--	--		
IFR7	IFR7	0.12	0.53	0.06	0.24	0.03	0.15	0.02	0.10	0.00	0.00	0.01	0.03	0.00	0.00	--	--	--	--		
IFR8	IFR8	0.12	0.53	0.06	0.24	0.03	0.15	0.02	0.10	0.00	0.00	0.01	0.03	0.00	0.00	--	--	--	--		
ECD1	ECD1	0.05	0.14	0.02	0.06	0.01	0.03	0.01	0.03	0.00	0.00	0.00	0.01	0.00	0.00	--	--	--	--		

Table 2-I: Stack Exit and Fugitive Emission Rates for HAPs and TAPs

In the table below, report the Potential to Emit for each HAP from each regulated emission unit listed in Table 2-A, only if the entire facility emits the HAP at a rate greater than or equal to one (1) ton per year For each such emission unit, HAPs shall be reported to the nearest 0.1 tpy. Each facility-wide Individual HAP total and the facility-wide Total HAPs shall be the sum of all HAP sources calculated to the nearest 0.1 ton per year. Per 20.2.72.403.A.1 NMAC, facilities not exempt [see 20.2.72.402.C NMAC] from TAP permitting shall report each TAP that has an uncontrolled emission rate in excess of its pounds per hour screening level specified in 20.2.72.502 NMAC. TAPs shall be reported using one more significant figure than the number of significant figures shown in the pound per hour threshold corresponding to the substance. Use the HAP nomenclature as it appears in Section 112 (b) of the 1990 CAAA and the TAP nomenclature as it listed in 20.2.72.502 NMAC. Include tank-flashing emissions estimates of HAPs in this table. For each HAP or TAP listed, fill all cells in this table with the emission numbers or a "-" symbol. A "-" symbol indicates that emissions of this pollutant are not expected or the pollutant is emitted in a quantity less than the threshold amounts described above.

Stack No.	Unit No.(s)	Total HAPs		n-Hexane ☑ HAP or ☐ TAP		Benzene ☑ HAP or ☐ TAP		Toluene ☑ HAP or ☐ TAP		Ethylbenzene ☑ HAP or ☐ TAP		Xylene ☑ HAP or ☐ TAP		Formaldehyde ☑ HAP or ☐ TAP		H2SO4 ☐ HAP or ☑ TAP		Ammonia ☐ HAP or ☑ TAP		Provide Pollutant Name Here ☐ HAP or ☐ TAP	
		lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
TO1	TO1	0.02	0.08	0.00	0.02	0.00	0.02	0.00	0.02	0.00	0.02	0.00	0.02	0.00	0.00	--	--	--	--		
TO2	TO2	0.02	0.08	0.00	0.02	0.00	0.02	0.00	0.02	0.00	0.02	0.00	0.02	0.00	0.00	--	--	--	--		
TO3	TO3	0.02	0.08	0.00	0.02	0.00	0.02	0.00	0.02	0.00	0.02	0.00	0.02	0.00	0.00	--	--	--	--		
TO4	TO4	0.02	0.08	0.00	0.02	0.00	0.02	0.00	0.02	0.00	0.02	0.00	0.02	0.00	0.00	--	--	--	--		
FUG	FUG	0.67	2.94	0.16	0.69	0.11	0.46	0.20	0.90	0.01	0.06	0.15	0.66	0.00	0.00	--	--	--	--		
SSM	SSM	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--		
ROAD	ROAD	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--	--		
TO1	AU1	Emissions are represented at TO1.																			
TO2	AU2	Emissions are represented at TO2.																			
TO3	AU3	Emissions are represented at TO3.																			
TO4	AU4	Emissions are represented at TO4.																			
ECD1	GBS1	Emissions are represented at ECD1.																			
ECD1	PWTK1	Emissions are represented at ECD1.																			
ECD1	PWTK2	Emissions are represented at ECD1.																			
ECD1	SOTK1	Emissions are represented at ECD1.																			
ECD1	SOTL	Emissions are represented at ECD1.																			
GEN1	GEN1	1.93	0.10	0.02	0.00	--	--	--	--	--	--	--	--	1.76	0.09	--	--	--	--		
GEN2	GEN2	1.93	0.10	0.02	0.00	--	--	--	--	--	--	--	--	1.76	0.09	--	--	--	--		
GEN3	GEN3	1.93	0.10	0.02	0.00	--	--	--	--	--	--	--	--	1.76	0.09	--	--	--	--		
GEN4	GEN4	1.93	0.10	0.02	0.00	--	--	--	--	--	--	--	--	1.76	0.09	--	--	--	--		
Totals:		28.8	16.5	11.1	11.3	5.7	1.5	3.5	1.6	0.0	0.1	0.8	0.9	7.1	0.7	0.0	0.0	0.0	0.0		

Table 2-J: Fuel

Specify fuel characteristics and usage. Unit and stack numbering must correspond throughout the application package.

Unit No.	Fuel Type (low sulfur Diesel, ultra low sulfur diesel, Natural Gas, Coal, …)	Fuel Source: purchased commercial, pipeline quality natural gas, residue gas, raw/field natural gas, process gas (e.g. SRU tail gas) or other	Specify Units				
			Lower Heating Value (Btu/scf)	Hourly Usage (scf)	Annual Usage (mmscf)	% Sulfur (by weight)	% Ash
SHTR1	Natural Gas	Field Gas	993	59345	519.9	< 0.0001	N/A
SHTR2	Natural Gas	Field Gas	993	59345	519.9	< 0.0001	N/A
SHTR3	Natural Gas	Field Gas	993	59345	519.9	< 0.0001	N/A
SHTR4	Natural Gas	Field Gas	993	59345	519.9	< 0.0001	N/A
SHTR5	Natural Gas	Field Gas	993	59345	519.9	< 0.0001	N/A
SHTR6	Natural Gas	Field Gas	993	59345	519.9	< 0.0001	N/A
SHTR7	Natural Gas	Field Gas	993	59345	519.9	< 0.0001	N/A
SHTR8	Natural Gas	Field Gas	993	59345	519.9	< 0.0001	N/A
SHTR9	Natural Gas	Field Gas	993	59345	519.9	< 0.0001	N/A
SHTR10	Natural Gas	Field Gas	993	59345	519.9	< 0.0001	N/A
SHTR11	Natural Gas	Field Gas	993	59345	519.9	< 0.0001	N/A
CHTR1	Natural Gas	Field Gas	993	95206	834.0	< 0.0001	N/A
CHTR2	Natural Gas	Field Gas	993	95206	834.0	< 0.0001	N/A
CHTR3	Natural Gas	Field Gas	993	95206	834.0	< 0.0001	N/A
CHTR4	Natural Gas	Field Gas	993	95206	834.0	< 0.0001	N/A
RHTR1	Natural Gas	Field Gas	993	35498	311.0	< 0.0001	N/A
RHTR2	Natural Gas	Field Gas	993	35498	311.0	< 0.0001	N/A
RHTR3	Natural Gas	Field Gas	993	35498	311.0	< 0.0001	N/A
RHTR4	Natural Gas	Field Gas	993	35498	311.0	< 0.0001	N/A
FL1	Natural Gas	Field Gas	1019	35498	311.0	< 0.0001	N/A
FL2	Natural Gas	Field Gas	1019	35498	311.0	< 0.0001	N/A
FL3	Natural Gas	Field Gas	1019	35498	311.0	< 0.0001	N/A
GEN1	Natural Gas	Field Gas	1001	24586	215.4	< 0.0001	N/A
GEN2	Natural Gas	Field Gas	1001	24586	215.4	< 0.0001	N/A
GEN3	Natural Gas	Field Gas	1001	24586	215.4	< 0.0001	N/A
GEN4	Natural Gas	Field Gas	1001	24586	215.4	< 0.0001	N/A

Table 2-K: Liquid Data for Tanks Listed in Table 2-L

For each tank, list the liquid(s) to be stored in each tank. If it is expected that a tank may store a variety of hydrocarbon liquids, enter "mixed hydrocarbons" in the Composition column for that tank and enter the corresponding data of the most volatile liquid to be stored in the tank. If tank is to be used for storage of different materials, list all the materials in the "All Calculations" attachment, run the newest version of TANKS on each, and use the material with the highest emission rate to determine maximum uncontrolled and requested allowable emissions rate. The permit will specify the most volatile category of liquids that may be stored in each tank. Include appropriate tank-flashing modeling input data. Use additional sheets if necessary. Unit and stack numbering must correspond throughout the application package.

Tank No.	SCC Code	Material Name	Composition	Liquid Density (lb/gal)	Vapor Molecular Weight (lb/lb*mol)	Average Storage Conditions		Max Storage Conditions	
						Temperature (°F)	True Vapor Pressure (psia)	Temperature (°F)	True Vapor Pressure (psia)
IFR1	40400331	Oil/Condensate	Oil/Condensate	6.6	62.20	84.15	8.24	93.16	9.38
IFR2	40400331	Oil/Condensate	Oil/Condensate	6.6	62.20	84.15	8.24	93.16	9.38
IFR3	40400331	Oil/Condensate	Oil/Condensate	6.6	62.20	84.15	8.24	93.16	9.38
IFR4	40400331	Oil/Condensate	Oil/Condensate	6.6	62.20	84.15	8.24	93.16	9.38
IFR5	40400331	Oil/Condensate	Oil/Condensate	6.6	57.26	84.86	8.33	93.80	9.46
IFR6	40400331	Oil/Condensate	Oil/Condensate	6.6	57.26	84.86	8.33	93.80	9.46
IFR7	40400331	Oil/Condensate	Oil/Condensate	6.6	57.26	84.86	8.33	93.80	9.46
IFR8	40400331	Oil/Condensate	Oil/Condensate	6.6	57.26	84.86	8.33	93.80	9.46
GBS1	31000506	Produced Water	Produced Water w/ Trace Oils	8.3	55.60	86.50	0.63	95.80	0.85
PWTK1	40400315	Produced Water	Produced Water w/ Trace Oils	8.3	55.60	81.25	11.74	90.51	13.20
PWTK2	40400315	Produced Water	Produced Water w/ Trace Oils	8.3	55.60	81.25	11.74	90.51	13.20
SOTK1	40400311	Oil/Condensate	Oil/Condensate	6.6	54.81	53.32	6.55	62.62	7.72

Table 2-L: Tank Data

Include appropriate tank-flashing modeling input data. Use an addendum to this table for unlisted data categories. Unit and stack numbering must correspond throughout the application package. Use additional sheets if necessary. See reference Table 2-L2. Note: 1.00 bbl = 10.159 M3 = 42.0 gal

Tank No.	Date Installed	Materials Stored	Seal Type (refer to Table 2-LR below)	Roof Type (refer to Table 2-LR below)	Capacity		Diameter (M)	Vapor Space (M)	Color (from Table VI-C)		Paint Condition (from Table VI-C)	Annual Throughput (gal/yr)	Turn-overs (per year)
					(bbl)	(M^3)			Roof	Shell			
IFR1	TBD	Oil/Condensate	C	IF	50,000	7,949	30.5	13.4	Tan	Tan	Good	766,500,000	365
IFR2	TBD	Oil/Condensate	C	IF	50,000	7,949	30.5	13.4	Tan	Tan	Good	766,500,000	365
IFR3	TBD	Oil/Condensate	C	IF	50,000	7,949	30.5	13.4	Tan	Tan	Good	766,500,000	365
IFR4	TBD	Oil/Condensate	C	IF	50,000	7,949	30.5	13.4	Tan	Tan	Good	766,500,000	365
IFR5	TBD	Oil/Condensate	C	IF	250,000	39,747	61.0	16.5	Tan	Tan	Good	1,533,000,000	146
IFR6	TBD	Oil/Condensate	C	IF	250,000	39,747	61.0	16.5	Tan	Tan	Good	1,533,000,000	146
IFR7	TBD	Oil/Condensate	C	IF	250,000	39,747	61.0	16.5	Tan	Tan	Good	1,533,000,000	146
IFR8	TBD	Oil/Condensate	C	IF	250,000	39,747	61.0	16.5	Tan	Tan	Good	1,533,000,000	146
GBS1	TBD	Produced Water	NA	FX	1,000	159	4.7	7.3	Tan	Tan	Good	64,313,353	1531
PWTK1	TBD	Produced Water	NA	FX	750	119	4.7	7.3	Tan	Tan	Good	32,155,018	1021
PWTK2	TBD	Produced Water	NA	FX	750	119	4.7	7.3	Tan	Tan	Good	32,155,018	1021
SOTK1	TBD	Slop - Oil/Condensate	NA	FX	500	79	4.7	4.9	Tan	Tan	Good	239,586	11

Table 2-L2: Liquid Storage Tank Data Codes Reference Table

Roof Type	Seal Type, Welded Tank Seal Type		Seal Type, Riveted Tank Seal Type		Roof, Shell Color	Paint Condition
	Mechanical Shoe Seal	Liquid-mounted resilient seal	Vapor-mounted resilient seal	Seal Type		
FX: Fixed Roof					**WH**: White	Good
IF: Internal Floating Roof	**A**: Primary only	**A**: Primary only	**A**: Primary only	**A**: Mechanical shoe, primary only	**AS**: Aluminum (specular)	Poor
EF: External Floating Roof	**B**: Shoe-mounted secondary	**B**: Weather shield	**B**: Weather shield	**B**: Shoe-mounted secondary	**AD**: Aluminum (diffuse)	
P: Pressure	**C**: Rim-mounted secondary	**C**: Rim-mounted secondary	**C**: Rim-mounted secondary	**C**: Rim-mounted secondary	**LG**: Light Gray	
					MG: Medium Gray	
					BL: Black	
					OT: Other (specify)	

Note: 1.00 bbl = 0.159 M^3 = 42.0 gal

Table 2-M: Materials Processed and Produced (Use additional sheets as necessary.)

Material Processed				Material Produced			
Description	**Chemical Composition**	**Phase (Gas, Liquid, or Solid)**	**Quantity (specify units)**	**Description**	**Chemical Composition**	**Phase**	**Quantity (specify units)**
Mixed Hydrocarbons	Oil/Condensate	Liquid (BOPD)	600,000	Mixed Hydrocarbons	Oil/Condensate	Liquid (BOPD)	600000
	Produced Water	Liquid (BWPD)	4,195		Produced Water	Liquid (BWPD)	4195
	Natural Gas	Gas (MMSCFD)	1,000		Natural Gas	Gas (MMSCFD)	1000
	Natural Gas Liquids	Liquid (BOPD)	190,000		Natural Gas Liquids	Liquid (BOPD)	190000

Table 2-N: CEM Equipment

Enter Continuous Emissions Measurement (CEM) Data in this table. If CEM data will be used as part of a federally enforceable permit condition, or used to satisfy the requirements of a state or federal regulation, include a copy of the CEM's manufacturer specification sheet in the Information Used to Determine Emissions attachment. Unit and stack numbering must correspond throughout the application package. Use additional sheets if necessary.

Stack No.	Pollutant(s)	Manufacturer	Model No.	Serial No.	Sample Frequency	Averaging Time	Range	Sensitivity	Accuracy
N/A									

Table 2-O: Parametric Emissions Measurement Equipment

Unit and stack numbering must correspond throughout the application package. Use additional sheets if necessary.

Unit No.	Parameter/Pollutant Measured	Location of Measurement	Unit of Measure	Acceptable Range	Frequency of Maintenance	Nature of Maintenance	Method of Recording	Averaging Time
N/A								

Table 2-P: Greenhouse Gas Emissions

Applications submitted under 20.2.70, 20.2.72, & 20.2.74 NMAC are required to complete this Table. Power plants, Title V major sources, and PSD major sources must report and calculate all GHG emissions for each unit. Applicants must report potential emission rates in short tons per year (see Section 6.a for assistance). Include GHG emissions during Startup, Shutdown, and Scheduled Maintenance in this table. For minor source facilities that are not power plants, are not Title V, or are not PSD, there are three options for reporting GHGs 1) report GHGs for each individual piece of equipment; 2) report all GHGs from a group of unit types, for example report all combustion source GHGs as a single unit and all venting GHG as a second separate unit; OR 3) check the following box ☐ By checking this box, the applicant acknowledges the total CO2e emissions are less than 75,000 tons per year.

		CO_2 ton/yr	N_2O ton/yr	CH_4 ton/yr	SF_6 ton/yr	PFC/HFC ton/yr[2]									Total GHG Mass ton/yr[4]	Total CO_2e ton/yr[5]
Unit No.	**GWPs [1]**	1	298	25	22,800	footnote 3										
SHTR1-11	mass GHG	332184.28	0.63	6.26											332191.2	
	CO_2e	332184.28	186.56	156.51												332527.4
CHTR1-4	mass GHG	193787.40	0.37	3.65											193791.4	
	CO_2e	193787.40	108.84	91.31												193987.5
RHTR1-4	mass GHG	72255.19	0.14	1.36											72256.7	
	CO_2e	72255.19	40.58	34.04												72329.8
FL1-FL3	mass GHG	6789.21	0.00	0.00											6789.2	
	CO_2e	6789.21	0.00	0.08												6789.3
FL1-FL3OVHD-SSM	mass GHG	3168.54	0.00	0.00											3169	
	CO_2e	3168.54	0.00	0.04												3169
FL1-FL3CRYO-SSM	mass GHG	5439.08	0.00	22.41											5461	
	CO_2e	5439.08	0.00	560.26												5999
IFR1-IFR4	mass GHG	0.02	0.00	0.00											0.0	
	CO_2e	0.02	0.00	0.00												0.0
IFR5-IFR8	mass GHG	0.06	0.00	0.00											0.1	
	CO_2e	0.06	0.00	0.00												0.1
ECD1	mass GHG	998.97	0.00	0.00											999.0	
	CO_2e	998.97	0.00	0.06												999.0
TO1	mass GHG	106227.53	0.00	40.80											106268.3	
	CO_2e	106227.53	0.00	1020.00												107247.5
TO2	mass GHG	106227.53	0.00	40.80											106268.3	
	CO_2e	106227.53	0.00	1020.00												107247.5
TO3	mass GHG	106227.53	0.00	40.80											106268.3	
	CO_2e	106227.53	0.00	1020.00												107247.5
TO4	mass GHG	106227.53	0.00	40.80											106268.3	
	CO_2e	106227.53	0.00	1020.00												107247.5
FUG	mass GHG	0.55	0.00	130.02											130.6	
	CO_2e	0.55	0.00	3250.42												3251.0
GEN1-GEN4	mass GHG	557.78	0.00	0.01											557.8	
	CO_2e	557.78	0.24	0.20												558.2
Total	mass GHG														1040419	
	CO_2e															1048600

[1] **GWP** (Global Warming Potential): Applicants must use the most current GWPs codified in Table A-1 of 40 CFR part 98. GWPs are subject to change, therefore, applicants need to check 40 CFR 98 to confirm GWP values.

[2] For **HFCs** or **PFCs** describe the specific HFC or PFC compound and use a separate column for each individual compound.

[3] For each new compound, enter the appropriate GWP for each HFC or PFC compound from Table A-1 in 40 CFR 98.

[4] Green house gas emissions on a **mass basis** is the ton per year green house gas emission before adjustment with its GWP.

[5] **CO_2e** means Carbon Dioxide Equivalent and is calculated by multiplying the TPY mass emissions of the green house gas by its GWP.

Tab 3
Section 3 - Application Summary

Section 3

Application Summary

The **Application Summary** shall include a brief description of the facility and its process, the type of permit application, the applicable regulation (i.e. 20.2.72.200.A.X, or 20.2.73 NMAC) under which the application is being submitted, and any air quality permit numbers associated with this site. If this facility is to be collocated with another facility, provide details of the other facility including permit number(s). In case of a revision or modification to a facility, provide the lowest level regulatory citation (i.e. 20.2.72.219.B.1.d NMAC) under which the revision or modification is being requested. Also describe the proposed changes from the original permit, how the proposed modification will affect the facility's operations and emissions, de-bottlenecking impacts, and changes to the facility's major/minor status (both PSD & Title V).

The **Process Summary** shall include a brief description of the facility and its processes.

Startup, Shutdown, and Maintenance (SSM) routine or predictable emissions: Provide an overview of how SSM emissions are accounted for in this application. Refer to "Guidance for Submittal of Startup, Shutdown, Maintenance Emissions in Permit Applications (http://www.env.nm.gov/aqb/permit/app_form.html) for more detailed instructions on SSM emissions.

This application requests modification of NSR Permit 7877 for the XTO Energy Inc. Cowboy Central Delivery Point (CDP) in accordance with 20.2.72.219.B.1.d NMAC. The facility is located approximately 14 miles southeast of Malaga in Eddy County, New Mexico.

The facility is proposing the following modifications:

1) Add selective catalytic reduction to five (5) stabilization heaters and two (2) cryo heaters;
2) Add truck loading of slop oil;
3) Increase stabilizer overhead and cryogenic blowdown startup, shutdown, and maintenance (SSM) emissions;
4) Update speciation profiles for several sources;
5) Update fugitive counts and control efficiencies based on proposed site monitoring;
6) Update tank throughputs;
7) Add four (4) emergency generators; and,
8) Update equipment nomenclature and unit numbers.
9) Add/show electric compressors that have NSPS OOOOa applicability.
10) Consolidate MSS floating roof tank landings under general SSM related VOC emissions at a rate of 10 tons per year per NMAQB guidance.

The facility will process natural gas using amine sweetening units. Sweetened gas will be dehydrated then flow to cryogenic units to remove NGLs for sale. Heat for the dehydration and cryogenic processes is supplied by gas-fired auxiliary heaters. NGLs from the inlet slug catcher and surrounding compressor stations are stabilized before being transferred offsite via pipeline. Heat for the stabilization process is supplied by gas-fired auxiliary heaters. The central delivery point portion of the facility will receive up to 600,000 barrels of oil/condensate (oil) per day from surrounding field production batteries. Oil will be transferred directly to storage or stabilized using auxiliary heaters. Oil is transferred offsite via pipeline. Incoming water will be temporarily stored onsite prior to being transferred offsite via pipeline. Water and slop oil can be transferred offsite by truck.

SSM emissions from equipment maintenance are routed to either the low pressure or high pressure flare header (FL1/FL2/FL3). SSM-related VOC emissions (tank landings/cleanings) are included at a rate of 10 tons per year per NMAQB guidance. Detailed calculations are included in the application.

Tab 4
Section 4 - Process Flow Sheet

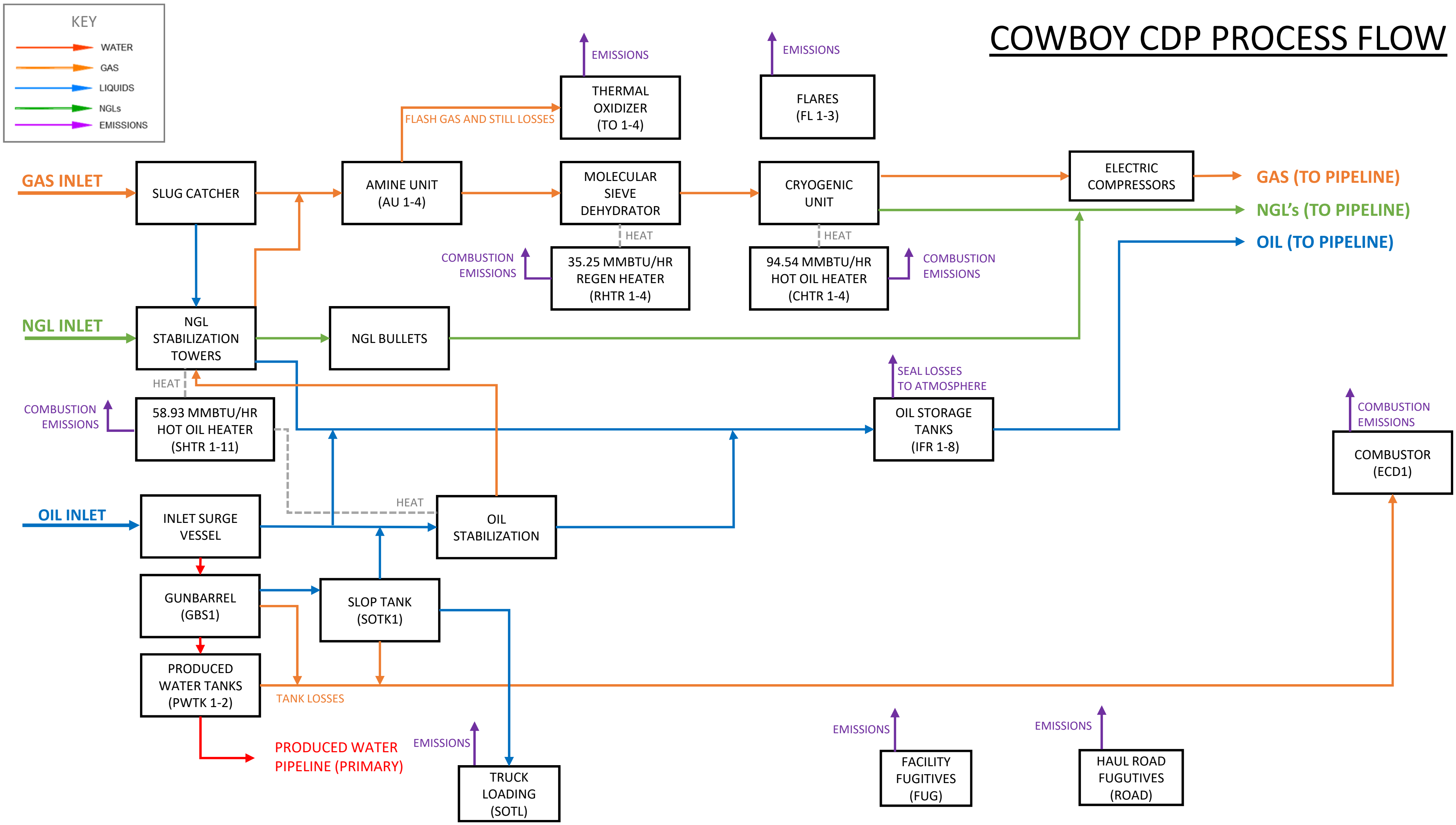
Section 4

Process Flow Sheet

A **process flow sheet** and/or block diagram indicating the individual equipment, all emission points and types of control applied to those points. The unit numbering system should be consistent throughout this application.

A process flow diagram is presented on the following page.

COWBOY CDP PROCESS FLOW



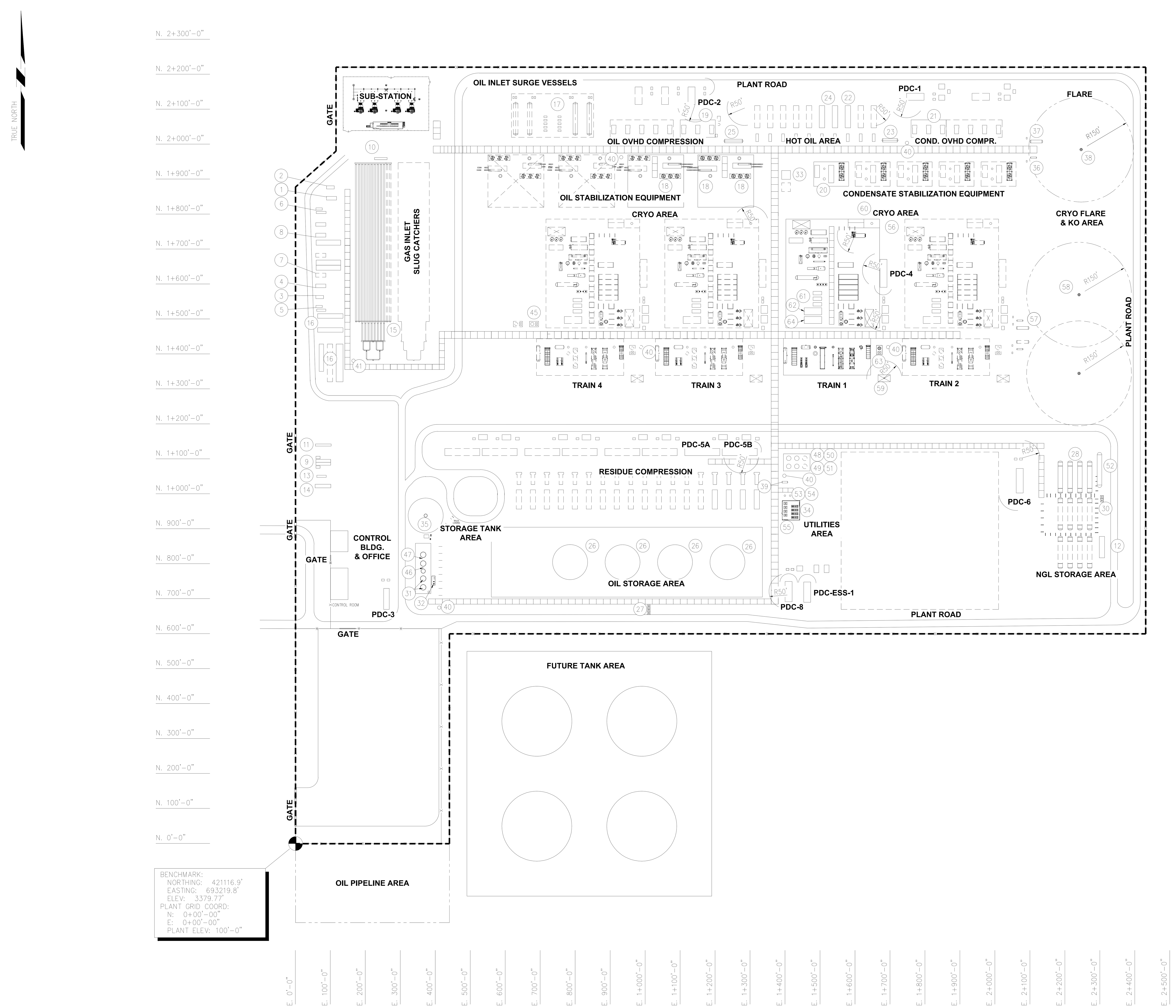
Tab 5
Section 5 - Plot Plan Drawn To Scale

Section 5

Plot Plan Drawn To Scale

A **plot plan drawn to scale** showing emissions points, roads, structures, tanks, and fences of property owned, leased, or under direct control of the applicant. This plot plan must clearly designate the restricted area as defined in UA1, Section 1-D.12. The unit numbering system should be consistent throughout this application.

A proposed plot plan is presented on the following page.



EQUIPMENT LIST		
1	16" NORTH GAS P/L PIG RECEIVER	PR-2002
2	20" NORTH GAS P/L PIG RECEIVER	PR-2001
3	16" SOUTH GAS P/L PIG RECEIVER	PR-2004
4	20" SOUTH GAS P/L PIG RECEIVER	PR-2003
5	SOUTH NGL P/L PIG RECEIVER & INLET METER SKID	PR-2006 & SK-2006
6	NORTH NGL P/L PIG RECEIVER & INLET METER SKID	PR-2005 & SK-2005
7	SOUTH OIL P/L PIG RECEIVER & INLET METER SKID	PR-1002 & SK-1002
8	NORTH OIL P/L PIG RECEIVER & INLET METER SKID	PR-1001 & SK-1001
9	NORTH & SOUTH FIELD FUEL GAS LAUNCHER & METER SKID	PL-2040/41 & SK-2040
10	CONDENSATE INLET METERING SKID	SK-2010
11	N & S LP GAS LAUNCHER & METER SKID	PL-2050 & SK-2050
12	Y-GRADE OUTLET METER SKID	SK-5550
13	PRODUCED WATER METER SKID	SK-7050
14	FRESH WATER INLET AND METER SKID	
15	GAS INLET SLUG CATCHER	SC-2010
16	RICH & RESIDUE GAS METER SKIDS & OUTLETS	SK-2025/2026/2030/XXXX
17	OIL INLET SURGE VESSELS & PUMPS	V-1011/1012 & P-1020A/B/C & P-1025A/B/C/D
18	OIL STABILIZER PACKAGES	PK-1100/1110/1200
19	OIL STAB. OVERHEAD GAS COMPRESSOR PACKAGE	PK-1600/1610/1620
20	CONDENSATE STABILIZER PACKAGE	PK-2100
21	COND. STAB. OVERHEAD GAS COMPRESSOR PACKAGE	PK-2600/2610/2620
22	COND. STABIL. HOT OIL PACKAGES/PUMPS/BURNERS	PK-6030 (SK-6031/6032)
23	COND. STABILIZATION HOT OIL EXPANSION VESSEL	V-6003
24	OIL STABIL. HOT OIL PACKAGES/PUMPS/BURNERS	PK-6010 (SK-6011/12) & PK-6020 (SK-6021/22)
25	OIL STABILIZATION HOT OIL EXPANSION VESSEL	V-6001
26	OIL STORAGE TANKS	TK-4201/4202/4203/4204
27	OIL BOOSTER PUMPS	P-4401/4402
28	NGL STORAGE VESSELS	V-5201/5202/5203/5204
29	DELETED	
30	NGL PIPELINE PUMPS	P-5501/5502
31	PRODUCED WATER TANKS	TK-7005/7006
32	PRODUCED WATER DISPOSAL PUMPS	P-7011/7012
33	FUEL GAS SKID	PK-6210 & FUTURE
34	INSTRUMENT AIR PACKAGE	PK-6260 & FUTURE
35	COMBUSTER W/ K.O. DRUM & PUMPS	V-6820 & P-6820A/B & FS-6820
36	LP FLARE K.O. DRUM & PUMPS	V-6808 & P-6808A/B
37	HP FLARE K.O. DRUM & PUMPS	V-6809 & P-6809A/B
38	FLARE STACK	FS-6810
39	CLOSED DRAIN DRUM	V-6860
40	OPEN DRAIN SUMPS & PUMPS	TK-6870/1/2/3/4 & P-6870/1/2/3/4
41	PIG RECEIVER OPEN DRAIN SUMP & PUMPS	TK-6875 & P-6875
42	DELETED	
43	DELETED	
44	DELETED	
45	RICH GAS SCRUBBER & PUMPS	V-2020 & P-2020 A/B
46	SLOP OIL TANK & PUMPS	TK-6895 & P-6895A/B
47	GUNBARREL TANK	TK-7001
48	RAW WATER TANK & PUMPS	TK-6450 & P-6451A/B
49	DEMINERALIZED WATER MAKE-UP TANK & PUMP	TK-6520 & P-6520A/B
50	AMINE MAKE-UP TANK & PUMP	TK-6500 & P-6500
51	LUBE OIL MAKE-UP TANK	--
52	PROPANE MAKE-UP TANK	V-6550
53	UTILITY AIR RECEIVER	V-6255
54	INSTRUMENT AIR RECEIVER	V-6250
55	UTILITY WATER TREATMENT PACKAGE	PK-6510
56	CRYO PACKAGE	--
57	CRYO TRAIN 1 & 2, LP & HP FLARE K.O. DRUM & PUMPS	V-6958 & P-6958A/B & V-6959 & P-6958A/B
58	CRYO TRAIN 1 & 2 FLARE STACK	FS-6960
59	THERMAL OXIDIZER	TO-6980
60	CRYO HOT OIL PACKAGE (PUMPS & BURNER SKIDS)	PK-6110 (SK-6111/6112)
61	CRYO NGL PIPELINE PUMPS	P-3151/3152/3153
62	CRYO NGL COOLER	AC-3155
63	CRYO RICH GAS SCRUBBER & PUMPS	V-3101 & P-3101A/B
64	RSV RECYCLE FILTER COALESCER	F-3190A/B

NOTES

EQUIPMENT SIZES ARE PRELIMINARY AND ARE SUBJECTED TO CHANGE UPON DETAIL ENGINEERING.

REFERENCE DRAWINGS

DWG. NO.	DESCRIPTION
--	--

REVISIONS

REV.	DESCRIPTION	DRWN	CHKD	APPRV	DATE
E	ISSUED FOR HAZOP	CA			
D	ISSUED FOR DESIGN	SG	DH	GG	10/11/18
C	NOT ISSUED				
B	ISSUED FOR REVIEW	CA	DH	GG	05/21/18
A	PRELIMINARY	CA	DH	GG	05/17/18

PROJECT INFO.

DRAWN BY: SJB
DATE: 10/23/17
AEC JOB NO.: 018193-001
AFE/P.O. NO.:
CLIENT FILE NO.:
SCALE: 1"=150'

XTO ENERGY

PLOT PLAN
COWBOY NATURAL GAS & OIL CDP

EDDY COUNTY NEW MEXICO

DWG. NO. CB-0300 REV. E

Tab 6
Section 6 - All Calculations

Section 6

All Calculations

Show all calculations used to determine both the hourly and annual controlled and uncontrolled emission rates. All calculations shall be performed keeping a minimum of three significant figures. Document the source of each emission factor used (if an emission rate is carried forward and not revised, then a statement to that effect is required). If identical units are being permitted and will be subject to the same operating conditions, submit calculations for only one unit and a note specifying what other units to which the calculations apply. All formulas and calculations used to calculate emissions must be submitted. The "Calculations" tab in the UA2 has been provided to allow calculations to be linked to the emissions tables. Add additional "Calc" tabs as needed. If the UA2 or other spread sheets are used, all calculation spread sheet(s) shall be submitted electronically in Microsoft Excel compatible format so that formulas and input values can be checked. Format all spread sheets and calculations such that the reviewer can follow the logic and verify the input values. Define all variables. If calculation spread sheets are not used, provide the original formulas with defined variables. Additionally, provide subsequent formulas showing the input values for each variable in the formula. All calculations, including those calculations are imbedded in the Calc tab of the UA2 portion of the application, the printed Calc tab(s), should be submitted under this section.

Tank Flashing Calculations: The information provided to the AQB shall include a discussion of the method used to estimate tank-flashing emissions, relative thresholds (i.e., NOI, permit, or major source (NSPS, PSD or Title V)), accuracy of the model, the input and output from simulation models and software, all calculations, documentation of any assumptions used, descriptions of sampling methods and conditions, copies of any lab sample analysis. If Hysis is used, all relevant input parameters shall be reported, including separator pressure, gas throughput, and all other relevant parameters necessary for flashing calculation.

SSM Calculations: It is the applicant's responsibility to provide an estimate of SSM emissions or to provide justification for not doing so. In this Section, provide emissions calculations for Startup, Shutdown, and Routine Maintenance (SSM) emissions listed in the Section 2 SSM and/or Section 22 GHG Tables and the rational for why the others are reported as zero (or left blank in the SSM/GHG Tables). Refer to "Guidance for Submittal of Startup, Shutdown, Maintenance Emissions in Permit Applications (http://www.env.nm.gov/aqb/permit/app_form.html) for more detailed instructions on calculating SSM emissions. If SSM emissions are greater than those reported in the Section 2, Requested Allowables Table, modeling may be required to ensure compliance with the standards whether the application is NSR or Title V. Refer to the Modeling Section of this application for more guidance on modeling requirements.

Glycol Dehydrator Calculations: The information provided to the AQB shall include the manufacturer's maximum design recirculation rate for the glycol pump. If GRI-Glycalc is used, the full input summary report shall be included as well as a copy of the gas analysis that was used.

Road Calculations: Calculate fugitive particulate emissions and enter haul road fugitives in Tables 2-A, 2-D and 2-E for:

1. If you transport raw material, process material and/or product into or out of or within the facility and have PER emissions greater than 0.5 tpy.
2. If you transport raw material, process material and/or product into or out of the facility more frequently than one round trip per day.

Significant Figures:
A. All emissions standards are deemed to have at least two significant figures, but not more than three significant figures.
B. At least 5 significant figures shall be retained in all intermediate calculations.
C. In calculating emissions to determine compliance with an emission standard, the following rounding off procedures shall be used:

(1) If the first digit to be discarded is less than the number 5, the last digit retained shall not be changed;
(2) If the first digit discarded is greater than the number 5, or if it is the number 5 followed by at least one digit other than the number zero, the last figure retained shall be increased by one unit; **and**
(3) If the first digit discarded is exactly the number 5, followed only by zeros, the last digit retained shall be rounded upward if it is an odd number, but no adjustment shall be made if it is an even number.
(4) The final result of the calculation shall be expressed in the units of the standard.

Control Devices: In accordance with 20.2.72.203.A(3) and (8) NMAC, 20.2.70.300.D(5)(b) and (e) NMAC, and 20.2.73.200.B(7) NMAC, the permittee shall report all control devices and list each pollutant controlled by the control device regardless if the applicant takes credit for the reduction in emissions. The applicant can indicate in this section of the application if they chose to not take credit for the reduction in emission rates. For notices of intent submitted under 20.2.73 NMAC, only uncontrolled emission rates can be considered to determine applicability unless the state or federal Acts require the control. This information is necessary to determine if federally enforceable conditions are necessary for the control device, and/or if the control device produces its own regulated pollutants or increases emission rates of other pollutants.

Hot Oil Heaters (SHTR1 – SHTR11, CHTR1 – CHTR4, RHTR1 – RHTR4)
The facility will be equipped with eleven (11) 58.93 Million British Thermal units per hour (MMbtu/hr) burners used for heating units in oil & NGL stabilization, four (4) 94.54 MMbtu/hr burners used for natural gas cryogenic heaters, and four (4) 35.25 MMbtu/hr burners used for amine regeneration. Four (4) 58.93 MMBtu/hr heaters and two (2) 94.54 MMbtu/hr heaters will be equipped with SCR catalysts to control NOx emissions. The heaters generate emissions of nitrogen oxides (NOx), carbon dioxide (CO), volatile organic compounds (VOC), sulfur dioxide (SO2), and Particulate Matter (PM). NOx, CO and VOC emissions were calculated using manufacturer's guaranteed exhaust concentrations. PM, hazardous air pollutants (HAPs), and SO2 emissions were calculated using emission factors from AP-42 Section 1.4 for natural gas combustion. Supporting manufacturer documentation is provided in Section 7. For all heaters, the rich fuel case was used to calculate hourly emissions and the design fuel case was used to calculate annual emissions.

Thermal Oxidizers (TO1 – TO4)
Thermal oxidizers (TO) will be used to control vapors from the amine flash vessels and acid gas from the amine still reflux accumulators. Speciated VOC, SO2 and HAP emissions associated with the flash vessels and still vents were calculated using Bryan Research and Engineering's (BR&E) Promax simulation software (see simulation report in Section 7). The ProMax simulation for each amine flash vessel and still vent was designed to simulate emissions at the maximum design gas throughput of 250 Million standard cubic feet per day (MMscfd) per cryo train and maximum design amine recirculation pump rates of 500 standard gallons per minute (sgpm). To be conservative, total HAP emissions were calculated assuming that the total molar concentration of hydrocarbon components that are hexanes or heavier (C6+) is equal to the molar concentration of each individual HAP component. A manufacturer guaranteed destruction efficiency of 99% was used for the TO. Emissions of NOx and CO from the TOs were calculated using manufacturer's guaranteed exhaust concentrations. PM emissions from TO combustion were calculated using AP-42 Section 1.4. Supporting manufacturer documentation is provided in Section 7.

SSM/Emergency Flares (FL1 – FL3)
The facility will be equipped with three (3) start, shutdown, and maintenance (SSM) activity/emergency dual-tip flares. NOx and CO emissions were calculated using emission factors from the Texas Commission on Environmental Quality (TCEQ) publication RG-360A/09. VOC emissions were calculated using a material balance and the manufacturer's guaranteed destruction efficiency. Emissions from FL1 and FL2 were each calculated to include a constant pilot fuel rate of 500 standard cubic feet per hour (scfh) and constant purge gas rates through the low pressure and high pressure header systems of 4,892 scfh per flare. FL3 will only operate as backup to FL1 and FL2 therefore emissions were not calculated for this flare. The flares have a control efficiency of 98%, with manufacturer documentation provided in Section 7 of the application.

SSM activities routed to the flares could include process vessel purging and maintenance blowdowns for process equipment associated with the oil and NGL stabilization and the natural gas processing cryo trains. Maximum SSM gas rates of 500,000 scf/hr and 20 MMscf/yr were included in the calculations for stabilizer overhead blowdowns. Maximum SSM gas rates of 2 MMscf/hr and 80 MMscf/yr were included for natural gas cryo train equipment blowdowns.

Combustor (ECD1)
An enclosed combustor will control flashing, working, and breathing losses from the gunbarrel separator and fixed roof tanks, as well as the displaced vapors from truck loading operations from the slop oil tank. Emissions of NOx and CO from the Combustor were calculated using manufacturer's guaranteed exhaust concentrations. VOC emissions were calculated using speciated streams determined from BR&E ProMax software and the manufacturer's guaranteed destruction efficiency of 99%. A constant pilot gas fuel rate of 180 scfh is included in the emission calculations for the combustor. Supporting manufacturer documentation is provided in Section 7.

Oil Storage Tanks (IFR1 – IFR8, GBS1, SOTK1, PWTK1 – PWTK2)
Flashing, working and breathing emissions from the eight (8) internal floating roof (IFR) crude oil tanks, one fixed roof gunbarrel tank, one (1) slop fixed roof oil tank, and two (2) fixed roof produced water storage tanks were calculated using BR&E ProMax simulation software. Emissions from the fixed roof tanks will be controlled by ECD1. The simulation reports' details and summaries are included in Section 7.

Truck Loading (SOTL)
Uncontrolled emissions from slop oil loading of trucks were calculated using Equation 1 of AP-42 Section 5.2. Maximum slop oil loading rates are calculated using 249 BOPD. Relevant portions of AP-42 Section 5.2 are included in Section 7. Slop oil truck loading will be uncontrolled.

Piping Component Fugitive Emissions (FUG)
Facility fugitive emissions were calculated using TCEQ's "Air Permit Technical Guidance for Chemical Sources – Fugitive Guidance" document, and conservatively assumed component counts. Reduction efficiencies were obtained from EPA's Protocol for Equipment Leak Emission Estimates (EPA-453/R-95-017). Relevant portions of the TCEQ document are included in Section 7.

Startup, Shutdown, and Maintenance
Startup, shutdown, and maintenance (SSM) emissions not routed to the flare system were assumed equal to the flat 10 tpy of VOC per State guidance. Specific SSM emissions include small equipment blowdowns, tank emptying and refilling, tank roof landing, and miscellaneous activities. Other SSM emissions are routed to the flare and calculated in accordance with the flare methodology above.

Haul Road Fugitive Emissions
Fugitive haul road emissions were calculated using Equations 1a and 2 of AP-42 Section 13.2.2. Relevant portions of AP-42 Section 13.2.2 are included in Section 7.

Emergency Generators (GEN1-GEN4)
Emission factors for NOx, CO, formaldehyde, and VOC are based on manufacturer's data. Emission rates TSP, PM_{10}, and $PM_{2.5}$ were calculated using AP-42 Table 3.2-3 emission factors. PM_{10} and $PM_{2.5}$ emissions are set equal to TSP emissions as a conservative measure. SO_2 emissions were calculated based on the units' fuel consumption and a maximum sulfur content of 0.75 grains per 100 standard cubic feet (0.75 gr/100 scf). Hazardous Air Pollutants (HAPs) except for formaldehyde were calculated using AP-42 factors. Annual operation was assumed to be 100 hours per generator.

Section 6.a

Green House Gas Emissions

(Submitting under 20.2.70, 20.2.72 20.2.74 NMAC)

Title V (20.2.70 NMAC), Minor NSR (20.2.72 NMAC), and PSD (20.2.74 NMAC) applicants must estimate and report greenhouse gas (GHG) emissions to verify the emission rates reported in the public notice, determine applicability to 40 CFR 60 Subparts, and to evaluate Prevention of Significant Deterioration (PSD) applicability. GHG emissions that are subject to air permit regulations consist of the sum of an aggregate group of these six greenhouse gases: carbon dioxide (CO_2), nitrous oxide (N_2O), methane (CH_4), hydrofluorocarbons (HFCs), perfluorocarbons (PFCs), and sulfur hexafluoride (SF_6).

Calculating GHG Emissions:

1. Calculate the ton per year (tpy) GHG mass emissions and GHG CO_2e emissions from your facility.
2. GHG mass emissions are the sum of the total annual tons of greenhouse gases without adjusting with the global warming potentials (GWPs). GHG CO_2e emissions are the sum of the mass emissions of each individual GHG multiplied by its GWP found in Table A-1 in 40 CFR 98 Mandatory Greenhouse Gas Reporting.
3. Emissions from routine or predictable start up, shut down, and maintenance must be included.
4. Report GHG mass and GHG CO_2e emissions in Table 2-P of this application. Emissions are reported in **short** tons per year and represent each emission unit's Potential to Emit (PTE).
5. All Title V major sources, PSD major sources, and all power plants, whether major or not, must calculate and report GHG mass and CO2e emissions for each unit in Table 2-P.
6. For minor source facilities that are not power plants, are not Title V, and are not PSD there are three options for reporting GHGs in Table 2-P: 1) report GHGs for each individual piece of equipment; 2) report all GHGs from a group of unit types, for example report all combustion source GHGs as a single unit and all venting GHGs as a second separate unit; 3) or check the following ☐ By checking this box, the applicant acknowledges the total CO2e emissions are less than 75,000 tons per year.

Sources for Calculating GHG Emissions:

- Manufacturer's Data
- AP-42 Compilation of Air Pollutant Emission Factors at http://www.epa.gov/ttn/chief/ap42/index.html
- EPA's Internet emission factor database WebFIRE at http://cfpub.epa.gov/webfire/
- 40 CFR 98 Mandatory Green House Gas Reporting except that tons should be reported in short tons rather than in metric tons for the purpose of PSD applicability.
- API Compendium of Greenhouse Gas Emissions Methodologies for the Oil and Natural Gas Industry. August 2009 or most recent version.
- Sources listed on EPA's NSR Resources for Estimating GHG Emissions at http://www.epa.gov/nsr/clean-air-act-permitting-greenhouse-gases:

Global Warming Potentials (GWP):
Applicants must use the Global Warming Potentials codified in Table A-1 of the most recent version of 40 CFR 98 Mandatory Greenhouse Gas Reporting. The GWP for a particular GHG is the ratio of heat trapped by one unit mass of the GHG to that of one unit mass of CO_2 over a specified time period.

"Greenhouse gas" for the purpose of air permit regulations is defined as the aggregate group of the following six gases: carbon dioxide, nitrous oxide, methane, hydrofluorocarbons, perfluorocarbons, and sulfur hexafluoride. **(20.2.70.7 NMAC, 20.2.74.7 NMAC).** You may also find GHGs defined in 40 CFR 86.1818-12(a).

Metric to Short Ton Conversion:
Short tons for GHGs and other regulated pollutants are the standard unit of measure for PSD and title V permitting programs. 40 CFR 98 Mandatory Greenhouse Reporting requires metric tons.
1 metric ton = 1.10231 short tons (per Table A-2 to Subpart A of Part 98 – Units of Measure Conversions)

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CONTROLLED FACILITY EMISSIONS SUMMARY

EMISSIONS SUMMARY TABLE

EMISSION SOURCE DESCRIPTION	FACILITY NUMBER	STACK NUMBER	NOx		CO		VOC (INCLUDES HAPs)		SO_2		TSP		PM_{10}		HAPs		CO2e
			lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	TPY
Stabilization Hot Oil Heater (58.93 MMBtu/hr)	SHTR1	SHTR1	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.12	0.48	30,230
Stabilization Hot Oil Heater (58.93 MMBtu/hr)	SHTR2	SHTR2	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.12	0.48	30,230
Stabilization Hot Oil Heater (58.93 MMBtu/hr)	SHTR3	SHTR3	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.12	0.48	30,230
Stabilization Hot Oil Heater (58.93 MMBtu/hr)	SHTR4	SHTR4	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.12	0.48	30,230
Stabilization Hot Oil Heater (58.93 MMBtu/hr)	SHTR5	SHTR5	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.12	0.48	30,230
Stabilization Hot Oil Heater (58.93 MMBtu/hr)	SHTR6	SHTR6	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.12	0.48	30,230
Stabilization Hot Oil Heater w/ SCR catalyst (58.93 MMBtu/hr)	SHTR7	SHTR7	0.43	1.73	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.12	0.48	30,230
Stabilization Hot Oil Heater w/ SCR catalyst (58.93 MMBtu/hr)	SHTR8	SHTR8	0.43	1.73	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.12	0.48	30,230
Stabilization Hot Oil Heater w/ SCR catalyst (58.93 MMBtu/hr)	SHTR9	SHTR9	0.43	1.73	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.12	0.48	30,230
Stabilization Hot Oil Heater w/ SCR catalyst (58.93 MMBtu/hr)	SHTR10	SHTR10	0.43	1.73	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.12	0.48	30,230
Stabilization Hot Oil Heater w/ SCR catalyst (58.93 MMBtu/hr)	SHTR11	SHTR11	0.43	1.73	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.12	0.48	30,230
Cryo Hot Oil Heater (94.54 MMBtu/hr)	CHTR1	CHTR1	3.47	13.83	1.70	6.75	0.67	2.65	0.23	1.00	0.77	3.39	0.77	3.39	0.19	0.76	48,497
Cryo Hot Oil Heater (94.54 MMBtu/hr)	CHTR2	CHTR2	3.47	13.83	1.70	6.75	0.67	2.65	0.23	1.00	0.77	3.39	0.77	3.39	0.19	0.76	48,497
Cryo Hot Oil Heater w/ SCR Catalyst (94.54 MMBtu/hr)	CHTR3	CHTR3	0.70	2.77	1.70	6.75	0.67	2.65	0.23	1.00	0.77	3.39	0.77	3.39	0.19	0.76	48,497
Cryo Hot Oil Heater w/ SCR Catalyst (94.54 MMBtu/hr)	CHTR4	CHTR4	0.70	2.77	1.70	6.75	0.67	2.65	0.23	1.00	0.77	3.39	0.77	3.39	0.19	0.76	48,497
Regen Heater (35.25 MMBtu/hr)	RHTR1	RHTR1	1.04	4.12	0.63	2.52	0.25	0.99	0.09	0.37	0.29	1.27	0.29	1.27	0.07	0.28	18,082
Regen Heater (35.25 MMBtu/hr)	RHTR2	RHTR2	1.04	4.12	0.63	2.52	0.25	0.99	0.09	0.37	0.29	1.27	0.29	1.27	0.07	0.28	18,082
Regen Heater (35.25 MMBtu/hr)	RHTR3	RHTR3	1.04	4.12	0.63	2.52	0.25	0.99	0.09	0.37	0.29	1.27	0.29	1.27	0.07	0.28	18,082
Regen Heater (35.25 MMBtu/hr)	RHTR4	RHTR4	1.04	4.12	0.63	2.52	0.25	0.99	0.09	0.37	0.29	1.27	0.29	1.27	0.07	0.28	18,082

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CONTROLLED FACILITY EMISSIONS SUMMARY

EMISSIONS SUMMARY TABLE

EMISSION SOURCE DESCRIPTION	FACILITY NUMBER	STACK NUMBER	NOx		CO		VOC (INCLUDES HAPs)		SO_2		TSP		PM_{10}		HAPs		CO2e
			lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	TPY
Stabilizer Flare 1 (Dual Tip Flare) Cryo Flare 2 (Dual Tip Flare) Backup SSM/Emergency Flare 3 (Dual Tip Flare)	FL1-FL3[1]	FL1-FL3[1]	1.40	6.14	2.80	12.26	0.29	1.29	0.00	0.00	0.08	0.33	0.08	0.33	0.00	0.00	6,789
FL1-FL3 Stabilizer Overhead SSM Gas	FL1-FL3OVHD-SSM	FL1-FL3[1]	165.59	3.31	330.57	6.61	1093.54	21.87	0.00	0.00	8.94	0.18	8.94	0.18	15.67	0.31	3,169
FL1-FL3 Cryo Blowdown SSM Gas	FL1-FL3CRYO-SSM	FL1-FL3[1]	323.31	6.47	645.44	12.91	517.03	10.34	0.00	0.00	54.81	1.10	54.81	1.10	1.62	0.03	5,999
Oil Storage Tank 1 (50,000 bbl)	IFR1	IFR1	--	--	--	--	0.98	4.27	--	--	--	--	--	--	0.05	0.21	0.00
Oil Storage Tank 2 (50,000 bbl)	IFR2	IFR2	--	--	--	--	0.98	4.27	--	--	--	--	--	--	0.05	0.21	0.00
Oil Storage Tank 3 (50,000 bbl)	IFR3	IFR3	--	--	--	--	0.98	4.27	--	--	--	--	--	--	0.05	0.21	0.00
Oil Storage Tank 4 (50,000 bbl)	IFR4	IFR4	--	--	--	--	0.98	4.27	--	--	--	--	--	--	0.05	0.21	0.00
Oil Storage Tank 5 (250,000 bbl)	IFR5	IFR5	--	--	--	--	2.59	11.36	--	--	--	--	--	--	0.12	0.53	0.01
Oil Storage Tank 6 (250,000 bbl)	IFR6	IFR6	--	--	--	--	2.59	11.36	--	--	--	--	--	--	0.12	0.53	0.01
Oil Storage Tank 7 (250,000 bbl)	IFR7	IFR7	--	--	--	--	2.59	11.36	--	--	--	--	--	--	0.12	0.53	0.01
Oil Storage Tank 8 (250,000 bbl)	IFR8	IFR8	--	--	--	--	2.59	11.36	--	--	--	--	--	--	0.12	0.53	0.01
Combustor	ECD1	ECD1	0.44	1.16	0.87	2.31	1.30	3.49	0.00	0.00	0.02	0.03	0.02	0.03	0.05	0.14	999
Thermal Oxidizer	TO1	TO1	3.56	15.59	2.17	9.49	0.79	3.51	0.88	3.87	0.22	0.95	0.22	0.95	0.02	0.08	107,248
Thermal Oxidizer	TO2	TO2	3.56	15.59	2.17	9.49	0.79	3.51	0.88	3.87	0.22	0.95	0.22	0.95	0.02	0.08	107,248
Thermal Oxidizer	TO3	TO3	3.56	15.59	2.17	9.49	0.79	3.51	0.88	3.87	0.22	0.95	0.22	0.95	0.02	0.08	107,248
Thermal Oxidizer	TO4	TO4	3.56	15.59	2.17	9.49	0.79	3.51	0.88	3.87	0.22	0.95	0.22	0.95	0.02	0.08	107,248
Fugitives	FUG	FUG	--	--	--	--	16.44	72.00	--	--	--	--	--	--	0.67	2.94	3251
SSM Emissions	SSM	SSM	--	--	--	--	--	10.00	--	--	--	--	--	--	--	--	--
Haul Road Fugitives	ROAD	ROAD	--	--	--	--	--	--	--	--	2.76	0.01	0.70	0.00	--	--	--

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			lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	TPY
Amine Sweetener 1	AU1	TO1	Emissions represented at TO1.														
Amine Sweetener 2	AU2	TO2	Emissions represented at TO2.														
Amine Sweetener 3	AU3	TO3	Emissions represented at TO3.														
Amine Sweetener 4	AU4	TO4	Emissions represented at TO4.														
Gunbarrel Tank	GBS1	ECD1	Emissions represented at ECD1														
Produced Water Tank 1	PWTK1	ECD1	Emissions represented at ECD1														
Produced Water Tank 2	PWTK2	ECD1	Emissions represented at ECD1														
Slop Oil Tank	SOTK1	ECD1	Emissions represented at ECD1														
Slop Oil Truck Loading	SOTL	ECD1	Emissions represented at ECD1														
Emergency Generator	GEN1	GEN1	3.38	0.17	12.69	0.63	4.54	0.23	0.04	0.00	0.18	0.01	0.18	0.01	1.93	0.10	139.55
Emergency Generator	GEN2	GEN2	3.38	0.17	12.69	0.63	4.54	0.23	0.04	0.00	0.18	0.01	0.18	0.01	1.93	0.10	139.55
Emergency Generator	GEN3	GEN3	3.38	0.17	12.69	0.63	4.54	0.23	0.04	0.00	0.18	0.01	0.18	0.01	1.93	0.10	139.55
Emergency Generator	GEN4	GEN4	3.38	0.17	12.69	0.63	4.54	0.23	0.04	0.00	0.18	0.01	0.18	0.01	1.93	0.10	139.55
Malfunction Emissions	Malfunction	Malfunction	--	--	--	--	--	10.00	--	--	--	--	--	--	--	--	--

TOTAL FACILITY EMISSIONS	NOx		CO		VOC (INCLUDES HAPs)		SO_2		TSP		PM_{10}		HAPs		CO2e
	lb/hr[2]	TPY	lb/hr[2]	TPY	lb/hr[2]	TPY	lb/hr[2]	TPY	lb/hr[2]	TPY	lb/hr[2]	TPY	lb/hr[2]	TPY	TPY
	543.5	**179.8**	**1060.1**	**157.9**	**1672.4**	**239.2**	**6.5**	**27.9**	**77.8**	**47.4**	**75.7**	**47.4**	**28.8**	**16.5**	**1,048,600**

[1] Since FL3 serves as a backup flare, the pilot/purge gas emissions for the flares includes only two flares. The NGL/condensate overheads and cryo SSM stream can be routed to any of the flare; therefore, emissions were combined between the three flares. Since the two SSM events cannot occur simulataneously, the highest of the two stream hourly rates was used in the Total Facility Emissions.

[2] For all pollutants except VOC/HAP, the hourly emission rate excludes overhead SSM stream as they cannot occur at the same time and the cryo SSM stream has a higher emission rate. For VOC, the overhead SSM stream is included with the highest hourly rate. For HAP, the generators have the highest hourly rate.

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UNCONTROLLED FACILITY EMISSIONS SUMMARY

UNCONTROLLED EMISSIONS SUMMARY TABLE

EMISSION SOURCE DESCRIPTION	FACILITY IDENTIFICATION NUMBER	STACK NUMBER	NOx		CO		VOC (INCLUDES HAPs)		SO_2		TSP		PM_{10}		HAPs	
			lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
Stabilization Hot Oil Heater (58.93 MMBtu/hr)	SHTR1	SHTR1	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.12	0.48
Stabilization Hot Oil Heater (58.93 MMBtu/hr)	SHTR2	SHTR2	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.12	0.48
Stabilization Hot Oil Heater (58.93 MMBtu/hr)	SHTR3	SHTR3	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.12	0.48
Stabilization Hot Oil Heater (58.93 MMBtu/hr)	SHTR4	SHTR4	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.12	0.48
Stabilization Hot Oil Heater (58.93 MMBtu/hr)	SHTR5	SHTR5	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.12	0.48
Stabilization Hot Oil Heater (58.93 MMBtu/hr)	SHTR6	SHTR6	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.12	0.48
Stabilization Hot Oil Heater w/ SCR catalyst (58.93 MMBtu/hr)	SHTR7	SHTR7	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.12	0.48
Stabilization Hot Oil Heater w/ SCR catalyst (58.93 MMBtu/hr)	SHTR8	SHTR8	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.12	0.48
Stabilization Hot Oil Heater w/ SCR catalyst (58.93 MMBtu/hr)	SHTR9	SHTR9	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.12	0.48
Stabilization Hot Oil Heater w/ SCR catalyst (58.93 MMBtu/hr)	SHTR10	SHTR10	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.12	0.48
Stabilization Hot Oil Heater w/ SCR catalyst (58.93 MMBtu/hr)	SHTR11	SHTR11	1.73	6.89	1.06	4.21	0.41	1.65	0.14	0.63	0.48	2.12	0.48	2.12	0.12	0.48
Cryo Hot Oil Heater (94.54 MMBtu/hr)	CHTR1	CHTR1	3.47	13.83	1.70	6.75	0.67	2.65	0.23	1.00	0.77	3.39	0.77	3.39	0.19	0.76
Cryo Hot Oil Heater (94.54 MMBtu/hr)	CHTR2	CHTR2	3.47	13.83	1.70	6.75	0.67	2.65	0.23	1.00	0.77	3.39	0.77	3.39	0.19	0.76
Cryo Hot Oil Heater w/ SCR Catalyst (94.54 MMBtu/hr)	CHTR3	CHTR3	3.47	13.83	1.70	6.75	0.67	2.65	0.23	1.00	0.77	3.39	0.77	3.39	0.19	0.76
Cryo Hot Oil Heater w/ SCR Catalyst (94.54 MMBtu/hr)	CHTR4	CHTR4	3.47	13.83	1.70	6.75	0.67	2.65	0.23	1.00	0.77	3.39	0.77	3.39	0.19	0.76
Regen Heater (35.25 MMBtu/hr)	RHTR1	RHTR1	1.04	4.12	0.63	2.52	0.25	0.99	0.09	0.37	0.29	1.27	0.29	1.27	0.07	0.28
Regen Heater (35.25 MMBtu/hr)	RHTR2	RHTR2	1.04	4.12	0.63	2.52	0.25	0.99	0.09	0.37	0.29	1.27	0.29	1.27	0.07	0.28
Regen Heater (35.25 MMBtu/hr)	RHTR3	RHTR3	1.04	4.12	0.63	2.52	0.25	0.99	0.09	0.37	0.29	1.27	0.29	1.27	0.07	0.28
Regen Heater (35.25 MMBtu/hr)	RHTR4	RHTR4	1.04	4.12	0.63	2.52	0.25	0.99	0.09	0.37	0.29	1.27	0.29	1.27	0.07	0.28

XTO Energy, Inc.

Cowboy CDP

UNCONTROLLED FACILITY EMISSIONS SUMMARY

UNCONTROLLED EMISSIONS SUMMARY TABLE

EMISSION SOURCE DESCRIPTION	FACILITY IDENTIFICATION NUMBER	STACK NUMBER	NOx		CO		VOC (INCLUDES HAPs)		SO_2		TSP		PM_{10}		HAPs	
			lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
Stabilizer Flare 1 (Dual Tip Flare) Cryo Flare 2 (Dual Tip Flare) Backup SSM/Emergency Flare 3 (Dual Tip Flare)	FL1-FL3[1]	FL1-FL3[1]	1.40	6.14	2.80	12.26	0.29	1.29	0.00	0.00	0.08	0.33	0.08	0.33	0.00	0.00
FL1-FL3 Stabilizer Overhead SSM Gas	FL1-FL3OVHD-SSM	FL1-FL3[1]	Not operating in uncontrolled emissions scenario.													
FL1-FL3 Cryo Blowdown SSM Gas	FL1-FL3OVHD-SSM	FL1-FL3[1]	Not operating in uncontrolled emissions scenario.													
Oil Storage Tank 1 (50,000 bbl)	IFR1	IFR1	--	--	--	--	0.98	4.27	--	--	--	--	--	--	0.05	0.21
Oil Storage Tank 2 (50,000 bbl)	IFR2	IFR2	--	--	--	--	0.98	4.27	--	--	--	--	--	--	0.05	0.21
Oil Storage Tank 3 (50,000 bbl)	IFR3	IFR3	--	--	--	--	0.98	4.27	--	--	--	--	--	--	0.05	0.21
Oil Storage Tank 4 (50,000 bbl)	IFR4	IFR4	--	--	--	--	0.98	4.27	--	--	--	--	--	--	0.12	0.53
Oil Storage Tank 5 (250,000 bbl)	IFR5	IFR5	--	--	--	--	2.59	11.36	--	--	--	--	--	--	0.12	0.53
Oil Storage Tank 6 (250,000 bbl)	IFR6	IFR6	--	--	--	--	2.59	11.36	--	--	--	--	--	--	0.12	0.53
Oil Storage Tank 7 (250,000 bbl)	IFR7	IFR7	--	--	--	--	2.59	11.36	--	--	--	--	--	--	0.12	0.53
Oil Storage Tank 8 (250,000 bbl)	IFR8	IFR8	--	--	--	--	2.59	11.36	--	--	--	--	--	--	0.05	0.14
Combustor	ECD1[1]	ECD1[1]	0.03	0.11	0.05	0.22	0.01	0.03	0.00	0.00	0.00	0.01	0.00	0.01	0.00	0.00
Thermal Oxidizer	TO1	TO1	0.33	1.45	0.20	0.89	0.36	1.58	0.00	0.00	0.18	0.79	0.18	0.79	0.00	0.00
Thermal Oxidizer	TO2	TO2	0.33	1.45	0.20	0.89	0.36	1.58	0.00	0.00	0.18	0.79	0.18	0.79	0.00	0.00
Thermal Oxidizer	TO3	TO3	0.33	1.45	0.20	0.89	0.36	1.58	0.00	0.00	0.18	0.79	0.18	0.79	0.00	0.00
Thermal Oxidizer	TO4	TO4	0.33	1.45	0.20	0.89	0.36	1.58	0.00	0.00	0.18	0.79	0.18	0.79	0.00	0.00

XTO Energy, Inc.

Cowboy CDP

UNCONTROLLED FACILITY EMISSIONS SUMMARY

UNCONTROLLED EMISSIONS SUMMARY TABLE

EMISSION SOURCE DESCRIPTION	FACILITY IDENTIFICATION NUMBER	STACK NUMBER	NOx		CO		VOC (INCLUDES HAPs)		SO_2		TSP		PM_{10}		HAPs	
			lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
Fugitives	FUG	FUG	--	--	--	--	33.82	148.15	--	--	--	--	--	--	--	--
SSM Emissions	SSM	SSM	--	--	--	--	--	10.00	--	--	--	--	--	--	--	--
Haul Road Fugitives	ROAD	ROAD	--	--	--	--	--	--	--	--	2.76	0.01	0.70	0.00	--	--
Amine Sweetener 1	AU1	TO1	--	--	--	--	80.16	351.11	--	--	--	--	--	--	1.80	7.87
Amine Sweetener 2	AU2	TO2	--	--	--	--	80.16	351.11	--	--	--	--	--	--	1.80	7.87
Amine Sweetener 3	AU3	TO3	--	--	--	--	80.16	351.11	--	--	--	--	--	--	1.80	7.87
Amine Sweetener 4	AU4	TO4	--	--	--	--	80.16	351.11	--	--	--	--	--	--	1.80	7.87
Gunbarrel Tank	GBS1	ECD1	--	--	--	--	15.80	69.21	--	--	--	--	--	--	0.55	2.39
Produced Water Tank 1	PWTK1	ECD1	--	--	--	--	2.68	11.75	--	--	--	--	--	--	0.43	1.86
Produced Water Tank 2	PWTK2	ECD1	--	--	--	--	2.68	11.75	--	--	--	--	--	--	0.43	1.86
Slop Oil Tank	SOTK1	ECD1	--	--	--	--	57.70	252.73	--	--	--	--	--	--	1.78	7.79
Slop Oil Truck Loading	SOTL	ECD1	--	--	--	--	53.34	0.58	--	--	--	--	--	--	1.60	
Emergency Generator	GEN1	GEN1	3.38	0.17	12.69	0.63	4.54	0.23	0.04	0.00	0.18	0.01	0.18	0.01	1.93	0.10
Emergency Generator	GEN2	GEN2	3.38	0.17	12.69	0.63	4.54	0.23	0.04	0.00	0.18	0.01	0.18	0.01	1.93	0.10
Emergency Generator	GEN3	GEN3	3.38	0.17	12.69	0.63	4.54	0.23	0.04	0.00	0.18	0.01	0.18	0.01	1.93	0.10
Emergency Generator	GEN4	GEN4	3.38	0.17	12.69	0.63	4.54	0.23	0.04	0.00	0.18	0.01	0.18	0.01	1.93	0.10
Malfunction Emissions	Malfunction	Malfunction	--	--	--	--	--	10.00	--	--	--	--	--	--	--	--

TOTAL FACILITY EMISSIONS	NOx		CO		VOC (INCLUDES HAPs)		SO_2		TSP		PM10		HAPs	
	lb/hr	**TPY**	**lb/hr**	**TPY**	**lb/hr**	**TPY**	**lb/hr**	**TPY**	**lb/hr**	**TPY**	**lb/hr**	**TPY**	**lb/hr**	**TPY**
	53.33	**160.36**	**75.37**	**101.90**	**529.07**	**2022.37**	**2.99**	**12.42**	**13.85**	**45.45**	**11.79**	**45.45**	**22.70**	**58.07**

[1] **Only includes pilot/purge gas emissions in uncontrolled scenario**

XTO Energy, Inc.

Cowboy CDP

Truck Loading Losses - Slop Oil

Truck Loading Losses Calculations

Average BOPD	**210**
Average BOPY	**5704**

LL= 12.46 * SPM/T * (1-EFF/100)

Saturation Factor (S) =	0.6
Average True Vapor Pressure of liquid loaded (P)[a] =	6.55
Maximum True Vapor Pressure of liquid loaded (P)[a] =	7.72
Average Temperature of liquid loaded in Rankin (T) =	535.8
Maximum Temperature of liquid loaded in Rankin (T) =	501.3
Molecular Weight (M)[a] =	54.55
Uncontrolled LL-Average (lb Total HC / bbl Throughput) =	0.2094
Uncontrolled LL-Maximum (lb Total HC / bbl Throughput) =	0.2638
Uncontrolled LL-Average (lb VOC / bbl Throughput) =	**0.2016**
Uncontrolled LL-Maximum (lb VOC / bbl Throughput) =	**0.2540**
Estimated Throughput (bbls/Year) =	5704
Truck Loading Rate (bbls/hour) =	210
Estimated # of Loads (Approximately 1 hr/Load) =	27

Total Uncontrolled Loading Emissions[b]

	lb/hr	TPY
Total Hydrocarbon Emissions	55.40	0.60
Total VOC Emissions	53.34	0.58
Total HAP Emissions	1.60	0.02

Uncollected Emissions Released at Rack[c]

	lb/hr	TPY
Total VOC Emissions	0.69	0.01
Total HAP Emissions	0.02	0.00

XTO Energy, Inc.

Cowboy CDP

Truck Loading Losses - Slop Oil

Truck Loading Losses Calculations

Component	Total Uncontrolled Speciated Vapors		Uncontrolled Speciated Vapors Collected to Combustor	
	Mass Fraction[d]	lb / hr	lb / hr	ton / year
Water	0.00	0.00	0.00	0.00
Hydrogen Sulfide	0.00	0.00	0.00	0.00
Nitrogen	0.00	0.00	0.00	0.00
Carbon Dioxide	0.03	0.02	0.02	0.00
Methane	0.05	0.03	0.03	0.00
Ethane	3.64	2.02	1.92	0.03
Propane	32.70	18.12	17.21	0.23
Iso-butane	9.74	5.40	5.13	0.07
N-butane	25.50	14.13	13.43	0.18
Iso-pentane	7.67	4.25	4.04	0.05
N-pentane	8.26	4.57	4.35	0.06
Cyclopentanes	0.00	0.00	0.00	0.00
Other Hexanes	3.26	1.81	1.72	0.02
n-Hexane	1.90	1.05	1.00	0.01
Methylcyclopentane	1.30	0.72	0.69	0.01
Benzene	0.59	0.33	0.31	0.00
Cyclohexane	1.92	1.06	1.01	0.01
2,2,4 Trimethylpentane	0.00	0.00	0.00	0.00
Other Heptanes	0.66	0.36	0.35	0.00
Methylcyclohexane	1.22	0.68	0.64	0.01
n-Heptane	0.73	0.41	0.39	0.01
Toluene	0.33	0.19	0.18	0.00
Octanes	0.35	0.19	0.18	0.00
Ethylbenzene	0.01	0.00	0.00	0.00
M&P-Xylene	0.06	0.03	0.03	0.00
Nonanes	0.07	0.04	0.04	0.00
Decanes	0.01	0.01	0.01	0.00
Undecanes Plus	0.00	0.00	0.00	0.00
Total	100.00	55.40	52.65	0.72
Total VOC	--	53.34	50.69	0.69
Total HAP	--	1.60	1.52	0.02

a Molecular Weight and VOC/HAP weight percent were obtained from Promax

b Loading emissions include total hydrocarbons as calculated using AP-42, Section 5.2.

c 98.7% of the vapors are collected and routed to the combustor. The remaining 1.3% is illustrated as truck loading emissions.

d The component speciation was obtained from Promax (Slop Tank W&B) and multiplied by the total hydrocarbon emissions. (VOC = 55.4 lb/hr * 98. 7% = 52.65 lb/hr)

XTO Energy, Inc.

Cowboy CDP

PSD MAJOR SOURCE THRESHOLD COMPARISON

PSD NESTED SOURCE CATEGORY Table 1 (20.2.74.501 NMAC)	NOx	CO	VOC (INCLUDES HAPs)	SO_2	TSP	$PM_{10 \& 2.5}$	H2SO4
	TPY	TPY	TPY	TPY	TPY	TPY	TPY
Fossil fuel boilers (or combination thereof) totaling more than 250 MMBtu/hr heat input	**99.70**	83.34	32.72	12.41	41.91	41.91	-
Petroleum storage transfer units, total storage capacity over 300,000 barrels	1.16	2.31	**66.00**	0.00	0.03	0.03	-

* The PSD significant emission rate (SER) for NOx, CO, VOC, SO2, and TSP/PM10, H2SO4 which emits, or has the potential to emit, emissions equal to or greater than 100 TPY.

XTO Energy, Inc.
Cowboy CDP
Generators (GEN1 - GEN4)

Uncontrolled Emissions Calculations

					Manufacturer's Data g/hp-hr				AP-42 Factors lb/MMBtu				lb/hr									tpy								
Source ID	Unit Description	Yearly Operating Hours	Rated HP	MMbtu/hp-hr[1]	NOx	CO	VOC[2]	HCHO	SO_2[3]	$PM_{10 \& 2.5}$[4]	Hexane	Acetaldehyde	NOx	CO	VOC	HCHO	SO_2	$PM_{10 \& 2.5}$	Hexane	Acetaldehyde	HAPs	NOx	CO	VOC	HCHO	SO_2	$PM_{10 \& 2.5}$	Hexane	Acetaldehyde	HAPs
GEN1	Caterpillar G3520H Emergency Generator	100	3063	0.005861	0.50	1.88	0.65	0.26	0.00216	0.01006	0.00111	0.00836	3.38	12.69	4.54	1.76	0.04	0.18	0.02	0.15	1.93	0.17	0.63	0.23	0.09	0.00	0.01	0.00	0.01	0.10
GEN2	Caterpillar G3520H Emergency Generator	100	3063	0.005861	0.50	1.88	0.65	0.26	0.00216	0.01006	0.00111	0.00836	3.38	12.69	4.54	1.76	0.04	0.18	0.02	0.15	1.93	0.17	0.63	0.23	0.09	0.00	0.01	0.00	0.01	0.10
GEN3	Caterpillar G3520H Emergency Generator	100	3063	0.005861	0.50	1.88	0.65	0.26	0.00216	0.01006	0.00111	0.00836	3.38	12.69	4.54	1.76	0.04	0.18	0.02	0.15	1.93	0.17	0.63	0.23	0.09	0.00	0.01	0.00	0.01	0.10
GEN4	Caterpillar G3520H Emergency Generator	100	3063	0.005861	0.50	1.88	0.65	0.26	0.00216	0.01006	0.00111	0.00836	3.38	12.69	4.54	1.76	0.04	0.18	0.02	0.15	1.93	0.17	0.63	0.23	0.09	0.00	0.01	0.00	0.01	0.10

Total Emissions Per Pollutant (TPY)	NOx	CO	VOC	HCHO	SO_2	$PM_{10 \& 2.5}$	Hexane	Acetaldehyde	HAPs
	0.68	**2.54**	**0.91**	**0.35**	**0.01**	**0.04**	**0.00**	**0.03**	**0.39**

[1]Fuel Consumption Rate @ 100% Load from the Gas Engine Rating Pro Report

[2]Emission Factor Includes HCHO

[3]SO_2 Emissions were calculated based on 0.75 gr S/100 scf

[4]PM Emission Factor = Sum of all PM factors in AP-42.

XTO Energy, Inc.
Cowboy CDP
Greenhouse Gas Emissions - Generators (GEN1 - GEN4)

Emission unit number(s):	GEN1-GEN4		
Source description:	Emergency Generators		
Fuel Consumption			
Input heat rate:	17.95	MMBtu/hr	Fired Capacity
Fuel heat value (LHV):	1019	Btu/scf	Field Gas
Fuel rate:	17612.5	scf/hr	Input heat rate / fuel heat value
Annual fuel usage:	154.3	MMscf/yr	8760 hrs/yr operation
Hours per year:	100	hrs/yr each	
Exhaust Parameters			
Heat Rate:	17952.243	MBtu/hr	
Exhaust temp (Tstk):	736	°F	Manufacturer
Stack diameter:	1.00	ft	Manufacturer
Stack height:	14	ft	Manufacturer
Exhaust velocity:	331.40	ft/sec	Manufacturer
Emission Rates			
Engine Output:	3063	horsepower	

GHG Emissions	CO_2	CH4	CH_4 as CO_2e	N_2O	N_2O as CO_2e	Total CO_2e	
	413	0.002	0.055	0.0002	0.066		lb/MMbtu
	2788.90	0.040	0.99	0.004	1.18	2791.07	lb/hr
	139.45	0.00	0.05	0.00	0.06	139.55	tpy (8760 hrs)

1 CO2 factor provided by engine manufacturer

2 40 CFR 98 Emission Factors. Global warming potential of 25 for CH4 and 298 for N20.

XTO Energy, Inc.

Cowboy CDP

BURNER CALCULATIONS

CRITERIA & REGULATED POLLUTANTS

							Manufacturer's Data (NOx, CO, VOC) and AP-42 Factors (SO2, PM)[2]					lb/hr[3]					tpy[4]				
Source ID	Source Description	Fuel Gas LHV Design Case (BTU/SCF)	Fuel Gas LHV Rich Case (BTU/SCF)	Operating Hours	Burner Rich Case (MMBTU/Hr)	Burner Design Case (MMBTU/Hr)	NOx (lb/MMBtu)	CO (lb/MMBtu)	VOC (lb/MMBtu)	SO_2 (lb/MMscf)	$PM_{10 \& 2.5}$ (lb/MMscf)	NOx	CO	VOC	SO_2	$PM_{10 \& 2.5}$	NOx	CO	VOC	SO_2	$PM_{10 \& 2.5}$
SHTR1	Stabilization Hot Oil Heater (58.93 MMBtu/hr)	993.0	1152.0	8760	64.83	58.93	0.0267	0.0163	0.0064	2.25	7.6	1.73	1.06	0.41	0.14	0.48	6.89	4.21	1.65	0.63	2.12
SHTR2	Stabilization Hot Oil Heater (58.93 MMBtu/hr)	993.0	1152.0	8760	64.83	58.93	0.0267	0.0163	0.0064	2.25	7.6	1.73	1.06	0.41	0.14	0.48	6.89	4.21	1.65	0.63	2.12
SHTR3	Stabilization Hot Oil Heater (58.93 MMBtu/hr)	993.0	1152.0	8760	64.83	58.93	0.0267	0.0163	0.0064	2.25	7.6	1.73	1.06	0.41	0.14	0.48	6.89	4.21	1.65	0.63	2.12
SHTR4	Stabilization Hot Oil Heater (58.93 MMBtu/hr)	993.0	1152.0	8760	64.83	58.93	0.0267	0.0163	0.0064	2.25	7.6	1.73	1.06	0.41	0.14	0.48	6.89	4.21	1.65	0.63	2.12
SHTR5	Stabilization Hot Oil Heater (58.93 MMBtu/hr)	993.0	1152.0	8760	64.83	58.93	0.0267	0.0163	0.0064	2.25	7.6	1.73	1.06	0.41	0.14	0.48	6.89	4.21	1.65	0.63	2.12
SHTR6	Stabilization Hot Oil Heater (58.93 MMBtu/hr)	993.0	1152.0	8760	64.83	58.93	0.0267	0.0163	0.0064	2.25	7.6	1.73	1.06	0.41	0.14	0.48	6.89	4.21	1.65	0.63	2.12
SHTR7	Stabilization Hot Oil Heater w/ SCR catalyst (58.93 MMBtu/hr)	993.0	1152.0	8760	64.83	58.93	0.0067	0.0163	0.0064	2.25	7.6	0.43	1.06	0.41	0.14	0.48	1.73	4.21	1.65	0.63	2.12
SHTR8	Stabilization Hot Oil Heater w/ SCR catalyst (58.93 MMBtu/hr)	993.0	1152.0	8760	64.83	58.93	0.0067	0.0163	0.0064	2.25	7.6	0.43	1.06	0.41	0.14	0.48	1.73	4.21	1.65	0.63	2.12
SHTR9	Stabilization Hot Oil Heater w/ SCR catalyst (58.93 MMBtu/hr)	993.0	1152.0	8760	64.83	58.93	0.0067	0.0163	0.0064	2.25	7.6	0.43	1.06	0.41	0.14	0.48	1.73	4.21	1.65	0.63	2.12
SHTR10	Stabilization Hot Oil Heater w/ SCR catalyst (58.93 MMBtu/hr)	993.0	1152.0	8760	64.83	58.93	0.0067	0.0163	0.0064	2.25	7.6	0.43	1.06	0.41	0.14	0.48	1.73	4.21	1.65	0.63	2.12
SHTR11	Stabilization Hot Oil Heater w/ SCR catalyst (58.93 MMBtu/hr)	993.0	1152.0	8760	64.83	58.93	0.0067	0.0163	0.0064	2.25	7.6	0.43	1.06	0.41	0.14	0.48	1.73	4.21	1.65	0.63	2.12
CHTR1	Cryo Hot Oil Heater (94.54 MMBtu/hr)	993.0	1152.0	8760	103.99	94.54	0.0334	0.0163	0.0064	2.25	7.6	3.47	1.70	0.67	0.23	0.77	13.83	6.75	2.65	1.00	3.39
CHTR2	Cryo Hot Oil Heater (94.54 MMBtu/hr)	993.0	1152.0	8760	103.99	94.54	0.0334	0.0163	0.0064	2.25	7.6	3.47	1.70	0.67	0.23	0.77	13.83	6.75	2.65	1.00	3.39
CHTR3	Cryo Hot Oil Heater w/ SCR Catalyst (94.54 MMBtu/hr)	993.0	1152.0	8760	103.99	94.54	0.0067	0.0163	0.0064	2.25	7.6	0.70	1.70	0.67	0.23	0.77	2.77	6.75	2.65	1.00	3.39
CHTR4	Cryo Hot Oil Heater w/ SCR Catalyst (94.54 MMBtu/hr)	993.0	1152.0	8760	103.99	94.54	0.0067	0.0163	0.0064	2.25	7.6	0.70	1.70	0.67	0.23	0.77	2.77	6.75	2.65	1.00	3.39
RHTR1	Regen Heater (35.25 MMBtu/hr)	993.0	1152.0	8760	38.77	35.25	0.0267	0.0163	0.0064	2.25	7.6	1.04	0.63	0.25	0.09	0.29	4.12	2.52	0.99	0.37	1.27
RHTR2	Regen Heater (35.25 MMBtu/hr)	993.0	1152.0	8760	38.77	35.25	0.0267	0.0163	0.0064	2.25	7.6	1.04	0.63	0.25	0.09	0.29	4.12	2.52	0.99	0.37	1.27
RHTR3	Regen Heater (35.25 MMBtu/hr)	993.0	1152.0	8760	38.77	35.25	0.0267	0.0163	0.0064	2.25	7.6	1.04	0.63	0.25	0.09	0.29	4.12	2.52	0.99	0.37	1.27
RHTR4	Regen Heater (35.25 MMBtu/hr)	993.0	1152.0	8760	38.77	35.25	0.0267	0.0163	0.0064	2.25	7.6	1.04	0.63	0.25	0.09	0.29	4.12	2.52	0.99	0.37	1.27

Total (tpy)	NOx	CO	VOC	SO_2	$PM_{10 \& 2.5}$
	99.70	**83.34**	**32.72**	**12.41**	**41.91**

[1] NOx, CO, and VOC factors were provided by the equipment manufacturers.

[2] SO2 and PM emission factors were adjusted based on site heat content versus the AP-42 value of 1,020 Btu/scf. SO2 factor was adjusted to 7500 gr/MMscf (0.75 gr/100 scf).

[3] LB/HR emissions were based on rich case fuel burner operating data.

[4] TPY emissions were based on design case fuel burner operating data.

XTO Energy, Inc.

Cowboy CDP

BURNER CALCULATIONS

HAZARDOUS AIR POLLUTANTS (HAPs)

							AP-42 Factors[3] lb/MMSCF					lb/hr[1]					tpy[2]				
Source ID	Source Description	Fuel Gas LHV Design Case (BTU/SCF)	Fuel Gas LHV Rich Case (BTU/SCF)	Operating Hours	Burner Rich Case (MMBTU/Hr)	Burner Design Case (MMBTU/Hr)	Benzene	Toluene	N-Hexane	HCHO	Mercury	Benzene	Toluene	N-Hexane	HCHO	Dichloro benzene	Benzene	Toluene	N-Hexane	HCHO	Mercury
SHTR1	Stabilization Hot Oil Heater (58.93 MMBtu/hr)	993.0	1152.0	8760	64.83	58.93	0.0021	0.0034	1.8	0.0750	0.0021	0.00	0.00	0.11	0.00	0.00	0.00	0.00	0.46	0.02	0.00
SHTR2	Stabilization Hot Oil Heater (58.93 MMBtu/hr)	993.0	1152.0	8760	64.83	58.93	0.0021	0.0034	1.8	0.0750	0.0012	0.00	0.00	0.11	0.00	0.00	0.00	0.00	0.46	0.02	0.00
SHTR3	Stabilization Hot Oil Heater (58.93 MMBtu/hr)	993.0	1152.0	8760	64.83	58.93	0.0021	0.0034	1.8	0.0750	0.0012	0.00	0.00	0.11	0.00	0.00	0.00	0.00	0.46	0.02	0.00
SHTR4	Stabilization Hot Oil Heater (58.93 MMBtu/hr)	993.0	1152.0	8760	64.83	58.93	0.0021	0.0034	1.8	0.0750	0.0012	0.00	0.00	0.11	0.00	0.00	0.00	0.00	0.46	0.02	0.00
SHTR5	Stabilization Hot Oil Heater (58.93 MMBtu/hr)	993.0	1152.0	8760	64.83	58.93	0.0021	0.0034	1.8	0.0750	0.0012	0.00	0.00	0.11	0.00	0.00	0.00	0.00	0.46	0.02	0.00
SHTR6	Stabilization Hot Oil Heater (58.93 MMBtu/hr)	993.0	1152.0	8760	64.83	58.93	0.0021	0.0034	1.8	0.0750	0.0012	0.00	0.00	0.11	0.00	0.00	0.00	0.00	0.46	0.02	0.00
SHTR7	Stabilization Hot Oil Heater w/ SCR catalyst (58.93 MMBtu/hr)	993.0	1152.0	8760	64.83	58.93	0.0021	0.0034	1.8	0.0750	0.0012	0.00	0.00	0.11	0.00	0.00	0.00	0.00	0.46	0.02	0.00
SHTR8	Stabilization Hot Oil Heater w/ SCR catalyst (58.93 MMBtu/hr)	993.0	1152.0	8760	64.83	58.93	0.0021	0.0034	1.8	0.0750	0.0012	0.00	0.00	0.11	0.00	0.00	0.00	0.00	0.46	0.02	0.00
SHTR9	Stabilization Hot Oil Heater w/ SCR catalyst (58.93 MMBtu/hr)	993.0	1152.0	8760	64.83	58.93	0.0021	0.0034	1.8	0.0750	0.0012	0.00	0.00	0.11	0.00	0.00	0.00	0.00	0.46	0.02	0.00
SHTR10	Stabilization Hot Oil Heater w/ SCR catalyst (58.93 MMBtu/hr)	993.0	1152.0	8760	64.83	58.93	0.0021	0.0034	1.8	0.0750	0.0012	0.00	0.00	0.11	0.00	0.00	0.00	0.00	0.46	0.02	0.00
SHTR11	Stabilization Hot Oil Heater w/ SCR catalyst (58.93 MMBtu/hr)	993.0	1152.0	8760	64.83	58.93	0.0021	0.0034	1.8	0.0750	0.0012	0.00	0.00	0.11	0.00	0.00	0.00	0.00	0.46	0.02	0.00
CHTR1	Cryo Hot Oil Heater (94.54 MMBtu/hr)	993.0	1152.0	8760	103.99	94.54	0.0021	0.0034	1.8	0.0750	0.0012	0.00	0.00	0.18	0.01	0.00	0.00	0.00	0.73	0.03	0.00
CHTR2	Cryo Hot Oil Heater (94.54 MMBtu/hr)	993.0	1152.0	8760	103.99	94.54	0.0021	0.0034	1.8	0.0750	0.0012	0.00	0.00	0.18	0.01	0.00	0.00	0.00	0.73	0.03	0.00
CHTR3	Cryo Hot Oil Heater w/ SCR Catalyst (94.54 MMBtu/hr)	993.0	1152.0	8760	103.99	94.54	0.0021	0.0034	1.8	0.0750	0.0012	0.00	0.00	0.18	0.01	0.00	0.00	0.00	0.73	0.03	0.00
CHTR4	Cryo Hot Oil Heater w/ SCR Catalyst (94.54 MMBtu/hr)	993.0	1152.0	8760	103.99	94.54	0.0021	0.0034	1.8	0.0750	0.0012	0.00	0.00	0.18	0.01	0.00	0.00	0.00	0.73	0.03	0.00
RHTR1	Regen Heater (35.25 MMBtu/hr)	993.0	1152.0	8760	38.77	35.25	0.0021	0.0034	1.8	0.0750	0.0012	0.00	0.00	0.07	0.00	0.00	0.00	0.00	0.27	0.01	0.00
RHTR2	Regen Heater (35.25 MMBtu/hr)	993.0	1152.0	8760	38.77	35.25	0.0021	0.0034	1.8	0.0750	0.0012	0.00	0.00	0.07	0.00	0.00	0.00	0.00	0.27	0.01	0.00
RHTR3	Regen Heater (35.25 MMBtu/hr)	993.0	1152.0	8760	38.77	35.25	0.0021	0.0034	1.8	0.0750	0.0012	0.00	0.00	0.07	0.00	0.00	0.00	0.00	0.27	0.01	0.00
RHTR4	Regen Heater (35.25 MMBtu/hr)	993.0	1152.0	8760	38.77	35.25	0.0021	0.0034	1.8	0.0750	0.0012	0.00	0.00	0.07	0.00	0.00	0.00	0.00	0.27	0.01	0.00

[1] LB/HR emissions were based on rich case fuel burner operating data.
[2] TPY emissions were based on design case fuel burner operating data.
[3] Source: AP-42 Table 1.4-1, 1.4-2, & 1.4-3

Total Individual HAPS (tpy)	Benzene	Toluene	N-Hexane	HCHO	Dichloro benzene
	0.01	**0.02**	**9.02**	**0.38**	**0.01**

Total Combined HAPS (tpy)	**9.43**

XTO Energy, Inc.
Cowboy CDP
HEATERS - EXHAUST STACK FLOW & FUEL CONSUMPTION RATES

Exhaust Stack and Fuel Consumption Data

Source	Stabilization Heaters (Design Case)
Burner Rating (btu/hr)	58,930,000
Heating Value (btu/scf)	993.0
Stack Temperature (°F)	488
Stack Diameter (ft)	4.0
Stack Height (ft)	33.0
Fuel Consumption (scf/hr)	59345
Fuel Consumption (scf/day)	1424290
Fuel Consumption (mmscf/year)	519.9
Air Injection Rate (scf/hr)	811845.3
Total exhaust flow rate @ STP (scf/hr)	871190.74
Total exhaust flow rate @ STP (scf/sec)	242.0
Total exhaust flow rate @ 488 °F (acf/hr)	1588247.7
Total exhaust flow rate @ 488 °F (acf/sec)	441.2
Exhaust Stack Exit Velocity @ STP (ft/sec)	19.3
Exhaust Stack Exit Velocity @ 488 °F (ft/sec)	35.1
Source	Cryogenic Heaters (Design Case)
Burner Rating (btu/hr)	94,540,000
Heating Value (btu/scf)	993.0
Stack Temperature (°F)	599
Stack Diameter (ft)	4.0
Stack Height (ft)	76.9
Fuel Consumption (scf/hr)	95206
Fuel Consumption (scf/day)	2284955
Fuel Consumption (mmscf/year)	834.0
Air Injection Rate (scf/hr)	1354787.7
Total exhaust flow rate @ STP (scf/hr)	1449994.16
Total exhaust flow rate @ STP (scf/sec)	402.8
Total exhaust flow rate @ 599 °F (acf/hr)	2952968.9
Total exhaust flow rate @ 599 °F (acf/sec)	820.3
Exhaust Stack Exit Velocity @ STP (ft/sec)	32.1
Exhaust Stack Exit Velocity @ 599 °F (ft/sec)	65.3
Source	Regeneration Heaters (Design Case)
Burner Rating (btu/hr)	35,250,000
Heating Value (btu/scf)	993.0
Stack Temperature (°F)	470
Stack Diameter (ft)	2.7
Stack Height (ft)	28.7
Fuel Consumption (scf/hr)	35498
Fuel Consumption (scf/day)	851964
Fuel Consumption (mmscf/year)	311.0
Air Injection Rate (scf/hr)	552001.5
Total exhaust flow rate @ STP (scf/hr)	587500.00
Total exhaust flow rate @ STP (scf/sec)	163.2
Total exhaust flow rate @ 470 °F (acf/hr)	1050721.2
Total exhaust flow rate @ 470 °F (acf/sec)	291.9
Exhaust Stack Exit Velocity @ STP (ft/sec)	29.2
Exhaust Stack Exit Velocity @ 470 °F (ft/sec)	52.3

XTO Energy, Inc.
Cowboy CDP
Greenhouse Gas Emissions - Stabilizer Heaters

Emission unit number(s): SHTR1,SHTR2,SHTR3,SHTR4,SHTR5,SHTR6,SHTR7,SHTR8,SHTR9,SHTR10,SHTR11
Source description: Stabilization Hot Oil Heater (58.93 MMBtu/hr)

Fuel Consumption

Input heat rate:	58.93	MMBtu/hr	Capacity
Fuel heat value:	993	Btu/scf	Field Gas
Fuel rate:	59,345	scf/hr	Input heat rate / fuel heat value
Annual fuel usage:	519.9	MMscf/yr	8760 hrs/yr operation
Hours per year:	8760	hrs/yr	

Exhaust Parameters

Heat Rate:	58,930	MBtu/hr	
Exhaust temp (Tstk):	488	°F	Manufacturer
Stack diameter:	4.00	ft	Manufacturer
Stack height:	33	ft	Manufacturer
Exhaust velocity:	35.1	ft/sec	Manufacturer

Emission Rates
Uncontrolled Heater Emissions

GHG Emissions	CO_2	CH4	CH_4 as CO_2e	N_2O	N_2O as CO_2e	Total CO_2e	
	117.00	0.002	0.055	0.0002	0.066		lb/MMbtu
	6,895	0.130	3.25	0.013	3.87	6,902	lb/hr
	30,199	0.57	14.23	0.06	16.96	30,230	tpy (8760 hrs)

1 40 CFR 98 Emission Factors. Global warming potential of 25 for CH4 and 298 for N20.

XTO Energy, Inc.
Cowboy CDP
Greenhouse Gas Emissions - Cryo Heaters

Emission unit number(s):	CHTR1,CHTR2,CHTR3,CHTR4
Source description:	Cryo Hot Oil Heater (94.54 MMBtu/hr)

Fuel Consumption

Input heat rate:	94.54	MMBtu/hr	Capacity
Fuel heat value:	993	Btu/scf	Field Gas
Fuel rate:	95,206	scf/hr	Input heat rate / fuel heat value
Annual fuel usage:	834.0	MMscf/yr	8760 hrs/yr operation
Hours per year:	8760	hrs/yr	

Exhaust Parameters

Heat Rate:	94,540	MBtu/hr	
Exhaust temp (Tstk):	599	°F	Manufacturer
Stack diameter:	4.00	ft	Manufacturer
Stack height:	76.875	ft	Manufacturer
Exhaust velocity:	65.3	ft/sec	Manufacturer

Emission Rates

Uncontrolled Heater Emissions

GHG Emissions	CO_2	CH4	CH_4 as CO_2e	N_2O	N_2O as CO_2e	Total CO_2e	
	117.00	0.002	0.055	0.0002	0.066		lb/MMbtu
	11,061	0.208	5.21	0.021	6.21	11,072	lb/hr
	48,447	0.91	22.83	0.09	27.21	48,497	tpy (8760 hrs)

1 40 CFR 98 Emission Factors. Global warming potential of 25 for CH4 and 298 for N20.

XTO Energy, Inc.
Cowboy CDP
Greenhouse Gas Emissions - Regen Heaters

Emission unit number(s):	RHTR1,RHTR2,RHTR3,RHTR4
Source description:	Regen Heater (35.25 MMBtu/hr)

Fuel Consumption

Input heat rate:	35.25	MMBtu/hr	Capacity
Fuel heat value:	993	Btu/scf	Field Gas
Fuel rate:	35,498	scf/hr	Input heat rate / fuel heat value
Annual fuel usage:	311.0	MMscf/yr	8760 hrs/yr operation
Hours per year:	8760	hrs/yr	

Exhaust Parameters

Heat Rate:	35,250	MBtu/hr	
Exhaust temp (Tstk):	470	°F	Manufacturer
Stack diameter:	2.67	ft	Manufacturer
Stack height:	28.7	ft	Manufacturer
Exhaust velocity:	52.3	ft/sec	Manufacturer

Emission Rates
Uncontrolled Heater Emissions

GHG Emissions	CO_2	CH4	CH_4 as CO_2e	N_2O	N_2O as CO_2e	Total CO_2e	
	117.00	0.002	0.055	0.0002	0.066		lb/MMbtu
	4,124	0.078	1.94	0.008	2.32	4,128	lb/hr
	18,064	0.34	8.51	0.03	10.15	18,082	tpy (8760 hrs)

1 *40 CFR 98 Emission Factors. Global warming potential of 25 for CH4 and 298 for N20.*

XTO Energy, Inc.
Cowboy CDP
DUAL TIP FLARE SUMMARY - FL1/FL2/FL3

Flare Emissions Summary Table

Stream Source[a,b,c]	NOx			CO			Total VOC			SO_2			$PM_{10 \& 2.5}$			Total HAPs		
	lb/hr	lb/day	TPY	lb/hr	lb/day	TPY	lb/hr	lb/day	TPY	lb/hr	lb/day	TPY	lb/hr	lb/day	TPY	lb/hr	lb/day	TPY
Stabilizer Overhead SSM Gas (FL1 - FL3OVHD-SSM)	165.59	331.17	3.31	330.57	661.15	6.61	1,093.54	2,187.09	21.87	0.00	0.00	0.00	8.94	17.88	0.18	15.67	31.35	0.31
Cryo Blowdown SSM Gas (FL1-FL3CRYO-SSM)	323.31	646.62	6.47	645.44	1,290.89	12.91	517.03	1,034.06	10.34	0.00	0.00	0.00	54.81	109.63	1.10	1.62	3.24	0.03
Pilot Fuel & Purge Gas (FL1)	0.70	16.82	3.07	1.40	33.58	6.13	0.15	3.54	0.65	0.00	0.00	0.00	0.04	0.91	0.17	0.00	0.00	0.00
Pilot Fuel & Purge Gas (FL2)	0.70	16.82	3.07	1.40	33.58	6.13	0.15	3.54	0.65	0.00	0.00	0.00	0.04	0.91	0.17	0.00	0.00	0.00
Pilot Fuel & Purge Gas (FL3)	Operated only as backup to FL1-FL2																	
Total Emissions	**324.71**	**680.25**	**15.92**	**648.24**	**1,358.04**	**25.16**	**1,093.84**	**2,194.16**	**23.16**	**--**	**--**	**--**	**54.89**	**111.44**	**1.43**	**15.67**	**31.35**	**0.31**

Footnotes:
[a] SSM gas can be routed to one or any combination of the three flares. For emissions tracking purposes in accordance with the permit, XTO Energy is requesting a combined emisison limit for flaring.
[b] SSM Stabilizer Overhead Gas and Cryo Blowdown SSM events can not occur within the same 24 hour period.
[c] SSM Stabilizer Overhead Gas and Cryo Blowdown SSM events can not occur within the same 24 hour period, so XTO conservatively is assuming each can occur 1 days per year.

