NEW MEXICO 20.2.70 NMAC APPLICATION TO RENEW TITLE V OPERATING PERMIT NUMBER P195-R3-M2

32-7 CENTRAL DELIVERY POINT

Submitted By:



Harvest Four Corners, LLC

1755 Arroyo Drive Bloomfield, New Mexico 87413

Prepared By:

Cirrus Consulting, LLC 11139 Crisp Air Drive Colorado Springs, CO 80908 (801) 294-3024

January 2022

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Introduction

The Harvest 32-7 Central Delivery Point (CDP) is a production gathering field compressor station that pressurizes and dehydrates natural gas for transport through natural gas pipelines.. The facility currently operates under Title V operating permit, P195-R3, issued January 31, 2018 (as modified in P195-R3-M2, August 14, 2020), and construction permit 1032-M9, dated October 11, 2018, as revised through –R5.

A list of the equipment currently approved for use at the facility by the Title V operating permit can be found in Tables 2-A and 2-B of Section 2 of this application.

This Title V renewal application is submitted under section 20.2.70.300.B(2) of the New Mexico Administrative Code (NMAC). The renewal application is due 12 months prior to the expiration of the current Title V Operating Permit on January 31, 2023.

The facility remains a minor source under the 20.2.74 NMAC Prevention of Significant Deterioration (PSD) program.

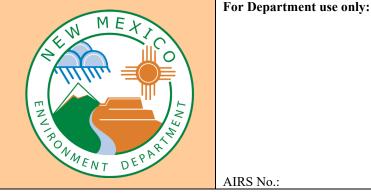
There are no modifications in this application that would de-bottleneck impacts or change the facility's major/minor status under either the Prevention of Significant Deterioration [PSD] or Title V permitting programs.

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Mail Application To:

New Mexico Environment Department Air Quality Bureau Permits Section 525 Camino de los Marquez, Suite 1 Santa Fe, New Mexico, 87505

Phone: (505) 476-4300 Fax: (505) 476-4375 www.env.nm.gov/aqb



AIRS No .:

Universal Air Quality Permit Application

Use this application for NOI, NSR, or Title V sources.

Use this application for: the initial application, modifications, technical revisions, and renewals. For technical revisions, complete Sections, 1-A, 1-B, 2-E, 3, 9 and any other sections that are relevant to the requested action; coordination with the Air Quality Bureau permit staff prior to submittal is encouraged to clarify submittal requirements and to determine if more or less than these sections of the application are needed. Use this application for streamline permits as well. See Section 1-I for submittal instructions for other permits.

This application is submitted as (check all that apply):
□ Request for a No Permit Required Determination (no fee) **Updating** an application currently under NMED review. Include this page and all pages that are being updated (no fee required). Construction Status: 🗆 Not Constructed 🗹 Existing Permitted (or NOI) Facility 🗆 Existing Non-permitted (or NOI) Facility Minor Source: □ a NOI 20.2.73 NMAC □ 20.2.72 NMAC application or revision □ 20.2.72.300 NMAC Streamline application Title V Source: 🗆 Title V (new) 🗹 Title V renewal 🗆 TV minor mod. 🗆 TV significant mod. TV Acid Rain: 🗆 New 🗆 Renewal PSD Major Source: PSD major source (new) minor modification to a PSD source a PSD major modification

Acknowledgements:

🗹 I acknowledge that a pre-application meeting is available to me upon request. 🗹 Title V Operating, Title IV Acid Rain, and NPR applications have no fees.

□ \$500 NSR application Filing Fee enclosed OR □ The full permit fee associated with 10 fee points (required w/ streamline applications).

 \Box Check No.: N/A in the amount of N/A

I acknowledge the required submittal format for the hard copy application is printed double sided 'head-to-toe', 2-hole punched (except the Sect. 2 landscape tables is printed 'head-to-head'), numbered tab separators. Incl. a copy of the check on a separate page.

□ This facility qualifies to receive assistance from the Small Business Environmental Assistance program (SBEAP) and qualifies for 50% of the normal application and permit fees. Enclosed is a check for 50% of the normal application fee which will be verified with the Small Business Certification Form for your company.

□ This facility qualifies to receive assistance from the Small Business Environmental Assistance Program (SBEAP) but does not qualify for 50% of the normal application and permit fees. To see if you qualify for SBEAP assistance and for the small business certification form go to https://www.env.nm.gov/aqb/sbap/small_business_criteria.html).

Citation: Please provide the low level citation under which this application is being submitted: 20.2.70.300.C(2) NMAC (e.g. application for a new minor source would be 20.2.72.200.A NMAC, one example for a Technical Permit Revision is 20.2.72.219.B.1.b NMAC, a Title V acid rain application would be: 20.2.70.200.C NMAC)

Section 1 – Facility Information

Sec	tion 1-A: Company Information	AI # if known (see 1 st 3 to 5 #s of permit IDEA ID No.): 1221	Updating Permit/NOI #: Application P195-R4	
1	Facility Name: 32-7 Central Delivery Point	Plant primary SIC Code (4 digits): 1389		
1	Facinty Name. 32-7 Central Denvery Foint	Plant NAIC code (6 digits): 213112		
a	Facility Street Address (If no facility street address, provide directions from See directions in Section 1-D4	n a prominent landmark)	:	
2	Plant Operator Company Name: Harvest Four Corners, LLC	Phone/Fax: (505) 632-	4600 / (505) 632-4782	
а	Plant Operator Address: 1755 Arroyo Drive, Bloomfield, New Mexico 87	413		
b	Plant Operator's New Mexico Corporate ID or Tax ID: 76-0451075			

3	Plant Owner(s) name(s): Same as #2 above	Phone/Fax: Same as #2 above
а	Plant Owner(s) Mailing Address(s): Same as #2a above	
4	Bill To (Company): Same as #2 above	Phone/Fax: Same as #2 above
а	Mailing Address: Same as #2a above	E-mail: N/A
5	 Preparer: Consultant: Lisa Killion, Cirrus Consulting, LLC 	Phone/Fax: 505-466-1790
а	Mailing Address: c/o 11139 Crisp Air Drive, Colorado Springs, Colorado 80908	E-mail: lkillion@cirrusllc.com
6	Plant Operator Contact: Oakley Hayes	Phone/Fax: 505-632-4421 / (505) 632-4782
а	Address: Same as #2a above	E-mail: Oakley.Hayes@harvestmidstream.com
7	Air Permit Contact: Same as #6 above	Title: Environmental Specialist
а	E-mail: Same as #6a above	Phone/Fax: Same as #6 above
b	Mailing Address: Same as #2a above	
с	The designated Air permit Contact will receive all official correspondence	(i.e. letters, permits) from the Air Quality Bureau.

Section 1-B: Current Facility Status

1.a	Has this facility already been constructed? \blacksquare Yes \Box No	1.b If yes to question 1.a, is it currently operating in New Mexico? \blacksquare Yes \Box No
2	If yes to question 1.a, was the existing facility subject to a Notice of Intent (NOI) (20.2.73 NMAC) before submittal of this application? □ Yes ☑ No	If yes to question 1.a, was the existing facility subject to a construction permit (20.2.72 NMAC) before submittal of this application? ✓ Yes □ No
3	Is the facility currently shut down? \Box Yes \blacksquare No	If yes, give month and year of shut down (MM/YY): N/A
4	Was this facility constructed before 8/31/1972 and continuously operated s	since 1972? □ Yes 🗹 No
5	If Yes to question 3, has this facility been modified (see 20.2.72.7.P NMA) \Box Yes \Box No \blacksquare N/A It is assumed this question refers to question 4 rather	
6	Does this facility have a Title V operating permit (20.2.70 NMAC)? \blacksquare Yes \Box No	If yes, the permit No. is: P195-R3-M2
7	Has this facility been issued a No Permit Required (NPR)? □ Yes ☑ No	If yes, the NPR No. is: N/A
8	Has this facility been issued a Notice of Intent (NOI)? \Box Yes \blacksquare No	If yes, the NOI No. is: N/A
9	Does this facility have a construction permit (20.2.72/20.2.74 NMAC)? \blacksquare Yes \Box No	If yes, the permit No. is: 1032-M9-R5
10	Is this facility registered under a General permit (GCP-1, GCP-2, etc.)? □ Yes ☑ No	If yes, the register No. is: N/A

Section 1-C: Facility Input Capacity & Production Rate

1	What is the facility's maximum input capacity, specify units (reference here and list capacities in Section 20, if more room is required)								
а	Current	Current Hourly: 6.6 MMCF ^(a) Daily: 157.2 MMCF ^(a) Annually: 57,380 MMCF ^(a)							
b	Proposed Hourly: 6.6 MMCF ^(a) Daily: 157.2 MMCF ^(a) Annually: 57,380 MMCF ^(a)								
2	2 What is the facility's maximum production rate, specify units (reference here and list capacities in Section 20, if more room is required)								
a	a Current Hourly: 6.6 MMCF ^(a) Daily: 157.2 MMCF ^(a) Annually: 57,380 MMCF ^(a)								
b	Proposed Hourly: 6.6 MMCF ^(a) Daily: 157.2 MMCF ^(a) Annually: 57,380 MMCF ^(a)								

^(a) The station capacity is a direct function of available horsepower. The throughput is therefore dependent on atmospheric temperature and pressure, gas temperature and pressure, relative humidity and gas quality, was well as other factors. The

"throughput" expressed above is a nominal quantity (with a 15 percent safety factor), neither an absolute maximum, nor an average. Actual throughput will vary from the nominal amount.

