

August 31, 2020

Kirby Olson New Mexico Environment Department Air Quality Bureau 525 Camino de los Marquez, Suite 1 Santa Fe, New Mexico, 87505

RE: Application for NSR Modification Bulldog Compressor Station NSR Permit No. 8153 XTO Energy Inc.

Dear Ms. Olson:

XTO Energy Inc. is submitting the attached New Source Review permit application for the referenced facility. A detailed list of proposed changes are included in Section 3 of the application. Also included is a check for the filing fee. The electronic files will be provided via email or secure transfer. Please contact me at 832-624-2768 or benjamin_schneider@xtoenergy.com should you have any questions.

Sincerely,

Schule Buy

Benjamin Schneider, P.E. Environmental Engineer

BULLDOG COMPRESSOR STATION Eddy County, NM NSR Permit Modification Application



PREPARED BY: BEN SCHNEIDER ENVIRONMENTAL ENGINEER XTO ENERGY INC. 8/31/2020

BULLDOG COMPRESSOR STATION

NSR Permit Modification Application

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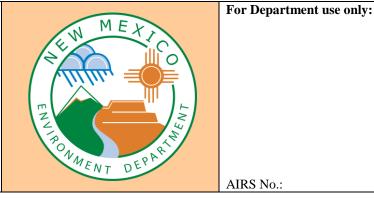
Tab 1

UA1 Form - Company and Facility Information

Mail Application To:

New Mexico Environment Department Air Ouality Bureau Permits Section 525 Camino de los Marquez, Suite 1 Santa Fe, New Mexico, 87505

Phone: (505) 476-4300 Fax: (505) 476-4375 www.env.nm.gov/aqb



AIRS No.:

Universal Air Quality Permit Application

Use this application for NOI, NSR, or Title V sources.

Use this application for: the initial application, modifications, technical revisions, and renewals. For technical revisions, complete Sections, 1-A, 1-B, 2-E, 3, 9 and any other sections that are relevant to the requested action; coordination with the Air Quality Bureau permit staff prior to submittal is encouraged to clarify submittal requirements and to determine if more or less than these sections of the application are needed. Use this application for streamline permits as well. See Section 1-I for submittal instructions for other permits.

This application is submitted as (check all that apply):
□ Request for a No Permit Required Determination (no fee)

Updating an application currently under NMED review. Include this page and all pages that are being updated (no fee required). Construction Status:
□ Not Constructed Existing Permitted (or NOI) Facility Existing Non-permitted (or NOI) Facility ☑ 20.2.72 NMAC application or revision □ 20.2.72.300 NMAC Streamline application Minor Source: a NOI 20.2.73 NMAC Title V Source: Title V (new) Title V renewal TV minor mod. TV significant mod. TV Acid Rain: New Renewal □ minor modification to a PSD source PSD Major Source:
□ PSD major source (new) □ a PSD major modification

Acknowledgements:

🗹 I acknowledge that a pre-application meeting is available to me upon request. 🗆 Title V Operating, Title IV Acid Rain, and NPR applications have no fees.

🗹 \$500 NSR application Filing Fee enclosed OR 🗆 The full permit fee associated with 10 fee points (required w/ streamline applications).

☑ Check No.: 2500132873 in the amount of \$500

I acknowledge the required submittal format for the hard copy application is printed double sided 'head-to-toe', 2-hole punched (except the Sect. 2 landscape tables is printed 'head-to-head'), numbered tab separators. Incl. a copy of the check on a separate page. □ This facility qualifies to receive assistance from the Small Business Environmental Assistance program (SBEAP) and qualifies for 50% of the normal application and permit fees. Enclosed is a check for 50% of the normal application fee which will be verified with the Small Business Certification Form for your company.

This facility qualifies to receive assistance from the Small Business Environmental Assistance Program (SBEAP) but does not qualify for 50% of the normal application and permit fees. To see if you qualify for SBEAP assistance and for the small business certification form go to https://www.env.nm.gov/aqb/sbap/small_business_criteria.html).

Citation: Please provide the **low level citation** under which this application is being submitted: **20.2.72.219.B.1.d NMAC** (e.g. application for a new minor source would be 20.2.72.200.A NMAC, one example for a Technical Permit Revision is 20.2.72.219.B.1.b NMAC, a Title V acid rain application would be: 20.2.70.200.C NMAC)

Section 1 – Facility Information

Sec	tion 1-A: Company Information	AI # if known (see 1st3 to 5 #s of permitIDEA ID No.): 38798Permit/NOI #: 8153			
1	Facility Name: Bulldog Compressor Station	Plant primary SIC Code (4 digits): 1311			
1		Plant NAIC code (6 digits): 211120			
a	a Facility Street Address (If no facility street address, provide directions from a prominent landmark): See 1-D.4.				
2	Plant Operator Company Name: XTO Energy Inc. Phone/Fax: (832) 624-4426				
a	a Plant Operator Address: 22777 Springwoods Village Parkway, W4.6B.374, Spring, TX 77389				
b	Plant Operator's New Mexico Corporate ID or Tax ID: 1522747				

3	Plant Operator Company Name: XTO Energy Inc.	Phone/Fax: (832) 624-4426			
a	Plant Owner(s) Mailing Address(s): 22777 Springwoods Village Parkway,	W4.6B.374, Spring, TX 77389			
4	Bill To (Company): XTO Energy Inc.	Phone/Fax: (832) 624-4426			
a	Mailing Address: 22777 Springwoods Village Parkway, W4.6B.374, Spring, TX 77389	E-mail: Benjamin_Schneider@xtoenergy.com			
5	☑ Preparer: Benjamin_Schneider@xtoenergy.com □ Consultant:	Phone/Fax: (832) 624-2768			
a	Mailing Address: 22777 Springwoods Village Parkway, W4.6B.374, Spring, TX 77389	E-mail: Benjamin_Schneider@xtoenergy.com			
6	Plant Operator Contact: Benjamin Schneider	Phone/Fax: (832) 624-2768			
a	Mailing Address: 22777 Springwoods Village Parkway, W4.6B.374, Spring, TX 77389	E-mail: Benjamin_Schneider@xtoenergy.com			
7	Air Permit Contact: Benjamin Schneider	Title: Environmental Engineer			
a	E-mail: Benjamin_Schneider@xtoenergy.com Phone/Fax: (832) 624-2768				
b	Mailing Address: 22777 Springwoods Village Parkway, W4.6B.374, Spring, TX 77389				
c	The designated Air permit Contact will receive all official correspondence (i.e. letters, permits) from the Air Quality Bureau.				

Section 1-B: Current Facility Status

1.a	Has this facility already been constructed? \blacksquare Yes \Box No	1.b If yes to question 1.a, is it currently operating in New Mexico?
2	If yes to question 1.a, was the existing facility subject to a Notice of Intent (NOI) (20.2.73 NMAC) before submittal of this application? □ Yes ☑ No	If yes to question 1.a, was the existing facility subject to a construction permit (20.2.72 NMAC) before submittal of this application? ✓ Yes □ No
3	Is the facility currently shut down? \Box Yes $\mathbf{\nabla}$ No	If yes, give month and year of shut down (MM/YY):
4	Was this facility constructed before 8/31/1972 and continuously operated s	since 1972? □ Yes ☑ No
5	If Yes to question 3, has this facility been modified (see 20.2.72.7.P NMA) \Box Yes \Box No \Box N/A	C) or the capacity increased since 8/31/1972?
6	Does this facility have a Title V operating permit (20.2.70 NMAC)? □ Yes ☑ No	If yes, the permit No. is: P-
7	Has this facility been issued a No Permit Required (NPR)? □ Yes ☑ No	If yes, the NPR No. is:
8	Has this facility been issued a Notice of Intent (NOI)?	If yes, the NOI No. is:
9	Does this facility have a construction permit (20.2.72/20.2.74 NMAC)? ☑ Yes □ No	If yes, the permit No. is: 8153
10	Is this facility registered under a General permit (GCP-1, GCP-2, etc.)? □ Yes ☑ No	If yes, the register No. is:

Section 1-C: Facility Input Capacity & Production Rate

1	What is the facility's maximum input capacity, specify units (reference here and list capacities in Section 20, if more room is required)						
a	a Current Hourly: 22.5 barrels; 8.8 MMscf Daily: 539.0 barrels; 210.1 MMscf Annually: 196,750 barrels; 76.7 Bs						
b	b Proposed Hourly: 33.9 barrels; 10 MMscf Daily: 814 barrels; 240 MMscf Annually: 297,184 barrels; 87.6 Bscf						
2	What is the facility's maximum production rate, specify units (reference here and list capacities in Section 20, if more room is required)						
a	a Current Hourly: 22.5 barrels; 8.8 MMscf Daily: 539.0 barrels; 210.1 MMscf Annually: 196,750 barrels; 76.7 Bscf						
b	b Proposed Hourly: 33.9 barrels; 10 MMscf Daily: 814 barrels; 240 MMscf Annually: 297,184 barrels; 87.6 Bsc						

Section 1-D: Facility Location Information

		acinty Loca		1				
1	Section: 22	Range: 31E	Township: 20S	County: E	Eddy		Elevatio	n (ft): 3500
2	UTM Zone:	□ 12 or ☑ 13		Datum:	□ NAD 27	□ NAD 8	3 🗹	WGS 84
a	UTM E (in meter	rs, to nearest 10 meter	s): 607470	UTM N (i	n meters, to neares	t 10 meters): 3	3602719	
b	AND Latitude	(deg., min., sec.):	32° 33' 24"	Longitude	e (deg., min., se	ec.): -103° 5	1' 19"	
3	Name and zip o	code of nearest Ne	ew Mexico town: Carlsbad	- 88220				
4		ng Instructions fro ve 1.8 mi. to L tur	om nearest NM town (attach n to site.	n a road ma	p if necessary):	Drive E on	NM 62 1	for 24.7 mi. to L on
5	The facility is 2	22 (distance) mile	s NE (direction) of Carlsba	d (nearest t	own).			
6	(specify)	•	one): 🗆 Private 🗆 Indian/Pu					
7	on which the f	acility is propose	ribes, and counties within ed to be constructed or op	erated: Ec	ldy County, Le	a County		
8	20.2.72 NMAC applications only : Will the property on which the facility is proposed to be constructed or operated be closer than 50 km (31 miles) to other states, Bernalillo County, or a Class I area (see <u>www.env.nm.gov/aqb/modeling/class1areas.html</u>)? □ Yes ☑ No (20.2.72.206.A.7 NMAC) If yes, list all with corresponding distances in kilometers:							
9	Name nearest (Class I area: Carls	bad Caverns					
10	Shortest distan	ce (in km) from fa	acility boundary to the bour	ndary of the	nearest Class	I area (to the	nearest 10 1	meters): 63.81
11	Distance (meters) from the perimeter of the Area of Operations (AO is defined as the plant site inclusive of all disturbed lands, including mining overburden removal areas) to nearest residence, school or occupied structure: <2 miles							
12	Method(s) used to delineate the Restricted Area: None " Restricted Area " is an area to which public entry is effectively precluded. Effective barriers include continuous fencing, continuous walls, or other continuous barriers approved by the Department, such as rugged physical terrain with steep grade that would require special equipment to traverse. If a large property is completely enclosed by fencing, a restricted area within the property may be identified with signage only. Public roads cannot be part of a Restricted Area.							
13	Does the owner/operator intend to operate this source as a portable stationary source as defined in 20.2.72.7.X NMAC? \Box Yes \blacksquare No A portable stationary source is not a mobile source, such as an automobile, but a source that can be installed permanently at one location or that can be re-installed at various locations, such as a hot mix asphalt plant that is moved to different job sites.							
14			unction with other air regulanit number (if known) of th	-	-	operty?	🛛 No	D Yes

Section 1-E: Proposed Operating Schedule (The 1-E.1 & 1-E.2 operating schedules may become conditions in the permit.)

1	Facility maximum operating $\left(\frac{\text{hours}}{\text{day}}\right)$: 24	(<u>days</u>): 7	$\left(\frac{\text{weeks}}{\text{year}}\right)$: 52	$(\frac{\text{hours}}{\text{year}})$: 8760		
2	Facility's maximum daily operating schedule (if less	s than $24 \frac{\text{hours}}{\text{day}}$)? Start:	□AM □PM	End:	□AM □PM	
3	3 Month and year of anticipated start of construction: Already started					
4	4 Month and year of anticipated construction completion: Train 1 completed July 7, 2020					
5	Month and year of anticipated startup of new or mod	dified facility: Train 1 complet	ed July 7, 202	0		
6	Will this facility operate at this site for more than or	ne year? 🗹 Yes 🗆 No				

Section 1-F: Other Facility Information

	Are there any current Notice of Violations (NOV), compliance orders, or any other compliance or enforcement issues related to this facility? \Box Yes \mathbf{V} No If yes, specify:			
а	If yes, NOV date or description of issue:	NOV Tracking No:		

b	Is this application in response to any issue listed in 1-F, 1 or 1a above? \Box Yes \Box No If Yes, provide the 1c & 1d info below:					
с	Document Title:	Date:	Requirement # (or page # and paragraph #):			
d	Provide the required text to be inserted in this permit:					
2	Is air quality dispersion modeling or modeling waiver being	g submitted with this	application? 🗹 Yes 🗆 No			
3	Does this facility require an "Air Toxics" permit under 20.2	2.72.400 NMAC & 20	0.2.72.502, Tables A and/or B? □ Yes Vo			
4	Will this facility be a source of federal Hazardous Air Pollu	utants (HAP)? 🗹 Yes	3 🗆 No			
а	If Yes, what type of source? \square Major ($\square \ge 10$ tpy of any single HAPOR $\square \ge 25$ tpy of any combination of HAPS)OR \square Minor ($\square < 10$ tpy of any single HAPAND $\square < 25$ tpy of any combination of HAPS)					
5	Is any unit exempt under 20.2.72.202.B.3 NMAC? □ Yes ☑ No					
	If yes, include the name of company providing commercial electric power to the facility:					
а	Commercial power is purchased from a commercial utility company, which specifically does not include power generated on site for the sole purpose of the user.					

Section 1-G: Streamline Application

(This section applies to 20.2.72.300 NMAC Streamline applications only)

1 □ I have filled out Section 18, "Addendum for Streamline Applications." ☑ N/A (This is not a Streamline application.)

Section 1-H: Current Title V Information - Required for all applications from TV Sources

(Title V-source required information for all applications submitted pursuant to 20.2.72 NMAC (Minor Construction Permits), or 20.2.74/20.2.79 NMAC (Major PSD/NNSR applications), and/or 20.2.70 NMAC (Title V))

1	Responsible Official (R.O.) (20.2.70.300.D.2 NMAC):		Phone:		
а	R.O. Title:	R.O. e-mail:			
b	R. O. Address:				
2	Alternate Responsible Official (20.2.70.300.D.2 NMAC):		Phone:		
а	A. R.O. Title:	A. R.O. e-mail:			
b	A. R. O. Address:				
3	Company's Corporate or Partnership Relationship to any other Air Quality Permittee (List the names of any companies that have operating (20.2.70 NMAC) permits and with whom the applicant for this permit has a corporate or partnership relationship):				
4	Name of Parent Company ("Parent Company" means the primary r permitted wholly or in part.):	ame of the organiza	tion that owns the company to be		
a	Address of Parent Company:				
5	Names of Subsidiary Companies ("Subsidiary Companies" means organizations, branches, divisions or subsidiaries, which are owned, wholly or in part, by the company to be permitted.):				
6	Telephone numbers & names of the owners' agents and site contacts familiar with plant operations:				
7	Affected Programs to include Other States, local air pollution contr Will the property on which the facility is proposed to be constructe states, local pollution control programs, and Indian tribes and pueb ones and provide the distances in kilometers:	d or operated be clos	ser than 80 km (50 miles) from other		

Section 1-I – Submittal Requirements

Each 20.2.73 NMAC (**NOI**), a 20.2.70 NMAC (**Title V**), a 20.2.72 NMAC (**NSR** minor source), or 20.2.74 NMAC (**PSD**) application package shall consist of the following:

Hard Copy Submittal Requirements:

- One hard copy original signed and notarized application package printed double sided 'head-to-toe' <u>2-hole punched</u> as we bind the document on top, not on the side; except Section 2 (landscape tables), which should be head-to-head. Please use numbered tab separators in the hard copy submittal(s) as this facilitates the review process. For NOI submittals only, hard copies of UA1, Tables 2A, 2D & 2F, Section 3 and the signed Certification Page are required. Please include a copy of the check on a separate page.
- 2) If the application is for a minor NSR, PSD, NNSR, or Title V application, include one working hard copy for Department use. This copy should be printed in book form, 3-hole punched, and must be double sided. Note that this is in addition to the head-toto 2-hole punched copy required in 1) above. Minor NSR Technical Permit revisions (20.2.72.219.B NMAC) only need to fill out Sections 1-A, 1-B, 3, and should fill out those portions of other Section(s) relevant to the technical permit revision. TV Minor Modifications need only fill out Sections 1-A, 1-B, 1-H, 3, and those portions of other Section(s) relevant to the minor modification. NMED may require additional portions of the application to be submitted, as needed.
- 3) The entire NOI or Permit application package, including the full modeling study, should be submitted electronically. Electronic files for applications for NOIs, any type of General Construction Permit (GCP), or technical revisions to NSRs must be submitted with compact disk (CD) or digital versatile disc (DVD). For these permit application submittals, two CD copies are required (in sleeves, not crystal cases, please), with additional CD copies as specified below. NOI applications require only a single CD submittal. Electronic files for other New Source Review (construction) permits/permit modifications or Title V permits/permit modifications can be submitted on CD/DVD or sent through AQB's secure file transfer service.

Electronic files sent by (check one):

□ CD/DVD attached to paper application

Z secure electronic transfer. Air Permit Contact Name Benjamin Schneider

Email benjamin_schneider@xtoenergy.com

Phone number (832) 624-2768

a. If the file transfer service is chosen by the applicant, after receipt of the application, the Bureau will email the applicant with instructions for submitting the electronic files through a secure file transfer service. Submission of the electronic files through the file transfer service needs to be completed within 3 business days after the invitation is received, so the applicant should ensure that the files are ready when sending the hard copy of the application. The applicant will not need a password to complete the transfer. **Do not use the file transfer service for NOIs, any type of GCP, or technical revisions to NSR permits.**

- 4) Optionally, the applicant may submit the files with the application on compact disk (CD) or digital versatile disc (DVD) following the instructions above and the instructions in 5 for applications subject to PSD review.
- 5) If air dispersion modeling is required by the application type, include the NMED Modeling Waiver and/or electronic air dispersion modeling report, input, and output files. The dispersion modeling <u>summary report only</u> should be submitted as hard copy(ies) unless otherwise indicated by the Bureau.
- 6) If the applicant submits the electronic files on CD and the application is subject to PSD review under 20.2.74 NMAC (PSD) or NNSR under 20.2.79 NMC include,
 - a. one additional CD copy for US EPA,
 - b. one additional CD copy for each federal land manager affected (NPS, USFS, FWS, USDI) and,
 - c. one additional CD copy for each affected regulatory agency other than the Air Quality Bureau.

If the application is submitted electronically through the secure file transfer service, these extra CDs do not need to be submitted.

Electronic Submittal Requirements [in addition to the required hard copy(ies)]:

- 1) All required electronic documents shall be submitted as 2 separate CDs or submitted through the AQB secure file transfer service. Submit a single PDF document of the entire application as submitted and the individual documents comprising the application.
- 2) The documents should also be submitted in Microsoft Office compatible file format (Word, Excel, etc.) allowing us to access the text and formulas in the documents (copy & paste). Any documents that cannot be submitted in a Microsoft Office compatible format shall be saved as a PDF file from within the electronic document that created the file. If you are unable to provide

Microsoft office compatible electronic files or internally generated PDF files of files (items that were not created electronically: i.e. brochures, maps, graphics, etc,), submit these items in hard copy format. We must be able to review the formulas and inputs that calculated the emissions.

- 3) It is preferred that this application form be submitted as 4 electronic files (3 MSWord docs: Universal Application section 1 [UA1], Universal Application section 3-19 [UA3], and Universal Application 4, the modeling report [UA4]) and 1 Excel file of the tables (Universal Application section 2 [UA2]). Please include as many of the 3-19 Sections as practical in a single MS Word electronic document. Create separate electronic file(s) if a single file becomes too large or if portions must be saved in a file format other than MS Word.
- 4) The electronic file names shall be a maximum of 25 characters long (including spaces, if any). The format of the electronic Universal Application shall be in the format: "A-3423-FacilityName". The "A" distinguishes the file as an application submittal, as opposed to other documents the Department itself puts into the database. Thus, all electronic application submittals should begin with "A-". Modifications to existing facilities should use the core permit number (i.e. '3423') the Department assigned to the facility as the next 4 digits. Use 'XXXX' for new facility applications. The format of any separate electronic submittals (additional submittals such as non-Word attachments, re-submittals, application updates) and Section document shall be in the format: "A-3423-9-description", where "9" stands for the section # (in this case Section 9-Public Notice). Please refrain, as much as possible, from submitting any scanned documents as this file format is extremely large, which uses up too much storage capacity in our database. Please take the time to fill out the header information throughout all submittals as this will identify any loose pages, including the Application Date (date submitted) & Revision number (0 for original, 1, 2, etc.; which will help keep track of subsequent partial update(s) to the original submittal. Do not use special symbols (#, @, etc.) in file names. The footer information should not be modified by the applicant.

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- Section 11: Source Determination
- Section 12: PSD Applicability Determination for All Sources & Special Requirements for a PSD Application
- Section 13: Discussion Demonstrating Compliance with Each Applicable State & Federal Regulation
- Section 14: Operational Plan to Mitigate Emissions
- Section 15: Alternative Operating Scenarios
- Section 16: Air Dispersion Modeling
- Section 17: Compliance Test History
- Section 18: Addendum for Streamline Applications (streamline applications only)
- Section 19: Requirements for the Title V (20.2.70 NMAC) Program (Title V applications only)
- Section 20: Other Relevant Information
- Section 21: Addendum for Landfill Applications
- Section 22: Certification Page

Tab 2 UA2 Form - Application Tables

Cross reference	e table of all	units in	both permits
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Previous Unit Number	Previous Source Description	New Unit Number	New Source Description	Notes
ENG1	Natural Gas Engine	ENG1	Natural Gas Compressor Engine	
ENG2	Natural Gas Engine	ENG2	Natural Gas Compressor Engine	Updated Caterpillar Gas Engine Rating Pr
ENG3	Natural Gas Engine	ENG3	Natural Gas Compressor Engine	(GERP) analysis with new fuel gas
ENG4	Natural Gas Engine	ENG4	Natural Gas Compressor Engine	analysis, which resulted in changes to
ENG5	Natural Gas Engine	ENG5	Natural Gas Compressor Engine	VOC/CO/formaldehyde emission factors.
ENG6	Natural Gas Engine	ENG6	Natural Gas Compressor Engine	Updated catalyst control efficiencies with
ENG7	Natural Gas Engine	ENG7	Natural Gas Compressor Engine	updated fuel gas specifications.
ENG8	Natural Gas Engine	ENG8	Natural Gas Compressor Engine	
ENG9	Natural Gas Engine	ENG9	Natural Gas Compressor Engine	
ENG10	Natural Gas Engine		· · ·	Removed
ENG11	Natural Gas Engine	ENG11	Natural Gas Compressor Engine	Same as ENG1-9.
ENG12	Natural Gas Engine	ENG12	Natural Gas Compressor Engine	Same as ENG1-9.
ENG13	Natural Gas Engine		· · ·	Removed
HTR1	Hot Oil Heater 1	HTR1	Fuel Line Heater	
HTR2	Hot Oil Heater 2			Removed
HTR3	Hot Oil Heater 3			Removed
RB1	Glycol Regenerator Reboiler	RB1	Glycol Regenerator Reboiler	
RB2	Glycol Regenerator Reboiler	RB2	Glycol Regenerator Reboiler	
RB3	Glycol Regenerator Reboiler	RB3	Glycol Regenerator Reboiler	
FL1	Flare 1	FL1	Flare 1	Changed combustion sources
FL2	Flare 2	FL2	Flare 2	Changed combustion sources
FL3	Flare 3			Removed
VC1	Combustor	VC1	Combustor	Changed combustion sources
GB1a	Gun Barrel Separator (Primary)	SKT1	Skim Tank	Renamed
GB1b	Gun Barrel Separator (Backup)	SKT2	Skim Tank (Backup)	Renamed
OT1	Condensate Tank	OT1	Condensate Tank	
OT2	Condensate Tank	OT2	Condensate Tank	
OT3	Condensate Tank	OT3	Condensate Tank	
OT4	Condensate Tank	OT4	Condensate Tank	
WT1	Produced Water Tank	WT1	Produced Water Tank	
WT2	Produced Water Tank	WT2	Produced Water Tank	
		VRU1	Low Pressure Separator VRU #1	Added control efficiency
		VRU2	Low Pressure Separator VRU Backup	Added control efficiency
DEHY1	TEG Dehydrator with Condenser	DEHY1	TEG Dehydrator with Condenser	, , , , , , , , , , , , , , , , , , ,
DEHY2	TEG Dehydrator with Condenser	DEHY2	TEG Dehydrator with Condenser	
DEHY3	TEG Dehydrator with Condenser	DEHY3	TEG Dehydrator with Condenser	
LPS	Low Pressure Separator	LPS	Low Pressure Separator	
LOAD	Truck Loading	LOAD	Condensate Truck Loading	
FUG	Fugitives	FUG	Fugitive Emissions	
SSM	SSM Activities	SSM	SSM Activities	
ROAD	HAUL ROAD EMISSIONS	ROAD	HAUL ROAD EMISSIONS	1

Unit numbers must correspond to unit numbers in the previous permit unless a complete cross reference table of all units in both permits

Table 2-A: Regulated Emission Sources

Unit and stack numbering must correspond throughout the application package. Equipment exemptions under 2.72.202 NMAC do not apply to 20.2.73 NMAC. Identify process equipment that is used to reroute emissions back into the process or sales pipeline in Table 2-A, such as a VRU, VRT, ULPS, Flashing Vessel, or Blowcase.

luolo 2 11, suoli	as a VRU, VRI, ULPS, Flashing	vessel, or blowease.					Date of Manufacture ²	Controlled by Unit #	Source		RICE Ignition	
Unit Number ¹	Source Description	Make	Model #	Serial #	Manufact-urer's Rated Capacity ³ (Specify Units)	Requested Permitted Capacity ³ (Specify Units)	Date of Construction/ Reconstruction ²	Emissions vented to Stack #	Classi- fication Code (SCC)	For Each Piece of Equipment, Check One	Type (CI, SI, 4SLB, 4SRB, 2SLB) ⁴	Replacing Unit No.
ENG1	Natural Gas Compressor Engine	Caterpillar	G3616	ZZY00890	5000	5000	1/1/2019	ENG1	20200254	 Existing (unchanged) To be Removed New/Additional Replacement Unit 	4SLB	N/A
ENGO	Natural Gas Compressor		62/1/	7771/0000	5000	5000	1/1/2019 2/1/2019	CAT1 ENG2		■ To Be Modified □ To be Replaced □ Existing (unchanged) □ To be Removed	451.0	N7/4
ENG2	Engine	Caterpillar	G3616	ZZY00986	5000	5000	2/1/2019	CAT2	20200254	New/Additional Replacement Unit To Be Modified To be Replaced	4SLB	N/A
ENG3	Natural Gas Compressor Engine	Caterpillar	G3616	ZZY00829	5000	5000	8/1/2018 8/1/2018	ENG3 CAT3	20200254	 □ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit ■ To Be Modified □ To be Replaced 	4SLB	N/A
ENG4	Natural Gas Compressor Engine	Caterpillar	G3616	TBD	5000	5000	TBD TBD	ENG4 CAT4	20200254	Existing (unchanged) To be Removed New/Additional Replacement Unit To Be Modified To be Replaced	4SLB	N/A
ENG5	Natural Gas Compressor Engine	Caterpillar	G3616	TBD	5000	5000	TBD	ENG5 CAT5	20200254	Existing (unchanged) To be Removed New/Additional Replacement Unit	4SLB	N/A
ENG6	Natural Gas Compressor	Caterpillar	G3616	TBD	5000	5000	TBD	ENG6	20200254	To Be Modified □ To be Replaced □ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit	4SLB	N/A
LINGO	Engine	Cutorpinu	00010	155	2000	2000	TBD	CAT6		To Be Modified To be Replaced Existing (unchanged) To be Removed	1020	
ENG7	Natural Gas Compressor Engine	Caterpillar	G3616	TBD	5000	5000	TBD TBD	ENG7 CAT7	20200254		4SLB	N/A
ENG8	Natural Gas Compressor Engine	Caterpillar	G3616	TBD	5000	5000	TBD TBD	ENG8 CAT8	20200254	Existing (unchanged) To be Removed New/Additional Replacement Unit	4SLB	N/A
ENG9	Natural Gas Compressor Engine	Caterpillar	G3616	TBD	5000	5000	TBD	ENG9 CAT9	20200254	Existing (unchanged) To be Removed New/Additional Replacement Unit	4SLB	N/A
ENG11	Natural Gas Compressor Engine	Caterpillar	3516J TA	N6W01221	1380	1380	2/1/2019	ENG11 CAT11	20200254	To Be Modified To be Replaced Existing (unchanged) To be Removed New/Additional Replacement Unit	4SLB	N/A
ENG12	Natural Gas Compressor Engine	Caterpillar	3516J TA	N6W01223	1380	1380	2/1/2019 2/1/2019 2/1/2019	ENG12 CAT12	20200254	To Be Modified To be Replaced Existing (unchanged) To be Removed New/Additional Replacement Unit	4SLB	N/A
ENG10	Natural Gas Compressor Engine	Caterpillar	G3606TA	TBD	1775	1775	TBD	ENG10 CAT10	20200254	To Be Modified □ To be Replaced □ Existing (unchanged) ■ To be Removed □ New/Additional □ Replacement Unit	4SLB	N/A
ENG13	Natural Gas Compressor	Caterpillar	G3306TA	TBD	203	203	TBD TBD	ENG13	20200254	To Be Modified To be Replaced Existing (unchanged) New/Additional Replacement Unit	4SRB	N/A
	Engine						TBD	CAT13 TBD		□ To Be Modified □ To be Replaced □ Existing (unchanged) □ To be Removed		
HTR1	Fuel Line Heater	Wenco Energy Corp	SB20-12H	0819-950	0.75 MMBtu/hr	0.75 MMBtu/hr	2019 2019	HTR1	31000228	New/Additional Replacement Unit To Be Modified To be Replaced	N/A	N/A
RB1	Glycol Regenerator Reboiler	Flameco	FA-40719-23	1861-095	2.0 MMBtu/hr	2.0 MMBtu/hr	2019 2019	N/A RB1	31000404	Existing (unchanged) To be Removed New/Additional To Be Modified To be Replaced	N/A	N/A
RB2	Glycol Regenerator Reboiler	TBD	TBD	TBD	2.0 MMBtu/hr	2.0 MMBtu/hr	TBD	N/A RB2	31000404	Existing (unchanged) To be Removed New/Additional Replacement Unit	N/A	N/A
RB3	Glycol Regenerator Reboiler	TBD	TBD	TBD	2.0 MMBtu/hr	2.0 MMBtu/hr	TBD	N/A	31000404	To Be Modified □ To be Replaced □ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit	N/A	N/A
HTR2	Fuel Line Heater	N/A	N/A	N/A	0.75 MMBtu/hr	0.75 MMBtu/hr	TBD TBD	RB3 N/A	31000228	To Be Modified □ To be Replaced □ Existing (unchanged) ■ To be Removed □ New/Additional □ Replacement Unit	N/A	N/A
HTR3	Fuel Line Heater	N/A	N/A	N/A	1.5 MMBtu/hr	1.5 MMBtu/hr	N/A TBD	HTR2 N/A	31000228	To Be Modified To be Replaced Existing (unchanged) New/Additional Replacement Unit	N/A	N/A
IIIKJ	Fuel Line Heatel	19/74	19/74	11/21	1.5 WIWIDU/III	1.5 WIWIDU/III	N/A	HTR3	51000220	□ To Be Modified □ To be Replaced	18/75	19/24

							Date of Manufacture ²	Controlled by Unit #	Source			gust 2020: Re
Unit Number ¹	Source Description	Make	Model #	Serial #	Manufact-urer's Rated Capacity ³ (Specify Units)	Requested Permitted Capacity ³ (Specify Units)	Date of Construction/ Reconstruction ²	Emissions vented to Stack #	Classi- fication Code (SCC)	For Each Piece of Equipment, Check One	RICE Ignition Type (CI, SI, 4SLB, 4SRB, 2SLB) ⁴	Replacing Unit No.
FL1	Flare 1	Tornado	GUYED DUAL AIR ASSIST	14783/17152	70 MMscf/d	70 MMscf/d	2019	N/A	31000205	Existing (unchanged) To be Removed New/Additional Replacement Unit	N/A	N/A
							2019 TBD	FL1 N/A		To Be Modified □ To be Replaced □ Existing (unchanged) □ To be Removed		
FL2	Flare 2	Tornado	TBD	TBD	70 MMscf/d	70 MMscf/d	TBD	FL2	31000205	□ New/Additional □ Replacement Unit ■ To Be Modified □ To be Replaced	N/A	N/A
VC1	Still Vent Emissions	CIMARRON ENERGY	N/A	5004793	N/A	N/A	2019 2019	N/A VC1	31000205	Existing (unchanged) To be Removed New/Additional To Be Modified To be Replaced	N/A	N/A
FL3	Flare 3	Tornado	TBD	TBD	70 MMscf/d	70 MMscf/d	TBD TBD	N/A FL3	31000205	Existing (unchanged) To be Removed New/Additional To Be Modified To be Replaced	N/A	N/A
SKT1	Skim Tank	STELLMATION	TBD	P-000-469- 918-000001	1000 bbl	1000 bbl	2019 2019	FL1-FL2 FL1-FL2	40400311	Existing (unchanged) To be Removed New/Additional To Be Modified To Be Modified To be Replaced	N/A	N/A
SKT2	Skim Tank (Backup)	TBD	TBD	TBD	1000 bbl	1000 bbl	TBD	FL1-FL2 FL1-FL2	40400311	Existing (unchanged) Existing (unchanged) New/Additional Replacement Unit To be Modified To be Replaced	N/A	N/A
				P-000-462-			2019	FL1-FL2		Existing (unchanged) To be Removed		
OT1	Condensate Tank	STELLMATION	TBD	144-000010	500 bbl	500 bbl	2019	FL1-FL2	40400311	 New/Additional Replacement Unit To Be Modified To be Replaced 	N/A	N/A
OT2	Condensate Tank	STELLMATION	TBD	P-000-462-	500 bbl	500 bbl	2019	FL1-FL2	40400311	Existing (unchanged) To be Removed New/Additional Replacement Unit	N/A	N/A
				144-000001			2019	FL1-FL2		■ To Be Modified □ To be Replaced		
OT3	Condensate Tank	STELLMATION	TBD	P-000-462- 114-000003	500 bbl	500 bbl	2019 2019	FL1-FL2 FL1-FL2	40400311	Existing (unchanged) To be Removed New/Additional Replacement Unit	N/A	N/A
				P-000-462-			2019	FL1-FL2 FL1-FL2		To Be Modified To be Replaced Existing (unchanged) To be Removed		
OT4	Condensate Tank	STELLMATION	TBD	P-000-482- 144-000007	500 bbl	500 bbl	2019	FL1-FL2	40400311	 New/Additional Replacement Unit To Be Modified To be Replaced 	N/A	N/4
WT1	Produced Water Tank	STELLMATION	TBD	P-000-462-	500 bbl	500 bbl	2019	FL1-FL2	40400315	Existing (unchanged) To be Removed New/Additional Replacement Unit	N/A	N/A
vv 1 1	Floduced water Talik	STELEMATION	IBD	114-000005	500 661	500 001	2019	FL1-FL2	40400313	■ To Be Modified □ To be Replaced	IN/A	IN/F
WT2	Produced Water Tank	STELLMATION	TBD	P-000-462- 144-000008	500 bbl	500 bbl	2019 2019	FL1-FL2 FL1-FL2	40400315	□ Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit ■ To Be Modified □ To be Replaced	N/A	N/A
VRU1	Low Pressure Separator VRU		PVR-1829	N/A	125 HP	125 HP	2019	FL1-FL2	N/A	Existing (unchanged) To be Removed New/Additional Replacement Unit	N/A	N/A
	#1	CONTROL			_	-	2019	FL1-FL2		To Be Modified D To be Replaced		
VRU2	Low Pressure Separator VRU Backup	PLATINUM VAPOR CONTROL	PVR-1828	N/A	125 HP	125 HP	2019	FL1-FL2	N/A	Existing (unchanged) To be Removed New/Additional Replacement Unit	N/A	N/A
		CONTROL					2019	FL1-FL2		To Be Modified To be Replaced Existing (unchanged) To be Removed		
DEHY1	TEG Dehydrator with Condenser	N/A	N/A	N/A	80 MMscfd	80 MMscfd	2019 2019	COND1 RB1	31000227	Existing (unchanged) To be Removed New/Additional Replacement Unit To Be Modified To be Replaced	N/A	N/A
	TEG Dehydrator with						TBD	COND2		■ 10 Be Moained □ 10 be Replaced □ Existing (unchanged) □ To be Removed		
DEHY2	Condenser	N/A	N/A	N/A	80 MMscfd	80 MMscfd	TBD	RB2	31000227	 New/Additional Replacement Unit To Be Modified To be Replaced 	N/A	N/A
DEUV2	TEG Dehydrator with	N1/A	N//A	NT/A	90 XO (61	80 MM 61	TBD	COND3	21000227	Existing (unchanged) To be Removed	NT/A	NU
DEHY3	Condenser	N/A	N/A	N/A	80 MMscfd	80 MMscfd	TBD	RB3	31000227	□ New/Additional □ Replacement Unit ■ To Be Modified □ To be Replaced	N/A	N/A
LPS	Low Pressure Separator	N/A	N/A	N/A	N/A	N/A	2019	FL1-FL2	N/A	Existing (unchanged) To be Removed New/Additional Replacement Unit	N/A	N/A
							2019	FL1-FL2		■ To Be Modified □ To be Replaced □ Existing (unchanged) □ To be Removed		
LOAD	Condensate Truck Loading	N/A	N/A	N/A	223 bbl/d	223 bbl/d	N/A N/A	N/A N/A	40400250	 New/Additional Replacement Unit To Be Modified To be Replaced 	N/A	N/A
FUG	Fugitive Emissions	N/A	N/A	N/A	N/A	N/A	N/A N/A	N/A N/A	31088811	Existing (unchanged) To be Removed New/Additional Replacement Unit To Be Modified To be Replaced	N/A	N/A
							N/A	N/A		■ Existing (unchanged) □ To be Removed	-	
SSM	SSM Activities	N/A	N/A	N/A	N/A	N/A	N/A	N/A	31088811	New/Additional Replacement Unit To Be Modified To be Replaced	N/A	N/A
Malfunction	Malfunction Emissions	N/A	N/A	N/A	N/A	N/A	N/A	N/A	31088811	Existing (unchanged) To be Removed New/Additional Replacement Unit	N/A	N/A
manuncuoli	Manufiction Lanssions	11/71	11/13	17/2	11/73	11/2	N/A	N/A	51000011	□ To Be Modified □ To be Replaced	11/13	14/1

Unit numbers must correspond to unit numbers in the previous NOI unless a complete cross reference table of all units in both NOIs is provided.

Construction of the function of the function of the previous for unless a comprete closs reference table of an units in bour foots is provided. ³ Specify dates required to determine regulatory applicability. ³ To properly account for power conversion efficiencies, generator set rated capacity shall be reported as the rated capacity of the engine in horsepower, not the kilowatt capacity of the generator set. ⁴ 4SLB* means four stroke lean burn engine, "4SRB* means four stroke rich burn engine, "2SLB* means two stroke lean burn engine, "CI* means compression ignition, and "SI* means spark ignition

Table 2-B: Insignificant Activities¹ (20.2.70 NMAC) OR Exempted Equipment (20.2.72 NMAC)

All 20.2.70 NMAC (Title V) applications must list all Insignificant Activities in this table. All 20.2.72 NMAC applications must list Exempted Equipment in this table. If equipment listed on this table is exempt under 20.2.72.202.B.5, include emissions calculations and emissions totals for 202.B.5 "similar functions" units, operations, and activities in Section 6, Calculations. Equipment and activities exempted under 20.2.72.202 NMAC may not necessarily be Insignificant under 20.2.70 NMAC (and vice versa). Unit & stack numbering must be consistent throughout the application package. Per Exemptions Policy 02-012.00 (see http://www.env.nm.gov/aqb/permit/aqb_pol.html), 20.2.72.202.B NMAC Exemptions do not apply, but 20.2.72.202.A NMAC exemptions do apply to NOI facilities under 20.2.73 NMAC. List 20.2.72.301.D.4 NMAC Auxiliary Equipment for Streamline applications in Table 2-A. The List of Insignificant Activities (for TV) can be found online at

http://www.env.nm.gov/aqb/forms/InsignificantListTitleV.pdf. TV sources may elect to enter both TV Insignificant Activities and Part 72 Exemptions on this form.

Unit Number	Source Description	Manufacturer	Model No.	Max Capacity	List Specific 20.2.72.202 NMAC Exemption (e.g. 20.2.72.202.B.5)	Date of Manufacture /Reconstruction ²	For Each Piece of Equipment, Check Onc
Omt Number	Source Description	Manufacturer	Serial No.	Capacity Units	Insignificant Activity citation (e.g. IA List Item #1.a)	Date of Installation /Construction ²	For Each Free of Equipment, Check One
			N/A	N/A	20.2.72.202.B.5	N/A	☑ Existing (unchanged) □ To be Removed
ROAD	Haul Road Emissions	N/A	N/A	N/A	20.2.72.202.B.5	N/A	 New/Additional To Be Modified To be Replaced
							Existing (unchanged) To be Removed New/Additional Replacement Unit To Be Modified To be Replaced
							Existing (unchanged) To be Removed New/Additional Replacement Unit To Be Modified To be Replaced
							Existing (unchanged) To be Removed New/Additional Replacement Unit To Be Modified To be Replaced
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							 Existing (unchanged) To be Removed New/Additional Replacement Unit To Be Modified To be Replaced

¹ Insignificant activities exempted due to size or production rate are defined in 20.2.70.300.D.6, 20.2.70.7.Q NMAC, and the NMED/AQB List of Insignificant Activities, dated September 15, 2008. Emissions from these insignificant activities do not need to be reported, unless specifically requested.

² Specify date(s) required to determine regulatory applicability.

Table 2-C: Emissions Control Equipment

Unit and stack numbering must correspond throughout the application package. The permittee shall report all control devices and list each pollutant controlled by the control device regardless if the applicant takes credit for the reduction in emissions. Flares, Enclosed Combustion Devices, Catalytic Converters and Air Fuel Ratio (AFR) Controllers shall be reported on Table 2-C. For each AFR, note whether the AFR are aftermarket or integral to the engine.

Control Equipment Unit No.	Control Equipment Description	Date Installed	Controlled Pollutant(s)	Controlling Emissions for Unit Number(s) ¹	Efficiency (% Control by Weight)	Method used to Estimate Efficiency
FL1	Flare 1	2019	VOC, HAP	Facility Inlet, OT1-OT4, WT1-WT2, SKTK1/SKTK2, LPS	98	Engineering Est.
FL2	Flare 2	TBD	VOC, HAP	Facility Inlet, OT1-OT4, WT1-WT2, SKTK1/SKTK2, LPS	98	Engineering Est.
VC1	Still Vent Emissions	2019	VOC, HAP	DEHY1-3 BTEX Condenser Vapors	98	Engineering Est.
FL3	Flare 3	TBD	VOC, HAP	Facility Inlet, OT1-OT4, WT1-WT2, SKTK1/SKTK2, LPS	98	Engineering Est.
VRU1	Low Pressure Separator VRU #1	2019	VOC, HAPs	LPS	98	Engineering Est.
VRU2	Low Pressure Separator VRU Backup	2019	VOC, HAPs	LPS	98	Engineering Est.
COND1- COND3	BTEX Condenser	2019	VOC, HAP	DEHY1-DEHY3	98	Engineering Est.
CAT1-CAT12	Engine Catalysts	2019	CO, VOC, HAP	ENG1-ENG12	CO-85, VOC/HAP-73	Engineering Est.
¹ List each con	ntrol device on a separate line. For each control device, list all er	nission units c	ontrolled by the control device.			

Table 2-D: Maximum Emissions (under normal operating conditions)

Maximum Emissions are the emissions at maximum capacity and prior to (in the absence of) pollution control, emission-reducing process equipment, or any other emission reduction. Calculate the hourly emissions using the worst case hourly emissions for each pollutant. For each pollutant, calculate the annual emissions as if the facility were operating at maximum plant capacity without pollution controls for 8760 hours per year, unless otherwise approved by the Department. List Hazardous Air Pollutants (HAP) & Toxic Air Pollutants (TAPs) in Table 2-1. Unit & stack numbering must be consistent throughout the application package. Fill all cells in this table with the emission numbers or a "-" symbol. A "-" symbol indicates that emissions of this pollutant are not expected. Numbers shall be expressed to at least 2 decimal points (e.g. 0.41, 1.41, or 1.41E-4).

IL VIN	N	Ox	C	0	V	OC	S	Ox	P	M	PM	I 10 ¹	PM	2.5 ¹	Н	$_{2}S$	Le	ead
Unit No.	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
ENG1	4.13	18.11	33.73	147.74	9.90	43.37	0.42	1.84	0.38	1.65	0.38	1.65	0.38	1.65	-	-	-	-
ENG2	4.13	18.11	33.73	147.74	9.90	43.37	0.42	1.84	0.38	1.65	0.38	1.65	0.38	1.65	-	-	-	-
ENG3	4.13	18.11	33.73	147.74	9.90	43.37	0.42	1.84	0.38	1.65	0.38	1.65	0.38	1.65	-	-	-	-
ENG4	4.13	18.11	33.73	147.74	9.90	43.37	0.42	1.84	0.38	1.65	0.38	1.65	0.38	1.65	-	-	-	-
ENG5	4.13	18.11	33.73	147.74	9.90	43.37	0.42	1.84	0.38	1.65	0.38	1.65	0.38	1.65	-	-	-	-
ENG6	4.13	18.11	33.73	147.74	9.90	43.37	0.42	1.84	0.38	1.65	0.38	1.65	0.38	1.65	-	-	-	-
ENG7	4.13	18.11	33.73	147.74	9.90	43.37	0.42	1.84	0.38	1.65	0.38	1.65	0.38	1.65	-	-	-	-
ENG8	4.13	18.11	33.73	147.74	9.90	43.37	0.42	1.84	0.38	1.65	0.38	1.65	0.38	1.65	-	-	-	-
ENG9	4.13	18.11	33.73	147.74	9.90	43.37	0.42	1.84	0.38	1.65	0.38	1.65	0.38	1.65	-	-	-	-
ENG11	1.90	8.33	7.76	33.98	3.96	17.33	0.13	0.55	0.11	0.49	0.11	0.49	0.11	0.49	-	-	-	-
ENG12	1.90	8.33	7.76	33.98	3.96	17.33	0.13	0.55	0.11	0.49	0.11	0.49	0.11	0.49	-	-	-	-
HTR1	0.11	0.50	0.10	0.42	0.01	0.03	0.01	0.04	0.01	0.04	0.01	0.04	0.01	0.04	-	-	-	-
RB1	0.31	1.34	0.26	1.12	0.02	0.07	0.03	0.12	0.02	0.10	0.02	0.10	0.02	0.10	-	-	-	-
RB2	0.31	1.34	0.26	1.12	0.02	0.07	0.03	0.12	0.02	0.10	0.02	0.10	0.02	0.10	-	-	-	-
RB3	0.31	1.34	0.26	1.12	0.02	0.07	0.03	0.12	0.02	0.10	0.02	0.10	0.02	0.10	-	-	-	-
FL1-FL2 Pilot	0.67	2.93	1.33	5.84	0.94	4.13	0.01	0.03	0.03	0.13	0.03	0.13	0.03	0.13	-	-	-	-
FL1-FL2 Norm							Emissions	s are not rou	ited to flai	e in unco	ntrolled so	cenario.						
FL1-FL2 SSM							Emissions	s are not rou	ited to flai	e in unco	ntrolled so	cenario.						
VC1	0.41	1.80	0.82	3.59	2.61	11.43	0.29	1.26	0.01	0.04	0.01	0.04	0.01	0.04	-	-	-	-
SKT1	-	-	-	-	4.87	21.32	-	-	-	-	-	-	-	-	-	-	-	-
SKT2	-	-	-	-	4.87	21.32	-	-	-	-	-	-	-	-	-	-	-	-
OT1	-	-	-	-	138.24	295.64	-	-	-	-	-	-	-	-	-	-	-	-
OT2	-	-	-	-	138.24	295.64	-	-	-	-	-	-	-	-	-	-	-	-
OT3	-	-	-	-	138.24	295.64	-	-	-	-	-	-	-	-	-	-	-	-
OT4	-	-	-	-	138.24	295.64	-	-	-	-	-	-	-	-	-	-	-	-
WT1	-	-	-	-	0.11	0.47	-	-	-	-	-	-	-	-	-	-	-	-
WT2	-	-	-	-	0.11	0.47	-	-	-	-	-	-	-	-	-	-	-	-
DEHY1	-	-	-	-	43.51	190.56	-	-	-	-	-	-	-	-	-	-	-	-
DEHY2	-	-	-	-	43.51	190.56	-	-	-	-	-	-	-	-	-	-	-	-
DEHY3	-	-	-	-	43.51	190.56	-	-	-	-	-	-	-	-	-	-	-	-
LPS	-	-	-	-	698.88	354.13	-	-	-	-	-	-	-	-	-	-	-	-
LOAD	-	-	-	-	65.70	11.14	-	-	-	-	-	-	-	-	-	-	-	-
FUG	-	-	-	-	4.89	21.43	-	-	-	-	-	-	-	-	-	-	-	-
SSM	-	-	-	-	-	10.00	-	-	-	-	-	-	-	-	-	-	-	-
ROAD	-	-	-	-	-	-	-	-	0.15	0.02	0.15	0.02	0.15	0.02	-	-	-	-
MALFUNCTION	-	-	-	-	-	10.00	-	-	-	-	-	-	-	-	-	-	-	-
Totals	43.11	188.84	322.11	1410.82	1563.54	2625.34	4.42	19.37	-	-	3.73	16.32	3.73	16.32	-	-	-	-

¹Condensable Particulate Matter: Include condensable particulate matter emissions for PM10 and PM2.5 if the source is a combustion source. Do not include condensable particulate matter for PM unless PM is set equal to PM10 and PM2.5. Particulate matter (PM) is not subject to an ambient air quality standard, but it is a regulated air pollutant under PSD (20.2.74 NMAC) and Title V (20.2.70 NMAC).

Table 2-E: Requested Allowable Emissions

Unit & stack numbering must be consistent throughout the application package. Fill all cells in this table with the emission numbers or a "-" symbol. A "-" symbol indicates that emissions of this pollutant are not expected. Numbers shall be expressed to at least 2 decimal points (e.g. 0.41, 1.41, or 1.41E⁴).

	N	Ox	C	0	V	DC	S	Ox	P	M1	PM	I10 ¹	PM2		Н	$_2S$	Le	ead
Unit No.	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
ENG1	4.13	18.11	4.38	19.21	3.47	15.18	0.42	1.84	0.38	1.65	0.38	1.65	0.38	1.65	-	-	-	-
ENG2	4.13	18.11	4.38	19.21	3.47	15.18	0.42	1.84	0.38	1.65	0.38	1.65	0.38	1.65	-	-	-	-
ENG3	4.13	18.11	4.38	19.21	3.47	15.18	0.42	1.84	0.38	1.65	0.38	1.65	0.38	1.65	-	-	-	-
ENG4	4.13	18.11	4.38	19.21	3.47	15.18	0.42	1.84	0.38	1.65	0.38	1.65	0.38	1.65	-	-	-	-
ENG5	4.13	18.11	4.38	19.21	3.47	15.18	0.42	1.84	0.38	1.65	0.38	1.65	0.38	1.65	-	-	-	-
ENG6	4.13	18.11	4.38	19.21	3.47	15.18	0.42	1.84	0.38	1.65	0.38	1.65	0.38	1.65	-	-	-	-
ENG7	4.13	18.11	4.38	19.21	3.47	15.18	0.42	1.84	0.38	1.65	0.38	1.65	0.38	1.65	-	-	-	-
ENG8	4.13	18.11	4.38	19.21	3.47	15.18	0.42	1.84	0.38	1.65	0.38	1.65	0.38	1.65	-	-	-	-
ENG9	4.13	18.11	4.38	19.21	3.47	15.18	0.42	1.84	0.38	1.65	0.38	1.65	0.38	1.65	-	-	-	-
ENG11	1.90	8.33	1.01	4.42	1.29	5.63	0.13	0.55	0.11	0.49	0.11	0.49	0.11	0.49	-	-	-	-
ENG12	1.90	8.33	1.01	4.42	1.29	5.63	0.13	0.55	0.11	0.49	0.11	0.49	0.11	0.49	-	-	-	-
HTR1	0.11	0.50	0.10	0.42	0.01	0.03	0.01	0.04	0.01	0.04	0.01	0.04	0.01	0.04	-	-	-	-
RB1	0.31	1.34	0.26	1.12	0.02	0.07	0.03	0.12	0.02	0.10	0.02	0.10	0.02	0.10	-	-	-	-
RB2	0.31	1.34	0.26	1.12	0.02	0.07	0.03	0.12	0.02	0.10	0.02	0.10	0.02	0.10	-	-	-	-
RB3	0.31	1.34	0.26	1.12	0.02	0.07	0.03	0.12	0.02	0.10	0.02	0.10	0.02	0.10	-	-	-	-
FL1-FL2 Pilot	0.67	2.93	1.33	5.84	0.94	4.13	0.01	0.03	0.03	0.13	0.03	0.13	0.03	0.13	-	-	-	-
FL1-FL2 Norm	1.85	7.72	3.69	15.41	11.53	25.60	0.01	0.04	0.03	0.15	0.03	0.15	0.03	0.15	-	-	-	-
VC1	0.41	1.80	0.82	3.59	2.61	11.43	0.29	1.26	0.01	0.04	0.01	0.04	0.01	0.04	-	-	-	-
SKT1			_		_		_	Emiss	ions Repr	esented at	FL1-FL2				_		_	
SKT2								Emiss	ions Repr	esented at	FL1-FL2							
OT1								Emiss	ions Repr	esented at	FL1-FL2							
OT2								Emiss	ions Repr	esented at	FL1-FL2							
OT3								Emiss	ions Repr	esented at	FL1-FL2							
OT4								Emiss	ions Repr	esented at	FL1-FL2							
WT1								Emiss	ions Repr	esented at	FL1-FL2							
WT2								Emiss	ions Repr	esented at	FL1-FL2							
DEHY1								Emi	issions Re	presented	at VC1							
DEHY2								Emi	issions Re	presented	at VC1							
DEHY3								Emi	issions Re	presented	at VC1							
LPS								Emiss	ions Repr	esented at	FL1-FL2				-			
LOAD	-	-	-	-	65.70	11.14	-	-	-	-	-	-	-	-	-	-	-	-
FUG	-	-	-	-	4.89	21.43	-	-	-	-	-	-	-	-	-	-	-	-
ROAD	-	-	-	-	-	-	-	-	0.15	0.02	0.15	0.02	0.15	0.02	-	-	-	-
MALFUNCTION	-	-	-	-	-	10.00	-	-	-	-	-	-	-	-	-	-	-	-
Totals	44.96	196.56	48.19	210.32	119.50	221.88	4.43	19.41	3.91	16.49	3.91	16.49	3.91	16.49	-	-	-	-

¹ Condensable Particulate Matter: Include condensable particulate matter emissions for PM10 and PM2.5 if the source is a combustion source. Do not include condensable particulate matter for PM unless PM is set equal to PM10 and PM2.5. Particulate matter (PM) is not subject to an ambient air quality standard, but it is a regulated air pollutant under PSD (20.2.74 NMAC) and Title V (20.2.70 NMAC).

Table 2-F: Additional Emissions during Startup, Shutdown, and Routine Maintenance (SSM)

This table is intentionally left blank since all emissions at this facility due to routine or predictable startup, shutdown, or scenduled maintenance are no higher than those listed in Table 2-E and a malfunction emission limit is not already permitted or requested. If you are required to report GHG emissions as described in Section 6a, include any GHG emissions during Startup, Shutdown, and/or Scheduled Maintenance (SSM) in Table 2-P. Provide an explanations of SSM emissions in Section 6 and 6a.

All applications for facilities that have emissions during routine our predictable startup, shutdown or scheduled maintenance $(SSM)^1$, including NOI applications, must include in this table the Maximum Emissions during routine or predictable startup, shutdown and scheduled maintenance (20.2.7 NMAC, 20.2.72.203.A.3 NMAC, 20.2.73.200.D.2 NMAC). In Section 6 and 6a, provide emissions calculations for all SSM emissions reported in this table. Refer to "Guidance for Submittal of Startup, Shutdown, Maintenance Emissions in Permit Applications (https://www.env.nm.gov/apb/permit/apb. nol html) for more detailed instructions. Numbers shall be expressed to at least 2 decimal points (e.g. 0.41 + 41 or 1.41 or 1.41

(https://www	.env.nm.go N(mit/aqb_p			DC		umbers sn Dx	all be expr PI		t least 2 de	110 ²		2.5^2	r 1.41E-4) H	s.	т.	ho
Unit No.												-		-				ead
	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
SSM	-	-	-	-	-	10.00												
FL1-FL2 SSM	541.65	8.10	1081.35	16.17	992.97	18.36	4.91	0.08	22.25	0.31	22.25	0.31	22.25	0.31	-	-	-	-
Totals	541.65	8.10	1081.35	16.17	992.97	28.36	4.91	0.08	22.25	0.31	22.25	0.31	22.25	0.31				

¹ For instance, if the short term steady-state Table 2-E emissions are 5 lb/hr and the SSM rate is 12 lb/hr, enter 7 lb/hr in this table. If the annual steady-state Table 2-E emissions are 21.9 TPY, and the number of scheduled SSM events result in annual emissions of 31.9 TPY, enter 10.0 TPY in the table below.

² Condensable Particulate Matter: Include condensable particulate matter emissions for PM10 and PM2.5 if the source is a combustion source. Do not include condensable particulate matter for PM unless PM is set equal to PM10 and PM2.5. Particulate matter (PM) is not subject to an ambient air quality standard, but it is a regulated air pollutant under PSD (20.2.74 NMAC) and Title V (20.2.70 NMAC).

Table 2-G: Stack Exit and Fugitive Emission Rates for Special Stacks

□ I have elected to leave this table blank because this facility does not have any stacks/vents that split emissions from a single source or combine emissions from more than one source listed in table 2-A. Additionally, the emission rates of all stacks match the Requested allowable emission rates stated in Table 2-E.

Use this table to list stack emissions (requested allowable) from split and combined stacks. List Toxic Air Pollutants (TAPs) and Hazardous Air Pollutants (HAPs) in Table 2-I. List all fugitives that are associated with the normal, routine, and non-emergency operation of the facility. Unit and stack numbering must correspond throughout the application package. Refer to Table 2-E for instructions on use of the "-" symbol and on significant figures.

	Serving Unit		Ox	C	0	V	DC	SC	Dx	P	М	PN	110	PM	[2.5	□ H ₂ S 0	r 🗆 Lead
Stack No.	Number(s) from Table 2-A	lb/hr	ton/yr	lb/hr	ton/yr												
,	Totals:	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00				

Table 2-H: Stack Exit Conditions

Unit and stack numbering must correspond throughout the application package. Include the stack exit conditions for each unit that emits from a stack, including blowdown venting parameters and tank emissions.

Stack	Serving Unit Number(s)	Orientation	Rain Caps	Height Above	Temp.	Flow	Rate	Moisture by	Velocity	Inside
Number	from Table 2-A	(H-Horizontal V=Vertical)	(Yes or No)	Ground (ft)	(F)	(acfs)	(dscfs)	Volume (%)	(ft/sec)	Diameter (ft)
ENG1	ENG1	V	No	25	809	523.40	Unknown	Unknown	296.18	1.50
ENG2	ENG2	V	No	25	809	523.40	Unknown	Unknown	296.18	1.50
ENG3	ENG3	V	No	25	809	523.40	Unknown	Unknown	296.18	1.50
ENG4	ENG4	V	No	25	809	523.40	Unknown	Unknown	296.18	1.50
ENG5	ENG5	V	No	25	809	523.40	Unknown	Unknown	296.18	1.50
ENG6	ENG6	V	No	25	809	523.40	Unknown	Unknown	296.18	1.50
ENG7	ENG7	V	No	25	809	523.40	Unknown	Unknown	296.18	1.50
ENG8	ENG8	V	No	25	809	523.40	Unknown	Unknown	296.18	1.50
ENG9	ENG9	V	No	25	809	523.40	Unknown	Unknown	296.18	1.50
ENG11	ENG11	V	No	20	997	135.13	Unknown	Unknown	172.06	1.00
ENG12	ENG12	V	No	20	997	135.13	Unknown	Unknown	172.06	1.00
HTR1	HTR1	V	Ν	15	800	5.07	Unknown	Unknown	6.45	0.75
RB1	RB1	V	Ν	15	800	13.52	Unknown	Unknown	7.65	1.00
RB2	RB2	V	N	15	800	13.52	Unknown	Unknown	7.65	1.00
RB3	RB3	V	N	15	800	13.52	Unknown	Unknown	7.65	1.00
FL1	FL1	V	No	145	1832	4123.47	Unknown	Unknown	65.60	0.83
FL2	FL2	V	No	145	1832	4123.47	Unknown	Unknown	65.60	0.83
VC1	VC1	V	No	20	1000	1331.91	Unknown	Unknown	65.60	1.00

Table 2-I: Stack Exit and Fugitive Emission Rates for HAPs and TAPs

In the table below, report the Potential to Emit for each HAP from each regulated emission unit listed in Table 2-A, only if the entire facility emits the HAP at a rate greater than or equal to one (1) ton per year For each such emission unit, HAPs shall be reported to the nearest 0.1 tpy. Each facility-wide Individual HAP total and the facility-wide Total HAPs shall be the sum of all HAP sources calculated to the nearest 0.1 ton per year. Per 20.2.72.403.A.1 NMAC, facilities not exempt [see 20.2.72.402.C NMAC] from TAP permitting shall report each TAP that has an uncontrolled emission rate in excess of its pounds per hour screening level specified in 20.2.72.502 NMAC. TAPs shall be reported using one more significant figure than the number of significant figures shown in the pound per hour threshold corresponding to the substance. Use the HAP nomenclature as it appears in Section 112 (b) of the 1990 CAAA and the TAP nomenclature as it listed in 20.2.72.502 NMAC. Include tank-flashing emissions estimates of HAPs in this table. For each HAP or TAP listed, fill all cells in this table with the emission numbers or a "-" symbol. A "-" symbol indicates that emissions of this pollutant are not expected or the pollutant is emitted in a quantity less than the threshold amounts described above.

Stack No.	Unit No.(s)	Total	HAPs		ldehyde P or □ AP		xane P or □ \P	🗹 HA	zene AP or 🗆 AP		dehyde or 🗆 TAP		eHere	Name	Pollutant e Here or 🗆 TAP	Nam	Pollutant e Here or 🗆 TAP	Name	Pollutant e Here or 🛛 TAP
		lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
ENG1	ENG1	0.54	2.36	0.4	1.9	-	-	-	-	0.1	0.5								
ENG2	ENG2	0.54	2.36	0.4	1.9	-	-	-	-	0.1	0.5								
ENG3	ENG3	0.54	2.36	0.4	1.9	-	-	-	-	0.1	0.5								
ENG4	ENG4	0.54	2.36	0.4	1.9	-	-	-	-	0.1	0.5								
ENG5	ENG5	0.54	2.36	0.4	1.9	-	-	-	-	0.1	0.5								
ENG6	ENG6	0.54	2.36	0.4	1.9	-	-	-	-	0.1	0.5								
ENG7	ENG7	0.54	2.36	0.4	1.9	-	-	-	-	0.1	0.5								
ENG8	ENG8	0.54	2.36	0.4	1.9	-	-	-	-	0.1	0.5								
ENG9	ENG9	0.54	2.36	0.4	1.9	-	-	-	-	0.1	0.5								
ENG11	ENG11	0.32	1.39	0.3	1.2	-	I	-	-	0.0	0.1								
ENG12	ENG12	0.32	1.39	0.3	1.2	-	-	-	-	0.0	0.1								
HTR1	HTR1	2.2E-03	0.01	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0								
RB1	RB1	0.01	0.03	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0								
RB1	RB2	0.01	0.03	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0								
RB1	RB3	0.01	0.03	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0								
FL1-FL2 Pilot	FL1-FL2 Pilot	0.01	0.04	-	-	0.0	0.0	4.9E-04	2.2E-03	-	-								
FL1-FL2 Norm	FL1-FL2 Norm	0.5	1.1	-	-	0.4	0.9	0.0	0.1	-	-								
FL1-FL2 SSM	FL1-FL2 SSM	27.5	0.5	-	-	24.3	0.5	1.3	0.0	-	-								
VC1	DEHY1	0.1	0.5	-	-	0.0	0.1	0.1	0.2	-	-								
VC1	DEHY2	0.1	0.5	-	-	0.0	0.1	0.1	0.2	-	-								
VC1	DEHY3	0.1	0.5	-	-	0.0	0.1	0.1	0.2	-	-								

Stack No.	Unit No.(s)		HAPs	☑ HA	ldehyde P or □ AP	☑ HA	exane Por□ AP	☑ HA	zene P or 🗆 AP		dehyde or 🗆 TAP	Name	Pollutant e Here or 🗆 TAP	Name	Pollutant Here Or 🗆 TAP	Name	Pollutant e Here or 🗆 TAP	Name	Pollutant e Here or 🗆 TAP
		lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
FL1-FL2	SKT1				Emissie	ons Repres	ented at F	L1-FL2											
FL1-FL2	SKT2				Emissie	ons Repres	ented at F	L1-FL2											
FL1-FL2	OT1		Emissions Represented at FL1-FL2																
FL1-FL2	OT2		Emissions Represented at FL1-FL2 Image: Constraint of the second of th																
FL1-FL2	OT3		Emissions Represented at FL1-FL2																
FL1-FL2	OT4																		
FL1-FL2	WT1				Emissie	ons Repres	ented at F	L1-FL2											
FL1-FL2	WT2				Emissie	ons Repres	ented at F	L1-FL2											
FL1-FL2	LPS				Emissie	ons Repres	ented at F	L1-FL2											
LOAD	LOAD	0.0	0.0	-	-	-	-	-	-	-	-								
FUG	FUG	0.4	1.6	-	-	0.09	0.39	0.04	0.17	-	-								
SSM	SSM	-	-	-	-	-	-	-	-	-	-								
ROAD	ROAD	-	-	-	-	-	-	-	-	-	-								
Tot	als:	34.2	28.8	4.4	19.4	24.9	2.2	1.6	1.0	1.0	4.6								

Table 2-J: Fuel

Specify fuel characteristics and usage. Unit and stack numbering must correspond throughout the application package.

	Fuel Type (low sulfur Diesel,	Fuel Source: purchased commercial,		Specif	fy Units		
Unit No.	ultra low sulfur diesel, Natural Gas, Coal,)	pipeline quality natural gas, residue gas, raw/field natural gas, process gas (e.g. SRU tail gas) or other	Lower Heating Value (btu/scf)	Hourly Usage (scf)	Annual Usage (mmscf)	% Sulfur	% Ash
ENG1	Natural Gas	Field Gas	1154	32394.2	283.77	Negligible	0
ENG2	Natural Gas	Field Gas	1154	32394.2	283.77	Negligible	0
ENG3	Natural Gas	Field Gas	1154	32394.2	283.77	Negligible	0
ENG4	Natural Gas	Field Gas	1154	32394.2	283.77	Negligible	0
ENG5	Natural Gas	Field Gas	1154	32394.2	283.77	Negligible	0
ENG6	Natural Gas	Field Gas	1154	32394.2	283.77	Negligible	0
ENG7	Natural Gas	Field Gas	1154	32394.2	283.77	Negligible	0
ENG8	Natural Gas	Field Gas	1154	32394.2	283.77	Negligible	0
ENG9	Natural Gas	Field Gas	1154	32394.2	283.77	Negligible	0
ENG11	Natural Gas	Field Gas	1154	9681.1	84.81	Negligible	0
ENG12	Natural Gas	Field Gas	1154	9681.1	84.81	Negligible	0
HTR1	Natural Gas	Field Gas	1154	590.9	5.18	Negligible	0
RB1	Natural Gas	Field Gas	1154	1575.7	13.80	Negligible	0
RB2	Natural Gas	Field Gas	1154	1575.7	13.80	Negligible	0
RB3	Natural Gas	Field Gas	1154	1575.7	13.80	Negligible	0
FL1	Natural Gas	Field Gas	1154	1906.3	16.70	Negligible	0
FL2	Natural Gas	Field Gas	1154	1906.3	16.70	Negligible	0
VC1	Natural Gas	Field Gas	1154	3812.5	33.40	Negligible	0

Table 2-K: Liquid Data for Tanks Listed in Table 2-L

For each tank, list the liquid(s) to be stored in each tank. If it is expected that a tank may store a variety of hydrocarbon liquids, enter "mixed hydrocarbons" in the Composition column for that tank and enter the corresponding data of the most volatile liquid to be stored in the tank. If tank is to be used for storage of different materials, list all the materials in the "All Calculations" attachment, run the newest version of TANKS on each, and use the material with the highest emission rate to determine maximum uncontrolled and requested allowable emissions rate. The permit will specify the most volatile category of liquids that may be stored in each tank. Include appropriate tank-flashing modeling input data. Use additional sheets if necessary. Unit and stack numbering must correspond throughout the application package.