XTO Energy, Inc.
Cowboy CDP
DUAL TIP FLARE CRYO SSM HOURLY EMISSIONS (COMBINED BETWEEN ALL FLARES)

DUAL TIP 20 MMSCFD FLARES - HOURLY (FL1 - FL3CRYO-SSM)

Maximum Hourly CRYO-SSM Emission Rates and Composition to Flare[a,b]

Component	CRYO Blowdown SSM Gas	Total	Destruction Efficiency	Exhaust Stream (controlled)
	(lb/hr)	(lb/hr)	(%)	(lb/hr)
Water	14	14	0%	**14.24**
Hydrogen Sulfide	0	0	98%	**0.00**
Nitrogen	1175	1175	0%	**1175.20**
Carbon Dioxide	262	262	0%	**262.09**
Methane	62157	62157	98%	**1243.14**
Ethane	23327	23327	98%	**466.54**
Propane	16770	16770	98%	**335.39**
Iso-butane	2218	2218	98%	**44.36**
N-butane	4972	4972	98%	**99.43**
Iso-pentane	791	791	98%	**15.82**
N-pentane	730	730	98%	**14.60**
Cyclopentanes	0	0	98%	**0.00**
Other Hexanes	168	168	98%	**3.36**
n-Hexane	73	73	98%	**1.45**
Methylcyclopentane	40	40	98%	**0.80**
Benzene	8	8	98%	**0.16**
Cyclohexane	40	40	98%	**0.80**
2,2,4 Trimethylpentane	0	0	98%	**0.00**
Other Heptanes	16	16	98%	**0.32**
Methylcyclohexane	16	16	98%	**0.31**
n-Heptane	5	5	98%	**0.11**
Toluene	0	0	98%	**0.00**
Octanes	6	6	98%	**0.12**
Ethylbenzene	0	0	98%	**0.00**
M&P-Xylene	0	0	98%	**0.00**
Nonanes	0	0	98%	**0.00**
Decanes	0	0	98%	**0.00**
Undecanes Plus	0	0	98%	**0.00**
Total	**112787**	**112787**	**--**	**3678.25**
Total VOC	**25851**	**25851**	**--**	**517.03**
Total HAP	**81**	**81**	**--**	**1.62**
Heating Value (Btu/scf)	1,171.41	**1,171.41**		
Molecular Weight	21.40	**--**		
SO2 Emissions (lb/hr)	0.00	**0.00**		
Volumetric Flow (scf/hr)	2,000,000	**2,000,000**		
Heat Release (MMBtu/hr)	2,342.81	**2,342.81**		

Criteria Pollutant Emissions from Flare [b]

Component	Emission Rate	Emission Factor	Emission Factor Units
	(lb/hr)		
NO_X	323.31	0.138	lb/MMBtu
CO	645.44	0.2755	lb/MMBtu
SO_2	0.00	--	--
PM_{10}	54.81	7.60	lb/MMscf
$PM_{2.5}$	54.81	7.60	lb/MMscf
H_2S	0.00	--	--

Flare DRE	98.00	%
CRYO-SSM Flare Time	1	blowdown/hr
	2	hrs/day
	40	hrs/year

Footnotes:
[a] Uncontrolled stream properties determined via ProMax.
[b] Flare CO and NOx emission factors from TCEQ Air Permit Techincal Guidance for Chemical Sources. PM and PM2.5 emission factors from AP-42, Table 1.4-1 and 1.4-2, July 1998. SO2 emissions assume 100% conversion of H2S to SO2.

XTO Energy, Inc.
Cowboy CDP
DUAL TIP FLARE CRYO SSM ANNUAL EMISSIONS (COMBINED BETWEEN ALL FLARES)

DUAL TIP 20 MMSCFD FLARES - ANNUAL (FL1 - FL3CRYO-SSM)

Annual Emission CRYO-SSM Rates and Composition to Flare[a,b]				
Component	CRYO Blowdown SSM Gas	Total	Destruction Efficiency	Exhaust Stream (controlled)
	(ton/yr)	ton/yr	(%)	(ton/yr)
Water	0.28	0.28	0%	**0.28**
Hydrogen Sulfide	0.00	0.00	98%	**0.00**
Nitrogen	23.50	23.50	0%	**23.50**
Carbon Dioxide	5.24	5.24	0%	**5.24**
Methane	1243.14	1243.14	98%	**24.86**
Ethane	466.54	466.54	98%	**9.33**
Propane	335.39	335.39	98%	**6.71**
Iso-butane	44.36	44.36	98%	**0.89**
N-butane	99.43	99.43	98%	**1.99**
Iso-pentane	15.82	15.82	98%	**0.32**
N-pentane	14.60	14.60	98%	**0.29**
Cyclopentanes	0.00	0.00	98%	**0.00**
Other Hexanes	3.36	3.36	98%	**0.07**
n-Hexane	1.45	1.45	98%	**0.03**
Methylcyclopentane	0.80	0.80	98%	**0.02**
Benzene	0.16	0.16	98%	**0.00**
Cyclohexane	0.80	0.80	98%	**0.02**
2,2,4 Trimethylpentane	0.00	0.00	98%	**0.00**
Other Heptanes	0.32	0.32	98%	**0.01**
Methylcyclohexane	0.31	0.31	98%	**0.01**
n-Heptane	0.11	0.11	98%	**0.00**
Toluene	0.00	0.00	98%	**0.00**
Octanes	0.12	0.12	98%	**0.00**
Ethylbenzene	0.00	0.00	98%	**0.00**
M&P-Xylene	0.00	0.00	98%	**0.00**
Nonanes	0.00	0.00	98%	**0.00**
Decanes	0.00	0.00	98%	**0.00**
Undecanes Plus	0.00	0.00	98%	**0.00**
Total	**2255.74**	**2255.74**	--	**73.56**
Total VOC	**517.03**	**517.03**	--	**10.34**
Total HAP	**1.62**	**0.00**	--	**0.03**
Heating Value (Btu/scf)	1,171.41	**1,171.41**		
Molecular Weight	21.40	--		
SO2 Emissions (lb/hr)	0.02	**0.02**		
Volumetric Flow (scf/year)	80,000,000	**80,000,000**		
Heat Release (MMBtu/hr)	93,712.50	**93,712.50**		

Criteria Pollutant Emissions from Flare[b]			
Component	Emission Rate	Emission Factor	Emission Factor Units
	ton/yr		
NO_X	6.47	0.138	lb/MMBtu
CO	12.91	0.5496	lb/MMBtu
SO_2	0.00	--	--
PM_{10}	0.30	7.60	lb/MMscf
$PM_{2.5}$	0.30	7.60	lb/MMscf
H_2S	0.00	--	--

Flare DRE	98.00	%
CRYO-SSM Flare Time	1.00	blowdown/hr
	2.00	hrs/day
	40.00	hrs/year
	4,000,000	MMscfd

Footnotes:

[a] Uncontrolled stream properties determined via ProMax.

[b] Flare CO and NOx emission factors from TCEQ Air Permit Techincal Guidance for Chemical Sources. PM and PM2.5 emission factors from AP-42, Table 1.4-1 and 1.4-2, July 1998. SO2 emissions assume 100% conversion of H2S to SO2.

XTO Energy, Inc.
Cowboy CDP
DUAL TIP FLARE OVERHEAD SSM HOURLY EMISSIONS (COMBINED BETWEEN ALL FLARES)

DUAL TIP 20 MMSCFD FLARES - HOURLY (FL1 - FL3OVHD-SSM)

Maximum Hourly OVHD-SSM Emission Rates and Composition to Flare[a,b]

Component	Stabilizer Overhead SSM Gas	Total	Destruction Efficiency	Exhaust Stream (controlled)
	(lb/hr)	(lb/hr)	(%)	(lb/hr)
Water	208.88	208.88	0%	**208.88**
Hydrogen Sulfide	0.00	0.00	98%	**0.00**
Nitrogen	0.00	0.00	0%	**0.00**
Carbon Dioxide	28.99	28.99	0%	**28.99**
Methane	4.23	4.23	98%	**0.08**
Ethane	5800.12	5800.12	98%	**116.00**
Propane	36556.18	36556.18	98%	**731.12**
Iso-butane	4472.31	4472.31	98%	**89.45**
N-butane	7658.06	7658.06	98%	**153.16**
Iso-pentane	1463.95	1463.95	98%	**29.28**
N-pentane	1435.43	1435.43	98%	**28.71**
Cyclopentanes	0.00	0.00	98%	**0.00**
Other Hexanes	647.19	647.19	98%	**12.94**
n-Hexane	340.63	340.63	98%	**6.81**
Methylcyclopentane	266.13	266.13	98%	**5.32**
Benzene	257.30	257.30	98%	**5.15**
Cyclohexane	498.99	498.99	98%	**9.98**
2,2,4 Trimethylpentane	0.00	0.00	98%	**0.00**
Other Heptanes	118.82	118.82	98%	**2.38**
Methylcyclohexane	323.42	323.42	98%	**6.47**
n-Heptane	198.04	198.04	98%	**3.96**
Toluene	157.82	157.82	98%	**3.16**
Octanes	150.51	150.51	98%	**3.01**
Ethylbenzene	0.00	0.00	98%	**0.00**
M&P-Xylene	27.98	27.98	98%	**0.56**
Nonanes	50.70	50.70	98%	**1.01**
Decanes	18.75	18.75	98%	**0.37**
Undecanes Plus	34.97	34.97	98%	**0.70**
Total	**60719.37**	**60719.37**	--	**1447.50**
Total VOC	**54677.15**	**54677.15**	--	**1093.54**
Total HAP	**783.72**	**783.72**	--	**15.67**
Heating Value (Btu/scf)	2,399.81	**2,399.81**		
Molecular Weight	46.08	--		
SO2 Emissions (lb/hr)	0.00	**0.00**		
Volumetric Flow (scf/hr)	500,000.00	**500,000.00**		
Heat Release (MMBtu/hr)	1,199.91	**1,199.91**		

Criteria Pollutant Emissions from Flare [b]

Component	Emission Rate	Emission Factor	Emission Factor Units
	(lb/hr)		
NO_X	165.59	0.138	lb/MMBtu
CO	330.57	0.2755	lb/MMBtu
SO_2	0.00	--	--
PM_{10}	8.94	7.60	lb/MMscf
$PM_{2.5}$	8.94	7.60	lb/MMscf
H_2S	0.00	--	--

Flare DRE	98.00	%
OVHD-SSM Flare Time	1.00	blowdown/hr
	2.00	hrs/day
	40.00	hrs/year

Footnotes:

[a] Uncontrolled stream properties determined via ProMax.

[b] Flare CO and NOx emission factors from TCEQ Air Permit Techincal Guidance for Chemical Sources. PM and PM2.5 emission factors from AP-42, Table 1.4-1 and 1.4-2, July 1998. SO2 emissions assume 100% conversion of H2S to SO2.

XTO Energy, Inc.
Cowboy CDP
DUAL TIP FLARE OVERHEAD SSM ANNUAL EMISSIONS (COMBINED BETWEEN ALL FLARES)

DUAL TIP 20 MMSCFD FLARES - ANNUAL (FL1 - FL3OVHD-MSS)

Annual Emission OVHD-SSM Rates and Composition to Flare[a,b]

Component	Stabilizer Overhead SSM Gas (ton/yr)	Total ton/yr	Destruction Efficiency (%)	Exhaust Stream (controlled) (ton/yr)
Water	4.18	4.18	0%	**4.18**
Hydrogen Sulfide	0.00	0.00	98%	**0.00**
Nitrogen	0.00	0.00	0%	**0.00**
Carbon Dioxide	0.58	0.58	0%	**0.58**
Methane	0.08	0.08	98%	**0.00**
Ethane	116.00	116.00	98%	**2.32**
Propane	731.12	731.12	98%	**14.62**
Iso-butane	89.45	89.45	98%	**1.79**
N-butane	153.16	153.16	98%	**3.06**
Iso-pentane	29.28	29.28	98%	**0.59**
N-pentane	28.71	28.71	98%	**0.57**
Cyclopentanes	0.00	0.00	98%	**0.00**
Other Hexanes	12.94	12.94	98%	**0.26**
n-Hexane	6.81	6.81	98%	**0.14**
Methylcyclopentane	5.32	5.32	98%	**0.11**
Benzene	5.15	5.15	98%	**0.10**
Cyclohexane	9.98	9.98	98%	**0.20**
2,2,4 Trimethylpentane	0.00	0.00	98%	**0.00**
Other Heptanes	2.38	2.38	98%	**0.05**
Methylcyclohexane	6.47	6.47	98%	**0.13**
n-Heptane	3.96	3.96	98%	**0.08**
Toluene	3.16	3.16	98%	**0.06**
Octanes	3.01	3.01	98%	**0.06**
Ethylbenzene	0.00	0.00	98%	**0.00**
M&P-Xylene	0.56	0.56	98%	**0.01**
Nonanes	1.01	1.01	98%	**0.02**
Decanes	0.37	0.37	98%	**0.01**
Undecanes Plus	0.70	0.70	98%	**0.01**
Total	**1214.39**	**1214.39**	**--**	**28.95**
Total VOC	**1093.54**	**1093.54**	**--**	**21.87**
Total HAP	**15.67**	**0.56**	**--**	**0.31**
Heating Value (Btu/scf)	2,399.81	**2,399.81**		
Molecular Weight	46.08	**--**		
SO2 Emissions (lb/hr)	0.02	**0.02**		
Volumetric Flow (scf/year)	20,000,000	**20,000,000**		
Heat Release (MMBtu/hr)	47,996.28	**47,996.28**		

Criteria Pollutant Emissions from Flare [b]

Component	Emission Rate ton/yr	Emission Factor	Emission Factor Units
NO_X	3.31	0.138	lb/MMBtu
CO	6.61	0.5496	lb/MMBtu
SO_2	0.00	--	--
PM_{10}	0.08	7.60	lb/MMscf
$PM_{2.5}$	0.08	7.60	lb/MMscf
H_2S	0.00	--	--

Flare DRE	98.00	%
OVHD-MSS Flare Time	1.00	blowdown/hr
	2.00	hrs/day
	40.00	hrs/year

Footnotes:
[a] Uncontrolled stream properties determined via ProMax.
[b] Flare CO and NOx emission factors from TCEQ Air Permit Techincal Guidance for Chemical Sources. PM and PM2.5 emission factors from AP-42, Table 1.4-1 and 1.4-2, July 1998. SO2 emissions assume 100% conversion of H2S to SO2.

XTO Energy, Inc.
Cowboy CDP
DUAL TIP FLARE PILOT/PURGE GAS HOURLY EMISSIONS (COMBINED BETWEEN ALL FLARES)

DUAL TIP 20 MMSCFD FLARES - HOURLY (FL1 - FL3)

Maximum Hourly Emission Rates and Composition to Flare[a,b]

Component	Pilot Fuel (Per Flare)	L.P. Cryo Flare Header Purge Gas	H.P. Cryo Flare Header Purge Gas	L.P. Backup Flare Header Purge Gas	H.P. Backup Flare Header Purge Gas	L.P. Stab Flare Header Purge Gas	H.P. Stab Flare Header Purge Gas	Total	Destruction Efficiency	Exhaust Stream (controlled)
	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(%)	(lb/hr)
Water	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0%	**0.00**
Hydrogen Sulfide	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
Nitrogen	0.72	0.37	0.25	0.37	0.25	0.98	0.62	3.55	0%	**3.55**
Carbon Dioxide	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0%	**0.00**
Methane	16.84	19.66	12.88	19.66	12.88	51.26	32.54	165.72	98%	**3.31**
Ethane	6.09	7.69	5.04	7.69	5.04	20.06	12.73	64.35	98%	**1.29**
Propane	0.63	0.89	0.58	0.89	0.58	2.32	1.47	7.37	98%	**0.15**
Iso-butane	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
N-butane	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
Iso-pentane	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
N-pentane	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
Cyclopentanes	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
Other Hexanes	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
n-Hexane	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
Methylcyclopentane	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
Benzene	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
Cyclohexane	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
2,2,4 Trimethylpentane	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
Other Heptanes	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
Methylcyclohexane	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
n-Heptane	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
Toluene	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
Octanes	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
Ethylbenzene	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
M&P-Xylene	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
Nonanes	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
Decanes	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
Undecanes Plus	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
Total	**24.28**	**28.62**	**18.75**	**28.62**	**18.75**	**74.61**	**47.37**	**241.00**	--	**8.30**
Total VOC	**0.63**	**0.89**	**0.58**	**0.89**	**0.58**	**2.32**	**1.47**	**7.37**	--	**0.15**
Total HAP	**0.00**	**0.00**	**0.00**	**0.00**	**0.00**	**0.00**	**0.00**	**0.00**	--	**0.00**
Heating Value (Btu/scf)	1,019.29	1,040.21	1,040.21	1,040.21	1,040.21	1,040.21	1,040.21	**1,038.07**		
Molecular Weight	18.43	18.73	18.73	18.73	18.73	18.73	18.73	--		
SO2 Emissions (lb/hr)	0.00	0.00	0.00	0.00	0.00	0.00	0.00	**0.00**		
Volumetric Flow (scf/hr)[c]	500.00	580.00	380.00	580.00	380.00	1,512.00	960.00	**4,892.00**		
Heat Release (MMBtu/hr)	0.51	0.60	0.40	0.60	0.40	1.57	1.00	**5.08**		

Criteria Pollutant Emissions from Flare [b]

Component	Emission Rate	Emission Factor	Emission Factor Units
	(lb/hr)		
NO_X	0.70	0.138	lb/MMBtu
CO	1.40	0.2755	lb/MMBtu
SO_2	0.00	--	--
PM_{10}	0.04	7.60	lb/MMscf
$PM_{2.5}$	0.04	7.60	lb/MMscf
H_2S	0.00	--	--

Flare DRE	98.00	%

Footnotes:

[a] Uncontrolled stream properties determined via ProMax.

[b] Flare CO and NOx emission factors from TCEQ Air Permit Techincal Guidance for Chemical Sources. PM and PM2.5 emission factors from AP-42, Table 1.4-1 and 1.4-2, July 1998. SO2 emissions assume 100% conversion of H2S to SO2.

[c] Flare purge gas flowrates were estimated in Promax and were doubled for conservative estimates.

XTO Energy, Inc.
Cowboy CDP
DUAL TIP FLARE PILOT/PURGE GAS ANNUAL EMISSIONS (COMBINED BETWEEN ALL FLARES)

DUAL TIP 20 MMSCFD FLARES - ANNUAL (FL1 - FL3)

Annual Emission Rates and Composition to Flare[a,b]

Component	Pilot Fuel (Per Flare)	L.P. Cryo Flare Header Purge Gas	H.P. Cryo Flare Header Purge Gas	L.P. Backup Flare Header Purge Gas	H.P. Backup Flare Header Purge Gas	L.P. Stab Flare Header Purge Gas	H.P. Stab Flare Header Purge Gas	Total	Destruction Efficiency	Exhaust Stream (controlled)
	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(%)	(ton/yr)
Water	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0%	**0.00**
Hydrogen Sulfide	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
Nitrogen	3.14	1.64	1.08	1.64	1.08	4.28	2.72	15.56	0%	**15.56**
Carbon Dioxide	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0%	**0.00**
Methane	73.75	86.12	56.42	86.12	56.42	224.50	142.54	725.86	98%	**14.52**
Ethane	26.67	33.70	22.08	33.70	22.08	87.85	55.78	281.86	98%	**5.64**
Propane	2.77	3.90	2.55	3.90	2.55	10.16	6.45	32.28	98%	**0.65**
Iso-butane	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
N-butane	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
Iso-pentane	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
N-pentane	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
Cyclopentanes	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
Other Hexanes	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
n-Hexane	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
Methylcyclopentane	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
Benzene	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
Cyclohexane	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
2,2,4 Trimethylpentane	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
Other Heptanes	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
Methylcyclohexane	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
n-Heptane	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
Toluene	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
Octanes	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
Ethylbenzene	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
M&P-Xylene	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
Nonanes	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
Decanes	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
Undecanes Plus	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	**0.00**
Total	**106.33**	**125.35**	**82.13**	**125.35**	**82.13**	**326.79**	**207.48**	**1055.57**	**--**	**36.36**
Total VOC	**2.77**	**3.90**	**2.55**	**3.90**	**2.55**	**10.16**	**6.45**	**32.28**	**--**	**0.65**
Total HAP	**0.00**	**0.00**	**0.00**	**0.00**	**0.00**	**0.00**	**0.00**	**0.00**	**--**	**0.00**
Heating Value (Btu/scf)	1,019.29	1,040.21	1,040.21	1,040.21	1,040.21	1,040.21	1,040.21	**1,038.07**		
Molecular Weight	18.43	18.73	18.73	18.73	18.73	18.73	18.73	**--**		
SO2 Emissions (lb/hr)	0.00	0.00	0.00	0.00	0.00	0.00	0.00	**0.00**		
Volumetric Flow (scf/year)	4,380,000	5,080,800	3,328,800	5,080,800	3,328,800	13,245,120	8,409,600	**42,853,920**		
Heat Release (MMBtu/hr)	4,464.48	5,285.10	3,462.65	5,285.10	3,462.65	13,777.70	8,747.75	**44,485.43**		

Criteria Pollutant Emissions from Flare[b]

Component	Emission Rate	Emission Factor	Emission Factor Units
	ton/yr		
NO_X	3.07	0.138	lb/MMBtu
CO	6.13	0.5496	lb/MMBtu
SO_2	0.00	--	--
PM_{10}	0.16	7.60	lb/MMscf
$PM_{2.5}$	0.16	7.60	lb/MMscf
H_2S	0.00	--	--

Flare DRE	98.00	%

Footnotes:

[a] Uncontrolled stream properties determined via ProMax.

[b] Flare CO and NOx emission factors from TCEQ Air Permit Techincal Guidance for Chemical Sources. PM and PM2.5 emission factors from AP-42, Table 1.4-1 and 1.4-2, July 1998. SO2 emissions assume 100% conversion of H2S to SO2.

XTO Energy, Inc.

Cowboy CDP

PILOT/PURGE GAS COMBUSTION (FL1-FL3) - GHG EMISSIONS SUMMARY

Flare Emissions Summary Table - Normal Operations

1) $E_{a,CH4} = V_a * X_{CH4} * [(1- \eta)* Z_L + Z_U$ = **171.42** **SCF/Yr**

Va =	**42,853,920.00**
X_{CH4} =	**0.0002**
N =	**0.98**
Z_L =	**1.00**
Z_U =	**0.00**

2) $E_{a,CO2}$ (uncombusted) = $V_a * X_{CO2}$ = **21,426.96** **SCF/Yr**

Va =	**42,853,920.00**
X_{CO2} =	**0.000500**

Source	Annual Volume
FL1-FL3 Purge	42853920
	42853920.00

3) $E_{a,CO2}$ (combusted) = Σ (η * Va * Yj * Rj * Z_L)

N =	**0.98**				
V_a =	**42,853,920.00**		**Rj =**	**$E_{a, CO2}$ =**	
Y_J=	**Methane**	0.0002	1	8,399.37	
	Ethane	0.1464	2	12,296,675.22	
	Propane	0.6292	3	79,273,238.20	
	Butane	0.1584	4	26,609,198.84	
	Pentane +	0.0565	5	11,864,107.75	
Z_L =	**1.00**			**130,051,619.38**	**SCF/Yr**

3) $E_{s,n} = \frac{E_{a,n} * (459.67 + T_s) * P_a}{(459.67 + T_a) * P_s}$

$E_{a,n}$(CH4) =	171.42		=	**154.31**	**SCF/Yr**
$E_{a,n}$(CO2) =	130,073,046.34		=	**117,092,660.95**	**SCF/Yr**
Ts =	60º F				
Ta =	93.7º F	Roswell, AP-42			
Ps =	13.28				
Pa =	12.73	Roswell, AP-42			

4) $Mass_{s,i} = E_{s,i} * \rho_i * 10^3$

$E_{s,i}$ (CH4) =	154.31				
$E_{s,i}$ (CO2) =	117,092,660.95				
p_i (CH4) =	0.0192	kg/ft3	=	0.00	metric tons
p_i (CO2) =	0.0526	kg/ft3	=	6159.07	metric tons

5) $CO_2e = CO_2 + (CH_4 X GWP)$

			short tons	CO_2e
CO2 =	6159.07	=	6789.21	6789.21
CH4 =	0.00	=	0.00	0.08
CH4 GWP =	25			**6789.30**

XTO Energy, Inc.

Cowboy CDP

OVERHEAD GAS COMBUSTION (FL1-FL3OVHD-SSM) - GHG EMISSIONS SUMMARY

Flare Emissions Summary Table - Normal Operations

Source	Annual Volume
FL1-FL3 MSS	20000000
	20000000.00

1) $E_{a,CH4} = V_a * X_{CH4} * [(1-\eta)* Z_L + Z_U$ = **80.00** **SCF/Yr**

Va = **20,000,000.00**

X_{CH4} = **0.0002**

N = **0.98**

Z_L = **1.00**

Z_U = **0.00**

2) $E_{a,CO2}$ (uncombusted) = $V_a * X_{CO2}$ = **10,000.00** **SCF/Yr**

Va = **20,000,000.00**

X_{CO2} = **0.000500**

3) $E_{a,CO2}$ (combusted) = $\Sigma (\eta * Va * Yj * Rj * Z_L)$

N = **0.98**

			Rj =	$E_{a, CO2}$ =	
V_a =	**20,000,000.00**				
Y_J=	**Methane**	0.0002	1	3,920.00	
	Ethane	0.1464	2	5,738,880.00	
	Propane	0.6292	3	36,996,960.00	
	Butane	0.1584	4	12,418,560.00	
	Pentane +	0.0565	5	5,537,000.00	
Z_L =	**1.00**			**60,695,320.00**	**SCF/Yr**

3) $E_{s,n} = \frac{E_{a,n} * (459.67 + T_s) * P_a}{(459.67 + T_a) * P_s}$

$E_{a,n}$(CH4) =	80.00		=	**72.02**	**SCF/Yr**
$E_{a,n}$(CO2) =	60,705,320.00		=	**54,647,351.26**	**SCF/Yr**
Ts =	60° F				
Ta =	93.7° F	Roswell, AP-42			
Ps =	13.28				
Pa =	12.73	Roswell, AP-42			

4) $Mass_{s,i} = E_{s,i} * \rho_i * 10^3$

$E_{s,i}$ (CH4) =	72.02				
$E_{s,i}$ (CO2) =	54,647,351.26				
p_i (CH4) =	0.0192	kg/ft3	=	0.00	metric tons
p_i (CO2) =	0.0526	kg/ft3	=	2874.45	metric tons

5) $CO_2e = CO_2 + (CH_4 \text{ X GWP})$

			short tons	CO_2e
CO2 =	2874.45	=	3168.54	3168.54
CH4 =	0.00	=	0.00	0.04
CH4 GWP =	25			**3168.58**

XTO Energy, Inc.

Cowboy CDP

CRYO GAS COMBUSTION (FL1-FL3CRYO-MSS) - GHG EMISSIONS SUMMARY

Flare Emissions Summary Table - Normal Operations

Source	Annual Volume
FL1-FL3 MSS	80000000
	80000000.00

1) $E_{a,CH4} = V_a * X_{CH4} * [(1-\eta)* Z_L + Z_U$ = **1,176,260.24** **SCF/Yr**

Va =	**80,000,000.00**
X_{CH4} =	**0.7352**
N =	**0.98**
Z_L =	**1.00**
Z_U =	**0.00**

2) $E_{a,CO2}$ (uncombusted) = $V_a * X_{CO2}$ = **90,399.10** **SCF/Yr**

Va =	**80,000,000.00**
X_{CO2} =	**0.001130**

3) $E_{a,CO2}$ (combusted) = Σ (η * Va * Yj * Rj * Z_L)

N =	**0.98**				
V_a =	**80,000,000.00**		**Rj =**	**$E_{a,CO2}$ =**	
Y_j=	**Methane**	0.7352	1	57,636,751.63	
	Ethane	0.1472	2	23,080,729.19	
	Propane	0.0722	3	16,971,862.28	
	Butane	0.0145	4	4,540,882.59	
	Pentane +	0.0048	5	1,885,501.14	
Z_L =	**1.00**			**104,115,726.84**	**SCF/Yr**

3) $E_{s,n} = \frac{E_{a,n} * (459.67 + T_s) * P_a}{(459.67 + T_a) * P_s}$

$E_{a,n}$(CH4) =	1,176,260.24		=	**1,058,877.65**	**SCF/Yr**
$E_{a,n}$(CO2) =	104,206,125.94		=	**93,807,079.31**	**SCF/Yr**
Ts =	60° F				
Ta =	93.7° F	Roswell, AP-42			
Ps =	13.28				
Pa =	12.73	Roswell, AP-42			

4) $Mass_{s,i} = E_{s,i} * \rho_i * 10^3$

$E_{s,i}$ (CH4) =	1,058,877.65				
$E_{s,i}$ (CO2) =	93,807,079.31				
ρ_i (CH4) =	0.0192	kg/ft3	=	20.33	metric tons
ρ_i (CO2) =	0.0526	kg/ft3	=	4934.25	metric tons

5) $CO_2e = CO_2 + (CH_4 \text{ X GWP})$

			short tons	CO_2e
CO2 =	4934.25	=	5439.08	5439.08
CH4 =	20.33	=	22.41	560.26
CH4 GWP =	25			**5999.34**

XTO Energy, Inc.

Cowboy CDP

STORAGE TANK EMISSIONS SUMMARY - UNCONTROLLED

TOTAL EMISSIONS SUMMARY

						VOC Working & Breathing Loss		VOC Flash Losses		VOC Total Emissions	
FIN	**Unit Description**	**Tank Controlled (Yes/No)**	**Control Type**	**Material Throughput (bbls/day)**	**Material Type**	**Lb/hr**	**TPY**	**Lb/hr**	**TPY**	**Lb/hr**	**TPY**
IFR1, IFR2, IFR3, IFR4[1]	**IFR Condensate Storage Tanks**	Yes	Internal Floating Roof	200,000	Condensate	3.90	17.09	---	---	3.90	17.09
IFR5, IFR6, IFR7, IFR8[1]	**IFR Condensate Storage Tanks**	Yes	Internal Floating Roof	400,000	Condensate	10.37	45.42	---	---	10.37	45.42
GBS1	**Gun Barrel Separator**	Yes	Combustor	4,195	Produced Water	0.02	0.09	15.78	69.12	15.80	69.21
PWTK1	**Produced Water Tank**	Yes	Combustor	2,098	Produced Water	1.81	7.91	0.88	3.84	2.68	11.75
PWTK2	**Produced Water Tank**	Yes	Combustor	2,098	Produced Water	1.81	7.91	0.88	3.84	2.68	11.75
SOTK1	**Slop Tank**	Yes	Combustor	16	Condensate	0.66	2.91	57.04	249.82	57.70	252.73
Storage Tank Emissions						18.57	81.33	74.57	326.61	93.14	407.94

[1]Throughput and emissions are grouped together for IFR1-4 and IFR 5-8 respectively.

XTO ENERGY INC.
Cowboy CDP
IFR 1-4 TANKS EMISSIONS SUMMARY

IFR 1-4 TANK EMISSIONS

50,000 BBL Internal Floating Roof Storage Tank Emissions (per tank)[a]		
Component	W&B Losses	
	(lb/hr)	(ton/yr)
Water	0.00	0.02
Hydrogen Sulfide	0.00	0.00
Nitrogen	0.00	0.00
Carbon Dioxide	0.00	0.00
Methane	0.00	0.00
Ethane	0.08	0.36
Propane	0.17	0.73
Iso-butane	0.08	0.37
N-butane	0.23	1.02
Iso-pentane	0.08	0.33
N-pentane	0.08	0.37
Cyclopentanes	0.00	0.00
Other Hexanes	0.03	0.15
n-Hexane	0.02	0.09
Methylcyclopentane	0.02	0.07
Benzene	0.01	0.06
Cyclohexane	0.03	0.11
2,2,4 Trimethylpentane	0.00	0.00
Other Heptanes	0.01	0.04
Methylcyclohexane	0.02	0.09
n-Heptane	0.01	0.06
Toluene	0.01	0.04
Octanes	0.02	0.07
Ethylbenzene	0.00	0.00
M&P-Xylene	0.00	0.02
Nonanes	0.01	0.06
Decanes	0.01	0.06
Undecanes Plus	0.12	0.54
Total	**1.06**	**4.65**
Total VOC	**0.98**	**4.27**
Total HAP	**0.05**	**0.21**

IFR 1-4 Tank Information		
Number of Tanks	4	--
Tank Size	50,000	BBL
Control Device	IFR	--
Total Condensate Throughput IFR1-4	200,000	BBL/Day

Footnotes:

[a] Uncontrolled stream properties determined via ProMax.

XTO ENERGY INC.
Cowboy CDP
IFR 5-8 TANKS EMISSION SUMMARY

IFR 5-8 TANK EMISSIONS

250,000 BBL Internal Floating Roof Storage Tank Emissions (per tank)[a]

Component	W&B Losses (lb/hr)	W&B Losses (ton/yr)
Water	0.01	0.05
Hydrogen Sulfide	0.00	0.00
Nitrogen	0.00	0.00
Carbon Dioxide	0.00	0.01
Methane	0.00	0.00
Ethane	0.25	1.11
Propane	0.51	2.24
Iso-butane	0.26	1.13
N-butane	0.71	3.11
Iso-pentane	0.23	1.00
N-pentane	0.25	1.09
Cyclopentanes	0.00	0.00
Other Hexanes	0.10	0.43
n-Hexane	0.06	0.24
Methylcyclopentane	0.04	0.18
Benzene	0.03	0.15
Cyclohexane	0.07	0.30
2,2,4 Trimethylpentane	0.00	0.00
Other Heptanes	0.02	0.10
Methylcyclohexane	0.05	0.21
n-Heptane	0.03	0.14
Toluene	0.02	0.10
Octanes	0.03	0.13
Ethylbenzene	0.00	0.00
M&P-Xylene	0.01	0.03
Nonanes	0.02	0.08
Decanes	0.02	0.07
Undecanes Plus	0.14	0.60
Total	**2.86**	**12.53**
Total VOC	**2.59**	**11.36**
Total HAP	**0.12**	**0.53**

IFR 5-8 Tank Information

Number of Tanks	4	--
Tank Size	250,000	BBL
Control Device	IFR	--
Total Condensate Throughput IFR5-8	400,000	BBL/Day

Footnotes:

[a] Uncontrolled stream properties determined via ProMax.

XTO ENERGY INC.
Cowboy CDP
COMBUSTOR HOURLY EMISSIONS

COMBUSTOR - HOURLY (EPN: ECD1)

Maximum Hourly Emission Rates and Composition to Combustor[a,b]

Component	Pilot Fuel[c]	Slop Oil Tank (OTK7)		Gunbarrel (GBS1)		PW Tanks (53-54)		Slop Oil Truck Loading (SOTL)	Total	Destruction Efficiency	Flare Exhaust (controlled)
		W&B Losses	Flashing Losses	W&B Losses	Flashing Losses	W&B Losses	Flashing Losses				
	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(%)	(lb/hr)
Water	0.00	0.00	0.02	1.98	0.29	1.68	0.03	0.00	3.99	0%	**3.99**
Hydrogen Sulfide	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	99%	**0.00**
Nitrogen	0.72	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.72	99%	**0.01**
Carbon Dioxide	0.00	0.00	0.02	0.04	0.17	0.72	0.02	0.02	0.99	0%	**0.99**
Methane	16.84	0.00	0.09	0.00	0.02	0.00	0.00	0.03	16.97	99%	**0.17**
Ethane	6.09	0.03	1.67	0.00	0.33	0.10	0.04	1.92	10.18	99%	**0.10**
Propane	0.63	0.23	18.71	0.01	4.12	0.91	0.46	17.21	42.28	99%	**0.42**
Iso-butane	0.00	0.07	6.22	0.00	1.58	0.22	0.18	5.13	13.40	99%	**0.13**
N-butane	0.00	0.18	15.77	0.00	4.10	0.83	0.46	13.43	34.75	99%	**0.35**
Iso-pentane	0.00	0.05	4.51	0.00	1.45	0.20	0.16	4.04	10.40	99%	**0.10**
N-pentane	0.00	0.06	4.79	0.00	1.69	0.10	0.19	4.35	11.17	99%	**0.11**
Cyclopentanes	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	99%	**0.00**
Other Hexanes	0.00	0.02	1.74	0.00	0.71	0.06	0.08	1.72	4.33	99%	**0.04**
n-Hexane	0.00	0.01	0.97	0.00	0.43	0.02	0.05	1.00	2.47	99%	**0.02**
Methylcyclopentane	0.00	0.01	0.74	0.00	0.31	0.09	0.03	0.69	1.87	99%	**0.02**
Benzene	0.00	0.00	0.48	0.00	0.04	0.24	0.00	0.31	1.08	99%	**0.01**
Cyclohexane	0.00	0.01	1.13	0.00	0.46	0.32	0.05	1.01	2.99	99%	**0.03**
2,2,4 Trimethylpentane	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	99%	**0.00**
Other Heptanes	0.00	0.00	0.36	0.00	0.17	0.01	0.02	0.35	0.92	99%	**0.01**
Methylcyclohexane	0.00	0.01	0.62	0.00	0.30	0.09	0.03	0.64	1.70	99%	**0.02**
n-Heptane	0.00	0.01	0.40	0.00	0.20	0.01	0.02	0.39	1.02	99%	**0.01**
Toluene	0.00	0.00	0.26	0.00	0.06	0.38	0.01	0.18	0.88	99%	**0.01**
Octanes	0.00	0.00	0.21	0.00	0.11	0.00	0.01	0.18	0.53	99%	**0.01**
Ethylbenzene	0.00	0.00	0.00	0.00	0.00	0.01	0.00	0.00	0.02	99%	**0.00**
M&P-Xylene	0.00	0.00	0.05	0.00	0.02	0.14	0.00	0.03	0.25	99%	**0.00**
Nonanes	0.00	0.00	0.05	0.00	0.03	0.00	0.00	0.04	0.11	99%	**0.00**
Decanes	0.00	0.00	0.01	0.00	0.01	0.00	0.00	0.01	0.03	99%	**0.00**
Undecanes Plus	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	99%	**0.00**
Total	**24.28**	**0.69**	**58.83**	**2.04**	**16.59**	**6.12**	**1.84**	**52.65**	**163.04**	**--**	**6.56**
Total VOC	**0.63**	**0.66**	**57.04**	**0.02**	**15.78**	**3.61**	**1.75**	**50.69**	**130.19**	**--**	**1.30**
Total HAP	**0.00**	**0.02**	**1.76**	**0.00**	**0.54**	**0.79**	**0.06**	**1.52**	**4.70**	**--**	**0.05**
Heating Value (Btu/scf)	1,019.29	3,061.07	3,072.55	62.16	3,026.17	1,204.88	3,026.17	3,061.07	**2,564.07**		
Molecular Weight	18.43	54.55	54.81	18.36	55.60	35.69	55.60	57.26	**--**		
SO2 Emissions (lb/hr)	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	**0.00**		
Volumetric Flow (scf/hr)	180.00	4.80	407.36	42.18	113.20	65.12	12.58	411.39	**1,236.64**		
Heat Release (MMBtu/hr)	0.18	0.01	1.25	0.00	0.34	0.08	0.04	1.26	**3.17**		

Criteria Pollutant Emissions from ECD [b]

Component	Emission Rate (lb/hr)	Emission Factor	Emission Factor Units
NO_X	0.44	0.138	lb/MMBtu
CO	0.87	0.2755	lb/MMBtu
SO_2	0.00	--	--
PM_{10}	0.02	7.60	lb/MMscf
$PM_{2.5}$	0.02	7.60	lb/MMscf
H_2S	0.00	--	--

Combustor DRE	99.00	%

Criteria Pollutant Emissions from Pilot Fuel

Component	Emission Rate (lb/hr)	Emission Factor	Emission Factor Units
NO_X	0.03	0.138	lb/MMBtu
CO	0.05	0.2755	lb/MMBtu
SO_2	0.00	--	--
PM_{10}	0.001	7.60	lb/MMscf
$PM_{2.5}$	0.001	7.60	lb/MMscf
H_2S	0.00	--	--

Footnotes:

[a] Uncontrolled stream properties determined via ProMax.

[b] Flare CO and NOx emission factors from TCEQ Air Permit Techincal Guidance for Chemical Sources. PM and PM2.5 emission factors from AP-42, Table 1.4-1 and 1.4-2, July 1998. SO2 emissions assume 100% conversion of H2S to SO2.

XTO Energy, Inc.
Cowboy CDP
COMBUSTOR ANNUAL EMISSIONS

COMBUSTOR - ANNUAL (EPN: ECD1)

Annual Emission Rates and Composition to Combustor[a,b]

Component	Pilot Fuel[c]	Slop Oil Tank (OTK7)		Gunbarrel (GBS1)		PW Tanks (53-54)		Slop Oil Truck Loading (SOTL)	Total	Destruction Efficiency	Exhaust Stream (controlled)
		W&B Losses	Flashing Losses	W&B Losses	Flashing Losses	W&B Losses	Flashing Losses				
	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(%)	(ton/yr)
Water	0.00	0.00	0.07	8.66	1.26	7.36	0.14	0.00	17.50	0%	**17.50**
Hydrogen Sulfide	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	99%	**0.00**
Nitrogen	3.14	0.00	0.00	0.00	0.01	0.00	0.00	0.00	3.15	99%	**0.03**
Carbon Dioxide	0.00	0.00	0.08	0.17	0.75	3.17	0.08	0.00	4.27	0%	**4.27**
Methane	73.75	0.00	0.38	0.00	0.08	0.02	0.01	0.00	74.23	99%	**0.74**
Ethane	26.67	0.11	7.33	0.02	1.43	0.45	0.16	0.03	36.20	99%	**0.36**
Propane	2.77	0.99	81.96	0.05	18.04	3.97	2.00	0.23	110.01	99%	**1.10**
Iso-butane	0.00	0.29	27.26	0.01	6.93	0.98	0.77	0.07	36.31	99%	**0.36**
N-butane	0.00	0.77	69.07	0.02	17.94	3.62	1.99	0.18	93.60	99%	**0.94**
Iso-pentane	0.00	0.23	19.74	0.00	6.35	0.85	0.71	0.05	27.94	99%	**0.28**
N-pentane	0.00	0.25	20.99	0.00	7.39	0.45	0.82	0.06	29.96	99%	**0.30**
Cyclopentanes	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	99%	**0.00**
Other Hexanes	0.00	0.10	7.63	0.00	3.11	0.24	0.35	0.02	11.46	99%	**0.11**
n-Hexane	0.00	0.06	4.26	0.00	1.86	0.07	0.21	0.01	6.48	99%	**0.06**
Methylcyclopentane	0.00	0.04	3.24	0.00	1.34	0.41	0.15	0.01	5.18	99%	**0.05**
Benzene	0.00	0.02	2.08	0.00	0.17	1.07	0.02	0.00	3.36	99%	**0.03**
Cyclohexane	0.00	0.06	4.96	0.00	2.03	1.38	0.23	0.01	8.67	99%	**0.09**
2,2,4 Trimethylpentane	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	99%	**0.00**
Other Heptanes	0.00	0.02	1.60	0.00	0.76	0.04	0.08	0.00	2.50	99%	**0.03**
Methylcyclohexane	0.00	0.04	2.73	0.00	1.33	0.38	0.15	0.01	4.63	99%	**0.05**
n-Heptane	0.00	0.02	1.76	0.00	0.87	0.02	0.10	0.01	2.78	99%	**0.03**
Toluene	0.00	0.01	1.12	0.00	0.25	1.65	0.03	0.00	3.07	99%	**0.03**
Octanes	0.00	0.01	0.92	0.00	0.50	0.01	0.06	0.00	1.50	99%	**0.01**
Ethylbenzene	0.00	0.00	0.02	0.00	0.01	0.05	0.00	0.00	0.09	99%	**0.00**
M&P-Xylene	0.00	0.00	0.21	0.00	0.09	0.62	0.01	0.00	0.94	99%	**0.01**
Nonanes	0.00	0.00	0.21	0.00	0.12	0.00	0.01	0.00	0.35	99%	**0.00**
Decanes	0.00	0.00	0.05	0.00	0.03	0.00	0.00	0.00	0.08	99%	**0.00**
Undecanes Plus	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	99%	**0.00**
Total	**106.33**	**3.02**	**257.68**	**8.94**	**72.65**	**26.82**	**8.07**	**0.72**	**484.24**	**--**	**26.39**
Total VOC	**2.77**	**2.91**	**249.82**	**0.09**	**69.12**	**15.81**	**7.68**	**0.69**	**348.89**	**--**	**3.49**
Total HAP	**0.00**	**0.09**	**7.70**	**0.00**	**2.39**	**3.46**	**0.27**	**0.02**	**13.92**	**--**	**0.14**
Heating Value (Btu/scf)	1,019.29	3,061.07	3,072.55	62.16	3,026.17	1,204.88	3,026.17	3,061.07	**2317.46**		
Molecular Weight	18.43	54.55	54.81	18.36	55.60	35.69	55.60	57.26	**--**		
SO2 Emissions (tpy)	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	**0.00**		
Volumetric Flow (scf/yr)	1,576,800.0	42,081.7	3,568,481.4	369,526.7	991,646.9	570,418.0	110,183.0	11,175.1	**7,240,312.79**		
Heat Release (MMBtu/yr)	1,607.21	128.81	10,964.34	22.97	3,000.90	687.29	333.43	34.21	**16,779.17**		

Criteria Pollutant Emissions from ECD[b]

Component	Emission Rate	Emission Factor	Emission Factor Units
	(ton/yr)		
NO_X	1.16	0.138	lb/MMBtu
CO	2.31	0.2755	lb/MMBtu
SO_2	0.00	--	--
PM_{10}	0.03	7.60	lb/MMscf
$PM_{2.5}$	0.03	7.60	lb/MMscf
H_2S	0.00	--	--

Combustor DRE	99.00	%

Footnotes:

[a] Uncontrolled stream properties determined via ProMax.

[b] Flare CO and NOx emission factors from TCEQ Air Permit Techincal Guidance for Chemical Sources. PM and PM2.5 emission factors from AP-42, Table 1.4-1 and 1.4-2, July 1998. SO2 emissions assume 100% conversion of H2S to SO2.

XTO Energy, Inc.

Cowboy CDP

COMBUSTOR (ECD1) GHG EMISSIONS SUMMARY

Flare Emissions Summary Table - Normal Operations

Source	Annual Volume
ECD1	7240313
	7240312.79

1) $E_{a,CH4} = V_a * X_{CH4} * [(1- \eta)* Z_L + Z_U$ = **117.74** **SCF/Yr**

Va = **7,240,312.79**
X_{CH4} = **0.0016**
N = **0.99**
Z_L = **1.00**
Z_U = **0.00**

2) $E_{a,CO2}$ (uncombusted) = $V_a * X_{CO2}$ = **36.00** **SCF/Yr**

Va = **7,240,312.79**
X_{CO2} = **0.000005**

3) $E_{a,CO2}$ (combusted) = $\Sigma (\eta * Va * Yj * Rj * Z_L)$

			Rj =	$E_{a, CO2}$ =	
N =	**0.99**				
V_a =	**7,240,312.79**				
Y_j=	**Methane**	0.0016	1	11,656.01	
	Ethane	0.0661	2	947,571.22	
	Propane	0.4045	3	8,697,207.64	
	Butane	0.3307	4	9,482,057.09	
	Pentane +	0.0000	5	422.24	
Z_L =	**1.00**			**19,138,914.21**	**SCF/Yr**

3) $E_{s,n} = \frac{E_{a,n} * (459.67 + T_s) * P_a}{(459.67 + T_a) * P_s}$

$E_{a,n}$(CH4) =	117.74		=	**105.99**	**SCF/Yr**
$E_{a,n}$(CO2) =	19,138,950.20		=	**17,229,016.08**	**SCF/Yr**
Ts =	60º F				
Ta =	93.7º F	Roswell, AP-42			
Ps =	13.28				
Pa =	12.73	Roswell, AP-42			

4) $Mass_{s,i} = E_{s,i} * \rho_i * 10^3$

$E_{s,i}$ (CH4) =	105.99				
$E_{s,i}$ (CO2) =	17,229,016.08				
p_i (CH4) =	0.0192	kg/ft3	=	0.00	metric tons
p_i (CO2) =	0.0526	kg/ft3	=	906.25	metric tons

5) $CO_2e = CO_2 + (CH_4 \text{ X } GWP)$

			short tons	CO_2e
CO2 =	906.25	=	998.97	998.97
CH4 =	0.00	=	0.00	0.06
CH4 GWP =	25			**999.02**

XTO ENERGY INC.
Cowboy CDP
THERMAL OXIDIZER HOURLY EMISSIONS (PER UNIT)

THERMAL OXIDIZERS - HOURLY (EPNS: TO1-TO4)

Maximum Hourly Emission Rates and Composition to Thermal Oxidizer[a,b]

Component	TO Assist Fuel (lb/hr)	Amine Flash Gas (lb/hr)	Amine Reboiler Still Vent (lb/hr)	Total (lb/hr)	Destruction Efficiency (%)	Exhaust Stream (controlled) (lb/hr)
Hydrogen Sulfide	0.00	0.00	0.47	0.47	99%	**0.00**
N2	30.36	2.12	0.03	32.51	0%	**32.51**
Carbon Dioxide	0.00	72.79	24180.07	24252.86	0%	**24252.86**
Methane	796.63	129.51	5.37	931.51	99%	**9.32**
Ethane	311.74	56.10	3.72	371.56	99%	**3.72**
Propane	36.05	27.90	1.52	65.47	99%	**0.65**
i-Butane	0.00	2.41	0.10	2.51	99%	**0.03**
n-Butane	0.00	8.18	0.49	8.67	99%	**0.09**
i-Pentane	0.00	0.75	0.03	0.78	99%	**0.01**
n-Pentane	0.00	0.90	0.04	0.94	99%	**0.01**
n-Hexane	0.00	0.35	0.01	0.36	99%	**0.00**
Benzene	0.00	0.35	0.01	0.36	99%	**0.00**
Toluene	0.00	0.35	0.01	0.36	99%	**0.00**
Ethylbenzene	0.00	0.35	0.01	0.36	99%	**0.00**
Xylene	0.00	0.35	0.01	0.36	99%	**0.00**
Water	0.00	8.21	700.92	709.13	99%	**7.09**
MDEA	0.00	0.00	0.00	0.00	99%	**0.00**
Piperazine	0.00	0.00	0.00	0.00	99%	**0.00**
O2	0.00	0.00	0.00	0.00	99%	**0.00**
Total	**1174.78**	**310.62**	**24892.81**	**26378.21**	**--**	**24306.30**
Total VOC	**36.05**	**41.88**	**2.24**	**80.16**	**--**	**0.79**
Total HAP	**0.00**	**1.74**	**0.06**	**1.80**	**--**	**0.02**
Heating Value (Btu/scf)	1,030.84	962.33	1.07	**115.92**		
Molecular Weight	18.97	23.85	26.00	**--**		
SO2 Emissions (lb/hr)	0.00	0.00	0.88	**0.88**		
Volumetric Flow (scf/hr)	23,500.00	4,920.46	223,460.74	**251,881.20**		
Heat Release (MMBtu/hr)	24.22	4.74	0.24	**29.20**		

Criteria Pollutant Emissions from TO [b]

Component	Emission Rate (lb/hr)	Emission Factor	Emission Factor Units
NO_X	3.56	--	--
CO	2.17	--	--
SO_2	0.88	--	--
PM_{10}	0.22	7.60	lb/MMscf
$PM_{2.5}$	0.22	7.60	lb/MMscf
H_2S	0.00	--	--
CO2e	24485.74	--	--
Thermal Oxidizer DRE		99.00	%

Criteria Pollutant Emissions from Assist Gas

Component	Emission Rate (lb/hr)	Emission Factor	Emission Factor Units
NO_X	0.33	0.068	lb/MMBtu
CO	0.20	--	--
SO_2	0.00	--	--
PM_{10}	0.18	7.60	lb/MMscf
$PM_{2.5}$	0.18	7.60	lb/MMscf
H_2S	0.00	--	--

Calculation Factors:

NO2 MW	46.0100	lb/lb-mole
CO MW	28.0000	lb/lb-mole
CO2 MW	44.0100	lb/lb-mole
H2O MW	18.0150	lb/lb-mole
N2 MW	28.0134	lb/lb-mole
SO2 MW	64.0660	lb/lb-mole
O2 MW	31.9980	lb/lb-mole

Total lb-Mol/hr 1547.26 Zeeco Specifications

PV=nRT

T =	1700	F	Normal Operating Temp
	50,226	lb/hr	Max Design Flowrate
n =	1,547	lbmol/hr	Max Design Flowrate
P =	12.73	psia	Roswell Atmospheric Pressure
R =	10.73	psi·ft3·lbmol/°R	Gas Constant
V =	2,817,002	ft3/hr	
	782.5	ft3/sec	

Velocity = Flow Rate/Area

Flow rate =	783	ft3/sec
Inside Diameter =	4.1	feet
Area =	13.4	ft2
Velocity =	58.6	ft/sec

Manufacturer's Guaranteed Outlet Concentration

Pollutant	(ppmv)
NOx	50
CO	50

Notes:

[a] Uncontrolled stream properties determined via ProMax.

[b] TO and NOx CO exhuast emissions gaurantee provided by ZEECO. PM and PM2.5 emission factors from AP-42, Table 1.4-1 and 1.4-2, July 1998. SO2 emissions assume 100% conversion of H2S to SO2.

XTO Energy, Inc.
Cowboy CDP
THERMAL OXIDIZER ANNUAL EMISSIONS (PER UNIT)

THERMAL OXIDIZER - ANNUAL (EPNS: TO1-TO4)

Annual Emission Rates and Composition to Thermal Oxidizer[a,b]

Component	TO Assist Fuel (ton/yr)	Amine Flash Gas (ton/yr)	Amine Reboiler Still Vent (ton/yr)	Total (ton/yr)	Destruction Efficiency (%)	Exhaust Stream (controlled) (ton/yr)
Hydrogen Sulfide	0.00	0.01	2.04	2.06	99%	**0.02**
N2	132.98	9.28	0.13	142.40	0%	**142.40**
Carbon Dioxide	0.00	318.82	105908.71	106227.53	0%	**106227.53**
Methane	3489.23	567.26	23.52	4080.00	99%	**40.80**
Ethane	1365.42	245.73	16.29	1627.45	99%	**16.27**
Propane	157.89	122.22	6.66	286.78	99%	**2.87**
i-Butane	0.00	10.56	0.42	10.98	99%	**0.11**
n-Butane	0.00	35.82	2.16	37.98	99%	**0.38**
i-Pentane	0.00	3.28	0.12	3.40	99%	**0.03**
n-Pentane	0.00	3.93	0.18	4.10	99%	**0.04**
n-Hexane	0.00	1.52	0.05	1.57	99%	**0.02**
Benzene	0.00	1.52	0.05	1.57	99%	**0.02**
Toluene	0.00	1.52	0.05	1.57	99%	**0.02**
Ethylbenzene	0.00	1.52	0.05	1.57	99%	**0.02**
Xylene	0.00	1.52	0.05	1.57	99%	**0.02**
Water	0.00	35.96	3070.02	3105.98	99%	**31.06**
MDEA	0.00	0.01	0.00	0.01	99%	**0.00**
Piperazine	0.00	0.00	0.00	0.00	99%	**0.00**
O2	0.00	0.00	0.00	0.00	99%	**0.00**
Total	**5145.52**	**1360.50**	**109030.53**	**115536.54**	**--**	**106461.60**
Total VOC	**157.89**	**183.42**	**9.80**	**351.11**	**--**	**3.51**
Total HAP	**0.00**	**7.61**	**0.26**	**7.87**	**--**	**0.08**
Heating Value (Btu/scf)	1,050.86	962.33	1.07	**117.79**		
Molecular Weight	16.81	23.85	26.00	**--**		
SO2 Emissions (tpy)	0.00	0.02	3.84	**3.87**		
Volumetric Flow (scf/yr)	205,860,000.0	43,103,237.4	1,957,516,073.9	**2,206,479,311.31**		
Heat Release (MMBtu/yr)	216,330.04	41,479.64	2,084.99	**259,894.68**		

Criteria Pollutant Emissions from TO [b]

Component	Emission Rate (ton/yr)	Emission Factor	Emission Factor Units
NO_X	15.59	--	lb/MMBtu
CO	9.49	--	--
SO_2	3.87	--	--
PM_{10}	0.95	7.60	lb/MMscf
$PM_{2.5}$	0.95	7.60	lb/MMscf
H_2S	0.02	--	--
CO2e	107247.53	--	--

Thermal Oxidizer DRE	99.00	%

Calculation Factors:

NO2 MW	46.0100	lb/lb-mole
CO MW	28.0000	lb/lb-mole

Manufacturers Guaranteed Outlet Concentration

Pollutant	(ppmv)
NOx	50
CO	50

Footnotes:

[a] Uncontrolled stream properties determined via ProMax.

[b] TO CO and NOx exhuast emissions gaurantee provided by ZEECO. PM and PM2.5 emission factors from AP-42, Table 1.4-1 and 1.4-2, July 1998. SO2 emissions assume 100% conversion of H2S to SO2.

XTO Energy, Inc.
Cowboy CDP
FUGITIVE EMISSIONS - VOCs

Uncontrolled VOC Emissions

Component Type	Service	Control (%)[1]	Estimated Components Count	Hours	Factors	Total VOC Weight %[2]	VOC Emissions lb/hour	VOC Emissions lb/year	VOC Emissions tons/year
Valves	Gas/Vapor		5699	8760	0.009920	22.92%	12.96	113511.25	56.76
	Light Oil		2442	8760	0.005500	99.95%	13.42	117592.96	58.80
	Heavy Oil		200	8760	0.000019	99.95%	0.00	33.27	0.02
	Water/Light Oil		0	8760	0.000216	99.95%	0.00	0.00	0.00
Pump Seals	Gas/Vapor		0	8760	0.005290	22.92%	0.00	0.00	0.00
	Light Oil		40	8760	0.028660	99.95%	1.15	10037.12	5.02
	Heavy Oil		0	8760	0.001130	99.95%	0.00	0.00	0.00
	Water/Light Oil		0	8760	0.000053	99.95%	0.00	0.00	0.00
Connectors	Gas/Vapor		17097	8760	0.000440	22.92%	1.72	15104.32	7.55
	Light Oil		7326	8760	0.000463	99.95%	3.39	29697.57	14.85
	Heavy Oil		0	8760	0.000017	99.95%	0.00	0.00	0.00
	Water/Light Oil		1400	8760	0.000243	99.95%	0.34	2978.57	1.49
Flanges	Gas/Vapor		1500	8760	0.000860	22.92%	0.30	2590.11	1.30
	Light Oil		1500	8760	0.000243	99.95%	0.36	3191.32	1.60
	Heavy Oil		0	8760	0.000001	99.95%	0.00	0.00	0.00
	Water/Light Oil		0	8760	0.000006	99.95%	0.00	0.00	0.00
Open-ended Lines	Gas/Vapor		0	8760	0.004410	22.92%	0.00	0.00	0.00
	Light Oil		0	8760	0.003090	99.95%	0.00	0.00	0.00
	Heavy Oil		0	8760	0.000309	99.95%	0.00	0.00	0.00
	Water/Light Oil		0	8760	0.000550	99.95%	0.00	0.00	0.00
Other:	Gas/Vapor		40	8760	0.019400	22.92%	0.18	1558.08	0.78
	Light Oil		0	8760	0.016500	99.95%	0.00	0.00	0.00
	Heavy Oil		0	8760	0.000068	99.95%	0.00	0.00	0.00
	Water/Light Oil		0	8760	0.030900	99.95%	0.00	0.00	0.00

Emission Component	lb/hr	lb/year	TPY
Uncontrolled VOC Emissions	33.82	296294.58	148.15

Controlled VOC Emissions

Component Type	Service	Control (%)[1]	Estimated Components Count	Hours	Factors	Total VOC Weight %[2]	VOC Emissions lb/hour	VOC Emissions lb/year	VOC Emissions tons/year
Valves	Gas/Vapor	67%	5699	8760	0.009920	22.92%	4.28	37,459	18.73
	Light Oil	61%	2442	8760	0.005500	99.95%	5.24	45,861	22.93
	Heavy Oil		200	8760	0.000019	99.95%	0.00	33	0.02
	Water/Light Oil		0	8760	0.000216	99.95%	0.00	0	0.00
Pump Seals	Gas/Vapor		0	8760	0.005290	22.92%	0.00	0	0.00
	Light Oil	45%	40	8760	0.028660	99.95%	0.63	5,520	2.76
	Heavy Oil		0	8760	0.001130	99.95%	0.00	0	0.00
	Water/Light Oil		0	8760	0.000053	99.95%	0.00	0	0.00
Connectors	Gas/Vapor		17097	8760	0.000440	22.92%	1.72	15,104	7.55
	Light Oil		7326	8760	0.000463	99.95%	3.39	29,698	14.85
	Heavy Oil		0	8760	0.000017	99.95%	0.00	0	0.00
	Water/Light Oil		1400	8760	0.000243	99.95%	0.34	2,979	1.49
Flanges	Gas/Vapor		1500	8760	0.000860	22.92%	0.30	2,590	1.30
	Light Oil		1500	8760	0.000243	99.95%	0.36	3,191	1.60
	Heavy Oil		0	8760	0.000001	99.95%	0.00	0	0.00
	Water/Light Oil		0	8760	0.000006	99.95%	0.00	0	0.00
Open-ended Lines	Gas/Vapor		0	8760	0.004410	22.92%	0.00	0	0.00
	Light Oil		0	8760	0.003090	99.95%	0.00	0	0.00
	Heavy Oil		0	8760	0.000309	99.95%	0.00	0	0.00
	Water/Light Oil		0	8760	0.000550	99.95%	0.00	0	0.00
Other:	Gas/Vapor		40	8760	0.019400	22.92%	0.18	1,558	0.78
	Light Oil		0	8760	0.016500	99.95%	0.00	0	0.00
	Heavy Oil		0	8760	0.000068	99.95%	0.00	0	0.00
	Water/Light Oil		0	8760	0.030900	99.95%	0.00	0	0.00

Emission Component	lb/hr	lb/year	TPY
Controlled VOC Emissions	16.44	143,994	72.00

Notes:

[1] **Control efficiencies are taken from EPA Document EPA-453/R-095-017, November 1995, Table 5-2**

Valves	**Gas Vapor**	**67%**	**Pump**	**45%**	**Flanges/Connectors**	**0%**
	Light Liquid	**61%**				

[2] **Gas/Vapor analysis based on inlet gas. Liquid analysis based on stabilized crude oil.**

XTO Energy, Inc.
Cowboy CDP
FUGITIVE GREENHOUSE GAS EMISSIONS

Uncontrolled Emissions

Component Type	Service	Estimated Components Count	Hours	Factors	Total CH4 Weight %	Total CO2 Weight %	CH4 Emissions[1]	CO2 Emissions[2]
							tons/year	tons/year
Valves	Gas/Vapor	5699	8760	0.00992070	55.11%	0.23%	111.16	0.47
	Light Oil	2442	8760	0.00550000	0.00%	0.00%	0.00	0.00
	Heavy Oil	200	8760	0.00001900	0.00%	0.00%	0.00	0.00
	Water/Light Oil	0	8760	0.00021600	0.00%	0.00%	0.00	0.00
Pump Seals	Gas/Vapor	0	8760	0.00529000	55.11%	0.23%	0.00	0.00
	Light Oil	40	8760	0.02866000	0.00%	0.00%	0.00	0.00
	Heavy Oil	0	8760	0.00113000	0.00%	0.00%	0.00	0.00
	Water/Light Oil	0	8760	0.00005300	0.00%	0.00%	0.00	0.00
Connectors	Gas/Vapor	17097	8760	0.00044000	55.11%	0.23%	14.79	0.06
	Light Oil	7326	8760	0.00046300	0.00%	0.00%	0.00	0.00
	Heavy Oil	0	8760	0.00001700	0.00%	0.00%	0.00	0.00
	Water/Light Oil	1400	8760	0.00024300	0.00%	0.00%	0.00	0.00
Flanges	Gas/Vapor	1500	8760	0.00086000	55.11%	0.23%	2.54	0.01
	Light Oil	1500	8760	0.00024300	0.00%	0.00%	0.00	0.00
	Heavy Oil	0	8760	0.00000086	0.00%	0.00%	0.00	0.00
	Water/Light Oil	0	8760	0.00000620	0.00%	0.00%	0.00	0.00
Open-ended Lines	Gas/Vapor	0	8760	0.00441000	55.11%	0.23%	0.00	0.00
	Light Oil	0	8760	0.00309000	0.00%	0.00%	0.00	0.00
	Heavy Oil	0	8760	0.00030900	0.00%	0.00%	0.00	0.00
	Water/Light Oil	0	8760	0.00055000	0.00%	0.00%	0.00	0.00
Other:	Gas/Vapor	40	8760	0.01940000	55.11%	0.23%	1.53	0.01
	Light Oil	0	8760	0.01650000	0.00%	0.00%	0.00	0.00
	Heavy Oil	0	8760	0.00006800	0.00%	0.00%	0.00	0.00
	Water/Light Oil	0	8760	0.03090000	0.00%	0.00%	0.00	0.00

Emission Component	CH4 TPY	CO2 TPY
Uncontrolled Emissions	130.02	0.55

Notes:
[1] **CH4 emissions were calculated as follow: TOC lb/hr * CH4 weight % = CH4 lb/hr.**
[2] **CO2 emissions are based ratio of CH4 weight % to CO2 weight % per Exhibit 6.1 of API Compendium of Greenhouse Gas Emission Methodologies for the Oil and Natural Gas Industry; August 2009.**

XTO Energy, Inc.
Cowboy CDP
FUGITIVE EMISSIONS - HAPs

Controlled HAP Emissions

Component Type	Service	Control (%)[1]	Estimated Components Count	Hours	Factors	Total HAPs Weight %	Emissions lb/hour	Emissions lb/year	Emissions tons/year
Valves	Gas/Vapor	67%	5699	8760	0.00992000	0.07%	0.013	117.22	0.059
	Light Oil	61%	2442	8760	0.00550000	6.54%	0.342	2999.84	1.500
	Heavy Oil		200	8760	0.00001900	6.54%	0.000	2.18	0.001
	Water/Light Oil		0	8760	0.00021600	6.54%	0.000	0.00	0.000
Pump Seals	Gas/Vapor		0	8760	0.00529000	0.07%	0.000	0.00	0.000
	Light Oil	45%	40	8760	0.02866000	6.54%	0.041	361.10	0.181
	Heavy Oil		0	8760	0.00113000	6.54%	0.000	0.00	0.000
	Water/Light Oil		0	8760	0.00005300	6.54%	0.000	0.00	0.000
Connectors	Gas/Vapor		17097	8760	0.00044000	0.07%	0.005	47.27	0.024
	Light Oil		7326	8760	0.00046300	6.54%	0.222	1942.55	0.971
	Heavy Oil		0	8760	0.00001700	6.54%	0.000	0.00	0.000
	Water/Light Oil		1400	8760	0.00024300	6.54%	0.022	194.83	0.097
Flanges	Gas/Vapor		1500	8760	0.00086000	0.07%	0.001	8.11	0.004
	Light Oil		1500	8760	0.00024300	6.54%	0.024	208.75	0.104
	Heavy Oil		0	8760	0.00000086	6.54%	0.000	0.00	0.000
	Water/Light Oil		0	8760	0.00000620	6.54%	0.000	0.00	0.000
Open-ended Lines	Gas/Vapor		0	8760	0.00441000	0.07%	0.000	0.00	0.000
	Light Oil		0	8760	0.00309000	6.54%	0.000	0.00	0.000
	Heavy Oil		0	8760	0.00030900	6.54%	0.000	0.00	0.000
	Water/Light Oil		0	8760	0.00055000	6.54%	0.000	0.00	0.000
Other:	Gas/Vapor		40	8760	0.01940000	0.07%	0.001	4.88	0.002
	Light Oil		0	8760	0.01650000	6.54%	0.000	0.00	0.000
	Heavy Oil		0	8760	0.00006800	6.54%	0.000	0.00	0.000
	Water/Light Oil		0	8760	0.03090000	6.54%	0.000	0.00	0.000

Emission Component	lb/hr	lb/year	TPY
Total HAPs	0.67	5886.71	2.94

Notes:
[1] **Control efficiencies based on Table 5.2 of EPA-453/R-095-017**

Valves	Gas Vapor	67%	**Pump**	45%	**Flanges/Connectors**	0%
	Light Liquid	61%				

XTO Energy, Inc.
Cowboy CDP
ROAD EMISSIONS

PM_{30} (Total) Emissions $E = k(s/12)^a(W/3)^b$	
a	0.7
b	0.45
k	4.9
Silt Loading	4.8
Vehicle Weight (tons)	28
E-Hourly (lbs/VMT)	7.05
Rain Days	70
E-Annual (lbs/VMT)	5.70
Truckloads per year	27
Driving Distance Per Load (ft)	3000
Annual Distance (miles)	15
Control Efficiency - 15 MPH Limit	0.57
Control Efficiency - Base Course	0.60
Emissions (lbs/hr)	2.76
Emissions (tpy)	0.01

PM_{10} Emissions $E = k(s/12)^a(W/3)^b$	
a	0.9
b	0.45
k	1.5
Silt Loading	4.8
Vehicle Weight (tons)	28
E-Hourly (lbs/VMT)	1.80
Rain Days	70
E-Annual (lbs/VMT)	1.45
Truckloads per year	27
Driving Distance Per Load (ft)	3000
Annual Distance (miles)	15
Control Efficiency - 15 MPH Limit	0.57
Control Efficiency - Base Course	0.60
Emissions (lbs/hr)	0.70
Emissions (tpy)	0.00

$PM_{2.5}$ Emissions $E = k(s/12)^a(W/3)^b$	
a	0.9
b	0.45
k	0.15
Silt Loading	4.8
Vehicle Weight (tons)	28
E-Hourly (lbs/VMT)	0.18
Rain Days	70
E-Annual (lbs/VMT)	0.15
Truckloads per year	27
Driving Distance Per Load (ft)	3000
Annual Distance (miles)	15
Control Efficiency - 15 MPH Limit	0.57
Control Efficiency - Base Course	0.60
Emissions (lbs/hr)	0.07
Emissions (tpy)	0.00

Notes:
Emissions (lbs/hr) = Driving Distance (ft)/ 5280 * E (lbs/VMT) * 4 * (1-control efficiency).
Emissions (tpy) = Annual Distance * E / 2000

References:
EPA. "Compilation of Air Pollutant Emission Factors, Volume 1: Stationary Point and Area Sources," AP-42, Section 13.2.1
WRAP Fugitive Dust Handbook; September 7, 2006

Tab 7
Section 7 - Information Used To Determine Emissions

Section 7

Information Used To Determine Emissions

<u>Information Used to Determine Emissions</u> shall include the following:

- ☑ If manufacturer data are used, include specifications for emissions units <u>and</u> control equipment, including control efficiencies specifications and sufficient engineering data for verification of control equipment operation, including design drawings, test reports, and design parameters that affect normal operation.
- ☐ If test data are used, include a copy of the complete test report. If the test data are for an emissions unit other than the one being permitted, the emission units must be identical. Test data may not be used if any difference in operating conditions of the unit being permitted and the unit represented in the test report significantly effect emission rates.
- ☑ If the most current copy of AP-42 is used, reference the section and date located at the bottom of the page. Include a copy of the page containing the emissions factors, and clearly mark the factors used in the calculations.
- ☐ If an older version of AP-42 is used, include a complete copy of the section.
- ☑ If an EPA document or other material is referenced, include a complete copy.
- ☐ Fuel specifications sheet.
- ☑ If computer models are used to estimate emissions, include an input summary (if available) and a detailed report, and a disk containing the input file(s) used to run the model. For tank-flashing emissions, include a discussion of the method used to estimate tank-flashing emissions, relative thresholds (i.e., permit or major source (NSPS, PSD or Title V)), accuracy of the model, the input and output from simulation models and software, all calculations, documentation of any assumptions used, descriptions of sampling methods and conditions, copies of any lab sample analysis.

The Cowboy CDP gas inlet and NGL inlet streams, labeled as "193H W gas" and "193 W NGL" in the CDP HYSYS model respectively, were determined from reservoir fluid study conducted on a well fluid sample taken from a representative formation in the Delaware Basin. The laboratory report is included as confidential information in Tab 24. The analysis was conducted to determine the type and character of the reservoir fluid, the compositional analyses of the separator gas, the separator hydrocarbon liquid, and the mathematically recombined wellstream fluid. The representative analysis was input into HYSYS as inlet composition of gas and hydrocarbon liquid to simulate the well fluids flowing into the surrounding batteries. XTO Energy then modeled the gas leaving the battery flowing into a compressor station and used the NGL and Gas sales lines from the HYSYS compressor station model as the inlet feeds to Cowboy CDP. Utilizing the CDP HYSYS model, the gas and NGL inlets were used as inputs for the cryogenic gas plant and NGL stabilization processes at the Cowboy facility. The HYSYS simulation results are provided in Section 7. The following HYSYS streams were taken directly from the confidential reservoir fluid study and are included as confidential information in Tab 24:

- "HC Gas" – "Separator gas" from the first-stage separator of the well fluid sample.
- "HC liq" – "Separator HC liquid" from the first-stage separator of the well fluid sample.

The Cowboy CDP oil inlet streams, labeled as "14 RVP" in the CDP HYSYS model, was determined from reservoir fluid study conducted on a well fluid sample taken from a representative formation in the Delaware Basin. The laboratory report is included as confidential information in Tab 24 of the HUSKY CDP XTO Energy PSD Major Source Air Quality Permit Application. The analysis was conducted to determine the type and character of the reservoir fluid, the compositional analyses of the separator gas, the separator hydrocarbon liquid, and the mathematically recombined wellstream fluid. The representative analysis was input into generic HYSYS tank battery model as inlet separator gas and hydrocarbon liquid. The oil inlet in the CDP HYSYS model, 14 RVP, was the sales oil leaving the battery (conservatively modeled to 14 RVP oil).

XTO used process stream compositions generated by the HSYS process simulation as input compositions in a ProMax simulation for the CDP, in order to simulate tank emissions and consolidate all relevant streams into one model. ProMax and HYSYS simulation results are provided in this section.

The following HYSYS process streams were extracted from the HYSYS report and used in ProMax CDP simulation:

- "Gas Inlet" –Used for fugitive VOC/HAP speciation.
- "To oil pl" – Used for IFR tank inlet composition
- "To slop oil" – Used for Drain Vessel oil that is sent to the slop tank
- "To GB2" – Used for Drain Vessel water that is sent to the gunbarrel

- “WiO2” – Used for Surge Vessel water that is sent to the gunbarrel
- “Oil OVHD” – Used for gas composition of the stabilizer overhead gas MSS events (process purge gas flaring).
- “Residue Gas” – Used for Pilot Fuel, LP Header Purge Gas Cryo, HP Header Purge Gas Cryo, LP Header Purge Gas Stabilizer, HP Header Purge Gas Stabilizer

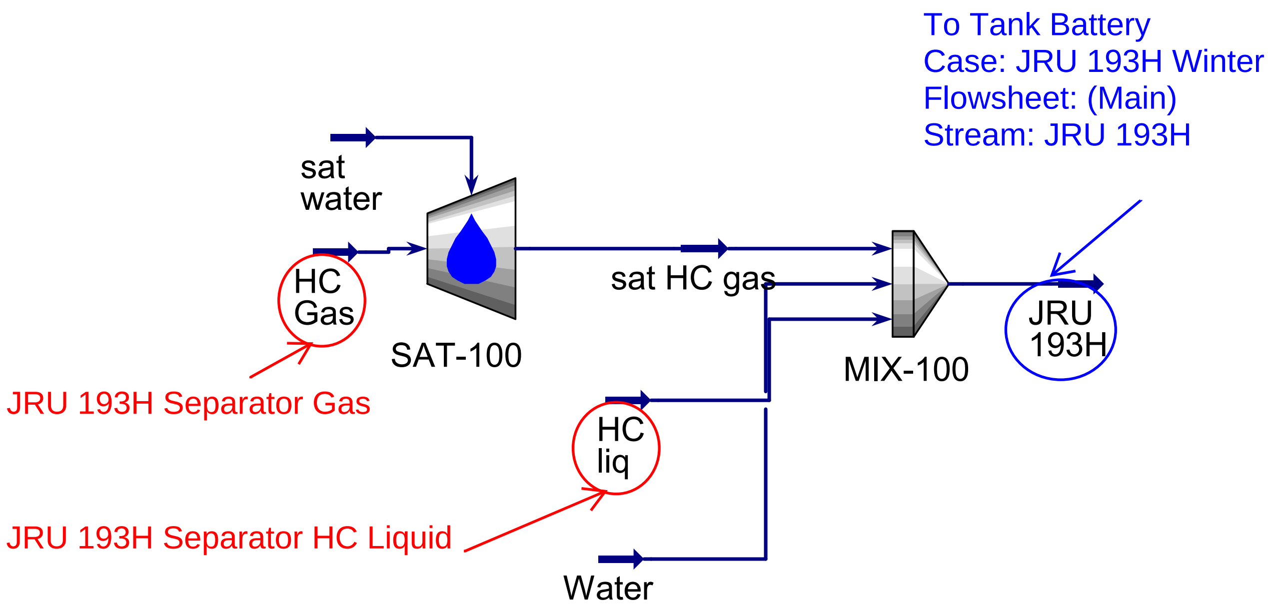
The following HYSYS process streams were extracted from the HYSYS report and used in ProMax Amine simulation:

- “Gas Int” – Used for Inlet Gas composition into Promax Amine Model
- “Residue Gas” – Used for TO Assist Fuel

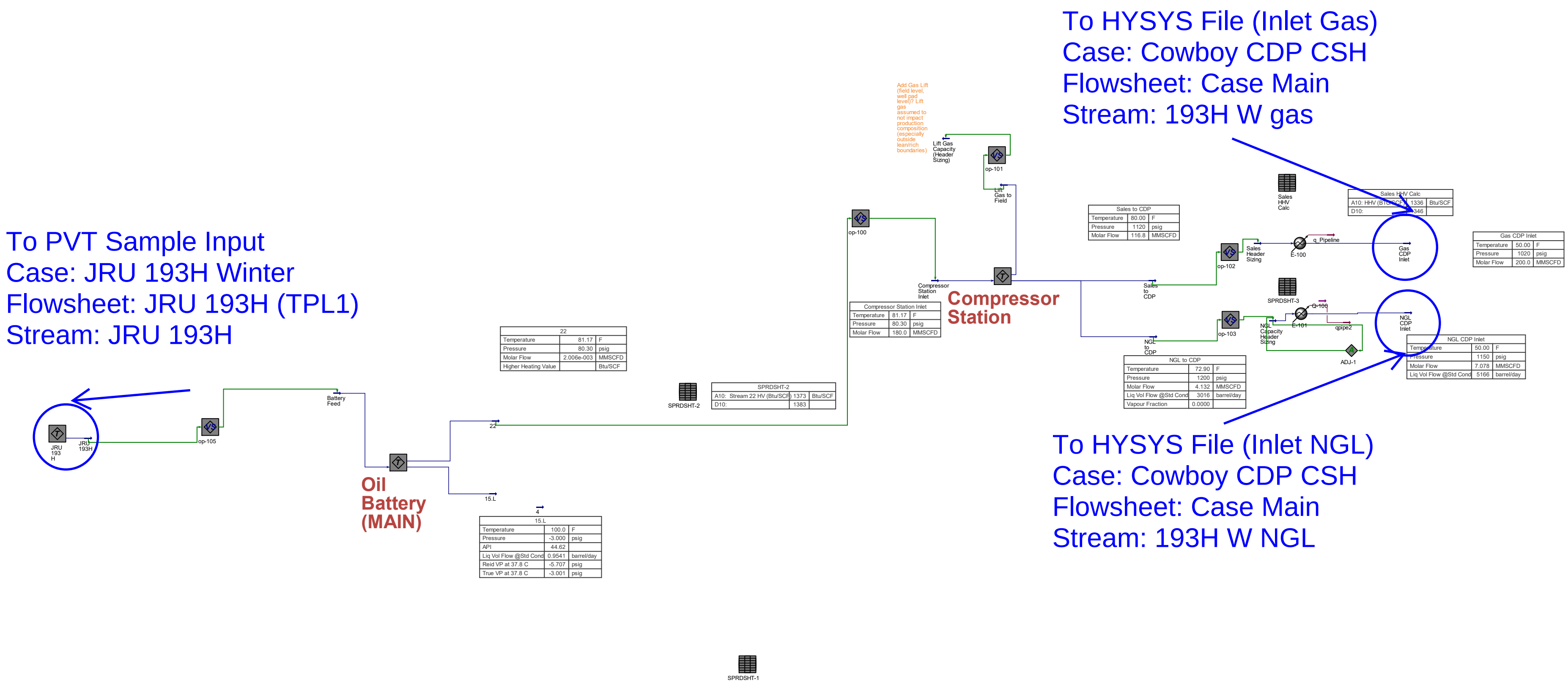
The following supplemental documents are provided in support of the calculations:

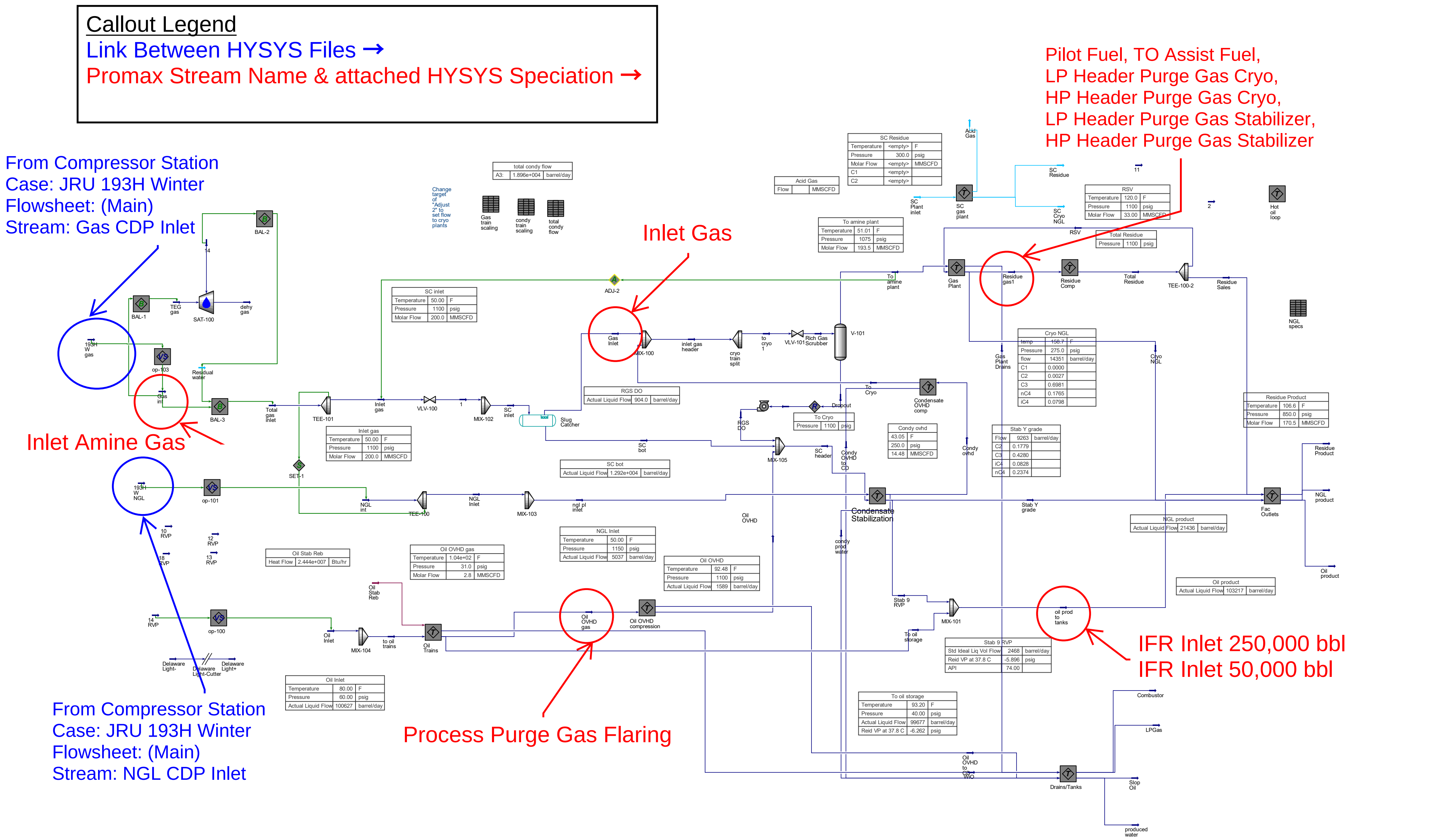
- HYSYS Simulation
- Promax CDP Simulation
- Promax Amine Unit Simulation
- Heater Manufacturer Data
- Thermal Oxidizer Manufacturer Data
- Flare Manufacturer Data
- Enclosed Combustor Manufacturer Data
- Generator Manufacturer Data
- AP-42 and Other Emissions Guidance as Noted
- Confidential PVT Analysis (See Tab 24)

Callout Legend
Link Between HYSYS Files →
Promax Stream Name & attached HYSYS Speciation →



Callout Legend
Link Between HYSYS Files →
Promax Stream Name & attached HYSYS Speciation →

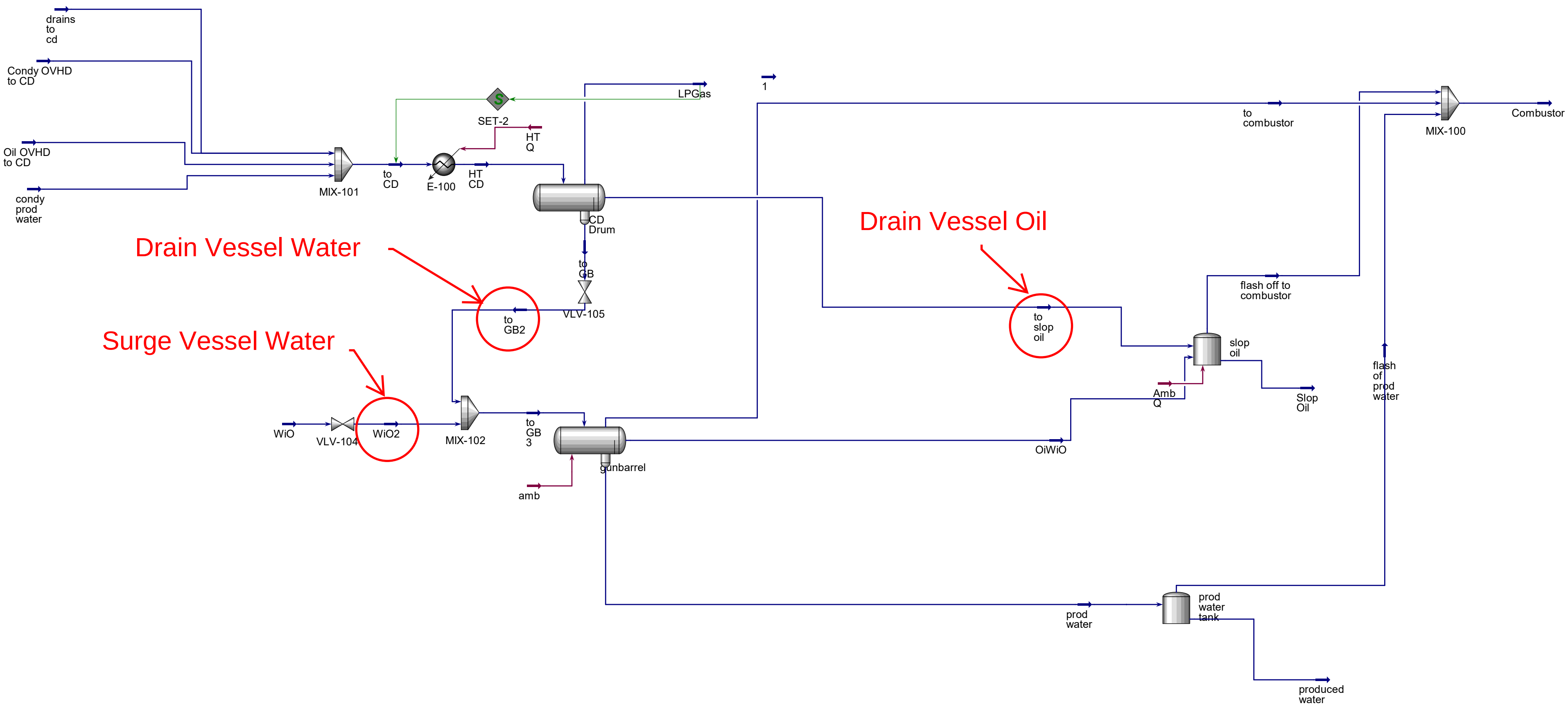



Callout Legend
Link Between HYSYS Files →
Promax Stream Name & attached HYSYS Speciation →
From Compressor Station
Case: JRU 193H Winter
Flowsheet: (Main)
Stream: Gas CDP Inlet
Inlet Amine Gas
Inlet Gas
Pilot Fuel, TO Assist Fuel,
LP Header Purge Gas Cryo,
HP Header Purge Gas Cryo,
LP Header Purge Gas Stabilizer,
HP Header Purge Gas Stabilizer
IFR Inlet 250,000 bbl
IFR Inlet 50,000 bbl
Process Purge Gas Flaring
From Compressor Station
Case: JRU 193H Winter
Flowsheet: (Main)
Stream: NGL CDP Inlet
Condensate Stabilization
Drains/Tanks

Callout Legend

Link Between HYSYS Files →

Promax Stream Name & attached HYSYS Speciation →



XTO ENERGY INC.
Cowboy CDP
PROCESS SIMULATION COMPONENTS

PROCESS SIMULATION COMPONENTS - INLET GAS

HYSYS PROCESS STREAM NAME:	Gas Int
HYSYS COMPONENTS	
Component	**Mole Frac**
Oxygen	0.00000
H2S	0.00000
Nitrogen	0.01480
CO2	0.00112
Methane	0.70205
Ethane	0.15319
Propane	0.08529
i-Butane	0.00984
n-Butane	0.02370
22-Mpropane	0.00011
i-Pentane	0.00377
n-Pentane	0.00378
22-Mbutane	0.00002
Cyclopentane	0.00000
23-Mbutane	0.00012
2-Mpentane	0.00042
3-Mpentane	0.00021
n-Hexane	0.00046
Hexanes*	0.00000
Mcyclopentan	0.00027
Benzene	0.00006
Cyclohexane	0.00028
2-Mhexane	0.00004
3-Mhexane	0.00003
224-Mpentane	0.00000
n-Heptane	0.00006
Heptanes*	0.00007
Mcyclohexane	0.00012
Toluene	0.00002
n-Octane	0.00000
Octanes*	0.00003
E-Benzene	0.00000
m-Xylene	0.00000
o-Xylene	0.00000
p-Xylene	0.00000
Nonanes*	0.00000
Decanes*	0.00000
Undecanes_3*	0.00000
Dodecanes_3*	0.00000
Triadecanes_3*	0.00000
Tetradecanes_3*	0.00000
Pentadecanes_3*	0.00000
Hexadecanes_3*	0.00000
Heptadecanes_3*	0.00000
Octadecanes_3*	0.00000
Nonadecanes_3*	0.00000
eicosanes_3*	0.00000
Heneicosanes_3*	0.00000
Dodocosanes_3*	0.00000
Triacosanes_3*	0.00000
Tetracosanes_3*	0.00000
Pentacosanes_3*	0.00000
Hexacosanes_3*	0.00000
Heptacosanes_3*	0.00000
Octacosanes_3*	0.00000
Nonacosanes_3*	0.00000
Triacontanes*	0.00000
C31+_2*	0.00000
H2O	0.00015
NC30*	0.00000
n-Nonane	0.00000
n-Decane	0.00000
NC31-35*	0.00000
TexaTherm	0.00000
NC31-35_1*	0.00000
CO	0.00000
TOTALS	1.000

PROMAX PROCESS STREAM NAME:	Inlet Gas AMINE	
PROMAX COMPONENTS		
Component	**Mole Frac**	**WT%**
Hydrogen Sulfide	0.000	0.00
N2	0.015	1.82
Carbon Dioxide	0.001	0.22
Methane	0.702	49.42
Ethane	0.153	20.21
Propane	0.085	16.50
i-Butane	0.010	2.51
n-Butane	0.024	6.04
i-Pentane	0.004	1.23
n-Pentane	0.004	1.20
n-Hexane	0.002	0.83
Water	0.000	0.01
MDEA	0.000	0.00
Piperazine	0.000	0.00
O2	0.000	0.00
Total	1.00000	

Specific Gravity	
Molecular Weight (lb/lbmol)	
VOC WT%	11.82
HAP WT%	0.826

Material Stream: Gas int

Fluid Package: Peng Robinson

Property Package: Peng-Robinson

CONDITIONS

		Overall	Vapour Phase	Liquid Phase		
Vapour / Phase Fraction		0.9008	0.9008	0.0992		
Temperature:	(F)	50.00	50.00	50.00		
Pressure:	(psig)	1150 *	1150	1150		
Molar Flow	(MMSCFD)	200.0	180.2	19.85		
Mass Flow	(lb/hr)	5.006e+005	4.291e+005	7.145e+004		
Std Ideal Liq Vol Flow	(barrel/day)	9.490e+004	8.363e+004	1.127e+004		
Molar Enthalpy	(Btu/lbmole)	-3.667e+004	-3.575e+004	-4.500e+004		
Molar Entropy	(Btu/lbmole-F)	33.47	34.06	28.14		
Heat Flow	(Btu/hr)	-8.053e+008	-7.072e+008	-9.807e+007		
Liq Vol Flow @Std Cond	(barrel/day)	3.538e+007 *	3.188e+007	8.511e+005		

PROPERTIES

		Overall	Vapour Phase	Liquid Phase		
Molecular Weight		22.79	21.69	32.79		
Molar Density	(lbmole/ft3)	0.3535	0.3353	0.6972		
Mass Density	(lb/ft3)	8.058	7.274	22.86		
Act. Volume Flow	(barrel/day)	2.655e+005	2.522e+005	1.336e+004		
Mass Enthalpy	(Btu/lb)	-1609	-1648	-1373		
Mass Entropy	(Btu/lb-F)	1.469	1.570	0.8583		
Heat Capacity	(Btu/lbmole-F)	19.52	18.82	25.92		
Mass Heat Capacity	(Btu/lb-F)	0.8565	0.8674	0.7907		
LHV Molar Basis (Std)	(Btu/SCF)	---	---	---		
LHV Mass Basis (Std)	(Btu/lb)	---	---	---		
Phase Fraction [Vol. Basis]		0.8813	0.8813	0.1187		
Phase Fraction [Mass Basis]		0.8573	0.8573	0.1427		
Partial Pressure of CO2	(psig)	-13.38	---	---		
Cost Based on Flow	(Cost/s)	0.0000	0.0000	0.0000		
Act. Gas Flow	(ACFM)	983.2	983.2	---		
Avg. Liq. Density	(lbmole/ft3)	0.9892	1.011	0.8267		
Specific Heat	(Btu/lbmole-F)	19.52	18.82	25.92		
Std. Gas Flow	(MMSCFD)	199.6	179.8	19.81		
Std. Ideal Liq. Mass Density	(lb/ft3)	22.55	21.93	27.10		
Act. Liq. Flow	(barrel/day)	1.336e+004	---	1.336e+004		
Z Factor		---	0.6350	0.3054		
Watson K		17.59	17.87	15.93		
User Property		---	---	---		
Cp/(Cp - R)		1.113	1.118	1.083		
Cp/Cv		2.058	2.193	1.083		
Heat of Vap.	(Btu/lbmole)	3032	---	---		
Kinematic Viscosity	(cSt)	---	0.1319	0.1654		
Liq. Mass Density (Std. Cond)	(lb/ft3)	6.047e-002	5.753e-002	0.3589		
Liq. Vol. Flow (Std. Cond)	(barrel/day)	3.538e+007	3.188e+007	8.511e+005		
Liquid Fraction		9.924e-002	0.0000	1.000		
Molar Volume	(ft3/lbmole)	2.829	2.982	1.434		
Mass Heat of Vap.	(Btu/lb)	133.0	---	---		
Phase Fraction [Molar Basis]		0.9008	0.9008	0.0992		
Surface Tension	(dyne/cm)	4.646	---	4.646		
Thermal Conductivity	(Btu/hr-ft-F)	---	2.373e-002	4.825e-002		
Viscosity	(cP)	---	1.536e-002	6.055e-002		
Cv (Semi-Ideal)	(Btu/lbmole-F)	17.54	16.83	23.94		
Mass Cv (Semi-Ideal)	(Btu/lb-F)	0.7694	0.7759	0.7302		

* Specified by user.

Material Stream: Gas int (continued)

Fluid Package: Peng Robinson

Property Package: Peng-Robinson

PROPERTIES

	Overall	Vapour Phase	Liquid Phase		
Cv (Btu/lbmole-F)	9.486	8.579	23.94		
Mass Cv (Btu/lb-F)	0.4162	0.3955	0.7302		
Cv (Ent. Method) (Btu/lbmole-F)	16.67	8.579	---		
Mass Cv (Ent. Method) (Btu/lb-F)	0.7312	0.3955	---		
Cp/Cv (Ent. Method)	1.171	2.193	---		
Liq. Vol. Flow - Sum(Std. Cond) (barrel/day)	3.274e+007	3.188e+007	8.511e+005		
Partial Pressure of H2S (psig)	-14.70	---	---		
Reid VP at 37.8 C (psig)	---	---	793.5		
True VP at 37.8 C (psig)	---	---	1342		
Viscosity Index	---	---	---		
HHV Molar Basis (Std) (Btu/SCF)	---	---	---		
HHV Mass Basis (Std) (Btu/lb)	---	---	---		
CO2 Loading	---	---	---		
CO2 Apparent Mole Conc. (lbmole/ft3)	---	---	7.020e-004		
CO2 Apparent Wt. Conc. (lbmol/lb)	---	---	3.071e-005		
Phase Fraction [Act. Vol. Basis]	0.9497	0.9497	5.032e-002		
Mass Exergy (Btu/lb)	189.1	---	---		
Ideal Gas Cp/Cv	1.236	1.246	1.170		
Ideal Gas Cp (Btu/lbmole-F)	10.42	10.06	13.65		
Mass Ideal Gas Cp (Btu/lb-F)	0.4570	0.4638	0.4163		
Bubble Point Pressure (psig)	---	---	---		

COMPOSITION

Overall Phase

Vapour Fraction 0.9008

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Oxygen	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2S	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nitrogen	325.0274	0.0148	9105.0887	0.0182	773.1458	0.0081
CO2	24.5967	0.0011	1082.5034	0.0022	89.8075	0.0009
Methane	15419.3477	0.7021	247373.6351	0.4942	56574.9325	0.5961
Ethane	3364.6347	0.1532	101175.2871	0.2021	19477.1345	0.2052
Propane	1873.3000	0.0853	82607.7728	0.1650	11163.5572	0.1176
i-Butane	216.0993	0.0098	12560.6881	0.0251	1530.4429	0.0161
n-Butane	520.4831	0.0237	30252.8769	0.0604	3551.7776	0.0374
22-Mpropane	2.3499	0.0001	169.5466	0.0003	19.4919	0.0002
i-Pentane	82.7942	0.0038	5973.7432	0.0119	656.0912	0.0069
n-Pentane	83.0138	0.0038	5989.5886	0.0120	651.2640	0.0069
22-Mbutane	0.3997	0.0000	34.4453	0.0001	3.6143	0.0000
Cyclopentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
23-Mbutane	2.5914	0.0001	223.3268	0.0004	22.9892	0.0002
2-Mpentane	9.3336	0.0004	804.3548	0.0016	83.8923	0.0009
3-Mpentane	4.6119	0.0002	397.4459	0.0008	40.7587	0.0004
n-Hexane	10.0144	0.0005	863.0254	0.0017	89.1752	0.0009
Hexanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Mcyclopentan	6.0174	0.0003	506.4411	0.0010	46.1092	0.0005
Benzene	1.2760	0.0001	99.6657	0.0002	7.7357	0.0001
Cyclohexane	6.1931	0.0003	521.2159	0.0010	45.6482	0.0005
2-Mhexane	0.8192	0.0000	82.0845	0.0002	8.2468	0.0001
3-Mhexane	0.7401	0.0000	74.1621	0.0001	7.3573	0.0001

* Specified by user.

Material Stream: Gas int (continued)

Fluid Package: Peng Robinson

Property Package: Peng-Robinson

COMPOSITION

Overall Phase (continued)

Vapour Fraction 0.9008

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
224-Mpentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Heptane	1.2408	0.0001	124.3371	0.0002	12.3958	0.0001
Heptanes*	1.4341	0.0001	137.6725	0.0003	12.9928	0.0001
Mcyclohexane	2.5475	0.0001	250.1403	0.0005	22.1738	0.0002
Toluene	0.3909	0.0000	36.0193	0.0001	2.8347	0.0000
n-Octane	0.0993	0.0000	11.3394	0.0000	1.1007	0.0000
Octanes*	0.6808	0.0000	72.8464	0.0001	6.6729	0.0001
E-Benzene	0.0067	0.0000	0.7111	0.0000	0.0560	0.0000
m-Xylene	0.0117	0.0000	1.2451	0.0000	0.0983	0.0000
o-Xylene	0.0122	0.0000	1.2940	0.0000	0.1003	0.0000
p-Xylene	0.0119	0.0000	1.2614	0.0000	0.0999	0.0000
Nonanes*	0.0591	0.0000	7.1483	0.0000	0.6386	0.0000
Decanes*	0.0050	0.0000	0.6710	0.0000	0.0589	0.0000
Undecanes_3*	0.0003	0.0000	0.0507	0.0000	0.0044	0.0000
Dodecanes_3*	0.0000	0.0000	0.0028	0.0000	0.0002	0.0000
Triadecanes_3*	0.0000	0.0000	0.0001	0.0000	0.0000	0.0000
Tetradecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Pentadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
eicosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heneicosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Dodocosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Tetracosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Pentacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacontanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C31+_2*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2O	0.7950	0.0000	14.3221	0.0000	0.9826	0.0000
NC30*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Nonane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Decane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC31-35*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TexaTherm	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC31-35_1*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
CO	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TEGlycol	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
SO2	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C10+ (SS1H)*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
464H C7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
474Y c7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Total	21960.9387	1.0000	500555.9597	1.0000	94903.3818	1.0000

* Specified by user.