		V							
1	Section: 34	Range: 07W	Township: 32N	County: San Juan	Elevation (ft): 6,740				
2	UTM Zone:	12 or 🗹 13		Datum: NAD 27 NAD 83 WGS 84					
а	UTM E (in meter	rs, to nearest 10 meter	s): 271,970 m	UTM N (in meters, to nearest 10 meters):	4,090,325 m				
b	AND Latitude	(deg., min., sec.):	36° 55' 53"	Longitude (deg., min., sec.): -107° 3	33' 37"				
3	Name and zip code of nearest New Mexico town: Navajo Dam, New Mexico 87419								
4	4 Detailed Driving Instructions from nearest NM town (attach a road map if necessary): From Aztec, drive north on Hwy 550 to Colorado 318. Turn right and drive to a "T" junction at Colorado 172 (Approx. 15 miles). Turn left, drive into Ignacio, and turn right on 151 to mile marker 11.9. Turn right on 330. Drive 1.9 miles to the NM line, turn right on 4020. Drive 5.1 miles to the "Y" and turn right. Drive 2.1 miles & turn left. The site is 0.3 miles on right.								
5	The facility is approximately ~9 miles north-northeast of Navajo Dam, New Mexico.								
6	Status of land at facility (check one): 🗹 Private 🗆 Indian/Pueblo 🗆 Federal BLM 🗆 Federal Forest Service 🗆 Other (specify)								
7	List all municipalities, Indian tribes, and counties within a ten (10) mile radius (20.2.72.203.B.2 NMAC) of the property on which the facility is proposed to be constructed or operated: None; So. Ute Tribe; San Juan Co. & Rio Arriba Co.								
8	than 50 km (31	miles) to other st	ates, Bernalillo County, or	ich the facility is proposed to be constr a Class I area (see <u>www.env.nm.gov/aqb/n</u> corresponding distances in kilometers	nodeling/class1areas.html)?				
9	Name nearest C	Class I area: Wen	ninuche Wilderness						
10	Shortest distance	ce (in km) from fa	acility boundary to the boundary	ndary of the nearest Class I area (to the	nearest 10 meters): 53.83 km				
11				ions (AO is defined as the plant site in est residence, school or occupied struct					
12	Method(s) used to delineate the Restricted Area: Fence "Restricted Area" is an area to which public entry is effectively precluded. Effective barriers include continuous fencing,								
13	□ Yes ☑ No A portable stati	onary source is n	ot a mobile source, such as	oortable stationary source as defined in an automobile, but a source that can b such as a hot mix asphalt plant that is	be installed permanently at				
14			nction with other air regul nit number (if known) of th	ated parties on the same property? ☑ ne other facility? N/A	No 🗆 Yes				

Section 1-D: Facility Location Information

Section 1-E: Proposed Operating Schedule (The 1-E.1 & 1-E.2 operating schedules may become conditions in the permit.)

1	Facility maximum operating $\left(\frac{\text{hours}}{\text{day}}\right)$: 24	$\left(\frac{\text{days}}{\text{week}}\right)$: 7	$(\frac{\text{weeks}}{\text{year}})$: 52		$(\frac{\text{hours}}{\text{year}})$: 8,760		
2	Facility's maximum daily operating schedule (if les	AM PM	End: N/A	AM PM			
3	3 Month and year of anticipated start of construction: N/A						
4	Month and year of anticipated construction completion: N/A						
5	Month and year of anticipated startup of new or modified facility: N/A						
6	Will this facility operate at this site for more than or	ne year? 🗹 Yes 🗆 No					

Section 1-F: Other Facility Information

1	Are there any current Notice of Violations (NOV), compliance orders, or any other compliance or enforcement issues related to this facility? Ves No If yes, specify: N/A						
а	If yes, NOV date or description of issue: N/A			NOV Tracking No: N/A			
b	Is this application in response to any issue listed in 1-F, 1 of	or 1a above? 🗆 Yes	☑ No If Y	Yes, provide the 1c & 1d info below:			
с	Document Title: N/A	Date: N/A	Requirer (or page	ment # # and paragraph #): N/A			
d	Provide the required text to be inserted in this permit: N/A						
2	Is air quality dispersion modeling or modeling waiver bein	g submitted with this	applicatio	n? 🗆 Yes 🗹 No			
3	Does this facility require an "Air Toxics" permit under 20.2.72.400 NMAC & 20.2.72.502, Tables A and/or B? 🗆 Yes 🗹 No						
4	Will this facility be a source of federal Hazardous Air Poll	utants (HAP)? 🗹 Ye	es 🗆 No				
a	If Yes, what type of source? \square Major ($\square \ge 10$ tpy of any single HAP OR $\square \ge 25$ tpy of any combination of HAPS) OR \square Minor ($\square < 10$ tpy of any single HAP AND $\square < 25$ tpy of any combination of HAPS)						
5	Is any unit exempt under 20.2.72.202.B.3 NMAC? Ves No						
a	If yes, include the name of company providing commercia Commercial power is purchased from a commercial utility site for the sole purpose of the user.						

Section 1-G: Streamline Application (This section applies to 20.2.72.300 NMAC Streamline applications only)

Section 1-H: Current Title V Information - Required for all applications from TV Sources (Title V-source required information for all applications submitted pursuant to 20.2.72 NMAC (Minor Construction Permits), or 20.2.74/20.2.79 NMAC (Major PSD/NNSR applications), and/or 20.2.70 NMAC (Title V)

1	Responsible Official (R.O.) (20.2.70.300.D.2 NMAC): Travis Jones		Phone: (713) 289-2630			
a	R.O. Title: EH&S Manager R.O. e-mail: trjones@harvestmidstream.com					
b	R. O. Address: 1111 Travis Street, Houston, Texas 77002					
2	Alternate Responsible Official (20.2.70.300.D.2 NMAC): TBD		Phone: TBD			
а	A. R.O. Title: TBD	A. R.O. e-mail: T	BD			
b	A. R. O. Address: TBD					
3	Company's Corporate or Partnership Relationship to any other Air have operating (20.2.70 NMAC) permits and with whom the applic relationship): N/A	cant for this permit h	as a corporate or partnership			
4	Name of Parent Company ("Parent Company" means the primary name of the organization that owns the company to be					
а						
5	Names of Subsidiary Companies ("Subsidiary Companies" means organizations, branches, divisions or subsidiaries, which are owned, wholly or in part, by the company to be permitted.): N/A					
6	Telephone numbers & names of the owners' agents and site contact	ts familiar with plan	t operations: N/A			
7	Affected Programs to include Other States, local air pollution contribution Will the property on which the facility is proposed to be constructed states, local pollution control programs, and Indian tribes and puebones and provide the distances in kilometers: Yes. Colorado (7.5 (32.4 km), Navajo Nation Tribal lands (34.2 km), Ute Mountain Uter States (34.2 km), Ute Mountain Uter States (34.2 km), Uter States (d or operated be clo los (20.2.70.402.A.2 km); Southern Ute	ser than 80 km (50 miles) from other 2 and 20.2.70.7.B)? If yes, state which			

Section 1-I – Submittal Requirements

Each 20.2.73 NMAC (**NOI**), a 20.2.70 NMAC (**Title V**), a 20.2.72 NMAC (**NSR** minor source), or 20.2.74 NMAC (**PSD**) application package shall consist of the following:

Hard Copy Submittal Requirements:

- One hard copy original signed and notarized application package printed double sided 'head-to-toe' <u>2-hole punched</u> as we bind the document on top, not on the side; except Section 2 (landscape tables), which should be head-to-head. Please use numbered tab separators in the hard copy submittal(s) as this facilitates the review process. For NOI submittals only, hard copies of UA1, Tables 2A, 2D & 2F, Section 3 and the signed Certification Page are required. Please include a copy of the check on a separate page.
- 2) If the application is for a minor NSR, PSD, NNSR, or Title V application, include one working hard **copy** for Department use. This <u>copy</u> should be printed in book form, 3-hole punched, and <u>must be double sided</u>. Note that this is in addition to the head-toto 2-hole punched copy required in 1) above. Minor NSR Technical Permit revisions (20.2.72.219.B NMAC) only need to fill out Sections 1-A, 1-B, 3, and should fill out those portions of other Section(s) relevant to the technical permit revision. TV Minor Modifications need only fill out Sections 1-A, 1-B, 1-H, 3, and those portions of other Section(s) relevant to the minor modification. NMED may require additional portions of the application to be submitted, as needed.
- 3) The entire NOI or Permit application package, including the full modeling study, should be submitted electronically. Electronic files for applications for NOIs, any type of General Construction Permit (GCP), or technical revisions to NSRs must be submitted with compact disk (CD) or digital versatile disc (DVD). For these permit application submittals, two CD copies are required (in sleeves, not crystal cases, please), with additional CD copies as specified below. NOI applications require only a single CD submittal. Electronic files for other New Source Review (construction) permits/permit modifications or Title V permits/permit modifications can be submitted on CD/DVD or sent through AQB's secure file transfer service.