					Vapor	Average Stor	age Conditions	Max Storage Conditions		
Tank No.	SCC Code	Material Name	Composition	Liquid Density (lb/gal)	Molecular Weight (lb/lb*mol)	Temperature (°F)	True Vapor Pressure (psia)	Temperature (°F)	True Vapor Pressure (psia)	
SKT1	40400311	Produced Water	Produced Water	8.2	50	72.74	11.14	82.04	12.88	
SKT2	40400311	Produced Water	Produced Water	8.2	50	72.74	11.14	82.04	12.88	
OT1	40400311	Condensate	Condensate	6.6	55	69.43	9.14	78.60	10.63	
OT2	40400311	Condensate	Condensate	6.6	55	69.43	9.14	78.60	10.63	
OT3	40400311	Condensate	Condensate	6.6	55	69.43	9.14	78.60	10.63	
OT4	40400311	Condensate	Condensate	6.6	55	69.43	9.14	78.60	10.63	
WT1	40400315	Produced Water	Produced Water	8.2	0	73.51	12.87	82.69	14.43	
WT2	40400315	Produced Water	Produced Water	8.2	0	73.51	12.87	82.69	14.43	

Table 2-L: Tank Data

Include appropriate tank-flashing modeling input data. Use an addendum to this table for unlisted data categories. Unit and stack numbering must correspond throughout the application package. Use additional sheets if necessary. See reference Table 2-L2. Note: 1.00 bbl = 10.159 M3 = 42.0 gal

Tank No.	Date Installed	Materials Stored	Seal Type (refer to Table 2- LR below)	Roof Type (refer to Table 2- LR below)	Сара	acity	Diameter (M)	Vapor Space		lor ble VI-C)	Paint Condition (from Table VI-	Annual Throughput	Turn- overs
			LK below)	LK below)	(bbl)	(M ³)		(M)	Roof	Shell	C)	(gal/yr)	(per year)
SKT1	Sep-20	Produced Water	N/A	FX	1000 bbl	159	4.75	9.1	Tan	Tan	Good	2,660,433	63
SKT2	TBD	Produced Water	N/A	FX	1000 bbl	159	4.75	9.1	Tan	Tan	Good	2,660,433	63
OT1	Sep-20	Condensate	N/A	FX	500 bbl	79.5	3.66	4.9	Tan	Tan	Good	3,120,436	149
OT2	Sep-20	Condensate	N/A	FX	500 bbl	79.5	3.66	4.9	Tan	Tan	Good	3,120,436	149
OT3	Sep-20	Condensate	N/A	FX	500 bbl	79.5	3.66	4.9	Tan	Tan	Good	3,120,436	149
OT4	Sep-20	Condensate	N/A	FX	500 bbl	79.5	3.66	4.9	Tan	Tan	Good	3,120,436	149
WT1	Sep-20	Produced Water	N/A	FX	500 bbl	79.5	3.66	4.9	Tan	Tan	Good	2,614,573	125
WT2	Sep-20	Produced Water	N/A	FX	500 bbl	79.5	3.66	4.9	Tan	Tan	Good	2,614,573	125
	<u> </u>												
								-					
								-					
													1

Roof Type	Seal Type, W	elded Tank Seal Type	Seal Type, Rive	Roof, Shell Color	Paint Condition				
FX: Fixed Roof	Mechanical Shoe Seal	Liquid-mounted resilient seal	Vapor-mounted resilient seal	Seal Type	WH: White	Good			
IF: Internal Floating Roof	A: Primary only	A: Primary only	A: Primary only	A: Mechanical shoe, primary only	AS: Aluminum (specular)	Poor			
EF: External Floating Roof	B: Shoe-mounted secondary	B: Weather shield	B: Weather shield	B: Shoe-mounted secondary	AD: Aluminum (diffuse)				
P: Pressure	C: Rim-mounted secondary	C: Rim-mounted secondary	C: Rim-mounted secondary	C: Rim-mounted secondary	LG: Light Gray				
					MG: Medium Gray				
Note: 1.00 bbl = 0.159 M	Note: $1.00 \text{ bbl} = 0.159 \text{ M}^3 = 42.0 \text{ gal}$								
					OT: Other (specify)				

Table 2-L2: Liquid Storage Tank Data Codes Reference Table

Table 2-M: Materials Processed and Produced	d (Use additional sheets as necessary.)
Matarial Dropaggad	Matani

	Materi	Material Produced						
Description	Chemical Composition	Chemical Composition Phase (Gas, Liquid, or Solid) Quantity (spec		Description	Chemical Composition	Phase	Quantity (specify units)	
Mixed Hydrocarbons	Oil (BOPD) Liquid		814	Mixed Hydrocarbons	Oil (BOPD)	Liquid	814	
	Produced Water (BWPD)	Liquid	341		Produced Water (BWPD)	Liquid	341	
	Natural Gas (MMSCFD)	Gas	240		Natural Gas (MMSCFD)	Gas	240	

Table 2-N: CEM Equipment

Enter Continuous Emissions Measurement (CEM) Data in this table. If CEM data will be used as part of a federally enforceable permit condition, or used to satisfy the requirements of a state or federal regulation, include a copy of the CEM's manufacturer specification sheet in the Information Used to Determine Emissions attachment. Unit and stack numbering must correspond throughout the application package. Use additional sheets if necessary.

Stack No.	Pollutant(s)	Manufacturer	Model No.	Serial No.	Sample Frequency	Averaging Time	Range	Sensitivity	Accuracy
N/A									

Table 2-O: Parametric Emissions Measurement Equipment

Unit and stack numbering must correspond throughout the application package. Use additional sheets if necessary.

Unit No.	Parameter/Pollutant Measured	Location of Measurement	Unit of Measure	Acceptable Range	Frequency of Maintenance	Nature of Maintenance	Method of Recording	Averaging Time
N/A								

Table 2-P: Greenhouse Gas Emissions

Applications submitted under 20.2.70, 20.2.72, & 20.2.74 NMAC are required to complete this Table. Power plants, Title V major sources, and PSD major sources must report and calculate all GHG emissions for each unit. Applicants must report potential emission rates in short tons per year (see Section 6.a for assistance). Include GHG emissions during Startup, Shutdown, and Scheduled Maintenance in this table. For minor source facilities that are not power plants, are not Title V, or are not PSD, there are three options for reporting GHGs 1) report GHGs for each individual piece of equipment; 2) report all GHGs from a group of unit types, for example report all combustion source GHGs as a single unit and all venting GHG as a second separate unit; OR 3) check the following box \square By checking this box, the applicant acknowledges the total CO2e emissions are less than 75,000 tons per year.

		CO ₂ ton/yr	N2O ton/yr	CH ₄ ton/yr	SF ₆ ton/yr	PFC/HFC ton/yr ²					GH	otal G Mass s ton/yr ⁴	Total CO ₂ e ton/yr ⁵
Unit No.	GWPs ¹	1	298	25	22,800	footnote 3							
ENG1	mass GHG	21967.59	0.04	0.36							219	968.0	
LINGI	CO ₂ e	21967.593	10.758167	9.0253076									21987.4
ENG2	mass GHG	21967.59	0.04	0.36							219	968.0	
	CO ₂ e	21967.59	10.76	9.03							 		21987.4
ENG3	mass GHG	21967.59	0.04	0.36			 				219	968.0	50000000
	CO ₂ e												500000.0
ENG4	mass GHG	21967.59	0.04	0.36				1			219	968.0	21007.4
	CO ₂ e mass GHG	21967.59 21967.59	10.76 0.04	9.03 0.36							21/	968.0	21987.4
ENG5	CO ₂ e	21967.593	10.758167	9.0253076			 -				21	/68.0	21987.4
	mass GHG	21907.595	0.04	0.36							210	968.0	21967.4
ENG6	CO ₂ e	21967.59	10.76	9.03							21;	/08.0	21987.4
	mass GHG	21967.59	0.04	0.36							210	968.0	21707.4
ENG7	CO ₂ e	21967.593	10.758167	9.0253076					1		21,	/00.0	21987.4
	mass GHG	21967.59	0.04	0.36							219	968.0	2170711
ENG8	CO ₂ e	21967.59	10.76	9.03							21	0010	21987.4
-	mass GHG	21967.59	0.04	0.36							219	968.0	
ENG9	CO ₂ e	21967.593	10.758167										21987.4
TNG11	mass GHG	6689.35	0.01	0.11							66	89.5	
ENG11	CO ₂ e	6689.35	3.22	2.70									6695.3
ENG12	mass GHG	6689.35	0.01	0.11							66	89.5	
ENG12	CO ₂ e	6689.3492	3.2151031	2.6972342									6695.3
HTR1	mass GHG	519.34	0.00	0.32							5	19.7	
IIIKI	CO ₂ e	519.34	0.22	7.95									527.5
RB1	mass GHG	1384.91	0.00	0.85							13	85.8	
KDI	CO ₂ e	1384.9065	0.5755123	21.209347									1406.7
RB2	mass GHG	1384.91	0.00	0.85							13	85.8	
	CO ₂ e	1384.91	0.58	21.21									1406.7
RB3	mass GHG	1384.91	0.00	0.85			 				13	85.8	11065
	CO ₂ e	1384.9065	0.5755123	21.209347							10	150.1	1406.7
FL1	mass GHG	10445.31	0.01	12.77							104	458.1	107(0.1
	CO ₂ e	10445.31	4.46	319.35							_10	450 1	10769.1
FL2	mass GHG	10445.31	0.01	12.77			 				104	458.1	10760.1
	CO ₂ e mass GHG	10445.308 20890.62	4.4619051 0.03	319.35375 25.55							204	916.2	10769.1
VC1	CO ₂ e	20890.62	8.92	25.55 638.71			 				209	/10.2	21538.2
	mass GHG	20890.82	0	57							25	7,600	21330.2
Total	CO ₂ e		123	1,436							25	,000	259,101
	CO ₂ e	257,542	125	1,430									259,101

¹GWP (Global Warming Potential): Applicants must use the most current GWPs codified in Table A-1 of 40 CFR part 98. GWPs are subject to change, therefore, applicants need to check 40 CFR 98 to confirm GWP values.

² For HFCs or PFCs describe the specific HFC or PFC compound and use a separate column for each individual compound.

³ For each new compound, enter the appropriate GWP for each HFC or PFC compound from Table A-1 in 40 CFR 98.

⁴ Green house gas emissions on a mass basis is the ton per year green house gas emission before adjustment with its GWP.

⁵ CO₂e means Carbon Dioxide Equivalent and is calculated by multiplying the TPY mass emissions of the green house gas by its GWP.

⁶ For Heaters/Boilers, CO₂ CH4, N2O emissions calculated according to §98.233(z)(1) and (2).

Tab 3Section 3 - Application Summary

Section 3

Application Summary

The <u>Application Summary</u> shall include a brief description of the facility and its process, the type of permit application, the applicable regulation (i.e. 20.2.72.200.A.X, or 20.2.73 NMAC) under which the application is being submitted, and any air quality permit numbers associated with this site. If this facility is to be collocated with another facility, provide details of the other facility including permit number(s). In case of a revision or modification to a facility, provide the lowest level regulatory citation (i.e. 20.2.72.219.B.1.d NMAC) under which the revision or modification is being requested. Also describe the proposed changes from the original permit, how the proposed modification will affect the facility's operations and emissions, de-bottlenecking impacts, and changes to the facility's major/minor status (both PSD & Title V).

The <u>**Process Summary</u>** shall include a brief description of the facility and its processes.</u>

<u>Startup, Shutdown, and Maintenance (SSM)</u> routine or predictable emissions: Provide an overview of how SSM emissions are accounted for in this application. Refer to "Guidance for Submittal of Startup, Shutdown, Maintenance Emissions in Permit Applications (http://www.env.nm.gov/aqb/permit/app_form.html) for more detailed instructions on SSM emissions.

XTO Energy Inc. is planning modification of the Bulldog Compressor Station in Eddy County, NM. The facility is a typical compressor station with natural gas engines, dehydration, storage tanks, and flares. Site construction is planned under NSR Permit 8153. This is a New Source Review permit application being submitted in accordance with 20.2.72 NMAC.

Routine SSM combustion emissions are included with the regular emissions of the facility. SSM emissions from equipment maintenance are routed to either the low pressure or high pressure flare header (FL1/FL2). SSM-related VOC emissions (tank landings/cleanings) are included at a rate of 10 tons per year per NMAQB guidance. Detailed calculations are included in the application.

The facility is proposing the following modifications:

- 1) Remove HTR2 and HTR3;
- 2) Remove ENG10 and ENG13;
- 3) Increase glycol circulation rate for DEHY1-3;
- 4) Decrease glycol regenerator reboiler (RB1-RB3) unit heat input from 3 MMBtu/hr to 2.0 MMBtu/hr;
- 5) Increase flare purge gas rates;
- 6) Remove FL3;
- 7) Update FL1-FL2 heights to 145';
- 8) Update tank throughputs;
- 9) Decrease condensate truck loading;
- 10) Add inlet gas flaring;
- 11) Increasing steady state flaring associated with increased tank throughput and glycol circulation rate; update sources that vent to flare.
- 12) Change sources that vent to VC1, only combusts vapors from DEHY1-3 still vent and pilot gas.
- 13) Update ENG1-9 and ENG11-12 VOC/formaldehyde/CO control efficiencies and update emissions factors from Caterpillar Gas Engine Rating Pro (GERP) analysis.
- 14) Update nomenclature of Gb1a and GB2a to SKT1 and SKT2.
- 15) Update facility location coordinates
- 16) Update low pressure separator pressure from 2 psig to 15 psig.
- 17) Added VOC malfunction emissions.

Tab 4 Section 4 - Process Flow Sheet

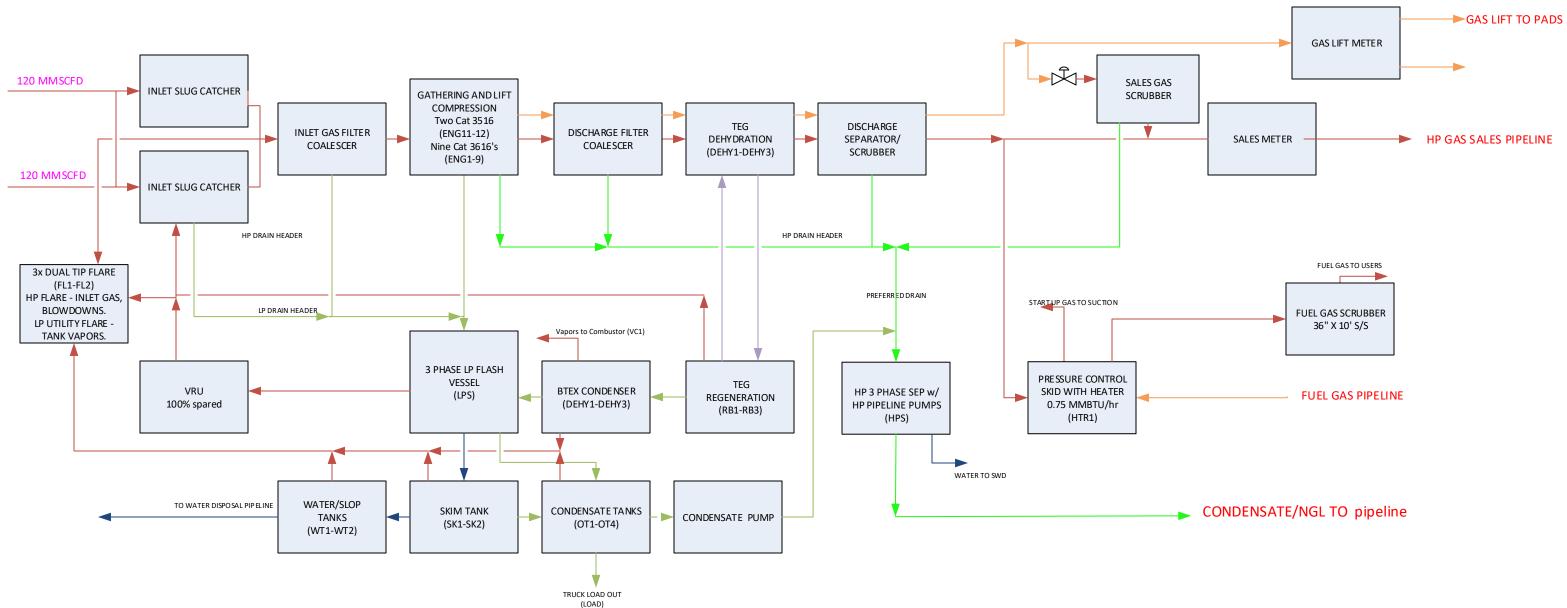
Section 4

Process Flow Sheet

A **process flow sheet** and/or block diagram indicating the individual equipment, all emission points and types of control applied to those points. The unit numbering system should be consistent throughout this application.

A process flow diagram is presented on the following page.

XTO DELAWARE BASIN GEN 2 COMPRESSOR STATION



REV 11/19/19

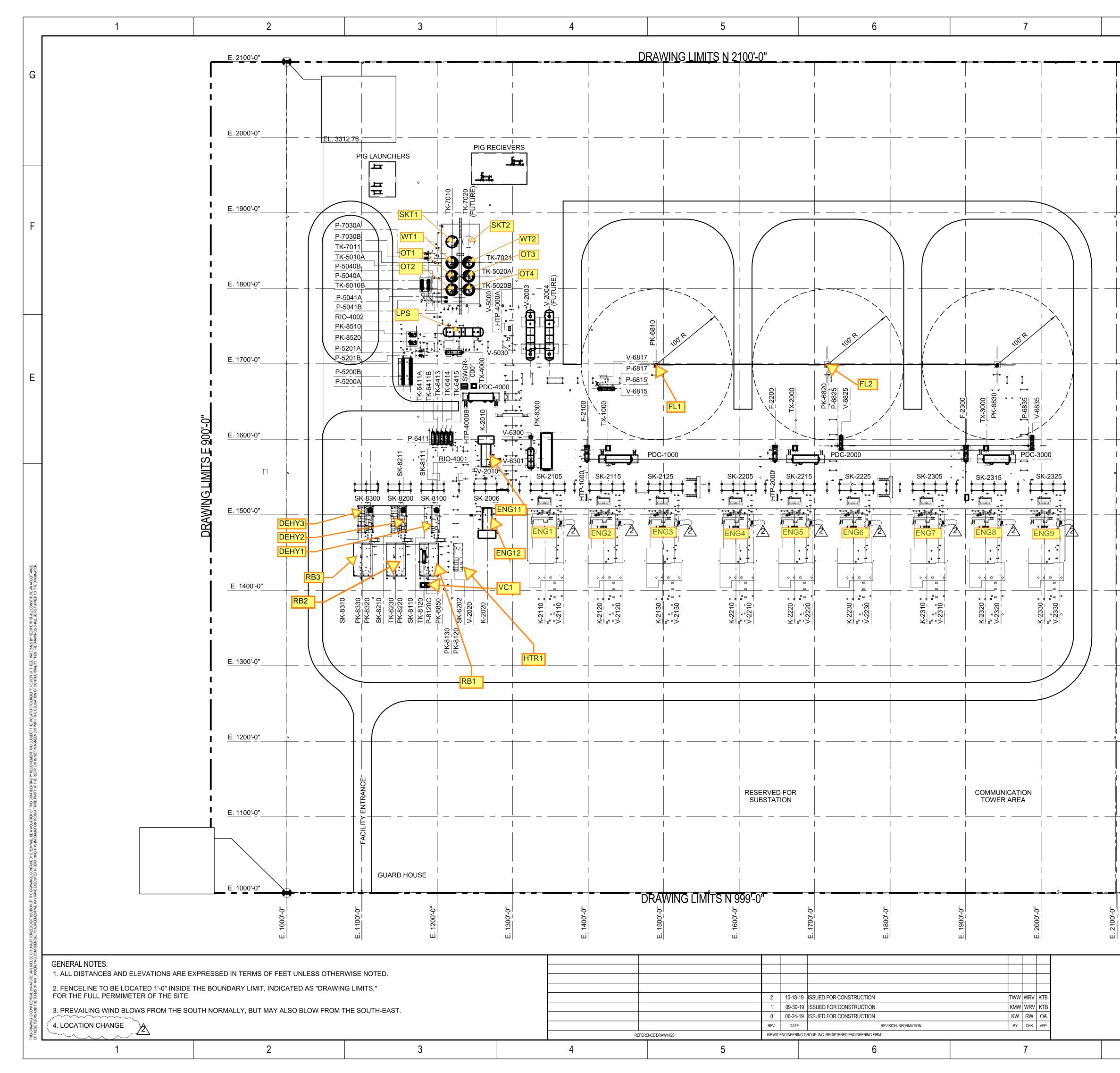
Tab 5 Section 5 - Plot Plan Drawn To Scale

Section 5

Plot Plan Drawn To Scale

A <u>plot plan drawn to scale</u> showing emissions points, roads, structures, tanks, and fences of property owned, leased, or under direct control of the applicant. This plot plan must clearly designate the restricted area as defined in UA1, Section 1-D.12. The unit numbering system should be consistent throughout this application.

A proposed plot plan is presented on the following page.



STD_BRD_24x36

8	9			10	
•			Tag	Description	-]
		K-2010 K-2020		START-UP COMPRESSOR 1 START-UP COMPRESSOR 2]
N 2100' 0" ———		K-2110		TRAIN 1 COMPRESSOR 1	
		K-2120 K-2130		TRAIN 1 COMPRESSOR 2 TRAIN 1 COMPRESSOR 3	— G
		K-2210 K-2220		TRAIN 2 COMPRESSOR 1 TRAIN 2 COMPRESSOR 2	
		K-2230		TRAIN 2 COMPRESSOR 3	
		K-2310 K-2320		TRAIN 3 COMPRESSOR 1 TRAIN 3 COMPRESSOR 2	
N 2000' 0"		K-2330 P-5040A		TRAIN 3 COMPRESSOR 3 LP CONDENSATE TRANSFER PUMP	
		P-5040B		LP CONDENSATE TRANSFER PUMP	
		P-5041A P-5041B		BOOSTER PUMP BOOSTER PUMP	
		P-5200A		CONDENSATE PIPELINE PUMP	
		P-5200B P-5201A		CONDENSATE PIPELINE PUMP CONDENSATE PIPELINE TRANSFER PUMP	
		P-5201B P-6411		CONDENSATE PIPELINE TRANSFER PUMP DAY TANK SUMP PUMP	
N 1900' 0"		P-6815 P-6817		TRAIN 1 HP FLARE KNOCK-OUT PUMP TRAIN 1 LP FLARE KNOCK-OUT PUMP	
		P-6825		TRAIN 2 HP FLARE KNOCK-OUT PUMP	I F
		P-6835 P-7030A		TRAIN 3 HP FLARE KNOCK-OUT PUMP PRODUCED WATER PUMP	
		P-7030B PK-6300		PRODUCED WATER PUMP INSTRUMENT AIR SKID	
		PK-6810		TRAIN 1 HP/LP FLARE PACKAGE	
		PK-6820 PK-6830		TRAIN 2 HP FLARE PACKAGE TRAIN 3 HP FLARE PACKAGE	
N 1800' 0"		PK-6850 PK-8130		THERMAL OXIDIZER PACKAGE BTEX PACKAGE	
		PK-8230		BTEX PACKAGE	
		PK-8330 PK-8510		BTEX PACKAGE VAPOR RECOVERY UNIT	
i		PK-8520 SK-6202		VAPOR RECOVERY UNIT FUEL GAS SKID]
		SK-8110		DISCHARGE FILTER SKID]
N 1700' 0"		SK-8111 PK-8120		TEG CONTACTOR/SCRUBBER SKID TEG REGEN PACKAGE TRAIN 0	
		SK-8210 SK-8211		DISCHARGE FILTER SKID TEG CONTACTOR/SCRUBBER SKID	
		PK-8220		TEG REGEN PACKAGE TRAIN 1	╡╵
		SK-8310 SK-8311		DISCHARGE FILTER SKID TEG CONTACTOR/SCRUBBER SKID	
		<u>PK-8320</u> TK-6411A		TEG REGEN PACKAGE TRAIN 3 COMPRESSOR OIL TANK	_
)0		TK-6411B TK-6413		COMPRESSOR OIL TANK ENGINE OIL TANK	
N 1600' 0" -OC		TK-6414		ENGINE COOLANT TANK	
i iii		TK-6415 TK-7010		METHANOL TANK SKIM TANK	
L S		TK-8120 V-2003		GLYCOL MAKE-UP TANK INLET SLUG CATCHER	
		V-2004		INLET SLUG CATCHER (FUTURE)	
		V-2010 V-2020		START-UP COMPRESSOR 1 BLOWCASE START-UP COMPRESSOR 2 BLOWCASE	
N 1500' 0"		V-2110		TRAIN 1 COMPRESSOR 1 BLOWCASE	
→→N 1500' 0"		V-2120 V-2130		TRAIN 1 COMPRESSOR 2 BLOWCASE TRAIN 1 COMPRESSOR 3 BLOWCASE	
		V-2210 V-2220		TRAIN 2 COMPRESSOR 1 BLOWCASE TRAIN 2 COMPRESSOR 2 BLOWCASE	
		V-2230		TRAIN 2 COMPRESSOR 3 BLOWCASE	
		V-2310 V-2320		TRAIN 3 CONFRESSOR 2 BLOWGASE	
		V-2330 V-5000		TRAIN 3 COMPRESSOR 3 BLOWCASE L.P. 3-PHASE SEPARATOR	
N 1400' 0"		V-5030		H.P. 3-PHASE SEPARATOR	
		V-6300 V-6301		WET AIR RECEIVER DRY AIR VOLUME TANK	
		V-6815 V-6817		TRAIN 1 HP FLARE KNOCK-OUT DRUM TRAIN 1 LP FLARE KNOCK-OUT DRUM	
		V-6825		TRAIN 2 HP FLARE KNOCK-OUT DRUM	
		V-6835 F-2100		TRAIN 3 HP FLARE KNOCK-OUT DRUM TRAIN 1 INLET GAS FILTER COALESCER	
		F-2200 F-2300		TRAIN 2 INLET GAS FILTER COALESCER TRAIN 3 INLET GAS FILTER COALESCER	
N 1300' 0"		TK-5010A		CONDENSATE TANK]
		<u>TK-5010B</u> TK-5020A		CONDENSATE TANK CONDENSATE TANK	C
		<u>TK-5020B</u> TK-7011		CONDENSATE TANK WATER TANK	
		TK-7021		WATER TANK	
		PDC-1000 HTP-1000		POWER DISTRIBUTION CENTER HEAT TRACE PANEL BOARD	
		TX-1000 PDC-2000		TRANSFORMER POWER DISTRIBUTION CENTER]
N 1200' 0" ■		HTP-2000		HEAT TRACE PANEL BOARD	
		TX-2000 PDC-3000		TRANSFORMER POWER DISTRIBUTION CENTER	
		HTP-3000 TX-3000		HEAT TRACE PANEL BOARD TRANSFORMER	
		PDC-4000		POWER DISTRIBUTION CENTER	
l I		HTP-4000 TX-4000		HEAT TRACE PANEL BOARD TRANSFORMER	
N 1100' 0"					
					В
N 1000' 0"					
1		60' 30'	0	60' 120'	
			1"=	60'	
1					
DISCIPLINE APP			XTU	ENERGY	-
PROCESS				MPRESSOR STATION	
PROCESS SAFETY MECHANICAL	ENERGY -	LUI		Y PLOT PLAN	A
PIPING CIVIL/STRUCTURAL					
18C		I: CARLSBAD, NM		SCALE: 1"=60'	
	Kiewit Engineering Group, Inc. Oil, Gas & Chemical	,		F	REV.
	Uil, Gas & Chemical		LH-0		2
0				STD BRD 24x36	

Tab 6Section 6 - All Calculations

Section 6

All Calculations

Show all calculations used to determine both the hourly and annual controlled and uncontrolled emission rates. All calculations shall be performed keeping a minimum of three significant figures. Document the source of each emission factor used (if an emission rate is carried forward and not revised, then a statement to that effect is required). If identical units are being permitted and will be subject to the same operating conditions, submit calculations for only one unit and a note specifying what other units to which the calculations apply. All formulas and calculations used to calculate emissions must be submitted. The "Calculations" tab in the UA2 has been provided to allow calculations to be linked to the emissions tables. Add additional "Calc" tabs as needed. If the UA2 or other spread sheets are used, all calculation spread sheet(s) shall be submitted electronically in Microsoft Excel compatible format so that formulas and input values can be checked. Format all spread sheets are not used, provide the original formulas with defined variables. Additionally, provide subsequent formulas showing the input values for each variable in the formula. All calculations, including those calculations are imbedded in the Calc tab of the UA2 portion of the application, the printed Calc tab(s), should be submitted under this section.

Tank Flashing Calculations: The information provided to the AQB shall include a discussion of the method used to estimate tank-flashing emissions, relative thresholds (i.e., NOI, permit, or major source (NSPS, PSD or Title V)), accuracy of the model, the input and output from simulation models and software, all calculations, documentation of any assumptions used, descriptions of sampling methods and conditions, copies of any lab sample analysis. If Hysis is used, all relevant input parameters shall be reported, including separator pressure, gas throughput, and all other relevant parameters necessary for flashing calculation.

SSM Calculations: It is the applicant's responsibility to provide an estimate of SSM emissions or to provide justification for not doing so. In this Section, provide emissions calculations for Startup, Shutdown, and Routine Maintenance (SSM) emissions listed in the Section 2 SSM and/or Section 22 GHG Tables and the rational for why the others are reported as zero (or left blank in the SSM/GHG Tables). Refer to "Guidance for Submittal of Startup, Shutdown, Maintenance Emissions in Permit Applications (http://www.env.nm.gov/aqb/permit/app_form.html) for more detailed instructions on calculating SSM emissions. If SSM emissions are greater than those reported in the Section 2, Requested Allowables Table, modeling may be required to ensure compliance with the standards whether the application is NSR or Title V. Refer to the Modeling Section of this application for more guidance on modeling requirements.

Glycol Dehydrator Calculations: The information provided to the AQB shall include the manufacturer's maximum design recirculation rate for the glycol pump. If GRI-Glycalc is used, the full input summary report shall be included as well as a copy of the gas analysis that was used.

Road Calculations: Calculate fugitive particulate emissions and enter haul road fugitives in Tables 2-A, 2-D and 2-E for:

- 1. If you transport raw material, process material and/or product into or out of or within the facility and have PER emissions greater than 0.5 tpy.
- 2. If you transport raw material, process material and/or product into or out of the facility more frequently than one round trip per day.

Significant Figures:

A. All emissions standards are deemed to have at least two significant figures, but not more than three significant figures.

B. At least 5 significant figures shall be retained in all intermediate calculations.

C. In calculating emissions to determine compliance with an emission standard, the following rounding off procedures shall be used:

- (1) If the first digit to be discarded is less than the number 5, the last digit retained shall not be changed;
- (2) If the first digit discarded is greater than the number 5, or if it is the number 5 followed by at least one digit other than the number zero, the last figure retained shall be increased by one unit; **and**
- (3) If the first digit discarded is exactly the number 5, followed only by zeros, the last digit retained shall be rounded upward if it is an odd number, but no adjustment shall be made if it is an even number.
- (4) The final result of the calculation shall be expressed in the units of the standard.

Control Devices: In accordance with 20.2.72.203.A(3) and (8) NMAC, 20.2.70.300.D(5)(b) and (e) NMAC, and 20.2.73.200.B(7) NMAC, the permittee shall report all control devices and list each pollutant controlled by the control device

XTO Energy Inc.

Bulldog Compressor Station

regardless if the applicant takes credit for the reduction in emissions. The applicant can indicate in this section of the application if they chose to not take credit for the reduction in emission rates. For notices of intent submitted under 20.2.73 NMAC, only uncontrolled emission rates can be considered to determine applicability unless the state or federal Acts require the control. This information is necessary to determine if federally enforceable conditions are necessary for the control device, and/or if the control device produces its own regulated pollutants or increases emission rates of other pollutants.

Caterpillar 3616TA (ENG-1 to ENG-9) and 3516TA (ENG-11 to ENG-12)

Emission factors for nitrogen oxides (NOx), carbon monoxide (CO), formaldehyde, and volatile organic compounds (VOC) are based on manufacturer's data. Emissions of particulate matter (PM/PM_{10} and $PM_{2.5}$) were calculated using AP-42 Table 3.2-3 factors. PM_{10} and $PM_{2.5}$ emissions are set equal to PM emissions. SO₂ emissions are based on the units' fuel consumption and a sulfur content of 5 grains per 100 standard cubic feet (5 gr/100 scf). Hazardous Air Pollutants (HAPs) except for formaldehyde were calculated using AP-42 factors.

Line Heater (HTR1) and Glycol Regenerator Heaters (RB1 to RB3)

Emission of NOx, CO, VOC, HAP, and $PM/PM_{10}/PM_{2.5}$ are based on AP-42 Table 3.2-3 emission factors. PM_{10} and $PM_{2.5}$ emissions are set equal to PM emissions. SO_2 emissions were based on the unit's fuel consumption and a maximum sulfur content of 5 grains per 100 standard cubic feet (5 gr/100 scf).

SSM/Emergency Flares (FL1 – FL2)

The facility will use two (2) dual-tip flares. NOx and CO emissions are based on factors from the Texas Commission on Environmental Quality (TCEQ) publication RG-360A/09. VOC emissions were calculated using a material balance and the manufacturer's guaranteed destruction efficiency (98%). Since gas can be routed to any or all of the flares, they are illustrated as one combine emission point. The flares have a control efficiency of 98%, with manufacturer documentation provided in Section 7 of the application. SSM activities routed to the flares could include process vessel purging and maintenance blowdowns for process equipment, high pressure gas flaring, and low pressure separator gas during VRU downtime. Tank vapors and 2% of the low pressure separator gas not collected by the VRU are continuously routed to the low pressure side of the flare.

Triethylene Glycol Dehydrators (DEHY1-DEHY3)

Emissions from the dehydrators are calculated using BR&E ProMax simulation software. Flash tank vapors are routed back to mixing with the inlet gas. Each dehydrator is equipped with a condenser. Condensed liquids are routed to the skim tank and any remaining gas is burned at the vapor combustor (VC1). The emissions being released at VC1 from the dehydration process are represented as a separate emission point (DEHY1-DEHY3).

Storage Tanks (SKT1-SKT2, OT1-OT4, WT1-WT2)

Flashing, working and breathing emissions from the skim tank, oil tanks, and water tanks were calculated using BR&E ProMax simulation software. Emissions from the tanks are controlled using FL1-FL2. The simulation reports are included in Section 7.

Truck Loading (LOAD)

Uncontrolled emissions from oil loading of trucks were calculated using Equation 1 of AP-42 Section 5.2. Maximum slop oil loading rates are calculated using 814 BOPD for 100 days of the year. Relevant portions of AP-42 Section 5.2 are included in Section 7. Oil truck loading will be uncontrolled.

Piping Component Fugitive Emissions (FUG)

Facility fugitive emissions were calculated using TCEQ's "Air Permit Technical Guidance for Chemical Sources – Fugitive Guidance" document, and conservatively assumed component counts. Reduction efficiencies were obtained from EPA's Protocol for Equipment Leak Emission Estimates (EPA-453/R-95-017). Relevant portions of the TCEQ document are included in Section 7.

Startup, Shutdown, and Maintenance (SSM)

SSM emissions not routed to the flare system were assumed equal to the flat 10 tpy of VOC per State guidance. Specific SSM emissions include small equipment blowdowns, tank emptying and refilling, tank roof landing, and miscellaneous activities. Other SSM emissions are routed to the flare and calculated in accordance with the flare methodology above.

Haul Road Fugitive Emissions

Fugitive haul road emissions were calculated using Equations 1a and 2 of AP-42 Section 13.2.2. Relevant portions of AP-42 Section 13.2.2 are included in Section 7.

Malfunction Emissions (MALFCUNTION)

Malfunction emissions not routed to the flare system were assumed equal to the flat 10 tpy of VOC per State guidance. Specific malfunction emissions include any sudden and unavoidable failure of air pollution control equipment or process equipment beyond the control of the owner or operator.

Section 6.a

Green House Gas Emissions

(Submitting under 20.2.70, 20.2.72 20.2.74 NMAC)

Title V (20.2.70 NMAC), Minor NSR (20.2.72 NMAC), and PSD (20.2.74 NMAC) applicants must estimate and report greenhouse gas (GHG) emissions to verify the emission rates reported in the public notice, determine applicability to 40 CFR 60 Subparts, and to evaluate Prevention of Significant Deterioration (PSD) applicability. GHG emissions that are subject to air permit regulations consist of the sum of an aggregate group of these six greenhouse gases: carbon dioxide (CO₂), nitrous oxide (N₂O), methane (CH₄), hydrofluorocarbons (HFCs), perfluorocarbons (PFCs), and sulfur hexafluoride (SF₆).

Calculating GHG Emissions:

1. Calculate the ton per year (tpy) GHG mass emissions and GHG CO₂e emissions from your facility.

2. GHG mass emissions are the sum of the total annual tons of greenhouse gases without adjusting with the global warming potentials (GWPs). GHG CO₂e emissions are the sum of the mass emissions of each individual GHG multiplied by its GWP found in Table A-1 in 40 CFR 98 <u>Mandatory Greenhouse Gas Reporting</u>.

3. Emissions from routine or predictable start up, shut down, and maintenance must be included.

4. Report GHG mass and GHG CO_2e emissions in Table 2-P of this application. Emissions are reported in <u>short</u> tons per year and represent each emission unit's Potential to Emit (PTE).

5. All Title V major sources, PSD major sources, and all power plants, whether major or not, must calculate and report GHG mass and CO2e emissions for each unit in Table 2-P.

6. For minor source facilities that are not power plants, are not Title V, and are not PSD there are three options for reporting GHGs in Table 2-P: 1) report GHGs for each individual piece of equipment; 2) report all GHGs from a group of unit types, for example report all combustion source GHGs as a single unit and all venting GHGs as a second separate unit; 3) or check the following \Box By checking this box, the applicant acknowledges the total CO2e emissions are less than 75,000 tons per year.

Sources for Calculating GHG Emissions:

- Manufacturer's Data
- AP-42 Compilation of Air Pollutant Emission Factors at http://www.epa.gov/ttn/chief/ap42/index.html
- EPA's Internet emission factor database WebFIRE at http://cfpub.epa.gov/webfire/

• 40 CFR 98 <u>Mandatory Green House Gas Reporting</u> except that tons should be reported in short tons rather than in metric tons for the purpose of PSD applicability.

• API Compendium of Greenhouse Gas Emissions Methodologies for the Oil and Natural Gas Industry. August 2009 or most recent version.

• Sources listed on EPA's NSR Resources for Estimating GHG Emissions at http://www.epa.gov/nsr/clean-air-act-permitting-greenhouse-gases:

Global Warming Potentials (GWP):

Applicants must use the Global Warming Potentials codified in Table A-1 of the most recent version of 40 CFR 98 Mandatory Greenhouse Gas Reporting. The GWP for a particular GHG is the ratio of heat trapped by one unit mass of the GHG to that of one unit mass of CO_2 over a specified time period.

"Greenhouse gas" for the purpose of air permit regulations is defined as the aggregate group of the following six gases: carbon dioxide, nitrous oxide, methane, hydrofluorocarbons, perfluorocarbons, and sulfur hexafluoride. (20.2.70.7 NMAC, 20.2.74.7 NMAC). You may also find GHGs defined in 40 CFR 86.1818-12(a).

Metric to Short Ton Conversion:

Short tons for GHGs and other regulated pollutants are the standard unit of measure for PSD and title V permitting programs. 40 CFR 98 <u>Mandatory Greenhouse Reporting</u> requires metric tons.

1 metric ton = 1.10231 short tons (per Table A-2 to Subpart A of Part 98 – Units of Measure Conversions)

				E	MISSIONS SU	MMARY TABI	.E								
	FACILITY		NI	Ox		20	VO	C	s	0 ₂	PM		HA	Pe	CO2e
EMISSION SOURCE DESCRIPTION	IDENTIFICATION NUMBER	STACK NUMBER	lb/hr	ТРҮ	lb/hr	ТРҮ	(INCLUDE		lb/hr	ТРҮ	lb/hr	0 & 2.5 TPY	lb/hr	TPY	ТРҮ
Caterpillar G3616 Natural Gas Compressor Engine	ENG1	ENG1	4.13	18.11	4.38	19.21	3.47	15.18	0.42	1.84	0.38	1.65	0.54	2.36	21987
Caterpillar G3616 Natural Gas Compressor Engine	ENG2	ENG2	4.13	18.11	4.38	19.21	3.47	15.18	0.42	1.84	0.38	1.65	0.54	2.36	21987
Caterpillar G3616 Natural Gas Compressor Engine	ENG3	ENG3	4.13	18.11	4.38	19.21	3.47	15.18	0.42	1.84	0.38	1.65	0.54	2.36	21987
Caterpillar G3616 Natural Gas Compressor Engine	ENG4	ENG4	4.13	18.11	4.38	19.21	3.47	15.18	0.42	1.84	0.38	1.65	0.54	2.36	21987
Caterpillar G3616 Natural Gas Compressor Engine	ENG5	ENG5	4.13	18.11	4.38	19.21	3.47	15.18	0.42	1.84	0.38	1.65	0.54	2.36	21987
Caterpillar G3616 Natural Gas Compressor Engine	ENG6	ENG6	4.13	18.11	4.38	19.21	3.47	15.18	0.42	1.84	0.38	1.65	0.54	2.36	21987
Caterpillar G3616 Natural Gas Compressor Engine	ENG7	ENG7	4.13	18.11	4.38	19.21	3.47	15.18	0.42	1.84	0.38	1.65	0.54	2.36	21987
Caterpillar G3616 Natural Gas Compressor Engine	ENG8	ENG8	4.13	18.11	4.38	19.21	3.47	15.18	0.42	1.84	0.38	1.65	0.54	2.36	21987
Caterpillar G3616 Natural Gas Compressor Engine	ENG9	ENG9	4.13	18.11	4.38	19.21	3.47	15.18	0.42	1.84	0.38	1.65	0.54	2.36	21987
Caterpillar 3516J TA Natural Gas Compressor Engine	ENG11	ENG11	1.90	8.33	1.01	4.42	1.29	5.63	0.13	0.55	0.11	0.49	0.32	1.39	6695
Caterpillar 3516J TA Natural Gas Compressor Engine	ENG12	ENG12	1.90	8.33	1.01	4.42	1.29	5.63	0.13	0.55	0.11	0.49	0.32	1.39	6695
Fuel Line Heater (0.75 MMBtu/hr)	HTR1	HTR1	0.11	0.50	0.10	0.42	0.01	0.03	0.01	0.04	0.01	0.04	0.002	0.01	528
Glycol Regenerator Reboiler (2.0 MMBtu/hr)	RB1	RB1	0.31	1.34	0.26	1.12	0.02	0.07	0.03	0.12	0.02	0.10	0.006	0.03	1407
Glycol Regenerator Reboiler (2.0 MMBtu/hr)	RB2	RB1	0.31	1.34	0.26	1.12	0.02	0.07	0.03	0.12	0.02	0.10	0.006	0.03	1407
Glycol Regenerator Reboiler (2.0 MMBtu/hr)	RB3	RB1	0.31	1.34	0.26	1.12	0.02	0.07	0.03	0.12	0.02	0.10	0.006	0.03	1407
Total Flare Pilot/Purge Emissions	FL1-FL2 Pilot	FL1-FL2 Pilot	0.67	2.93	1.33	5.84	0.94	4.13	0.01	0.03	0.03	0.13	0.01	0.04	3489
Total Flare Normal Operations	FL1-FL2 Norm	FL1-FL2 Norm	1.85	7.72	3.69	15.41	11.53	25.60	0.01	0.04	0.03	0.15	0.48	1.10	8057
Total Flare SSM	FL1-FL2 SSM	FL1-FL2 SSM	541.65	8.10	1081.35	16.17	992.97	18.36	4.91	0.08	22.25	0.31	27.52	0.55	9993
3TEX Vapor Combustor	VC1	VC1	0.41	1.80	0.82	3.59	2.61	11.43	0.29	1.26	0.010	0.04	0.32	1.38	2461
TEG Dehydrator with Condenser	DEHY1	VC1						Emis	sions Represe	ented at VC1					
TEG Dehydrator with Condenser	DEHY2	VC1						Emis	sions Repres	ented at VC1					
TEG Dehydrator with Condenser	DEHY3	VC1						Emis	sions Repres	ented at VC1					
Skim Tank	SKT1	FL1-FL2						Emissic	ons Represen	ted at FL1-FL	2				
Skim Tank (Backup)	SKT2	FL1-FL2	2 Emissions Represented at FL1-FL2												
Condensate Tank	OT1	FL1-FL2						Emissic	ons Represen	ted at FL1-FL	2				
Condensate Tank	OT2	FL1-FL2	Emissions Represented at FL1-FL2												

BULLDOG COMPRESSOR STATION

FACILITY EMISSIONS SUMMARY

				E	MISSIONS SU	MMARY TAB	LE								
EMISSION SOURCE DESCRIPTION	FACILITY IDENTIFICATION	STACK NUMBER	N	Ox	c	0	VC (INCLUDI		s	O ₂	PM	10 & 2.5	н	APs	CO2
	NUMBER		lb/hr	ТРҮ	lb/hr	ТРҮ	lb/hr	ТРҮ	lb/hr	ТРҮ	lb/hr	ТРҮ	lb/hr	ТРҮ	TPY
Condensate Tank	OT3	FL1-FL2						Emissi	ons Represen	ted at FL1-FL	.2				
Condensate Tank	OT4	FL1-FL2						Emissi	ons Represen	ted at FL1-FL	2				
Produced Water Tank	WT1	FL1-FL2						Emissi	ons Represen	ted at FL1-FL	2				
Produced Water Tank	WT2	FL1-FL2	Emissions Represented at FL1-FL2												
Low Pressure Separator	LPS	FL1-FL2	Emissions Represented at FL1-FL2												
Condensate Truck Loading	LOAD	N/A	-	-	-	-	65.70	11.14	-	-	-	-	0.03	0.01	-
Fugitive Emissions	FUG	N/A	_	-	-	-	4.89	21.43	-	-	-	-	0.38	1.64	-
SSM Activities	SSM	N/A	_	-	-	-	-	10.00	-	-	-	-	-	-	_
ROAD EMISSIONS	ROAD	ROAD	-	-	-	-	-	-	-	-	0.15	0.02	-	-	-
Malfunction Emissions	MALFUNCTION	MALFUNCTION	-	-	-	-	-	10.00	-	-	-	-	-	-	-
							NC								
			N	Ox	C	0	VC (INCLUD)		S	O ₂		10 & 2.5	H	APs	CO2
TOTAL FACILITY	WIDE EMISSIONS		lb/hr	ТРҮ	lb/hr	ТРҮ	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	ТРҮ	TPY
			586.62	204.66	1129.54	226.49	1112.48	260.24	9.34	19.49	26.16	16.80	34.24	28.84	240,02

BULLDOG COMPRESSOR STATION

FACILITY EMISSIONS SUMMARY

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BULLDOG COMPRESSOR STATION

Methodology for Burner Calculations

Burner Emission Calculations

AP 42 Emission Factors: Tables 1.4-1, 1.4-2, & 1.4-3

Emission Rate_x (lb/hr) = Burner Rating (MMBTU/hr) * EF_x (lb/MMSCF) / 1020 (Btu/scf) * Heating Value of Fuel Gas (BTU/SCF) / 1020 (Btu/scf) + 25%

Annual Emission Rate_X (TPY) = Emission Rate (lb/hr) * 8760 (hour/year) / 2000 (lb/ton)

Mass Balance - SO₂ & H₂S Calculations

 H_2S Mass Flow Rate (lb/hr) = P * V / 10.73 / T * MW_{GAS} * $H_2S_{WEIGHT \%}$ * (1 - DRE)

P = Pressure (psia), V = Fuel Consumed in a hour (ft^3/hr), 10.73 = Ideal Gas Constant, T = Temperature (°R)

Uncontrolled H₂S Mass Flow Rate (lb/hr) = P * V / 10.73 / T * MW_{GAS} * H₂S_{WEIGHT %}

SO₂ Emission Rate (lb/hr) = Uncontrolled H₂S Mass Rate (lb/hr) * SO₂ Conversion Efficiency * (MW of SO₂ (lb/lb-mol) / MW of H₂S (lb/lb-mol))

Annual Emission Rate (TPY) = Emission Rate (lb/hr) * 8760 (hour/year) / 2000 (lb/ton)

 MW_{GAS} = Molecular Weight of the Gas, $H_2S_{WEIGHT\%}$ = Weight Percent of the H_2S in the Fuel Gas, DRE = Burner Combustion Efficiency of H_2S

WILDCAT COMPRESSOR STATION

Methodology for Engine Calculations

Engine Emission Calculations

Manufacturer's Data or NSPS Subpart JJJJ Limit Calculations

Emission Rate_X (lb/hr) = Emission Factor_X (g/hp-hr) * Rated hp / 453.6 (g/lb)

Annual Emission $Rate_{X}$ (TPY) = Emission Rate (lb/hr) * 8760 (hour/year) / 2000 (lb/ton)

AP 42 Emission Factors

Emission Rate_X (lb/hr) = Fuel Consumption (MMBTU/hp-hr) * EF_X (lb/MMBTU) * Rated hp

Annual Emission Rate_{X} (TPY) = Emission Rate_{X} (lb/hr) * 8760 (hour/year) / 2000 (lb/ton)

WILDCAT COMPRESSOR STATION

Methodology for Flare Calculations

Flare Calculations

VOC Flare Calculations - Uses the Ideal Gas Law for Mixtures

The mass flow rate of VOCs to the flare were modeled using Promax. The mass rate was then reduced by the destruction efficiency of the flare (98%).

NOx & CO Calculations - TCEQ Emission Factors Used

NOx (lb/day) = Heating Value (BTU/ft³) * EF (lb/MMBTU) * V (ft³/Day) / 10^{6} (BTU/MMBTU)

CO (lb/day) = Heating Value (BTU/ft³) * EF (lb/MMBTU) * V (ft³/Day) / 10^{6} (BTU/MMBTU)

COEF = 0.5496 or 0.2755, NOxEF = 0.138, EF = Emission Factor, V = Volume of Gas in a Day

SO₂ & H₂S Calculations - Mass Balance

 H_2S Mass Flow Rate (lb/hr) = P * V / 10.73 / T * MW_{GAS} * $H_2S_{WEIGHT \%}$ * (1 - DRE)

P = Pressure (psia), V = Fuel Consumed in a hour (ft^3/hr), 10.73 = Ideal Gas Constant, T = Temperature (°R)

Uncontrolled H₂S Mass Flow Rate (lb/hr) = P * V / 10.73 / T * MW_{GAS} * H₂S_{WEIGHT %}

 SO_2 Emission Rate (lb/hr) = Uncontrolled H₂S Mass Rate (lb/hr) * SO_2 Conversion Efficiency * (MW of SO_2 (lb/lb-mol) / MW of H₂S (lb/lb-mol))

Annual Emission Rate (TPY) = Emission Rate (lb/hr) * 8760 (hour/year) / 2000 (lb/ton)

 MW_{GAS} = Molecular Weight of the Gas, $H_2S_{WEIGHT\%}$ = Weight Percent of the H_2S in Gas Stream, DRE = Flare Destruction Efficiency of H_2S

XTO ENERGY, INC. BULLDOG COMPRESSOR STATION COMPRESSOR ENGINES

									U	ncontrolle	d Emissio	ns Calc	ulation	S											
					M	anufactı	urer's Da	ata		AP-42 Facto	ors														
						g/hp	o-hr ²			lb/MMBtu	3,4				lb/hr ⁵							tpy ⁵			
Source ID	Unit Description	Annual Hours	Rated HP	MMbtu/hp- hr ¹ (HHV)	NOx	со	VOC	нсно	SO ₂	PM _{10 & 2.5}	Acetal- dehyde	NOx	CO	VOC	нсно	SO ₂	PM _{10 & 2.5}	Acetal- dehyde	NOx	СО	voc	НСНО	SO ₂	PM _{10 & 2.5}	Acetal- dehyde
ENG1	Caterpillar G3616 Natural Gas Compressor Engine	8760	5000	0.007476	0.30	3.06	0.87	0.15	0.01125	0.01006	0.00836	4.13	33.73	9.90	1.65	0.42	0.38	0.31	18.11	147.74	43.37	7.24	1.84	1.65	1.37
ENG2	Caterpillar G3616 Natural Gas Compressor Engine	8760	5000	0.007476	0.30	3.06	0.87	0.15	0.01125	0.01006	0.00836	4.13	33.73	9.90	1.65	0.42	0.38	0.31	18.11	147.74	43.37	7.24	1.84	1.65	1.37
ENG3	Caterpillar G3616 Natural Gas Compressor Engine	8760	5000	0.007476	0.30	3.06	0.87	0.15	0.01125	0.01006	0.00836	4.13	33.73	9.90	1.65	0.42	0.38	0.31	18.11	147.74	43.37	7.24	1.84	1.65	1.37
ENG4	Caterpillar G3616 Natural Gas Compressor Engine	8760	5000	0.007476	0.30	3.06	0.87	0.15	0.01125	0.01006	0.00836	4.13	33.73	9.90	1.65	0.42	0.38	0.31	18.11	147.74	43.37	7.24	1.84	1.65	1.37
ENG5	Caterpillar G3616 Natural Gas Compressor Engine	8760	5000	0.007476	0.30	3.06	0.87	0.15	0.01125	0.01006	0.00836	4.13	33.73	9.90	1.65	0.42	0.38	0.31	18.11	147.74	43.37	7.24	1.84	1.65	1.37
ENG6	Caterpillar G3616 Natural Gas Compressor Engine	8760	5000	0.007476	0.30	3.06	0.87	0.15	0.01125	0.01006	0.00836	4.13	33.73	9.90	1.65	0.42	0.38	0.31	18.11	147.74	43.37	7.24	1.84	1.65	1.37
ENG7	Caterpillar G3616 Natural Gas Compressor Engine	8760	5000	0.007476	0.30	3.06	0.87	0.15	0.01125	0.01006	0.00836	4.13	33.73	9.90	1.65	0.42	0.38	0.31	18.11	147.74	43.37	7.24	1.84	1.65	1.37
ENG8	Caterpillar G3616 Natural Gas Compressor Engine	8760	5000	0.007476	0.30	3.06	0.87	0.15	0.01125	0.01006	0.00836	4.13	33.73	9.90	1.65	0.42	0.38	0.31	18.11	147.74	43.37	7.24	1.84	1.65	1.37
ENG9	Caterpillar G3616 Natural Gas Compressor Engine	8760	5000	0.007476	0.30	3.06	0.87	0.15	0.01125	0.01006	0.00836	4.13	33.73	9.90	1.65	0.42	0.38	0.31	18.11	147.74	43.37	7.24	1.84	1.65	1.37
ENG11	Caterpillar 3516J TA Natural Gas Compressor Engine	8760	1380	0.008095	0.50	2.55	0.91	0.36	0.01125	0.01006	0.00836	1.90	7.76	3.96	1.10	0.13	0.11	0.09	8.33	33.98	17.33	4.80	0.55	0.49	0.41
ENG12	Caterpillar 3516J TA Natural Gas Compressor Engine	8760	1380	0.008095	0.50	2.55	0.91	0.36	0.01125	0.01006	0.00836	1.90	7.76	3.96	1.10	0.13	0.11	0.09	8.33	33.98	17.33	4.80	0.55	0.49	0.41

¹HHV is based on the Fuel Consumption Rate @ 75% Load from the Gas Engine Rating Pro Report

²The VOC emission factor (g/hp-hr) includes HCHO. Emission factors based on Gas Engine Rating Pro Report @ 100% Load.

³SO₂ Emissions were calculated using the emission factor from Table 3.2-2

⁴PM Emission Factor = 7.71E-05 lb/MMBTU + 7.71E-05 lb/MMBTU + 9.91E-03 lb/MMBTU = 0.01006 lb/MMBTU

⁵25% safety factor was added to NOx on all engines. 25% safety factor was added to VOC on 3516. VOC lb/hr rates include acetaldehyde emissions.

Total Emissions Per Pollutant (TPY)	NOx	СО	VOC	нсно	SO_2	PM _{10 & 2.5}	Acetal- dehyde
Total Emissions Fer Fonutant (TF 1)	179.60	1397.60	425.02	74.77	17.69	15.81	13.14

XTO ENERGY, INC. BULLDOG COMPRESSOR STATION COMPRESSOR ENGINES

Controlled Emissions Calculations

								171	anufactı (w/ co		ala		AP-42 Facto	ors														
					Cont	rol Efficio	ency (%)		g/hp	p-hr ²			lb/MMBtı	1 ³				lb/ł	ur ⁴						tpy	у		
Source ID	Unit Description	Annual Hours	Rated HP	MMbtu/hp- hr ¹ (HHV)	СО	VOC	нсон	NOx	CO	VOC ²	нсно	SO ₂	PM _{10 & 2.5}	Acetal- dehyde	NOx	CO	VOC	НСНО	SO ₂	PM _{10 & 2.5}	Acetal- dehyde	NOx	CO	VOC	нсно	SO ₂	PM _{10 & 2.5}	Ace dehy
ENG1	Caterpillar G3616 Natural Gas Compressor Engine	8760	5000	0.007476	87.0	65.0	74.0	0.30	0.40	0.30	0.04	0.0113	0.01006	0.00836	4.13	4.38	3.47	0.43	0.42	0.38	0.11	18.11	19.21	15.18	1.88	1.84	1.65	0.4
ENG2	Caterpillar G3616 Natural Gas Compressor Engine	8760	5000	0.007476	87.0	65.0	74.0	0.30	0.40	0.30	0.04	0.0113	0.01006	0.00836	4.13	4.38	3.47	0.43	0.42	0.38	0.11	18.11	19.21	15.18	1.88	1.84	1.65	0.4
ENG3	Caterpillar G3616 Natural Gas Compressor Engine	8760	5000	0.007476	87.0	65.0	74.0	0.30	0.40	0.30	0.04	0.0113	0.01006	0.00836	4.13	4.38	3.47	0.43	0.42	0.38	0.11	18.11	19.21	15.18	1.88	1.84	1.65	0.4
ENG4	Caterpillar G3616 Natural Gas Compressor Engine	8760	5000	0.007476	87.0	65.0	74.0	0.30	0.40	0.30	0.04	0.0113	0.01006	0.00836	4.13	4.38	3.47	0.43	0.42	0.38	0.11	18.11	19.21	15.18	1.88	1.84	1.65	0.4
ENG5	Caterpillar G3616 Natural Gas Compressor Engine	8760	5000	0.007476	87.0	65.0	74.0	0.30	0.40	0.30	0.04	0.0113	0.01006	0.00836	4.13	4.38	3.47	0.43	0.42	0.38	0.11	18.11	19.21	15.18	1.88	1.84	1.65	0.4
ENG6	Caterpillar G3616 Natural Gas Compressor Engine	8760	5000	0.007476	87.0	65.0	74.0	0.30	0.40	0.30	0.04	0.0113	0.01006	0.00836	4.13	4.38	3.47	0.43	0.42	0.38	0.11	18.11	19.21	15.18	1.88	1.84	1.65	0.4
ENG7	Caterpillar G3616 Natural Gas Compressor Engine	8760	5000	0.007476	87.0	65.0	74.0	0.30	0.40	0.30	0.04	0.0113	0.01006	0.00836	4.13	4.38	3.47	0.43	0.42	0.38	0.11	18.11	19.21	15.18	1.88	1.84	1.65	0.4
ENG8	Caterpillar G3616 Natural Gas Compressor Engine	8760	5000	0.007476	87.0	65.0	74.0	0.30	0.40	0.30	0.04	0.0113	0.01006	0.00836	4.13	4.38	3.47	0.43	0.42	0.38	0.11	18.11	19.21	15.18	1.88	1.84	1.65	0.4
ENG9	Caterpillar G3616 Natural Gas Compressor Engine	8760	5000	0.007476	87.0	65.0	74.0	0.30	0.40	0.30	0.04	0.0113	0.01006	0.00836	4.13	4.38	3.47	0.43	0.42	0.38	0.11	18.11	19.21	15.18	1.88	1.84	1.65	0.4
ENG11	Caterpillar 3516J TA Natural Gas Compressor Engine	8760	1380	0.008095	87.0	65.0	74.0	0.50	0.33	0.32	0.09	0.0113	0.01006	0.00836	1.90	1.01	1.29	0.28	0.13	0.11	0.03	8.33	4.42	5.63	1.25	0.55	0.49	0.1
ENG12	Caterpillar 3516J TA Natural Gas Compressor Engine	8760	1380	0.008095	87.0	65.0	74.0	0.50	0.33	0.32	0.09	0.0113	0.01006	0.00836	1.90	1.01	1.29	0.28	0.13	0.11	0.03	8.33	4.42	5.63	1.25	0.55	0.49	0.1

 ${}^{3}SO_{2}$ Emissions were calculated using the emission factor from Table 3.2-2

⁴PM Emission Factor = 7.71E-05 lb/MMBTU + 7.71E-05 lb/MMBTU + 9.91E-03 lb/MMBTU = 0.01006 lb/MMBTU

⁵25% safety factor was added to NOx on all engines. 25% safety factor was added to VOC on 3516. VOC lb/hr rates include acetaldehyde emissions.

Total Emissions Per Pollutant (TPY)	NOx	СО	VOC	нсно	SO ₂	PM _{10 & 2.5}	Acet- aldehyde
Total Emissions Fer Fondtant (TF F)	179.60	181.69	147.89	19.44	17.69	15.81	4.60

XTO ENERGY, INC. BULLDOG COMPRESSOR STATION COMPRESSOR ENGINES

					Gree	enhouse	Gas Emi	ssions C	alculati	ons								
					Engine Data	Fact	FR 98 tors ²			11. //								
Source ID	Unit Description	Annual Hours	Rated HP	MMbtu/hp- hr ¹ (HHV)	g/hp-hr CO2	CH ₄	MBtu N ₂ O	CO2	CH ₄	lb/hr N ₂ O	CH ₄ as CO2e	N ₂ O as CO2e	CO2	CH ₄	tj N ₂ O	CH₄ as CO2e	N ₂ O as CO2e	Total CO2e
ENG1	Caterpillar G3616 Natural Gas Compressor Engine	8760	5000	0.007476	455	0.002205	0.000221	5015.43	0.0824	0.0082	2.06	2.46	21967.59	0.36	0.04	9.03	10.76	21987.38
ENG2	Caterpillar G3616 Natural Gas Compressor Engine	8760	5000	0.007476	455	0.002205	0.000221	5015.43	0.0824	0.0082	2.06	2.46	21967.59	0.36	0.04	9.03	10.76	21987.38
ENG3	Caterpillar G3616 Natural Gas Compressor Engine	8760	5000	0.007476	455	0.002205	0.000221	5015.43	0.0824	0.0082	2.06	2.46	21967.59	0.36	0.04	9.03	10.76	21987.38
ENG4	Caterpillar G3616 Natural Gas Compressor Engine	8760	5000	0.007476	455	0.002205	0.000221	5015.43	0.0824	0.0082	2.06	2.46	21967.59	0.36	0.04	9.03	10.76	21987.38
ENG5	Caterpillar G3616 Natural Gas Compressor Engine	8760	5000	0.007476	455	0.002205	0.000221	5015.43	0.0824	0.0082	2.06	2.46	21967.59	0.36	0.04	9.03	10.76	21987.38
ENG6	Caterpillar G3616 Natural Gas Compressor Engine	8760	5000	0.007476	455	0.002205	0.000221	5015.43	0.0824	0.0082	2.06	2.46	21967.59	0.36	0.04	9.03	10.76	21987.38
ENG7	Caterpillar G3616 Natural Gas Compressor Engine	8760	5000	0.007476	455	0.002205	0.000221	5015.43	0.0824	0.0082	2.06	2.46	21967.59	0.36	0.04	9.03	10.76	21987.38
ENG8	Caterpillar G3616 Natural Gas Compressor Engine	8760	5000	0.007476	455	0.002205	0.000221	5015.43	0.0824	0.0082	2.06	2.46	21967.59	0.36	0.04	9.03	10.76	21987.38
ENG9	Caterpillar G3616 Natural Gas Compressor Engine	8760	5000	0.007476	455	0.002205	0.000221	5015.43	0.0824	0.0082	2.06	2.46	21967.59	0.36	0.04	9.03	10.76	21987.38
ENG11	Caterpillar 3516J TA Natural Gas Compressor Engine	8760	1380	0.008095	502	0.002205	0.000221	1527.25	0.0246	0.0025	0.62	0.73	6689.35	0.11	0.01	2.70	3.22	6695.26
ENG12	Caterpillar 3516J TA Natural Gas Compressor Engine	8760	1380	0.008095	502	0.002205	0.000221	1527.25	0.0246	0.0025	0.62	0.73	6689.35	0.11	0.01	2.70	3.22	6695.26
¹ HHV is based	l on the Fuel Consumption Rate @ 75% L	load from the	Gas Engine	Rating Pro Report			1											
	ential for CH4 is 25. N2O is 298.		0	~ 1						Total	Emission	s (TPY)				Tota	al CO2e	
																	070.01	

211276.91

BULLDOG COMPRESSOR STATION

HEATERS - BURNER CALCULATIONS & EXHAUST STACK FLOW & FUEL CONSUMPTION RATES

						CRITERI	A & REGULA	TED POLLU	UTANTS	EMISS	IONS								
						1	AP-42 Factors ¹												
							lb/MMBtu					lb/hr ²					tpy ²		
Source ID	Promax Fuel Gas Stream	Fuel Gas HHV (BTU/SCF)	Hours	Burner Rating (MMBTU/Hr)		СО	VOC	SO ₂	$PM_{10 \ \& \ 2.5}$	NOx	СО	VOC	SO_2	$PM_{10 \& 2.5}$	NOx	СО	VOC	SO_2	$PM_{10 \& 2.5}$
HTR1	3. Fuel Gas	1,269	8,760	0.75	0.10	0.08	0.01	0.01	0.01	0.11	0.10	0.01	0.01	0.01	0.50	0.42	0.03	0.04	0.04
RB1	3. Fuel Gas	1,269	8,760	2.00	0.10	0.08	0.01	0.01	0.01	0.31	0.26	0.02	0.03	0.02	1.34	1.12	0.07	0.12	0.10
RB2	3. Fuel Gas	1,269	8,760	2.00	0.10	0.08	0.01	0.01	0.01	0.31	0.26	0.02	0.03	0.02	1.34	1.12	0.07	0.12	0.10
RB3	3. Fuel Gas	1,269	8,760	2.00	0.10	0.08	0.01	0.01	0.01	0.31	0.26	0.02	0.03	0.02	1.34	1.12	0.07	0.12	0.10

¹Source: Emission factors from AP-42, Chapter 1, Tables 1.4-1, 1.4-2 and 1.4-3, converted from lb/MMscf to lb/MMbtu by dividing by 1,020 Btu/scf (per AP-42, Chapter 1 guidance). SO2 - 5 gr/100 scf

²Burners - 25% Safety Factor

Total (try)	NOx	СО	VOC	SO_2	$PM_{10 \& 2.5}$
Total (tpy)	4.51	3.79	0.25	0.39	0.34

BULLDOG COMPRESSOR STATION

HEATERS - BURNER CALCULATIONS & EXHAUST STACK FLOW & FUEL CONSUMPTION RATES

						HAZA	RDOUS AIR P	OLLUTANTS	(HAP) EM	IISSIONS									
							P-42 Factors ¹ lb/MMBtu					lb/hr²					tpy ²		
Source ID	Promax Stream	Fuel Gas (BTU/SCF)	Operating Hours	Burner Rating (MMBTU/Hr)	Benzene	Toluene	N- Hexane	НСНО	Dichloro benzene	Benzene	Toluene	N- Hexane	НСНО	Dichloro benzene	Benzene	Toluene	N- Hexane		Dichloro benzene
HTR1	3. Fuel Gas	1,269	8760	0.75	2.1E-06	3.3E-06	1.8E-03	7.4E-05	1.2E-06	<0.001	<0.001	0.00	<0.001	<0.001	<0.001	<0.001	0.01	<0.001	<0.001
RB1	3. Fuel Gas	1,269	8760	2.00	2.1E-06	3.3E-06	1.8E-03	7.4E-05	1.2E-06	<0.001	<0.001	0.01	<0.001	<0.001	<0.001	<0.001	0.02	0.00	<0.001
RB2	3. Fuel Gas	1,269	8760	2.00	2.1E-06	3.3E-06	1.8E-03	7.4E-05	1.2E-06	<0.001	<0.001	0.01	<0.001	<0.001	<0.001	<0.001	0.02	0.00	<0.001
RB3	3. Fuel Gas	1,269	8760	2.00	2.1E-06	3.3E-06	1.8E-03	7.4E-05	1.2E-06	<0.001	<0.001	0.01	<0.001	<0.001	<0.001	<0.001	0.02	0.00	<0.001

¹Source: Emission factors from AP-42, Chapter 1, Tables 1.4-1, 1.4-2 and 1.4-3, converted from lb/MMscf to lb/MMbtu by dividing by 1,020 Btu/scf (per AP-42, Chapter 1 guidance). SO2 - 5 gr/100 scf

²Burners - 25% Safety Factor

Total Individual	Benzene	Toluene	N- Hexane	НСНО	Dichloro benzene
HAPS (tpy)	0.00	0.00	0.08	0.00	0.00
		_			
Total Combined HAPS (tpy)	0.08				

BULLDOG COMPRESSOR STATION

HEATERS - BURNER CALCULATIONS & EXHAUST STACK FLOW & FUEL CONSUMPTION RATES

				Exhaust Stack an	nd Fuel Consumption
Source	HTR1	RB1	RB2	RB3	
Burner Rating (btu/hr)	750000	2000000	2000000	2000000	
Gross Heating Value (btu/scf)	1269.3	1269.3	1269.3	1269.3	
3" eclipse air mixer: (Air/Gas Ratio) ¹	5/1	5/1	5/1	5/1	
Stack Temperature (°F)	1000	1000	1000	1000	
Stack Diameter (ft)	1	1.5	1.5	1.5	
Stack Height (ft)	20	20	20	20	
Fuel Consumption (scf/hr)	591	1576	1576	1576	
Fuel Consumption (scf/day)	14181	37816	37816	37816	
Fuel Consumption (mmscf/year)	5	14	14	14	
Air Injection Rate (scf/hr)	5909	15757	15757	15757	
Total exhaust flow rate @ STP (scf/hr)	6500	17332	17332	17332	
Total exhaust flow rate @ STP (scf/sec)	2	5	5	5	
Total exhaust flow rate @ 1000 °F (acf/hr)	18249	48664	48664	48664	
Total exhaust flow rate @ 1000 °F (acf/sec)	5.07	14	14	14	
Exhaust Stack Exit Velocity @ STP (ft/sec)	2.30	3	3	3	
Exhaust Stack Exit Velocity @ 1000 °F (ft/sec)	6.45	8	8	8	
Total CH4 (ton/yr) ²	0.32	0.85	0.85	0.85	
Total N2O (ton/yr) ²	0.001	0.002	0.002	0.002	
Total CO2 (ton/yr) ²	519	1385	1385	1385	
Total CO2e (ton/yr) ²	527.51	1407	1407	1407	

¹ Air/Gas Ratio is based on the Manufacturer's Data of XTO's typical burner installations

² GHG emissions source is 40 CFR § 98.233 (n), 40 CFR § 98.233(v) for CH4 and CO2 mass emissions, 40 CFR § 98.233(z) for N2O mass emissions,

Promax Stream Name	3. Fuel Gas
Component	Mass Frac
Triethylene Glycol	0.00
Water	0.00
Hydrogen Sulfide	0.00
Carbon Dioxide	0.00
Nitrogen	0.01
Methane	0.58
Ethane	0.18
Propane	0.13
Isobutane	0.02
n-Butane	0.05
Isopentane	0.01
n-Pentane	0.01
i-C6	0.01
i-C7	0.00
Octane	0.00
Nonane	0.00
Benzene	0.00
Toluene	0.00
Ethylbenzene	0.00
o-Xylene	0.00
n-Hexane	0.00
2,2,4-Trimethylpentane	0.00
Decanes Plus	0.00
Decanes Plus Sat	0.00

XTO ENERGY, INC. BULLDOG COMPRESSOR STATION STORAGE TANK EMISSIONS SUMMARY

							VOC EM	ISSIONS SUN	IMARY										
								Wo	Uncontrolled rking & Breathin				ncontrolled ash Losses			Uncon Total En		Contro Total Em	
Unit Number	Source Description	Material Type (Oil/Produced Water)	Number of Tanks in Category	Controlled by Unit #	Control Efficiency (%)	Promax Stream Liquid Material	Material Throughput (bbls/day)	Promax Stream (Hrly)	Promax Stream (Annual)	Lb/hr	ТРҮ	Promax Stream Proma (Hrly) (Aı	ax Stream nnual)	b/hr	ТРҮ	Lb/hr	ТРҮ	Lb/hr	ТРҮ
SKT1	Skim Tank	Produced Water	2	FL1-FL2	98	14. Skim Tank Inlet	173.54	8. Skim Tank W&B	8. Skim Tank W&B	3.62	15.85		kim Tank Ash Gas	.25	5.47	4.87	21.32	0.10	0.43
SKT2	Skim Tank (Backup)	Produced Water	2	FL1-FL2	98	14. Skim Tank Inlet	173.54	8. Skim Tank W&B	8. Skim Tank W&B	3.62	15.85		kim Tank ash Gas	.25	5.47	4.87	21.32	0.10	0.43
OT1	Condensate Tank	Condensate	4	FL1-FL2	98	11. Condensate Sales Liquid	203.55	10. Condensate Tank W&B	10. Condensate Tank W&B	4.55	19.91		ondensate Flash Gas	33.69	275.73	138.24	295.64	2.76	5.91
OT2	Condensate Tank	Condensate	4	FL1-FL2	98	11. Condensate Sales Liquid	203.55	10. Condensate Tank W&B	10. Condensate Tank W&B	4.55	19.91	Hash Losses Hrly	ondensate Flash Gas	33.69	275.73	138.24	295.64	2.76	5.91
OT3	Condensate Tank	Condensate	4	FL1-FL2	98	11. Condensate Sales Liquid	203.55	10. Condensate Tank W&B	10. Condensate Tank W&B	4.55	19.91		ondensate Flash Gas	33.69	275.73	138.24	295.64	2.76	5.91
OT4	Condensate Tank	Condensate	4	FL1-FL2	98	11. Condensate Sales Liquid	203.55	10. Condensate Tank W&B	10. Condensate Tank W&B	4.55	19.91		ondensate Flash Gas	33.69	275.73	138.24	295.64	2.76	5.91
WT1	Produced Water Tank	Produced Water	2	FL1-FL2	98	12. Produced Water Liquid	170.55	9. Water Tank W&B	9. Water Tank W&B	0.11	0.47		ater Tank ash Gas).00	0.00	0.11	0.47	0.00	0.01
WT2	Produced Water Tank	Produced Water	2	FL1-FL2	98	12. Produced Water Liquid	170.55	9. Water Tank W&B	9. Water Tank W&B	0.11	0.47	5. Water Tank 5. Wa Flash Gas Flas	ater Tank ash Gas).00	0.00	0.11	0.47	0.00	0.01
			Storage Tank E	missions						25.64	112.28		53	37.26	1113.85	562.90	1226.13	11.26	24.52
																	0.10		

XTO ENERGY, INC. BULLDOG COMPRESSOR STATION OIL TRUCK LOADING LOSSES - UNCONTROLLED

	Truck Loading Loss	es Calculations										
	~ 											
	Promax Stream Production	11. Condensate Sa	ales Liquid									
	Promax Stream Emissions	10. Condensate T	ank W&B									
	Controlled/Uncontrolled	UNCONTRC	DLLED									
	Operating Schedule^c	100	Day/Year									
	Condensate Production	814	bbls/Day									
	Promax Repor	rt Results										
	LL= 12.46 * SPM/1	[* (1-EFF/100)										
	Saturation Factor (S) = Average True Vapor Pressure of liquid loaded $(P)^a$ =											
	Max True Vapor Pressure of liquid loaded (P) ^a =											
Averag	e Temperature of bulk liquid lo	529	9.10									
Ma		erature of bulk liquid loaded in Rankin (T) ^a =										
		Molecular Weight (M) ^a =										
	Control Efficiency * Collec)								
	,	rbon Content $(\% wt)^a =$		00								
		VOC Content (wt%) ^a =	0.									
		HAP Conent $(wt\%)^a$ =	0.									
	Uncontrolled LL (lb Total HC		0.2									
	rage Uncontrolled LL (lb VOC	<u> </u>	0.2									
	Uncontrolled LL (lb Total HC	01,	0.3									
	Max Uncontrolled LL (lb VOC	0		129 420								
		<pre>bughput (bbls/Year) = bughput (bbls/hear) = bughput (bbls/hea</pre>		10								
	0 (/ /											
	Estimated # of Loads (Approx	(intately 1 III / Load) -		38								
	lb/hr											
10	tal Hydrocarbon Emissions		71.36	12.10								
			lb/hr	TPY								
	Total VOC Emissions		65.70	11.14								
			lb/hr	TPY								
	Total HAP Emissions		0.03	0.01								

XTO ENERGY, INC. BULLDOG COMPRESSOR STATION OIL TRUCK LOADING LOSSES - UNCONTROLLED

Component		Total Speciated Emitted During I	-
	Mass Fraction ^d	lb/hr ^d	ton/yr
Triethylene Glycol	0.00	0.00	0.00
Water	0.00	0.00	0.00
Hydrogen Sulfide	0.00	0.00	0.00
Carbon Dioxide	0.00	0.00	0.00
Nitrogen	0.00	0.00	0.00
Methane	0.00	0.17	0.03
Ethane	0.08	5.49	0.93
Propane	0.24	17.42	2.95
Isobutane	0.08	5.87	1.00
n-Butane	0.24	17.45	2.96
Isopentane	0.08	5.99	1.02
n-Pentane	0.10	6.98	1.18
i-C6	0.08	5.93	1.01
i-C7	0.03	2.39	0.40
Octane	0.01	0.62	0.10
Nonane	0.00	0.09	0.01
Benzene	0.00	0.19	0.03
Toluene	0.00	0.16	0.03
Ethylbenzene	0.00	0.00	0.00
o-Xylene	0.00	0.03	0.01
n-Hexane	0.04	2.58	0.44
2,2,4-Trimethylpentane	0.00	0.00	0.00
Decanes Plus	0.00	0.00	0.00
Decanes Plus Sat	0.00	0.00	0.00
Total HC	1.00	71.36	12.10
Total VOC	0.92	65.70	11.14
Total HAP	0.04	2.97	0.50
Heating Value (Btu/scf)	3080.19	3080.19	3080.19
Molecular Weight (lb/lbmol)	54.80	54.80	54.80
SO2 Emissions (lb/hr)	N/A	N/A	N/A
Operating Hours (hr/yr)	N/A	N/A	2400
Mass Flow	N/A	71.36 lb/hr	12.10 ton/yr
Volumetric Flow (scf/hr)	N/A	494.13	83.78
Heat Release (MMBtu/hr)	N/A	1.52	0.26

Footnotes:

^a Values were obtained from Promax.