Material Stream: Gas int (continued)

Fluid Package: Peng Robinson

Property Package: Peng-Robinson

COMPOSITION

Vapour Phase

Phase Fraction 0.9008

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Oxygen	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2S	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nitrogen	314.3313	0.0159	8805.4534	0.0205	747.7027	0.0089
CO2	22.4022	0.0011	985.9228	0.0023	81.7949	0.0010
Methane	14509.8332	0.7335	232782.2333	0.5425	53237.8445	0.6366
Ethane	2913.3313	0.1473	87604.4961	0.2042	16864.6376	0.2016
Propane	1441.6125	0.0729	63571.4481	0.1481	8591.0015	0.1027
i-Butane	146.5501	0.0074	8518.1675	0.0199	1037.8865	0.0124
n-Butane	331.0336	0.0167	19241.1983	0.0448	2258.9738	0.0270
22-Mpropane	1.4212	0.0001	102.5452	0.0002	11.7891	0.0001
i-Pentane	43.5355	0.0022	3141.1591	0.0073	344.9909	0.0041
n-Pentane	40.4254	0.0020	2916.7608	0.0068	317.1472	0.0038
22-Mbutane	0.1679	0.0000	14.4722	0.0000	1.5185	0.0000
Cyclopentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
23-Mbutane	1.0318	0.0001	88.9179	0.0002	9.1532	0.0001
2-Mpentane	3.6008	0.0002	310.3084	0.0007	32.3644	0.0004
3-Mpentane	1.7123	0.0001	147.5608	0.0003	15.1326	0.0002
n-Hexane	3.4653	0.0002	298.6358	0.0007	30.8576	0.0004
Hexanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Mcyclopentan	2.0242	0.0001	170.3645	0.0004	15.5109	0.0002
Benzene	0.4372	0.0000	34.1498	0.0001	2.6506	0.0000
Cyclohexane	2.0066	0.0001	168.8769	0.0004	14.7903	0.0002
2-Mhexane	0.2135	0.0000	21.3970	0.0000	2.1497	0.0000
3-Mhexane	0.1892	0.0000	18.9572	0.0000	1.8807	0.0000
224-Mpentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Heptane	0.2885	0.0000	28.9140	0.0001	2.8826	0.0000
Heptanes*	0.3552	0.0000	34.1025	0.0001	3.2184	0.0000
Mcyclohexane	0.6159	0.0000	60.4743	0.0001	5.3608	0.0001
Toluene	0.0897	0.0000	8.2692	0.0000	0.6508	0.0000
n-Octane	0.0148	0.0000	1.6872	0.0000	0.1638	0.0000
Octanes*	0.1194	0.0000	12.7746	0.0000	1.1702	0.0000
E-Benzene	0.0009	0.0000	0.0948	0.0000	0.0075	0.0000
m-Xylene	0.0016	0.0000	0.1682	0.0000	0.0133	0.0000
o-Xylene	0.0016	0.0000	0.1706	0.0000	0.0132	0.0000
p-Xylene	0.0016	0.0000	0.1718	0.0000	0.0136	0.0000
Nonanes*	0.0066	0.0000	0.7930	0.0000	0.0708	0.0000
Decanes*	0.0004	0.0000	0.0483	0.0000	0.0042	0.0000
Undecanes_3*	0.0000	0.0000	0.0024	0.0000	0.0002	0.0000
Dodecanes_3*	0.0000	0.0000	0.0001	0.0000	0.0000	0.0000
Triadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Tetradecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Pentadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
eicosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heneicosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000

* Specified by user.

Material Stream: Gas int (continued)

Fluid Package: Peng Robinson

Property Package: Peng-Robinson

COMPOSITION

Vapour Phase (continued)

Phase Fraction 0.9008

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Dodocosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Tetracosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Pentacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacontanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C31+_2*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2O	0.7209	0.0000	12.9871	0.0000	0.8911	0.0000
NC30*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Nonane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Decane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC31-35*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TexaTherm	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC31-35_1*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
CO	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TEGlycol	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
SO2	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C10+ (SS1H)*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
464H C7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
474Y c7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Total	19781.5420	1.0000	429103.6833	1.0000	83634.2377	1.0000

Liquid Phase

Phase Fraction 9.924e-002

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Oxygen	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2S	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nitrogen	10.6962	0.0049	299.6353	0.0042	25.4431	0.0023
CO2	2.1945	0.0010	96.5806	0.0014	8.0126	0.0007
Methane	909.5145	0.4173	14591.4018	0.2042	3337.0879	0.2961
Ethane	451.3034	0.2071	13570.7910	0.1899	2612.4969	0.2318
Propane	431.6876	0.1981	19036.3247	0.2664	2572.5557	0.2283
i-Butane	69.5492	0.0319	4042.5206	0.0566	492.5564	0.0437
n-Butane	189.4495	0.0869	11011.6786	0.1541	1292.8038	0.1147
22-Mpropane	0.9286	0.0004	67.0013	0.0009	7.7028	0.0007
i-Pentane	39.2587	0.0180	2832.5841	0.0396	311.1003	0.0276
n-Pentane	42.5884	0.0195	3072.8278	0.0430	334.1168	0.0296
22-Mbutane	0.2318	0.0001	19.9731	0.0003	2.0957	0.0002
Cyclopentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
23-Mbutane	1.5597	0.0007	134.4089	0.0019	13.8360	0.0012
2-Mpentane	5.7328	0.0026	494.0464	0.0069	51.5279	0.0046
3-Mpentane	2.8996	0.0013	249.8851	0.0035	25.6261	0.0023
n-Hexane	6.5491	0.0030	564.3896	0.0079	58.3176	0.0052
Hexanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Mcyclopentan	3.9932	0.0018	336.0766	0.0047	30.5983	0.0027

* Specified by user.

Material Stream: Gas int (continued)

Fluid Package: Peng Robinson
Property Package: Peng-Robinson

COMPOSITION

Liquid Phase (continued)

Phase Fraction 9.924e-002

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Benzene	0.8388	0.0004	65.5159	0.0009	5.0851	0.0005
Cyclohexane	4.1865	0.0019	352.3391	0.0049	30.8579	0.0027
2-Mhexane	0.6056	0.0003	60.6875	0.0008	6.0971	0.0005
3-Mhexane	0.5509	0.0003	55.2049	0.0008	5.4767	0.0005
224-Mpentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Heptane	0.9523	0.0004	95.4231	0.0013	9.5132	0.0008
Heptanes*	1.0788	0.0005	103.5700	0.0014	9.7744	0.0009
Mcyclohexane	1.9316	0.0009	189.6660	0.0027	16.8130	0.0015
Toluene	0.3012	0.0001	27.7501	0.0004	2.1839	0.0002
n-Octane	0.0845	0.0000	9.6521	0.0001	0.9369	0.0001
Octanes*	0.5614	0.0003	60.0718	0.0008	5.5027	0.0005
E-Benzene	0.0058	0.0000	0.6164	0.0000	0.0485	0.0000
m-Xylene	0.0101	0.0000	1.0768	0.0000	0.0851	0.0000
o-Xylene	0.0106	0.0000	1.1234	0.0000	0.0871	0.0000
p-Xylene	0.0103	0.0000	1.0895	0.0000	0.0863	0.0000
Nonanes*	0.0525	0.0000	6.3553	0.0001	0.5678	0.0001
Decanes*	0.0046	0.0000	0.6227	0.0000	0.0546	0.0000
Undecanes_3*	0.0003	0.0000	0.0483	0.0000	0.0042	0.0000
Dodecanes_3*	0.0000	0.0000	0.0027	0.0000	0.0002	0.0000
Triadecanes_3*	0.0000	0.0000	0.0001	0.0000	0.0000	0.0000
Tetradecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Pentadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
eicosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heneicosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Dodocosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Tetracosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Pentacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacontanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C31+_2*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2O	0.0741	0.0000	1.3350	0.0000	0.0916	0.0000
NC30*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Nonane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Decane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC31-35*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TexaTherm	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC31-35_1*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
CO	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TEGlycol	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
SO2	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000

* Specified by user.

Material Stream: Gas int (continued)

Fluid Package: Peng Robinson

Property Package: Peng-Robinson

COMPOSITION

Liquid Phase (continued)

Phase Fraction 9.924e-002

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
C10+ (SS1H)*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
464H C7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
474Y c7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Total	2179.3967	1.0000	71452.2765	1.0000	11269.1442	1.0000

* Specified by user.

XTO ENERGY INC.
Cowboy CDP
PROCESS SIMULATION COMPONENTS

PROCESS SIMULATION COMPONENTS - INLET GAS

HYSYS PROCESS STREAM NAME:	Gas Inlet
HYSYS COMPONENTS	
Component	**Mole Frac**
Oxygen	0.000
H2S	0.000
Nitrogen	0.016
CO2	0.001
Methane	0.735
Ethane	0.147
Propane	0.072
i-Butane	0.007
n-Butane	0.016
22-Mpropane	0.000
i-Pentane	0.002
n-Pentane	0.002
22-Mbutane	0.000
Cyclopentane	0.000
23-Mbutane	0.000
2-Mpentane	0.000
3-Mpentane	0.000
n-Hexane	0.000
Hexanes*	0.000
Mcyclopentan	0.000
Benzene	0.000
Cyclohexane	0.000
2-Mhexane	0.000
3-Mhexane	0.000
224-Mpentane	0.000
n-Heptane	0.000
Heptanes*	0.000
Mcyclohexane	0.000
Toluene	0.000
n-Octane	0.000
Octanes*	0.000
E-Benzene	0.000
m-Xylene	0.000
o-Xylene	0.000
p-Xylene	0.000
Nonanes*	0.000
Decanes*	0.000
Undecanes_3*	0.000
Dodecanes_3*	0.000
Triadecanes_3*	0.000
Tetradecanes_3*	0.000
Pentadecanes_3*	0.000
Hexadecanes_3*	0.000
Heptadecanes_3*	0.000
Octadecanes_3*	0.000
Nonadecanes_3*	0.000
eicosanes_3*	0.000
Heneicosanes_3*	0.000
Dodocosanes_3*	0.000
Triacosanes_3*	0.000
Tetracosanes_3*	0.000
Pentacosanes_3*	0.000
Hexacosanes_3*	0.000
Heptacosanes_3*	0.000
Octacosanes_3*	0.000
Nonacosanes_3*	0.000
Triacontanes*	0.000
C31+_2*	0.000
H2O	0.000
NC30*	0.000
n-Nonane	0.000
n-Decane	0.000
NC31-35*	0.000
TexaTherm	0.000
NC31-35_1*	0.000
CO	0.000
TOTALS	1.000

PROMAX PROCESS STREAM NAME:	Inlet Gas	
PROMAX COMPONENTS		
Component	**Mole Frac**	**WT%**
Water	0.00015	0.01
Hydrogen Sulfide	0.00000	0.00
Nitrogen	0.01592	1.04
Carbon Dioxide	0.00113	0.23
Methane	0.73517	55.11
Ethane	0.14720	20.68
Propane	0.07216	14.87
Iso-butane	0.00724	1.97
N-butane	0.01623	4.41
Iso-pentane	0.00208	0.70
N-pentane	0.00192	0.65
Cyclopentanes	0.00000	0.00
Other Hexanes	0.00037	0.15
n-Hexane	0.00016	0.06
Methylcyclopentane	0.00009	0.04
Benzene	0.00002	0.01
Cyclohexane	0.00009	0.04
2,2,4 Trimethylpentane	0.00000	0.00
Other Heptanes	0.00003	0.01
Methylcyclohexane	0.00003	0.01
n-Heptane	0.00001	0.00
Toluene	0.00000	0.00
Octanes	0.00001	0.01
Ethylbenzene	0.00000	0.00
M&P-Xylene	0.00000	0.00
Nonanes	0.00000	0.00
Decanes	0.00000	0.00
Undecanes	0.00000	0.00
Total	1.000	100.000

Characteristics of Undecanes Plus	
Specific Gravity	0.8661
Molecular Weight (lb/lbmol)	262.912
VOC WT%	22.92
HAP WT%	0.072

Material Stream: Gas Inlet

Fluid Package: Peng Robinson

Property Package: Peng-Robinson

CONDITIONS

		Overall	Vapour Phase	Liquid Phase		
Vapour / Phase Fraction		1.0000	1.0000	0.0000		
Temperature:	(F)	50.00	50.00	50.00		
Pressure:	(psig)	1100 *	1100	1100		
Molar Flow	(MMSCFD)	180.4	180.4	0.0000		
Mass Flow	(lb/hr)	4.283e+005	4.283e+005	0.0000		
Std Ideal Liq Vol Flow	(barrel/day)	8.364e+004	8.364e+004	0.0000		
Molar Enthalpy	(Btu/lbmole)	-3.564e+004	-3.564e+004	-4.558e+004		
Molar Entropy	(Btu/lbmole-F)	34.27	34.27	27.85		
Heat Flow	(Btu/hr)	-7.061e+008	-7.061e+008	0.0000		
Liq Vol Flow @Std Cond	(barrel/day)	3.193e+007 *	3.193e+007	0.0000		

PROPERTIES

		Overall	Vapour Phase	Liquid Phase		
Molecular Weight		21.62	21.62	33.55		
Molar Density	(lbmole/ft3)	0.3133	0.3133	0.7119		
Mass Density	(lb/ft3)	6.774	6.774	23.89		
Act. Volume Flow	(barrel/day)	2.703e+005	2.703e+005	0.0000		
Mass Enthalpy	(Btu/lb)	-1648	-1648	-1358		
Mass Entropy	(Btu/lb-F)	1.585	1.585	0.8301		
Heat Capacity	(Btu/lbmole-F)	18.04	18.04	25.91		
Mass Heat Capacity	(Btu/lb-F)	0.8343	0.8343	0.7722		
LHV Molar Basis (Std)	(Btu/SCF)	---	---	---		
LHV Mass Basis (Std)	(Btu/lb)	---	---	---		
Phase Fraction [Vol. Basis]		1.000	1.000	---		
Phase Fraction [Mass Basis]		1.000	1.000	0.0000		
Partial Pressure of CO2	(psig)	-13.43	---	---		
Cost Based on Flow	(Cost/s)	0.0000	0.0000	0.0000		
Act. Gas Flow	(ACFM)	1054	1054	---		
Avg. Liq. Density	(lbmole/ft3)	1.012	1.012	0.8170		
Specific Heat	(Btu/lbmole-F)	18.04	18.04	25.91		
Std. Gas Flow	(MMSCFD)	180.1	180.1	0.0000		
Std. Ideal Liq. Mass Density	(lb/ft3)	21.89	21.89	27.41		
Act. Liq. Flow	(barrel/day)	---	---	---		
Z Factor		---	0.6506	0.2863		
Watson K		17.89	17.89	15.83		
User Property		---	---	---		
Cp/(Cp - R)		1.124	1.124	1.083		
Cp/Cv		2.116	2.116	1.083		
Heat of Vap.	(Btu/lbmole)	2615	---	---		
Kinematic Viscosity	(cSt)	0.1372	0.1372	0.1694		
Liq. Mass Density (Std. Cond)	(lb/ft3)	5.734e-002	5.734e-002	22.83		
Liq. Vol. Flow (Std. Cond)	(barrel/day)	3.193e+007	3.193e+007	0.0000		
Liquid Fraction		0.0000	0.0000	1.000		
Molar Volume	(ft3/lbmole)	3.192	3.192	1.405		
Mass Heat of Vap.	(Btu/lb)	120.9	---	---		
Phase Fraction [Molar Basis]		1.0000	1.0000	0.0000		
Surface Tension	(dyne/cm)	---	---	4.888		
Thermal Conductivity	(Btu/hr-ft-F)	2.300e-002	2.300e-002	4.862e-002		
Viscosity	(cP)	1.489e-002	1.489e-002	6.480e-002		
Cv (Semi-Ideal)	(Btu/lbmole-F)	16.05	16.05	23.93		
Mass Cv (Semi-Ideal)	(Btu/lb-F)	0.7424	0.7424	0.7130		

* Specified by user.

Material Stream: Gas Inlet (continued)

Fluid Package: Peng Robinson

Property Package: Peng-Robinson

PROPERTIES

	Overall	Vapour Phase	Liquid Phase		
Cv (Btu/lbmole-F)	8.525	8.525	23.93		
Mass Cv (Btu/lb-F)	0.3943	0.3943	0.7130		
Cv (Ent. Method) (Btu/lbmole-F)	8.526	8.526	---		
Mass Cv (Ent. Method) (Btu/lb-F)	0.3943	0.3943	---		
Cp/Cv (Ent. Method)	2.116	2.116	---		
Liq. Vol. Flow - Sum(Std. Cond) (barrel/day)	3.193e+007	3.193e+007	0.0000		
Partial Pressure of H2S (psig)	-14.70	---	---		
Reid VP at 37.8 C (psig)	---	---	745.1		
True VP at 37.8 C (psig)	---	---	1296		
Viscosity Index	---	---	---		
HHV Molar Basis (Std) (Btu/SCF)	---	---	---		
HHV Mass Basis (Std) (Btu/lb)	---	---	---		
CO2 Loading	---	---	---		
CO2 Apparent Mole Conc. (lbmole/ft3)	---	---	---		
CO2 Apparent Wt. Conc. (lbmol/lb)	---	---	---		
Phase Fraction [Act. Vol. Basis]	1.000	1.000	0.0000		
Mass Exergy (Btu/lb)	199.5	---	---		
Ideal Gas Cp/Cv	1.247	1.247	1.167		
Ideal Gas Cp (Btu/lbmole-F)	10.04	10.04	13.90		
Mass Ideal Gas Cp (Btu/lb-F)	0.4643	0.4643	0.4142		
Bubble Point Pressure (psig)	---	---	---		
CO2E-AR4[Gas] (lb/hr)	5.842e+006	5.842e+006	0.0000		
CO2E-SAR[Gas] (lb/hr)	4.907e+006	4.907e+006	0.0000		
CO2E-US[Gas] (lb/hr)	4.907e+006	4.907e+006	0.0000		
HC Dew Point[Gas] (F)	50.01	50.01	190.9		
HHV Mass Basis[Gas] (Btu/lb)	2.248e+004	2.248e+004	2.192e+004		
HHV Molar Basis[Gas] (Btu/lbmole)	4.861e+005	4.861e+005	7.355e+005		
HHV Vol. Basis[Gas] (MMBtu/gal)	1.722e-004	1.722e-004	2.624e-004		
LHV Mass Basis[Gas] (Btu/lb)	2.041e+004	2.041e+004	2.008e+004		
LHV Molar Basis[Gas] (Btu/lbmole)	4.413e+005	4.413e+005	6.739e+005		
LHV Vol. Basis[Gas] (MMBtu/gal)	1.563e-004	1.563e-004	2.404e-004		
Mass Density (Std. Cond)[Gas] (lb/ft3)	5.731e-002	5.731e-002	8.953e-002		
Water Content[Gas] (lb/MMSCF)	7.032	7.032	6.435		
Water Dew Point[Gas] (F)	37.33	37.33	35.81		
Wobbe Index[Gas] (MMBtu/gal)	1.990e-004	1.990e-004	2.425e-004		

COMPOSITION

Overall Phase

Vapour Fraction 1.0000

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Oxygen	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2S	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nitrogen	315.3253	0.0159	8833.3007	0.0206	750.0673	0.0090
CO2	22.4726	0.0011	989.0232	0.0023	82.0521	0.0010
Methane	14562.7148	0.7352	233630.6163	0.5454	53431.8717	0.6389
Ethane	2915.7957	0.1472	87678.6010	0.2047	16878.9035	0.2018
Propane	1429.3947	0.0722	63032.6777	0.1472	8518.1924	0.1018
i-Butane	143.3569	0.0072	8332.5659	0.0195	1015.2721	0.0121
n-Butane	321.4514	0.0162	18684.2381	0.0436	2193.5850	0.0262
22-Mpropane	1.3711	0.0001	98.9286	0.0002	11.3733	0.0001

* Specified by user.

Material Stream: Gas Inlet (continued)

Fluid Package: Peng Robinson
Property Package: Peng-Robinson

COMPOSITION

Overall Phase (continued)

Vapour Fraction 1.0000

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
i-Pentane	41.2817	0.0021	2978.5436	0.0070	327.1309	0.0039
n-Pentane	37.9670	0.0019	2739.3848	0.0064	297.8606	0.0036
22-Mbutane	0.1549	0.0000	13.3488	0.0000	1.4007	0.0000
Cyclopentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
23-Mbutane	0.9444	0.0000	81.3907	0.0002	8.3783	0.0001
2-Mpentane	3.2825	0.0002	282.8856	0.0007	29.5043	0.0004
3-Mpentane	1.5539	0.0001	133.9124	0.0003	13.7329	0.0002
n-Hexane	3.1176	0.0002	268.6703	0.0006	27.7613	0.0003
Hexanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Mcyclopentan	1.8170	0.0001	152.9251	0.0004	13.9231	0.0002
Benzene	0.3936	0.0000	30.7423	0.0001	2.3861	0.0000
Cyclohexane	1.7924	0.0001	150.8526	0.0004	13.2117	0.0002
2-Mhexane	0.1857	0.0000	18.6047	0.0000	1.8692	0.0000
3-Mhexane	0.1642	0.0000	16.4506	0.0000	1.6320	0.0000
224-Mpentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Heptane	0.2477	0.0000	24.8225	0.0001	2.4747	0.0000
Heptanes*	0.3073	0.0000	29.5023	0.0001	2.7843	0.0000
Mcyclohexane	0.5319	0.0000	52.2288	0.0001	4.6298	0.0001
Toluene	0.0770	0.0000	7.0990	0.0000	0.5587	0.0000
n-Octane	0.0121	0.0000	1.3813	0.0000	0.1341	0.0000
Octanes*	0.0995	0.0000	10.6444	0.0000	0.9751	0.0000
E-Benzene	0.0007	0.0000	0.0770	0.0000	0.0061	0.0000
m-Xylene	0.0013	0.0000	0.1368	0.0000	0.0108	0.0000
o-Xylene	0.0013	0.0000	0.1384	0.0000	0.0107	0.0000
p-Xylene	0.0013	0.0000	0.1397	0.0000	0.0111	0.0000
Nonanes*	0.0052	0.0000	0.6316	0.0000	0.0564	0.0000
Decanes*	0.0003	0.0000	0.0370	0.0000	0.0032	0.0000
Undecanes_3*	0.0000	0.0000	0.0018	0.0000	0.0002	0.0000
Dodecanes_3*	0.0000	0.0000	0.0001	0.0000	0.0000	0.0000
Triadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Tetradecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Pentadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
eicosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heneicosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Dodocosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Tetracosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Pentacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacontanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C31+_2*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000

* Specified by user.

Material Stream: Gas Inlet (continued)

Fluid Package: Peng Robinson
Property Package: Peng-Robinson

COMPOSITION

Overall Phase (continued)

Vapour Fraction 1.0000

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
H2O	2.9397	0.0001	52.9599	0.0001	3.6336	0.0000
NC30*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Nonane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Decane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC31-35*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TexaTherm	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC31-35_1*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
CO	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TEGlycol	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
SO2	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C10+ (SS1H)*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
464H C7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
474Y c7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Total	19808.7630	1.0000	428327.4632	1.0000	83635.3974	1.0000

Vapour Phase

Phase Fraction 1.000

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Oxygen	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2S	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nitrogen	315.3253	0.0159	8833.3007	0.0206	750.0673	0.0090
CO2	22.4726	0.0011	989.0232	0.0023	82.0521	0.0010
Methane	14562.7148	0.7352	233630.6163	0.5454	53431.8717	0.6389
Ethane	2915.7957	0.1472	87678.6010	0.2047	16878.9035	0.2018
Propane	1429.3947	0.0722	63032.6777	0.1472	8518.1924	0.1018
i-Butane	143.3569	0.0072	8332.5659	0.0195	1015.2721	0.0121
n-Butane	321.4514	0.0162	18684.2381	0.0436	2193.5850	0.0262
22-Mpropane	1.3711	0.0001	98.9286	0.0002	11.3733	0.0001
i-Pentane	41.2817	0.0021	2978.5436	0.0070	327.1309	0.0039
n-Pentane	37.9670	0.0019	2739.3848	0.0064	297.8606	0.0036
22-Mbutane	0.1549	0.0000	13.3488	0.0000	1.4007	0.0000
Cyclopentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
23-Mbutane	0.9444	0.0000	81.3907	0.0002	8.3783	0.0001
2-Mpentane	3.2825	0.0002	282.8856	0.0007	29.5043	0.0004
3-Mpentane	1.5539	0.0001	133.9124	0.0003	13.7329	0.0002
n-Hexane	3.1176	0.0002	268.6703	0.0006	27.7613	0.0003
Hexanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Mcyclopentan	1.8170	0.0001	152.9251	0.0004	13.9231	0.0002
Benzene	0.3936	0.0000	30.7423	0.0001	2.3861	0.0000
Cyclohexane	1.7924	0.0001	150.8526	0.0004	13.2117	0.0002
2-Mhexane	0.1857	0.0000	18.6047	0.0000	1.8692	0.0000
3-Mhexane	0.1642	0.0000	16.4506	0.0000	1.6320	0.0000
224-Mpentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Heptane	0.2477	0.0000	24.8225	0.0001	2.4747	0.0000
Heptanes*	0.3073	0.0000	29.5023	0.0001	2.7843	0.0000
Mcyclohexane	0.5319	0.0000	52.2288	0.0001	4.6298	0.0001
Toluene	0.0770	0.0000	7.0990	0.0000	0.5587	0.0000
n-Octane	0.0121	0.0000	1.3813	0.0000	0.1341	0.0000

* Specified by user.

Material Stream: Gas Inlet (continued)

Fluid Package: Peng Robinson

Property Package: Peng-Robinson

COMPOSITION

Vapour Phase (continued)

Phase Fraction 1.000

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Octanes*	0.0995	0.0000	10.6444	0.0000	0.9751	0.0000
E-Benzene	0.0007	0.0000	0.0770	0.0000	0.0061	0.0000
m-Xylene	0.0013	0.0000	0.1368	0.0000	0.0108	0.0000
o-Xylene	0.0013	0.0000	0.1384	0.0000	0.0107	0.0000
p-Xylene	0.0013	0.0000	0.1397	0.0000	0.0111	0.0000
Nonanes*	0.0052	0.0000	0.6316	0.0000	0.0564	0.0000
Decanes*	0.0003	0.0000	0.0370	0.0000	0.0032	0.0000
Undecanes_3*	0.0000	0.0000	0.0018	0.0000	0.0002	0.0000
Dodecanes_3*	0.0000	0.0000	0.0001	0.0000	0.0000	0.0000
Triadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Tetradecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Pentadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
eicosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heneicosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Dodocosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Tetracosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Pentacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacontanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C31+_2*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2O	2.9397	0.0001	52.9599	0.0001	3.6336	0.0000
NC30*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Nonane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Decane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC31-35*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TexaTherm	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC31-35_1*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
CO	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TEGlycol	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
SO2	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C10+ (SS1H)*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
464H C7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
474Y c7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Total	19808.7630	1.0000	428327.4632	1.0000	83635.3974	1.0000

Liquid Phase

Phase Fraction 0.0000

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Oxygen	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2S	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000

* Specified by user.

Material Stream: Gas Inlet (continued)

Fluid Package: Peng Robinson
Property Package: Peng-Robinson

COMPOSITION

Liquid Phase (continued)

Phase Fraction 0.0000

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Nitrogen	0.0000	0.0045	0.0000	0.0037	0.0000	0.0020
CO2	0.0000	0.0010	0.0000	0.0013	0.0000	0.0007
Methane	0.0000	0.3972	0.0000	0.1899	0.0000	0.2786
Ethane	0.0000	0.2084	0.0000	0.1867	0.0000	0.2305
Propane	0.0000	0.2062	0.0000	0.2709	0.0000	0.2348
i-Butane	0.0000	0.0338	0.0000	0.0585	0.0000	0.0457
n-Butane	0.0000	0.0925	0.0000	0.1601	0.0000	0.1206
22-Mpropane	0.0000	0.0005	0.0000	0.0010	0.0000	0.0007
i-Pentane	0.0000	0.0193	0.0000	0.0415	0.0000	0.0292
n-Pentane	0.0000	0.0209	0.0000	0.0450	0.0000	0.0314
22-Mbutane	0.0000	0.0001	0.0000	0.0003	0.0000	0.0002
Cyclopentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
23-Mbutane	0.0000	0.0008	0.0000	0.0020	0.0000	0.0013
2-Mpentane	0.0000	0.0028	0.0000	0.0072	0.0000	0.0048
3-Mpentane	0.0000	0.0014	0.0000	0.0036	0.0000	0.0024
n-Hexane	0.0000	0.0032	0.0000	0.0082	0.0000	0.0055
Hexanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Mcyclopentan	0.0000	0.0020	0.0000	0.0049	0.0000	0.0029
Benzene	0.0000	0.0004	0.0000	0.0010	0.0000	0.0005
Cyclohexane	0.0000	0.0020	0.0000	0.0051	0.0000	0.0029
2-Mhexane	0.0000	0.0003	0.0000	0.0009	0.0000	0.0006
3-Mhexane	0.0000	0.0003	0.0000	0.0008	0.0000	0.0005
224-Mpentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Heptane	0.0000	0.0005	0.0000	0.0014	0.0000	0.0009
Heptanes*	0.0000	0.0005	0.0000	0.0015	0.0000	0.0009
Mcyclohexane	0.0000	0.0009	0.0000	0.0027	0.0000	0.0016
Toluene	0.0000	0.0001	0.0000	0.0004	0.0000	0.0002
n-Octane	0.0000	0.0000	0.0000	0.0001	0.0000	0.0001
Octanes*	0.0000	0.0003	0.0000	0.0009	0.0000	0.0005
E-Benzene	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
m-Xylene	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
o-Xylene	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
p-Xylene	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonanes*	0.0000	0.0000	0.0000	0.0001	0.0000	0.0001
Decanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Undecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Dodecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Tetradecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Pentadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
eicosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heneicosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Dodocosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000

* Specified by user.

Material Stream: Gas Inlet (continued)

Fluid Package: Peng Robinson
Property Package: Peng-Robinson

COMPOSITION

Liquid Phase (continued)

Phase Fraction 0.0000

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Tetracosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Pentacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacontanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C31+_2*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2O	0.0000	0.0001	0.0000	0.0001	0.0000	0.0000
NC30*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Nonane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Decane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC31-35*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TexaTherm	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC31-35_1*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
CO	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TEGlycol	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
SO2	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C10+ (SS1H)*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
464H C7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
474Y c7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Total	0.0000	1.0000	0.0000	1.0000	0.0000	1.0000

* Specified by user.

XTO ENERGY INC.
Cowboy CDP
PROCESS SIMULATION COMPONENTS

PROCESS SIMULATION COMPONENTS - IFR TANKS INLET OIL

HYSYS PROCESS STREAM NAME:	Oil prod to tanks
HYSYS COMPONENTS	
Component	**Mole Frac**
Oxygen	0.000
H2S	0.000
Nitrogen	0.000
CO2	0.000
Methane	0.000
Ethane	0.003
Propane	0.013
i-Butane	0.012
n-Butane	0.048
22-Mpropane	0.001
i-Pentane	0.033
n-Pentane	0.047
22-Mbutane	0.001
Cyclopentane	0.000
23-Mbutane	0.006
2-Mpentane	0.018
3-Mpentane	0.011
n-Hexane	0.028
Hexanes*	0.000
Mcyclopentan	0.022
Benzene	0.021
Cyclohexane	0.049
2-Mhexane	0.009
3-Mhexane	0.009
224-Mpentane	0.000
n-Heptane	0.038
Heptanes*	0.001
Mcyclohexane	0.058
Toluene	0.035
n-Octane	0.068
Octanes*	0.002
E-Benzene	0.002
m-Xylene	0.009
o-Xylene	0.005
p-Xylene	0.009
Nonanes*	0.001
Decanes*	0.000
Undecanes_3*	0.042
Dodecanes_3*	0.030
Triadecanes_3*	0.032
Tetradecanes_3*	0.027
Pentadecanes_3*	0.024
Hexadecanes_3*	0.017
Heptadecanes_3*	0.014
Octadecanes_3*	0.013
Nonadecanes_3*	0.012
eicosanes_3*	0.008
Heneicosanes_3*	0.008
Dodocosanes_3*	0.007
Triacosanes_3*	0.006
Tetracosanes_3*	0.005
Pentacosanes_3*	0.004
Hexacosanes_3*	0.004
Heptacosanes_3*	0.004
Octacosanes_3*	0.004
Nonacosanes_3*	0.003
Triacontanes*	0.000
C31+_2*	0.058
H2O	0.000
NC30*	0.003
n-Nonane	0.061
n-Decane	0.058
NC31-35*	0.000
TexaTherm	0.000
NC31-35_1*	0.000
CO	0.000
TOTALS	1.000

Promax PROCESS STREAM NAME:	IFR Inlet 50,000 bbl IFR Inlet 250,000 bbl
PROMAX COMPONENTS	
Component	**Mole Frac**
Water	0.00015
Hydrogen Sulfide	0.00000
Nitrogen	0.00000
Carbon Dioxide	0.00001
Methane	0.00000
Ethane	0.00255
Propane	0.01252
Iso-butane	0.01218
N-butane	0.04830
Iso-pentane	0.03253
N-pentane	0.04661
Cyclopentanes	0.00000
Other Hexanes	0.03628
n-Hexane	0.02844
Methylcyclopentane	0.02229
Benzene	0.02097
Cyclohexane	0.04914
2,2,4 Trimethylpentane	0.00000
Other Heptanes	0.01916
Methylcyclohexane	0.05789
n-Heptane	0.03847
Toluene	0.03458
Octanes	0.06987
Ethylbenzene	0.00190
M&P-Xylene	0.02196
Nonanes	0.06475
Decanes	0.05869
Undecanes	0.32075
Total	1.000

Characteristics of Undecanes Plus	
Specific Gravity	0.8661
Molecular Weight (lb/lbmol)	262.912
VOC WT%	0.00
HAP WT%	0.000

Material Stream: oil prod to tanks

Fluid Package: Peng Robinson

Property Package: Peng-Robinson

CONDITIONS

		Overall	Liquid Phase			
Vapour / Phase Fraction		0.0000	1.0000			
Temperature:	(F)	92.69	92.69			
Pressure:	(psig)	30.00	30.00			
Molar Flow	(MMSCFD)	69.50	69.50			
Mass Flow	(lb/hr)	1.169e+006	1.169e+006			
Std Ideal Liq Vol Flow	(barrel/day)	1.005e+005	1.005e+005			
Molar Enthalpy	(Btu/lbmole)	-1.335e+005	-1.335e+005			
Molar Entropy	(Btu/lbmole-F)	57.35	57.35			
Heat Flow	(Btu/hr)	-1.019e+009	-1.019e+009			
Liq Vol Flow @Std Cond	(barrel/day)	1.002e+005 *	1.002e+005			

PROPERTIES

		Overall	Liquid Phase			
Molecular Weight		153.1	153.1			
Molar Density	(lbmole/ft3)	0.3193	0.3193			
Mass Density	(lb/ft3)	48.90	48.90			
Act. Volume Flow	(barrel/day)	1.022e+005	1.022e+005			
Mass Enthalpy	(Btu/lb)	-871.6	-871.6			
Mass Entropy	(Btu/lb-F)	0.3745	0.3745			
Heat Capacity	(Btu/lbmole-F)	72.55	72.55			
Mass Heat Capacity	(Btu/lb-F)	0.4738	0.4738			
LHV Molar Basis (Std)	(Btu/SCF)	---	---			
LHV Mass Basis (Std)	(Btu/lb)	---	---			
Phase Fraction [Vol. Basis]		0.0000	1.000			
Phase Fraction [Mass Basis]		0.0000	1.000			
Partial Pressure of CO2	(psig)	-14.70	---			
Cost Based on Flow	(Cost/s)	0.0000	0.0000			
Act. Gas Flow	(ACFM)	---	---			
Avg. Liq. Density	(lbmole/ft3)	0.3245	0.3245			
Specific Heat	(Btu/lbmole-F)	72.55	72.55			
Std. Gas Flow	(MMSCFD)	69.37	69.37			
Std. Ideal Liq. Mass Density	(lb/ft3)	49.69	49.69			
Act. Liq. Flow	(barrel/day)	1.022e+005	1.022e+005			
Z Factor		2.361e-002	2.361e-002			
Watson K		11.85	11.85			
User Property		---	---			
Cp/(Cp - R)		1.028	1.028			
Cp/Cv		1.213	1.213			
Heat of Vap.	(Btu/lbmole)	7.710e+004	---			
Kinematic Viscosity	(cSt)	2.300	2.300			
Liq. Mass Density (Std. Cond)	(lb/ft3)	49.83	49.83			
Liq. Vol. Flow (Std. Cond)	(barrel/day)	1.002e+005	1.002e+005			
Liquid Fraction		1.000	1.000			
Molar Volume	(ft3/lbmole)	3.131	3.131			
Mass Heat of Vap.	(Btu/lb)	503.5	---			
Phase Fraction [Molar Basis]		0.0000	1.0000			
Surface Tension	(dyne/cm)	22.01	22.01			
Thermal Conductivity	(Btu/hr-ft-F)	6.865e-002	6.865e-002			
Viscosity	(cP)	1.802	1.802			
Cv (Semi-Ideal)	(Btu/lbmole-F)	70.56	70.56			
Mass Cv (Semi-Ideal)	(Btu/lb-F)	0.4608	0.4608			

* Specified by user.

Material Stream: oil prod to tanks (continued)

Fluid Package: Peng Robinson
Property Package: Peng-Robinson

PROPERTIES

	Overall	Liquid Phase			
Cv (Btu/lbmole-F)	59.79	59.79			
Mass Cv (Btu/lb-F)	0.3905	0.3905			
Cv (Ent. Method) (Btu/lbmole-F)	63.71	63.71			
Mass Cv (Ent. Method) (Btu/lb-F)	0.4161	0.4161			
Cp/Cv (Ent. Method)	1.139	1.139			
Liq. Vol. Flow - Sum(Std. Cond) (barrel/day)	1.002e+005	1.002e+005			
Partial Pressure of H2S (psig)	-14.70	---			
Reid VP at 37.8 C (psig)	-6.225	-6.225			
True VP at 37.8 C (psig)	-4.010	-4.010			
Viscosity Index	12.77	---			
HHV Molar Basis (Std) (Btu/SCF)	---	---			
HHV Mass Basis (Std) (Btu/lb)	---	---			
CO2 Loading	---	---			
CO2 Apparent Mole Conc. (lbmole/ft3)	2.822e-006	2.822e-006			
CO2 Apparent Wt. Conc. (lbmol/lb)	5.770e-008	5.770e-008			
Phase Fraction [Act. Vol. Basis]	0.0000	1.000			
Mass Exergy (Btu/lb)	0.2308	---			
Ideal Gas Cp/Cv	1.035	1.035			
Ideal Gas Cp (Btu/lbmole-F)	58.34	58.34			
Mass Ideal Gas Cp (Btu/lb-F)	0.3810	0.3810			
Bubble Point Pressure (psig)	-5.041	---			
API[Petrol]	46.11	---			
SG (60/60)[Petrol]	0.7967	---			
Std. Liquid Density[Petrol] (lb/ft3)	49.69	---			
TBP 0%[Petrol] (F)	-213.2	---			
TBP 5%[Petrol] (F)	83.35	---			
TBP 10%[Petrol] (F)	142.2	---			
TBP 30%[Petrol] (F)	255.9	---			
TBP 50%[Petrol] (F)	378.7	---			
TBP 70%[Petrol] (F)	613.0	---			
TBP 90%[Petrol] (F)	990.2	---			
TBP 95%[Petrol] (F)	1035	---			
TBP 100%[Petrol] (F)	1069	---			
D86 IBP[Petrol] (F)	---	---			
D86 5%[Petrol] (F)	159.3	---			
D86 10%[Petrol] (F)	190.5	---			
D86 30%[Petrol] (F)	271.0	---			
D86 50%[Petrol] (F)	372.8	---			
D86 70%[Petrol] (F)	623.3	---			
D86 90%[Petrol] (F)	1216	---			
D86 95%[Petrol] (F)	1252	---			
D86 FBP[Petrol] (F)	1266	---			
Sulfur Wt Pct[Petrol] (%)	---	---			
Nitrogen Content[Petrol] (ppmwt)	---	---			
Basic Nitrogen Content[Petrol] (ppmwt)	---	---			
Conradson Carbon Content[Petrol] (%)	---	---			
RON (Clear)[Petrol]	---	---			
MON (Clear)[Petrol]	---	---			
Cetane Idx D4737[Petrol]	-27.11	---			
Kinematic Viscosity @ X C[Petrol] (cSt)	2.153	---			
Reid Vapour Pressure[Petrol] (psig)	-4.745	---			

* Specified by user.

Material Stream: oil prod to tanks (continued)

Fluid Package: Peng Robinson

Property Package: Peng-Robinson

PROPERTIES

		Overall	Liquid Phase			
Flash Point[Petrol]	(F)	7.431	---			
Cloud Point[Petrol]	(F)	-59.24	---			
Pour Point[Petrol]	(F)	---	---			
Aniline Point[Petrol]	(F)	-235.7	---			
Paraffins by Volume[Petrol]	(%)	---	---			
Olefins by Volume[Petrol]	(%)	---	---			
Naphthenes by Volume[Petrol]	(%)	---	---			
Aromatics by Volume[Petrol]	(%)	---	---			

COMPOSITION

Overall Phase

Vapour Fraction 0.0000

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Oxygen	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2S	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nitrogen	0.0000	0.0000	0.0001	0.0000	0.0000	0.0000
CO2	0.0674	0.0000	2.9676	0.0000	0.2462	0.0000
Methane	0.0248	0.0000	0.3974	0.0000	0.0909	0.0000
Ethane	19.4522	0.0025	584.9332	0.0005	112.6048	0.0011
Propane	95.5485	0.0125	4213.4445	0.0036	569.4020	0.0057
i-Butane	92.9320	0.0122	5401.6387	0.0046	658.1566	0.0065
n-Butane	368.6291	0.0483	21426.4231	0.0183	2515.5257	0.0250
22-Mpropane	4.3786	0.0006	315.9201	0.0003	36.3196	0.0004
i-Pentane	248.2642	0.0325	17912.6979	0.0153	1967.3366	0.0196
n-Pentane	355.7096	0.0466	25665.0722	0.0220	2790.6318	0.0278
22-Mbutane	3.8194	0.0005	329.1484	0.0003	34.5368	0.0003
Cyclopentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
23-Mbutane	48.2206	0.0063	4155.5931	0.0036	427.7750	0.0043
2-Mpentane	138.0094	0.0181	11893.4825	0.0102	1240.4618	0.0123
3-Mpentane	82.4365	0.0108	7104.2803	0.0061	728.5558	0.0072
n-Hexane	217.0512	0.0284	18705.2097	0.0160	1932.7823	0.0192
Hexanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Mcyclopentan	170.0998	0.0223	14316.0705	0.0122	1303.4134	0.0130
Benzene	160.0302	0.0210	12500.0895	0.0107	970.2077	0.0096
Cyclohexane	375.0150	0.0491	31561.5939	0.0270	2764.1701	0.0275
2-Mhexane	71.6377	0.0094	7178.5299	0.0061	721.2047	0.0072
3-Mhexane	65.1386	0.0085	6527.2783	0.0056	647.5464	0.0064
224-Mpentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Heptane	293.6061	0.0385	29421.1045	0.0252	2933.1410	0.0292
Heptanes*	9.4716	0.0012	909.2825	0.0008	85.8130	0.0009
Mcyclohexane	441.8170	0.0579	43382.0213	0.0371	3845.6174	0.0382
Toluene	263.9275	0.0346	24318.7424	0.0208	1913.8753	0.0190
n-Octane	521.5489	0.0683	59578.1964	0.0510	5783.3542	0.0575
Octanes*	11.7076	0.0015	1252.7314	0.0011	114.7532	0.0011
E-Benzene	14.4646	0.0019	1535.6694	0.0013	120.8581	0.0012
m-Xylene	65.3032	0.0086	6933.0555	0.0059	547.6189	0.0054
o-Xylene	36.9521	0.0048	3923.0937	0.0034	304.1658	0.0030
p-Xylene	65.3040	0.0086	6933.1387	0.0059	549.3066	0.0055
Nonanes*	4.1344	0.0005	500.2732	0.0004	44.6925	0.0004
Decanes*	1.4735	0.0002	197.4553	0.0002	17.3241	0.0002

* Specified by user.

Material Stream: oil prod to tanks (continued)

Fluid Package: Peng Robinson
Property Package: Peng-Robinson

COMPOSITION

Overall Phase (continued)

Vapour Fraction 0.0000

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Undecanes_3*	322.2860	0.0422	47376.5329	0.0405	4096.3839	0.0407
Dodecanes_3*	227.9376	0.0299	36698.3413	0.0314	3128.7310	0.0311
Triadecanes_3*	243.1504	0.0319	42551.7648	0.0364	3584.0395	0.0356
Tetradecanes_3*	204.1308	0.0267	38785.2624	0.0332	3229.8081	0.0321
Pentadecanes_3*	179.6583	0.0235	37009.9953	0.0317	3049.0950	0.0303
Hexadecanes_3*	127.6705	0.0167	28343.1517	0.0243	2313.0896	0.0230
Heptadecanes_3*	107.0287	0.0140	25366.0606	0.0217	2052.7164	0.0204
Octadecanes_3*	100.9126	0.0132	25329.3202	0.0217	2035.1341	0.0202
Nonadecanes_3*	94.0321	0.0123	24730.7024	0.0212	1975.2181	0.0196
eicosanes_3*	61.7707	0.0081	16987.1121	0.0145	1348.9506	0.0134
Heneicosanes_3*	61.7707	0.0081	17975.4496	0.0154	1417.2547	0.0141
Dodocosanes_3*	49.8446	0.0065	14953.5479	0.0128	1174.0353	0.0117
Triacosanes_3*	44.3403	0.0058	13834.3249	0.0118	1080.4847	0.0107
Tetracosanes_3*	37.9951	0.0050	12310.5307	0.0105	956.7409	0.0095
Pentacosanes_3*	32.4908	0.0043	10949.4979	0.0094	846.7528	0.0084
Hexacosanes_3*	30.8853	0.0040	10779.0917	0.0092	829.7407	0.0083
Heptacosanes_3*	30.1208	0.0039	10843.6151	0.0093	831.2572	0.0083
Octacosanes_3*	27.6745	0.0036	10295.0126	0.0088	785.9342	0.0078
Nonacosanes_3*	24.5401	0.0032	9374.4062	0.0080	713.2597	0.0071
Triacontanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C31+_2*	439.5808	0.0576	230782.3119	0.1975	16944.3857	0.1685
H2O	1.1664	0.0002	21.0124	0.0000	1.4417	0.0000
NC30*	25.3046	0.0033	11564.3057	0.0099	861.5560	0.0086
n-Nonane	464.7155	0.0609	59604.5688	0.0510	5666.4600	0.0564
n-Decane	446.4277	0.0585	63520.6345	0.0544	5935.9458	0.0590
NC31-35*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TexaTherm	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC31-35_1*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
CO	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TEGlycol	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
SO2	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C10+ (SS1H)*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
464H C7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
474Y c7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Total	7631.6101	1.0000	1.168666089e+06	1.0000	100539.9041	1.0000

Liquid Phase

Phase Fraction 1.000

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Oxygen	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2S	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nitrogen	0.0000	0.0000	0.0001	0.0000	0.0000	0.0000
CO2	0.0674	0.0000	2.9676	0.0000	0.2462	0.0000
Methane	0.0248	0.0000	0.3974	0.0000	0.0909	0.0000
Ethane	19.4522	0.0025	584.9332	0.0005	112.6048	0.0011
Propane	95.5485	0.0125	4213.4445	0.0036	569.4020	0.0057
i-Butane	92.9320	0.0122	5401.6387	0.0046	658.1566	0.0065
n-Butane	368.6291	0.0483	21426.4231	0.0183	2515.5257	0.0250

* Specified by user.

Material Stream: oil prod to tanks (continued)

Fluid Package: Peng Robinson
Property Package: Peng-Robinson

COMPOSITION

Liquid Phase (continued)

Phase Fraction 1.000

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
22-Mpropane	4.3786	0.0006	315.9201	0.0003	36.3196	0.0004
i-Pentane	248.2642	0.0325	17912.6979	0.0153	1967.3366	0.0196
n-Pentane	355.7096	0.0466	25665.0722	0.0220	2790.6318	0.0278
22-Mbutane	3.8194	0.0005	329.1484	0.0003	34.5368	0.0003
Cyclopentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
23-Mbutane	48.2206	0.0063	4155.5931	0.0036	427.7750	0.0043
2-Mpentane	138.0094	0.0181	11893.4825	0.0102	1240.4618	0.0123
3-Mpentane	82.4365	0.0108	7104.2803	0.0061	728.5558	0.0072
n-Hexane	217.0512	0.0284	18705.2097	0.0160	1932.7823	0.0192
Hexanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Mcyclopentan	170.0998	0.0223	14316.0705	0.0122	1303.4134	0.0130
Benzene	160.0302	0.0210	12500.0895	0.0107	970.2077	0.0096
Cyclohexane	375.0150	0.0491	31561.5939	0.0270	2764.1701	0.0275
2-Mhexane	71.6377	0.0094	7178.5299	0.0061	721.2047	0.0072
3-Mhexane	65.1386	0.0085	6527.2783	0.0056	647.5464	0.0064
224-Mpentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Heptane	293.6061	0.0385	29421.1045	0.0252	2933.1410	0.0292
Heptanes*	9.4716	0.0012	909.2825	0.0008	85.8130	0.0009
Mcyclohexane	441.8170	0.0579	43382.0213	0.0371	3845.6174	0.0382
Toluene	263.9275	0.0346	24318.7424	0.0208	1913.8753	0.0190
n-Octane	521.5489	0.0683	59578.1964	0.0510	5783.3542	0.0575
Octanes*	11.7076	0.0015	1252.7314	0.0011	114.7532	0.0011
E-Benzene	14.4646	0.0019	1535.6694	0.0013	120.8581	0.0012
m-Xylene	65.3032	0.0086	6933.0555	0.0059	547.6189	0.0054
o-Xylene	36.9521	0.0048	3923.0937	0.0034	304.1658	0.0030
p-Xylene	65.3040	0.0086	6933.1387	0.0059	549.3066	0.0055
Nonanes*	4.1344	0.0005	500.2732	0.0004	44.6925	0.0004
Decanes*	1.4735	0.0002	197.4553	0.0002	17.3241	0.0002
Undecanes_3*	322.2860	0.0422	47376.5329	0.0405	4096.3839	0.0407
Dodecanes_3*	227.9376	0.0299	36698.3413	0.0314	3128.7310	0.0311
Triadecanes_3*	243.1504	0.0319	42551.7648	0.0364	3584.0395	0.0356
Tetradecanes_3*	204.1308	0.0267	38785.2624	0.0332	3229.8081	0.0321
Pentadecanes_3*	179.6583	0.0235	37009.9953	0.0317	3049.0950	0.0303
Hexadecanes_3*	127.6705	0.0167	28343.1517	0.0243	2313.0896	0.0230
Heptadecanes_3*	107.0287	0.0140	25366.0606	0.0217	2052.7164	0.0204
Octadecanes_3*	100.9126	0.0132	25329.3202	0.0217	2035.1341	0.0202
Nonadecanes_3*	94.0321	0.0123	24730.7024	0.0212	1975.2181	0.0196
eicosanes_3*	61.7707	0.0081	16987.1121	0.0145	1348.9506	0.0134
Heneicosanes_3*	61.7707	0.0081	17975.4496	0.0154	1417.2547	0.0141
Dodocosanes_3*	49.8446	0.0065	14953.5479	0.0128	1174.0353	0.0117
Triacosanes_3*	44.3403	0.0058	13834.3249	0.0118	1080.4847	0.0107
Tetracosanes_3*	37.9951	0.0050	12310.5307	0.0105	956.7409	0.0095
Pentacosanes_3*	32.4908	0.0043	10949.4979	0.0094	846.7528	0.0084
Hexacosanes_3*	30.8853	0.0040	10779.0917	0.0092	829.7407	0.0083
Heptacosanes_3*	30.1208	0.0039	10843.6151	0.0093	831.2572	0.0083
Octacosanes_3*	27.6745	0.0036	10295.0126	0.0088	785.9342	0.0078
Nonacosanes_3*	24.5401	0.0032	9374.4062	0.0080	713.2597	0.0071
Triacontanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000

* Specified by user.

Material Stream: oil prod to tanks (continued)

Fluid Package: Peng Robinson
Property Package: Peng-Robinson

COMPOSITION

Liquid Phase (continued)

Phase Fraction 1.000

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
C31+_2*	439.5808	0.0576	230782.3119	0.1975	16944.3857	0.1685
H2O	1.1664	0.0002	21.0124	0.0000	1.4417	0.0000
NC30*	25.3046	0.0033	11564.3057	0.0099	861.5560	0.0086
n-Nonane	464.7155	0.0609	59604.5688	0.0510	5666.4600	0.0564
n-Decane	446.4277	0.0585	63520.6345	0.0544	5935.9458	0.0590
NC31-35*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TexaTherm	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC31-35_1*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
CO	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TEGlycol	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
SO2	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C10+ (SS1H)*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
464H C7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
474Y c7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Total	7631.6101	1.0000	1.168666089e+06	1.0000	100539.9041	1.0000

* Specified by user.

XTO ENERGY INC.
Cowboy CDP
PROCESS SIMULATION COMPONENTS

PROCESS SIMULATION COMPONENTS - DRAIN VESSEL OUTLET OIL

HYSYS PROCESS STREAM NAME:	To slop oil
HYSYS COMPONENTS	
Component	**Mole Frac**
Oxygen	0.000
H2S	0.000
Nitrogen	0.000
CO2	0.000
Methane	0.002
Ethane	0.023
Propane	0.194
i-Butane	0.058
n-Butane	0.166
22-Mpropane	0.001
i-Pentane	0.058
n-Pentane	0.073
22-Mbutane	0.001
Cyclopentane	0.000
23-Mbutane	0.007
2-Mpentane	0.021
3-Mpentane	0.012
n-Hexane	0.031
Hexanes*	0.000
Mcyclopentan	0.024
Benzene	0.020
Cyclohexane	0.049
2-Mhexane	0.008
3-Mhexane	0.008
224-Mpentane	0.000
n-Heptane	0.031
Heptanes*	0.003
Mcyclohexane	0.050
Toluene	0.028
n-Octane	0.042
Octanes*	0.004
E-Benzene	0.001
m-Xylene	0.006
o-Xylene	0.003
p-Xylene	0.006
Nonanes*	0.001
Decanes*	0.000
Undecanes_3*	0.011
Dodecanes_3*	0.004
Triadecanes_3*	0.002
Tetradecanes_3*	0.001
Pentadecanes_3*	0.000
Hexadecanes_3*	0.000
Heptadecanes_3*	0.000
Octadecanes_3*	0.000
Nonadecanes_3*	0.000
eicosanes_3*	0.000
Heneicosanes_3*	0.000
Dodocosanes_3*	0.000
Triacosanes_3*	0.000
Tetracosanes_3*	0.000
Pentacosanes_3*	0.000
Hexacosanes_3*	0.000
Heptacosanes_3*	0.000
Octacosanes_3*	0.000
Nonacosanes_3*	0.000
Triacontanes*	0.000
C31+_2*	0.000
H2O	0.000
NC30*	0.000
n-Nonane	0.029
n-Decane	0.019
NC31-35*	0.000
TexaTherm	0.000
NC31-35_1*	0.000
CO	0.000
TOTALS	1.000

Promax PROCESS STREAM NAME:	Drain Vessel Oil
PROMAX COMPONENTS	
Component	**Mole Frac**
Water	0.0002971
Hydrogen Sulfide	0.0000000
Nitrogen	0.0000069
Carbon Dioxide	0.0001589
Methane	0.0021530
Ethane	0.0231583
Propane	0.1937441
Iso-butane	0.0580180
N-butane	0.1661328
Iso-pentane	0.0580547
N-pentane	0.0729616
Cyclopentanes	0.0000000
Other Hexanes	0.0417720
n-Hexane	0.0313494
Methylcyclopentane	0.0244580
Benzene	0.0204093
Cyclohexane	0.0488517
2,2,4 Trimethylpentane	0.0000000
Other Heptanes	0.0194914
Methylcyclohexane	0.0503883
n-Heptane	0.0307889
Toluene	0.0280248
Octanes	0.0463735
Ethylbenzene	0.0013415
M&P-Xylene	0.0142718
Nonanes	0.0300359
Decanes	0.0191314
Undecanes	0.0186267
Total	1.000

Characteristics of Undecanes Plus	
Specific Gravity	0.8661
Molecular Weight (lb/lbmol)	262.912

aspentech	EXXONMOBIL TECHNICAL COM Bedford, MA USA	Case Name:	Cowboy CDP CSH V6.4 winter-conservative.hsc
		Unit Set:	CSH 5b1
		Date/Time:	Wed Mar 18 18:25:10 2020

Material Stream: to slop oil

Fluid Package: Peng Robinson

Property Package: Peng-Robinson

CONDITIONS

		Overall	Liquid Phase			
Vapour / Phase Fraction		0.0000	1.0000			
Temperature:	(F)	60.00	60.00			
Pressure:	(psig)	30.00	30.00			
Molar Flow	(MMSCFD)	6.294e-003	6.294e-003			
Mass Flow	(lb/hr)	51.67	51.67			
Std Ideal Liq Vol Flow	(barrel/day)	5.422	5.422			
Molar Enthalpy	(Btu/lbmole)	-6.923e+004	-6.923e+004			
Molar Entropy	(Btu/lbmole-F)	12.48	12.48			
Heat Flow	(Btu/hr)	-4.785e+004	-4.785e+004			
Liq Vol Flow @Std Cond	(barrel/day)	5.303 *	5.303			

PROPERTIES

		Overall	Liquid Phase			
Molecular Weight		74.77	74.77			
Molar Density	(lbmole/ft3)	0.5566	0.5566			
Mass Density	(lb/ft3)	41.61	41.61			
Act. Volume Flow	(barrel/day)	5.308	5.308			
Mass Enthalpy	(Btu/lb)	-926.0	-926.0			
Mass Entropy	(Btu/lb-F)	0.1670	0.1670			
Heat Capacity	(Btu/lbmole-F)	36.84	36.84			
Mass Heat Capacity	(Btu/lb-F)	0.4928	0.4928			
LHV Molar Basis (Std)	(Btu/SCF)	---	---			
LHV Mass Basis (Std)	(Btu/lb)	---	---			
Phase Fraction [Vol. Basis]		0.0000	1.000			
Phase Fraction [Mass Basis]		0.0000	1.000			
Partial Pressure of CO2	(psig)	-14.70	---			
Cost Based on Flow	(Cost/s)	0.0000	0.0000			
Act. Gas Flow	(ACFM)	---	---			
Avg. Liq. Density	(lbmole/ft3)	0.5449	0.5449			
Specific Heat	(Btu/lbmole-F)	36.84	36.84			
Std. Gas Flow	(MMSCFD)	6.282e-003	6.282e-003			
Std. Ideal Liq. Mass Density	(lb/ft3)	40.74	40.74			
Act. Liq. Flow	(barrel/day)	5.308	5.308			
Z Factor		1.440e-002	1.440e-002			
Watson K		12.66	12.66			
User Property		---	---			
Cp/(Cp - R)		1.057	1.057			
Cp/Cv		1.057	1.057			
Heat of Vap.	(Btu/lbmole)	1.884e+004	---			
Kinematic Viscosity	(cSt)	0.4850	0.4850			
Liq. Mass Density (Std. Cond)	(lb/ft3)	41.65	41.65			
Liq. Vol. Flow (Std. Cond)	(barrel/day)	5.303	5.303			
Liquid Fraction		1.000	1.000			
Molar Volume	(ft3/lbmole)	1.797	1.797			
Mass Heat of Vap.	(Btu/lb)	252.0	---			
Phase Fraction [Molar Basis]		0.0000	1.0000			
Surface Tension	(dyne/cm)	16.35	16.35			
Thermal Conductivity	(Btu/hr-ft-F)	6.326e-002	6.326e-002			
Viscosity	(cP)	0.3233	0.3233			
Cv (Semi-Ideal)	(Btu/lbmole-F)	34.86	34.86			
Mass Cv (Semi-Ideal)	(Btu/lb-F)	0.4662	0.4662			

* Specified by user.

Material Stream: to slop oil (continued)

Fluid Package: Peng Robinson

Property Package: Peng-Robinson

PROPERTIES

		Overall	Liquid Phase			
Cv	(Btu/lbmole-F)	34.86	34.86			
Mass Cv	(Btu/lb-F)	0.4662	0.4662			
Cv (Ent. Method)	(Btu/lbmole-F)	---	---			
Mass Cv (Ent. Method)	(Btu/lb-F)	---	---			
Cp/Cv (Ent. Method)		---	---			
Liq. Vol. Flow - Sum(Std. Cond)	(barrel/day)	5.303	5.303			
Partial Pressure of H2S	(psig)	-14.70	---			
Reid VP at 37.8 C	(psig)	41.53	41.53			
True VP at 37.8 C	(psig)	57.26	57.26			
Viscosity Index		-9.130	---			
HHV Molar Basis (Std)	(Btu/SCF)	---	---			
HHV Mass Basis (Std)	(Btu/lb)	---	---			
CO2 Loading		---	---			
CO2 Apparent Mole Conc.	(lbmole/ft3)	8.845e-005	8.845e-005			
CO2 Apparent Wt. Conc.	(lbmol/lb)	2.125e-006	2.125e-006			
Phase Fraction [Act. Vol. Basis]		0.0000	1.000			
Mass Exergy	(Btu/lb)	3.927	---			
Ideal Gas Cp/Cv		1.079	1.079			
Ideal Gas Cp	(Btu/lbmole-F)	27.12	27.12			
Mass Ideal Gas Cp	(Btu/lb-F)	0.3628	0.3628			
Bubble Point Pressure	(psig)	30.00	---			

COMPOSITION

Overall Phase

Vapour Fraction 0.0000

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Oxygen	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2S	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nitrogen	0.0000	0.0000	0.0001	0.0000	0.0000	0.0000
CO2	0.0001	0.0002	0.0048	0.0001	0.0004	0.0001
Methane	0.0015	0.0022	0.0239	0.0005	0.0055	0.0010
Ethane	0.0160	0.0232	0.4813	0.0093	0.0927	0.0171
Propane	0.1339	0.1937	5.9047	0.1143	0.7980	0.1472
i-Butane	0.0401	0.0580	2.3307	0.0451	0.2840	0.0524
n-Butane	0.1148	0.1661	6.6738	0.1292	0.7835	0.1445
22-Mpropane	0.0008	0.0012	0.0600	0.0012	0.0069	0.0013
i-Pentane	0.0401	0.0581	2.8949	0.0560	0.3179	0.0586
n-Pentane	0.0504	0.0730	3.6383	0.0704	0.3956	0.0730
22-Mbutane	0.0004	0.0006	0.0376	0.0007	0.0039	0.0007
Cyclopentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
23-Mbutane	0.0048	0.0069	0.4131	0.0080	0.0425	0.0078
2-Mpentane	0.0144	0.0208	1.2418	0.0240	0.1295	0.0239
3-Mpentane	0.0084	0.0122	0.7237	0.0140	0.0742	0.0137
n-Hexane	0.0217	0.0313	1.8672	0.0361	0.1929	0.0356
Hexanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Mcyclopentan	0.0169	0.0245	1.4226	0.0275	0.1295	0.0239
Benzene	0.0141	0.0204	1.1018	0.0213	0.0855	0.0158
Cyclohexane	0.0338	0.0489	2.8415	0.0550	0.2489	0.0459
2-Mhexane	0.0058	0.0084	0.5791	0.0112	0.0582	0.0107
3-Mhexane	0.0053	0.0077	0.5348	0.0103	0.0531	0.0098

* Specified by user.

Material Stream: to slop oil (continued)

Fluid Package: Peng Robinson
Property Package: Peng-Robinson

COMPOSITION

Overall Phase (continued)

Vapour Fraction 0.0000

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
224-Mpentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Heptane	0.0213	0.0308	2.1323	0.0413	0.2126	0.0392
Heptanes*	0.0024	0.0034	0.2261	0.0044	0.0213	0.0039
Mcyclohexane	0.0348	0.0504	3.4194	0.0662	0.3031	0.0559
Toluene	0.0194	0.0280	1.7847	0.0345	0.1405	0.0259
n-Octane	0.0292	0.0423	3.3368	0.0646	0.3239	0.0597
Octanes*	0.0028	0.0041	0.3039	0.0059	0.0278	0.0051
E-Benzene	0.0009	0.0013	0.0984	0.0019	0.0077	0.0014
m-Xylene	0.0038	0.0055	0.4069	0.0079	0.0321	0.0059
o-Xylene	0.0022	0.0032	0.2352	0.0046	0.0182	0.0034
p-Xylene	0.0038	0.0055	0.4052	0.0078	0.0321	0.0059
Nonanes*	0.0009	0.0012	0.1044	0.0020	0.0093	0.0017
Decanes*	0.0002	0.0003	0.0300	0.0006	0.0026	0.0005
Undecanes_3*	0.0078	0.0113	1.1432	0.0221	0.0988	0.0182
Dodecanes_3*	0.0030	0.0043	0.4762	0.0092	0.0406	0.0075
Triadecanes_3*	0.0014	0.0021	0.2523	0.0049	0.0212	0.0039
Tetradecanes_3*	0.0005	0.0007	0.0917	0.0018	0.0076	0.0014
Pentadecanes_3*	0.0002	0.0002	0.0316	0.0006	0.0026	0.0005
Hexadecanes_3*	0.0000	0.0001	0.0089	0.0002	0.0007	0.0001
Heptadecanes_3*	0.0000	0.0000	0.0030	0.0001	0.0002	0.0000
Octadecanes_3*	0.0000	0.0000	0.0013	0.0000	0.0001	0.0000
Nonadecanes_3*	0.0000	0.0000	0.0006	0.0000	0.0000	0.0000
eicosanes_3*	0.0000	0.0000	0.0002	0.0000	0.0000	0.0000
Heneicosanes_3*	0.0000	0.0000	0.0001	0.0000	0.0000	0.0000
Dodocosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Tetracosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Pentacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacontanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C31+_2*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2O	0.0002	0.0003	0.0037	0.0001	0.0003	0.0000
NC30*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Nonane	0.0199	0.0288	2.5519	0.0494	0.2426	0.0447
n-Decane	0.0130	0.0188	1.8495	0.0358	0.1728	0.0319
NC31-35*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TexaTherm	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC31-35_1*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
CO	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TEGlycol	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
SO2	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C10+ (SS1H)*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
464H C7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
474Y c7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Total	0.6911	1.0000	51.6730	1.0000	5.4219	1.0000

* Specified by user.

Material Stream: to slop oil (continued)

Fluid Package: Peng Robinson

Property Package: Peng-Robinson

COMPOSITION

Liquid Phase

Phase Fraction 1.000

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Oxygen	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2S	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nitrogen	0.0000	0.0000	0.0001	0.0000	0.0000	0.0000
CO2	0.0001	0.0002	0.0048	0.0001	0.0004	0.0001
Methane	0.0015	0.0022	0.0239	0.0005	0.0055	0.0010
Ethane	0.0160	0.0232	0.4813	0.0093	0.0927	0.0171
Propane	0.1339	0.1937	5.9047	0.1143	0.7980	0.1472
i-Butane	0.0401	0.0580	2.3307	0.0451	0.2840	0.0524
n-Butane	0.1148	0.1661	6.6738	0.1292	0.7835	0.1445
22-Mpropane	0.0008	0.0012	0.0600	0.0012	0.0069	0.0013
i-Pentane	0.0401	0.0581	2.8949	0.0560	0.3179	0.0586
n-Pentane	0.0504	0.0730	3.6383	0.0704	0.3956	0.0730
22-Mbutane	0.0004	0.0006	0.0376	0.0007	0.0039	0.0007
Cyclopentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
23-Mbutane	0.0048	0.0069	0.4131	0.0080	0.0425	0.0078
2-Mpentane	0.0144	0.0208	1.2418	0.0240	0.1295	0.0239
3-Mpentane	0.0084	0.0122	0.7237	0.0140	0.0742	0.0137
n-Hexane	0.0217	0.0313	1.8672	0.0361	0.1929	0.0356
Hexanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Mcyclopentan	0.0169	0.0245	1.4226	0.0275	0.1295	0.0239
Benzene	0.0141	0.0204	1.1018	0.0213	0.0855	0.0158
Cyclohexane	0.0338	0.0489	2.8415	0.0550	0.2489	0.0459
2-Mhexane	0.0058	0.0084	0.5791	0.0112	0.0582	0.0107
3-Mhexane	0.0053	0.0077	0.5348	0.0103	0.0531	0.0098
224-Mpentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Heptane	0.0213	0.0308	2.1323	0.0413	0.2126	0.0392
Heptanes*	0.0024	0.0034	0.2261	0.0044	0.0213	0.0039
Mcyclohexane	0.0348	0.0504	3.4194	0.0662	0.3031	0.0559
Toluene	0.0194	0.0280	1.7847	0.0345	0.1405	0.0259
n-Octane	0.0292	0.0423	3.3368	0.0646	0.3239	0.0597
Octanes*	0.0028	0.0041	0.3039	0.0059	0.0278	0.0051
E-Benzene	0.0009	0.0013	0.0984	0.0019	0.0077	0.0014
m-Xylene	0.0038	0.0055	0.4069	0.0079	0.0321	0.0059
o-Xylene	0.0022	0.0032	0.2352	0.0046	0.0182	0.0034
p-Xylene	0.0038	0.0055	0.4052	0.0078	0.0321	0.0059
Nonanes*	0.0009	0.0012	0.1044	0.0020	0.0093	0.0017
Decanes*	0.0002	0.0003	0.0300	0.0006	0.0026	0.0005
Undecanes_3*	0.0078	0.0113	1.1432	0.0221	0.0988	0.0182
Dodecanes_3*	0.0030	0.0043	0.4762	0.0092	0.0406	0.0075
Triadecanes_3*	0.0014	0.0021	0.2523	0.0049	0.0212	0.0039
Tetradecanes_3*	0.0005	0.0007	0.0917	0.0018	0.0076	0.0014
Pentadecanes_3*	0.0002	0.0002	0.0316	0.0006	0.0026	0.0005
Hexadecanes_3*	0.0000	0.0001	0.0089	0.0002	0.0007	0.0001
Heptadecanes_3*	0.0000	0.0000	0.0030	0.0001	0.0002	0.0000
Octadecanes_3*	0.0000	0.0000	0.0013	0.0000	0.0001	0.0000
Nonadecanes_3*	0.0000	0.0000	0.0006	0.0000	0.0000	0.0000
eicosanes_3*	0.0000	0.0000	0.0002	0.0000	0.0000	0.0000
Heneicosanes_3*	0.0000	0.0000	0.0001	0.0000	0.0000	0.0000

* Specified by user.

Material Stream: to slop oil (continued)

Fluid Package: Peng Robinson
Property Package: Peng-Robinson

COMPOSITION

Liquid Phase (continued)

Phase Fraction 1.000

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Dodocosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Tetracosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Pentacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacontanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C31+_2*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2O	0.0002	0.0003	0.0037	0.0001	0.0003	0.0000
NC30*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Nonane	0.0199	0.0288	2.5519	0.0494	0.2426	0.0447
n-Decane	0.0130	0.0188	1.8495	0.0358	0.1728	0.0319
NC31-35*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TexaTherm	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC31-35_1*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
CO	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TEGlycol	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
SO2	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C10+ (SS1H)*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
464H C7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
474Y c7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Total	0.6911	1.0000	51.6730	1.0000	5.4219	1.0000

* Specified by user.

XTO ENERGY INC.
Cowboy CDP
PROCESS SIMULATION COMPONENTS

PROCESS SIMULATION COMPONENTS - DRAIN VESSEL OUTLET WATER

HYSYS PROCESS STREAM NAME:	To GB2
HYSYS COMPONENTS	
Component	**Mole Frac**
Oxygen	0.0000
H2S	0.0000
Nitrogen	0.0000
CO2	0.0000
Methane	0.0000
Ethane	0.0000
Propane	0.0000
i-Butane	0.0000
n-Butane	0.0000
22-Mpropane	0.0000
i-Pentane	0.0000
n-Pentane	0.0000
22-Mbutane	0.0000
Cyclopentane	0.0000
23-Mbutane	0.0000
2-Mpentane	0.0000
3-Mpentane	0.0000
n-Hexane	0.0000
Hexanes*	0.0000
Mcyclopentan	0.0000
Benzene	0.0000
Cyclohexane	0.0000
2-Mhexane	0.0000
3-Mhexane	0.0000
224-Mpentane	0.0000
n-Heptane	0.0000
Heptanes*	0.0000
Mcyclohexane	0.0000
Toluene	0.0000
n-Octane	0.0000
Octanes*	0.0000
E-Benzene	0.0000
m-Xylene	0.0000
o-Xylene	0.0000
p-Xylene	0.0000
Nonanes*	0.0000
Decanes*	0.0000
Undecanes_3*	0.0000
Dodecanes_3*	0.0000
Triadecanes_3*	0.0000
Tetradecanes_3*	0.0000
Pentadecanes_3*	0.0000
Hexadecanes_3*	0.0000
Heptadecanes_3*	0.0000
Octadecanes_3*	0.0000
Nonadecanes_3*	0.0000
eicosanes_3*	0.0000
Heneicosanes_3*	0.0000
Dodocosanes_3*	0.0000
Triacosanes_3*	0.0000
Tetracosanes_3*	0.0000
Pentacosanes_3*	0.0000
Hexacosanes_3*	0.0000
Heptacosanes_3*	0.0000
Octacosanes_3*	0.0000
Nonacosanes_3*	0.0000
Triacontanes*	0.0000
C31+_2*	0.0000
H2O	0.9998
NC30*	0.0000
n-Nonane	0.0000
n-Decane	0.0000
NC31-35*	0.0000
TexaTherm	0.0000
NC31-35_1*	0.0000
CO	0.0000
TOTALS	1.000

Promax PROCESS STREAM NAME:	Drain Vessel Water
PROMAX COMPONENTS	
Component	**Mole Frac**
Water	0.9997937
Hydrogen Sulfide	0.0000000
Nitrogen	0.0000001
Carbon Dioxide	0.0000061
Methane	0.0000004
Ethane	0.0000046
Propane	0.0000388
Iso-butane	0.0000116
N-butane	0.0000333
Iso-pentane	0.0000116
N-pentane	0.0000146
Cyclopentanes	0.0000000
Other Hexanes	0.0000084
n-Hexane	0.0000063
Methylcyclopentane	0.0000049
Benzene	0.0000041
Cyclohexane	0.0000098
2,2,4 Trimethylpentane	0.0000000
Other Heptanes	0.0000039
Methylcyclohexane	0.0000101
n-Heptane	0.0000062
Toluene	0.0000056
Octanes	0.0000093
Ethylbenzene	0.0000003
M&P-Xylene	0.0000029
Nonanes	0.0000060
Decanes	0.0000038
Undecanes	0.0000037
Total	1.000

Characteristics of Undecanes Plus	
Specific Gravity	0.8661
Molecular Weight (lb/lbmol)	262.912

Material Stream: to GB2

Fluid Package: Peng Robinson

Property Package: Peng-Robinson

CONDITIONS

		Overall	Vapour Phase	Liquid Phase	Aqueous Phase
Vapour / Phase Fraction		0.0001	0.0001	0.0001	0.9998
Temperature:	(F)	60.05	60.05	60.05	60.05
Pressure:	(psig)	0.2500	0.2500	0.2500	0.2500
Molar Flow	(MMSCFD)	0.3176	2.143e-005	4.270e-005	0.3176
Mass Flow	(lb/hr)	628.7	0.1209	0.4027	628.2
Std Ideal Liq Vol Flow	(barrel/day)	43.15	1.507e-002	3.982e-002	43.10
Molar Enthalpy	(Btu/lbmole)	-1.234e+005	-5.216e+004	-7.444e+004	-1.234e+005
Molar Entropy	(Btu/lbmole-F)	12.23	38.28	8.324	12.23
Heat Flow	(Btu/hr)	-4.302e+006	-122.8	-349.0	-4.302e+006
Liq Vol Flow @Std Cond	(barrel/day)	42.41 *	1.475e-002	3.928e-002	42.38

PROPERTIES

		Overall	Vapour Phase	Liquid Phase	Aqueous Phase
Molecular Weight		18.03	51.37	85.89	18.02
Molar Density	(lbmole/ft3)	3.234	2.746e-003	0.5098	3.515
Mass Density	(lb/ft3)	58.29	0.1411	43.79	63.33
Act. Volume Flow	(barrel/day)	46.11	3.663	3.931e-002	42.40
Mass Enthalpy	(Btu/lb)	-6843	-1015	-866.7	-6848
Mass Entropy	(Btu/lb-F)	0.6786	0.7451	9.692e-002	0.6789
Heat Capacity	(Btu/lbmole-F)	18.57	20.12	40.58	18.57
Mass Heat Capacity	(Btu/lb-F)	1.030	0.3917	0.4725	1.031
LHV Molar Basis (Std)	(Btu/SCF)	---	---	---	2.291e-008
LHV Mass Basis (Std)	(Btu/lb)	---	---	---	4.826e-007
Phase Fraction [Vol. Basis]		3.492e-004	3.492e-004	9.228e-004	0.9987
Phase Fraction [Mass Basis]		1.923e-004	1.923e-004	6.405e-004	0.9992
Partial Pressure of CO2	(psig)	-14.56	---	---	---
Cost Based on Flow	(Cost/s)	0.0000	0.0000	0.0000	0.0000
Act. Gas Flow	(ACFM)	1.428e-002	1.428e-002	---	---
Avg. Liq. Density	(lbmole/ft3)	3.455	0.6676	0.5033	3.458
Specific Heat	(Btu/lbmole-F)	18.57	20.12	40.58	18.57
Std. Gas Flow	(MMSCFD)	0.3170	2.139e-005	4.262e-005	0.3170
Std. Ideal Liq. Mass Density	(lb/ft3)	62.27	34.29	43.22	62.30
Act. Liq. Flow	(barrel/day)	42.44	---	3.931e-002	42.40
Z Factor		---	0.9759	5.256e-003	7.623e-004
Watson K		12.58	14.00	12.28	8.520
User Property		---	---	---	---
Cp/(Cp - R)		1.120	1.109	1.051	1.120
Cp/Cv		1.000	1.120	1.335	1.141
Heat of Vap.	(Btu/lbmole)	2.176e+004	---	---	---
Kinematic Viscosity	(cSt)	---	3.354	0.6102	1.103
Liq. Mass Density (Std. Cond)	(lb/ft3)	63.37	35.04	43.82	63.35
Liq. Vol. Flow (Std. Cond)	(barrel/day)	42.41	1.475e-002	3.928e-002	42.38
Liquid Fraction		0.9999	0.0000	1.000	1.000
Molar Volume	(ft3/lbmole)	0.3093	364.2	1.961	0.2845
Mass Heat of Vap.	(Btu/lb)	1207	---	---	---
Phase Fraction [Molar Basis]		0.0001	0.0001	0.0001	0.9998
Surface Tension	(dyne/cm)	---	---	19.31	73.72
Thermal Conductivity	(Btu/hr-ft-F)	---	9.072e-003	6.677e-002	0.3445
Viscosity	(cP)	---	7.579e-003	0.4280	1.119
Cv (Semi-Ideal)	(Btu/lbmole-F)	16.59	18.14	38.59	16.58
Mass Cv (Semi-Ideal)	(Btu/lb-F)	0.9201	0.3531	0.4493	0.9205

* Specified by user.

Material Stream: to GB2 (continued)

Fluid Package: Peng Robinson

Property Package: Peng-Robinson

PROPERTIES

		Overall	Vapour Phase	Liquid Phase	Aqueous Phase	
Cv	(Btu/lbmole-F)	18.57	17.97	30.39	16.28	
Mass Cv	(Btu/lb-F)	1.030	0.3498	0.3538	0.9037	
Cv (Ent. Method)	(Btu/lbmole-F)	---	---	35.34	17.73	
Mass Cv (Ent. Method)	(Btu/lb-F)	---	---	0.4114	0.9839	
Cp/Cv (Ent. Method)		---	---	1.148	1.048	
Liq. Vol. Flow - Sum(Std. Cond)	(barrel/day)	42.44	1.475e-002	3.928e-002	42.38	
Partial Pressure of H2S	(psig)	-14.70	---	---	---	
Reid VP at 37.8 C	(psig)	57.13	125.9	8.717	-13.54	
True VP at 37.8 C	(psig)	56.09	164.0	12.14	-13.54	
Viscosity Index		4.562	---	---	---	
HHV Molar Basis (Std)	(Btu/SCF)	---	---	---	46.46	
HHV Mass Basis (Std)	(Btu/lb)	---	---	---	978.7	
CO2 Loading		---	---	---	---	
CO2 Apparent Mole Conc.	(lbmole/ft3)	1.982e-005	---	7.319e-005	1.939e-005	
CO2 Apparent Wt. Conc.	(lbmol/lb)	3.399e-007	---	1.672e-006	3.062e-007	
Phase Fraction [Act. Vol. Basis]		7.946e-002	7.946e-002	8.526e-004	0.9197	
Mass Exergy	(Btu/lb)	0.2848	---	---	---	
Ideal Gas Cp/Cv		1.330	1.111	1.070	1.330	
Ideal Gas Cp	(Btu/lbmole-F)	8.012	19.94	30.49	8.008	
Mass Ideal Gas Cp	(Btu/lb-F)	0.4444	0.3881	0.3550	0.4445	
Bubble Point Pressure	(psig)	28.16	---	---	---	

COMPOSITION

Overall Phase

Vapour Fraction 0.0001

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Oxygen	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2S	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nitrogen	0.0000	0.0000	0.0001	0.0000	0.0000	0.0000
CO2	0.0002	0.0000	0.0094	0.0000	0.0008	0.0000
Methane	0.0000	0.0000	0.0002	0.0000	0.0001	0.0000
Ethane	0.0002	0.0000	0.0049	0.0000	0.0009	0.0000
Propane	0.0014	0.0000	0.0596	0.0001	0.0081	0.0002
i-Butane	0.0004	0.0000	0.0235	0.0000	0.0029	0.0001
n-Butane	0.0012	0.0000	0.0674	0.0001	0.0079	0.0002
22-Mpropane	0.0000	0.0000	0.0006	0.0000	0.0001	0.0000
i-Pentane	0.0004	0.0000	0.0292	0.0000	0.0032	0.0001
n-Pentane	0.0005	0.0000	0.0368	0.0001	0.0040	0.0001
22-Mbutane	0.0000	0.0000	0.0004	0.0000	0.0000	0.0000
Cyclopentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
23-Mbutane	0.0000	0.0000	0.0042	0.0000	0.0004	0.0000
2-Mpentane	0.0001	0.0000	0.0125	0.0000	0.0013	0.0000
3-Mpentane	0.0001	0.0000	0.0073	0.0000	0.0007	0.0000
n-Hexane	0.0002	0.0000	0.0189	0.0000	0.0019	0.0000
Hexanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Mcyclopentan	0.0002	0.0000	0.0144	0.0000	0.0013	0.0000
Benzene	0.0001	0.0000	0.0111	0.0000	0.0009	0.0000
Cyclohexane	0.0003	0.0000	0.0287	0.0000	0.0025	0.0001
2-Mhexane	0.0001	0.0000	0.0058	0.0000	0.0006	0.0000
3-Mhexane	0.0001	0.0000	0.0054	0.0000	0.0005	0.0000

* Specified by user.

Material Stream: to GB2 (continued)

Fluid Package: Peng Robinson

Property Package: Peng-Robinson

COMPOSITION

Overall Phase (continued)

Vapour Fraction 0.0001

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
224-Mpentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Heptane	0.0002	0.0000	0.0215	0.0000	0.0021	0.0000
Heptanes*	0.0000	0.0000	0.0023	0.0000	0.0002	0.0000
Mcyclohexane	0.0004	0.0000	0.0345	0.0001	0.0031	0.0001
Toluene	0.0002	0.0000	0.0180	0.0000	0.0014	0.0000
n-Octane	0.0003	0.0000	0.0337	0.0001	0.0033	0.0001
Octanes*	0.0000	0.0000	0.0031	0.0000	0.0003	0.0000
E-Benzene	0.0000	0.0000	0.0010	0.0000	0.0001	0.0000
m-Xylene	0.0000	0.0000	0.0041	0.0000	0.0003	0.0000
o-Xylene	0.0000	0.0000	0.0024	0.0000	0.0002	0.0000
p-Xylene	0.0000	0.0000	0.0041	0.0000	0.0003	0.0000
Nonanes*	0.0000	0.0000	0.0011	0.0000	0.0001	0.0000
Decanes*	0.0000	0.0000	0.0003	0.0000	0.0000	0.0000
Undecanes_3*	0.0001	0.0000	0.0115	0.0000	0.0010	0.0000
Dodecanes_3*	0.0000	0.0000	0.0048	0.0000	0.0004	0.0000
Triadecanes_3*	0.0000	0.0000	0.0025	0.0000	0.0002	0.0000
Tetradecanes_3*	0.0000	0.0000	0.0009	0.0000	0.0001	0.0000
Pentadecanes_3*	0.0000	0.0000	0.0003	0.0000	0.0000	0.0000
Hexadecanes_3*	0.0000	0.0000	0.0001	0.0000	0.0000	0.0000
Heptadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
eicosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heneicosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Dodocosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Tetracosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Pentacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacontanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C31+_2*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2O	34.8691	0.9998	628.1761	0.9992	43.0993	0.9987
NC30*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Nonane	0.0002	0.0000	0.0258	0.0000	0.0025	0.0001
n-Decane	0.0001	0.0000	0.0187	0.0000	0.0017	0.0000
NC31-35*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TexaTherm	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC31-35_1*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
CO	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TEGlycol	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
SO2	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C10+ (SS1H)*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
464H C7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
474Y c7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Total	34.8762	1.0000	628.7074	1.0000	43.1549	1.0000

* Specified by user.

Material Stream: to GB2 (continued)

Fluid Package: Peng Robinson
Property Package: Peng-Robinson

COMPOSITION

Vapour Phase

Phase Fraction 6.748e-005

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Oxygen	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2S	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nitrogen	0.0000	0.0008	0.0001	0.0004	0.0000	0.0003
CO2	0.0000	0.0088	0.0009	0.0075	0.0001	0.0050
Methane	0.0000	0.0063	0.0002	0.0020	0.0001	0.0036
Ethane	0.0002	0.0642	0.0045	0.0376	0.0009	0.0580
Propane	0.0011	0.4491	0.0466	0.3855	0.0063	0.4180
i-Butane	0.0002	0.0969	0.0133	0.1097	0.0016	0.1072
n-Butane	0.0005	0.2303	0.0315	0.2606	0.0037	0.2454
22-Mpropane	0.0000	0.0014	0.0002	0.0020	0.0000	0.0018
i-Pentane	0.0001	0.0428	0.0073	0.0601	0.0008	0.0529
n-Pentane	0.0001	0.0420	0.0071	0.0590	0.0008	0.0514
22-Mbutane	0.0000	0.0002	0.0000	0.0004	0.0000	0.0003
Cyclopentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
23-Mbutane	0.0000	0.0020	0.0004	0.0034	0.0000	0.0028
2-Mpentane	0.0000	0.0055	0.0011	0.0093	0.0001	0.0078
3-Mpentane	0.0000	0.0029	0.0006	0.0048	0.0001	0.0039
n-Hexane	0.0000	0.0059	0.0012	0.0099	0.0001	0.0082
Hexanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Mcyclopentan	0.0000	0.0043	0.0009	0.0071	0.0001	0.0052
Benzene	0.0000	0.0035	0.0006	0.0053	0.0000	0.0033
Cyclohexane	0.0000	0.0069	0.0014	0.0114	0.0001	0.0080
2-Mhexane	0.0000	0.0007	0.0002	0.0013	0.0000	0.0011
3-Mhexane	0.0000	0.0006	0.0001	0.0012	0.0000	0.0009
224-Mpentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Heptane	0.0000	0.0018	0.0004	0.0036	0.0000	0.0029
Heptanes*	0.0000	0.0002	0.0001	0.0005	0.0000	0.0003
Mcyclohexane	0.0000	0.0033	0.0008	0.0063	0.0001	0.0045
Toluene	0.0000	0.0014	0.0003	0.0024	0.0000	0.0015
n-Octane	0.0000	0.0008	0.0002	0.0017	0.0000	0.0014
Octanes*	0.0000	0.0001	0.0000	0.0002	0.0000	0.0002
E-Benzene	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
m-Xylene	0.0000	0.0001	0.0000	0.0001	0.0000	0.0001
o-Xylene	0.0000	0.0000	0.0000	0.0001	0.0000	0.0000
p-Xylene	0.0000	0.0001	0.0000	0.0001	0.0000	0.0001
Nonanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Decanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Undecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Dodecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Tetradecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Pentadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
eicosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heneicosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000

* Specified by user.

Material Stream: to GB2 (continued)

Fluid Package: Peng Robinson
Property Package: Peng-Robinson

COMPOSITION

Vapour Phase (continued)

Phase Fraction 6.748e-005

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Dodocosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Tetracosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Pentacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacontanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C31+_2*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2O	0.0000	0.0167	0.0007	0.0059	0.0000	0.0032
NC30*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Nonane	0.0000	0.0002	0.0001	0.0004	0.0000	0.0003
n-Decane	0.0000	0.0000	0.0000	0.0001	0.0000	0.0001
NC31-35*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TexaTherm	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC31-35_1*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
CO	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TEGlycol	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
SO2	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C10+ (SS1H)*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
464H C7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
474Y c7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Total	0.0024	1.0000	0.1209	1.0000	0.0151	1.0000

Liquid Phase

Phase Fraction 1.344e-004

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Oxygen	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2S	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nitrogen	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
CO2	0.0000	0.0001	0.0000	0.0001	0.0000	0.0001
Methane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Ethane	0.0000	0.0023	0.0003	0.0008	0.0001	0.0016
Propane	0.0003	0.0630	0.0130	0.0324	0.0018	0.0442
i-Butane	0.0002	0.0377	0.0103	0.0255	0.0013	0.0315
n-Butane	0.0006	0.1318	0.0359	0.0892	0.0042	0.1059
22-Mpropane	0.0000	0.0011	0.0004	0.0009	0.0000	0.0011
i-Pentane	0.0003	0.0650	0.0220	0.0546	0.0024	0.0606
n-Pentane	0.0004	0.0876	0.0296	0.0736	0.0032	0.0809
22-Mbutane	0.0000	0.0008	0.0003	0.0008	0.0000	0.0009
Cyclopentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
23-Mbutane	0.0000	0.0093	0.0038	0.0093	0.0004	0.0097
2-Mpentane	0.0001	0.0283	0.0114	0.0284	0.0012	0.0299
3-Mpentane	0.0001	0.0167	0.0067	0.0167	0.0007	0.0173
n-Hexane	0.0002	0.0437	0.0177	0.0438	0.0018	0.0458
Hexanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Mcyclopentan	0.0002	0.0342	0.0135	0.0336	0.0012	0.0309

* Specified by user.

Material Stream: to GB2 (continued)

Fluid Package: Peng Robinson
Property Package: Peng-Robinson

COMPOSITION

Liquid Phase (continued)

Phase Fraction 1.344e-004

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Benzene	0.0001	0.0286	0.0105	0.0261	0.0008	0.0204
Cyclohexane	0.0003	0.0693	0.0273	0.0679	0.0024	0.0601
2-Mhexane	0.0001	0.0121	0.0057	0.0141	0.0006	0.0144
3-Mhexane	0.0001	0.0112	0.0053	0.0131	0.0005	0.0131
224-Mpentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Heptane	0.0002	0.0449	0.0211	0.0524	0.0021	0.0528
Heptanes*	0.0000	0.0050	0.0022	0.0055	0.0002	0.0053
Mcyclohexane	0.0003	0.0734	0.0338	0.0839	0.0030	0.0752
Toluene	0.0002	0.0410	0.0177	0.0440	0.0014	0.0350
n-Octane	0.0003	0.0625	0.0335	0.0832	0.0033	0.0816
Octanes*	0.0000	0.0061	0.0030	0.0075	0.0003	0.0070
E-Benzene	0.0000	0.0020	0.0010	0.0025	0.0001	0.0020
m-Xylene	0.0000	0.0082	0.0041	0.0102	0.0003	0.0081
o-Xylene	0.0000	0.0048	0.0024	0.0059	0.0002	0.0046
p-Xylene	0.0000	0.0082	0.0041	0.0101	0.0003	0.0081
Nonanes*	0.0000	0.0019	0.0011	0.0026	0.0001	0.0024
Decanes*	0.0000	0.0005	0.0003	0.0008	0.0000	0.0007
Undecanes_3*	0.0001	0.0167	0.0115	0.0287	0.0010	0.0251
Dodecanes_3*	0.0000	0.0064	0.0048	0.0119	0.0004	0.0103
Triadecanes_3*	0.0000	0.0031	0.0025	0.0063	0.0002	0.0054
Tetradecanes_3*	0.0000	0.0010	0.0009	0.0023	0.0001	0.0019
Pentadecanes_3*	0.0000	0.0003	0.0003	0.0008	0.0000	0.0007
Hexadecanes_3*	0.0000	0.0001	0.0001	0.0002	0.0000	0.0002
Heptadecanes_3*	0.0000	0.0000	0.0000	0.0001	0.0000	0.0001
Octadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
eicosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heneicosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Dodocosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Tetracosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Pentacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacontanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C31+_2*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2O	0.0000	0.0003	0.0000	0.0001	0.0000	0.0000
NC30*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Nonane	0.0002	0.0428	0.0257	0.0639	0.0024	0.0614
n-Decane	0.0001	0.0280	0.0187	0.0464	0.0017	0.0438
NC31-35*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TexaTherm	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC31-35_1*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
CO	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TEGlycol	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
SO2	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000

* Specified by user.

Material Stream: to GB2 (continued)

Fluid Package: Peng Robinson
Property Package: Peng-Robinson

COMPOSITION

Liquid Phase (continued)

Phase Fraction 1.344e-004

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
C10+ (SS1H)*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
464H C7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
474Y c7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Total	0.0047	1.0000	0.4027	1.0000	0.0398	1.0000

Aqueous Phase

Phase Fraction 0.9998

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Oxygen	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2S	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nitrogen	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
CO2	0.0002	0.0000	0.0085	0.0000	0.0007	0.0000
Methane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Ethane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Propane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
i-Butane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Butane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
22-Mpropane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
i-Pentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Pentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
22-Mbutane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Cyclopentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
23-Mbutane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
2-Mpentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
3-Mpentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Hexane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Mcyclopentan	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Benzene	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Cyclohexane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
2-Mhexane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
3-Mhexane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
224-Mpentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Heptane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Mcyclohexane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Toluene	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Octane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
E-Benzene	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
m-Xylene	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
o-Xylene	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
p-Xylene	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Decanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Undecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Dodecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000

* Specified by user.

Material Stream: to GB2 (continued)

Fluid Package: Peng Robinson
Property Package: Peng-Robinson

COMPOSITION

Aqueous Phase (continued)

Phase Fraction 0.9998

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Tetradecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Pentadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
eicosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heneicosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Dodocosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Tetracosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Pentacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacontanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C31+_2*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2O	34.8690	1.0000	628.1753	1.0000	43.0993	1.0000
NC30*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Nonane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Decane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC31-35*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TexaTherm	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC31-35_1*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
CO	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TEGlycol	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
SO2	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C10+ (SS1H)*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
464H C7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
474Y c7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Total	34.8692	1.0000	628.1838	1.0000	43.1000	1.0000

* Specified by user.

XTO ENERGY INC.
Cowboy CDP
PROCESS SIMULATION COMPONENTS

PROCESS SIMULATION COMPONENTS - SURGE VESSEL WATER

HYSYS PROCESS STREAM NAME:	WiO2
HYSYS COMPONENTS	
Component	**Mole Frac**
Oxygen	0.0000
H2S	0.0000
Nitrogen	0.0000
CO2	0.0000
Methane	0.0000
Ethane	0.0000
Propane	0.0000
i-Butane	0.0000
n-Butane	0.0000
22-Mpropane	0.0000
i-Pentane	0.0000
n-Pentane	0.0000
22-Mbutane	0.0000
Cyclopentane	0.0000
23-Mbutane	0.0000
2-Mpentane	0.0000
3-Mpentane	0.0000
n-Hexane	0.0000
Hexanes*	0.0000
Mcyclopentan	0.0000
Benzene	0.0000
Cyclohexane	0.0000
2-Mhexane	0.0000
3-Mhexane	0.0000
224-Mpentane	0.0000
n-Heptane	0.0000
Heptanes*	0.0000
Mcyclohexane	0.0000
Toluene	0.0000
n-Octane	0.0000
Octanes*	0.0000
E-Benzene	0.0000
m-Xylene	0.0000
o-Xylene	0.0000
p-Xylene	0.0000
Nonanes*	0.0000
Decanes*	0.0000
Undecanes_3*	0.0000
Dodecanes_3*	0.0000
Triadecanes_3*	0.0000
Tetradecanes_3*	0.0000
Pentadecanes_3*	0.0000
Hexadecanes_3*	0.0000
Heptadecanes_3*	0.0000
Octadecanes_3*	0.0000
Nonadecanes_3*	0.0000
eicosanes_3*	0.0000
Heneicosanes_3*	0.0000
Dodocosanes_3*	0.0000
Triacosanes_3*	0.0000
Tetracosanes_3*	0.0000
Pentacosanes_3*	0.0000
Hexacosanes_3*	0.0000
Heptacosanes_3*	0.0000
Octacosanes_3*	0.0000
Nonacosanes_3*	0.0000
Triacontanes*	0.0000
C31+_2*	0.0000
H2O	0.9998
NC30*	0.0000
n-Nonane	0.0000
n-Decane	0.0000
NC31-35*	0.0000
TexaTherm	0.0000
NC31-35_1*	0.0000
CO	0.0000
TOTALS	100.000

Promax PROCESS STREAM NAME:	Surge Vessel Water
PROMAX COMPONENTS	
Component	**Mole Frac**
Water	0.99979373
Hydrogen Sulfide	0.00000000
Nitrogen	0.00000007
Carbon Dioxide	0.00000613
Methane	0.00000043
Ethane	0.00000464
Propane	0.00003878
Iso-butane	0.00001161
N-butane	0.00003325
Iso-pentane	0.00001162
N-pentane	0.00001460
Cyclopentanes	0.00000000
Other Hexanes	0.00000836
n-Hexane	0.00000628
Methylcyclopentane	0.00000490
Benzene	0.00000409
Cyclohexane	0.00000978
2,2,4 Trimethylpentane	0.00000000
Other Heptanes	0.00000390
Methylcyclohexane	0.00001009
n-Heptane	0.00000616
Toluene	0.00000561
Octanes	0.00000928
Ethylbenzene	0.00000027
M&P-Xylene	0.00000286
Nonanes	0.00000601
Decanes	0.00000383
Undecanes	0.00000373
Total	1.000

Characteristics of Undecanes Plus	
Specific Gravity	0.8661
Molecular Weight (lb/lbmol)	262.912

aspentech	EXXONMOBIL TECHNICAL COM Bedford, MA USA	Case Name: Cowboy CDP CSH V6.4 winter-conservative.hsc Unit Set: CSH 5b1 Date/Time: Thu Mar 19 09:14:22 2020

Material Stream: WiO2

Fluid Package: Peng Robinson

Property Package: Peng-Robinson

CONDITIONS

		Overall	Vapour Phase	Liquid Phase	Aqueous Phase
Vapour / Phase Fraction		0.0000	0.0000	0.0019	0.9981
Temperature:	(F)	79.80	79.80	79.80	79.80
Pressure:	(psig)	0.2500	0.2500	0.2500	0.2500
Molar Flow	(MMSCFD)	7.297	5.548e-005	1.400e-002	7.283
Mass Flow	(lb/hr)	1.464e+004	0.2808	233.4	1.441e+004
Std Ideal Liq Vol Flow	(barrel/day)	1009	3.760e-002	20.14	988.5
Molar Enthalpy	(Btu/lbmole)	-1.230e+005	-4.830e+004	-1.336e+005	-1.230e+005
Molar Entropy	(Btu/lbmole-F)	13.01	41.31	56.44	12.92
Heat Flow	(Btu/hr)	-9.858e+007	-294.3	-2.054e+005	-9.837e+007
Liq Vol Flow @Std Cond	(barrel/day)	988.6 *	3.566e-002	20.04	972.1

PROPERTIES

		Overall	Vapour Phase	Liquid Phase	Aqueous Phase
Molecular Weight		18.27	46.09	151.8	18.02
Molar Density	(lbmole/ft3)	3.389	2.629e-003	0.3241	3.487
Mass Density	(lb/ft3)	61.93	0.1212	49.21	62.81
Act. Volume Flow	(barrel/day)	1011	9.906	20.27	980.5
Mass Enthalpy	(Btu/lb)	-6733	-1048	-880.2	-6828
Mass Entropy	(Btu/lb-F)	0.7119	0.8963	0.3718	0.7174
Heat Capacity	(Btu/lbmole-F)	18.66	18.66	70.88	18.56
Mass Heat Capacity	(Btu/lb-F)	1.021	0.4049	0.4669	1.030
LHV Molar Basis (Std)	(Btu/SCF)	---	---	---	6.393e-008
LHV Mass Basis (Std)	(Btu/lb)	---	---	---	1.346e-006
Phase Fraction [Vol. Basis]		3.728e-005	3.728e-005	1.996e-002	0.9800
Phase Fraction [Mass Basis]		1.918e-005	1.918e-005	1.594e-002	0.9840
Partial Pressure of CO2	(psig)	-14.67	---	---	---
Cost Based on Flow	(Cost/s)	0.0000	0.0000	0.0000	0.0000
Act. Gas Flow	(ACFM)	3.862e-002	3.862e-002	---	---
Avg. Liq. Density	(lbmole/ft3)	3.396	0.6925	0.3264	3.458
Specific Heat	(Btu/lbmole-F)	18.66	18.66	70.88	18.56
Std. Gas Flow	(MMSCFD)	7.284	5.538e-005	1.398e-002	7.270
Std. Ideal Liq. Mass Density	(lb/ft3)	62.05	31.92	49.55	62.30
Act. Liq. Flow	(barrel/day)	1001	---	20.27	980.5
Z Factor		---	0.9821	7.965e-003	7.404e-004
Watson K		11.86	14.80	11.86	8.524
User Property		---	---	---	---
Cp/(Cp - R)		1.119	1.119	1.029	1.120
Cp/Cv		1.000	1.128	1.214	1.148
Heat of Vap.	(Btu/lbmole)	2.253e+004	---	---	---
Kinematic Viscosity	(cSt)	---	4.251	2.581	0.8544
Liq. Mass Density (Std. Cond)	(lb/ft3)	63.31	33.65	49.79	63.35
Liq. Vol. Flow (Std. Cond)	(barrel/day)	988.6	3.566e-002	20.04	972.1
Liquid Fraction		1.000	0.0000	1.000	1.000
Molar Volume	(ft3/lbmole)	0.2951	380.4	3.085	0.2868
Mass Heat of Vap.	(Btu/lb)	1233	---	---	---
Phase Fraction [Molar Basis]		0.0000	0.0000	0.0019	0.9981
Surface Tension	(dyne/cm)	---	---	22.30	71.83
Thermal Conductivity	(Btu/hr-ft-F)	0.3448	1.020e-002	6.914e-002	0.3544
Viscosity	(cP)	0.8955	8.250e-003	2.035	0.8597
Cv (Semi-Ideal)	(Btu/lbmole-F)	16.67	16.67	68.89	16.57
Mass Cv (Semi-Ideal)	(Btu/lb-F)	0.9126	0.3618	0.4538	0.9200

* Specified by user.