Electronic files sent by (check one):

☑ CD/DVD attached to paper application

□ secure electronic transfer. Air Permit Contact Name_____

E			
Email			
Linun			

Phone number_____

a. If the file transfer service is chosen by the applicant, after receipt of the application, the Bureau will email the applicant with instructions for submitting the electronic files through a secure file transfer service. Submission of the electronic files through the file transfer service needs to be completed within 3 business days after the invitation is received, so the applicant should ensure that the files are ready when sending the hard copy of the application. The applicant will not need a password to complete the transfer. **Do not use the file transfer service for NOIs, any type of GCP, or technical revisions to NSR permits.**

- 4) Optionally, the applicant may submit the files with the application on compact disk (CD) or digital versatile disc (DVD) following the instructions above and the instructions in 5 for applications subject to PSD review.
- 5) If air dispersion modeling is required by the application type, include the NMED Modeling Waiver and/or electronic air dispersion modeling report, input, and output files. The dispersion modeling <u>summary report only</u> should be submitted as hard copy(ies) unless otherwise indicated by the Bureau.
- 6) If the applicant submits the electronic files on CD and the application is subject to PSD review under 20.2.74 NMAC (PSD) or NNSR under 20.2.79 NMC include,
 - a. one additional CD copy for US EPA,
 - b. one additional CD copy for each federal land manager affected (NPS, USFS, FWS, USDI) and,
 - c. one additional CD copy for each affected regulatory agency other than the Air Quality Bureau.

If the application is submitted electronically through the secure file transfer service, these extra CDs do not need to be submitted.

Electronic Submittal Requirements [in addition to the required hard copy(ies)]:

- 1) All required electronic documents shall be submitted as 2 separate CDs or submitted through the AQB secure file transfer service. Submit a single PDF document of the entire application as submitted and the individual documents comprising the application.
- 2) The documents should also be submitted in Microsoft Office compatible file format (Word, Excel, etc.) allowing us to access the text and formulas in the documents (copy & paste). Any documents that cannot be submitted in a Microsoft Office compatible format shall be saved as a PDF file from within the electronic document that created the file. If you are unable to provide

Microsoft office compatible electronic files or internally generated PDF files of files (items that were not created electronically: i.e. brochures, maps, graphics, etc.), submit these items in hard copy format. We must be able to review the formulas and inputs that calculated the emissions.

- 3) It is preferred that this application form be submitted as 4 electronic files (3 MSWord docs: Universal Application section 1 [UA1], Universal Application section 3-19 [UA3], and Universal Application 4, the modeling report [UA4]) and 1 Excel file of the tables (Universal Application section 2 [UA2]). Please include as many of the 3-19 Sections as practical in a single MS Word electronic document. Create separate electronic file(s) if a single file becomes too large or if portions must be saved in a file format other than MS Word.
- 4) The electronic file names shall be a maximum of 25 characters long (including spaces, if any). The format of the electronic Universal Application shall be in the format: "A-3423-FacilityName". The "A" distinguishes the file as an application submittal, as opposed to other documents the Department itself puts into the database. Thus, all electronic application submittals should begin with "A-". Modifications to existing facilities should use the core permit number (i.e. '3423') the Department assigned to the facility as the next 4 digits. Use 'XXXX' for new facility applications. The format of any separate electronic submittals (additional submittals such as non-Word attachments, re-submittals, application updates) and Section document shall be in the format: "A-3423-9-description", where "9" stands for the section # (in this case Section 9-Public Notice). Please refrain, as much as possible, from submitting any scanned documents as this file format is extremely large, which uses up too much storage capacity in our database. Please take the time to fill out the header information throughout all submittals as this will identify any loose pages, including the Application Date (date submitted) & Revision number (0 for original, 1, 2, etc.; which will help keep track of subsequent partial update(s) to the original submittal. Do not use special symbols (#, @, etc.) in file names. The footer information should not be modified by the applicant.

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Table 2-A: Regulated Emission Sources

Unit and stack numbering must correspond throughout the application package. If applying for a NOI under 20.2.73 NMAC, equipment exemptions under 2.72.202 NMAC do not apply.

Unit Number ¹	Source Description	Make	Model #	Serial #	Manufact- urer's Rated Capacity ³ (Specify Units)	Requested Permitted Capacity ³ (Specify Units)	Date of Manufacture ² Date of Construction/ Reconstruction ²	Controlled by Unit # Emissions vented to Stack #	Source Classi- fication Code (SCC)	For Each Piece of Equipment, Check One	RICE Ignition Type (CI, SI, 4SLB, 4SRB, 2SLB) ⁴	Replacing Uni No.														
1	Compressor Engine	Waukesha	7042GL	TBD	1,478 hp	1,357 hp	TBD	N/A	20200202	X Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit	4SLB	N/A														
1	Compressor Engine	W dulcoshu	7012GE	TDD	1,170 пр	1,557 np	TBD	1	20200202	□ To Be Modified □ To be Replaced	ISED	10/11														
2	Compressor Engine	Waukesha	7042GL	C-10607/4	1,478 hp	1,357 hp	5/15/1992	N/A	20200202	X Existing (unchanged)	4SLB	N/A														
2			701202	(Pkg. X00009)	1,170 lip	1,507 np	5/15/1992	2		□ To Be Modified □ To be Replaced		1011														
3	Compressor Engine	Waukesha	7042GL	402862	1,478 hp	1,357 hp	12/4/1990	N/A	20200202	X Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit	4SLB	N/A														
J			701202	(Pkg. 76540)	1,170 lip	1,507 np	12/4/1990	3		□ To Be Modified □ To be Replaced		1011														
4	Compressor Engine	Waukesha	7042GL	C-10413/3	1,478 hp	1,357 hp	9/23/1991	N/A	20200202	X Existing (unchanged)	4SLB	N/A														
			701202	(Pkg. X00060)	1,170 lip	1,507 np	9/23/1991	4		□ To Be Modified □ To be Replaced		1.011														
5	Compressor Engine	Waukesha	7042GL	TBD	1,478 hp	1,357 hp	TBD	N/A	20200202	X Existing (unchanged)	4SLB	N/A														
5	Compressor Engine	waukesha	704202	TDD	1,470 np	1,557 np	TBD	5	20200202	□ To Be Modified □ To be Replaced	TOLD	1071														
6	Compressor Engine	Waukesha	7042GL	C-12553/5	1,478 hp	1,357 hp	2/18/1998	N/A	20200202	X Existing (unchanged)	4SLB	N/A														
0	Compressor Engine	waukesna	7042GL	(Pkg. X00022)	1,478 np	1,557 np	2/18/1998	6	20200202	□ To Be Modified □ To be Replaced	45LB	IN/A														
7		Washaaba	704201	C-338549	1 470 1	1.257.1	8/26/1998	7	20200202	20200202	X Existing (unchanged)	461 D	NT/ A													
7	Compressor Engine	Waukesha	7042GL	(Pkg. X00097)	1,478 hp	1,357 hp	8/26/1998	7			 New/Additional Replacement Unit To Be Modified To be Replaced 	4SLB	N/A													
							TBD	8	2020020	20200200	X Existing (unchanged)															
8	Compressor Engine	Waukesha	7042GL	2GL TBD 1,478 hp 1,357 hp TBD 8	8	20200202	 New/Additional Replacement Unit To Be Modified To be Replaced 	4SLB	N/A																	
				C-12679/2			9/24/1998	13																X Existing (unchanged)		
13	Compressor Engine	Waukesha	7042GL	(Pkg. X00098)	1,478 hp	1,357 hp	9/24/1998	13	20200202	 New/Additional Replacement Unit To Be Modified To be Replaced 	4SLB	N/A														
				C-12703/1			11/19/1998	15		X Existing (unchanged)																
15	Compressor Engine	Waukesha	7042GL	(Pkg. X00033)	1,478 hp	1,357 hp	11/19/1998	15	20200202	 New/Additional Replacement Unit To Be Modified To be Replaced 	4SLB	N/A														
							TBD	16		X Existing (unchanged)																
16	Compressor Engine	Waukesha	7042GL	TBD	1,478 hp	1,357 hp	TBD	16	20200202	 New/Additional Replacement Unit To Be Modified To be Replaced 	4SLB	N/A														
							TBD	18		X Existing (unchanged)																
18	Compressor Engine	Waukesha	7042GL	TBD	1,478 hp	1,357 hp	TBD	18	20200202	 New/Additional Replacement Unit To Be Modified To be Replaced 	4SLB	N/A														
				C-11474/1			10/17/1994	19		X Existing (unchanged) □ To be Removed																
19	Compressor Engine	Waukesha	7042GL	(Pkg. X00118)	1,478 hp	1,357 hp	10/17/1994	19	20200202	 New/Additional Replacement Unit To Be Modified To be Replaced 	4SLB	N/A														
				C-12572/2			2/27/1998	20		X Existing (unchanged) □ To be Removed																
20	Compressor Engine	Waukesha	7042GL	(Pkg. X00117)	1,478 hp	1,357 hp	2/27/1998	20	20200202	 New/Additional Replacement Unit To Be Modified To be Replaced 	4SLB	N/A														
				C-11906/1			6/6/1996	20		X Existing (unchanged) □ To be Removed																
21	Compressor Engine	Waukesha	7042GL	(Pkg. X00037)	1,478 hp	1,357 hp	6/6/1996	21	20200202	- 1	4SLB	N/A														
				/			TBD	21	-	To Be Modified To be Replaced X Existing (unchanged) To be Removed																
22	Compressor Engine	Waukesha	7042GL	TBD	1,478 hp	1,357 hp	TBD	2	2	22 20200202	□ New/Additional □ Replacement Unit	4SLB	N/A													
			+				TBD	22		To Be Modified To be Replaced X Existing (unchanged) To be Removed																
23	Compressor Engine	Waukesha	7042GL	TBD	1,478 hp	1,357 hp			20200202	□ New/Additional □ Replacement Unit	4SLB	N/A														
20	Compressor Engine		/01202	155	1,170 Hp	1,507 np	TBD	23		□ To Be Modified □ To be Replaced	1028	1.														