Loading emissions include total hydrocarbons as calculated using AP-42, Section 5.2.

Condensate tanks are only trucked out when transfer to pipeline is unavailable.

d The component speciation was obtained from Promax Stream " and multiplied by the total hydrocarbon emissions. (VOC = 0.00 lb/hr * 0.00 wt% VOC = 0.00 lb/hr)

e Loading emissions are uncontrolled.

XTO ENERGY INC. BULLDOG COMPRESSOR STATION FLARE 1-3 EMISSION SUMMARY

						F	lare Emis	sions Su	mmary T	able								
Stream Source	Stream Source	N	Ox	C	0		VOC Total HAPs)	S	O ₂	PM	0 & 2.5	Total	HAPs	CO2e	n-He	exane	Ben	zene
Stream Source	Stream Source	lb/hr	ТРҮ	lb/hr	TPY	lb/hr	ТРҮ	lb/hr	ТРҮ	lb/hr	ТРҮ	lb/hr	TPY	ТРҮ	lb/hr	ТРҮ	lb/hr	TPY
FL1-FL2 Pilot	FL1 Pilot/Purge	0.33	1.46	0.67	2.92	0.47	2.07	0.00	0.01	0.01	0.06	0.00	0.02	1744.35	0.00	0.02	0.00	0.00
1.	FL2 Pilot / Purge	0.33	1.46	0.67	2.92	0.47	2.07	0.00	0.01	0.01	0.06	0.00	0.02	1744.35	0.00	0.02	0.00	0.00
	PW Tank Vapors (WT1-2)	0.00	0.00	0.00	0.01	0.00	0.02	0.00	0.00	0.00	0.00	0.00	0.01	5.77	0.00	0.00	0.00	0.00
	Skim Tank Vapors (SKT1-2)	0.03	0.13	0.06	0.26	0.19	0.85	0.00	0.00	0.00	0.00	0.01	0.05	133.28	0.01	0.04	0.00	0.00
FL1-FL2 Norm	Oil Tank Vapors (OT1-4)	1.76	7.35	3.52	14.68	11.06	23.65	0.01	0.03	0.03	0.14	0.46	1.00	7641.37	0.36	0.81	0.04	0.09
	Low Presure Separator Vapors Normal Operation	0.06	0.23	0.12	0.46	0.27	1.08	0.00	0.00	0.00	0.01	0.01	0.04	276.51	0.01	0.03	0.00	0.00
	Low Presure Separator Vapors VRU Downtime	2.94	1.29	5.86	2.57	13.70	6.00	0.04	0.02	0.08	0.03	0.47	0.21	1536.18	0.38	0.17	0.05	0.02
FL1-FL2 SSM	HP Flare Blowdowns	0.17	0.08	0.33	0.17	0.24	0.12	0.00	0.00	0.01	0.00	0.00	0.00	99.40	0.00	0.00	0.00	0.00
	HP Flare Inlet Gas Flaring	538.55	6.73	1075.15	13.44	979.03	12.24	4.87	0.06	22.17	0.28	27.05	0.34	8357.04	23.90	0.30	1.28	0.02
Total	Total Emissions	544.17	18.74	1086.37	37.42	1005.45	48.09	4.93	0.15	22.31	0.59	28.01	1.68	21538.25	24.66	1.38	1.37	0.14
FL1-FL2 Pilot	Total Flare Pilot/Purge Emissions	0.67	2.93	1.33	5.84	0.94	4.13	0.01	0.03	0.03	0.13	0.01	0.04	3488.70	0.01	0.04	0.00	0.00
FL1-FL2 Norm	Total Flare Normal Operations	1.85	7.72	3.69	15.41	11.53	25.60	0.01	0.04	0.03	0.15	0.48	1.10	8056.93	0.38	0.88	0.04	0.11
FL1-FL2 SSM	Total Flare SSM	541.65	8.10	1081.35	16.17	992.97	18.36	4.91	0.08	22.25	0.31	27.52	0.55	9992.62	24.28	0.47	1.33	0.04
Total	Total Emissions	544.17	18.74	1086.37	37.42	1005.45	48.09	4.93	0.15	22.31	0.59	28.01	1.68	21538.25	24.66	1.38	1.37	0.14
FL1-FL2 HP	High Pressure Gas Flaring (No Pilot)	538.72	6.82	1075.48	13.61	979.27	12.36	4.87	0.06	22.17	0.28	27.05	0.34	8456.44	23.90	0.30	1.28	0.02
FL1-FL2 LP	Low Pressure Gas Flaring (No Pilot)	4.79	9.00	9.56	17.98	25.23	31.61	0.05	0.06	0.11	0.18	0.95	1.30	9593.11	0.76	1.05	0.09	0.13

XTO ENERGY INC. BULLDOG COMPRESSOR STATION FLARE 1-3 HOURLY EMISSIONS WINTER SEASON - NORMAL OPERATIONS

					Uncapt	ured Maximum Ho	ourly Emission Rat	es and Compositio	n to Flare ^{a,b}							Crite	eria Pollutant Emi	issions from	Flare ^e
		SSM		HP Flare	LP Flare	Oil Tank Va			apors (SKT1-2)	PW Tank Va	pors (WT1-2)	Low Pres Sep ^d							
Stream	HP Flare Blowdowns ^f	Low Pres Sep ^d Flash (VRU Off)	Inlet Gas Flaring ^g	Pilot/Purge ^c	Pilot/Purge ^c	Flash	W&B	Flash	W&B	Flash	W&B	Flash (VRU On) 98% Col Eff	Total Vapors to Flare	Destruction	Total		Estate Date		
Promax Stream Name	17. HPF Blowdowns	1. LP Separator Gas	19. Inlet Flaring	15. HPF Pilot/ Purge Gas	16. LPF Pilot/ Purge Gas	22. Condensate Flash Losses Hrly	10. Condensate Tank W&B	6. Skim Tank Flash Gas	8. Skim Tank W&B	5. Water Tank Flash Gas	9. Water Tank W&B	1. LP Separator Gas	(Uncontrolled Max Hourly)	Efficiency	Flare Exhaust (controlled)	Component	Emission Rate	Emission Factor	Emission Factor Units
Component	(lb/hr)	(lb/hr)	(lb/hr)	(1b/hr)	(1b/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(1b/hr)	(1b/hr)	(lb/hr)	(%)	(lb/hr)		(1b/hr)		
Triethylene Glycol	0.00	0.00	0.98	0.00	0.00	0.00	0.00	0.00	0.00	0	0.00	0.00	0.98	98%	0.02	NO _X	544.17	0.138	lb/MMBtu
Water	0.00	7.45	5.62	0.00	0.00	0.00	0.00	0.03	0.13	0.00	0.13	0.15	13.52	0%	13.52	СО	1086.37	0.2755	lb/MMBtu
Hydrogen Sulfide	0.00	0.02	2.59	0.00	0.00	0.01	0.00	0.00	0.00	0.00	0.00	0.00	2.62	98%	0.05	SO ₂	4.93		
Carbon Dioxide	0.14	1.27	411.01	0.36	0.19	0.11	0.00	0.00	0.01	0.00	0.01	0.03	413.13	0%	413.13	PM ₁₀	22.31	7.60	lb/MMscf
Nitrogen	0.64	0.93	1874.31	1.68	0.88	0.00	0.00	0.00	0.00	0.00	0.00	0.02	1878.46	0%	1878.46	PM _{2.5}	22.31	7.60	lb/MMscf
Methane	30.88	126.60	91413.17	81.13	42.59	1.27	0.05	0.08	0.01	0.00	0.01	2.53	91698.33	98%	1833.97	N ₂ O	0.87	0.00022	lb/MMBtu
Ethane	9.74	163.71	30115.57	25.59	13.43	42.37	1.52	0.25	0.09	0.00	0.03	3.27	30375.57	98%	607.51	H_2S	0.05		
Propane	6.70	252.44	22642.86	17.60	9.24	144.70	4.82	0.68	0.67	0.00	0.05	5.05	23084.80	98%	461.70				-
Isobutane	1.08	63.24	4178.60	2.85	1.49	48.41	1.63	0.23	0.57	0.00	0.01	1.26	4299.39	98%	85.99		por Controls / Fla	-	4
n-Butane	2.39	165.60	10051.87	6.29	3.30	152.63	4.83	0.65	2.39	0.00	0.04	3.31	10393.31	98%	207.87		llection Efficiency	98%	
Isopentane	0.54	50.92	2947.97	1.43	0.75	50.52	1.66	0.23	0.86	0.00	0.01	1.02	3055.91	98%	61.12	````	l Operations)		-
n-Pentane	0.56	58.45 45.76	3381.48 2735.89	1.48 0.77	0.78	60.13	1.93	0.26	1.01	0.00	0.01	1.17	3507.27	98% 98%	70.15	4 1	U Downtime	10.00%	(876 hrs)
i-C6	0.29	45.76	1239.87	0.18	0.40	24.30 26.60	1.64 0.66	0.22	0.83	0.00	0.01	0.92	2811.04 1286.95	98% 98%	56.22 25.74		Operations) uction Efficiency		-
i-C7 Octane	0.07	5.44	373.94	0.02	0.10	4.92	0.88	0.03	0.10	0.00	0.00	0.11	384.73	98%	7.69	1 1	C4+	98%	
Nonane	0.00	0.87	46.16	0.02	0.00	0.54	0.02	0.00	0.02	0.00	0.00	0.02	47.64	98%	0.95		uction Efficiency		-
Benzene	0.00	2.30	63.97	0.02	0.00	1.84	0.05	0.00	0.02	0.00	0.04	0.05	68.33	98%	1.37	Plate Desti	C3	98%	
Toluene	0.00	1.87	71.14	0.02	0.00	1.52	0.04	0.01	0.03	0.00	0.03	0.04	74.71	98%	1.49				1
Ethylbenzene	0.00	0.05	2.48	0.00	0.00	0.04	0.04	0.00	0.00	0.00	0.00	0.00	2.58	98%	0.05	H2S molecul	ar weight	34.08	3
o-Xylene	0.00	0.46	19.96	0.00	0.00	0.30	0.01	0.00	0.01	0.00	0.01	0.01	20.76	98%	0.42	SO2 molecul	0	64.06	_
n-Hexane	0.10	19.07	1194.79	0.27	0.14	17.26	0.71	0.09	0.35	0.00	0.00	0.38	1233.17	98%	24.66		ne (scf/lbmol)	379.484	-
2,2,4-Trimethylpentane	0.00	0.00	0.00	0.00	0.00	1.06	0.00	0.00	0.00	0.00	0.00	0.00	1.06	98%	0.02	Flare Operat		8760	
Decanes Plus	0.00	0.04	0.68	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.72	98%	0.01		0		-
Decanes Plus Sat	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	0.00				
Total	53.17	985.17	172774.91	139.69	73.34	578.52	19.75	2.87	7.47	0.00	0.38	19.70	174654.97		5752.10	1			
Total VOC	11.77	685.17	48951.66	30.92	16.23	534.77	18.18	2.50	7.24	0.00	0.21	13.70	50258.65		1005.17				
Total HAP	0.11	23.75	1352.34	0.30	0.16	22.03	0.82	0.11	0.43	0.00	0.09	0.47	1400.61		28.01				
Heating Value (Btu/scf)	1,269.30	2,154.40	1,338.01	1269.30	1269.30	3064.41	3080.19	2769.57	3346.32	0.00	1149.83	2154.40	1343.20			-			
Molecular Weight (lb/lbmol)	21.20	37.83	22.48	21.20	21.20	54.51	54.80	49.73	61.12	0.00	32.03	37.83							
Operating Hours (hr/yr)	1,000	876	20	8760	8760	8760	8760	8760	8760	8760	8760	7884							
Mass Flow (lb/hr)	53.17	985.17	172,774.91	139.69	73.34	578.52	19.75	2.87	7.47	0.00	0.38	19.70	174654.97						
Volumetric Flow (scf/hr)	952	9,881 21.29	2,916,667	2,500	1,313	4,027	136.77	21.88	46.41	0.00	4.53	197.63	2935746.45						
Heat Release (MMBtu/hr)	1.21	21.29	3,902.54	3.17	1.67	12.34	0.42	0.06	0.16	0.00	0.01	0.43	3943.28	l					
					Con	nbustion Emissions	from Flare												
	(lb/hr)	(lb/hr)	(1b/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(1b/hr)	(lb/hr)						
Total NO _x	0.17	2.94	538.55	0.44	0.23	1.70	0.06	0.01	0.02	0.00	0.00	0.06	544.17						
Total CO	0.33	5.86	1075.15	0.87	0.46	3.40	0.12	0.02	0.04	0.00	0.00	0.12	1086.37						
Total SO ₂	0.00	0.04	4.87	0.00	0.00	0.01	0.00	0.00	0.00	0.00	0.00	0.00	4.93						
Total PM ₁₀	0.01	0.08	22.17	0.02	0.01	0.03	0.00	0.00	0.00	0.00	0.00	0.00	22.31						
Total PM _{2.5}	0.01	0.08	22.17	0.02	0.01	0.03	0.00	0.00	0.00	0.00	0.00	0.00	22.31						
Total VOC after comb.	0.24	13.70	979.03	0.62	0.32	10.70	0.36	0.05	0.14	0.00	0.00	0.27	1005.45						
Total HAP after comb.	0.00	0.47	27.05	0.01	0.00	0.44	0.02	0.00	0.01	0.00	0.00	0.01	28.01						
Total n-Hexane after comb.	0.00	0.38	23.90	0.01	0.00	0.35	0.01	0.00	0.01	0.00	0.00	0.01	24.66						
Total Benzene after comb.	0.00	0.05	1.28	0.00	0.00	0.04	0.00	0.00	0.00	0.00	0.00	0.00	1.37						
Total CH ₄	0.47	1.08	1306.41	1.23	0.65	0.01	0.00	0.00	0.00	0.00	0.00	0.02	1309.86						
Total N ₂ O	0.000	0.01	1.90	0.00	0.00	0.01	0.00	0.00	0.00	0.00	0.00	0.00	1.92						
Total CO ₂	188.08	3587.65	647106.92	494.12	259.41	1795.42	61.31	9.39	22.63		1.32	71.75	653,598.01						
		1		525.31	275.79	1797.39	61.38	9.42	22.66	0.00	1.32	72.35	686,915.56						

StreamHP Flar BlowdowPromax Stream Name17. HP BlowdowComponent(lb/hr)Triethylene Glycol0.00Water0.00Hydrogen Sulfide0.00Carbon Dioxide0.14Nitrogen0.64Methane30.88Ethane9.74Propane6.70Isobutane1.08n-Butane2.39Isopentane0.54n-Pentane0.56i-C60.29i-C70.07Octane0.01Nonane0.00Benzene0.01Oloo0.00Ethylbenzene0.00n-Hexane0.00Decanes Plus Sat0.00Total VOC11.77	ownsfFlassIPF1. Lipowns1. Lipowns1. Lipout1. Lipout <th< th=""><th>SSM w Pres Sepd sh (VRU Off) Sh (VRU Off) LP Separator Gas (lb/hr) 0.00 7.45 0.02 1.27 0.93 126.60 163.71 252.44 63.24</th><th>Inlet Gas Flaring^g 19. Inlet Flaring (lb/hr) 0.98 5.62 2.59 411.01 1874.31 91413.17</th><th>HP Flare Pilot/Purge^c</th><th>LP Flare Pilot/Purge^c 16. LPF Pilot / Purge Gas (lb/hr) 0.00 0.00 0.00 0.00</th><th>Oil Tank Va Flash 22. Condensate Flash Losses Hrly (lb/hr) 0.00</th><th>W&B 10. Condensate Tank W&B (lb/hr)</th><th>Flash 6. Skim Tank Flash Gas</th><th>apors (SKT1-2) W&B 8. Skim Tank W&B</th><th>Flash 5. Water Tank</th><th>pors (WT1-2) W&B 9. Water Tank</th><th>Low Pres Sep^d Flash (VRU On) 98% Col Eff 1. LP Separator</th><th>Total Vapors to Flare (Uncontrolled</th><th>Destruction Efficiency</th><th>Total Flare Exhaust</th><th>Comment</th><th>Emission Rate</th><th>Emission</th><th>Emission</th></th<>	SSM w Pres Sepd sh (VRU Off) Sh (VRU Off) LP Separator Gas (lb/hr) 0.00 7.45 0.02 1.27 0.93 126.60 163.71 252.44 63.24	Inlet Gas Flaring ^g 19. Inlet Flaring (lb/hr) 0.98 5.62 2.59 411.01 1874.31 91413.17	HP Flare Pilot/Purge ^c	LP Flare Pilot/Purge ^c 16. LPF Pilot / Purge Gas (lb/hr) 0.00 0.00 0.00 0.00	Oil Tank Va Flash 22. Condensate Flash Losses Hrly (lb/hr) 0.00	W&B 10. Condensate Tank W&B (lb/hr)	Flash 6. Skim Tank Flash Gas	apors (SKT1-2) W&B 8. Skim Tank W&B	Flash 5. Water Tank	pors (WT1-2) W&B 9. Water Tank	Low Pres Sep ^d Flash (VRU On) 98% Col Eff 1. LP Separator	Total Vapors to Flare (Uncontrolled	Destruction Efficiency	Total Flare Exhaust	Comment	Emission Rate	Emission	Emission
BlowdowPromax Stream Name17. HP BlowdowComponent(lb/hr)Triethylene Glycol0.00Water0.00Hydrogen Sulfide0.00Carbon Dioxide0.14Nitrogen0.64Methane30.88Ethane9.74Propane6.70Isobutane1.08n-Butane2.39Isopentane0.54n-Pentane0.56i-C60.29i-C70.07Octane0.01Nonane0.00Benzene0.01Toluene0.00c-Xylene0.00n-Hexane0.00Decanes Plus Sat0.00Total VOC11.77	ownsfFlassIPF1. Lipowns1. Lipowns1. Lipout1. Lipout <th< td=""><td>Sh (VRU Off) LP Separator Gas (Ib/hr) 0 0.00 7 7.45 0 0.02 1 1.27 0 0.93 1 126.60 1 163.71 2 252.44 1</td><td>Flaring^g 19. Inlet Flaring (lb/hr) 0.98 5.62 2.59 411.01 1874.31</td><td>Pilot/Purge^c 15. HPF Pilot / Purge Gas (lb/hr) 0.00 0.00 0.00 0.00 0.00 0.36</td><td>Pilot/Purge^c 16. LPF Pilot / Purge Gas 0.00 0.00 0.00</td><td>22. Condensate Flash Losses Hrly (lb/hr) 0.00</td><td>10. Condensate Tank W&B (lb/hr)</td><td>6. Skim Tank Flash Gas</td><td>8. Skim Tank</td><td>5. Water Tank</td><td></td><td>98% Col Eff</td><td>Vapors to Flare</td><td></td><td>Flare Exhaust</td><td>Comment</td><td>Emission Rate</td><td></td><td>Emission</td></th<>	Sh (VRU Off) LP Separator Gas (Ib/hr) 0 0.00 7 7.45 0 0.02 1 1.27 0 0.93 1 126.60 1 163.71 2 252.44 1	Flaring ^g 19. Inlet Flaring (lb/hr) 0.98 5.62 2.59 411.01 1874.31	Pilot/Purge ^c 15. HPF Pilot / Purge Gas (lb/hr) 0.00 0.00 0.00 0.00 0.00 0.36	Pilot/Purge ^c 16. LPF Pilot / Purge Gas 0.00 0.00 0.00	22. Condensate Flash Losses Hrly (lb/hr) 0.00	10. Condensate Tank W&B (lb/hr)	6. Skim Tank Flash Gas	8. Skim Tank	5. Water Tank		98% Col Eff	Vapors to Flare		Flare Exhaust	Comment	Emission Rate		Emission
Promax Stream Name Blowdow Component (lb/hr) Triethylene Glycol 0.00 Water 0.00 Hydrogen Sulfide 0.00 Carbon Dioxide 0.14 Nitrogen 0.64 Methane 30.88 Ethane 9.74 Propane 6.70 Isobutane 1.08 n-Butane 2.39 Isopentane 0.54 n-Pentane 0.56 i-C6 0.29 i-C7 0.07 Octane 0.01 Nonane 0.00 Benzene 0.01 Toluene 0.00 O-Xylene 0.00 Decanes Plus 0.00 Decanes Plus Sat 0.00	Dwns ur) 0 0 0 0 0 4 38 4 0 8 9 4	Gas I (lb/hr) 0.00 0.00 1 0.02 1 1.27 0.93 126.60 1 163.71 2 252.44 1	Flaring (lb/hr) 0.98 5.62 2.59 411.01 1874.31	Purge Gas (lb/hr) 0.00 0.00 0.00 0.36	Purge Gas (lb/hr) 0.00 0.00	Flash Losses Hrly (lb/hr) 0.00	Tank W&B (lb/hr)	Flash Gas			9. Water Tank	1 IP Separator	(Uncontrolled	Efficiencv		Comment	Limission Rate		
Triethylene Glycol 0.00 Water 0.00 Hydrogen Sulfide 0.00 Carbon Dioxide 0.14 Nitrogen 0.64 Methane 30.88 Ethane 9.74 Propane 6.70 Isobutane 1.08 n-Butane 2.39 Isopentane 0.54 n-Pentane 0.56 i-C6 0.29 i-C7 0.07 Octane 0.01 Nonane 0.00 Benzene 0.01 O.00 Ethylbenzene 0.00 Decanes Plus 0.00 Decanes Plus Sat 0.00 Total VOC 11.77	0 0 0 4 4 38 4 0 8 9 4 4 0 8 9 4 4 0 1 1 1 1 1 1 1 1 1 1 1 1 1	0.00 7.45 0.02 1.27 0.93 126.60 163.71 252.44	0.98 5.62 2.59 411.01 1874.31	0.00 0.00 0.00 0.36	0.00	0.00		(11-/L)		Flash Gas	W&B	Gas	Max Hourly)	5	(controlled)	Component		Factor	Factor Units
Water 0.00 Hydrogen Sulfide 0.00 Carbon Dioxide 0.14 Nitrogen 0.64 Methane 30.88 Ethane 9.74 Propane 6.70 Isobutane 1.08 n-Butane 2.39 Isopentane 0.54 n-Pentane 0.56 i-C6 0.29 i-C7 0.07 Octane 0.01 Nonane 0.00 Benzene 0.01 Ootane 0.00 Ethylbenzene 0.00 Decanes Plus 0.00 Decanes Plus Sat 0.00 Total VOC 11.77	0 0 4 4 4 4 0 8 8 9 4 0 4 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	7.45 0.02 1.27 0.93 126.60 163.71 252.44	5.62 2.59 411.01 1874.31	0.00 0.00 0.36	0.00		0.00	(1b/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(1b/hr)	(%)	(lb/hr)		(lb/hr)		1
Hydrogen Sulfide0.00Carbon Dioxide0.14Nitrogen0.64Methane30.88Ethane9.74Propane6.70Isobutane1.08n-Butane2.39Isopentane0.54n-Pentane0.56i-C60.29i-C70.07Octane0.01Nonane0.00Benzene0.01Toluene0.00ethylbenzene0.00n-Hexane0.102,2,4-Trimethylpentane0.00Decanes Plus Sat0.00Total VOC11.77	0 4 4 4 8 8 4 0 8 9 4 4	0.02 1.27 0.93 126.60 163.71 252.44	2.59 411.01 1874.31	0.00 0.36		0.00	0.00	0.00	0.00	0	0.00	0.00	0.98	98%	0.02	NO _X	544.17	0.138	lb/MMBtu
Carbon Dioxide 0.14 Nitrogen 0.64 Methane 30.88 Ethane 9.74 Propane 6.70 Isobutane 1.08 n-Butane 2.39 Isopentane 0.54 n-Pentane 0.56 i-C6 0.29 i-C7 0.07 Octane 0.01 Nonane 0.00 Benzene 0.01 Octane 0.00 Ethylbenzene 0.00 Decanes Plus 0.00 Decanes Plus Sat 0.00 Total VOC 11.77	4 4 38 4 0 5 8 5 9 6 4 7 4 7 5 6 7 7 7 7 7 7 7 7 7 7 7 7 7	1.27 0.93 126.60 163.71 252.44	411.01 1874.31	0.36	0.00	0.00	0.00	0.03	0.13	0.00	0.13	0.15	13.52	0%	13.52	СО	1086.37	0.2755	lb/MMBtu
Nitrogen0.64Methane30.88Ethane9.74Propane6.70Isobutane1.08n-Butane2.39Isopentane0.54n-Pentane0.56i-C60.29i-C70.07Octane0.01Nonane0.00Benzene0.01Toluene0.00Ethylbenzene0.00Octane0.00Decanes Plus0.00Decanes Plus Sat0.00Total VOC11.77	4 38 4 0 8 9 4	0.93 126.60 163.71 252.44	1874.31		0.00	0.01	0.00	0.00	0.00	0.00	0.00	0.00	2.62	98%	0.05	SO ₂	4.93		
Methane 30.88 Ethane 9.74 Propane 6.70 Isobutane 1.08 n-Butane 2.39 Isopentane 0.54 n-Pentane 0.56 i-C6 0.29 i-C7 0.07 Octane 0.01 Nonane 0.00 Benzene 0.01 Toluene 0.00 Ethylbenzene 0.00 Octane 0.00 Decanes Plus 0.00 Decanes Plus Sat 0.00 Total VOC 11.77	38 4 0 8 9 4	126.60 163.71 252.44			0.19	0.11	0.00	0.00	0.01	0.00	0.01	0.03	413.13	0%	413.13	PM ₁₀	22.31	7.60	lb/MMscf
Ethane 9.74 Propane 6.70 Isobutane 1.08 n-Butane 2.39 Isopentane 0.54 n-Pentane 0.56 i-C6 0.29 i-C7 0.07 Octane 0.01 Nonane 0.00 Benzene 0.01 Toluene 0.00 Ethylbenzene 0.00 Decanes Plus 0.00 Decanes Plus Sat 0.00 Total VOC 11.77	4 0 8 9 4 0	163.71 252.44	9141317	1.68	0.88	0.00	0.00	0.00	0.00	0.00	0.00	0.02	1878.46	0%	1878.46	PM _{2.5}	22.31	7.60	lb/MMscf
Propane 6.70 Isobutane 1.08 n-Butane 2.39 Isopentane 0.54 n-Pentane 0.56 i-C6 0.29 i-C7 0.07 Octane 0.01 Nonane 0.00 Benzene 0.01 Toluene 0.00 Ethylbenzene 0.00 n-Hexane 0.10 Decanes Plus 0.00 Decanes Plus Sat 0.00 Total VOC 11.77	0 8 8 9 4 1	252.44	/ = = = 0, = /	81.13	42.59	1.27	0.05	0.08	0.01	0.00	0.01	2.53	91698.33	98%	1833.97	N ₂ O	0.87	0.00022	lb/MMBtu
Isobutane 1.08 n-Butane 2.39 Isopentane 0.54 n-Pentane 0.56 i-C6 0.29 i-C7 0.07 Octane 0.01 Nonane 0.00 Benzene 0.01 Toluene 0.00 Ethylbenzene 0.00 n-Hexane 0.00 Decanes Plus 0.00 Decanes Plus Sat 0.00 Total 53.17 Total VOC 11.77	8 9 4		30115.57	25.59	13.43	42.37	1.52	0.25	0.09	0.00	0.03	3.27	30375.57	98%	607.51	H_2S	0.05		
n-Butane 2.39 Isopentane 0.54 n-Pentane 0.56 i-C6 0.29 i-C7 0.07 Octane 0.01 Nonane 0.00 Benzene 0.01 Toluene 0.00 Ethylbenzene 0.00 n-Hexane 0.10 2,2,4-Trimethylpentane 0.00 Decanes Plus 0.00 Total 53.17 Total VOC 11.77	9 4	63.24	22642.86	17.60	9.24	144.70	4.82	0.68	0.67	0.00	0.05	5.05	23084.80	98%	461.70				
Isopentane0.54n-Pentane0.56i-C60.29i-C70.07Octane0.01Nonane0.00Benzene0.01Toluene0.00Ethylbenzene0.00Octane0.00Decanes Plus0.00Decanes Plus Sat0.00Total VOC11.77	4		4178.60	2.85	1.49	48.41	1.63	0.23	0.57	0.00	0.01	1.26	4299.39	98%	85.99	LPS Vapr	or Controls / Flar	re DRE	
n-Pentane 0.56 i-C6 0.29 i-C7 0.07 Octane 0.01 Nonane 0.00 Benzene 0.01 Toluene 0.00 Ethylbenzene 0.00 O-Xylene 0.00 Decanes Plus 0.00 Decanes Plus Sat 0.00 Total VOC 11.77		165.60	10051.87	6.29	3.30	152.63	4.83	0.65	2.39	0.00	0.04	3.31	10393.31	98%	207.87	LPS VRU Colle	ection Efficiency	98%	
i-C6 0.29 i-C7 0.07 Octane 0.01 Nonane 0.00 Benzene 0.01 Toluene 0.00 Ethylbenzene 0.00 o-Xylene 0.00 n-Hexane 0.10 2,2,4-Trimethylpentane 0.00 Decanes Plus 0.00 Total 53.17 Total VOC 11.77	6	50.92	2947.97	1.43	0.75	50.52	1.66	0.23	0.86	0.00	0.01	1.02	3055.91	98%	61.12	(Normal (Operations)	20 /0	
i-C7 0.07 Octane 0.01 Nonane 0.00 Benzene 0.01 Toluene 0.00 Ethylbenzene 0.00 o-Xylene 0.00 n-Hexane 0.10 2,2,4-Trimethylpentane 0.00 Decanes Plus 0.00 Total 53.17 Total VOC 11.77		58.45	3381.48	1.48	0.78	60.13	1.93	0.26	1.01	0.00	0.01	1.17	3507.27	98%	70.15	LPS VRU	Downtime	10.00%	(876 hrs)
Octane 0.01 Nonane 0.00 Benzene 0.01 Toluene 0.00 Ethylbenzene 0.00 o-Xylene 0.00 n-Hexane 0.10 2,2,4-Trimethylpentane 0.00 Decanes Plus 0.00 Total 53.17 Total VOC 11.77	9	45.76	2735.89	0.77	0.40	24.30	1.64	0.22	0.83	0.00	0.01	0.92	2811.04	98%	56.22	(MSS O	perations)	10.00 /0	
Nonane 0.00 Benzene 0.01 Toluene 0.00 Ethylbenzene 0.00 o-Xylene 0.00 n-Hexane 0.10 2,2,4-Trimethylpentane 0.00 Decanes Plus 0.00 Decanes Plus Sat 0.00 Total 53.17 Total VOC 11.77	7	18.66	1239.87	0.18	0.10	26.60	0.66	0.09	0.34	0.00	0.00	0.37	1286.95	98%	25.74	Flare Destruc	ction Efficiency	98%	
Benzene 0.01 Toluene 0.00 Ethylbenzene 0.00 o-Xylene 0.00 n-Hexane 0.10 2,2,4-Trimethylpentane 0.00 Decanes Plus 0.00 Decanes Plus Sat 0.00 Total 53.17 Total VOC 11.77	1	5.44	373.94	0.02	0.01	4.92	0.17	0.03	0.10	0.00	0.00	0.11	384.73	98%	7.69	C	C4+	20 /0	
Toluene 0.00 Ethylbenzene 0.00 o-Xylene 0.00 n-Hexane 0.10 2,2,4-Trimethylpentane 0.00 Decanes Plus 0.00 Decanes Plus Sat 0.00 Total 53.17 Total VOC 11.77	0	0.87	46.16	0.00	0.00	0.54	0.02	0.00	0.02	0.00	0.00	0.02	47.64	98%	0.95	Flare Destruc	ction Efficiency	98%	
Ethylbenzene 0.00 o-Xylene 0.00 n-Hexane 0.10 2,2,4-Trimethylpentane 0.00 Decanes Plus 0.00 Decanes Plus Sat 0.00 Total 53.17 Total VOC 11.77	1	2.30	63.97	0.02	0.01	1.84	0.05	0.01	0.04	0.00	0.04	0.05	68.33	98%	1.37	<u>ا</u> لــــــــــــــــــــــــــــــــــــ	C3	2010	
o-Xylene 0.00 n-Hexane 0.10 2,2,4-Trimethylpentane 0.00 Decanes Plus 0.00 Decanes Plus Sat 0.00 Total 53.17 Total VOC 11.77	0	1.87	71.14	0.01	0.00	1.52	0.04	0.01	0.03	0.00	0.03	0.04	74.71	98%	1.49				
n-Hexane 0.10 2,2,4-Trimethylpentane 0.00 Decanes Plus 0.00 Decanes Plus Sat 0.00 Total 53.17 Total VOC 11.77	0	0.05	2.48	0.00	0.00	0.04	0.00	0.00	0.00	0.00	0.00	0.00	2.58	98%	0.05	H2S molecular	r weight	34.08	
2,2,4-Trimethylpentane 0.00 Decanes Plus 0.00 Decanes Plus Sat 0.00 Total 53.17 Total VOC 11.77	0	0.46	19.96	0.00	0.00	0.30	0.01	0.00	0.01	0.00	0.01	0.01	20.76	98%	0.42	SO2 molecular	: weight	64.06	
Decanes Plus 0.00 Decanes Plus Sat 0.00 Total 53.17 Total VOC 11.77	0	19.07	1194.79	0.27	0.14	17.26	0.71	0.09	0.35	0.00	0.00	0.38	1233.17	98%	24.66	Molar Volume	: (scf/lbmol)	379.484	
Decanes Plus Sat 0.00 Total 53.17 Total VOC 11.77	0	0.00	0.00	0.00	0.00	1.06	0.00	0.00	0.00	0.00	0.00	0.00	1.06	98%	0.02	Flare Operatin	ıg Hours	8760	
Total 53.17 Total VOC 11.77	0	0.04	0.68	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.72	98%	0.01				
Total VOC 11.77	0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	0.00	1			
	7	985.17	172774.91	139.69	73.34	578.52	19.75	2.87	7.47	0.00	0.38	19.70	174654.97		5752.10	1			
	7	685.17	48951.66	30.92	16.23	534.77	18.18	2.50	7.24	0.00	0.21	13.70	50258.65		1005.17				
Total HAP 0.11	1	23.75	1352.34	0.30	0.16	22.03	0.82	0.11	0.43	0.00	0.09	0.47	1400.61		28.01				
Heating Value (Btu/scf) 1,269.30	.30	2,154.40	1,338.01	1269.30	1269.30	3064.41	3080.19	2769.57	3346.32	0.00	1149.83	2154.40	1343.20						
Molecular Weight (lb/lbmol) 21.20	20	37.83	22.48	21.20	21.20	54.51	54.80	49.73	61.12	0.00	32.03	37.83							
Operating Hours (hr/yr) 1,000		876	20	8760	8760	8760	8760	8760	8760	8760	8760	7884							
Mass Flow (lb/hr) 53.17		985.17	172,774.91	139.69	73.34	578.52	19.75	2.87	7.47	0.00	0.38	19.70	174654.97						
Volumetric Flow (scf/hr)952Heat Release (MMBtu/hr)1.21		9,881 21.29	2,916,667 3,902.54	2,500 3.17	1,313 1.67	4,027 12.34	136.77 0.42	21.88	46.41 0.16	0.00	4.53	197.63	2935746.45 3943.28						
Heat Release (MMBtu/hr) 1.21	1	21.29	3,902.54	3.17	1.67	12.34	0.42	0.06	0.16	0.00	0.01	0.43	3943.28						
					Con	nbustion Emissions	from Flare												
(lb/hr)	nr)	(1b/hr)	(1b/hr)	(1b/hr)	(lb/hr)	(1b/hr)	(lb/hr)	(1b/hr)	(lb/hr)	(lb/hr)	(1b/hr)	(1b/hr)	(1b/hr)						
Total NO _x 0.17	,	2.94	538.55	0.44	0.23	1.70	0.06	0.01	0.02	0.00	0.00	0.06	544.17						
Total CO 0.33		5.86	1075.15	0.87	0.46	3.40	0.12	0.02	0.04	0.00	0.00	0.12	1086.37						
Total SO2 0.00		0.04	4.87	0.00	0.00	0.01	0.00	0.02	0.04	0.00	0.00	0.00	4.93						
1000000000000000000000000000000000000		0.08	22.17	0.02	0.01	0.03	0.00	0.00	0.00	0.00	0.00	0.00	22.31						
Total PM2.5 0.01		0.08	22.17	0.02	0.01	0.03	0.00	0.00	0.00	0.00	0.00	0.00	22.31						
Total VOC after comb.0.24		13.70	979.03	0.62	0.32	10.70	0.36	0.05	0.14	0.00	0.00	0.27	1005.45						
Total HAP after comb.0.00		0.47	27.05	0.02	0.00	0.44	0.02	0.00	0.01	0.00	0.00	0.01	28.01						
Total n-Hexane after comb.0.00		0.38	23.90	0.01	0.00	0.35	0.02	0.00	0.01	0.00	0.00	0.01	23.61						
Total Benzene after comb.0.00		0.05	1.28	0.00	0.00	0.04	0.00	0.00	0.00	0.00	0.00	0.00	1.37						
Total CH40.47		1.08	1306.41	1.23	0.65	0.04	0.00	0.00	0.00	0.00	0.00	0.02	1309.86						
Total N2O 0.000		0.01	1.90	0.00	0.00	0.01	0.00	0.00	0.00	0.00	0.00	0.02	1.92						
Total CO2 188.08		3587.65	1.90 647106.92	494.12	259.41	0.01	0.00 61.31		22.63	0.00		0.00 71.75							
	00							9.39		0.00	1.32		653,598.01 686.015.56						
Total CO ₂ e 199.85	9E	3617.61	680332.48	525.31	275.79	1797.39	61.38	9.42	22.66	0.00	1.32	72.35	686,915.56						

<u>Footnotes:</u>

^a Uncontrolled stream properties determined via ProMax.

^b Tank emissions determined in ProMax are calculated at the maximum daily liquid surface temperature.

^c Pilot fuel gas emissions are conservatively calculated based on observed flowrates

^dControlled Emissions Were Calculated by the Following: Uncontrolled Emissions * (1 - VRU Efficiency) * (1 - Flare Destruction Efficiency)

^e Flare CO and NOx emission factors from TCEQ Air Permit Techincal Guidance for Chemical Sources. PM and PM2.5 emission factors from AP-42, Table 1.4-1 and 1.4-2, July 1998. SO2 emissions assume 100% conversion of H2S to SO2.

f Blowdowns are estimated to be @ 952 SCF per blowdown. XTO conservatively estimates 1000 blowdowns per year and 1 blowdown per hour

g XTO conservatively estimates 58 MMscf of inlet gas flaring per year @ 2.92 MMscf/hr max rate

h GHG emissions source is 40 CFR § 98.233 (n), 40 CFR § 98.233(v) for CH4 and CO2 mass emissions, 40 CFR § 98.233(z) for N2O mass emissions.

FLARE 1-3 HOURLY - NORMAL OPERATIONS

XTO ENERGY INC. BULLDOG COMPRESSOR STATION FLARE 1-3 ANNUAL EMISSIONS WINTER SEASON - NORMAL OPERATIONS

FLARE ANNUAL - NORMAL OPERATIONS

					Uncant	ured Maximum Ho	urly Emission Rate	es and Compositio	n to Flare ^{a,b}							Criteri	a Pollutant Emi	ssions from	Flare ^e
		SSM			-	Oil Tank Va	-	-	apors (SKT1-2)	PW Tank Va	pors (PWT1-2)	Low Pres Sep ^d							
Stream	HP Flare Blowdowns ^f	Low Pres Sep ^d Flash (VRU Off)	Inlet Gas Flaring ^g	HP Flare ⁵ Pilot/Purge ^c	LP Flare Pilot/Purge ^c	Flash	W&B	Flash	W&B	Flash	W&B	Flash (VRU On) 98% Col Eff	Total Vapors to Flare	Destruction	Total Flare Exhaust		Emission Rate	Emission	Emission
Promax Stream Name	17. HPF Blowdowns	1. LP Separator Gas	19. Inlet Flaring	15. HPF Pilot/ Purge Gas	16. LPF Pilot/ Purge Gas	7. Condensate Tank Flash Gas	10. Condensate Tank W&B	6. Skim Tank Flash Gas	8. Skim Tank W&B	5. Water Tank Flash Gas	9. Water Tank W&B	1. LP Separator Gas	(uncontrolled)	Efficiency	(controlled)	Component		Factor	Factor Units
Component	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(%)	(ton/yr)		(ton/yr)	1	
Triethylene Glycol	0.00	0.00	0.01	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.01	98%	0.00	NO _X	18.74	0.138	lb/MMBtu
Water	0.00	3.26	0.07	0.02	0.01	3.00	0.00	0.15	0.56	0.00	0.56	0.59	8.24	0%	8.24	СО	37.42	0.2755	lb/MMBtu
Hydrogen Sulfide	0.00	0.01	0.03	0.01	0.01	0.02	0.00	0.00	0.00	0.00	0.00	0.00	0.08	98%	0.00	SO ₂	0.15		
Carbon Dioxide	0.07	0.56	5.14	1.57	0.83	0.44	0.02	0.02	0.04	0.00	0.03	0.10	8.81	0%	8.81	PM ₁₀	0.59	7.60	lb/MMscf
Nitrogen	0.32	0.41	23.43	7.35	3.86	0.04	0.00	0.00	0.00	0.00	0.00	0.07	35.48	0%	35.48	PM _{2.5}	0.59	7.60	lb/MMscf
Methane	15.44	55.45	1142.66	355.36	186.56	17.62	0.20	0.35	0.04	0.00	0.02	9.98	1783.70	98%	35.67	N ₂ O	0.03	0.00022	lb/MMBtu
Ethane	4.87	71.71	376.44	112.07	58.84	106.47	6.65	1.10	0.39	0.00	0.12	12.91	751.58	98%	15.03	H_2S	0.00		
Propane	3.35	110.57 27.70	283.04 52.23	77.10 12.47	40.48 6.55	320.02 103.04	21.11	2.97	2.95	0.00	0.22 0.05	19.90 4.99	881.70 218.20	98% 98%	17.63 4.36	LPS Van	or Controls / Fla	TRO DRE	1
Isobutane n-Butane	0.54	72.53	125.65	27.55	6.55 14.46	287.44	7.12 21.15	1.00 2.87	2.51 10.49	0.00	0.05	4.99 13.06	576.57	98% 98%	4.36	LPS VRU Colle	-		ł
Isopentane	0.27	22.30	36.85	6.27	3.29	95.82	7.26	0.99	3.76	0.00	0.05	4.01	180.88	98%	3.62		Operations)	98.0%	
n-Pentane	0.28	25.60	42.27	6.49	3.41	111.46	8.46	1.16	4.43	0.00	0.02	4.61	208.19	98%	4.16	`````	Downtime		(876 hrs)
i-C6	0.15	20.04	34.20	3.38	1.77	89.49	7.19	0.94	3.65	0.00	0.02	3.61	164.45	98%	3.29		perations)	10.0%	(-)
i-C7	0.03	8.17	15.50	0.80	0.42	36.67	2.89	0.39	1.50	0.00	0.01	1.47	67.85	98%	1.36	· · · ·	tion Efficiency	000%	
Octane	0.00	2.38	4.67	0.09	0.05	10.61	0.75	0.11	0.43	0.00	0.00	0.43	19.52	98%	0.39	0	<u>'</u> 4+	98%	
Nonane	0.00	0.38	0.58	0.00	0.00	1.71	0.11	0.02	0.07	0.00	0.00	0.07	2.94	98%	0.06	Flare Destruc	tion Efficiency	98%	
Benzene	0.00	1.01	0.80	0.07	0.04	4.49	0.23	0.05	0.18	0.00	0.18	0.18	7.22	98%	0.14	(C3	90 /0	
Toluene	0.00	0.82	0.89	0.04	0.02	3.66	0.20	0.04	0.15	0.00	0.15	0.15	6.11	98%	0.12				_
Ethylbenzene	0.00	0.02	0.03	0.00	0.00	0.10	0.01	0.00	0.00	0.00	0.00	0.00	0.17	98%	0.00	H2S molecular	0	34.08	4
o-Xylene	0.00	0.20	0.25	0.00	0.00	0.90	0.04	0.01	0.04	0.00	0.04	0.04	1.52	98%	0.03	SO2 molecular	0	64.06	4
n-Hexane	0.05	8.35	14.93	1.19	0.62	37.44	3.13	0.40	1.53	0.00	0.01	1.50	69.15	98%		Molar Volume		379.484	-
2,2,4-Trimethylpentane	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	0.00	Flare Operatin	g Hours	8760	1
Decanes Plus	0.00	0.02	0.01	0.00	0.00	0.07	0.00	0.00	0.00	0.00	0.00	0.00	0.10 0.00	98% 98%	0.00				
Decanes Plus Sat Total	26.58	431.51	2159.69	611.83	321.21	1230.50	86.51	12.56	32.74	0.00 0.00	1.67	77.67	4992.46	98%	151.32				
Total VOC	5.88	300.11	611.90	135.44	71.10	1102.91	79.64	10.94	31.70	0.00	0.94	54.02	2404.57		48.09				
Total HAP	0.06	10.40	16.90	1.30	0.68	46.58	3.60	0.49	1.90	0.00	0.37	1.87	84.17		1.68				
Heating Value (Btu/scf)	1269.30	2154.40	1338.01	1269.30	1269.30	2915.86	3080.19	2769.57	3346.32	0.00	1149.83	2154.40	1757.26		1.00	L			
Molecular Weight (lb/lbmol)	21.20	37.83	22.48	21.20	21.20	51.88	54.80	49.73	61.12	0.00	32.03	37.83							
Operating Hours (hr/yr)	1000	876	25	8760	8760	8760	8760	8760	8760	8760	8760	7884							
Mass Flow (ton/yr)	26.58	431.51	2159.69	611.83	321.21	1230.50	86.51	12.56	32.74	0.00	1.67	77.67	4992.46						
Volumetric Flow (MMscf/yr)	0.95	8.66	72.92	21.90	11.50	35.28	1.20	0.19	0.41	0.00	0.04	1.56	154.59						
Heat Release (MMBtu/yr)	1207.83	18648.47	97563.43	27797.66	14593.77	102867.32	3690.47	530.88	1360.44	0.00	45.58	3356.72	271662.57						
					Com	bustion Emissions	from Flare												
	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)						
Total NO _x	0.08	1.29	6.73	1.92	1.01	7.10	0.25	0.04	0.09	0.00	0.00	0.23	18.74						
Total CO	0.17	2.57	13.44	3.83	2.01	14.17	0.51	0.07	0.19	0.00	0.01	0.46	37.42						
Total SO ₂	0.00	0.02	0.06	0.02	0.01	0.03	0.00	0.00	0.00	0.00	0.00	0.00	0.15						
Total PM ₁₀	0.00	0.03	0.28	0.08	0.04	0.13	0.00	0.00	0.00	0.00	0.00	0.01	0.59						
Total PM _{2.5}	0.00	0.03	0.28	0.08	0.04	0.13	0.00	0.00	0.00	0.00	0.00	0.01	0.59						
Total VOC after comb.	0.12	6.00	12.24	2.71	1.42	22.06	1.59	0.22	0.63	0.00	0.02	1.08	48.09						
Total HAP after comb.	0.00	0.21	0.34	0.03	0.01	0.93	0.07	0.01	0.04	0.00	0.01	0.04	1.68						
Total n-Hexane after comb.	0.00	0.17	0.30	0.02	0.01	0.75	0.06	0.01	0.03	0.00	0.00	0.03	1.38						
Total Benzene after comb.	0.00	0.02	0.02	0.00 E 28	0.00	0.09	0.00	0.00	0.00	0.00	0.00	0.00	0.14						
Total CH ₄ Total N ₂ O	0.23	0.47	16.33	5.38 0.00	2.83 0.00	0.21	0.00	0.00	0.00	0.00	0.00	0.08	25.55 0.03						
		-	0.01	0.00 2152.15		0.01	0.00	0.00	0.00	0.00	0.00	0.00							
Total CO ₂ Total CO ₂ e	93.51 99.40	1523.80	7945.58 8357.04		1129.88 1201.03	7376.27 7385.00	256.22 256.37	39.44 39.51	93.72 93.77	0.00	5.76	274.28	20890.62 21 538 25						
	99.40	1536.18	8357.04	2287.67	1201.03	7385.00	250.57	39.51	93.77	0.00	5.77	276.51	21,538.25						
<u>Footnotes:</u> ^a Uncontrolled stream properties deterr																			
^b Tank emissions determined in ProMa		<i>y</i> 1		e.															
^c Pilot fuel gas emissions are conservati	•																		
^d Controlled Emissions Were Calculated	d by the Following: Ur	controlled Emissions	s * (1 - VRU Efficiency)) * (1 - Flare Destr	uction Efficiency))													

					Uncent	ired Maximum Ho	urly Emission Rat	es and Compositio	n to Flare ^{a,b}							Criteria	a Pollutant Emi	issions from	Flare ^e
		SSM			-	Oil Tank Va	<u>,</u>		apors (SKT1-2)	PW Tank Va	pors (PWT1-2)	Low Pres Sep ^d				Cincila			
Stream	HP Flare Blowdowns ^f	Low Pres Sep ^d Flash (VRU Off)	Inlet Gas Flaring ^g	HP Flare Pilot/Purge ^c	LP Flare Pilot/Purge ^c	Flash	W&B	Flash	W&B	Flash	W&B	Flash (VRU On) 98% Col Eff	Total Vapors to Flare	Destruction	Total Flare Exhaust		Emission Rate	Emission	Emission
Promax Stream Name	17. HPF	1. LP Separator	19. Inlet Flaring	15. HPF Pilot/	-	7. Condensate Tank Flash Gas	10. Condensate Tank W&B	6. Skim Tank Flash Gas	8. Skim Tank W&B	5. Water Tank Flash Gas	9. Water Tank W&B	1. LP Separator	(uncontrolled)	Efficiency	(controlled)	Component -		Factor	Factor Units
Component	Blowdowns (ton/yr)	Gas (ton/yr)	(ton/yr)	Purge Gas (ton/yr)	Purge Gas (ton/yr)	tank Flash Gas (ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	Gas (ton/yr)	(ton/yr)	(%)	(ton/yr)		(ton/yr)	-	
Triethylene Glycol	0.00	0.00	0.01	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.01	98%	0.00	NO _X	18.74	0.138	lb/MMBtu
Water	0.00	3.26	0.07	0.02	0.01	3.00	0.00	0.15	0.56	0.00	0.56	0.59	8.24	0%	8.24	CO	37.42	0.2755	lb/MMBtu
Hydrogen Sulfide	0.00	0.01	0.03	0.01	0.01	0.02	0.00	0.00	0.00	0.00	0.00	0.00	0.08	98%	0.00	SO ₂	0.15		
Carbon Dioxide	0.07	0.56	5.14	1.57	0.83	0.44	0.02	0.02	0.04	0.00	0.03	0.10	8.81	0%	8.81	PM ₁₀	0.59	7.60	lb/MMscf
Nitrogen	0.32	0.41	23.43	7.35	3.86	0.04	0.00	0.00	0.00	0.00	0.00	0.07	35.48	0%	35.48	PM _{2.5}	0.59	7.60	lb/MMscf
Methane	15.44	55.45	1142.66	355.36	186.56	17.62	0.20	0.35	0.04	0.00	0.02	9.98	1783.70	98%	35.67	N ₂ O	0.03	0.00022	lb/MMBtu
Ethane	4.87	71.71	376.44	112.07	58.84	106.47	6.65	1.10	0.39	0.00	0.12	12.91	751.58	98%	15.03	H ₂ S	0.00		
Propane	3.35	110.57	283.04	77.10	40.48	320.02	21.11	2.97	2.95	0.00	0.22	19.90	881.70	98%	17.63				
Isobutane	0.54	27.70	52.23	12.47	6.55	103.04	7.12	1.00	2.51	0.00	0.05	4.99	218.20	98%	4.36		or Controls / Fla	-	
n-Butane	1.20	72.53	125.65	27.55	14.46	287.44	21.15	2.87	10.49	0.00	0.19	13.06	576.57	98%	11.53	LPS VRU Colle		y 98.0%	
Isopentane	0.27	22.30	36.85	6.27	3.29	95.82	7.26	0.99	3.76	0.00	0.05	4.01	180.88	98%	3.62	· · ·	Operations)		
n-Pentane	0.28	25.60	42.27	6.49	3.41	111.46	8.46	1.16	4.43	0.00	0.02	4.61	208.19	98%	4.16		Downtime	10.0%	(876 hrs)
i-C6	0.15	20.04	34.20	3.38	1.77	89.49	7.19	0.94	3.65	0.00	0.02	3.61	164.45	98%	3.29	<u>`</u>	perations)		
i-C7	0.03	8.17	15.50	0.80	0.42	36.67	2.89	0.39	1.50	0.00	0.01	1.47	67.85 10.52	98%	1.36	Flare Destruc	5	98%	
Octane	0.00	2.38 0.38	4.67 0.58	0.09	0.05	10.61	0.75	0.11 0.02	0.43	0.00	0.00	0.43	19.52	98% 98%	0.39		24+ tion Efficiency		1
Nonane	0.00	1.01	0.58	0.00	0.00	1.71 4.49	0.11 0.23	0.02	0.18	0.00	0.00	0.07	2.94 7.22	98 % 98 %	0.06		C3	98%	(
Benzene Toluene	0.00	0.82	0.89	0.07	0.04	3.66	0.23	0.03	0.18	0.00	0.18	0.18	6.11	98 %	0.14				•
Ethylbenzene	0.00	0.02	0.03	0.04	0.02	0.10	0.20	0.04	0.00	0.00	0.00	0.00	0.11	98%	0.00	H2S molecular	woight	34.08	(
o-Xylene	0.00	0.20	0.05	0.00	0.00	0.90	0.04	0.00	0.04	0.00	0.04	0.00	1.52	98%	0.03	SO2 molecular	0	64.06	(
n-Hexane	0.05	8.35	14.93	1.19	0.62	37.44	3.13	0.40	1.53	0.00	0.01	1.50	69.15	98%		Molar Volume	0	379.484	•
2,2,4-Trimethylpentane	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%		Flare Operating		8760	•
Decanes Plus	0.00	0.02	0.01	0.00	0.00	0.07	0.00	0.00	0.00	0.00	0.00	0.00	0.10	98%	0.00		0		
Decanes Plus Sat	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	98%	0.00				
Total	26.58	431.51	2159.69	611.83	321.21	1230.50	86.51	12.56	32.74	0.00	1.67	77.67	4992.46		151.32				
Total VOC	5.88	300.11	611.90	135.44	71.10	1102.91	79.64	10.94	31.70	0.00	0.94	54.02	2404.57		48.09				
Total HAP	0.06	10.40	16.90	1.30	0.68	46.58	3.60	0.49	1.90	0.00	0.37	1.87	84.17		1.68				
Heating Value (Btu/scf)	1269.30	2154.40	1338.01	1269.30	1269.30	2915.86	3080.19	2769.57	3346.32	0.00	1149.83	2154.40	1757.26						
Molecular Weight (lb/lbmol)	21.20	37.83	22.48	21.20	21.20	51.88	54.80	49.73	61.12	0.00	32.03	37.83							
Operating Hours (hr/yr)	1000	876	25	8760	8760	8760	8760	8760	8760	8760	8760	7884							
Mass Flow (ton/yr)	26.58	431.51	2159.69	611.83	321.21	1230.50	86.51	12.56	32.74	0.00	1.67	77.67	4992.46						
Volumetric Flow (MMscf/yr) Heat Release (MMBtu/yr)	0.95 1207.83	8.66 18648.47	72.92 97563.43	21.90 27797.66	11.50 14593.77	35.28 102867.32	1.20 3690.47	0.19 530.88	0.41 1360.44	0.00	0.04 45.58	1.56 3356.72	154.59 271662.57						
Theat Release (Minibidi yi)	1207.05	10040.47	97505.45	21191.00	14090.77	102007.52	3090.47	550.88	1300.44	0.00	40.00	5550.72	271002.57	1					
-					Com	bustion Emissions	from Flare]					
	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)]					
Total NO _x	0.08	1.29	6.73	1.92	1.01	7.10	0.25	0.04	0.09	0.00	0.00	0.23	18.74						
Total CO	0.17	2.57	13.44	3.83	2.01	14.17	0.51	0.07	0.19	0.00	0.01	0.46	37.42						
Total SO ₂	0.00	0.02	0.06	0.02	0.01	0.03	0.00	0.00	0.00	0.00	0.00	0.00	0.15						
Total PM ₁₀	0.00	0.03	0.28	0.08	0.04	0.13	0.00	0.00	0.00	0.00	0.00	0.01	0.59						
Total PM _{2.5}	0.00	0.03	0.28	0.08	0.04	0.13	0.00	0.00	0.00	0.00	0.00	0.01	0.59						
Total VOC after comb.	0.12	6.00	12.24	2.71	1.42	22.06	1.59	0.22	0.63	0.00	0.02	1.08	48.09						
Total HAP after comb.	0.00	0.21	0.34	0.03	0.01	0.93	0.07	0.01	0.04	0.00	0.01	0.04	1.68						
Total n-Hexane after comb.	0.00	0.17	0.30	0.02	0.01	0.75	0.06	0.01	0.03	0.00	0.00	0.03	1.38						
Total Benzene after comb.	0.00	0.02	0.02	0.00	0.00	0.09	0.00	0.00	0.00	0.00	0.00	0.00	0.14						
Total CH ₄	0.23	0.47	16.33	5.38	2.83	0.21	0.00	0.00	0.00	0.00	0.00	0.08	25.55						
Total N ₂ O	0.000	0.00	0.01	0.00	0.00	0.01	0.00	0.00	0.00	0.00	0.00	0.00	0.03						
Total CO ₂	93.51	1523.80	7945.58	2152.15	1129.88	7376.27	256.22	39.44	93.72	0.00	5.76	274.28	20890.62						
Total CO ₂ e	99.40	1536.18	8357.04	2287.67	1201.03	7385.00	256.37	39.51	93.77	0.00	5.77	276.51	21,538.25						
Footnotes:																		1	
^a Uncontrolled stream properties determ	nined via ProMax.																		
^b Tank emissions determined in ProMa	x are calculated at the	maximum daily liqui	d surface temperature	2.															
^c Pilot fuel gas emissions are conservati	vely calculated based	on observed flowrates	S																
^d Controlled Emissions Were Calculated	l by the Following: Ur	controlled Emissions	* (1 - VRU Efficiency)	* (1 - Flare Destr	uction Efficiency)														

^e Flare CO and NOx emission factors from TCEQ Air Permit Techincal Guidance for Chemical Sources. PM and PM2.5 emission factors from AP-42, Table 1.4-1 and 1.4-2, July 1998. SO2 emissions assume 100% conversion of H2S to SO2.

f Blowdowns are estimated to be @ 952 SCF per blowdown. XTO conservatively estimates 1000 blowdowns per year and 1 blowdown per hour

g XTO conservatively estimates 73 MMscf of inlet gas flaring per year @ 2.92 MMscf/hr max rate

h GHG emissions source is 40 CFR § 98.233 (n), 40 CFR § 98.233(v) for CH4 and CO2 mass emissions, 40 CFR § 98.233(z) for N2O mass emissions,

BULLDOG COMPRESSOR STATION

HPF FLARE BLOWDOWN GAS ROUTED TO FLARE (EXAMPLE CALCULATION)

					s Emissions San	ipre curcuru		
1) $E_{s,CH4} = V_a * 2$	X _{CH4} * [(1- η)*	$Z_{L} + Z_{U}$]	=	11,053.82	SCF/Yr		Source	Annual Volume
	951,570.00						17. HPF Blowdowns	951,570.00
	0.580820292							
N =	0.98							
$Z_L =$	1.00						Total	951,570.00
$Z_U =$	0.00							
2) E _{s,CO2} (uncon	$hbusted) = V_a$	* X _{CO2}	=	2,447.09	SCF/Yr			
. , .	951,570.00							
$X_{CO2} =$								
3) E _{s,CO2} (combu	$(sted) = \sum (n)^2$	* V2 * Vi * Ri *	7.)					
$S_{s,CO2}$ (combe N =	0.98	va ij Rj	ΣL)					
$V_a =$			Rj =		$E_{a, CO2} =$			
$\ddot{\mathbf{Y}}_{J} =$	Methane	0.5808	, 1		541,637.34			
,	Ethane	0.1832	2		341,643.21			
	Propane	0.1260	3		352,523.10			
	Butane	0.0654	4		243,978.51			
	Pentane +	0.0280	5		130,567.61			
$Z_L =$	1.00				1,610,349.77	SCF/Yr		
4) Mass _{s,i} = $E_{s,i}$	* ρ; * 10 ³							
$E_{s,i}$ (CH4) =								
E _{s,i} (CO2) =		36						
p_i (CH4) =		kg/ft3	=	0.21	metric tons			
p _i (CO2) =	0.0526	kg/ft3	=	84.83	metric tons			
5) CO ₂ e = CO ₂ -	+ (CH ₄ X GW	P)	short tons	CO ₂ e				
CO2 =	84.83	=	93.51	93.51				
CH4 =	0.21	=	0.23	5.85				
CH4 GWP =	25			99.36				

Footnotes: ^a Source is 40 CFR § 98.233 (n), 40 CFR § 98.233(v) for CH4 and CO2 mass emissions, 40 CFR § 98.233(z) for N2O mass emissions,

XTO ENERGY INC. BULLDOG COMPRESSOR STATION DEHYDRATORS 1-3 VAPORS ROUTED TO VAPOR COMBUSTOR (VC1)

VOC/HAP Emissions for Dehydration Units (DEHY1 - DEHY3) - Routed to Vapor Combustor (VC1)

													- • () h
		Uncontrolled	Maximum Hourly Emission Rate	es and Composition to Combustion	Device(s)"		r			Criteria Pollut	ant Emissions Co	mbustion E	Jevice(s)
Stream	Pilot	Emissions		Column Emissions	-	ombustion Device(s) ntrolled)	Destruction Efficiency	Combustion I	Fotal Device(s) Exhaust	Component	Emission Rate	Emission	Emission
Promax Stream Name	24. VC1 Pilot Fuel	24. VC1 Pilot Fuel	13. BTEX Cond Vapors to Combustion	13. BTEX Cond Vapors to Combustion	(0			(con	trolled)	Component		Factor	Factor Units
Component	(1b/hr)	(ton/yr)	(1b/hr)	(ton/yr)	(lb/hr)	(ton/yr)	(%)	(lb/hr)	(ton/yr)		(lb/hr)		
Triethylene Glycol	0.00	9.67E-05	0.00	1.74E-07	0.00	0.00	98%	0.00	0.00	NO _X	0.45	0.138	lb/MMBtu
Water	0.00	2.16E-03	1.87	8.20	1.87	8.20	0%	1.87	8.20	СО	0.90	0.2755	lb/MMBtu
Hydrogen Sulfide	0.00	9.57E-04	0.15	0.67	0.15	0.67	98%	0.00	0.01	SO ₂	0.29		
Carbon Dioxide	0.04	0.16	2.39	10.47	2.43	10.63	0%	2.43	10.63	PM ₁₀	0.01	7.60	lb/MMscf
Nitrogen	0.17	0.74	0.02	0.07	0.18	0.81	0%	0.18	0.81	PM _{2.5}	0.01	7.60	lb/MMscf
Methane	8.11	35.54	9.50	41.62	17.61	77.15	98%	0.35	1.54	N ₂ O	0.00	0.00022	lb/MMBtu
Ethane	2.56	11.21	22.15	97.03	24.71	108.24	98%	0.49	2.16	H_2S	0.00		
Propane	1.76	7.71	38.47	168.51	40.23	176.22	98%	0.80	3.52				
Isobutane	0.28	1.25	6.77	29.63	7.05	30.88	98%	0.14	0.62	Combustion Dev	ice Destruction	98%	
n-Butane	0.63	2.75	27.45	120.23	28.08	122.98	98%	0.56	2.46	Efficienc	y C4+	98%	
Isopentane	0.14	0.63	10.71	46.93	10.86	47.56	98%	0.22	0.95			000/	
n-Pentane	0.15	0.65	14.75	64.59	14.90	65.24	98%	0.30	1.30	Combustion Devi	ce Efficiency C3	98%	
i-C6	0.08	0.34	10.17	44.56	10.25	44.90	98%	0.21	0.90			•	
i-C7	0.02	0.08	2.99	13.08	3.01	13.16	98%	0.06	0.26	H2S molecular weig	zht	34.08	3
Octane	0.00	0.01	0.31	1.36	0.31	1.36	98%	0.01	0.03	SO2 molecular weig		64.06	-
Nonane	0.00	3.84E-04	0.02	0.07	0.02	0.07	98%	0.00	0.00	Molar Volume (scf/		379.484	-
Benzene	0.00	0.01	7.52	32.95	7.52	32.96	98%	0.15	0.66	Combustor Operati	,	8760	
Toluene	0.00	3.38E-03	3.74	16.36	3.74	16.36	98%	0.07	0.33	Compusier offerna	1.6 1 10 010		1
Ethylbenzene	0.00	5.06E-05	0.03	0.15	0.03	0.15	98%	0.00	0.00				
o-Xylene	0.00	3.32E-04	0.36	1.58	0.36	1.58	98%	0.00	0.03				
n-Hexane	0.03	0.12	4.14	18.14	4.17	18.26	98%	0.01	0.37				
2,2,4-Trimethylpentane	0.00		0.00		0.00	0.00	98%	0.00	0.00				
Decanes Plus	0.00	1.66E-06	0.00	8.82E-04	0.00	0.00	98%	0.00	0.00				
Decanes Plus Sat	0.00		0.00	0.02E-04	0.00	0.00	98%	0.00	0.00				
Total	13.97	61.18	163.52	716.20	177.48	777.38	1	7.94	34.79				
Total VOC	3.09		103.32	558.14	130.52	571.69		2.61	11.43				
		13.54						1	+				
Total HAP	0.03	0.13	15.80	69.18	15.83	69.31		0.32	1.39				
Heating Value (Btu/scf)	1,269.31	1,269.31	2,460.05	2,460.05	2460.05	2460.05	-						
Molecular Weight (lb/lbmol)	21.20	21.20	44.85	44.85			4						
Operating Hours (hr/yr) Mass Flow	8,760 13.97 lb/hr	8,760 61.18 ton/yr	8,760 127.87 lb/hr	8,760 560.09 ton/yr	 127.87 lb/hr	 560.09 ton/yr	4						
Volumetric Flow	250 scf/hr	2 MMscf/yr	1,082 scf/hr	9 MMscf/yr	1,332 scf/hr	12 MMscf/yr	-						
Heat Release (MMBtu/hr)	0.32 MMBtu/hr	2,779.79 MMBtu/yr	2.66 MMBtu/hr	23,315.17 MMBtu/yr	3.28 MMBtu/hr	23,315.17 MMBtu/yr	1						
(/	· · · · · · · · · · · · · · · · · · ·				, , , , , , , , , , , , , , , , , , , ,	-						
		Combustion Emiss	sions from Combustion Device(s)			1						
	(1b/hr)	(ton/yr)	(lb/hr)	(ton/yr)	(lb/hr)	(ton/yr)							
Total NO _x	0.04	0.19	0.37	1.61	0.41	1.80							
Total CO	0.09	0.38	0.73	3.21	0.82	3.59							
Total SO ₂	0.00	1.80E-03	0.29	1.26	0.29	1.26							
Total PM ₁₀	0.002	0.01	0.008	0.04	0.01	0.04							
Total PM _{2.5}	0.00	0.01	0.01	0.04	0.01	0.04							
Total VOC (slip)	0.06	0.27	2.55	11.16	2.61	11.43							
Total HAP (slip)	0.00	2.59E-03	0.32	1.38	0.32	1.39							
Total n-Hexane (slip)	0.00	0.00	0.08	0.36	0.08	0.37	1						
Total Benzene (slip)	0.00	0.00	0.15	0.66	0.15	0.66							
Total CH ₄	0.12	0.54	0.07	0.30	0.19	0.84				Large	Glycol Unit - MA		ck l
Total N ₂ O	0.000	6.76E-04	0.07	0.01	0.00	0.04						Limit	<u></u>
Total CO ₂			559.83			2,668.48				# of Units	3 10,655		
	49.41	216.43 230.09		2,452.05	609.24	-				Flow per Dehy	0.22	85,000 SCF	-/Day
Total CO ₂ e	52.53	230.09	561.92	2,461.19	614.45	2,691.28	J			Benzene Emissions	0.22	1 ton/yr	

Footnotes:

^a Uncontrolled stream properties determined via ProMax.