Material Stream: WiO2 (continued)

Fluid Package: Peng Robinson

Property Package: Peng-Robinson

PROPERTIES

		Overall	Vapour Phase	Liquid Phase	Aqueous Phase	
Cv	(Btu/lbmole-F)	18.65	16.55	58.38	16.17	
Mass Cv	(Btu/lb-F)	1.021	0.3591	0.3845	0.8974	
Cv (Ent. Method)	(Btu/lbmole-F)	---	---	62.28	15.82	
Mass Cv (Ent. Method)	(Btu/lb-F)	---	---	0.4103	0.8781	
Cp/Cv (Ent. Method)		---	---	1.138	1.173	
Liq. Vol. Flow - Sum(Std. Cond)	(barrel/day)	992.2	3.566e-002	20.04	972.1	
Partial Pressure of H2S	(psig)	-14.70	---	---	---	
Reid VP at 37.8 C	(psig)	-0.6078	208.0	-1.318	-13.72	
True VP at 37.8 C	(psig)	5.705	255.3	4.434	-13.72	
Viscosity Index		1.705	---	---	---	
HHV Molar Basis (Std)	(Btu/SCF)	---	---	---	46.46	
HHV Mass Basis (Std)	(Btu/lb)	---	---	---	978.7	
CO2 Loading		---	---	---	---	
CO2 Apparent Mole Conc.	(lbmole/ft3)	3.393e-006	---	9.387e-006	3.252e-006	
CO2 Apparent Wt. Conc.	(lbmol/lb)	5.480e-008	---	1.908e-007	5.177e-008	
Phase Fraction [Act. Vol. Basis]		9.802e-003	9.802e-003	2.006e-002	0.9701	
Mass Exergy	(Btu/lb)	8.320e-003	---	---	---	
Ideal Gas Cp/Cv		1.324	1.120	1.036	1.329	
Ideal Gas Cp	(Btu/lbmole-F)	8.115	18.52	56.70	8.022	
Mass Ideal Gas Cp	(Btu/lb-F)	0.4441	0.4018	0.3735	0.4453	
Bubble Point Pressure	(psig)	0.9793	---	---	---	

COMPOSITION

Overall Phase

Vapour Fraction 0.0000

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Oxygen	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2S	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nitrogen	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
CO2	0.0008	0.0000	0.0353	0.0000	0.0029	0.0000
Methane	0.0000	0.0000	0.0003	0.0000	0.0001	0.0000
Ethane	0.0131	0.0000	0.3933	0.0000	0.0757	0.0001
Propane	0.0586	0.0001	2.5848	0.0002	0.3493	0.0003
i-Butane	0.0224	0.0000	1.3000	0.0001	0.1584	0.0002
n-Butane	0.0802	0.0001	4.6622	0.0003	0.5474	0.0005
22-Mpropane	0.0009	0.0000	0.0658	0.0000	0.0076	0.0000
i-Pentane	0.0443	0.0001	3.1942	0.0002	0.3508	0.0003
n-Pentane	0.0585	0.0001	4.2181	0.0003	0.4586	0.0005
22-Mbutane	0.0006	0.0000	0.0544	0.0000	0.0057	0.0000
Cyclopentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
23-Mbutane	0.0087	0.0000	0.7484	0.0001	0.0770	0.0001
2-Mpentane	0.0238	0.0000	2.0472	0.0001	0.2135	0.0002
3-Mpentane	0.0144	0.0000	1.2416	0.0001	0.1273	0.0001
n-Hexane	0.0381	0.0000	3.2834	0.0002	0.3393	0.0003
Hexanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Mcyclopentan	0.0307	0.0000	2.5835	0.0002	0.2352	0.0002
Benzene	0.0316	0.0000	2.4700	0.0002	0.1917	0.0002
Cyclohexane	0.0714	0.0001	6.0106	0.0004	0.5264	0.0005
2-Mhexane	0.0135	0.0000	1.3556	0.0001	0.1362	0.0001
3-Mhexane	0.0123	0.0000	1.2288	0.0001	0.1219	0.0001

* Specified by user.

Material Stream: WiO2 (continued)

Fluid Package: Peng Robinson

Property Package: Peng-Robinson

COMPOSITION

Overall Phase (continued)

Vapour Fraction 0.0000

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
224-Mpentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Heptane	0.0574	0.0001	5.7500	0.0004	0.5732	0.0006
Heptanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Mcyclohexane	0.0856	0.0001	8.4060	0.0006	0.7452	0.0007
Toluene	0.0526	0.0001	4.8466	0.0003	0.3814	0.0004
n-Octane	0.1047	0.0001	11.9644	0.0008	1.1614	0.0012
Octanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
E-Benzene	0.0029	0.0000	0.3046	0.0000	0.0240	0.0000
m-Xylene	0.0131	0.0000	1.3887	0.0001	0.1097	0.0001
o-Xylene	0.0073	0.0000	0.7795	0.0001	0.0604	0.0001
p-Xylene	0.0131	0.0000	1.3887	0.0001	0.1100	0.0001
Nonanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Decanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Undecanes_3*	0.0649	0.0001	9.5463	0.0007	0.8254	0.0008
Dodecanes_3*	0.0460	0.0001	7.4008	0.0005	0.6310	0.0006
Triadecanes_3*	0.0491	0.0001	8.5842	0.0006	0.7230	0.0007
Tetradecanes_3*	0.0412	0.0001	7.8253	0.0005	0.6516	0.0006
Pentadecanes_3*	0.0362	0.0000	7.4674	0.0005	0.6152	0.0006
Hexadecanes_3*	0.0258	0.0000	5.7188	0.0004	0.4667	0.0005
Heptadecanes_3*	0.0216	0.0000	5.1181	0.0003	0.4142	0.0004
Octadecanes_3*	0.0204	0.0000	5.1107	0.0003	0.4106	0.0004
Nonadecanes_3*	0.0190	0.0000	4.9899	0.0003	0.3985	0.0004
eicosanes_3*	0.0125	0.0000	3.4275	0.0002	0.2722	0.0003
Heneicosanes_3*	0.0125	0.0000	3.6269	0.0002	0.2860	0.0003
Dodocosanes_3*	0.0101	0.0000	3.0172	0.0002	0.2369	0.0002
Triacosanes_3*	0.0089	0.0000	2.7914	0.0002	0.2180	0.0002
Tetracosanes_3*	0.0077	0.0000	2.4839	0.0002	0.1930	0.0002
Pentacosanes_3*	0.0066	0.0000	2.2093	0.0002	0.1709	0.0002
Hexacosanes_3*	0.0062	0.0000	2.1749	0.0001	0.1674	0.0002
Heptacosanes_3*	0.0061	0.0000	2.1879	0.0001	0.1677	0.0002
Octacosanes_3*	0.0056	0.0000	2.0772	0.0001	0.1586	0.0002
Nonacosanes_3*	0.0050	0.0000	1.8915	0.0001	0.1439	0.0001
Triacontanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C31+_2*	0.0887	0.0001	46.5652	0.0032	3.4189	0.0034
H2O	799.7391	0.9981	14407.5306	0.9840	988.5049	0.9800
NC30*	0.0051	0.0000	2.3333	0.0002	0.1738	0.0002
n-Nonane	0.0938	0.0001	12.0289	0.0008	1.1436	0.0011
n-Decane	0.0901	0.0001	12.8176	0.0009	1.1978	0.0012
NC31-35*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TexaTherm	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC31-35_1*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
CO	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TEGlycol	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
SO2	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C10+ (SS1H)*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
464H C7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
474Y c7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Total	801.2824	1.0000	14641.2309	1.0000	1008.6803	1.0000

* Specified by user.

Material Stream: WiO2 (continued)

Fluid Package: Peng Robinson
Property Package: Peng-Robinson

COMPOSITION

Vapour Phase

Phase Fraction 7.603e-006

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Oxygen	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2S	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nitrogen	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
CO2	0.0000	0.0020	0.0005	0.0019	0.0000	0.0012
Methane	0.0000	0.0012	0.0001	0.0004	0.0000	0.0007
Ethane	0.0017	0.2763	0.0506	0.1803	0.0097	0.2591
Propane	0.0023	0.3769	0.1012	0.3606	0.0137	0.3639
i-Butane	0.0003	0.0559	0.0198	0.0705	0.0024	0.0641
n-Butane	0.0009	0.1432	0.0507	0.1807	0.0060	0.1584
22-Mpropane	0.0000	0.0012	0.0005	0.0018	0.0001	0.0016
i-Pentane	0.0002	0.0307	0.0135	0.0481	0.0015	0.0395
n-Pentane	0.0002	0.0304	0.0134	0.0477	0.0015	0.0387
22-Mbutane	0.0000	0.0002	0.0001	0.0003	0.0000	0.0003
Cyclopentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
23-Mbutane	0.0000	0.0021	0.0011	0.0039	0.0001	0.0030
2-Mpentane	0.0000	0.0051	0.0027	0.0096	0.0003	0.0075
3-Mpentane	0.0000	0.0028	0.0015	0.0052	0.0001	0.0040
n-Hexane	0.0000	0.0059	0.0031	0.0111	0.0003	0.0085
Hexanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Mcyclopentan	0.0000	0.0048	0.0024	0.0087	0.0002	0.0059
Benzene	0.0000	0.0050	0.0024	0.0084	0.0002	0.0049
Cyclohexane	0.0001	0.0090	0.0046	0.0164	0.0004	0.0107
2-Mhexane	0.0000	0.0009	0.0005	0.0019	0.0001	0.0014
3-Mhexane	0.0000	0.0008	0.0005	0.0017	0.0000	0.0013
224-Mpentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Heptane	0.0000	0.0028	0.0017	0.0060	0.0002	0.0045
Heptanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Mcyclohexane	0.0000	0.0048	0.0029	0.0102	0.0003	0.0068
Toluene	0.0000	0.0024	0.0013	0.0047	0.0001	0.0028
n-Octane	0.0000	0.0016	0.0011	0.0039	0.0001	0.0028
Octanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
E-Benzene	0.0000	0.0000	0.0000	0.0001	0.0000	0.0001
m-Xylene	0.0000	0.0002	0.0001	0.0004	0.0000	0.0002
o-Xylene	0.0000	0.0001	0.0001	0.0002	0.0000	0.0001
p-Xylene	0.0000	0.0002	0.0001	0.0004	0.0000	0.0002
Nonanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Decanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Undecanes_3*	0.0000	0.0001	0.0001	0.0002	0.0000	0.0001
Dodecanes_3*	0.0000	0.0000	0.0000	0.0001	0.0000	0.0000
Triadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Tetradecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Pentadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
eicosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heneicosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000

* Specified by user.

Material Stream: WiO2 (continued)

Fluid Package: Peng Robinson
Property Package: Peng-Robinson

COMPOSITION

Vapour Phase (continued)

Phase Fraction 7.603e-006

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Dodocosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Tetracosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Pentacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacontanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C31+_2*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2O	0.0002	0.0331	0.0036	0.0129	0.0002	0.0066
NC30*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Nonane	0.0000	0.0005	0.0004	0.0013	0.0000	0.0009
n-Decane	0.0000	0.0001	0.0001	0.0005	0.0000	0.0003
NC31-35*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TexaTherm	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC31-35_1*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
CO	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TEGlycol	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
SO2	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C10+ (SS1H)*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
464H C7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
474Y c7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Total	0.0061	1.0000	0.2808	1.0000	0.0376	1.0000

Liquid Phase

Phase Fraction 1.919e-003

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Oxygen	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2S	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nitrogen	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
CO2	0.0000	0.0000	0.0020	0.0000	0.0002	0.0000
Methane	0.0000	0.0000	0.0001	0.0000	0.0000	0.0000
Ethane	0.0114	0.0074	0.3427	0.0015	0.0660	0.0033
Propane	0.0563	0.0366	2.4836	0.0106	0.3356	0.0167
i-Butane	0.0220	0.0143	1.2803	0.0055	0.1560	0.0077
n-Butane	0.0793	0.0516	4.6115	0.0198	0.5414	0.0269
22-Mpropane	0.0009	0.0006	0.0653	0.0003	0.0075	0.0004
i-Pentane	0.0441	0.0287	3.1807	0.0136	0.3493	0.0173
n-Pentane	0.0583	0.0379	4.2047	0.0180	0.4572	0.0227
22-Mbutane	0.0006	0.0004	0.0543	0.0002	0.0057	0.0003
Cyclopentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
23-Mbutane	0.0087	0.0056	0.7473	0.0032	0.0769	0.0038
2-Mpentane	0.0237	0.0154	2.0445	0.0088	0.2132	0.0106
3-Mpentane	0.0144	0.0094	1.2401	0.0053	0.1272	0.0063
n-Hexane	0.0381	0.0248	3.2803	0.0141	0.3390	0.0168
Hexanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Mcyclopentan	0.0307	0.0199	2.5810	0.0111	0.2350	0.0117

* Specified by user.

EXXONMOBIL TECHNICAL COM
Bedford, MA
USA

Case Name:	Cowboy CDP CSH V6.4 winter-conservative.hsc
Unit Set:	CSH 5b1
Date/Time:	Thu Mar 19 09:14:22 2020

Material Stream: WiO2 (continued)

Fluid Package: Peng Robinson
Property Package: Peng-Robinson

COMPOSITION

Liquid Phase (continued)

Phase Fraction 1.919e-003

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Benzene	0.0316	0.0205	2.4676	0.0106	0.1915	0.0095
Cyclohexane	0.0714	0.0464	6.0060	0.0257	0.5260	0.0261
2-Mhexane	0.0135	0.0088	1.3550	0.0058	0.1361	0.0068
3-Mhexane	0.0123	0.0080	1.2284	0.0053	0.1219	0.0061
224-Mpentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Heptane	0.0574	0.0373	5.7483	0.0246	0.5731	0.0285
Heptanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Mcyclohexane	0.0856	0.0557	8.4031	0.0360	0.7449	0.0370
Toluene	0.0526	0.0342	4.8453	0.0208	0.3813	0.0189
n-Octane	0.1047	0.0681	11.9633	0.0513	1.1613	0.0577
Octanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
E-Benzene	0.0029	0.0019	0.3046	0.0013	0.0240	0.0012
m-Xylene	0.0131	0.0085	1.3886	0.0059	0.1097	0.0054
o-Xylene	0.0073	0.0048	0.7795	0.0033	0.0604	0.0030
p-Xylene	0.0131	0.0085	1.3886	0.0059	0.1100	0.0055
Nonanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Decanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Undecanes_3*	0.0649	0.0422	9.5462	0.0409	0.8254	0.0410
Dodecanes_3*	0.0460	0.0299	7.4007	0.0317	0.6310	0.0313
Triadecanes_3*	0.0491	0.0319	8.5842	0.0368	0.7230	0.0359
Tetradecanes_3*	0.0412	0.0268	7.8253	0.0335	0.6516	0.0324
Pentadecanes_3*	0.0362	0.0236	7.4674	0.0320	0.6152	0.0306
Hexadecanes_3*	0.0258	0.0168	5.7188	0.0245	0.4667	0.0232
Heptadecanes_3*	0.0216	0.0140	5.1181	0.0219	0.4142	0.0206
Octadecanes_3*	0.0204	0.0132	5.1107	0.0219	0.4106	0.0204
Nonadecanes_3*	0.0190	0.0123	4.9899	0.0214	0.3985	0.0198
eicosanes_3*	0.0125	0.0081	3.4275	0.0147	0.2722	0.0135
Heneicosanes_3*	0.0125	0.0081	3.6269	0.0155	0.2860	0.0142
Dodocosanes_3*	0.0101	0.0065	3.0172	0.0129	0.2369	0.0118
Triacosanes_3*	0.0089	0.0058	2.7914	0.0120	0.2180	0.0108
Tetracosanes_3*	0.0077	0.0050	2.4839	0.0106	0.1930	0.0096
Pentacosanes_3*	0.0066	0.0043	2.2093	0.0095	0.1709	0.0085
Hexacosanes_3*	0.0062	0.0041	2.1749	0.0093	0.1674	0.0083
Heptacosanes_3*	0.0061	0.0040	2.1879	0.0094	0.1677	0.0083
Octacosanes_3*	0.0056	0.0036	2.0772	0.0089	0.1586	0.0079
Nonacosanes_3*	0.0050	0.0032	1.8915	0.0081	0.1439	0.0071
Triacontanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C31+_2*	0.0887	0.0577	46.5652	0.1995	3.4189	0.1698
H2O	0.0008	0.0005	0.0141	0.0001	0.0010	0.0000
NC30*	0.0051	0.0033	2.3333	0.0100	0.1738	0.0086
n-Nonane	0.0938	0.0610	12.0285	0.0515	1.1435	0.0568
n-Decane	0.0901	0.0586	12.8175	0.0549	1.1978	0.0595
NC31-35*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TexaTherm	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC31-35_1*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
CO	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TEGlycol	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
SO2	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000

* Specified by user.

Material Stream: WiO2 (continued)

Fluid Package: Peng Robinson

Property Package: Peng-Robinson

COMPOSITION

Liquid Phase (continued)

Phase Fraction 1.919e-003

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
C10+ (SS1H)*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
464H C7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
474Y c7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Total	1.5374	1.0000	233.4045	1.0000	20.1363	1.0000

Aqueous Phase

Phase Fraction 0.9981

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Oxygen	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2S	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nitrogen	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
CO2	0.0007	0.0000	0.0328	0.0000	0.0027	0.0000
Methane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Ethane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Propane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
i-Butane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Butane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
22-Mpropane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
i-Pentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Pentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
22-Mbutane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Cyclopentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
23-Mbutane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
2-Mpentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
3-Mpentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Hexane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Mcyclopentan	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Benzene	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Cyclohexane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
2-Mhexane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
3-Mhexane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
224-Mpentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Heptane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Mcyclohexane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Toluene	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Octane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
E-Benzene	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
m-Xylene	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
o-Xylene	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
p-Xylene	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Decanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Undecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Dodecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000

* Specified by user.

Material Stream: WiO2 (continued)

Fluid Package: Peng Robinson

Property Package: Peng-Robinson

COMPOSITION

Aqueous Phase (continued)

Phase Fraction 0.9981

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Tetradecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Pentadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
eicosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heneicosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Dodocosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Tetracosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Pentacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacontanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C31+_2*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2O	799.7381	1.0000	14407.5129	1.0000	988.5037	1.0000
NC30*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Nonane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Decane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC31-35*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TexaTherm	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC31-35_1*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
CO	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TEGlycol	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
SO2	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C10+ (SS1H)*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
464H C7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
474Y c7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Total	799.7389	1.0000	14407.5457	1.0000	988.5064	1.0000

* Specified by user.

XTO ENERGY INC.
Cowboy CDP
PROCESS SIMULATION COMPONENTS

PROCESS SIMULATION COMPONENTS - STABILIZER OVERHEAD GAS

HYSYS PROCESS STREAM NAME:	Oil OVHD Gas
HYSYS COMPONENTS	
Component	**Mole Frac**
Oxygen	0.000
H2S	0.000
Nitrogen	0.000
CO2	0.001
Methane	0.000
Ethane	0.146
Propane	0.629
i-Butane	0.058
n-Butane	0.100
22-Mpropane	0.001
i-Pentane	0.015
n-Pentane	0.015
22-Mbutane	0.000
Cyclopentane	0.000
23-Mbutane	0.001
2-Mpentane	0.003
3-Mpentane	0.001
n-Hexane	0.003
Hexanes*	0.000
Mcyclopentan	0.002
Benzene	0.002
Cyclohexane	0.005
2-Mhexane	0.000
3-Mhexane	0.000
224-Mpentane	0.000
n-Heptane	0.002
Heptanes*	0.000
Mcyclohexane	0.003
Toluene	0.001
n-Octane	0.001
Octanes*	0.000
E-Benzene	0.000
m-Xylene	0.000
o-Xylene	0.000
p-Xylene	0.000
Nonanes*	0.000
Decanes*	0.000
Undecanes_3*	0.000
Dodecanes_3*	0.000
Triadecanes_3*	0.000
Tetradecanes_3*	0.000
Pentadecanes_3*	0.000
Hexadecanes_3*	0.000
Heptadecanes_3*	0.000
Octadecanes_3*	0.000
Nonadecanes_3*	0.000
eicosanes_3*	0.000
Heneicosanes_3*	0.000
Dodocosanes_3*	0.000
Triacosanes_3*	0.000
Tetracosanes_3*	0.000
Pentacosanes_3*	0.000
Hexacosanes_3*	0.000
Heptacosanes_3*	0.000
Octacosanes_3*	0.000
Nonacosanes_3*	0.000
Triacontanes*	0.000
C31+_2*	0.000
H2O	0.009
NC30*	0.000
n-Nonane	0.000
n-Decane	0.000
NC31-35*	0.000
TexaTherm	0.000
NC31-35_1*	0.000
CO	0.000
TOTALS	100.000

PROMAX PROCESS STREAM NAME:	Process Purge Gas Flaring	
PROMAX COMPONENTS		
Component	**Mole Frac**	**WT%**
Water	0.0088	0.34
Hydrogen Sulfide	0.0000	0.00
Nitrogen	0.0000	0.00
Carbon Dioxide	0.0005	0.05
Methane	0.0002	0.01
Ethane	0.1464	9.55
Propane	0.6292	60.21
Iso-butane	0.0584	7.37
N-butane	0.1000	12.61
Iso-pentane	0.0154	2.41
N-pentane	0.0151	2.36
Cyclopentanes	0.0000	0.00
Other Hexanes	0.0057	1.07
n-Hexane	0.0030	0.56
Methylcyclopentane	0.0024	0.44
Benzene	0.0025	0.42
Cyclohexane	0.0045	0.82
2,2,4 Trimethylpentane	0.0000	0.00
Other Heptanes	0.0009	0.20
Methylcyclohexane	0.0025	0.53
n-Heptane	0.0015	0.33
Toluene	0.0013	0.26
Octanes	0.0010	0.25
Ethylbenzene	0.0000	0.00
M&P-Xylene	0.0002	0.05
Nonanes	0.0003	0.08
Decanes	0.0001	0.03
Undecanes	0.0001	0.06
Total	1.000	

Characteristics of Undecanes Plus	
Specific Gravity	0.8661
Molecular Weight (lb/lbmol)	262.912
VOC WT%	90.05
HAP WT%	2.066

Case Name:	Cowboy CDP CSH V6.4 winter-conservative.hsc
Unit Set:	CSH 5b1
Date/Time:	Tue Mar 10 09:18:10 2020

Material Stream: Oil OVHD gas

Fluid Package: Peng Robinson

Property Package: Peng-Robinson

CONDITIONS

		Overall	Vapour Phase
Vapour / Phase Fraction		1.0000	1.0000
Temperature:	(F)	104.2	104.2
Pressure:	(psig)	31.00	31.00
Molar Flow	(MMSCFD)	2.822	2.822
Mass Flow	(lb/hr)	1.428e+004	1.428e+004
Std Ideal Liq Vol Flow	(barrel/day)	1911	1911
Molar Enthalpy	(Btu/lbmole)	-4.624e+004	-4.624e+004
Molar Entropy	(Btu/lbmole-F)	39.11	39.11
Heat Flow	(Btu/hr)	-1.433e+007	-1.433e+007
Liq Vol Flow @Std Cond	(barrel/day)	1857 *	1857

PROPERTIES

		Overall	Vapour Phase
Molecular Weight		46.07	46.07
Molar Density	(lbmole/ft3)	7.948e-003	7.948e-003
Mass Density	(lb/ft3)	0.3661	0.3661
Act. Volume Flow	(barrel/day)	1.667e+005	1.667e+005
Mass Enthalpy	(Btu/lb)	-1004	-1004
Mass Entropy	(Btu/lb-F)	0.8489	0.8489
Heat Capacity	(Btu/lbmole-F)	19.70	19.70
Mass Heat Capacity	(Btu/lb-F)	0.4277	0.4277
LHV Molar Basis (Std)	(Btu/SCF)	---	---
LHV Mass Basis (Std)	(Btu/lb)	---	---
Phase Fraction [Vol. Basis]		1.000	1.000
Phase Fraction [Mass Basis]		1.000	1.000
Partial Pressure of CO2	(psig)	-14.67	---
Cost Based on Flow	(Cost/s)	0.0000	0.0000
Act. Gas Flow	(ACFM)	649.8	649.8
Avg. Liq. Density	(lbmole/ft3)	0.6933	0.6933
Specific Heat	(Btu/lbmole-F)	19.70	19.70
Std. Gas Flow	(MMSCFD)	2.817	2.817
Std. Ideal Liq. Mass Density	(lb/ft3)	31.94	31.94
Act. Liq. Flow	(barrel/day)	---	---
Z Factor		0.9501	0.9501
Watson K		14.69	14.69
User Property		---	---
Cp/(Cp - R)		1.112	1.112
Cp/Cv		1.137	1.137
Heat of Vap.	(Btu/lbmole)	1.009e+004	---
Kinematic Viscosity	(cSt)	1.482	1.482
Liq. Mass Density (Std. Cond)	(lb/ft3)	32.85	32.85
Liq. Vol. Flow (Std. Cond)	(barrel/day)	1857	1857
Liquid Fraction		0.0000	0.0000
Molar Volume	(ft3/lbmole)	125.8	125.8
Mass Heat of Vap.	(Btu/lb)	219.0	---
Phase Fraction [Molar Basis]		1.0000	1.0000
Surface Tension	(dyne/cm)	---	---
Thermal Conductivity	(Btu/hr-ft-F)	1.113e-002	1.113e-002
Viscosity	(cP)	8.692e-003	8.692e-003
Cv (Semi-Ideal)	(Btu/lbmole-F)	17.71	17.71
Mass Cv (Semi-Ideal)	(Btu/lb-F)	0.3846	0.3846

* Specified by user.

aspentech	EXXONMOBIL TECHNICAL COM Bedford, MA USA	Case Name:	Cowboy CDP CSH V6.4 winter-conservative.hsc
		Unit Set:	CSH 5b1
		Date/Time:	Tue Mar 10 09:18:10 2020

Material Stream: Oil OVHD gas (continued)

Fluid Package: Peng Robinson

Property Package: Peng-Robinson

PROPERTIES

		Overall	Vapour Phase			
Cv	(Btu/lbmole-F)	17.33	17.33			
Mass Cv	(Btu/lb-F)	0.3761	0.3761			
Cv (Ent. Method)	(Btu/lbmole-F)	---	---			
Mass Cv (Ent. Method)	(Btu/lb-F)	---	---			
Cp/Cv (Ent. Method)		---	---			
Liq. Vol. Flow - Sum(Std. Cond)	(barrel/day)	1857	1857			
Partial Pressure of H2S	(psig)	-14.70	---			
Reid VP at 37.8 C	(psig)	182.2	182.2			
True VP at 37.8 C	(psig)	206.2	206.2			
Viscosity Index		---	---			
HHV Molar Basis (Std)	(Btu/SCF)	---	---			
HHV Mass Basis (Std)	(Btu/lb)	---	---			
CO2 Loading		---	---			
CO2 Apparent Mole Conc.	(lbmole/ft3)	---	---			
CO2 Apparent Wt. Conc.	(lbmol/lb)	---	---			
Phase Fraction [Act. Vol. Basis]		1.000	1.000			
Mass Exergy	(Btu/lb)	25.64	---			
Ideal Gas Cp/Cv		1.115	1.115			
Ideal Gas Cp	(Btu/lbmole-F)	19.27	19.27			
Mass Ideal Gas Cp	(Btu/lb-F)	0.4182	0.4182			
Bubble Point Pressure	(psig)	216.9	---			

COMPOSITION

Overall Phase

Vapour Fraction 1.0000

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Oxygen	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2S	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nitrogen	0.0000	0.0000	0.0002	0.0000	0.0000	0.0000
CO2	0.1573	0.0005	6.9244	0.0005	0.5745	0.0003
Methane	0.0578	0.0002	0.9272	0.0001	0.2121	0.0001
Ethane	45.3764	0.1464	1364.4779	0.0956	262.6740	0.1375
Propane	194.9733	0.6292	8597.8273	0.6023	1161.9044	0.6081
i-Butane	18.0985	0.0584	1051.9690	0.0737	128.1760	0.0671
n-Butane	31.0001	0.1000	1801.8696	0.1262	211.5448	0.1107
22-Mpropane	0.2057	0.0007	14.8396	0.0010	1.7060	0.0009
i-Pentane	4.7755	0.0154	344.5606	0.0241	37.8428	0.0198
n-Pentane	4.6790	0.0151	337.5973	0.0236	36.7079	0.0192
22-Mbutane	0.0282	0.0001	2.4304	0.0002	0.2550	0.0001
Cyclopentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
23-Mbutane	0.3180	0.0010	27.4045	0.0019	2.8210	0.0015
2-Mpentane	0.7929	0.0026	68.3295	0.0048	7.1266	0.0037
3-Mpentane	0.4296	0.0014	37.0256	0.0026	3.7970	0.0020
n-Hexane	0.9302	0.0030	80.1621	0.0056	8.2830	0.0043
Hexanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Mcyclopentan	0.7333	0.0024	61.7138	0.0043	5.6188	0.0029
Benzene	0.7678	0.0025	59.9759	0.0042	4.6551	0.0024
Cyclohexane	1.3959	0.0045	117.4780	0.0082	10.2887	0.0054
2-Mhexane	0.1473	0.0005	14.7571	0.0010	1.4826	0.0008
3-Mhexane	0.1294	0.0004	12.9663	0.0009	1.2863	0.0007

* Specified by user.

Material Stream: Oil OVHD gas (continued)

Fluid Package: Peng Robinson
Property Package: Peng-Robinson

COMPOSITION

Overall Phase (continued)

Vapour Fraction 1.0000

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
224-Mpentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Heptane	0.4716	0.0015	47.2543	0.0033	4.7110	0.0025
Heptanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Mcyclohexane	0.7830	0.0025	76.8827	0.0054	6.8153	0.0036
Toluene	0.3981	0.0013	36.6840	0.0026	2.8870	0.0015
n-Octane	0.2955	0.0010	33.7544	0.0024	3.2766	0.0017
Octanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
E-Benzene	0.0075	0.0000	0.7940	0.0001	0.0625	0.0000
m-Xylene	0.0295	0.0001	3.1317	0.0002	0.2474	0.0001
o-Xylene	0.0155	0.0001	1.6498	0.0001	0.1279	0.0001
p-Xylene	0.0296	0.0001	3.1454	0.0002	0.2492	0.0001
Nonanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Decanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Undecanes_3*	0.0155	0.0001	2.2802	0.0002	0.1972	0.0001
Dodecanes_3*	0.0043	0.0000	0.6852	0.0000	0.0584	0.0000
Triadecanes_3*	0.0017	0.0000	0.3010	0.0000	0.0254	0.0000
Tetradecanes_3*	0.0005	0.0000	0.0996	0.0000	0.0083	0.0000
Pentadecanes_3*	0.0002	0.0000	0.0329	0.0000	0.0027	0.0000
Hexadecanes_3*	0.0000	0.0000	0.0091	0.0000	0.0007	0.0000
Heptadecanes_3*	0.0000	0.0000	0.0031	0.0000	0.0002	0.0000
Octadecanes_3*	0.0000	0.0000	0.0013	0.0000	0.0001	0.0000
Nonadecanes_3*	0.0000	0.0000	0.0006	0.0000	0.0000	0.0000
eicosanes_3*	0.0000	0.0000	0.0002	0.0000	0.0000	0.0000
Heneicosanes_3*	0.0000	0.0000	0.0001	0.0000	0.0000	0.0000
Dodocosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Tetracosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Pentacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacontanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C31+_2*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2O	2.7215	0.0088	49.0280	0.0034	3.3638	0.0018
NC30*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Nonane	0.0946	0.0003	12.1345	0.0008	1.1536	0.0006
n-Decane	0.0336	0.0001	4.7809	0.0003	0.4468	0.0002
NC31-35*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TexaTherm	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC31-35_1*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
CO	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TEGlycol	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
SO2	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C10+ (SS1H)*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
464H C7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
474Y c7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Total	309.8984	1.0000	14275.8892	1.0000	1910.5909	1.0000

* Specified by user.

Material Stream: Oil OVHD gas (continued)

Fluid Package: Peng Robinson
Property Package: Peng-Robinson

COMPOSITION

Vapour Phase

Phase Fraction 1.000

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Oxygen	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2S	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nitrogen	0.0000	0.0000	0.0002	0.0000	0.0000	0.0000
CO2	0.1573	0.0005	6.9244	0.0005	0.5745	0.0003
Methane	0.0578	0.0002	0.9272	0.0001	0.2121	0.0001
Ethane	45.3764	0.1464	1364.4779	0.0956	262.6740	0.1375
Propane	194.9733	0.6292	8597.8273	0.6023	1161.9044	0.6081
i-Butane	18.0985	0.0584	1051.9690	0.0737	128.1760	0.0671
n-Butane	31.0001	0.1000	1801.8696	0.1262	211.5448	0.1107
22-Mpropane	0.2057	0.0007	14.8396	0.0010	1.7060	0.0009
i-Pentane	4.7755	0.0154	344.5606	0.0241	37.8428	0.0198
n-Pentane	4.6790	0.0151	337.5973	0.0236	36.7079	0.0192
22-Mbutane	0.0282	0.0001	2.4304	0.0002	0.2550	0.0001
Cyclopentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
23-Mbutane	0.3180	0.0010	27.4045	0.0019	2.8210	0.0015
2-Mpentane	0.7929	0.0026	68.3295	0.0048	7.1266	0.0037
3-Mpentane	0.4296	0.0014	37.0256	0.0026	3.7970	0.0020
n-Hexane	0.9302	0.0030	80.1621	0.0056	8.2830	0.0043
Hexanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Mcyclopentan	0.7333	0.0024	61.7138	0.0043	5.6188	0.0029
Benzene	0.7678	0.0025	59.9759	0.0042	4.6551	0.0024
Cyclohexane	1.3959	0.0045	117.4780	0.0082	10.2887	0.0054
2-Mhexane	0.1473	0.0005	14.7571	0.0010	1.4826	0.0008
3-Mhexane	0.1294	0.0004	12.9663	0.0009	1.2863	0.0007
224-Mpentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Heptane	0.4716	0.0015	47.2543	0.0033	4.7110	0.0025
Heptanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Mcyclohexane	0.7830	0.0025	76.8827	0.0054	6.8153	0.0036
Toluene	0.3981	0.0013	36.6840	0.0026	2.8870	0.0015
n-Octane	0.2955	0.0010	33.7544	0.0024	3.2766	0.0017
Octanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
E-Benzene	0.0075	0.0000	0.7940	0.0001	0.0625	0.0000
m-Xylene	0.0295	0.0001	3.1317	0.0002	0.2474	0.0001
o-Xylene	0.0155	0.0001	1.6498	0.0001	0.1279	0.0001
p-Xylene	0.0296	0.0001	3.1454	0.0002	0.2492	0.0001
Nonanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Decanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Undecanes_3*	0.0155	0.0001	2.2802	0.0002	0.1972	0.0001
Dodecanes_3*	0.0043	0.0000	0.6852	0.0000	0.0584	0.0000
Triadecanes_3*	0.0017	0.0000	0.3010	0.0000	0.0254	0.0000
Tetradecanes_3*	0.0005	0.0000	0.0996	0.0000	0.0083	0.0000
Pentadecanes_3*	0.0002	0.0000	0.0329	0.0000	0.0027	0.0000
Hexadecanes_3*	0.0000	0.0000	0.0091	0.0000	0.0007	0.0000
Heptadecanes_3*	0.0000	0.0000	0.0031	0.0000	0.0002	0.0000
Octadecanes_3*	0.0000	0.0000	0.0013	0.0000	0.0001	0.0000
Nonadecanes_3*	0.0000	0.0000	0.0006	0.0000	0.0000	0.0000
eicosanes_3*	0.0000	0.0000	0.0002	0.0000	0.0000	0.0000
Heneicosanes_3*	0.0000	0.0000	0.0001	0.0000	0.0000	0.0000

* Specified by user.

Material Stream: Oil OVHD gas (continued)

Fluid Package: Peng Robinson

Property Package: Peng-Robinson

COMPOSITION

Vapour Phase (continued)

Phase Fraction 1.000

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Dodocosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Tetracosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Pentacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacontanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C31+_2*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2O	2.7215	0.0088	49.0280	0.0034	3.3638	0.0018
NC30*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Nonane	0.0946	0.0003	12.1345	0.0008	1.1536	0.0006
n-Decane	0.0336	0.0001	4.7809	0.0003	0.4468	0.0002
NC31-35*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TexaTherm	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC31-35_1*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
CO	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TEGlycol	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
SO2	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C10+ (SS1H)*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
464H C7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
474Y c7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Total	309.8984	1.0000	14275.8892	1.0000	1910.5909	1.0000

* Specified by user.

XTO ENERGY INC.
Cowboy CDP
PROCESS SIMULATION COMPONENTS

PROCESS SIMULATION COMPONENTS - RESIDUE GAS - ETHANE REJECTION

HYSYS PROCESS STREAM NAME:	Residue Gas
HYSYS COMPONENTS	
Component	**Mole Frac**
Oxygen	0.000
H2S	0.000
Nitrogen	0.018
CO2	0.000
Methane	0.802
Ethane	0.167
Propane	0.013
i-Butane	0.000
n-Butane	0.000
22-Mpropane	0.000
i-Pentane	0.000
n-Pentane	0.000
22-Mbutane	0.000
Cyclopentane	0.000
23-Mbutane	0.000
2-Mpentane	0.000
3-Mpentane	0.000
n-Hexane	0.000
Hexanes*	0.000
Mcyclopentan	0.000
Benzene	0.000
Cyclohexane	0.000
2-Mhexane	0.000
3-Mhexane	0.000
224-Mpentane	0.000
n-Heptane	0.000
Heptanes*	0.000
Mcyclohexane	0.000
Toluene	0.000
n-Octane	0.000
Octanes*	0.000
E-Benzene	0.000
m-Xylene	0.000
o-Xylene	0.000
p-Xylene	0.000
Nonanes*	0.000
Decanes*	0.000
Undecanes_3*	0.000
Dodecanes_3*	0.000
Triadecanes_3*	0.000
Tetradecanes_3*	0.000
Pentadecanes_3*	0.000
Hexadecanes_3*	0.000
Heptadecanes_3*	0.000
Octadecanes_3*	0.000
Nonadecanes_3*	0.000
eicosanes_3*	0.000
Heneicosanes_3*	0.000
Dodocosanes_3*	0.000
Triacosanes_3*	0.000
Tetracosanes_3*	0.000
Pentacosanes_3*	0.000
Hexacosanes_3*	0.000
Heptacosanes_3*	0.000
Octacosanes_3*	0.000
Nonacosanes_3*	0.000
Triacontanes*	0.000
C31+_2*	0.000
H2O	0.000
NC30*	0.000
n-Nonane	0.000
n-Decane	0.000
NC31-35*	0.000
TexaTherm	0.000
NC31-35_1*	0.000
CO	0.000
TOTALS	1.000

PROMAX PROCESS STREAM NAME:	Pilot Fuel, TO Assist Fuel, LP Header Purge Gas, HP Header Purge gas
PROMAX COMPONENTS	
Component	**Mole Frac**
Water	0.0000
Hydrogen Sulfide	0.0000
Nitrogen	0.0175
Carbon Dioxide	0.0000
Methane	0.8018
Ethane	0.1674
Propane	0.0132
Iso-butane	0.0000
N-butane	0.0000
Iso-pentane	0.0000
N-pentane	0.0000
Cyclopentanes	0.0000
Other Hexanes	0.0000
n-Hexane	0.0000
Methylcyclopentane	0.0000
Benzene	0.0000
Cyclohexane	0.0000
2,2,4 Trimethylpentane	0.0000
Other Heptanes	0.0000
Methylcyclohexane	0.0000
n-Heptane	0.0000
Toluene	0.0000
Octanes	0.0000
Ethylbenzene	0.0000
M&P-Xylene	0.0000
Nonanes	0.0000
Decanes	0.0000
Undecanes	0.0000
Total	1.000

Characteristics of Undecanes Plus	
Specific Gravity	0.8661
Molecular Weight (lb/lbmol)	262.912

EXXONMOBIL TECHNICAL COM Bedford, MA USA	Case Name:	Cowboy CDP CSH V6.4 winter-conservative.hsc
	Unit Set:	CSH 5b1
	Date/Time:	Tue Mar 10 09:20:25 2020

Material Stream: Residue gas1

Fluid Package: Peng Robinson

Property Package: Peng-Robinson

CONDITIONS

		Overall	Vapour Phase			
Vapour / Phase Fraction		1.0000	1.0000			
Temperature:	(F)	113.2	113.2			
Pressure:	(psig)	301.0	301.0			
Molar Flow	(MMSCFD)	203.5	203.5			
Mass Flow	(lb/hr)	4.239e+005	4.239e+005			
Std Ideal Liq Vol Flow	(barrel/day)	9.007e+004	9.007e+004			
Molar Enthalpy	(Btu/lbmole)	-3.237e+004	-3.237e+004			
Molar Entropy	(Btu/lbmole-F)	39.57	39.57			
Heat Flow	(Btu/hr)	-7.232e+008	-7.232e+008			
Liq Vol Flow @Std Cond	(barrel/day)	3.605e+007 *	3.605e+007			

PROPERTIES

		Overall	Vapour Phase			
Molecular Weight		18.97	18.97			
Molar Density	(lbmole/ft3)	5.418e-002	5.418e-002			
Mass Density	(lb/ft3)	1.028	1.028			
Act. Volume Flow	(barrel/day)	1.763e+006	1.763e+006			
Mass Enthalpy	(Btu/lb)	-1706	-1706			
Mass Entropy	(Btu/lb-F)	2.085	2.085			
Heat Capacity	(Btu/lbmole-F)	10.23	10.23			
Mass Heat Capacity	(Btu/lb-F)	0.5392	0.5392			
LHV Molar Basis (Std)	(Btu/SCF)	1031	1031			
LHV Mass Basis (Std)	(Btu/lb)	2.062e+004	2.062e+004			
Phase Fraction [Vol. Basis]		1.000	1.000			
Phase Fraction [Mass Basis]		1.000	1.000			
Partial Pressure of CO2	(psig)	-14.70	---			
Cost Based on Flow	(Cost/s)	0.0000	0.0000			
Act. Gas Flow	(ACFM)	6873	6873			
Avg. Liq. Density	(lbmole/ft3)	1.060	1.060			
Specific Heat	(Btu/lbmole-F)	10.23	10.23			
Std. Gas Flow	(MMSCFD)	203.1	203.1			
Std. Ideal Liq. Mass Density	(lb/ft3)	20.12	20.12			
Act. Liq. Flow	(barrel/day)	---	---			
Z Factor		0.9478	0.9478			
Watson K		18.92	18.92			
User Property		---	---			
Cp/(Cp - R)		1.241	1.241			
Cp/Cv		1.328	1.328			
Heat of Vap.	(Btu/lbmole)	3833	---			
Kinematic Viscosity	(cSt)	0.7417	0.7417			
Liq. Mass Density (Std. Cond)	(lb/ft3)	5.027e-002	5.027e-002			
Liq. Vol. Flow (Std. Cond)	(barrel/day)	3.605e+007	3.605e+007			
Liquid Fraction		0.0000	0.0000			
Molar Volume	(ft3/lbmole)	18.46	18.46			
Mass Heat of Vap.	(Btu/lb)	202.0	---			
Phase Fraction [Molar Basis]		1.0000	1.0000			
Surface Tension	(dyne/cm)	---	---			
Thermal Conductivity	(Btu/hr-ft-F)	2.044e-002	2.044e-002			
Viscosity	(cP)	1.221e-002	1.221e-002			
Cv (Semi-Ideal)	(Btu/lbmole-F)	8.244	8.244			
Mass Cv (Semi-Ideal)	(Btu/lb-F)	0.4345	0.4345			

* Specified by user.

Material Stream: Residue gas1 (continued)

Fluid Package: Peng Robinson

Property Package: Peng-Robinson

PROPERTIES

		Overall	Vapour Phase			
Cv	(Btu/lbmole-F)	7.702	7.702			
Mass Cv	(Btu/lb-F)	0.4059	0.4059			
Cv (Ent. Method)	(Btu/lbmole-F)	---	---			
Mass Cv (Ent. Method)	(Btu/lb-F)	---	---			
Cp/Cv (Ent. Method)		---	---			
Liq. Vol. Flow - Sum(Std. Cond)	(barrel/day)	3.605e+007	3.605e+007			
Partial Pressure of H2S	(psig)	-14.70	---			
Reid VP at 37.8 C	(psig)	---	---			
True VP at 37.8 C	(psig)	---	---			
Viscosity Index		-28.07	---			
HHV Molar Basis (Std)	(Btu/SCF)	1131	1131			
HHV Mass Basis (Std)	(Btu/lb)	2.262e+004	2.262e+004			
CO2 Loading		---	---			
CO2 Apparent Mole Conc.	(lbmole/ft3)	---	---			
CO2 Apparent Wt. Conc.	(lbmol/lb)	---	---			
Phase Fraction [Act. Vol. Basis]		1.000	1.000			
Mass Exergy	(Btu/lb)	169.4	---			
Ideal Gas Cp/Cv		1.260	1.260			
Ideal Gas Cp	(Btu/lbmole-F)	9.617	9.617			
Mass Ideal Gas Cp	(Btu/lb-F)	0.5069	0.5069			
Bubble Point Pressure	(psig)	---	---			

COMPOSITION

Overall Phase

Vapour Fraction 1.0000

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Oxygen	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2S	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nitrogen	391.3446	0.0175	10962.8501	0.0259	930.8950	0.0103
CO2	0.0133	0.0000	0.5833	0.0000	0.0484	0.0000
Methane	17912.5128	0.8018	287371.6517	0.6779	65722.5730	0.7296
Ethane	3740.5554	0.1674	112479.3029	0.2653	21653.2572	0.2404
Propane	295.9642	0.0132	13051.2704	0.0308	1763.7396	0.0196
i-Butane	0.4689	0.0000	27.2538	0.0001	3.3207	0.0000
n-Butane	0.1110	0.0000	6.4517	0.0000	0.7574	0.0000
22-Mpropane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
i-Pentane	0.0000	0.0000	0.0034	0.0000	0.0004	0.0000
n-Pentane	0.0000	0.0000	0.0004	0.0000	0.0000	0.0000
22-Mbutane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Cyclopentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
23-Mbutane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
2-Mpentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
3-Mpentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Hexane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Mcyclopentan	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Benzene	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Cyclohexane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
2-Mhexane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
3-Mhexane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000

* Specified by user.

Material Stream: Residue gas1 (continued)

Fluid Package: Peng Robinson
Property Package: Peng-Robinson

COMPOSITION

Overall Phase (continued)

Vapour Fraction 1.0000

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
224-Mpentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Heptane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Mcyclohexane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Toluene	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Octane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
E-Benzene	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
m-Xylene	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
o-Xylene	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
p-Xylene	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Decanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Undecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Dodecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Tetradecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Pentadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
eicosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heneicosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Dodocosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Tetracosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Pentacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacontanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C31+_2*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2O	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC30*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Nonane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Decane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC31-35*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TexaTherm	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC31-35_1*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
CO	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TEGlycol	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
SO2	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C10+ (SS1H)*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
464H C7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
474Y c7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Total	22340.9702	1.0000	423899.3677	1.0000	90074.5918	1.0000

Material Stream: Residue gas1 (continued)

Fluid Package: Peng Robinson
Property Package: Peng-Robinson

COMPOSITION

Vapour Phase

Phase Fraction 1.000

COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Oxygen	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2S	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nitrogen	391.3446	0.0175	10962.8501	0.0259	930.8950	0.0103
CO2	0.0133	0.0000	0.5833	0.0000	0.0484	0.0000
Methane	17912.5128	0.8018	287371.6517	0.6779	65722.5730	0.7296
Ethane	3740.5554	0.1674	112479.3029	0.2653	21653.2572	0.2404
Propane	295.9642	0.0132	13051.2704	0.0308	1763.7396	0.0196
i-Butane	0.4689	0.0000	27.2538	0.0001	3.3207	0.0000
n-Butane	0.1110	0.0000	6.4517	0.0000	0.7574	0.0000
22-Mpropane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
i-Pentane	0.0000	0.0000	0.0034	0.0000	0.0004	0.0000
n-Pentane	0.0000	0.0000	0.0004	0.0000	0.0000	0.0000
22-Mbutane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Cyclopentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
23-Mbutane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
2-Mpentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
3-Mpentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Hexane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Mcyclopentan	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Benzene	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Cyclohexane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
2-Mhexane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
3-Mhexane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
224-Mpentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Heptane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Mcyclohexane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Toluene	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Octane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
E-Benzene	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
m-Xylene	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
o-Xylene	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
p-Xylene	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Decanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Undecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Dodecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Tetradecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Pentadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonadecanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
eicosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heneicosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000

* Specified by user.

Material Stream: Residue gas1 (continued)

Fluid Package: Peng Robinson
Property Package: Peng-Robinson

COMPOSITION

Vapour Phase (continued)

Phase Fraction 1.000

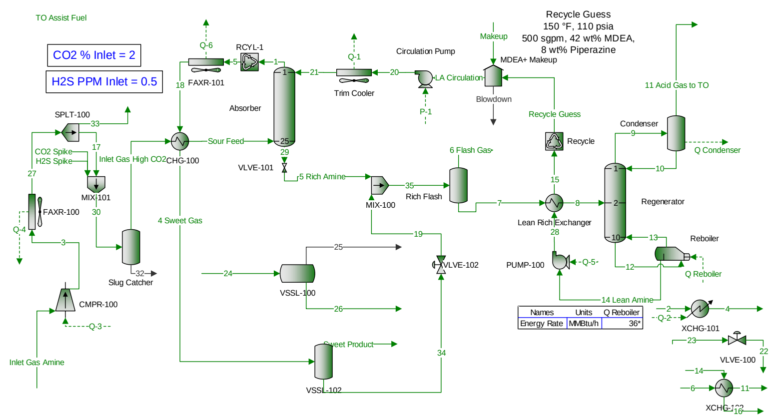
COMPONENTS	MOLAR FLOW (lbmole/hr)	MOLE FRACTION	MASS FLOW (lb/hr)	MASS FRACTION	LIQUID VOLUME FLOW (barrel/day)	LIQUID VOLUME FRACTION
Dodocosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Tetracosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Pentacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Hexacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonacosanes_3*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Triacontanes*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C31+_2*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
H2O	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC30*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Nonane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Decane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC31-35*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TexaTherm	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NC31-35_1*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
CO	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
TEGlycol	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
SO2	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C10+ (SS1H)*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
464H C7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
474Y c7+*	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Total	22340.9702	1.0000	423899.3677	1.0000	90074.5918	1.0000

* Specified by user.

MDEA Flowsheet
Plant Schematic

Client Name:	Cowboy Amine - Max Capacity	Job:	
Location:			
Flowsheet:	MDEA Flowsheet		

MDEA Sweetening with 50 wt% MDEA+Piperazine



Names	Units	Sour Feed	4 Sweet Gas	11 Acid Gas to TO	5 Rich Amine	6 Flash Gas	21	Sweet Product
Std Vapor Volumetric Flow	MMSCFD	251	246	5.36	76.8	0.118	72.3	246
Hydrogen Sulfide(Mole Fraction)	ppm	0.5	0.0001805	23.26	1.675	5.951	0.04447	0.0001659
Carbon Dioxide(Mole Fraction)	ppm	2e+04	5.4	9.33e+05	6.6e+04	1.28e+05	650	3.93
Carbon Dioxide(Mole Fraction)	%	2	0.00054048	93.305	6.5957	12.756	0.06505	0.00039322
Carbon Dioxide(Partial Molar Volumetric Fraction)	ppm	19315	3.9836	9.3345e+05	24612	1.2731e+05	-776.15	3.8287
Total Acid Gas Loading/Mole Amine					0.50586		0.0047004	

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	Cowboy Amine - Max Capacity	Job:	
Location:			
Flowsheet:	MDEA Flowsheet		

Connections

	Blowdown	CO2 Spike	H2S Spike	Inlet Gas Amine	Inlet Gas High CO2
From Block	MDEA+ Makeup	--	--	--	Slug Catcher
To Block	--	MIX-101	MIX-101	CMPR-100	XCHG-100

Stream Composition

Mole Fraction	Blowdown %	CO2 Spike %	H2S Spike %	Inlet Gas Amine %	Inlet Gas High CO2 %
Hydrogen Sulfide	4.48765E-06	0 *	100 *	0 *	5E-05
N2	0	0 *	0 *	1.47987 *	1.4519
Carbon Dioxide	0.0656401	100 *	0 *	0.111991 *	2
Methane	0	0 *	0 *	70.2052 *	68.8782
Ethane	0	0 *	0 *	15.3194 *	15.0298
Propane	0	0 *	0 *	8.52924 *	8.36802
i-Butane	0	0 *	0 *	0.983915 *	0.965317
n-Butane	0	0 *	0 *	2.36979 *	2.325
i-Pentane	0	0 *	0 *	0.387662 *	0.380334
n-Pentane	0	0 *	0 *	0.379782 *	0.372603
n-Hexane	0	0 *	0 *	0.218501 *	0.214371
Water	85.9688	0 *	0 *	0.0147201 *	0.0144418
MDEA	11.0531	0 *	0 *	0 *	0
Piperazine	2.9125	0 *	0 *	0 *	0
O2	0	0 *	0 *	0 *	0

Mass Fraction	Blowdown %	CO2 Spike %	H2S Spike %	Inlet Gas Amine %	Inlet Gas High CO2 %
Hydrogen Sulfide	4.90262E-06	0 *	100 *	0 *	7.34853E-05
N2	0	0 *	0 *	1.81922 *	1.75396
Carbon Dioxide	0.0926007	100 *	0 *	0.216285 *	3.79574
Methane	0	0 *	0 *	49.424 *	47.651
Ethane	0	0 *	0 *	20.2143 *	19.4891
Propane	0	0 *	0 *	16.5045 *	15.9125
i-Butane	0	0 *	0 *	2.50956 *	2.41953
n-Butane	0	0 *	0 *	6.04436 *	5.82753
i-Pentane	0	0 *	0 *	1.22738 *	1.18335
n-Pentane	0	0 *	0 *	1.20243 *	1.1593
n-Hexane	0	0 *	0 *	0.826294 *	0.796652
Water	49.6456	0 *	0 *	0.0116372 *	0.0112197
MDEA	42.2201	0 *	0 *	0 *	0
Piperazine	8.0417	0 *	0 *	0 *	0
O2	0	0 *	0 *	0 *	0

Mass Flow	Blowdown lb/h	CO2 Spike lb/h	H2S Spike lb/h	Inlet Gas Amine lb/h	Inlet Gas High CO2 lb/h
Hydrogen Sulfide	0	0 *	0.469624 *	0 *	0.469624
N2	0	0 *	0 *	11379.5 *	11209.1
Carbon Dioxide	0	22924.8 *	0 *	1352.89 *	24257.5
Methane	0	0 *	0 *	309154 *	304524
Ethane	0	0 *	0 *	126443 *	124550
Propane	0	0 *	0 *	103238 *	101692
i-Butane	0	0 *	0 *	15697.7 *	15462.5
n-Butane	0	0 *	0 *	37808.3 *	37242.1
i-Pentane	0	0 *	0 *	7677.46 *	7562.47
n-Pentane	0	0 *	0 *	7521.4 *	7408.75
n-Hexane	0	0 *	0 *	5168.59 *	5091.18
Water	0	0 *	0 *	72.7924 *	71.7022
MDEA	0	0 *	0 *	0 *	0

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	Cowboy Amine - Max Capacity	Job:	
Location:			
Flowsheet:	MDEA Flowsheet		

Mass Flow	Blowdown lb/h	CO2 Spike lb/h	H2S Spike lb/h	Inlet Gas Amine lb/h	Inlet Gas High CO2 lb/h
Piperazine	0	0 *	0 *	0 *	0
O2	0	0 *	0 *	0 *	0

Std Vapor Volumetric Flow	Blowdown MMSCFD	CO2 Spike MMSCFD	H2S Spike MMSCFD	Inlet Gas Amine MMSCFD	Inlet Gas High CO2 MMSCFD
Hydrogen Sulfide	0	0 *	0.0001255 *	0 *	0.0001255
N2	0	0 *	0 *	3.69967 *	3.64426
Carbon Dioxide	0	4.74422 *	0 *	0.279976 *	5.02
Methane	0	0 *	0 *	175.513 *	172.884
Ethane	0	0 *	0 *	38.2984 *	37.7248
Propane	0	0 *	0 *	21.3231 *	21.0037
i-Butane	0	0 *	0 *	2.45979 *	2.42295
n-Butane	0	0 *	0 *	5.92448 *	5.83575
i-Pentane	0	0 *	0 *	0.969155 *	0.954639
n-Pentane	0	0 *	0 *	0.949455 *	0.935234
n-Hexane	0	0 *	0 *	0.546253 *	0.538071
Water	0	0 *	0 *	0.0368002 *	0.036249
MDEA	0	0 *	0 *	0 *	0
Piperazine	0	0 *	0 *	0 *	0
O2	0	0 *	0 *	0 *	0

Stream Properties

Property	Units	Blowdown	CO2 Spike	H2S Spike	Inlet Gas Amine	Inlet Gas High CO2
Temperature	°F		100 *	100	50 *	84.5174
Pressure	psia	110	1014 *	1014	1100 *	1014
Molecular Weight	lb/lbmol	31.1962	44.0095	34.0809	22.7878	23.1889
Mass Flow	lb/h	0	22924.8	0.469624	625515	639071
Std Vapor Volumetric Flow	MMSCFD	0	4.74422 *	0.0001255 *	250 *	251
Std Liquid Volumetric Flow	sgpm	0	56.0819	0.0011752	3458.13	3462.42
Mass Cp	Btu/(lb*°F)		0.614535	0.586905	0.816909	0.69854
Net Ideal Gas Heating Value	Btu/ft^3	488.159	0	586.79	1222.83	1199.72
Gross Ideal Gas Heating Value	Btu/ft^3	574.838	0	637.1	1345.22	1319.8

Remarks

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	Cowboy Amine - Max Capacity	Job:	
Location:			
Flowsheet:	MDEA Flowsheet		

Connections

	LA Circulation	Makeup	Recycle Guess	Sour Feed	Sweet Product
From Block	MDEA+ Makeup	--	Recycle	XCHG-100	VSSL-102
To Block	Circulation Pump	MDEA+ Makeup	MDEA+ Makeup	Absorber	--

Stream Composition

Mole Fraction	LA Circulation %	Makeup %	Recycle Guess %	Sour Feed %	Sweet Product %
Hydrogen Sulfide	4.4473E-06	0	4.48765E-06	5E-05	1.65904E-08
N2	0	0	0	1.4519	1.4801
Carbon Dioxide	0.0650499	0	0.0656401	2	0.00039322
Methane	0	0	0	68.8782	70.1988
Ethane	0	0	0	15.0298	15.3174
Propane	0	0	0	8.36802	8.52977
i-Butane	0	0	0	0.965317	0.984101
n-Butane	0	0	0	2.325	2.37007
i-Pentane	0	0	0	0.380334	0.387758
n-Pentane	0	0	0	0.372603	0.379867
n-Hexane	0	0	0	0.214371	0.218563
Water	86.0949	99.9905	85.9688	0.0144418	0.133186
MDEA	10.9537	0.000256913	11.0531	0	6.60675E-07
Piperazine	2.8864	0.00929296	2.9125	0	2.44502E-05
O2	0	0	0	0	0

Mass Fraction	LA Circulation %	Makeup %	Recycle Guess %	Sour Feed %	Sweet Product %
Hydrogen Sulfide	4.87706E-06	0	4.90262E-06	7.34853E-05	2.48434E-08
N2	0	0	0	1.75396	1.8218
Carbon Dioxide	0.0921179	0	0.0926007	3.79574	0.000760371
Methane	0	0	0	47.651	49.4816
Ethane	0	0	0	19.4891	20.2371
Propane	0	0	0	15.9125	16.5263
i-Butane	0	0	0	2.41953	2.51319
n-Butane	0	0	0	5.82753	6.05267
i-Pentane	0	0	0	1.18335	1.22923
n-Pentane	0	0	0	1.1593	1.20422
n-Hexane	0	0	0	0.796652	0.827565
Water	49.9079	99.9539	49.6456	0.0112197	0.105425
MDEA	42	0.00169873	42.2201	0	3.45915E-06
Piperazine	8	0.0444157	8.0417	0	9.25357E-05
O2	0	0	0	0	0

Mass Flow	LA Circulation lb/h	Makeup lb/h	Recycle Guess lb/h	Sour Feed lb/h	Sweet Product lb/h
Hydrogen Sulfide	0.0120311	0	0.0120311	0.469624	0.000152825
N2	0	0	0	11209.1	11206.9
Carbon Dioxide	227.243	0	227.243	24257.5	4.67747
Methane	0	0	0	304524	304389
Ethane	0	0	0	124550	124490
Propane	0	0	0	101692	101663
i-Butane	0	0	0	15462.5	15460
n-Butane	0	0	0	37242.1	37233.4
i-Pentane	0	0	0	7562.47	7561.69
n-Pentane	0	0	0	7408.75	7407.81
n-Hexane	0	0	0	5091.18	5090.82
Water	123116	1285.67	121831	71.7022	648.526

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	Cowboy Amine - Max Capacity	Job:	
Location:			
Flowsheet:	MDEA Flowsheet		

Mass Flow	LA Circulation lb/h	Makeup lb/h	Recycle Guess lb/h	Sour Feed lb/h	Sweet Product lb/h
MDEA	103609	0.0218501	103609	0	0.0212792
Piperazine	19735	0.571302	19734.4	0	0.569239
O2	0	0	0	0	0

Std Vapor Volumetric Flow	LA Circulation MMSCFD	Makeup MMSCFD	Recycle Guess MMSCFD	Sour Feed MMSCFD	Sweet Product MMSCFD
Hydrogen Sulfide	3.21513E-06	0	3.21513E-06	0.0001255	4.08403E-08
N2	0	0	0	3.64426	3.64356
Carbon Dioxide	0.0470271	0	0.0470271	5.02	0.000967986
Methane	0	0	0	172.884	172.808
Ethane	0	0	0	37.7248	37.7067
Propane	0	0	0	21.0037	20.9977
i-Butane	0	0	0	2.42295	2.42255
n-Butane	0	0	0	5.83575	5.83439
i-Pentane	0	0	0	0.954639	0.954541
n-Pentane	0	0	0	0.935234	0.935116
n-Hexane	0	0	0	0.538071	0.538033
Water	62.2414	0.649969	61.5914	0.036249	0.327862
MDEA	7.91884	1.67001E-06	7.91884	0	1.62638E-06
Piperazine	2.08669	6.04071E-05	2.08663	0	6.01889E-05
O2	0	0	0	0	0

Stream Properties

Property	Units	LA Circulation	Makeup	Recycle Guess	Sour Feed	Sweet Product
Temperature	°F	170.237	80 *	170.771	98.6691	104.178
Pressure	psia	110	110 *	110	1004	984
Molecular Weight	lb/lbmol	31.0777	18.0219	31.1962	23.1889	22.7592
Mass Flow	lb/h	246687	1286.26	245401	639071	615156
Std Vapor Volumetric Flow	MMSCFD	72.2939	0.650031	71.6439	251	246.169
Std Liquid Volumetric Flow	sgpm	500 *	2.57177	497.428	3462.42	3402.85
Mass Cp	Btu/(lb*°F)	0.862976	0.998589	0.862662	0.666302	0.66551
Net Ideal Gas Heating Value	Btu/ft^3	483.772	0.304496	488.159	1199.72	1222.78
Gross Ideal Gas Heating Value	Btu/ft^3	570.125	50.6339	574.838	1319.8	1345.22

Remarks

* User Specified Values
? Extrapolated or Approximate Values

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	Cowboy Amine - Max Capacity	Job:	
Location:			
Flowsheet:	MDEA Flowsheet		

Connections

	TO Assist Fuel	1	2	3	4
From Block	--	Absorber	--	CMPR-100	XCHG-101
To Block	--	RCYL-1	XCHG-101	FAXR-100	--

Stream Composition

Mole Fraction	TO Assist Fuel %	1 %	2 %	3 %	4 %
Hydrogen Sulfide	0 *	1.74766E-08	0 *	0	0
N2	1.75018 *	1.47818	2.2881 *	1.47987	2.2881
Carbon Dioxide	0 *	0.000534743	2.09826 *	0.111991	2.09826
Methane	80.188 *	70.1073	70.0718 *	70.2052	70.0718
Ethane	16.7417 *	15.2974	13.1491 *	15.3194	13.1491
Propane	1.32013 *	8.51866	7.7036 *	8.52924	7.7036
i-Butane	0 *	0.982819	0.859286 *	0.983915	0.859286
n-Butane	0 *	2.36698	2.24813 *	2.36979	2.24813
i-Pentane	0 *	0.387253	0.439635 *	0.387662	0.439635
n-Pentane	0 *	0.379372	0.46961 *	0.379782	0.46961
n-Hexane	0 *	0.218278	0.579518 *	0.218501	0.579518
Water	0 *	0.262385	0.0930397 *	0.0147201	0.0930397
MDEA	0 *	0.000169799	0 *	0	0
Piperazine	0 *	0.000597088	0 *	0	0
O2	0 *	0	0 *	0	0

Mass Fraction	TO Assist Fuel %	1 %	2 %	3 %	4 %
Hydrogen Sulfide	0 *	2.61769E-08	0 *	0	0
N2	2.58444 *	1.81988	2.77062 *	1.81922	2.77062
Carbon Dioxide	0 *	0.00103429	3.99155 *	0.216285	3.99155
Methane	67.8109 *	49.4293	48.5904 *	49.424	48.5904
Ethane	26.5361 *	20.2157	17.0904 *	20.2143	17.0904
Propane	3.06854 *	16.5088	14.6834 *	16.5045	14.6834
i-Butane	0 *	2.51053	2.15882 *	2.50956	2.15882
n-Butane	0 *	6.04627	5.64808 *	6.04436	5.64808
i-Pentane	0 *	1.22793	1.37106 *	1.22738	1.37106
n-Pentane	0 *	1.20294	1.46455 *	1.20243	1.46455
n-Hexane	0 *	0.826689	2.15867 *	0.826294	2.15867
Water	0 *	0.207744	0.0724513 *	0.0116372	0.0724513
MDEA	0 *	0.000889251	0 *	0	0
Piperazine	0 *	0.00226033	0 *	0	0
O2	0 *	0	0 *	0	0

Mass Flow	TO Assist Fuel lb/h	1 lb/h	2 lb/h	3 lb/h	4 lb/h
Hydrogen Sulfide	0 *	0.0001612	0 *	0	0
N2	30.3614 *	11206.9	14075.6 *	11379.5	14075.6
Carbon Dioxide	0 *	6.36923	20278.2 *	1352.89	20278.2
Methane	796.627 *	304390	246854 *	309154	246854
Ethane	311.74 *	124490	86824 *	126443	86824
Propane	36.0485 *	101663	74595.8 *	103238	74595.8
i-Butane	0 *	15460	10967.4 *	15697.7	10967.4
n-Butane	0 *	37233.4	28693.9 *	37808.3	28693.9
i-Pentane	0 *	7561.69	6965.4 *	7677.46	6965.4
n-Pentane	0 *	7407.81	7440.32 *	7521.4	7440.32
n-Hexane	0 *	5090.82	10966.7 *	5168.59	10966.7
Water	0 *	1279.31	368.073 *	72.7924	368.073
MDEA	0 *	5.47608	0 *	0	0
Piperazine	0 *	13.9193	0 *	0	0

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	Cowboy Amine - Max Capacity	Job:	
Location:			
Flowsheet:	MDEA Flowsheet		

Mass Flow	TO Assist Fuel lb/h	1 lb/h	2 lb/h	3 lb/h	4 lb/h
O2	0 *	0	0 *	0	0

Std Vapor Volumetric Flow	TO Assist Fuel MMSCFD	1 MMSCFD	2 MMSCFD	3 MMSCFD	4 MMSCFD
Hydrogen Sulfide	0 *	4.30782E-08	0 *	0	0
N2	0.00987099 *	3.64356	4.5762 *	3.69967	4.5762
Carbon Dioxide	0 *	0.00131809	4.19651 *	0.279976	4.19651
Methane	0.45226 *	172.808	140.144 *	175.513	140.144
Ethane	0.094423 *	37.7067	26.2981 *	38.2984	26.2981
Propane	0.00744554 *	20.9977	15.4072 *	21.3231	15.4072
i-Butane	0 *	2.42255	1.71857 *	2.45979	1.71857
n-Butane	0 *	5.83439	4.49626 *	5.92448	4.49626
i-Pentane	0 *	0.954541	0.879269 *	0.969155	0.879269
n-Pentane	0 *	0.935116	0.939219 *	0.949455	0.939219
n-Hexane	0 *	0.538033	1.15904 *	0.546253	1.15904
Water	0 *	0.646753	0.186079 *	0.0368002	0.186079
MDEA	0 *	0.000418539	0 *	0	0
Piperazine	0 *	0.00147176	0 *	0	0
O2	0 *	0	0 *	0	0

Stream Properties

Property	Units	TO Assist Fuel	1	2	3	4
Temperature	°F	65 *	134.62	50 *	43.8765	80 *
Pressure	psia	50 *	999	1000 *	1009 *	1000
Molecular Weight	lb/lbmol	18.9706	22.7536	23.1347	22.7878	23.1347
Mass Flow	lb/h	1174.78	615808	508029	625515	508029
Std Vapor Volumetric Flow	MMSCFD	0.564 *	246.49	200 *	250	200
Std Liquid Volumetric Flow	sgpm	7.2773	3404.16	2728.1	3458.13	2728.1
Mass Cp	Btu/(lb*°F)	0.490766	0.640455	0.717859	0.776746	0.678773
Net Ideal Gas Heating Value	Btu/ft^3	1030.84	1221.21	1181.12	1222.83	1181.12
Gross Ideal Gas Heating Value	Btu/ft^3	1139.39	1343.56	1299.56	1345.22	1299.56

Remarks

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	Cowboy Amine - Max Capacity	Job:	
Location:			
Flowsheet:	MDEA Flowsheet		

Connections

	4 Sweet Gas	5	5 Rich Amine	6	6 Flash Gas
From Block	XCHG-100	RCYL-1	VLVE-101	--	Rich Flash
To Block	VSSL-102	FAXR-101	MIX-100	XCHG-102	--

Stream Composition

Mole Fraction	4 Sweet Gas %	5 %	5 Rich Amine %	6 %	6 Flash Gas %
Hydrogen Sulfide	1.80487E-08	1.80487E-08	0.000167534	0 *	0.000595084
N2	1.47817	1.47817	0.000905831	2.2897 *	0.583606
Carbon Dioxide	0.000540475	0.000540475	6.59567	2.09972 *	12.7559
Methane	70.1073	70.1073	0.099376	70.1208 *	62.2627
Ethane	15.2974	15.2974	0.0235366	13.1583 *	14.3897
Propane	8.51865	8.51865	0.00789564	7.70898 *	4.8805
i-Butane	0.982818	0.982818	0.000510626	0.859887 *	0.319872
n-Butane	2.36698	2.36698	0.00176595	2.2497 *	1.0851
i-Pentane	0.387253	0.387253	0.000127512	0.439942 *	0.080147
n-Pentane	0.379372	0.379372	0.000153654	0.469938 *	0.0958045
n-Hexane	0.218277	0.218277	4.93621E-05	0.579924 *	0.0310918
Water	0.262446	0.262446	80.2449	0.0231808 *	3.51479
MDEA	0.000169857	0.000169857	10.31	0 *	0.000128191
Piperazine	0.000597097	0.000597097	2.71501	0 *	1.02709E-05
O2	0	0	0	0 *	0

Mass Fraction	4 Sweet Gas %	5 %	5 Rich Amine %	6 %	6 Flash Gas %
Hydrogen Sulfide	2.70338E-08	2.70338E-08	0.000178364	0 *	0.000850405
N2	1.81988	1.81988	0.000792693	2.77213 *	0.685523
Carbon Dioxide	0.00104538	0.00104538	9.06772	3.99373 *	23.5394
Methane	49.4293	49.4293	0.0498018	48.6169 *	41.8828
Ethane	20.2157	20.2157	0.0221083	17.0997 *	18.143
Propane	16.5088	16.5088	0.0108762	14.6914 *	9.02395
i-Butane	2.51053	2.51053	0.000927122	2.16 *	0.779571
n-Butane	6.04627	6.04627	0.00320636	5.65115 *	2.64452
i-Pentane	1.22793	1.22793	0.00028739	1.37181 *	0.242467
n-Pentane	1.20294	1.20294	0.000346311	1.46534 *	0.289835
n-Hexane	0.826689	0.826689	0.000132883	2.15985 *	0.112348
Water	0.207793	0.207793	45.1596	0.0180484 *	2.65508
MDEA	0.000889552	0.000889552	38.3786	0 *	0.000640521
Piperazine	0.00226036	0.00226036	7.30543	0 *	3.70961E-05
O2	0	0	0	0 *	0

Mass Flow	4 Sweet Gas lb/h	5 lb/h	5 Rich Amine lb/h	6 lb/h	6 Flash Gas lb/h
Hydrogen Sulfide	0.000166476	0.000166476	0.481493	0 *	0.00262967
N2	11206.9	11206.9	2.13988	14188.4 *	2.11981
Carbon Dioxide	6.43751	6.43751	24478.3	20440.8 *	72.7899
Methane	304390	304390	134.44	248832 *	129.512
Ethane	124490	124490	59.6815	87519.9 *	56.1028
Propane	101663	101663	29.3602	75193.7 *	27.9044
i-Butane	15460	15460	2.50277	11055.3 *	2.41063
n-Butane	37233.4	37233.4	8.65558	28923.8 *	8.17755
i-Pentane	7561.69	7561.69	0.775812	7021.23 *	0.749771
n-Pentane	7407.81	7407.81	0.934868	7499.95 *	0.896246
n-Hexane	5090.82	5090.82	0.358718	11054.6 *	0.347409
Water	1279.61	1279.61	121909	92.3759 *	8.21019
MDEA	5.47793	5.47793	103603	0 *	0.00198066
Piperazine	13.9195	13.9195	19721	0 *	0.000114711
O2	0	0	0	0 *	0

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	Cowboy Amine - Max Capacity	Job:	
Location:			
Flowsheet:	MDEA Flowsheet		

Std Vapor Volumetric Flow	4 Sweet Gas MMSCFD	5 MMSCFD	5 Rich Amine MMSCFD	6 MMSCFD	6 Flash Gas MMSCFD
Hydrogen Sulfide	4.44883E-08	4.44883E-08	0.000128672	0 *	7.02741E-07
N2	3.64356	3.64356	0.00069571	4.61287 *	0.000689186
Carbon Dioxide	0.00133222	0.00133222	5.06571	4.23015 *	0.0150636
Methane	172.808	172.808	0.0763243	141.267 *	0.0735267
Ethane	37.7067	37.7067	0.0180769	26.5089 *	0.016993
Propane	20.9977	20.9977	0.00606413	15.5307 *	0.00576343
i-Butane	2.42255	2.42255	0.000392178	1.73235 *	0.000377741
n-Butane	5.83439	5.83439	0.00135631	4.5323 *	0.0012814
i-Pentane	0.954541	0.954541	9.79336E-05	0.886316 *	9.46465E-05
n-Pentane	0.935116	0.935116	0.000118012	0.946747 *	0.000113137
n-Hexane	0.538033	0.538033	3.79118E-05	1.16833 *	3.67166E-05
Water	0.646904	0.646904	61.6309	0.0467006 *	0.00415066
MDEA	0.000418681	0.000418681	7.91842	0 *	1.51382E-07
Piperazine	0.00147179	0.00147179	2.08522	0 *	1.2129E-08
O2	0	0	0	0 *	0

Stream Properties

Property	Units	4 Sweet Gas	5	5 Rich Amine	6	6 Flash Gas
Temperature	°F	104.517	134.63	115.988	100 *	115.98
Pressure	psia	989	999	89.7 *	956.73 *	37.73 *
Molecular Weight	lb/lbmol	22.7536	22.7536	32.0116	23.1382	23.8486
Mass Flow	lb/h	615808	615808	269950	511822 *	309.226
Std Vapor Volumetric Flow	MMSCFD	246.491	246.491	76.8035	201.462	0.118091
Std Liquid Volumetric Flow	sgpm	3404.16	3404.16	558.262	2749.41	1.53076
Mass Cp	Btu/(lb*°F)	0.666775	0.640448	0.667262	0.641496	0.428747
Net Ideal Gas Heating Value	Btu/ft^3	1221.21	1221.21	456.837	1181.94	962.332
Gross Ideal Gas Heating Value	Btu/ft^3	1343.56	1343.56	537.87	1300.43	1062.41

Remarks

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	Cowboy Amine - Max Capacity	Job:	
Location:			
Flowsheet:	MDEA Flowsheet		

Connections

	7	8	9	10	11
From Block	Rich Flash	Lean Rich Exchanger	Regenerator	Condenser	XCHG-102
To Block	Lean Rich Exchanger	Regenerator	Condenser	Regenerator	--

Stream Composition

Mole Fraction	7 %	8 %	9 %	10 %	11 %
Hydrogen Sulfide	0.000166184	0.000166184	0.00132096	4.63265E-06	0
N2	1.27887E-05	1.27887E-05	0.000104117	3.04006E-09	2.2897
Carbon Dioxide	6.55916	6.55916	52.9283	0.0588414	2.09972
Methane	0.00395807	0.00395807	0.0322246	1.81698E-06	70.1208
Ethane	0.00146328	0.00146328	0.0119133	7.48744E-07	13.1583
Propane	0.000408082	0.000408082	0.00332238	1.60248E-07	7.70898
i-Butane	1.96877E-05	1.96877E-05	0.000160285	4.87157E-09	0.859887
n-Butane	0.000100484	0.000100484	0.000818086	3.74622E-08	2.2497
i-Pentane	4.46982E-06	4.46982E-06	3.63904E-05	8.39914E-10	0.439942
n-Pentane	6.57199E-06	6.57199E-06	5.35051E-05	1.52444E-09	0.469938
n-Hexane	1.61391E-06	1.61391E-06	1.31394E-05	2.11654E-10	0.579924
Water	80.4418	80.4418	47.0217	99.9411	0.0231808
MDEA	10.2833	10.2833	8.31424E-06	1.9201E-05	0
Piperazine	2.70967	2.70967	1.01086E-05	2.33449E-05	0
O2	0	0	0	0	0

Mass Fraction	7 %	8 %	9 %	10 %	11 %
Hydrogen Sulfide	0.000177169	0.000177169	0.00141678	8.75649E-06	0
N2	1.12068E-05	1.12068E-05	9.17891E-05	4.72322E-09	2.77213
Carbon Dioxide	9.02993	9.02993	73.3054	0.143621	3.99373
Methane	0.0019863	0.0019863	0.016269	1.61663E-06	48.6169
Ethane	0.00137637	0.00137637	0.0112734	1.24865E-06	17.0997
Propane	0.000562901	0.000562901	0.00461049	3.91903E-07	14.6914
i-Butane	3.57953E-05	3.57953E-05	0.000293182	1.57036E-08	2.16
n-Butane	0.000182696	0.000182696	0.00149638	1.2076E-07	5.65115
i-Pentane	1.00881E-05	1.00881E-05	8.26262E-05	3.36088E-09	1.37181
n-Pentane	1.48325E-05	1.48325E-05	0.000121486	6.09999E-09	1.46534
n-Hexane	4.35062E-06	4.35062E-06	3.56336E-05	1.01158E-09	2.15985
Water	45.3328	45.3328	26.6588	99.8561	0.0180484
MDEA	38.3319	38.3319	3.1179E-05	0.000126897	0
Piperazine	7.3011	7.3011	2.74014E-05	0.000111523	0
O2	0	0	0	0	0

Mass Flow	7 lb/h	8 lb/h	9 lb/h	10 lb/h	11 lb/h
Hydrogen Sulfide	0.478877	0.478877	0.467555	0.000710019	0
N2	0.0302912	0.0302912	0.0302916	3.82982E-07	14188.4
Carbon Dioxide	24407.3	24407.3	24191.7	11.6455	20440.8
Methane	5.36883	5.36883	5.36896	0.000131085	248832
Ethane	3.72025	3.72025	3.72035	0.000101247	87519.9
Propane	1.52149	1.52149	1.52152	3.17774E-05	75193.7
i-Butane	0.0967523	0.0967523	0.0967536	1.27333E-06	11055.3
n-Butane	0.493815	0.493815	0.493825	9.79185E-06	28923.8
i-Pentane	0.0272674	0.0272674	0.0272677	2.72517E-07	7021.23
n-Pentane	0.0400914	0.0400914	0.0400919	4.94617E-07	7499.95
n-Hexane	0.0117594	0.0117594	0.0117595	8.20238E-08	11054.6
Water	122532	122532	8797.74	8096.82	92.3759
MDEA	103609	103609	0.0102895	0.0102895	0
Piperazine	19734.4	19734.4	0.00904282	0.00904282	0
O2	0	0	0	0	0

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	Cowboy Amine - Max Capacity	Job:	
Location:			
Flowsheet:	MDEA Flowsheet		

Std Vapor Volumetric Flow	7 MMSCFD	8 MMSCFD	9 MMSCFD	10 MMSCFD	11 MMSCFD
Hydrogen Sulfide	0.000127973	0.000127973	0.000124947	1.89742E-07	0
N2	9.84815E-06	9.84815E-06	9.84828E-06	1.24514E-10	4.61287
Carbon Dioxide	5.05101	5.05101	5.00639	0.00241	4.23015
Methane	0.00304799	0.00304799	0.00304806	7.44192E-08	141.267
Ethane	0.00112683	0.00112683	0.00112686	3.06667E-08	26.5089
Propane	0.000314251	0.000314251	0.000314258	6.56339E-09	15.5307
i-Butane	1.51609E-05	1.51609E-05	1.51611E-05	1.99528E-10	1.73235
n-Butane	7.73797E-05	7.73797E-05	7.73812E-05	1.53436E-09	4.5323
i-Pentane	3.44207E-06	3.44207E-06	3.4421E-06	3.44009E-11	0.886316
n-Pentane	5.06089E-06	5.06089E-06	5.06095E-06	6.24374E-11	0.946747
n-Hexane	1.24282E-06	1.24282E-06	1.24283E-06	8.66884E-12	1.16833
Water	61.9457	61.9457	4.44769	4.09335	0.0467006
MDEA	7.91884	7.91884	7.86428E-07	7.86428E-07	0
Piperazine	2.08663	2.08663	9.5615E-07	9.5615E-07	0
O2	0	0	0	0	0

Stream Properties

Property	Units	7	8	9	10	11
Temperature	°F	115.98	190 *	202.59	120	120 *
Pressure	psia	37.73	27.73	26	26	952.73 *
Molecular Weight	lb/lbmol	31.9676	31.9676	31.7759	18.0306	23.1382
Mass Flow	lb/h	270294	270294	33001.3	8108.49	511822
Std Vapor Volumetric Flow	MMSCFD	77.007	77.007	9.45881	4.09576	201.462
Std Liquid Volumetric Flow	sgpm	558.048	558.048	76.8347	16.2147	2749.41
Mass Cp	Btu/(lb*°F)	0.668315	0.747892	0.283566	0.997566	0.621407
Net Ideal Gas Heating Value	Btu/ft^3	454.236	454.236	0.604559	0.00148998	1181.94
Gross Ideal Gas Heating Value	Btu/ft^3	535.117	535.117	24.3217	50.282	1300.43

Remarks

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	Cowboy Amine - Max Capacity	Job:
Location:		
Flowsheet:	MDEA Flowsheet	

Connections

	11 Acid Gas to TO	12	13	14	14 Lean Amine
From Block	Condenser	Regenerator	Reboiler	--	Reboiler
To Block	--	Reboiler	Regenerator	XCHG-102	PUMP-100

Stream Composition

Mole Fraction	11 Acid Gas to TO %	12 %	13 %	14 %	14 Lean Amine %
Hydrogen Sulfide	0.00232624	5.14145E-06	7.61524E-06	0 *	4.48809E-06
N2	0.000183629	0	0	2.33595 *	0
Carbon Dioxide	93.3047	0.106152	0.259539	0.00490265 *	0.0656399
Methane	0.056833	0	0	71.5074 *	0
Ethane	0.0210109	0	0	13.4159 *	0
Propane	0.00585956	0	0	7.86277 *	0
i-Butane	0.000282691	0	0	0.877226 *	0
n-Butane	0.00144283	0	0	2.29484 *	0
i-Pentane	6.41811E-05	0	0	0.448848 *	0
n-Pentane	9.43657E-05	0	0	0.479427 *	0
n-Hexane	2.31737E-05	0	0	0.591698 *	0
Water	6.60722	88.7973	99.5064	0.180543 *	85.9688
MDEA	7.92995E-14	8.75693	0.0632636	0.000146088 *	11.0531
Piperazine	3.15836E-14	2.33966	0.170741	0.000341412 *	2.9125
O2	0	0	0	0 *	0

Mass Fraction	11 Acid Gas to TO %	12 %	13 %	14 %	14 Lean Amine %
Hydrogen Sulfide	0.00187542	6.14955E-06	1.42109E-05	0 *	4.9031E-06
N2	0.000121687	0	0	2.88456 *	0
Carbon Dioxide	97.1369	0.163953	0.625426	0.00951104 *	0.0926004
Methane	0.0215678	0	0	50.5677 *	0
Ethane	0.0149451	0	0	17.7823 *	0
Propane	0.00611216	0	0	15.2835 *	0
i-Butane	0.000388676	0	0	2.24752 *	0
n-Butane	0.00198377	0	0	5.87957 *	0
i-Pentane	0.00010954	0	0	1.42751 *	0
n-Pentane	0.000161056	0	0	1.52476 *	0
n-Hexane	4.72404E-05	0	0	2.24768 *	0
Water	2.81575	56.1419	98.1565	0.143374 *	49.6456
MDEA	2.23534E-13	36.6215	0.412781	0.000767368 *	42.2201
Piperazine	6.43546E-14	7.07264	0.80528	0.00129632 *	8.0417
O2	0	0	0	0 *	0

Mass Flow	11 Acid Gas to TO lb/h	12 lb/h	13 lb/h	14 lb/h	14 Lean Amine lb/h
Hydrogen Sulfide	0.466845	0.0174244	0.00539214	0 *	0.0120323
N2	0.0302912	0	0	14355.9 *	0
Carbon Dioxide	24180.1	464.552	237.31	47.3346 *	227.242
Methane	5.36883	0	0	251666 *	0
Ethane	3.72025	0	0	88499.3 *	0
Propane	1.52149	0	0	76062.9 *	0
i-Butane	0.0967523	0	0	11185.5 *	0
n-Butane	0.493815	0	0	29261.5 *	0
i-Pentane	0.0272674	0	0	7104.44 *	0
n-Pentane	0.0400914	0	0	7588.44 *	0
n-Hexane	0.0117594	0	0	11186.3 *	0
Water	700.919	159075	37244.3	713.546 *	121831
MDEA	5.56438E-11	103765	156.625	3.81904 *	103609
Piperazine	1.60196E-11	20039.9	305.554	6.45153 *	19734.4

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	Cowboy Amine - Max Capacity	Job:	
Location:			
Flowsheet:	MDEA Flowsheet		

Mass Flow	11 Acid Gas to TO lb/h	12 lb/h	13 lb/h	14 lb/h	14 Lean Amine lb/h
O2	0	0	0	0 *	0

Std Vapor Volumetric Flow	11 Acid Gas to TO MMSCFD	12 MMSCFD	13 MMSCFD	14 MMSCFD	14 Lean Amine MMSCFD
Hydrogen Sulfide	0.000124758	4.65642E-06	1.44097E-06	0 *	3.21544E-06
N2	9.84815E-06	0	0	4.66734 *	0
Carbon Dioxide	5.00398	0.0961375	0.0491106	0.00979574 *	0.047027
Methane	0.00304799	0	0	142.875 *	0
Ethane	0.00112683	0	0	26.8056 *	0
Propane	0.000314251	0	0	15.7102 *	0
i-Butane	1.51609E-05	0	0	1.75274 *	0
n-Butane	7.73797E-05	0	0	4.58521 *	0
i-Pentane	3.44207E-06	0	0	0.89682 *	0
n-Pentane	5.06089E-06	0	0	0.957918 *	0
n-Hexane	1.24282E-06	0	0	1.18224 *	0
Water	0.354349	80.4202	18.8288	0.360733 *	61.5914
MDEA	4.25288E-15	7.93081	0.0119709	0.000291891 *	7.91884
Piperazine	1.69385E-15	2.11894	0.032308	0.000682158 *	2.08663
O2	0	0	0	0 *	0

Stream Properties

Property	Units	11 Acid Gas to TO	12	13	14	14 Lean Amine
Temperature	°F	120	254.519	256.237	141 *	256.237
Pressure	psia	26	29	29	950.73 *	29
Molecular Weight	lb/lbmol	42.2732	28.494	18.263	22.6856	31.1962
Mass Flow	lb/h	24892.8	283345	37943.8	497681 *	245401
Std Vapor Volumetric Flow	MMSCFD	5.36306	90.5661	18.9222	199.805	71.6439
Std Liquid Volumetric Flow	sgpm	60.62	573.611	76.1824	2731.57	497.428
Mass Cp	Btu/(lb*°F)	0.216219	0.939121	0.465779	0.622691	0.930976
Net Ideal Gas Heating Value	Btu/ft^3	1.06512	387.773	7.68997	1205.38	488.159
Gross Ideal Gas Heating Value	Btu/ft^3	4.4959	466.935	58.3874	1326.3	574.838

Remarks

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	Cowboy Amine - Max Capacity	Job:	
Location:			
Flowsheet:	MDEA Flowsheet		

Connections

	15	16	17	18	19
From Block	Lean Rich Exchanger	XCHG-102	SPLT-100	FAXR-101	VLVE-102
To Block	Recycle	--	MIX-101	XCHG-100	MIX-100

Stream Composition

Mole Fraction	15 %	16 %	17 %	18 %	19 %
Hydrogen Sulfide	4.48809E-06	0	0	1.80487E-08	1.1345E-06
N2	0	2.33595	1.47987	1.47817	0.00103384
Carbon Dioxide	0.0656399	0.00490265	0.111991	0.000540475	0.113275
Methane	0	71.5074	70.2052	70.1073	0.0778747
Ethane	0	13.4159	15.3194	15.2974	0.0133299
Propane	0	7.86277	8.52924	8.51865	0.00421561
i-Butane	0	0.877226	0.983915	0.982818	0.000224871
n-Butane	0	2.29484	2.36979	2.36698	0.000769357
i-Pentane	0	0.448848	0.387662	0.387253	4.81832E-05
n-Pentane	0	0.479427	0.379782	0.379372	5.7677E-05
n-Hexane	0	0.591698	0.218501	0.218277	1.48184E-05
Water	85.9688	0.180543	0.0147201	0.262446	99.2205
MDEA	11.0531	0.000146088	0	0.000169857	0.129702
Piperazine	2.9125	0.000341412	0	0.000597097	0.439
O2	0	0	0	0	0

Mass Fraction	15 %	16 %	17 %	18 %	19 %
Hydrogen Sulfide	4.9031E-06	0	0	2.70338E-08	2.09263E-06
N2	0	2.88456	1.81922	1.81988	0.00156745
Carbon Dioxide	0.0926004	0.00951104	0.216285	0.00104538	0.269809
Methane	0	50.5677	49.424	49.4293	0.067615
Ethane	0	17.7823	20.2143	20.2157	0.0216931
Propane	0	15.2835	16.5045	16.5088	0.0100608
i-Butane	0	2.24752	2.50956	2.51053	0.000707377
n-Butane	0	5.87957	6.04436	6.04627	0.00242017
i-Pentane	0	1.42751	1.22738	1.22793	0.000188148
n-Pentane	0	1.52476	1.20243	1.20294	0.00022522
n-Hexane	0	2.24768	0.826294	0.826689	6.9113E-05
Water	49.6456	0.143374	0.0116372	0.207793	96.7426
MDEA	42.2201	0.000767368	0	0.000889552	0.836489
Piperazine	8.0417	0.00129632	0	0.00226036	2.04655
O2	0	0	0	0	0

Mass Flow	15 lb/h	16 lb/h	17 lb/h	18 lb/h	19 lb/h
Hydrogen Sulfide	0.0120323	0	0	0.000166476	1.36508E-05
N2	0	14355.9	11209.1	11206.9	0.0102249
Carbon Dioxide	227.242	47.3346	1332.63	6.43751	1.76004
Methane	0	251666	304524	304390	0.441072
Ethane	0	88499.3	124550	124490	0.14151
Propane	0	76062.9	101692	101663	0.0656293
i-Butane	0	11185.5	15462.5	15460	0.00461442
n-Butane	0	29261.5	37242.1	37233.4	0.0157874
i-Pentane	0	7104.44	7562.47	7561.69	0.00122734
n-Pentane	0	7588.44	7408.75	7407.81	0.00146917
n-Hexane	0	11186.3	5091.18	5090.82	0.000450844
Water	121831	713.546	71.7022	1279.61	631.079
MDEA	103609	3.81904	0	5.47793	5.45665
Piperazine	19734.4	6.45153	0	13.9195	13.3502
O2	0	0	0	0	0

* User Specified Values
? Extrapolated or Approximate Values

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	Cowboy Amine - Max Capacity	Job:	
Location:			
Flowsheet:	MDEA Flowsheet		

Std Vapor Volumetric Flow	15 MMSCFD	16 MMSCFD	17 MMSCFD	18 MMSCFD	19 MMSCFD
Hydrogen Sulfide	3.21544E-06	0	0	4.44883E-08	3.64797E-09
N2	0	4.66734	3.64426	3.64356	3.3243E-06
Carbon Dioxide	0.047027	0.00979574	0.275783	0.00133222	0.000364235
Methane	0	142.875	172.884	172.808	0.000250405
Ethane	0	26.8056	37.7248	37.7067	4.2862E-05
Propane	0	15.7102	21.0037	20.9977	1.35552E-05
i-Butane	0	1.75274	2.42295	2.42255	7.23069E-07
n-Butane	0	4.58521	5.83575	5.83439	2.47386E-06
i-Pentane	0	0.89682	0.954639	0.954541	1.54932E-07
n-Pentane	0	0.957918	0.935234	0.935116	1.85459E-07
n-Hexane	0	1.18224	0.538071	0.538033	4.76483E-08
Water	61.5914	0.360733	0.036249	0.646904	0.319042
MDEA	7.91884	0.000291891	0	0.000418681	0.000417054
Piperazine	2.08663	0.000682158	0	0.00147179	0.0014116
O2	0	0	0	0	0

Stream Properties

Property	Units	15	16	17	18	19
Temperature	°F	170.771	119.877	85	120 *	106.328
Pressure	psia	110	947.73 *	1014	994	89.7 *
Molecular Weight	lb/lbmol	31.1962	22.6856	22.7878	22.7536	18.4767
Mass Flow	lb/h	245401	497681	616146	615808	652.328
Std Vapor Volumetric Flow	MMSCFD	71.6439	199.805	246.256	246.491	0.321548
Std Liquid Volumetric Flow	sgpm	497.428	2731.57	3406.34	3404.16	1.31747
Mass Cp	Btu/(lb*°F)	0.862662	0.633719	0.710092	0.650734	0.981707
Net Ideal Gas Heating Value	Btu/ft^3	488.159	1205.38	1222.83	1221.21	19.6484
Gross Ideal Gas Heating Value	Btu/ft^3	574.838	1326.3	1345.22	1343.56	71.2029

Remarks

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	Cowboy Amine - Max Capacity	Job:	
Location:			
Flowsheet:	MDEA Flowsheet		

Connections

	20	21	22	23	24
From Block	Circulation Pump	Trim Cooler	VLVE-100	--	--
To Block	Trim Cooler	Absorber	--	VLVE-100	VSSL-100

Stream Composition

Mole Fraction	20 %	21 %	22 %	23 %	24 %
Hydrogen Sulfide	4.4473E-06	4.4473E-06	0	0 *	0 *
N2	0	0	2.33375	2.33375 *	0 *
Carbon Dioxide	0.0650499	0.0650499	0.0006829	0.0006829 *	0 *
Methane	0	0	71.4498	71.4498 *	0 *
Ethane	0	0	13.4068	13.4068 *	0 *
Propane	0	0	7.85615	7.85615 *	0 *
i-Butane	0	0	0.876419	0.876419 *	0 *
n-Butane	0	0	2.29276	2.29276 *	0 *
i-Pentane	0	0	0.448435	0.448435 *	0 *
n-Pentane	0	0	0.478995	0.478995 *	0 *
n-Hexane	0	0	0.591136	0.591136 *	0 *
Water	86.0949	86.0949	0.263749	0.263749 *	86.1729 *
MDEA	10.9537	10.9537	0.000199277	0.000199277 *	10.9434 *
Piperazine	2.8864	2.8864	0.00106768	0.00106768 *	2.88369 *
O2	0	0	0	0 *	0 *

Mass Fraction	20 %	21 %	22 %	23 %	24 %
Hydrogen Sulfide	4.87706E-06	4.87706E-06	0	0 *	0 *
N2	0	0	2.88241	2.88241 *	0 *
Carbon Dioxide	0.0921179	0.0921179	0.00132507	0.00132507 *	0 *
Methane	0	0	50.5368	50.5368 *	0 *
Ethane	0	0	17.7738	17.7738 *	0 *
Propane	0	0	15.2736	15.2736 *	0 *
i-Butane	0	0	2.2459	2.2459 *	0 *
n-Butane	0	0	5.8754	5.8754 *	0 *
i-Pentane	0	0	1.42647	1.42647 *	0 *
n-Pentane	0	0	1.52369	1.52369 *	0 *
n-Hexane	0	0	2.24598	2.24598 *	0 *
Water	49.9079	49.9079	0.209492	0.209492 *	50 *
MDEA	42	42	0.00104696	0.00104696 *	42 *
Piperazine	8	8	0.0040547	0.0040547 *	8 *
O2	0	0	0	0 *	0 *

Mass Flow	20 lb/h	21 lb/h	22 lb/h	23 lb/h	24 lb/h
Hydrogen Sulfide	0.0120311	0.0120311	0	0 *	0 *
N2	0	0	14356.4	14356.4 *	0 *
Carbon Dioxide	227.243	227.243	6.59977	6.59977 *	0 *
Methane	0	0	251708	251708 *	0 *
Ethane	0	0	88525.9	88525.9 *	0 *
Propane	0	0	76073	76073 *	0 *
i-Butane	0	0	11186.1	11186.1 *	0 *
n-Butane	0	0	29263.5	29263.5 *	0 *
i-Pentane	0	0	7104.83	7104.83 *	0 *
n-Pentane	0	0	7589.02	7589.02 *	0 *
n-Hexane	0	0	11186.5	11186.5 *	0 *
Water	123116	123116	1043.42	1043.42 *	135705 *
MDEA	103609	103609	5.21461	5.21461 *	113993 *
Piperazine	19735	19735	20.1952	20.1952 *	21712.9 *
O2	0	0	0	0 *	0 *

* User Specified Values
? Extrapolated or Approximate Values

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	Cowboy Amine - Max Capacity	Job:	
Location:			
Flowsheet:	MDEA Flowsheet		

Std Vapor Volumetric Flow	20 MMSCFD	21 MMSCFD	22 MMSCFD	23 MMSCFD	24 MMSCFD
Hydrogen Sulfide	3.21513E-06	3.21513E-06	0	0 *	0 *
N2	0	0	4.6675	4.6675 *	0 *
Carbon Dioxide	0.0470271	0.0470271	0.0013658	0.0013658 *	0 *
Methane	0	0	142.9	142.9 *	0 *
Ethane	0	0	26.8136	26.8136 *	0 *
Propane	0	0	15.7123	15.7123 *	0 *
i-Butane	0	0	1.75284	1.75284 *	0 *
n-Butane	0	0	4.58553	4.58553 *	0 *
i-Pentane	0	0	0.89687	0.89687 *	0 *
n-Pentane	0	0	0.957991	0.957991 *	0 *
n-Hexane	0	0	1.18227	1.18227 *	0 *
Water	62.2414	62.2414	0.527499	0.527499 *	68.6058 *
MDEA	7.91884	7.91884	0.000398555	0.000398555 *	8.7125 *
Piperazine	2.08669	2.08669	0.00213536	0.00213536 *	2.29583 *
O2	0	0	0	0 *	0 *

Stream Properties

Property	Units	20	21	22	23	24
Temperature	°F	172.737	121 *	-16.5011	100 *	125 *
Pressure	psia	1012.73 *	1012.73	15 *	1222.73 *	100 *
Molecular Weight	lb/lbmol	31.0777	31.0777	22.6811	22.6811	31.0486
Mass Flow	lb/h	246687	246687	498069	498069	271411
Std Vapor Volumetric Flow	MMSCFD	72.2939	72.2939	200	200 *	79.6141
Std Liquid Volumetric Flow	sgpm	500	500	2732.66	2732.66	550 *
Mass Cp	Btu/(lb*°F)	0.861367	0.823736	0.432798 ?	0.72949	0.831485
Net Ideal Gas Heating Value	Btu/ft^3	483.772	483.772	1204.44	1204.44	483.319
Gross Ideal Gas Heating Value	Btu/ft^3	570.125	570.125	1325.3	1325.3	569.67

Remarks

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	Cowboy Amine - Max Capacity	Job:	
Location:			
Flowsheet:	MDEA Flowsheet		

Connections

	25	26	27	28	29
From Block	VSSL-100	VSSL-100	FAXR-100	PUMP-100	Absorber
To Block	--	--	SPLT-100	Lean Rich Exchanger	VLVE-101

Stream Composition

Mole Fraction	25 %	26 %	27 %	28 %	29 %
Hydrogen Sulfide		0	0	4.48809E-06	0.000167534
N2		0	1.47987	0	0.000905831
Carbon Dioxide		0	0.111991	0.0656399	6.59567
Methane		0	70.2052	0	0.099376
Ethane		0	15.3194	0	0.0235366
Propane		0	8.52924	0	0.00789564
i-Butane		0	0.983915	0	0.000510626
n-Butane		0	2.36979	0	0.00176595
i-Pentane		0	0.387662	0	0.000127512
n-Pentane		0	0.379782	0	0.000153654
n-Hexane		0	0.218501	0	4.93621E-05
Water		86.1729	0.0147201	85.9688	80.2449
MDEA		10.9434	0	11.0531	10.31
Piperazine		2.88369	0	2.9125	2.71501
O2		0	0	0	0

Mass Fraction	25 %	26 %	27 %	28 %	29 %
Hydrogen Sulfide		0	0	4.9031E-06	0.000178364
N2		0	1.81922	0	0.000792693
Carbon Dioxide		0	0.216285	0.0926004	9.06772
Methane		0	49.424	0	0.0498018
Ethane		0	20.2143	0	0.0221083
Propane		0	16.5045	0	0.0108762
i-Butane		0	2.50956	0	0.000927122
n-Butane		0	6.04436	0	0.00320636
i-Pentane		0	1.22738	0	0.00028739
n-Pentane		0	1.20243	0	0.000346311
n-Hexane		0	0.826294	0	0.000132883
Water		50	0.0116372	49.6456	45.1596
MDEA		42	0	42.2201	38.3786
Piperazine		8	0	8.0417	7.30543
O2		0	0	0	0