					Manufact- urer's Rated	Requested Permitted	Date of Manufacture ²	Controlled by Unit #	Source Classi-		RICE Ignition Type (CI, SI,	Replacing Uni
Unit Number ¹	Source Description	Make	Model #	Serial #	Capacity ³ (Specify Units)	Capacity ³ (Specify Units)	Date of Construction/ Reconstruction ²	Emissions vented to Stack #	fication Code (SCC)	For Each Piece of Equipment, Check One	4SLB, 4SRB, 2SLB) ⁴	No.
SSM	Compressors & Associated	N/A	N/A	N/A	N/A	N/A	N/A	N/A	31000299	Existing (unchanged) To be Removed New/Additional Replacement Unit	N/A	N/A
33141	Piping	19/24	11/24	IV/A	19/24	IN/A	N/A	N/A	51000255	X To Be Modified To be Replaced 	INA	11/74
9a	Dehydrator Still Vent	Enertek	J2P12M1	41662	12 mmcfd	12 mmcfd	4/1/1992	N/A	31000227	X Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit	N/A	N/A
98	Denydrator Still Vent	Lifertek	1109	41002	12 minera	12 minera	4/1/1992	9a	51000227	□ To Be Modified □ To be Replaced	IN/A	IN/A
9b	Dehydrator Reboiler	Enertek	J2P12M1	41662	1,208 scfh	1,208 scfh	4/1/1992	N/A	31000228	X Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit	N/A	N/A
90	Deliyurator Reboner	Lifertek	1109	41002	1,208 Selli	1,208 Sem	4/1/1992	9b	51000228	□ To Be Modified □ To be Replaced	18/24	IN/ A
10		E (1	J2P12M1	41000	12 61	10 01	11/1/1992	N/A		X Existing (unchanged)	27/4	27/4
10a	Dehydrator Still Vent	Enertek	1109	41999	12 mmcfd	12 mmcfd	11/1/1992	10a	31000227	New/Additional Replacement Unit To Be Modified To be Replaced	N/A	N/A
			J2P12M1				11/1/1992	N/A		X Existing (unchanged)		
10b	Dehydrator Reboiler	Enertek	1109	41999	1,208 scfh	1,208 scfh	11/1/1992	10b	31000228	Image: New/Additional Image: Replacement Unit Image: To Be Modified Image: To be Replaced	N/A	N/A
			J2P20M1				10/1/1993	N/A		X Existing (unchanged) To be Removed		
11a	Dehydrator Still Vent	Enertek	1109	42670	20 mmcfd	20 mmcfd	10/1/1993	11a	31000227	New/Additional Replacement Unit Ta Ba Madified Ta ba Bardward	N/A	N/A
			100000111				10/1/1993	N/A		□ To Be Modified □ To be Replaced X Existing (unchanged) □ To be Removed		
11b	Dehydrator Reboiler	Enertek	J2P20M1 1109	42670	1,648 scfh	1,648 scfh	10/1/1993	11b	31000228	New/Additional Replacement Unit	N/A	N/A
										□ To Be Modified □ To be Replaced X Existing (unchanged) □ To be Removed		
12a	Dehydrator Still Vent	Enertek	J2P20M1 1109	3869-C	20 mmcfd	20 mmcfd	Not available	N/A	31000227	□ New/Additional □ Replacement Unit	N/A	N/A
			1109				Not available	12a		□ To Be Modified □ To be Replaced		
12b	Dehydrator Reboiler	Enertek	J2P20M1	3869-C	1,648 scfh	1,648 scfh	Not available	N/A	31000228	X Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit	N/A	N/A
			1109		·		Not available	12b		□ To Be Modified □ To be Replaced		
24a	Dehydrator Still Vent	Enertek	J2P20M1	42268	20 mmcfd	20 mmcfd	Not available	N/A	31000227	X Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit	N/A	N/A
244	Denydrator Still Vent	Lifertex	1109	42200	20 millerd	20 millerd	Not available	24a	01000227	□ To Be Modified □ To be Replaced	1074	10/74
241		E. th	J2P20M1	422(8	1 (49 9	1 (49 0	3/1/1993	N/A	31000228	X Existing (unchanged)	21/4	NT/ A
24b	Dehydrator Reboiler	Enertek	1109	42268	1,648 sefh	1,648 scfh	3/1/1993	24b	31000228	New/Additional Replacement Unit To Be Modified To be Replaced	N/A	N/A
			J2P20M1				TBD	N/A		X Existing (unchanged)		
25a	Dehydrator Still Vent	Enertek	1109	TBD	20 mmcfd	20 mmcfd	TBD	25a	31000227	New/Additional Replacement Unit To Be Modified To be Replaced	N/A	N/A
			J2P20M1				TBD	N/A		X Existing (unchanged) □ To be Removed		
25b	Dehydrator Reboiler	Enertek	1109	TBD	1,648 scfh	1,648 scfh	TBD	25b	31000228	New/Additional Replacement Unit To Be Modified To be Replaced	N/A	N/A
	D 1 1W/ C		27.1				3/1/1992	230 N/A		X Existing (unchanged) To be Removed		
T-38	Produced Water Storage Tank	Not available	Not available	Not available	300 bbl	300 bbl	1993	T38	40400315	□ New/Additional □ Replacement Unit	N/A	N/A
								138 N/A		□ To Be Modified □ To be Replaced X Existing (unchanged) □ To be Removed		
T-39	Produced Water Storage Tank	Permian Tank & Mfg. Co.	Not available	24383	300 bbl	300 bbl	5/1/1991		40400315	□ New/Additional □ Replacement Unit	N/A	N/A
		Milg. Co.	avanable				5/1/1991	T39		□ To Be Modified □ To be Replaced X Existing (unchanged) □ To be Removed		
T-40	Produced Water Storage	Benchmark Eqpt &		3645	500 bbl	500 bbl	2015	N/A	40400315		N/A	N/A
	Tank	Tanks, Inc.	available				2015	T40		□ To Be Modified □ To be Replaced		
F-1	Fugitive Emissions	N/A	N/A	N/A	N/A	N/A	N/A	N/A	.	X Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit	N/A	N/A
	č						N/A	N/A		□ To Be Modified □ To be Replaced		
M-1	Malfunction Emissions	N/A	N/A	N/A	N/A	N/A	N/A	N/A	31000299	□ Existing (unchanged) X To be Removed □ New/Additional □ Replacement Unit	N/A	N/A
141-1	manufaction Emissions	11/11	11/11	11/21	11/71	11/71	N/A	N/A	51000239	□ To Be Modified □ To be Replaced	11/23	11/21

					Manufact- urer's Rated	Requested Permitted	Date of Manufacture ²	Controlled by Unit #	Classi-		RICE Ignition Type (CI, SI,	Replacing Unit
Unit Number ¹	Source Description	Make	Model #	Serial #	Capacity ³ (Specify Units)	Capacity ³ (Specify Units)	Date of Construction/ Reconstruction ²	Emissions vented to Stack #	fication Code (SCC)	For Each Piece of Equipment, Check One	4SLB, 4SRB, 2SLB) ⁴	No.
C1-8, C13. C15, C16, &	Reciptocating Compressor	N/A	N/A	N/A	N/A	N/A	N/A	N/A	21000200	X Existing (unchanged)	N/A	N/A
C13, C10, & C18 - 23	Venting	IN/A	IN/A	IN/A	IN/A	IN/A	N/A	N/A	51000299	□ To Be Modified □ To be Replaced	IN/A	IN/A
PC 1 -	Pneumatic Controllers	N/A	N/A	N/A	N/A	N/A	N/A	N/A	21000200	X Existing (unchanged) □ To be Removed □ New/Additional □ Replacement Unit	N/A	N/A
PC 116	i neumatic Controllers	18/24	19/24	18/24	11/24	11/24	N/A	N/A	31000233	□ To Be Modified □ To be Replaced	1 N/ PA	11/24

¹ Unit numbers must correspond to unit numbers in the previous permit unless a complete cross reference table of all units in both permits is provided.

² Specify dates required to determine regulatory applicability.

³ To properly account for power conversion efficiencies, generator set rated capacity shall be reported as the rated capacity of the engine in horsepower, not the kilowatt capacity of the generator set.