^b Flare CO and NOx emission factors from TCEQ Air Permit Techincal Guidance for Chemical Sources. PM and PM2.5 emission factors from AP-42, Table 1.4-1 and 1.4-2, July 1998. SO2 emissions assume 100% conversion of H2S to SO2. ^cFlash tank emissions are routed back to inlet slug catcher.

BULLDOG COMPRESSOR STATION

ROAD EMISSIONS

Total Suspended Particle Emiss E = k(sL/2) ^a (W/3) ^b	sions	$PM_{10} Emissions$ $E = k(sL/2)^{a}(W/3)^{b}$		$PM_{2.5} Emissions$ $E = k(sL/2)^{a}(W/3)^{b}$	
a	0.7	a	0.9	а	0.9
b	0.45	b	0.45	b	0.45
k	4.9	k	1.5	k	0.15
Silt %	4.8	Silt %	4.8	Silt %	4.8
Vehicle Weight (tons)	28	Vehicle Weight (tons)	28	Vehicle Weight (tons)	28
E (lbs/VMT)	7.05	E (lbs/VMT)	1.80	E (lbs/VMT)	0.18
Rain Days	70	Rain Days	70	Rain Days	70
E-Annual (lbs/VMT)	5.70	E-Annual (lbs/VMT)	1.45	E-Annual (lbs/VMT)	0.15
Truckloads per year	210	Truckloads per day	210	Truckloads per day	210
Driving Distance Per Load (ft)	1000	Driving Distance Per Load (ft)	1000	Driving Distance Per Load (ft)	1000
Annual Distance (miles)	40	Annual Distance (miles)	40	Annual Distance (miles)	40
Control Efficiency - 15 MPH Limit	0.44	Control Efficiency - 15 MPH Limit	0.44	Control Efficiency - 15 MPH Limit	0.44
Emissions (lbs/hr)	0.60	Emissions (lbs/hr)	0.15	Emissions (lbs/hr)	0.02
Emissions (tpy)	0.06	Emissions (tpy)	0.02	Emissions (tpy)	0.00

Emissions (lbs/hr) = Driving Distance (ft)/ 5280 * E (lbs/VMT) Emissions (tpy) = Annual Distance * E / 2000

References:

EPA. "Compilation of Air Pollutant Emission Factors, Volume 1: Stationary Point and Area Sources," Section 13.2.2 AP-42, Ofice of Air Quality Planning and Standards, Research Triangle Park, NC. 5th edition (11/2006).

XTO ENERGY, INC. BULLDOG COMPRESSOR STATION FUGITIVE EMISSIONS

	Operating Hours:					8760 hours	/vear				
	Emission Factor So	urce				Standard EFs - EPA-453/	<i>v</i>	able 2-4			
	Control Efficiency					None					
	Emission Buffer (%					0					
		•]•		<u> </u>		, i i i i i i i i i i i i i i i i i i i					
Service	Component Type	Count		n Factor source) ^a	Control (%) ^b Pollutant	Mass	Uncontrolled Emissions	Uncontrolled Emissions	Controlled Emissions	Controlled Emissions	
	1 51		Table 2-4	Table 2-8			Fraction	(1b/hr)	(tpy)	(1b/hr)	(tpy)
	Valves	720	9.92E-03	5.51E-05	0.0%	VOC	0.300	2.6726	11.7061	2.6726	11.7061
	Pump Seals	0	5.29E-03	7.72E-04	0.0%	H2S	0.000	0.0001	0.0004	0.0001	0.0004
	Connectors	1440	4.41E-04	2.20E-05	0.0%	Benzene	0.001	0.0045	0.0199	0.0045	0.0199
0	Flanges	720	8.60E-04	1.26E-05	0.0%	Toluene	0.001	0.0072	0.0316	0.0072	0.0316
Gas	Open-Ended Lines	72	4.41E-03	3.31E-05	0.0%	E-Benzene	0.000	0.0004	0.0020	0.0004	0.0020
	Other	10	1.94E-02	2.65E-04	0.0%	Xylenes	0.000	0.0041	0.0179	0.0041	0.0179
	Relief Valves	0	1.94E-02	2.65E-04	0.0%	n-Hexane	0.008	0.0742	0.3250	0.0742	0.3250
						2,2,4 Trimethylpentane	0.000	0.0000	0.0000	0.0000	0.0000
	Valves	0	1.85E-05	1.85E-05	0.0%	VOC	0.978	0.0000	0.0000	0.0000	0.0000
	Pump Seals	0	0.00E+00	0.00E+00	0.0%	H2S	0.000	0.0000	0.0000	0.0000	0.0000
	Connectors	0	1.65E-05	1.65E-05	0.0%	Benzene	0.015	0.0000	0.0000	0.0000	0.0000
	Flanges	0	8.60E-06	8.60E-07	0.0%	Toluene	0.005	0.0000	0.0000	0.0000	0.0000
Heavy Oil	Open-Ended Lines	0	3.09E-04	1.59E-05	0.0%	E-Benzene	0.012	0.0000	0.0000	0.0000	0.0000
	Other	0	3.09E-04	7.05E-05	0.0%	Xylenes	0.001	0.0000	0.0000	0.0000	0.0000
	Relief Valves	0	3.09E-04	7.05E-05	0.0%	n-Hexane	0.007	0.0000	0.0000	0.0000	0.0000
						2,2,4 Trimethylpentane	0.085	0.0000	0.0000	0.0000	0.0000
	Valves	236	5.51E-03	4.19E-05	0.0%	VOC	0.978	1.9625	8.5958	1.9625	8.5958
	Pump Seals	15	2.87E-02	1.12E-03	0.0%	H2S	0.000	0.0000	0.0000	0.0000	0.0000
	Connectors	472	4.63E-04	2.14E-05	0.0%	Benzene	0.015	0.0303	0.1327	0.0303	0.1327
1.1.01	Flanges	236	2.43E-04	5.29E-06	0.0%	Toluene	0.005	0.0100	0.0438	0.0100	0.0438
Light Oil	Open-Ended Lines	0	2.87E-03	3.09E-05	0.0%	E-Benzene	0.012	0.0242	0.1058	0.0242	0.1058
	Other	0	1.65E-02	2.43E-04	0.0%	Xylenes	0.001	0.0026	0.0112	0.0026	0.0112
	Relief Valves	0	1.65E-02	2.43E-04	0.0%	n-Hexane	0.007	0.0135	0.0593	0.0135	0.0593
						2,2,4 Trimethylpentane	0.085	0.1713	0.7502	0.1713	0.7502
	Valves	153	2.16E-04	2.14E-05	0.0%	VOC	0.978	0.2573	1.1272	0.2573	1.1272
	Pump Seals	10	5.29E-05	5.29E-05	0.0%	H2S	0.000	0.0000	0.0000	0.0000	0.0000
	Connectors	306	2.43E-04	2.20E-05	0.0%	Benzene	0.015	0.0040	0.0174	0.0040	0.0174
	Flanges	153	6.39E-06	6.39E-06	0.0%	Toluene	0.005	0.0013	0.0057	0.0013	0.0057
Water/Oil	Open-Ended Lines	0	5.51E-04	7.72E-06	0.0%	E-Benzene	0.012	0.0032	0.0139	0.0032	0.0139
	Other	5	3.09E-02	1.30E-04	0.0%	Xylenes	0.001	0.0003	0.0015	0.0003	0.0015
	Relief Valves	0	3.09E-02	1.30E-04	0.0%	n-Hexane	0.007	0.0018	0.0078	0.0018	0.0078
						2,2,4 Trimethylpentane	0.085	0.0225	0.0984	0.0225	0.0984

Fugitive Emission Summary

Pollutant	Uncontroll	ed Emissions	Controlled	Emissions
	(lb/hr)	(tpy)	(lb/hr)	(tpy)
VOC	4.89	21.43	4.89	21.43
HAPs	0.38	1.64	0.38	1.64
H2S	0.00	0.00	0.00	0.00
Benzene	0.04	0.17	0.04	0.17
Toluene	0.02	0.08	0.02	0.08
E-Benzene	0.03	0.12	0.03	0.12
Xylenes	0.01	0.03	0.01	0.03
n-Hexane	0.09	0.39	0.09	0.39
2,2,4 Trimethylpentane	0.19	0.85	0.19	0.85

Footnotes:

^a Factors are taken from EPA Document EPA-453/R-095-017, November 1995, Table 2-4

^bControl efficiencies are taken from EPA Document EPA-453/R-095-017, November 1995, Table 5-2

^cGas/Vapor based inlet gas. Heavy Oil, Light Oil, and Water/Oil fugitives were based on liquid analysis of inlet separator hydrocarbon liquid.

XTO ENERGY, INC. BULLDOG COMPRESSOR STATION FACILITY INLET GAS ANALYSIS - PROMAX

(Gas Composition			
Component	Mole %	Weight %		
TEG	0.000	0.0000		
Water	0.000	0.0000		
Hydrogen Sulfide	0.001	0.0010		
Carbon Dioxide	0.121	0.2330		
Nitrogen	0.864	1.0580		
Methane	73.632	51.6360		
Ethane	12.988	17.0720		
Propane	6.704	12.9230		
Isobutane	0.949	2.4110		
n-Butane	2.303	5.8510		
Isopentane	0.551	1.7380		
n-Pentane	0.664	2.0950		
Other C-6's	0.482	1.8000		
Heptanes	0.327	1.4200		
Octanes	0.111	0.5390		
Nonanes	0.032	0.1770		
Benzene	0.015	0.0510		
Toluene	0.020	0.0810		
E-Benzene	0.001	0.0050		
Xylenes	0.010	0.0460		
n-Hexane	0.221	0.8330		
2,2,4 Trimethylpentane	0.000	0.0000		
Decanes Plus	0.005	0.0310		
Decanes Plus Satellite	0.000	0.0000		
Total	100.001	100.0010		
MOLECULAR W	JEICHT	22.89		
SATURATED		22.88 1371		
NMHC (WT		47.073		
VOCs (WT	,	30.00		
HAPs (WT	/	1.02		
H2S (MOL	/0)	0.00		

XTO ENERGY, INC. BULLDOG COMPRESSOR STATION FACILITY INLET FLUID ANALYSIS - PROMAX

Fl	uid Composition	
		T
Component	Mole %	Weight %
TEG	0.0000	0.0000
Water	0.0000	0.0000
Hydrogen Sulfide	0.0000	0.0000
Carbon Dioxide	0.0129	0.0075
Nitrogen	0.0167	0.0062
Methane	2.8473	0.6026
Ethane	3.9579	1.5701
Propane	8.4770	4.9315
Isobutane	3.2673	2.5054
n-Butane	12.1250	9.3186
Isopentane	8.1300	7.7386
n-Pentane	12.6670	12.0571
Other C-6's	7.9339	9.0203
Heptanes	17.1885	20.9987
Octanes	10.5388	14.6036
Nonanes	1.6426	2.7426
Benzene	0.7463	1.5099
Toluene	0.4833	0.4981
E-Benzene	0.9907	1.2043
Xylenes	0.0912	0.1277
n-Hexane	0.4815	0.6744
2,2,4 Trimethylpentane	7.5090	8.5370
Decanes Plus	0.8930	1.3457
Decanes Plus Satellite	0.0000	0.0000
Total	100.000	100.0000
MOLECULAR W	FICHT	75.80
SATURATED		75.00
NMHC (WT		99.38
VOCs (WT)		97.81
HAPs (WT		12.55
H2S (MOL	0.000	

Tab 7

Section 7 - Information Used To Determine Emissions

Section 7

Information Used To Determine Emissions

Information Used to Determine Emissions shall include the following:

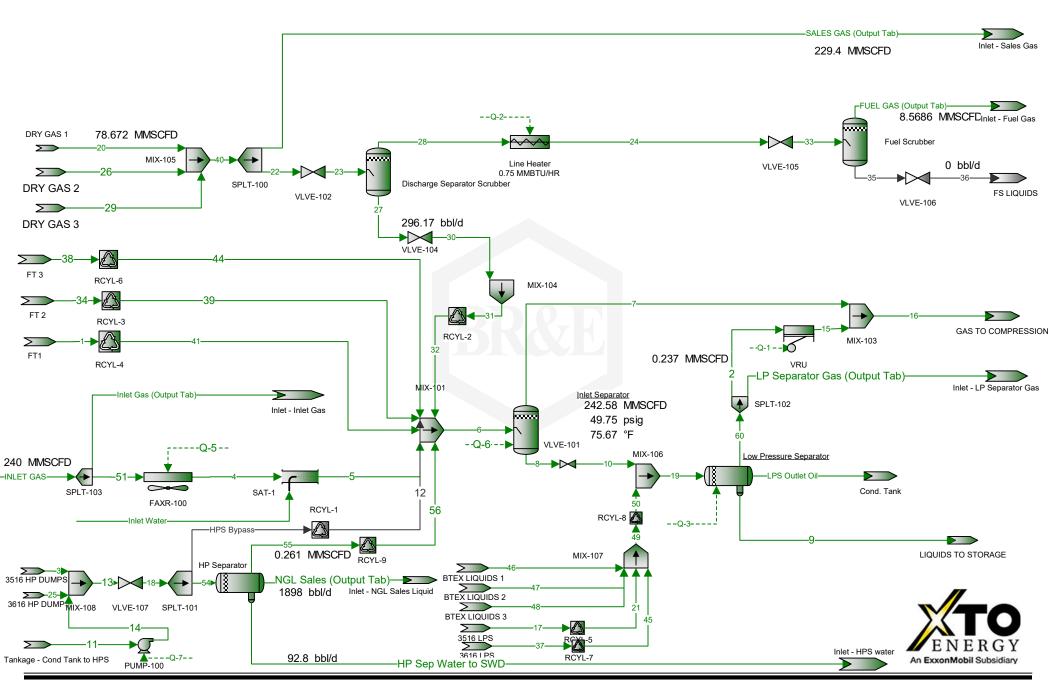
- \square If manufacturer data are used, include specifications for emissions units <u>and</u> control equipment, including control efficiencies specifications and sufficient engineering data for verification of control equipment operation, including design drawings, test reports, and design parameters that affect normal operation.
- □ If test data are used, include a copy of the complete test report. If the test data are for an emissions unit other than the one being permitted, the emission units must be identical. Test data may not be used if any difference in operating conditions of the unit being permitted and the unit represented in the test report significantly effect emission rates.
- ☑ If the most current copy of AP-42 is used, reference the section and date located at the bottom of the page. Include a copy of the page containing the emissions factors, and clearly mark the factors used in the calculations.
- □ If an older version of AP-42 is used, include a complete copy of the section.
- \blacksquare If an EPA document or other material is referenced, include a complete copy.
- □ Fuel specifications sheet.
- ☑ If computer models are used to estimate emissions, include an input summary (if available) and a detailed report, and a disk containing the input file(s) used to run the model. For tank-flashing emissions, include a discussion of the method used to estimate tank-flashing emissions, relative thresholds (i.e., permit or major source (NSPS, PSD or Title V)), accuracy of the model, the input and output from simulation models and software, all calculations, documentation of any assumptions used, descriptions of sampling methods and conditions, copies of any lab sample analysis.

The Bulldog Compressor Station gas inlet composition was obtained from the Muy Wano 18 Tank Battery Inlet Separator hydrocarbon gas sample. The Muy Wano 18 Tank Battery gas analysis is representative of the hydrocarbons from the surrounding wells and batteries. The sales gas composition from this battery was used as the inlet gas composition for the station in the ProMax process simulation.

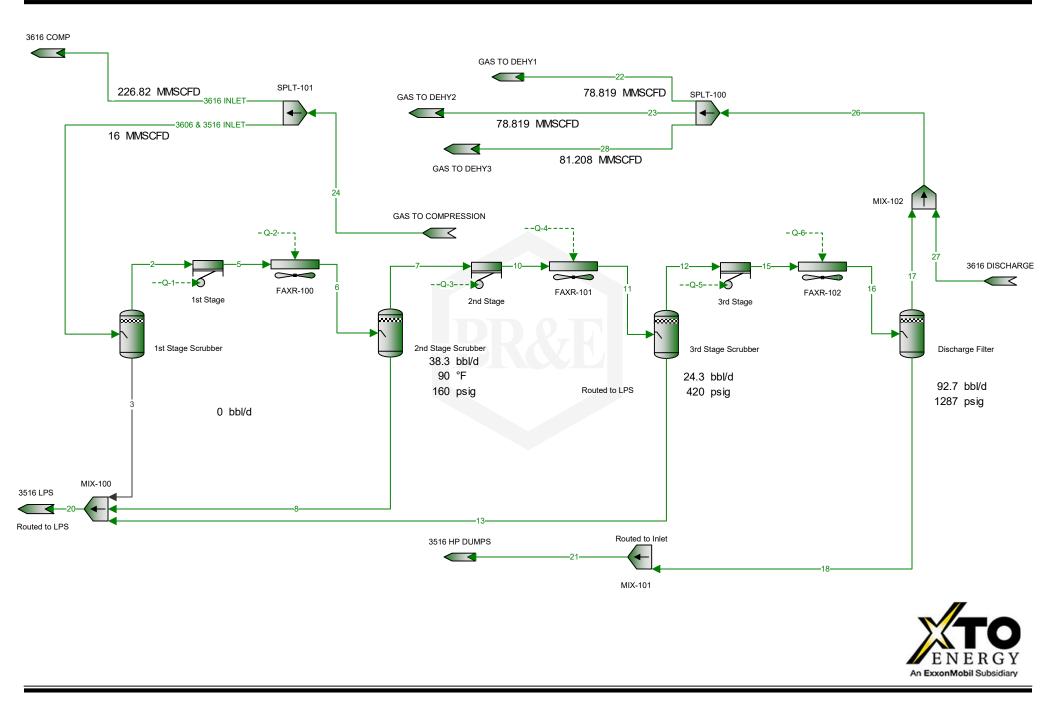
A liquid sample was taken from the Wolverine Compressor station Inlet Separator Hydrocarbon liquid sample was used for the decanes plus speciation in the ProMax process simulation.

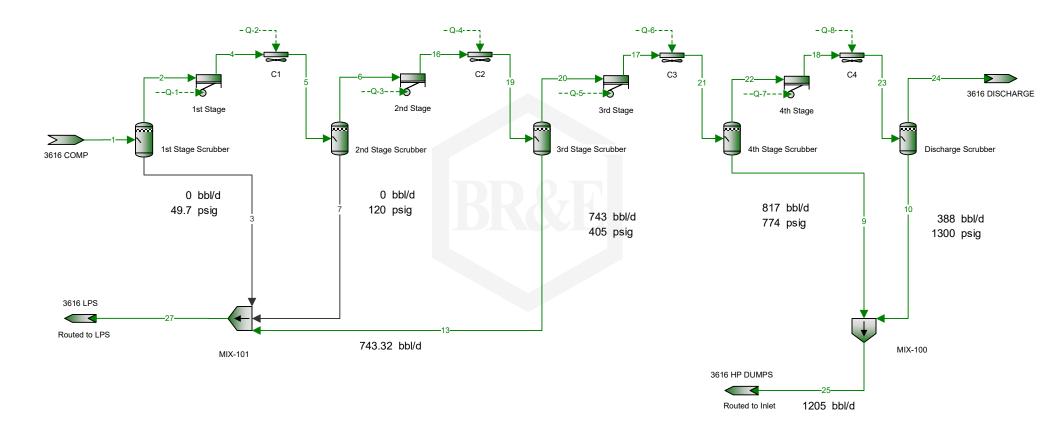
All supporting documentation is provided in this section.

BULLDOG COMPRESSOR STATION

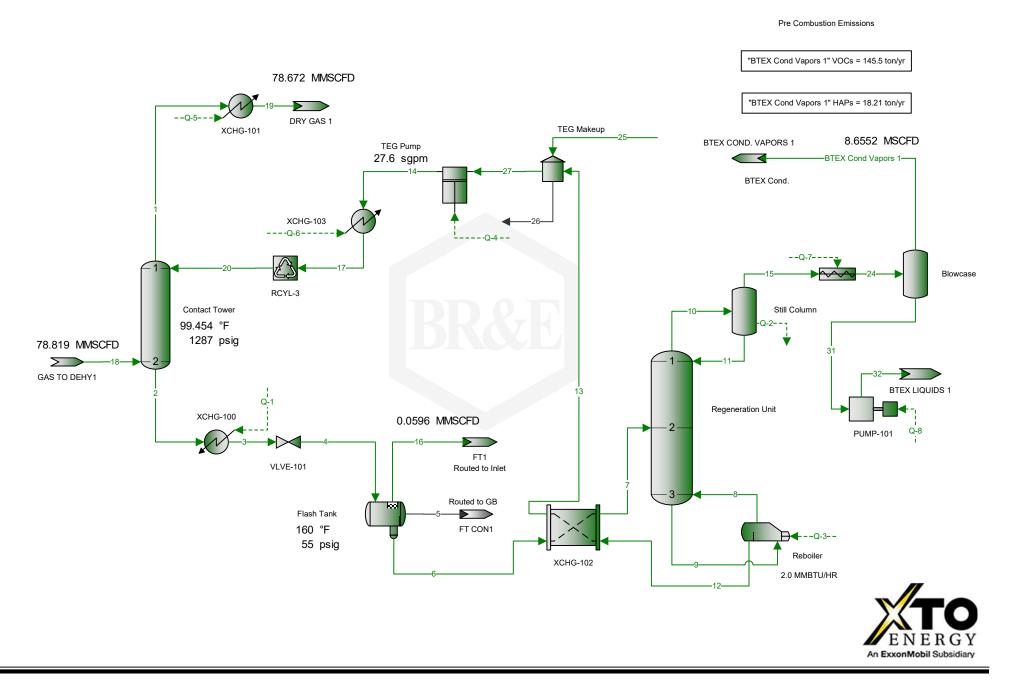


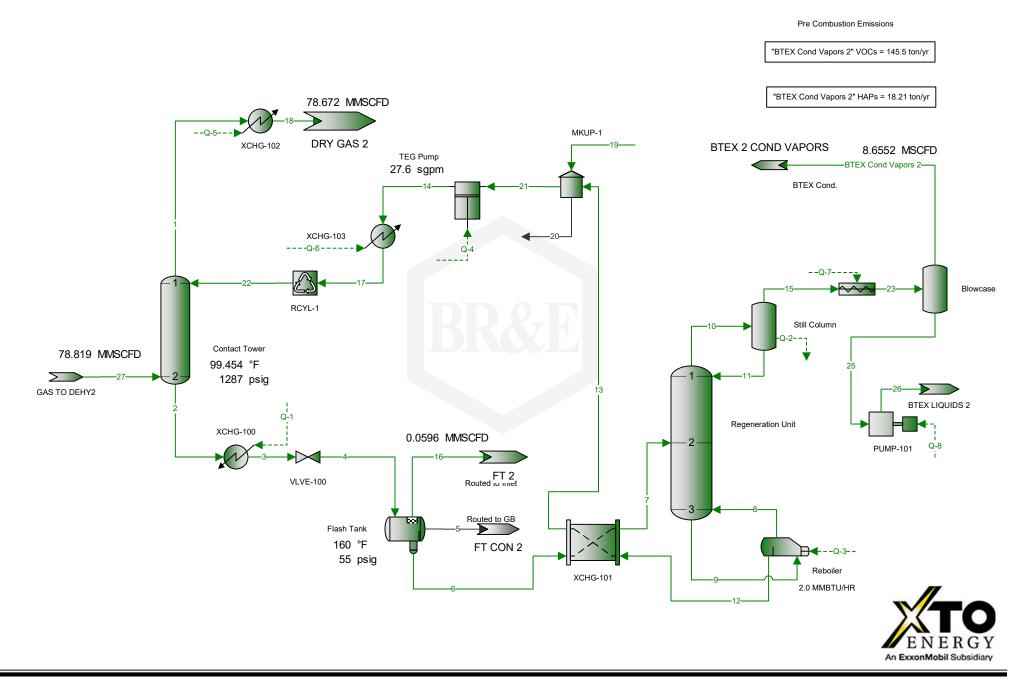
BULLDOG COMPRESSOR STATION

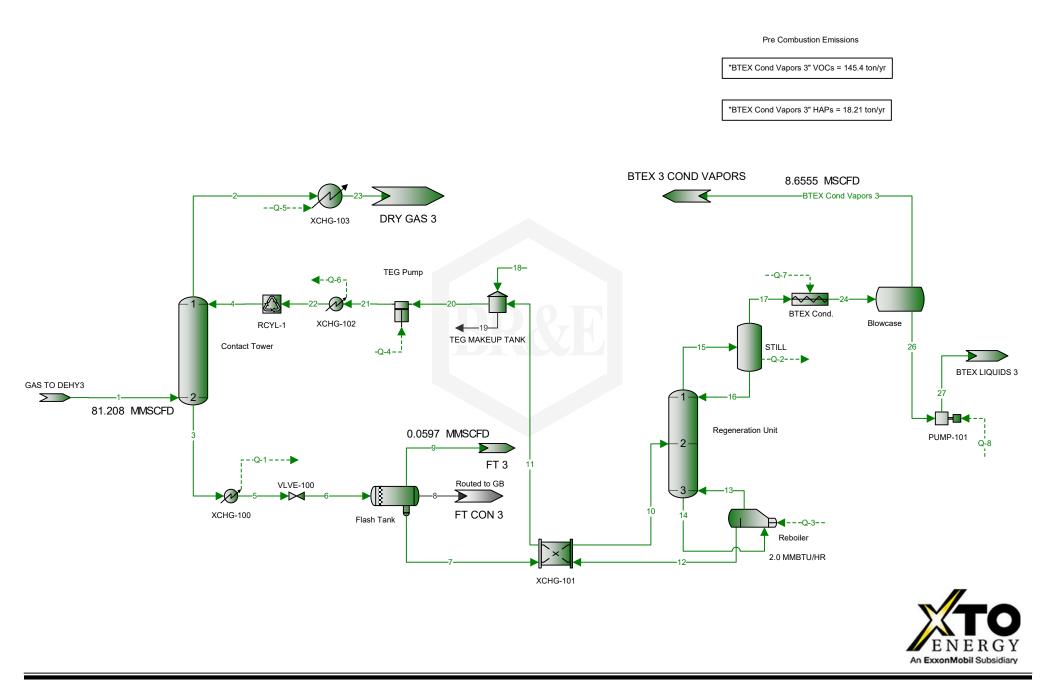


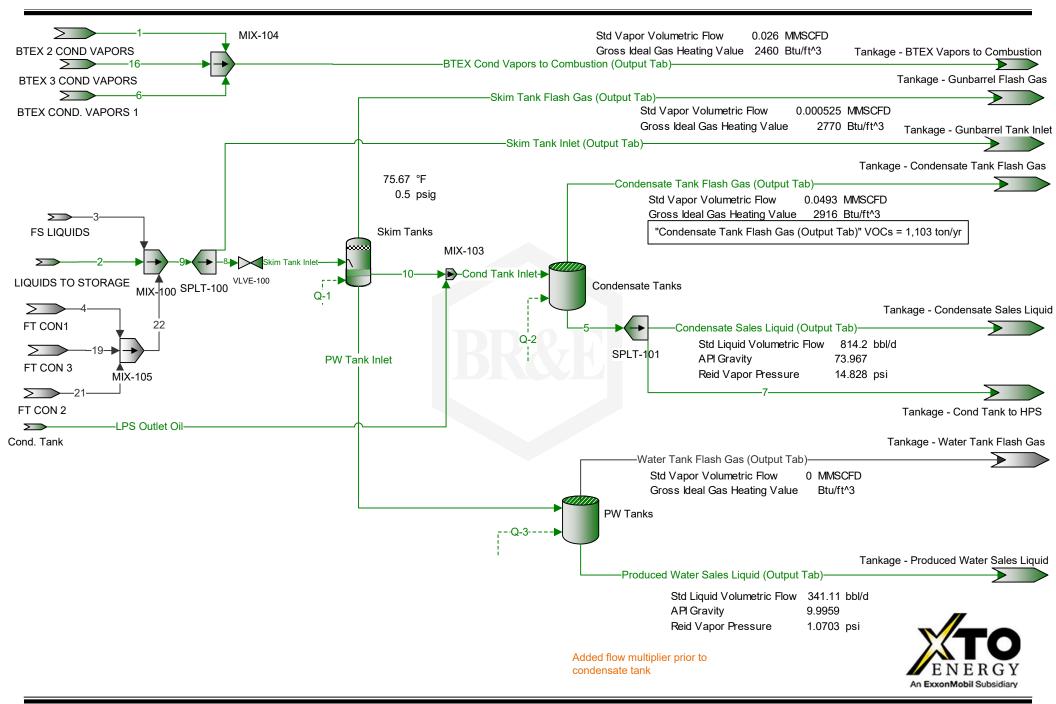


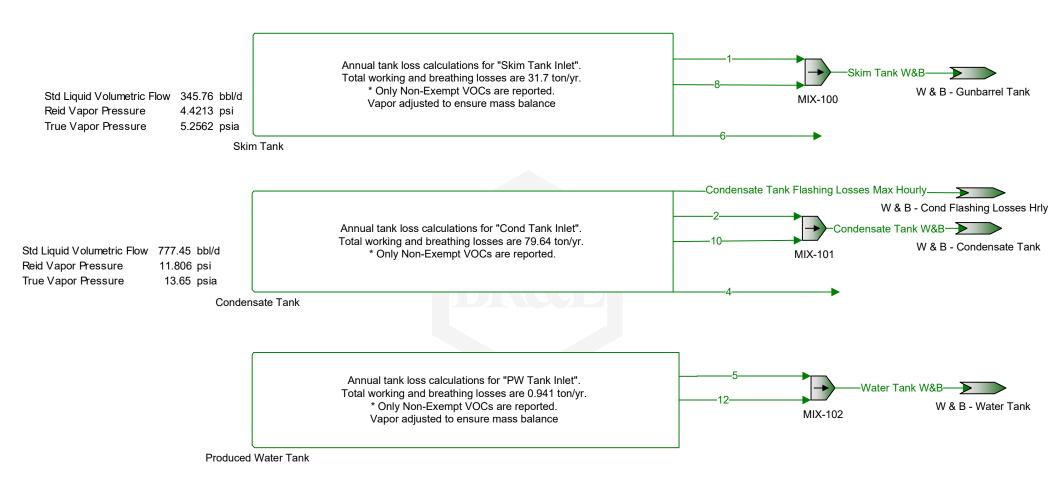




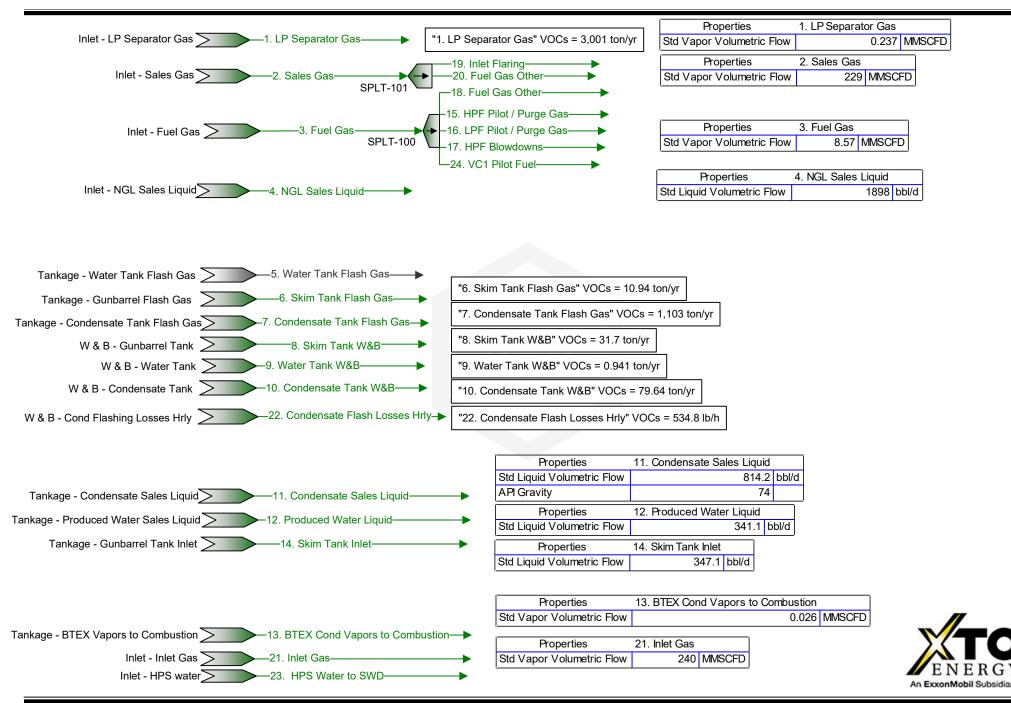












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				Train NSR Bulldog CS.pn			Page 1 of 11
			All St	reams Report treams by Total Phase			
Client Name:	DELAWARE DI				Job:		
	Bulldog Compre				JOD:		
	<u> </u>	ssor station					
Flowsheet:	Output						
			Conn	ections			
			1. LP	2. Sales Gas	3. Fuel Gas	4. NGL Sales	5. Water Tank
			Separator Gas	2. 00103 003	5.1 461 643	Liquid	Flash Gas
From Block			Inlet - LP	Inlet - Sales	Inlet - Fuel Gas	Inlet - NGL	Tankage -
			Separator Gas	Gas	The Fuel Gas	Sales Liquid	Water Tank
			Separator Gas	Gas		Sales Liquiu	
							Flash Gas
To Block				SPLT-101	SPLT-100		
			Stream C	omposition			
			1. LP	2. Sales Gas	3. Fuel Gas	4. NGL Sales	5. Water Tank
			Separator Gas	2. Jaies Gas	S. Fuel Gas		Flash Gas
Mass Flow				lh/h	lh/h	Liquid Ib/h	lb/h
			lb/h	lb/h	lb/h		n/ai
Triethylene Glycol			2.37625E-08	3.22561	0.00440314	4.28295E-08	
Water			7.45215	18.4076	0.703934	3.21159	
Hydrogen Sulfide			0.0215286	8.48825	0.312073	0.0660887	
Carbon Dioxide			1.27446	1346.94	51.3005	4.37797	
Nitrogen			0.93287	6142.43	239.69	2.01282	
Methane			126.605	299577	11586.5	399.866	
Ethane			163.713	98694	3654.16	632.061	
Propane			252.436	74204.6	2513.69	1211.24	
Isobutane			63.245	13694	406.627	456.031	
n-Butane			165.6	32941.7	898.152	1521.54	
Isopentane			50.9199	9661.03	204.434	887.67	
n-Pentane			58.4506	11081.7	211.527	1279.22	
i-C6			45.7636	8966	110.123	2169.81	
i-C7			18.6612	4063.28	25.9636	2386.48	
Octane			5.43716	1225.46	2.82376	2667.63	
Nonane			0.874389	151.26	0.125044	1224.52	
Benzene			2.30013	209.647	2.30186	112.905	
Toluene			1.87123	233.133	1.17281	311.96	
Ethylbenzene			0.0512527	8.12908	0.0183593	25.2738	
o-Xylene			0.460731	65.4087	0.123331	274.284	
n-Hexane			19.0656	3915.53	38.7864	1249.82	
2,2,4-Trimethylpenta	ne		0	0	0	0	
, _, _, _ , _ , moony poind			0				
Decanes Plus			0.0363429	2.21742	0.000503746	279.402	
			· ·	2.21742	0.000503746	279.402	
Decanes Plus			0.0363429				
Decanes Plus			0.0363429				5. Water Tank Flash Gas
Decanes Plus			0.0363429 0 1. LP Separator Gas %	0 2. Sales Gas %	0 3. Fuel Gas %	0 4. NGL Sales Liquid %	
Decanes Plus Decanes Plus Sat			0.0363429 0 1. LP Separator Gas	0 2. Sales Gas	0 3. Fuel Gas	0 4. NGL Sales Liquid	Flash Gas
Decanes Plus Decanes Plus Sat Mole Fraction			0.0363429 0 1. LP Separator Gas %	0 2. Sales Gas %	0 3. Fuel Gas %	0 4. NGL Sales Liquid %	Flash Gas
Decanes Plus Decanes Plus Sat Mole Fraction Triethylene Glycol			0.0363429 0 1. LP Separator Gas % 6.0769E-10	0 2. Sales Gas % 8.52759E-05	0 3. Fuel Gas % 3.11649E-06	0 4. NGL Sales Liquid % 1.17031E-10	Flash Gas
Decanes Plus Decanes Plus Sat Mole Fraction Triethylene Glycol Water Hydrogen Sulfide			0.0363429 0 1. LP Separator Gas % 6.0769E-10 1.58862 0.00242597	0 2. Sales Gas % 8.52759E-05 0.00405662 0.000988813	0 3. Fuel Gas % 3.11649E-06 0.00415324 0.000973289	0 4. NGL Sales Liquid % 1.17031E-10 0.0731522 0.000795728	Flash Gas
Decanes Plus Decanes Plus Sat Mole Fraction Triethylene Glycol Water Hydrogen Sulfide Carbon Dioxide			0.0363429 0 1. LP Separator Gas % 6.0769E-10 1.58862 0.00242597 0.111214	0 2. Sales Gas % 8.52759E-05 0.00405662 0.000988813 0.121509	0 3. Fuel Gas % 3.11649E-06 0.00415324 0.000973289 0.1239	0 4. NGL Sales Liquid % 1.17031E-10 0.0731522 0.000795728 0.0408202	Flash Gas
Decanes Plus Decanes Plus Sat Mole Fraction Triethylene Glycol Water Hydrogen Sulfide Carbon Dioxide Nitrogen			0.0363429 0 1. LP Separator Gas % 6.0769E-10 1.58862 0.00242597 0.111214 0.12789	0 2. Sales Gas % 8.52759E-05 0.00405662 0.000988813 0.121509 0.870525	0 3. Fuel Gas % 3.11649E-06 0.00415324 0.000973289 0.1239 0.909452	0 4. NGL Sales Liquid % 1.17031E-10 0.0731522 0.000795728 0.0408202 0.029484	Flash Gas
Decanes Plus Decanes Plus Sat Mole Fraction Triethylene Glycol Water Hydrogen Sulfide Carbon Dioxide Nitrogen Methane			0.0363429 0 1. LP Separator Gas % 6.0769E-10 1.58862 0.00242597 0.111214 0.12789 30.3082	0 2. Sales Gas % 8.52759E-05 0.00405662 0.000988813 0.121509 0.870525 74.1386	0 3. Fuel Gas % 3.11649E-06 0.00415324 0.000973289 0.1239 0.909452 76.7678	0 4. NGL Sales Liquid % 1.17031E-10 0.0731522 0.000795728 0.0408202 0.029484 10.228	Flash Gas
Decanes Plus Decanes Plus Sat Mole Fraction Triethylene Glycol Water Hydrogen Sulfide Carbon Dioxide Nitrogen Methane Ethane			0.0363429 0 1. LP Separator Gas % 6.0769E-10 1.58862 0.00242597 0.111214 0.12789 30.3082 20.9095	0 2. Sales Gas % 8.52759E-05 0.00405662 0.000988813 0.121509 0.870525 74.1386 13.031	0 3. Fuel Gas % 3.11649E-06 0.00415324 0.000973289 0.1239 0.909452 76.7678 12.9171	0 4. NGL Sales Liquid % 1.17031E-10 0.0731522 0.000795728 0.0408202 0.029484 10.228 8.62557	Flash Gas
Decanes Plus Decanes Plus Sat Mole Fraction Triethylene Glycol Water Hydrogen Sulfide Carbon Dioxide Nitrogen Methane Ethane Propane			0.0363429 0 1. LP Separator Gas % 6.0769E-10 1.58862 0.00242597 0.111214 0.12789 30.3082 20.9095 21.9855	0 2. Sales Gas % 8.52759E-05 0.00405662 0.000988813 0.121509 0.870525 74.1386 13.031 6.68101	0 3. Fuel Gas % 3.11649E-06 0.00415324 0.000973289 0.1239 0.909452 76.7678 12.9171 6.05916	0 4. NGL Sales Liquid % 1.17031E-10 0.0731522 0.000795728 0.0408202 0.029484 10.228 8.62557 11.2715	Flash Gas
Decanes Plus Decanes Plus Sat Mole Fraction Triethylene Glycol Water Hydrogen Sulfide Carbon Dioxide Nitrogen Methane Ethane Propane Isobutane			0.0363429 0 1. LP Separator Gas % 6.0769E-10 1.58862 0.00242597 0.111214 0.12789 30.3082 20.9095 21.9855 4.17893	0 2. Sales Gas % 8.52759E-05 0.00405662 0.000988813 0.121509 0.870525 74.1386 13.031 6.68101 0.935396	0 3. Fuel Gas % 3.11649E-06 0.00415324 0.000973289 0.1239 0.909452 76.7678 12.9171 6.05916 0.743618	0 4. NGL Sales Liquid % 1.17031E-10 0.0731522 0.000795728 0.0408202 0.029484 10.228 8.62557 11.2715 3.21959	Flash Gas
Decanes Plus Decanes Plus Sat Decanes Plus Sat Mole Fraction Triethylene Glycol Water Hydrogen Sulfide Carbon Dioxide Nitrogen Methane Ethane Propane Isobutane n-Butane			0.0363429 0 1. LP Separator Gas % 6.0769E-10 1.58862 0.00242597 0.111214 0.12789 30.3082 20.9095 21.9855 4.17893 10.9421	0 2. Sales Gas % 8.52759E-05 0.00405662 0.000988813 0.121509 0.870525 74.1386 13.031 6.68101 0.935396 2.25015	0 3. Fuel Gas % 3.11649E-06 0.00415324 0.000973289 0.1239 0.909452 76.7678 12.9171 6.05916 0.743618 1.64249	0 4. NGL Sales Liquid % 1.17031E-10 0.0731522 0.000795728 0.0408202 0.029484 10.228 8.62557 11.2715 3.21959 10.7421	Flash Gas
Decanes Plus Decanes Plus Sat Decanes Plus Sat Mole Fraction Triethylene Glycol Water Hydrogen Sulfide Carbon Dioxide Nitrogen Methane Ethane Propane Isobutane n-Butane Isopentane			0.0363429 0 1. LP Separator Gas % 6.0769E-10 1.58862 0.00242597 0.111214 0.12789 30.3082 20.9095 21.9855 4.17893 10.9421 2.71044	0 2. Sales Gas % 8.52759E-05 0.00405662 0.000988813 0.121509 0.870525 74.1386 13.031 6.68101 0.935396 2.25015 0.53162	0 3. Fuel Gas % 3.11649E-06 0.00415324 0.000973289 0.1239 0.909452 76.7678 12.9171 6.05916 0.743618 1.64249 0.301176	0 4. NGL Sales Liquid % 1.17031E-10 0.0731522 0.000795728 0.0408202 0.029484 10.228 8.62557 11.2715 3.21959 10.7421 5.0486	Flash Gas
Decanes Plus Decanes Plus Sat Decanes Plus Sat Mole Fraction Triethylene Glycol Water Hydrogen Sulfide Carbon Dioxide Nitrogen Methane Ethane Propane Isobutane n-Butane Isopentane n-Pentane			0.0363429 0 1. LP Separator Gas % 6.0769E-10 1.58862 0.00242597 0.111214 0.12789 30.3082 20.9095 21.9855 4.17893 10.9421 2.71044 3.11129	0 2. Sales Gas % 8.52759E-05 0.00405662 0.000988813 0.121509 0.870525 74.1386 13.031 6.68101 0.935396 2.25015 0.53162 0.609797	0 3. Fuel Gas % 3.11649E-06 0.00415324 0.000973289 0.1239 0.909452 76.7678 12.9171 6.05916 0.743618 1.64249 0.301176 0.311625	0 4. NGL Sales Liquid % 1.17031E-10 0.0731522 0.000795728 0.0408202 0.029484 10.228 8.62557 11.2715 3.21959 10.7421 5.0486 7.27551	Flash Gas
Decanes Plus Decanes Plus Sat Decanes Plus Sat Mole Fraction Triethylene Glycol Water Hydrogen Sulfide Carbon Dioxide Nitrogen Methane Ethane Propane Isobutane n-Butane Isopentane n-Pentane i-C6			0.0363429 0 1. LP Separator Gas % 6.0769E-10 1.58862 0.00242597 0.111214 0.12789 30.3082 20.9095 21.9855 4.17893 10.9421 2.71044 3.11129 2.03947	0 2. Sales Gas % 8.52759E-05 0.00405662 0.000988813 0.121509 0.870525 74.1386 13.031 6.68101 0.935396 2.25015 0.53162 0.609797 0.413069	0 3. Fuel Gas % 3.11649E-06 0.00415324 0.000973289 0.1239 0.909452 76.7678 12.9171 6.05916 0.743618 1.64249 0.301176 0.311625 0.135828	0 4. NGL Sales Liquid % 1.17031E-10 0.0731522 0.000795728 0.0408202 0.029484 10.228 8.62557 11.2715 3.21959 10.7421 5.0486 7.27551 10.3321	Flash Gas
Decanes Plus Decanes Plus Sat Decanes Plus Sat Mole Fraction Triethylene Glycol Water Hydrogen Sulfide Carbon Dioxide Nitrogen Methane Ethane Propane Isobutane n-Butane Isopentane n-Pentane i-C6 i-C7			0.0363429 0 1. LP Separator Gas % 6.0769E-10 1.58862 0.00242597 0.111214 0.12789 30.3082 20.9095 21.9855 4.17893 10.9421 2.71044 3.11129 2.03947 0.715228	0 2. Sales Gas % 8.52759E-05 0.00405662 0.000988813 0.121509 0.870525 74.1386 13.031 6.68101 0.935396 2.25015 0.53162 0.609797 0.413069 0.160993	0 3. Fuel Gas % 3.11649E-06 0.00415324 0.000973289 0.1239 0.909452 76.7678 12.9171 6.05916 0.743618 1.64249 0.301176 0.311625 0.135828 0.0275413	0 4. NGL Sales Liquid % 1.17031E-10 0.0731522 0.000795728 0.0408202 0.029484 10.228 8.62557 11.2715 3.21959 10.7421 5.0486 7.27551 10.3321 9.77305	Flash Gas
Decanes Plus Decanes Plus Sat Decanes Plus Sat Mole Fraction Triethylene Glycol Water Hydrogen Sulfide Carbon Dioxide Nitrogen Methane Ethane Propane Isobutane n-Butane Isopentane n-Pentane i-C6			0.0363429 0 1. LP Separator Gas % 6.0769E-10 1.58862 0.00242597 0.111214 0.12789 30.3082 20.9095 21.9855 4.17893 10.9421 2.71044 3.11129 2.03947 0.715228 0.182801	0 2. Sales Gas % 8.52759E-05 0.00405662 0.000988813 0.121509 0.870525 74.1386 13.031 6.68101 0.935396 2.25015 0.53162 0.609797 0.413069 0.160993 0.0425924	0 3. Fuel Gas % 3.11649E-06 0.00415324 0.000973289 0.1239 0.909452 76.7678 12.9171 6.05916 0.743618 1.64249 0.301176 0.311625 0.135828	0 4. NGL Sales Liquid % 1.17031E-10 0.0731522 0.000795728 0.0408202 0.029484 10.228 8.62557 11.2715 3.21959 10.7421 5.0486 7.27551 10.3321 9.77305 9.58295	Flash Gas
Decanes Plus Decanes Plus Sat Decanes Plus Sat Mole Fraction Triethylene Glycol Water Hydrogen Sulfide Carbon Dioxide Nitrogen Methane Ethane Propane Isobutane n-Butane Isopentane n-Pentane i-C6 i-C7 Octane			0.0363429 0 1. LP Separator Gas % 6.0769E-10 1.58862 0.00242597 0.111214 0.12789 30.3082 20.9095 21.9855 4.17893 10.9421 2.71044 3.11129 2.03947 0.715228	0 2. Sales Gas % 8.52759E-05 0.00405662 0.000988813 0.121509 0.870525 74.1386 13.031 6.68101 0.935396 2.25015 0.53162 0.609797 0.413069 0.160993	0 3. Fuel Gas % 3.11649E-06 0.00415324 0.000973289 0.1239 0.909452 76.7678 12.9171 6.05916 0.743618 1.64249 0.301176 0.311625 0.135828 0.0275413	0 4. NGL Sales Liquid % 1.17031E-10 0.0731522 0.000795728 0.0408202 0.029484 10.228 8.62557 11.2715 3.21959 10.7421 5.0486 7.27551 10.3321 9.77305	Flash Gas
Decanes Plus Decanes Plus Sat Decanes Plus Sat Mole Fraction Triethylene Glycol Water Hydrogen Sulfide Carbon Dioxide Nitrogen Methane Ethane Propane Isobutane n-Butane Isopentane n-Pentane i-C6 i-C7 Octane Nonane			0.0363429 0 1. LP Separator Gas % 6.0769E-10 1.58862 0.00242597 0.111214 0.12789 30.3082 20.9095 21.9855 4.17893 10.9421 2.71044 3.11129 2.03947 0.715228 0.182801	0 2. Sales Gas % 8.52759E-05 0.00405662 0.000988813 0.121509 0.870525 74.1386 13.031 6.68101 0.935396 2.25015 0.53162 0.609797 0.413069 0.160993 0.0425924	0 3. Fuel Gas % 3.11649E-06 0.00415324 0.000973289 0.1239 0.909452 76.7678 12.9171 6.05916 0.743618 1.64249 0.301176 0.311625 0.135828 0.0275413 0.00262754	0 4. NGL Sales Liquid % 1.17031E-10 0.0731522 0.000795728 0.0408202 0.029484 10.228 8.62557 11.2715 3.21959 10.7421 5.0486 7.27551 10.3321 9.77305 9.58295	Flash Gas
Decanes Plus Decanes Plus Sat Decanes Plus Sat Mole Fraction Triethylene Glycol Water Hydrogen Sulfide Carbon Dioxide Nitrogen Methane Ethane Propane Isobutane n-Butane Isopentane n-Pentane i-C6 i-C7 Octane Nonane Benzene			0.0363429 0 1. LP Separator Gas % 6.0769E-10 1.58862 0.00242597 0.111214 0.12789 30.3082 20.9095 21.9855 4.17893 10.9421 2.71044 3.11129 2.03947 0.715228 0.182801 0.0261825 0.113088	0 2. Sales Gas % 8.52759E-05 0.00405662 0.000988813 0.121509 0.870525 74.1386 13.031 6.68101 0.935396 2.25015 0.53162 0.609797 0.413069 0.160993 0.0425924 0.00468226 0.0106556	0 3. Fuel Gas % 3.11649E-06 0.00415324 0.000973289 0.1239 0.909452 76.7678 12.9171 6.05916 0.743618 1.64249 0.301176 0.311625 0.135828 0.0275413 0.00262754 0.00010363 0.00313226	0 4. NGL Sales Liquid % 1.17031E-10 0.0731522 0.000795728 0.0408202 0.029484 10.228 8.62557 11.2715 3.21959 10.7421 5.0486 7.27551 10.3321 9.77305 9.58295 3.91776 0.593121	Flash Gas
Decanes Plus Decanes Plus Sat Decanes Plus Sat Mole Fraction Triethylene Glycol Water Hydrogen Sulfide Carbon Dioxide Nitrogen Methane Ethane Propane Isobutane n-Butane Isopentane n-Pentane i-C6 i-C7 Octane Nonane Benzene Toluene			0.0363429 0 1. LP Separator Gas % 6.0769E-10 1.58862 0.00242597 0.111214 0.12789 30.3082 20.9095 21.9855 4.17893 10.9421 2.71044 3.11129 2.03947 0.715228 0.182801 0.0261825 0.113088 0.077995	0 2. Sales Gas % 8.52759E-05 0.00405662 0.000988813 0.121509 0.870525 74.1386 13.031 6.68101 0.935396 2.25015 0.53162 0.609797 0.413069 0.160993 0.0425924 0.00468226 0.0106556 0.0100455	0 3. Fuel Gas % 3.11649E-06 0.00415324 0.000973289 0.1239 0.909452 76.7678 12.9171 6.05916 0.743618 1.64249 0.301176 0.311625 0.135828 0.0275413 0.00262754 0.00010363 0.00313226 0.00135296	0 4. NGL Sales Liquid % 1.17031E-10 0.0731522 0.000795728 0.0408202 0.029484 10.228 8.62557 11.2715 3.21959 10.7421 5.0486 7.27551 10.3321 9.77305 9.58295 3.91776 0.593121 1.38933	Flash Gas
Decanes Plus Decanes Plus Sat Decanes Plus Sat Mole Fraction Triethylene Glycol Water Hydrogen Sulfide Carbon Dioxide Nitrogen Methane Ethane Propane Isobutane n-Butane Isopentane i-C6 i-C7 Octane Nonane Benzene Toluene Ethylbenzene			0.0363429 0 0 1. LP Separator Gas % 6.0769E-10 1.58862 0.00242597 0.111214 0.12789 30.3082 20.9095 21.9855 4.17893 10.9421 2.71044 3.11129 2.03947 0.715228 0.182801 0.0261825 0.113088 0.077995 0.00185403	0 2. Sales Gas % 8.52759E-05 0.00405662 0.000988813 0.121509 0.870525 74.1386 13.031 6.68101 0.935396 2.25015 0.53162 0.609797 0.413069 0.160993 0.0425924 0.00468226 0.0106556 0.0100455 0.000303995	0 3. Fuel Gas % 3.11649E-06 0.00415324 0.000973289 0.1239 0.909452 76.7678 12.9171 6.05916 0.743618 1.64249 0.301176 0.311625 0.135828 0.0275413 0.00262754 0.00010363 0.00313226 0.00135296 1.83811E-05	0 4. NGL Sales Liquid % 1.17031E-10 0.0731522 0.000795728 0.0408202 0.029484 10.228 8.62557 11.2715 3.21959 10.7421 5.0486 7.27551 10.3321 9.77305 9.58295 3.91776 0.593121 1.38933 0.097687	Flash Gas
Decanes Plus Decanes Plus Sat Decanes Plus Sat Mole Fraction Triethylene Glycol Water Hydrogen Sulfide Carbon Dioxide Nitrogen Methane Ethane Propane Isobutane n-Butane Isopentane n-Pentane i-C6 i-C7 Octane Nonane Benzene Toluene Ethylbenzene o-Xylene			0.0363429 0 0 1. LP Separator Gas % 6.0769E-10 1.58862 0.00242597 0.111214 0.12789 30.3082 20.9095 21.9855 4.17893 10.9421 2.71044 3.11129 2.03947 0.715228 0.182801 0.0261825 0.113088 0.077995 0.00185403 0.0166666	0 2. Sales Gas % 8.52759E-05 0.00405662 0.000988813 0.121509 0.870525 74.1386 13.031 6.68101 0.935396 2.25015 0.53162 0.609797 0.413069 0.160993 0.0425924 0.00468226 0.0106556 0.0100455 0.000303995 0.00244603	0 3. Fuel Gas % 3.11649E-06 0.00415324 0.000973289 0.1239 0.909452 76.7678 12.9171 6.05916 0.743618 1.64249 0.301176 0.311625 0.135828 0.0275413 0.00262754 0.00010363 0.00313226 0.00135296 1.83811E-05 0.000123477	0 4. NGL Sales Liquid % 1.17031E-10 0.0731522 0.000795728 0.0408202 0.029484 10.228 8.62557 11.2715 3.21959 10.7421 5.0486 7.27551 10.3221 9.77305 9.58295 3.91776 0.593121 1.38933 0.097687 1.06015	Flash Gas
Decanes Plus Decanes Plus Sat Decanes Plus Sat Mole Fraction Triethylene Glycol Water Hydrogen Sulfide Carbon Dioxide Nitrogen Methane Ethane Propane Isobutane n-Butane Isopentane n-Butane Isopentane i-C6 i-C7 Octane Nonane Benzene Toluene Ethylbenzene			0.0363429 0 0 1. LP Separator Gas % 6.0769E-10 1.58862 0.00242597 0.111214 0.12789 30.3082 20.9095 21.9855 4.17893 10.9421 2.71044 3.11129 2.03947 0.715228 0.182801 0.0261825 0.113088 0.077995 0.00185403	0 2. Sales Gas % 8.52759E-05 0.00405662 0.000988813 0.121509 0.870525 74.1386 13.031 6.68101 0.935396 2.25015 0.53162 0.609797 0.413069 0.160993 0.0425924 0.00468226 0.0106556 0.0100455 0.000303995	0 3. Fuel Gas % 3.11649E-06 0.00415324 0.000973289 0.1239 0.909452 76.7678 12.9171 6.05916 0.743618 1.64249 0.301176 0.311625 0.135828 0.0275413 0.00262754 0.00010363 0.00313226 0.00135296 1.83811E-05	0 4. NGL Sales Liquid % 1.17031E-10 0.0731522 0.000795728 0.0408202 0.029484 10.228 8.62557 11.2715 3.21959 10.7421 5.0486 7.27551 10.3321 9.77305 9.58295 3.91776 0.593121 1.38933 0.097687	Flash Gas

* User Specified Values ? Extrapolated or Approximate Values

				reams Report treams by Total Phase			
Client Name: DI	ELAWARE DI	VISION			Job:		
Location: Bu	ulldog Compre	essor Station					
Flowsheet: O	utput						
·							
Mole Fraction			1. LP Separator Gas %	2. Sales Gas %	3. Fuel Gas %	4. NGL Sales Liquid %	5. Water Tank Flash Gas %
Decanes Plus			0.000909861	5.73892E-05	3.49045E-07	0.747399	/0
	ecanes Plus Sat		0.000909861	0	3.49045E-07 0	0.747399	
Jecanes Flus Sat			0	0	0	0	
			4.1.5				-
Mass Fraction		1. LP Separator Gas %	2. Sales Gas %	3. Fuel Gas %	4. NGL Sales Liquid %	5. Water Tank Flash Gas %	
			2.41202E-09	0.00056968	2.20724E-05	2.50474E-10	/0
Friethylene Glycol Nater			0.75643	0.00056968	0.00352874	0.0187819	
lydrogen Sulfide			0.75643	0.003251	0.00352874	0.000386498	
Carbon Dioxide			0.00218526	0.237886	0.257163	0.0256031	
Vitrogen			0.094691	1.08483	1.20154	0.0256031	
lethane			12.851	52.9088	58.082	2.33849	
Ethane			16.6177	17.4305	18.3179	3.6964	
Propane			25.6236	13.1054	12.6008	7.08351	
sobutane			6.41968	2.41852	2.03837	2.66695	
-Butane			16.8092	5.8179	4.50233	8.89825	
sopentane			5.16863	1.70625	1.0248	5.19124	
n-Pentane			5.93303	1.95716	1.06036	7.48107	
·C6			4.64524	1.5835	0.552033	12.6894	
-C7			1.89421	0.717624	0.130152	13.9565	
Octane			0.551899	0.216431	0.0141552	15.6007	
Nonane			0.0887549	0.0267142	0.000626833	7.16117	
Benzene			0.233475	0.0370262	0.011539	0.660285	
Foluene			0.189939	0.041174	0.00587918	1.8244	
Ethylbenzene			0.00520241	0.00143569	9.2033E-05	0.147805	
o-Xylene			0.0467665	0.011552	0.000618245	1.60406	
n-Hexane			1.93525	0.691528	0.194432	7.30913	
2,2,4-Trimethylpentane			0	0	0	0	
Decanes Plus			0.00368899	0.000391623	2.52522E-06	1.63399	
Decanes Plus Sat			0	0	0	0	
			Stream	Properties			
Property		Units	1. LP Separator Gas	2. Sales Gas	3. Fuel Gas	4. NGL Sales Liquid	5. Water Tank Flash Gas
Femperature		°F	75.7	93.2634	76.5751	94.2513	
ressure		psig	15	1272	120	400	0.25
Iolecular Weight		lb/lbmo1	37.8349	22.4795	21.2035	70.1663	
lass Flow		lb/h	985.173	566214	19948.6	17099.4	0
Std Vapor Volumetric F		MMSCFD	0.237151	229.402	8.56858	2.21951	0
Std Liquid Volumetric F	low	sgpm	4.19696	3145.36	114.762	55.3492	0
API Gravity						90.3641	
Gross Ideal Gas Heatin		Btu/ft^3	2154.4	1338.01	1269.3	3872.94	

		reams Report			
		t reams by Total Phase			
Client Name: DELAWARE DI			Job:		
Location: Bulldog Compre			JUD.		
Flowsheet: Output					
	Conn	ections			
	6. Skim Tank Flash Gas	7. Condensate Tank Flash Gas	8. Skim Tank W&B	9. Water Tank W&B	10. Condensate Tank W&B
From Block	Tankage -	Tankage -	W & B -	W & B - Water	W & B -
	Gunbarrel Flash Gas	Condensate Tank Flash	Gunbarrel Tank	Tank	Condensate Tank
To Block		Gas			
TO DIOCK					
	Stream C	omposition			
	6. Skim Tank	7. Condensate	8. Skim Tank	9. Water Tank	10.
	Flash Gas	Tank Flash Gas	W&B	W&B	Condensate Tank W&B
Mass Flow	lb/h	Ib/h	lb/h	Ib/h	lb/h
Triethylene Glycol Water	1.05113E-10 0.0344037	9.89993E-09 0.685708	3.35172E-10 0.128969	3.50942E-10 0.128727	5.18578E-13 1.48305E-05
Vvater Hydrogen Sulfide	0.0344037 8.67221E-05	0.00376113	0.128969	0.128727	0.000156105
Carbon Dioxide	0.004085	0.101373	0.00808979	0.00583444	0.00415695
Nitrogen	0.000266502	0.00858354	1.25307E-05	9.23318E-06	2.02214E-05
Methane	0.0797425	4.02196	0.00905685	0.00566605	0.045702
Ethane	0.251762	24.3092	0.0896923	0.0265713	1.51883
Propane	0.678089	73.0639	0.673562	0.0503116	4.81968
Isobutane n-Butane	0.22913	23.5242 65.6254	0.572777 2.39439	0.0118203 0.0442942	1.62503 4.82784
Isopentane	0.225636	21.8774	0.858766	0.0107872	1.65793
n-Pentane	0.264221	25.4475	1.0121	0.00503188	1.93243
i-C6	0.215024	20.4322	0.834406	0.00561285	1.64047
i-C7	0.0886189	8.37174	0.34338	0.00158052	0.660169
Octane	0.0256788	2.42189	0.0981846	0.000103378	0.170885
Nonane Benzene	0.00414491 0.0106819	0.39021 1.02405	0.0156978 0.041327	1.70199E-05 0.0409704	0.0241421 0.0530051
Toluene	0.00881074	0.835936	0.0339768	0.0338291	0.0446708
Ethylbenzene	0.000241112	0.0228023	0.000920905	0.000917679	0.00124543
o-Xylene	0.00216757	0.204988	0.00827137	0.00826299	0.00960647
n-Hexane	0.0902174	8.54749	0.349857	0.00116802	0.714413
2,2,4-Trimethylpentane	0	0	0	0	0
Decanes Plus Decanes Plus Sat	0.000168879	0.0159356	0.00062722	0.000139556	0.000862324
	6. Skim Tank Flash Gas	7. Condensate Tank Flash	8. Skim Tank W&B	9. Water Tank W&B	10. Condensate
Mole Fraction	%	Gas %	%	%	Tank W&B %
Triethylene Glycol	1.21388E-09	1.21739E-09	1.825E-09	1.95962E-08	9.5811E-13
Water	3.3119	0.70289	5.8537	59.9177	0.000228406
Hydrogen Sulfide	0.00441298	0.00203796	0.00787378	0.083641	0.00127086
Carbon Dioxide	0.160975	0.0425368	0.150306	1.11168	0.0262073
Nitrogen Methane	0.0164986 8.62049	0.00565835 4.62974	0.000365759 0.461629	0.00276384 2.96167	0.000200281 0.79042
Ethane	14.5206	14.9293	2.43906	7.41005	14.0147
Propane	26.6688	30.5982	12.4902	9.56755	30.3261
Isobutane	6.83681	7.47414	8.05807	1.70535	7.75734
n-Butane	19.5179	20.8506	33.6853	6.39047	23.0465
Isopentane	5.42366	5.59959	9.73269	1.25374	6.37576
n-Pentane i-C6	<u> </u>	6.51335 4.37845	11.4705 7.91737	0.584829 0.54617	7.43136 5.28175
i-C7	4.32729	1.54287	2.80211	0.132267	1.82798
Octane	0.389864	0.391533	0.702839	0.00758893	0.41507
Nonane	0.0560471	0.056184	0.100081	0.00111278	0.052227
Benzene	0.007404	0.0404	0.432618	4 00 007	0 400070
Toluene	0.237161 0.165838	0.2421 0.167541	0.301528	4.39827 3.07877	0.188276 0.134517