Mass Flow	25 lb/h	26 lb/h	27 lb/h	28 lb/h	29 lb/h
Hydrogen Sulfide		0	0	0.0120323	0.481493
N2		0	11379.5	0	2.13988
Carbon Dioxide		0	1352.89	227.242	24478.3
Methane		0	309154	0	134.44
Ethane		0	126443	0	59.6815
Propane		0	103238	0	29.3602
i-Butane		0	15697.7	0	2.50277
n-Butane		0	37808.3	0	8.65558
i-Pentane		0	7677.46	0	0.775812
n-Pentane		0	7521.4	0	0.934868
n-Hexane		0	5168.59	0	0.358718
Water		135705	72.7924	121831	121909
MDEA		113993	0	103609	103603
Piperazine		21712.9	0	19734.4	19721
O2		0	0	0	0

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	Cowboy Amine - Max Capacity	Job:	
Location:			
Flowsheet:	MDEA Flowsheet		

Std Vapor Volumetric Flow	25 MMSCFD	26 MMSCFD	27 MMSCFD	28 MMSCFD	29 MMSCFD
Hydrogen Sulfide		0	0	3.21544E-06	0.000128672
N2		0	3.69967	0	0.00069571
Carbon Dioxide		0	0.279976	0.047027	5.06571
Methane		0	175.513	0	0.0763243
Ethane		0	38.2984	0	0.0180769
Propane		0	21.3231	0	0.00606413
i-Butane		0	2.45979	0	0.000392178
n-Butane		0	5.92448	0	0.00135631
i-Pentane		0	0.969155	0	9.79336E-05
n-Pentane		0	0.949455	0	0.000118012
n-Hexane		0	0.546253	0	3.79118E-05
Water		68.6058	0.0368002	61.5914	61.6309
MDEA		8.7125	0	7.91884	7.91842
Piperazine		2.29583	0	2.08663	2.08522
O2		0	0	0	0

Stream Properties

Property	Units	25	26	27	28	29
Temperature	°F	125	125	85 *	256.511	112.879
Pressure	psia	100	100	1014 *	115 *	1004
Molecular Weight	lb/lbmol		31.0486	22.7878	31.1962	32.0116
Mass Flow	lb/h	0	271411	625515	245401	269950
Std Vapor Volumetric Flow	MMSCFD	0	79.6141	250	71.6439	76.8035
Std Liquid Volumetric Flow	sgpm	0	550	3458.13	497.428	558.262
Mass Cp	Btu/(lb*°F)		0.831485	0.710092	0.93074	0.665536
Net Ideal Gas Heating Value	Btu/ft^3		483.319	1222.83	488.159	456.837
Gross Ideal Gas Heating Value	Btu/ft^3		569.67	1345.22	574.838	537.87

Remarks

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	Cowboy Amine - Max Capacity	Job:
Location:		
Flowsheet:	MDEA Flowsheet	

Connections

	30	32	33	34	35
From Block	MIX-101	Slug Catcher	SPLT-100	VSSL-102	MIX-100
To Block	Slug Catcher	--	--	VLVE-102	Rich Flash

Stream Composition

Mole Fraction	30 %	32 %	33 %	34 %	35 %
Hydrogen Sulfide	5E-05		0	1.1345E-06	0.00016684
N2	1.4519		1.47987	0.00103384	0.000906365
Carbon Dioxide	2		0.111991	0.113275	6.56865
Methane	68.8782		70.2052	0.0778747	0.0992864
Ethane	15.0298		15.3194	0.0133299	0.0234941
Propane	8.36802		8.52924	0.00421561	0.0078803
i-Butane	0.965317		0.983915	0.000224871	0.000509434
n-Butane	2.325		2.36979	0.000769357	0.00176179
i-Pentane	0.380334		0.387662	4.81832E-05	0.000127181
n-Pentane	0.372603		0.379782	5.7677E-05	0.000153254
n-Hexane	0.214371		0.218501	1.48184E-05	4.92181E-05
Water	0.0144418		0.0147201	99.2205	80.324
MDEA	0		0	0.129702	10.2675
Piperazine	0		0	0.439	2.70552
O2	0		0	0	0

Mass Fraction	30 %	32 %	33 %	34 %	35 %
Hydrogen Sulfide	7.34853E-05		0	2.09263E-06	0.000177939
N2	1.75396		1.81922	0.00156745	0.000794561
Carbon Dioxide	3.79574		0.216285	0.269809	9.04651
Methane	47.651		49.424	0.067615	0.0498447
Ethane	19.4891		20.2143	0.0216931	0.0221073
Propane	15.9125		16.5045	0.0100608	0.0108742
i-Butane	2.41953		2.50956	0.000707377	0.000926593
n-Butane	5.82753		6.04436	0.00242017	0.00320446
i-Pentane	1.18335		1.22738	0.000188148	0.000287151
n-Pentane	1.1593		1.20243	0.00022522	0.000346019
n-Hexane	0.796652		0.826294	6.9113E-05	0.000132729
Water	0.0112197		0.0116372	96.7426	45.284
MDEA	0		0	0.836489	38.2881
Piperazine	0		0	2.04655	7.29275
O2	0		0	0	0

Mass Flow	30 lb/h	32 lb/h	33 lb/h	34 lb/h	35 lb/h
Hydrogen Sulfide	0.469624		0	1.36508E-05	0.481507
N2	11209.1		170.435	0.0102249	2.1501
Carbon Dioxide	24257.5		20.2628	1.76004	24480.1
Methane	304524		4630.32	0.441072	134.881
Ethane	124550		1893.79	0.14151	59.823
Propane	101692		1546.24	0.0656293	29.4259
i-Butane	15462.5		235.11	0.00461442	2.50739
n-Butane	37242.1		566.269	0.0157874	8.67137
i-Pentane	7562.47		114.988	0.00122734	0.777039
n-Pentane	7408.75		112.651	0.00146917	0.936337
n-Hexane	5091.18		77.4119	0.000450844	0.359169
Water	71.7022		1.09024	631.079	122540
MDEA	0		0	5.45665	103609
Piperazine	0		0	13.3502	19734.4
O2	0		0	0	0

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	Cowboy Amine - Max Capacity	Job:	
Location:			
Flowsheet:	MDEA Flowsheet		

Std Vapor Volumetric Flow	30 MMSCFD	32 MMSCFD	33 MMSCFD	34 MMSCFD	35 MMSCFD
Hydrogen Sulfide	0.0001255		0	3.64797E-09	0.000128676
N2	3.64426		0.0554113	3.3243E-06	0.000699034
Carbon Dioxide	5.02		0.00419331	0.000364235	5.06607
Methane	172.884		2.62872	0.000250405	0.0765747
Ethane	37.7248		0.57361	4.2862E-05	0.0181198
Propane	21.0037		0.319364	1.35552E-05	0.00607769
i-Butane	2.42295		0.0368411	7.23069E-07	0.000392902
n-Butane	5.83575		0.0887331	2.47386E-06	0.00135878
i-Pentane	0.954639		0.0145154	1.54932E-07	9.80886E-05
n-Pentane	0.935234		0.0142203	1.85459E-07	0.000118197
n-Hexane	0.538071		0.00818143	4.76483E-08	3.79595E-05
Water	0.036249		0.00055117	0.319042	61.9499
MDEA	0		0	0.000417054	7.91884
Piperazine	0		0	0.0014116	2.08663
O2	0		0	0	0

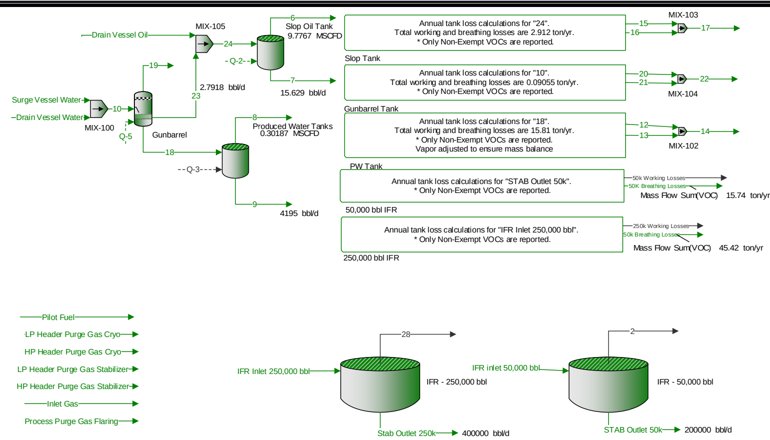
Stream Properties

Property	Units	30	32	33	34	35
Temperature	°F	84.5174		85	104.178	115.969
Pressure	psia	1014	1014	1014	984	89.7
Molecular Weight	lb/lbmol	23.1889		22.7878	18.4767	31.9552
Mass Flow	lb/h	639071	0	9368.56	652.328	270603
Std Vapor Volumetric Flow	MMSCFD	251 *	0	3.74434	0.321548	77.125
Std Liquid Volumetric Flow	sgpm	3462.42	0	51.7938	1.31747	559.579
Mass Cp	Btu/(lb*°F)	0.69854		0.710092	0.981414	0.667963
Net Ideal Gas Heating Value	Btu/ft^3	1199.72		1222.83	19.6484	455.014
Gross Ideal Gas Heating Value	Btu/ft^3	1319.8		1345.22	71.2029	535.925

Remarks

CDP
Plant Schematic

Client Name:	XTO ENERGY INC	Job: DELAWARE DEVELOPMENT
Location:	Cowboy CDP	
Flowsheet:	CDP	



Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	XTO ENERGY INC	Job: DELAWARE DEVELOPMENT
Location:	Cowboy CDP	
Flowsheet:	CDP	

Connections

	Drain Vessel Oil	Drain Vessel Water	HP Header Purge Gas Cryo	HP Header Purge Gas Stabilizer	IFR inlet 50,000 bbl
From Block	--	--	--	--	--
To Block	MIX-105	MIX-100	--	--	IFR - 50,000 bbl

Stream Composition

Mole Fraction	Drain Vessel Oil %	Drain Vessel Water %	HP Header Purge Gas Cryo %	HP Header Purge Gas Stabilizer %	IFR inlet 50,000 bbl %
Water	0.02971 *	99.9794 *	0 *	0 *	0.0150002 *
Hydrogen Sulfide	0 *	0 *	0 *	0 *	0 *
Nitrogen, Atomic	0.00069 *	10E-06 *	1.75018 *	1.75018 *	0 *
Carbon Dioxide	0.01589 *	0.00061 *	0 *	0 *	0.00100001 *
Methane	0.2153 *	4E-05 *	80.188 *	80.188 *	0 *
Ethane	2.31583 *	0.00046 *	16.7417 *	16.7417 *	0.255003 *
Propane	19.3744 *	0.00388 *	1.32013 *	1.32013 *	1.25201 *
Isobutane	5.8018 *	0.00116 *	0 *	0 *	1.21801 *
Butane	16.6133 *	0.00333 *	0 *	0 *	4.83005 *
Isopentane	5.80547 *	0.00116 *	0 *	0 *	3.25303 *
Pentane	7.29616 *	0.00146 *	0 *	0 *	4.66105 *
Cyclopentane	0 *	0 *	0 *	0 *	0 *
i-C6	4.1772 *	0.00084 *	0 *	0 *	3.62804 *
n-Hexane	3.13494 *	0.00063 *	0 *	0 *	2.84403 *
Methylcyclopentane	2.4458 *	0.00049 *	0 *	0 *	2.22902 *
Benzene	2.04093 *	0.00041 *	0 *	0 *	2.09702 *
Cyclohexane	4.88517 *	0.00098 *	0 *	0 *	4.91405 *
2,2,4-Trimethylpentane	0 *	0 *	0 *	0 *	0 *
i-C7	1.94914 *	0.00039 *	0 *	0 *	1.91602 *
Methylcyclohexane	5.03883 *	0.00101 *	0 *	0 *	5.78906 *
n-Heptane	3.07889 *	0.00062 *	0 *	0 *	3.84704 *
Toluene	2.80248 *	0.00056 *	0 *	0 *	3.45803 *
Octane	4.63735 *	0.00093 *	0 *	0 *	6.98707 *
Ethylbenzene	0.13415 *	3E-05 *	0 *	0 *	0.190002 *
m-Xylene	1.42718 *	0.00029 *	0 *	0 *	2.19602 *
Nonane	3.00359 *	0.0006 *	0 *	0 *	6.47506 *
Decane	1.91314 *	0.00038 *	0 *	0 *	5.86906 *
Undecanes Plus	1.86267 *	0.00037 *	0 *	0 *	32.0753 *

Mass Fraction	Drain Vessel Oil %	Drain Vessel Water %	HP Header Purge Gas Cryo %	HP Header Purge Gas Stabilizer %	IFR inlet 50,000 bbl %
Water	0.00696258 *	99.9131 *	0 *	0 *	0.00180123 *
Hydrogen Sulfide	0 *	0 *	0 *	0 *	0 *
Nitrogen, Atomic	0.000125722 *	7.76975E-06 *	1.30914 *	1.30914 *	0 *
Carbon Dioxide	0.00909697 *	0.00148918 *	0 *	0 *	0.000293348 *
Methane	0.0449305 *	3.55961E-05 *	68.6986 *	68.6986 *	0 *
Ethane	0.905843 *	0.00076727 *	26.8835 *	26.8835 *	0.0511089 *
Propane	11.1135 *	0.0094907 *	3.10871 *	3.10871 *	0.36799 *
Isobutane	4.38663 *	0.00374 *	0 *	0 *	0.471874 *
Butane	12.561 *	0.0107364 *	0 *	0 *	1.87122 *
Isopentane	5.4487 *	0.00464257 *	0 *	0 *	1.56441 *
Pentane	6.84778 *	0.00584323 *	0 *	0 *	2.24153 *
Cyclopentane	0 *	0 *	0 *	0 *	0 *
i-C6	4.68268 *	0.00401544 *	0 *	0 *	2.08395 *
n-Hexane	3.5143 *	0.00301158 *	0 *	0 *	1.63361 *
Methylcyclopentane	2.67763 *	0.00228755 *	0 *	0 *	1.2504 *
Benzene	2.07382 *	0.00177653 *	0 *	0 *	1.09182 *

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	XTO ENERGY INC	Job: DELAWARE DEVELOPMENT
Location:	Cowboy CDP	
Flowsheet:	CDP	

Mass Fraction	Drain Vessel Oil %		Drain Vessel Water %		HP Header Purge Gas Cryo %		HP Header Purge Gas Stabilizer %		IFR inlet 50,000 bbl %	
Cyclohexane	5.34822	*	0.0045751	*	0	*	0	*	2.75661	*
2,2,4-Trimethylpentane	0	*	0	*	0	*	0	*	0	*
i-C7	2.54065	*	0.00216776	*	0	*	0	*	1.2797	*
Methylcyclohexane	6.43585	*	0.00550101	*	0	*	0	*	3.7887	*
n-Heptane	4.01326	*	0.00344619	*	0	*	0	*	2.56942	*
Toluene	3.359	*	0.0028622	*	0	*	0	*	2.12375	*
Octane	6.89082	*	0.00589289	*	0	*	0	*	5.31988	*
Ethylbenzene	0.185267	*	0.000176674	*	0	*	0	*	0.134453	*
m-Xylene	1.971	*	0.00170785	*	0	*	0	*	1.554	*
Nonane	5.0112	*	0.00426871	*	0	*	0	*	5.53543	*
Decane	3.54097	*	0.00299919	*	0	*	0	*	5.56609	*
Undecanes Plus	6.43078	*	0.0054472	*	0	*	0	*	56.742	*

Mass Flow	Drain Vessel Oil lb/h		Drain Vessel Water lb/h		HP Header Purge Gas Cryo lb/h		HP Header Purge Gas Stabilizer lb/h		IFR inlet 50,000 bbl lb/h	
Water	0.013378	*	2914.18	*	0	*	0	*	41.3361	*
Hydrogen Sulfide	0	*	0	*	0	*	0	*	0	*
Nitrogen, Atomic	0.000241563	*	0.000226622	*	0.245475	*	0.620148	*	0	*
Carbon Dioxide	0.017479	*	0.0434352	*	0	*	0	*	6.732	*
Methane	0.0863298	*	0.00103824	*	12.8816	*	32.5431	*	0	*
Ethane	1.74049	*	0.0223791	*	5.04091	*	12.7349	*	1172.89	*
Propane	21.3535	*	0.276817	*	0.582912	*	1.47262	*	8444.95	*
Isobutane	8.42851	*	0.109085	*	0	*	0	*	10829	*
Butane	24.1348	*	0.31315	*	0	*	0	*	42942.4	*
Isopentane	10.4692	*	0.135411	*	0	*	0	*	35901.3	*
Pentane	13.1574	*	0.170431	*	0	*	0	*	51440.5	*
Cyclopentane	0	*	0	*	0	*	0	*	0	*
i-C6	8.99734	*	0.117119	*	0	*	0	*	47824.2	*
n-Hexane	6.7524	*	0.0878394	*	0	*	0	*	37489.5	*
Methylcyclopentane	5.14482	*	0.0667213	*	0	*	0	*	28695.3	*
Benzene	3.98466	*	0.0518163	*	0	*	0	*	25056.1	*
Cyclohexane	10.2761	*	0.133443	*	0	*	0	*	63260.9	*
2,2,4-Trimethylpentane	0	*	0	*	0	*	0	*	0	*
i-C7	4.88163	*	0.0632275	*	0	*	0	*	29367.6	*
Methylcyclohexane	12.3659	*	0.160449	*	0	*	0	*	86946.2	*
n-Heptane	7.7111	*	0.100516	*	0	*	0	*	58965.2	*
Toluene	6.454	*	0.0834823	*	0	*	0	*	48737.5	*
Octane	13.2401	*	0.171879	*	0	*	0	*	122085	*
Ethylbenzene	0.355974	*	0.0051531	*	0	*	0	*	3085.55	*
m-Xylene	3.78709	*	0.0498133	*	0	*	0	*	35662.4	*
Nonane	9.62856	*	0.124506	*	0	*	0	*	127032	*
Decane	6.80365	*	0.0874779	*	0	*	0	*	127735	*
Undecanes Plus	12.3561	*	0.15888	*	0	*	0	*	1.30216E+06	*

Std Vapor Volumetric Flow	Drain Vessel Oil MMSCFD		Drain Vessel Water MMSCFD		HP Header Purge Gas Cryo MMSCFD		HP Header Purge Gas Stabilizer MMSCFD		IFR inlet 50,000 bbl MMSCFD	
Water	6.76322E-06	*	1.47326	*	0	*	0	*	0.0208975	*
Hydrogen Sulfide	0	*	0	*	0	*	0	*	0	*
Nitrogen, Atomic	1.57072E-07	*	1.47357E-07	*	0.000159616	*	0.00040324	*	0	*
Carbon Dioxide	3.61722E-06	*	8.98877E-06	*	0	*	0	*	0.00139316	*
Methane	4.90111E-05	*	5.89427E-07	*	0.00731315	*	0.0184753	*	0	*
Ethane	0.000527178	*	6.77841E-06	*	0.00152684	*	0.00385728	*	0.355257	*
Propane	0.00441041	*	5.71744E-05	*	0.000120396	*	0.000304158	*	1.74424	*
Isobutane	0.00132073	*	1.70934E-05	*	0	*	0	*	1.69687	*
Butane	0.00378186	*	4.90698E-05	*	0	*	0	*	6.72898	*

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	XTO ENERGY INC	Job: DELAWARE DEVELOPMENT
Location:	Cowboy CDP	
Flowsheet:	CDP	

Std Vapor Volumetric Flow	Drain Vessel Oil MMSCFD	Drain Vessel Water MMSCFD	HP Header Purge Gas Cryo MMSCFD	HP Header Purge Gas Stabilizer MMSCFD	IFR inlet 50,000 bbl MMSCFD
Isopentane	0.00132156 *	1.70934E-05 *	0 *	0 *	4.53196 *
Pentane	0.00166091 *	2.15141E-05 *	0 *	0 *	6.49353 *
Cyclopentane	0 *	0 *	0 *	0 *	0 *
i-C6	0.000950902 *	1.2378E-05 *	0 *	0 *	5.0544 *
n-Hexane	0.000713641 *	9.28348E-06 *	0 *	0 *	3.96216 *
Methylcyclopentane	0.000556765 *	7.22048E-06 *	0 *	0 *	3.10536 *
Benzene	0.000464599 *	6.04163E-06 *	0 *	0 *	2.92146 *
Cyclohexane	0.00111207 *	1.4441E-05 *	0 *	0 *	6.846 *
2,2,4-Trimethylpentane	0 *	0 *	0 *	0 *	0 *
i-C7	0.000443704 *	5.74692E-06 *	0 *	0 *	2.6693 *
Methylcyclohexane	0.00114704 *	1.4883E-05 *	0 *	0 *	8.06502 *
n-Heptane	0.000700882 *	9.13612E-06 *	0 *	0 *	5.3595 *
Toluene	0.00063796 *	8.25198E-06 *	0 *	0 *	4.81756 *
Octane	0.00105565 *	1.37042E-05 *	0 *	0 *	9.73403 *
Ethylbenzene	3.0538E-05 *	4.4207E-07 *	0 *	0 *	0.264701 *
m-Xylene	0.000324885 *	4.27335E-06 *	0 *	0 *	3.05939 *
Nonane	0.00068374 *	8.84141E-06 *	0 *	0 *	9.02073 *
Decane	0.000435509 *	5.59956E-06 *	0 *	0 *	8.17648 *
Undecanes Plus	0.00042402 *	5.4522E-06 *	0 *	0 *	44.6857 *

Stream Properties

Property	Units	Drain Vessel Oil	Drain Vessel Water	HP Header Purge Gas Cryo	HP Header Purge Gas Stabilizer	IFR inlet 50,000 bbl
Temperature	°F	75 *	100 *	65 *	65	90 *
Pressure	psig	30 *	30 *	50 *	50	0 *
Molecular Weight	lb/lbmol	76.8729	18.0272	18.7255	18.7255	150.026
Molar Flow	lbmol/h	2.49946	161.795	1.00136	2.52975	15296.5
Std Vapor Volumetric Flow	MMSCFD	0.0227641	1.47357	0.00912 *	0.02304 *	139.315
Std Liquid Volumetric Flow	sgpm	0.583333 *	5.83333 *	0.117067	0.295749	5833.33 *
Net Ideal Gas Heating Value	Btu/ft^3	3888.41	0.778807	1040.21	1040.21	7401.09
Gross Ideal Gas Heating Value	Btu/ft^3	4187.78	51.1384	1148.76	1148.76	7911.89

Remarks

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	XTO ENERGY INC	Job: DELAWARE DEVELOPMENT
Location:	Cowboy CDP	
Flowsheet:	CDP	

Connections

	IFR Inlet 250,000 bbl	Inlet Gas	LP Header Purge Gas Cryo	LP Header Purge Gas Stabilizer	Pilot Fuel
From Block	--	--	--	--	--
To Block	IFR - 250,000 bbl	--	--	--	--

Stream Composition

Mole Fraction	IFR Inlet 250,000 bbl %	Inlet Gas %	LP Header Purge Gas Cryo %	LP Header Purge Gas Stabilizer %	Pilot Fuel %
Water	0.0150002 *	0.0149999 *	0 *	0 *	0 *
Hydrogen Sulfide	0 *	0 *	0 *	0 *	0 *
Nitrogen, Atomic	0 *	1.59198 *	1.75018 *	1.75018 *	3.88039 *
Carbon Dioxide	0.00100001 *	0.112999 *	0 *	0 *	0 *
Methane	0 *	73.5163 *	80.188 *	80.188 *	79.658 *
Ethane	0.255003 *	14.7199 *	16.7417 *	16.7417 *	15.3715 *
Propane	1.25201 *	7.21593 *	1.32013 *	1.32013 *	1.09011 *
Isobutane	1.21801 *	0.723993 *	0 *	0 *	0 *
Butane	4.83005 *	1.62298 *	0 *	0 *	0 *
Isopentane	3.25303 *	0.207998 *	0 *	0 *	0 *
Pentane	4.66105 *	0.191998 *	0 *	0 *	0 *
Cyclopentane	0 *	0 *	0 *	0 *	0 *
i-C6	3.62804 *	0.0369996 *	0 *	0 *	0 *
n-Hexane	2.84403 *	0.0159998 *	0 *	0 *	0 *
Methylcyclopentane	2.22902 *	0.00899991 *	0 *	0 *	0 *
Benzene	2.09702 *	0.00199998 *	0 *	0 *	0 *
Cyclohexane	4.91405 *	0.00899991 *	0 *	0 *	0 *
2,2,4-Trimethylpentane	0 *	0 *	0 *	0 *	0 *
i-C7	1.91602 *	0.00299997 *	0 *	0 *	0 *
Methylcyclohexane	5.78906 *	0.00299997 *	0 *	0 *	0 *
n-Heptane	3.84704 *	0.00099999 *	0 *	0 *	0 *
Toluene	3.45803 *	0 *	0 *	0 *	0 *
Octane	6.98707 *	0.00099999 *	0 *	0 *	0 *
Ethylbenzene	0.190002 *	0 *	0 *	0 *	0 *
m-Xylene	2.19602 *	0 *	0 *	0 *	0 *
Nonane	6.47506 *	0 *	0 *	0 *	0 *
Decane	5.86906 *	0 *	0 *	0 *	0 *
Undecanes Plus	32.0753 *	0 *	0 *	0 *	0 *

Mass Fraction	IFR Inlet 250,000 bbl %	Inlet Gas %	LP Header Purge Gas Cryo %	LP Header Purge Gas Stabilizer %	Pilot Fuel %
Water	0.00180123 *	0.0126271 *	0 *	0 *	0 *
Hydrogen Sulfide	0 *	0 *	0 *	0 *	0 *
Nitrogen, Atomic	0 *	1.04196 *	1.30914 *	1.30914 *	2.94981 *
Carbon Dioxide	0.000293348 *	0.232379 *	0 *	0 *	0 *
Methane	0 *	55.1101 *	68.6986 *	68.6986 *	69.356 *
Ethane	0.0511089 *	20.6824 *	26.8835 *	26.8835 *	25.0854 *
Propane	0.36799 *	14.8684 *	3.10871 *	3.10871 *	2.60885 *
Isobutane	0.471874 *	1.96632 *	0 *	0 *	0 *
Butane	1.87122 *	4.40792 *	0 *	0 *	0 *
Isopentane	1.56441 *	0.701238 *	0 *	0 *	0 *
Pentane	2.24153 *	0.647296 *	0 *	0 *	0 *
Cyclopentane	0 *	0 *	0 *	0 *	0 *
i-C6	2.08395 *	0.14899 *	0 *	0 *	0 *
n-Hexane	1.63361 *	0.0644282 *	0 *	0 *	0 *
Methylcyclopentane	1.2504 *	0.0353931 *	0 *	0 *	0 *
Benzene	1.09182 *	0.00729995 *	0 *	0 *	0 *

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	XTO ENERGY INC	Job: DELAWARE DEVELOPMENT
Location:	Cowboy CDP	
Flowsheet:	CDP	

Mass Fraction	IFR Inlet 250,000 bbl %	Inlet Gas %	LP Header Purge Gas Cryo %	LP Header Purge Gas Stabilizer %	Pilot Fuel %
Cyclohexane	2.75661 *	0.0353931 *	0 *	0 *	0 *
2,2,4-Trimethylpentane	0 *	0 *	0 *	0 *	0 *
i-C7	1.2797 *	0.0140466 *	0 *	0 *	0 *
Methylcyclohexane	3.7887 *	0.013764 *	0 *	0 *	0 *
n-Heptane	2.56942 *	0.00468219 *	0 *	0 *	0 *
Toluene	2.12375 *	0 *	0 *	0 *	0 *
Octane	5.31988 *	0.00533762 *	0 *	0 *	0 *
Ethylbenzene	0.134453 *	0 *	0 *	0 *	0 *
m-Xylene	1.554 *	0 *	0 *	0 *	0 *
Nonane	5.53543 *	0 *	0 *	0 *	0 *
Decane	5.56609 *	0 *	0 *	0 *	0 *
Undecanes Plus	56.742 *	0 *	0 *	0 *	0 *

Mass Flow	IFR Inlet 250,000 bbl lb/h	Inlet Gas lb/h	LP Header Purge Gas Cryo lb/h	LP Header Purge Gas Stabilizer lb/h	Pilot Fuel lb/h
Water	82.6722 *	14.2418 *	0 *	0 *	0 *
Hydrogen Sulfide	0 *	0 *	0 *	0 *	0 *
Nitrogen, Atomic	0 *	1175.2 *	0.374673 *	0.976733 *	0.716123 *
Carbon Dioxide	13.464 *	262.094 *	0 *	0 *	0 *
Methane	0 *	62157.1 *	19.6614 *	51.2553 *	16.8375 *
Ethane	2345.78 *	23327 *	7.69401 *	20.0575 *	6.08995 *
Propane	16889.9 *	16769.7 *	0.889708 *	2.31938 *	0.633347 *
Isobutane	21657.9 *	2217.75 *	0 *	0 *	0 *
Butane	85884.8 *	4971.56 *	0 *	0 *	0 *
Isopentane	71802.6 *	790.905 *	0 *	0 *	0 *
Pentane	102881 *	730.067 *	0 *	0 *	0 *
Cyclopentane	0 *	0 *	0 *	0 *	0 *
i-C6	95648.4 *	168.042 *	0 *	0 *	0 *
n-Hexane	74979.1 *	72.6667 *	0 *	0 *	0 *
Methylcyclopentane	57390.6 *	39.9188 *	0 *	0 *	0 *
Benzene	50112.1 *	8.2334 *	0 *	0 *	0 *
Cyclohexane	126522 *	39.9188 *	0 *	0 *	0 *
2,2,4-Trimethylpentane	0 *	0 *	0 *	0 *	0 *
i-C7	58735.3 *	15.8427 *	0 *	0 *	0 *
Methylcyclohexane	173892 *	15.524 *	0 *	0 *	0 *
n-Heptane	117930 *	5.28091 *	0 *	0 *	0 *
Toluene	97475 *	0 *	0 *	0 *	0 *
Octane	244170 *	6.02014 *	0 *	0 *	0 *
Ethylbenzene	6171.1 *	0 *	0 *	0 *	0 *
m-Xylene	71324.9 *	0 *	0 *	0 *	0 *
Nonane	254063 *	0 *	0 *	0 *	0 *
Decane	255470 *	0 *	0 *	0 *	0 *
Undecanes Plus	2.60432E+06 *	0 *	0 *	0 *	0 *

Std Vapor Volumetric Flow	IFR Inlet 250,000 bbl MMSCFD	Inlet Gas MMSCFD	LP Header Purge Gas Cryo MMSCFD	LP Header Purge Gas Stabilizer MMSCFD	Pilot Fuel MMSCFD
Water	0.0417949 *	0.00719993 *	0 *	0 *	0 *
Hydrogen Sulfide	0 *	0 *	0 *	0 *	0 *
Nitrogen, Atomic	0 *	0.764152 *	0.000243624 *	0.000635104 *	0.000465647 *
Carbon Dioxide	0.00278633 *	0.0542395 *	0 *	0 *	0 *
Methane	0 *	35.2878 *	0.0111622 *	0.0290986 *	0.00955896 *
Ethane	0.710513 *	7.06553 *	0.00233044 *	0.00607522 *	0.00184458 *
Propane	3.48848 *	3.46365 *	0.000183762 *	0.00047905 *	0.000130813 *
Isobutane	3.39375 *	0.347517 *	0 *	0 *	0 *
Butane	13.458 *	0.779032 *	0 *	0 *	0 *

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	XTO ENERGY INC	Job: DELAWARE DEVELOPMENT
Location:	Cowboy CDP	
Flowsheet:	CDP	

Std Vapor Volumetric Flow	IFR Inlet 250,000 bbl MMSCFD		Inlet Gas MMSCFD		LP Header Purge Gas Cryo MMSCFD		LP Header Purge Gas Stabilizer MMSCFD		Pilot Fuel MMSCFD	
Isopentane	9.06392	*	0.099839	*	0	*	0	*	0	*
Pentane	12.9871	*	0.0921591	*	0	*	0	*	0	*
Cyclopentane	0	*	0	*	0	*	0	*	0	*
i-C6	10.1088	*	0.0177598	*	0	*	0	*	0	*
n-Hexane	7.92431	*	0.00767992	*	0	*	0	*	0	*
Methylcyclopentane	6.21072	*	0.00431996	*	0	*	0	*	0	*
Benzene	5.84293	*	0.00095999	*	0	*	0	*	0	*
Cyclohexane	13.692	*	0.00431996	*	0	*	0	*	0	*
2,2,4-Trimethylpentane	0	*	0	*	0	*	0	*	0	*
i-C7	5.3386	*	0.00143999	*	0	*	0	*	0	*
Methylcyclohexane	16.13	*	0.00143999	*	0	*	0	*	0	*
n-Heptane	10.719	*	0.000479995	*	0	*	0	*	0	*
Toluene	9.63512	*	0	*	0	*	0	*	0	*
Octane	19.4681	*	0.000479995	*	0	*	0	*	0	*
Ethylbenzene	0.529402	*	0	*	0	*	0	*	0	*
m-Xylene	6.11877	*	0	*	0	*	0	*	0	*
Nonane	18.0415	*	0	*	0	*	0	*	0	*
Decane	16.353	*	0	*	0	*	0	*	0	*
Undecanes Plus	89.3714	*	0	*	0	*	0	*	0	*

Stream Properties

Property	Units	IFR Inlet 250,000 bbl		Inlet Gas		LP Header Purge Gas Cryo		LP Header Purge Gas Stabilizer		Pilot Fuel	
Temperature	°F	90	*	65	*	65	*	65		65	*
Pressure	psig	0	*	1150	*	50	*	50		50	*
Molecular Weight	lb/lbmol	150.026		21.4004		18.7255		18.7255		18.4254	
Molar Flow	lbmol/h	30593.1		5270.32		1.52839		3.98436		1.31758	
Std Vapor Volumetric Flow	MMSCFD	278.63		48	*	0.01392	*	0.036288	*	0.012	*
Std Liquid Volumetric Flow	sgpm	11666.7	*	645.753		0.178682		0.465805		0.150691	
Net Ideal Gas Heating Value	Btu/ft^3	7401.09		1171.41		1040.21		1040.21		1019.29	
Gross Ideal Gas Heating Value	Btu/ft^3	7911.89		1289.45		1148.76		1148.76		1124.78	

Remarks

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	XTO ENERGY INC	Job: DELAWARE DEVELOPMENT
Location:	Cowboy CDP	
Flowsheet:	CDP	

Connections

	Process Purge Gas Flaring	STAB Outlet 50k	Stab Outlet 250k	Surge Vessel Water	2
From Block	--	IFR - 50,000 bbl	IFR - 250,000 bbl	--	IFR - 50,000 bbl
To Block	--	--	--	MIX-100	--

Stream Composition

Mole Fraction	Process Purge Gas Flaring %	STAB Outlet 50k %	Stab Outlet 250k %	Surge Vessel Water %	2 %
Water	0.88 *	0.0150002	0.0150002	99.9794 *	
Hydrogen Sulfide	0 *	0	0	0 *	
Nitrogen, Atomic	0 *	0	0	7E-06 *	
Carbon Dioxide	0.05 *	0.00100001	0.00100001	0.000613 *	
Methane	0.02 *	0	0	4.3E-05 *	
Ethane	14.64 *	0.255003	0.255003	0.000464 *	
Propane	62.92 *	1.25201	1.25201	0.003878 *	
Isobutane	5.84 *	1.21801	1.21801	0.001161 *	
Butane	10 *	4.83005	4.83005	0.003325 *	
Isopentane	1.54 *	3.25303	3.25303	0.001162 *	
Pentane	1.51 *	4.66105	4.66105	0.00146 *	
Cyclopentane	0 *	0	0	0 *	
i-C6	0.57 *	3.62804	3.62804	0.000836 *	
n-Hexane	0.3 *	2.84403	2.84403	0.000628 *	
Methylcyclopentane	0.24 *	2.22902	2.22902	0.00049 *	
Benzene	0.25 *	2.09702	2.09702	0.000409 *	
Cyclohexane	0.45 *	4.91405	4.91405	0.000978 *	
2,2,4-Trimethylpentane	0 *	0	0	0 *	
i-C7	0.09 *	1.91602	1.91602	0.00039 *	
Methylcyclohexane	0.25 *	5.78906	5.78906	0.001009 *	
n-Heptane	0.15 *	3.84704	3.84704	0.000616 *	
Toluene	0.13 *	3.45803	3.45803	0.000561 *	
Octane	0.1 *	6.98707	6.98707	0.000928 *	
Ethylbenzene	0 *	0.190002	0.190002	2.7E-05 *	
m-Xylene	0.02 *	2.19602	2.19602	0.000286 *	
Nonane	0.03 *	6.47506	6.47506	0.000601 *	
Decane	0.01 *	5.86906	5.86906	0.000383 *	
Undecanes Plus	0.01 *	32.0753	32.0753	0.000373 *	

Mass Fraction	Process Purge Gas Flaring %	STAB Outlet 50k %	Stab Outlet 250k %	Surge Vessel Water %	2 %
Water	0.344012 *	0.00180123	0.00180123	99.9132 *	
Hydrogen Sulfide	0 *	0	0	0 *	
Nitrogen, Atomic	0 *	0	0	5.43883E-06 *	
Carbon Dioxide	0.0477492 *	0.000293348	0.000293348	0.0014965 *	
Methane	0.00696226 *	0	0	3.82658E-05 *	
Ethane	9.55234 *	0.0511089	0.0511089	0.000773943 *	
Propane	60.2051 *	0.36799	0.36799	0.00948581 *	
Isobutane	7.36553 *	0.471874	0.471874	0.00374322 *	
Butane	12.6122 *	1.87122	1.87122	0.0107203 *	
Isopentane	2.41101 *	1.56441	1.56441	0.00465057 *	
Pentane	2.36404 *	2.24153	2.24153	0.00584323 *	
Cyclopentane	0 *	0	0	0 *	
i-C6	1.06588 *	2.08395	2.08395	0.00399632 *	
n-Hexane	0.560988 *	1.63361	1.63361	0.00300202 *	
Methylcyclopentane	0.438292 *	1.2504	1.2504	0.00228755 *	
Benzene	0.423747 *	1.09182	1.09182	0.00177219 *	

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	XTO ENERGY INC	Job: DELAWARE DEVELOPMENT
Location:	Cowboy CDP	
Flowsheet:	CDP	

Mass Fraction	Process Purge Gas Flaring %		STAB Outlet 50k %	Stab Outlet 250k %	Surge Vessel Water %		2 %
Cyclohexane	0.821798	*	2.75661	2.75661	0.00456576	*	
2,2,4-Trimethylpentane	0	*	0	0	0	*	
i-C7	0.19569	*	1.2797	1.2797	0.00216776	*	
Methylcyclohexane	0.532647	*	3.7887	3.7887	0.00549556	*	
n-Heptane	0.326149	*	2.56942	2.56942	0.00342396	*	
Toluene	0.259916	*	2.12375	2.12375	0.00286731	*	
Octane	0.24787	*	5.31988	5.31988	0.00588022	*	
Ethylbenzene	0	*	0.134453	0.134453	0.000159007	*	
m-Xylene	0.0460745	*	1.554	1.554	0.0016843	*	
Nonane	0.0834921	*	5.53543	5.53543	0.00427583	*	
Decane	0.0308744	*	5.56609	5.56609	0.00302287	*	
Undecanes Plus	0.0575904	*	56.742	56.742	0.00549137	*	

Mass Flow	Process Purge Gas Flaring lb/h		STAB Outlet 50k lb/h	Stab Outlet 250k lb/h	Surge Vessel Water lb/h		2 lb/h
Water	208.882	*	41.3361	82.6722	58283.7	*	
Hydrogen Sulfide	0	*	0	0	0	*	
Nitrogen, Atomic	0	*	0	0	0.0031727	*	
Carbon Dioxide	28.993	*	6.732	13.464	0.872977	*	
Methane	4.22744	*	0	0	0.0223221	*	
Ethane	5800.12	*	1172.89	2345.78	0.451475	*	
Propane	36556.2	*	8444.95	16889.9	5.53349	*	
Isobutane	4472.31	*	10829	21657.9	2.18358	*	
Butane	7658.06	*	42942.4	85884.8	6.25359	*	
Isopentane	1463.95	*	35901.3	71802.6	2.71288	*	
Pentane	1435.43	*	51440.5	102881	3.40861	*	
Cyclopentane	0	*	0	0	0	*	
i-C6	647.194	*	47824.2	95648.4	2.33123	*	
n-Hexane	340.628	*	37489.5	74979.1	1.75121	*	
Methylcyclopentane	266.128	*	28695.3	57390.6	1.33443	*	
Benzene	257.296	*	25056.1	50112.1	1.0338	*	
Cyclohexane	498.99	*	63260.9	126522	2.66341	*	
2,2,4-Trimethylpentane	0	*	0	0	0	*	
i-C7	118.822	*	29367.6	58735.3	1.26455	*	
Methylcyclohexane	323.42	*	86946.2	173892	3.2058	*	
n-Heptane	198.036	*	58965.2	117930	1.99734	*	
Toluene	157.82	*	48737.5	97475	1.67263	*	
Octane	150.505	*	122085	244170	3.43019	*	
Ethylbenzene	0	*	3085.55	6171.1	0.0927558	*	
m-Xylene	27.9761	*	35662.4	71324.9	0.982524	*	
Nonane	50.6959	*	127032	254063	2.49428	*	
Decane	18.7467	*	127735	255470	1.76337	*	
Undecanes Plus	34.9685	*	1.30216E+06	2.60432E+06	3.20336	*	

Std Vapor Volumetric Flow	Process Purge Gas Flaring MMSCFD		STAB Outlet 50k MMSCFD	Stab Outlet 250k MMSCFD	Surge Vessel Water MMSCFD		2 MMSCFD
Water	0.1056	*	0.0208975	0.0417949	29.4653	*	
Hydrogen Sulfide	0	*	0	0	0	*	
Nitrogen, Atomic	0	*	0	0	2.063E-06	*	
Carbon Dioxide	0.006	*	0.00139316	0.00278633	0.00018066	*	
Methane	0.0024	*	0	0	1.26727E-05	*	
Ethane	1.7568	*	0.355257	0.710513	0.000136747	*	
Propane	7.5504	*	1.74424	3.48848	0.0011429	*	
Isobutane	0.7008	*	1.69687	3.39375	0.000342163	*	
Butane	1.2	*	6.72898	13.458	0.000979923	*	

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	XTO ENERGY INC	Job: DELAWARE DEVELOPMENT
Location:	Cowboy CDP	
Flowsheet:	CDP	

Std Vapor Volumetric Flow	Process Purge Gas Flaring MMSCFD	STAB Outlet 50k MMSCFD	Stab Outlet 250k MMSCFD	Surge Vessel Water MMSCFD	2 MMSCFD
Isopentane	0.1848 *	4.53196	9.06392	0.000342457 *	
Pentane	0.1812 *	6.49353	12.9871	0.000430282 *	
Cyclopentane	0 *	0	0	0 *	
i-C6	0.0684 *	5.0544	10.1088	0.000246381 *	
n-Hexane	0.036 *	3.96216	7.92431	0.00018508 *	
Methylcyclopentane	0.0288 *	3.10536	6.21072	0.00014441 *	
Benzene	0.03 *	2.92146	5.84293	0.000120538 *	
Cyclohexane	0.054 *	6.846	13.692	0.00028823 *	
2,2,4-Trimethylpentane	0 *	0	0	0 *	
i-C7	0.0108 *	2.6693	5.3386	0.000114938 *	
Methylcyclohexane	0.03 *	8.06502	16.13	0.000297366 *	
n-Heptane	0.018 *	5.3595	10.719	0.000181544 *	
Toluene	0.0156 *	4.81756	9.63512	0.000165334 *	
Octane	0.012 *	9.73403	19.4681	0.000273494 *	
Ethylbenzene	0 *	0.264701	0.529402	7.95727E-06 *	
m-Xylene	0.0024 *	3.05939	6.11877	8.42881E-05 *	
Nonane	0.0036 *	9.02073	18.0415	0.000177123 *	
Decane	0.0012 *	8.17648	16.353	0.000112875 *	
Undecanes Plus	0.0012 *	44.6857	89.3714	0.000109928 *	

Stream Properties

Property	Units	Process Purge Gas Flaring	STAB Outlet 50k	Stab Outlet 250k	Surge Vessel Water	2
Temperature	°F	65 *	90	90	100 *	
Pressure	psig	1150 *	0	0	5 *	0 *
Molecular Weight	lb/lbmol	46.0841	150.026	150.026	18.0272	
Molar Flow	lbmol/h	1317.58	15296.5	30593.1	3235.91	0
Std Vapor Volumetric Flow	MMSCFD	12 *	139.315	278.63	29.4714	0
Std Liquid Volumetric Flow	sgpm	236.904	5833.33	11666.7	116.667 *	0
Net Ideal Gas Heating Value	Btu/ft^3	2399.81	7401.09	7401.09	0.778404	
Gross Ideal Gas Heating Value	Btu/ft^3	2606.34	7911.89	7911.89	51.1379	

Remarks

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	XTO ENERGY INC	Job: DELAWARE DEVELOPMENT
Location:	Cowboy CDP	
Flowsheet:	CDP	

Connections

	6	7	8	9	10
From Block	Slop Oil Tank	Slop Oil Tank	Produced Water Tanks	Produced Water Tanks	MIX-100
To Block	--	--	--	--	Gunbarrel

Stream Composition

Mole Fraction	6 %	7 %	8 %	9 %	10 %
Water	0.0879855	0.00144971	5.35318	99.9972	99.9794
Hydrogen Sulfide	0	0	0	0	0
Nitrogen, Atomic	0.00163655	2.83221E-06	0.0729867	1.20371E-08	7.14286E-06
Carbon Dioxide	0.04013	0.000491757	1.30441	0.000484461	0.000612857
Methane	0.498263	0.00215766	0.364216	7.19926E-06	4.28571E-05
Ethane	5.18558	0.144318	3.6464	0.000100406	0.00046381
Propane	39.5322	3.92941	31.308	0.000599379	0.0038781
Isobutane	9.97561	2.52308	9.11903	0.000111588	0.00116095
Butane	25.2753	9.5727	23.6289	0.000414408	0.00332524
Isopentane	5.81939	5.65243	6.73203	7.84121E-05	0.0011619
Pentane	6.18706	8.04114	7.83556	4.11176E-05	0.00146
Cyclopentane	0	0	0	0	0
i-C6	1.88319	5.9821	2.76608	1.86134E-05	0.00083619
n-Hexane	1.0515	4.81409	1.65509	5.69474E-06	0.000628095
Methylcyclopentane	0.818112	3.71651	1.21798	3.21685E-05	0.00049
Benzene	0.567427	2.70599	0.161757	0.000346784	0.000409048
Cyclohexane	1.25339	7.68273	1.84743	0.000109775	0.000978095
2,2,4-Trimethylpentane	0	0	0	0	0
i-C7	0.338974	3.27789	0.579407	2.32298E-06	0.00039
Methylcyclohexane	0.590718	8.70381	1.03329	2.60872E-05	0.00100905
n-Heptane	0.374001	5.33103	0.666389	1.59478E-06	0.00061619
Toluene	0.25936	4.30879	0.210587	0.0003408	0.000560952
Octane	0.171849	8.40704	0.334859	3.57229E-07	0.000928095
Ethylbenzene	0.00421662	0.228145	0.00621393	8.4984E-06	2.71429E-05
m-Xylene	0.0423252	2.47536	0.0682491	6.40514E-05	0.00028619
Nonane	0.034407	5.52115	0.0721118	6.47871E-08	0.000600952
Decane	0.00731248	3.53185	0.015892	4.37825E-09	0.000382857
Undecanes Plus	5.28141E-07	3.44631	1.71347E-06	3.64412E-11	0.000372857

Mass Fraction	6 %	7 %	8 %	9 %	10 %
Water	0.0289221	0.000276175	1.73443	99.9904	99.9131
Hydrogen Sulfide	0	0	0	0	0
Nitrogen, Atomic	0.000418256	4.19492E-07	0.0183858	9.35812E-09	5.54982E-06
Carbon Dioxide	0.0322251	0.000228855	1.03244	0.00118341	0.00149616
Methane	0.14585	0.000366031	0.105083	6.41044E-06	3.81387E-05
Ethane	2.84508	0.0458884	1.97191	0.000167575	0.000773625
Propane	31.8071	1.83225	24.8287	0.00146699	0.00948604
Isobutane	10.5794	1.55073	9.53222	0.00035999	0.00374307
Butane	26.805	5.88355	24.6995	0.0013369	0.010721
Isopentane	7.66098	4.31248	8.73531	0.000314008	0.00465019
Pentane	8.145	6.13492	10.1672	0.000164659	0.00584323
Cyclopentane	0	0	0	0	0
i-C6	2.96111	5.45129	4.28698	8.90304E-05	0.00399723
n-Hexane	1.65338	4.38693	2.56513	2.72387E-05	0.00300248
Methylcyclopentane	1.2563	3.30751	1.84351	0.000150267	0.00228755
Benzene	0.808732	2.23515	0.227239	0.00150351	0.0017724
Cyclohexane	1.92472	6.83725	2.79624	0.000512785	0.00456621
2,2,4-Trimethylpentane	0	0	0	0	0
i-C7	0.619756	3.47323	1.04415	1.29197E-05	0.00216776
Methylcyclohexane	1.0583	9.03696	1.82463	0.00014217	0.00549582
n-Heptane	0.683797	5.64872	1.2009	8.86965E-06	0.00342501
Toluene	0.436036	4.19816	0.34896	0.00174289	0.00286707

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	XTO ENERGY INC	Job: DELAWARE DEVELOPMENT
Location:	Cowboy CDP	
Flowsheet:	CDP	

Mass Fraction	**6 %**	**7 %**	**8 %**	**9 %**	**10 %**
Octane	0.358179	10.155	0.687924	2.26491E-06	0.00588083
Ethylbenzene	0.00816814	0.256127	0.0118645	5.00781E-05	0.000159848
m-Xylene	0.0819896	2.77896	0.130311	0.000377432	0.00168542
Nonane	0.0805191	7.48802	0.166335	4.61204E-07	0.00427549
Decane	0.0189842	5.31391	0.0406658	3.45764E-08	0.00302174
Undecanes Plus	2.55758E-06	9.67206	8.17861E-06	5.36813E-10	0.00548927

Mass Flow	**6 lb/h**	**7 lb/h**	**8 lb/h**	**9 lb/h**	**10 lb/h**
Water	0.0170152	0.000448821	0.0319647	61197.6	61197.9
Hydrogen Sulfide	0	0	0	0	0
Nitrogen, Atomic	0.000246065	6.81731E-07	0.000338842	5.7275E-06	0.00339933
Carbon Dioxide	0.0189584	0.000371919	0.0190273	0.724287	0.916412
Methane	0.0858056	0.000594849	0.00193663	0.00392341	0.0233603
Ethane	1.6738	0.0745748	0.0363414	0.102562	0.473854
Propane	18.7125	2.97766	0.45758	0.897847	5.81031
Isobutane	6.22397	2.52014	0.175674	0.220326	2.29267
Butane	15.7697	9.56155	0.4552	0.818229	6.56674
Isopentane	4.50705	7.00836	0.160988	0.192184	2.84829
Pentane	4.79181	9.97007	0.187377	0.100777	3.57904
Cyclopentane	0	0	0	0	0
i-C6	1.74206	8.85908	0.0790069	0.0544897	2.44835
n-Hexane	0.972701	7.12934	0.047274	0.016671	1.83905
Methylcyclopentane	0.739097	5.37515	0.0339749	0.0919685	1.40115
Benzene	0.475787	3.63241	0.00418791	0.920198	1.08561
Cyclohexane	1.13234	11.1114	0.0515334	0.313842	2.79685
2,2,4-Trimethylpentane	0	0	0	0	0
i-C7	0.36461	5.64446	0.0192432	0.00790728	1.32778
Methylcyclohexane	0.622609	14.6863	0.033627	0.0870128	3.36625
n-Heptane	0.402286	9.17992	0.022132	0.00542853	2.09786
Toluene	0.256525	6.82257	0.00643117	1.06671	1.75611
Octane	0.210721	16.5033	0.0126781	0.0013862	3.60207
Ethylbenzene	0.00480542	0.416241	0.000218658	0.0306495	0.0979089
m-Xylene	0.0482355	4.51618	0.00240157	0.231002	1.03234
Nonane	0.0473704	12.169	0.00306548	0.000282273	2.61878
Decane	0.0111686	8.63581	0.000749452	2.11619E-05	1.85085
Undecanes Plus	1.50465E-06	15.7184	1.50728E-07	3.28548E-07	3.36224

Std Vapor Volumetric Flow	**6 MMSCFD**	**7 MMSCFD**	**8 MMSCFD**	**9 MMSCFD**	**10 MMSCFD**
Water	8.60204E-06	2.26901E-07	1.61597E-05	30.9384	30.9386
Hydrogen Sulfide	0	0	0	0	0
Nitrogen, Atomic	1.6E-07	4.43284E-10	2.20326E-07	3.72421E-09	2.21035E-06
Carbon Dioxide	3.92338E-06	7.69674E-08	3.93764E-06	0.000149889	0.000189648
Methane	4.87135E-05	3.37707E-07	1.09946E-06	2.2274E-06	1.32621E-05
Ethane	0.000506976	2.2588E-05	1.10074E-05	3.10649E-05	0.000143526
Propane	0.00386493	0.000615012	9.45097E-05	0.000185444	0.00120007
Isobutane	0.000975282	0.0003949	2.75277E-05	3.45246E-05	0.000359256
Butane	0.00247108	0.00149827	7.13288E-05	0.000128215	0.00102899
Isopentane	0.000568942	0.000884691	2.03221E-05	2.42601E-05	0.000359551
Pentane	0.000604888	0.00125856	2.36533E-05	1.27215E-05	0.000451796
Cyclopentane	0	0	0	0	0
i-C6	0.000184113	0.000936289	8.35E-06	5.75885E-06	0.000258759
n-Hexane	0.000102802	0.000753479	4.99625E-06	1.76191E-06	0.000194364
Methylcyclopentane	7.9984E-05	0.000581691	3.67672E-06	9.95269E-06	0.00015163
Benzene	5.54754E-05	0.000423528	4.88298E-07	0.000107292	0.00012658
Cyclohexane	0.00012254	0.00120246	5.57686E-06	3.39636E-05	0.000302671
2,2,4-Trimethylpentane	0	0	0	0	0
i-C7	3.31404E-05	0.00051304	1.74906E-06	7.18713E-07	0.000120685
Methylcyclohexane	5.77525E-05	0.00136228	3.1192E-06	8.0712E-06	0.000312249

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	XTO ENERGY INC	Job: DELAWARE DEVELOPMENT
Location:	Cowboy CDP	
Flowsheet:	CDP	

Std Vapor Volumetric Flow	6 MMSCFD	7 MMSCFD	8 MMSCFD	9 MMSCFD	10 MMSCFD
n-Heptane	3.65648E-05	0.000834387	2.01164E-06	4.93413E-07	0.00019068
Toluene	2.53568E-05	0.000674391	6.35703E-07	0.000105441	0.000173586
Octane	1.68011E-05	0.00131583	1.01084E-06	1.10524E-07	0.000287199
Ethylbenzene	4.12244E-07	3.57082E-05	1.87581E-08	2.62934E-06	8.39934E-06
m-Xylene	4.138E-06	0.000387431	2.06024E-07	1.9817E-05	8.85615E-05
Nonane	3.36385E-06	0.000864144	2.17685E-07	2.00447E-08	0.000185964
Decane	7.14917E-07	0.000552788	4.79733E-08	1.3546E-09	0.000118475
Undecanes Plus	5.16345E-11	0.000539401	5.17246E-12	1.12746E-11	0.00011538

Stream Properties

Property	Units	6	7	8	9	10
Temperature	°F	75 *	75	90 *	90	100.001
Pressure	psig	0.25 *	0.25	0.25 *	0.25	5
Molecular Weight	lb/lbmol	54.8052	94.5665	55.6028	18.0165	18.0272
Molar Flow	lbmol/h	1.07346	1.71851	0.0331449	3397.08	3397.7
Std Vapor Volumetric Flow	MMSCFD	0.00977666	0.0156515	0.000301871	30.9393	30.9449
Std Liquid Volumetric Flow	sgpm	0.208926	0.455834	0.00631	122.355	122.5
Net Ideal Gas Heating Value	Btu/ft^3	2835.78	4736.56	2792.05	0.0748971	0.778423
Gross Ideal Gas Heating Value	Btu/ft^3	3072.55	5087.9	3026.17	50.3886	51.138

Remarks

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	XTO ENERGY INC	Job: DELAWARE DEVELOPMENT
Location:	Cowboy CDP	
Flowsheet:	CDP	

Connections

	12	13	14	15	16
From Block	--	--	MIX-102	--	--
To Block	MIX-102	MIX-102	--	MIX-103	MIX-103

Stream Composition

Mole Fraction	12 %	13 %	14 %	15 %	16 %
Water	54.393	54.393	54.393	3.25635E-05	3.25635E-05
Hydrogen Sulfide	0	0	0	0	0
Nitrogen, Atomic	0.000233769	0.000233769	0.000233769	0.000166384	0.000166384
Carbon Dioxide	9.5975	9.5975	9.5975	0.0361079	0.0361079
Methane	0.143449	0.143449	0.143449	0.162614	0.162614
Ethane	2.00114	2.00114	2.00114	6.60982	6.60982
Propane	11.973	11.973	11.973	40.4451	40.4451
Isobutane	2.24331	2.24331	2.24331	9.1404	9.1404
Butane	8.2811	8.2811	8.2811	23.9308	23.9308
Isopentane	1.57513	1.57513	1.57513	5.79605	5.79605
Pentane	0.824635	0.824635	0.824635	6.24117	6.24117
Cyclopentane	0	0	0	0	0
i-C6	0.374299	0.374299	0.374299	2.06379	2.06379
n-Hexane	0.114703	0.114703	0.114703	1.20022	1.20022
Methylcyclopentane	0.642237	0.642237	0.642237	0.844528	0.844528
Benzene	1.81914	1.81914	1.81914	0.412786	0.412786
Cyclohexane	2.18396	2.18396	2.18396	1.24562	1.24562
2,2,4-Trimethylpentane	0	0	0	0	0
i-C7	0.0472998	0.0472998	0.0472998	0.358304	0.358304
Methylcyclohexane	0.521455	0.521455	0.521455	0.679171	0.679171
n-Heptane	0.0323082	0.0323082	0.0323082	0.399209	0.399209
Toluene	2.3798	2.3798	2.3798	0.197937	0.197937
Octane	0.00722268	0.00722268	0.00722268	0.167086	0.167086
Ethylbenzene	0.0679991	0.0679991	0.0679991	0.00330374	0.00330374
m-Xylene	0.775683	0.775683	0.775683	0.0312005	0.0312005
Nonane	0.00133298	0.00133298	0.00133298	0.029147	0.029147
Decane	8.98609E-05	8.98609E-05	8.98609E-05	0.00542155	0.00542155
Undecanes Plus	7.36483E-07	7.36483E-07	7.36483E-07	1.51676E-07	1.51676E-07

Mass Fraction	12 %	13 %	14 %	15 %	16 %
Water	27.4585	27.4585	27.4585	1.07551E-05	1.07551E-05
Hydrogen Sulfide	0	0	0	0	0
Nitrogen, Atomic	9.1752E-05	9.1752E-05	9.1752E-05	4.27256E-05	4.27256E-05
Carbon Dioxide	11.8358	11.8358	11.8358	0.0291333	0.0291333
Methane	0.0644853	0.0644853	0.0644853	0.0478265	0.0478265
Ethane	1.68612	1.68612	1.68612	3.64376	3.64376
Propane	14.7942	14.7942	14.7942	32.6966	32.6966
Isobutane	3.65363	3.65363	3.65363	9.73975	9.73975
Butane	13.4872	13.4872	13.4872	25.5	25.5
Isopentane	3.18449	3.18449	3.18449	7.66657	7.66657
Pentane	1.66719	1.66719	1.66719	8.25535	8.25535
Cyclopentane	0	0	0	0	0
i-C6	0.903846	0.903846	0.903846	3.26054	3.26054
n-Hexane	0.27698	0.27698	0.27698	1.8962	1.8962
Methylcyclopentane	1.51458	1.51458	1.51458	1.30304	1.30304
Benzene	3.98176	3.98176	3.98176	0.591129	0.591129
Cyclohexane	5.15039	5.15039	5.15039	1.9219	1.9219
2,2,4-Trimethylpentane	0	0	0	0	0
i-C7	0.132809	0.132809	0.132809	0.658215	0.658215
Methylcyclohexane	1.43469	1.43469	1.43469	1.22256	1.22256
n-Heptane	0.0907157	0.0907157	0.0907157	0.73336	0.73336
Toluene	6.14433	6.14433	6.14433	0.334355	0.334355
Octane	0.0231188	0.0231188	0.0231188	0.349908	0.349908

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	XTO ENERGY INC	Job: DELAWARE DEVELOPMENT
Location:	Cowboy CDP	
Flowsheet:	CDP	

Mass Fraction	12 %	13 %	14 %	15 %	16 %
Ethylbenzene	0.202292	0.202292	0.202292	0.00643024	0.00643024
m-Xylene	2.30759	2.30759	2.30759	0.0607272	0.0607272
Nonane	0.00479063	0.00479063	0.00479063	0.0685344	0.0685344
Decane	0.000358272	0.000358272	0.000358272	0.0141421	0.0141421
Undecanes Plus	5.47718E-06	5.47718E-06	5.47718E-06	7.38005E-07	7.38005E-07

Mass Flow	12 lb/h	13 lb/h	14 lb/h	15 lb/h	16 lb/h
Water	1.64416	0.0372723	1.68143	2.13932E-08	5.2869E-08
Hydrogen Sulfide	0	0	0	0	0
Nitrogen, Atomic	5.49393E-06	1.24545E-07	5.61847E-06	8.49869E-08	2.10028E-07
Carbon Dioxide	0.708704	0.016066	0.72477	5.79499E-05	0.000143211
Methane	0.00386125	8.75325E-05	0.00394878	9.51332E-05	0.000235102
Ethane	0.100962	0.00228875	0.10325	0.00724791	0.0179117
Propane	0.885846	0.0200817	0.905928	0.0650377	0.160728
Isobutane	0.218772	0.00495945	0.223732	0.0193736	0.047878
Butane	0.807589	0.0183076	0.825897	0.0507228	0.125351
Isopentane	0.190681	0.00432263	0.195003	0.0152498	0.0376868
Pentane	0.0998277	0.00226304	0.102091	0.016421	0.0405811
Cyclopentane	0	0	0	0	0
i-C6	0.0541205	0.00122688	0.0553474	0.00648564	0.0160279
n-Hexane	0.016585	0.000375974	0.016961	0.00377179	0.00932122
Methylcyclopentane	0.0906899	0.00205589	0.0927458	0.00259192	0.0064054
Benzene	0.23842	0.00540486	0.243825	0.00117583	0.00290583
Cyclohexane	0.308395	0.00699116	0.315387	0.0038229	0.00944753
2,2,4-Trimethylpentane	0	0	0	0	0
i-C7	0.00795235	0.000180276	0.00813263	0.00130928	0.00323561
Methylcyclohexane	0.0859066	0.00194746	0.0878541	0.00243183	0.00600977
n-Heptane	0.00543188	0.000123138	0.00555501	0.00145875	0.003605
Toluene	0.367911	0.00834034	0.376251	0.000665075	0.0016436
Octane	0.00138431	3.13816E-05	0.00141569	0.000696013	0.00172006
Ethylbenzene	0.0121128	0.000274591	0.0123874	1.27906E-05	3.16094E-05
m-Xylene	0.138174	0.00313233	0.141306	0.000120794	0.000298519
Nonane	0.000286853	6.50282E-06	0.000293356	0.000136324	0.000336897
Decane	2.14526E-05	4.8632E-07	2.19389E-05	2.81304E-05	6.95186E-05
Undecanes Plus	3.27962E-07	7.43474E-09	3.35397E-07	1.46799E-09	3.62783E-09

Std Vapor Volumetric Flow	12 MMSCFD	13 MMSCFD	14 MMSCFD	15 MMSCFD	16 MMSCFD
Water	0.000831205	1.8843E-05	0.000850048	1.08153E-11	2.67279E-11
Hydrogen Sulfide	0	0	0	0	0
Nitrogen, Atomic	3.57233E-09	8.0983E-11	3.65332E-09	5.52613E-11	1.36567E-10
Carbon Dioxide	0.000146664	3.3248E-06	0.000149989	1.19925E-08	2.96371E-08
Methane	2.19211E-06	4.96939E-08	2.2418E-06	5.4009E-08	1.33472E-07
Ethane	3.05803E-05	6.93239E-07	3.12735E-05	2.19532E-06	5.42529E-06
Propane	0.000182965	4.14772E-06	0.000187113	1.3433E-05	3.3197E-05
Isobutane	3.42811E-05	7.77135E-07	3.50582E-05	3.0358E-06	7.50237E-06
Butane	0.000126547	2.86876E-06	0.000129416	7.94814E-06	1.96422E-05
Isopentane	2.40704E-05	5.45663E-07	2.4616E-05	1.92504E-06	4.75735E-06
Pentane	1.26016E-05	2.85673E-07	1.28873E-05	2.07288E-06	5.12271E-06
Cyclopentane	0	0	0	0	0
i-C6	5.71983E-06	1.29666E-07	5.8495E-06	6.85447E-07	1.69394E-06
n-Hexane	1.75282E-06	3.97356E-08	1.79256E-06	3.98629E-07	9.85132E-07
Methylcyclopentane	9.81433E-06	2.22486E-07	1.00368E-05	2.80493E-07	6.93183E-07
Benzene	2.77991E-05	6.30191E-07	2.84293E-05	1.37099E-07	3.38811E-07
Cyclohexane	3.33741E-05	7.56573E-07	3.41307E-05	4.13709E-07	1.0224E-06
2,2,4-Trimethylpentane	0	0	0	0	0
i-C7	7.2281E-07	1.63857E-08	7.39196E-07	1.19003E-07	2.94093E-07
Methylcyclohexane	7.96859E-06	1.80644E-07	8.14924E-06	2.25573E-07	5.57459E-07
n-Heptane	4.93717E-07	1.11923E-08	5.0491E-07	1.32589E-07	3.27668E-07

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	XTO ENERGY INC	Job: DELAWARE DEVELOPMENT
Location:	Cowboy CDP	
Flowsheet:	CDP	

Std Vapor Volumetric Flow	12 MMSCFD	13 MMSCFD	14 MMSCFD	15 MMSCFD	16 MMSCFD
Toluene	3.63669E-05	8.24419E-07	3.71913E-05	6.57407E-08	1.62465E-07
Octane	1.10373E-07	2.5021E-09	1.12875E-07	5.54942E-08	1.37143E-07
Ethylbenzene	1.03913E-06	2.35565E-08	1.06268E-06	1.09727E-09	2.71168E-09
m-Xylene	1.18536E-05	2.68714E-07	1.21223E-05	1.03626E-08	2.56092E-08
Nonane	2.037E-08	4.61776E-10	2.08317E-08	9.68059E-09	2.39236E-08
Decane	1.37321E-09	3.11299E-11	1.40434E-09	1.80066E-09	4.44997E-09
Undecanes Plus	1.12545E-11	2.55135E-13	1.15097E-11	5.03763E-14	1.24495E-13

Stream Properties

Property	Units	12	13	14	15	16
Temperature	°F	90.5103	90.5103		62.6173	62.6173
Pressure	psig	-11.4239	-11.4239	-11.4239	-3.0257	-3.0257
Molecular Weight	lb/lbmol	35.6868	35.6868	35.6868	54.5456	54.5456
Molar Flow	lbmol/h	0.167788	0.00380366	0.171591	0.00364673	0.00901216
Std Vapor Volumetric Flow	MMSCFD	0.00152815	3.46423E-05	0.00156279	3.3213E-05	8.20793E-05
Std Liquid Volumetric Flow	sgpm	0.0168065	0.000380995	0.0171875	0.000709932	0.00175445
Net Ideal Gas Heating Value	Btu/ft^3	1094.46	1094.46	1094.46	2824.83	2824.83
Gross Ideal Gas Heating Value	Btu/ft^3	1204.88	1204.88	1204.88	3061.07	3061.07

Remarks

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	XTO ENERGY INC	Job: DELAWARE DEVELOPMENT
Location:	Cowboy CDP	
Flowsheet:	CDP	

Connections

	17	18	19	20	21
From Block	MIX-103	Gunbarrel	Gunbarrel	--	--
To Block	--	Produced Water Tanks	--	MIX-104	MIX-104

Stream Composition

Mole Fraction	17 %	18 %	19 %	20 %	21 %
Water	3.25635E-05	99.9963	5.35318	98.7145	98.7145
Hydrogen Sulfide	0	0	0	0	0
Nitrogen, Atomic	0.000166384	7.24154E-07	0.0729867	1.78981E-05	1.78981E-05
Carbon Dioxide	0.0361079	0.000497183	1.30441	0.811608	0.811608
Methane	0.162614	1.07528E-05	0.364216	0.00787515	0.00787515
Ethane	6.60982	0.000135982	3.6464	0.110058	0.110058
Propane	40.4451	0.000904839	31.308	0.216497	0.216497
Isobutane	9.1404	0.00020056	9.11903	0.0263789	0.0263789
Butane	23.9308	0.000644946	23.6289	0.0675657	0.0675657
Isopentane	5.79605	0.000144094	6.73203	0.0131909	0.0131909
Pentane	6.24117	0.000117567	7.83556	0.01363	0.01363
Cyclopentane	0	0	0	0	0
i-C6	2.06379	4.56013E-05	2.76608	0.0046309	0.0046309
n-Hexane	1.20022	2.18431E-05	1.65509	0.00274772	0.00274772
Methylcyclopentane	0.844528	4.40517E-05	1.21798	0.00198041	0.00198041
Benzene	0.412786	0.000348359	0.161757	0.00145363	0.00145363
Cyclohexane	1.24562	0.000127799	1.84743	0.00303705	0.00303705
2,2,4-Trimethylpentane	0	0	0	0	0
i-C7	0.358304	7.97612E-06	0.579407	0.000867053	0.000867053
Methylcyclohexane	0.679171	3.61686E-05	1.03329	0.00165932	0.00165932
n-Heptane	0.399209	8.09659E-06	0.666389	0.00100204	0.00100204
Toluene	0.197937	0.000342851	0.210587	0.000613938	0.000613938
Octane	0.167086	3.62438E-06	0.334859	0.000476987	0.000476987
Ethylbenzene	0.00330374	8.55894E-06	0.00621393	1.03612E-05	1.03612E-05
m-Xylene	0.0312005	6.47166E-05	0.0682491	9.57939E-05	9.57939E-05
Nonane	0.029147	7.68367E-07	0.0721118	8.46198E-05	8.46198E-05
Decane	0.00542155	1.59433E-07	0.015892	1.39246E-05	1.39246E-05
Undecanes Plus	1.51676E-07	5.31582E-11	1.71341E-06	1.48802E-09	1.48802E-09

Mass Fraction	17 %	18 %	19 %	20 %	21 %
Water	1.07551E-05	99.9874	1.73443	96.8546	96.8546
Hydrogen Sulfide	0	0	0	0	0
Nitrogen, Atomic	4.27256E-05	5.62972E-07	0.0183858	1.36534E-05	1.36534E-05
Carbon Dioxide	0.0291333	0.00121446	1.03244	1.94532	1.94532
Methane	0.0478265	9.57441E-06	0.105083	0.00688063	0.00688063
Ethane	3.64376	0.000226946	1.97191	0.180235	0.180235
Propane	32.6966	0.00221456	24.8287	0.51993	0.51993
Isobutane	9.73975	0.000647004	9.53222	0.0835019	0.0835019
Butane	25.5	0.00208059	24.6995	0.213878	0.213878
Isopentane	7.66657	0.000577028	8.73531	0.0518324	0.0518324
Pentane	8.25535	0.000470799	10.1672	0.053558	0.053558
Cyclopentane	0	0	0	0	0
i-C6	3.26054	0.000218113	4.28698	0.0217344	0.0217344
n-Hexane	1.8962	0.000104476	2.56513	0.012896	0.012896
Methylcyclopentane	1.30304	0.000205772	1.84351	0.00907728	0.00907728
Benzene	0.591129	0.0015103	0.227239	0.006184	0.006184
Cyclohexane	1.9219	0.000596968	2.79624	0.0139205	0.0139205
2,2,4-Trimethylpentane	0	0	0	0	0
i-C7	0.658215	4.43596E-05	1.04415	0.00473173	0.00473173
Methylcyclohexane	1.22256	0.000197107	1.82463	0.00887317	0.00887317
n-Heptane	0.73336	4.50297E-05	1.2009	0.00546839	0.00546839
Toluene	0.334355	0.00175334	0.34896	0.0030808	0.0030808

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	XTO ENERGY INC	Job: DELAWARE DEVELOPMENT
Location:	Cowboy CDP	
Flowsheet:	CDP	

Mass Fraction	17 %	18 %	19 %	20 %	21 %
Octane	0.349908	2.29789E-05	0.687924	0.00296742	0.00296742
Ethylbenzene	0.00643024	5.04338E-05	0.0118645	5.99087E-05	5.99087E-05
m-Xylene	0.0607272	0.000381345	0.130311	0.000553882	0.000553882
Nonane	0.0685344	5.4697E-06	0.166335	0.000591078	0.000591078
Decane	0.0141421	1.25906E-06	0.0406658	0.000107902	0.000107902
Undecanes Plus	7.38005E-07	7.83054E-10	8.17835E-06	2.15084E-08	2.15084E-08

Mass Flow	17 lb/h	18 lb/h	19 lb/h	20 lb/h	21 lb/h
Water	7.42623E-08	61197.6	0.287682	1.96209	0.0147454
Hydrogen Sulfide	0	0	0	0	0
Nitrogen, Atomic	2.95015E-07	0.000344569	0.00304957	2.76592E-07	2.07863E-09
Carbon Dioxide	0.000201161	0.743315	0.171246	0.0394084	0.000296161
Methane	0.000330236	0.00586005	0.0174297	0.000139388	1.04753E-06
Ethane	0.0251596	0.138903	0.327072	0.00365122	2.74395E-05
Propane	0.225765	1.35543	4.11822	0.0105328	7.91556E-05
Isobutane	0.0672516	0.396001	1.58107	0.00169159	1.27126E-05
Butane	0.176074	1.27343	4.0968	0.00433277	3.25614E-05
Isopentane	0.0529366	0.353172	1.44889	0.00105003	7.89112E-06
Pentane	0.0570021	0.288154	1.68639	0.00108498	8.15382E-06
Cyclopentane	0	0	0	0	0
i-C6	0.0225136	0.133497	0.711062	0.000440296	3.3089E-06
n-Hexane	0.013093	0.0639451	0.425466	0.000261248	1.96332E-06
Methylcyclopentane	0.00899731	0.125943	0.305774	0.000183888	1.38195E-06
Benzene	0.00408166	0.924386	0.0376912	0.000125276	9.41469E-07
Cyclohexane	0.0132704	0.365376	0.4638	0.000282002	2.11929E-06
2,2,4-Trimethylpentane	0	0	0	0	0
i-C7	0.00454489	0.0271505	0.173189	9.58559E-05	7.20372E-07
Methylcyclohexane	0.0084416	0.12064	0.302643	0.000179753	1.35088E-06
n-Heptane	0.00506375	0.0275606	0.199188	0.000110779	8.32524E-07
Toluene	0.00230867	1.07314	0.0578805	6.24111E-05	4.6903E-07
Octane	0.00241607	0.0140643	0.114103	6.01143E-05	4.51769E-07
Ethylbenzene	4.43999E-05	0.0308682	0.00196792	1.21364E-06	9.12067E-09
m-Xylene	0.000419313	0.233403	0.0216141	1.12206E-05	8.43246E-08
Nonane	0.000473221	0.00334775	0.0275893	1.19741E-05	8.99874E-08
Decane	9.7649E-05	0.000770614	0.00674507	2.18589E-06	1.64273E-08
Undecanes Plus	5.09582E-09	4.79271E-07	1.35651E-06	4.35719E-10	3.2745E-12

Std Vapor Volumetric Flow	17 MMSCFD	18 MMSCFD	19 MMSCFD	20 MMSCFD	21 MMSCFD
Water	3.75432E-11	30.9384	0.000145438	0.000991933	7.45454E-06
Hydrogen Sulfide	0	0	0	0	0
Nitrogen, Atomic	1.91828E-10	2.2405E-07	1.98293E-06	1.79849E-10	1.3516E-12
Carbon Dioxide	4.16296E-08	0.000153826	3.54388E-05	8.15544E-06	6.12895E-08
Methane	1.87481E-07	3.32686E-06	9.89518E-06	7.91334E-08	5.94701E-10
Ethane	7.62061E-06	4.20723E-05	9.9067E-05	1.10592E-06	8.31117E-09
Propane	4.66301E-05	0.000279953	0.000850587	2.17547E-06	1.6349E-08
Isobutane	1.05382E-05	6.20524E-05	0.00024775	2.65068E-07	1.99203E-09
Butane	2.75904E-05	0.000199543	0.000641959	6.78934E-07	5.1023E-09
Isopentane	6.68239E-06	4.45822E-05	0.000182899	1.32549E-07	9.96126E-10
Pentane	7.19559E-06	3.63748E-05	0.00021288	1.36961E-07	1.02929E-09
Cyclopentane	0	0	0	0	0
i-C6	2.37939E-06	1.41089E-05	7.515E-05	4.65336E-08	3.49708E-10
n-Hexane	1.38376E-06	6.75816E-06	4.49663E-05	2.76105E-08	2.07497E-10
Methylcyclopentane	9.73676E-07	1.36294E-05	3.30905E-05	1.99001E-08	1.49553E-10
Benzene	4.7591E-07	0.000107781	4.39468E-06	1.46068E-08	1.09773E-10
Cyclohexane	1.43611E-06	3.95404E-05	5.01918E-05	3.05178E-08	2.29346E-10
2,2,4-Trimethylpentane	0	0	0	0	0
i-C7	4.13097E-07	2.46778E-06	1.57416E-05	8.71259E-09	6.54765E-11
Methylcyclohexane	7.83032E-07	1.11904E-05	2.80728E-05	1.66737E-08	1.25306E-10

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	XTO ENERGY INC	Job: DELAWARE DEVELOPMENT
Location:	Cowboy CDP	
Flowsheet:	CDP	

Std Vapor Volumetric Flow	17 MMSCFD	18 MMSCFD	19 MMSCFD	20 MMSCFD	21 MMSCFD
n-Heptane	4.60257E-07	2.50505E-06	1.81047E-05	1.0069E-08	7.56702E-11
Toluene	2.28206E-07	0.000106077	5.72132E-06	6.16916E-09	4.63622E-11
Octane	1.92637E-07	1.12137E-06	9.0976E-06	4.793E-09	3.60202E-11
Ethylbenzene	3.80895E-09	2.6481E-06	1.68823E-07	1.04115E-10	7.82439E-13
m-Xylene	3.59718E-08	2.0023E-05	1.85422E-06	9.62585E-10	7.23399E-12
Nonane	3.36042E-08	2.37729E-07	1.95916E-06	8.50302E-10	6.39016E-12
Decane	6.25063E-09	4.93279E-08	4.31759E-07	1.39922E-10	1.05153E-12
Undecanes Plus	1.74871E-13	1.64469E-11	4.65507E-11	1.49524E-14	1.1237E-16

Stream Properties

Property	Units	17	18	19	20	21
Temperature	°F	62.6173	90	90 *	95.7977	95.7977
Pressure	psig	-3.0257	0.25	0.25 *	-11.8827	-11.8827
Molecular Weight	lb/lbmol	54.5456	18.0169	55.6028	18.3612	18.3612
Molar Flow	lbmol/h	0.0126589	3397.11	0.298304	0.110331	0.000829154
Std Vapor Volumetric Flow	MMSCFD	0.000115292	30.9396	0.00271684	0.00100485	7.55161E-06
Std Liquid Volumetric Flow	sgpm	0.00246439	122.362	0.05679	0.00411439	3.09203E-05
Net Ideal Gas Heating Value	Btu/ft^3	2824.83	0.102138	2792.05	11.5124	11.5124
Gross Ideal Gas Heating Value	Btu/ft^3	3061.07	50.4176	3026.17	62.1629	62.1629

Remarks

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	XTO ENERGY INC	Job: DELAWARE DEVELOPMENT
Location:	Cowboy CDP	
Flowsheet:	CDP	

Connections

	22	23	24	28	50K Breathing Losses
From Block	MIX-104	Gunbarrel	MIX-105	IFR - 250,000 bbl	--
To Block	--	MIX-105	Slop Oil Tank	--	--

Stream Composition

Mole Fraction	22 %	23 %	24 %	28 %	50K Breathing Losses %
Water	98.7145	0.0775403	0.0347211		1.15564
Hydrogen Sulfide	0	0	0		0
Nitrogen, Atomic	1.78981E-05	0.000126525	0.000630966		0
Carbon Dioxide	0.811608	0.0143814	0.0157319		0.138619
Methane	0.00787515	0.0015044	0.192901		0
Ethane	0.110058	0.0895742	2.08259		16.0241
Propane	0.216497	2.61007	17.618		22.1197
Isobutane	0.0263789	1.85634	5.38844		8.49409
Butane	0.0675657	7.03774	15.6101		23.4033
Isopentane	0.0131909	4.95745	5.71662		6.1578
Pentane	0.01363	7.60272	7.32828		6.77277
Cyclopentane	0	0	0		0
i-C6	0.0046309	6.36244	4.40614		2.36046
n-Hexane	0.00274772	5.35419	3.36745		1.36868
Methylcyclopentane	0.00198041	3.93797	2.60213		1.04794
Benzene	0.00145363	0.540684	1.88375		0.945441
Cyclohexane	0.00303705	7.99299	5.21077		1.80298
2,2,4-Trimethylpentane	0	0	0		0
i-C7	0.000867053	3.84659	2.14793		0.524039
Methylcyclohexane	0.00165932	10.247	5.58448		1.23235
n-Heptane	0.00100204	6.38384	3.42514		0.823647
Toluene	0.000613938	2.31932	2.75186		0.649319
Octane	0.000476987	10.3969	5.24076		0.861553
Ethylbenzene	1.03612E-05	0.209545	0.142049		0.0221607
m-Xylene	9.57939E-05	2.5031	1.5399		0.249697
Nonane	8.46198E-05	6.898	3.4116		0.625724
Decane	1.39246E-05	4.42908	2.17673		0.518341
Undecanes Plus	1.48802E-09	4.33098	2.12127		2.70172

Mass Fraction	22 %	23 %	24 %	28 %	50K Breathing Losses %
Water	96.8546	0.0139917	0.00788999		0.334696
Hydrogen Sulfide	0	0	0		0
Nitrogen, Atomic	1.36534E-05	1.77506E-05	0.000111476		0
Carbon Dioxide	1.94532	0.0063394	0.00873314		0.0980747
Methane	0.00688063	0.000241733	0.0390344		0
Ethane	0.180235	0.0269777	0.789887		7.74605
Propane	0.51993	1.15279	9.79929		15.6805
Isobutane	0.0835019	1.08069	3.95045		7.93681
Butane	0.213878	4.09711	11.4443		21.8678
Isopentane	0.0518324	3.58253	5.20248		7.14236
Pentane	0.053558	5.49414	6.66918		7.85565
Cyclopentane	0	0	0		0
i-C6	0.0217344	5.49172	4.78943		3.27015
n-Hexane	0.012896	4.62145	3.66038		1.89614
Methylcyclopentane	0.00907728	3.31954	2.76232		1.41783
Benzene	0.006184	0.423021	1.85602		1.18724
Cyclohexane	0.0139205	6.73774	5.53155		2.43939
2,2,4-Trimethylpentane	0	0	0		0
i-C7	0.00473173	3.8606	2.71481		0.844164

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	XTO ENERGY INC	Job: DELAWARE DEVELOPMENT
Location:	Cowboy CDP	
Flowsheet:	CDP	

Mass Fraction	22 %	23 %	24 %	28 %	50K Breathing Losses %
Methylcyclohexane	0.00887317	10.0774	6.9163		1.94523
n-Heptane	0.00546839	6.40708	4.32909		1.3268
Toluene	0.0030808	2.14044	3.19822		0.961803
Octane	0.00296742	11.8954	7.55111		1.58214
Ethylbenzene	5.99087E-05	0.222823	0.190222		0.0378226
m-Xylene	0.000553882	2.66171	2.06213		0.426169
Nonane	0.000591078	8.86134	5.51918		1.29016
Decane	0.000107902	6.31196	3.90657		1.18564
Undecanes Plus	2.15084E-08	11.513	7.10132		11.5273

Mass Flow	22 lb/h	23 lb/h	24 lb/h	28 lb/h	50K Breathing Losses lb/h
Water	1.97683	0.0040861	0.0174641		0.0142199
Hydrogen Sulfide	0	0	0		0
Nitrogen, Atomic	2.78671E-07	5.18386E-06	0.000246747		0
Carbon Dioxide	0.0397046	0.00185134	0.0193303		0.0041668
Methane	0.000140436	7.05952E-05	0.0864004		0
Ethane	0.00367866	0.0078785	1.74837		0.329099
Propane	0.0106119	0.336658	21.6902		0.666203
Isobutane	0.0017043	0.315602	8.74411		0.337203
Butane	0.00436533	1.19651	25.3313		0.929077
Isopentane	0.00105792	1.04623	11.5154		0.30345
Pentane	0.00109314	1.6045	14.7619		0.333755
Cyclopentane	0	0	0		0
i-C6	0.000443605	1.60379	10.6011		0.138936
n-Hexane	0.000263211	1.34964	8.10204		0.0805595
Methylcyclopentane	0.00018527	0.969431	6.11425		0.060238
Benzene	0.000126217	0.123538	4.1082		0.0504411
Cyclohexane	0.000284121	1.96767	12.2438		0.10364
2,2,4-Trimethylpentane	0	0	0		0
i-C7	9.65762E-05	1.12744	6.00907		0.0358651
Methylcyclohexane	0.000181104	2.94297	15.3089		0.0826449
n-Heptane	0.000111612	1.87111	9.58221		0.0563702
Toluene	6.28801E-05	0.62509	7.07909		0.0408631
Octane	6.05661E-05	3.4739	16.714		0.0672186
Ethylbenzene	1.22276E-06	0.0650728	0.421047		0.00160693
m-Xylene	1.13049E-05	0.77732	4.56441		0.0181062
Nonane	1.20641E-05	2.58785	12.2164		0.0548138
Decane	2.20232E-06	1.84333	8.64698		0.0503729
Undecanes Plus	4.38994E-10	3.36224	15.7184		0.489749

Std Vapor Volumetric Flow	22 MMSCFD	23 MMSCFD	24 MMSCFD	28 MMSCFD	50K Breathing Losses MMSCFD
Water	0.000999387	2.06573E-06	8.82894E-06		7.18885E-06
Hydrogen Sulfide	0	0	0		0
Nitrogen, Atomic	1.81201E-10	3.37072E-09	1.60443E-07		0
Carbon Dioxide	8.21673E-06	3.83129E-07	4.00035E-06		8.62305E-07
Methane	7.97281E-08	4.00783E-08	4.90512E-05		0
Ethane	1.11423E-06	2.38632E-06	0.000529564		9.96807E-05
Propane	2.19182E-06	6.95341E-05	0.00447995		0.000137599
Isobutane	2.6706E-07	4.94542E-05	0.00137018		5.2839E-05
Butane	6.84037E-07	0.00018749	0.00396936		0.000145584
Isopentane	1.33545E-07	0.00013207	0.00145363		3.83057E-05
Pentane	1.37991E-07	0.000202542	0.00186345		4.21312E-05
Cyclopentane	0	0	0		0
i-C6	4.68833E-08	0.0001695	0.0011204		1.46837E-05
n-Hexane	2.7818E-08	0.000142639	0.00085628		8.51409E-06
Methylcyclopentane	2.00497E-08	0.00010491	0.000661675		6.51887E-06

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	XTO ENERGY INC	Job: DELAWARE DEVELOPMENT
Location:	Cowboy CDP	
Flowsheet:	CDP	

Std Vapor Volumetric Flow	22 MMSCFD	23 MMSCFD	24 MMSCFD	28 MMSCFD	50K Breathing Losses MMSCFD
Benzene	1.47166E-08	1.44042E-05	0.000479004		5.88128E-06
Cyclohexane	3.07472E-08	0.000212939	0.001325		1.12157E-05
2,2,4-Trimethylpentane	0	0	0		0
i-C7	8.77806E-09	0.000102476	0.00054618		3.25988E-06
Methylcyclohexane	1.6799E-08	0.000272986	0.00142003		7.66604E-06
n-Heptane	1.01447E-08	0.00017007	0.000870952		5.12364E-06
Toluene	6.21552E-09	6.17884E-05	0.000699748		4.0392E-06
Octane	4.82903E-09	0.00027698	0.00133263		5.35944E-06
Ethylbenzene	1.04897E-10	5.58242E-06	3.61205E-05		1.37854E-07
m-Xylene	9.69819E-10	6.66842E-05	0.000391569		1.55328E-06
Nonane	8.56692E-10	0.000183768	0.000867508		3.89242E-06
Decane	1.40973E-10	0.000117994	0.000553503		3.22443E-06
Undecanes Plus	1.50648E-14	0.00011538	0.000539401		1.68065E-05

Stream Properties

Property	Units	22	23	24	28	50K Breathing Losses
Temperature	°F	95.7977	90	41.2703		93.1604
Pressure	psig	-11.8827	0.25	0.25	0	50.3378
Molecular Weight	lb/lbmol	18.3612	99.8385	79.279		62.2032
Molar Flow	lbmol/h	0.11116	0.29251	2.79197	0	0.0683019
Std Vapor Volumetric Flow	MMSCFD	0.0010124	0.00266407	0.0254282	0	0.000622067
Std Liquid Volumetric Flow	sgpm	0.00414531	0.0814272	0.664761	0	0.0143664
Net Ideal Gas Heating Value	Btu/ft^3	11.5124	5008.36	4005.75		3173.81
Gross Ideal Gas Heating Value	Btu/ft^3	62.1629	5383.38	4313.04		3429.67

Remarks

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	XTO ENERGY INC	Job: DELAWARE DEVELOPMENT
Location:	Cowboy CDP	
Flowsheet:	CDP	

Connections

	50k Working Losses	250k Breathing Losses	250k Working Losses		
From Block	--	--	--		
To Block	--	--	--		

Stream Composition

Mole Fraction	50k Working Losses %	250k Breathing Losses %	250k Working Losses %		
Water	1.15564	1.21467	1.21467		
Hydrogen Sulfide	0	0	0		
Nitrogen, Atomic	0	0	0		
Carbon Dioxide	0.138619	0.145629	0.145629		
Methane	0	0	0		
Ethane	16.0241	16.8447	16.8447		
Propane	22.1197	23.2642	23.2642		
Isobutane	8.49409	8.91027	8.91027		
Butane	23.4033	24.484	24.484		
Isopentane	6.1578	6.3417	6.3417		
Pentane	6.77277	6.91802	6.91802		
Cyclopentane	0	0	0		
i-C6	2.36046	2.29993	2.29993		
n-Hexane	1.36868	1.2924	1.2924		
Methylcyclopentane	1.04794	0.98596	0.98596		
Benzene	0.945441	0.884802	0.884802		
Cyclohexane	1.80298	1.63532	1.63532		
2,2,4-Trimethylpentane	0	0	0		
i-C7	0.524039	0.44772	0.44772		
Methylcyclohexane	1.23235	0.979293	0.979293		
n-Heptane	0.823647	0.656033	0.656033		
Toluene	0.649319	0.492573	0.492573		
Octane	0.861553	0.515752	0.515752		
Ethylbenzene	0.0221607	0.0126686	0.0126686		
m-Xylene	0.249697	0.13955	0.13955		
Nonane	0.625724	0.293533	0.293533		
Decane	0.518341	0.213782	0.213782		
Undecanes Plus	2.70172	1.02747	1.02747		

Mass Fraction	50k Working Losses %	250k Breathing Losses %	250k Working Losses %		
Water	0.334696	0.382194	0.382194		
Hydrogen Sulfide	0	0	0		
Nitrogen, Atomic	0	0	0		
Carbon Dioxide	0.0980747	0.111938	0.111938		
Methane	0	0	0		
Ethane	7.74605	8.84643	8.84643		
Propane	15.6805	17.9171	17.9171		
Isobutane	7.93681	9.04519	9.04519		
Butane	21.8678	24.8548	24.8548		
Isopentane	7.14236	7.99134	7.99134		
Pentane	7.85565	8.71757	8.71757		
Cyclopentane	0	0	0		
i-C6	3.27015	3.46165	3.46165		
n-Hexane	1.89614	1.9452	1.9452		
Methylcyclopentane	1.41783	1.44926	1.44926		
Benzene	1.18724	1.20711	1.20711		
Cyclohexane	2.43939	2.40376	2.40376		

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	XTO ENERGY INC	Job: DELAWARE DEVELOPMENT
Location:	Cowboy CDP	
Flowsheet:	CDP	

Mass Fraction	50k Working Losses %	250k Breathing Losses %	250k Working Losses %		
2,2,4-Trimethylpentane	0	0	0		
i-C7	0.844164	0.783551	0.783551		
Methylcyclohexane	1.94523	1.67937	1.67937		
n-Heptane	1.3268	1.14812	1.14812		
Toluene	0.961803	0.792677	0.792677		
Octane	1.58214	1.02896	1.02896		
Ethylbenzene	0.0378226	0.0234906	0.0234906		
m-Xylene	0.426169	0.258759	0.258759		
Nonane	1.29016	0.657532	0.657532		
Decane	1.18564	0.531257	0.531257		
Undecanes Plus	11.5273	4.76272	4.76272		

Mass Flow	50k Working Losses lb/h	250k Breathing Losses lb/h	250k Working Losses lb/h		
Water	0	0.0437205	0		
Hydrogen Sulfide	0	0	0		
Nitrogen, Atomic	0	0	0		
Carbon Dioxide	0	0.012805	0		
Methane	0	0	0		
Ethane	0	1.01197	0		
Propane	0	2.04961	0		
Isobutane	0	1.03471	0		
Butane	0	2.84323	0		
Isopentane	0	0.914158	0		
Pentane	0	0.997234	0		
Cyclopentane	0	0	0		
i-C6	0	0.395991	0		
n-Hexane	0	0.222518	0		
Methylcyclopentane	0	0.165786	0		
Benzene	0	0.138086	0		
Cyclohexane	0	0.274974	0		
2,2,4-Trimethylpentane	0	0	0		
i-C7	0	0.0896332	0		
Methylcyclohexane	0	0.19211	0		
n-Heptane	0	0.131337	0		
Toluene	0	0.0906771	0		
Octane	0	0.117707	0		
Ethylbenzene	0	0.00268717	0		
m-Xylene	0	0.0296004	0		
Nonane	0	0.0752175	0		
Decane	0	0.0607724	0		
Undecanes Plus	0	0.544824	0		

Std Vapor Volumetric Flow	50k Working Losses MMSCFD	250k Breathing Losses MMSCFD	250k Working Losses MMSCFD		
Water	0	2.21029E-05	0		
Hydrogen Sulfide	0	0	0		
Nitrogen, Atomic	0	0	0		
Carbon Dioxide	0	2.64995E-06	0		
Methane	0	0	0		
Ethane	0	0.000306517	0		
Propane	0	0.000423331	0		
Isobutane	0	0.000162137	0		
Butane	0	0.000445527	0		
Isopentane	0	0.000115398	0		

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	XTO ENERGY INC	Job: DELAWARE DEVELOPMENT
Location:	Cowboy CDP	
Flowsheet:	CDP	

Std Vapor Volumetric Flow	50k Working Losses MMSCFD	250k Breathing Losses MMSCFD	250k Working Losses MMSCFD		
Pentane	0	0.000125885	0		
Cyclopentane	0	0	0		
i-C6	0	4.18511E-05	0		
n-Hexane	0	2.35173E-05	0		
Methylcyclopentane	0	1.79412E-05	0		
Benzene	0	1.61004E-05	0		
Cyclohexane	0	2.97573E-05	0		
2,2,4-Trimethylpentane	0	0	0		
i-C7	0	8.147E-06	0		
Methylcyclohexane	0	1.78199E-05	0		
n-Heptane	0	1.19376E-05	0		
Toluene	0	8.96317E-06	0		
Octane	0	9.38496E-06	0		
Ethylbenzene	0	2.30525E-07	0		
m-Xylene	0	2.53934E-06	0		
Nonane	0	5.34132E-06	0		
Decane	0	3.89011E-06	0		
Undecanes Plus	0	1.86965E-05	0		

Stream Properties

Property	Units	50k Working Losses	250k Breathing Losses	250k Working Losses		
Temperature	°F	93.1604	93.7973	93.7973		
Pressure	psig		49.4423			
Molecular Weight	lb/lbmol	62.2032	57.2552	57.2552		
Molar Flow	lbmol/h	0	0.199796	0		
Std Vapor Volumetric Flow	MMSCFD	0	0.00181966	0		
Std Liquid Volumetric Flow	sgpm	0	0.0400952	0		
Net Ideal Gas Heating Value	Btu/ft^3	3173.81	2935.74	2935.74		
Gross Ideal Gas Heating Value	Btu/ft^3	3429.67	3177.26	3177.26		

Remarks

Heaters (RH1-4, SHTR1-11,CHTR1-4) Specs

Owner:	XTO	Owner Ref.:	H-16-F700
Purchaser:	Linde Engineering N.A.	Purchaser Ref.:	2110A4YK
Manufacturer:	Tulsa Heaters Midstream	THM Ref.:	MJ18-327
Service:	Regen Gas Heater	Project:	Cowboy Cryo Plant
Number:	1	Location:	New Mexico
SHO Duty:	27.73 MMBTU/ hr	SHO Model:	SHO2500

Guarantees:

NOx	0.0267	Lb/MMBTU	20	ppm
SOx	no quote	Lb/MMBTU	-	ppm
CO	0.0163	Lb/MMBTU	20	ppm
VOC	0.0064	Lb/MMBTU	5	ppm
UHC	0.007	Lb/MMBTU	15	ppm
SPM	0.0128	Lb/MMBTU	15	ppm

35.25 MMBTU Regen Heaters

			Design Case				Maximum Case			
Heat Release	LHV Basis		35.25	MMBTU/hr			38.77	MMBTU/hr		
	HHV Basis		39.14	MMBTU/hr						
Products of Combus		MW								
	O2	32.00	886	Lbm/ hr			1,083	Lbm/ hr		
	N2 + Ar	28.15	22,517	Lbm/ hr			27,520	Lbm/ hr		
	CO2	44.01	4,051	Lbm/ hr			4,952	Lbm/ hr		
	H2O	18.02	3,490	Lbm/ hr			4,265	Lbm/ hr		
	NOx	46.01	0.85	Lbm/ hr /	20	ppm	0.93	Lbm/ hr /	20	ppm
	SOx	64.06	0.00	Lbm/ hr /	0	ppm	0.00	Lbm/ hr /	0	ppm
	CO	28.01	0.52	Lbm/ hr /	20	ppm	0.57	Lbm/ hr /	20	ppm
	VOC	44.10	0.20	Lbm/ hr /	5	ppm	0.22	Lbm/ hr /	5	ppm
	UHC	16.04	0.22	Lbm/ hr /	15	ppm	0.24	Lbm/ hr /	15	ppm
	SPM		0.40	Lbm/ hr /	15	ppm	0.44	Lbm/ hr /	15	ppm
	Total		30,946	Lbm/ hr			37,821	Lbm/ hr		
Flue Gas Exit Temp.			470	°F						
Flue Gas Exit Velocity			52.3	Ft/sec			57.5	Ft/sec		
Stack Height			~~27.1~~	ft			27.1	ft		
Stack ID			32	in			32	in		

28.7 (See drawing on following page)

NOTE:

THM emissions guarantees applicable between 50-100% of Design Case combustion conditions w/ 15% excess air.

THM emissions guarantees applicable for firebox temperatures above 1100°F.

Emissions above are for Design Case operation with air and fuel in ratio control. Upset conditions, such as operation outside the design, high turndown or start-up are not considered as guaranteed emissions cases.