⁴ "4SLB" means four stroke lean burn engine, "4SRB" means four stroke rich burn engine, "2SLB" means two stroke lean burn engine, "CI" means compression ignition, and "SI" means spark ignition

Table 2-B: Insignificant Activities¹ (20.2.70 NMAC) OR Exempted Equipment (20.2.72 NMAC)

All 20.2.70 NMAC (Title V) applications must list all Insignificant Activities in this table. All 20.2.72 NMAC applications must list Exempted Equipment in this table. If equipment listed on this table is exempt under 20.2.72.202.B.5, include emissions calculations and emissions totals for 202.B.5 "similar functions" units, operations, and activities in Section 6, Calculations. Equipment and activities exempted under 20.2.72.202 NMAC may not necessarily be Insignificant under 20.2.70 NMAC (and vice versa). Unit & stack numbering must be consistent throughout the application package. Per Exemptions Policy 02-012.00 (see http://www.env.nm.gov/aqb/permit/aqb_pol.html), 20.2.72.202.B NMAC Exemptions do not apply, but 20.2.72.202.A NMAC exemptions do apply to NOI facilities under 20.2.73 NMAC. List 20.2.72.301.D.4 NMAC Auxiliary Equipment for Streamline applications in Table 2-A. The List of Insignificant Activities (for TV) can be found online at http://www.env.nm.gov/aqb/forms/InsignificantListTitleV.pdf. TV sources may elect to enter both TV Insignificant Activities and Part 72 Exemptions on this form.

Unit Number	Source Description	Manufacturer	Model No.	Max Capacity	List Specific 20.2.72.202 NMAC Exemption (e.g. 20.2.72.202.B.5)	Date of Manufacture /Reconstruction ²	For Each Piece of Equipment, Check Onc
	•		Serial No.	Capacity Units	Insignificant Activity citation (e.g. IA List Item #1.a)	Date of Installation /Construction ²	
T-1	Wastewater Storage Tank			165	20.2.72.202.B(2) NMAC		X Existing (unchanged) To be Removed New/Additional Replacement Unit
1-1	wastewater Storage Talik			bbl	Insignificant Activity List Item #5		□ To Be Modified □ To be Replaced
T-2	Used Oil Storage Tank			165	20.2.72.202.B(2) NMAC		X Existing (unchanged) To be Removed New/Additional Replacement Unit
12	osed on Storage Tank			bbl	Insignificant Activity List Item #5		□ To Be Modified □ To be Replaced
T-3	Lubrication Oil Storage Tank			100	20.2.72.202.B(2) NMAC		X Existing (unchanged) To be Removed New/Additional Replacement Unit
1-5	Luoncation On Storage Tank			bbl	Insignificant Activity List Item #5		□ To Be Modified □ To be Replaced
T 6 T 17				500	20.2.72.202.B(2) NMAC		X Existing (unchanged)
T-5 - T-17	Lubrication Oil Storage Tank			gal	Insignificant Activity List Item #5		 New/Additional Replacement Unit To Be Modified To be Replaced
m 40 m a 4	Triethylene Glycol (TEG)			100	20.2.72.202.B(2) NMAC		X Existing (unchanged)
T-18 - T-21	Storage Tank			gal	Insignificant Activity List Item #5		 New/Additional Replacement Unit To Be Modified To be Replaced
	Triethylene Glycol (TEG)			50	20.2.72.202.B(2) NMAC		X Existing (unchanged) To be Removed
T-22 - T-25	Storage Tank			gal	Insignificant Activity List Item #5		 New/Additional Replacement Unit To Be Modified To be Replaced
				500	20.2.72.202.B(5) NMAC		X Existing (unchanged) To be Removed
T-26	Methanol			gal	Insignificant Activity List Item #1		 New/Additional Replacement Unit To Be Modified To be Replaced
				500	20.2.72.202.B(2) NMAC		X Existing (unchanged)
T-27	Solvent Storage Tank			gal	Insignificant Activity List Item #5		 New/Additional Replacement Unit To Be Modified To be Replaced
	Triethylene Glycol (TEG)			500	20.2.72.202.B(2) NMAC		X Existing (unchanged) To be Removed
T-28	Storage Tank			gal	Insignificant Activity List Item #5		 New/Additional Replacement Unit To Be Modified To be Replaced
				500	20.2.72.202.B(2) NMAC		X Existing (unchanged)
T-29	Antifreeze Storage Tank			gal	Insignificant Activity List Item #5		 New/Additional Replacement Unit To Be Modified To be Replaced
				500	20.2.72.202.B(2) NMAC		X Existing (unchanged) □ To be Removed
T-30 - T-33	Lubrication Oil Storage Tank			gal	Insignificant Activity List Item #5		 New/Additional Replacement Unit To Be Modified To be Replaced
	Triethylene Glycol (TEG)			100	20.2.72.202.B(2) NMAC		X Existing (unchanged) To be Removed
T-34 - T-35	Storage Tank			gal	Insignificant Activity List Item #5		 New/Additional Replacement Unit To Be Modified To be Replaced
	Triethylene Glycol (TEG)			50	20.2.72.202.B(2) NMAC		X Existing (unchanged) To be Removed
T-36 - T-37	Storage Tank			gal	Insignificant Activity List Item #5		 New/Additional Replacement Unit To Be Modified To be Replaced
	-			gai N/A	20.2.72.202.B(5) NMAC		X Existing (unchanged) To be Removed
L-1	Truck Loading Emissions			N/A N/A	Insignificant Activity List Item #1		New/Additional Replacement Unit
				N/A N/A	20.2.72.202.B(5) NMAC		□ To Be Modified □ To be Replaced X Existing (unchanged) □ To be Removed
PR1	Pig Receiver						New/Additional Replacement Unit
				N/A	Insignificant Activity List Item #1		To Be Modified To be Replaced Existing (unchanged) To be Removed
							New/Additional Replacement Unit
							To Be Modified To be Replaced

¹ Insignificant activities exempted due to size or production rate are defined in 20.2.70.300.D.6, 20.2.70.7.Q NMAC, and the NMED/AQB List of Insignificant Activities, dated September 15, 2008. Emissions from these insignificant activities do not need to be reported, unless specifically requested.

² Specify date(s) required to determine regulatory applicability.

Table 2-C: Emissions Control Equipment

Unit and stack numbering must correspond throughout the application package. Only list control equipment for TAPs if the TAP's maximum uncontrolled emissions rate is over its respective threshold as listed in 20.2.72 NMAC, Subpart V, Tables A and B. In accordance with 20.2.72.203.A(3) and (8) NMAC, 20.2.70.300.D(5)(b) and (e) NMAC, and 20.2.73.200.B(7) NMAC, the permittee shall report all control devices and list each pollutant controlled by the control device regardless if the applicant takes credit for the reduction in emissions.

Control Equipment Unit No.	Control Equipment Description	Date Installed	Controlled Pollutant(s)	Controlling Emissions for Unit Number(s) ¹	Efficiency (% Control by Weight)	Method used to Estimate Efficiency
7	Oxidation Catalytic Converter	8/26/1998	CO, VOC, HCHO	7	CO >93%; VOC >79%; HCHO >79%	Mfg. specs
8	Oxidation Catalytic Converter	10/15/1998	CO, VOC, HCHO	8	CO >93%; VOC >79%; HCHO >79%	Mfg. specs
13	Oxidation Catalytic Converter	10/24/1996	CO, VOC, HCHO	13	CO >90%; VOC >80%; HCHO >80%	Mfg. specs
15	Oxidation Catalytic Converter	5/5/2000	CO, VOC, HCHO	15	CO >93%; VOC >79%; HCHO >79%	Mfg. specs
16	Oxidation Catalytic Converter	TBD	CO, VOC, HCHO	16	CO >93%; VOC >79%; HCHO >79%	Mfg. specs
18	Oxidation Catalytic Converter	TBD	CO, VOC, HCHO	18	CO >93%; VOC >79%; HCHO >79%	Mfg. specs
19	Oxidation Catalytic Converter	9/20/2004	CO, VOC, HCHO	19	CO >93%; VOC >79%; HCHO >79%	Mfg. specs
20	Oxidation Catalytic Converter	9/20/2004	CO, VOC, HCHO	20	CO >93%; VOC >79%; HCHO >79%	Mfg. specs
21	Oxidation Catalytic Converter	10/7/2004	CO, VOC, HCHO	21	CO >93%; VOC >79%; HCHO >79%	Mfg. specs
22	Oxidation Catalytic Converter	TBD	CO, VOC, HCHO	22	CO >93%; VOC >79%; HCHO >79%	Mfg. specs
23	Oxidation Catalytic Converter	TBD	CO, VOC, HCHO	23	CO >93%; VOC >79%; HCHO >79%	Mfg. specs

¹ List each control device on a separate line. For each control device, list all emission units controlled by the control device.

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Table 2-D: Maximum Emissions (under normal operating conditions)

□ This Table was intentionally left blank because it would be identical to Table 2-E.

Maximum Emissions are the emissions at maximum capacity and prior to (in the absence of) pollution control, emission-reducing process equipment, or any other emission reduction. Calculate the hourly emissions using the worst case hourly emissions for each pollutant. For each pollutant, calculate the annual emissions as if the facility were operating at maximum plant capacity without pollution controls for 8760 hours per year, unless otherwise approved by the Department. List Hazardous Air Pollutants (HAP) & Toxic Air Pollutants (TAPs) in Table 2-I. Unit & stack numbering must be consistent throughout the application package. Fill all cells in this table with the emission numbers or a "-" symbol. A "-" symbol indicates that emissions of this pollutant are not expected. Numbers shall be expressed to at least 2 decimal points (e.g. 0.41, 1.41, or 1.41E-4).