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			All S	reams Report treams by Total Phase			
Client Name: D	ELAWARE DI	VISION			Job:		
	ulldog Compre						
	utput						
			6. Skim Tank Flash Gas	7. Condensate Tank Flash Gas	8. Skim Tank W&B	9. Water Tank W&B	10. Condensate Tank W&B
Mole Fraction			%	%	%	%	%
Ethylbenzene			0.00393867	0.0039663	0.00709285	0.0724832	0.00325484
o-Xylene			0.0354082	0.0356564	0.0637064	0.652655	0.0251059
n-Hexane			1.8156	1.83166	3.31967	0.113657	2.30017
2,2,4-Trimethylpentane	•		0	0	0	0	0
Decanes Plus			0.00190925	0.00191837	0.00334335	0.00762869	0.00155969
Decanes Plus Sat			0	0	0	0	0
			6. Skim Tank Flash Gas	7. Condensate Tank Flash Gas	8. Skim Tank W&B	9. Water Tank W&B	10. Condensate Tank W&B
Mass Fraction			%	%	%	%	%
Triethylene Glycol			3.66591E-09	3.52391E-09	4.48427E-09	9.1871E-08	2.62554E-12
Water			1.19986	0.24408	1.72547	33.6986	7.50861E-05
Hydrogen Sulfide			0.00302452	0.00133878	0.00439067	0.0889909	0.000790354
Carbon Dioxide			0.142468	0.036084	0.108233	1.52736	0.0210465
Nitrogen			0.00929453	0.00305533	0.000167648	0.0024171	0.00010238
Methane			2.7811	1.43163	0.121172	1.48328	0.231388
Ethane			8.78044	8.65291	1.19999	6.95594	7.68981
Propane			23.649	26.0073	9.01159	13.1708	24.4019
Isobutane			7.99114	8.37349	7.6632	3.09437	8.22747
n-Butane			22.8133	23.3595	32.0346	11.5955	24.4432
Isopentane			7.86928	7.78734	11.4894	2.82392	8.39407
n-Pentane			9.21497	9.05809	13.5409	1.31727	9.78383
i-C6			7.49916	7.27289	11.1635	1.46935	8.30562
i-C0			3.09067	2.97994	4.59408	0.413756	3.34241
Octane			0.895573	0.862078	1.31361	0.0270627	0.865182
Nonane			0.144558	0.138896	0.210021	0.0270627	0.122231
				0.364514		10.7254	0.122231
Benzene Toluene			0.37254 0.307283	0.364514	0.552915 0.454575	8.85591	0.200303
Ethylbenzene			0.00840901	0.00811653 0.0729662	0.0123208 0.110663	0.240234 2.16312	0.00630555 0.0486372
o-Xylene			0.0755961	3.0425	4.68074	0.305769	
n-Hexane			3.14642	3.0425	4.68074	0.305769	3.61705 0
2,2,4-Trimethylpentane			-	-	-	-	-
Decanes Plus			0.00588982	0.00567233	0.00839158	0.0365334	0.00436592
Decanes Plus Sat			0	0	0	0	0
				Properties			
Property		Units	6. Skim Tank Flash Gas	7. Condensate Tank Flash Gas	8. Skim Tank W&B	9. Water Tank W&B	10. Condensate Tank W&B
Temperature		°F	75.67	75.67	82.0362	82.6855	78.6044
Pressure		psig	0.5	0.25	-3.9673	-11.8056	0.0439129
Molecular Weight		lb/lbmol	49.7263	51.8796	61.1171	32.032	54.801
Mass Flow		lb/h	2.8673	280.936	7.4744	0.381994	19.7513
Std Vapor Volumetric F		MMSCFD	0.00052516	0.0493191	0.00111383	0.000108612	0.00328255
Std Liquid Volumetric F			0.0106263	1.0366	0.024787	0.000108612	0.00328255
API Gravity		sgpm					
Gross Ideal Gas Heatin	ng Value	Btu/ft^3	2769.57	2915.86	3346.32	1149.83	3080.19

Remarks

Client Name: DELAWARE DIVISI Location: Bulldog Compresson Flowsheet: Output	Tabulated k				
			Job:		
	Station				
	Conn	ections			
	11.	12. Produced	13. BTEX	14. Skim Tank	15. HPF Pilot /
	Condensate Sales Liquid	Water Liquid	Cond Vapors to Combustion	Inlet	Purge Gas
From Block	Tankage - Condensate Sales Liquid	Tankage - Produced Water Sales Liquid	Tankage - BTEX Vapors to Combustion	Tankage - Gunbarrel Tank Inlet	SPLT-100
To Block					
	·				
	Stream C	omposition			
	11. Condensate Sales Liquid	12. Produced Water Liquid	13. BTEX Cond Vapors to Combustion	14. Skim Tank Inlet	15. HPF Pilot / Purge Gas
Mass Flow	lb/h	lb/h	lb/h	lb/h	lb/h
Triethylene Glycol	6.33307E-05	1.07682 4975	3.11343E-08	1.07682 4975.04	3.08322E-05
Water Hydrogen Sulfide	0.170596	0.000559356	1.46396 0.119759	0.000680464	0.00492918 0.00218524
Carbon Dioxide	0.0208007	0.00862534	1.86983	0.0132616	0.359223
Nitrogen	0.00017029	1.36499E-05	0.01261	0.000283619	1.67839
Methane	0.29209	0.00837641	7.43021	0.0919205	81.1328
Ethane	11.4203	0.0392817	17.3237	0.36877	25.5877
Propane Isobutane	122.333 98.6614	0.0743783 0.0174746	30.0862 5.29049	1.49888 0.87855	17.6017 2.84734
n-Butane	407.601	0.0654824	21.4663	3.3908	6.28916
Isopentane	335.495	0.0159473	8.37887	2.51756	1.43152
n-Pentane	518.971	0.00743889	11.5326	3.81717	1.48118
i-C6	1039	0.00829776	7.95601	7.41869	0.771116
i-C7 Octane	<u> </u>	0.00233657 0.000152829	2.33582 0.242183	9.48463 12.8911	0.181805 0.0197729
Nonane	976.464	2.51614E-05	0.0121609	6.83122	0.000875601
Benzene	75.3806	0.149919	5.88284	0.679596	0.0161184
Toluene	214.168	0.0925825	2.92114	1.59148	0.00821242
Ethylbenzene	18.3062	0.00225858	0.0270334	0.130307	0.000128558
o-Xylene	203.647	0.0301824	0.282454	1.454	0.000863606 0.271595
n-Hexane 2,2,4-Trimethylpentane	632.092	0.00172674	3.23896	4.48253	0.271595
Decanes Plus	263.639	0.000206312	0.000157435	1.84393	3.52739E-06
Decanes Plus Sat	0	0	0	0	0
	11. Condensate Sales Liquid	12. Produced Water Liquid	13. BTEX Cond Vapors to Combustion	14. Skim Tank Inlet	15. HPF Pilot / Purge Gas
Mole Fraction	%	%	%	%	%
Triethylene Glycol	4.82495E-07	0.00259642	7.27194E-09	0.00259024	3.11649E-06
Water	0.0108342	99.9942	2.8503	99.7571	0.00415324
Hydrogen Sulfide	7.60547E-05	5.94292E-06	0.123254	7.21244E-06	0.000973289
Carbon Dioxide	0.000540756	7.09664E-05	1.49025	0.000108853	0.1239 0.909452
Nitrogen Methane	6.95492E-06 0.0208313	1.76435E-07 0.000189064	0.0157889 16.2455	3.65727E-06 0.0020698	0.909452
Ethane	0.434539	0.000473035	20.2081	0.0020098	12.9171
Propane	3.17407	0.000610764	23.9318	0.0122789	6.05916
Isobutane	1.94212	0.000108865	3.19269	0.00546025	0.743618
n-Butane	8.02349	0.000407948	12.9544	0.021074	1.64249
Isopentane	5.32019	8.0035E-05	4.07342 5.60661	0.0126049 0.0191118	0.301176 0.311625
n-Pentane i-C6	<u>8.2297</u> 13.7944	3.73337E-05 3.48659E-05	3.23829	0.0191118	0.311625
i-C7	15.3858	8.44354E-06	0.817649	0.0341926	0.0275413
Octane	18.4389	4.84455E-07	0.0743657	0.0407663	0.00262754

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			All S	reams Report treams by Total Phase			
	ELAWARE DI				Job:		
	ulldog Compre	ssor Station					
Flowsheet: C	utput						
			44	40. Dae dues d		44 Chim Taula	
			11. Condensate Sales Liquid	12. Produced Water Liquid	13. BTEX Cond Vapors to Combustion	14. Skim Tank Inlet	15. HPF Pilot / Purge Gas
Mole Fraction			%	%	%	%	%
Nonane			8.71067	7.10367E-08	0.00332577	0.0192403	0.00010363
Benzene			1.10411	0.000694964	2.64164	0.00314284	0.00313226
Toluene			2.6594	0.00036384	1.11203	0.00623948	0.00135296
Ethylbenzene			0.197281 2.19465	7.70328E-06 0.000102942	0.00893145	0.000443378	1.83811E-05 0.000123477
o-Xylene n-Hexane			8.39203	7.25549E-06	0.093319 1.31833	0.00494735	0.000123477
2,2,4-Trimethylpentane	1		0.39203	1.25549E-08	1.31633	0.0187901	0.0476401
Decanes Plus			1.96632	4.86992E-07	3.5998E-05	0.00434218	3.49045E-07
Decanes Plus Sat			0	0	0	0	0
			11. Condensate Sales Liquid	12. Produced Water Liquid	13. BTEX Cond Vapors to	14. Skim Tank Inlet	15. HPF Pilot / Purge Gas
Mass Fraction			%	%	Combustion %	%	%
Triethylene Glycol			7.81272E-07	0.0216377	2.43478E-08	0.0213846	2.20724E-05
Water			0.00210454	99.9678	1.14485	98.7993	0.00352874
Hydrogen Sulfide			2.79483E-05	1.12397E-05	0.0936543	1.35133E-05	0.00156439
Carbon Dioxide			0.000256606	0.000173318	1.46225	0.000263363	0.257163
Nitrogen			2.10076E-06	2.74281E-07	0.00986132	5.63239E-06	1.20154
Methane Ethane			0.00360334	0.000168316 0.000789328	5.8106 13.5476	0.00182545 0.0073234	58.082 18.3179
Propane			1.50914	0.00149456	23.5281	0.0297662	12.6008
Isobutane			1.21713	0.000351134	4.13729	0.0174471	2.03837
n-Butane			5.02833	0.00131581	16.7872	0.0673378	4.50233
Isopentane			4.1388	0.000320445	6.55248	0.0499962	1.0248
n-Pentane			6.40223	0.000149477	9.01875	0.0758052	1.06036
i-C6			12.8175	0.000166736	6.2218	0.147328	0.552033
i-C7			16.6232	4.6951E-05	1.82667	0.188355	0.130152
Octane			22.7106	3.07095E-06	0.189393	0.256003	0.0141552
Nonane Benzene			0.929925	5.05594E-07 0.00301248	0.00951008 4.60052	0.135661 0.0134961	0.000626833
Toluene			2.64206	0.00301248	2.2844	0.0134961	0.00587918
Ethylbenzene			0.225832	4.53839E-05	0.0211408	0.00258776	9.2033E-05
o-Xylene			2.51226	0.000606485	0.220886	0.0288751	0.000618245
n-Hexane			7.79773	3.46972E-05	2.53294	0.0890185	0.194432
2,2,4-Trimethylpentane	•		0	0	0	0	0
Decanes Plus			3.25235	4.14564E-06	0.000123118	0.0366186	2.52522E-06
Decanes Plus Sat			0	0	0	0	0
			Stream	Properties			
Property		Units	11.	12. Produced	13. BTEX	14. Skim Tank	15. HPF Pilot /
ropeny		Units	Condensate Sales Liquid	Water Liquid	Cond Vapors to Combustion	Inlet	Purge Gas
Temperature		°F	75.67	75.8095	70	75.7	76.5751
Pressure		psig	0.25	0.25	0	15	120
Molecular Weight		lb/lbmol	92.7432	18.02	44.8521	18.1899	21.2035
Mass Flow		lb/h	8106.1	4976.6	127.873	5035.5	139.687
Std Vapor Volumetric F	low	MMSCFD	0.79604	2.51525	0.0259658	2.52125	0.06
Std Liquid Volumetric F		sgpm	23.7476	9.94891	0.49092	10.1234	0.8036
API Gravity			73.9665	9.99586		10.7657	
Gross Ideal Gas Heatin		Btu/ft^3	5054.3	50.5119	2460.05	61.9959	1269.3

Remarks

		Process Streams Report All Streams Tabulated by Total Phase		
Client Name:	DELAWARE DI	/ISION	Job:	
Location:	Bulldog Compre	ssor Station		
Flowsheet:	Output			

			All St	reams Report reams by Total Phase			
Client Name:	DELAWARE DI	VISION			Job:		
Location:	Bulldog Compre						
Flowsheet:	Output						
			Conn	ections			
			16. LPF Pilot /	17. HPF	18. Fuel Gas	19. inlet	20. Fuel Gas
			Purge Gas	Blowdowns	Other	Flaring	Other
From Block			SPLT-100	SPLT-100	SPLT-100	SPLT-101	SPLT-101
To Block							
			Stream C	omposition			
			16. LPF Pilot /	17. HPF	18. Fuel Gas	19. Inlet	20. Fuel Gas
			Purge Gas	Blowdowns	Other	Flaring	Other
Mass Flow			lb/h	lb/h	lb/h	lb/h	lb/h
Triethylene Glycol			1.61869E-05	1.17356E-05	0.00653115	0.984264	2.24134
Water			0.00258782	0.00187618	1.04414	5.61692	12.7907
Hydrogen Sulfide			0.00114725	0.000831763	0.462897	2.59011	5.89814
Carbon Dioxide			0.188592	0.13673	76.0938	411.007	935.936
Nitrogen			0.881154	0.638841	355.531	1874.31	4268.12
Methane			42.5947	30.8814	17186.3	91413.2	208164
Ethane			13.4335	9.73938	5420.2	30115.6	68578.4
Propane			9.24089	6.6997	3728.54	22642.9	51561.8
Isobutane			1.49485	1.08378	603.147	4178.6	9515.41
n-Butane			3.30181	2.39383	1332.22	10051.9	22889.9
Isopentane			0.751546	0.544875	303.236	2947.97	6713.05
n-Pentane			0.777619	0.563778	313.756	3381.48	7700.23
i-C6			0.404836	0.293508	163.345	2735.89	6230.11
i-C7 Octane			0.0954478	0.0692002	<u>38.5116</u> 4.18846	1239.87 373.938	2823.41 851.523
Nonane			0.000459691	0.000333278	0.185478	46.1555	105.104
Benzene			0.00846215	0.00613511	3.41434	63.972	145.675
Toluene			0.00431152	0.00312588	1.73963	71.1383	161.994
Ethylbenzene			6.74929E-05	4.89327E-05	0.0272322	2.48051	5.64856
o-Xylene			0.000453393	0.000328713	0.182937	19.9589	45.4499
n-Hexane			0.142587	0.103377	57.5316	1194.79	2720.74
2,2,4-Trimethylpen	itane		0	0	0	0	0
Decanes Plus			1.85188E-06	1.34262E-06	0.000747203	0.676627	1.5408
Decanes Plus Sat			0	0	0	0	0
			16. LPF Pilot /	17. HPF	18. Fuel Gas	19. Inlet	20. Fuel Gas
			Purge Gas	Blowdowns	Other	Flaring	Other
Mole Fraction			%	%	%	%	%
Triethylene Glycol			3.11649E-06	3.11649E-06	3.11649E-06	8.52759E-05	8.52759E-05
Water			0.00415324	0.00415324	0.00415324	0.00405662	0.00405662
Hydrogen Sulfide Carbon Dioxide			0.000973289 0.1239	0.000973289 0.1239	0.000973289 0.1239	0.000988813 0.121509	0.000988813 0.121509
Nitrogen			0.1239	0.1239	0.1239	0.121509	0.121509
Methane			76.7678	76.7678	76.7678	74.1386	74.1386
Ethane			12.9171	12.9171	12.9171	13.031	13.031
Propane			6.05916	6.05916	6.05916	6.68101	6.68101
Isobutane			0.743618	0.743618	0.743618	0.935396	0.935396
n-Butane			1.64249	1.64249	1.64249	2.25015	2.25015
Isopentane			0.301176	0.301176	0.301176	0.53162	0.53162
n-Pentane			0.311625	0.311625	0.311625	0.609797	0.609797
i-C6			0.135828	0.135828	0.135828	0.413069	0.413069
			0.0075440	0.0275413	0.0275413	0.160993	0.160993
i-C7			0.0275413				
i-C7 Octane			0.00262754	0.00262754	0.00262754	0.0425924	0.0425924
i-C7 Octane Nonane			0.00262754 0.00010363	0.00262754 0.00010363	0.00010363	0.00468226	0.00468226
i-C7 Octane Nonane Benzene			0.00262754 0.00010363 0.00313226	0.00262754 0.00010363 0.00313226	0.00010363 0.00313226	0.00468226 0.0106556	0.00468226 0.0106556
i-C7 Octane Nonane Benzene Toluene			0.00262754 0.00010363 0.00313226 0.00135296	0.00262754 0.00010363 0.00313226 0.00135296	0.00010363 0.00313226 0.00135296	0.00468226 0.0106556 0.0100455	0.00468226 0.0106556 0.0100455
i-C7 Octane Nonane Benzene Toluene Ethylbenzene			0.00262754 0.00010363 0.00313226 0.00135296 1.83811E-05	0.00262754 0.00010363 0.00313226 0.00135296 1.83811E-05	0.00010363 0.00313226 0.00135296 1.83811E-05	0.00468226 0.0106556 0.0100455 0.000303995	0.00468226 0.0106556 0.0100455 0.000303995
i-C7 Octane Nonane Benzene Toluene Ethylbenzene o-Xylene			0.00262754 0.00010363 0.00313226 0.00135296 1.83811E-05 0.000123477	0.00262754 0.00010363 0.00313226 0.00135296 1.83811E-05 0.000123477	0.00010363 0.00313226 0.00135296 1.83811E-05 0.000123477	0.00468226 0.0106556 0.0100455 0.000303995 0.00244603	0.00468226 0.0106556 0.0100455 0.000303995 0.00244603
i-C7 Octane Nonane Benzene Toluene Ethylbenzene o-Xylene n-Hexane			0.00262754 0.00010363 0.00313226 0.00135296 1.83811E-05 0.000123477 0.0478401	0.00262754 0.00010363 0.00313226 0.00135296 1.83811E-05 0.000123477 0.0478401	0.00010363 0.00313226 0.00135296 1.83811E-05 0.000123477 0.0478401	0.00468226 0.0106556 0.0100455 0.000303995 0.00244603 0.180391	0.00468226 0.0106556 0.0100455 0.000303995 0.00244603 0.180391
i-C7 Octane Nonane Benzene Toluene Ethylbenzene o-Xylene n-Hexane 2,2,4-Trimethylpen	itane		0.00262754 0.00010363 0.00313226 0.00135296 1.83811E-05 0.000123477 0.0478401 0	0.00262754 0.00010363 0.00313226 0.00135296 1.83811E-05 0.000123477 0.0478401 0	0.00010363 0.00313226 0.00135296 1.83811E-05 0.000123477 0.0478401 0	0.00468226 0.0106556 0.0100455 0.000303995 0.00244603 0.180391 0	0.00468226 0.0106556 0.0100455 0.000303995 0.00244603 0.180391 0
i-C7 Octane Nonane Benzene Toluene Ethylbenzene o-Xylene n-Hexane	tane		0.00262754 0.00010363 0.00313226 0.00135296 1.83811E-05 0.000123477 0.0478401	0.00262754 0.00010363 0.00313226 0.00135296 1.83811E-05 0.000123477 0.0478401	0.00010363 0.00313226 0.00135296 1.83811E-05 0.000123477 0.0478401	0.00468226 0.0106556 0.0100455 0.000303995 0.00244603 0.180391	0.00468226 0.0106556 0.0100455 0.000303995 0.00244603 0.180391

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				reams Report treams by Total Phase			
Client Name:	DELAWARE DIV	ISION			Job:	1	
Location:	Bulldog Compres	sor Station					
Flowsheet:	Output						
Mass Fraction			16. LPF Pilot / Purge Gas %	17. HPF Blowdowns %	18. Fuel Gas Other %	19. Inlet Flaring %	20. Fuel Gas Other %
Triethylene Glycol			2.20724E-05	2.20724E-05	2.20724E-05	0.00056968	0.00056968
Water			0.00352874	0.00352874	0.00352874	0.003251	0.003251
Hydrogen Sulfide			0.00156439	0.00156439	0.00156439	0.00149912	0.00149912
Carbon Dioxide			0.257163	0.257163	0.257163	0.237886	0.237886
Nitrogen			1.20154	1.20154	1.20154	1.08483	1.08483
Methane			58.082	58.082	58.082	52.9088	52.9088
Ethane			18.3179	18.3179	18.3179	17.4305	17.4305
Propane			12.6008	12.6008	12.6008	13.1054	13.1054
Isobutane			2.03837	2.03837	2.03837	2.41852	2.41852
n-Butane			4.50233	4.50233	4.50233	5.8179	5.8179
Isopentane			1.0248	1.0248	1.0248	1.70625	1.70625
n-Pentane			1.06036	1.06036	1.06036	1.95716	1.95716
i-C6			0.552033	0.552033	0.552033	1.5835	1.5835
i-C7			0.130152	0.130152	0.130152	0.717624	0.717624
Octane			0.0141552	0.0141552	0.0141552	0.216431	0.216431
Nonane			0.000626833	0.000626833	0.000626833	0.0267142	0.0267142
Benzene			0.011539	0.011539	0.011539	0.0370262	0.0370262
Toluene			0.00587918	0.00587918	0.00587918	0.041174	0.041174
Ethylbenzene			9.2033E-05	9.2033E-05	9.2033E-05	0.00143569	0.00143569
o-Xylene			0.000618245	0.000618245	0.000618245	0.011552	0.011552
n-Hexane			0.194432	0.194432	0.194432	0.691528	0.691528
2,2,4-Trimethylpent	tane		0	0	0	0	0
Decanes Plus			2.52522E-06	2.52522E-06	2.52522E-06	0.000391623	0.000391623
Decanes Plus Sat			0	0	0	0	0
			Stroom	Properties			
Property		Units	16. LPF Pilot /	17. HPF	18. Fuel Gas	19. Inlet	20. Fuel Gas

Property	Units	16. LPF Pilot / Purge Gas	17. HPF Blowdowns	18. Fuel Gas Other	19. Inlet Flaring	20. Fuel Gas Other
Temperature	°F	76.5751	76.5751	76.5751	93.2634	93.2634
Pressure	psig	120	120	120	1272	1272
Molecular Weight	lb/lbmo1	21.2035	21.2035	21.2035	22.4795	22.4795
Mass Flow	lb/h	73.3355	53.1686	29589.6	172775	393439
Std Vapor Volumetric Flow	MMSCFD	0.0315 *	0.0228377 *	12.7097	70 *	159.402
Std Liquid Volumetric Flow	sgpm	0.42189	0.305873	170.226	959.779	2185.59
API Gravity						
Gross Ideal Gas Heating Value	Btu/ft^3	1269.3	1269.3	1269.3	1338.01	1338.01

Remarks

				reams Report treams by Total Phase			
Client Name:	DELAWARE DI				Job:		
Location:	Bulldog Compre	ssor Station					
Flowsheet:	Output						
			Comm	a ati a ma			
				ections			
			21. Inlet Gas	22. Condensate Flash Losses Hrly	23. HPS Water to SWD	24. VC1 Pilot Fuel	
From Block			Inlet - Inlet Gas	W & B - Cond Flashing Losses Hrly	Inlet - HPS water	SPLT-100	
To Block							
			Stream C	omposition			
Mass Flow			21. Inlet Gas Ib/h	22. Condensate Flash Losses Hrly Ib/h	23. HPS Water to SWD Ib/h	24. VC1 Pilot Fuel Ib/h	
Triethylene Glycol			0	1.05542E-11	6.32885E-05	1.47995E-05	
Water			0	0.000371915	1350.9	0.00236601	
Hydrogen Sulfide			8.98948	0.00504789	0.000733058	0.00104892	
Carbon Dioxide			1404.61	0.114158	0.0419495	0.172427	
Nitrogen			6384.15	0.000752227	0.00410197	0.805626	
Methane			311574	1.26894	0.513033	38.9438	
Ethane			103011	42.3671	0.199228	12.2821	
Propane Isobutane			77974.6 14549	144.696 48.413	0.0815392 0.00802087	8.44881 1.36672	
n-Butane			35306.9	152.628	0.0276614	3.0188	
Isopentane			10676.2	50.5162	0.00443203	0.687127	
n-Pentane			12446	60.1251	0.00235678	0.710966	
i-C6			10956	24.3019	0.00211499	0.370136	
i-C7			6078.94	26.5986	0.000458523	0.0872666	
Octane			3344.42	4.91654	3.44751E-05	0.00949098	
Nonane			1082.55	0.543479	3.89191E-06	0.000420289	
Benzene Toluene			309.052 486.065	1.83996 1.52189	0.027322	0.00773682 0.00394196	
Ethylbenzene			28.003	0.044416	0.00040446	6.17077E-05	
o-Xylene			280.03	0.300355	0.00538719	0.000414531	
n-Hexane			5023.42	17.2603	0.000445207	0.130366	
2,2,4-Trimethylpenta	ane		0	1.06002	0	0	
Decanes Plus			202.311	0.000358566	3.05808E-05	1.69315E-06	
Decanes Plus Sat			0	0	0	0	
			21. Inlet Gas	22. Condensate Flash Losses Hrly	23. HPS Water to SWD	24. VC1 Pilot Fuel	
Mole Fraction			%	%	%	%	
Triethylene Glycol			0	6.62247E-13	5.61696E-07	3.11649E-06	
Water			0	0.000194532	99.9428	0.00415324	
Hydrogen Sulfide			0.00100096	0.00139568	2.86679E-05	0.000973289	
Carbon Dioxide Nitrogen			0.121116 0.86483	0.0244426 0.000253029	0.00127042	0.1239 0.909452	
Methane			73.7028	0.745348	0.0426229	76.7678	
Ethane			13.0005	13.2769	0.00883077	12.9171	
Propane			6.71044	30.9207	0.00246456	6.05916	
Isobutane			0.949912	7.84887	0.000183928	0.743618	
n-Butane			2.30521	24.7445	0.000634307	1.64249	
Isopentane			0.561539	6.59765	8.18732E-05	0.301176	
n-Pentane			0.654628	7.85262	4.3537E-05	0.311625	
i-C6			0.482463	2.65732	3.27109E-05	0.135828	
i-C7 Octane			0.230221 0.111107	2.50133 0.405576	6.09893E-06 4.02253E-07	0.0275413 0.00262754	
Nonane			0.0320307	0.405576	4.04442E-08	0.00010363	
			1	0.0399297	7.07772L-00	0.00010303	I

				reams Report treams by Total Phase			
Client Name: D	ELAWARE DI	VISION			Job:		
	ulldog Compre	ssor Station					
Flowsheet: O	utput						
	•						
			21. Inlet Gas	22. Condensate Flash Losses	23. HPS Water to SWD	24. VC1 Pilot Fuel	
Mala Frantian			0/	Hrly	0/	0/	
Mole Fraction			%	%	%	%	
Benzene Toluene			0.0150144 0.0200192	0.221963 0.155643	0.000466191 0.000258392	0.00313226 0.00135296	
Ethylbenzene			0.0200192	0.00394226	5.07764E-06	1.83811E-05	
o-Xylene			0.0100096	0.0266588	6.76316E-05	0.000123477	
n-Hexane			0.221212	1.88736	6.88568E-06	0.0478401	
2,2,4-Trimethylpentane			0.221212	0.0874435	0.000001-00	0.0470401	
Decanes Plus			0.0050048	2.20258E-05	2.657E-07	3.49045E-07	
Decanes Plus Sat			0.0000040	0	0	0	
Deciance i lue dal			0	0	0	0	
			21. Inlet Gas	22.	23. HPS	24. VC1 Pilot	
			21. Inlet Gas	Condensate Flash Losses Hrly	Water to SWD	Fuel	
Mass Fraction			%	%	%	%	
Triethylene Glycol			0	1.82433E-12	4.68165E-06	2.20724E-05	
Water			0	6.42871E-05	99.9307	0.00352874	
Hydrogen Sulfide			0.00149544	0.00087255	5.42267E-05	0.00156439	
Carbon Dioxide			0.233663	0.0197327	0.00310314	0.257163	
Nitrogen			1.06203	0.000130026	0.000303436	1.20154	
Methane			51.8317	0.219342	0.0379507	58.082	
Ethane			17.1364	7.32333	0.0147375	18.3179	
Propane			12.9714	25.0113	0.00603172	12.6008	
Isobutane			2.42028	8.36839	0.00059333	2.03837	
n-Butane			5.87345	26.3823	0.0020462	4.50233	
Isopentane			1.77603	8.73194	0.000327851	1.0248	
n-Pentane			2.07045	10.3929	0.000174339	1.06036	
i-C6			1.82259	4.20068	0.000156452	0.552033	
i-C7			1.01126	4.59769	3.39184E-05	0.130152	
Octane			0.556359	0.849845	2.55023E-06	0.0141552	
Nonane			0.180087	0.0939427	2.87897E-07	0.000626833	
Benzene			0.0514122	0.318045	0.0020211	0.011539	
Toluene			0.080859	0.263065	0.00132138	0.00587918	
Ethylbenzene			0.00465842	0.00767749	2.99192E-05	9.2033E-05	
o-Xylene n-Hexane			0.0465842	0.0519176 2.98352	0.000398508 3.29334E-05	0.000618245 0.194432	
2,2,4-Trimethylpentane			0.035007	0.183229	3.29334E-03 0	0.194432	
Decanes Plus			0.0336553	6.19796E-05	2.26216E-06	2.52522E-06	
Decanes Plus Sat			0.0550555	0.197902-03	0	2.525222-00	
Decalles Flus Sat			0	0	0	0	
			Stream	Properties			
Property		Units	21. Inlet Gas	22.	23. HPS	24. VC1 Pilot	
				Condensate Flash Losses Hrly	Water to SWD	Fuel	
Temperature		°F	110	92.65	94.2513	76.5751	
Pressure		psig	110	6.06136	400	120	
Molecular Weight		lb/lbmol	22.8118	54.5139	18.0175	21.2035	
Mass Flow		lb/h	601127	578.522	1351.84	67.0496	
Std Vapor Volumetric F	low	MMSCFD	240	0.0966534	0.683339	0.0288 *	
Std Liquid Volumetric F		sgpm	3309.52	2.09364	2.7058	0.385728	
API Gravity					10.0439		

Remarks

	User Value Sets Report	
Client Name: Location:	DELAWARE DIVISION Job: Buildog Compressor Station Image: Complexity of the state of the stateo	
	Skim Tank	
	User Value [BlockReady]	
* Parameter	1 * Enforce Bounds	False
	User Value [ShellLength]	
* Parameter	30 ft * Enforce Bounds	False
* Parameter	User Value [ShellDiam] 15.5 ft * Enforce Bounds	False
Falameter		Faise
	User Value [BreatherVP]	
* Parameter	0.03 psig * Enforce Bounds	False
	User Value [BreatherVacP]	
* Parameter	-0.03 psig * Enforce Bounds	False
	Lines Maless (Dama Dadius)	
* Enforce Bounds	User Value [DomeRadius]	
Enforce Boardo		
	User Value [OpPress]	
* Parameter	0.25 psig * Enforce Bounds	False
	User Value [AvgPercentLiq]	
* Parameter	80 % * Enforce Bounds	False
* Parameter	User Value [MaxPercentLiq] 90 % * Enforce Bounds	False
		1 0.00
	User Value [MinPercentLiq]	
* Parameter	10 % * Enforce Bounds	False
	User Value [AnnNetTP]	
* Parameter	347.202 bbl/day * Enforce Bounds	False
* Enforce Bounds	User Value [OREff]	
	User Value [MaxAvgT]	
* Parameter	75.8 °F * Enforce Bounds	False
	User Value [MinAvgT]	
* Parameter	47.6 °F * Enforce Bounds	False
	Have Maless (Della 1971)	
* Parameter	User Value [BulkLiqT] 75.6428 °F * Enforce Bounds	False
	User Value [AvgP]	
* Parameter	12.88 psia * Enforce Bounds	False
	User Value [Therml]	
* Parameter	1722 Btu/ft^2/day * Enforce Bounds	False

Oligati Magazi	User Value Sets Re	·
Client Name: Location:	DELAWARE DIVISION Bulldog Compressor Station	Job:
Location.		
	User Value [AvgWindS	ipeed]
* Parameter	8.7 mi/h * Enforce	Bounds False
* 5 (User Value [MaxHourlyLoa	idingRate]
* Enforce Bounds	False	
	User Value [SumLiqLe	vellnc]
* Enforce Bounds	False	
	User Value [Flashin	gT]
* Parameter	82.0362 °F * Enforce	
* Dana 1	User Value [EntrainedC	
* Parameter	1 % * Enforce	Bounds False
		Patol
* Parameter	User Value [Turnover 78.5512 * Enforce	
1 didineter	10.5512	
* Enforce Bounds	User Value [LLossSatF False	actor]
* Parameter	User Value [AtmPress 12.88 psia * Enforce	
1 didifictor		
	User Value [TVP]	
* Parameter	11.1351 psia * Enforce	
	User Value [MaxV	
* Parameter	12.88 psia * Enforce	Bounds False
* Parameter	User Value [MinVI 9.59201 psia * Enforce	
T and motor		
	User Value [AvgLiqSur	faceT1
* Parameter	72.7396 °F * Enforce	
	User Value [MaxLiqSur	
* Parameter	82.0362 °F * Enforce	Bounds False
		1
* Doromotor	User Value [TotalLos 31.7035 ton/yr * Enforce	
* Parameter		Bounds False
	User Value [WorkingLo	[20220
* Parameter	12.6077 ton/yr * Enforce	
	User Value [StandingLo	osses]
* Parameter	3.24402 ton/yr * Enforce	
	User Value [RimSealLo	
* Parameter	0 ton/yr * Enforce	Bounds False
* 5	User Value [Withdrawa	
* Parameter	0 ton/yr * Enforce	Bounds False

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		User Val	ue Sets Report		
Client Name:	DELAWARE DIVIS			Job:	
ocation:	Bulldog Compress	or Station			
			e [LoadingLosses]		
Parameter		0 ton/yr	* Enforce Bounds		False
		Lisor Value [Mr	xHourlyLoadingLoss]		
Parameter		0 lb/hr	* Enforce Bounds		False
			Value [PStar]		
Enforce Bounds		False			
		Llear Value	[AllCTotalLosses]		
Parameter		32.7379 ton/yr	* Enforce Bounds		False
			AllCLoadingLosses]		
Parameter		0 ton/yr	* Enforce Bounds		False
Parameter		User value [Al 0 lb/hr	ICMaxHLoadingLoss] * Enforce Bounds		False
Falameter			Eniorce Bounds		T alse
		User Value [/	AllCFlashingLosses]		
Parameter		17.0612 ton/yr	* Enforce Bounds		False
			DeckFittingLosses]		
Parameter		0 ton/yr	* Enforce Bounds		False
		User Value	[DeckSeamLosses]		
Parameter		0 ton/yr	* Enforce Bounds		False
			[FlashingLosses]		
Parameter		15.2029 ton/yr	* Enforce Bounds		False
		User Valu	e [TotalResidual]		
Parameter		22005.7 ton/yr	* Enforce Bounds		False
			[GasMoleWeight]		
Parameter		0.0510921 kg/mol	* Enforce Bounds		False
		lleer Value I	VapReportableFrac]		
Parameter		96.8406 %	* Enforce Bounds		False
			LiqReportableFrac]		
Parameter		1.12322 %	* Enforce Bounds		False
Parameter		User Value [F 89.108 %	IashReportableFrac] * Enforce Bounds		False
		00.100 /0			
temarks This User Value Set	was programmatica	Ily generated. GUID={60FAD	E6C-8D03-40FF-A704-07DD6	E91075D}	
			lensate Tank		
Doromotor			ue [BlockReady]		Foloo
Parameter		1	* Enforce Bounds		False

* User Specified Values ? Extrapolated or Approximate Values

* Enforce Bounds ProMax 5.0.19050.0 Copyright © 2002-2019 BRE Group, Ltd.

	User Value Sets Report	
Client Name: Location:	DELAWARE DIVISION Job: Bulldog Compressor Station	
	User Value [ShellLength]	
* Parameter	16 ft * Enforce Bounds	False
* Parameter	User Value [ShellDiam] 15.5 ft * Enforce Bounds	False
Falameter		T alse
	User Value [BreatherVP]	
* Parameter	0.03 psig * Enforce Bounds	False
	Lloor Value [BrootherVaeP]	
* Parameter	User Value [BreatherVacP] -0.03 psig * Enforce Bounds	False
	User Value [DomeRadius]	
* Enforce Bounds	False	
	User Value [OpPress]	
* Parameter	0.25 psig * Enforce Bounds	False
	User Value [AvgPercentLiq]	
* Parameter	50 % * Enforce Bounds	False
	User Value [MaxPercentLiq]	
* Parameter	90 % * Enforce Bounds	False
* Parameter	User Value [MinPercentLiq] 10 % * Enforce Bounds	False
Falameter		False
	User Value [AnnNetTP]	
* Parameter	778.81 bbl/day * Enforce Bounds	False
* Parameter	User Value [OREff] 0 % * Enforce Bounds	False
	User Value [MaxAvgT]	
* Parameter	75.8 °F * Enforce Bounds	False
	User Value [MinAvgT]	
* Parameter	47.6 °F * Enforce Bounds	False
	User Value [BulkLiqT]	
* Parameter	68.8214 °F * Enforce Bounds	False
	User Value [AvgP]	
* Parameter	12.88 psia * Enforce Bounds	False
* Daramatar	User Value [ThermI] 1722 Btu/ft^2/day * Enforce Bounds	False
* Parameter	1122 Diu/It*2/day Enforce Bounds	raise
	User Value [AvgWindSpeed]	
* Parameter	8.7 mi/h * Enforce Bounds	False

	User Value Sets Report	
Client Name:	DELAWARE DIVISION Job:	
Location:	Bulldog Compressor Station	
	<u> </u>	
	User Value [MaxHourlyLoadingRate]	
* Parameter	210 bbl/hr * Enforce Bounds	False
	User Value [SumLiqLevelInc]	
* Enforce Bounds	False	
	User Value [FlashingT]	
* Parameter	92.65 °F * Enforce Bounds	False
		1400
	User Value [EntrainedOilFrac]	
* Parameter	1 % * Enforce Bounds	False
	User Value [TurnoverRate]	
* Parameter	165.186 * Enforce Bounds	False
* Parameter	User Value [LLossSatFactor] 0.6 * Enforce Bounds	False
Falameter		Faise
	User Value [AtmPressure]	
* Parameter	12.88 psia * Enforce Bounds	False
	User Value [TVP]	
* Parameter	9.13802 psia * Enforce Bounds	False
	User Value [MaxVP]	
* Parameter	10.6294 psia * Enforce Bounds	False
	User Value [MinVP]	
* Parameter	7.82126 psia * Enforce Bounds	False
	User Value [AvgLiqSurfaceT]	
* Parameter	69.4251 °F * Enforce Bounds	False
	User Value [MaxLiqSurfaceT]	
* Parameter	78.6044 °F * Enforce Bounds	False
	User Value [TotalLosses]	
* Parameter	79.6388 ton/yr * Enforce Bounds	False
	User Value [WorkingLosses]	
* Parameter	16.2044 ton/yr * Enforce Bounds	False
	User Value [StandingLosses]	
* Parameter	3.7053 ton/yr * Enforce Bounds	False
* Paramotor	User Value [RimSealLosses] 0 ton/yr * Enforce Bounds	Ealea
* Parameter	0 ton/yr * Enforce Bounds	False
	User Value [WithdrawalLoss]	
* Parameter	0 ton/yr * Enforce Bounds	False
	User Value [LoadingLosses]	
* Parameter	38.8844 ton/yr * Enforce Bounds	False

	User Value Sets Report	
Client Name:	DELAWARE DIVISION Job:	
Location:	Bulldog Compressor Station	
	User Value [MaxHourlyLoadingLoss]	
* Parameter	57.4514 lb/hr * Enforce Bounds	False
	User Value [PStar]	
* Enforce Bounds	False	
* Deverse star	User Value [AllCTotalLosses]	Falsa
* Parameter	86.5106 ton/yr * Enforce Bounds	False
	User Value [AllCLoadingLosses]	
* Parameter	42.2396 ton/yr * Enforce Bounds	False
* Parameter	User Value [AllCMaxHLoadingLoss] 62.4086 lb/hr * Enforce Bounds	False
	User Value [AllCFlashingLosses]	
* Parameter	2533.93 ton/yr * Enforce Bounds	False
* Parameter	User Value [DeckFittingLosses] 0 ton/yr * Enforce Bounds	False
1 arameter		1 8150
	User Value [DeckSeamLosses]	
* Parameter	0 ton/yr * Enforce Bounds	False
	Heer Value [Fleehing] ecces]	
* Parameter	User Value [FlashingLosses] 2381.84 ton/yr * Enforce Bounds	False
T didinotor		1 dibb
	User Value [TotalResidual]	
* Parameter	34114.8 ton/yr * Enforce Bounds	False
	User Value [GasMoleWeight]	
* Parameter	0.054801 kg/mol * Enforce Bounds	False
	User Value [VapReportableFrac]	
* Parameter	92.0568 % * Enforce Bounds	False
	User Value [LiqReportableFrac]	
* Parameter	99.9191 % * Enforce Bounds	False
* Denessata	User Value [FlashReportableFrac]	E.L.
* Parameter	93.998 % * Enforce Bounds	False
Remarks		
This User Value Se	et was programmatically generated. GUID={AE1B16B2-2B8A-47A4-8AEF-7E4BCD819B7B}	
	Produced Water Tank	
	User Value [BlockReady]	
* Parameter	1 * Enforce Bounds	False
	Lloor Voluo [Chall] angth]	
* Parameter	User Value [ShellLength] 16 ft * Enforce Bounds	False
* User Specified Values	ProMax 5.0.19050.0	Licensed to Esso Exploration. Inc

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Client Name:			e Sets Report	lah	
Location:	Bulldog Compressor S			Job:	
Loodion.	Dundog Complessor d				
			e [ShellDiam]		
* Parameter		15.5 ft	* Enforce Bounds	False	
* Doromotor		0.03 psig	* Enforce Bounds	Falsa	
* Parameter		0.03 psig	Enforce Bounds	False	
		User Value	[BreatherVacP]		
* Parameter		-0.03 psig	* Enforce Bounds	False	
		User Value	[DomeRadius]		
* Enforce Bounds		False			
			ie [OpPress]		
* Parameter		0.25 psig	* Enforce Bounds	False	
* Demonstra			AvgPercentLiq]	Esta a	
* Parameter		50 %	* Enforce Bounds	False	
		Lleor Value [MaxPercentLiq]		
* Parameter			* Enforce Bounds	False	
		00 /0	Enforce Bounds	1 400	
		User Value (MinPercentLiq]		
* Parameter		10 %	* Enforce Bounds	False	
			e [AnnNetTP]		
* Parameter		341.738 bbl/day	* Enforce Bounds	False	
			lue [OREff]		
* Parameter		0 %	* Enforce Bounds	False	
			e [MaxAvgT]		
* Parameter		75.8 °F	* Enforce Bounds	False	
		10.0			
		User Valu	ie [MinAvgT]		
* Parameter		47.6 °F	* Enforce Bounds	False	
			ie [BulkLiqT]		
* Parameter		75.67 °F	* Enforce Bounds	False	
* D			lue [AvgP]		
* Parameter		12.88 psia	* Enforce Bounds	False	
		Lleen Vel			
* Parameter		1722 Btu/ft^2/day	ue [Therml] * Enforce Bounds	False	
		User Value L	AvgWindSpeed]		
* Parameter		8.7 mi/h	* Enforce Bounds	False	
		User Value [Max	HourlyLoadingRate]		
* Parameter		210 bbl/hr	* Enforce Bounds	False	

Client Name:	User Value Sets Report	
Client Name: Location:	DELAWARE DIVISION Job: Buildog Compressor Station Image: Compressor Station	
* Enforce Bounds	User Value [SumLiqLevelInc]	
Enforce Bounds		
	User Value [FlashingT]	
* Parameter	82.6855 °F * Enforce Bounds	False
	Lisen Velue (Entreine dOilErse)	
* Parameter	User Value [EntrainedOilFrac] 1 % * Enforce Bounds	False
T didificitor		1 460
	User Value [TurnoverRate]	
* Parameter	144.966 * Enforce Bounds	False
* Parameter	User Value [LLossSatFactor] 0.6 * Enforce Bounds	False
	User Value [AtmPressure]	
* Parameter	12.88 psia * Enforce Bounds	False
* Denere eter	User Value [TVP] 12.8672 psia * Enforce Bounds	Falsa
* Parameter	12.8672 psia * Enforce Bounds	False
	User Value [MaxVP]	
* Parameter	14.4348 psia * Enforce Bounds	False
	User Value [MinVP]	
* Parameter	11.3779 psia * Enforce Bounds	False
	User Value [AvgLiqSurfaceT]	
* Parameter	73.5062 °F * Enforce Bounds	False
	User Value [MaxLiqSurfaceT]	
* Parameter	82.6855 °F * Enforce Bounds	False
	User Value [TotalLosses]	
* Parameter	0.941029 ton/yr * Enforce Bounds	False
	User Value [WorkingLosses]	
* Parameter	0.378072 ton/yr * Enforce Bounds	False
	User Value [StandingLosses]	
* Parameter	0.0924424 ton/yr * Enforce Bounds	False
	User Value [RimSealLosses]	
* Parameter	0 ton/yr * Enforce Bounds	False
	User Value [WithdrawalLoss]	
* Parameter	0 ton/yr * Enforce Bounds	False
	User Value [LoadingLosses]	
* Parameter	0.450142 ton/yr * Enforce Bounds	False
* Parameter	User Value [MaxHourlyLoadingLoss] 1.5157 lb/hr * Enforce Bounds	False
r aidilletël		raise

			ue Sets Report		
Client Name:	DELAWARE DI			Job:	
ocation:	Bulldog Compre	ssor Station			
Enforce Bounds		False	Value [PStar]		
		1 4/30			
			[AllCTotalLosses]		
Parameter		1.67313 ton/yr	* Enforce Bounds	_	False
		User Value [AllCLoadingLosses]		
Parameter		0.800346 ton/yr	* Enforce Bounds		False
^r Parameter		User Value [Al 2.69489 lb/hr	IICMaxHLoadingLoss] * Enforce Bounds		Falsa
Parameter		2.09489 ID/11	Enforce Bounds		False
		User Value [/	AllCFlashingLosses]		
Parameter		0 ton/yr	* Enforce Bounds		False
		Lloor Volue			
⁷ Parameter		0 ton/yr	[DeckFittingLosses] * Enforce Bounds		False
T didifictor		o tonyi	Enforce Bounde		T GIOG
			[DeckSeamLosses]		
Parameter		0 ton/yr	* Enforce Bounds		False
		User Value	[FlashingLosses]		
Parameter		0 ton/yr	* Enforce Bounds		False
Parameter		21795.8 ton/yr	IE [TotalResidual] * Enforce Bounds		False
Falameter		21795.8 101891	Enforce Bounds		Faise
		User Value	e [GasMoleWeight]		
Parameter		0.0497059 kg/mol	* Enforce Bounds		False
			VanBanartablaEraal		
Parameter		56.2435 %	VapReportableFrac] * Enforce Bounds		False
			[LiqReportableFrac]		
Parameter		0.0310499 %	* Enforce Bounds		False
		User Value IF	FlashReportableFrac]		
^r Parameter		0 %	* Enforce Bounds		False

01/03/2020

FESCO, Ltd. 1100 Fesco Ave. - Alice, Texas 78332

For: XTO Energy, Inc. 22777 Springswoods Village Pkwy., W4.6B.345 Spring, Texas 77389

Sample: Muy Wano 18 Tank Battery Inlet Separator Spot Gas Sample @ 124 psig & 110 °F

Date Sampled: 12/17/2019

Job Number: 193997.011

CHROMATOGRAPH EXTENDED ANALYSIS - GPA 2286

COMPONENT	MOL%	GPM
Hydrogen Sulfide*	< 0.001	
Nitrogen	0.864	
Carbon Dioxide	0.121	
Methane	73.632	
Ethane	12.988	3.558
Propane	6.704	1.892
Isobutane	0.949	0.318
n-Butane	2.303	0.744
2-2 Dimethylpropane	0.010	0.004
Isopentane	0.551	0.206
n-Pentane	0.654	0.243
Hexanes	0.513	0.216
Heptanes Plus	<u>0.711</u>	<u>0.302</u>
Totals	100.000	7.484

Computed Real Characteristics Of Heptanes Plus:

Specific Gravity	3.402	(Air=1)
Molecular Weight	98.09	
Gross Heating Value	5217	BTU/CF

Computed Real Characteristics Of Total Sample:

Specific Gravity	0.793	(Air=1)
Compressibility (Z)	0.9955	
Molecular Weight	22.88	
Gross Heating Value		
Dry Basis	1394	BTU/CF
Saturated Basis	1371	BTU/CF

*Hydrogen Sulfide tested on location by: Stain Tube Method (GPA 2377) Results: 0.038 Gr/100 CF, 0.6 PPMV or <0.0001 Mol%

Base Conditions: 15.025 PSI & 60 Deg F

Sampled By: (24) DF Analyst: LPJ Processor: RG Cylinder ID: T-5881 Certified: FESCO, Ltd. - Alice, Texas

David Dannhaus 361-661-7015

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FESCO, Ltd.

CHROMATOGRAPH EXTENDED ANALYSIS - GPA 2286 TOTAL REPORT			
NENT	MOL %	GPM	۱

COMPONENT	MOL %	GPM		WT %
Hydrogen Sulfide*	< 0.001			< 0.001
Nitrogen	0.864			1.058
Carbon Dioxide	0.121			0.233
Methane	73.632			51.636
Ethane	12.988	3.558		17.072
Propane	6.704	1.892		12.923
Isobutane	0.949	0.318		2.411
n-Butane	2.303	0.744		5.851
2,2 Dimethylpropane	0.010	0.004		0.032
Isopentane	0.551	0.206		1.738
n-Pentane	0.654	0.243		2.063
	0.008	0.243		0.030
2,2 Dimethylbutane				
Cyclopentane	0.000	0.000		0.000
2,3 Dimethylbutane	0.045	0.019		0.170
2 Methylpentane	0.156	0.066		0.588
3 Methylpentane	0.083	0.035		0.313
n-Hexane	0.221	0.093		0.833
Methylcyclopentane	0.088	0.031		0.324
Benzene	0.015	0.004		0.051
Cyclohexane	0.102	0.036		0.375
2-Methylhexane	0.032	0.015		0.140
3-Methylhexane	0.034	0.016		0.149
2,2,4 Trimethylpentane	0.000	0.000		0.000
Other C7's	0.088	0.039		0.382
n-Heptane	0.076	0.036		0.333
Methylcyclohexane	0.097	0.040		0.416
Toluene	0.020	0.007		0.081
Other C8's	0.087	0.041		0.419
n-Octane	0.024	0.013		0.120
Ethylbenzene	0.001	0.000		0.005
M & P Xylenes	0.008	0.000		0.003
O-Xylene	0.002	0.003		0.009
Other C9's	0.027	0.014		0.149
n-Nonane	0.005	0.003		0.028
Other C10's	0.004	0.002		0.025
n-Decane	0.001	0.001		0.006
Undecanes (11)	<u>0.000</u>	<u>0.000</u>		<u>0.000</u>
Totals	100.000	7.484		100.000
	teristics of Total Sample			
		0.793	(Air=1)	
		0.9955		
		22.88		
Gross Heating Value				
		1394	BTU/CF	
Saturated Basis -		1371	BTU/CF	

Page 2 of 3

FESCO, Ltd. 1100 Fesco Ave. - Alice, Texas 78332

Sample: Muy Wano 18 Tank Battery Inlet Separator

Spot Gas Sample @ 124 psig & 110 °F

Date Sampled: 12/17/2019

Job Number: 193997.011

	GLYCALC FORM	ТАТ	
COMPONENT	MOL%	GPM	Wt %
Carbon Dioxide	0.121		0.233
Hydrogen Sulfide	< 0.001		< 0.001
Nitrogen	0.864		1.058
Methane	73.632		51.636
Ethane	12.988	3.558	17.072
Propane	6.704	1.892	12.923
Isobutane	0.949	0.318	2.411
n-Butane	2.313	0.748	5.883
Isopentane	0.551	0.206	1.738
n-Pentane	0.654	0.243	2.063
Cyclopentane	0.000	0.000	0.000
n-Hexane	0.221	0.093	0.833
Cyclohexane	0.102	0.036	0.375
Other C6's	0.292	0.123	1.101
Heptanes	0.318	0.137	1.328
Methylcyclohexane	0.097	0.040	0.416
2,2,4 Trimethylpentane	0.000	0.000	0.000
Benzene	0.015	0.004	0.051
Toluene	0.020	0.007	0.081
Ethylbenzene	0.001	0.000	0.005
Xylenes	0.010	0.004	0.046
Octanes Plus	<u>0.148</u>	<u>0.074</u>	<u>0.747</u>
Totals	100.000	7.484	100.000

Real Characteristics Of Octanes Plus:

Specific Gravity	4.004	(Air=1)
Molecular Weight	115.46	
Gross Heating Value	6049	BTU/CF

Real Characteristics Of Total Sample:

Real Characteristics Of Total Sample:		
Specific Gravity	0.793	(Air=1)
Compressibility (Z)	0.9955	
Molecular Weight	22.88	
Gross Heating Value		
Dry Basis	1394	BTU/CF
Saturated Basis	1371	BTU/CF

Page 3 of 3

FESCO, Ltd. 1100 FESCO Avenue - Alice, Texas 78332

For: XTO Energy, Inc. 22777 Springswoods Village Pkwy., W4.6B.345 Spring, Texas 77389

Sample: Wolverine Compressor Station Inlet Separator Hydrocarbon Liquid Sampled @ 100 psig & 61 °F

Date Sampled: 12/17/19

Job Number: 193998.012

CHROMATOGRAPH EXTENDED ANALYSIS - GPA 2186-M

COMPONENT	MOL %	LIQ VOL %	WT %
Nitrogen	0.017	0.005	0.006
Carbon Dioxide	0.013	0.006	0.008
Methane	2.847	1.310	0.603
Ethane	3.958	2.874	1.570
Propane	8.477	6.341	4.931
Isobutane	3.267	2.903	2.505
n-Butane	12.011	10.281	9.210
2,2 Dimethylpropane	0.114	0.119	0.109
Isopentane	8.130	8.073	7.739
n-Pentane	12.667	12.467	12.057
2,2 Dimethylbutane	0.157	0.178	0.179
Cyclopentane	0.000	0.000	0.000
2,3 Dimethylbutane	0.947	1.054	1.077
2 Methylpentane	4.348	4.900	4.943
3 Methylpentane	2.482	2.751	2.821
n-Hexane	7.509	8.384	8.537
Heptanes Plus	<u>33.056</u>	<u>38.355</u>	<u>43.705</u>
Totals:	100.000	100.000	100.000

Characteristics of Heptanes Plus:

Specific Gravity	0.7431	(Water=1)
°API Gravity	58.92	@ 60°F
Molecular Weight	100.2	
Vapor Volume	22.95	CF/Gal
Weight	6.19	Lbs/Gal

Characteristics of Total Sample:

Specific Gravity	0.6521	(Water=1)
°API Gravity	85.48	@ 60°F
Molecular Weight	75.8	
Vapor Volume	26.62	CF/Gal
Weight	5.43	Lbs/Gal

Base Conditions: 15.025 PSI & 60 °F

Certified: FESCO, Ltd. - Alice, Texas

Sampled By: (24) DF Analyst: RR Processor: RLdjv Cylinder ID: W-1544

David Dannhaus 361-661-7015

FESCO, Ltd.

TANKS DATA INPUT REPORT - GPA 2186-M

COMPONENT	Mol %	LiqVol %	Wt %
Carbon Dioxide	0.013	0.006	0.008
Nitrogen	0.017	0.005	0.006
Methane	2.847	1.310	0.603
Ethane	3.958	2.874	1.570
Propane	8.477	6.341	4.931
Isobutane	3.267	2.903	2.505
n-Butane	12.125	10.400	9.319
Isopentane	8.130	8.073	7.739
n-Pentane	12.667	12.467	12.057
Other C-6's	7.934	8.883	9.020
Heptanes	17.188	18.903	20.999
Octanes	10.539	12.691	14.604
Nonanes	1.643	2.375	2.743
Decanes Plus	0.746	1.256	1.510
Benzene	0.483	0.367	0.498
Toluene	0.991	0.901	1.204
E-Benzene	0.091	0.096	0.128
Xylenes	0.481	0.505	0.674
n-Hexane	7.509	8.384	8.537
2,2,4 Trimethylpentane	0.893	<u>1.260</u>	<u>1.346</u>
Totals:	100.000	100.000	100.000
Characteristics of Total Sample:			
Specific Gravity		0.6521	(Water=1)
°API Gravity		85.48	@ 60°F
Molecular Weight		75.8	
Vapor Volume		26.62	CF/Gal
Weight		5.43	Lbs/Gal

Characteristics of Decanes (C10) Plus:Specific Gravity ------0.7837 (Water=1)Molecular Weight-----153.4

Characteristics of Atmospheric Sample:

°API Gravity	73.81	@ 60°F
Reid Vapor Pressure Equivalent (D-6377)	15.83	psi

QUALITY CONTROL CHECK			
	Sampling		
	Conditions	Test Samples	
Cylinder Number		W-1544*	
Pressure, PSIG	100	110	
Temperature, °F	61	61	

* Sample used for analysis

FESCO, Ltd.

TOTAL EXTENDED REPORT - GPA 2186-M

Job Number: 193998.012

COMPONENT	Mol %	LiqVol %	Wt %
Nitrogen	0.017	0.005	0.006
Carbon Dioxide	0.013	0.006	0.008
Methane	2.847	1.310	0.603
Ethane	3.958	2.874	1.570
Propane	8.477	6.341	4.931
Isobutane	3.267	2.903	2.505
n-Butane	12.011	10.281	9.210
2,2 Dimethylpropane	0.114	0.119	0.109
Isopentane	8.130	8.073	7.739
n-Pentane	12.667	12.467	12.057
2,2 Dimethylbutane	0.157	0.178	0.179
Cyclopentane	0.000	0.000	0.000
2,3 Dimethylbutane	0.947	1.054	1.077
2 Methylpentane 3 Methylpentane	4.348 2.482	4.900 2.751	4.943 2.821
n-Hexane	7.509	8.384	8.537
Methylcyclopentane	3.546	3.407	3.937
Benzene	0.483	0.367	0.498
Cyclohexane	4.466	4.128	4.958
2-Methylhexane	1.797	2.268	2.375
3-Methylhexane	1.575	1.964	2.083
2,2,4 Trimethylpentane	0.893	1.260	1.346
Other C-7's	2.140	2.545	2.800
n-Heptane	3.665	4.591	4.845
Methylcyclohexane	4.915	5.364	6.366
Toluene	0.991	0.901	1.204
Other C-8's	4.505	5.771	6.551
n-Octane	1.119	1.556	1.686
E-Benzene	0.091	0.096	0.128
M & P Xylenes	0.393	0.413	0.550
O-Xylene	0.089	0.092	0.125
Other C-9's	1.383	1.979	2.304
n-Nonane	0.259	0.396	0.438
Other C-10's	0.442	0.696	0.825
n-decane	0.058	0.096	0.108
Undecanes(11)	0.142	0.229	0.275
Dodecanes(12)	0.044	0.077	0.094
Tridecanes(13)	0.020	0.037	0.045
Tetradecanes(14)	0.006	0.013	0.016
Pentadecanes(15) Hexadecanes(16)	0.004 0.002	0.008 0.005	0.010 0.006
Heptadecanes(17)	0.002	0.005	0.006
Octadecanes(18)	0.002	0.000	0.000
Nonadecanes(19)	0.000	0.001	0.002
Eicosanes(20)	0.001	0.004	0.002
Heneicosanes(21)	0.001	0.002	0.002
Docosanes(22)	0.002	0.002	0.002
Tricosanes(23)	0.002	0.003	0.003
Tetracosanes(24)	0.003	0.009	0.013
Pentacosanes(25)	0.001	0.004	0.006
Hexacosanes(26)	0.004	0.015	0.020
Heptacosanes(27)	0.003	0.012	0.016
Octacosanes(28)	0.007	0.025	0.034
Nonacosanes(29)	0.003	0.011	0.015
Triacontanes(30)	0.000	0.000	0.000
Hentriacontanes Plus(31+)	0.000	<u>0.000</u>	0.000
Total	100.000	100.000	100.000

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Tab 8 Section 8 - Map(s)



ITEM 2 - ECD - 60" Combustor 57.6 MCF/D Max - skid package with blowcase

Combustor details

Combustor:	• Dimensions 60"D x 13'	
p/n ECD60STD	Atmospheric MAWP	
	• 6.1 MMBTU/HR	
Plumbing:	Stainless Steel Jets	
per ARC config	• Flamecell	
· -	• 34"L x 41"W Burner	
Concrete pad:	3" Wenco Flame Arrestor	
p/n n/a	3" NPT Inlet Connection	
	• ¼" Fisher 67CR-206 Pilot Regulator	
BMS p/n:	• Installed on a 6' x 10' skid, with (1) 24"x48" knockout drum, (1) 10.75"x36" blowcase, (1) 1" Kimray Direct acting, (1) 1"	
p/n 148392	Kimray Reverse acting, (1)Kimray CUA Level Control, fully assembled and plumbed	
	Paint color: Black	
	• ARC™ PREMIER BMS Package includes: smart auto-ignition, CLS I, DIV II (pending),Modbus RTU over RS-485, Advance	

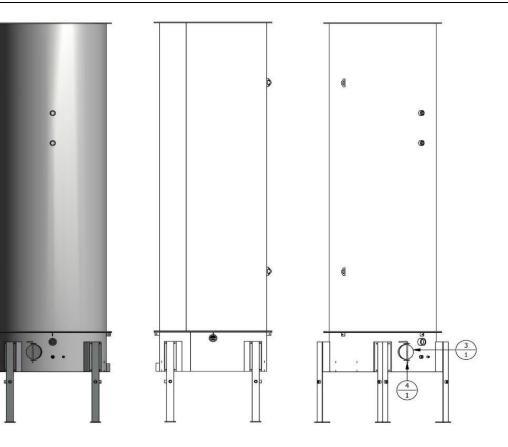
(pending), Modbus RTU over RS-485, Advanced Datalogging, Premier combustion Kit: Includes (2) 1/4" 0.55W ASCO Solenoid Valves, 1/4" 0-5 PSI Transducer, (1) Dual Process Type K Thermocouple w/ Thermowell, no solar package, shipped loose

Item 2 Description		Price Each
ECD - 60" Combustor 57.6 MCF/D Max w/ skid package with blowcase	1 to 4	\$27,760
CCD - 80 Composion 37.0 MCL/D Max w/ skid package with blowcase	5+	\$25,817
ARC™ PREMIER BMS Package		\$4,112

Terms/Delivery

Subject to Prior Sale / 7-8 weeks ARO, Ex Works Mfg Facility: Evans, CO, based on availability at time of quote. Availability will be confirmed after receipt of Purchase Order. Expediting 1-3 business days - 15% upcharge; 4-10 business days - 5% upcharge

Drawing is for information only. Unit specific drawing available upon request.





ENCLOSED COMBUSTORS



Cimarron's enclosed combustion units provide a clean, safe, and efficient solution for eliminating tank vapors and ensuring regulatory compliance. Their performance has been proven to exceed the US EPA's strict requirements with a greater than 99% destruction rate. Designed for both low and high volume applications, the enclosed flares are easy to install and require little ongoing maintenance. Ignition systems include automation capability and data logging features. Standard models have flame cells ranging from 24" to 60", with capacity of 2,000 to 75,000 SCFD. The larger high volume units contain four 24" flame cells and can accommodate up to 200,000 SCFD. ECDs typically operate at pressures of 1 to 12 oz/in².

DESIGN FEATURES AND OPTIONS

- Five Models Manufacturer Performance Tested as per NSPS OOOO §60.5413(d)
- Demonstrated VOC Destruction Efficiency >99%
- Eliminates the requirement for in-field testing to demonstrate continous compliance.
- Solar powered BMS and data logging functions
- Cimarron actuator package for low flow and flameout shutdown
- Drip tank for free liquid removal
- Blowcase skids and modular package options available
- User friendly and easy to install





Confidential [8]

March 15, 2019



XTO Energy 3104 E Greene St. Carlsbad, NM 88220

Attention: To Whom It May Concern

Subject: Compliance with 40 CFR 60.18 Flare Requirements and Destruction Removal Efficiency Confirmation

The Tornado Combustion Technologies Inc. (TCTI) designed two (2) separate dual air assisted flare systems for XTO Energy Midstream Operations Compressor Facilities designed with a maximum buildout design flowrate of 100 to 180 MMSCFD, as per XTO Energy/Select Engineering Flare Specification 1332-SP-P-013 (XTO Energy/Select Engineering Project No.: 1332) on February 20, 2018 (TCTI Design Reference No.: TOR0218 Rev. 0).

The first flare has a 30-inch outer diameter air tip, 22-inch outer diameter annular low pressure air assisted waste gas tip for continuous flaring operations, and 20-inch outer diameter high pressure waste gas tip for facility emergency relieving cases. The tip as previously described is mounted on a riser and guy wire supporting structure so that the overall flare height is 140-feet tall. To date TCTI has provided One (1) flare of this design to XTO Energy Midstream Operations Compressor Facilities, under the following job number:

• 14170 (16495).

This flare design is intended to operate such that:

- i) The maximum high pressure emergency flow rate does not exceed a maximum flow rate of 59,767,069 SCFD, and a maximum net heat release of 6,069,175,258.85 BTU/h; and,
- ii) The maximum low pressure intermittent flow rate does not exceed a maximum flow rate of 952,833 SCFD, a maximum continuous flowrate of 124,363 SCFD which will operate without visible emissions (i.e. excessive soot formation) and a maximum net heat release of 104,435,128.72 BTU/h. For more detailed information please refer to the enclosed design datasheets.

To meet the requirements of 40 CFR 60.18 and industry best practices Tornado has designed the flare to operate as follows:

• TCTI has been designed the flare so each riser of the dual flare system will operate independently. Thus the calculated 40 CFR 60.18 maximum exit velocity for the high pressure non-assisted flare is 391.39 ft/s, 377.63 ft/s and 400 ft/s, for the winter and summer heavy, and winter and summer rich and lean cases respectfully, and low pressure air assisted flare is 170.85 ft/s, 258.33 ft/s, 220.10 ft/s, 146.38 ft/s, 248.24 ft/s and 219.78 ft/s, for the winter and summer heavy, rich and lean cases respectfully, as per paragraphs (c)(3)(ii), (c)(4)(iii), (c)(5), and (f)(6). The actual exit velocities of the flare as determined by paragraph (f)(4) in 40 CFR 60.18, are 364.15 ft/s, 348.57 ft/s, 356.60 ft/s, 367.91 ft/s, 366.37 ft/s, and 372.10 ft/s, for the winter and summer heavy, rich and lean cases respectfully, and low pressure air assisted flare is 11.05 ft/s, 41.31 ft/s, 7.79 ft/s, 18.71 ft/s, 27.39 ft/s and 17.56 ft/s, for the winter and summer heavy, rich and lean cases respectfully, and low pressure air assisted flare is 11.05 ft/s, 41.31 ft/s, 7.79 ft/s, 18.71 ft/s, 27.39 ft/s and 17.56 ft/s, for the winter and summer heavy, rich and lean cases respectfully. As can be seen the actual exit velocity of each low pressure air assisted flare is within the requirements of 40 CFR 60.18. The high pressure air assisted flare's exit velocity although greater than the requirements of 40 CFR

60.18, is exempt from compliance with the standard as per Section 40 CFR 60.11 paragraph (a), and 40 CFR 60.8 paragraph (c), as all cases presented to TCTI for the high pressure air assisted flare have been presented as emergency cases, that are not representative of the flare's performance;

- The calculated lower heating value of the waste gas for the high pressure non-assisted flare are 992.73 BTU/SCF, 1,233.19 BTU/SCF, 1,262.23 BTU/SCF, 979.52 BTU/SCF, 1,222.20 BTU/SCF, and 1,287.62 BTU/SCF, for the winter and summer heavy, rich and lean cases respectfully, and low pressure air assisted flare are 1,641.36 BTU/SCF, 2,650.44 BTU/SCF, 742.52 BTU/SCF, 1,926.09 BTU/SCF, 2,965.73 BTU/SCF, and 1,658.18 BTU/SCF, for the winter and summer heavy, rich and lean cases respectfully. The lower heating value of the provided waste gas composition was calculated as per paragraph (f)(3) of 40 CFR 60.18. This complies with paragraphs (c)(3)(ii) of 40 CFR 60.18 for both a non-assisted and an air assisted flare, as the heating value of the waste gas is greater than 200 BTU/SCF and 300 BTU/SCF, respectfully;
- Tornado has designed this flare to operate with a TSI #6 pilot and TPMR automatic relight and pilot monitoring system. If the flame failure contact is monitored by the client to the satisfaction of the local environmental authority having jurisdiction, then this complies with paragraph (f)(2) of 40 CFR 60.18;
- Tornado has designed the flare to modulate the air flow based upon the waste gas flow rate to the flare for the cases presented which are not considered startup, shutdown, or malfunction as per 40 CFR 60.8(c). By doing this in conjunction with proper flare tuning, the flare's air blower cannot introduce too much air into the jet exit stream thus lowering the destruction efficiency of the flare by quenching mechanisms.

The second flare has a 30-inch outer diameter air tip, 22.5-inch outer diameter annular low pressure air assisted waste gas tip for continuous flaring operations, and 21-inch outer diameter high pressure waste gas tip for facility emergency relieving cases. The tip as previously described is mounted on a riser and guy wire supporting structure so that the overall flare height is 145-feet tall. To date TCTI has provided eleven (11) flares of this design to XTO Energy Midstream Operations Compressor Facilities, under the following job numbers:

- 14274;
- 14275;
- 14276;
- 14277A;
- 14277B;
- 14278A;
- 14278B;
- 14287;
- 14318;
- 14319A;
- 14319B.

This flare design is intended to operate such that:

- i) The maximum high pressure emergency flow rate does not exceed a maximum flow rate of 70,000,000 SCFD, and a maximum net heat release of 7,108,300,193 BTU/h; and,
- ii) The maximum low pressure intermittent flow rate does not exceed a maximum flow rate of 952,833 SCFD, a maximum continuous flowrate of 124,363 SCFD which will operate without visible emissions (i.e. excessive soot formation) and a maximum net heat release of 104,435,128.72 BTU/h. For more detailed information please refer to the enclosed design datasheets.

Due to the volume of sales of this flare design to XTO Energy specifically TCTI has provided this flare with the following model designation moving forward:

• XTO0218R0-145FT.