The Maximum Case is the the specified heat release for the burner purchased. Extra duty is spec'd into the burner to ensure that the burner is never the limiting factor on duty.

revision	date	description	by	chk'd	appv'd

TULSA HEATERS MIDSTREAM

USA Applications

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EMISSIONS PERMIT DATA SHEET
AMERICAN ENGINEERING SYSTEM of UNITS

MJ18-327-Emissions- Pg 1 of 1

COMPONENT DESCRIPTION

ITEM	QTY	DESCRIPTION
1	1	CALLIDUS BURNER (ENHANCED IFGR ULTRA LOW NOX CUBL-8W-HC-HZ)
2	2	3/16" PL RADIANT SIDE WALLS – A36
3	1	3/16" PL RADIANT ROOF – A36
4	1	3/16" PL RADIANT FLOOR – A36
5	2	3/16" PL RADIANT END WALL – A36
6	2	3/16" PL CONVECTION SIDE WALL – A36
7	2	3/8" PL CONVECTION TUBE SHEETS – A36
8	2	10 GA. PL RETURN COVERS – A36
9	1	3/16" PL TRANSITION – A36
10	1	32" O.D. x 3/16" PL. STACK – A36
11	1	24" x 24" ACCESS DOOR @ RADIANT END WALL
12		NOT USED
13		LIFTING LUGS (STRAIGHT UP LIFT ONLY) – A36
14		5/8" GALV. HIGH STRENGTH BOLT w/ BEVEL WASHER & HEAVY HEX NUT – A325
15		5/8" GALV. HIGH STRENGTH BOLT w/ HARDENED WASHER & HEAVY HEX NUT – A325
16		5/8" GALV. MACHINE BOLT w/ FLAT WASHER & HEX NUT – A307
17A	1	1 1/2" – 3000# THR'D COUPLING w/ PLUG (CS) w/ 304SS PIPE SLEEVE – SPARE
17B	1	1 1/2" – 3000# THR'D COUPLING w/ PLUG (CS) w/ 304SS PIPE SLEEVE – STACK TEMPERATURE
18A	1	1 1/2" – 3000# THR'D COUPLING w/ PLUG (CS) w/ 304SS PIPE SLEEVE – SPARE
18B	1	1 1/2" – 3000# THR'D COUPLING w/ PLUG (CS) w/ 304SS PIPE SLEEVE – SPARE
19A	1	1 1/2" – 3000# THR'D COUPLING w/ PLUG (CS) w/ 304SS PIPE SLEEVE – FURNACE PRESSURE
19B	1	1 1/2" – 3000# THR'D COUPLING w/ PLUG (CS) w/ 304SS PIPE SLEEVE – SPARE
20		NOT USED
21		NOT USED
22	1	1 1/2" – 3000# THR'D COUPLING w/ PLUG (CS) w/ 304SS PIPE SLEEVE – SPARE
23	2	4" – 150# RFWN FLG w/ BLIND (CS) w/ CS PIPE SLEEVE – SAMPLE PORT
24		NOT USED
25		14 GA. FERRULES – 304SS (@ TUBE SHEET)
26		10 GA. FERRULES – C.S. (@ RETURN COVERS)
27		10 GA. FERRULES – 304SS (@ RADIANT SHELL)
28	1	4" SITE PORT w/ 304SS PIPE SLEEVE (@ RADIANT SHELL)
29	1	THM NAME PLATE (304SS)
30	8	FLEXIBLE TUBE SEALS (SOCK & CLAMP) – SHOP INSTALLED
31		1/2" DIA. GALV MACHINE BOLT w/ FLAT WASHER & HEAVY HEX NUT – A307
32		3/4" GALV. HIGH STRENGTH BOLT w/ HARDENED WASHER & HEAVY HEX NUT – A325
33	1	OUTLET SUPPORT – A36
34	1	COMBUSTION MODULE SKID 5500 W/ CONTROL PANEL

DRAWING LIST

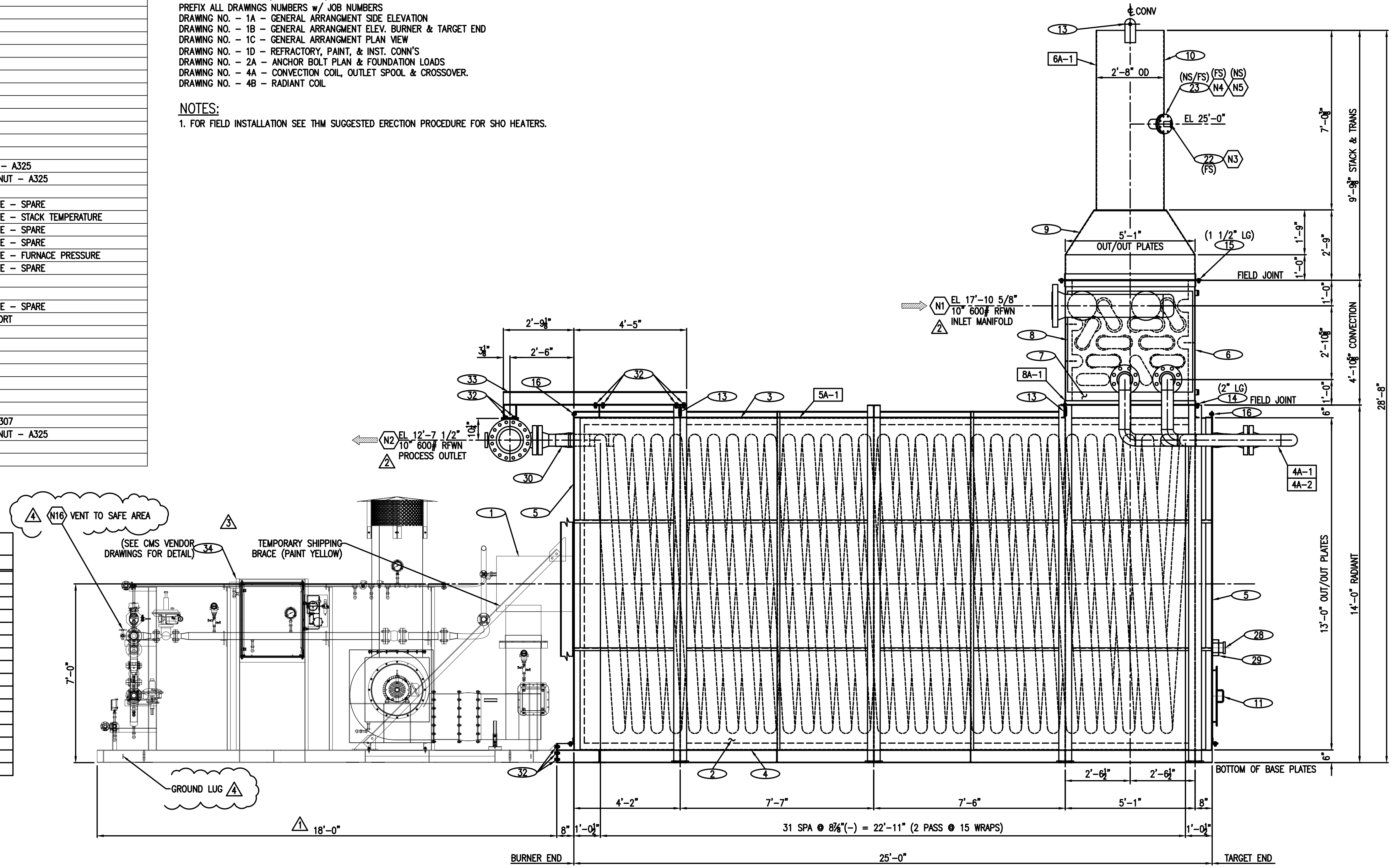
GENERAL ARRANGEMENT, FOUNDATION, & COIL FABRICATION DRAWING LIST IS AS FOLLOWS:
PREFIX ALL DRAWINGS NUMBERS w/ JOB NUMBERS
DRAWING NO. – 1A – GENERAL ARRANGMENT SIDE ELEVATION
DRAWING NO. – 1B – GENERAL ARRANGMENT ELEV. BURNER & TARGET END
DRAWING NO. – 1C – GENERAL ARRANGMENT PLAN VIEW
DRAWING NO. – 1D – REFRACTORY, PAINT, & INST. CONN'S
DRAWING NO. – 2A – ANCHOR BOLT PLAN & FOUNDATION LOADS
DRAWING NO. – 4A – CONVECTION COIL, OUTLET SPOOL & CROSSOVER.
DRAWING NO. – 4B – RADIANT COIL

NOTES:

1. FOR FIELD INSTALLATION SEE THM SUGGESTED ERECTION PROCEDURE FOR SHO HEATERS.

CUSTOMER CONNECTIONS

MARK	SIZE	RATING	TYPE	MATERIAL	SERVICE
2 N1	10"	600#	RFWN	SA105	PROCESS INLET
2 N2	10"	600#	RFWN	SA105	PROCESS OUTLET
N3	1 1/2"	3000#	FNPT	SA105	SPARE
N4	4"	150#	RFWN	SA105	SAMPLE PORT
N5	4"	150#	RFWN	SA105	SAMPLE PORT
N6	1 1/2"	3000#	FNPT	SA105	TEMPERATURE CONNECTION
N7	1 1/2"	3000#	FNPT	SA105	SPARE
N8	1 1/2"	3000#	FNPT	SA105	SPARE
N9	1 1/2"	3000#	FNPT	SA105	SPARE
N10	1 1/2"	3000#	FNPT	SA105	SPARE
N11	1 1/2"	3000#	FNPT	SA105	FURNACE PRESSURE
N12	1 1/2"	900#	RFWN	SA105	SPARE CONNECTION
N13	1 1/2"	900#	RFWN	SA105	P.I. CONNECTION
N14	1 1/2"	900#	RFWN	SA105	SPARE CONNECTION
N15	1 1/2"	900#	RFWN	SA105	SPARE CONNECTION
4 N16	1/2"	150#	RF	SA105	FUEL GAS VENT



SIDE ELEVATION

Customer:
LINDE ENGINEERING NA
XTO

LOCATION : NEW MEXICO
UNIT : N/A
SERVICE : REGEN GAS HEATER
EQUIPMENT No. : H-3132
P.O. No. : 004 2DA64□0 2
SHO : 2500

Rev.	Date	By	Revision Description
1	5/2□	SDB	REV ADDED CMS
2	7/23	SDB	REV PER CUSTOMER COMMENTS
3	11/22	SDB	REV CMS
4	1/7/1□	RU	REV PER CUSTOMER COMMENTS

THM TULSA HEATERS MIDSTREAM

Title: GENERAL ARRANGEMENT SIDE ELEV

Drawn By: JRW	Date: 4/14/18	Job No.: MJ18-327	
Checked By: ASW	Date: 4/18/18	Drawing No.: MJ18327-1A	Rev.: 4
Approved By	Certified By		

Owner:	XTO Energy	Owner Ref.:	PK-6010
Purchaser:	Audubon	Purchaser Ref.:	018193001
Manufacturer:	Tulsa Heaters Midstream	THM Ref.:	MJ18-346
Service:	Hot Oil Heater	Project:	Cowboy CDP
Number:	1	Location:	Carlsbad, NM
SHO Duty:	50.00 MMBTU/ hr	SHO Model:	SHO5000

Guarantees:

NOx	0.0067	Lb/MMBTU	5	ppm
SOx	no quote	Lb/MMBTU	-	ppm
CO	0.0163	Lb/MMBTU	20	ppm
VOC	0.0064	Lb/MMBTU	5	ppm
UHC	0.007	Lb/MMBTU	15	ppm
SPM	0.0134	Lb/MMBTU	15	ppm

58.93 MMBTU Stabilizer Heaters
w/ SCR NOx Control

		Design Case				Maximum Case			
Heat Release	LHV Basis	58.93	MMBTU/hr			64.83	MMBTU/hr		
Products of Combustion	MW								
O2	32.00	1,578	Lbm/ hr			1,778	Lbm/ hr		
N2 + Ar	28.15	40,582	Lbm/ hr			45,725	Lbm/ hr		
CO2	44.01	7,847	Lbm/ hr			8,841	Lbm/ hr		
H2O	18.02	5,817	Lbm/ hr			6,554	Lbm/ hr		
NOx	46.01	0.38	Lbm/ hr /	5	ppm	0.42	Lbm/ hr /	5	ppm
SOx	64.06	0.00	Lbm/ hr /	0	ppm	0.00	Lbm/ hr /	0	ppm
CO	28.01	0.94	Lbm/ hr /	20	ppm	1.03	Lbm/ hr /	20	ppm
VOC	44.10	0.37	Lbm/ hr /	5	ppm	0.41	Lbm/ hr /	5	ppm
UHC	16.04	0.40	Lbm/ hr /	15	ppm	0.44	Lbm/ hr /	15	ppm
SPM		0.77	Lbm/ hr /	15	ppm	0.85	Lbm/ hr /	15	ppm
Total		55,827	Lbm/ hr			62,901	Lbm/ hr		
Flue Gas Exit Temp.		488	°F						
Flue Gas Exit Velocity		35.1	Ft/sec			38.6	Ft/sec		
Stack Height		32.6	ft			32.6	ft		
Stack ID		48	in			48	in		

33' per drawing

NOTE:

THM emissions guarantees applicable between 50-100% of Design Case combustion conditions w/ 15% excess air.

THM emissions guarantees applicable for firebox temperatures above 1100°F.

Emissions above are for Design Case operation with air and fuel in ratio control. Upset conditions, such as operation outside the design, high turndown or start-up are not considered as guaranteed emissions cases.

The Maximum Case is the the specified heat release for the burner purchased. Extra duty is spec'd into the burner to ensure that the burner is never the limiting factor on duty.

revision	date	description	by	chk'd	appv'd

TULSA HEATERS MIDSTREAM

USA Applications

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EMISSIONS PERMIT DATA SHEET
AMERICAN ENGINEERING SYSTEM of UNITS

MJ18-346-Emissions-

Owner:	XTO Energy	Owner Ref.:	PK-6010
Purchaser:	Audubon	Purchaser Ref.:	018193001
Manufacturer:	Tulsa Heaters Midstream	THM Ref.:	MJ18-346
Service:	Hot Oil Heater	Project:	Cowboy CDP
Number:	1	Location:	Carlsbad, NM
SHO Duty:	50.00 MMBTU/ hr	SHO Model:	SHO5000

Guarantees:

58.93 MMBTU Stabilizer Heaters no SCR

NOx	0.0267	Lb/MMBTU	20	ppm
SOx	no quote	Lb/MMBTU	-	ppm
CO	0.0163	Lb/MMBTU	20	ppm
VOC	0.0064	Lb/MMBTU	5	ppm
UHC	0.007	Lb/MMBTU	15	ppm
SPM	0.0134	Lb/MMBTU	15	ppm

		Design Case				Maximum Case			
Heat Release	LHV Basis	58.93	MMBTU/hr			64.83	MMBTU/hr		
Products of Combustion									
	MW								
O2	32.00	1,578	Lbm/ hr			1,778	Lbm/ hr		
N2 + Ar	28.15	40,581	Lbm/ hr			45,723	Lbm/ hr		
CO2	44.01	7,847	Lbm/ hr			8,841	Lbm/ hr		
H2O	18.02	5,817	Lbm/ hr			6,554	Lbm/ hr		
NOx	46.01	1.54	Lbm/ hr /	20	ppm	1.69	Lbm/ hr /	20	ppm
SOx	64.06	0.00	Lbm/ hr /	0	ppm	0.00	Lbm/ hr /	0	ppm
CO	28.01	0.94	Lbm/ hr /	20	ppm	1.03	Lbm/ hr /	20	ppm
VOC	44.10	0.37	Lbm/ hr /	5	ppm	0.41	Lbm/ hr /	5	ppm
UHC	16.04	0.40	Lbm/ hr /	15	ppm	0.44	Lbm/ hr /	15	ppm
SPM		0.77	Lbm/ hr /	15	ppm	0.85	Lbm/ hr /	15	ppm
Total		55,827	Lbm/ hr			62,901	Lbm/ hr		
Flue Gas Exit Temp.		488	°F						
Flue Gas Exit Velocity		35.1	Ft/sec			38.6	Ft/sec		
Stack Height		32.6	ft			32.6	ft		
Stack ID		48	in			48	in		

33' per drawing

NOTE:

THM emissions guarantees applicable between 50-100% of Design Case combustion conditions w/ 15% excess air.

THM emissions guarantees applicable for firebox temperatures above 1100°F.

Emissions above are for Design Case operation with air and fuel in ratio control. Upset conditions, such as operation outside the design, high turndown or start-up are not considered as guaranteed emissions cases.

The Maximum Case is the the specified heat release for the burner purchased. Extra duty is spec'd into the burner to ensure that the burner is never the limiting factor on duty.

revision	date	description	by	chk'd	appv'd

USA Applications

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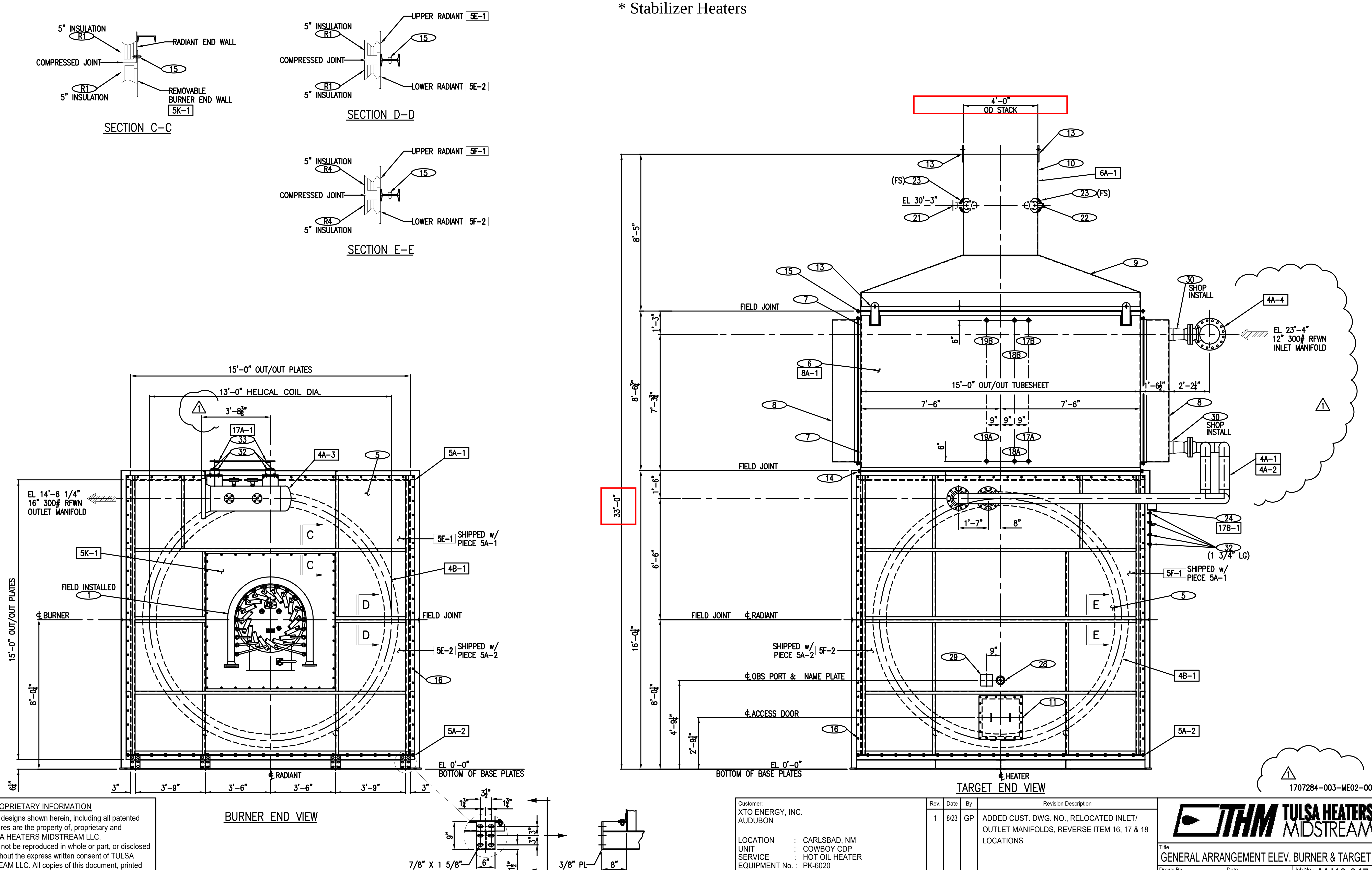
EMISSIONS PERMIT DATA SHEET

AMERICAN ENGINEERING SYSTEM of UNITS

MJ18-346-Emissions-

* Stabilizer Heaters



PROPRIETARY INFORMATION

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This document shall not be reproduced in whole or part, or disclosed to any third party without the express written consent of TULSA HEATERS MIDSTREAM LLC. All copies of this document, printed or electronic, are null and void if modified or altered in any way. Only TULSA HEATERS MIDSTREAM LLC possesses the controlling document in its original state and shall govern over any copy, printed or electronic.

Customer:
XTO ENERGY, INC.
AUDUBON

LOCATION	:	CARLSBAD, NM
UNIT	:	COWBOY CDP
SERVICE	:	HOT OIL HEATER
EQUIPMENT No.	:	PK-6020
P.O. No.	:	1707284-003
SHO	:	5000

Rev.	Date	By	Revision Description
1	8/23	GP	ADDED CUST. DWG. NO., RELOCATED INLET/ OUTLET MANIFOLDS, REVERSE ITEM 16, 17 & 18 LOCATIONS

THM TULSA HEATERS MIDSTREAM

Title: GENERAL ARRANGEMENT ELEV. BURNER & TARGET END

Drawn By: JPW	Date: 7/14/18	Job No.: MJ18-347
Checked By: ASW	Date: 7/15/18	Drawing No.: MJ18347-1B
Approved By:	Certified By:	Rev.: 1

Owner:	XTO Energy	Owner Ref.:	PK-6310
Purchaser:	Audubon	Purchaser Ref.:	018193001
Manufacturer:	Tulsa Heaters Midstream	THM Ref.:	MJ19-395
Service:	Hot Oil Heater	Project:	Cowboy CDP
Number:	1	Location:	Carlsbad, NM
SHO Duty:	79.30 MMBTU/ hr	SHO Model:	SHO5000

Guarantees:

NOx	0.0067	Lb/MMBTU	5	ppm
SOx	no quote	Lb/MMBTU	-	ppm
CO	0.0163	Lb/MMBTU	20	ppm
VOC	0.0064	Lb/MMBTU	5	ppm
UHC	0.007	Lb/MMBTU	15	ppm
SPM	0.013	Lb/MMBTU	15	ppm

94.54 MMBTU Cryo Heaters /w SCR NOx Control

		Design Case				Maximum Case			
Heat Release LHV Basis		94.54	MMBTU/hr			103.99	MMBTU/hr		
Products of Combustion	MW								
O2	32.00	2,657	Lbm/ hr			2,923	Lbm/ hr		
N2 + Ar	28.15	66,981	Lbm/ hr			73,679	Lbm/ hr		
CO2	44.01	12,059	Lbm/ hr			13,265	Lbm/ hr		
H2O	18.02	10,400	Lbm/ hr			11,440	Lbm/ hr		
NOx	46.01	0.63	Lbm/ hr /	5	ppm	0.69	Lbm/ hr /	5	ppm
SOx	64.06	0.00	Lbm/ hr /	0	ppm	0.00	Lbm/ hr /	0	ppm
CO	28.01	1.54	Lbm/ hr /	20	ppm	1.69	Lbm/ hr /	20	ppm
VOC	44.10	0.61	Lbm/ hr /	5	ppm	0.67	Lbm/ hr /	5	ppm
UHC	16.04	0.66	Lbm/ hr /	15	ppm	0.73	Lbm/ hr /	15	ppm
SPM		1.23	Lbm/ hr /	15	ppm	1.35	Lbm/ hr /	15	ppm
Total		92,101	Lbm/ hr			101,311	Lbm/ hr		
Flue Gas Exit Temp.		599	°F						
Flue Gas Exit Velocity		65.3	Ft/sec			71.8	Ft/sec		
Stack Height		~~34.3~~	ft			34.3	ft		
Stack ID		48	in			48	in		

76.9' per drawing

NOTE:

THM emissions guarantees applicable between 50-100% of Design Case combustion conditions w/ 15% excess air.

THM emissions guarantees applicable for firebox temperatures above 1100°F.

Emissions above are for Design Case operation with air and fuel in ratio control. Upset conditions, such as operation outside the design, high turndown or start-up are not considered as guaranteed emissions cases.

The Maximum Case is the the specified heat release for the burner purchased. Extra duty is spec'd into the burner to ensure that the burner is never the limiting factor on duty.

revision	date	description	by	chk'd	appv'd

TULSA HEATERS MIDSTREAM

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EMISSIONS PERMIT DATA SHEET
AMERICAN ENGINEERING SYSTEM of UNITS

MJ19-395-Emissions-

Owner:	XTO Energy	Owner Ref.:	PK-6110
Purchaser:	Audubon	Purchaser Ref.:	018193001
Manufacturer:	Tulsa Heaters Midstream	THM Ref.:	MJ18-349
Service:	Hot Oil Heater	Project:	Cowboy CDP
Number:	1	Location:	Carlsbad, NM
SHO Duty:	79.30 MMBTU/ hr	SHO Model:	SHO5000

Guarantees:

NOx	0.0334	Lb/MMBTU	25	ppm
SOx	no quote	Lb/MMBTU	-	ppm
CO	0.0163	Lb/MMBTU	20	ppm
VOC	0.0064	Lb/MMBTU	5	ppm
UHC	0.007	Lb/MMBTU	15	ppm
SPM	0.013	Lb/MMBTU	15	ppm

94.54 MMBTU Cryo Heaters no SCR

		Design Case				Maximum Case			
Heat Release	LHV Basis	94.54	MMBTU/hr			103.99	MMBTU/hr		
Products of Combustion									
	MW								
O_2	32.00	2,657	Lbm/ hr			2,923	Lbm/ hr		
N_2 + Ar	28.15	66,978	Lbm/ hr			73,676	Lbm/ hr		
CO_2	44.01	12,059	Lbm/ hr			13,265	Lbm/ hr		
H_2O	18.02	10,400	Lbm/ hr			11,440	Lbm/ hr		
NOx	46.01	3.16	Lbm/ hr /	25	ppm	3.47	Lbm/ hr /	25	ppm
SOx	64.06	0.00	Lbm/ hr /	0	ppm	0.00	Lbm/ hr /	0	ppm
CO	28.01	1.54	Lbm/ hr /	20	ppm	1.69	Lbm/ hr /	20	ppm
VOC	44.10	0.61	Lbm/ hr /	5	ppm	0.67	Lbm/ hr /	5	ppm
UHC	16.04	0.66	Lbm/ hr /	15	ppm	0.73	Lbm/ hr /	15	ppm
SPM		1.23	Lbm/ hr /	15	ppm	1.35	Lbm/ hr /	15	ppm
Total		92,101	Lbm/ hr			101,311	Lbm/ hr		
Flue Gas Exit Temp.		599	°F						
Flue Gas Exit Velocity		65.3	Ft/sec			71.8	Ft/sec		
Stack Height		34.3	ft			34.3	ft		
Stack ID		48	in			48	in		

76.9 per drawing

NOTE:

THM emissions guarantees applicable between 50-100% of Design Case combustion conditions w/ 15% excess air.

THM emissions guarantees applicable for firebox temperatures above 1100°F.

Emissions above are for Design Case operation with air and fuel in ratio control. Upset conditions, such as operation outside the design, high turndown or start-up are not considered as guaranteed emissions cases.

The Maximum Case is the the specified heat release for the burner purchased. Extra duty is spec'd into the burner to ensure that the burner is never the limiting factor on duty.

revision	date	description	by	chk'd	appv'd

THM TULSA HEATERS MIDSTREAM

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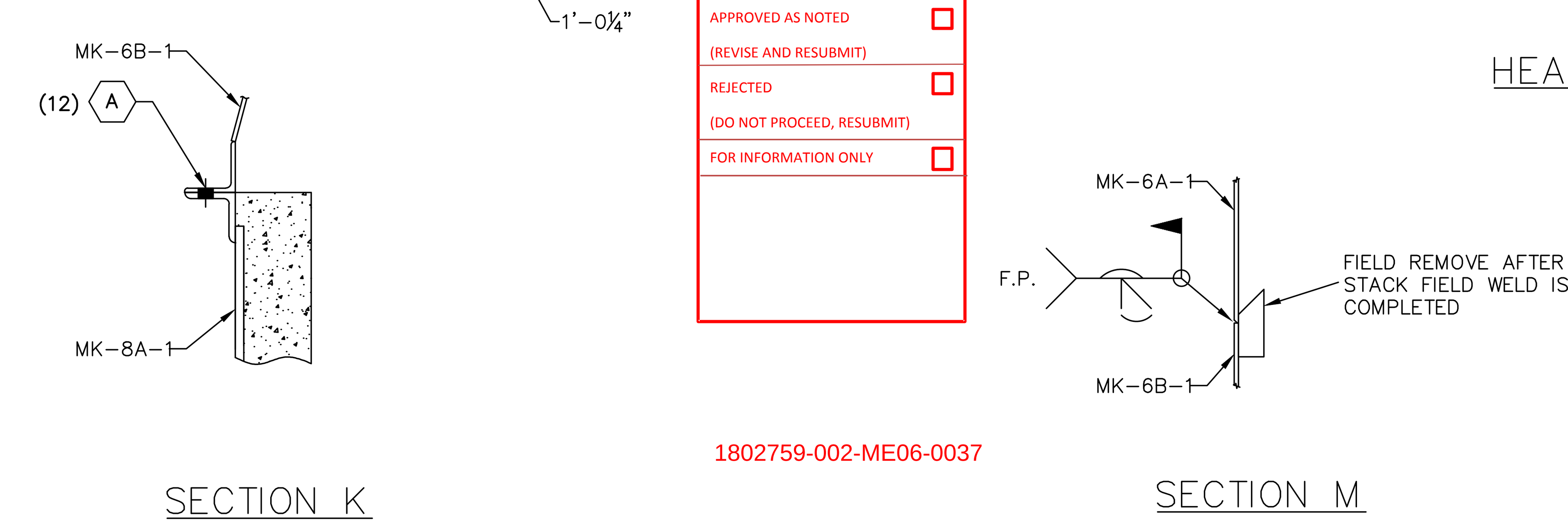
EMISSIONS PERMIT DATA SHEET
AMERICAN ENGINEERING SYSTEM of UNITS

MJ18-349-Emissions-

APPROVED
(PROCEED AS IS)
APPROVED AS NOTED
(REVISE AND RESUBMIT)
REJECTED
(DO NOT PROCEED, RESUBMIT)
FOR INFORMATION ONLY

1802759-002-ME06-0037



PROPRIETARY INFORMATION

Customer:
AUDUBON / XTO ENERGY

LOCATION : CARLSBAD, NM.
UNIT : CRYO UNIT
SERVICE : HOT OIL HEATER
EQUIP. No. : PK-6110
P.O. No. : 1802759-002
THI JOB No.: 18925

Rev.	Date	By	Revision Description

THI TULSA HEATERS INC.

Title	FIELD ERECTION		
Drawn By GG	Date 7-24-18	Job No.: 18925	
Checked By KEN	Date 7-25-18	Drawing No. 18925-3A	Rev. 0

Thermal Oxidizer (TO1-TO4) Specs

4.4 Flue Gas at 1700°F, Normal Operation

	Normal Case
COMPONENT:	**lb/hr**
CO_2	22743.78
H_2O	3869.91
N_2	17926.10
SO_2	2.72
O_2	1376.65
TOTAL	**45919.16**

4.5 System Performance

Stack Emission	**Expected Performance**
Destruction Efficiency	> 99.95% of all H2S / VOC
NOx, ppm_{vd} @ 3% O2	50
CO, ppm_{vd} @ 3% O2	50

These values are understood to apply only when the system is operated in accordance with the operating conditions stipulated in the design summary and for the waste stipulated in the design basis sections of this proposal.

Tulsa, Oklahoma

Thermal Oxidizer Datasheet

Customer Document No.

REV	BY	DATE	DESCRIPTION
A	JNM	16-Jul-18	Issued for Review
B	SN	9-Aug-18	Issued for Review
C	SN	31-Aug-18	Issued for Review

Zeeco Document No. 35595-2031

Project: Cowboy - CDP

BY	APPR	DATE
JNM	SN	16-Jul-18

Client:	XTO Energy
End User:	Cowboy CDP
Job Site:	Carlsbad, NM
Tag Number:	TO Thermal Oxidizer / TO-6980

#						
	DESIGN					
1	Service	Acid Gas Incineration				
2	Waste Gas Flow (Max), lb/hr	22,541 (Acid Gas) / 547 (Flash Gas) / 588 (BTEX w/ Stripping Gas)				
3	Incinerator Operating Temp, ^{o}F	1700-1800				
4	Altitude ASL, ft	3400				
5	Product Flow Max, lb/hr	50,226				
6	Air Flow Design, lb/hr	26,973				
7	Max Waste Release, mmBTU/HR	21.6				
8	Max Total Heat Release, mmBTU/HR	24.1				
9	Number Required	1				
10	**INCINERATOR SPECIFICATIONS**					
11	Type	Vertical Thermal Oxidizer				
12	Size	7' OD x 52' OAH				
13						
14	Shell Material	SA-36				
15, 16	Refractory	Floor: 4" 3000°F Castable, backed w/ 2" Insulating Castable. Stack: 4" 2300°F Insulating Castable				
17	Mechanical Design Temp (°F) / Pressure (psig)	650 / 0				
18	Mastic (Y/N)	N				
19	Refractory Anchors	310 SS				
20	Burner Connection, in.	36"				
21	Jacket	Corrugated Rainshield				
23	Access Door	30" Manway with Davit				
24	Lifting Lug Design	X	YES		NO	Two(2) lifting trunnions 180° apart
25	Slide Plates		YES	X	NO	
26	Rainshield	X	YES		NO	
28	**BURNER SPECIFICATIONS**					
29	Type	Forced Draft Design				
30	Pilot	Premix with High Energy Ignitor				
31	Combustion Air Change in Pressure (in WC)	3				
33	Fuel Gas Rel, mmBTU/HR	25				
34	Waste Gas Rel, mmBTU/HR	0.8 (Acid Gas) / 10.74 (Flash Gas) / 10.01 (BTEX w/ Stripping Gas)				
35						
36	**NOZZLES**					

#	Noz.	Description	Size (in)
38	N1	Burner Connection	36"
39	N2A/B	Sample Ports w/ Blind	4"
40	N3A/B	Thermocouple	1-1/2"
41	N4	Sampling Port	4"
42	N5A/B	Spare Conn.	2"
43	N6	Sight Port w/ Blast Gate	4"
44	M1	Manway w/ Davit	30"
45			

46–60 **NOTES:** Reference Document for Nozzles - 35595-G065A-001

Tulsa, Oklahoma

Burner Datasheet

Customer Doc No.	
Zeeco Doc No.	35595-2030
Project:	Cowboy - CDP

REV	BY	DATE	DESCRIPTION
A	JNM	16-Jul-18	Issued for Review
B	SN	9-Aug-18	Issued for Review

BY	APPR	DATE
JNM	SN	16-Jul-18

Client:	XTO Energy
Customer:	
Job Site:	Cowboy CDP
Tag Number:	GB Burner / BR-6980

VESSEL DATA	
Firing Direction	Vertical
Refractory Thickness at Burner Nozzle (in.)	6"
Type of Draft (Natural, Forced, Induced)	Forced
BURNER MECHANICAL DATA	
Burner Item Number	
Type	GB
Quantity	1
Location	Carlsbad, NM
Burner Mounting	Bolted
Burner Design Code	None
Burner Case Material	Carbon Steel
Tile Block Material	60% Alumina
Scanner Type	1" Swivel Scanner
Scanner Quantity / Connection Quantity	2
Paint	Per Customer Specifications
BURNER PROCESS DATA	
Maximum Burner Combustion Air Pressure Drop, in WC	2.9
Design Combustion Air Temperature, °F	100
Design Combustion Air Flowrate, lb/hr	28,151
Combustion Air Turn Down lb/hr	5,630
Maximum Excess Air (%)	35%

HEAT RELEASE (mmBTU/hr)		
Case	Fuel Gas	
	Heat Release	
Maximum (Rated)	25	
Minimum	2.5	

PILOT DATA	
Model:	AR/GS-1
Quantity per Burner	1
Size (in.)	1 1/2"
Ignition	Electronic HEI
Operating Pressure (PSI)	10
Air / Gas Consumption (SCFH)	1609/178 (methane)

FUEL CHARACTERISTICS

Type of Fuel	Rich Fuel Gas	Lean Fuel Gas			
LHV (BTU/SCF)	1153	885			
Molecular Weight	21.52	16.43			
Pressure Avail. (psig)	125	125			
Temperature (°F)	35-80	110			
Composition - VOL %					
Nitrogen	2.1448	3.166			
CO2	0.2038	0.006			
Methane	74.43	96.7529			
Ethane	13.73	0.075			
Propane	6.4286				
i-Butane	0.628				
n-Butane	1.6049				
i-Pentane	0.2989				
n-Pentane	0.3112				
n-Hexane	0.1				
n-Heptane	0.1				
H2O	0.0192				
Total:	99.9994	99.9999			

NOZZLE SCHEDULE

ITEM	QTY	SIZE / RATING	SERVICE
B1	1	36" / FAB	Mounting Flange
B2	1	16" / 150#	Waste Gas Conn. /Acid gas
B3	1	20" / FAB	Combuston Air Conn.
B4	1	2" / 150#	Fuel Gas Conn.
B5	1	2" / 150#	Flash Gas Conn.
B6	1	1-1/2" / 150#	Pilot Mounting Conn.
B7	1	1" / 150#	Drain w/ Blind
B8	1	1" / 150#	Drain w/ Blind
B9	1	1" NPT	Pilot Sight Port Conn. w/ Purge
B10	1	2" NPT	Sight Port Conn. w/ Purge
B11	1	1" NPT	Main Flame Scanner Conn. w/ Purge
B12	1	3" / 150#	BTEX Stream Conn.

NOTES:

1. Reference Documents - P&ID for Burner 35595-04-11001-002 (Cust. No. 1802750-003-ME08-0007)
2. Reference Documents - Burner General Arrangement 35595-G006A-001 (Cust. No. 1802759-003-ME02-0040)
3. Expected NOx & CO ppmv included in proposal as indicated here:

Stack Emission	Expected Performance
Destruction Efficiency	*> 99.95% of all H2S / VOC*
NOx, ppm_{vd} @ 3% O2	50
CO, ppm_{vd} @ 3% O2	*50*

– DESIGN DATA –

DESIGN CODE:	ASME STS-1-2011
DESIGN PRESSURE INTERNAL	0 PSI @ 650°F
HYDRO TEST	NONE
MAWP	5 PSI @ 650°F
MDMT	-20°F
PWHT	NO
LETHAL SERVICE:	NO
SEISMIC CODE PER ASCE 7-10	SITE CLASS = C, IMP FACTOR = 1.25, Ss = 0.24%, S1 = 0.05%, R = 3
WIND CODE PER ASCE 7-10	WIND SPEED = 120 MPH, EXP. = C, IMP FACTOR = 1.15
RADIOGRAPH	SHELL: SPOT, SHELL CIRC.: SPOT, SHELL LONG.: SPOT
JOINT EFFICIENCY	SHELL: 0.85, SHELL CIRC.: 0.85, SHELL LONG.: 0.85
ALLOWABLE CORROSION:	1/8"
ESTIMATED STEEL FABRICATION WT.	20,375 LB.
ESTIMATED TEST WEIGHT	N/A
ESTIMATED OPERATING/EMPTY WEIGHT	59,806 LB.
ESTIMATED CAPACITY	10,411 GAL.

– NOZZLE LEGEND –

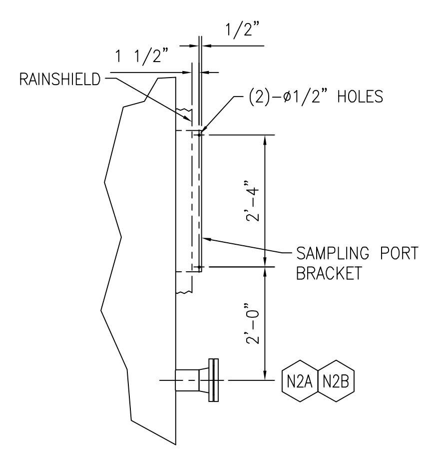
ITEM	SERVICE	SIZE	RATING	TYPE	CODE	SCH/BORE	FLG. MAT'L.	NECK MAT'L.
N1	BURNER CONNECTION	36"	FAB.	FAB.	FABRICATED	---	A-36	---
N2A/B	SAMPLE PORTS w/ BLIND	4"	150#	RFWN	ASME B16.5	STD.	A-105	A-106-B
N3A/B	THERMOCOUPLE	1 1/2"	150#	RFWN	ASME B16.5	XH	A-105	A-106-B
N4	SPARE O_2 ANALYZER CONN. w/ BLIND	4"	150#	RFWN	ASME B16.5	STD.	A-105	A-106-B
N5A/B	SPARE CONNECTION	2"	---	M.N.P.T.	------	STD.	----	A-106-B
N6	SIGHT PORT W/ BLAST GATE	4"	150#	RFWN	ASME B16.5	STD.	A-105	A-106-B
M1	MANWAY WITH DAVIT	30"	FAB.	FAB.	FABRICATED	.250"	A-36	A-36
C1	PURGE CONNECTION	3/4"	6000#	F.N.P.T.	------	-----	A-105	------
C2	PURGE CONNECTION	3/4"	6000#	F.N.P.T.	------	-----	A-105	------
C3	PURGE CONNECTION	3/4"	6000#	F.N.P.T.	------	-----	A-105	------

– GENERAL NOTES –

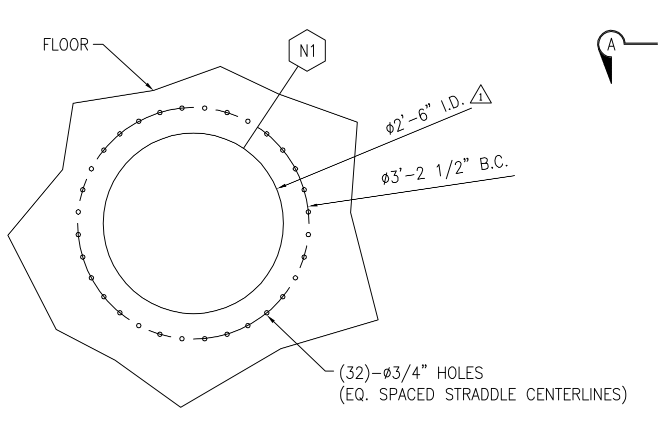
1. ONE UNIT REQUIRED. TAG NUMBER: TO-1801
2. ALL FABRICATION IN ACCORDANCE WITH ASME STS-1-2011.
3. FLANGE HOLES SHALL STRADDLE NORMAL VESSEL CENTERLINES UNLESS OTHERWISE NOTED.
4. FOR PAINT, SEE ZEECO DOCUMENT 35595-4030.
5. REFRACTORY IS TO BE FURNISHED AND SHOP INSTALLED BY ZEECO.
6. FOR REFRACTORY, REFRACTORY LEGEND AND REFRACTORY NOTES, SEE DRAWING 35595-R064A-001.
7. FOR LIFTING DIAGRAM, SEE DRAWING 35595-G064A-010.

– MATERIALS –

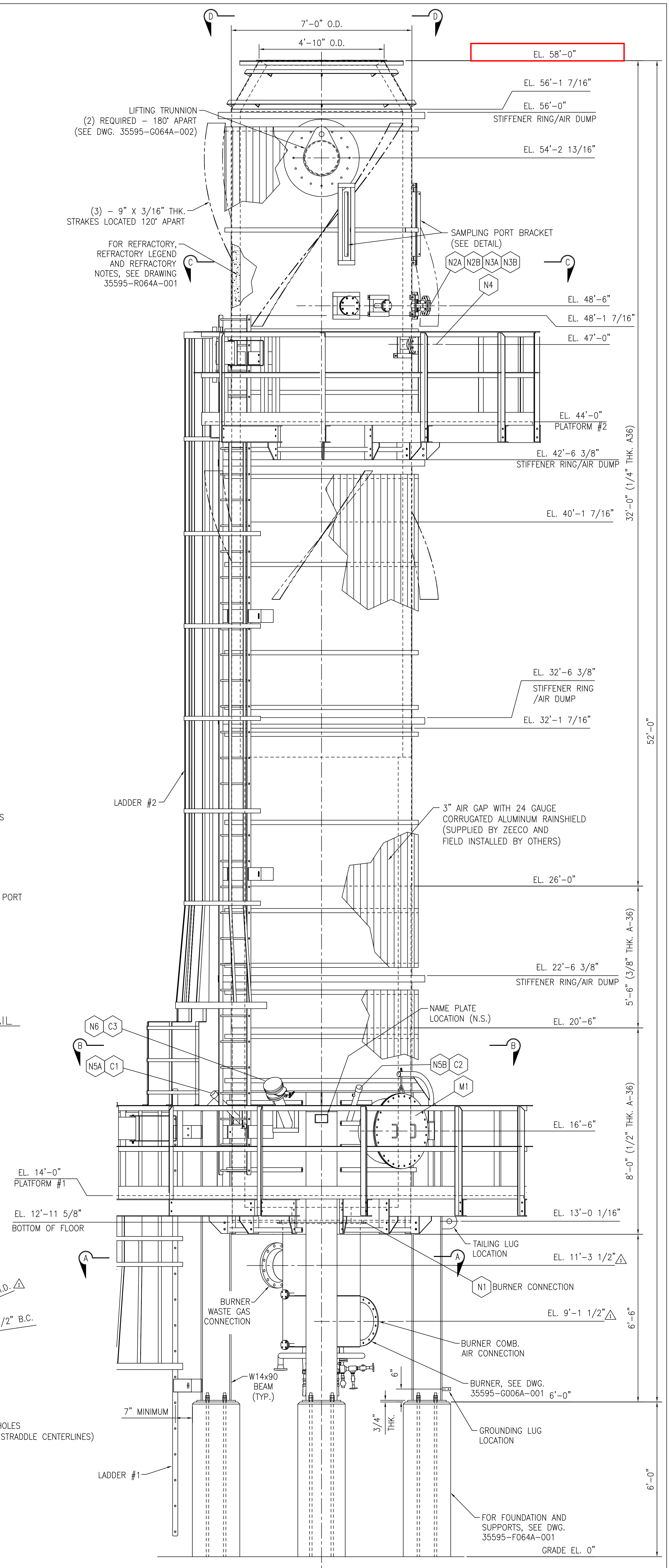
SHELL	A-36
NOZZLE CYLINDERS & PIPES	A-36 / A-106-B
FLANGE FORGINGS	A-105
STUD BOLTS/NUTS	A-193-B7 / A-194-2H ZINC PLATED
GASKETS	1/8" SERVICE SHEET GASKET
VESSEL SUPPORT COLUMNS	A-992
COUPLINGS	A-105
TAILING LUGS	A-36
LIFTING TRUNNIONS	A-36



SAMPLING PORT BRACKET DETAIL



BURNER MOUNTING



ELEVATION VIEW
(LOOKING NORTH)

REFERENCE DRAWINGS:

THERMAL OXIDIZER SYSTEM GENERAL ARRANGEMENT ____ 35595-G061A-001, 002, 003
FOUNDATION PLAN THERMAL OXIDIZER SYSTEM __________ 35595-F061A-001
THERMAL OXIDIZER FOUNDATION PLAN __________________ 35595-F064A-001
THERMAL OXIDIZER REFRACTORY DETAILS _____________ 35595-R064A-001

NO	DATE	REVISION DESCRIPTION	BY	CKD	APP.
2	31AUG18	REVISED AS NOTED	SAN	DAK	SAN
1	16JUL18	REVISED AS NOTED	ABG	JGH	SAN
0	12JUL18	ISSUED FOR APPROVAL	ABG	JGH	SAN

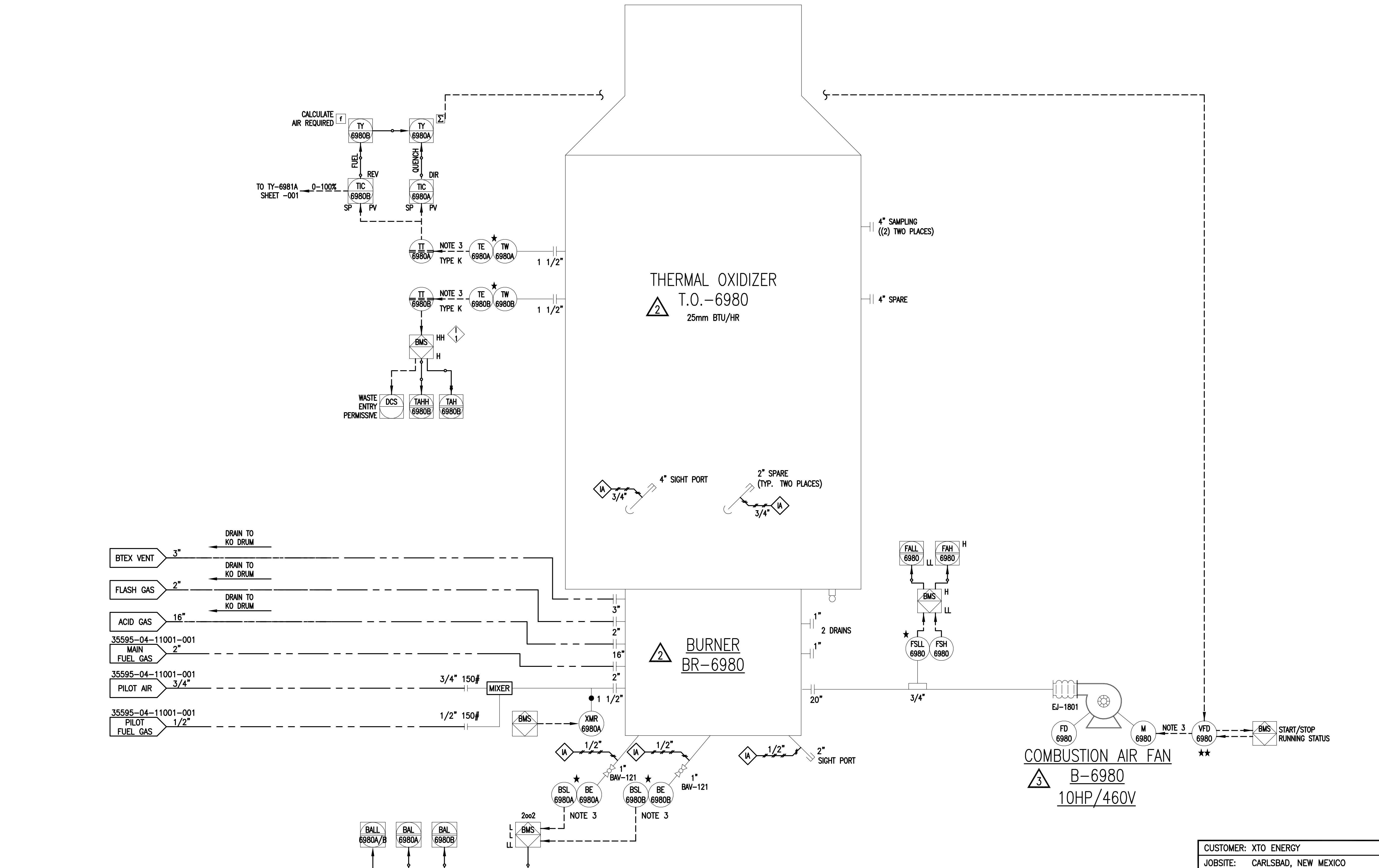
CUSTOMER: XTO ENERGY, INC.
JOBSITE: COWBOY CDP, CARLSBAD, NEW MEXICO
END USER: AUDUBON COMPANIES
P.O. NO.: 1802759-003-ME02-0035

ZEECO, INC.
22151 EAST 91st STREET
BROKEN ARROW, OK 74014
PHONE: (918) 258-8551
FAX: (918) 251-5519
www.zeeco.com
sales@zeeco.com

THERMAL OXIDIZER
GENERAL ARRANGEMENT

S.O. NO. TO-6980
DWG., SUB. CAT. & SYSTEM NO.
35595 - G064A - 001

DRAWN	DATE	CHK	APP	SCALE	APP	DWG. NO.	REV. NO.
ABG	12JUL18	JGH	SAN	NONE	JM		2



SEE PID-35595-04-11001-001 FOR LEGEND AND NOTES

NO.	DATE	REVISION DESCRIPTION	BY	CKD.	APP.
3	03OCT18	REVISED AS NOTED	SAN	EK	SAN
2	31AUG18	REVISED PER CUSTOMER COMMENTS	BLS	EK	SN
1	02AUG18	REVISED PER CUSTOMER COMMENTS	BLC	EK	SN
0	28JUN18	ISSUED FOR APPROVAL	BLC	JEA	SN

CUSTOMER: XTO ENERGY
JOBSITE: CARLSBAD, NEW MEXICO
END USER: AUDOBON COMPANIES
P.O. NO.: 1802759-003

ZEECO, INC.
22151 EAST 91st STREET
BROKEN ARROW, OK 74014
PHONE: (918) 258-8551
FAX: (918) 251-5519
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P & I DIAGRAM
INCINERATOR PACKAGE
THERMAL OXIDIZER

DRAWN	DATE
BLC	28JUN18
CHK JEA	APP SN
SCALE N.T.S.	APP –

S.O. NO. GROUP DWG. SUB CAT. SYSTEM NO. DWG. NO. REV. NO.
35595-04-11001-002 3

Flare (FL1-3) Specs

audubon
D: 713.452.3123
kejones@auduboncompanies.com

10205 Westheimer Road, Suite 100
Houston, Texas 77042
auduboncompanies.com | LinkedIn

From: Cody Faulkenberry <Cody_Faulkenberry@zeeco.com>
Sent: Friday, May 4, 2018 5:30 PM
To: Kelly Jones <kejones@auduboncompanies.com>; Kirsten Berg <Kirsten_Berg@zeeco.com>; Gabriel Garcia <ggarcia@auduboncompanies.com>
Cc: Nikki Jenlink <Nikki_Jenlink@zeeco.com>; Scott Reed <Scott_Reed@zeeco.com>; Blake Knight <Blake_Knight@zeeco.com>; Alan Forman <integratedcontrols@prodigy.net>; John Ehlig <John_Ehlig@zeeco.com>; Sean O'Grady <Sean_OGrady@zeeco.com>
Subject: RE: 2018-02438FL-01: RFQ 018193001-AE-RFQ-ME0018 - Combustor Package - XTO Energy Cowboy Natural Gas and Oil CDP

Kelly,

Below are the guaranteed DRE's for each piece of combustion equipment in regards to the XTO Cowboy project.

There will be no cost impact added to our proposals to meet the DRE's listed below. If a higher DRE is required, we can provide equipment that meets the request.

1. CDP Flare System, 98% DRE
2. CDP Combustor, 99% DRE
3. Thermal Oxidizer, 99.99% DRE

Please let us know if you have any questions or more official documentation is needed. Thanks!

Cody Faulkenberry
Applications Engineer, Sales

Zeeco Houston | Cell: +1 713 859 6047 | Direct: +1 918 893 8816

From: Kelly Jones [mailto:kejones@auduboncompanies.com]
Sent: Wednesday, May 02, 2018 7:18 AM
To: Kirsten Berg <Kirsten_Berg@zeeco.com>; Gabriel Garcia <ggarcia@auduboncompanies.com>
Cc: Nikki Jenlink <Nikki_Jenlink@zeeco.com>; Scott Reed <Scott_Reed@zeeco.com>; Blake Knight <Blake_Knight@zeeco.com>; Alan Forman <integratedcontrols@prodigy.net>; Cody Faulkenberry <Cody_Faulkenberry@zeeco.com>; John Ehlig <John_Ehlig@zeeco.com>
Subject: RE: 2018-02438FL-01: RFQ 018193001-AE-RFQ-ME0018 - Combustor Package - XTO Energy Cowboy Natural Gas and Oil CDP
Importance: High

Kirsten,

Stabilizer Flare (F1 Specs)

ZEECO, INC.

CLIENT:	Audubon	DOCUMENT NO:	35284-8020
USER:	XTO Energy	PAGES:	1258 + Cover
PROJECT:	Cowboy CDP		
CLIENT P.O. #:	1707284-002 / 1707285-003	ZEECO SO:	35284

1707284-002-1707285-03-AA01-0021

FLARE SYSTEM

FS -6810 HP LP Flare Stack

FINAL DATA BOOK

REV	DATE	BY	APP	DESCRIPTION
0	01MAY19	ADM	TRD	FOR YOUR USE

Predicted Utility Requirements

Client:	Audubon	Zeeco Ref.:	35284	Date:	11-Apr-19
Location:	New Mexico - XTO Cowboy	Client Ref.:	1707284-002 / 1707285-003	Rev.	0

Equipment	Normal Operations Utility Requirements
HP / LP AFTAMJ-18/50-12	**Pilot Gas Consumption (Fuel Gas):** 65.12 SCFH @ 15 PSIG Per Pilot (Lean Fuel) 56.17 @ 15 PSIG Per Pilot (Rich Fuel) **HP Purge Gas requirement:** 480 SCFH (Fuel Gas) or 180 SCFH (N2) **LP Purge Gas Requirement:** 706 SCFH (Fuel Gas From Pilot Gas Manifold) and 50 SCFH (Fuel Gas From LP Riser) or 530 SCFH (N2 From LP Riser)
GENERAL	**Electrical Consumption per Ignition Rack (HP & Acid)** 700 W @ 120V, 60 Hz, 1 Ph During Ignition 400 W @ 110V, 60 Hz, 1 Ph After Ignition **Ignition Timing** 1 pulse per 3 seconds, Timeout after 3 minutes **Ignition Gas Consumption On Control Rack Assembly:** 109 SCFH @ 15 PSIG (Ignition Period Only) **Instrument Air Consumption On Control Rack Assembly:** 986 @ 15 PSIG (Ignition Period Only)

NOTES:
(1) Pilot fuel gas requirements are based upon a fuel gas with an LHV of 923 BTU/SCF and a specific gravity of 0.56.
(2) If ignition is made and pilot temperature returns to high temperature above setpoint before 5 minutes, then igniter will cease and timer will not timeout. System will go back to high temperature state.
(3) Electrical Consumption during ignition includes all power required for the entire panel.

Air Assisted Flare Tip Specification Sheet

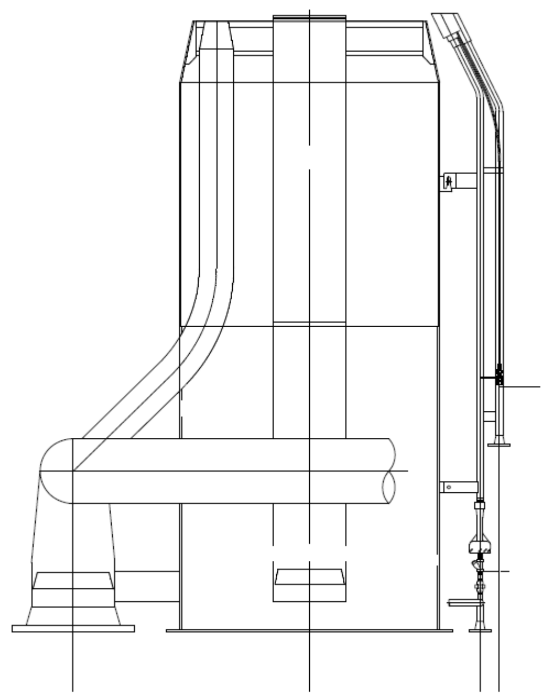
Client:	Audobon Engineering	Zeeco Ref.:	2018-01056FL-02	Date:	14-May-18
Location:	Carlsbad, NM	Client Ref.:	018193001-AE-RFQ-ME0017	Rev.	3

General Information:

Tag No.:	F-1		
Model:	AFTA-18/50-12	Type:	Air-Assisted
Length:	10'- 0 "		
Weight:	5000 lbs		
No. of Pilots:	3		

Design Case:

Governing Case:	HP Max Case	
Molecular weight:	21.3	
L. H. V. :	1,143	BTU/SCF
Temperature:	-50	Deg. F
Available Static Pressure:	50.0	psig
Design Flow Rate:	467,821	lbs/hr
Governing Smokeless Case:	Case A	
Design Smokeless Rate:	46,782	lbs/hr
Approximate Exit Velocity:	1122	ft/s
Mach No.:	1.00	
Approx. Tip Press. Drop:	41.29	psig



(Typical drawing only)

Construction:

Upper Section:	310 SS	Windshield:	NO
Lower Section:	Carbon Steel	Flame Retention Hub:	310 SS
Refractory:	None	Lifting Lugs:	NO
Refractory Thk:	N/A		

Surface Finish (Carbon Steel Surfaces):

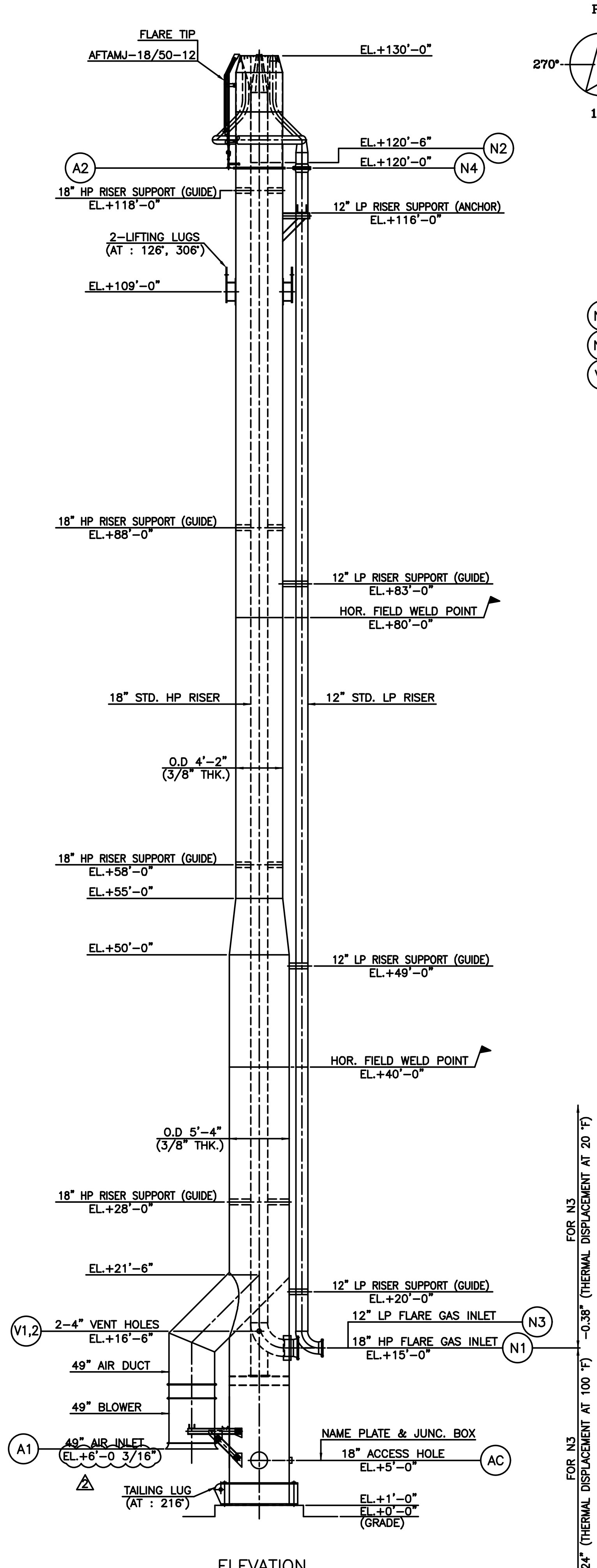
Surface Preparation:	SSPC-SP6	Primer:	Inorganic Zinc
Paint (c. s. surfaces):	High Heat Aluminum		

Connections:

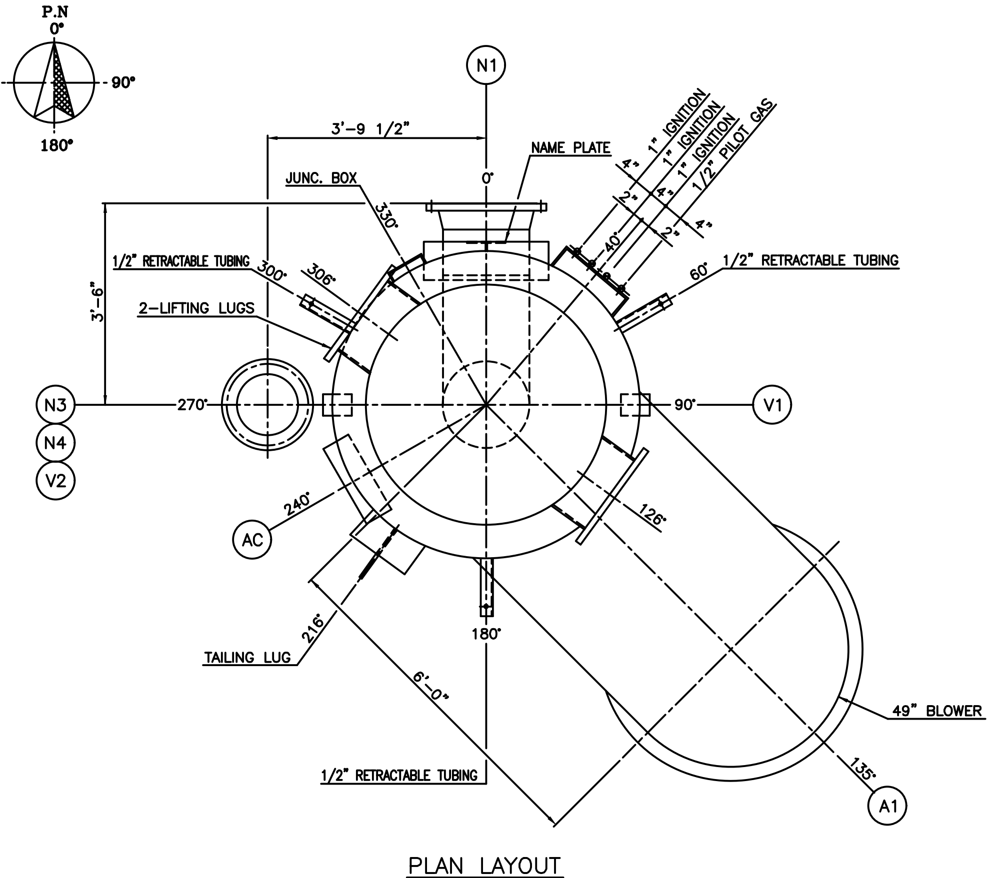
	Qty.	Size	Type	Material
N1 - HP Flare Gas Inlet:	1	18 "	Beveled ; Weld	Carbon Steel
N2 - Combustion Air Inlet:	1	50 "	Fab. Plate Flange	Carbon Steel
N3 - LP Flare Gas Inlet:	1	12 "	150# RF	Carbon Steel
N4 - Pilot Gas:	1	1 "	150# RF	Carbon Steel

Miscellaneous Notes:

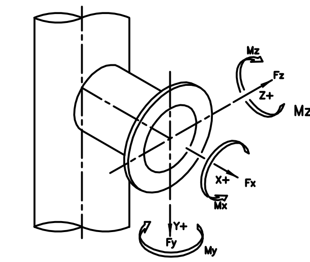
1. Includes Integral Purge Reducing Velocity Seal.
2. Recommended Purge Rate for HP: 480 SCFH (Fuel Gas) or 180 (Nitrogen).
3. Recommended Purge Rate for LP Flare: 320 SCFH (Fuel Gas) or 60 SCFH (Nitrogen).
4. See Attachment C, Process Conditions, for HP / LP Process Conditions.



ELEVATION

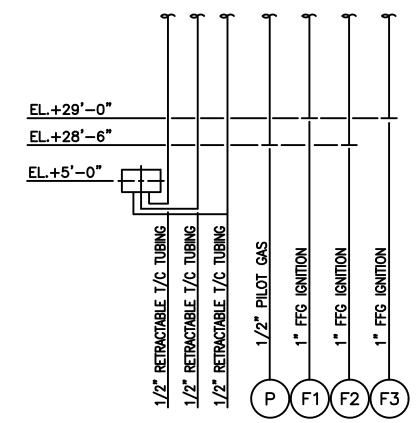


PLAN LAYOUT
(SCALE : 1/20)



PIPE SIZE (IN)	Fx	Fy	Fz	Mx	My	Mz
	lb	lb	lb	lb-ft	lb-ft	lb-ft
12"	400	700	700	1000	750	750
18"	550	850	850	1210	900	900

MAX. ALLOWABLE INLET NOZZLE LOADS
(PER API537)



UTILITY PIPING DETAIL

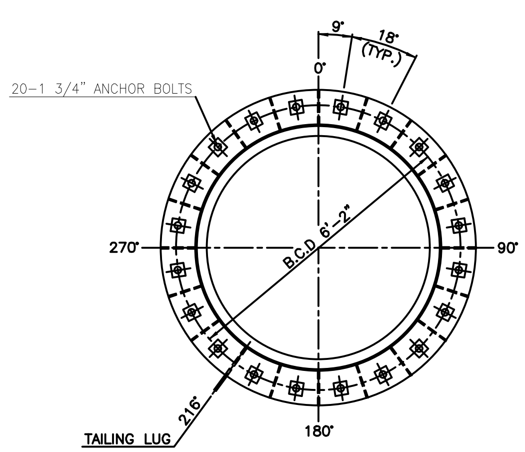
MATERIAL SPECIFICATIONS		DESIGN DATA		
HP GAS RISER	A333-6	TYPE	SELF SUPPORT TYPE	
LP GAS RISER	A106-B	DESIGN CODE	ASME-STS-1 / AISC	
AIR RISER	A36	WIND DESIGN	ASCE-7-10/ V=120mph/ EXP.=C	
SKIRT	A36	SEISMIC DESIGN	ASCE-7-10/ SITE CLASS=D/ Ss=0.153/ S1=0.045/ I.F=1.25	
FLARE TIP	SEE FLARE TIP DWG.	FLUID	FLARE GAS	
RISER FLANGE (HP/LP)	A350-LF2 CL.1 / A105	DESIGN PRESS.(HP/LP/AIR)	50 / 50 / ATM	psig
RISER FLANGE (AIR)	A36	DESIGN TEMP.(HP/LP/AIR)	-50~350 / 20~100 / AMB	°F
RISER BOLT/NUT	A193-B7/A194-2H	M.A.W.P.(NEW & COLD)	-	psig
RISER GASKET	C4401	OPERATING PRESS.(HP/LP)	-	psig
BASE PLATE	A36	OPERATING TEMP.(HP/LP/AIR)	-50 / 25 / 20~100	°F
ANCHOR BOLT	F1554 Gr. 36	HYDRO'C TEST PRESS.	-	psig
EARTH LUG	304 S.S	PNEUM'C TEST PRESS.	-	psig
NAME PLATE	304 S.S	P.W.H.T.	NO	
NAME PLATE BRACKET	A36 OR EQ.	RADIOGRAPH	AS PER ITP, SPOT	
UTILITY LINE	A106-B	JOINT EFFICIENCY	85	%
CONDUIT LINE	C.S (GALV.)	CORROSION ALLOWANCE (HP/LP)	1/16" / 1/16"	INCH
LIFTING LUG	A36	CORROSION ALLOWANCE (AIR)	0"	INCH
TALING LUG	A36	PAINTING	SEE NOTE 2	

NOZZLE AND CONNECTIONS

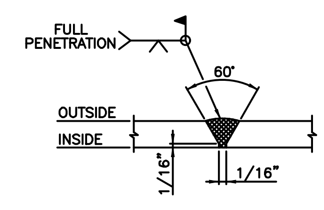
MARK	Q'TY	SIZE	SCH.	RATING	FACING	FLG. MAT'L	MATERIAL NOZZLE	SERVICE	REMARKS	℄ TO FACE
N1	1	18"	STD.	ASME #150	WN, RF	A350-LF2 CL.1	A333-6	HP FLARE GAS INLET		3'-8"
N2	1	18"	STD.	-	-	-	A333-6	HP FLARE GAS OUTLET		SEE DWG.
N3	1	12"	STD.	ASME #150	WN, RF	A105	A106-B	LP FLARE GAS INLET		SEE DWG.
N4	1	12"	STD.	ASME #150	WN, RF	A105	A106-B	LP FLARE GAS OUTLET		SEE DWG.
A1	1	49"	3/8"	3/8" PLATE FLANGE	-	A36	A36	AIR INLET		SEE DWG.
A2	1	50"	3/8"	3/4" PLATE FLANGE	-	A36	A36	AIR OUTLET		SEE DWG.
V1,2	2	4"	STD.	-	-	-	A53-B	VENT HOLE		-
AC	1	18"	3/8"	-	-	-	A36	ACCESS HOLE		-
P	1	1/2"	40	ASME #150	SW, RF	A105	A106-B	PILOT GAS		SEE DWG.
F1~3	3	1"	40	ASME #150	SW, RF	A105	A106-B	FFG IGNITION		SEE DWG.

NOTE

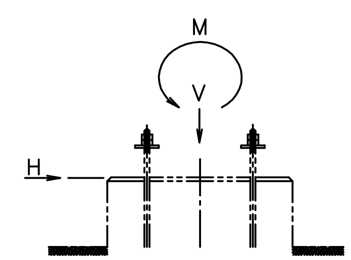
1. FLANGE BOLTING TO STRADDLE CENTERLINES INDICATED BY CENTERLINE UNLESS NOTED OTHERWISE.
2. PAINTING
   - EXTERNAL CARBON STEEL SURFACE (AIR RISER & LP RISER)
     - PAINT SPEC. : 018193001-AE-SP-ME1007
     - CHART 4 : SSPC-SP10
     - AMERON, CARBOLINE, SHERWIN WILLIAMS
   - EXTERNAL CARBON STEEL SURFACE (HP RISER)
     - SSPC-SP10
     - PRIMER ONLY : SAME AS AIR & LP RISER
   - INTERNAL CARBON STEEL (SKIRT TO BLOWER PLATE)
     - SSPC-SP10
     - PRIMER ONLY : SAME AS AIR & LP RISER
3. ALL UTILITY PIPING LINES WILL BE SUPPLIED IN RANDOM LENGTH FOR FIELD WELDING AND INSTALLATION AT JOB SITE.
4. CONCRETE COMPRESSIVE STRENGTH AT 28 DAYS , FC' = 4000 PSI
5. LOADING DATA INCLUDES OVERAGE FACTOR OF 10% ABOVE CALCULATED LOADS.
6. FLARE STACK STRUCTURAL DESIGN ASSUMES ELASTIC FOUNDATION SUPPORT PER ASME STS-1.



ANCHOR BOLT PLAN
(SCALE : 1/25)

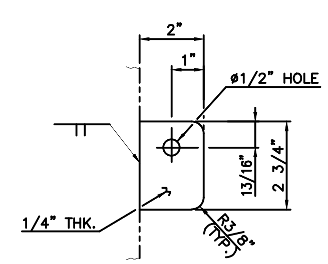


FIELD WELD DETAIL
(TYP.)



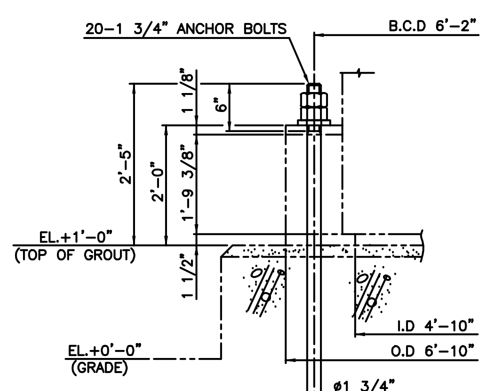
LOADING DATA
(FOR STACK RISER)

FS 6810 ON ALL DRAWINGS



EARTH LUG
(AT : 90°, 270°)
(SCALE : 1/3)

LOADING DATA			
	V(kip)	H(kip)	M(kip-ft)
DEAD LOAD	66.5	0.0	0.0
WIND LOAD	0.0	18.3	1377.7
SEISMIC LOAD	2.2	1.5	138
NOZZLE LOAD	1.7	2.0	31.0



ANCHOR BOLT
(FOR STACK RISER)

REFERENCE DRAWING NO.	DESCRIPTION
SD-7438	FLARE TIP ASSEMBLY
SD-7509	CONDUIT DETAIL
SD-7508	PIPING DETAIL
SD-7507	PIPING ARRANGEMENT
SD-7506	RISER DETAIL
SD-7505	TEMPLATE DETAIL

NO	DATE	REVISION DESCRIPTION	BY	CKD	APP.
2	29NOV18	REVISED AS MARKED	MGE	CK	TRD
1	01NOV18	REVISED AS MARKED	MGE	CK	TRD

JOBSITE: Eddy County, New Mexico

END USER: XTO Energy

S.O. NO.: 35284 | P.O. NO.: 1707284-002 | APP KNB

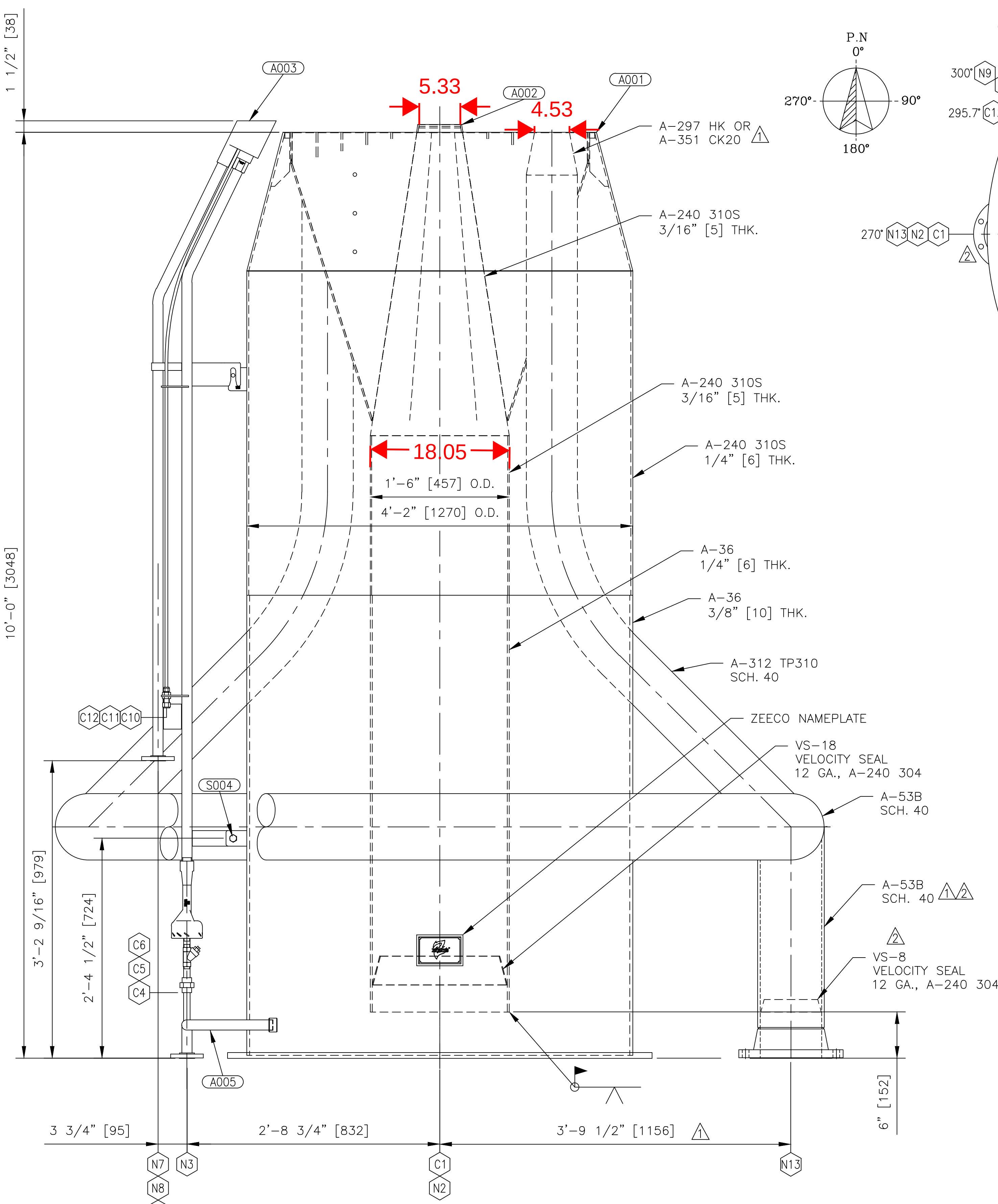
ZEECO, INC.
22151 EAST 91st STREET
BROKEN ARROW, OK 74014
PHONE: (918) 258-8551
FAX: (918) 251-5519
www.zeeco.com
sales@zeeco.com

SELF SUPPORTED
FLARE STACK SYSTEM
GENERAL ARRANGEMENT & LOADING DATA

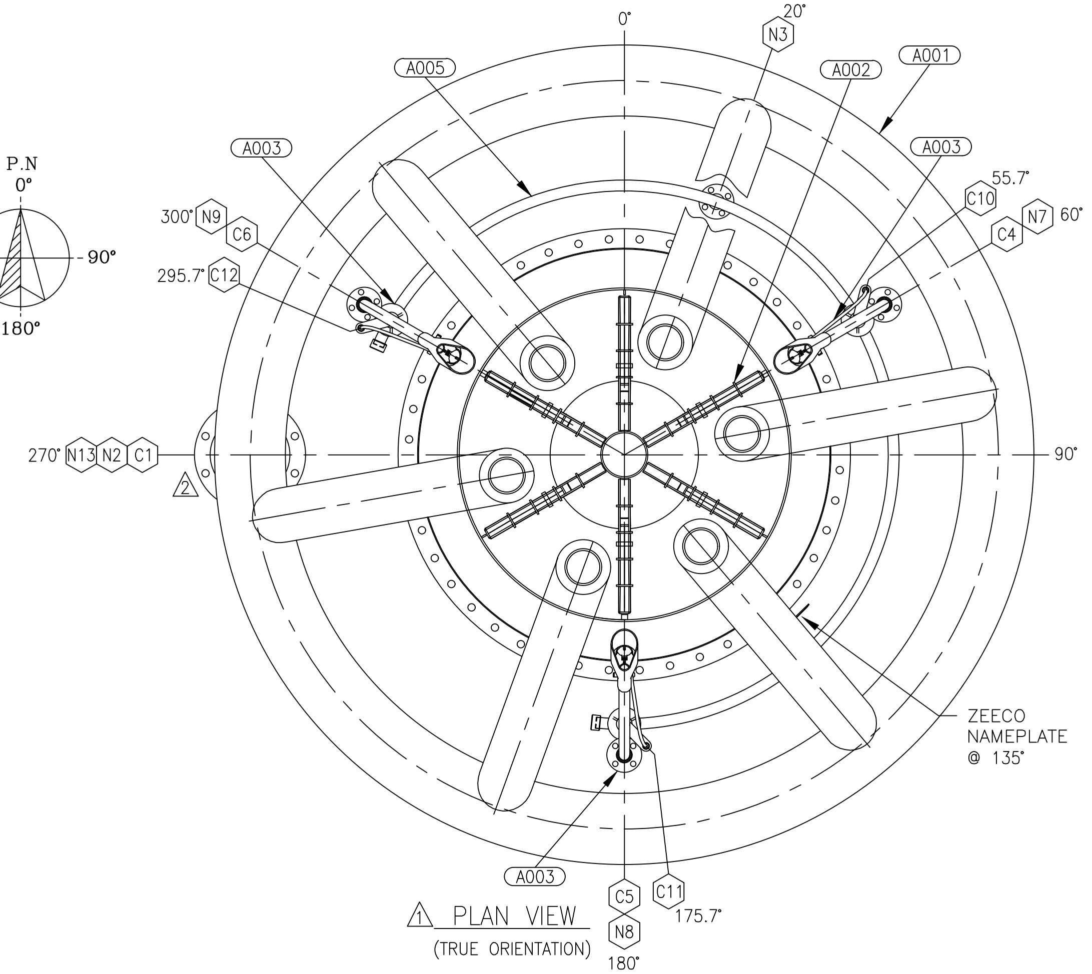
FOR: AUDUBON ENGINEERING

DRAWN	DATE
MGE	27JUL18
CHK CK	APP TRD
SCALE 1/80	REV 2

DRAWING NUMBER SD-7441
SHT. 1 OF 1



ELEVATION VIEW
(PORTIONS ROTATED FOR CLARITY)



PLAN VIEW
(TRUE ORIENTATION)

ZEECO, INC.®
Tulsa, Oklahoma USA
For parts & service: +1-918-258-8551 / sales@zeeco.com
AFTAMJ-18/50-8 FLARE TIP ASSEMBLY
TAG NUMBER: F-1
P.O. NO: 1707284-002
2018 — YEAR BUILT
35284 — S.O. NUMBER

ZEECO NAMEPLATE

- SD-7438 PARTS LIST -

ITEM	QTY	Description	P/N
A001	1	AFTAMJ-18/50-8 PLENUM ASSEMBLY	KC-7653-A001
A002	1	AFTAMJ-18/50-8 CENTER ASSEMBLY	KC-7654-A002
A003	3	HSLF-Z-FFG-RDT/C PILOT ASSEMBLY	MB-4868-A003
		COMPLETE WITH:	
		HEI IGNITION PROBE	
		THERMOCOUPLE (SEE DATASHEET)	
		HSLF-Z MIXER BODY	
		HSLF-Z MIXER SPUD	
		STRAINER W/PLUG	
S004	3	HEAVY HEX BOLT: 1/2-13UNC X 1 1/2" LG. (A-193 B8M)	080001-0069
		W/ HEAVY HEX NUT: 1/2-13 UNC (A-194 GR. 8M)	081001-0135
A005	1	PILOT MANIFOLD ASSEMBLY	KC-7655-A005

-NOTES-

1. PILOT MIXER ORIFICE DRILLED: 3/64"Ø [1.19 mm]
2a. PILOT GAS CONSUMPTION LEAN FUEL: 65.12 SCFH @ 15 PSIG PER PILOT [1.74 Nm³ /HR @ 1.05 kg/cm² g]
2b. PILOT GAS CONSUMPTION RICH FUEL: 56.17 SCFH @ 15 PSIG PER PILOT [1.50 Nm³ /HR @ 1.05 kg/cm² g]
3. PILOT ORIFICE DRILLING BASED ON 923 BTU/SCF (LHV) [8683 kcal/Nm³] GAS WITH 0.563 SP. GR.
4a. THE HP FLARE TIP REQUIRES A CONTINUOUS PURGE OF 480 SCFH [12.86 Nm³ /HR] OR 180 SCFH [4.82 Nm³ /HR] (N_2) OF A GAS THAT WILL NOT GO TO DEW POINT AT OPERATING TEMPERATURES. TO ENSURE AIR DOES NOT MIGRATE DOWN THE FLARE STACK. IT SHOULD BE NOTED THAT DEPENDING UPON THE TURNDOWN OPERATION OF THE FAN AND THE TYPE OF PURGE GAS USED IT MAY BE NECESSARY TO INCREASE THIS MINIMUM PURGE RATE TO ENSURE PROPER COMBUSTION OF THE PURGE GAS DURING IDLE OPERATION.
4b. THE LP FLARE TIP REQUIRES A CONTINUOUS PURGE OF 706 SCFH [18.91 Nm³ /HR] OR 530 SCFH [14.20 Nm³ /HR] (N_2) OF A GAS THAT WILL NOT GO TO DEW POINT AT OPERATING TEMPERATURES. TO ENSURE AIR DOES NOT MIGRATE DOWN THE FLARE STACK. IT SHOULD BE NOTED THAT DEPENDING UPON THE TURNDOWN OPERATION OF THE FAN AND THE TYPE OF PURGE GAS USED IT MAY BE NECESSARY TO INCREASE THIS MINIMUM PURGE RATE TO ENSURE PROPER COMBUSTION OF THE PURGE GAS DURING IDLE OPERATION.
5. ALL FLANGE BOLTING TO STRADDLE NORMAL CENTERLINES, UNLESS NOTED OTHERWISE.
6. ALL TESTING PER INSPECTION TEST PLAN DOCUMENT NO. 35284-4010
7. THE PILOT THERMOCOUPLE IS FOR ON/OFF INDICATION ONLY, NOT FOR ACCURATE MEASUREMENT OF THE PILOT FLAME TEMPERATURE.
8. WHEN INSTALLING THE CENTER ASSEMBLY THE GAS EXIT ARMS MUST BE CENTERED ON THE PILOT AS PER THE PLAN VIEW.
9. APPROXIMATE WEIGHT FOR FLARE TIP ASS'Y: 4,731 LBS. [2,146 Kg]
10. APPROXIMATE WEIGHT FOR FOR EACH PILOT: 65 LBS. [29 Kg.]
11. ALL EXTERNAL CARBON STEEL SURFACES TO BE PREPARED PER SSPC-SP10. PRIME WITH ONE COAT INORGANIC ZINC (2-3 MILS DFT MIN.). PAINT ONE COAT HIGH HEAT ALUMINUM (1-2 MILS DFT MIN.). FINISH COLOR: ALUMINUM. CUSTOMER PAINT SPEC: 018193001-AE-SP-ME1007
12. LP FLARE GAS INLET (N13) WILL NEED TO BE ABLE TO CONTRACT 0.34" VERTICALLY.

DRAWING	DRAWING NUMBER
P & I DIAGRAM FOR FLARE SYSTEM	YA-3129
GENERAL ARRANGEMENT	SD-7441
LMC-3-DT/S FFG IGNITION RACK ASSEMBLY	WD-0071

-NOZZLE LEGEND-

ITEM	SERVICE	SIZE	RATING	TYPE	SCH./BORE	FLG. MAT'L
C1	HP FLARE GAS INLET	18"	N/A	B.W.	SCH. 10	N/A
N2	FLARE AIR INLET	55" O.D. X 3/4" THK. X 50 1/4" I.D. W/ (44) 7/8"ø HOLES ON A 52 1/2" B.C.				A-36
N3	PILOT GAS MANIFOLD INLET	1"	150#	RFSW	SCH.40	A-105
C4-C6	PILOT GAS INLET	1/2"	3000#	SW UNION	SCH. 40	A-182 F304/L
N7-N9	IGNITION GAS INLET	1"	150#	RFSW	SCH.40	A-182 F304
C10-C12	RT/C CONNECTION	1/2"	N/A	TUBE	N/A	A-479 TP316
N13	LP FLARE GAS INLET	8"	150#	RFWN	SCH. 40	A-105

NO.	DATE	REVISION DESCRIPTION	BY	CKD.	APP.
3	30nov18	APPROVED	MKN	MDK	TRD
2	12SEP18	REVISED PER ENGINEERING	ASW	MKN	TRD
1	28AUG18	REVISED PER ENGINEERING	MDK	MKN	TRD
0	20JUL18	ISSUED FOR APPROVAL	MKN	RLO	TRD

JOBSITE: EDDY COUNTY, NEW MEXICO
END USER: XTO ENERGY
S.O. NO.: 35284
P.O. NO.: 1707284-002
APP: KNB

ZEECO, INC.
22151 EAST 91st STREET
BROKEN ARROW, OK 74014
PHONE: (918) 258-8551
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sales@zeeco.com

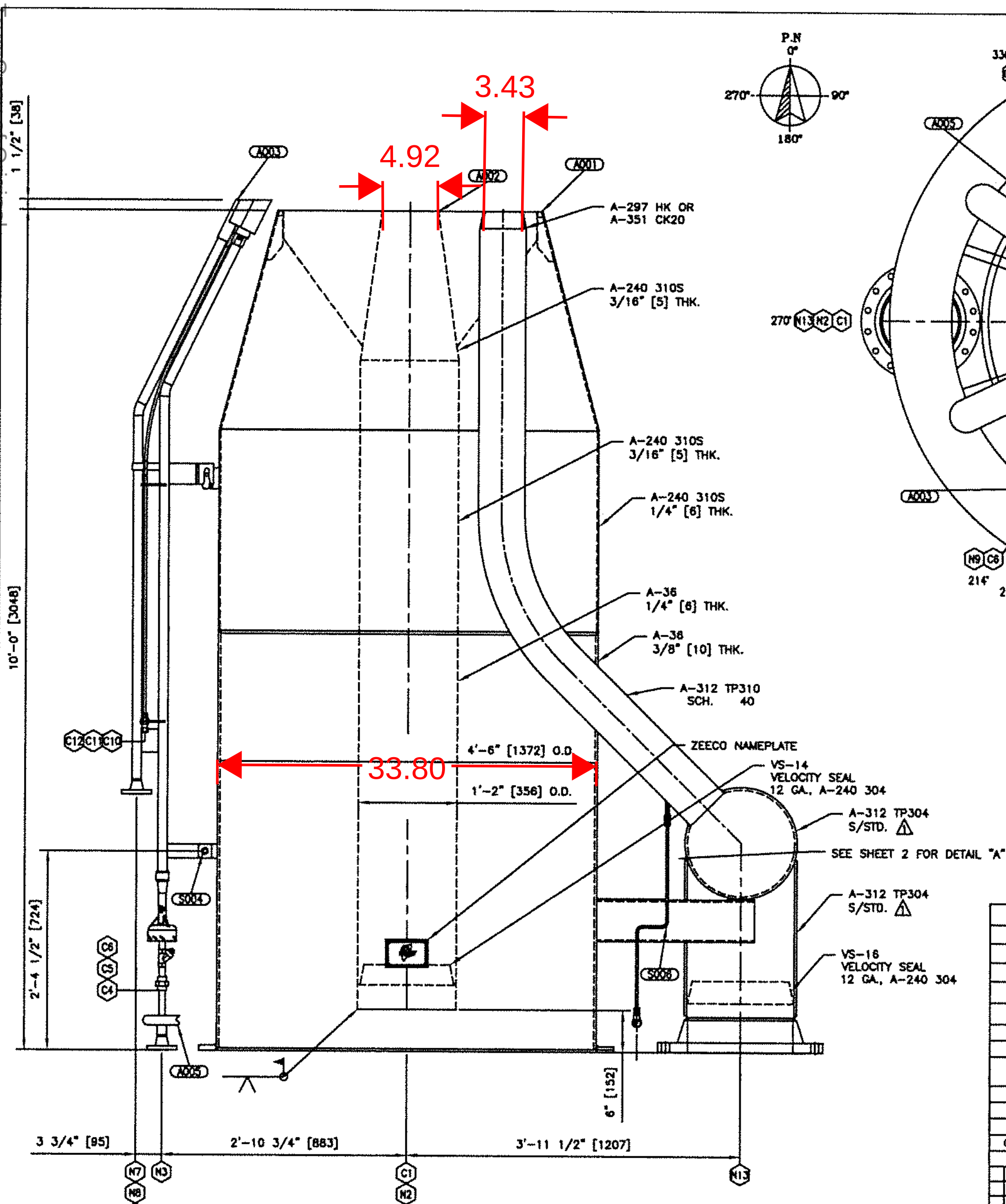
AFTAMJ-18/50-8
FLARE TIP ASSEMBLY

FOR: AUDUBON

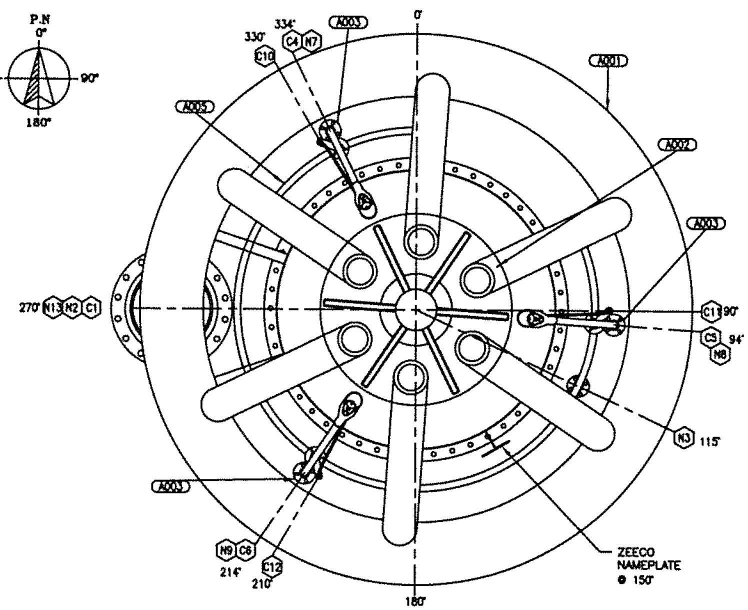
DRAWN	DATE
MKN	20JUL18
CHK: RLO	APP: TRD
SCALE: NONE	REV: 3

DRAWING NUMBER: SD-7438
SHT. 1 OF 1

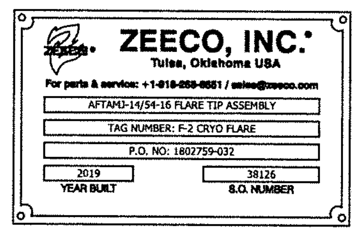
Cryo Flare (F2 Specs)



ELEVATION VIEW
(PORTIONS ROTATED FOR CLARITY)



PLAN VIEW
(TRUE ORIENTATION)



ZEECO NAMEPLATE

DRAWING	DRAWING NUMBER
P & I DIAGRAM FOR FLARE SYSTEM	YA-3310
GENERAL ARRANGEMENT	SD-8259
LMC-3-DT/S FFG IGNITION RACK ASSEMBLY	WD-0610

-NOZZLE LEGEND-

ITEM	SERVICE	SIZE	RATING	TYPE	SCH./BORE	FLG. MAT'L
C1	LP FLARE GAS INLET	14"	N/A	B.W.	SCH. 10	N/A
N2	FLARE AIR INLET	59" O.D. X 3/4" THK. X 54 1/4" I.D. W/ (48) 7/8"φ HOLES ON A 56 1/2" B.C.				A-36
N3	PILOT GAS MANIFOLD INLET	1"	150#	RFWN	SCH.40	A-105
C4-C6	PILOT GAS INLET	1/2"	3000#	SW UNION	SCH. 40	A-182 F304/L
N7-N9	IGNITION GAS INLET	1"	150#	RFSW	SCH. 40	A-182 F304/L
C10-C12	RT/C CONNECTION	1/2"	N/A	TUBE	N/A	A-479 TP316
N13	HP FLARE GAS INLET	16"	150#	RFWN	SCH. 40	A-182 F304

NO.	DATE	REVISION DESCRIPTION	BY	CKD.	APP.
1	27MAR19	REVISED PER ENGINEERING / CUSTOMER COMMENTS	MKN/ASW	RLO	JSK
0	25FEB19	ISSUED FOR APPROVAL	MKN	RLO	JSK

- SD-8301 PARTS LIST -

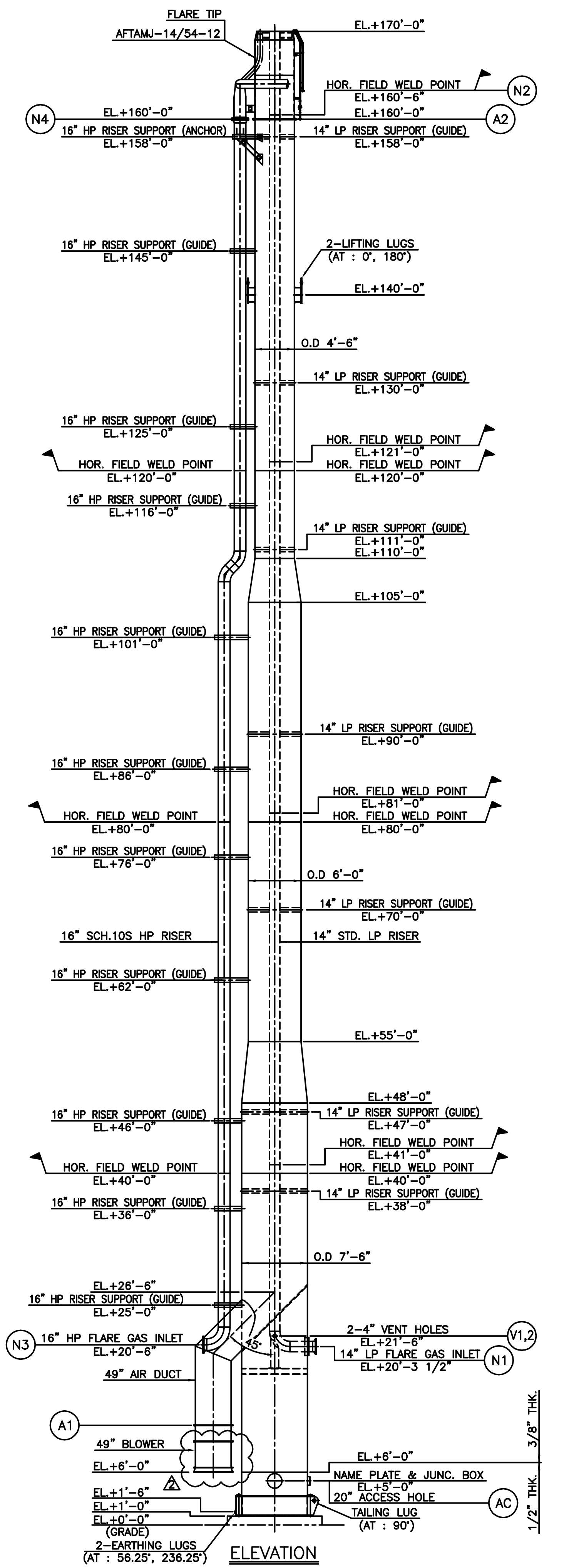
ITEM	QTY	Description	P/N
A001	1	AFTAMJ-14/54-16 PLENUM ASSEMBLY	KC-8197-A001
A002	1	AFTAMJ-14/54-16 CENTER ASSEMBLY	KC-8198-A002
A003	3	HSLF-Z-FFG-RDT/C PILOT ASSEMBLY	MB-5232-A003
		COMPLETE WITH:	
		THERMOCOUPLE (SEE DATASHEET)	
		HSLF-Z MIXER BODY	
		HSLF-Z MIXER SPUD	
		STRAINER W/PLUG	
S004	3	HEAVY HEX BOLT: 1/2-13UNC X 1 1/2" LG. (A-193 B8M)	080001-0069
		W/ HEAVY HEX NUT: 1/2-13 UNC (A-194 GR. 8M)	081001-0135
A005	1	PILOT MANIFOLD ASSEMBLY	KC-8199-A005
S006	6	FUEL INJECTION TUBE	033005-0001

-NOTES-

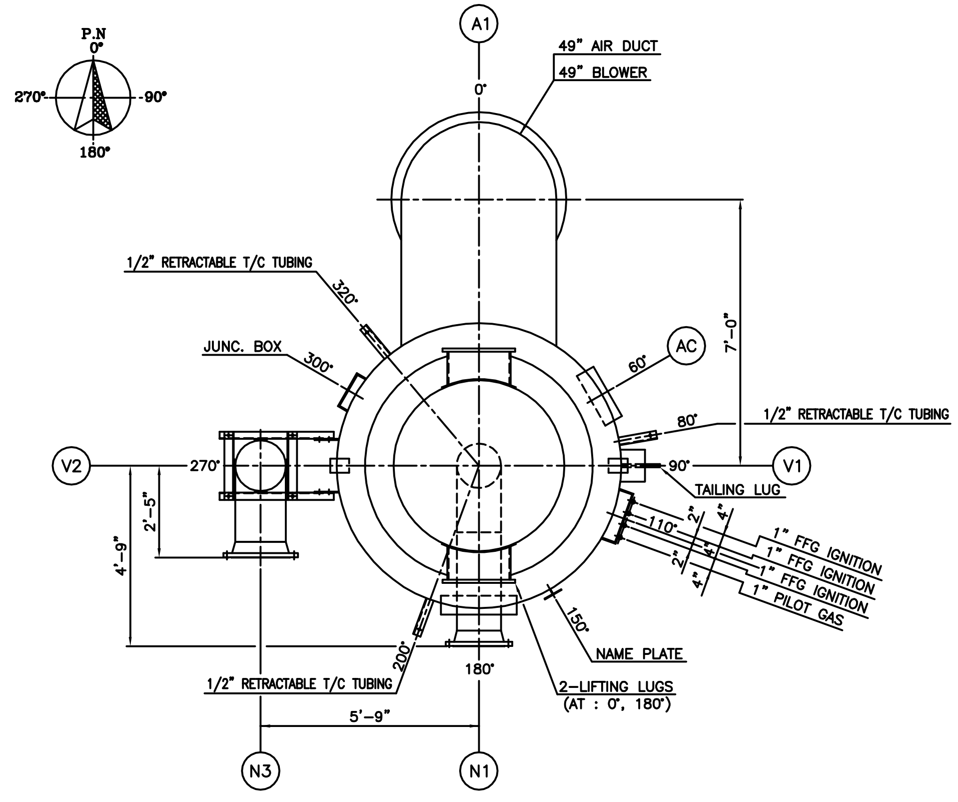
1a. PILOT MIXER ORIFICE DRILLED: 3/64"Ø [1.19 mm]
1b. MJ ARMS PURGE ORIFICE DRILLED: #50 MTD [1.78 MM]
2a. PILOT GAS CONSUMPTION LEAN FUEL: 61.36 SCFH @ 15 PSIG PER PILOT [1.64 Nm^3 /HR @ 1.05 kg/cm^2 g]
2b. PILOT GAS CONSUMPTION RICH FUEL: 53.49 SCFH @ 15 PSIG PER PILOT [1.43 NM^3 /HR @ 1.05 KG/CM^2 G]
3a. PILOT ORIFICE DRILLING LEAN FUEL BASED ON 879 BTU/SCF (LHV) [8269 $kcal/Nm^3$] GAS WITH 0.57 SP. GR.
3A. PILOT ORIFICE DRILLING RICH FUEL BASED ON 1158 BTU/SCF (LHV) [10893 $KCAL/NM^3$] GAS WITH 0.75 SP. GR.
4a. THE HP FLARE TIP REQUIRES A CONTINUOUS PURGE OF 190 SCFH [5.09 Nm^3 /HR] OR 143 SCFH [3.83 Nm^3 /HR] (N_2) OF A GAS THAT WILL NOT GO TO DEW POINT AT OPERATING TEMPERATURES. TO ENSURE AIR DOES NOT MIGRATE DOWN THE FLARE STACK. IT SHOULD BE NOTED THAT DEPENDING UPON THE TURNDOWN OPERATION OF THE FAN AND THE TYPE OF PURGE GAS USED IT MAY BE NECESSARY TO INCREASE THIS MINIMUM PURGE RATE TO ENSURE PROPER COMBUSTION OF THE PURGE GAS DURING IDLE OPERATION.
4b. THE LP FLARE TIP REQUIRES A CONTINUOUS PURGE OF 290 SCFH [7.77 Nm^3 /HR] OR 110 SCFH [2.95 Nm^3 /HR] (N_2) OF A GAS THAT WILL NOT GO TO DEW POINT AT OPERATING TEMPERATURES. TO ENSURE AIR DOES NOT MIGRATE DOWN THE FLARE STACK. IT SHOULD BE NOTED THAT DEPENDING UPON THE TURNDOWN OPERATION OF THE FAN AND THE TYPE OF PURGE GAS USED IT MAY BE NECESSARY TO INCREASE THIS MINIMUM PURGE RATE TO ENSURE PROPER COMBUSTION OF THE PURGE GAS DURING IDLE OPERATION.
△ 4c.
OF A GAS THAT WILL NOT GO TO DEW POINT AT OPERATING TEMPERATURES.
5. ALL FLANGE BOLTING TO STRADDLE NORMAL CENTERLINES, UNLESS NOTED OTHERWISE.
6. ALL TESTING PER INSPECTION TEST PLAN DOCUMENT NO. 38126-4010
7. THE PILOT THERMOCOUPLE IS FOR ON/OFF INDICATION ONLY, NOT FOR ACCURATE MEASUREMENT OF THE PILOT FLAME TEMPERATURE.
8. WHEN INSTALLING THE CENTER ASSEMBLY THE GAS EXIT ARMS MUST BE CENTERED ON THE PILOT AS PER THE PLAN VIEW.
9. APPROXIMATE WEIGHT FOR FLARE TIP ASS'Y: 5,755 LBS. [2610 Kg] △
10. APPROXIMATE WEIGHT FOR FOR EACH PILOT: 65 LBS. [29 Kg.]
11. ALL EXTERNAL CARBON STEEL SURFACES TO BE PREPARED PER SSPC-SP10.
PRIME: 1 COAT CARBOZINC 11 (2-3 MILS DFT MIN.)
PAINT: 1 COAT THERMALINE 4900 (1-2 MILS DFT MIN.)
FINISH COLOR: CARLSBAD CANYON 9265
12. MJ ARM GAS CONSUMPTION: 137 SCFH @ 15 PSIG PER ARM △ [3.67 NM^3 /HR @ 1.05 KG/CM^2 G]

JOBSITE: △ COWBOY CDP--EDDY COUNTY, NEW MEXICO
END USER: XTO ENERGY

S.O. NO.: 38126	P.O. NO.: 1802759--032	APP KNB	
ZEECO	AFTAMJ-14/54-16 FLARE TIP ASSEMBLY	DRAWN MKN	DATE 25FEB19
		CHK RLO	APP JSK
		SCALE NONE	REV 1
	FOR: AUDOBON	DRAWING NUMBER SD-8301 △ SHT. 1 OF 2	

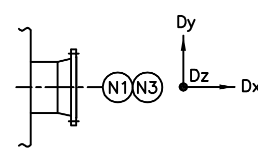


ELEVATION



PLAN LAYOUT

(SCALE : 1/30)

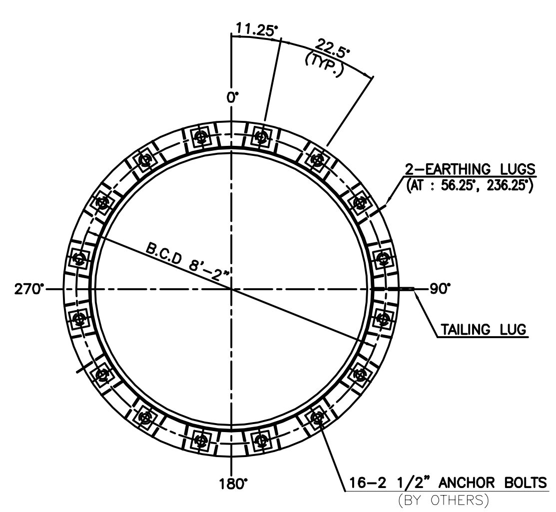


INLET DISPLACEMENT FOR "N1" LP NOZZLE

CASE	Dx (inch)	Dy (inch)	Dz (inch)
MIN. CONTRACTION	-0.03	-0.12	0.0
MAX. EXPANSION	0.02	0.08	0.0

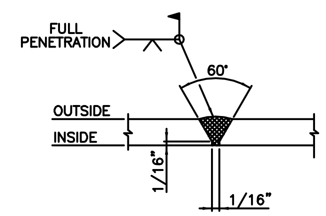
INLET DISPLACEMENT FOR "N3" HP NOZZLE

CASE	Dx (inch)	Dy (inch)	Dz (inch)
MIN. CONTRACTION	-0.02	-1.66	0.0
MAX. EXPANSION	0.01	2.44	0.0



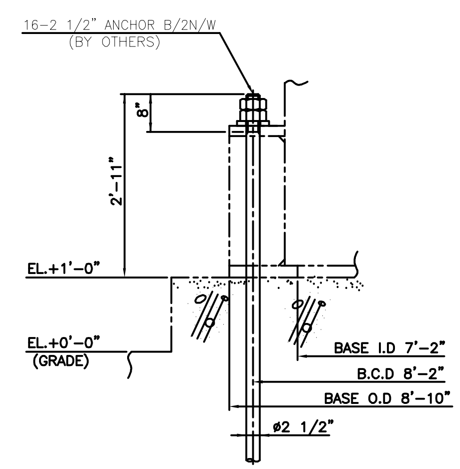
ANCHOR BOLT PLAN

(SCALE : 1/30)



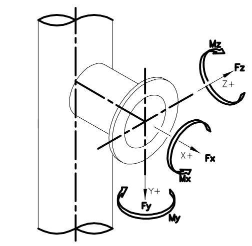
FIELD WELD DETAIL

(TYP.)
(SCALE : N/S)



ANCHOR BOLT

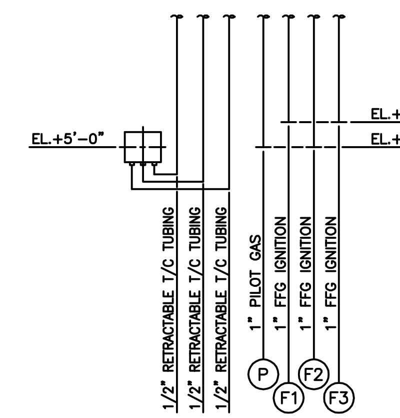
(FOR STACK RISER)



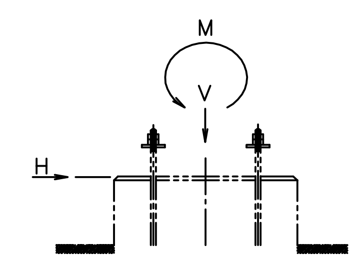
PIPE SIZE (IN)	Fx	Fy	Fz	Mx	My	Mz
	lb	lb	lb	lb-ft	lb-ft	lb-ft
14	450	750	750	1070	800	800
16	500	800	800	1140	850	850

MAX. ALLOWABLE INLET NOZZLE LOAD

(PER API 537)

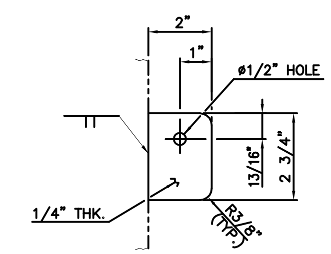


UTILITY PIPING DETAIL



LOADING DATA

(FOR STACK RISER)



EARTHING LUG

(AT : 56.25°, 236.25°)
(SCALE : 1/3)

LOADING DATA	V(kip)	H(kip)	M(kip-ft)
DEAD LOAD	86.0	0.0	0.0
WIND LOAD	0.0	55.8	4668.1
SEISMIC LOAD	2.8	1.9	224.7
NOZZLE LOAD	1.7	2.0	31.0

MATERIAL SPECIFICATIONS		DESIGN DATA	
AIR RISER	A36 OR EQ.	TYPE	SELF SUPPORTED
LP GAS RISER	A106-B OR EQ.	STRUCTURE CODE	ASME STS-1 / AISC
HP GAS RISER	A312-TP304	WIND DESIGN	ASCE 7-10/ V=120mph/ EXP.=C
BOTTOM PLATE	A36 OR EQ.	SEISMIC DESIGN	ASCE 7-10/ Ss=0.153/ S1=0.045/ I.F=1.25/ SITE CLASS=D
SKIRT	A36 OR EQ.	FLUID	FLARE GAS
FLARE TIP	SEE FLARE TIP DWG.	DESIGN PRESS.(HP/LP/AIR)	75 / 50 / ATM psig
AIR RISER FLANGE	A36 OR EQ.	DESIGN TEMP.(HP/LP/AIR)	-65~120/-10~120/-10~120 °F
LP RISER FLANGE	A105	OPERATING PRESS.(HP/LP/AIR)	66 / 1 / ATM psig
HP RISER FLANGE	A182-F304	OPERATING TEMP.(HP/LP/AIR)	-65~115/-5~115/-5~115 °F
RISER GASKET	C4401	AMBIENT TEMP (MIN./MAX.)	-5 ~ 115 °F
BASE PLATE	A36 OR EQ.	P.W.H.T.	NO
ANCHOR BOLT	F1554 GR. 36	NDE	AS PER ITP
EARTHING LUG	304 S.S	CORROSION ALLOWANCE (HP/LP/AIR)	0.0 / 1/16" / 1/16"
NAME PLATE	304 S.S	COATING	SEE NOTE 2
NAME PLATE BRACKET	A36 OR EQ.		
UTILITY LINE	A106-B		
TUBING LINE	316 S.S		
LIFTING LUG	A53-B/A36 OR EQ.		
TAILING LUG	A36 OR EQ.		