Unit No.	N	Dx	С	0	VC	DC	S	Ox	PI	M ¹	PM	[10 ¹	PM	2.5 ¹	Н	₂ S	Le	ead
Unit No.	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
1	2.7	11.8	8.2	36.1	3.0	13.1	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	-	-
2	2.7	11.8	8.2	36.1	3.0	13.1	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	-	-
3	2.7	11.8	8.2	36.1	3.0	13.1	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	-	-
4	2.7	11.8	8.2	36.1	3.0	13.1	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	-	-
5	2.7	11.8	8.2	36.1	3.0	13.1	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	-	-
6	2.7	11.8	8.2	36.1	3.0	13.1	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	-	-
7	2.7	11.8	8.2	36.1	3.0	13.1	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	-	-
8	2.7	11.8	8.2	36.1	3.0	13.1	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	-	-
13	2.7	11.8	8.2	36.1	3.0	13.1	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	-	-
15	2.7	11.8	8.2	36.1	3.0	13.1	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	-	-
16	2.7	11.8	8.2	36.1	3.0	13.1	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	-	-
18	2.7	11.8	8.2	36.1	3.0	13.1	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	-	-
19	2.7	11.8	8.2	36.1	3.0	13.1	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	-	-
20	2.7	11.8	8.2	36.1	3.0	13.1	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	-	-
21	2.7	11.8	8.2	36.1	3.0	13.1	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	-	-
22	2.7	11.8	8.2	36.1	3.0	13.1	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	-	-
23	2.7	11.8	8.2	36.1	3.0	13.1	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	-	-
SSM	-	-	-	-	-	6.37	-	-	-	-	-	-	-	-	-	-	-	-
9a ²	-	-	-	-	3.4	15.0	-	-	-	-	-	-	-	-	-	-	-	-
9b	4.3E-02	0.19	3.3E-02	0.14	4.8E-03	2.1E-02	8.3E-04	3.7E-03	9.2E-03	4.0E-02	9.2E-03	4.0E-02	9.2E-03	4.0E-02	-	-	-	-
10a ²	-	-	-	-	3.4	15.0	-	-	-	-	-	-	-	-	-	-	-	-
10b	4.3E-02	0.19	3.3E-02	0.14	4.8E-03	2.1E-02	8.3E-04	3.7E-03	9.2E-03	4.0E-02	9.2E-03	4.0E-02	9.2E-03	4.0E-02	-	-	-	-
11a ²	-	-	-	-	3.5	15.3	-	-	-	-	-	-	-	-	-	-	-	-
11b	4.3E-02	0.19	4.5E-02	0.20	6.5E-03	2.8E-02	8.3E-04	3.7E-03	1.3E-02	5.5E-02	1.3E-02	5.5E-02	1.3E-02	5.5E-02	-	-	-	-

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Unit No.	NO	Ox	С	0	VO	DC	SC	Dx	PN	M ¹	PM	[10 ¹	PM	2.5 ¹	Н	$_{2}S$	Le	ead
	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
$12a^2$	-	-	-	-	3.5	15.3	-	-	-	-	-	-	-	-	-	-	-	-
12b	4.3E-02	0.19	4.5E-02	0.20	6.5E-03	2.8E-02	8.3E-04	3.7E-03	1.3E-02	5.5E-02	1.3E-02	5.5E-02	1.3E-02	5.5E-02	-	-	-	-
24a ²	-	-	-	-	3.5	15.3	-	-	-	-	-	-	-	-	-	-	-	-
24b	4.3E-02	0.19	4.5E-02	0.20	6.5E-03	2.8E-02	8.3E-04	3.7E-03	1.3E-02	5.5E-02	1.3E-02	5.5E-02	1.3E-02	5.5E-02	-	-	-	-
25a ²	-	-	-	-	3.5	15.3	-	-	-	-	-	-	-	-	-	-	-	-
25b	4.3E-02	0.19	4.5E-02	0.20	6.5E-03	2.8E-02	8.3E-04	3.7E-03	1.3E-02	5.5E-02	1.3E-02	5.5E-02	1.3E-02	5.5E-02	-	-	-	-
T-38	-	-	-	-	0.93	4.1	-	-	-	-	-	-	-	-	-	-	-	-
T-39	-	-	-	-	With T-38	With T-38	-	-	-	-	-	-	-	-	-	-	-	-
T-40					With T-38	With T-38												
F-1 ²	-	-	-	-	0.91	4.00	-	-	-	-	-	-	-	-	-	-	-	-
Totals	46.16	201.73	140.15	613.92	73.55	328.61	0.11	0.46	1.77	7.75	1.77	7.75	1.77	7.75	-	-	-	-

¹Condensable Particulate Matter: Include condensable particulate matter emissions for PM10 and PM2.5 if the source is a combustion source. Do not include condensable particulate matter for PM unless PM is set equal to PM10 and PM2.5. Particulate matter (PM) is not subject to an ambient air quality standard, but PM is a regulated air pollutant under PSD (20.2.74 NMAC) and Title V (20.2.70 NMAC).

² The VOC emission rate(s) of dehydrators (units 9a, 10a, 11a, 12a, 24a, & 25a) and fugitive emissions (unit F-1) are carried forward from Operating Permit P195-R3.

Table 2-E: Requested Allowable Emissions

Unit & stack numbering must be consistent throughout the application package. Fill all cells in this table with the emission numbers or a "-" symbol. A "-" symbol indicates that emissions of this pollutant are not expected. Numbers shall be expressed to at least 2 decimal points (e.g. 0.41, 1.41, or 1.41E⁻⁴).

Unit No.	N	Dx	С	0	V	DC	S	Ox	PI	M ¹	PM	[10 ¹	PM	2.5 ¹	Н	₂ S	Le	ead
Unit No.	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
1	2.7	11.8	8.2	36.1	3.0	13.1	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	-	-
2	2.7	11.8	8.2	36.1	3.0	13.1	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	I	-
3	2.7	11.8	8.2	36.1	3.0	13.1	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	I	-
4	2.7	11.8	8.2	36.1	3.0	13.1	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	I	-
5	2.7	11.8	8.2	36.1	3.0	13.1	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	-	-
6	2.7	11.8	8.2	36.1	3.0	13.1	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	-	-
7	2.7	11.8	0.6	2.5	0.6	2.8	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	1	-
8	2.7	11.8	0.6	2.5	0.6	2.8	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	-	-
13	2.7	11.8	0.8	3.6	0.6	2.6	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	-	-
15	2.7	11.8	0.6	2.5	0.6	2.8	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	-	-
16	2.7	11.8	0.6	2.5	0.6	2.8	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	-	-
18	2.7	11.8	0.6	2.5	0.6	2.8	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	-	-
19	2.7	11.8	0.6	2.5	0.6	2.8	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	-	-
20	2.7	11.8	0.6	2.5	0.6	2.8	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	-	-
21	2.7	11.8	0.6	2.5	0.6	2.8	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	-	-
22	2.7	11.8	0.6	2.5	0.6	2.8	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	-	-
23	2.7	11.8	0.6	2.5	0.6	2.8	5.9E-03	2.6E-02	0.10	0.44	0.10	0.44	0.10	0.44	-	-	-	-
SSM	-	-	-	-	-	6.37	-	-	I	-	-	-	I	-	-	-	I	-
9a ²	-	-	-	-	3.4	15.0	-	-	-	-	-	-	-	-	-	-	-	-
9b	4.3E-02	0.19	3.3E-02	0.14	4.8E-03	2.1E-02	8.3E-04	3.7E-03	9.2E-03	4.0E-02	9.2E-03	4.0E-02	9.2E-03	4.0E-02	-	-	-	-
$10a^2$	-	-	-	-	3.4	15.0	-	-	-	-	-	-	-	-	-	-	-	-
10b	4.3E-02	0.19	3.3E-02	0.14	4.8E-03	2.1E-02	8.3E-04	3.7E-03	9.2E-03	4.0E-02	9.2E-03	4.0E-02	9.2E-03	4.0E-02	-	-	-	-
$11a^2$	-	-	-	-	3.5	15.3	-	-	-	-	-	-	-	-	-	-	-	-
11b	4.3E-02	0.19	4.5E-02	0.20	6.5E-03	2.8E-02	8.3E-04	3.7E-03	1.3E-02	5.5E-02	1.3E-02	5.5E-02	1.3E-02	5.5E-02	-	-	-	-
$12a^2$	-	-	-	-	3.5	15.3	-	-	-	-	-	-	-	-	-	-	-	-