Thus either the above provided TCTI job numbers or above model number can be used to relate back to this design and the intended operating parameters of the flare system design.

To meet the requirements of 40 CFR 60.18 and industry best practices Tornado has designed the flare to operate as follows:

- TCTI has been designed the flare so each riser of the dual flare system will operate independently. Thus the calculated 40 CFR 60.18 maximum exit velocity for the high pressure non-assisted flare is 391.39 ft/s, 377.63 ft/s and 400 ft/s, for the winter and summer heavy, and winter and summer rich and lean cases respectfully, and low pressure air assisted flare is 170.85 ft/s, 258.33 ft/s, 220.10 ft/s, 146.38 ft/s, 248.24 ft/s and 219.78 ft/s, for the winter and summer heavy, rich and lean cases respectfully, as per paragraphs (c)(3)(ii), (c)(4)(iii), (c)(5), and (f)(6). The actual exit velocities of the flare as determined by paragraph (f)(4) in 40 CFR 60.18, are 415.42 ft/s, 400.47 ft/s, 409.91 ft/s, 420.94 ft/s, 420.19 ft/s, and 426.12 ft/s, for the winter and summer heavy, rich and lean cases respectfully, and low pressure air assisted flare is 11.05 ft/s, 41.31 ft/s, 7.79 ft/s, 18.71 ft/s, 27.39 ft/s and 17.56 ft/s, for the winter and summer heavy, rich and lean cases respectfully. As can be seen the actual exit velocity of each low pressure air assisted flare is within the requirements of 40 CFR 60.18. The high pressure air assisted flare's exit velocity although greater than the requirements of 40 CFR 60.18, is exempt from compliance with the standard as per Section 40 CFR 60.11 paragraph (a), and 40 CFR 60.8 paragraph (c), as all cases presented to TCTI for the high pressure air assisted flare have been presented as emergency cases, that are not representative of the flare's performance;
- The calculated lower heating value of the waste gas for the high pressure non-assisted flare are 992.73 BTU/SCF, 1,233.19 BTU/SCF, 1,262.23 BTU/SCF, 979.52 BTU/SCF, 1,222.20 BTU/SCF, and 1,287.62 BTU/SCF, for the winter and summer heavy, rich and lean cases respectfully, and low pressure air assisted flare are 1,641.36 BTU/SCF, 2,650.44 BTU/SCF, 742.52 BTU/SCF, 1,926.09 BTU/SCF, 2,965.73 BTU/SCF, and 1,658.18 BTU/SCF, for the winter and summer heavy, rich and lean cases respectfully. The lower heating value of the provided waste gas composition was calculated as per paragraph (f)(3) of 40 CFR 60.18. This complies with paragraphs (c)(3)(ii) of 40 CFR 60.18 for both a non-assisted and an air assisted flare, as the heating value of the waste gas is greater than 200 BTU/SCF and 300 BTU/SCF, respectfully;
- Tornado has designed this flare to operate with a TSI #6 pilot and TPMR automatic relight and pilot monitoring system. If the flame failure contact is monitored by the client to the satisfaction of the local environmental authority having jurisdiction, then this complies with paragraph (f)(2) of 40 CFR 60.18;
- Tornado has designed the flare to modulate the air flow based upon the waste gas flow rate to the flare for the cases presented which are not considered startup, shutdown, or malfunction as per 40 CFR 60.8(c). By doing this in conjunction with proper flare tuning, the flare's air blower cannot introduce too much air into the jet exit stream thus lowering the destruction efficiency of the flare by quenching mechanisms.

With both flares being designed to operate as described above the Tornado Combustion Technologies Inc. flare system has been designed to operate in compliance with 40 CFR 60.18. As per EPA studies EPA-600/2-83-052, EPA-600/2-86-080, and EPA-600/2-85-106 meeting the criteria of 40 CFR 60.18 will attain a minimum Destruction Removal Efficiency (DRE) of 98% for hydrocarbon compounds.

XTO Energy has advised that the site under consideration does not need to meet the requirements of 40 CFR 60 Subpart OOOO and only the general requirements must be adhered.

Regards,



Brian Herrler, P.Eng Combustion Engineering **Tornado Combustion Technologies Inc.** 200 – 261200 Wagon Wheel Way Municipal District of Rocky View, Alberta T4A 0E3 Phone: (403) 244-3333 Direct: (403) 567-2223 Mobile: (403) 669-3400 Email: bherrler@tornadotech.com

Cc:(4) Gene Kazmir, General Manager USA, Tornado Combustion Technologies Inc; Cliff Kazmir, General Manager USA, Tornado Combustion Technologies Inc; Bryce Thomas, Flare Manager, Tornado Combustion Technologies Inc; Ian Burge, Combustion Engineering, Tornado Combustion Technologies Inc.

G3516J

ENGINE SPEED (rpm

GAS COMPRESSION

APPLICATION	Bulldo	g Compressor Station 3516J
):	1400	RATING STRATEGY:
IO:	8	FUEL SYSTEM:
E:	SCAC	

130

201

210

ΤA

0.5 28

ADEM3

ASWC

COMPRESSION RATIO:
AFTERCOOLER TYPE:
AFTERCOOLER - STAGE 2 INLET (°F):
AFTERCOOLER - STAGE 1 INLET (°F):
JACKET WATER OUTLET (°F):
ASPIRATION:
COOLING SYSTEM:
CONTROL SYSTEM:
EXHAUST MANIFOLD:
COMBUSTION:
NOx EMISSION LEVEL (g/bhp-hr NOx):
SET POINT TIMING:

ATING STRATEGY: FUEL SYSTEM: SITE CONDITIONS: FUEL: JW+OC+1AC, 2AC LOW EMISSION

GAS ENGINE SITE SPECIFIC TECHNICAL DATA

CATERPILLAR®

STANDARD CAT WIDE RANGE WITH AIR FUEL RATIO CONTROL

FUEL PRESSURE RANGE(psig): (See note 1) FUEL METHANE NUMBER: FUEL LHV (Btu/scf): ALTITUDE(ft): INLET AIR TEMPERATURE(°F): STANDARD RATED POWER:

7.0-40.0 48.1 1126 1067 77 1380 bhp@1400rpm

RATING NOTES LOAD 100% 75% 50% ENGINE POWER (WITHOUT FAN) (2) bhp 1380 1380 1035 690 INLET AIR TEMPERATURE ''F' 77 77 77 77 77 ENGINE DATA (3) Btu/bhp-hr 8095 8497 9133 FUEL CONSUMPTION (LHV) (3) Btu/bhp-hr 8095 8497 9133 AIR FLOW (@inlet air temp, 14.7 psia) (WET) (4)(5) Ib/n' 13879 10606 7283 FUEL LONSUMPTION (HHV) (3) scfm 150 15879 1606 7283 FUEL HOW (60%F, 14.7 psia) (WET) (4)(5) Ib/n' 138379 10606 7283 FUEL ADWIGOL PRESSURE (G) in Hg(abs) 87.9 87.9 69.9 48.1 EXHAUST GAS FLOW (@engine outlet temp, 14.5 psia) (WET) (8)(5) Ib/n' 14383 11002 7567 EXHAUST GAS FLOW (@engine outlet temp, 14.5 psia) (WET) (9)(10) g/hp-hr					MAXIMUM RATING	-	TING AT M IR TEMPE	
INLET AIR TEMPERATURE ref 77 77 77 77 ENGINE DATA FUEL CONSUMPTION (LHV) (3) Btu/bhp-hr 8095 8497 9133 FUEL CONSUMPTION (LHV) (3) Btu/bhp-hr 8095 8095 8497 9133 AIR FLOW (@inlet air temp, 14.7 psia) (WET) (4)(5) ff3/min 3130 3130 2392 1642 AIR FLOW (60%F, 14.7 psia) (WET) (4)(5) ff3/min 1360 118 85 FUEL FLOW (60%F, 14.7 psia) (WET) (4)(5) sdm 150 150 118 85 NLET MANIFOLD PRESSURE (6) in Hg(abs) 87.9 87.9 69.9 48.1 EXHAUST GAS FLOW (@engine outlet temp, 14.5 psia) (WET) (8)(5) ff3/min 8108 6107 74567 NoX (as NO2) (9)(10) g/bhp-hr 0.50 0.50 0.50 0.50 0.50 CO (9)(10) g/bhp-hr 0.36 0.36 0.34 0.33 NMHC (cro	RATING		NOTES	LOAD	100%	100%	75%	50%
ENGINE DATA Image: Construct of the second sec		(WITHOUT FAN)	(2)		1			
FUEL CONSUMPTION (LHV) (3) Btu/bhp-hr 7344 7344 7709 8286 FUEL CONSUMPTION (HHV) (3) Btu/bhp-hr 8095 8497 9133 AIR FLOW (emlet air temp, 14.7 psia) (WET) (4)(5) ft3/min 3130 3130 2322 1642 AIR FLOW (eff, 14.7 psia) (WET) (4)(5) ft3/min 13879 10606 7283 INLET MANIFOLD PRESSURE (6) in Hg(abs) 87.9 87.9 69.9 48.1 EXHAUST GAS FLOW (engine outlet temp, 14.5 psia) (WET) (8)(5) ft3/min 8108 6197 4453 EXHAUST GAS S FLOW (WET) (8)(5) ft3/min 14383 11002 7567 EMISSIONS DATA - ENGINE OUT (8)(5) (9)(10) g/bhp-hr 2.55 2.56 2.47 NMC (Col. wt. of 15.84) (9)(10) g/bhp-hr 3.77 3.77 3.88 3.47 NMHC (VOCs) (mol. wt. of 15.84) (9)(10) g/bhp-hr 0.36 0.36 0.34 0.33	INLET AIR TEMPERATURE			°F	77	77	77	77
FUEL CONSUMPTION (HHV) (3) Btu/bip-hr 8095 8095 8497 9133 AIR FLOW (@inlet air temp, 14.7 psia) (WET) (4)(5) Bt/hr 13879 13879 1300 2392 1642 AIR FLOW (@inlet air temp, 14.7 psia) (WET) (4)(5) Bt/hr 13879 13879 10606 7283 FUEL FLOW (60°F, 14.7 psia) (WET) (4)(5) Bt/hr 150 150 118 85 INLET MANIFOLD PRESSURE (6) in Hg(abs) 87.9 87.9 69.9 48.1 EXHAUST GAS FLOW (@engine outlet temp, 14.5 psia) (WET) (8)(5) It3/min 8108 6197 4453 EXHAUST GAS FLOW (@engine outlet temp, 14.5 psia) (WET) (8)(5) Ib/hr 14383 14383 11002 7567 EMISSIONS DATA - ENGINE OUT (8)(5) (9)(10) g/bhp-hr 2.55 2.56 2.47 THC (mol. wt. of 15.84) (9)(10) g/bhp-hr 0.50 0.50 0.50 0.50 0.50 0.50 0.50	ENGINE DATA							
AIR FLOW (@inlet air temp, 14.7 psia) (WET) (4)(5) ft3/min 3130 3130 2392 1642 AIR FLOW (WET) (4)(5) ft3/min 13879 13879 13879 10606 7283 AIR FLOW (60°F, 14.7 psia) (WET) (4)(5) ft3/min 150 118 85 INLET MANIFOLD PRESSURE (6) in Hg(abs) 87.9 87.9 69.9 48.1 EXHAUST GAS FLOW (engine outlet temp, 14.5 psia) (WET) (8)(5) ft3/min 8108 6197 4453 EXHAUST GAS FLOW (engine outlet temp, 14.5 psia) (WET) (8)(5) ft3/min 8108 6197 4453 EXHAUST GAS RASS FLOW (WET) (8)(5) ft3/min 14383 11002 7567 EMISSIONS DATA - ENGINE OUT (9)(10) g/bp-hr 0.50 <td>FUEL CONSUMPTION (LHV)</td> <td></td> <td>(3)</td> <td>Btu/bhp-hr</td> <td>7344</td> <td>7344</td> <td>7709</td> <td>8286</td>	FUEL CONSUMPTION (LHV)		(3)	Btu/bhp-hr	7344	7344	7709	8286
AR FLOW (WET) (4)(5) Ib/hr 13879 13879 13879 10606 7283 FUEL FLOW (60°F, 14.7 psia) INLET MANIFOLD PRESSURE (6) in Hg(abs) 87.9 87.9 69.9 48.1 EXHAUST TEMPERATURE - ENGINE OUTLET (7) °F 837 837 835 892 EXHAUST GAS MASS FLOW (WET) (8)(5) ft3/min 8108 6197 4453 EXHAUST GAS MASS FLOW (WET) (8)(5) ft3/min 8108 8108 6197 4453 EXHAUST GAS MASS FLOW (WET) (8)(10) g/bhp-hr 14.383 11002 7567 CO (9)(10) g/bhp-hr 2.55 2.56 2.47 7 NMC (mol. wt. of 15.84) (9)(10) g/bhp-hr 1.52 1.52 1.49 1.41 NMHC (mol. wt. of 15.84) (9)(10) g/bhp-hr 0.36 0.36 0.34 0.33 CO2 (mol. wt. of 15.84) (9)(10) g/bhp-hr 0.36 0.36 0.34	FUEL CONSUMPTION (HHV)		(3)	Btu/bhp-hr	8095	8095	8497	9133
FUEL FLOW (60°F, 14.7 psia) scfm 150 150 118 85 INLET MANIFOLD PRESSURE (6) in Hig(abs) 87.9 87.9 69.9 48.1 EXHAUST TEMPERATURE - ENGINE OUTLET (7) ° F 837 837 835 892 EXHAUST GAS FLOW (@engine outlet temp, 14.5 psia) (WET) (8)(5) ft3/min 8108 6197 4453 EXHAUST GAS MASS FLOW (WET) (8)(5) ft3/min 8108 6197 4453 EXHAUST GAS MASS FLOW (WET) (8)(5) ft3/min 8108 6197 4453 CO (9)(10) g/bhp-hr 1.52 2.55 2.56 2.47 THC (mol. wt. of 15.84) (9)(10) g/bhp-hr 3.77 3.77 3.68 3.47 NMNEHC (VOCS) (mol. wt. of 15.84) (9)(10) g/bhp-hr 0.36 0.36 0.34 0.33 CO2 (9)(10) g/bhp-hr 0.36 0.36 0.34 0.33 CO2 (9)(10) g/bhp-hr	AIR FLOW (@inlet air temp, 14.7 psia)	(WET)	(4)(5)	ft3/min	3130	3130	2392	1642
INLET MANIFOLD PRESSURE (6) in Hg(abs) 87.9 87.9 69.9 48.1 EXHAUST TEMPERATURE - ENGINE OUTLET (7) °F 837 837 835 892 EXHAUST GAS FLOW (@engine outlet temp, 14.5 psia) (WET) (8)(5) ft3/min 8108 619.7 445.3 EXHAUST GAS MASS FLOW (WET) (8)(5) ft3/min 14383 11002 7567 EMISSIONS DATA - ENGINE OUT (WET) (9)(10) g/bhp-hr 0.50 0.50 0.50 0.50 CO (9)(10) g/bhp-hr 2.55 2.55 2.56 2.47 THC (mol. wt. of 15.84) (9)(10) g/bhp-hr 3.77 3.68 3.47 NMHC (mol. wt. of 15.84) (9)(10) g/bhp-hr 0.91 0.89 0.84 CO2 (9)(10) g/bhp-hr 0.91 0.91 0.89 0.33 CO2 (9)(10) g/bhp-hr 0.36 0.36 0.34 0.33 EXHAUST OXYGEN (9)(10) g/bhp-hr 0.36<	AIR FLOW	(WET)	(4)(5)	lb/hr	13879	13879	10606	7283
EXHAUST TEMPERATURE - ENGINE OUTLET (7)	FUEL FLOW (60°F, 14.7 psia)			scfm	150	150	118	85
EXHAUST GAS FLOW (@engine outlet temp, 14.5 psia) (WET) (8)(5) ft3/min 8108 8108 6197 4453 EXHAUST GAS MASS FLOW (WET) (8)(5) ft3/min 8108 6197 4453 EXHAUST GAS MASS FLOW (WET) (8)(5) ft3/min 8108 6197 4453 EXHAUST GAS MASS FLOW (WET) (9)(10) g/bhp-hr 14383 11002 7567 EMISSIONS DATA - ENGINE OUT (9)(10) g/bhp-hr 0.50	INLET MANIFOLD PRESSURE		(6)	in Hg(abs)	87.9	87.9	69.9	48.1
EXHAUST GAS MASS FLOW I. I	EXHAUST TEMPERATURE - ENGINE OUTLET		(7)	°F	837	837	835	892
EMISSIONS DATA - ENGINE OUT NOx (as NO2) (9)(10) g/bhp-hr 0.50 0.50 0.50 CO (9)(10) g/bhp-hr 2.55 2.55 2.56 2.47 THC (mol. wt. of 15.84) (9)(10) g/bhp-hr 3.77 3.77 3.68 3.47 NMHE (mol. wt. of 15.84) (9)(10) g/bhp-hr 1.52 1.49 1.41 NMNEHC (VOCs) (mol. wt. of 15.84) (9)(10) g/bhp-hr 0.91 0.89 0.84 HCHO (Formaldehyde) (9)(10) g/bhp-hr 0.91 0.89 0.84 CO2 (9)(10) g/bhp-hr 0.91 0.89 0.84 HCHO (Formaldehyde) (9)(10) g/bhp-hr 0.91 0.89 0.84 CO2 (9)(10) g/bhp-hr 0.502 502 502 525 568 EXHAUST OXYGEN (13) Btu/min 36153 31130 25945 HEAT REJ. TO JACKET WATER (JW) (13) Btu/min 5313 5428 34428 3543	EXHAUST GAS FLOW (@engine outlet temp, 14.5 psia)	(WET)	(8)(5)	ft3/min	8108	8108	6197	4453
NOx (as NO2) CO (9)(10) (9)(10) g/bhp-hr (9)(10) 0.50 0.50 0.50 0.50 CO (9)(10) g/bhp-hr 2.55 2.55 2.56 2.47 THC (mol. wt. of 15.84) (9)(10) g/bhp-hr 3.77 3.77 3.68 3.47 NMHC (mol. wt. of 15.84) (9)(10) g/bhp-hr 1.52 1.49 1.41 NMNEHC (VOCs) (mol. wt. of 15.84) (9)(10) g/bhp-hr 0.91 0.89 0.84 HCHO (Formaldehyde) (9)(10) g/bhp-hr 0.36 0.34 0.33 CO2 (9)(10) g/bhp-hr 502 502 525 568 EXHAUST OXYGEN (13) Btu/min 36153 31130 25945 HEAT REJ. TO JACKET WATER (JW) (13) Btu/min 5313 4428 3543 HEAT REJ. TO ATMOSPHERE (13) Btu/min 5313 5313 4428 3543 HEAT REJ. TO A/C - STAGE 1 (1AC) (13)(14) Btu/min 5064 5064 4393 2761 <td>EXHAUST GAS MASS FLOW</td> <td>(WET)</td> <td>(8)(5)</td> <td>lb/hr</td> <td>14383</td> <td>14383</td> <td>11002</td> <td>7567</td>	EXHAUST GAS MASS FLOW	(WET)	(8)(5)	lb/hr	14383	14383	11002	7567
CO (9)(10) g/bhp-hr 2.55 2.56 2.47 THC (mol. wt. of 15.84) (9)(10) g/bhp-hr 3.77 3.77 3.68 3.47 NMHC (mol. wt. of 15.84) (9)(10) g/bhp-hr 1.52 1.52 1.49 1.41 NMNEHC (VOCS) (mol. wt. of 15.84) (9)(10) g/bhp-hr 0.91 0.89 0.84 HCHO (Formaldehyde) (9)(10) g/bhp-hr 0.36 0.36 0.33 CO2 (9)(10) g/bhp-hr 502 502 525 568 EXHAUST OXYGEN (9)(12) % DRY 9.1 9.1 8.8 8.4 HEAT REJ. TO JACKET WATER (JW) (13) Btu/min 5313 5133 31130 25945 HEAT REJ. TO ATMOSPHERE (13) Btu/min 5313 4428 3543 HEAT REJ. TO ACKET WATER (JW) (13) Btu/min 7839 7839 5810 1168 HEAT REJ. TO ATMOSPHERE (13)(14) Btu/min 5064 4393 2761	EMISSIONS DATA - ENGINE OUT							
THC (mol. wt. of 15.84) (9)(10) g/bhp-hr 3.77 3.68 3.47 NMHC (mol. wt. of 15.84) (9)(10) g/bhp-hr 1.52 1.49 1.41 NMNEHC (VOCs) (mol. wt. of 15.84) (9)(10) g/bhp-hr 0.91 0.89 0.84 HCHO (Formaldehyde) (9)(10) g/bhp-hr 0.36 0.36 0.34 0.33 CO2 (9)(10) g/bhp-hr 502 502 525 568 EXHAUST OXYGEN (9)(12) % DRY 9.1 9.1 8.8 8.4 HEAT REJ. TO JACKET WATER (JW) (13) Btu/min 5313 5313 4128 3543 HEAT REJ. TO ATMOSPHERE (13) Btu/min 5313 5313 43743 3136 HEAT REJ. TO ACKET WATER (JW) (13) Btu/min 5313 5313 4128 3543 HEAT REJ. TO ATMOSPHERE (13) Btu/min 5313 5313 4128 3543 HEAT REJ. TO A/C - STAGE 1 (1AC) (13)(14) Btu/min 7839 7839 35810 1168 HEAT REJ. TO A/C - STAGE 2 (2AC) (13)(14)	NOx (as NO2)		(9)(10)	g/bhp-hr	0.50	0.50	0.50	0.50
NMHC (mol. wt. of 15.84) (9)(10) g/bhp-hr 1.52 1.52 1.49 1.41 NMNEHC (VOCs) (mol. wt. of 15.84) (9)(10) g/bhp-hr 0.91 0.91 0.89 0.84 HCHO (Formaldehyde) (9)(10) g/bhp-hr 0.36 0.36 0.34 0.33 CO2 (9)(10) g/bhp-hr 502 502 525 568 EXHAUST OXYGEN (9)(12) % DRY 9.1 9.1 8.8 8.4 HEAT REJ. TO JACKET WATER (JW) (13) Btu/min 36153 36153 31130 25945 HEAT REJ. TO JACKET WATER (JW) (13) Btu/min 5313 4428 3543 HEAT REJ. TO ATMOSPHERE (13) Btu/min 5313 5313 4428 3543 HEAT REJ. TO A/C - STAGE 1 (1AC) (13)(14) Btu/min 7839 7839 5810 1168 HEAT REJ. TO A/C - STAGE 1 (1AC) (13)(14) Btu/min 5064 4393 2761 MEAT REJ. TO A/C - STAGE 2 (2AC) (14)(15) Btu/min <td>со</td> <td></td> <td>(9)(10)</td> <td>g/bhp-hr</td> <td>2.55</td> <td>2.55</td> <td>2.56</td> <td>2.47</td>	со		(9)(10)	g/bhp-hr	2.55	2.55	2.56	2.47
NMNEHC (VOCs) (mol. wt. of 15.84) (9)(10)(11) g/bhp-hr 0.91 0.91 0.89 0.84 HCHO (Formaldehyde) (9)(10) g/bhp-hr 0.36 0.36 0.34 0.33 CO2 (9)(10) g/bhp-hr 502 502 525 568 EXHAUST OXYGEN (9)(12) % DRY 9.1 9.1 8.8 8.4 HEAT REJECTION HEAT REJ. TO JACKET WATER (JW) (13) Btu/min 36153 36153 31130 25945 HEAT REJ. TO ATMOSPHERE (13) Btu/min 5313 5313 4428 3543 HEAT REJ. TO LUBE OIL (OC) (13) Btu/min 4370 3763 3136 HEAT REJ. TO A/C - STAGE 1 (1AC) (13)(14) Btu/min 7839 7839 5810 1168 HEAT REJ. TO A/C - STAGE 2 (2AC) (13)(14) Btu/min 5064 4393 2761 COOLING SYSTEM SIZING CRITERIA (14)(15) Btu/min 53243 5317 5317	THC (mol. wt. of 15.84)		(9)(10)	g/bhp-hr	3.77	3.77	3.68	3.47
HCHO (Formaldehyde) (9)(10) g/bhp-hr 0.36 0.34 0.33 CO2 (9)(10) g/bhp-hr 502 502 525 568 EXHAUST OXYGEN (9)(12) % DRY 9.1 9.1 8.8 8.4 HEAT REJECTION HEAT REJ. TO JACKET WATER (JW) (13) Btu/min 36153 36153 31130 25945 HEAT REJ. TO ATMOSPHERE (13) Btu/min 5313 5313 4428 3543 HEAT REJ. TO LUBE OIL (OC) (13) Btu/min 5313 5313 4428 3543 HEAT REJ. TO A/C - STAGE 1 (1AC) (13)(14) Btu/min 7839 7839 5810 1168 HEAT REJ. TO A/C - STAGE 2 (2AC) (13)(14) Btu/min 5064 4393 2761 COOLING SYSTEM SIZING CRITERIA TOTAL JACKET WATER CIRCUIT (JW+OC+1AC) (14)(15) Btu/min 53243 TOTAL JACKET WATER CIRCUIT (2AC) (14)(15) Btu/min 5317	NMHC (mol. wt. of 15.84)		(9)(10)	g/bhp-hr	1.52	1.52	1.49	1.41
CO2 (9)(10) g/bhp-hr 502 502 525 568 EXHAUST OXYGEN (9)(12) % DRY 9.1 9.1 8.8 8.4 HEAT REJECTION HEAT REJ. TO JACKET WATER (JW) (13) Btu/min 36153 36153 31130 25945 HEAT REJ. TO ATMOSPHERE (13) Btu/min 5313 5313 4428 3543 HEAT REJ. TO LUBE OIL (OC) (13) Btu/min 4370 4370 3763 3136 HEAT REJ. TO A/C - STAGE 1 (1AC) (13)(14) Btu/min 7839 7839 5810 1168 HEAT REJ. TO A/C - STAGE 2 (2AC) (13)(14) Btu/min 5064 4393 2761 COOLING SYSTEM SIZING CRITERIA (14)(15) Btu/min 53243 5317	NMNEHC (VOCs) (mol. wt. of 15.84)		(9)(10)(11)	g/bhp-hr	0.91	0.91	0.89	0.84
EXHAUST OXYGEN (9)(12) % DRY 9.1 9.1 8.8 8.4 HEAT REJECTION HEAT REJ. TO JACKET WATER (JW) (13) Btu/min 36153 36153 31130 25945 HEAT REJ. TO JACKET WATER (JW) (13) Btu/min 5313 5313 4428 3543 HEAT REJ. TO LUBE OIL (OC) (13) Btu/min 5310 3763 3136 HEAT REJ. TO A/C - STAGE 1 (1AC) (13)(14) Btu/min 7839 7839 5810 1168 HEAT REJ. TO A/C - STAGE 2 (2AC) (13)(14) Btu/min 5064 4393 2761 COOLING SYSTEM SIZING CRITERIA TOTAL JACKET WATER CIRCUIT (JW+OC+1AC) (14)(15) Btu/min 5317	HCHO (Formaldehyde)		(9)(10)	g/bhp-hr	0.36	0.36	0.34	0.33
HEAT REJ. TO JACKET WATER (JW) (13) Btu/min 36153 31130 25945 HEAT REJ. TO JACKET WATER (JW) (13) Btu/min 5313 5313 31130 25945 HEAT REJ. TO ATMOSPHERE (13) Btu/min 5313 5313 4428 3543 HEAT REJ. TO LUBE OIL (OC) (13) Btu/min 4370 4370 3763 3136 HEAT REJ. TO A/C - STAGE 1 (1AC) (13)(14) Btu/min 7839 7839 5810 1168 HEAT REJ. TO A/C - STAGE 2 (2AC) (13)(14) Btu/min 5064 4393 2761 COOLING SYSTEM SIZING CRITERIA TOTAL JACKET WATER CIRCUIT (JW+OC+1AC) (14)(15) Btu/min 53243 TOTAL AFTERCOOLER CIRCUIT (2AC) (14)(15) Btu/min 5317	CO2		(9)(10)	g/bhp-hr	502	502	525	568
HEAT REJ. TO JACKET WATER (JW) (13) Btu/min 36153 36153 31130 25945 HEAT REJ. TO ATMOSPHERE (13) Btu/min 5313 5313 4428 3543 HEAT REJ. TO LUBE OIL (OC) (13) Btu/min 4370 3763 3136 HEAT REJ. TO A/C - STAGE 1 (1AC) (13)(14) Btu/min 7839 7839 5810 1168 HEAT REJ. TO A/C - STAGE 2 (2AC) (13)(14) Btu/min 5064 4393 2761 COOLING SYSTEM SIZING CRITERIA TOTAL JACKET WATER CIRCUIT (JW+OC+1AC) (14)(15) Btu/min 53243 TOTAL AFTERCOOLER CIRCUIT (2AC) (14)(15) Btu/min 5317	EXHAUST OXYGEN		(9)(12)	% DRY	9.1	9.1	8.8	8.4
HEAT REJ. TO ATMOSPHERE (13) Btu/min 5313 5313 4428 3543 HEAT REJ. TO LUBE OIL (OC) (13) Btu/min 4370 3763 3136 HEAT REJ. TO A/C - STAGE 1 (1AC) (13)(14) Btu/min 7839 7839 5810 1168 HEAT REJ. TO A/C - STAGE 2 (2AC) (13)(14) Btu/min 5064 4393 2761 COOLING SYSTEM SIZING CRITERIA TOTAL JACKET WATER CIRCUIT (JW+OC+1AC) (14)(15) Btu/min 53243 TOTAL AFTERCOOLER CIRCUIT (2AC) (14)(15) Btu/min 5317	HEAT REJECTION							
HEAT REJ. TO LUBE OIL (OC) (13) Btu/min 4370 3763 3136 HEAT REJ. TO A/C - STAGE 1 (1AC) (13)(14) Btu/min 7839 7839 5810 1168 HEAT REJ. TO A/C - STAGE 2 (2AC) (13)(14) Btu/min 5064 4393 2761 COOLING SYSTEM SIZING CRITERIA TOTAL JACKET WATER CIRCUIT (JW+OC+1AC) (14)(15) Btu/min 53243 TOTAL AFTERCOOLER CIRCUIT (2AC) (14)(15) Btu/min 5317	HEAT REJ. TO JACKET WATER (JW)		(13)	Btu/min	36153	36153	31130	25945
HEAT REJ. TO A/C - STAGE 1 (1AC) (13)(14) Btu/min 7839 5810 1168 HEAT REJ. TO A/C - STAGE 2 (2AC) (13)(14) Btu/min 5064 4393 2761 COOLING SYSTEM SIZING CRITERIA TOTAL JACKET WATER CIRCUIT (JW+OC+1AC) (14)(15) Btu/min 53243 TOTAL AFTERCOOLER CIRCUIT (2AC) (14)(15) Btu/min 5317	HEAT REJ. TO ATMOSPHERE		(13)	Btu/min	5313	5313	4428	3543
HEAT REJ. TO A/C - STAGE 2 (2AC) (13)(14) Btu/min 5064 5064 4393 2761 COOLING SYSTEM SIZING CRITERIA TOTAL JACKET WATER CIRCUIT (JW+OC+1AC) (14)(15) Btu/min 53243 TOTAL AFTERCOOLER CIRCUIT (2AC) (14)(15) Btu/min 5317	HEAT REJ. TO LUBE OIL (OC)		(13)	Btu/min	4370	4370	3763	3136
COOLING SYSTEM SIZING CRITERIA TOTAL JACKET WATER CIRCUIT (JW+OC+1AC) TOTAL AFTERCOOLER CIRCUIT (2AC) (14)(15) Btu/min 5317	HEAT REJ. TO A/C - STAGE 1 (1AC)		(13)(14)	Btu/min	7839	7839	5810	1168
TOTAL JACKET WATER CIRCUIT (JW+OC+1AC) (14)(15) Btu/min 53243 TOTAL AFTERCOOLER CIRCUIT (2AC) (14)(15) Btu/min 5317	HEAT REJ. TO A/C - STAGE 2 (2AC)		(13)(14)	Btu/min	5064	5064	4393	2761
TOTAL AFTERCOOLER CIRCUIT (2AC) (14)(15) Btu/min 5317	COOLING SYSTEM SIZING CRITERIA							
TOTAL AFTERCOOLER CIRCUIT (2AC) (14)(15) Btu/min 5317	TOTAL JACKET WATER CIRCUIT (JW+OC+1AC)		(14)(15)	Btu/min	53243			
A cooling system safety factor of 0% has been added to the cooling system sizing criteria.	TOTAL AFTERCOOLER CIRCUIT (2AC)			Btu/min	5317			
	A cooling system safety factor of 0% has been added to the cool	ing system sizing criteria.		•		1		

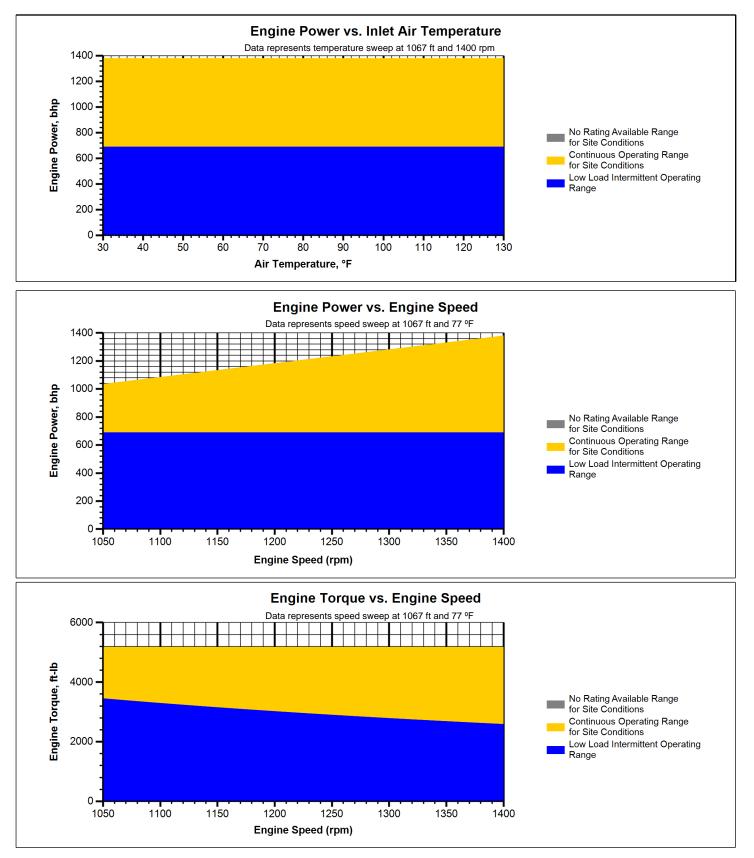
CONDITIONS AND DEFINITIONS

Engine rating obtained and presented in accordance with ISO 3046/1, adjusted for fuel, site altitude and site inlet air temperature. 100% rating at maximum inlet air temperature is the maximum engine capability for the specified fuel at site altitude and maximum site inlet air temperature. Maximum rating is the maximum capability at the specified aftercooler inlet temperature for the specified fuel at site altitude and reduced inlet air temperature. Lowest load point is the lowest continuous duty operating load allowed. No overload permitted at rating shown.

For notes information consult page three.

GAS COMPRESSION APPLICATION

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Note:

At site conditions of 1067 ft and 77°F inlet air temp., constant torque can be maintained down to 1050 rpm. The minimum speed for loading at these conditions is 1050 rpm.

G3516J

GAS COMPRESSION APPLICATION

GAS ENGINE SITE SPECIFIC TECHNICAL DATA Bulldog Compressor Station 3516J



NOTES:

1. Fuel pressure range specified is to the engine fuel pressure regulator. Additional fuel train components should be considered in pressure and flow calculations.

2. Engine rating is with two engine driven water pumps. Tolerance is $\pm\,3\%$ of full load.

3. Engine rating obtained and presented in accordance with ISO 3046/1, adjusted for fuel, site altitude and site ambient temperature.

4. Air flow value is on a 'wet' basis. Flow is a nominal value with a tolerance of ± 5 %.

5. Inlet and Exhaust Restrictions must not exceed A&I limits based on full load flow rates from the standard technical data sheet.

6. Inlet manifold pressure is a nominal value with a tolerance of ± 5 %.

7. Exhaust temperature is a nominal value with a tolerance of (+)63°F, (-)54°F.

8. Exhaust flow value is on a "wet" basis. Flow is a nominal value with a tolerance of \pm 6 %.

9. Emissions data is at engine exhaust flange prior to any after treatment.

10. Values listed are higher than nominal levels to allow for instrumentation, measurement, and engine-to-engine variations. They indicate the maximum values expected under steady state conditions. Fuel methane number cannot vary more than ± 3. THC, NMHC, and NMNEHC do not include aldehydes. An oxidation catalyst may be required to meet Federal, State or local CO or HC requirements.

11. VOCs - Volatile organic compounds as defined in US EPA 40 CFR 60, subpart JJJJ

12. Exhaust Oxygen level is the result of adjusting the engine to operate at the specified NOx level. Tolerance is ± 0.5 .

13. Heat rejection values are nominal. Tolerances, based on treated water, are ± 10% for jacket water circuit, ± 50% for radiation, ± 20% for lube oil circuit, and ± 5% for aftercooler circuit.

14. Aftercooler heat rejection includes an aftercooler heat rejection factor for the site elevation and inlet air temperature specified. Aftercooler heat rejection values at part load are for reference only. Do not use part load data for heat exchanger sizing.

15. Cooling system sizing criteria are maximum circuit heat rejection for the site, with applied tolerances.

G3516J

Constituent

GAS ENGINE SITE SPECIFIC TECHNICAL DATA Bulldog Compressor Station 3516J

GAS COMPRESSION APPLICATION

Abbrou

Mala %

Norm

Constituent	Abbrev	Mole %	Norm		
Water Vapor	H2O	0.0000	0.0000	Fuel Makeup:	
Methane	CH4	78.0190	78.0190	Unit of Measure:	English
Ethane	C2H6	10.6670	10.6670		
Propane	C3H8	4.8170	4.8170	Calculated Fuel Properties	
Isobutane	iso-C4H10	0.5560	0.5560	Caterpillar Methane Number:	48.1
Norbutane	nor-C4H10	1.4030	1.4030		
Isopentane	iso-C5H12	0.3190	0.3190	Lower Heating Value (Btu/scf):	1126
Norpentane	nor-C5H12	0.3610	0.3610	Higher Heating Value (Btu/scf):	1241
Hexane	C6H14	0.3720	0.3720	WOBBE Index (Btu/scf):	1313
Heptane	C7H16	0.5440	0.5440		
Nitrogen	N2	2.0010	2.0010	THC: Free Inert Ratio:	32.99
Carbon Dioxide	CO2	0.9410	0.9410	Total % Inerts (% N2, CO2, He):	2.942%
Hydrogen Sulfide	H2S	0.0000	0.0000	RPC (%) (To 905 Btu/scf Fuel):	100%
Carbon Monoxide	CO	0.0000	0.0000		
Hydrogen	H2	0.0000	0.0000	Compressibility Factor:	0.996
Oxygen	O2	0.0000	0.0000	Stoich A/F Ratio (Vol/Vol):	11.68
Helium	HE	0.0000	0.0000	Stoich A/F Ratio (Mass/Mass):	15.87
Neopentane	neo-C5H12	0.0000	0.0000	Specific Gravity (Relative to Air):	0.736
Octane	C8H18	0.0000	0.0000		
Nonane	C9H20	0.0000	0.0000	Fuel Specific Heat Ratio (K):	1.285
Ethylene	C2H4	0.0000	0.0000		1.200
Propylene	C3H6	0.0000	0.0000		
TOTAL (Volume %)	-	100.0000	100.0000		

CONDITIONS AND DEFINITIONS

Caterpillar Methane Number represents the knock resistance of a gaseous fuel. It should be used with the Caterpillar Fuel Usage Guide for the engine and rating to determine the rating for the fuel specified. A Fuel Usage Guide for each rating is included on page 2 of its standard technical data sheet.

RPC always applies to naturally aspirated (NA) engines, and turbocharged (TA or LE) engines only when they are derated for altitude and ambient site conditions.

Project specific technical data sheets generated by the Caterpillar Gas Engine Rating Pro program take the Caterpillar Methane Number and RPC into account when generating a site rating.

Fuel properties for Btu/scf calculations are at 60F and 14.696 psia.

Caterpillar shall have no liability in law or equity, for damages, consequently or otherwise, arising from use of program and related material or any part thereof.

FUEL LIQUIDS

Field gases, well head gases, and associated gases typically contain liquid water and heavy hydrocarbons entrained in the gas. To prevent detonation and severe damage to the engine, hydrocarbon liquids must not be allowed to enter the engine fuel system. To remove liquids, a liquid separator and coalescing filter are recommended, with an automatic drain and collection tank to prevent contamination of the ground in accordance with local codes and standards.

To avoid water condensation in the engine or fuel lines, limit the relative humidity of water in the fuel to 80% at the minimum fuel operating temperature.

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G3616

ASPIRATION:

COMBUSTION:

COOLING SYSTEM:

CONTROL SYSTEM:

SET POINT TIMING:

EXHAUST MANIFOLD:

ENGINE SPEED (rpm):

COMPRESSION RATIO:

AFTERCOOLER TYPE:

GAS COMPRESSION APPLICATION

AFTERCOOLER - STAGE 2 INLET (°F):

AFTERCOOLER - STAGE 1 INLET (°F): JACKET WATER OUTLET (°F):

NOx EMISSION LEVEL (g/bhp-hr NOx):

GAS ENGINE SITE SPECIFIC TECHNICAL D	ΑΤΑ
Bulldog Compressor Station 3616	

RATING STRATEGY:



STANDARD GAV WITH AIR FUEL RATIO CONTROL

FUEL SYSTEM: SITE CONDITIONS: FUEL: JW+1AC, OC+2AC ADEM4 LOW EMISSION

1000

SCAC

7.6

130

174

190

ΤA

DRY

0.3

16

FUEL PRESSURE RANGE(psig): (See note 1) FUEL METHANE NUMBER: FUEL LHV (Btu/scf): ALTITUDE(ft): INLET AIR TEMPERATURE(°F): STANDARD RATED POWER:

BEU DI 4 Bat Inlet Sep Gas 58.0-70.3 48.1 1126 3502 77 5000 bhp@1000rpm

				MAXIMUM RATING		TING AT M IR TEMPEI	
RATING		NOTES	LOAD	100%	100%	75%	50%
ENGINE POWER	(WITHOUT FAN)	(2)	bhp	5000	5000	3750	2500
INLET AIR TEMPERATURE			°F	77	77	77	77
ENGINE DATA							
FUEL CONSUMPTION (LHV)		(3)	Btu/bhp-hr	6783	6783	6951	7415
FUEL CONSUMPTION (HHV)		(3)	Btu/bhp-hr	7476	7476	7661	8173
AIR FLOW (@inlet air temp, 14.7 psia)	(WET)	(4)(5)	ft3/min	12542	12542	9468	6445
AIR FLOW	(WET)	(4)(5)	lb/hr	55614	55614	41981	28579
FUEL FLOW (60°F, 14.7 psia)			scfm	502	502	386	274
INLET MANIFOLD PRESSURE		(6)	in Hg(abs)	108.6	108.6	81.1	56.6
EXHAUST TEMPERATURE - ENGINE OUTLET		(7)	°F	805	805	851	916
EXHAUST GAS FLOW (@engine outlet temp, 14.5 psia)	(WET)	(8)(5)	ft3/min	31404	31404	24582	17603
EXHAUST GAS MASS FLOW	(WET)	(8)(5)	lb/hr	57302	57302	43278	29502
EMISSIONS DATA - ENGINE OUT							
		(0)(10)		0.00	0.00	0.00	0.00
NOx (as NO2) CO		(9)(10)	g/bhp-hr	0.30	0.30	0.30	0.30 3.07
		(9)(10)	g/bhp-hr	3.06	3.06	3.06	
THC (mol. wt. of 15.84) NMHC (mol. wt. of 15.84)		(9)(10)	g/bhp-hr	3.59	3.59	3.93	4.17 1.69
NMNEHC (VOCs) (mol. wt. of 15.84)		(9)(10)	g/bhp-hr	1.45 0.87	1.45 0.87	1.59	1.09
		(9)(10)(11)	g/bhp-hr			0.95	
HCHO (Formaldehyde) CO2		(9)(10)	g/bhp-hr	0.15 455	0.15 455	0.16 473	0.20 500
EXHAUST OXYGEN		(9)(10) (9)(12)	g/bhp-hr % DRY	400 11.2	455 11.2	473	10.6
		(9)(12)	70 DK 1	11.2	11.2	10.9	10.0
HEAT REJECTION		(10)		50/00	== (= =		
HEAT REJ. TO JACKET WATER (JW)		(13)	Btu/min	53193	53193	43314	36619
HEAT REJ. TO ATMOSPHERE		(13)	Btu/min	18158	18158	17058	15595
HEAT REJ. TO LUBE OIL (OC)		(13)	Btu/min	30493	30493	27342	24076
HEAT REJ. TO A/C - STAGE 1 (1AC)		(13)(14)	Btu/min	54824	54824	28621	8232
HEAT REJ. TO A/C - STAGE 2 (2AC)		(13)(14)	Btu/min	11970	11970	8316	5067
COOLING SYSTEM SIZING CRITERIA							
TOTAL JACKET WATER CIRCUIT (JW+1AC)		(14)(15)	Btu/min	116078			
TOTAL STAGE 2 AFTERCOOLER CIRCUIT (OC+2AC)		(14)(15)	Btu/min	49160			
A cooling system safety factor of 0% has been added to the cooling s	system sizing criteria.						

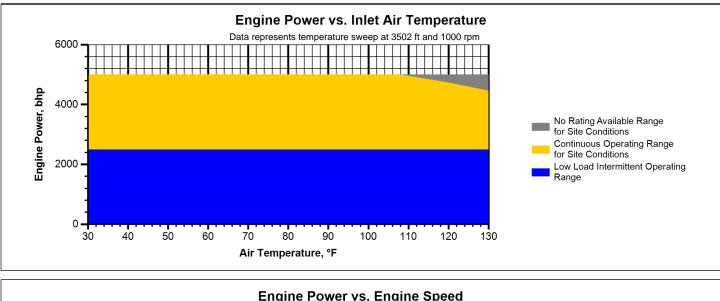
CONDITIONS AND DEFINITIONS

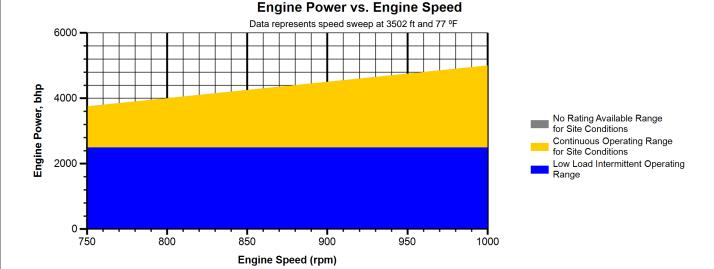
Engine rating obtained and presented in accordance with ISO 3046/1, adjusted for fuel, site altitude and site inlet air temperature. 100% rating at maximum inlet air temperature is the maximum engine capability for the specified fuel at site altitude and maximum site inlet air temperature. Maximum rating is the maximum capability at the specified aftercooler inlet temperature for the specified fuel at site altitude and reduced inlet air temperature. Lowest load point is the lowest continuous duty operating load allowed. No overload permitted at rating shown.

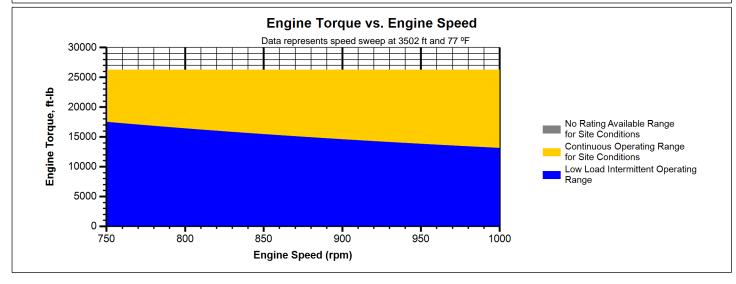
For notes information consult page three.

GAS COMPRESSION APPLICATION

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Note:

At site conditions of 3502 ft and 77°F inlet air temp., constant torque can be maintained down to 750 rpm. The minimum speed for loading at these conditions is 750 rpm.

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GAS ENGINE SITE SPECIFIC TECHNICAL DATA Bulldog Compressor Station 3616



GAS COMPRESSION APPLICATION

NOTES:

1. Fuel pressure range specified is to the engine gas shutoff valve (GSOV). Additional fuel train components should be considered in pressure and flow calculations.

2. Engine rating is with two engine driven water pumps. Tolerance is \pm 3% of full load.

3. Engine rating obtained and presented in accordance with ISO 3046/1, adjusted for fuel, site altitude and site ambient temperature.

4. Air flow value is on a 'wet' basis. Flow is a nominal value with a tolerance of ± 5 %.

5. Inlet and Exhaust Restrictions must not exceed A&I limits based on full load flow rates from the standard technical data sheet.

6. Inlet manifold pressure is a nominal value with a tolerance of ± 5 %.

7. Exhaust temperature is a nominal value with a tolerance of (+)63°F, (-)54°F.

8. Exhaust flow value is on a "wet" basis. Flow is a nominal value with a tolerance of ± 6 %.

9. Emissions data is at engine exhaust flange prior to any after treatment.

10. Values listed are higher than nominal levels to allow for instrumentation, measurement, and engine-to-engine variations. They indicate the maximum values expected under steady state conditions. Fuel methane number cannot vary more than ± 3. THC, NMHC, and NMNEHC do not include aldehydes. An oxidation catalyst may be required to meet Federal, State or local CO or HC requirements.

11. VOCs - Volatile organic compounds as defined in US EPA 40 CFR 60, subpart JJJJ

12. Exhaust Oxygen level is the result of adjusting the engine to operate at the specified NOx level. Tolerance is ± 0.5 .

13. Heat rejection values are nominal. Tolerances, based on treated water, are ± 10% for jacket water circuit, ± 50% for radiation, ± 20% for lube oil circuit, and ± 5% for aftercooler circuit.

14. Aftercooler heat rejection includes an aftercooler heat rejection factor for the site elevation and inlet air temperature specified. Aftercooler heat rejection values at part load are for reference only. Do not use part load data for heat exchanger sizing.

15. Cooling system sizing criteria are maximum circuit heat rejection for the site, with applied tolerances.

G3616

GAS ENGINE SITE SPECIFIC TECHNICAL DATA **Bulldog Compressor Station 3616**

GAS COMPRESSION APPLICATION

Constituent	Abbrev	Mole %	Norm		
Water Vapor	H2O	0.0000	0.0000	Fuel Makeup:	BEU DI 4 Bat Inlet Sep Ga
Methane	CH4	78.0190	78.0190	Unit of Measure:	Englis
Ethane	C2H6	10.6670	10.6670		
Propane	C3H8	4.8170	4.8170	Calculated Fuel Properties	
Isobutane	iso-C4H10	0.5560	0.5560	Caterpillar Methane Number:	48.
Norbutane	nor-C4H10	1.4030	1.4030		
Isopentane	iso-C5H12	0.3190	0.3190	Lower Heating Value (Btu/scf):	112
Norpentane	nor-C5H12	0.3610	0.3610	Higher Heating Value (Btu/scf):	124
Hexane	C6H14	0.3720	0.3720	WOBBE Index (Btu/scf):	131
Heptane	C7H16	0.5440	0.5440		
Nitrogen	N2	2.0010	2.0010	THC: Free Inert Ratio:	32.9
Carbon Dioxide	CO2	0.9410	0.9410	Total % Inerts (% N2, CO2, He):	2.942%
Hydrogen Sulfide	H2S	0.0000	0.0000	RPC (%) (To 905 Btu/scf Fuel):	100%
Carbon Monoxide	CO	0.0000	0.0000		
Hydrogen	H2	0.0000	0.0000	Compressibility Factor:	0.99
Oxygen	O2	0.0000	0.0000	Stoich A/F Ratio (Vol/Vol):	11.6
Helium	HE	0.0000	0.0000	Stoich A/F Ratio (Mass/Mass):	15.8
Neopentane	neo-C5H12	0.0000	0.0000	Specific Gravity (Relative to Air):	0.73
Octane	C8H18	0.0000	0.0000		0.10
Nonane	C9H20	0.0000	0.0000	Fuel Specific Heat Ratio (K):	1.28
Ethylene	C2H4	0.0000	0.0000		1.20
Propylene	C3H6	0.0000	0.0000		
TOTAL (Volume %)	_	100.0000	100.0000		

CONDITIONS AND DEFINITIONS

Caterpillar Methane Number represents the knock resistance of a gaseous fuel. It should be used with the Caterpillar Fuel Usage Guide for the engine and rating to determine the rating for the fuel specified. A Fuel Usage Guide for each rating is included on page 2 of its standard technical data sheet.

RPC always applies to naturally aspirated (NA) engines, and turbocharged (TA or LE) engines only when they are derated for altitude and ambient site conditions.

Project specific technical data sheets generated by the Caterpillar Gas Engine Rating Pro program take the Caterpillar Methane Number and RPC into account when generating a site rating.

Fuel properties for Btu/scf calculations are at 60F and 14.696 psia.

Caterpillar shall have no liability in law or equity, for damages, consequently or otherwise, arising from use of program and related material or any part thereof.

FUEL LIQUIDS

Field gases, well head gases, and associated gases typically contain liquid water and heavy hydrocarbons entrained in the gas. To prevent detonation and severe damage to the engine, hydrocarbon liquids must not be allowed to enter the engine fuel system. To remove liquids, a liquid separator and coalescing filter are recommended, with an automatic drain and collection tank to prevent contamination of the ground in accordance with local codes and standards.

To avoid water condensation in the engine or fuel lines, limit the relative humidity of water in the fuel to 80% at the minimum fuel operating temperature.

CATERPILLAR®

Power Emission Group 311 Riggs Street, Bloomer, WI 54724 Tel: (715) 568-2882 • Fax: (715)568-2884 Email bweninger@catalyticcombustion.com



EMISSION TECHNOLOGIES

To XTO					Our Ref. 001-00-268588.00
Attn Ben					Date: 09 July, 2020
Via E-mail					Page: 1 of 2
			Catalyst Performance		
For :			Project/Location : Bulldo	g	
Parameters					
Engine Manufacturer	Cate	rpillar			Raw Exhaust
Engine Model	G361	16	NOx	0.30	g/bhp-hr
Horsepower		5000 bhp	со	3.06	g/bhp-hr
Speed		1000 rpm	NMHC	1.45	g/bhp-hr
Exhaust Flowrate	:	31404 acfm	NMNEHC (VOC)	0.87	g/bhp-hr
Exhaust Temperature		805 ° F	НСНО	0.15	g/bhp-hr
Fuel	Natu	ral Gas	Oxygen	11.20	%
st Description and Perforn	nance Expect	ations			
Catalyst Model	RGTE	3-2516F-D-20HF-HFX4	Overall Dimensions		5 x 15.44 x 3.7
Catalyst Model Cell Pattern, Substrate	RGTE 20HF	3-2516F-D-20HF-HFX4 -	Catalyst Qty Required	12 p	er Unit
Catalyst Model Cell Pattern, Substrate Formulation	RGTE 20HF HFX4	3-2516F-D-20HF-HFX4 = 1		12 p	
Catalyst Model Cell Pattern, Substrate	RGTE 20HF	3-2516F-D-20HF-HFX4 = 1	Catalyst Qty Required	12 p	er Unit
Catalyst Model Cell Pattern, Substrate Formulation	RGTE 20HF HFX4 8000	3-2516F-D-20HF-HFX4 = 1	Catalyst Qty Required	12 p	er Unit
Catalyst Model Cell Pattern, Substrate Formulation Warranty Period [hrs]	RGTE 20HF HFX4 8000	3-2516F-D-20HF-HFX4 = 4	Catalyst Qty Required	12 p	er Unit
Catalyst Model Cell Pattern, Substrate Formulation Warranty Period [hrs] NOx	RGTE 20HF HFX4 8000	3-2516F-D-20HF-HFX4 = 4	Catalyst Qty Required	12 p	er Unit
Catalyst Model Cell Pattern, Substrate Formulation	RGTE 20HF HFX4 8000	3-2516F-D-20HF-HFX4	Catalyst Qty Required	12 p	er Unit
Catalyst Model Cell Pattern, Substrate Formulation Warranty Period [hrs] NOx CO	RGTE 20HF HFX4 8000	3-2516F-D-20HF-HFX4	Catalyst Qty Required	12 p	er Unit

Please contact us if you have any questions or to let us know how we can be of further help.

Best regards,

Brian Weninger

Product and Application Engineer, Power Emission Group

Power Emission Group 311 Riggs Street, Bloomer, WI 54724 Tel: (715) 568-2882 • Fax: (715)568-2884 Email bweninger@catalyticcombustion.com



EMISSION TECHNOLOGIES

To XTO					Our Ref. 001-00-268588.00
Attn Ben					Date: 09 July, 2020
Via E-mail					Page: 2 of 2
			Catalyst Performance		
For :			Project/Location : Bulldog		
e Parameters					
Engine Manufacturer	Cater	pillar			Raw Exhaust
Engine Model	G3516	5J	NOx	0.50	g/bhp-hr
Horsepower	1	L380 bhp	СО	2.55	g/bhp-hr
Speed	1	1400 rpm	NMHC	1.52	g/bhp-hr
Exhaust Flowrate	8	3108 acfm	NMNEHC (VOC)	0.91	g/bhp-hr
Exhaust Temperature		837 ° F	НСНО	0.36	g/bhp-hr
Fuel	Natur	al Gas	Oxygen	9.10	%
st Description and Perform Catalyst Model		-2516F-D-20HF-HFX4	Overall Dimensions	24.7	5 x 15.44 x 3.7
Cell Pattern, Substrate	20HF	25101 0 2011 11174	Catalyst Qty Required		r Unit
Formulation	HFX4		Pressure Drop		nches of H2O
Warranty Period [hrs]	16000)			
	F	Performance			
NOx					
CO	88	% Conversion			
NMHC					
	65	% Conversion			
NMNEHC (VOC)					

Please contact us if you have any questions or to let us know how we can be of further help.

Best regards,

Weinger Brian Weninger

Product and Application Engineer, Power Emission Group

Table 1.4-1. EMISSION FACTORS FOR NITROGEN OXIDES (NOx) AND CARBON MONOXIDE (CO)FROM NATURAL GAS COMBUSTIONa

	NO _x ^b		(CO
Combustor Type (MMBtu/hr Heat Input) [SCC]	Emission Factor (lb/10 ⁶ scf)	Emission Factor Rating	Emission Factor (lb/10 ⁶ scf)	Emission Factor Rating
Large Wall-Fired Boilers (>100) [1-01-006-01, 1-02-006-01, 1-03-006-01]				
Uncontrolled (Pre-NSPS) ^c	280	А	84	В
Uncontrolled (Post-NSPS) ^c	190	А	84	В
Controlled - Low NO _x burners	140	А	84	В
Controlled - Flue gas recirculation	100	D	84	В
Small Boilers (<100) [1-01-006-02, 1-02-006-02, 1-03-006-02, 1-03-006-03]				
Uncontrolled	100	В	<mark>84</mark>	В
Controlled - Low NO _x burners	50	D	84	В
Controlled - Low NO _x burners/Flue gas recirculation	32	С	84	В
Tangential-Fired Boilers (All Sizes) [1-01-006-04]				
Uncontrolled	170	А	24	С
Controlled - Flue gas recirculation	76	D	98	D
Residential Furnaces (<0.3) [No SCC]				
Uncontrolled	94	В	40	В

^a Reference 11. Units are in pounds of pollutant per million standard cubic feet of natural gas fired. To convert from $lb/10^{6}$ scf to $kg/10^{6}$ m³, multiply by 16. Emission factors are based on an average natural gas higher heating value of 1,020 Btu/scf. To convert from $1b/10^{6}$ scf to lb/MMBtu, divide by 1,020. The emission factors in this table may be converted to other natural gas heating values by multiplying the given emission factor by the ratio of the specified heating value to this average heating value. SCC = Source Classification Code. ND = no data. NA = not applicable. ^b Expressed as NO₂. For large and small wall fired boilers with SNCR control, apply a 24 percent reduction to the appropriate NO x emission factor. For

^b Expressed as NO₂. For large and small wall fired boilers with SNCR control, apply a 24 percent reduction to the appropriate NO x emission factor. For tangential-fired boilers with SNCR control, apply a 13 percent reduction to the appropriate NO x emission factor.
 ^c NSPS=New Source Performance Standard as defined in 40 CFR 60 Subparts D and Db. Post-NSPS units are boilers with greater than 250 MMBtu/hr of

^c NSPS=New Source Performance Standard as defined in 40 CFR 60 Subparts D and Db. Post-NSPS units are boilers with greater than 250 MMBtu/hr of heat input that commenced construction modification, or reconstruction after August 17, 1971, and units with heat input capacities between 100 and 250 MMBtu/hr that commenced construction modification, or reconstruction after June 19, 1984.

1.4-5

Pollutant	Emission Factor (lb/10 ⁶ scf)	Emission Factor Rating
CO ₂ ^b	120,000	А
Lead	0.0005	D
N ₂ O (Uncontrolled)	2.2	Е
N ₂ O (Controlled-low-NO _X burner)	0.64	Е
PM (Total) ^c	7.6	D
PM (Condensable) ^c	5.7	D
PM (Filterable) ^c	1.9	В
$SO_2^{\ d}$	0.6	А
TOC	11	В
Methane	2.3	В
VOC	5.5	С

TABLE 1.4-2. EMISSION FACTORS FOR CRITERIA POLLUTANTS AND GREENHOUSE GASESFROM NATURAL GAS COMBUSTION^a

^a Reference 11. Units are in pounds of pollutant per million standard cubic feet of natural gas fired. Data are for all natural gas combustion sources. To convert from $lb/10^6$ scf to $kg/10^6$ m³, multiply by 16. To convert from $lb/10^6$ scf to 1b/MMBtu, divide by 1,020. The emission factors in this table may be converted to other natural gas heating values by multiplying the given emission factor by the ratio of the specified heating value to this average heating value. TOC = Total Organic Compounds. VOC = Volatile Organic Compounds.

- ^b Based on approximately 100% conversion of fuel carbon to CO_2 . $CO_2[lb/10^6 \text{ scf}] = (3.67)$ (CON) (C)(D), where CON = fractional conversion of fuel carbon to CO_2 , C = carbon content of fuel by weight (0.76), and D = density of fuel, $4.2 \times 10^4 \text{ lb}/10^6 \text{ scf}$.
- ^c All PM (total, condensible, and filterable) is assumed to be less than 1.0 micrometer in diameter. Therefore, the PM emission factors presented here may be used to estimate PM_{10} , $PM_{2.5}$ or PM_1 emissions. Total PM is the sum of the filterable PM and condensible PM. Condensible PM is the particulate matter collected using EPA Method 202 (or equivalent). Filterable PM is the particulate matter collected on, or prior to, the filter of an EPA Method 5 (or equivalent) sampling train.

^d Based on 100% conversion of fuel sulfur to SO_2 . Assumes sulfur content is natural gas of 2,000 grains/10⁶ scf. The SO_2 emission factor in this table can be converted to other natural gas sulfur contents by multiplying the SO_2 emission factor by the ratio of the site-specific sulfur content (grains/10⁶ scf) to 2,000 grains/10⁶ scf.

CAS No.	Pollutant	Emission Factor (lb/10 ⁶ scf)	Emission Factor Rating
91-57-6	2-Methylnaphthalene ^{b, c}	2.4E-05	D
56-49-5	3-Methylchloranthrene ^{b, c}	<1.8E-06	Е
	7,12-Dimethylbenz(a)anthracene ^{b,c}	<1.6E-05	Е
83-32-9	Acenaphthene ^{b,c}	<1.8E-06	Е
203-96-8	Acenaphthylene ^{b,c}	<1.8E-06	Е
120-12-7	Anthracene ^{b,c}	<2.4E-06	Е
56-55-3	Benz(a)anthracene ^{b,c}	<1.8E-06	Е
71-43-2	Benzene ^b	2.1E-03	В
50-32-8	Benzo(a)pyrene ^{b,c}	<1.2E-06	Е
205-99-2	Benzo(b)fluoranthene ^{b,c}	<1.8E-06	Е
191-24-2	Benzo(g,h,i)perylene ^{b,c}	<1.2E-06	Е
205-82-3	Benzo(k)fluoranthene ^{b,c}	<1.8E-06	Е
106-97-8	Butane	2.1E+00	Е
218-01-9	Chrysene ^{b,c}	<1.8E-06	Е
53-70-3	Dibenzo(a,h)anthracene ^{b,c}	<1.2E-06	Е
25321-22-6	Dichlorobenzene ^b	1.2E-03	Е
74-84-0	Ethane	3.1E+00	Е
206-44-0	Fluoranthene ^{b,c}	3.0E-06	Е
86-73-7	Fluorene ^{b,c}	2.8E-06	Е
50-00-0	Formaldehyde ^b	7.5E-02	В
110-54-3	Hexane ^b	1.8E+00	Е
193-39-5	Indeno(1,2,3-cd)pyrene ^{b,c}	<1.8E-06	Е
91-20-3	Naphthalene ^b	6.1E-04	Е
109-66-0	Pentane	2.6E+00	Е
85-01-8	Phenanathrene ^{b,c}	1.7E-05	D

TABLE 1.4-3. EMISSION FACTORS FOR SPECIATED ORGANIC COMPOUNDS FROM NATURAL GAS COMBUSTION^a

TABLE 1.4-3. EMISSION FACTORS FOR SPECIATED ORGANIC COMPOUNDS FROM NATURAL GAS COMBUSTION (Continued)

CAS No.	Pollutant	Emission Factor (lb/10 ⁶ scf)	Emission Factor Rating
74-98-6	Propane	1.6E+00	Е
129-00-0	Pyrene ^{b, c}	5.0E-06	Е
108-88-3	Toluene ^b	3.4E-03	С

^a Reference 11. Units are in pounds of pollutant per million standard cubic feet of natural gas fired. Data are for all natural gas combustion sources. To convert from lb/10⁶ scf to kg/10⁶ m³, multiply by 16. To convert from 1b/10⁶ scf to lb/MMBtu, divide by 1,020. Emission Factors preceeded with a less-than symbol are based on method detection limits.

^b Hazardous Air Pollutant (HAP) as defined by Section 112(b) of the Clean Air Act.

^c HAP because it is Polycyclic Organic Matter (POM). POM is a HAP as defined by Section 112(b) of the Clean Air Act.

^d The sum of individual organic compounds may exceed the VOC and TOC emission factors due to differences in test methods and the availability of test data for each pollutant.

Pollutant	Emission Factor (lb/MMBtu) ^b (fuel input)	Emission Factor Rating
Criteria Pollutants and Greenhou	ise Gases	
NO _x ^c 90 - 105% Load	4.08 E+00	В
NO _x ^c <90% Load	8.47 E-01	В
CO ^c 90 - 105% Load	3.17 E-01	С
CO ^c <90% Load	5.57 E-01	В
$\mathrm{CO_2}^d$	1.10 E+02	А
SO ₂ ^e	5.88 E-04	А
TOC ^f	1.47 E+00	А
Methane ^g	1.25 E+00	С
VOC ^h	1.18 E-01	С
PM10 (filterable) ⁱ	7.71 E-05	D
PM2.5 (filterable) ⁱ	7.71 E-05	D
PM Condensable ^j	9.91 E-03	D
Trace Organic Compounds		
1,1,2,2-Tetrachloroethane ^k	<4.00 E-05	Е
1,1,2-Trichloroethane ^k	<3.18 E-05	Е
1,1-Dichloroethane	<2.36 E-05	Е
1,2,3-Trimethylbenzene	2.30 E-05	D
1,2,4-Trimethylbenzene	1.43 E-05	С
1,2-Dichloroethane	<2.36 E-05	Е
1,2-Dichloropropane	<2.69 E-05	Е
1,3,5-Trimethylbenzene	3.38 E-05	D
1,3-Butadiene ^k	2.67E-04	D
1,3-Dichloropropene ^k	<2.64 E-05	Е
2-Methylnaphthalene ^k	3.32 E-05	С
2,2,4-Trimethylpentane ^k	2.50 E-04	С
Acenaphthene ^k	1.25 E-06	С

Table 3.2-2. UNCONTROLLED EMISSION FACTORS FOR 4-STROKE LEAN-BURN ENGINESa(SCC 2-02-002-54)

Pollutant	Emission Factor (lb/MMBtu) ^b (fuel input)	Emission Factor Rating
Acenaphthylene ^k	5.53 E-06	С
Acetaldehyde ^{k,1}	8.36 E-03	А
Acrolein ^{k,1}	5.14 E-03	А
Benzene ^k	4.40 E-04	А
Benzo(b)fluoranthene ^k	1.66 E-07	D
Benzo(e)pyrene ^k	4.15 E-07	D
Benzo(g,h,i)perylene ^k	4.14 E-07	D
Biphenyl ^k	2.12 E-04	D
Butane	5.41 E-04	D
Butyr/Isobutyraldehyde	1.01 E-04	С
Carbon Tetrachloride ^k	<3.67 E-05	Е
Chlorobenzene ^k	<3.04 E-05	Е
Chloroethane	1.87 E-06	D
Chloroform ^k	<2.85 E-05	Е
Chrysene ^k	6.93 E-07	С
Cyclopentane	2.27 E-04	С
Ethane	1.05 E-01	С
Ethylbenzene ^k	3.97 E-05	В
Ethylene Dibromide ^k	<4.43 E-05	Е
Fluoranthene ^k	1.11 E-06	С
Fluorene ^k	5.67 E-06	С
Formaldehyde ^{k,1}	5.28 E-02	А
Methanol ^k	2.50 E-03	В
Methylcyclohexane	1.23 E-03	С
Methylene Chloride ^k	2.00 E-05	С
n-Hexane ^k	1.11 E-03	С
n-Nonane	1.10 E-04	С

Table 3.2-2. UNCONTROLLED EMISSION FACTORS FOR 4-STROKE LEAN-BURN ENGINES (Continued)

Section 8

Map(s)

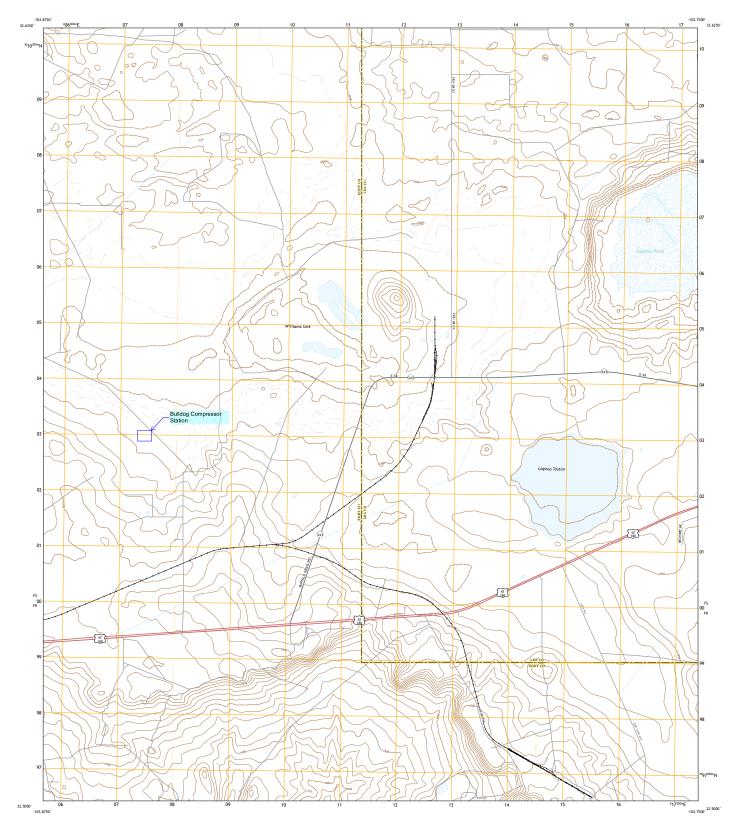
<u>A map</u> such as a 7.5 minute topographic quadrangle showing the exact location of the source. The map shall also include the following:

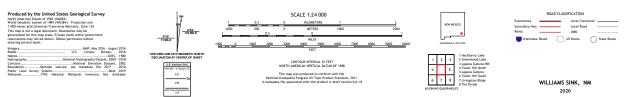
The UTM or Longitudinal coordinate system on both axes	An indicator showing which direction is north
A minimum radius around the plant of 0.8km (0.5 miles)	Access and haul roads
Topographic features of the area	Facility property boundaries
The name of the map	The area which will be restricted to public access
A graphical scale	

A site location map and aerial image illustrating the property boundary and surrounding access roads is provided.