NOZZLE AND CONNECTIONS

MARK	Q'TY	SIZE	SCH.	RATING	FACING	FLG. MAT'L	MATERIAL NOZZLE	SERVICE	REMARKS
N1	1	14"	STD.	ASME #150	WN, RF	A105	A106-B OR EQ.	LP GAS INLET	
N2	1	14"	STD.	-	-	-	A106-B OR EQ.	LP GAS OUTLET	
N3	1	16"	SCH.10S	ASME #150	WN, RF	A182-F304	A403-WP304	HP GAS INLET	
N4	1	16"	SCH.10S	ASME #150	WN, RF	A182-F304	A312-TP304	HP GAS OUTLET	
A1	1	49"	3/8" THK.	PLATE FLANGE	-	A36 OR EQ.	A36 OR EQ.	AIR INLET	
A2	1	54"	3/8" THK.	PLATE FLANGE	-	A36 OR EQ.	A36 OR EQ.	AIR OUTLET	
V1,2	2	4"	STD.	-	-	-	A53-B ERW	VENT HOLE	
AC	1	20"	1/2" THK.	-	-	-	A36 OR EQ.	ACCESS HOLE	
P	1	1"	STD.	ASME #150	SW, RF	A105	A106-B	PILOT GAS	
F1~3	3	1"	STD.	ASME #150	SW, RF	A105	A106-B	FFG IGNITION	

NOTE

1. ALL FLANGE BOLTING TO STRADDLE CENTERLINES INDICATED BY CENTERLINE UNLESS NOTED OTHERWISE.
2. COATING SYSTEM (AS PER CHART 1, AUDUBON COATING SPEC.)
   - EXTERNAL CARBON STEEL FOR AIR RISER & UTILITY PIPING
     - SURFACE PREPARATION : SSPC-SP10
     - PRIMER : INORGANIC ZINC (DRY MILS 2~3)
     - BUILD : EPOXY (DRY MILS 4~6)
     - TOP : POLYURETHANE (DRY MILS 2~3)
     - TOP COAT COLOR : CARLSBAD CANYON 9265
3. ALL PIPING 2" & SMALLER AND ALL CONDUIT WILL BE SUPPLIED IN RANDOM LENGTH WITH LOOSE FITTING FOR FIELD ASSEMBLY.
4. LOADING DATA INCLUDES OVERAGE FACTOR OF 10% ABOVE CALCULATED LOADS.
5. FLARE STACK STRUCTURAL DESIGN ASSUMES ELASTIC FOUNDATION SUPPORT PER ASME STS-1.
6. ANCHOR BOLT ARE NOT BY ZEECO. (BY OTHERS)
7. CONCRETE COMPRESSIVE STRENGTH AT 28 DAYS , FC' = 4000 PSI.

APPROVED
(PROCEED AS IS) ✓
APPROVED AS NOTED ☐
(REVISE AND RESUBMIT)
REJECTED ☐
(DO NOT PROCEED, RESUBMIT)
FOR INFORMATION ONLY ☐

1802759-032-ME02-0001

REFERENCE DRAWING NO.	DESCRIPTION
SD-8264	CONDUIT DETAIL
SD-8263	PIPING DETAIL
SD-8262	PIPING ARRANGEMENT
SD-8261	RISER DETAIL
SD-8260	TEMPLATE DETAIL

PROJECT NAME: CRYO FLARE STACK
JOBSITE: CARLSBAD, NM.
END USER: XTO ENERGY
S.O. NO.: 38126
P.O. NO.: 1802759-032
APP KB

NO	DATE	REVISION DESCRIPTION	BY	CKD	APP.
2	13JUN19	REVISED AS MARKED	MGE	KWH	JK
1	19MAR19	REVISED AS MARKED	MGE	KWH	JK

ZEECO, INC.
22151 EAST 91st STREET
BROKEN ARROW, OK 74014
PHONE: (918) 258-8551
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www.zeeco.com
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SELF SUPPORTED
FLARE STACK SYSTEM
GENERAL ARRANGEMENT & LOADING DATA
(FS-6960)

FOR: AUDUBON ENGINEERING

DRAWN	DATE
MGE	15FEB19
CHK KWH	APP JK
SCALE 1/100	REV 2
DRAWING NUMBER SD-8259	SHT. 1 OF 1

Combustor(ECD1) Specs

• Burners
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General Process Performance Warranty for Flare System

Zeeco Inc. warrants the process performance of this unit will meet or exceed the contract requirements. Specific process performance requirements and acceptance criteria will be defined and mutually agreed to by both parties within two (2) months of receipt of the purchase order for supply of the equipment. Performance of the system is to be defined under normal ambient conditions of temperature, wind, etc. Such performance acceptance criteria in general to be as follows:

Based on provided Datasheet 019141001-AE-DS-ME0018 and Agreed Flow Rates:

1) Hydrocarbon Destruction efficiency of the unit will be 99% or higher when operated and maintained per the operating instructions and industry standards for this type of equipment.
2) The expected NOx and CO emissions will be 124 ppm and 204 ppm (corrected to 3% O2), +/- 10%, using calibrated measurement equipment under defined flow conditions at the specified gas composition in the contract and when operated and maintained per the operating instructions and industry standards for this type of equipment.. The specific operating temperature required to meet all three conditions will be determined upon field testing of the equipment.

Process performance of the system, if required, will be confirmed at a performance test to take place within 90 days after the unit is fully assembled and erected at site. The cost for Zeeco Inc. personnel to be on site for any testing is at the expense of the customer. The cost for testing equipment would also be to the account of the customer, if not readily available in the process system as installed. The specific conditions of the performance test, and the measurement and acceptance criteria for the above process performance points, including specific liability points associated with each process item, are to be mutually agreed to by both buyer and seller prior to shipment of the equipment. Successful completion of the process performance test at site will be deemed as compliance with the process performance warranty for any and all reasons. In the event the site performance test is postponed or delayed for more than 90 days after completion of erection of the unit at site, prior to the test, Zeeco Inc. will inspect the unit and any required refurbishment / repair to like new condition must be completed prior to testing, at purchaser's sole expense. If the testing is not completed within 6 months of the startup of the unit, the unit will have been deemed to have met any and all performance requirements.

Enclosed Flare Stack Specification Sheet

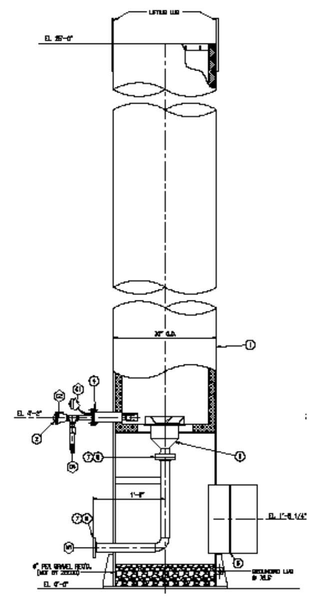
Client: Audobon Engineering	Zeeco Ref.: 2018-02438FL-01	Date:	22-May-18
Location: Carlsbad, NM	Client Ref.: 018193001-AE-RFQ	Rev.	1

General Information:

Tag No.:	EGF-1
Overall Height:	40 ft
Model No.	EF-9/40

Design Criteria:

Wind Design Code:	ASCE 7-10
Seismic Design Code:	ASCE 7-10
Importance Factor:	1.25
Structural Design Code:	AISC
Wind Speed (Structural):	120 mph
Seismic Zone:	0
Max. Design Temperature:	300 Deg. F
Min. Design Temperature:	20 Deg. F
Design Pressure:	Atmospheric
Stack Corrosion Allow.:	0.000 in.



(Typical drawing only)

Construction:

Stack Material:	Carbon Steel	Ladders & Step-offs:	None
Stack Height (approx.)	40 ft	Platform at tip:	None
Stack Width (approx.):	9 ft	Additional Platforms:	None
Flare Gas Inlet Diameter:	8 in		

Surface Preparation:	SSPC-SP-6	Primer:	Inorganic Zinc
		Finish Paint:	Per Specification

Utility piping:

Per Attached Utility Piping Scope of Supply

Miscellaneous Notes:

Generators (GEN1-4) Specs

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GAS ENGINE SITE SPECIFIC TECHNICAL DATA
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ENGINE SPEED (rpm):	1500
COMPRESSION RATIO:	12.1
AFTERCOOLER TYPE:	SCAC
AFTERCOOLER - STAGE 2 INLET (°F):	118
AFTERCOOLER - STAGE 1 INLET (°F):	192
JACKET WATER OUTLET (°F):	210
ASPIRATION:	TA
COOLING SYSTEM:	JW+OC+1AC, 2AC+GB
CONTROL SYSTEM:	ADEM4 W/ IM
EXHAUST MANIFOLD:	DRY
COMBUSTION:	LOW EMISSION
NOx EMISSION LEVEL (g/bhp-hr NOx):	0.5
SET POINT TIMING:	22

RATING STRATEGY:	HIGH ALTITUDE/AMBIENT
RATING LEVEL:	CONTINUOUS
FUEL SYSTEM:	CAT LOW PRESSURE WITH AIR FUEL RATIO CONTROL

SITE CONDITIONS:

FUEL:	Nat Gas
FUEL PRESSURE RANGE(psig): (See note 1)	2.0-5.0
FUEL METHANE NUMBER:	84.7
FUEL LHV (Btu/scf):	905
ALTITUDE(ft):	3400
INLET AIR TEMPERATURE(°F):	97
STANDARD RATED POWER:	3448 bhp@1500rpm
POWER FACTOR:	0.8
VOLTAGE(V):	4160-13800

				MAXIMUM RATING	SITE RATING AT MAXIMUM INLET AIR TEMPERATURE		
RATING		**NOTES**	**LOAD**	**100%**	**100%**	**75%**	**51%**
GENSET POWER	(WITH GEARBOX, WITHOUT FAN)	(2)(3)	ekW	2414	2377	1783	1213
GENSET POWER	(WITH GEARBOX, WITHOUT FAN)	(2)(3)	kVA	3018	2971	2228	1517
ENGINE POWER	(WITHOUT GEARBOX, WITHOUT FAN)	(3)	bhp	3372	3320	2497	1714
INLET AIR TEMPERATURE			°F	77	97	97	97
GENERATOR EFFICIENCY		(2)	%	96.8	96.8	96.5	95.7
GENSET EFFICIENCY	(ISO 3046/1)	(4)(5)	%	42.5	42.4	41.4	39.4
THERMAL EFFICIENCY		(4)(6)	%	41.9	42.0	43.7	46.3
TOTAL EFFICIENCY		(4)(7)	%	84.4	84.4	85.1	85.7
ENGINE DATA							
GENSET FUEL CONSUMPTION	(ISO 3046/1)	(8)	Btu/ekW-hr	8033	8043	8236	8665
GENSET FUEL CONSUMPTION	(NOMINAL)	(8)	Btu/ekW-hr	8310	8321	8520	8964
ENGINE FUEL CONSUMPTION	(NOMINAL)	(8)	Btu/bhp-hr	5950	5957	6083	6347
AIR FLOW (@inlet air temp, 14.7 psia)	(WET)	(9)	ft3/min	6523	6659	4959	3400
AIR FLOW	(WET)	(9)	lb/hr	28923	28467	21197	14532
FUEL FLOW (60ºF, 14.7 psia)			scfm	369	364	280	200
INLET MANIFOLD PRESSURE		(10)	in Hg(abs)	139.4	137.3	103.1	71.8
EXHAUST TEMPERATURE - ENGINE OUTLET		(11)	°F	736	740	800	902
EXHAUST GAS FLOW (@engine outlet temp, 14.5 psia)	(WET)	(12)	ft3/min	15617	15416	12074	8973
EXHAUST GAS MASS FLOW	(WET)	(12)	lb/hr	29935	29465	21963	15081
MAX INLET RESTRICTION		(13)	in H2O	14.08	13.81	9.78	7.25
MAX EXHAUST RESTRICTION		(13)	in H2O	19.31	18.79	10.67	5.25
EMISSIONS DATA - ENGINE OUT							
NOx (as NO2)		(14)(15)	g/bhp-hr	0.50	0.50	0.50	0.50
CO		(14)(15)	g/bhp-hr	1.88	1.88	1.73	1.58
THC (mol. wt. of 15.84)		(14)(15)	g/bhp-hr	3.23	3.23	3.10	2.81
NMHC (mol. wt. of 15.84)		(14)(15)	g/bhp-hr	0.48	0.48	0.47	0.42
NMNEHC (VOCs) (mol. wt. of 15.84)		(14)(15)(16)	g/bhp-hr	0.39	0.39	0.37	0.34
HCHO (Formaldehyde)		(14)(15)	g/bhp-hr	0.26	0.26	0.25	0.24
CO2		(14)(15)	g/bhp-hr	416	417	425	441
EXHAUST OXYGEN		(14)(17)	% DRY	9.9	9.9	9.6	9.1
HEAT REJECTION							
LHV INPUT		(18)	Btu/min	334354	329631	253148	181284
HEAT REJ. TO JACKET WATER (JW)		(19)	Btu/min	36555	36328	31335	25731
HEAT REJ. TO ATMOSPHERE	(INCLUDES GENERATOR)	(19)	Btu/min	9213	9115	7544	6296
HEAT REJ. TO LUBE OIL (OC)		(19)	Btu/min	10542	10480	9402	8143
HEAT REJECTION TO EXHAUST (LHV TO 248°F)		(19)	Btu/min	64185	63689	54198	43947
HEAT REJ. TO A/C - STAGE 1 (1AC)		(19)(21)	Btu/min	26561	25742	14223	5537
HEAT REJ. TO A/C - STAGE 2 (2AC)		(19)(21)	Btu/min	19716	19272	12737	7316
HEAT REJECTION FROM GEARBOX (GB)		(19)	Btu/min	1130	1112	836	574
PUMP POWER		(20)	Btu/min	859	859	859	859
COOLING SYSTEM SIZING CRITERIA							
TOTAL JACKET WATER CIRCUIT (JW+OC+1AC)		(22)	Btu/min	84554	87900		
TOTAL STAGE 2 AFTERCOOLER CIRCUIT (2AC+GB)		(22)	Btu/min	23609	25089		
HEAT REJECTION TO EXHAUST (LHV TO 248°F)		(22)	Btu/min	70603	70058		
A cooling system safety factor of 0% has been added to the cooling system sizing criteria.							
MINIMUM HEAT RECOVERY							
TOTAL JACKET WATER CIRCUIT (JW+OC+1AC)		(23)	Btu/min	66565	65534		
TOTAL STAGE 2 AFTERCOOLER CIRCUIT (2AC+GB)		(23)	Btu/min	19803	19365		
HEAT REJECTION TO EXHAUST(LHV TO 248°F)		(23)	Btu/min	54700	50042		

CONDITIONS AND DEFINITIONS

Engine rating obtained and presented in accordance with ISO 3046/1, adjusted for fuel, site altitude and site inlet air temperature. 100% rating at maximum inlet air temperature is the maximum engine capability for the specified fuel at site altitude and maximum site inlet air temperature. Maximum rating is the maximum capability at the specified aftercooler inlet temperature for the specified fuel at site altitude and reduced inlet air temperature. Lowest load point is the lowest continuous duty operating load allowed. No overload permitted at rating shown.

For notes information consult page three.

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Ref. Data Set EM0923-04-001, Printed 23Jan2019

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GAS ENGINE SITE SPECIFIC TECHNICAL DATA
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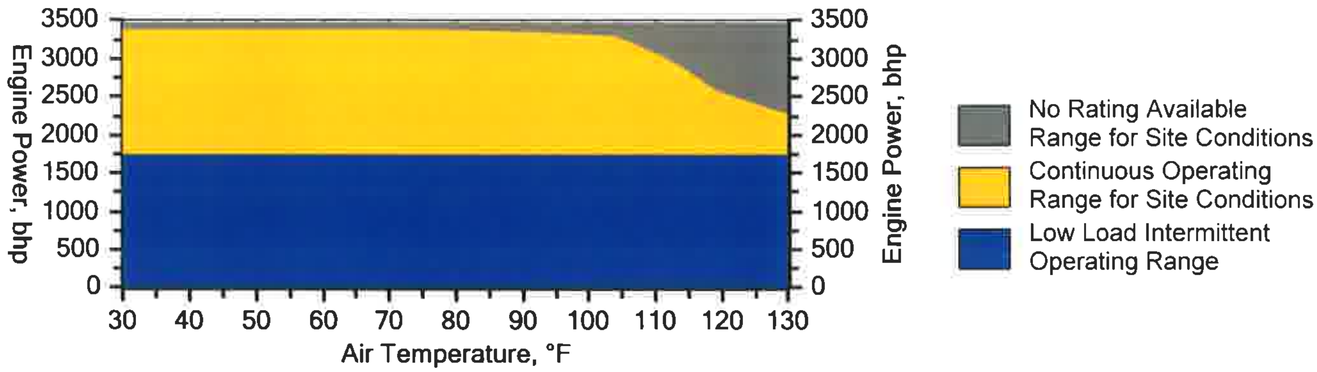
Engine Power vs. Inlet Air Temperature

Data represents temperature sweep at 3400 ft and 1500 rpm



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GENSET - WITHOUT RADIATOR

GAS ENGINE SITE SPECIFIC TECHNICAL DATA
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NOTES

1. Fuel pressure range specified is to the engine fuel control valve. Additional fuel train components should be considered in pressure and flow calculations

2. Generator efficiencies, power factor, and voltage are based on specified generator. [Genset Power (ekW) is calculated as: (Engine Power (bkW) - Gearbox Power (bkW)) x Generator Efficiency], [Genset Power (kVA) is calculated as: (Engine Power (bkW) - Gearbox Power (bkW)) x Generator Efficiency / Power Factor]

3. Rating is with two engine driven water pumps. Tolerance is (+)3, (-)0% of full load. All derates are applied without pumps , then pump power is subtracted to obtain final rating.

4. Efficiency represents a Closed Crankcase Ventilation (CCV) system installed on the engine

5. Genset Effieciency published in accordance with ISO 3046/1.

6. Thermal Efficiency is calculated based on energy recovery from the jacket water, lube oil, 1st stage aftercooler, and exhaust to 248ºF with engine operation at ISO 3046/1 Genset Efficiency, and assumes unburned fuel is converted in an oxidation catalyst.

7. Total efficiency is calculated as: Genset Efficiency + Thermal Efficiency. Tolerance is ±10% of full load data.

8. ISO 3046/1 Genset fuel consumption tolerance is (+)5, (-)0% at the specified power factor. Nominal genset and engine fuel consumption tolerance is ± 1.5% of full load data at the specified power factor.

9. Air flow value is on a 'wet' basis. Flow is a nominal value with a tolerance of ± 5 %.

10. Inlet manifold pressure is a nominal value with a tolerance of ± 5 %.

11. Exhaust temperature is a nominal value with a tolerance of (+)63°F, (-)54°F.

12. Exhaust flow value is on a "wet" basis. Flow is a nominal value with a tolerance of ± 6 %.

13. Inlet and Exhaust Restrictions are maximum allowed values at the corresponding loads. Increasing restrictions beyond what is specified will result in a significant engine derate.

14. Emissions data is at engine exhaust flange prior to any after treatment.

15. NOx tolerance's are ± 18% of specified value. All other emission values listed are higher than nominal levels to allow for instrumentation, measurement, and engine-to-engine variations. They indicate the maximum values expected under steady state conditions. Fuel methane number cannot vary more than ± 3. THC, NMHC, and NMNEHC do not include aldehydes

16. VOCs - Volatile organic compounds as defined in US EPA 40 CFR 60, subpart JJJJ

17. Exhaust Oxygen level is the result of adjusting the engine to operate at the specified NOx level. Tolerance is ± 0.5.

18. LHV rate tolerance is ± 1.5%.

19. Heat rejection values are representative of site conditions. Tolerances, based on treated water, are ± 10% for jacket water circuit, ± 50% for atmosphere, ± 20% for lube oil circuit, ± 10% for exhaust, ± 5% for aftercooler circuit, and ± 5% for Gearbox.

20. Pump power includes engine driven jacket water and aftercooler water pumps. Engine brake power includes effects of pump power.

21. Aftercooler heat rejection is nominal for site conditions and does not include an aftercooler heat rejection factor. Aftercooler heat rejection values at part load are for reference only.

22. Cooling system sizing criteria represent the expected maximum circuit heat rejection for the ratings at site, with applied plus tolerances. Total circuit heat rejection is calculated using formulas referenced in the notes on the standard tech data sheet with the following qualifications. Aftercooler heat rejection data (1AC & 2AC) is based on the standard rating. Jacket Water (JW), Oil Cooler (OC), and Gearbox (GB) heat rejection values are based on the respective site or maximum column. Aftercooler heat rejection factors (ACHRF) are specific for the site elevation and inlet air temperature specified in the site or maximum column, referenced from the table on the standard data sheet

23. Minimum heat recovery values represent the expected minimum heat recovery for the site, with applied minus tolerances. Do not use these values for cooling system sizing.

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Constituent	Abbrev	Mole %	Norm
Water Vapor	H2O	0.0000	0.0000
Methane	CH4	92.2700	92.2700
Ethane	C2H6	2.5000	2.5000
Propane	C3H8	0.5000	0.5000
Isobutane	iso-C4H1O	0.0000	0.0000
Norbutane	nor-C4H1O	0.2000	0.2000
Isopentane	iso-C5H12	0.0000	0.0000
Norpentane	nor-C5H12	0.1000	0.1000
Hexane	C6H14	0.0500	0.0500
Heptane	C7H16	0.0000	0.0000
Nitrogen	N2	3.4800	3.4800
Carbon Dioxide	CO2	0.9000	0.9000
Hydrogen Sulfide	H2S	0.0000	0.0000
Carbon Monoxide	CO	0.0000	0.0000
Hydrogen	H2	0.0000	0.0000
Oxygen	O2	0.0000	0.0000
Helium	HE	0.0000	0.0000
Neopentane	neo-C5H12	0.0000	0.0000
Octane	C8H18	0.0000	0.0000
Nonane	C9H20	0.0000	0.0000
Ethylene	C2H4	0.0000	0.0000
Propylene	C3H6	0.0000	0.0000
TOTAL (Volume %)		100.0000	100.0000

Fuel Makeup:	Nat Gas
Unit of Measure:	English

Calculated Fuel Properties

Caterpillar Methane Number:	84.7
Lower Heating Value (Btu/scf):	905
Higher Heating Value (Btu/scf):	1004
WOBBE Index (Btu/scf):	1168
THC: Free Inert Ratio:	21.83
Total % Inerts (% N2, CO2, He):	4.38%
RPC (%) (To 905 Btu/scf Fuel):	100%
Compressibility Factor:	0.998
Stoich A/F Ratio (Vol/Vol):	9.45
Stoich A/F Ratio (Mass/Mass):	15.75
Specific Gravity (Relative to Air):	0.600
Fuel Specific Heat Ratio (K):	1.313

CONDITIONS AND DEFINITIONS

Caterpillar Methane Number represents the knock resistance of a gaseous fuel It should be used with the Caterpillar Fuel Usage Guide for the engine and rating to determine the rating for the fuel specified A Fuel Usage Guide for each rating is included on page 2 of its standard technical data sheet.

RPC always applies to naturally aspirated (NA) engines, and turbocharged (TA or LE) engines only when they are derated for altitude and ambient site conditions.

Project specific technical data sheets generated by the Caterpillar Gas Engine Rating Pro program take the Caterpillar Methane Number and RPC into account when generating a site rating.

Fuel properties for Btu/scf calculations are at 60F and 14 696 psia

Caterpillar shall have no liability in law or equity, for damages, consequently or otherwise, arising from use of program and related material or any part thereof

FUEL LIQUIDS

Field gases, well head gases, and associated gases typically contain liquid water and heavy hydrocarbons entrained in the gas. To prevent detonation and severe damage to the engine, hydrocarbon liquids must not be allowed to enter the engine fuel system. To remove liquids, a liquid separator and coalescing filter are recommended, with an automatic drain and collection tank to prevent contamination of the ground in accordance with local codes and standards.

To avoid water condensation in the engine or fuel lines, limit the relative humidity of water in the fuel to 80% at the minimum fuel operating temperature.

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For flares subject to Chapter 115, Subchapter H, relating to highly reactive volatile organic compounds, flow rate and composition data required by 30 TAC 115.725–26 should be used to determine emissions for any portions of 2009 that HRVOC monitors were installed and operational.

In the absence of monitoring data, selection of the most accurate method may sometimes require exercising scientific judgment. For example, when using the results of a one-time performance test, the test conditions should be compared to the flare's actual operating conditions during the inventory year to determine whether the test accurately represents the flare's performance. If test conditions do not accurately model flare operation, then engineering determinations based on detailed process evaluation may provide the best data.

NO_x and CO Emissions

To calculate NO_x and CO emissions, the net heating value of the flared gas must be known. Using the actual short-term flared gas composition and flow rate data for the inventory year, calculate the net heating value of the flared gas and the total heat release for each short time period. Use these total heat release data, in conjunction with the appropriate emission factors from TCEQ Air Permits guidance, to determine NO_x and CO emissions for each time segment. Since the calculated net heating value of the gas and the assist gas type will determine the appropriate emission factors, carefully select the correct factors for each flare from Table A-6.

Calculate emissions using the most accurate data for the gas flow rate and composition available. (See "Flared Gas Flow Rate and Composition" earlier in this supplement for more information on preferred data.)

Table A-6. TCEQ Air Permits Flare Emission Factors

Contaminant	Assist Type	Waste Gas Stream Net Heating Value[a,b]	Emission Factor
NO_x	Steam	High Btu	0.0485 lb/MMBtu
		Low Btu	0.068 lb/MMBtu
	Air or Unassisted	High Btu	0.138 lb/MMBtu
		Low Btu	0.0641 lb/MMBtu
CO	Steam	High Btu	0.3503 lb/MMBtu
		Low Btu	0.3465 lb/MMBtu
	Air or Unassisted	High Btu	0.2755 lb/MMBtu
		Low Btu	0.5496 lb/MMBtu

[a] High Btu: > 1000 Btu/scf

[b] Low Btu: 192–1000 Btu/scf

TABLE 1.4-2. EMISSION FACTORS FOR CRITERIA POLLUTANTS AND GREENHOUSE GASES FROM NATURAL GAS COMBUSTION[a]

Pollutant	Emission Factor ($lb/10^6$ scf)	Emission Factor Rating
CO_2[b]	120,000	A
Lead	0.0005	D
N_2O (Uncontrolled)	2.2	E
N_2O (Controlled-low-NO_X burner)	0.64	E
PM (Total)[c]	7.6	D
PM (Condensable)[c]	5.7	D
PM (Filterable)[c]	1.9	B
SO_2[d]	0.6	A
TOC	11	B
Methane	2.3	B
VOC	5.5	C

[a] Reference 11. Units are in pounds of pollutant per million standard cubic feet of natural gas fired. Data are for all natural gas combustion sources. To convert from $lb/10^6$ scf to $kg/10^6$ m^3, multiply by 16. To convert from $lb/10^6$ scf to 1b/MMBtu, divide by 1,020. The emission factors in this table may be converted to other natural gas heating values by multiplying the given emission factor by the ratio of the specified heating value to this average heating value. TOC = Total Organic Compounds. VOC = Volatile Organic Compounds.

[b] Based on approximately 100% conversion of fuel carbon to CO_2. CO_2[$lb/10^6$ scf] = (3.67) (CON) (C)(D), where CON = fractional conversion of fuel carbon to CO_2, C = carbon content of fuel by weight (0.76), and D = density of fuel, $4.2x10^4$ $lb/10^6$ scf.

[c] All PM (total, condensible, and filterable) is assumed to be less than 1.0 micrometer in diameter. Therefore, the PM emission factors presented here may be used to estimate PM_{10}, $PM_{2.5}$ or PM_1 emissions. Total PM is the sum of the filterable PM and condensible PM. Condensible PM is the particulate matter collected using EPA Method 202 (or equivalent). Filterable PM is the particulate matter collected on, or prior to, the filter of an EPA Method 5 (or equivalent) sampling train.

[d] Based on 100% conversion of fuel sulfur to SO_2.
Assumes sulfur content is natural gas of 2,000 grains/10^6 scf. The SO_2 emission factor in this table can be converted to other natural gas sulfur contents by multiplying the SO_2 emission factor by the ratio of the site-specific sulfur content (grains/10^6 scf) to 2,000 grains/10^6 scf.

TABLE 1.4-3. EMISSION FACTORS FOR SPECIATED ORGANIC COMPOUNDS FROM NATURAL GAS COMBUSTION[a]

CAS No.	Pollutant	Emission Factor (lb/10^6 scf)	Emission Factor Rating
91-57-6	2-Methylnaphthalene[b, c]	2.4E-05	D
56-49-5	3-Methylchloranthrene[b, c]	<1.8E-06	E
	7,12-Dimethylbenz(a)anthracene[b,c]	<1.6E-05	E
83-32-9	Acenaphthene[b,c]	<1.8E-06	E
203-96-8	Acenaphthylene[b,c]	<1.8E-06	E
120-12-7	Anthracene[b,c]	<2.4E-06	E
56-55-3	Benz(a)anthracene[b,c]	<1.8E-06	E
71-43-2	Benzene[b]	2.1E-03	B
50-32-8	Benzo(a)pyrene[b,c]	<1.2E-06	E
205-99-2	Benzo(b)fluoranthene[b,c]	<1.8E-06	E
191-24-2	Benzo(g,h,i)perylene[b,c]	<1.2E-06	E
205-82-3	Benzo(k)fluoranthene[b,c]	<1.8E-06	E
106-97-8	Butane	2.1E+00	E
218-01-9	Chrysene[b,c]	<1.8E-06	E
53-70-3	Dibenzo(a,h)anthracene[b,c]	<1.2E-06	E
25321-22-6	Dichlorobenzene[b]	1.2E-03	E
74-84-0	Ethane	3.1E+00	E
206-44-0	Fluoranthene[b,c]	3.0E-06	E
86-73-7	Fluorene[b,c]	2.8E-06	E
50-00-0	Formaldehyde[b]	7.5E-02	B
110-54-3	Hexane[b]	1.8E+00	E
193-39-5	Indeno(1,2,3-cd)pyrene[b,c]	<1.8E-06	E
91-20-3	Naphthalene[b]	6.1E-04	E
109-66-0	Pentane	2.6E+00	E
85-01-8	Phenanathrene[b,c]	1.7E-05	D

TABLE 1.4-3. EMISSION FACTORS FOR SPECIATED ORGANIC COMPOUNDS FROM NATURAL GAS COMBUSTION (Continued)

CAS No.	Pollutant	Emission Factor ($lb/10^6$ scf)	Emission Factor Rating
74-98-6	Propane	1.6E+00	E
129-00-0	Pyrene[b, c]	5.0E-06	E
108-88-3	Toluene[b]	3.4E-03	C

[a] Reference 11. Units are in pounds of pollutant per million standard cubic feet of natural gas fired. Data are for all natural gas combustion sources. To convert from $lb/10^6$ scf to $kg/10^6$ m^3, multiply by 16. To convert from $1b/10^6$ scf to lb/MMBtu, divide by 1,020. Emission Factors preceeded with a less-than symbol are based on method detection limits.

[b] Hazardous Air Pollutant (HAP) as defined by Section 112(b) of the Clean Air Act.

[c] HAP because it is Polycyclic Organic Matter (POM). POM is a HAP as defined by Section 112(b) of the Clean Air Act.

[d] The sum of individual organic compounds may exceed the VOC and TOC emission factors due to differences in test methods and the availability of test data for each pollutant.

TABLE 1.4-4. EMISSION FACTORS FOR METALS FROM NATURAL GAS COMBUSTION[a]

CAS No.	Pollutant	Emission Factor (lb/10^6 scf)	Emission Factor Rating
7440-38-2	Arsenic[b]	2.0E-04	E
7440-39-3	Barium	4.4E-03	D
7440-41-7	Beryllium[b]	<1.2E-05	E
7440-43-9	Cadmium[b]	1.1E-03	D
7440-47-3	Chromium[b]	1.4E-03	D
7440-48-4	Cobalt[b]	8.4E-05	D
7440-50-8	Copper	8.5E-04	C
7439-96-5	Manganese[b]	3.8E-04	D
7439-97-6	Mercury[b]	2.6E-04	D
7439-98-7	Molybdenum	1.1E-03	D
7440-02-0	Nickel[b]	2.1E-03	C
7782-49-2	Selenium[b]	<2.4E-05	E
7440-62-2	Vanadium	2.3E-03	D
7440-66-6	Zinc	2.9E-02	E

[a] Reference 11. Units are in pounds of pollutant per million standard cubic feet of natural gas fired. Data are for all natural gas combustion sources. Emission factors preceeded by a less-than symbol are based on method detection limits. To convert from lb/10^6 scf to kg/10^6 m^3, multiply by l6. To convert from lb/10^6 scf to 1b/MMBtu, divide by 1,020.

[b] Hazardous Air Pollutant as defined by Section 112(b) of the Clean Air Act.

Table 3.1-3. EMISSION FACTORS FOR HAZARDOUS AIR POLLUTANTS FROM NATURAL GAS-FIRED STATIONARY GAS TURBINES[a]

Emission Factors[b] - Uncontrolled		
Pollutant	Emission Factor (lb/MMBtu)[c]	Emission Factor Rating
1,3-Butadiene[d]	< 4.3 E-07	D
Acetaldehyde	4.0 E-05	C
Acrolein	6.4 E-06	C
Benzene[e]	1.2 E-05	A
Ethylbenzene	3.2 E-05	C
Formaldehyde[f]	7.1 E-04	A
Naphthalene	1.3 E-06	C
PAH	2.2 E-06	C
Propylene Oxide[d]	< 2.9 E-05	D
Toluene	1.3 E-04	C
Xylenes	6.4 E-05	C

[a] SCC for natural gas-fired turbines include 2-01-002-01, 2-02-002-01, 2-02-002-03, 2-03-002-02, and 2-03-002-03. Hazardous Air Pollutants as defined in Section 112 (b) of the *Clean Air Act*.

[b] Factors are derived from units operating at high loads (≥ 80 percent load) only. For information on units operating at other loads, consult the background report for this chapter (Reference 16), available at "www.epa.gov/ttn/chief".

[c] Emission factors based on an average natural gas heating value (HHV) of 1020 Btu/scf at 60^{o}F. To convert from (lb/MMBtu) to (lb/10^6 scf), multiply by 1020. These emission factors can be converted to other natural gas heating values by multiplying the given emission factor by the ratio of the specified heating value to this heating value.

[d] Compound was not detected. The presented emission value is based on one-half of the detection limit.

[e] Benzene with SCONOX catalyst is 9.1 E-07, rating of D.

[f] Formaldehyde with SCONOX catalyst is 2.0 E-05, rating of D.

loading operation, resulting in high levels of vapor generation and loss. If the turbulence is great enough, liquid droplets will be entrained in the vented vapors.

A second method of loading is submerged loading. Two types are the submerged fill pipe method and the bottom loading method. In the submerged fill pipe method, the fill pipe extends almost to the bottom of the cargo tank. In the bottom loading method, a permanent fill pipe is attached to the cargo tank bottom. During most of submerged loading by both methods, the fill pipe opening is below the liquid surface level. Liquid turbulence is controlled significantly during submerged loading, resulting in much lower vapor generation than encountered during splash loading.

The recent loading history of a cargo carrier is just as important a factor in loading losses as the method of loading. If the carrier has carried a nonvolatile liquid such as fuel oil, or has just been cleaned, it will contain vapor-free air. If it has just carried gasoline and has not been vented, the air in the carrier tank will contain volatile organic vapors, which will be expelled during the loading operation along with newly generated vapors.

Cargo carriers are sometimes designated to transport only one product, and in such cases are practicing "dedicated service". Dedicated gasoline cargo tanks return to a loading terminal containing air fully or partially saturated with vapor from the previous load. Cargo tanks may also be "switch loaded" with various products, so that a nonvolatile product being loaded may expel the vapors remaining from a previous load of a volatile product such as gasoline. These circumstances vary with the type of cargo tank and with the ownership of the carrier, the petroleum liquids being transported, geographic location, and season of the year.

One control measure for vapors displaced during liquid loading is called "vapor balance service", in which the cargo tank retrieves the vapors displaced during product unloading at bulk plants or service stations and transports the vapors back to the loading terminal. Figure 5.2-5 shows a tank truck in vapor balance service filling a service station underground tank and taking on displaced gasoline vapors for return to the terminal. A cargo tank returning to a bulk terminal in vapor balance service normally is saturated with organic vapors, and the presence of these vapors at the start of submerged loading of the tanker truck results in greater loading losses than encountered during nonvapor balance, or "normal", service. Vapor balance service is usually not practiced with marine vessels, although some vessels practice emission control by means of vapor transfer within their own cargo tanks during ballasting operations, discussed below.

Emissions from loading petroleum liquid can be estimated (with a probable error of ±30 percent)[4] using the following expression:

$$L_L = 12.46 \frac{SPM}{T} \qquad (1)$$

where:

L_L = loading loss, pounds per 1000 gallons (lb/10^3 gal) of liquid loaded

S = a saturation factor (see Table 5.2-1)
P = true vapor pressure of liquid loaded, pounds per square inch absolute (psia) (see Section 7.1, "Organic Liquid Storage Tanks")
M = molecular weight of vapors, pounds per pound-mole (lb/lb-mole) (see Section 7.1, "Organic Liquid Storage Tanks")
T = temperature of bulk liquid loaded, °R (°F + 460)

Table 3.2-2. UNCONTROLLED EMISSION FACTORS FOR 4-STROKE LEAN-BURN ENGINES[a]
(SCC 2-02-002-54)

Pollutant	Emission Factor (lb/MMBtu)[b] (fuel input)	Emission Factor Rating
Criteria Pollutants and Greenhouse Gases		
NO_x[c] 90 - 105% Load	4.08 E+00	B
NO_x[c] <90% Load	8.47 E-01	B
CO[c] 90 - 105% Load	3.17 E-01	C
CO[c] <90% Load	5.57 E-01	B
CO_2[d]	1.10 E+02	A
SO_2[e]	5.88 E-04	A
TOC[f]	1.47 E+00	A
Methane[g]	1.25 E+00	C
VOC[h]	1.18 E-01	C
PM10 (filterable)[i]	7.71 E-05	D
PM2.5 (filterable)[i]	7.71 E-05	D
PM Condensable[j]	9.91 E-03	D
Trace Organic Compounds		
1,1,2,2-Tetrachloroethane[k]	<4.00 E-05	E
1,1,2-Trichloroethane[k]	<3.18 E-05	E
1,1-Dichloroethane	<2.36 E-05	E
1,2,3-Trimethylbenzene	2.30 E-05	D
1,2,4-Trimethylbenzene	1.43 E-05	C
1,2-Dichloroethane	<2.36 E-05	E
1,2-Dichloropropane	<2.69 E-05	E
1,3,5-Trimethylbenzene	3.38 E-05	D
1,3-Butadiene[k]	2.67E-04	D
1,3-Dichloropropene[k]	<2.64 E-05	E
2-Methylnaphthalene[k]	3.32 E-05	C
2,2,4-Trimethylpentane[k]	2.50 E-04	C
Acenaphthene[k]	1.25 E-06	C

Table 3.2-2. UNCONTROLLED EMISSION FACTORS FOR 4-STROKE LEAN-BURN ENGINES (Continued)

Pollutant	Emission Factor (lb/MMBtu)[b] (fuel input)	Emission Factor Rating
Acenaphthylene[k]	5.53 E-06	C
Acetaldehyde[k,l]	8.36 E-03	A
Acrolein[k,l]	5.14 E-03	A
Benzene[k]	4.40 E-04	A
Benzo(b)fluoranthene[k]	1.66 E-07	D
Benzo(e)pyrene[k]	4.15 E-07	D
Benzo(g,h,i)perylene[k]	4.14 E-07	D
Biphenyl[k]	2.12 E-04	D
Butane	5.41 E-04	D
Butyr/Isobutyraldehyde	1.01 E-04	C
Carbon Tetrachloride[k]	<3.67 E-05	E
Chlorobenzene[k]	<3.04 E-05	E
Chloroethane	1.87 E-06	D
Chloroform[k]	<2.85 E-05	E
Chrysene[k]	6.93 E-07	C
Cyclopentane	2.27 E-04	C
Ethane	1.05 E-01	C
Ethylbenzene[k]	3.97 E-05	B
Ethylene Dibromide[k]	<4.43 E-05	E
Fluoranthene[k]	1.11 E-06	C
Fluorene[k]	5.67 E-06	C
Formaldehyde[k,l]	5.28 E-02	A
Methanol[k]	2.50 E-03	B
Methylcyclohexane	1.23 E-03	C
Methylene Chloride[k]	2.00 E-05	C
n-Hexane[k]	1.11 E-03	C
n-Nonane	1.10 E-04	C

Table 3.2-2. UNCONTROLLED EMISSION FACTORS FOR 4-STROKE LEAN-BURN ENGINES
(Continued)

Pollutant	Emission Factor (lb/MMBtu)[b] (fuel input)	Emission Factor Rating
n-Octane	3.51 E-04	C
n-Pentane	2.60 E-03	C
Naphthalene[k]	7.44 E-05	C
PAH[k]	2.69 E-05	D
Phenanthrene[k]	1.04 E-05	D
Phenol[k]	2.40 E-05	D
Propane	4.19 E-02	C
Pyrene[k]	1.36 E-06	C
Styrene[k]	<2.36 E-05	E
Tetrachloroethane[k]	2.48 E-06	D
Toluene[k]	4.08 E-04	B
Vinyl Chloride[k]	1.49 E-05	C
Xylene[k]	1.84 E-04	B

[a] Reference 7. Factors represent uncontrolled levels. For NO_x, CO, and PM10, "uncontrolled" means no combustion or add-on controls; however, the factor may include turbocharged units. For all other pollutants, "uncontrolled" means no oxidation control; the data set may include units with control techniques used for NOx control, such as PCC and SCR for lean burn engines, and PSC for rich burn engines. Factors are based on large population of engines. Factors are for engines at all loads, except as indicated. SCC = Source Classification Code. TOC = Total Organic Compounds. PM-10 = Particulate Matter $\leq$ 10 microns (μm) aerodynamic diameter. A "<" sign in front of a factor means that the corresponding emission factor is based on one-half of the method detection limit.

[b] Emission factors were calculated in units of (lb/MMBtu) based on procedures in EPA Method 19. To convert from (lb/MMBtu) to (lb/10^6 scf), multiply by the heat content of the fuel. If the heat content is not available, use 1020 Btu/scf. To convert from (lb/MMBtu) to (lb/hp-hr) use the following equation:

$$\text{lb/hp-hr} = (\text{lb/MMBtu})\ (\text{heat input, MMBtu/hr})\ (\text{1/operating HP, 1/hp})$$

[c] Emission tests with unreported load conditions were not included in the data set.

[d] Based on 99.5% conversion of the fuel carbon to CO_2. CO_2 [lb/MMBtu] = (3.67)(%CON)(C)(D)(1/h), where %CON = percent conversion of fuel carbon to CO_2, C = carbon content of fuel by weight (0.75), D = density of fuel, 4.1 E+04 lb/10^6 scf, and

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Title 40: Protection of Environment
PART 98—MANDATORY GREENHOUSE GAS REPORTING
Subpart C—General Stationary Fuel Combustion Sources

TABLE C-1 TO SUBPART C OF PART 98—DEFAULT CO_2 EMISSION FACTORS AND HIGH HEAT VALUES FOR VARIOUS TYPES OF FUEL

Link to an amendment published at 81 FR 89252, Dec. 9, 2016.

DEFAULT CO_2 EMISSION FACTORS AND HIGH HEAT VALUES FOR VARIOUS TYPES OF FUEL

Fuel type	Default high heat value	Default CO_2 emission factor
Coal and coke	mmBtu/short ton	kg CO_2/mmBtu
Anthracite	25.09	103.69
Bituminous	24.93	93.28
Subbituminous	17.25	97.17
Lignite	14.21	97.72
Coal Coke	24.80	113.67
Mixed (Commercial sector)	21.39	94.27
Mixed (Industrial coking)	26.28	93.90
Mixed (Industrial sector)	22.35	94.67
Mixed (Electric Power sector)	19.73	95.52
Natural gas	mmBtu/scf	kg CO_2/mmBtu
(Weighted U.S. Average)	1.026×10^{-3}	53.06
Petroleum products	mmBtu/gallon	kg CO_2/mmBtu
Distillate Fuel Oil No. 1	0.139	73.25
Distillate Fuel Oil No. 2	0.138	73.96
Distillate Fuel Oil No. 4	0.146	75.04
Residual Fuel Oil No. 5	0.140	72.93
Residual Fuel Oil No. 6	0.150	75.10
Used Oil	0.138	74.00
Kerosene	0.135	75.20
Liquefied petroleum gases (LPG)[1]	0.092	61.71
Propane[1]	0.091	62.87
Propylene[2]	0.091	67.77
Ethane[1]	0.068	59.60
Ethanol	0.084	68.44
Ethylene[2]	0.058	65.96
Isobutane[1]	0.099	64.94
Isobutylene[1]	0.103	68.86
Butane[1]	0.103	64.77
Butylene[1]	0.105	68.72
Naphtha (<401 deg F)	0.125	68.02
Natural Gasoline	0.110	66.88
Other Oil (>401 deg F)	0.139	76.22
Pentanes Plus	0.110	70.02
Petrochemical Feedstocks	0.125	71.02
Petroleum Coke	0.143	102.41
Special Naphtha	0.125	72.34
Unfinished Oils	0.139	74.54
Heavy Gas Oils	0.148	74.92
Lubricants	0.144	74.27
Motor Gasoline	0.125	70.22
Aviation Gasoline	0.120	69.25
Kerosene-Type Jet Fuel	0.135	72.22
Asphalt and Road Oil	0.158	75.36
Crude Oil	0.138	74.54
Other fuels—solid	mmBtu/short ton	kg CO_2/mmBtu
Municipal Solid Waste	9.95[3]	90.7
Tires	28.00	85.97
Plastics	38.00	75.00

Petroleum Coke	30.00	102.41
Other fuels—gaseous	mmBtu/scf	kg CO_2/mmBtu
Blast Furnace Gas	0.092×10^{-3}	274.32
Coke Oven Gas	0.599×10^{-3}	46.85
Propane Gas	2.516×10^{-3}	61.46
Fuel Gas[4]	1.388×10^{-3}	59.00
Biomass fuels—solid	mmBtu/short ton	kg CO_2/mmBtu
Wood and Wood Residuals (dry basis)[5]	17.48	93.80
Agricultural Byproducts	8.25	118.17
Peat	8.00	111.84
Solid Byproducts	10.39	105.51
Biomass fuels—gaseous	mmBtu/scf	kg CO_2/mmBtu
Landfill Gas	0.485×10^{-3}	52.07
Other Biomass Gases	0.655×10^{-3}	52.07
Biomass Fuels—Liquid	mmBtu/gallon	kg CO_2/mmBtu
Ethanol	0.084	68.44
Biodiesel (100%)	0.128	73.84
Rendered Animal Fat	0.125	71.06
Vegetable Oil	0.120	81.55

[1]The HHV for components of LPG determined at 60 °F and saturation pressure with the exception of ethylene.

[2]Ethylene HHV determined at 41 °F (5 °C) and saturation pressure.

[3]Use of this default HHV is allowed only for: (a) Units that combust MSW, do not generate steam, and are allowed to use Tier 1; (b) units that derive no more than 10 percent of their annual heat input from MSW and/or tires; and (c) small batch incinerators that combust no more than 1,000 tons of MSW per year.

[4]Reporters subject to subpart X of this part that are complying with §98.243(d) or subpart Y of this part may only use the default HHV and the default CO_2 emission factor for fuel gas combustion under the conditions prescribed in §98.243(d)(2)(i) and (d)(2)(ii) and §98.252(a)(1) and (a)(2), respectively. Otherwise, reporters subject to subpart X or subpart Y shall use either Tier 3 (Equation C-5) or Tier 4.

[5]Use the following formula to calculate a wet basis HHV for use in Equation C-1: $HHV_w = ((100 - M)/100)*HHV_d$ where HHV_w = wet basis HHV, M = moisture content (percent) and HHV_d = dry basis HHV from Table C-1.

[78 FR 71950, Nov. 29, 2013]

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Title 40: Protection of Environment
PART 98—MANDATORY GREENHOUSE GAS REPORTING
Subpart C—General Stationary Fuel Combustion Sources

TABLE C-2 TO SUBPART C OF PART 98—DEFAULT CH_4 AND N_2O EMISSION FACTORS FOR VARIOUS TYPES OF FUEL

Link to an amendment published at 81 FR 89252, Dec. 9, 2016.

Fuel type	Default CH_4 emission factor (kg CH_4/mmBtu)	Default N_2O emission factor (kg N_2O/mmBtu)
Coal and Coke (All fuel types in Table C-1)	1.1×10^{-02}	1.6×10^{-03}
Natural Gas	1.0×10^{-03}	1.0×10^{-04}
Petroleum (All fuel types in Table C-1)	3.0×10^{-03}	6.0×10^{-04}
Fuel Gas	3.0×10^{-03}	6.0×10^{-04}
Municipal Solid Waste	3.2×10^{-02}	4.2×10^{-03}
Tires	3.2×10^{-02}	4.2×10^{-03}
Blast Furnace Gas	2.2×10^{-05}	1.0×10^{-04}
Coke Oven Gas	4.8×10^{-04}	1.0×10^{-04}
Biomass Fuels—Solid (All fuel types in Table C-1, except wood and wood residuals)	3.2×10^{-02}	4.2×10^{-03}
Wood and wood residuals	7.2×10^{-03}	3.6×10^{-03}
Biomass Fuels—Gaseous (All fuel types in Table C-1)	3.2×10^{-03}	6.3×10^{-04}
Biomass Fuels—Liquid (All fuel types in Table C-1)	1.1×10^{-03}	1.1×10^{-04}

Note: Those employing this table are assumed to fall under the IPCC definitions of the “Energy Industry” or “Manufacturing Industries and Construction”. In all fuels except for coal the values for these two categories are identical. For coal combustion, those who fall within the IPCC “Energy Industry” category may employ a value of 1g of CH_4/mmBtu.

[78 FR 71952, Nov. 29, 2013]

Table II: Facility/Compound Specific Fugitive Emission Factors

Equipment/Service	Compound Specific See Section I for more information			Facility Specific[1]					
	Ethylene Oxide[2] w/LDAR	Phosgene[3] w/LDAR	Butadiene w/LDAR[4]	Petroleum Marketing Terminal[5, 6] w/28PET	Oil and Gas ProductionOperation[6]				Refinery[6]
					Gas	Heavy Oil < 20 API	Light Oil	Water/ Light Oil	
Valves					0.00992	0.0000185	0.0055	0.000216	
Gas/Vapor	0.000444	0.00000216	0.001105	0.0000287					0.059
Light Liquid	0.00055	0.00000199	0.00314	0.0000948					0.024
Heavy Liquid				0.0000948					0.00051
Pumps	0.042651	0.0000201	0.05634		0.00529	0.00113[7]	0.02866	0.000052	
Light Liquid				0.00119					0.251
Heavy Liquid				0.00119					0.046
Flanges/Connectors[11]	0.000555	0.00000011	0.000307		0.00086	0.00000086	0.000243	0.000006	0.00055
					0.00044	0.0000165	0.000463	0.000243	
Gas/Vapor				0.000092604					
Light Liquid				0.00001762					
Heavy Liquid				0.0000176					
Compressors	0.000767		0.000004		0.0194	0.0000683	0.0165	0.0309	1.399
Relief Valve	0.000165	0.0000162	0.02996		0.0194	0.0000683	0.0165	0.0309	0.35
Open-ended Lines[8]	0.001078	0.00000007	0.00012		0.00441	0.000309	0.00309	0.00055	0.0051
Sampling[9]	0.000088		0.00012						0.033
Other[10]					0.0194	0.0000683	0.0165	0.0309	
Gas/Vapor				0.000265					
Light/Heavy Liquid				0.000287					
Process Drains					0.0194	0.0000683	0.0165	0.0309	0.07

Endnotes Table II

1 **Factors give the total organic compound emission rate. Multiply by the weight percent of non-methane, non-ethane organics to get the VOC emission rate.**

2 **These emission factors require the use of the 28MID fugitive program. Monitoring must occur at a leak definition of 500 ppmv. No additional control credit can be applied to these factors except 28CNTQ and 28CNTA. Emission factors are from EOIC Fugitive Emission Study, summer 1988.**

3 **These emission factors require the use of the 28MID fugitive program. Monitoring must occur at a leak definition of 50 ppmv. No additional control credit can be applied to these factors. Emission factors are from Phosgene Panel Study, summer 1988.**

4 **These emission factors require the use of the 28MID fugitive program. Monitoring must occur at a leak definition of 100 ppmv. No additional control credit can be applied to these factors. Emission factors are from Randall, J. L., et al., Radian Corporation. Fugitive Emissions from the 1,3-butadiene Production Industry: A Field Study. Final Report. Prepared for the 1,3-Butadiene Panel for the Chemical Manufacturers Association. April 1989.**

5 **Control credit is included in the factor; no additional control credit can be applied to these factors. Monthly 28 PET inspection is required.**

6 **Factors are taken from EPA Document EPA-453/R-95-017, November 1995, pages 2-13, 2-14, and 2-15.**

7 **Heavy liquid oil – Pump factor was not derived during the API study. The factor is the SOCMI without C_2 Heavy Liquid – Pump factor with a 93% reduction credit for the physical inspection.**

Table III: Leak Detection and Repair (LDAR) Program Instrument Monitoring Options

LDAR Program	28M	28RCT	28VHP	28MID	28LAER	28CNTQ	28CNTA
Leak Definition for Pumps and Compressors	10,000 ppmv	10,000 ppmv	2,000 ppmv	500 ppmv	500 ppmv	N/A	N/A
Leak Definition for All Other Components	10,000 ppmv	500 ppmv	500 ppmv	500 ppmv	500 ppmv	500 ppmv	500 ppmv
Applicable Vapor Pressure	>0.5 psia at 100°F	>0.044 psia at 68°F	>0.044 psia at 68°F	>0.044 psia at 68°F	>0.044 psia at 68°F	>0.044 psia at 68°F	>0.044 psia at 68°F
Monitoring Frequency	Quarterly	Quarterly	Quarterly	Quarterly	Quarterly	Quarterly	Annually
Directed/Nondirected Maintenance	Nondirected	Nondirected	Nondirected	Directed	Directed	Nondirected	Nondirected
Most Common State/Federal Programs with Similar Requirements	40 CFR Part 60 Subpart VV 40 CFR Part 61 30 TAC §115.322	30 TAC §115.352[1]	40 CFR Part 60 Subpart VVa 40 CFR Part 63 Subparts H, CC	N/A	Nonattainment NSR	N/A	40 CFR Part 60Subpart VVa, 40 CFR Part 63 Subparts H, CC

Endnotes Table III

[1] **Except in Gregg, Nueces, and Victoria Counties where 28M applies.**

Table V: Control Efficiencies for LDAR

Equipment/Service	28M	28RCT	28VHP	28MID	28LAER	28CNTQ	28CNTA	28PI	28AVO[9]
Valves[1]									97%
Gas/Vapor	75%	97%	97%	97%	97%			30%	
Light Liquid	75%	97%	97%	97%	97%			30%	
Heavy Liquid[5]	0%[6]	0%[6]	0%[6]	0%[6]	30%[6, 8]			30%[8]	
Pumps[1]									93%
Light Liquid	75%	75%	85%	93%	93%			30%	
Heavy Liquid[5]	0%	0%[7]	0%[7]	0%[8, 10]	30%[8]			30%[8]	
Flanges/Connectors[1]	30%	30%	30%	30%				30%	97%
Gas/Vapor					97%	97%	75%		
Light Liquid					97%	97%	75%		
Heavy Liquid[8]					30%	30%	30%		
Compressors[1]	75%	75%	85%	95%	95%			30%	95%
Relief Valves[1, 2] (Gas/Vapor)	75%	97%	97%	97%	97%			30%	97%
Sampling Connection[3] (pounds per hour per sample taken)	0%	0%	0%	0%	0%			0%	0%
Open Ended Lines[1, 4]									

It should be noted in the application and added to the permit conditions if any of the footnotes are applicable. For example, if components in heavy liquid service are monitored, then the application should include the monitored concentration and the concentration of saturation, in ppmv and such monitoring will be added as a separate condition.

Endnotes Table V

1 **Control efficiencies apply only to components that are actually monitored. Control efficiencies do not apply to components that are difficult or unsafe-to-monitor on the standard schedule. However, difficult-to-monitor gas or light liquid valves under the 28RCT, 28VHP, 28MID, or 28LAER programs that are monitored once per year may apply a 75% reduction credit.**

2 **100% control may be taken if a relief valve vents to an operating control device or if it is equipped with a rupture disc and a pressure-sensing device between the valve and disc to monitor for disc integrity. For new facilities, BACT guidelines generally require that all relief valves vent to a control device. When there are safety reasons that the relief valve cannot achieve 100% control, the relief valve can be monitored under the LDAR programs for the credit listed. This monitoring must be performed regardless of whether the relief valve is considered accessible, difficult-to-monitor or unsafe-to-monitor. Relief valves that do not achieve 100% control should not be built in locations that are unsafe-to-monitor.**

3 **Sampling connection control efficiencies are covered under other equipment and services. Sampling emissions are based on the number of samples taken per year as opposed to the number of connections. Fugitives for a closed loop sampling system are based on the component count.**

4 **Good design criteria for special chemicals handling and most LDAR programs require open-ended lines to be equipped with an appropriately sized cap, blind flange, plug, or a second valve. If so equipped, open-ended lines may be given a 100% control credit. Regardless of the lines given 100% credit, these lines should be mentioned in permit applications. Exceptions to the LDAR program criteria may be made for safety reasons with the approval of TCEQ management.**

TABLE 5-2. CONTROL EFFECTIVENESS FOR AN LDAR PROGRAM AT A SOCMI PROCESS UNIT

Equipment type and service	Control effectiveness (%)		
	Monthly monitoring 10,000 ppmv leak definition	Quarterly monitoring 10,000 ppmv leak definition	HON reg neg[a]
Valves - gas	87	67	92
Valves - light liquid	84	61	88
Pumps - light liquid	69	45	75
Connectors - all	b	b	93

[a] Control effectiveness attributable to the requirements of the proposed hazardous organic NESHAP equipment leak negotiated regulation are estimated based on equipment-specific leak definitions and performance levels.

[b] Data are not available to estimate control effectiveness.

AP-42 Section 13.2

Unpaved Roads

Table 13.2.2-1. TYPICAL SILT CONTENT VALUES OF SURFACE MATERIAL ON INDUSTRIAL UNPAVED ROADS[a]

Industry	Road Use Or Surface Material	Plant Sites	No. Of Samples	Silt Content (%)	
				Range	Mean
Copper smelting	Plant road	1	3	16 - 19	17
Iron and steel production	Plant road	19	135	0.2 - 19	6.0
Sand and gravel processing	Plant road	1	3	4.1 - 6.0	4.8
	Material storage area	1	1	-	7.1
Stone quarrying and processing	Plant road	2	10	2.4 - 16	10
	Haul road to/from pit	4	20	5.0-15	8.3
Taconite mining and processing	Service road	1	8	2.4 - 7.1	4.3
	Haul road to/from pit	1	12	3.9 - 9.7	5.8
Western surface coal mining	Haul road to/from pit	3	21	2.8 - 18	8.4
	Plant road	2	2	4.9 - 5.3	5.1
	Scraper route	3	10	7.2 - 25	17
	Haul road (freshly graded)	2	5	18 - 29	24
Construction sites	Scraper routes	7	20	0.56-23	8.5
Lumber sawmills	Log yards	2	2	4.8-12	8.4
Municipal solid waste landfills	Disposal routes	4	20	2.2 - 21	6.4

[a]References 1,5-15.

The following empirical expressions may be used to estimate the quantity in pounds (lb) of size-specific particulate emissions from an unpaved road, per vehicle mile traveled (VMT):

For vehicles traveling on unpaved surfaces at industrial sites, emissions are estimated from the following equation:

$$E = k\ (s/12)^a (W/3)^b \tag{1a}$$

and, for vehicles traveling on publicly accessible roads, dominated by light duty vehicles, emissions may be estimated from the following:

$$E = \frac{k\ (s/12)^a (S/30)^d}{(M/0.5)^c} - C \tag{1b}$$

where k, a, b, c and d are empirical constants (Reference 6) given below and

E = size-specific emission factor (lb/VMT)
s = surface material silt content (%)
W = mean vehicle weight (tons)
M = surface material moisture content (%)
S = mean vehicle speed (mph)
C = emission factor for 1980's vehicle fleet exhaust, brake wear and tire wear.

The source characteristics s, W and M are referred to as correction parameters for adjusting the emission estimates to local conditions. The metric conversion from lb/VMT to grams (g) per vehicle kilometer traveled (VKT) is as follows:

1 lb/VMT = 281.9 g/VKT

The constants for Equations 1a and 1b based on the stated aerodynamic particle sizes are shown in Tables 13.2.2-2 and 13.2.2-4. The PM-2.5 particle size multipliers (k-factors) are taken from Reference 27.

Table 13.2.2-2. CONSTANTS FOR EQUATIONS 1a AND 1b

Constant	Industrial Roads (Equation 1a)			Public Roads (Equation 1b)		
	PM-2.5	PM-10	PM-30*	PM-2.5	PM-10	PM-30*
k (lb/VMT)	0.15	1.5	4.9	0.18	1.8	6.0
a	0.9	0.9	0.7	1	1	1
b	0.45	0.45	0.45	-	-	-
c	-	-	-	0.2	0.2	0.3
d	-	-	-	0.5	0.5	0.3
Quality Rating	B	B	B	B	B	B

*Assumed equivalent to total suspended particulate matter (TSP)
"-" = not used in the emission factor equation

Table 13.2.2-2 also contains the quality ratings for the various size-specific versions of Equation 1a and 1b. The equation retains the assigned quality rating, if applied within the ranges of source conditions, shown in Table 13.2.2-3, that were tested in developing the equation:

Table 13.2.2-3. RANGE OF SOURCE CONDITIONS USED IN DEVELOPING EQUATION 1a AND 1b

Emission Factor	Surface Silt Content, %	Mean Vehicle Weight		Mean Vehicle Speed		Mean No. of Wheels	Surface Moisture Content, %
		Mg	ton	km/hr	mph		
Industrial Roads (Equation 1a)	1.8-25.2	1.8-260	2-290	8-69	5-43	4-17[a]	0.03-13
Public Roads (Equation 1b)	1.8-35	1.4-2.7	1.5-3	16-88	10-55	4-4.8	0.03-13

[a] See discussion in text.

As noted earlier, the models presented as Equations 1a and 1b were developed from tests of traffic on unpaved surfaces. Unpaved roads have a hard, generally nonporous surface that usually dries quickly after a rainfall or watering, because of traffic-enhanced natural evaporation. (Factors influencing how fast a road dries are discussed in Section 13.2.2.3, below.) The quality ratings given above pertain to the mid-range of the measured source conditions for the equation. A higher mean vehicle weight and a higher than normal traffic rate may be justified when performing a worst-case analysis of emissions from unpaved roads.

The emission factors for the exhaust, brake wear and tire wear of a 1980's vehicle fleet (*C*) was obtained from EPA's MOBILE6.2 model [23]. The emission factor also varies with aerodynamic size range

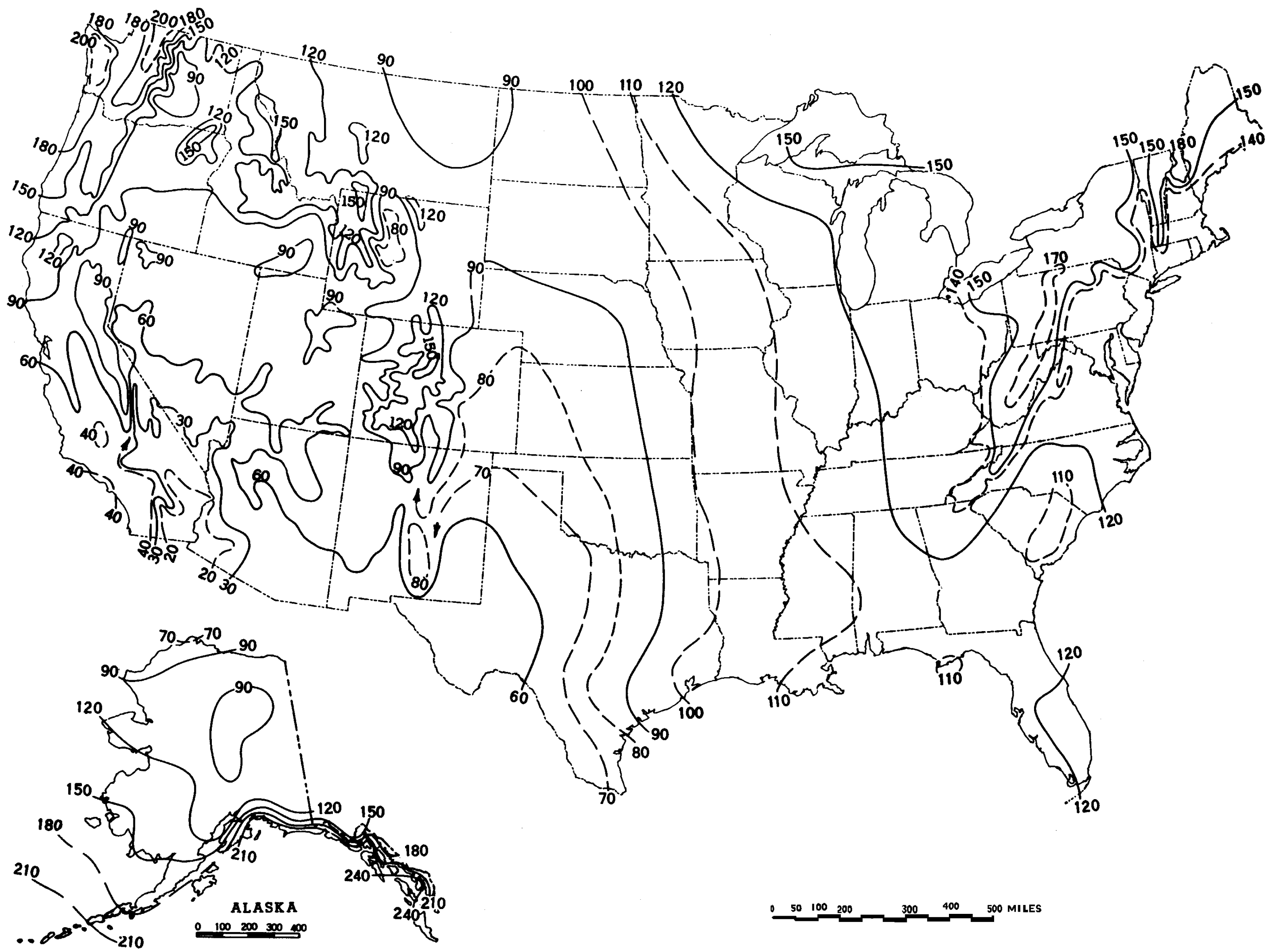


Figure 13.2.2-1. Mean number of days with 0.01 inch or more of precipitation in United States.

Tab 8
Section 8 - Map(s)

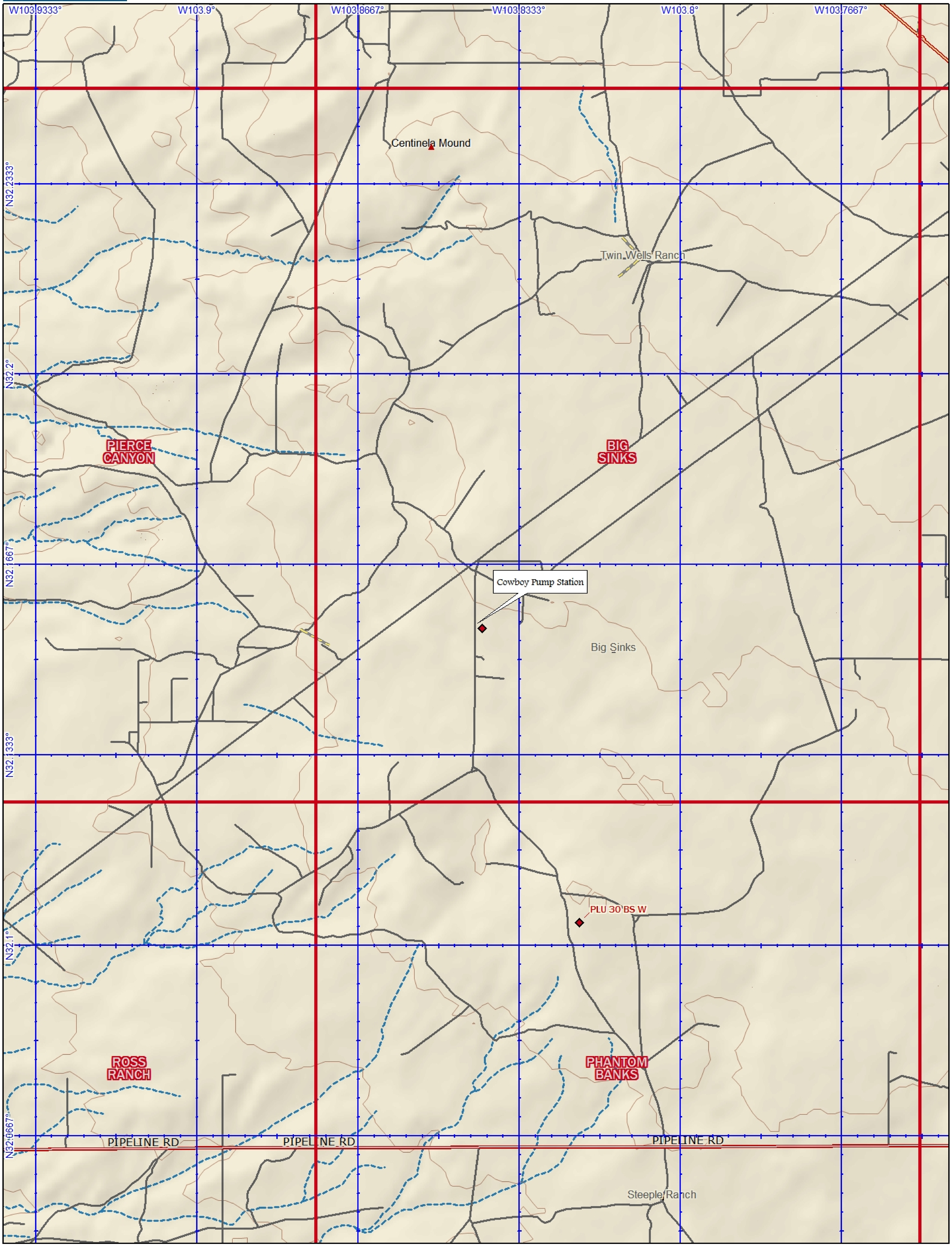
Section 8

Map(s)

A map such as a 7.5 minute topographic quadrangle showing the exact location of the source. The map shall also include the following:

The UTM or Longitudinal coordinate system on both axes	An indicator showing which direction is north
A minimum radius around the plant of 0.8km (0.5 miles)	Access and haul roads
Topographic features of the area	Facility property boundaries
The name of the map	The area which will be restricted to public access
A graphical scale	

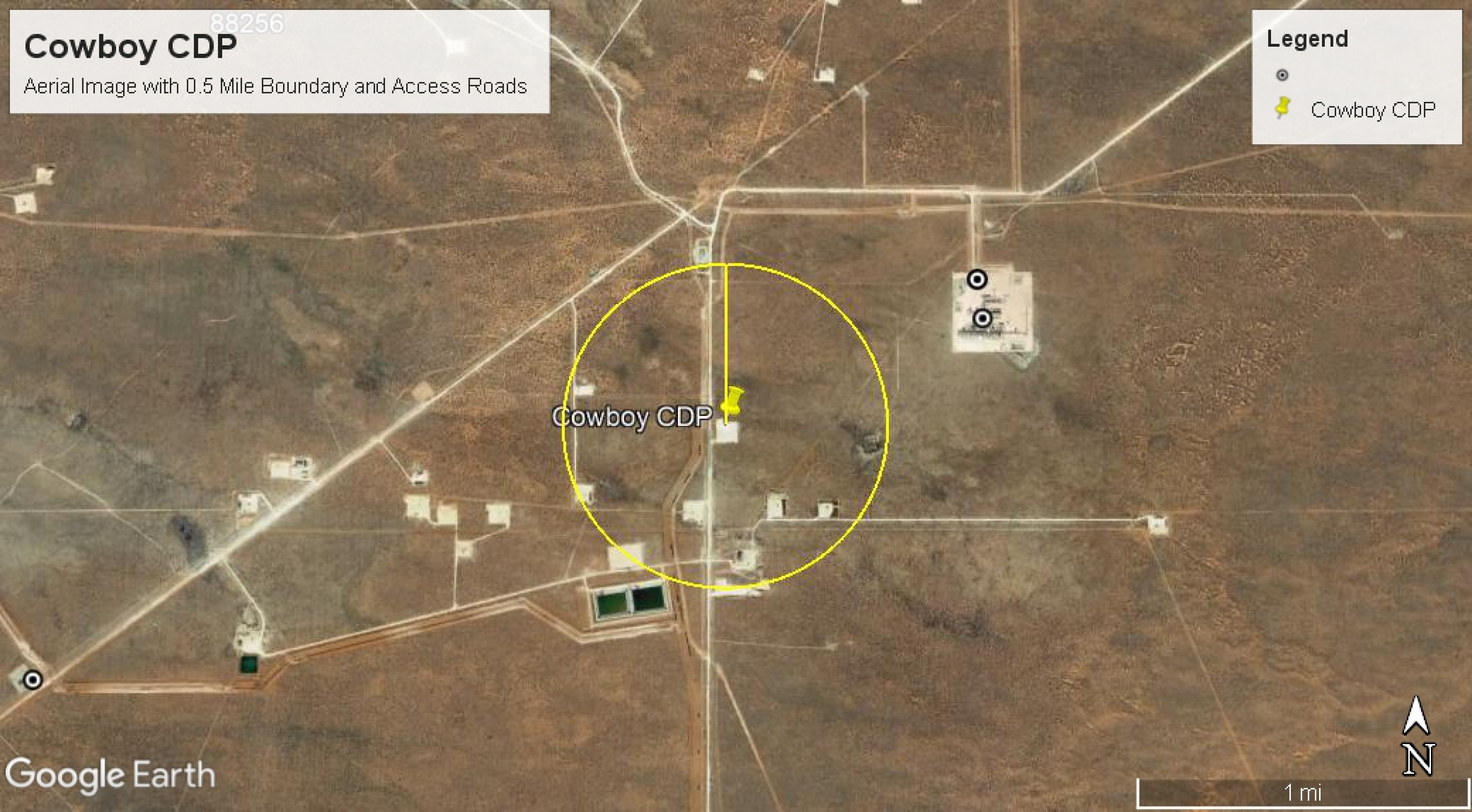
A site location map and aerial image illustrating the property boundary and surrounding access roads is provided.



MN (7.4° E)

0 ½ 1 1½ 2 2½ mi

Data Zoom 11-0


88256
Cowboy CDP
Aerial Image with 0.5 Mile Boundary and Access Roads
Legend
Cowboy CDP
Cowboy CDP
Google Earth
N
1 mi

Tab 9
Section 9 - Proof of Public Notice

Section 9

Proof of Public Notice

(for NSR applications submitting under 20.2.72 or 20.2.74 NMAC)
(This proof is required by: 20.2.72.203.A.14 NMAC "Documentary Proof of applicant's public notice")

☑ **I have read the AQB "Guidelines for Public Notification for Air Quality Permit Applications"**
This document provides detailed instructions about public notice requirements for various permitting actions. It also provides public notice examples and certification forms. Material mistakes in the public notice will require a re-notice before issuance of the permit.

Unless otherwise allowed elsewhere in this document, the following items document proof of the applicant's Public Notification. Please include this page in your proof of public notice submittal with checkmarks indicating which documents are being submitted with the application.

New Permit and **Significant Permit Revision** public notices must include all items in this list.

Technical Revision public notices require only items 1, 5, 9, and 10.

Per the Guidelines for Public Notification document mentioned above, include:

1. ☑ A copy of the certified letter receipts with post marks (20.2.72.203.B NMAC)
2. ☑ A list of the places where the public notice has been posted in at least four publicly accessible and conspicuous places, including the proposed or existing facility entrance. (e.g: post office, library, grocery, etc.)
3. ☑ A copy of the property tax record (20.2.72.203.B NMAC).
4. ☑ A sample of the letters sent to the owners of record.
5. ☑ A sample of the letters sent to counties, municipalities, and Indian tribes.
6. ☑ A sample of the public notice posted and a verification of the local postings.
7. ☑ A table of the noticed citizens, counties, municipalities and tribes and to whom the notices were sent in each group.
8. ☑ A copy of the public service announcement (PSA) sent to a local radio station and documentary proof of submittal.
9. ☑ A copy of the classified or legal ad including the page header (date and newspaper title) or its affidavit of publication stating the ad date, and a copy of the ad. When appropriate, this ad shall be printed in both English and Spanish.
10. ☑ A copy of the display ad including the page header (date and newspaper title) or its affidavit of publication stating the ad date, and a copy of the ad. When appropriate, this ad shall be printed in both English and Spanish.
11. ☑ A map with a graphic scale showing the facility boundary and the surrounding area in which owners of record were notified by mail. This is necessary for verification that the correct facility boundary was used in determining distance for notifying land owners of record.

The required documentation for Section 9 is included.

Certified Mail Receipts with Postmarks

7017 3040 0000 9587 9749

U.S. Postal Service™
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For delivery information, visit our website at www.usps.com®.

OFFICIAL USE

SANTA FE, NM 8750

Certified Mail Fee $ $3.55

Extra Services & Fees (*check box, add fee as appropriate*)
- ☐ Return Receipt (hardcopy) $ $0.00
- ☐ Return Receipt (electronic) $ $0.00
- ☐ Certified Mail Restricted Delivery $ $0.00
- ☐ Adult Signature Required $ $0.00
- ☐ Adult Signature Restricted Delivery $ $0.00

Postage $ $0.55

Total Postage and Fees $ $4.10

Postmark Here: EDWARDSVILLE IL 62025 USPS APR 10 2020 — 0425 13 — 04/10/2020

Sent To: State of NM Land Office

Street and Apt. No., or PO Box No.: 310 Old Santa Fe Trail

City, State, ZIP+4®: Santa Fe, NM 8759

PS Form 3800, April 2015 PSN 7530-02-000-9047 — See Reverse for Instructions

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LOVINGTON, NM 88260

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Extra Services & Fees (*check box, add fee as appropriate*)
- ☐ Return Receipt (hardcopy) $ $0.00
- ☐ Return Receipt (electronic) $ $0.00
- ☐ Certified Mail Restricted Delivery $ $0.00
- ☐ Adult Signature Required $ $0.00
- ☐ Adult Signature Restricted Delivery $ $0.00

Postage $ $0.55

Total Postage and Fees $ $4.10

Postmark Here: EDWARDSVILLE IL 62025 USPS APR 10 2020 — 0425 13 — 04/10/2020

Sent To: Lea County Manager

Street and Apt. No., or PO Box No.: 100 N. Main, Suite 4

City, State, ZIP+4®: Lovington, NM 88260

PS Form 3800, April 2015 PSN 7530-02-000-9047 — See Reverse for Instructions

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CARLSBAD, NM 88220

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Extra Services & Fees (*check box, add fee as appropriate*)
- ☐ Return Receipt (hardcopy) $ $0.00
- ☐ Return Receipt (electronic) $ $0.00
- ☐ Certified Mail Restricted Delivery $ $0.00
- ☐ Adult Signature Required $ $0.00
- ☐ Adult Signature Restricted Delivery $ $0.00

Postage $ $0.55

Total Postage and Fees $ $4.10

Postmark Here: EDWARDSVILLE IL 62025 USPS APR 10 2020 — 0425 13 — 04/10/2020

Sent To: BLM c/o David Evans

Street and Apt. No., or PO Box No.: 620 E. Greene St

City, State, ZIP+4®: Carlsbad, NM 88220-6292

PS Form 3800, April 2015 PSN 7530-02-000-9047 — See Reverse for Instructions

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CARLSBAD, NM 88220

Certified Mail Fee $ $3.55

Extra Services & Fees (*check box, add fee as appropriate*)
- ☐ Return Receipt (hardcopy) $ $0.00
- ☐ Return Receipt (electronic) $ $0.00
- ☐ Certified Mail Restricted Delivery $ $0.00
- ☐ Adult Signature Required $ $0.00
- ☐ Adult Signature Restricted Delivery $ $0.00

Postage $ $0.55

Total Postage and Fees $ $4.10

Postmark Here: EDWARDSVILLE IL 62025 USPS APR 10 2020 — 0425 13 — 04/10/2020

Sent To: Eddy County Manager

Street and Apt. No., or PO Box No.: 101 W. Greene St., Suite 110

City, State, ZIP+4®: Carlsbad, NM 88220

PS Form 3800, April 2015 PSN 7530-02-000-9047 — See Reverse for Instructions

List of Places Posted Site Location

Exxon Mobil Main Entrance

Carlsbad Library

Carlsbad Post Office

Property Tax Records

Property Record Card

Eddy Assessor

BUREAU OF LAND MANAGEMENT

Account: R051897

Tax Area: CO_NR - CARLSBAD-OUT (Nonresidential)

Acres: 0.000

Parcel: 4-180-145-266-335

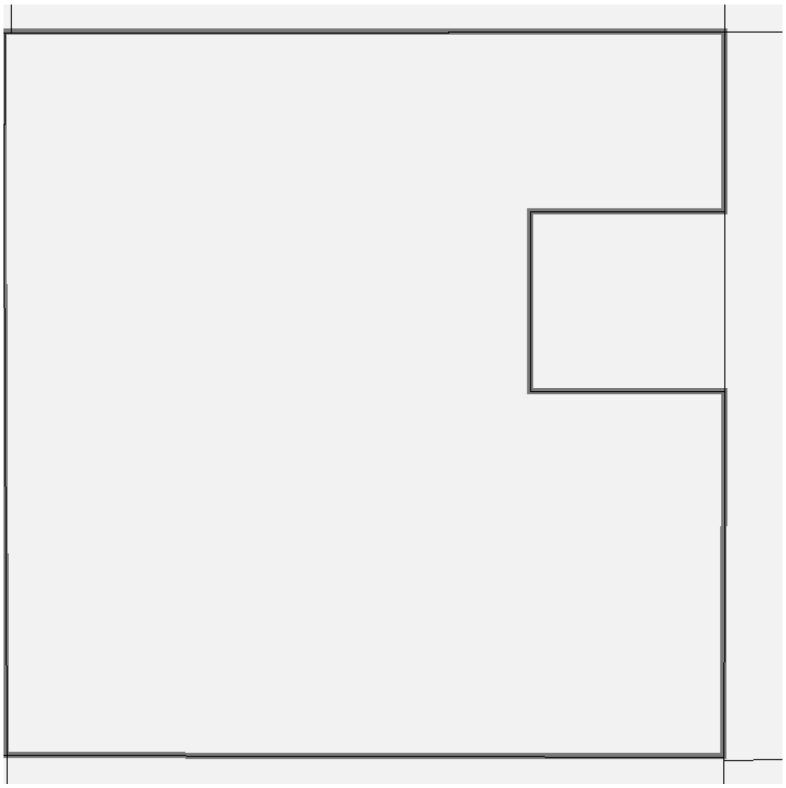
Situs Address:
900 BUCK JACKSON ROAD

Value Summary

Value By:	Market	Override
Land (1)	$2,700	N/A
Total	**$2,700**	**$2,700**

Legal Description

Quarter: NE S: 1 T: 25S R: 30E Quarter: NW S: 1 T: 25S R: 30E Quarter: SW S: 1 T: 25S R: 30E Quarter: SE S: 1 T: 25S R: 30E ALL LESS SENE MAP# 385-1 LOC S & W OF 900 BUCK JACKSON EXEMPT



Land Occurrence 1

Property Code	9200 - EXEMPT NON-RESIDENTIAL LAND	Land Code	141_4_5 - Grazing E Federal - 4.5

Abstract Summary

Code	Classification	Actual Value Value	Taxable Value	Actual Value Override	Taxable Override
9200	EXEMPT NON-RESIDENTIAL LAND	$2,700	$900	NA	NA
Total		**$2,700**	**$900**	**NA**	**NA**

Property Record Card

Eddy Assessor

COUNTY OF EDDY
101 W GREENE ST STE 110
CARLSBAD, NM 88220

Account: R065349
Tax Area: CO_NR - CARLSBAD-OUT (Nonresidential)
Acres: 40.000

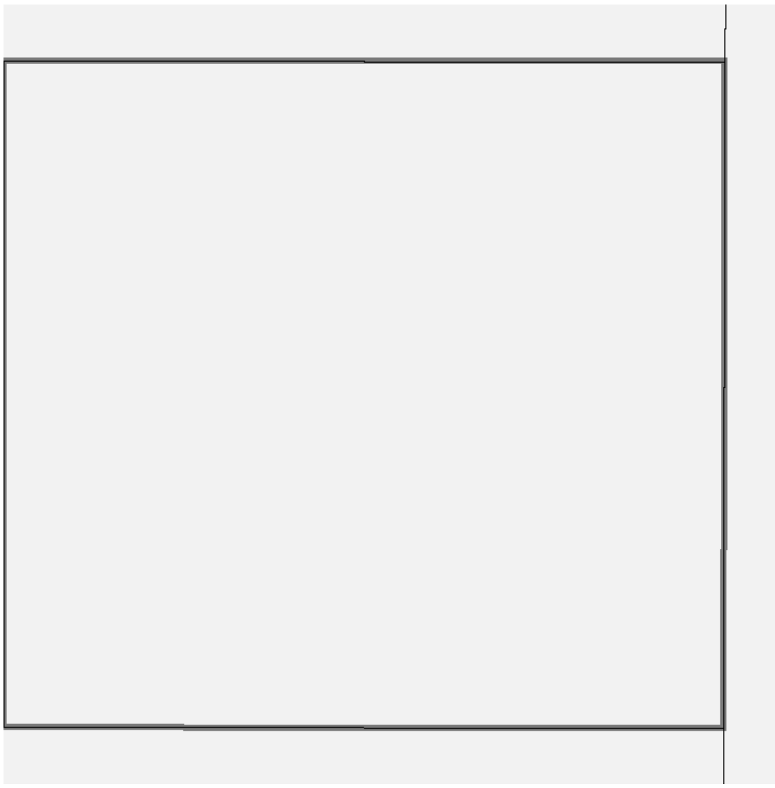
Parcel: 4-180-145-465-199
Situs Address:
810 BUCK JACKSON ROAD
CARLSBAD, 88220

Value Summary

Value By:	Market	Override
Land (1)	$100,000	N/A
Total	**$100,000**	**$100,000**

Legal Description

S: 1 T: 25S R: 30E SENE MAP# 385-1.1 LOC 810 BUCK JACKSON ROAD EXEMPT



Public Remarks

Entry Date	Model	Remark
07/31/2015		BOOK 1032 PG 1102

Land Occurrence 1

Property Code	9200 - EXEMPT NON-RESIDENTIAL LAND	Land Code	111_2499_99 - Commercial Land N/R - 2499.99
Description	EXEMPT NON-RESIDENTIAL LAND	Measure	A - Acres

Abstract Summary

Code	Classification	Actual Value Value	Taxable Value	Actual Value Override	Taxable Override
9200	EXEMPT NON-RESIDENTIAL LAND	$100,000	$33,333	NA	NA
Total		**$100,000**	**$33,333**	**NA**	**NA**

Property Record Card

Eddy Assessor

STATE OF NEW MEXICO
310 OLD SANTA FE TRAIL
SANTA FE, NM 87504

Account: R091436
Tax Area: CO_NR - CARLSBAD-OUT (Nonresidential)
Acres: 0.000

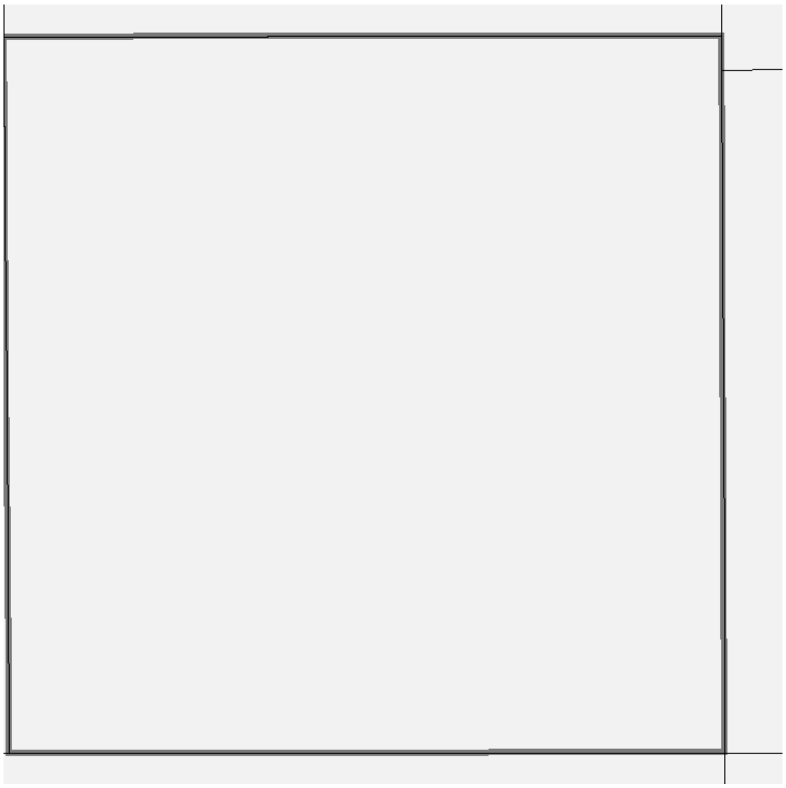
Parcel: 4-180-144-264-264
Situs Address:

Value Summary

Value By:	Market	Override
Land (1)	$2,880	N/A
Total	**$2,880**	**$2,880**

Legal Description

Quarter: NE S: 36 T: 24S R: 30E Quarter: NW S: 36 T: 24S R: 30E Quarter: SW S: 36 T: 24S R: 30E Quarter: SE S: 36 T: 24S R: 30E ALL EXEMPT



Land Occurrence 1

Property Code	9200 - EXEMPT NON-RESIDENTIAL LAND	Land Code	149_4_5 - Grazing A NM - 4.5

Abstract Summary

Code	Classification	Actual Value Value	Taxable Value	Actual Value Override	Taxable Override
9200	EXEMPT NON-RESIDENTIAL LAND	$2,880	$960	NA	NA
Total		**$2,880**	**$960**	**NA**	**NA**

Property Record Card

Eddy Assessor

BUREAU OF LAND MANAGEMENT

Account: R091909

Tax Area: CO_NR - CARLSBAD-OUT (Nonresidential)

Acres: 0.000

Parcel: 4-181-144-265-253

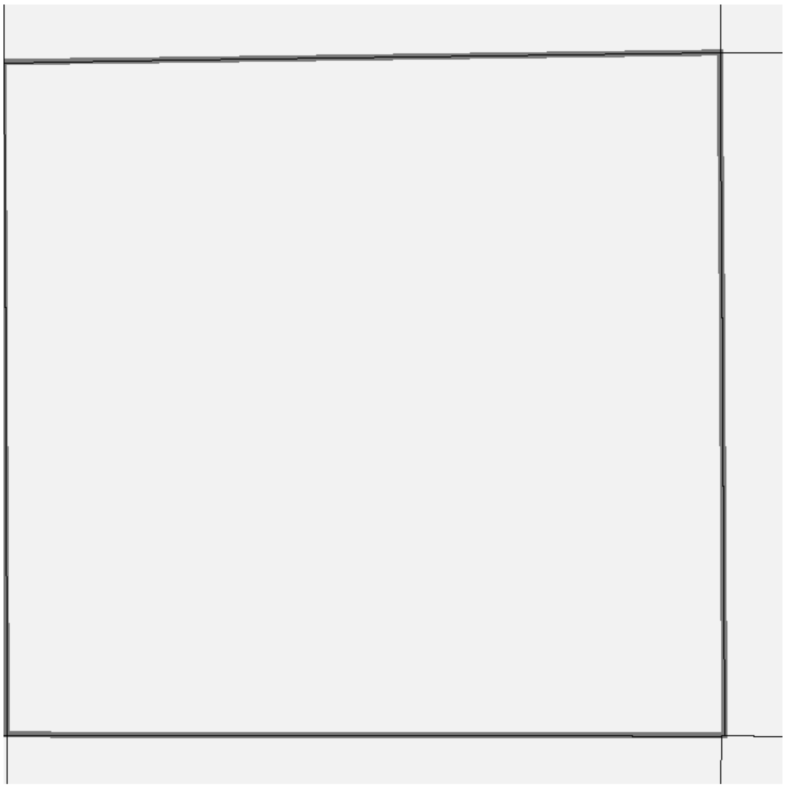
Situs Address:

Value Summary

Value By:	Market	Override
Land (1)	$2,880	N/A
Total	**$2,880**	**$2,880**

Legal Description

Quarter: NE S: 31 T: 24S R: 31E Quarter: NW S: 31 T: 24S R: 31E Quarter: SW S: 31 T: 24S R: 31E Quarter: SE S: 31 T: 24S R: 31E ALL MAP# 370-31 EXEMPT



Land Occurrence 1

Property Code	9200 - EXEMPT NON-RESIDENTIAL LAND	Land Code	141_4_5 - Grazing E Federal - 4.5

Abstract Summary

Code	Classification	Actual Value Value	Taxable Value	Actual Value Override	Taxable Override
9200	EXEMPT NON-RESIDENTIAL LAND	$2,880	$960	NA	NA
Total		**$2,880**	**$960**	**NA**	**NA**

Property Record Card

Eddy Assessor

BUREAU OF LAND MANAGEMENT

Account: R092037

Tax Area: CO_NR - CARLSBAD-OUT (Nonresidential)

Acres: 0.000

Parcel: 4-181-145-265-266

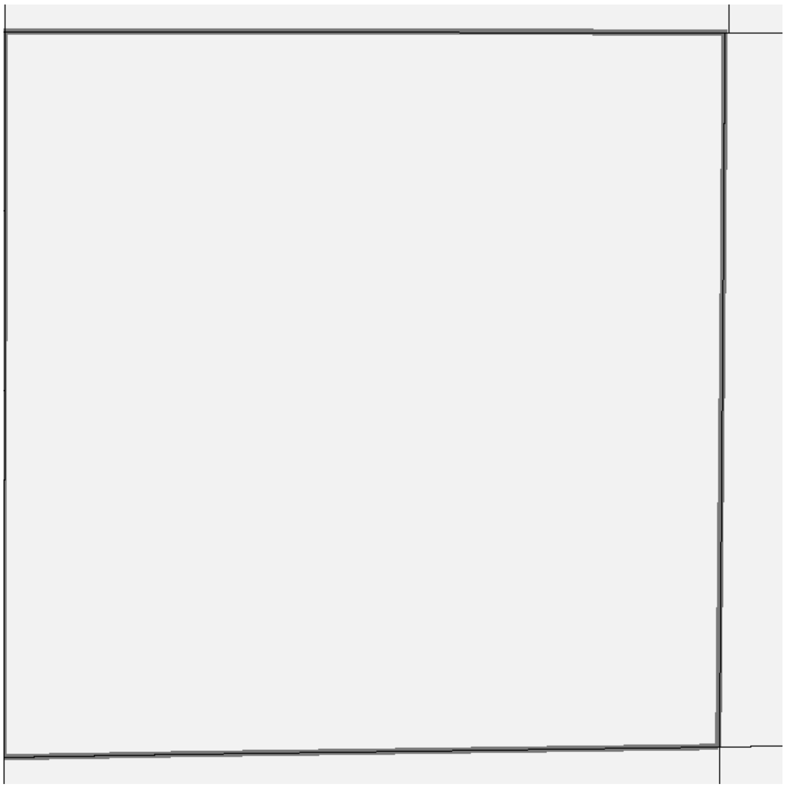
Situs Address:

Value Summary

Value By:	Market	Override
Land (1)	$2,916	N/A
Total	**$2,916**	**$2,916**

Legal Description

Quarter: NE S: 6 T: 25S R: 31E Quarter: NW S: 6 T: 25S R: 31E Quarter: SW S: 6 T: 25S R: 31E Quarter: SE S: 6 T: 25S R: 31E ALL MAP# 386-6 LOC CARLSBAD EXEMPT



Land Occurrence 1

Property Code	9200 - EXEMPT NON-RESIDENTIAL LAND	Land Code	141_4_5 - Grazing E Federal - 4.5

Abstract Summary

Code	Classification	Actual Value Value	Taxable Value	Actual Value Override	Taxable Override
9200	EXEMPT NON-RESIDENTIAL LAND	$2,916	$972	NA	NA
Total		**$2,916**	**$972**	**NA**	**NA**

Letters to Owners of Record and Applicable Counties, Municipalities, and Tribes

XTO ENERGY

April 9, 2020 Certified Mail 7017 3040 000 9587 9718

David Evans – Acting Field Manager
Bureau of Land Management
620 E. Greene St.
Carlsbad, New Mexico, 88220-6292

RE: NSR Permit Application
Cowboy CDP
XTO Energy Inc.