Unit No.	NO	Ox	С	0	V	DC	SC	Ox	P	M ¹	PM	10 ¹	PM	2.5 ¹	Н	₂ S	Le	ead
Unit No.	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
12b	4.3E-02	0.19	4.5E-02	0.20	6.5E-03	2.8E-02	8.3E-04	3.7E-03	1.3E-02	5.5E-02	1.3E-02	5.5E-02	1.3E-02	5.5E-02	-	-	-	-
24a ²	-	-	-	-	3.5	15.3	-	-	-	-	-	-	-	-	-	-	-	-
24b	4.3E-02	0.19	4.5E-02	0.20	6.5E-03	2.8E-02	8.3E-04	3.7E-03	1.3E-02	5.5E-02	1.3E-02	5.5E-02	1.3E-02	5.5E-02	-	-	-	-
25a ²	-	-	-	-	3.5	15.3	-	-	-	-	-	-	-	-	-	-	-	-
25b	4.3E-02	0.19	4.5E-02	0.20	6.5E-03	2.8E-02	8.3E-04	3.7E-03	1.3E-02	5.5E-02	1.3E-02	5.5E-02	1.3E-02	5.5E-02	-	-	-	-
T-38	-	-	-	-	0.93	4.1	-	-	-	-	-	-	-	-	-	-	-	-
T-39	-	-	-	-	With T-38	With T-38	-	-	-	-	-	-	-	-	-	-	-	-
T-40					With T-38	With T-38	-	-	-	-	-	-	-	-	-	-	-	-
F-1 ²	-	-	-	-	0.91	4.0	-	-	-	-	-	-	-	-	-	-	-	-
Totals	46.16	201.73	56.20	246.50	47.56	214.98	0.11	0.46	1.77	7.75	1.77	7.75	1.77	7.75	-	-	-	-

¹Condensable Particulate Matter: Include condensable particulate matter emissions for PM10 and PM2.5 if the source is a combustion source. Do not include condensable particulate matter for PM unless PM is set equal to PM10 and PM2.5. Particulate matter (PM) is not subject to an ambient air quality standard, but it is a regulated air pollutant under PSD (20.2.74 NMAC) and Title V (20.2.70 NMAC).

² The VOC emission rate(s) of dehydrators (units 9a, 10a, 11a, 12a, 24a, & 25a) and fugitive emissions (unit F-1) are carried forward from Operating Permit P195-R3.

Table 2-F: Additional Emissions during Startup, Shutdown, and Routine Maintenance (SSM)

This table is intentionally left blank since all emissions at this facility due to routine or predictable startup, shutdown, or scenduled maintenance are no higher than those listed in Table 2-E and a malfunction emission limit is not already permitted or requested. If you are required to report GHG emissions as described in Section 6a, include any GHG emissions during Startup, Shutdown, and/or Scheduled Maintenance (SSM) in Table 2-P. Provide an explanations of SSM emissions in Section 6 and 6a.

All applications for facilities that have emissions during routine our predictable startup, shutdown or scheduled maintenance (SSM)¹, including NOI applications, must include in this table the Maximum Emissions during routine or predictable startup, shutdown and scheduled maintenance (20.2.7 NMAC, 20.2.72.203.A.3 NMAC, 20.2.73.200.D.2 NMAC). In Section 6 and 6a, provide emissions calculations for all SSM emissions reported in this table. Refer to "Guidance for Submittal of Startup, Shutdown, Maintenance Emissions in Permit Applications (https://www.env.nm.gov/aqb/permit/aqb pol.html) for more detailed instructions. Numbers shall be expressed to at least 2 decimal points (e.g. 0.41, 1.41, or 1.41E-4).

Unit No.	N	Ox	С	0	VC)C	S	Ox	PI	M ²	PM	(10 ²	PM	2.5 ²	Н	$_2S$	Le	ead
Unit No.	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
SSM	-	-	-	-	not specified	6.37	-	-	-	-	-	-	-	-	-	-	-	-
Totals	-	-	-	-	not specified	6.37	-	-	-	-	-	-	-	-	-	-	-	-

¹ For instance, if the short term steady-state Table 2-E emissions are 5 lb/hr and the SSM rate is 12 lb/hr, enter 7 lb/hr in this table. If the annual steady-state Table 2-E emissions are 21.9 TPY, and the number of scheduled SSM events result in annual emissions of 31.9 TPY, enter 10.0 TPY in the table below.

²Condensable Particulate Matter: Include condensable particulate matter emissions for PM10 and PM2.5 if the source is a combustion source. Do not include condensable particulate matter for PM unless PM is set equal to PM10 and PM2.5. Particulate matter (PM) is not subject to an ambient air quality standard, but it is a regulated air pollutant under PSD (20.2.74 NMAC) and Title V (20.2.70 NMAC).

Table 2-G: Stack Exit and Fugitive Emission Rates for Special Stacks

X I have elected to leave this table blank because this facility does not have any stacks/vents that split emissions from a single source or combine emissions from more than one source listed in table 2-A. Additionally, the emission rates of all stacks match the Requested allowable emission rates stated in Table 2-E.

Use this table to list stack emissions (requested allowable) from split and combined stacks. List Toxic Air Pollutants (TAPs) and Hazardous Air Pollutants (HAPs) in Table 2-1. List all fugitives that are associated with the normal, routine, and non-emergency operation of the facility. Unit and stack numbering must correspond throughout the application package. Refer to Table 2-E for instructions on use of the "-" symbol and on significant figures.

	l and on significant fig Serving Unit		Ox	С	0	V	DC	SO	Ox	P	М	PN	110	PM	12.5	\Box H ₂ S o	r 🗆 Lead
Stack No.	Number(s) from Table 2-A	lb/hr	ton/yr	lb/hr	ton/yr												
	Totals:																

Table 2-H: Stack Exit Conditions

Unit and stack numbering must correspond throughout the application package. Include the stack exit conditions for each unit that emits from a stack, including blowdown venting parameters and tank emissions. If the facility has multiple operating scenarios, complete a separate Table 2-H for each scenario and, for each, type scenario name here:

Stack	Serving Unit Number(s)	Orientation	Rain Caps	Height Above	Temp.	Flow	Rate	Moisture by	Velocity	Inside
Number	from Table 2-A	(H-Horizontal V=Vertical)	(Yes or No)	Ground (ft)	(F)	(acfs)	(dscfs)	Volume (%)	(ft/sec)	Diameter (ft)
1	1	V	No	22	701	125.8	-	-	153.7	1.02
2	2	V	No	22	701	125.8	-	-	153.7	1.02
3	3	V	No	22	701	125.8	-	-	153.7	1.02
4	4	V	No	22	701	125.8	-	-	153.7	1.02
5	5	V	No	22	701	125.8	-	-	153.7	1.02
6	6	V	No	22	701	125.8	-	-	153.7	1.02
7	7	V	No	22	701	125.8	-	-	153.7	1.02
8	8	V	No	22	701	125.8	-	-	153.7	1.02
13	9	V	No	22	701	125.8	-	-	153.7	1.02
15	17	V	No	22	701	125.8	-	-	153.7	1.02
16	18	V	No	22	701	125.8	-	-	153.7	1.02
18	19	V	No	22	701	125.8	-	-	153.7	1.02
19	20	V	No	22	701	125.8	-	-	153.7	1.02
20	21	V	No	22	701	125.8	-	-	153.7	1.02
21	22	V	No	22	701	125.8	-	-	153.7	1.02
22	23	V	No	22	701	125.8	-	-	153.7	1.02
23	24	V	No	22	701	125.8	-	-	153.7	1.02
9b	9b	V	No	10	600	3.33	-	-	6.1	0.83
10b	10b	V	No	10	600	3.33	-	-	6.1	0.83
11b	11b	V	No	10	600	4.79	-	-	6.1	1.00
12b	12b	V	No	10	600	4.79	-	-	6.1	1.00
24b	24b	V	No	10	600	4.79	-	-	6.1	1.00
25b	25b	V	No	10	600	4.79	-	-	6.1	1.00

Table 2-I: Stack Exit and Fugitive Emission Rates for HAPs and TAPs

In the table below, report the Potential to Emit for each HAP from each regulated emission unit listed in Table 2-A, only if the entire facility emits the HAP at a rate greater than or equal to one (1) ton per year For each such emission unit, HAPs shall be reported to the nearest 0.1 tpy. Each facility-wide Individual HAP total and the facility-wide Total HAPs shall be the sum of all HAP sources calculated to the nearest 0.1 ton per year. Per 20.2.72.403.A.1 NMAC, facilities not exempt [see 20.2.72.402.C NMAC] from TAP permitting shall report each TAP that has an uncontrolled emission rate in excess of its pounds per hour screening level specified in 20.2.72.502 NMAC. TAPs shall be reported using one more significant figure than the number of significant figures shown in the pound per hour threshold corresponding to the substance. Use the HAP nomenclature as it appears in Section 112 (b) of the 1990 CAAA and the TAP nomenclature as it listed in 20.2.72.502 NMAC. Include tank-flashing emissions estimates of HAPs in this table. For each HAP or TAP listed, fill all cells in this table with the emission numbers or a "-" symbol. A "-" symbol indicates that emissions of this pollutant are not expected or the pollutant is emitted in a quantity less than the threshold amounts described above.