U.S. DEPARTMENT OF THE INTERIOR U.S. GEOLOGICAL SURVEY







Tab 9 Section 9 - Proof of Public Notice Item 1.

Certified Mail Receipts with Postmarks

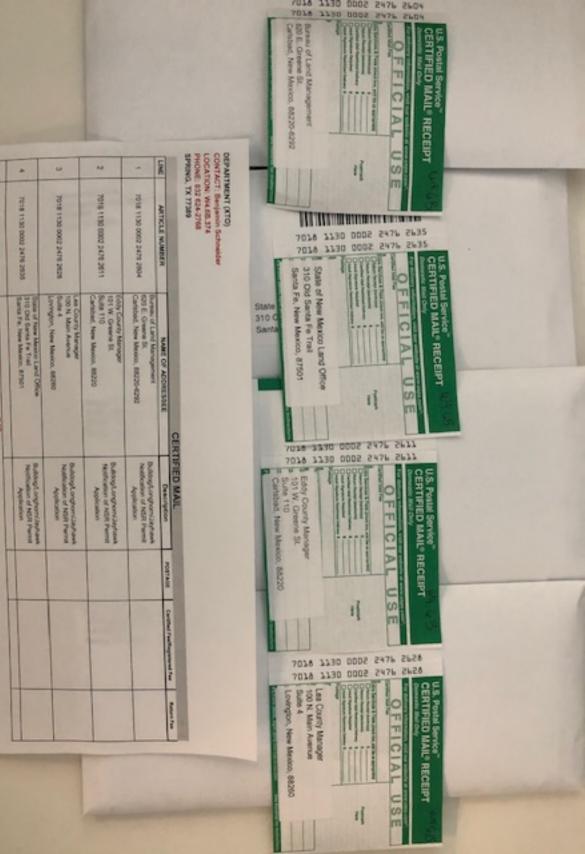
DEPARTMENT (XTO) CONTACT: Benjamin Schneider LOCATION: W4.6B.374 PHONE: 832 624-2768 SPRING, TX 77389

5

Mail	4	ω	N	-	LINE	
Center: Please have this	7018 1130 0002 2476 2635	7018 1130 0002 2476 2628	7018 1130 0002 2476 2611	7018 1130 0002 2476 2604 🗸	ARTICLE NUMBER	
Mail Center: Please have this form stamped by the Post Office	State of New Mexico Land Office 310 Old Santa Fe Trail Santa Fe, New Mexico, 87501	Lea County Manager 100 N. Main Avenue Suite 4 Lovington, New Mexico, 88260	Eddy County Manager 101 W. Greene St. Suite 110 Carlsbad, New Mexico, 88220	Bureau of Land Management 620 E. Greene St. Carlsbad, New Mexico, 88220-6292	NAME OF ADDRESSEE	CER
	Bulldog/Longhom/Jayhawk Notification of NSR Permit Application	Bulldog/Longhorn/Jayhawk Notification of NSR Permit Application	Bulldog/Longhorn/Jayhawk Notification of NSR Permit Application	Bulldog/Longhom/Jayhawk Notification of NSR Permit Application	Description	CERTIFIED MAIL
AUS 31 2020				6.65	POSTAGE	
18ELL NOILDIG				3.55	Certified Fee/Registered Fee	ALAN CONTRACTOR
				2.85	Return Fee	at the second second

Mail Center : Please have this form date stamped by the Post Office.

SdSy



Mail Center: Please have this form stamped by the Post Office

Item 2.

List of Places Posted

Site Location

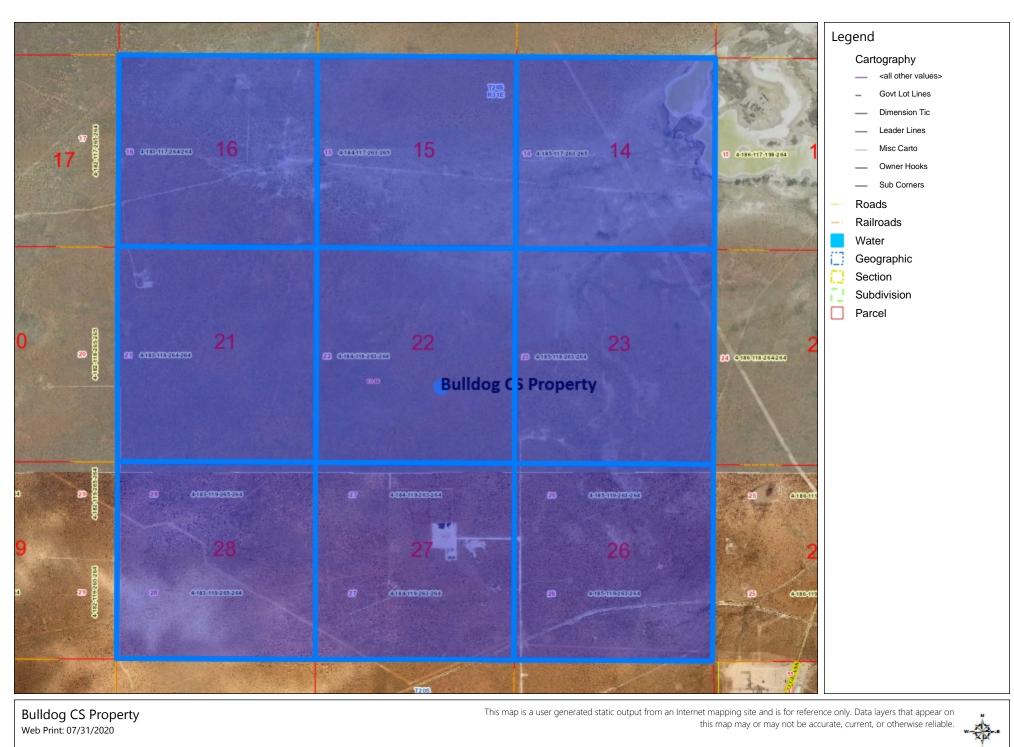
Carlsbad Post Office

Carlsbad Public Library

Hobbs Post Office

Item 3.

Property Tax Records



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3,009

0

6,019 Feet



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Property Record Card

Eddy Assessor

BUREAU OF LAND MANAGEMENT		Account: R074 Tax Area: CO_NR OUT (Nonresident Acres: 0.000	- CARLSBAD-	Parcel: 4-184-118-263-264 Situs Address:
Value Summary			Legal Description	on
Value By: Land (1) Total	Market \$2,880 \$2,880	Override N/A \$2,880	Quarter: NE S: 22 T Quarter: SW S: 22 T MAP# 174-22 LOC	: 20S R: 31E Quarter: NW S: 22 T: 20S R: 31E : 20S R: 31E Quarter: SE S: 22 T: 20S R: 31E ALL N OF HWY 62-180 EXEMPT

Land Occurrence 1

Property Code

9200 - EXEMPT NON-RESIDENTIAL Land Code LAND 141_4_5 - Grazing E Federal - 4.5

Abstract Summary

Code	Classification	Actual Value Value	Taxable Value	Actual Value Override	Taxable Override
9200	EXEMPT NON-RESIDENTIAL LAND	\$2,880	\$960	NA	NA
Total		\$2,880	\$960	NA	NA



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Property Record Card

Eddy Assessor

Parcel: 4-183-117-264-264 **STATE OF NEW MEXICO Account: R074877** 310 OLD SANTA FE TRAIL

SANTA FE, NM 87504

Tax Area: CO_NR - CARLSBAD-OUT (Nonresidential) Acres: 0.000

Situs Address:

Value Summary

Legal Description

Value By:	Market	Override	Quarter: NE S: 16 T: 20S R: 31E Quarter: NW S: 16 T: 20S R: 31E Quarter: SW S: 16 T: 20S R: 31E Quarter: SE S: 16 T: 20S R: 31E NE, NW, SW, SE LESS 6.1 AC, 9.25 AC VALOR,15.5 AC HWY, SW LESS
		Override N/A	Quarter: SW S: 16 1: 20S R: 31E Quarter: SE S: 16 1: 20S R: 31E NE, NW SW SELESS 6 1 AC 9 25 AC VALOR 15 5 AC HWY SWLESS
Land (1)	\$2,643		
Total	\$2,643	\$2,643	

Land Occurrence 1

Property Code

9200 - EXEMPT NON-RESIDENTIAL LAND Land Code 153_4_5 - Grazing E NM - 4.5

Abstract Summary

Code	Classification	Actual Value Value	Taxable Value	Actual Value Override	Taxable Override
9200	EXEMPT NON-RESIDENTIAL LAND	\$2,643	\$881	NA	NA
Total		\$2,643	\$881	NA	NA



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Property Record Card

Eddy Assessor

BUREAU OF LAND MANAGEMENT		Account: R074781 Tax Area: CO_NR - CARLSBAD- OUT (Nonresidential) Acres: 0.000		Parcel: 4-185-118-263-264 Situs Address:
Value Summary			Legal Descript	tion
Value By: Land (1) Total	Market \$2,880 \$2,880	Override N/A \$2,880	Quarter: NE S: 23 Quarter: SW S: 23 MAP# 174-23 LOC	T: 20S R: 31E Quarter: NW S: 23 T: 20S R: 31E T: 20S R: 31E Quarter: SE S: 23 T: 20S R: 31E ALL C W OF BUFFALO GRASS RD EXEMPT

Land Occurrence 1

Property Code

9200 - EXEMPT NON-RESIDENTIAL Land Code LAND 141_4_5 - Grazing E Federal - 4.5

Abstract Summary

Code	Classification	Actual Value Value	Taxable Value	Actual Value Override	Taxable Override
9200	EXEMPT NON-RESIDENTIAL LAND	\$2,880	\$960	NA	NA
Total		\$2,880	\$960	NA	NA



OBJECTID_12_13_14: 5503 UPC: 4-184-119-263-264 UPC_join: 4184119263264 ACCOUNTNUMBER: R074786 LEGALSUMMARY: Quarter: NE S: 27 T: 20S R: 31E Quarter: NW S: 27 T: 20S R: 31E Quarter: SW S: 27 T: 20S R: 31E Quarter: SE S: 27 T: 20S R: 31E NE, NW, SE LESS 6.14 AC, SW MAP# 174-27 LOC N OF HWY 62-180 OWNERNAME: BUREAU OF LAND MANAGEMENT LANDACTUAL: 2853 OBJECTID_1: 45221 TAXYEAR_1: 2020 ACCOUNTNUMBER 1: R074786 SEQUENCE_R: 0 OWNER_OCCURENCE: 0 INTERNALID: C20160020093.1451631600000 DOCUMEN_TTYPE: Owner ACTIVE_1: A CONFIDENTIAL: 0 OWNERID_1: C20160020093 OBJECTID_12: 35989 TAXYEAR_12: 2020 ACCOUNTNUMBER_12: R074786 SEQUENCE_R_1: 0 INTERNALID_1: R074786.LAND2767745.1511254993524 MODEL TYPE: Land ACCOUNTNUMBER_12_13: R074786 ACTUALAREA: 633.86 LANDCODE: 141 4 5 TAXAREA: CO_NR VERSIONEND 1: 9223372036854775807 VERSIONSTART_1: 1511254993524

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Property Record Card

Eddy Assessor

BUREAU OF LAND MANAGEMENT		Account: R074 Tax Area: CO_NR OUT (Nonresident Acres: 0.000	- CARLSB	Parcel: 4-184-119-263-264 SAD- Situs Address:
Value Summary			Legal Desc	
Value By: Land (1) Total	Market \$2,853 \$2,853	Override N/A \$2,853		S: 27 T: 20S R: 31E Quarter: NW S: 27 T: 20S R: 31E S: 27 T: 20S R: 31E Quarter: SE S: 27 T: 20S R: 31E NE, S 6.14 AC, SW MAP# 174-27 LOC N OF HWY 62-180

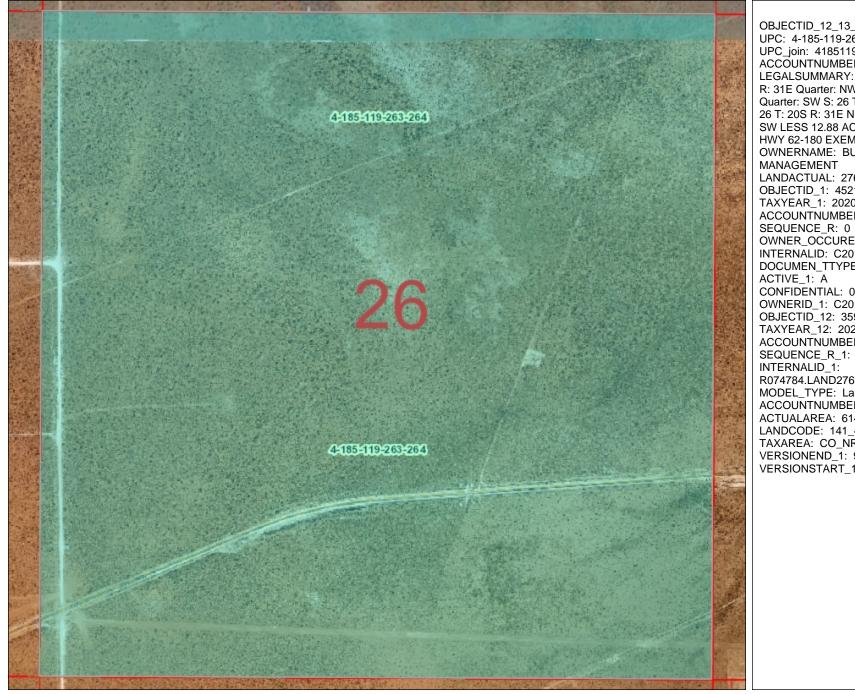
Land Occurrence 1

Property Code

9200 - EXEMPT NON-RESIDENTIAL Land Code 141_4_5 - Grazing E Federal - 4.5 LAND

Abstract Summary

Code	Classification	Actual Value Value	Taxable Value	Actual Value Override	Taxable Override
9200	EXEMPT NON-RESIDENTIAL LAND	\$2,853	\$951	NA	NA
Total		\$2,853	\$951	NA	NA



OBJECTID_12_13_14: 5520 UPC: 4-185-119-263-264 UPC_join: 4185119263264 ACCOUNTNUMBER: R074784 LEGALSUMMARY: Quarter: NE S: 26 T: 20S R: 31E Quarter: NW S: 26 T: 20S R: 31E Quarter: SW S: 26 T: 20S R: 31E Quarter: SE S: 26 T: 20S R: 31E NE, NW, SE LESS 12.17 AC, SW LESS 12.88 AC MAP# 174-26 LOC N OF HWY 62-180 EXEMPT OWNERNAME: BUREAU OF LAND LANDACTUAL: 2766 OBJECTID_1: 45219 TAXYEAR_1: 2020 ACCOUNTNUMBER 1: R074784 OWNER_OCCURENCE: 0 INTERNALID: C20160020093.1451631600000 DOCUMEN_TTYPE: Owner CONFIDENTIAL: 0 OWNERID_1: C20160020093 OBJECTID_12: 35987 TAXYEAR_12: 2020 ACCOUNTNUMBER_12: R074784 SEQUENCE_R_1: 0 R074784.LAND2767744.1511254992221 MODEL TYPE: Land ACCOUNTNUMBER_12_13: R074784 ACTUALAREA: 614.95 LANDCODE: 141_4_5 TAXAREA: CO_NR VERSIONEND 1: 9223372036854775807 VERSIONSTART_1: 1511254992221

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Property Record Card

Eddy Assessor

BUREAU OF LAND MANAGEMENT		Account: R074784 Tax Area: CO_NR - CARLSBAD- OUT (Nonresidential) Acres: 0.000		Parcel: 4-185-119-263-264 D- Situs Address:
Value Summary			Legal Descri	ption
Value By: Land (1) Total	Market \$2,766 \$2,766	Override N/A \$2,766	Quarter: SW S ⁺	26 T: 20S R: 31E Quarter: NW S: 26 T: 20S R: 31E 26 T: 20S R: 31E Quarter: SE S: 26 T: 20S R: 31E NE, 2.17 AC, SW LESS 12.88 AC MAP# 174-26 LOC N OF KEMPT

Land Occurrence 1

Property Code

9200 - EXEMPT NON-RESIDENTIAL Land Code 141_4_5 - Grazing E Federal - 4.5 LAND

Abstract Summary

Code	Classification	Actual Value Value	Taxable Value	Actual Value Override	Taxable Override
9200	EXEMPT NON-RESIDENTIAL LAND	\$2,766	\$922	NA	NA
Total		\$2,766	\$922	NA	NA



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Property Record Card

Eddy Assessor

BUREAU OF LAND MANAGEMENT		Account: R074 Tax Area: CO_NR OUT (Nonresident Acres: 0.000	- CARLSBAD-	Parcel: 4-183-118-264-264 Situs Address:
Value Summary			Legal Description	n
Value By: Land (1) Total	Market \$2,880 \$2,880	Override N/A \$2,880	Quarter: NE S: 21 T: 2 Quarter: SW S: 21 T: 2 MAP# 174-21 LOC N	20S R: 31E Quarter: NW S: 21 T: 20S R: 31E 20S R: 31E Quarter: SE S: 21 T: 20S R: 31E ALL OF HWY 62-180 EXEMPT

Land Occurrence 1

Property Code

9200 - EXEMPT NON-RESIDENTIAL Land Code LAND 141_4_5 - Grazing E Federal - 4.5

Abstract Summary

Code	Classification	Actual Value Value	Taxable Value	Actual Value Override	Taxable Override
9200	EXEMPT NON-RESIDENTIAL LAND	\$2,880	\$960	NA	NA
Total		\$2,880	\$960	NA	NA



OBJECTID_12_13_14: 5518 UPC: 4-185-117-263-265 UPC_join: 4185117263265 ACCOUNTNUMBER: R074767 LEGALSUMMARY: Quarter: NE S: 14 T: 20S R: 31E Quarter: NW S: 14 T: 20S R: 31E Quarter: SW S: 14 T: 20S R: 31E Quarter: SE S: 14 T: 20S R: 31E ALL MAP# 174-14 LOC N OF HWY 62-180 EXEMPT OWNERNAME: BUREAU OF LAND MANAGEMENT LANDACTUAL: 2880 **OBJECTID 1: 45202** TAXYEAR_1: 2020 ACCOUNTNUMBER 1: R074767 SEQUENCE R: 0 OWNER_OCCURENCE: 0 INTERNALID: C20160020093.1451631600000 DOCUMEN_TTYPE: Owner ACTIVE_1: A CONFIDENTIAL: 0 OWNERID_1: C20160020093 OBJECTID_12: 35970 TAXYEAR_12: 2020 ACCOUNTNUMBER_12: R074767 SEQUENCE_R_1: 0 INTERNALID 1: R074767.LAND2767733.1511254982422 MODEL_TYPE: Land ACCOUNTNUMBER_12_13: R074767 ACTUALAREA: 640 LANDCODE: 141_4_5 TAXAREA: CO_NR VERSIONEND_1: 9223372036854775807 VERSIONSTART 1: 1511254982422

This map is a user generated static output from an Internet mapping site and is for reference only. Data layers that appear on this map may or may not be accurate, current, or otherwise reliable.

Property Record Card

Eddy Assessor

BUREAU OF LAND MANAGEMENT	,	Account: R074 Tax Area: CO_NR OUT (Nonresidenti Acres: 0.000	- CARLSBAI	Parcel: 4-185-117-263-265 D- Situs Address:
		Acres: 0.000		
Value Summary			Legal Descri	
Value By:	Market	Override	Quarter: NE S: 1 Quarter: SW S: 1	4 T: 20S R: 31E Quarter: NW S: 14 T: 20S R: 31E 4 T: 20S R: 31E Quarter: SE S: 14 T: 20S R: 31E ALL
Land (1)	\$2,880	N/A	MAP# 174-14 L	OC N OF HWY 62-180 EXEMPT
Total	\$2,880	\$2,880		

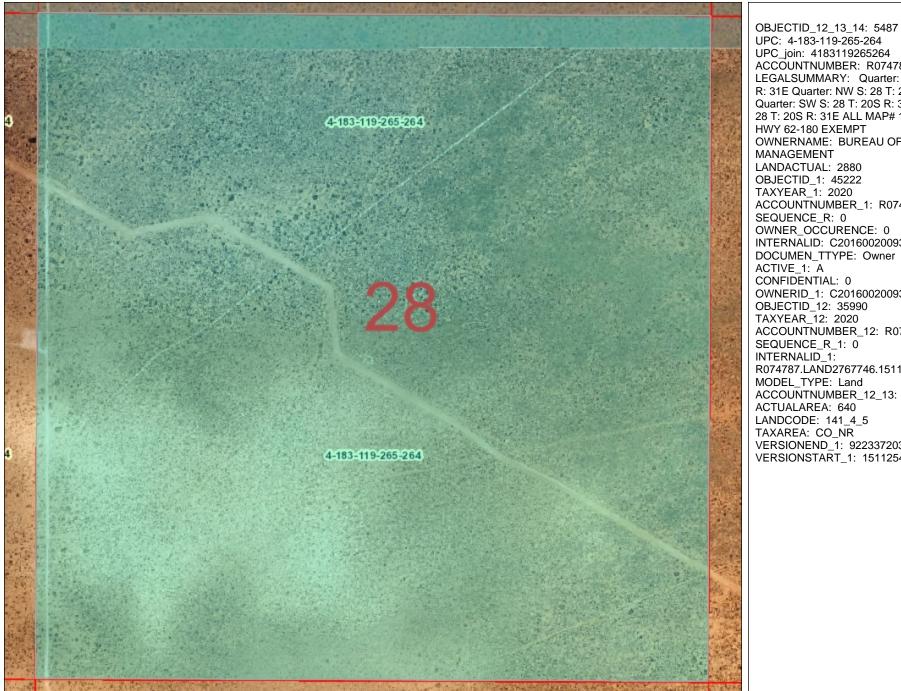
Land Occurrence 1

Property Code

9200 - EXEMPT NON-RESIDENTIAL Land Code 141_4_5 - Grazing E Federal - 4.5 LAND

Abstract Summary

Code	Classification	Actual Value Value	Taxable Value	Actual Value Override	Taxable Override
9200	EXEMPT NON-RESIDENTIAL LAND	\$2,880	\$960	NA	NA
Total		\$2,880	\$960	NA	NA



UPC_join: 4183119265264 ACCOUNTNUMBER: R074787 LEGALSUMMARY: Quarter: NE S: 28 T: 20S R: 31E Quarter: NW S: 28 T: 20S R: 31E Quarter: SW S: 28 T: 20S R: 31E Quarter: SE S: 28 T: 20S R: 31E ALL MAP# 174-28 LOC N OF HWY 62-180 EXEMPT OWNERNAME: BUREAU OF LAND LANDACTUAL: 2880 **OBJECTID 1: 45222** TAXYEAR_1: 2020 ACCOUNTNUMBER_1: R074787 SEQUENCE R: 0 OWNER_OCCURENCE: 0 INTERNALID: C20160020093.1451631600000 DOCUMEN_TTYPE: Owner CONFIDENTIAL: 0 OWNERID_1: C20160020093 OBJECTID_12: 35990 TAXYEAR_12: 2020 ACCOUNTNUMBER_12: R074787 SEQUENCE_R_1: 0 R074787.LAND2767746.1511254993993 MODEL TYPE: Land ACCOUNTNUMBER_12_13: R074787 ACTUALAREA: 640 LANDCODE: 141 4 5 TAXAREA: CO_NR VERSIONEND_1: 9223372036854775807 VERSIONSTART 1: 1511254993993

This map is a user generated static output from an Internet mapping site and is for reference only. Data layers that appear on this map may or may not be accurate, current, or otherwise reliable.

Property Record Card

Eddy Assessor

MANAGEMENT Tax Ar		ccount: R074 ax Area: CO_NR UT (Nonresident	- CARLSBAD-	Parcel: 4-183-119-265-264 Situs Address:
	A	cres: 0.000		
Value Summary			Legal Descriptio	
Value By: Land (1) Total	Market \$2,880 \$2,880	Override N/A \$2,880	Quarter: NE S: 28 T: Quarter: SW S: 28 T: MAP# 174-28 LOC N	20S R: 31E Quarter: NW S: 28 T: 20S R: 31E 20S R: 31E Quarter: SE S: 28 T: 20S R: 31E ALI OF HWY 62-180 EXEMPT

Land Occurrence 1

Property Code

9200 - EXEMPT NON-RESIDENTIAL Land Code 141_4_5 - Grazing E Federal - 4.5 LAND

Abstract Summary

Code	Classification	Actual Value Value	Taxable Value	Actual Value Override	Taxable Override
9200	EXEMPT NON-RESIDENTIAL LAND	\$2,880	\$960	NA	NA
Total		\$2,880	\$960	NA	NA



OBJECTID_12_13_14: 5501 UPC: 4-184-117-263-265 UPC_join: 4184117263265 ACCOUNTNUMBER: R074768 LEGALSUMMARY: Quarter: NE S: 15 T: 20S R: 31E Quarter: NW S: 15 T: 20S R: 31E Quarter: SW S: 15 T: 20S R: 31E Quarter: SE S: 15 T: 20S R: 31E ALL MAP# 174-15 LOC N OF HWY 62-180 EXEMPT OWNERNAME: BUREAU OF LAND MANAGEMENT LANDACTUAL: 2880 **OBJECTID 1: 45203** TAXYEAR_1: 2020 ACCOUNTNUMBER_1: R074768 SEQUENCE R: 0 OWNER_OCCURENCE: 0 INTERNALID: C20160020093.1451631600000 DOCUMEN_TTYPE: Owner ACTIVE_1: A CONFIDENTIAL: 0 OWNERID_1: C20160020093 OBJECTID_12: 35971 TAXYEAR_12: 2020 ACCOUNTNUMBER_12: R074768 SEQUENCE_R_1: 0 INTERNALID 1: R074768.LAND2767734.1511254982892 MODEL_TYPE: Land ACCOUNTNUMBER_12_13: R074768 ACTUALAREA: 640 LANDCODE: 141 4 5 TAXAREA: CO_NR VERSIONEND_1: 9223372036854775807 VERSIONSTART 1: 1511254982892

This map is a user generated static output from an Internet mapping site and is for reference only. Data layers that appear on this map may or may not be accurate, current, or otherwise reliable.

Property Record Card

Eddy Assessor

BUREAU OF LAND MANAGEMENT	,	Account: R074 Tax Area: CO_NR OUT (Nonresident Acres: 0.000	- CARLSBAD	Parcel: 4-184-117-263-265 Situs Address:
Value Summary		Acres: 0.000	Legal Descri	ntion
Value By: Land (1) Total	Market \$2,880 \$2,880	Override N/A \$2,880		5 T: 20S R: 31E Quarter: NW S: 15 T: 20S R: 31E 5 T: 20S R: 31E Quarter: SE S: 15 T: 20S R: 31E ALL OC N OF HWY 62-180 EXEMPT

Land Occurrence 1

Property Code

9200 - EXEMPT NON-RESIDENTIAL Land Code 141_4_5 - Grazing E Federal - 4.5 LAND

Abstract Summary

Code	Classification	Actual Value Value	Taxable Value	Actual Value Override	Taxable Override
9200	EXEMPT NON-RESIDENTIAL LAND	\$2,880	\$960	NA	NA
Total		\$2,880	\$960	NA	NA

Items 4 & 5.

Letters to Owners of Record and Applicable Counties, Municipalities, and Tribes



Certified Mail No. 7018 1130 0002 2476 2604

Bureau of Land Management 620 E. Greene St. Carlsbad, New Mexico, 88220-6292

RE: NSR Permit Application Bulldog Compressor Station XTO Energy Inc.

Dear Federal Official,

In accordance with the application requirements of 20.2.72 NMAC, XTO Energy Inc. is providing notification of the planned modification of the Bulldog Compressor Station on your property in Eddy County, NM. A public notice will be published in the Artesia Daily Press newspaper, at the proposed site location, two other locations in Carlsbad, NM and one location in Hobbs, NM. A copy of the notice is attached. Please contact me at (832) 624-2768 should you have any questions.

Sincerely,

Bon Schneider

Benjamin Schneider Environmental Engineer



Certified Mail No. 7018 1130 0002 2476 2611

Eddy County 101 W. Greene St. Suite 110 Carlsbad, New Mexico, 88220

RE: NSR Permit Application Bulldog Compressor Station XTO Energy Inc.

Dear County Manager,

In accordance with the application requirements of 20.2.72 NMAC, XTO Energy Inc. is providing notification of the planned modification of the Bulldog Compressor Station in Eddy County, NM. A public notice will be published in the Artesia Daily Press newspaper, at the proposed site location, two other locations in Carlsbad, NM and one location in Hobbs, NM. A copy of the notice is attached. Please contact me at (832) 624-2768 should you have any questions.

Sincerely,

Ban Schmeider

Benjamin Schneider Environmental Engineer



Certified Mail No. 7018 1130 0002 2476 2628

Lea County Manager 100 N. Main Avenue Suite 4 Lovington, New Mexico, 88260

RE: NSR Permit Application Bulldog Compressor Station XTO Energy Inc.

Dear County Manager,

In accordance with the application requirements of 20.2.72 NMAC, XTO Energy Inc. is providing notification of the planned modification of the Bulldog Compressor Station in Eddy County, NM. The proposed site is within 10 miles of Lea County. A public notice will be published in the Artesia Daily Press newspaper, at the proposed site location, two other locations in Carlsbad, NM and one location in Hobbs, NM. A copy of the notice is attached. Please contact me at (832) 624-2768 should you have any questions.

Sincerely,

Ben Schneider

Benjamin Schneider Environmental Engineer



Certified Mail No. 7018 1130 0002 2476 2635

State of New Mexico Land Office 310 Old Santa Fe Trail Santa Fe, New Mexico, 87501

RE: NSR Permit Application Bulldog Compressor Station XTO Energy Inc.

Dear Commissioner,

In accordance with the application requirements of 20.2.72 NMAC, XTO Energy Inc. is providing notification of the planned modification of the Bulldog Compressor Station near your property in Eddy County, NM. A public notice will be published in the Artesia Daily Press newspaper, at the proposed site location, two other locations in Carlsbad, NM and one location in Hobbs, NM. A copy of the notice is attached. Please contact me at (832) 624-2768 should you have any questions.

Sincerely,

Ben Schmeider

Benjamin Schneider Environmental Engineer

Item 6.

Sample of Notice posted and Verification of Postings

NOTICE OF AIR QUALITY PERMIT APPLICATION

XTO Energy, Inc. announces its application to the New Mexico Environment Department for an air quality permit for the modification of the Bulldog Compressor Station. The expected date of application submittal to the Air Quality Bureau is August 28, 2020.

The exact location for the facility known as the Bulldog Compressor Station will be latitude 32 deg, 33 min, 24 sec and longitude -103 deg, 51 min, 19 sec. The approximate location of this facility is 22 miles northeast of Carlsbad in Eddy County.

The proposed modification consists removing two engines, updating engine emission rates, updating glycol recirculation rate, removing two heaters, and updating oil/water production rates.

The estimated maximum quantities of any regulated air contaminants will be as follows in pound per hour (pph) and tons per year (tpy). These reported emissions could change slightly during the course of the Department's review:

Pollutant:	Pounds per hour	Tons per year
Particulate Matter (PM)	27 pph	17 tpy
PM 10	27 pph	17 tpy
PM _{2.5}	27 pph	17 tpy
Sulfur Dioxide (SO ₂)	10 pph	20 tpy
Nitrogen Oxides (NO _x)	587 pph	206 tpy
Carbon Monoxide (CO)	1130 pph	228 tpy
Volatile Organic Compounds (VOC)	1113 pph	260 tpy
Total sum of all Hazardous Air Pollutants (HAPs)	35 pph	29 tpy
Toxic Air Pollutant (TAP)	35 pph	29 tpy
Green House Gas Emissions as Total CO2e	n/a	240,024 tpy

The standard and maximum operating schedule of the facility will be 24 hours per day, 7 days a week and a maximum of 52 weeks per year. The owner and/or operator of the Facility is: XTO Energy, Inc.; 22777 Springwoods Village Pkwy-W4.6B.347; Spring, Texas 77389.

If you have any comments about the construction or operation of this facility, and you want your comments to be made as part of the permit review process, you must submit your comments in writing to this address: Permit Programs Manager; New Mexico Environment Department; Air Quality Bureau; 525 Camino de los Marquez, Suite 1; Santa Fe, New Mexico; 87505-1816; (505) 476-4300; 1 800 224-7009; https://www.env.nm.gov/aqb/permit/aqb_draft_permits.html. Other comments and questions may be submitted verbally.

Please refer to the company name and site name, or send a copy of this notice along with your comments, since the Department may have not yet received the permit application. Please include a legible return mailing address with your comments. Once the Department has performed a preliminary review of the application and its air quality impacts, the Department's notice will be published in the legal section of a newspaper circulated near the facility location.

General information about air quality and the permitting process can be found at the Air Quality Bureau's web site. The regulation dealing with public participation in the permit review process is 20.2.72.206 NMAC. This regulation can be found in the "Permits" section of this web site.

Attención

Este es un aviso de la oficina de Calidad del Aire del Departamento del Medio Ambiente de Nuevo México, acerca de las emisiones producidas por un establecimiento en esta área. Si usted desea información en español, por favor comuníquese con esa oficina al teléfono 505-476-5557.

Notice of Non-Discrimination

NMED does not discriminate on the basis of race, color, national origin, disability, age or sex in the administration of its programs or activities, as required by applicable laws and regulations. NMED is responsible for coordination of compliance efforts and receipt of inquiries concerning non-discrimination requirements implemented by 40 C.F.R. Part 7, including Title VI of the Civil Rights Act of 1964, as amended; Section 504 of the Rehabilitation Act of 1973; the Age Discrimination Act of 1975, Title IX of the Education Amendments of 1972, and Section 13 of the Federal Water Pollution Control Act Amendments of 1972. If you have any questions about this notice or any of NMED's non-discrimination programs, policies or procedures, or if you believe that you have been discriminated against with respect to a NMED program or activity, you may contact: Kristine Yurdin, Non-Discrimination Coordinator, NMED, 1190 St. Francis Dr., Suite N4050, P.O. Box 5469, Santa Fe, NM 87502, (505) 827-2855, nd.coordinator@state.nm.us. You may also visit our website at https://www.env.nm.gov/non-employee-discrimination-complaint-page/ to learn how and where to file a complaint of discrimination.

General Posting of Notices - Certification

Bulldog Compressor Station Longhorn Compressor Station Jayhawk Compressor Station

I. Gary G. Goodgome, the undersigned, certify that on {DATE}, posted a true and correct copy of the attached Public Notice in the following publicly accessible and conspicuous places in the Carlsbad of Eddy County, State of New Mexico on the following dates:

All locations lited above:

- 1. Eacility entrance (DATE) Constant Post Office 8-27-20 2. (Location 2) (DATE) Constant Public Library 8-27-20 3. (Location 3) (DATE) Hobbs Past Office 8-28-20

- 4. {Location 4}{DATE}

Signed this 27 day of August, 2010.

Jay A. Roodyane

8-27-20

Printed Name C. Boodgame

Environmental & Daste Coordina tor Title (APPLICANT OR RELATIONSHIP TO APPLICANT)

General Posting of Notices - Certification

Bulldog Compressor Station Longhorn Compressor Station Javhawk Compressor Station

I, <u>Gary G. Coochama</u>, the undersigned, certify that on {DATE}, posted a true and correct copy of the attached Public Notice in the following publicly accessible and conspicuous places in the Carlsbad of Eddy County, State of New Mexico on the following dates:

- 1. Facility entrance {DATE} Bulldog CS off of 62/180 8.27-20 2. {Location 2}{DATE} Jayhow & CS off of 243 8-27-20 3. {Location 3}{DATE} Longhorn CS off of 128 8-27-20

- 4. {Location 4}{DATE}

Signed this 27 day of August, 2020,

Hoodyame

Signature

8-27-20

G. Goodgame

Environmental + Waste Coordinator



NOTICE OF AIR QUALITY PERMIT APPLICATION

STO Darry, inc. encourses in application in the New York, Conferences Statement for an an entry preve for the models of the Redding Compressor Statem. The expected data of application entering to be An Quality Review in August 20, 2020. The result instance for the facility instance in the Backing Comparison Station will be instants [2] day, 21 min, 24 we and langitude (10) day, 21 min, 14 min. The approximate locations of this facility is 22 while software of Cariford in Eddy County

The property and function consists succeeding test and an instant, and spherical of some production succe

an, updating angles on losion rates the entrument maximum quantities of any regulated air domasticants with the follows in pound per-base (spin) and tens per year (spin).

Particular Manae (Port) PM -	Panals per low	Transmission		
PM	27 ppin	Taxa per your 17 apr		
Safe Denils (SO)	27 aph	17 99		
Normann Dealer (NOL)	27 ppa	17.89		
Carbon Minnesola (200)	10,598	New		
Committee Commit	247 ppm	201 (89		
Taxet and of all Harpenberg Air Publicanis (HAPs)	1130 pph	228 (8)		
These Are Publicant (TAP)	1110 pph	200 gy		
Orma house the Databases on Taked COAR	23 pps. 28 pps	29 gy		
The number and many		29.99		
the second se	and the second se	240,004 899		

make and a maxim of 12 -200

can be found at the AS Quality Barnes's such one. The segments

in del Mader Andrews de Name Mérico, access de las responses

Two VII of the Chief and Weaper of 1970, VII of the Chief Rights Are of 1970, Taxa IX of the Areas tering Wards, No. 0 427-24875, adv

Item 7.

A table of the noticed citizens, counties, munipalities and tribes and to whom the notices were sent in each group.

Noticed Citizens, Counties, Municipalities, and Tribes

Eddy County: Eddy County Manager

Lea County: Lea County Manager

Bureau Of Land Management: Carlsbad Field Office (David Evans)

State of NM: Commissioner

Item 8.

A copy of the public service announcement (PSA) sent to a local radio station and documentary proof of submittal.

Activity Report

Date/Time	08-31-2020	02:53:47 p.m.	Transmit Header Text
Local ID 1	8326252631		Local Name 1

Completed Jobs : 1

No.	Job	Remote Station	Start Time	Duration	Pages	Line	Mode	Job Type	Results
001	450	VFD212M6N22	02:51:05 p.m. 08-31-2020	00:02:04	6/6	1	G3	HS	CP14400

Abbreviations: HS: Host send

HR: Host receive	
W5: Waiting send	

PL: Polled local PR: Polled remote MS: Mallbox save MP: Mallbox print RP: Report FF: Fax Forward CP: Completed FA: Fall TU: Terminated by user TS: Terminated by system G3: Group 3 EC: Error Correct Date/Time Local ID 1 08–31–2020 02:53:47 p.m. 8326252631 **Transmission Report**

Transmit Header Text Local Name 1

This document : Confirmed (reduced sample and details below) Document size : 8.5"x11"

August 31, 2020

KATK 92.1 FM (575) 887-7000

Rc: Public Service Announcement

As part of the sir quality permitting process in New Mexico, applicants for certain sir permits must attempt to provide notice to the public of the proposed permit action via public service announcement (PSA). The announcement is attached. Will you air the PSA?

Thank you.

Benjamin Schneider XTO Energy Inc. (832) 624-2768

Total Pages Scanned : 6

Total Pages Confirmed : 6

No.	Jop	Remote Station	Start Time	Duration	Pages	Line	Mode	Job Type	Results
001	450	VFD212M6N22	02:51:05 p.m. 08-31-2020	00:02:04	6/6	1	G3	HS	CP14400

Abbreviations: HS: Host send

HR: Host receive

WS: Waiting send

PL: Polled local PR: Polled remote MS: Mailbox save MP: Mailbox print RP: Report FF: Fax Forward CP: Completed FA: Fall TU: Terminated by user TS: Terminated by system G3: Group 3 EC: Error Correct

KATK 92.1 FM (575) 887-7000

Re: Public Service Announcement

As part of the air quality permitting process in New Mexico, applicants for certain air permits must attempt to provide notice to the public of the proposed permit action via public service announcement (PSA). The announcement is attached. Will you air the PSA?

Thank you.

Benjamin Schneider XTO Energy Inc. (832) 624-2768

NOTICE OF AIR QUALITY PERMIT APPLICATION

XTO Energy, Inc. announces its application to the New Mexico Environment Department for an air quality permit for the modification of the Bulldog Compressor Station. The expected date of application submittal to the Air Quality Bureau is September 4, 2020. XTO Energy Inc. is planning to remove two engines, update engine emission rates, update glycol recirculation rate, remove two heaters, and update oil/water production rates.

The exact location for the proposed facility known as the Bulldog Compressor Station will be latitude 32 deg, 33 min, 24 sec and longitude - 103 deg, 51 min, 19 sec. The approximate location of this facility is 22 miles northeast of Carlsbad in Eddy County.

The notice was posted at the facility and three other public locations: The Carlsbad post office, the Carlsbad public library, and the Hobbs post office. If you have any comments about the construction or operation of the above facility, and you want your comments to be made as part of the permit review process, you must submit your comments in writing to the address below:

Permit Programs Manager New Mexico Environment Department Air Quality Bureau 525 Camino de los Marquez, Suite 1 Santa Fe, New Mexico 87505-1816 (505) 476-4300 Item 9.

A copy of the classified or legal ad including the page header (date and newspaper title)

Affidavit of Publication
No. 25527
State of New Mexico Publisher
County of Eddy:
Danny Scott a con
being duly sworn sayes that he is the Publisher
of the Artesia Daily Press, a daily newspaper of General
circulation, published in English at Artesia, said county
and state, and that the hereto attached
Legal Ad
was published in a regular and entire issue of the said
Artesia Daily Press, a daily newspaper duly qualified
for that purpose within the meaning of Chapter 167 of
the 1937 Session Laws of the state of New Mexico for
1 Consecutive weeks/day on the same
day as follows:
First Publication August 20, 2020
Second Publication
Third Publication
Fourth Publication
Fifth Publication
Sixth Publication
Seventh Publication
Subscribed and sworn before me this
20th day of August 2020
OFFICIAL SEAL Latisha Romine NOTARY PUBLIC-STATE OF NEW MEXICO My commission expires: 5112 2023
Latisha Romine

Notary Public, Eddy County, New Mexico

Copy of Publication:

Legal Notice

NOTICE OF AIR QUALITY PERMIT APPLICATION XTO Energy, Inc. announces its application to the New Mexico Environment Department for an air quality permit for the modification of the Bulldog Compressor Station. The expected date of application submittal to the Air Quality Bureau is August 28, 2020.

The exact location for the facility known as the Bulldog Compressor Station will be latitude 32 deg, 33 min, 24 sec and longitude

-103 deg, 51 min, 19 sec. The approximate location of this facility is 22 miles northeast of Carlsbad in Eddy County.

The proposed modification consists removing two engines, updating engine emission rates, updating glycol recirculation rate, removing two heaters, and updating oil/water production rates.

The estimated maximum quantities of any regulated air contaminants will be as follows in pound per hour (pph) and tons per year (tpy). These reported emissions could change slightly during the course of the Department's review:

Pollutant:	Pounds per hour	Tons per year
Particulate		
Matter (PM)	27 pph	17 tpy
PM 10	27 pph	17 tpy
PM 2.5	27 pph	17 tpy
Sulfur Dioxide (SO2)	10 pph	20 tpy
Nitrogen Oxides (NO)	() 587 pph	206 tpy
Carbon	**	·F/
Monoxide (CO)	1130 pph	228 tpy
Volatile Organic	I WALK AND A STATE	==0 (P)
Compounds (VOC)	1113 pph	260 tpy
Total sum of all	18.18	-00 (P)
Hazardous Air Polluta	nts	
(HAPs)	35 pph	29 tpy
Toxic Air Pollutant	TI - Selected	ar cpy
(TAP)	35 pph	29 tpy
Green House Gas		as epy
Emissions as Total CO	2e n/a	240,024 tpy
10. 800 St. 1918		a rosoar thà

The standard and maximum operating schedule of the facility will be 24 hours per day, 7 days a week and a maximum of 52 weeks per year. The owner and/or operator of the Facility is: XTO Energy, Inc.; 22777 Springwoods Village Pkwy-W4.6B.347; Spring, Texas 77389.

If you have any comments about the construction or operation of this facility, and you want your comments to be made as part of the permit review process, you must submit your comments in writing to this address: Permit Programs Manager; New Mexico Environment Department; Air Quality Bureau; 525 Camino de los Marquez, Suite 1; Santa Fe, New Mexico; 87505-1816; (505) 476-4300; 1 800 224-7009; https:// www.env.nm.gov/aqb/permit/aqb_draft_permits.html. Other comments and questions may be submitted verbally.

Please refer to the company name and site name, or send a copy of this notice along with your comments, since the Department may have not yet received the permit application. Please include a legible return mailing address with your comments. Once the Department has performed a preliminary review of the application and its air quality impacts, the Department's notice will be published in the legal section of a newspaper circulated near the facility location.

General information about air quality and the permitting process can be found at the Air Quality Bureau's web site. The

Legal Notice

STATE OF NEW MEXICO COUNTY OF EDDY

FIFTH JUDICIAL DISTRICT COURT IN THE MATTER OF THE PETITION FOR NAME CHANGE OF Benjamin Flores Petitioner.

No. D-503-CV-2020-552

NOTICE OF CHANGE OF NAME NOTICE IS GIVEN as required by NMSA 1978, 40-8-1 to 40-8-3 that the Petition for Name Change of the Petitioner Benjamin Flores, shall come before the Honorable <u>Raymond</u> <u>L Romero</u>, District Judge of the Hith Judicial District, Eddy County, New Mexico at the Eddy County Courthouse, 102 N. Canal, Carlsbad, New Mexico 88220 at 1.45 pm on the 28-d dua of Sentember 2000 advect the Distinguill request and day of <u>September</u> 2020, where the Petitioner will request entry of an Order Changing Name changing the Petitioner's name from <u>Benjamin Cordell Flores to Benjamin Cordell</u> Orosco

KAREN CHRISTESSON CLERK OF THE DISTRICT COURT

/s/ Deputy Clerk/Clerk

Submitted by: Benjamin Cordell Flores

Published in the Artesia Daily Press, Artesia, N.M., Aug 13, 20 2020 Legal No. 25520.

Legal Notice

Legal Notice NOTICE OF AIR QUALITY PERMIT APPLICATION Crestwood New Mexico Pipeline LLC (Crestwood) an-nounces its application submittal to the New Mexico Envi-ronment Department for an air quality permit for the mod-ification of its gas processing facilty. The expected date of application submittal to the Air Quality Bureau is August 24 th , 2020. The exact location for the facility known as, Willow Lake Gas Processing Plant, is at 393 Higby Hole Road, Malaga, NM 88263. The approximate location of this facility is 2.7 miles southwest of Malaga, NM in Eddy County. The proposed modification consists of adding new equipment and transitioning the facility from a GCP-4 permit to a minor NSR.

NSR. NSR. The estimated maximum quantities of any regulated air con-taminant will be as follows in pound per hour (pph) and tons per year (tpy) and could change slightly during the course of the Department's review: Pollutant: Pounds per hour Tons per year

Pollutant:	Pounds per nour	Tons per year
Particulate		
Matter (PM)	3 pph	10 tpy
PM 10	3 pph	10 tpy
PM 2.5	3 pph	9 tpy
Sulfur Dioxide (SO2)	3 pph	11 tpy
Hydrogen		
Sulfide (H 2 S)	1 pph	2 tpy
Nitrogen Oxides		
(NOx)	175 pph	158 tpy
Carbon Monoxide		
(CO)	308 pph	134 tpy
Volatile Organic		
Compounds (VOC)	1977 pph	157 tpy
Total sum of all		
Hazardous Air		
Pollutants(HAPs)	67 pph	24 tpy
Toxic Air Pollutant		
(TAP)	N/A	N/A
Green House Gas		
Emissions as Total		
CO2c	N/A	120,000 tpy

The standard and maximum operating schedules of the fa-cility will be continuous 7 days a week and a maximum of weeks per year

The owner and/or operator of the Facility is:

Crestwood New Mexico Pipeline LLC 811 Main Street, Suite 3400 Houston, TX 77002

Houston, TX 77002 If you have any comments about the construction or opera-tion of this facility, and you want your comments to be made as part of the permit review process, you must submit your comments in writing to this address. Permit Programs Man-ager; New Mexico Environment Department, Air Quality Bureau, 525 Camino de los Marquez, Suite 1; Santa Fe, New Mexico; 87505-1816; (505) 476-4300; 1 800 224-7009; https://www.env.nm.gov/adp/permit/adb_draft_permits.html. Other comments and questions nay be submitted verbally.

Other comments and questions may be submitted verbally. Please refer to the company name and site name, or send a copy of this notice along with your comments, since the Department may have not yet received the permit applica-tion. Please include a legible return mailing address with your comments. Once the Department has performed a prelimi-nary review of the application and its air quality impacts, the Department's notice will be published in the legal section of a newspaper circulated near the facility location.

General information about air quality and the permitting process can be found at the Air Quality Bureau's web site. The regulation dealing with public participation in the permit review process is 20.2.72.206 NMAC. This regulation can be found in the "Permits" section of this web site.

Attención

Attención Este es un aviso de la oficina de Calidad del Aire del Depar-tamento del Medio Ambiente de Nuevo México, acerca de las emisiones producidas por un estaolecimiento en esta área. Si usted desea información en español, por favor comuniquese con esa oficina al teléfono 505 476 5557.

usted desea information en español, por lavor comuniquese con esa oficina al telébrico 505 476 5557. **Notice of Non-Discriminate** on the basis of race, color, na-tional origin, disability, age or sex in the administration of its programs or activities, as requirec by applicable laws and reg-ulations. NMED is responsible for coordination of compliance efforts and receipt of inquiries concerning non-discrimination requirements implemented by 40 C.E.R. Part 7, including Title VI of the Civil Rights Act of 1964, as amended; Section 504 of the Rchabilitation Act of 1973; the Age Discrimination Act of 1975, Title IX of the Education Amendments of 1972, and Section 13 of the Federal Water Pollution Control Act Amendments of 1972. If you have any questions about this notice or any of NMED's non-discrimination programs, policies or procedures, or if you believe that you have been discriminated against with respect to a NMED program or activity, you may contact: Kristine Yurdin, Non-Discrim-ination Coordinator, NMED, 1190 St. Francis Dr, Suite Ad050, PO. Box 5469, Santa Fe, NM 87502, (505) 827-2855, nd.coordinator@state.nm.us. You may also visit our website at https://www.env.nm.gov/non-employce-discrimination-complaint-page/ to learn how and where to file a complaint of discrimination.

Published in the Artesia Daily Press, Artesia, N.M., August 20, 2020 Legal No. 25528.

Legal Notice

STATE OF NEW MEXICO COUNTY OF EDDY

FIFTH JUDICIAL DISTRICT COURT

IN THE MATTER OF THE PETITION FOR NAME CHANGE OF Hector Flores Petitioner. No. D-503-CV-2020-552

NOTICE OF CHANGE OF V2220302 NOTICE IS GIVEN as required by NMSA 1978, 40-8-1 to 40-8-3 that the Petition for Name Change of the Petitioner Hector Flores, shall come before the Honorable Raymond L. Romero, District Judge of the Fifth Judicial District, Eddy County, New Mexico at the Eddy County Courthouse, 102 N. Canal, Carlsbad, New Mexico 8820 at 1,320 µm on the 3rd day of September 2020, where the Petitioner will request participal Development of the Development of Development name from Hector Jesus Flores to Hector Jesus Orosco

KAREN CHRISTESSON CLERK OF THE DISTRICT COURT

/s/ Deputy Clerk/Clerk

Submitted by: Hector Jesus Flores Published in the Artesia Daily Press, Artesia, N.M., Aug 13, 20 2020 Legal No. 25521.

Legal Notice

NOTICE OF AIR QUALITY PERMIT APPLICATION XTO Energy, Inc. announces its application to the New Mex-ico Environment Department for an air quality permit for the modification of the Bulldog Compressor Station. The expect-ed date of application submittal to the Air Quality Bureau is August 28, 2020.

The exact location for the facility known as the Bulldog Compressor Station will be latitude 32 deg, 33 min, 24 sec and longitude

-103 deg, 51 min, 19 sec. The approximate location of this facility is 22 miles northeast of Carlsbad in Eddy County.

The proposed modification consists removing two engines, updating engine emission rates, updating glycol recirculation rate, removing two heaters, and updating oil/water production rates.

The estimated maximum quantities of any regulated air con-taminants will be as follows in pound per hour (pph) and tons per year (pp). These reported emissions could change slightly during the course of the Department's review:

Pollutant:	Pounds per hour	Tons per year
Particulate	-	
Matter (PM)	27 pph	17 tpy
PM 10	27 pph	17 tpy
PM 2.5	27 pph	17 tpy
Sulfur Dioxide (SO2)	10 pph	20 tpy
Nitrogen Oxides (NO:	x) 587 pph	206 tpy
Carbon		
Monoxide (CO)	1130 pph	228 tpy
Volatile Organic		
Compounds (VOC)	1113 pph	260 tpy
Total sum of all		
Hazardous Air Polluta	ints	
(HAPs)	35 pph	29 tpy
Toxic Air Pollutant	••	
(TAP)	35 pph	29 tpy
Green House Gas		
Emissions as Total CC	02c n/a	240,024 tpy

Emissions as Total CO2c n/a 240,024 tpy The standard and maximum operating schedule of the facil-ity will be 24 hours per day, / days a week and a maximum of 52 weeks per year. The owner and/or operator of the Fa-cility is: XTO Energy, Inc.; 22777 Springwoods Village Pk-wy-W4.6B.347; Spring, Texas 77389. If you have any comments about the construction or opera-tion of this facility, and you want your comments to be made as part of the permit review process. You must submit your comments in writing to this address: Permit Programs Man-ager; New Mexico Environment Department: Air Quality Bureau; 525 Camino de los Marquez, Suite 1; Santa Fe, New Mexico; 87505-1816; (505) 476-4300; 1 800 224-7009; https:// ww.env.n.mgov/adb/permit/ab_c_faft_permits.hun. Other www.env.nm.gov/aqb/permit/aqb_draft_permits.html. Other comments and questions may be submitted verbally.

comments and questions may be submitted verbally. Please refer to the company name and site name, or send a copy of this notice along with your comments, since the Department may have not yet received the permit applica-tion. Please include a legible return mailing address with your comments. Once the Department has performed a prelimi-nary review of the application and its air quality impacts, the Department's notice will be published in the legal section of a newspaper circulated near the facility location. Commend information a house is in submitted on the second time.

General information about air quality and the permitting process can be found at the Air Quality Bureau's web site. The regulation dealing with public participation in the permit review process is 20.2.72.206 NMAC. This regulation can be found in the "Permits" section of this web site.

Attención

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Notice of Non-Discrimination

Notice of Non-Discrimination NMED does not discriminate on the basis of race, color, na-tional origin, disability, age or sex in the administration of its programs or activities, as required by applicable laws and reg-ulations. NMED is responsible for coordination of compliance efforts and receipt of inquiries concerning non-discrimination requirements implemented by 40 C.E.R. Part 7, including 1714 VI of Circl Disc Art of United Section 2015 Title VI of the Civil Rights Act of 1964, as amended; Section 504 of the Rehabilitation Act of 1973; the Age Discrimina-tion Act of 1975, Title IX of the Education Amendments of 1972, and Section 13 of the Federal Water Pollution Control Act Amendments of 1972. If you have any questions about this notice or any of NMED's non-discrimination programs, policies or procedures, or if you believe that you have been discriminated against with respect to a NMED program or activity, you may contact: Kristine Yurdin, Non-Discrimina-tion Coordinator, NMED, 1190 St. Francis Dr., Suite N4050, P.O. Box 5469, Santa Fe, NM 87502, (505) 827-2855, nd.conot box 5405 saila re, from 6502, 600 627-2605, indee ordinator@state.nm.us. You may also visit our website at https://www.env.nm.gov/non-employce-discrimination-cc plaint-page/ to learn how and where to file a complaint of discrimination.

Published in the Artesia Daily Press, Artesia, N.M., August 20, 2020 Legal No. 25527.

The Artesia (NM) Daily Press - Aug. 20, 2020-Page 11

Legal Notice FIFTH JUDICIAL DISTRICT COURT

COUNTY OF EDDY STATE OF NEW MEXICO

IN THE MATTER OF THE ESTATE OF No. D-503-PB-2020-00036 CECILIA ANN B. CHENEY, Deceased.

AMENDED NOTICE OF HEARING ON PETITION FOR PETITION FOR ADJUDICATION OF INTESTACY AND DETERMINATION OF HEIRS

TO: Unknown heirs of C3CILIA ANN B. CHENEY, deceased, and all unknown persons who have or claim any interest in the estate of CECLIA ANN B. CHENEY, deceased ("Decedent")

NOTICE IS HEREBY GIVEN that Frank Harry Chency has filed with the above-named Court a Petition for Adjudication of Intestacy and Determination of Heirs, which requests the Court to enter an Order that determines Dece-dent died intestate; determines the heirs of Decedent; and

Provides for such other and further relief as may be proper. Hearing has been set to consider the Petition at 1:30 p.m. on September 28, 2020, at the Eddy County Courthouse, Carlsbad, New Mexico, Defore the Learning Romero, District Judge. The attorneys for Petitioner are Holloman Law, LLC, P. O. Box 3408, Hobbs, New Mexico 88241-3408. HOLLOMAN LAW, LLC Dated August 18, 2020 By: Is/Scotty Holloman SCOTTY HOLLOMAN Carlsbad, New Mexico, before the Honorable Raymond L.

Attorneys for Petitioner P. O. Box 3408 Hobbs, New Mexico 88241-340 575/441-0056 scotty.holloman@outlook.com

Published in the Artesia Daily Press, Artesia, N.M., August 20, 27, September 3, 2020 Legal No. 25530.

Legal Notice

FIFTH JUDICIAL DISTRICT COURT COUNTY OF EDDY STATE OF NEW MEXICO

IN THE MATTER OF THE ESTATE

OF No. D-503-PB-2019-00095 PHOEBE JANE WELCH, Deceased. NOTICE OF HEARING ON PETITION FOR PETITION FOR ADJUDICATION OF INTESTACY AND DETERMI-NATION OF HEIRS

TO: Unknown heirs of PHOEBE JANE WELCH, deceased, and all unknown persons who have or claim any interest in the estate of PHOEBE JANE WELCH, deceased ("Decedent")

NOTICE IS HEREBY GIVEN that Michael I. Welch

NOTICE IS TREAD OF VERY that Principles 1. Needs has filed with the above-named Court a Petition for Adjudica-tion of Intestacy and Determination of Heirs, which requests the Court to enter an Order that determines Decedent died intestate; determines the heirs of Decedent; and provides for

Heating, declining the heat of Decembra and protect of such other and further relief as may be proper. Hearing has been set to consider the Petition at 9:30 a. m. on September 28, 2020, at the Eddy County Courthouse, Carlsbad, New Mexico, before the Honorable Jane Shul-

Carlsbad, New Mexico, Vector er-Gray, District Judge. The attorneys for Petitioner are Holloman Law, LLC, P. O. Box 3408, Hobbs, New Mexico 88241-3408. HOLLOMAN LAW, LLC Prov. JeffContry Holloman

Dated August 18, 2020

<u>By: /s/Scotty Holloman</u> SCOTTY HOLLOMAN

Attorneys for Petitioner P. O. Box 3408 Hobbs, New Mexico 88241-3408 575/441-0056

scotty.holloman@outlook.com

Published in the Artesia Daily Press, Artesia, N.M., August 20, 27, September 3, 2020 Legal No. 25529.

Legal Notice

NOTICE OF PUBLIC HEARING AND REQUEST FOR PUBLIC COMMENTS ON THE

STATE OF NEW MEXICO LOW INCOME HOUSING TAX CREDIT QUALIFIED ALLOCATION PLAN EFFECTIVE FOR 2021

The New Mexico Mortgage Finance Authority (MFA), as the designated Housing Credit Agency for the state of New Mex-ico, is responsible for administering the Low Income Hous-ing Tax Credit Program and allocating tax credits to eligible low-income housing projects. MFA will make allocations of tax credits pursuant to a Qualified Allocation Plan which: 1.) sets forth selection criteria to be used to determine housing priorities appropriate to local conditions; 2.) gives preference in allocating Housing credit dollar amounts among selected projects to: a.) projects serving the lowest income tenants; b.) projects obligated to serve qualified tenants for the longest periods; and 3.) provides a procedure that MFA will use in monitoring for noncompliance. monitoring for noncompliance.

This notice is to advise that the draft Low Income Housing Tax Credit Qualified Allocation Plan effective for 2021 will be available for review and download (both a clean version and a redline comparison version to the 2020 QAP) on August 17, 2020 from the MFA website at www.housingpm.org/develop-ers/low-income-housing-tax-credits-lihte. The 21-day public comment period begins on August 17, 2020 and continues through 5:00 p.m. on September 8, 2020.

Written comments on the Draft Qualified Allocation Plan may be delivered by email, mail, by courier service or by hand to MFA at the following address:

MFA MrA Attn: Kathryn Turner 344 4.h Street SW Albuquerque, NM 87102 kturner@housingnm.org

Comments may also be made verbally at the following web-based public hearing:

September 2, 2020 from 1:30 p.m. to 3:00 p.m. Register for free for the virtual hearing by visiting www.hous-ingnm.org/developers

If you would like additional information, please contact Kath-ryn Turner at kturner@housingnm.org or 505.843.6880.

Published in the Artesia Daily Press, Artesia, N.M., August 20, 2020 Legal No. 25523.

Item 10.

A copy of the display ad including the page header (date and newspaper title) or its affidavit of publication stating the ad date, and a copy of the ad.

Affidavit of Publication				
No.				
State of New Mexico Publisher				
County of Eddy:				
Danny Scott & any A Ca				
being duly sworn sayes that he is the Publisher				
of the Artesia Daily Press, a daily newspaper of General				
circulation, published in English at Artesia, said county				
and state, and that the hereto attached				
Display Ad				
was published in a regular and entire issue of the said				
Artesia Daily Press, a daily newspaper duly qualified				
for that purpose within the meaning of Chapter 167 of				
the 1937 Session Laws of the state of New Mexico for				
Consecutive weeks/day on the same				
day as follows:				
First Publication August 20, 2020				
Second Publication				
Third Publication				
Fourth Publication				
Fifth Publication				
Sixth Publication				
Seventh Publication				
Subscribed and sworn before me this				
20th day of August 2020				
OFFICIAL SEAL Latisha Romine NOTARY PUBLIC-STATE OF NEW MEXICO My commission expires: 5/12/2023				
0				
Late O'				
(attisto 140mine				
Latisha Romine				

Notary Public, Eddy County, New Mexico

Copy of Publication:

NOTICE OF AIR QUALITY PERMIT APPLICATION XTO Energy, Inc. announces its application to the New Mexico Environment Department for an air quality permit for the modification of the Bulldog Compressor Station. The expected date of application submittal to the Air Quality Bureau is August 28, 2020.

The exact location for the facility known as the Bulldog Compressor Station will be latitude 32 deg, 33 min, 24 sec and longitude

-103 deg, 51 min, 19 sec. The approximate location of this facility is 22 miles northeast of Carlsbad in Eddy County.

The proposed modification consists removing two engines, updating engine emission rates, updating glycol recirculation rate, removing two heaters, and updating oil/water production rates.

The estimated maximum quantities of any regulated air contaminants will be as follows in pound per hour (pph) and tons per year (tpy). These reported emissions could change slightly during the course of the Department's review:

Pollutant:	Pounds per hour	Tons per year
Particulate	175 pph	* *
Matter (PM)	27 pph	17 tpy
PM 10	27 pph	17 tpy
PM 2.5	27 pph	17 tpy
Sulfur Dioxide (SO2)	10 pph	20 tpy
Nitrogen Oxides (NOx Carbon		206 tpy
Monoxide (CO) Volatile Organic	1130 pph	228 tpy
Compounds (VOC) Total sum of all	1113 pph	260 tpy
Hazardous Air Polluta	nts	
(HAPs) Toxic Air Pollutant	35 pph	29 tpy
(TAP)	35 pph	29 tpy
Green House Gas		1987 199 285
Emissions as Total CO	2e n/a	240,024 tpy
	A REAL PROPERTY AND A REAL PROPERTY.	

The standard and maximum operating schedule of the facility will be 24 hours per day, 7 days a week and a maximum of 52 weeks per year. The owner and/or operator of the Facility is: XTO Energy, Inc.; 22777 Springwoods Village Pkwy-W4.6B.347; Spring, Texas 77389.

If you have any comments about the construction or operation of this facility, and you want your comments to be made as part of the permit review process, you must submit your comments in writing to this address: Permit Programs Manager; New Mexico Environment Department; Air Quality Bureau; 525 Camino de los Marquez, Suite 1; Santa Fe, New Mexico; 87505-1816; (505) 476-4300; 1 800 224-7009; https://www.env.nm.gov/aqb/permit/aqb_draft_permits. html. Other comments and questions may be submitted verbally.

Please refer to the company name and site name, or send a copy of this notice along with your comments, since the Department may have not yet received the permit application. Please include a legible return mailing address with your comments. Once the Department has performed a preliminary review of the application and its air quality impacts, the Department's notice will be published in the legal section of a newspaper circulated near the facility location.

General information about air quality and the permitting process can be found at the Air Quality Bureau's web site. The regulation dealing with public participation in the per-

Obituaries

Dwaine Howard

Graveside services are scheduled for 10 a.m. Wednesday, Aug. 19, at Woodbine Cemetery for Truman Dwaine Howard of Roswell.

Howard, 82, passed away Thursday, Aug. 13, 2020, at his home.

Wayne Derrick will officiate the services.

Dwaine was born Feb. 14, 1938, in Cottonwood to Truman Wesley and Minnie Opal (Parker) Howard. He came to Artesia in 1938.

On May 12, 1955, he married Evelyn Savoie.

Survivors include his wife, Evelyn Howard, of Roswell; daughters Debra Carre and husband Ronnie of Loco Hills, Dwanna Casabonne and husband Mike of Hope, Susan Kinnibrugh and husband Arvin of Artesia, and Brenda Howard of Lubbock, Texas; sister Rita Butts of San Antonio, Texas; grandchildren Jimmy Masters of Roswell, Kami Horton of Farmersville, Texas, Kellen Casabonne of Hope, Toby Kinnibrugh of Albuquerque, Cody Kinnibrugh of Artesia, and Amber Tumbleson of Lubbock; and six great-grandchildren.

He was preceded in death by his parents, Truman and Minnie Opal Howard; stepmother Pam Howard; Monroe and Elizabeth Howard; H.V. and Carrie Parker; Linda Ellington; and Jim and Kevin Masters.

Arrangements are under the direction of Terpening & Son Mortuary. Condolences may be expressed online at www.artesiafunerals.com.



Curtis Allen Jr.

Graveside services were held Tuesday, Aug. 18, at Resthaven Cemetery in Lovington for Curtis Allen Jr. of Artesia.

ARTESIA POLICE DEPARTMENT Aug. 19

SUSPICIOUS ACTIVITY 2 a.m. - Officer dispatched to the 300 block of West Gage Avenue in reference to suspicious activity.

2:17 a.m. - Officer dispatched to the 300 block of West Gage Avenue in reference to suspicious activity.

2:38 a.m. - Officer dispatched to the 900 block of South Sixth Street in reference to suspicious activity.

DISTURBANCE

2:38 a.m. - Officer dispatched to the 700 block of North 14th Street in reference to a disturbance.

BREAKING AND ENTERING

3:25 a.m. - Officer dispatched to 702 N. 14th St. in reference to breaking and entering. ACCIDENT

6:18 a.m. - Officer dispatched to 13th and Main streets in reference to a motor vehicle accident.

Aug. 18 ARREST

2:45 p.m. - Judy Ann Carrillo, 50, of Artesia, arrested on two district warrants for failure to comply.

LOUD NOISE

2:10 a.m. - Officer dispatched to the 2500 block of West Bullock Avenue in reference to loud noise.

BATTERY

2:11 a.m. - Officer dispatched to the 900 block of North Sixth Street in reference to battery.

ALARM

4:52 a.m. - Officer dispatched to AFS Energy Services in reference to an alarm.

6:42 a.m. - Officer dispatched to 105 E. Castleberry Road in reference to an alarm.

VANDALISM

9:19 a.m. - Officer dispatched to 402 W. Main St. in reference to vandalism.

SUSPICIOUS ACTIVITY

9:59 a.m. - Officer dispatched to the 1300 block of West Merchant Avenue in reference to suspicious activity.

10:03 a.m. - Officer dispatched to Bowman and JJ Clarke drives in reference to suspicious activity.