Dear Federal Official,

In accordance with the application requirements of 20.2.72 NMAC, XTO Energy Inc. is providing notification of the planned construction of the Cowboy CDP near your property in Eddy County, NM. A public notice will be posted in the Carlsbad Current Argus newspaper, at the proposed site location, and three other locations in Carlsbad, NM. A copy of the notice is attached. Please contact me at (832) 624-2768 or benjamin_schnieder@xtoenergy.com should you have any questions.

Sincerely,

Ben Schneider

Ben Schneider
Environmental Engineer

Attachment: Public Notice

USPS Tracking®

FAQs >

Track Another Package +

Tracking Number: 70173040000095879718

Remove ×

We attempted to deliver your package at 10:20 am on April 14, 2020 in CARLSBAD, NM 88220 but could not access the delivery location. We will redeliver on the next business day.

Alert

April 14, 2020 at 10:20 am
Delivery Attempted - No Access to Delivery Location
CARLSBAD, NM 88220

Get Updates

Feedback

Text & Email Updates

Tracking History

Product Information

See Less

Can't find what you're looking for?

Go to our FAQs section to find answers to your tracking questions.

FAQs

April 9, 2020 Certified Mail 7017 3040 0000 9587 9725

Eddy County Manager
101 W. Greene St.
Suite 110
Carlsbad, New Mexico, 88220

RE: NSR Permit Application
Cowboy CDP
XTO Energy Inc.

Dear County Manager,

In accordance with the application requirements of 20.2.72 NMAC, XTO Energy Inc. is providing notification of the planned construction of the Cowboy CDP on your property in Eddy County, NM. A public notice will be posted in the Carlsbad Current Argus newspaper, at the proposed site location, and three other locations in Carlsbad, NM. A copy of the notice is attached. Please contact me at (832) 624-2768 or benjamin_schnieder@xtoenergy.com should you have any questions.

Sincerely,

Ben Schneider

Ben Schneider
Environmental Engineer

Attachment: Public Notice

April 9, 2020 Certified Mail 7017 3040 0000 9587 9732

Mike Gallagher – County Manager
Lea County
100 N. Main Avenue
Suite 4
Lovington, New Mexico, 88260

RE: NSR Permit Application
Cowboy CDP
XTO Energy Inc.

Dear County Manager,

In accordance with the application requirements of 20.2.72 NMAC, XTO Energy Inc. is providing notification of the planned construction of the Cowboy CDP near your property in Eddy County, NM. A public notice will be posted in the Carlsbad Current Argus newspaper, at the proposed site location, and three other locations in Carlsbad, NM. A copy of the notice is attached. Please contact me at (832) 624-2768 or benjamin_schnieder@xtoenergy.com should you have any questions.

Sincerely,

Ben Schneider

Ben Schneider
Environmental Engineer

Attachment: Public Notice

USPS Tracking®

FAQs >

Track Another Package +

Remove ×

Tracking Number: 70173040000095879732

Your item was delivered to an individual at the address at 9:59 am on April 13, 2020 in LOVINGTON, NM 88260.

Delivered

April 13, 2020 at 9:59 am
Delivered, Left with Individual
LOVINGTON, NM 88260

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Product Information

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Go to our FAQs section to find answers to your tracking questions.

FAQs

April 9, 2020 Certified Mail 7017 3040 000 9587 9749

State of New Mexico Land Office
310 Old Santa Fe Trail
Santa Fe, New Mexico, 87501

RE: NSR Permit Application
Cowboy CDP
XTO Energy Inc.

Dear Commissioner,

In accordance with the application requirements of 20.2.72 NMAC, XTO Energy Inc. is providing notification of the planned construction of the Cowboy CDP within 10 miles of Lea County, NM. A public notice will be posted in the Carlsbad Current Argus newspaper, at the proposed site location, and three other locations in Carlsbad, NM. A copy of the notice is attached. Please contact me at (832) 624-2768 or benjamin_schnieder@xtoenergy.com should you have any questions.

Sincerely,

Ben Schneider

Ben Schneider
Environmental Engineer

Attachment: Public Notice

USPS Tracking®

FAQs >

Track Another Package +

Remove ✕

Tracking Number: 70173040000095879749

Your item has been delivered and is available at a PO Box at 7:11 am on April 13, 2020 in SANTA FE, NM 87501.

Delivered

April 13, 2020 at 7:11 am
Delivered, PO Box
SANTA FE, NM 87501

Get Updates

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FAQs

Sample of Notice posted and

Verification of Postings

NOTICE

XTO Energy Inc. announces its application to the New Mexico Environment Department for the modification of the air quality permit for the Cowboy CDP. The expected date of application submittal to the Air Quality Bureau is April 15, 2020. The proposed modification primarily consists of adding controls on certain heaters, updating SSM emissions, adding produced gas flaring, updating fugitive counts, adding emergency generators, adding slop oil loading, and updating equipment nomenclature.

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PM_{10}	85	52
$PM_{2.5}$	85	52
Sulfur Dioxide (SO_2)	8	30
Nitrogen Oxides (NO_x)	600	180
Carbon Monoxide (CO)	1,150	175
Volatile Organic Compounds (VOC)	1,900	240
Total sum of all Hazardous Air Pollutants (HAPs)	31	19
Toxic Air Pollutant (TAP)	n/a	n/a
Green House Gas Emissions as Total CO_2e	n/a	1,100,000

The standard and maximum operating schedules of the facility will be 24 hours per day, 7 days a week and a maximum of 52 weeks per year. The owner and/or operator of the Facility is: The owner and/or operator of the Facility is: XTO Energy, Inc.; 22777 Springwoods Village Pkwy; Spring, Texas 77389.

If you have any comments about the construction or operation of this facility, and you want your comments to be made as part of the permit review process, you must submit your comments in writing to this address: Permit Programs Manager; New Mexico Environment Department; Air Quality Bureau; 525 Camino de los Marquez, Suite 1; Santa Fe, New Mexico; 87505-1816; (505) 476-4300; 1 800 224-7009; https://www.env.nm.gov/aqb/permit/aqb_draft_permits.html. Other comments and questions may be submitted verbally.

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General Posting of Notices – Certification

Cowboy CDP

I, Bryan Jacob Foust, the undersigned, certify that on 4-17-20, a true and correct copy of the attached Public Notice was posted in the following publicly accessible and conspicuous places in Loving, Eddy County, State of New Mexico on the following dates:

1. Facility entrance -
2. Post office
3. Library
4. Exxon - Greene/main ST

Signed this 17th day of April, 2020

[signature] 4-17-20

Signature Date

Bryan Jacob Foust

Printed Name

XTO - SHE

Title {APPLICANT OR RELATIONSHIP TO APPLICANT}

Noticed Citizens, Counties, Municipalities, and Tribes Eddy County:

Eddy County Manager

Lea County: Lea County Manager (Mike Gallagher)

Bureau Of Land Management:Carlsbad Field Office (David Evans)

State of NM: Commissioner

Public Service Announcement Documentation

Submittal of Public Service Announcement – Certification

I, _Evan Tullos, the undersigned, certify that on **April 9, 2020**, submitted a public service announcement to **Carlsbad Radio** that serves Carlsbad, **Eddy** County, New Mexico, in which the source is or is proposed to be located and that Carlsbad Radio did not respond regarding the airing of the announcement.

Signed this 9th day of April, 2020,

4/9/2020

Signature   Date

Evan Tullos
Printed Name

Vice President – Consultant for XTO Energy Inc.
Title {APPLICANT OR RELATIONSHIP TO APPLICANT}

CLOSE

Transmission Status

Your transmission has completed.

DOC Identifier : 34276558
Fax Number : 5758877000
Recipient : KATK FM
Status Classification : "Success"
Status Outcome : "Success"
Last Attempt Date : 04/09/2020
Last Attempt Time : 07:53:06
Pages Scheduled : 3
Pages Sent : 3
Baud Rate : 31200
Duration (in seconds) : 39
Number of Retries : 1
Remote CSID : "15758877000"

Cover page

Public Service Announcement_Cowboy.docx

April 9, 2020

KATK 92.1 FM
(575) 887-7000

Re: Public Service Announcement

As part of the air quality permitting process in New Mexico, applicants for certain air permits must attempt to provide notice to the public of the proposed permit action via public service announcement (PSA). The announcement is attached. Will you air the PSA? Thank you.

Evan Tullos
PEI
(865) 850-2007

NOTICE OF AIR QUALITY PERMIT APPLICATION

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The notice was posted at the facility and three other public locations in Carlsbad such as the library, post office, and grocery store. If you have any comments about the construction or operation of the above facility, and you want your comments to be made as part of the permit review process, you must submit your comments in writing to the address below:

Permit Programs Manager
New Mexico Environment Department
Air Quality Bureau
525 Camino de los Marquez, Suite 1
Santa Fe, New Mexico 87505-1816
(505) 476-4300

Legal Ad

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To advertise, visit:
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all kinds of things...

Miscellaneous

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Real Estate Rentals

PUBLISHER'S NOTICE
All real estate advertised herein is subject to the Federal Fair Housing Act, which makes it illegal to advertise any preference, limitation, or discrimination because of race, color, religion, sex, handicap, familial status, or national origin, or intention to make any such preference, limitation, or discrimination. "We will not knowingly accept any advertising for real estate which is in violation of the law. All persons are hereby informed that all dwellings advertised are available on an equal opportunity basis.

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ATTENTION!
3 Bed 2 Bath. Big Yard! Rent to Own.
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Legal Notices

FIFTH JUDICIAL DISTRICT COURT
STATE OF NEW MEXICO
COUNTY OF EDDY
JETSTREAM ROYALTY PARTNERS, LP
Plaintiff,
v.
UNKNOWN HEIRS, IF ANY, OF HENRY FRANK GROOMS AKA H.F. GROOMS, DECEASED; UNKNOWN HEIRS, IF ANY, OF PEARL GROOMS, DECEASED; UNKNOWN HEIRS, IF ANY, OF RUTH ESTA GROOMS FARRER, DECEASED; UNKNOWN HEIRS, IF ANY, OF HAROLD GROOMS, DECEASED; UNKNOWN HEIRS, IF ANY, OF DARWIN GROOMS, DECEASED; UNKNOWN HEIRS, IF ANY, OF NAOMI GROOMS, DECEASED; UNKNOWN HEIRS, IF ANY, OF EVA MAE GROOMS, DECEASED; UNKNOWN HEIRS, IF ANY, OF HERSCHEL GROOMS, DECEASED; RUTH ANN FARRER MATTHEWS AKA RUTH ANN FARRER IF LIVING, IF DECEASED, UNKNOWN HEIRS; FRANK MATTHEWS, JR., IF LIVING, IF DECEASED, UNKNOWN HEIRS; JAMES FRANKLIN FARRER, IF LIVING, IF DECEASED, UNKNOWN HEIRS; BETTY JO FARRER LANDON, IF LIVING, IF DECEASED, UNKNOWN HEIRS; ROGERS LANDON, IF LIVING, IF DECEASED, UNKNOWN HEIRS,

UNKNOWN HEIRS OF RUTH BEHYMER, DECEASED, UNKNOWN HEIRS OF WILLIAM ARNOLD BEHYMER aka WILLIAM A. BEYHMER aka BILL A. BEHYMER aka BILL WILLIAM A. BEYHMER aka W.A. "BILL" BEHYMER; ROGINA BEHYMER aka ROJENA BEHYMER, WILLIAM ARNOLD BEHYMER, IF LIVING, IF DECEASED, UNKNOWN HEIRS; RAYMOND BEHYMER, IF LIVING, IF DECEASED, UNKNOWN HEIRS; MARY ANN BEHYMER,
and
ANY AND ALL UNKNOWN CLAIMANTS OF INTERESTS IN THE PREMISES ADVERSE TO THE PLAINTIFF,
Defendant.
No. D-503-CV-2020-00227
NOTICE OF PENDENCY OF SUIT

TO: Unknown Heirs, if any, of Henry Frank Grooms aka H.F. Grooms, Deceased; Unknown Heirs, if any, of Pearl Grooms, Deceased; Unknown Heirs, if any, of Ruth Esta Grooms Farrer, Deceased; Unknown Heirs, if any, of Harold Grooms, Deceased; Unknown Heirs, if any, of Darwin Grooms, Deceased; Unknown Heirs, if any, of Naomi Grooms, Deceased; Unknown Heirs, if any, of Eva Mae Grooms, Deceased; Unknown Heirs, if any, of Herschel Grooms, Deceased; Ruth Ann Farrer Matthews aka Ruth Ann Farrer if living, if Deceased, Unknown Heirs; Frank Matthews, Jr., if living, if Deceased, Unknown Heirs; James Franklin Farrer, if living if Deceased, Unknown Heirs; Betty Jo Farrer Landon, if living, if Deceased, Unknown Heirs; Rogers Landon, if living if Deceased, Unknown Heirs; Unknown Heirs of Ruth Behymer, Deceased, Unknown Heirs of William Arnold Behymer aka William A. Beyhmer aka Bill A. Behymer aka Bill William A. Beyhmer aka W.A. "Bill" Behymer; Rogina Behymer aka Rojena Behymer; William Arnold Behymer, if living, if Deceased, Unknown Heirs; Raymond Behymer, if living if Deceased, Unknown Heirs; and Mary Ann Behymer.

GREETINGS:

YOU and EACH of YOU are hereby notified that there has been filed in the Fifth Judicial District Court of Eddy County, New Mexico, in the above entitled cause of action, a Complaint to Quiet Title, wherein John Edward Fifer and Echo Mae Mason are Plaintiffs and you and each of you are the Defendants. The object and purpose of said suit is to quiet and set at rest the Plaintiffs' title described in the Complaint to the following described real property in Eddy County, New Mexico:

Township 24 South, Range 28 East, NMPM
Section 9: W/2NE/4SW/4SE/4

containing 5.00 acres, more or less

referring to both the surface estate and all oil and gas interests.
You, and each of you, are further notified that unless you enter your appearance in said cause on or before May 11, 2020, judgment by default will be rendered in said cause against each of you so failing to appear, and Plaintiffs will apply to the Court for the relief demanded in the Complaint.

Cavin & Ingram, P.A. (Scott S. Morgan) are attorneys for the Plaintiffs and their office address is 40 First Plaza NW, Suite 610, Albuquerque, New Mexico 87102 (mailing address is P.O. Box 1216, Albuquerque, New Mexico, 87103-1216); telephone number 505-243-5400.
Karen Christesson, Clerk of the Court
JUDICIAL DISTRICT COURT
EDDY COUNTY
By s/Emily I. Gonzales, Deputy Clerk
CAVIN & INGRAM, P.A.
By:/s/Scott S. Morgan
Scott S. Morgan
P. O. Box 1216
Albuquerque, NM 87103
(505) 243-5400
smorgan@cilawnm.com
ATTORNEYS FOR PLAINTIFFS
#4071838, Current Argus, 3/21, 3/28, 4/4, 4/11/2020

Your Source Public Notices

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Legal Notices

NOTICE OF AIR QUALITY PERMIT APPLICATION

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4147647, Carlsbad Current-Argus, April 11, 2020

Display Ad

MLB

Continued from Page 1B

Sports, and realign all six divisions for an abbreviated season.

The official spoke on the condition of anonymity because the proposal is one of several being discussed.

The plan would have all 30 teams returning to their spring training sites in Florida and Arizona, playing regular-season games only in those two states and without fans in an effort to reduce travel and minimize risks in the midst of the COVID-19 pandemic.

The divisions would be realigned based on the geography of their spring training homes.

The plan would allow teams to return to the comforts of their spring training sites for three weeks of training, which would also include exhibition games, before opening the regular season and playing a schedule with wholly different divisional opponents.

Here's a look at one realignment structure:

GRAPEFRUIT LEAGUE

▮ **NORTH:** New York Yankees, Philadelphia Phillies, Toronto Blue Jays, Detroit Tigers, Pittsburgh Pirates.

▮ **SOUTH:** Boston Red Sox, Minnesota Twins, Atlanta Braves, Tampa Bay Rays, Baltimore Orioles.

▮ **EAST:** Washington Nationals, Houston Astros, New York Mets, St. Louis Cardinals, Miami Marlins.

CACTUS LEAGUE

▮ **NORTHEAST:** Chicago Cubs, San Francisco Giants, Arizona Diamondbacks, Colorado Rockies, Oakland Athletics.

▮ **WEST:** Los Angeles Dodgers, Chicago White Sox, Cincinnati Reds, Cleveland Indians, Los Angeles Angels.

▮ **NORTHWEST:** Milwaukee Brewers, San Diego Padres, Seattle Mariners, Texas Rangers, Kansas City Royals.

"When you're trying to get really creative, why say no now?" says Hall of Fame manager Tony La Russa, the Angels' senior adviser of baseball operations who has been briefed of the potential plan. "So you have a unique season. I've got no problem with that.

"I'm not sure we'll be able play in our own cities across the country, so if you split it up like that, it's a possibility."

The Cactus League provides more flexibility given all of the teams are within an hour's drive of each other.

Also, Florida, with teams spread throughout the state, presents a bigger challenge if players, officials and support staff would needed to be quarantined, which has not been determined.

Earlier this week, following a report by ESPN, MLB said it was having preliminary discussions about playing the season exclusively in Arizona.

The Arizona-Florida plan has several advantages, including allowing teams to establish home bases with facilities they are familiar with. There would be 26 ballparks available to be used, including three major league domed stadiums – Tropicana Field in St. Petersburg, Florida, Marlins Park in Miami and Chase Field in Phoenix.

Financially, it could be a huge boon for the TV rights holders. You could have a captive TV audience the entire day. Games in Florida could begin at 11 a.m. ET and still have games in prime-time for East Coast teams and their fans. The time slots still would permit West Coast teams to play prime-time games in Arizona.

Baseball, even with the realignment, could still play 12 games apiece against their new divisional opponents and six games apiece against the other teams in the state. There would be at least one doubleheader a night when all teams are scheduled to play because of the odd number of teams in each state.

The DH would likely be universally implemented as well.

There could still be division winners and wild-card winners, perhaps adding two more wild-card teams to each league, or a postseason tournament with all 30 teams.

The winner of the Cactus League in Arizona would play the winner of the Grapefruit League in Florida for the World Series championship, utilizing the domed stadiums in late November.

Coaches

Continued from Page 1B

sissippi State, Sam Pittman at Arkansas, Michigan State's Mel Tucker and Karl Dorrell at Colorado.

"I'd be lying if I said that doesn't hurt us," Pittman said. "We know our players as well as we can in the short period of time that we've been together, but man, it would have been nice to see what they can do and how they react to coaching and how they react to techniques and things of that nature. We just weren't able to do it."

Coaches like Rolovich and Pittman, who was hired on Dec. 8, had a few months to begin molding their programs before the outbreak.

Dorrell had a few weeks.

A former Buffaloes assistant, Dorrell returned to Boulder on Feb. 23 after Mel Tucker left to become Michigan State's head coach. Dorrell worked quickly to hire coaches, interview his players and begin laying the schematic groundwork.

Colorado's spring football was suspended indefinitely three days before the first practice, leaving Dorrell and his staff no chance to work with their players on the field.

"I'm not looking at it as a detriment just because I'm new. I look at it like everybody's dealing with this," he said. "I know that they're all under the same guidance and standards of what's going on right now with our country, so from our perspective, we're just going to try to maximize whatever chance we get with our players."

Coaches across the country are trying to navigate the locked-down, no-football world of the pandemic, preparing for a season while not knowing when it will begin. Meetings between coaches, players and positional groups are done virtually as teams do the best they can to ensure they're ready when football starts up again, whenever that is.

The first-year coaches are also using the time to get to know their players and make sure there's still a connection when they're allowed to return to the field.

"I'm working through our roster, calling about 15 or so guys a day and spending time with them, getting to know their families, getting to know their daily routine, getting to know their goals and their vision for themselves and their futures and how I can help with that," Aranda said. "I think when it's slowed down to the point to where it is now, it allows us to fill in that space and that time with people."

William Byron, driver of the No.24 Chevrolet, leads the pack during an iRacing event at virtual Bristol Motor Speedway. CHRIS GRAYTHEN/GETTY IMAGES

Racing

Continued from Page 1B

product, swap the amateur racers with its stars, and Fox Sports said it would broadcast the races. Viewership in two of the last three Fox races were the most watched in esports history and the cable networks have all scrambled to create their own virtual racing content.

"All of the race teams are trying everything they can to keep their sponsors and keep their employees," said Dale Earnhardt Jr., the retired NASCAR star who is a longtime virtual racing fanatic, owner of an Xfinity Series team and NBC Sports analyst.

IndyCar will race Saturday at a virtual Michigan International Speedway, a beloved track that long ago fell off the open-wheel racing schedule. The race will be aired on NBC Sports with Earnhardt Jr. making his IndyCar virtual debut. It will also be the debut in the series for Marco Andretti, who didn't compete in IndyCar's first two events on road courses, along with his real-life teammate Ryan Hunter-Reay.

The entry list for Michigan cites a whopping 31 drivers.

Part of the appeal is the ability to watch the drivers in action on home-based simulators that can cost up to six figures. Drivers are smartly using online social feeds to give viewers an inside look and listen – ringside seats to the bad-mouthing, cursing and comedic talents of the racers.

It's a rare chance for a fan to follow the emotions of a driver in real time – and a rarity for television producers.

"The drivers are the star and the more we can get the driver engagement, the driver as part of the story, it makes for a better race," said Sam Flood, executive producer of NBC Sports and NBCSN.

"Most sports, hockey players trash talk on the ice, and NASCAR you can shake your fist out the window, throw up a middle finger or do something to salute one of your competitors, but you really can't talk to them while the race is going on," Flood said. "Football players can stand over a quarterback and say something. So it's fun now that in these races the drivers are able to get at it a little bit verbally, which is something we'd love to see more of."

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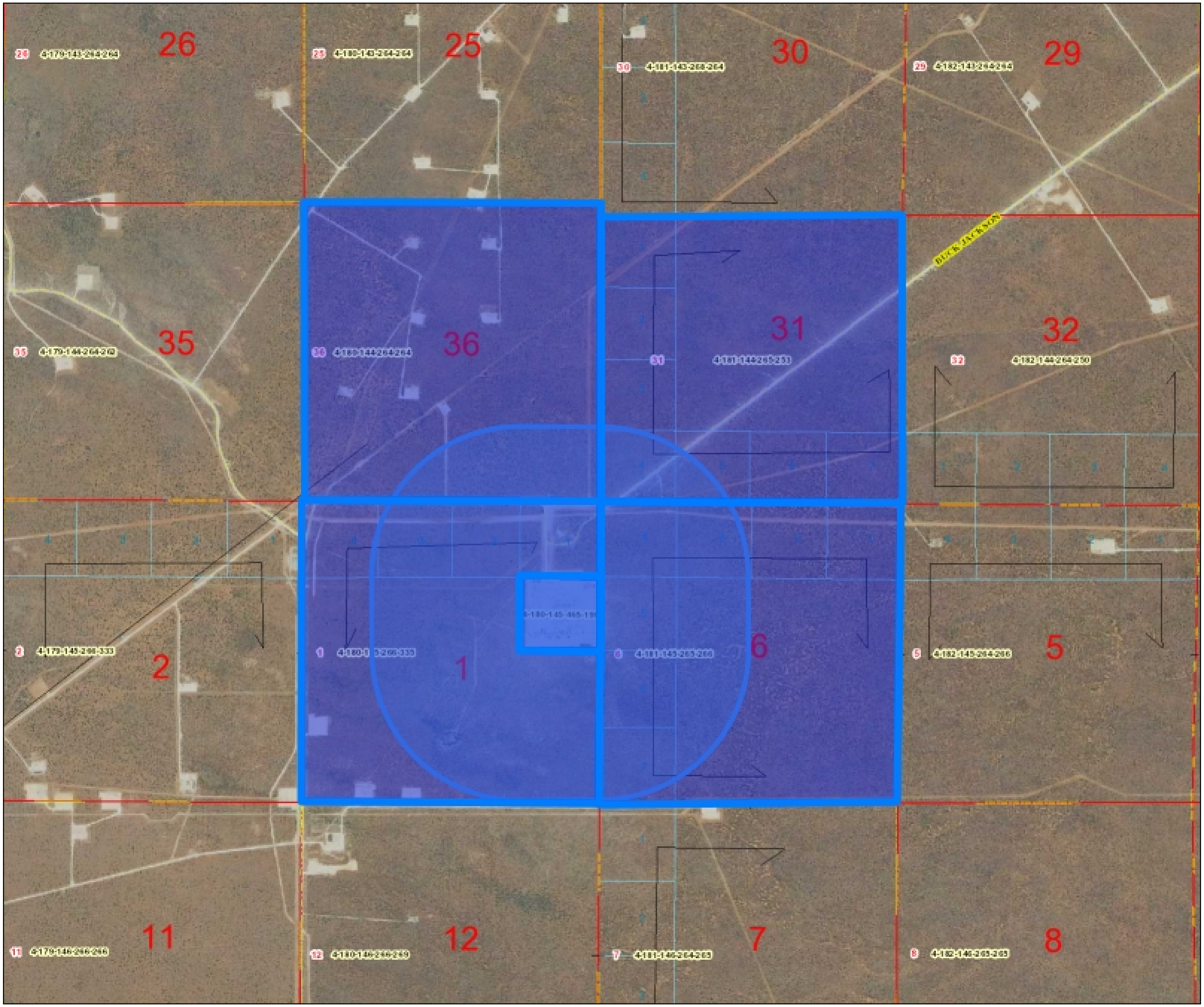
TX-GCI0405128-01

Eddy County Property Tax Map



Legend

Cartography
- <all other values>
- Govt Lot Lines
- Dimension Tic
- Leader Lines
- Misc Carto
- Owner Hooks
- Sub Corners

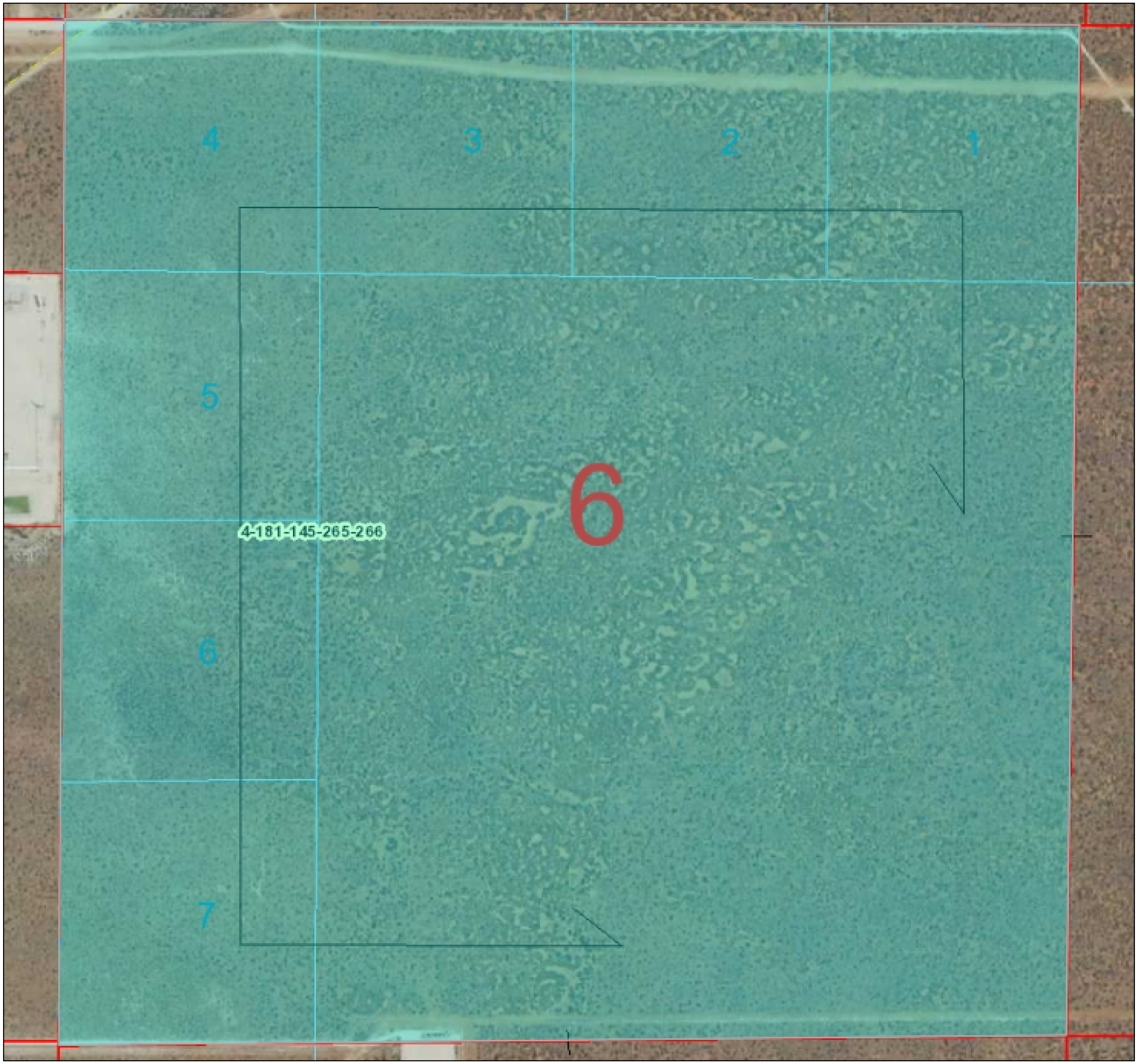
Roads
Railroads
Water
Geographic
Section
Subdivision
Parcel

XTO Energy Cowboy CDP

Web Print: 04/09/2020

0 3,009 6,019 Feet

This map is a user generated static output from an Internet mapping site and is for reference only. Data layers that appear on this map may or may not be accurate, current, or otherwise reliable.



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OWNERNAME: BUREAU OF LAND MANAGEMENT
LANDACTUAL: 2916
OBJECTID_1: 60987
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ACCOUNTNUMBER_1: R092037
SEQUENCE_R: 0
OWNER_OCCURENCE: 0
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VERSIONSTART_1: 1511265518670

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UPC_join: 4180145266335
ACCOUNTNUMBER: R051897
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OWNERNAME: BUREAU OF LAND MANAGEMENT
SITUS: 900 BUCK JACKSON ROAD
LANDACTUAL: 2700
OBJECTID_1: 27597
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ACCOUNTNUMBER_1: R051897
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TAXAREA: CO_NR
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VERSIONSTART_1: 1511239112785

OBJECTID_12_13_14: 20663
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UPC_join: 4180145465199
ACCOUNTNUMBER: R065349
LEGALSUMMARY: S: 1 T: 25S R: 30E SENE MAP# 385-1.1 LOC 810 BUCK JACKSON ROAD EXEMPT
OWNERNAME: COUNTY OF EDDY
SITUS: 810 BUCK JACKSON ROAD
LANDACTUAL: 18000
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OWNERADDRESS_STATE: NM
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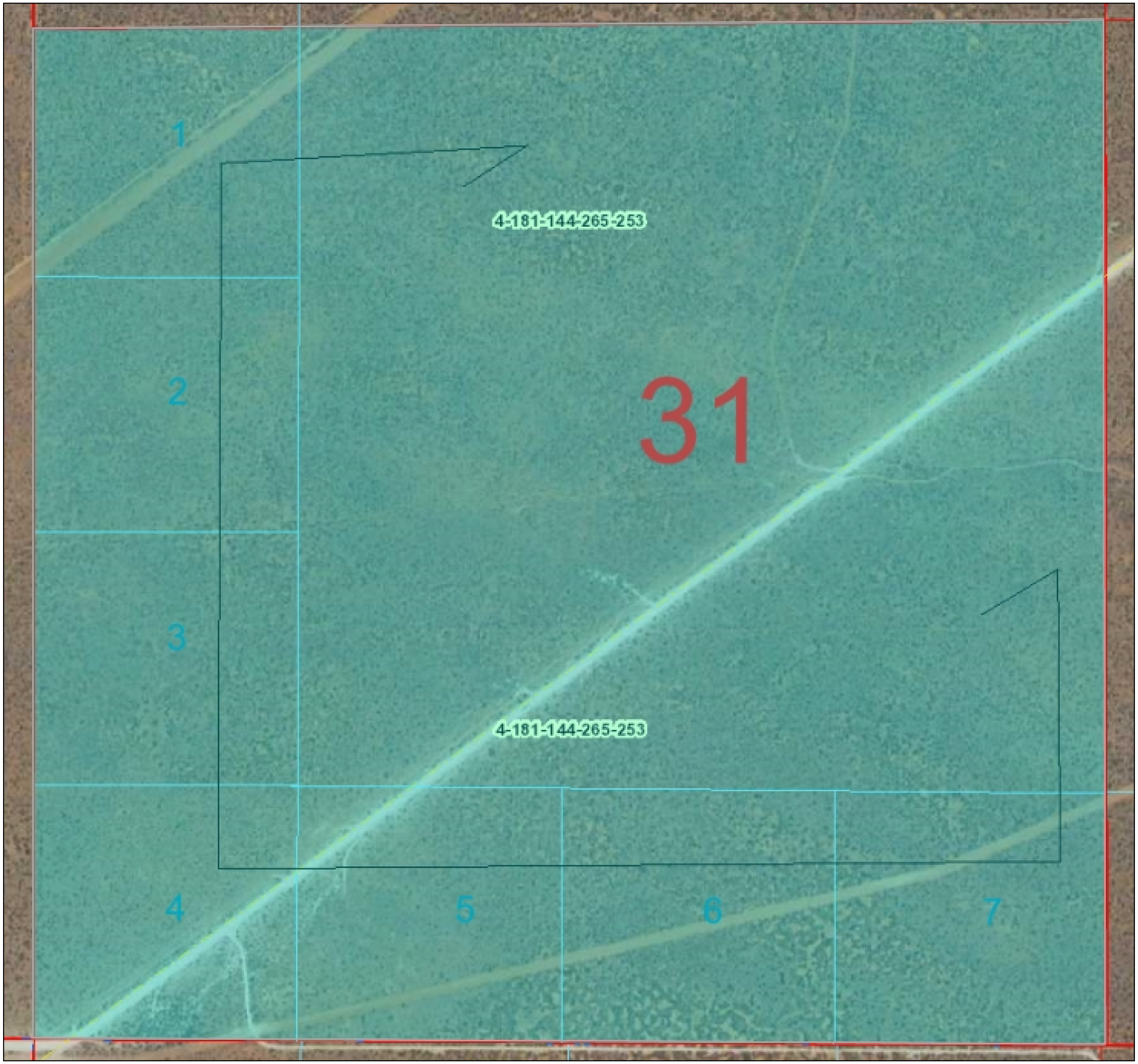

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LANDACTUAL: 2880
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TAXAREA: CO_NR
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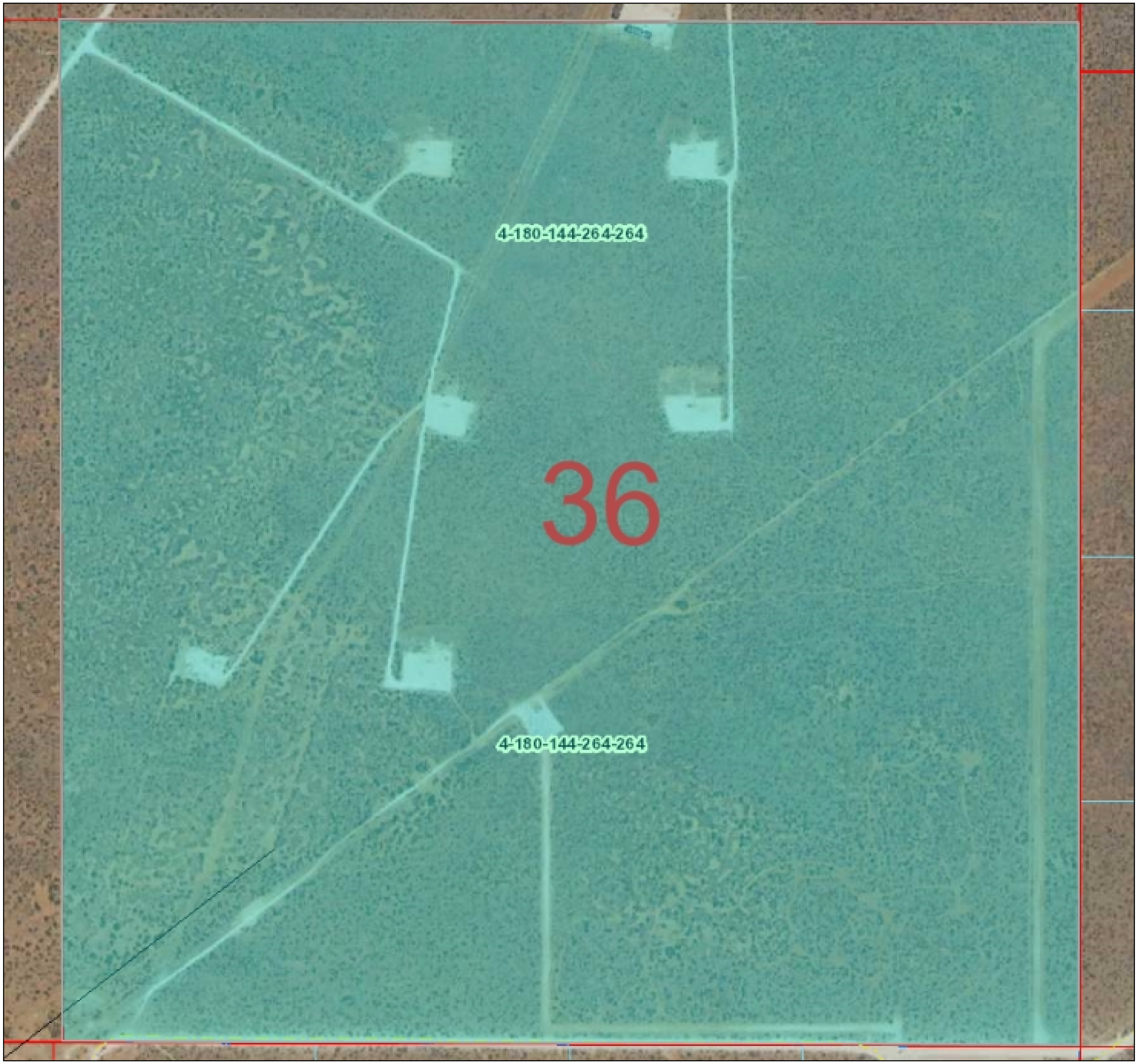
VERSIONSTART_1: 1511265495055



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LANDACTUAL: 2880
OBJECTID_1: 60280
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ACCOUNTNUMBER_1: R091436
SEQUENCE_R: 0
OWNER_OCCURENCE: 0
INTERNALID: C20160020105.1451631600000
DOCUMEN_TTYPE: Owner
ACTIVE_1: A
CONFIDENTIAL: 0
OWNERADDRESS_ADDRESS1: 310 OLD SANTA FE TRAIL
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OWNERADDRESS_STATE: NM
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TAXYEAR_12: 2019
ACCOUNTNUMBER_12: R091436
SEQUENCE_R_1: 0
INTERNALID_1: R091436.LAND2769066.1511265229098
MODEL_TYPE: Land
ACCOUNTNUMBER_12_13: R091436
ACTUALAREA: 640
LANDCODE: 149_4_5
TAXAREA: CO_NR
VERSIONEND_1: 9223372036854775807
VERSIONSTART_1: 1511265229098

Tab 10

Section 10 - Written Description of the Routine Operations of the Facility

Section 10

Written Description of the Routine Operations of the Facility

<u>A written description of the routine operations of the facility</u>. Include a description of how each piece of equipment will be operated, how controls will be used, and the fate of both the products and waste generated. For modifications and/or revisions, explain how the changes will affect the existing process. In a separate paragraph describe the major process bottlenecks that limit production. The purpose of this description is to provide sufficient information about plant operations for the permit writer to determine appropriate emission sources.

The Cowboy Central Delivery Point (CDP) is a gas processing facility with oil and NGL stabilization. The facility will produce sales gas, Y-Grade NGL, and spec oil products. The Cowboy CDP will be built over multiple phases to reach a full processing capacity of 1.0 BCFD of Natural Gas, 600,000 BPD of Oil Stabilization and 190,000 BPD of NGL Stabilization. The overall facility will be designed to accommodate four (4) cryogenic (cryo) trains.

Natural Gas System
The Cowboy CDP gas handling system will be fed by natural gas gathering lines, delivering sweet natural gas to the facility. At the inlet of the facility, these pipelines will be routed to the inlet slug catcher where condensate is separated and routed to the NGL stabilizers to produce Y-Grade NGL product. Gas from the slug catcher will feed each of the four (4) cryo trains. Each cryo train will have a dedicated amine unit (AU1-AU4) to remove CO2 and a molecular sieve dehydration unit to remove water. The gas will first be treated using MDEA and piperizine in the amine unit to remove carbon dioxide from the gas streams. In the amine regeneration unit for each train, flash gas from the amine flash tank and amine still will be routed to a thermal oxidizer (TO1-TO4) to destroy hazardous air pollutants (HAPs) and volatile organic compounds (VOCs). In the molecular sieve dehydration units, molecular sieve beds are used as to dehydrate the treated gas. The units are not point sources of emissions and therefore not included in Table 2A. In this two-unit design, one unit operates in dehydration mode while the other operates in regeneration mode. Switching from dehydration to regeneration is done by use of automatic switching valves. As the dehydrated unit becomes saturated with water vapor, it is automatically switched to regeneration mode while the regeneration unit becomes active in dehydration mode. When the beds require regeneration due to saturation, a fired regeneration gas heater (RHTR1-RHTR4) with a maximum heat input rate of 35.25 MMBtu/hr will be used to remove water from the mol sieve beds. Following dehydration, the dry gas is cooled and expanded in the cryo units before being boosted by electric drive residue compressor engines into the sales gas pipeline.

NGL System
Natural gas liquids (NGLs) are gathered from surrounding compressor stations and piped into the facility. These pipelines will be combined with the condensate dropout from the slug catcher. This combined liquid stream will be processed through a two-tower condensate stabilization system to produce a "Y-Grade" NGL and a 9 RVP stabilized spec oil. From the first stabilization tower, the overhead gas will be compressed using electric drive compressor engine and sent to the cryo trains, whereas the liquids will be sent to the second tower to produce Y-Grade NGL. The Y-Grade liquids from the second tower will be stored in pressurized bullets and pumped to the NGL sales pipeline. Any gas from the second tower is routed to the cryo trains. Note that the NGLs from the cryo trains will also be pumped to and exported via the same pipeline. The stabilized oil from the second tower will be pumped to the internal floating roof oil storage tanks (IFR1-IFR8), where it is combined with on-spec oil, then routed to the oil sales pipeline. Heat for the stabilization process is provided by eleven (11) heaters, each with a maximum heat input rate of 58.93 MMBtu/hr (SHTR1-SHTR11).

Oil System
Oil from surrounding batteries will be routed through the oil inlet surge vessel, which provides initial phase separation of oil and water. Any free water dropout will be routed through a 1,000 bbl gunbarrel separator (GBS1). From GBS1, skimmed oil will be sent to the 500 bbl slop oil tank (OTK7) and the heavier water will be sent to 750 bbl produced water tanks (PWTK1-PWTK2). All tanks are gas blanketed. Slop oil will be pumped back to oil stabilization or trucked offsite. Produced water will be transported offsite via pipeline.

Under normal circumstances, the oil received at the CDP is sent directly from the inlet surge vessel to IFR1-IFR8 for temporary storage before transporting the oil offsite via pipeline. If the incoming oil RVP does not meet sales specifications, it is sent to the oil stabilization process. Following stabilization, on-spec oil product will be sent to IFR1-IFR8. For flexibility, the inlet oil may be blended with the oil stabilization product to create desired product. Flash gas from oil stabilization will be recompressed to liquid and routed to the NGL stabilizers.

Hot Oil System
Closed-loop natural gas-fired heater hot oil systems will be used to provide process heat to the NGL and oil stabilization packages, as well as the amine and the cryo units. The systems will be packaged units with fired heating, expansion vessel, pumps, and filtration. All NGL stabilizers will be served by a common hot oil loop operating with a 500°F supply temperature. All oil stabilizers will be served by a common hot oil loop. Supply to each oil/NGL stabilizer hot oil loop will be from 58.93 MMBtu/hr burner packages (SHTR1-SHTR11) and circulation pump skids, which can be set to run at either temperature. Each Amine/Cryo train will have its own dedicated hot oil loop served by a 94.54 MMBtu/hr burner package (CHTR1-CHTR4) and pump skid with expansion vessel.

Flare System
All automated vents and process reliefs will be routed to either the low pressure or high pressure headers for the dual-tip flare system, which consists of three dual-tip flares (FL1-FL3). The flares are permitted to manage pilot, purge, and process vessel SSM gas. Any gas that must be removed from the system during an emergency would also be routed to FL1-FL3. Gas may be routed to one or all of the flares at any given time.

Combustor
A combustor (ECD1) is used collect and dispose of vapors emitted from GBS1, SOTK1, PWTK1-PWTK2, and SOTL.

Emergency Generators
The emergency generators for the CDP portion of the plant (GEN1-GEN4) will be used to power safety-sensitive equipment in the event of grid power outages.

Tab 11
Section 11 -Source Determination

Section 11

Source Determination

Source submitting under 20.2.70, 20.2.72, 20.2.73, and 20.2.74 NMAC

Sources applying for a construction permit, PSD permit, or operating permit shall evaluate surrounding and/or associated sources (including those sources directly connected to this source for business reasons) and complete this section. Responses to the following questions shall be consistent with the Air Quality Bureau's permitting guidance, Single Source Determination Guidance, which may be found on the Applications Page in the Permitting Section of the Air Quality Bureau website.

Typically, buildings, structures, installations, or facilities that have the same SIC code, that are under common ownership or control, and that are contiguous or adjacent constitute a single stationary source for 20.2.70, 20.2.72, 20.2.73, and 20.2.74 NMAC applicability purposes. Submission of your analysis of these factors in support of the responses below is optional, unless requested by NMED.

A. Identify the emission sources evaluated in this section (list and describe)**:**
See Table 2A

B. Apply the 3 criteria for determining a single source:

SIC Code: Surrounding or associated sources belong to the same 2-digit industrial grouping (2-digit SIC code) as this facility, OR surrounding or associated sources that belong to different 2-digit SIC codes are support facilities for this source.

☑ **Yes** ☐ **No**

Common Ownership or Control: Surrounding or associated sources are under common ownership or control as this source.

☐ **Yes** ☑ **No**

Contiguous or Adjacent: Surrounding or associated sources are contiguous or adjacent with this source.

☑ **Yes** ☐ **No**

C. Make a determination:

☑ The source, as described in this application, constitutes the entire source for 20.2.70, 20.2.72, 20.2.73, or 20.2.74 NMAC applicability purposes. If in "A" above you evaluated only the source that is the subject of this application, all "**YES**" boxes should be checked. If in "A" above you evaluated other sources as well, you must check **AT LEAST ONE** of the boxes "**NO**" to conclude that the source, as described in the application, is the entire source for 20.2.70, 20.2.72, 20.2.73, and 20.2.74 NMAC applicability purposes.
* ExxonMobil Pipeline Company (EMPCo) owns and will operate the Cowboy Pump Station, which is located directly adjacent to the Cowboy CDP. This source consists of electric pumps, a small solvent tank, a sump, and fugitive components. Since the site operates under a different Standard Industrial Classification and is operated by a different company, EMPCo has filed a Notice of Intent (NOI) separately from the Cowboy CDP to be operated by XTO.

☐ The source, as described in this application, **does not** constitute the entire source for 20.2.70, 20.2.72, 20.2.73, or 20.2.74 NMAC applicability purposes (A permit may be issued for a portion of a source). The entire source consists of the following facilities or emissions sources (list and describe):

Tab 12
Section 12 - PSD Applicability Determination for All Sources

Section 12

Section 12.A
PSD Applicability Determination for All Sources

(Submitting under 20.2.72, 20.2.74 NMAC)

A PSD applicability determination for all sources. For sources applying for a significant permit revision, apply the applicable requirements of 20.2.74.AG and 20.2.74.200 NMAC and to determine whether this facility is a major or minor PSD source, and whether this modification is a major or a minor PSD modification. It may be helpful to refer to the procedures for Determining the Net Emissions Change at a Source as specified by Table A-5 (Page A.45) of the EPA New Source Review Workshop Manual to determine if the revision is subject to PSD review.

A. This facility is:

- ☑ **a minor PSD source before and after this modification (if so, delete C and D below).**
- ☐ **a major PSD source before this modification. This modification will make this a PSD minor source.**
- ☐ **an existing PSD Major Source that has never had a major modification requiring a BACT analysis.**
- ☐ **an existing PSD Major Source that has had a major modification requiring a BACT analysis**
- ☑ **a new PSD Major Source after this modification. (Note: This is a proposed new site, not a modification.)**

Tab 13

Section 13 - Determination of State & Federal Air Quality Regulations

Section 13

Determination of State & Federal Air Quality Regulations

This section lists each state and federal air quality regulation that may apply to your facility and/or equipment that are stationary sources of regulated air pollutants.

Not all state and federal air quality regulations are included in this list. Go to the Code of Federal Regulations (CFR) or to the Air Quality Bureau's regulation page to see the full set of air quality regulations.

Required Information for Specific Equipment:
For regulations that apply to specific source types, in the 'Justification' column **provide any information needed to determine if the regulation does or does not apply**. **For example**, to determine if emissions standards at 40 CFR 60, Subpart IIII apply to your three identical stationary engines, we need to know the construction date as defined in that regulation; the manufacturer date; the date of reconstruction or modification, if any; if they are or are not fire pump engines; if they are or are not emergency engines as defined in that regulation; their site ratings; and the cylinder displacement.

Required Information for Regulations that Apply to the Entire Facility:
See instructions in the 'Justification' column for the information that is needed to determine if an 'Entire Facility' type of regulation applies (e.g. 20.2.70 or 20.2.73 NMAC).

Regulatory Citations for Regulations That Do Not, but Could Apply:
If there is a state or federal air quality regulation that does not apply, but you have a piece of equipment in a source category for which a regulation has been promulgated, you must **provide the low level regulatory citation showing why your piece of equipment is not subject to or exempt from the regulation. For example** if you have a stationary internal combustion engine that is not subject to 40 CFR 63, Subpart ZZZZ because it is an existing 2 stroke lean burn stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions, your citation would be 40 CFR 63.6590(b)(3)(i). **We don't want a discussion of every non-applicable regulation, but if it is possible a regulation could apply, explain why it does not. For example,** if your facility is a power plant, you do not need to include a citation to show that 40 CFR 60, Subpart OOO does not apply to your non-existent rock crusher.

Regulatory Citations for Emission Standards:
For each unit that is subject to an emission standard in a source specific regulation, such as 40 CFR 60, Subpart OOO or 40 CFR 63, Subpart HH, include the low level regulatory citation of that emission standard. Emission standards can be numerical emission limits, work practice standards, or other requirements such as maintenance. **Here are examples:** a glycol dehydrator is subject to the general standards at 63.764C(1)(i) through (iii); an engine is subject to 63.6601, Tables 2a and 2b; a crusher is subject to 60.672(b), Table 3 and all transfer points are subject to 60.672(e)(1)

Federally Enforceable Conditions:
All federal regulations are federally enforceable. All Air Quality Bureau State regulations are federally enforceable except for the following: affirmative defense portions at 20.2.7.6.B, 20.2.7.110(B)(15), 20.2.7.11 through 20.2.7.113, 20.2.7.115, and 20.2.7.116; 20.2.37; 20.2.42; 20.2.43; 20.2.62; 20.2.63; 20.2.86; 20.2.89; and 20.2.90 NMAC. Federally enforceable means that EPA can enforce the regulation as well as the Air Quality Bureau and federally enforceable regulations can count toward determining a facility's potential to emit (PTE) for the Title V, PSD, and nonattainment permit regulations.

INCLUDE ANY OTHER INFORMATION NEEDED TO COMPLETE AN APPLICABILITY DETERMINATION OR THAT IS RELEVENT TO YOUR FACILITY'S NOTICE OF INTENT OR PERMIT.

EPA Applicability Determination Index for 40 CFR 60, 61, 63, etc: http://cfpub.epa.gov/adi/

STATE REGU-LATIONS CITATION	Title	Applies? Enter Yes or No	Unit(s) or Facility	JUSTIFICATION: (You may delete instructions or statements that do not apply in the justification column to shorten the document.)
20.2.1 NMAC	General Provisions	Yes	Facility	General Provisions apply to Notice of Intent, Construction, and Title V permit applications.
20.2.3 NMAC	Ambient Air Quality Standards NMAAQS	Yes	Facility	20.2.3 NMAC is a SIP approved regulation that limits the maximum allowable concentration of Total Suspended Particulates, Sulfur Compounds, Carbon Monoxide and Nitrogen Dioxide.
20.2.7 NMAC	Excess Emissions	Yes	Facility	
20.2.23 NMAC	Fugitive Dust Control	No	N/A	**20.2.23.108 APPLICABILITY:** **B.** The following fugitive dust sources are exempt from this part: **(3)** operations issued permits pursuant to the state of New Mexico Air Quality Control Act, Mining Act or Surface Mining Act; a
20.2.33 NMAC	Gas Burning Equipment - Nitrogen Dioxide	No	N/A	None of the equipment has a heat input greater than 1,000,000 million British Thermal Units per year per unit
20.2.34 NMAC	Oil Burning Equipment: NO_2	No	N/A	None of the equipment burns oil.
20.2.35 NMAC	Natural Gas Processing Plant – Sulfur	No	N/A	This regulation is not applicable because sulfur emissions from the plant are below the applicability thresholds established in the regulation.
20.2.37 and 20.2.36 NMAC	Petroleum Processing and Petroleum Refineries	N/A	N/A	These regulations were repealed as of 9/12/2016.
20.2.38 NMAC	Hydrocarbon Storage Facility	Yes	IFR1-8 SOTK1	The tanks are subject to 109 and 112 due to throughput and storage capacity. IFR1-IFR8 are each equipped with a floating roof while SOTK1 is controlled using a combustor.
20.2.39 NMAC	Sulfur Recovery Plant – Sulfur	No	N/A	This is not an affected facility.
20.2.61.109 NMAC	Smoke & Visible Emissions	Yes	SHTR1-11, CHTR1-4, RHTR1-4, FL1-3, ECD1, TO1-4, GEN1-4	Engines, heaters, and turbines are Stationary Combustion Equipment
20.2.70 NMAC	Operating Permits	Yes	Facility	This site will be a Part 70 source.
20.2.71 NMAC	Operating Permit Fees	Yes	Facility	This site will be a Part 70 source.
20.2.72 NMAC	Construction Permits	Yes	Facility	This permit application requests a Part 72 permit.
20.2.73 NMAC	NOI & Emissions Inventory Requirements	Yes	Facility	The site is subject to inventory reporting.
20.2.74 NMAC	Permits – Prevention of Significant Deterioration (PSD)	No	N/A	The facility is not a major PSD source.
20.2.75 NMAC	Construction Permit Fees	Yes	Facility	A permit fee will be paid.

STATE REGU-LATIONS CITATION	Title	Applies? Enter Yes or No	Unit(s) or Facility	JUSTIFICATION: (You may delete instructions or statements that do not apply in the justification column to shorten the document.)
20.2.77 NMAC	New Source Performance	Yes	Units subject to 40 CFR 60	This is a stationary source subject to the requirements of 40 CFR Part 60.
20.2.78 NMAC	Emission Standards for HAPS	No	N/A	There are no affected sources.
20.2.79 NMAC	Permits – Nonattainment Areas	No	N/A	The site is not located in a nonattainment area.
20.2.80 NMAC	Stack Heights	No	N/A	This regulation establishes requirements for the evaluation of stack heights and other dispersion techniques. This regulation does not apply as all stacks at the facility follow good engineering practice.
20.2.82 NMAC	MACT Standards for source categories of HAPS	Yes	Units Subject to 40 CFR 63	This is a stationary source subject to the requirements of 40 CFR Part 63.

FEDERAL REGU-LATIONS CITATION	Title	Applies? Enter Yes or No	Unit(s) or Facility	JUSTIFICATION:
40 CFR 50	NAAQS	Yes	Facility	This regulation defines national ambient air quality standards. The facility meets all applicable national ambient air quality standards for NOx, CO, SO_2, H_2S, PM_{10}, and $PM_{2.5}$ under this regulation.
NSPS 40 CFR 60, Subpart A	General Provisions	Yes	Units subject to 40 CFR 60	See discussion of 40 CFR 60 Subparts below.
NSPS 40 CFR60.40a, Subpart Da	Subpart Da, Performance Standards for **Electric Utility Steam Units**	No	N/A	The site does not operate any affected sources.
NSPS 40 CFR60.40b Subpart Db	**Electric Utility Steam Generating Units**	No	N/A	None of the units have a heat input exceeding 100 MMBtu/hr.
40 CFR 60.40c, Subpart Dc	Standards of Performance for Small Industrial-Commercial-Institutional Steam Generating Units	Yes	SHTR1-11, RHTR1-4, CHTR1-4	The heaters have an input rating greater than 10 MMBtu/hr and are subject per §60.40c(a). Since the units burn only natural gas, there are no applicable control, monitoring, or reporting requirements. Fuel use records are required per §60.48c(g).
NSPS 40 CFR 60, Subpart Ka	**Petroleum Liquids** After May 18, 1978, and **Prior** to July 23, 1984	No	N/A	The hydrocarbons are stored prior to custody transfer.

FEDERAL REGU-LATIONS CITATION	**Title**	**Applies? Enter Yes or No**	**Unit(s) or Facility**	**JUSTIFICATION:**
NSPS 40 CFR 60, Subpart Kb	Standards for Volatile Organic Liquid Storage Vessels July 23, 1984	Yes	IFR1-IFR8	The hydrocarbons are stored prior to custody transfer but the storage volume is equal to 1,589,875 m3 so the exemption in §60.110b(d) no longer applies. The tanks use internal floating roof tanks to comply with the control requirements.
NSPS 40 CFR 60.330 Subpart GG	Stationary Gas Turbines	No	N/A	The site does not operate any affected sources.
NSPS 40 CFR 60, Subpart KKK	Leaks of VOC from Onshore Gas Plants	No	N/A	The site will be constructed after 8/23/2011.
NSPS 40 CFR Part 60 Subpart LLL	Standards of Performance for Onshore Natural Gas Processing: SO_2 Emissions	No	N/A	The site will be constructed after 8/23/2011.
NSPS 40 CFR 60, Subparts WWW, XXX, Cc, and Cf	Standards of performance for Municipal Solid Waste (MSW) Landfills	No	N/A	This is not a MSW landfill.
NSPS 40 CFR 60, Subpart KKKK	Stationary Gas Turbines	No	N/A	The site does not operate any affected sources.
NSPS 40 CFR Part 60 Subpart OOOO	Oil and Gas after August 23, 2011 and before September 18, 2015	No	N/A	The site will be constructed after 9/18/15. See NSPS OOOOa discussion below.
NSPS 40 CFR Part 60 Subpart OOOOa	Oil and Natural Gas After September 18, 2015	Yes	FUG, EOOSCOMP1-7, ECOSCOMP1-7, ERESCOMP1-18, CRYO1-4, MOL1-4	The electric drive centrifugal compressors for regen gas are exempt from §60.5365a(b) since they all use dry seals. The electric drive screw compressors for the refrigeration gas and instrument air are exempt from the definition of centrifugal compressor per §60.5430a. The reciprocating compressors used for oil stabilization gas, condensate stabilization gas and residue gas air are subject to rule per from §60.5365a(c). All storage tanks were constructed after the applicability date of the rule; however, since emissions will be limited by permit to less than 6 tpy, all tanks except IFR5-IFR 8 are exempt per §60.5365a(e). IFR5-IFR8 comply with NSPS Kb to comply with NSPS OOOOa. The site uses compressed air for pneumatic controllers. The site will be subject to leak monitoring from fugitive components per §60.5365a(f). Since the sweetening units process less than 2 lt/d of sulfur, they are exempt for §60.5365a(g).
NSPS 40 CFR 60 Subpart IIII	Stationary Compression Ignition Engines	No	N/A	The facility does not operate any affected sources.
NSPS 40 CFR Part 60 Subpart JJJJ	Stationary Spark Ignition Internal Combustion Engines	Yes (Limited)	GEN1-GEN4	The generators must meet the monitoring requirements of §60.4243(d).
NSPS 40 CFR 60 Subpart TTTT	Greenhouse Gas Emissions for Electric Generating Units	No	N/A	The facility does not operate any affected sources.
NSPS 40 CFR 60 Subpart UUUU	GHG Emissions and Compliance Times for EGUs	No	N/A	Per §60.5710a, this subpart applies to Governors of States with one or more designated facilities.

FEDERAL REGU-LATIONS **CITATION**	**Title**	**Applies? Enter Yes or No**	**Unit(s) or Facility**	**JUSTIFICATION:**
NESHAP 40 CFR 61 Subpart A	General Provisions	No	N/A	There are no affected sources.
NESHAP 40 CFR 61 Subpart E	National Emission Standards for **Mercury**	No	N/A	This facility does not process mercury ore to recover mercury, use mercury chlor-alkali cells to produce chlorine gas and alkali metal hydroxide, and incinerate or dry wastewater treatment plant sludge.
NESHAP 40 CFR 61 Subpart V	National Emission Standards for **Equipment Leaks**	No	N/A	The facility does not have equipment that operates in volatile hazardous air pollutant (VHAP) service [40 CFR Part 61.240].
MACT 40 CFR 63, Subpart A	General Provisions	Yes	Units Subject to 40 CFR 63	See discussion of 40 CFR 63 Subparts below.
MACT 40 CFR 63.760 Subpart HH	Oil and Natural Gas Production Facilities	No	N/A	As a major source of HAP, sources subject to HH include storage vessels with flash emissions, fugitive components, and compressors in VHAP service ((see §63.760(b)(1)(ii), (iii), and (iv)). Fugitives and compressors are exempt per §63.769(b) since they are subject to NSPS OOOO. Storage vessels use a closed vent system connected to a combustor to comply with §63.766(b).
MACT 40 CFR 63 Subpart HHH	Natural Gas Transmission and Storage Facilities	No	N/A	This regulation does not apply as the plant is not a natural gas transmission and storage facility as defined by the subpart (§63.1270(a)).
40 CFR 63 Subpart DDDDD	Boilers & Process Heaters	Yes	SHTR1-11, RHTR1-4, CHTR1-4	Per §63.7500(e), boilers and heaters designed to burn gas 1 fuels must comply with work practice standards in Table 3 and does not have emission or operating limits.
MACT 40 CFR 63 Subpart UUUUU	Coal & Oil Fire Electric Utility Steam Generating Unit	No	N/A	There are no affected sources.
MACT 40 CFR 63 Subpart YYYY	Turbine MACT	No	N/A	There are no affected sources.
MACT 40 CFR 63 Subpart ZZZZ	RICE MACT	Yes (Limited)	GEN1-GEN4	Per §63.6585(e), the generators must meet definition in §63.6675 and the operating limitation in §63.6640(f). No other requirements apply. The generators meet the definition of emergency stationary internal combustion engine and are exempt.
MACT 40 CFR 63 Subpart JJJJJJ	Boilers and Process Heaters	No	N/A	The units are exempt per §63.1195(e) since they burn natural gas.
40 CFR 64	CAM	Yes	AU1-4	These sources will be subject to CAM and will be addressed during the Title V permitting process.
40 CFR 68	Accident Prevention	No	N/A	The facility will not store more than the regulated quantity of regulated substances.
Acid Rain 40 CFR 72	Acid Rain	No	N/A	The facility does not generate commercial electric power.
Acid Rain 40 CFR 73	Sulfur Dioxide Allowance	No	N/A	The facility does not generate commercial electric power.
Acid Rain 40 CFR 75	CEMS	No	N/A	The facility does not generate commercial electric power
Acid Rain 40 CFR 76	Acid Rain	No	N/A	The facility does not generate commercial electric power.
Title VI – 40 CFR 82	Protection of Stratospheric Ozone	No	N/A	The regulation is not applicable per §40 CFR Part 82.1(a) because the facility does not service, maintain or repair class I or class II appliances.

Tab 14

Section 14 - Operational Plan to Mitigate Emissions

Section 14

Operational Plan to Mitigate Emissions

(Submitting under 20.2.70, 20.2.72, 20.2.74 NMAC)

☑ **Title V Sources** (20.2.70 NMAC)**:** By checking this box and certifying this application the permittee certifies that it has developed an **Operational Plan to Mitigate Emissions During Startups, Shutdowns, and Emergencies** defining the measures to be taken to mitigate source emissions during startups, shutdowns, and emergencies as required by 20.2.70.300.D.5(f) and (g) NMAC. This plan shall be kept on site to be made available to the Department upon request. This plan should not be submitted with this application.

☑ **NSR** (20.2.72 NMAC)**, PSD** (20.2.74 NMAC) **& Nonattainment** (20.2.79 NMAC) **Sources:** By checking this box and certifying this application the permittee certifies that it has developed an **Operational Plan to Mitigate Source Emissions During Malfunction, Startup, or Shutdown** defining the measures to be taken to mitigate source emissions during malfunction, startup, or shutdown as required by 20.2.72.203.A.5 NMAC. This plan shall be kept on site to be made available to the Department upon request. This plan should not be submitted with this application.

☑ **Title V** (20.2.70 NMAC)**, NSR** (20.2.72 NMAC)**, PSD** (20.2.74 NMAC) **& Nonattainment** (20.2.79 NMAC) **Sources:** By checking this box and certifying this application the permittee certifies that it has established and implemented a Plan to Minimize Emissions During Routine or Predictable Startup, Shutdown, and Scheduled Maintenance through work practice standards and good air pollution control practices as required by 20.2.7.14.A and B NMAC. This plan shall be kept on site or at the nearest field office to be made available to the Department upon request. This plan should not be submitted with this application.

XTO Energy maintains written procedures to mitigate emissions during startups, shutdowns, and emergencies. In the event of a malfunction, startup, shutdown, or scheduled maintenance in which emission rates from the facility exceed permitted allowable emission rates, XTO Energy will notify the AQB in accordance with 20.2.7 NMAC and the equipment responsible for the exceedance will be repaired as soon as possible.

Tab 15
Section 15 - Alternative Operating Scenarios

Section 15

Alternative Operating Scenarios

(Submitting under 20.2.70, 20.2.72, 20.2.74 NMAC)

Alternative Operating Scenarios: Provide all information required by the department to define alternative operating scenarios. This includes process, material and product changes; facility emissions information; air pollution control equipment requirements; any applicable requirements; monitoring, recordkeeping, and reporting requirements; and compliance certification requirements. Please ensure applicable Tables in this application are clearly marked to show alternative operating scenario.

Construction Scenarios: When a permit is modified authorizing new construction to an existing facility, NMED includes a condition to clearly address which permit condition(s) (from the previous permit and the new permit) govern during the interval between the date of issuance of the modification permit and the completion of construction of the modification(s). There are many possible variables that need to be addressed such as: Is simultaneous operation of the old and new units permitted and, if so for example, for how long and under what restraints? In general, these types of requirements will be addressed in Section A100 of the permit, but additional requirements may be added elsewhere. Look in A100 of our NSR and/or TV permit template for sample language dealing with these requirements. Find these permit templates at: https://www.env.nm.gov/aqb/permit/aqb_pol.html. Compliance with standards must be maintained during construction, which should not usually be a problem unless simultaneous operation of old and new equipment is requested.

In this section, under the bolded title "Construction Scenarios", specify any information necessary to write these conditions, such as: conservative-realistic estimated time for completion of construction of the various units, whether simultaneous operation of old and new units is being requested (and, if so, modeled), whether the old units will be removed or decommissioned, any PSD ramifications, any temporary limits requested during phased construction, whether any increase in emissions is being requested as SSM emissions or will instead be handled as a separate Construction Scenario (with corresponding emission limits and conditions, etc.

There are no alternate operating scenarios proposed for the Cowboy CDP.

Tab 16
Section 16 - Air Dispersion Modeling

Section 16

Air Dispersion Modeling

1) Minor Source Construction (20.2.72 NMAC) and Prevention of Significant Deterioration (PSD) (20.2.74 NMAC) ambient impact analysis (modeling): Provide an ambient impact analysis as required at 20.2.72.203.A(4) and/or 20.2.74.303 NMAC and as outlined in the Air Quality Bureau's Dispersion Modeling Guidelines found on the Planning Section's modeling website. If air dispersion modeling has been waived for one or more pollutants, attach the AQB Modeling Section modeling waiver approval documentation.
2) SSM Modeling: Applicants must conduct dispersion modeling for the total short term emissions during routine or predictable startup, shutdown, or maintenance (SSM) using realistic worst case scenarios following guidance from the Air Quality Bureau's dispersion modeling section. Refer to "Guidance for Submittal of Startup, Shutdown, Maintenance Emissions in Permit Applications (http://www.env.nm.gov/aqb/permit/app_form.html) for more detailed instructions on SSM emissions modeling requirements.
3) Title V (20.2.70 NMAC) ambient impact analysis: Title V applications must specify the construction permit and/or Title V Permit number(s) for which air quality dispersion modeling was last approved. Facilities that have only a Title V permit, such as landfills and air curtain incinerators, are subject to the same modeling required for preconstruction permits required by 20.2.72 and 20.2.74 NMAC.

What is the purpose of this application?	Enter an X for each purpose that applies
New PSD major source or PSD major modification (20.2.74 NMAC). See #1 above.	
New Minor Source or significant permit revision under 20.2.72 NMAC (20.2.72.219.D NMAC). See #1 above. **Note:** Neither modeling nor a modeling waiver is required for VOC emissions.	X
Reporting existing pollutants that were not previously reported.	
Reporting existing pollutants where the ambient impact is being addressed for the first time.	
Title V application (new, renewal, significant, or minor modification. 20.2.70 NMAC). See #3 above.	
Relocation (20.2.72.202.B.4 or 72.202.D.3.c NMAC)	
Minor Source Technical Permit Revision 20.2.72.219.B.1.d.vi NMAC for like-kind unit replacements.	
Other: i.e. SSM modeling. See #2 above.	
This application does not require modeling since this is a No Permit Required (NPR) application.	
This application does not require modeling since this is a Notice of Intent (NOI) application (20.2.73 NMAC).	
This application does not require modeling according to 20.2.70.7.E(11), 20.2.72.203.A(4), 20.2.74.303, 20.2.79.109.D NMAC and in accordance with the Air Quality Bureau's Modeling Guidelines.	

Check each box that applies:

☐ See attached, approved modeling **waiver for all** pollutants from the facility.
☐ See attached, approved modeling **waiver for some** pollutants from the facility.
☑ Attached in Universal Application Form 4 (UA4) is a **modeling report for all** pollutants from the facility.
☐ Attached in UA4 is a **modeling report for some** pollutants from the facility.
☐ No modeling is required.

Tab 17
Section 17 - Compliance Test History

Section 17

Compliance Test History

(Submitting under 20.2.70, 20.2.72, 20.2.74 NMAC)

To show compliance with existing NSR permits conditions, you must submit a compliance test history. The table below provides an example.

This is a proposed facility. There is no history of compliance testing.

Tab 18

Section 18 - Addendum for Streamline Applications

(Not Applicable)

Section 18

Addendum for Streamline Applications

Do not print this section unless this is a streamline application.

Streamline Applications do not require a complete application. Submit Sections 1-A, 1-B, 1-D, 1-F, 1-G, 2-A, 2-C thru L, Sections 3 thru 8, Section 13, Section 18, Section 22, and Section 23 (Certification). Other sections may be required at the discretion of the Department. 20.2.72.202 NMAC Exemptions do not apply to Streamline sources. 20.2.72.219 NMAC revisions and modifications do not apply to Streamline sources, thus 20.2.72.219 type actions require a complete new application submittal. Please do not print sections of a streamline application that are not required.

This section is not applicable since this is not a Streamline Permit Application.

Tab 19
Section 19 - Requirements for Title V Program

Section 19

Requirements for Title V Program

Do not print this section unless this is a Title V application.

<u>Who Must Use this Attachment</u>:

* Any major source as defined in 20.2.70 NMAC.
* Any source, including an area source, subject to a standard or other requirement promulgated under Section 111 - Standards of Performance for New Stationary Sources, or Section 112 Hazardous Air Pollutants, of the 1990 federal Clean Air Act ("federal Act"). Non-major sources subject to Sections 111 or 112 of the federal Act are exempt from the obligation to obtain an 20.2.70 NMAC operating permit until such time that the EPA Administrator completes rulemakings that require such sources to obtain operating permits. In addition, sources that would be required to obtain an operating permit solely because they are subject to regulations or requirements under Section 112(r) of the federal Act are exempt from the requirement to obtain an Operating Permit.
* Any Acid Rain source as defined under title IV of the federal Act. The Acid Rain program has additional forms. See http://www.env.nm.gov/aqb/index.html. Sources that are subject to both the Title V and Acid Rain regulations are encouraged to submit both applications simultaneously.
* Any source in a source category designated by the EPA Administrator ("Administrator"), in whole or in part, by regulation, after notice and comment.

This is not a Title V application.

Tab 20
Section 20 - Other Relevant Information

Section 20

Other Relevant Information

Other relevant information. Use this attachment to clarify any part in the application that you think needs explaining. Reference the section, table, column, and/or field. Include any additional text, tables, calculations or clarifying information.

Additionally, the applicant may propose specific permit language for AQB consideration. In the case of a revision to an existing permit, the applicant should provide the old language and the new language in track changes format to highlight the proposed changes. If proposing language for a new facility or language for a new unit, submit the proposed operating condition(s), along with the associated monitoring, recordkeeping, and reporting conditions. In either case, please limit the proposed language to the affected portion of the permit.

No other relevant information is provided.

Tab 21

Section 21 - Addendum for Landfill Applications

(Not Applicable)

Section 21

Addendum for Landfill Applications

Do not print this section unless this is a landfill application.

Landfill Applications are not required to complete Sections 1-C Input Capacity and Production Rate, 1-E Operating Schedule, 17 Compliance Test History, and 18 Streamline Applications. Section 12 – PSD Applicability is required only for Landfills with Gas Collection and Control Systems and/or landfills with other non-fugitive stationary sources of air emissions such as engines, turbines, boilers, heaters. All other Sections of the Universal Application Form are required.

EPA Background Information for MSW Landfill Air Quality Regulations:
https://www3.epa.gov/airtoxics/landfill/landflpg.html

NM Solid Waste Bureau Website: https://www.env.nm.gov/swb/

This is not a landfill.

Tab 22
Section 22 - Certification

Section 22: Certification

Company Name: PEI on behalf XTO Energy Inc.

I, Evan Tullos , hereby certify that the information and data submitted in this application are true and as accurate as possible, to the best of my knowledge and professional expertise and experience.

Signed this 24th day of April , 2020 , upon my oath or affirmation, before a notary of the State of Illinois.

*Signature

4.24.20
Date

Evan Tullos
Printed Name

Vice President
Title

Scribed and sworn before me on this 24th day of April , 2020 .

My authorization as a notary of the State of Illinois expires on the 2nd day of August, 2020 .

Notary's Signature

4/24/2020
Date

Mark Reed
Notary's Printed Name

MARK L. REED
OFFICIAL SEAL
Notary Public, State of Illinois
My Commission Expires
August 02, 2020

*For Title V applications, the signature must be of the Responsible Official as defined in 20.2.70.7.AE NMAC.

Tab 23
Section 23 - UA4

Universal Application 4

Air Dispersion Modeling Report

Refer to and complete Section 16 of the Universal Application form (UA3) to assist your determination as to whether modeling is required. If, after filling out Section 16, you are still unsure if modeling is required, e-mail the completed Section 16 to the AQB Modeling Manager for assistance in making this determination. If modeling is required, a modeling protocol would be submitted and approved prior to an application submittal. The protocol should be emailed to the modeling manager. A protocol is recommended but optional for minor sources and is required for new PSD sources or PSD major modifications. Fill out and submit this portion of the Universal Application form (UA4), the "Air Dispersion Modeling Report", only if air dispersion modeling is required for this application submittal. This serves as your modeling report submittal and should contain all the information needed to describe the modeling. No other modeling report or modeling protocol should be submitted with this permit application.

16-A: Identification		
1	Name of facility:	Cowboy CDP
2	Name of company:	XTO Energy Inc.
3	Current Permit number:	7877
4	Name of applicant's modeler:	Bruce Ferguson
5	Phone number of modeler:	601-824-1860
6	E-mail of modeler:	bferguson@fce-engineering.com

16-B: Brief			
1	Was a modeling protocol submitted and approved?	Yes☐	No☒
2	Why is the modeling being done?	Adding New Equipment	
3	Describe the permit changes relevant to the modeling.		
4	What geodetic datum was used in the modeling?	NAD83	
5	How long will the facility be at this location?	Indefinite	
6	Is the facility a major source with respect to Prevention of Significant Deterioration (PSD)?	Yes☐	No☒
7	Identify the Air Quality Control Region (AQCR) in which the facility is located	155	

16-B: Brief

8	List the PSD baseline dates for this region (minor or major, as appropriate).	
	NO_2	3/16/1988
	SO_2	7/28/1978
	PM_{10}	2/20/1979
	$PM_{2.5}$	11/13/2013
9	Provide the name and distance to Class I areas within 50 km of the facility (300 km for PSD permits).	
	Carlsbad Caverns NP, 50 km	

10	Is the facility located in a non-attainment area? If so describe below	Yes☐	No☒
11	Describe any special modeling requirements, such as streamline permit requirements.		

16-C: Modeling History of Facility

1 Describe the modeling history of the facility, including the air permit numbers, the pollutants modeled, the National Ambient Air Quality Standards (NAAQS), New Mexico AAQS (NMAAQS), and PSD increments modeled. (Do not include modeling waivers).

Pollutant	Latest permit and modification number that modeled the pollutant facility-wide.	Date of Permit	Comments
CO	7877	10/2/2018	
NO_2	7877	10/2/2018	
SO_2			
H_2S			
PM2.5	7877	10/2/2018	
PM10	7877	10/2/2018	
TSP	7877	10/2/2018	
Lead			
Ozone (PSD only)			
NM Toxic Air Pollutants (20.2.72.402 NMAC)			

16-D: Modeling performed for this application

1	For each pollutant, indicate the modeling performed and submitted with this application. Choose the most complicated modeling applicable for that pollutant, i.e., culpability analysis assumes ROI and cumulative analysis were also performed.					
	Pollutant	ROI	Cumulative analysis	Culpability analysis	Waiver approved	Pollutant not emitted or not changed.
	CO	☒	☐	☐	☐	☐
	NO_2	☒	☒	☐	☐	☐
	SO_2	☒	☒	☐	☐	☐
	H_2S	☐	☐	☐	☐	☒
	PM2.5	☒	☒	☒	☐	☐
	PM10	☒	☒	☐	☐	☐
	TSP	☐	☐	☐	☐	☐
	Lead	☐	☐	☐	☐	☒
	Ozone*	☐	☐	☐	☐	☐
	State air toxic(s) (20.2.72.402 NMAC)	☐	☐	☐	☐	☒

***Ozone and Volatile Organic Compound (VOC) emissions do not currently require a modeling analysis for a PSD minor source.**

16-E: New Mexico toxic air pollutants modeling

1	List any New Mexico toxic air pollutants (NMTAPs) from Tables A and B in 20.2.72.502 NMAC that are modeled for this application. None					
2	List any NMTAPs that are emitted but not modeled because stack height correction factor. Add additional rows to the table below, if required.					
	Pollutant	Emission Rate (pounds/hour)	Emission Rate Screening Level (pounds/hour)	Stack Height (meters)	Correction Factor	Emission Rate/ Correction Factor

16-F: Modeling options

1	Was the latest version of AERMOD used with regulatory default options? If not explain below.	Yes☒	No☐

16-G: Surrounding source modeling		
1	Date of surrounding source retrieval	December 6, 2019
2	If the surrounding source inventory provided by the Air Quality Bureau was believed to be inaccurate, describe how the sources modeled differ from the inventory provided. If changes to the surrounding source inventory were made, use the table below to describe them. Add rows as needed.	
	AQB Source ID	Description of Corrections
	>10 km	Sources greater than 10 km having a source ID less than 10,000 were removed from the model.
	34514A1 (10042)	Haul Road $PM_{2.5}$ emissions were changed from 0.091 lb/hr in the provided inventory to 0.053 lb/hr to correspond to the December 2018 application
	39069E3 (10164)	Flare $PM_{2.5}$ emissions were changed from 19.65 lb/hr, reflecting SSM emissions, to 0.002 lb/hr, reflecting normal operation as the diameter provided would not correspond to the effective diameter
	34582E3 (10170)	Flare $PM_{2.5}$ emissions were changed from 4.76 lb/hr, reflecting SSM emissions, to 0.002 lb/hr, reflecting normal operation as the diameter provided would not correspond to the effective diameter.
	39045E3 (10230)	Flare $PM_{2.5}$ emissions were changed from 19.65 lb/hr, reflecting SSM emissions, to 0.002 lb/hr, reflecting normal operation as the diameter provided would not correspond to the effective diameter.
	39068C1 (10291)	Flare $PM_{2.5}$ emissions were changed from 19.65 lb/hr, reflecting SSM emissions, to 0.002 lb/hr, reflecting normal operation as the diameter provided would not correspond to the effective diameter.
	39111E4 (10306)	Flare $PM_{2.5}$ emissions were changed from 19.01 lb/hr, reflecting SSM emissions, to 0.002 lb/hr, reflecting normal operation as the diameter provided would not correspond to the effective diameter.
	38927R3 (10365)	The emissions for the source are duplicative of 38927R2 (10374), so the source was removed.

16-H: Building and structure downwash				
1	How many buildings are present at the facility?	2		
2	How many above ground storage tanks are present at the facility?	12		
3	Was building downwash modeled for all buildings and tanks? If not explain why below.		Yes☒	No☐
4	Building comments	In addition to the buildings and tanks the emission point structures were entered into the BPIP program		

16-I: Receptors and modeled property boundary

1	"Restricted Area" is an area to which public entry is effectively precluded. Effective barriers include continuous fencing, continuous walls, or other continuous barriers approved by the Department, such as rugged physical terrain with a steep grade that would require special equipment to traverse. If a large property is completely enclosed by fencing, a restricted area within the property may be identified with signage only. Public roads cannot be part of a Restricted Area. A Restricted Area is required in order to exclude receptors from the facility property. If the facility does not have a Restricted Area, then receptors shall be placed within the property boundaries of the facility. Describe the fence or other physical barrier at the facility that defines the restricted area.		
	The facility contains continuous fencing to preclude public access.		
2	Receptors must be placed along publicly accessible roads in the restricted area. Are there public roads passing through the restricted area?	Yes☐	No☒
3	Are restricted area boundary coordinates included in the modeling files?	Yes☒	No☐

4 Describe the receptor grids and their spacing. The table below may be used, adding rows as needed.

Grid Type	Shape	Spacing	Start distance from center of facility	End distance from center of facility	Comments
Cartesian	Circle	50 m	0	1 km	
Cartesian	Circle	100 m	1 km	3 km	
Cartesian	Circle	250 m	3 km	6 km	
Cartesian	Circle	500 m	6 km	10 km	
Cartesian	Circle	1,000 m	10 km	50 km	

5 Describe receptor spacing along the fence line.

50 meter

6 Describe the PSD Class I area receptors.

The facility is almost exactly 50 km from the Class I. A 50 km grid at 1,000 meter spacing was used. The radius of impact above the Class I SILs was determined as follows:

NO_2 Annual increment (0.1 ug/m^3) 37.712 km
$PM_{2.5}$ 24-hr increment (0.27 ug/m^3) 16.305 km
$PM_{2.5}$ Annual increment (0.05 ug/m^3) 12.624 km
PM_{10} 24-hr increment (0.3 ug/m^3) 15.934 km
PM_{10} Annual increment (0.2 ug/m^3) 2.974 km
SO_2 3-hr increment (1.0 ug/m^3) 15.222 km
SO_2 24-hr increment (0.2 ug/m^3) 15.222 km
SO_2 Annual increment (0.1 ug/m^3) 2.837 km

All of the impacts fall below the Class I significant impact levels well before the 50 km distance to the Class I area.

16-J: Sensitive areas

1	Are there schools or hospitals or other sensitive areas near the facility? If so describe below. This information is optional (and purposely undefined) but may help determine issues related to public notice.	Yes☐	No☒
3	The modeling review process may need to be accelerated if there is a public hearing. Are there likely to be public comments opposing the permit application?	Yes☐	No☒

16-K: Modeling Scenarios

1	Identify, define, and describe all modeling scenarios. Examples of modeling scenarios include using different production rates, times of day, times of year, simultaneous or alternate operation of old and new equipment during transition periods, etc. Alternative operating scenarios should correspond to all parts of the Universal Application and should be fully described in Section 15 of the Universal Application (UA3).		
	In addition to modeling emissions as presented on Tab 2-E, because the SSM flaring OVHD and CRYO will not occur at the same time, the SSM events were evaluated individually with the gas split between two flares.		
2	Which scenario produces the highest concentrations? Why?		
	All the flaring events evaluated produced essentially the same results, indicating that the maximum impacts are not controlled by the flaring. The scenario as presented on tab 2-E was used in cumulative analyses.		
3	Were emission factor sets used to limit emission rates or hours of operation? (This question pertains to the "SEASON", "MONTH", "HROFDY" and related factor sets, not to the factors used for calculating the maximum emission rate.)	Yes☐	No☒
4	If so, describe factors for each group of sources. List the sources in each group before the factor table for that group. (Modify or duplicate table as necessary. It's ok to put the table below section 16-K if it makes formatting easier.) Sources:		

5

Hour of Day	Factor	Hour of Day	Factor								
1		13									
2		14									
3		15									
4		16									
5		17									
6		18									
7		19									
8		20									
9		21									
10		22									
11		23									
12		24									

If hourly, variable emission rates were used that were not described above, describe them below.

6	Were different emission rates used for short-term and annual modeling? If so describe below.	Yes☐	No☒

16-L: NO_2 Modeling

1	Which types of NO_2 modeling were used? Check all that apply.	
	☒	ARM2
	☐	100% NO_X to NO_2 conversion
	☐	PVMRM
	☐	OLM
	☐	Other:

2	Describe the NO_2 modeling.		
	The modeling assumed full conversion of NOx to NO_2 for modeling with source groups for flaring scenarios. For the flaring scenario producing the highest results, the model was rerun using the ARM2 and only the scenario producing the highest results in the initial modeling..		
3	Were default NO_2/NO_X ratios (0.5 minimum, 0.9 maximum or equilibrium) used? If not describe and justify the ratios used below.	Yes☒	No☐
4	Describe the design value used for each averaging period modeled.		
	1-hour: High eighth high Annual: One Year Annual Average		

16-M: Particulate Matter Modeling

1	Select the pollutants for which plume depletion modeling was used.	
	☐	PM2.5
	☐	PM10
	☒	None
2	Describe the particle size distributions used. Include the source of information.	

3	Does the facility emit at least 40 tons per year of NO_X or at least 40 tons per year of SO_2? Sources that emit at least 40 tons per year of NO_X or at least 40 tons per year of SO_2 are considered to emit significant amounts of precursors and must account for secondary formation of $PM_{2.5}$.	Yes☒	No☐
4	Was secondary PM modeled for PM2.5?	Yes☐	No☒

5	If MERPs were used to account for secondary $PM_{2.5}$ fill out the information below. If another method was used describe below.			
	NO_X (ton/yr)	SO_2 (ton/yr)	$[PM2.5]_{annual}$	$[PM2.5]_{24\text{-hour}}$
	181.2	27.5	0.014	0.335
	$[PM_{2.5}]_{annual} = ((181.2/3184) + (27.5/2289)) \times 0.2\ \mu g/m^3 = 0.014$ $[PM_{2.5}]_{24\text{-hour}} = ((181.2/1155) + (27.5/225)) \times 1.2\ \mu g/m^3 = 0.335$			

16-N: Setback Distances

1	Portable sources or sources that need flexibility in their site configuration requires that setback distances be determined between the emission sources and the restricted area boundary (e.g. fence line) for both the initial location and future locations. Describe the setback distances for the initial location.	
2	Describe the requested, modeled, setback distances for future locations, if this permit is for a portable stationary source. Include a haul road in the relocation modeling.	

16-O: PSD Increment and Source IDs

1	The unit numbers in the Tables 2-A, 2-B, 2-C, 2-E, 2-F, and 2-I should match the ones in the modeling files. Do these match? If not, provide a cross-reference table between unit numbers if they do not match below.	Yes☒	No☐
	Unit Number in UA-2	Unit Number in Modeling Files	
2	The emission rates in the Tables 2-E and 2-F should match the ones in the modeling files. Do these match? If not, explain why below.	Yes☒	No☐
3	Have the minor NSR exempt sources or Title V Insignificant Activities" (Table 2-B) sources been modeled?	Yes☐	No☒
4	Which units consume increment for which pollutants?		

Unit ID	NO_2	SO_2	PM_{10}	$PM_{2.5}$
SHTR1 – SHTR11	x	x	x	x
CHTR1 – CHTR4	x	x	x	x
RHTR3 – RHTR4	x	x	x	x
FL1 – FL3	x		x	x
ECD1	x	x	x	x
TO1 – TO4	x	x	x	x
ROAD			x	x
GEN1 – GEN4	x	x	x	x

5	PSD increment description for sources. (for unusual cases, i.e., baseline unit expanded emissions after baseline date).			
6	Are all the actual installation dates included in Table 2A of the application form, as required? This is necessary to verify the accuracy of PSD increment modeling. If not please explain how increment consumption status is determined for the missing installation dates below.		Yes☒	No☐

16-P: Flare Modeling

1	For each flare or flaring scenario, complete the following			
	Flare ID (and scenario)	Average Molecular Weight	Gross Heat Release (cal/s)	Effective Flare Diameter (m)
	FL1 (2E)	20.99	160,397,086	11.186
	FL2 (2E)	46.08	83,993,483	7.525
	FL3 (2E)	18.43	349,045	0.526
	FL1 (Cryo)	20.99	80,198,543	7.91
	FL2 (Cryo)	20.99	80,198,543	7.91
	FL3 (Cryo)	18.43	349,045	0.526
	FL1(OVHD)	46.08	41,996,741	5.321
	FL2 (OVHD)	46.08	41,996,741	5.321
	FL3 (OVHD)	18.43	349,045	0.526

16-Q: Volume and Related Sources

1	Were the dimensions of volume sources different from standard dimensions in the Air Quality Bureau (AQB) Modeling Guidelines? If not please explain how increment consumption status is determined for the missing installation dates below.	Yes☐	No☒
2	Describe the determination of sigma-Y and sigma-Z for fugitive sources.		
3	Describe how the volume sources are related to unit numbers. Or say they are the same.		
4	Describe any open pits.		
5	Describe emission units included in each open pit.		

16-R: Background Concentrations

1	Were NMED provided background concentrations used? Identify the background station used below. If non-NMED provided background concentrations were used describe the data that was used.	Yes☒	No☐
	CO: Del Norte High School (350010023)		
	NO_2: Outside Carlsbad (350151005)		
	PM2.5: Hobbs-Jefferson (350450019)		
	PM10: Hobbs-Jefferson (350250008)		
	SO_2: Amarillo (483751025)		
	Other:		
	Comments:		
2	Were background concentrations refined to monthly or hourly values? If so describe below.	Yes☐	No☒

16-S: Meteorological Data

1	Was NMED provided meteorological data used? If so select the station used. Artesia	Yes☒	No☐
2	If NMED provided meteorological data was not used describe the data set(s) used below. Discuss how missing data were handled, how stability class was determined, and how the data were processed.		

16-T: Terrain

1	Was complex terrain used in the modeling? If not, describe why below.	Yes☒	No☐
2	What was the source of the terrain data?		
	NED data through http://www.webgis.com/, downloaded through the Lakes Environmental GUI.		

16-U: Modeling Files

1	Describe the modeling files:		
	File name (or folder and file name)	Pollutant(s)	Purpose (ROI/SIA, cumulative, culpability analysis, other)
	CO\CO.ADI, *.ADO, *.SUM (input/output)	CO	ROI and worst flare impacts
	CO\CO.AD*.plt, Format - [xx][Hx][Gxxx] [xx] indicates avg period - 1,3,24, An [Hx] indicates rank – H1, H2, etc. [Gxxx] indicates source group G001 – "2E" G002 – "OVHD" G003 – "CRYO"		
	NOx\NOx.ADI, *.ADO	NOx	Worst flare impacts full conversion to NO2
	NOx\NOx.AD*.plt (as noted above)		
	PM10\PM10.ADI, *.ADO, *.SUM	PM10	ROI and worst flare impacts
	PM10\PM10.AD*.plt (as noted above)		
	PM25\PM25.ADI, *.ADO, *.SUM	PM2.5	ROI and worst flare impacts
	PM25\PM25.AD*.plt (as noted above)		
	SO2\SO2.ADI, *.ADO, *.SUM	SO2	ROI
	SO2\SO2.AD*.plt (as noted above except the only source group is ALL)		
	NO2\NO2.ADI, *.ADO, *.SUM	NO2	ROI and Cumulative Impact using ARM2
	NO2\NO2.AD*.plot (as noted above except the only source group is "2E")		
	Surrounding Sources\		
	\PM10\PM10.ADI, *.ADO, *.SUM	PM10	Cumulative Impact Analysis
	\PM10\PM10.AD*.PLT (as noted above except that G001 –"SROUND") G002 – "PSD")		
	\PM25\PM25.ADI, *.ADO, *.SUM	PM2.5	Cumulative Impact
	\PM25\PM25.AD*.PLT (as discussed above except that G001 – SROUND G002 – PSD G003 – SEDDY G004 – XTO)		
	PSD.DAT	PM2.5	PM2.5 Culpability
	\PM25_offsite*.ADI, *.ADO, *.SUM	PM2.5	Cumulative Impact
	\PM25_offsite\PM25_offsite.AD*.PLT (as discussed above)		
	\SO2*.ADI, *.ADO, *.SUM	SO2	Cumulative Increment Impact
	\SO2\SO2.PLT (as discussed above)		

16-V: PSD New or Major Modification Applications			
1	A new PSD major source or a major modification to an existing PSD major source requires additional analysis. Was preconstruction monitoring done (see 20.2.74.306 NMAC and PSD Preapplication Guidance on the AQB website)?	Yes☐	No☐
2	If not, did AQB approve an exemption from preconstruction monitoring?	Yes☐	No☐
3	Describe how preconstruction monitoring has been addressed or attach the approved preconstruction monitoring or monitoring exemption.		
4	Describe the additional impacts analysis required at 20.2.74.304 NMAC.		
5	If required, have ozone and secondary PM2.5 ambient impacts analyses been completed? If so describe below.	Yes☐	No☐

16-W: Modeling Results

1	If ambient standards are exceeded because of surrounding sources, a culpability analysis is required for the source to show that the contribution from this source is less than the significance levels for the specific pollutant. Was culpability analysis performed? If so describe below.	Yes☒	No☐
	The South Eddy Cryo Plant is located near the XTO – Cowboy CDP site and is within the significant receptor grid from the preliminary analysis (ROI). Exceedances of the PM2.5 24-hr increment were identified around the South Eddy Cryo Plant sources. There was only one exceedance where the XTO – Cowboy CDP sources contributed above the significance level. The location of the exceedance was in the middle of the South Eddy Cryo Plant property. A facility cannot cause or contribute to a violation within its restricted boundary. When the contribution from the South Eddy Cryo Plant was removed, there was no exceedance. The model was rerun after removing the receptors within the fence line of the South Eddy Cryo Plant and placing receptors at 50 meters along the fence line. Additionally, the South Eddy Cryo Plant sources were moved to the locations indicated in the application on the NMED website (RS20712_Application 5945M5), page 29 of 229. All modeled concentrations were then found to be below the PSD increment.		
2	Identify the maximum concentrations from the modeling analysis. Rows may be modified, added and removed from the table below as necessary.		

Pollutant, Time Period and Standard	Modeled Facility Concentration (μg/m3)	Modeled Concentration with Surrounding	Secondary PM (μg/m3)	Background Concentration (μg/m3)	Cumulative Concentration (μg/m3)	Value of Standard (μg/m3)	Percent of Standard	Location		
								UTM E (m)	UTM N (m)	Elevation (ft)
NO_2 1-hr NAAQS	113.06545	N/A		38.7	151.76545	188.03	80.7	609600.00	3558500.00	1030.63
NO_2 Annual NMAAQS	5.45798	N/A		5.0	10.56266	94.02	11.2	609500.00	3559200.00	1041.41
NO2 Annual Increment	5.45798	N/A		5.0	10.56266	25	42.3	609500.00	3559200.00	1041.41
CO 1-hr NMAAQS	366.01442	N/A		2203	2569.01442	14,997.5	17.1	609603.00	3558584.60	1032.82
CO 8-hr NMAAQS	260.60929	N/A		1524	1784.60929	9,960.1	17.9	609650.00	3558550.00	1030.98
SO_2 1-hr NAAQS	24.72282	N/A		47.0	71.72282	196.4	36.5	609700.00	3559100.00	1041.64
SO_2 3-hr SIL	19.38053	N/A		N/A	19.38053	25	77.5	609700.00	3559100.00	1041.64
SO_2 24-hr Increment	5.66998	N/A		N/A	5.66998	91	6.2	609450.00	3559250.00	1041.00
SO_2 Annual Increment	1.87711	N/A		N/A	1.87711	20	9.4	609500.00	3559200.00	1041.41
PM_{10} 24-hr NAAQS	7.98132*	10.96062		37.3	48.26062	150	32.1	609450.00	3559100.00	1040.69
PM_{10} 24-hr Increment	7.98132*	9.18430		N/A	9.18430	30	30.6	609450.00	3559150.00	1040.88
PM_{10} Annual Increment	1.73385	3.36222		N/A	3.36222	17	19.8	609500.00	3559200.00	1041.41
$PM_{2.5}$ 24-hr NAAQS	5.48455	6.43647	0.335	13.4	20.17147	35	57.6	609700.00	3559100.00	1041.64
$PM_{2.5}$ 24-hr Increment	0.01231	7.92173	0.335	N/A	8.25673	9	91.7	610541.95	3558752.69	1035.38
$PM_{2.5}$ Annual NAAQS	1.72899	2.75494	0.014	5.9	8.66894	12	72.2	609500.00	3559200.00	1041.41
$PM_{2.5}$ Annual Increment	1.72899	2.74495	0.014	N/A	2.75895	4	69.0	609500.00	3559200.00	1041.41

***maximum from ROI modeling**

16-X: Summary/conclusions	
	A statement that modeling requirements have been satisfied and that the permit can be issued.
1	Modeling was performed using the maximum emission presented in the application following the New Mexico Air Quality Bureau Air Dispersion Modeling Guidelines Revised June 6, 2019. The ambient air quality impacts resulting from the facility are incompliance with the ambient air quality standards; NAAQS, NMAAQS and PSD increment. The facility will not cause or contribute to an exceedance of the ambient air quality standards and the permit can be issued.

Tab 24

Confidential PVT Fluid Study & HYSYS Model