FRAUD

patched to 1117 S. Fourth St. in erence to vandalism.

on a magistrate warrant for failure to appear.

7:17 p.m. - Josiah Daniel Olguin, 23, of Artesia, arrested on a magistrate warrant for failure to pay fines.

7:56 p.m. - Robert Paul Martinez, 37, of El Paso, Texas, arrested and charged with battery upon a peace officer.

SUSPICIOUS ACTIVITY 1:10 a.m. - Officer dispatched to the 300 block of West Gage Avenue in reference to suspicious activity.

BURGLARY

8:13 a.m. - Officer dispatched to 308 McArthur Ave. in reference to burglary

LITTERING

9:25 a.m. - Officer dispatched to the 400 block of West Cleveland Avenue in reference to littering.

ALARM

9:37 a.m. - Officer dispatched to 612 N. 14th St. in reference to an alarm.

ACCIDENT

10:39 a.m. - Officer dispatched to Roselawn and Dallas avenues in reference to a motor vehicle accident.

THREATS

11:33 a.m. - Officer dispatched to the 1900 block of West Grand Avenue in reference to threats.

SUSPICIOUS ACTIVITY 11:48 a.m. - Officer dispatched to the 2300 block of West Mann Avenue in reference to suspicious activity.

FIREWORKS

12:03 p.m. - Officer dispatched to the Abo Apartments, Bldg. G, in reference to fireworks.

HARASSMENT

12:57 p.m. - Officer dispatched to the 2400 block of Sierra Vista Road in reference to harassment.

FRAUD

1:32 p.m. - Officer dispatched to Artesia Credit Union in reference to fraud.

ALARM

2:05 p.m. - Officer dispatched to 1301 S. 23rd St. in reference to an alarm BATTERY

4:47 p.m. - Officer dispatched to Wal-Mart in reference to battery.

VANDALISM

5:05 p.m. - Officer dispatched 12:02 p.m. - Officer dis- to 405 W. Cleveland Ave. in ref-

Public Record

to suspicious activity.

ence to fraud.

9:43 p.m. - Officer dispatched

to the 1300 block of West Hermosa Drive in reference to suspicious activity.

FRAUD

9:43 p.m. - Officer dispatched to 705 W. Lolita Ave. in refer-

DISTURBANCE

9:58 p.m. - Officer dispatched to South Ninth Street and West Centre Avenue in reference to a disturbance.

SUSPICIOUS ACTIVITY 11:08 p.m. - Officer dis-patched to the 300 block of

Aug. 16

ARRESTS

12:53 a.m. - Gabriel Alexander Norman, 19, of Greensboro,

N.C., arrested and charged with

two counts of battery upon a

peace officer, aggravated DWI,

battery, assault, and resisting,

evading or obstructing an offi-

Huertas, 22, of Artesia, arrest-

ed and charged with aggravated

DWI, unlawful use of a license,

seatbelts required, reckless

driving, and proof of insurance

8:49 a.m. - Bret Harden, 28,

of Artesia, arrested on a magis-

trate warrant for failure to pay

DOMESTIC

12:16 a.m. - Officer dis-

patched to the 2100 block of

Currier Avenue in reference to

DWI

12:25 a.m. - Officer dis-

patched to the 1800 block of

Currier Avenue in reference to

ACCIDENT

1:40 a.m. - Officer dispatched

to the 1000 block of West Bull-

ock Avenue in reference to a

SUSPICIOUS ACTIVITY

2:27 a.m. - Officer dispatched

2:39 a.m. - Officer dispatched

to the Comfort Inn & Suites in

reference to suspicious activity.

to the 300 block of West Gage

Avenue in reference to suspi-

BREAKING AND

ENTERING

3:12 a.m. - Officer dispatched

SUSPICIOUS ACTIVITY

3:40 a.m. - Officer dispatched

to 306 W. Gage Ave. in refer-

ence to breaking and entering.

motor vehicle accident.

cious activity.

a domestic dispute.

to suspicious activity.

cer.

required.

fines.

DWI.

West Gage Avenue in reference reference to a wanted subject.

HAZARD

8:46 p.m. - Officer dispatched to the Abo Apartments in reference to a hazard.

DOMESTIC

9:11 p.m. - Officer dispatched to the 1000 block of South Sixth Street in reference to a domestic dispute.

4:46 a.m. - Adrian Roman

3:05 a.m. - Garrett Frazier, 18, of Jal, arrested and charged

LIVESTOCK

2:22 p.m. - Officer dispatched to the 1300 block of West Dallas Avenue in reference to livestock in the roadway.

12:11 a.m. - Officer dis-

patched to the 1800 block of

West Centre Avenue in refer-

ALARM

LOUD NOISE

12:33 a.m. - Officer dis-

patched to the 1800 block of

West Centre Avenue in refer-

1:01 a.m. - Officer dispatched

THREATS

1:17 a.m. - Officer dispatched

to the 1800 block of West

Centre Avenue in reference to

DISTURBANCE

1:22 a.m. - Officer dispatched

ACCIDENT

1:51 a.m. - Officer dispatched

to North Eighth Street and West

Cannon Avenue in reference to

SUSPICIOUS ACTIVITY

3:03 a.m. - Officer dispatched

Tons per year

17 tpy

17 tpy

17 tpy

20 tpy

206 tpy

228 tpy

to the 300 block of West Gage

Avenue in reference to suspi-

a motor vehicle accident.

to the 500 block of North Sev-

enth Street in reference to a dis-

to the 1800 block of West Cen-

tre Avenue in reference to loud

12:30 a.m. - Officer dispatched to 909 S. Second St. in

ence to loud noise.

reference to an alarm.

ence to loud noise.

noise.

threats.

turbance.

OPEN DOOR

5:39 p.m. - Officer dispatched to Redline Fitness in reference to an open door.

DOMESTIC

5:44 p.m. - Officer dispatched to the 1400 block of West Yucca Avenue in reference to a domestic dispute.

WANTED SUBJECT

8:38 p.m. - Officer dispatched to the Public Safety Complex in

11:41 p.m. - Officer dispatched to the Abo Apartments in reference to a domestic dispute.

Aug. 15 ARREST

with unlawful use of a license.

tion rates.

Pollutant:

PM 10

PM 2.5

Carbon

Particulate

Matter (PM)

Sulfur Dioxide (SO2)

Monoxide (CO)

Nitrogen Oxides (NOx) 587 pph

cious activity. LOUD NOISE NOTICE OF AIR OUALITY PERMIT APPLICATION XTO Energy, Inc. announces its application to the New

Mexico Environment Department for an air quality permit for the modification of the Bulldog Compressor Station. The expected date of application submittal to the Air Quality Bureau is August 28, 2020.

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The proposed modification consists removing two engines,

rate, removing two heaters, and updating oil/water produc-

The estimated maximum quantities of any regulated air

slightly during the course of the Department's review:

updating engine emission rates, updating glycol recirculation

contaminants will be as follows in pound per hour (pph) and

Pounds per hour

27 pph

27 pph

27 pph

10 pph

1130 pph

tons per year (tpy). These reported emissions could change

Allen, 77, passed away Thursday, Aug. 13, 2020, in Artesia. He was born June 28, 1943, in Lamesa, Texas, to Curtis and Ruth Allen.

Curtis spent his life in the oil and gas industry, working for Fina, Marbob and Concho. He loved to hunt and fish. He was a loving husband, father and grandfather.

Survivors include his wife, Marilyn Allen, of the home; sons Kevin Allen and wife Pam, and Shane Allen, both of Midland, Texas; daughters Christy McDonald of Hamilton, Texas, and Dallas Landreville and husband Chris of Fort Worth, Texas; stepson David Bonds and wife Donna of Lovington; 10 grandchildren; and six great-grandchildren.

He was preceded in death by his parents.

Arrangements are under the direction of Kirby Ratliff Funeral Home of Lovington.

Bush

reference to fraud. ACCIDENT

12:41 p.m. - Officer dispatched to the 200 block of North Fourth Street in reference to a motor vehicle accident.

SUSPICIOUS ACTIVITY 12:42 p.m. - Officer dis-

patched to the 900 block of North Sixth Street in reference to suspicious activity. ACCIDENT

3:13 p.m. - Officer dispatched to fourth and Main streets in reference to a motor vehicle accident.

DOMESTIC

4:57 p.m. - Officer dispatched to South 28th Street and West Richardson Avenue in reference to a domestic dispute.

SHOTS FIRED

9:16 p.m. - Officer dispatched to the 2800 block of West Main Street in reference to shots fired in the area.

Aug. 17

ARRESTS 6:43 p.m. - Jaclyn Danielle Roark, 19, of Artesia, arrested

(Continued from Page 1)

Benjamin Valenzuela, 33, of Artesia, was arrested Aug. 4 for his involvement in the shooting in the 500 block of Bush Avenue. Valenzuela allegedly made contact with a male subject, asking to speak to the man's son. When the man advised his son was not home, the criminal complaint states, Valenzuela retrieved a firearm from a vehicle and fired three shots at the door.

His amended APD charges also include attempted murder in the first degree and conspiracy to commit first-degree murder.

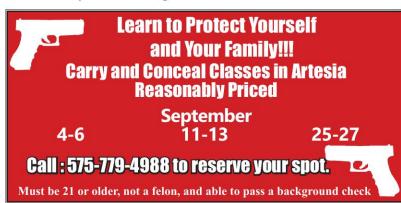
Nava, according to the report, drove Valenzuela to Bush Avenue and observed him shooting at the residence after speaking with the occupant. The complaint states that Nava then drove to Cleveland Avenue, where he exited the vehicle. Valenzuela told investigators that Nava had instructed him to shoot the Bush Avenue victim's son.

After leaving Cleveland Avenue without Nava, Valenzuela is al-leged to have proceeded to the Morningside area and executed a drive-by shooting around Oak Street and Avenue A. He was origi-nally charged with two counts of aggravated assault with a deadly weapon, being a felon in possession of a firearm, and tampering with evidence in connection with that incident

with evidence in connection with that incident. The ECSO reported this week that, following further investiga-tion, charges had been updated to also include attempted murder

in the first degree, conspiracy to commit attempted murder in the first degree, and criminal damage to property. Valenzuela is scheduled to appear before Judge Jimmy C. Fos-ter for preliminary examination in Artesia Magistrate at 9 a.m. Wednesday, Aug. 26.

Nava has yet to be arraigned.



WANTED SUBJECT 5:07 p.m. - Officer dispatched

to Wal-Mart in reference to a wanted subject.

ALARM

5:23 p.m. - Officer dispatched to City Hall in reference to an alarm.

BATTERY

5:29 p.m. - Officer dispatched to the Abo Apartments, Bldg. I, in reference to battery. SUSPICIOUS ACTIVITY

6:36 p.m. - Officer dispatched to Clayton Court in reference to suspicious activity.

8:13 p.m. - Officer dispatched to the 1800 block of West Sears Avenue in reference to suspicious activity.

UNWANTED SUBJECT

8:32 p.m. - Officer dispatched to Fenn's Country Market in reference to an unwanted subject.

SUSPICIOUS ACTIVITY 8:44 p.m. - Officer dispatched to the 1500 block of West Hermosa Drive in reference to suspicious activity.

9:08 p.m. - Officer dispatched to the 1000 block of South Roselawn Avenue in reference

to the 300 block of West Gage Avenue in reference to suspicious activity.

GRAFFITI 9:53 a.m. - Officer dispatched

to Allsup's, 800 S. First St., in reference to graffiti.

HAZARD 10:13 a.m. - Officer dis-

West Centre Avenue in reference to a hazard.

patched to the 700 block of

FRAUD

12:37 p.m. - Officer dis-patched to 1102 Cannon Court in reference to fraud. SUSPICIOUS ACTIVITY 1:06 p.m. - Officer dispatched to the Public Safety Complex in reference to suspicious activity.

HAZARD

1:25 p.m. - Officer dispatched to South First Street and West Quay Avenue in reference to a hazard.

1:53 p.m. - Officer dispatched to the 1900 block of West Main Street in reference to a hazard. GRAFFITI

2:19 p.m. - Officer dispatched to the Dr. Martin Luther King Jr. Recreational Complex in reference to graffiti.

Nonstop Flights to Houston Denver Returning Soon!

NO QUARANTINE FOR ESSENTIAL BUSINESS TRAVEL



Volatile Organic	63 53	12.5
Compounds (VOC)	1113 pph	260 tpy
Total sum of all		17
Hazardous Air Polluta	ints	
(HAPs)	35 pph	29 tpy
Toxic Air Pollutant		17
(TAP)	35 pph	29 tpy
Green House Gas		17

Emissions as Total CO2e n/a 240,024 tpy

The standard and maximum operating schedule of the facility will be 24 hours per day, 7 days a week and a maximum of 52 weeks per year. The owner and/or operator of the Facility is: XTO Energy, Inc.; 22777 Springwoods Village Pkwy-W4.6B.347; Spring, Texas 77389.

If you have any comments about the construction or operation of this facility, and you want your comments to be made as part of the permit review process, you must submit your comments in writing to this address: Permit Programs Manager; New Mexico Environment Department; Air Quality Bureau; 525 Camino de los Marquez, Suite 1; Santa Fe, New Mexico; 87505-1816; (505) 476-4300; 1 800 224-7009; https://www.env.nm.gov/aqb/permit/aqb_draft_permits. html. Other comments and questions may be submitted verbally.

Please refer to the company name and site name, or send a copy of this notice along with your comments, since the Department may have not yet received the permit application. Please include a legible return mailing address with your comments. Once the Department has performed a preliminary review of the application and its air quality impacts, the Department's notice will be published in the legal section of a newspaper circulated near the facility location.

General information about air quality and the permitting process can be found at the Air Quality Bureau's web site. The regulation dealing with public participation in the permit review process is 20.2.72.206 NMAC. This regulation can be found in the "Permits" section of this web site.

Attención

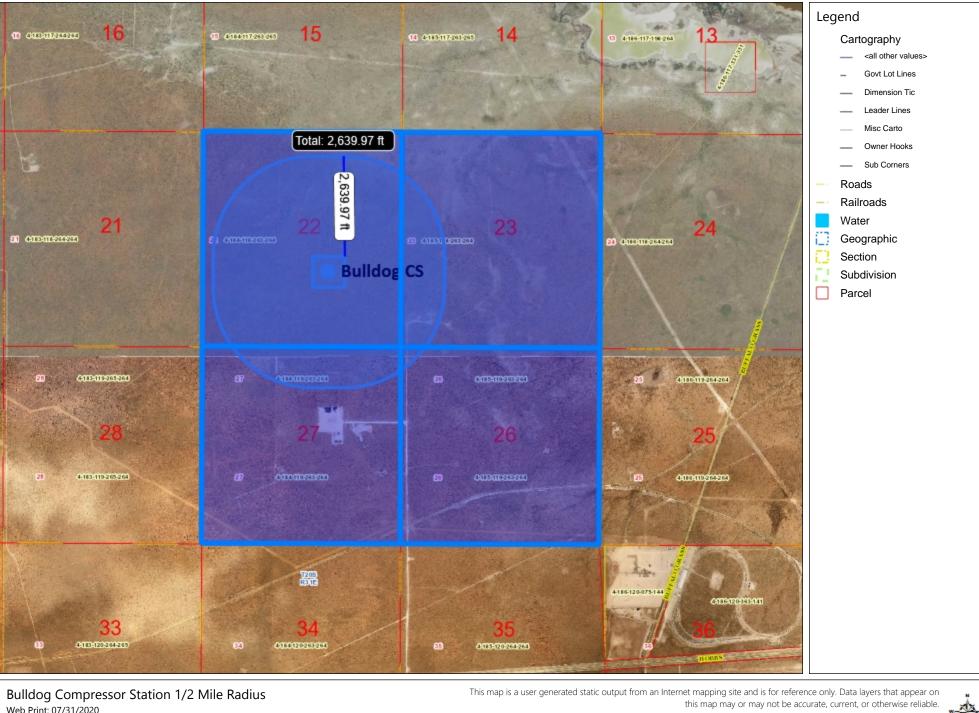
Este es un aviso de la oficina de Calidad del Aire del Departamento del Medio Ambiente de Nuevo México, acerca de las emisiones producidas por un establecimiento en esta área. Si usted desea información en español, por favor comuníquese con esa oficina al teléfono 505-476-5557.

Notice of Non-Discrimination

NMED does not discriminate on the basis of race, color, national origin, disability, age or sex in the administration of its programs or activities, as required by applicable laws and regulations. NMED is responsible for coordination of compliance efforts and receipt of inquiries concerning non-discrimination requirements implemented by 40 C.F.R. Part 7, including Title VI of the Civil Rights Act of 1964, as amended; Section 504 of the Rehabilitation Act of 1973; the Age Discrimination Act of 1975, Title IX of the Education Amendments of 1972, and Section 13 of the Federal Water Pollution Control Act Amendments of 1972. If you have any questions about this notice or any of NMED's non-discrimination programs, policies or procedures, or if you believe that you have been discriminated against with respect to a NMED program or activity, you may contact: Kristine Yurdin, Non-Discrimination Coordinator, NMED, 1190 St. Francis Dr., Suite N4050, P.O. Box 5469, Santa Fe, NM 87502, (505) 827-2855, nd.coordinator@state.nm.us. You may also visit our website at https://www.env.nm.gov/non-employee-discrimination-complaint-page/ to learn how and where to file a complaint of discrimination.

ltem 11.

A map with a graphic scale showing the facility boundary and the surrounding area in which owners of record were notified by mail.



Web Hinte 0	1/51/2020	
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Feet

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Tab 10

Section 10 - Written Description of the Routine Operations of the Facility

Written Description of the Routine Operations of the Facility

<u>A written description of the routine operations of the facility</u>. Include a description of how each piece of equipment will be operated, how controls will be used, and the fate of both the products and waste generated. For modifications and/or revisions, explain how the changes will affect the existing process. In a separate paragraph describe the major process bottlenecks that limit production. The purpose of this description is to provide sufficient information about plant operations for the permit writer to determine appropriate emission sources.

Field gas flows into two inlet slug catchers. The site uses natural gas engines to compress the field gas to 1200-1300 psig, including nine (9) Caterpillar 3616TA engines (ENG1-ENG9) and two (2) Caterpillar 3516J engines (ENG11-ENG12). The Caterpillar engines are equipped with oxidation catalysts to reduce CO, VOC, and formaldehyde emissions.

The high-pressure gas is then dehydrated using triethylene glycol dehydration units (DEHY1-DEHY3), each handling up to 80 MMscfd each. The systems are equipped with flash tanks and condensers. Flash tank vapors are recycled in the dehydration system. The glycol still vent vapors are routed to condensers. Uncondensed vapors are controlled by the vapor combustor (VC1). Dehydrated gas is then transferred to a sales pipeline.

Low pressure liquids generated anywhere in the system are routed to a low pressure three phase separator (LPS). Vapors from the LPS are controlled by a VRU and routed to compression. When the LPS VRU is not operational, vapors from the LPS are routed to the flare system (FL1/FL2). From the LPS, oil at approximately 15 psig is dumped to four (4) oil storage tanks (OT1-OT4), which are controlled by the flare system (FL1/FL2). Water from the LPS flows to redundant skim tanks (SKT1/SKT2). The skim tanks are arranged as a redundant system in which one unit can be used if another is down for unforeseen circumstances. Water is then dumped to two (2) water tanks (WT1-WT2).

Any residual oil flows from the skim tanks into the oil storage tanks. The oil from the oil storage tanks are then pumped back into the high pressure three phase separator (HPS), to be transferred offsite via pipeline. Vapors from the water storage tanks and skim tanks are also controlled by the flare system (FL1/FL2). Oil can be trucked offsite or pumped offsite via pipeline, water is transferred offsite via pipeline to saltwater disposal (SWD).

High pressure liquids generated anywhere in the system are routed to high pressure three phase separator (HPS). Vapors from the high pressure separator are routed back to the inlet slug catchers. From the HPS, liquid hydrocarbons at approximately 400 psig are transferred offsite via pipeline pipeline. Water from the HPS is transferred offsite via pipeline to SWD.

The flare system (FL1/FL2) is also used to flare gas in the event of an emergency.

Tab 11 Section 11 -Source Determination

Source Determination

Source submitting under 20.2.70, 20.2.72, 20.2.73, and 20.2.74 NMAC

Sources applying for a construction permit, PSD permit, or operating permit shall evaluate surrounding and/or associated sources (including those sources directly connected to this source for business reasons) and complete this section. Responses to the following questions shall be consistent with the Air Quality Bureau's permitting guidance, <u>Single Source Determination Guidance</u>, which may be found on the Applications Page in the Permitting Section of the Air Quality Bureau website.

Typically, buildings, structures, installations, or facilities that have the same SIC code, that are under common ownership or control, and that are contiguous or adjacent constitute a single stationary source for 20.2.70, 20.2.72, 20.2.73, and 20.2.74 NMAC applicability purposes. Submission of your analysis of these factors in support of the responses below is optional, unless requested by NMED.

A. Identify the emission sources evaluated in this section (list and describe): See Table 2A

B. Apply the 3 criteria for determining a single source:

<u>SIC</u> <u>Code</u>: Surrounding or associated sources belong to the same 2-digit industrial grouping (2-digit SIC code) as this facility, <u>OR</u> surrounding or associated sources that belong to different 2-digit SIC codes are support facilities for this source.

☑ Yes □ No

<u>Common</u> <u>Ownership</u> or <u>Control</u>: Surrounding or associated sources are under common ownership or control as this source.

☑ Yes □ No

<u>Contiguous</u> or <u>Adjacent</u>: Surrounding or associated sources are contiguous or adjacent with this source.

☑ Yes □ No

C. Make a determination:

- ☑ The source, as described in this application, constitutes the entire source for 20.2.70, 20.2.72, 20.2.73, or 20.2.74 NMAC applicability purposes. If in "A" above you evaluated only the source that is the subject of this application, all "YES" boxes should be checked. If in "A" above you evaluated other sources as well, you must check AT LEAST ONE of the boxes "NO" to conclude that the source, as described in the application, is the entire source for 20.2.70, 20.2.72, 20.2.73, and 20.2.74 NMAC applicability purposes.
- □ The source, as described in this application, <u>does not</u> constitute the entire source for 20.2.70, 20.2.72, 20.2.73, or 20.2.74 NMAC applicability purposes (A permit may be issued for a portion of a source). The entire source consists of the following facilities or emissions sources (list and describe):

Tab 12

Section 12 - PSD Applicability Determination for All Sources

Section 12.A PSD Applicability Determination for All Sources

(Submitting under 20.2.72, 20.2.74 NMAC)

A PSD applicability determination for all sources. For sources applying for a significant permit revision, apply the applicable requirements of 20.2.74.AG and 20.2.74.200 NMAC and to determine whether this facility is a major or minor PSD source, and whether this modification is a major or a minor PSD modification. It may be helpful to refer to the procedures for Determining the Net Emissions Change at a Source as specified by Table A-5 (Page A.45) of the EPA New Source Review Workshop Manual to determine if the revision is subject to PSD review.

- A. This facility is:
 - **a** minor PSD source before and after this modification (if so, delete C and D below).
 - $\hfill\square$ a major PSD source before this modification. This modification will make this a PSD minor source.
 - □ an existing PSD Major Source that has never had a major modification requiring a BACT analysis.
 - □ an existing PSD Major Source that has had a major modification requiring a BACT analysis
 - □ a new PSD Major Source after this modification.

Tab 13

Section 13 - Determination of State & Federal Air Quality Regulations

Determination of State & Federal Air Quality Regulations

This section lists each state and federal air quality regulation that may apply to your facility and/or equipment that are stationary sources of regulated air pollutants.

Not all state and federal air quality regulations are included in this list. Go to the Code of Federal Regulations (CFR) or to the Air Quality Bureau's regulation page to see the full set of air quality regulations.

Required Information for Specific Equipment:

For regulations that apply to specific source types, in the 'Justification' column **provide any information needed to determine if the regulation does or does not apply**. For example, to determine if emissions standards at 40 CFR 60, Subpart IIII apply to your three identical stationary engines, we need to know the construction date as defined in that regulation; the manufacturer date; the date of reconstruction or modification, if any; if they are or are not fire pump engines; if they are or are not emergency engines as defined in that regulation; their site ratings; and the cylinder displacement.

Required Information for Regulations that Apply to the Entire Facility:

See instructions in the 'Justification' column for the information that is needed to determine if an 'Entire Facility' type of regulation applies (e.g. 20.2.70 or 20.2.73 NMAC).

Regulatory Citations for Regulations That Do Not, but Could Apply:

If there is a state or federal air quality regulation that does not apply, but you have a piece of equipment in a source category for which a regulation has been promulgated, you must **provide the low level regulatory citation showing why your piece of equipment is not subject to or exempt from the regulation. For example** if you have a stationary internal combustion engine that is not subject to 40 CFR 63, Subpart ZZZZ because it is an existing 2 stroke lean burn stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions, your citation would be 40 CFR 63.6590(b)(3)(i). We don't want a discussion of every non-applicable regulation, but if it is possible a regulation could apply, explain why it does not. For example, if your facility is a power plant, you do not need to include a citation to show that 40 CFR 60, Subpart OOO does not apply to your non-existent rock crusher.

Regulatory Citations for Emission Standards:

For each unit that is subject to an emission standard in a source specific regulation, such as 40 CFR 60, Subpart OOO or 40 CFR 63, Subpart HH, include the low level regulatory citation of that emission standard. Emission standards can be numerical emission limits, work practice standards, or other requirements such as maintenance. Here are examples: a glycol dehydrator is subject to the general standards at 63.764C(1)(i) through (iii); an engine is subject to 63.6601, Tables 2a and 2b; a crusher is subject to 60.672(b), Table 3 and all transfer points are subject to 60.672(e)(1)

Federally Enforceable Conditions:

All federal regulations are federally enforceable. All Air Quality Bureau State regulations are federally enforceable except for the following: affirmative defense portions at 20.2.7.6.B, 20.2.7.110(B)(15), 20.2.7.11 through 20.2.7.113, 20.2.7.115, and 20.2.7.116; 20.2.37; 20.2.42; 20.2.43; 20.2.62; 20.2.63; 20.2.86; 20.2.89; and 20.2.90 NMAC. Federally enforceable means that EPA can enforce the regulation as well as the Air Quality Bureau and federally enforceable regulations can count toward determining a facility's potential to emit (PTE) for the Title V, PSD, and nonattainment permit regulations.

INCLUDE ANY OTHER INFORMATION NEEDED TO COMPLETE AN APPLICABILITY DETERMINATION OR THAT IS RELEVENT TO YOUR FACILITY'S NOTICE OF INTENT OR PERMIT.

EPA Applicability Determination Index for 40 CFR 60, 61, 63, etc: http://cfpub.epa.gov/adi/

<u>STATE</u> <u>REGU-</u> <u>LATIONS</u> CITATION	Title	Applies? Enter Yes or No	Unit(s) or Facility	JUSTIFICATION: (You may delete instructions or statements that do not apply in the justification column to shorten the document.)	
20.2.1 NMAC	General Provisions	Yes	Facility	General Provisions apply to Notice of Intent, Construction, and Title V permit applications.	
20.2.3 NMAC	Ambient Air Quality Standards NMAAQS	Yes	Facility	If subject, this would normally apply to the entire facility. 20.2.3 NMAC is a State Implementation Plan (SIP) approved regulation that limits the maximum allowable concentration of Total Suspended Particulates, Sulfur Compounds, Carbon Monoxide and Nitrogen Dioxide. Title V applications, see exemption at 20.2.3.9 NMAC	
				If subject, this would normally apply to the entire facility.	
20.2.7 NMAC	Excess Emissions	Yes	Facility	If your entire facility or individual pieces of equipment are subject to emissions limits in a permit or numerical emissions standards in a federal or state regulation, this applies. This would not apply to Notices of Intent since these are not permits.	
20.2.33 NMAC	Gas Burning Equipment - Nitrogen Dioxide	No	N/A	None of the equipment has a rating greater than 1 MMBtu/hr.	
20.2.34 NMAC	Oil Burning Equipment: NO ₂	No	N/A	This facility has no oil burning equipment.	
20.2.35 NMAC	Natural Gas Processing Plant – Sulfur	No	N/A	The facility is not a gas processing plant.	
20.2.38 NMAC	Hydrocarbon Storage Facility	Yes	OT1- OT4	The site uses a flare to comply with 20.2.38 NMAC.	
20.2.39 NMAC	Sulfur Recovery Plant - Sulfur	No	N/A	The facility does not operate a sulfur recovery plant.	
20.2.61.109 NMAC	Smoke & Visible Emissions	Yes	FL1-3, RB1-3, ENG1- 9, ENG11 -12, HTR1	This regulation that limits opacity to 20% applies to Stationary Combustion Equipment, such as engines, boilers, heaters, and flares unless your equipment is subject to another state regulation that limits particulate matter such as 20.2.19 NMAC (see 20.2.61.109 NMAC).	
20.2.70 NMAC	Operating Permits	Yes	Facility	The facility is a major source and will apply for a Title V Operating Permit.	
20.2.71 NMAC	Operating Permit Fees	Yes	Facility	The facility is a major source and will apply for a Title V Operating Permit.	
20.2.72 NMAC	Construction Permits	Yes	Facility	This application requests a NSR in accordance with 20.2.72.	
20.2.73 NMAC	NOI & Emissions Inventory Requirements	No	N/A	The site is subject to 20.2.72 NMAC.	
20.2.74 NMAC	Permits – Prevention of Significant Deterioration (PSD)	No	N/A	The facility is not a major PSD site.	
20.2.75 NMAC	Construction Permit Fees	Yes	Facility	A permit fee is included with this application.	

STATE REGU- LATIONS CITATION	Title	Applies? Enter Yes or No	Unit(s) or Facility	JUSTIFICATION: (You may delete instructions or statements that do not apply in the justification column to shorten the document.)
20.2.77 NMAC	New Source Performance	Yes	Facility	See regulatory discussion in Federal Regulations Citation section.
20.2.78 NMAC	Emission Standards for HAPS	No	N/A	The facility does not fit into any of the source categories.
20.2.79 NMAC	Permits – Nonattainment Areas	No	N/A	The facility is not located in a nonattainment area.
20.2.80 NMAC	Stack Heights	No	N/A	There are no stacks to which this regulation would apply.
20.2.82 NMAC	MACT Standards for source categories of HAPS	Yes	DEHY1- 3, ENG1-9, ENG11- 12	See regulatory discussion in Federal Regulations Citation section.
20.2.1 NMAC	General Provisions	Yes	Facility	General Provisions apply to Notice of Intent, Construction, and Title V permit applications.
20.2.3 NMAC	Ambient Air Quality Standards NMAAQS	Yes	Facility	If subject, this would normally apply to the entire facility. 20.2.3 NMAC is a State Implementation Plan (SIP) approved regulation that limits the maximum allowable concentration of Total Suspended Particulates, Sulfur Compounds, Carbon Monoxide and Nitrogen Dioxide. Title V applications, see exemption at 20.2.3.9 NMAC

FEDERAL REGU- LATIONS CITATION	Title	Applies? Enter Yes or No	Unit(s) or Facility	JUSTIFICATION:
40 CFR 50	NAAQS	Yes	Facility	Compliance with the requirements of the GCP indicates compliance with NAAQS.
NSPS 40 CFR 60, Subpart A	General Provisions	Yes	Facility	See regulatory discussion below.
NSPS 40 CFR60.40a, Subpart Da	Subpart Da, Performance Standards for Electric Utility Steam Generating Units	No	N/A	The facility does not operate any electric utility steam generating units.
NSPS 40 CFR60.40b Subpart Db	Electric Utility Steam Generating Units	No	N/A	The facility does not operate any electric utility steam generating units.

<u>FEDERAL</u> <u>REGU-</u> <u>LATIONS</u> CITATION	Title	Applies? Enter Yes or No	Unit(s) or Facility	JUSTIFICATION:
NSPS 40 CFR 60, Subpart Ka	Storage Vessels for Petroleum Liquids Commenced After May 18, 1978, and Prior to July 23, 1984	No	N/A	The hydrocarbons are stored prior to custody transfer.
NSPS 40 CFR 60, Subpart Kb	Standards of Performance for Volatile Organic Liquid Storage Commenced After July 23, 1984	No	N/A	The hydrocarbons are stored prior to custody transfer.
NSPS 40 CFR 60.330 Subpart GG	Stationary Gas Turbines	No	N/A	There are no turbines.
NSPS 40 CFR 60, Subpart KKK	Leaks of VOC from Onshore Gas Plants	No	N/A	This is not a gas plant.
NSPS 40 CFR Part 60 Subpart LLL	Standards of Performance for Onshore Natural Gas Processing: SO2 Emissions	No	N/A	The facility does not operate a sweetening unit.
NSPS 40 CFR Part 60 Subpart OOOO	Crude Oil and Natural Gas Production, Transmission, and Distribution after August 23, 2011 and before September 18, 2015	No	N/A	The site will be constructed after 9/18/15. See NSPS OOOOa discussion below.
NSPS 40 CFR Part 60 Subpart OOOOa	Crude Oil and Natural Gas Facilities for which Construction, Modification or Reconstruction Commenced After September 18, 2015	Yes	FUG	The storage tanks were constructed after the applicability date of the rule; however, XTO is requesting emissions be limited by permit to less than 6 tpy. The regulation is applicable to the storage tanks but the tanks are not affected sources. The site uses low-bleed pneumatic controllers. The site is subject to leak monitoring from fugitive components.
NSPS 40 CFR 60 Subpart IIII	Standards of performance for Stationary Compression Ignition Internal Combustion Engines	No	N/A	The facility does not operate any affected sources.
NSPS 40 CFR Part 60 Subpart JJJJ	Standards of Performance for Stationary Spark Ignition Internal Combustion Engines	TBD	ENG1-9, ENG11- 12	ENG1-ENG3 are subject to the engines are subject to the limitations in Table 1 per 40 CFR 60.4233(e). A determination of applicability will be made for each engine to be used at the site.

<u>FEDERAL</u> <u>REGU-</u> <u>LATIONS</u> CITATION	Title	Applies? Enter Yes or No	Unit(s) or Facility	JUSTIFICATION:	
NSPS 40 CFR 60 Subpart TTTT	Greenhouse Gas Emissions for Electric Generating Units	No	N/A	The facility does not operate any affected sources.	
NSPS 40 CFR 60 Subpart UUUU	Greenhouse Gas Emissions and Compliance Times for Electric Utility Generating Units	No	N/A	The facility does not operate any affected sources.	
NSPS 40 CFR 60, Subparts WWW, XXX, Cc, and Cf	Standards of performance for Municipal Solid Waste (MSW) Landfills	No	N/A	The facility does not operate any affected sources.	
NESHAP 40 CFR 61 Subpart A	General Provisions	See Below	See Below	See regulatory discussion below.	
NESHAP 40 CFR 61 Subpart E	National Emission Standards for Mercury	No	N/A	The facility does not operate any affected sources.	
NESHAP 40 CFR 61 Subpart V	National Emission Standards for Equipment Leaks (Fugitive Emission Sources)	No	N/A	The facility does not operate any affected sources.	
MACT 40 CFR 63, Subpart A	General Provisions	No	N/A	See regulatory discussion below.	
MACT 40 CFR 63.760 Subpart HH	Oil and Natural Gas Production Facilities	Yes	DEHY1- 3	As a major source of HAP, sources subject to HH include storage vessels with flash emissions, fugitive components, and compressors in VHAP service ((see §63.760(b)(1)(ii), (iii), and (iv)). Fugitives and compressors are exempt per §63.769(b) since they are subject to NSPS OOOO. Storage vessels use a closed vent system connected to a combustor to comply with §63.766(b). The dehydrators process more than 3 mmscfd; however, since benzene emissions are less than 1 tpy, there are no applicable requirements. (See §63.764(E)(1))	
MACT 40 CFR 63 Subpart HHH	Natural Gas Transmission and Storage Facilities	No	N/A	This regulation does not apply as the plant is not a natural gas transmission and storage facility as defined by the subpart (§63.1270(a)).	
MACT 40 CFR 63 Subpart DDDDD	Major Industrial, Commercial, and Institutional Boilers & Process Heaters	No	N/A	The facility is not a major source of HAP as defined in §63.7575 "Major source for oil and natural gas production facilities". Therefore, MACT 40 CFR 63 Subpart DDDDD does not apply.	
MACT 40 CFR 63 Subpart JJJJJJ	Boilers and Process Heaters	No	N/A	The units are exempt per §63.1195(e) since they burn natural gas.	
MACT 40 CFR 63 Subpart UUUUU	NESHAP Coal & Oil Fire Electric Utility Steam Generating Unit	No	N/A	The facility does not operate any affected sources.	
MACT 40 CFR 63 Subpart ZZZZ	RICE MACT	TBD	ENG1-9, ENG11- 12	ENG1-ENG3 comply with NSPS JJJJ to comply with NESHAP ZZZZ per 60.6590(c)(1). A determination of applicability will be made for each engine to be used at the site.	

FEDERAL REGU- LATIONS CITATION	Title	Applies? Enter Yes or No	Unit(s) or Facility	JUSTIFICATION:
40 CFR 64	Compliance Assurance Monitoring	No	N/A	The facility is not subject to CAM.
40 CFR 68	Chemical Accident Prevention	No	N/A	The facility does not store any chemicals above threshold quantities.
Acid Rain 40 CFR 72	Acid Rain	No	N/A	The facility does not have any units subject to the Acid Rain regulations.
Title IV – Acid Rain 40 CFR 73	Sulfur Dioxide Allowance Emissions	No	N/A	The facility does not have any units subject to the Acid Rain regulations.
Title IV-Acid Rain 40 CFR 75	Continuous Emissions Monitoring	No	N/A	The facility does not have any units subject to the Acid Rain regulations.
Title IV – Acid Rain 40 CFR 76	Acid Rain Nitrogen Oxides Emission Reduction Program	No	N/A	The facility does not have any units subject to the Acid Rain regulations.
Title VI – 40 CFR 82	Protection of Stratospheric Ozone	No	N/A	The facility does not service, maintain, or repair equipment containing refrigerants.

Tab 14Section 14 - Operational Plan to Mitigate Emissions

Operational Plan to Mitigate Emissions

(Submitting under 20.2.70, 20.2.72, 20.2.74 NMAC)

✓ Title V Sources (20.2.70 NMAC): By checking this box and certifying this application the permittee certifies that it has developed an <u>Operational Plan to Mitigate Emissions During Startups</u>, <u>Shutdowns</u>, <u>and Emergencies</u> defining the measures to be taken to mitigate source emissions during startups, shutdowns, and emergencies as required by 20.2.70.300.D.5(f) and (g) NMAC. This plan shall be kept on site to be made available to the Department upon request. This plan should not be submitted with this application.

- ✓ NSR (20.2.72 NMAC), PSD (20.2.74 NMAC) & Nonattainment (20.2.79 NMAC) Sources: By checking this box and certifying this application the permittee certifies that it has developed an <u>Operational Plan to Mitigate Source Emissions</u> <u>During Malfunction, Startup, or Shutdown</u> defining the measures to be taken to mitigate source emissions during malfunction, startup, or shutdown as required by 20.2.72.203.A.5 NMAC. This plan shall be kept on site to be made available to the Department upon request. This plan should not be submitted with this application.
- ☑ Title V (20.2.70 NMAC), NSR (20.2.72 NMAC), PSD (20.2.74 NMAC) & Nonattainment (20.2.79 NMAC) Sources: By checking this box and certifying this application the permittee certifies that it has established and implemented a Plan to Minimize Emissions During Routine or Predictable Startup, Shutdown, and Scheduled Maintenance through work practice standards and good air pollution control practices as required by 20.2.7.14.A and B NMAC. This plan shall be kept on site or at the nearest field office to be made available to the Department upon request. This plan should not be submitted with this application.

Emissions during startups, shutdowns, maintenance and emergencies (ESDs) will be minimized through the application of industry standards and /or manufacturer recommended operating practices as described below. Trained technicians are responsible for the timely and effective implementation of these actions.

Startup procedures for the engines are normally completed in less than 15 minutes and shutdown procedures are normally completed in less than 5 minutes. During a cold startup, the units may emit at a higher rate than normal as the units warm to operating temperature; however, if the unit has been shut down for long enough that a warm up is required, the small excess emissions occurring during warmup will be more than offset by the lack of emissions during the shutdown period. Similarly, if the unit is restarted while warm, there should be no excess emissions as the unit is already at operating temperature.

Tab 15Section 15 - Alternative Operating Scenarios

Alternative Operating Scenarios

(Submitting under 20.2.70, 20.2.72, 20.2.74 NMAC)

Alternative Operating Scenarios: Provide all information required by the department to define alternative operating scenarios. This includes process, material and product changes; facility emissions information; air pollution control equipment requirements; any applicable requirements; monitoring, recordkeeping, and reporting requirements; and compliance certification requirements. Please ensure applicable Tables in this application are clearly marked to show alternative operating scenario.

Construction Scenarios: When a permit is modified authorizing new construction to an existing facility, NMED includes a condition to clearly address which permit condition(s) (from the previous permit and the new permit) govern during the interval between the date of issuance of the modification permit and the completion of construction of the modification(s). There are many possible variables that need to be addressed such as: Is simultaneous operation of the old and new units permitted and, if so for example, for how long and under what restraints? In general, these types of requirements will be addressed in Section A100 of the permit, but additional requirements may be added elsewhere. Look in A100 of our NSR and/or TV permit template for sample language dealing with these requirements. Find these permit templates at: https://www.env.nm.gov/aqb/permit/aqb_pol.html. Compliance with standards must be maintained during construction, which should not usually be a problem unless simultaneous operation of old and new equipment is requested.

In this section, under the bolded title "Construction Scenarios", specify any information necessary to write these conditions, such as: conservative-realistic estimated time for completion of construction of the various units, whether simultaneous operation of old and new units is being requested (and, if so, modeled), whether the old units will be removed or decommissioned, any PSD ramifications, any temporary limits requested during phased construction, whether any increase in emissions is being requested as SSM emissions or will instead be handled as a separate Construction Scenario (with corresponding emission limits and conditions, etc.

XTO is not proposing any alternative operating scenarios.

Tab 16Section 16 - Air Dispersion Modeling

Section 16 Air Dispersion Modeling

- Minor Source Construction (20.2.72 NMAC) and Prevention of Significant Deterioration (PSD) (20.2.74 NMAC) ambient impact analysis (modeling): Provide an ambient impact analysis as required at 20.2.72.203.A(4) and/or 20.2.74.303 NMAC and as outlined in the Air Quality Bureau's Dispersion Modeling Guidelines found on the Planning Section's modeling website. If air dispersion modeling has been waived for one or more pollutants, attach the AQB Modeling Section modeling waiver approval documentation.
- 2) SSM Modeling: Applicants must conduct dispersion modeling for the total short term emissions during routine or predictable startup, shutdown, or maintenance (SSM) using realistic worst case scenarios following guidance from the Air Quality Bureau's dispersion modeling section. Refer to "Guidance for Submittal of Startup, Shutdown, Maintenance Emissions in Permit Applications (<u>http://www.env.nm.gov/aqb/permit/app_form.html</u>) for more detailed instructions on SSM emissions modeling requirements.
- 3) Title V (20.2.70 NMAC) ambient impact analysis: Title V applications must specify the construction permit and/or Title V Permit number(s) for which air quality dispersion modeling was last approved. Facilities that have only a Title V permit, such as landfills and air curtain incinerators, are subject to the same modeling required for preconstruction permits required by 20.2.72 and 20.2.74 NMAC.

What is the purpose of this application?	Enter an X for each purpose that applies
New PSD major source or PSD major modification (20.2.74 NMAC). See #1 above.	
New Minor Source or significant permit revision under 20.2.72 NMAC (20.2.72.219.D NMAC).	Х
See #1 above. Note: Neither modeling nor a modeling waiver is required for VOC emissions.	
Reporting existing pollutants that were not previously reported.	
Reporting existing pollutants where the ambient impact is being addressed for the first time.	
Title V application (new, renewal, significant, or minor modification. 20.2.70 NMAC). See #3	
above.	
Relocation (20.2.72.202.B.4 or 72.202.D.3.c NMAC)	
Minor Source Technical Permit Revision 20.2.72.219.B.1.d.vi NMAC for like-kind unit	
replacements.	
Other: i.e. SSM modeling. See #2 above.	
This application does not require modeling since this is a No Permit Required (NPR) application.	
This application does not require modeling since this is a Notice of Intent (NOI) application	
(20.2.73 NMAC).	
This application does not require modeling according to 20.2.70.7.E(11), 20.2.72.203.A(4),	
20.2.74.303, 20.2.79.109.D NMAC and in accordance with the Air Quality Bureau's Modeling	
Guidelines.	

Check each box that applies:

- □ See attached, approved modeling **waiver for all** pollutants from the facility.
- □ See attached, approved modeling **waiver for some** pollutants from the facility.
- Attached in Universal Application Form 4 (UA4) is a **modeling report for all** pollutants from the facility.
- □ Attached in UA4 is a **modeling report for some** pollutants from the facility.
- \Box No modeling is required.

Tab 17Section 17 - Compliance Test History

Compliance Test History

(Submitting under 20.2.70, 20.2.72, 20.2.74 NMAC)

To show compliance with existing NSR permits conditions, you must submit a compliance test history. The table below provides an example.

No tests have been performed.

Tab 18

Section 18 - Addendum for Streamline Applications (Not Applicable)

Addendum for Streamline Applications

Do not print this section unless this is a streamline application.

Streamline Applications do not require a complete application. Submit Sections 1-A, 1-B, 1-D, 1-F, 1-G, 2-A, 2-C thru L, Sections 3 thru 8, Section 13, Section 18, Section 22, and Section 23 (Certification). Other sections may be required at the discretion of the Department. 20.2.72.202 NMAC Exemptions do not apply to Streamline sources. 20.2.72.219 NMAC revisions and modifications do not apply to Streamline sources, thus 20.2.72.219 type actions require a complete new application submittal. Please do not print sections of a streamline application that are not required.

This section is not applicable since this is not a Streamline Permit Application.

Tab 19

Section 19 - Requirements for Title V Program

Requirements for Title V Program

Do not print this section unless this is a Title V application.

Who Must Use this Attachment:

* Any major source as defined in 20.2.70 NMAC.

- * Any source, including an area source, subject to a standard or other requirement promulgated under Section 111 Standards of Performance for New Stationary Sources, or Section 112 Hazardous Air Pollutants, of the 1990 federal Clean Air Act ("federal Act"). Non-major sources subject to Sections 111 or 112 of the federal Act are exempt from the obligation to obtain an 20.2.70 NMAC operating permit until such time that the EPA Administrator completes rulemakings that require such sources to obtain operating permits. In addition, sources that would be required to obtain an operating permit solely because they are subject to regulations or requirements under Section 112(r) of the federal Act are exempt from the requirement to obtain an Operating Permit.
- * Any Acid Rain source as defined under title IV of the federal Act. The Acid Rain program has additional forms. See <u>http://www.env.nm.gov/aqb/index.html</u>. Sources that are subject to both the Title V and Acid Rain regulations are encouraged to submit both applications simultaneously.
- * Any source in a source category designated by the EPA Administrator ("Administrator"), in whole or in part, by regulation, after notice and comment.

This is not a Title V application.

Tab 20Section 20 - Other Relevant Information

Other Relevant Information

<u>Other relevant information</u>. Use this attachment to clarify any part in the application that you think needs explaining. Reference the section, table, column, and/or field. Include any additional text, tables, calculations or clarifying information.

Additionally, the applicant may propose specific permit language for AQB consideration. In the case of a revision to an existing permit, the applicant should provide the old language and the new language in track changes format to highlight the proposed changes. If proposing language for a new facility or language for a new unit, submit the proposed operating condition(s), along with the associated monitoring, recordkeeping, and reporting conditions. In either case, please limit the proposed language to the affected portion of the permit.

No other relevant information is provided.

Tab 21

Section 21 - Addendum for Landfill Applications (Not Applicable)

Addendum for Landfill Applications

Do not print this section unless this is a landfill application.

Landfill Applications are not required to complete Sections 1-C Input Capacity and Production Rate, 1-E Operating Schedule, 17 Compliance Test History, and 18 Streamline Applications. Section 12 – PSD Applicability is required only for Landfills with Gas Collection and Control Systems and/or landfills with other non-fugitive stationary sources of air emissions such as engines, turbines, boilers, heaters. All other Sections of the Universal Application Form are required.

EPA Background Information for MSW Landfill Air Quality Regulations: <u>https://www3.epa.gov/airtoxics/landfill/landflpg.html</u>

NM Solid Waste Bureau Website: https://www.env.nm.gov/swb/

This is not a landfill.

Tab 22Section 22 - Certification

Section 22: Certification

Company Name: XTO Energy Inc.

I, <u>Benjamin Schneider</u>, hereby certify that the information and data submitted in this application are true and as accurate as possible, to the best of my knowledge and professional expertise and experience.

Signed this _____ day of <u>Sedewker</u> 2020 , upon my oath or affirmation, before a notary of the State of <u>Illinois</u>.

Benjamin Schneider Printed Name

Scribed and sworn before me on this M day of September 2020 .

My authorization as a notary of the State of whether and the 24 day of mach, 2022

ignature of thathan

Preschay Chathe Notary's Printed

1 2020 THERESA LAY CHATHAM Notary Public, State of Texas Comm. Expires 03-24-2022 Notary ID 1026023-7

9/1/2022

Environmental Engineer

Date

Title

*For Title V applications, the signature must be of the Responsible Official as defined in 20.2.70.7.AE NMAC.

Tab 23 Section 23 - UA4

Universal Application 4

Air Dispersion Modeling Report

Refer to and complete Section 16 of the Universal Application form (UA3) to assist your determination as to whether modeling is required. If, after filling out Section 16, you are still unsure if modeling is required, e-mail the completed Section 16 to the AQB Modeling Manager for assistance in making this determination. If modeling is required, a modeling protocol would be submitted and approved prior to an application submittal. The protocol should be emailed to the modeling manager. A protocol is recommended but optional for minor sources and is required for new PSD sources or PSD major modifications. Fill out and submit this portion of the Universal Application form (UA4), the "Air Dispersion Modeling Report", only if air dispersion modeling is required for this application submittal. This serves as your modeling report submittal and should contain all the information needed to describe the modeling. No other modeling report or modeling protocol should be submitted with this permit application.

16	16-A: Identification				
1	Name of facility:	Bulldog Compressor Station			
2	Name of company:	XTO Energy Inc.			
3	Current Permit number:	8153			
4	Name of applicant's modeler:	Bruce Ferguson			
5	Phone number of modeler:	(601) 824-1860			
6	E-mail of modeler:	bferguson@fce-engineering.com			

16	-B: Brief						
1	Was a modeling protocol submitted and approved?	Yes□	No⊠				
2	Why is the modeling being done? Other (describe below)						
3	Describe the permit changes relevant to the modeling.						
	Change in facility equipment models, addition of flaring SSM emissions, facility location adjusted.						
4	What geodetic datum was used in the modeling? NAD83						
5	How long will the facility be at this location? Indefinite						
6	Is the facility a major source with respect to Prevention of Significant Deterioration (PSD)?	Yes□	No⊠				
7	Identify the Air Quality Control Region (AQCR) in which the facility is located	155					

16	-B: Brief								
	List the PSD baseline dates for this region (minor or major, as appropriate).								
0	NO2	3/16/1988							
8	SO2	7/28/1978							
	PM10	2/20/1979							
	PM2.5 11/13/2013								
	Provide the name and distance to Class	s I areas within 50 km of the facility (300 km for PS	D permits).						
9	None								
10	Is the facility located in a non-attainme	ent area? If so describe below	Yes□	No⊠					
11	Describe any special modeling requirements, such as streamline permit requirements. None								

16	-C: Modeling H	listory of Facility							
	Describe the modeling history of the facility, including the air permit numbers, the pollutants modeled, the National Ambient Air Quality Standards (NAAQS), New Mexico AAQS (NMAAQS), and PSD increments modeled. (Do not include modeling waivers).								
	Pollutant	Latest permit and modification number that modeled the pollutant facility-wide.	Date of Permit	Comments					
	СО	8153	5/7/2019						
	NO ₂	8153	5/7/2019						
1	SO ₂	8153	5/7/2019						
	H ₂ S								
	PM2.5	8153	5/7/2019						
	PM10	8153	5/7/2019						
	TSP								
	Lead								
	Ozone (PSD only)								
	NM Toxic Air Pollutants (20.2.72.402 NMAC)								

16-D: Modeling performed for this application

For each pollutant, indicate the modeling performed and submitted with this application.							
Choose the most complicated modeling applicable for that pollutant, i.e., culpability analysis assumes ROI and cumulative							
analysis were also performed.							

	Pollutant	ROI	Cumulative analysis	Culpability analysis	Waiver approved	Pollutant not emitted or not changed.
	СО	\boxtimes				
	NO ₂	\boxtimes	\boxtimes			
1	SO ₂	\boxtimes	\boxtimes			
1	H ₂ S					\boxtimes
	PM2.5	\boxtimes	\boxtimes			
	PM10	\boxtimes	\boxtimes			
	TSP*					
	Lead					\boxtimes
	Ozone*					
	State air toxic(s) (20.2.72.402 NMAC)					

*Modeling was not performed for TSP because the standard was removed. Ozone was not evaluated because the permitting action is a minor NSR.

16-E: New Mexico toxic air pollutants modeling

1	List any New Mexico toxic air pollutants (NMTAPs) from Tables A and B in 20.2.72.502 NMAC that are modeled for this									
1	application									
		None								
	List any N	MTAPs that are em	itted but not modeled becaus	se stack height co	rrection factor. Add addit	ional rows to the table				
	below, if required.									
	Pollutant	Emission Rate	Emission Rate Screening	Stack Height	Correction Factor	Emission Rate/				
2	Tonutant	(pounds/hour)	Level (pounds/hour)	(meters)	Contection 1 actor	Correction Factor				
	N/A									

16-	F: Modeling options		
1	Was the latest version of AERMOD used with regulatory default options? If not explain below.	Yes⊠	No□

16	16-G: Surrounding source modeling									
1	Date of surroundi	ng source retrieval	March 11, 2020, MergeMaster File Spoke with Eric Peters by phone 8/19/20, and Eric relayed that the 3/11/20 was the best available data and could be used.							
	sources modeled		r Quality Bureau was believed to be inaccurate, describe how the changes to the surrounding source inventory were made, use the table							
2	AQB Source ID	Description of Corrections								
		All neighboring sources within 10 km were retained for cumulative modeling.								
	Various	Neighboring sources between 10 and 25 km with source IDs less than 10,000 were removed from the inventory.								
	Various	None of the neighboring sources were found to have emissions of 1000 lb/hr or greater and neighboring sources greater than 25 km were removed from the inventory.								

16	16-H: Building and structure downwash										
1	¹ How many buildings are present at the facility? No buildings.										
2	2 How many above ground storage tanks are present at the facility? There are eight above ground storage tanks.										
3	Was building downwash modeled for all buildings and	tanks? If not explain why below.	Yes⊠	No□							
4	Building comments	N/A									

16-I: Receptors and modeled property boundary "Restricted Area" is an area to which public entry is effectively precluded. Effective barriers include continuous fencing, continuous walls, or other continuous barriers approved by the Department, such as rugged physical terrain with a steep grade that would require special equipment to traverse. If a large property is completely enclosed by fencing, a restricted area within the property may be identified with signage only. Public roads cannot be part of a Restricted Area. A Restricted Area is required in order to exclude receptors from the facility property. If the facility does not have a Restricted Area, then 1 receptors shall be placed within the property boundaries of the facility. Describe the fence or other physical barrier at the facility that defines the restricted area. No fence line was used. Modeling was conducted with on-site receptors at 10 m spacing. Receptors must be placed along publicly accessible roads in the restricted area. 2 Are there public roads passing through the restricted area? Yes□ No⊠ 3 Are restricted area boundary coordinates included in the modeling files? Yes□ No⊠ Describe the receptor grids and their spacing. The table below may be used, adding rows as needed. Start distance from End distance from Grid Type Shape Spacing restricted area or restricted area or Comments center of facility center of facility 10 m 0 Cartesian Circle 250 m 4 Cartesian Circle 50 m 250 m 1 km 100 m 1 km 3 km Cartesian Circle Cartesian Circle 250 m 3 km 6 km Cartesian Circle 500 m 6 km 10 km Cartesian Circle 1 km 10 km 50 km Describe receptor spacing along the fence line. 5 No fence line was used. Receptors were placed on-site at 10-meter spacings Describe the PSD Class I area receptors. 6 None

16	-J: Sensitive areas		
1	Are there schools or hospitals or other sensitive areas near the facility? If so describe below. This information is optional (and purposely undefined) but may help determine issues related to public notice.	Yes□	No⊠
3	The modeling review process may need to be accelerated if there is a public hearing. Are there likely to be public comments opposing the permit application?	Yes□	No⊠

16	-K: Mo	deling	Scena	rios								
1	rates, times etc. Alterna in Section	Identify, define, and describe all modeling scenarios. Examples of modeling scenarios include using different production rates, times of day, times of year, simultaneous or alternate operation of old and new equipment during transition periods, etc. Alternative operating scenarios should correspond to all parts of the Universal Application and should be fully described in Section 15 of the Universal Application (UA3).										periods, ly described
	distributed	evenly be	tween the t	wo facility	y flares.		l operation	is, flaring f	or SSM ever	its and al	l flare ei	missions
	Which scen	nario produ	uces the hi	ghest conc	entrations	? Why?						
2	There were maximum				e scenario	s, indicatii	ng that the	flares are 1	not the contro	olling fac	tor for t	he
3	Were emission factor sets used to limit emission rates or hours of operation? (This question pertains to the "SEASON", "MONTH", "HROFDY" and related factor sets, not to the factors used for calculating the maximum emission rate.)											
4									re the factor if it makes fo			
	Hour of Day	Factor	Hour of Day	Factor								
[1		13									
	2		14									
	3		15									
-	4		16									
5	5		17									
5	6 7		18 19									
-	8		20									
-	9		20									
-	10		22									
-	11		23									
ł	12		24									
Ì	If hourly.	variable en	nission rate	es were use	d that wer	e not desc	ribed abov	e. describe	them below			
ŀ								.,				
6	Were diffe	rent emissi	ion rates us	sed for sho	ort-term and	d annual n	nodeling?	If so descri	be below.	Yes□		No⊠

16	L: NO ₂	Modeling								
	Which types	Which types of NO ₂ modeling were used?								
	Check all th	Check all that apply.								
	\boxtimes	ARM2								
1		100% NO _X to NO ₂ conversion								
		PVMRM								
		OLM OLM								
		Other:								
2	Describe the	Describe the NO ₂ modeling.								
2		The modeled scenarios were modeled in separate runs for NOx instead of using source groups. The use of source groups with ARM2 underestimates the NO_2 impacts when the sources cannot operate simultaneously.								
3		t NO ₂ /NO _x ratios (0.5 minimum, 0.9 maximum or equilibrium) used? If not l justify the ratios used below.	Yes⊠	No□						
4	Describe the	Describe the design value used for each averaging period modeled.								
4	1-hour: Hig	n eighth high								
	Annual: One Year Annual Average									

	Select the pol	lutants for which	h plume depletion m	odeling was	used.					
1	□ PM2.5									
		PM10								
	\boxtimes	None								
2 Describe the particle size distributions used. Include the source of information.										
	N/A									
3	Sources that e considered to	Does the facility emit at least 40 tons per year of NO_X or at least 40 tons per year of SO_2 ?Yes \boxtimes Sources that emit at least 40 tons per year of NO_X or at least 40 tons per year of SO_2 are considered to emit significant amounts of precursors and must account for secondaryYes \boxtimes No \square								
4	Was secondar	y PM modeled	for PM2.5?				Yes[□ No⊠		
	If MERPs were used to account for secondary PM2.5 fill o below.				ne information be	ow. If ano	ther metho	d was used descri		
	NO _X (ton/yr)		SO ₂ (ton/yr)	SO_2 (ton/yr)			[PM2	[PM2.5] _{24-hour}		
	205.38 (inclue	ding SSM)	SM)	0.004 ug/m ³	0.054	0.054 ug/m^3				
	Southwest Climate Zone Lowest MERPs									
	State	County	Metric	Precurso	or Emissions	Stack	MERP			
	Colorado	Weld Co	Annual PM _{2.5}	NOx	100	10	10530			
5	Colorado	Weld Co	Annual PM _{2.5}	SO ₂	100	10	7359			
	Colorado	Weld Co	Daily PM _{2.5}	NOx	100) 10	5215			
	Colorado	Weld Co	Daily PM _{2.5}	SO ₂	100) 10	814			
	[PM2.5] _{annual} =									

16	-N: Setback Distances
1	Portable sources or sources that need flexibility in their site configuration requires that setback distances be determined between the emission sources and the restricted area boundary (e.g. fence line) for both the initial location and future locations. Describe the setback distances for the initial location.
	None
2	Describe the requested, modeled, setback distances for future locations, if this permit is for a portable stationary source. Include a haul road in the relocation modeling.
	N/A

16-	O: PSD Increm	ent and Source	IDs				
	The unit numbers in the T modeling files. Do these if they do not match below		Yes⊠	No□			
	Unit Number in UA-2	Unit Numbe	r in Modeling Files	S			
1				FL1_Norma	l (Normal Operatir	ng Emissions sc	enario)
	FL1			FL1_SSM (SSM scenario)		
				FL1_Even (All flare emissions	distributed eve	nly)
				FL2_Norma	l (Normal Operatir	ng Emissions sc	enario)
	FL2			FL2_SSM (SSM scenario)		
				FL2_Even (All flare emissions	distributed eve	nly)
2	The emission rates in the these match? If not, expla		ld match the	ones in the m	odeling files. Do	Yes⊠	No□
	Normal operations match two flares, this should pro plume rise.						
3	Have the minor NSR exe been modeled?	mpt sources or Title V Ins	significant A	Activities" (Ta	ble 2-B) sources	Yes⊠	No□
	Which units consume inc	rement for which pollutar	nts?				
4	Unit ID	NO_2	<u> </u>	O_2	PM10		PM2.5
	All Facility Units	X		X	X		X
5	PSD increment description (for unusual cases, i.e., bat after baseline date).	n for sources. aseline unit expanded emi	issions	N/A			
6	This is necessary to verify	Are all the actual installation dates included in Table 2A of the application form, as required? This is necessary to verify the accuracy of PSD increment modeling. If not please explain how increment consumption status is determined for the missing installation dates below.					No□
	Facility has not begun co	nstruction					

16-P: Flare Modeling 1 For each flare or flaring scenario, complete the following

Flare ID (and scenario)	Average Molecular Weight	Gross Heat Release (cal/s)	Effective Flare Diameter (m)
FL1_Normal	43.98	1,107,992	0.869
FL1_SSM	21.20	169,394	0.363
FL1_Even	22.58	138,014,571	10.322
FL2_Normal	21.20	169,394	0.363
FL2_SSM	22.53	274,921,149	14.570
FL2_Even	22.58	138,014,571	10.322

16-	Q: Volume and Related Sources								
1	1 Were the dimensions of volume sources different from standard dimensions in the Air Quality Bureau (AQB) Modeling Guidelines? Yes□ N								
2	Describe the determination of sigma-Y and sigma-Z for fugitive sources.								
	Values for large trucks in the NMED Guideline								
Describe how the volume sources are related to unit numbers. 3 Or say they are the same.									
	Unit No. ROAD represented by L0000001 through L0000024								
4	Describe any open pits.								
	None								
5	Describe emission units included in each open pit.								
	None								

16-	16-R: Background Concentrations							
	Were NMED provided background concentrations used? Identify the background station used							
	below. If non-	below. If non-NMED provided background concentrations were used describe the data that $Yes \boxtimes No \square$						
	was used.							
	CO: Del Nort	CO: Del Norte High School (350010023)						
	NO ₂ : Hobbs	Jefferson (350250008)						
1	PM2.5: Hobbs-Jefferson (350450019)							
	PM10: Hobbs-Jefferson (350250008)							
	SO ₂ : Amarillo (483751025)							
	Other:							
	Comments:							
2	Were backgro	ound concentrations refined to monthly or hourly values? If so describe below.	Yes□	No⊠				

16-S: Meteorological Data							
	Was NMED provided meteorological data used? If so select the station used.						
1	Artesia Year 2015	Yes⊠	No□				
2	If NMED provided meteorological data was not used describe the data set(s) used below. Discuss how missing data were handled, how stability class was determined, and how the data were processed.						
	N/A						

16-T: Terrain								
1	Was complex terrain used in the modeling? If not, describe why below.	Yes⊠	No□					
2	What was the source of the terrain data?							
	NED data through http://www.webgis.com/, downloaded through the Lakes Environmental GUI							

16	-U: Modeling Files				
	Describe the modeling files:				
	File name (or folder and file name)	Pollutant(s)	Purpose (ROI/SIA, cumulative, culpability analysis, other)		
	SIA\NOx\		ROI and Cumulative analysis		
	NOx_Normal.zip		Normal Operating Scenario		
	NOx_SSM.zip	NO2	SSM Scenario		
1	NOx_Even.zip		SSM Flare Emission evenly distributed to both flares		
	SIA\CO.zip	СО	ROI		
	SIA\SO2.zip	SO2	ROI & Cumulative		
	SIA\PM10.zip	PM10	ROI		
	SIA\PM25.zip	PM2.5	ROI		
	CIA\PM10.zip	PM10	Cumulative		
	CIA\PM25.zip	PM2.5	Cumulative		
	Generic zip file contents are summarized	l below			
	Artesia-Midland_2015.PFL & .SFC	Met Data as downloaded from NMED			
	Pages from A-8153_UA Calculations_XTO Bulldog CS NSR_07.11.20 - Bruce.jgw, .jpg, .wdt	Georeferenced facility layout			
	Surrounding Sources	Surrounding source files generated by MergeMaster			
	MERPs table_export.xlsx	MERPs downloaded from EPA for Southwest Climate Zone			
	[Pollutant].ADI	AERMOD input file			
	[Pollutant].ADO	AERMOD output file			
	[Pollutant].sum	AERMOD output summary file			
	[Pollutant].bpi	BPIP input file			
	[Pollutant].pro	BPIP output file			
	\[Pollutant].AD\	Plot File Directory			
	[Avg Period][Rank]G[xxx].PLT	Plot file naming convention. Where facil denotes normal operation, G002 denotes flaring evenly distributed between flares denotes NAAQS modeling and G002 den	SSM operations and G003 denotes . For PM10 & PM2.5 cumulative G001		

16-	V: PSD New or Major Modification Applications (Not A	Applicable	2)					
1	A new PSD major source or a major modification to an existing PSD major source requires additional analysis. Was preconstruction monitoring done (see 20.2.74.306 NMAC and PSD Preapplication Guidance on the AQB website)?	Yes No						
2	If not, did AQB approve an exemption from preconstruction monitoring?	Yes□	No□					
3	Describe how preconstruction monitoring has been addressed or attach the approved preconstruction monitoring or monitoring exemption.							
4	Describe the additional impacts analysis required at 20.2.74.304 NMAC.							
5	If required, have ozone and secondary PM2.5 ambient impacts analyses been completed? If so describe below.	Yes□	No□					

16-W: Mod	lelin	g Result	ts								
1	requ sign	ambient standards are exceeded because of surrounding sources, a culpability analysis is quired for the source to show that the contribution from this source is less than the gnificance levels for the specific pollutant. Was culpability analysis performed? If so scribe below.							Yes□	No⊠	
2		tify the maxinecessary.	num concen	trations from	the modeling	analysis. Row	s may be mod	ified, add	led and remov	ved from the t	able below
	ility ion	cility ion	d n with ources	PM (nd ion	/e ion ndard ndard	andard	Location			
Pollutant, Time Pe and Standard	eriod	Modeled Facility Concentration (µg/m3)	Concentration (μg/m3) Modeled Concentration with Surrounding Sources (μg/m3) (μg/m3) (μg/m3) (μg/m3) (μg/m3)	Cumulati Concentrat (µg/m3)	Value of Standard (µg/m3)	Percent of Standard	UTM E (m)	UTM N (m)	Elevation (ft)		
CO 1hr NMAAQS		188.85719	N/A	N/A	2,203	2,391.86	9,960.1	24%	607740	3602720	3,497
CO 8hr NMAAQS		101.16457	N/A	N/A	1,524	1,625.16	14,997.5	11%	607740	3602740	3,497
NO ₂ 1hr NAAQS		108.45874	N/A	N/A	64.2	172.66	188.03	92%	607750	3602780	3,497
NO ₂ Annual NMA	AQS	10.99693	N/A	N/A	8.1	19.10	94.02	20%	607360	3602760	3,499
SO ₂ 1hr NAAQS		14.48833	N/A	N/A	47.0	61.49	196.4	31%	607760	3602760	3,499
SO ₂ Annual NMAA	AQS	1.47230	N/A	N/A	0.670	2.14	52.4	4%	607360	3602760	3,499
SO ₂ Annual PSD 1		1.47230	N/A	N/A	0.670	2.14	20	11%	607360	3602760	3,499
PM ₁₀ 24hr NAAQS			5.17563	N/A	37.3	42.48	150	28%	607340	3602830	3,499
PM ₁₀ 24hr PSD			4.74807	N/A	N/A	4.75	30	16%	607340	3602830	3,499
PM ₁₀ Annual PSD			2.00135	N/A	N/A	2.00	17	12%	607370	3602790	3,499
PM _{2.5} 24hr NAAQS			4.98135	0.054	13.4	18.44	35	53%	607530	3602510	3,503
PM _{2.5} Annual NAAQS			1.52053	0.004	5.9	7.42	12	62%	607360	3602780	3,499
PM _{2.5} 24hr PSD			3.29759	0.054	N/A	3.35	9	37%	607330	3602740	3,500
PM _{2.5} Annual PSD			1.32172	0.004	N/A	1.33	4	33%	607360	3602780	3,499

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16-X: Summary/conclusions

A statement that modeling requirements have been satisfied and that the permit can be issued.

A significant impact analysis was performed for pollutants identified in Section 16-D. CO impacts were found to be below the modeling significance level. Impacts for the remaining pollutants were found to be above the modeling significance level and a cumulative impact was required for these pollutants.

 PM_{10} and $PM_{2.5}$ impacts from surrounding sources was accounted for by explicitly modeling all sources within 10 km of the project and all increment consuming sources within 25 km of the project. Existing air quality modeling values were added to the modeled PM_{10} and $PM_{2.5}$ impacts to account for distant surrounding sources. Nearby and distant surrounding sources impacts for SO₂, NO_x and CO were accounted for in the analysis by using existing air quality monitoring in the area.

The modeled impacts combined with the existing air quality in the area were found to be compliant with the ambient air quality standards, i.e., NAAQS, NMAAQS and PSD increment. The proposed project will not cause or contribute to an exceedance of the ambient air quality standards. The NMED modeling requirements have been satisfied and the permit can be issued.