Stack No.	Unit No.(s)	Total	HAPs	Formal X HAP o	dehyde or 🗆 TAP	Tolu X HAP o		Xyl X HAP o		Name	Pollutant e Here or 🛛 TAP		Pollutant Here or 🗆 TAP	Name	Pollutant Here or 🗆 TAP	Name	Pollutant e Here or 🗆 TAP	Name	Pollutant e Here or 🛛 TAP
		lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
1	1	0.5	2.3	0.5	2.2	-	-	-	-										
2	2	0.5	2.3	0.5	2.2	-	-	-	-										
3	3	0.5	2.3	0.5	2.2	-	-	-	-										
4	4	0.5	2.3	0.5	2.2	-	-	-	-										
5	5	0.5	2.3	0.5	2.2	-	-	-	-										
6	6	0.5	2.3	0.5	2.2	-	-	-	-										
7	7	0.1	0.5	0.1	0.5	-	-	-	-										
8	8	0.1	0.5	0.1	0.5	-	-	-	-										
13	13	0.1	0.5	0.1	0.4	-	-	-	-										
15	15	0.1	0.5	0.1	0.5	-	-	-	-										
16	16	0.1	0.5	0.1	0.5	-	-	-	-										
18	18	0.1	0.5	0.1	0.5	-	-	-	-										
19	19	0.1	0.5	0.1	0.5	-	-	-	-										
20	20	0.1	0.5	0.1	0.5	-	-	-	-										
21	21	0.1	0.5	0.1	0.5	-	-	-	-										
22	22	0.1	0.5	0.1	0.5	-	-	-	-										
23	23	0.1	0.5	0.1	0.5	-	-	-	-										
SSM	SSM	-	-	-	-	-	-	-	-										
9a	9a	0.2	0.8	-	-	0.1	0.3	0.1	0.5										
9b	9b	-	-	-	-	-	-	-	-										
10a	10a	0.2	0.8	-	-	0.1	0.3	0.1	0.5										
10b	10b	-	-	-	-	-	-	-	-										
11a	11a	0.2	0.8	-	-	0.1	0.3	0.1	0.5										

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Stack No.	Unit No.(s)	Total	HAPs	Formal X HAP o	ldehyde or □ TAP	Tolu X HAP o		•	lene or 🗆 TAP		Pollutant e Here or 🗆 TAP	Name		Name			Here	Name	Pollutant e Here or 🗆 TAP
		lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr lb/hr ton/yr		lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	
11b	11b	-	-	-	-	-	-	-	-										
12a	12a	0.2	0.8	-	-	0.1	0.3	0.1	0.5										
12b	12b	-	-	-	-	-	-	-	-										
24a	24a	0.2	0.8	-	-	0.1	0.3	0.1	0.5										
24b	24b	-	-	-	-	-	-	-	-										
25a	25a	0.2	0.8	-	-	0.1	0.3	0.1	0.5										
25b	25b	-	-	-	-	-	-	-	-										
T-38	T-38	-	0.7	-	-	-	0.1	-	0.1										
T-39	T-39	-	With T-38	-	With T-38	-	With T-38	-	With T-38										
T-40	T-40	-	With T-38	-	With T-38	-	With T-38	-	With T-38										
F-1	F-1	-	-	-	-	-	-	-	-										
Totals		5.7	25.0	4.2	18.3	0.5	2.3	0.7	3.2										

Table 2-J: Fuel

Specify fuel characteristics and usage. Unit and stack numbering must correspond throughout the application package.

	Fuel Type (low sulfur Diesel,	Fuel Source: purchased commercial,		Specif	y Units		
Unit No.	ultra low sulfur diesel, Natural Gas, Coal,)	pipeline quality natural gas, residue gas, raw/field natural gas, process gas (e.g. SRU tail gas) or other	Lower Heating Value	Hourly Usage	Annual Usage	% Sulfur	% Ash
1	Natural gas	Raw/Field Natural Gas	900 Btu/scf	11,123 scfh	97.44 MMscfy	-	-
2	Natural gas	Raw/Field Natural Gas	900 Btu/scf	11,123 scfh	97.44 MMscfy	-	-
3	Natural gas	Raw/Field Natural Gas	900 Btu/scf	11,123 scfh	97.44 MMscfy	-	-
4	Natural gas	Raw/Field Natural Gas	900 Btu/scf	11,123 scfh	97.44 MMscfy	-	-
5	Natural gas	Raw/Field Natural Gas	900 Btu/scf	11,123 scfh	97.44 MMscfy	-	-
6	Natural gas	Raw/Field Natural Gas	900 Btu/scf	11,123 scfh	97.44 MMscfy	-	-
7	Natural gas	Raw/Field Natural Gas	900 Btu/scf	11,123 scfh	97.44 MMscfy	-	-
8	Natural gas	Raw/Field Natural Gas	900 Btu/scf	11,123 scfh	97.44 MMscfy	-	-
13	Natural gas	Raw/Field Natural Gas	900 Btu/scf	11,123 scfh	97.44 MMscfy	-	-
15	Natural gas	Raw/Field Natural Gas	900 Btu/scf	11,123 scfh	97.44 MMscfy	-	-
16	Natural gas	Raw/Field Natural Gas	900 Btu/scf	11,123 scfh	97.44 MMscfy	-	-
18	Natural gas	Raw/Field Natural Gas	900 Btu/scf	11,123 scfh	97.44 MMscfy	-	-
19	Natural gas	Raw/Field Natural Gas	900 Btu/scf	11,123 scfh	97.44 MMscfy	-	-
20	Natural gas	Raw/Field Natural Gas	900 Btu/scf	11,123 scfh	97.44 MMscfy	-	-
21	Natural gas	Raw/Field Natural Gas	900 Btu/scf	11,123 scfh	97.44 MMscfy	-	-
22	Natural gas	Raw/Field Natural Gas	900 Btu/scf	11,123 scfh	97.44 MMscfy	-	-
23	Natural gas	Raw/Field Natural Gas	900 Btu/scf	11,123 scfh	97.44 MMscfy	-	-
9b	Natural gas	Raw/Field Natural Gas	900 Btu/scf	1,208 scfh	10.58 MMscfy	-	-

	Fuel Type (low sulfur Diesel,	Fuel Source: purchased commercial,		Specif	y Units		
Unit No.	ultra low sulfur diesel, Natural Gas, Coal,)	pipeline quality natural gas, residue gas, raw/field natural gas, process gas (e.g. SRU tail gas) or other	Lower Heating Value	Hourly Usage	Annual Usage	% Sulfur	% Ash
10b	Natural gas	Raw/Field Natural Gas	900 Btu/scf	1,208 scfh	10.58 MMscfy	-	-
11b	Natural gas	Raw/Field Natural Gas	900 Btu/scf	1,648 scfh	14.44 MMscfy	-	-
12b	Natural gas	Raw/Field Natural Gas	900 Btu/scf	1,648 scfh	14.44 MMscfy	-	-
24b	Natural gas	Raw/Field Natural Gas	900 Btu/scf	1,648 scfh	14.44 MMscfy	-	-
25b	Natural gas	Raw/Field Natural Gas	900 Btu/scf	1,648 scfh	14.44 MMscfy	-	-

Table 2-K: Liquid Data for Tanks Listed in Table 2-L

For each tank, list the liquid(s) to be stored in each tank. If it is expected that a tank may store a variety of hydrocarbon liquids, enter "mixed hydrocarbons" in the Composition column for that tank and enter the corresponding data of the most volatile liquid to be stored in the tank. If tank is to be used for storage of different materials, list all the materials in the "All Calculations" attachment, run the newest version of TANKS on each, and use the material with the highest emission rate to determine maximum uncontrolled and requested allowable emissions rate. The permit will specify the most volatile category of liquids that may be stored in each tank. Include appropriate tank-flashing modeling input data. Use additional sheets if necessary. Unit and stack numbering must correspond throughout the application package.

					Vapor	Average Stor	age Conditions	Max Stora	ge Conditions
Tank No.	SCC Code	Material Name	Composition	Liquid Density (lb/gal)	Molecular Weight (lb/lb*mol)	Temperature (°F)	True Vapor Pressure (psia)	Temperature (°F)	True Vapor Pressure (psia)
T-1	40400313	Waste Water	Water; <1% hydrocarbon liquids	Insignifica	ant source				
T-2	40400313	Used Oil	Used Lubrication Oil	Insignifica	int source				
T-3	40400313	Lubrication Oil	Lubrication Oil	Insignifica	int source				
T-5 - T-17 (each)	40400313	Lubrication Oil	Used Lubrication Oil	Insignifica	int source				
T-18 - T-21 (each)	40705218	Glycol	Triethylene Glycol (TEG)	Insignificant source					
T-22 - T-25 (each)	40705218	Glycol	Triethylene Glycol (TEG)	Insignificant source					
T-26	40700816	Methanol	Methanol	Insignifica	ant source				
T-27		Solvent	Jet kerosene	Insignifica	ant source				
T-28	40705218	Glycol	Triethylene Glycol (TEG)	Insignifica	int source				
T-29	31000299	Antifreeze	Triethylene Glycol (TEG)	Insignifica	ant source				
T-30 - T-33 (each)	40400313	Lubrication Oil	Lubrication Oil	Insignifica	ant source				
T-34 - T-35 (each)	40705218	Glycol	Triethylene Glycol (TEG)	Insignifica	ant source				
T-36 - T-37 (each)	40705218	Glycol	Triethylene Glycol (TEG)	Insignifica	ant source				
T-38 - T-37 (each)	40400315	Produced Water	Produced water w/trace of hydrocarbons	8.3	N/A*	N/A*	N/A*	N/A*	N/A*
T40	40400315	Produced Water	Produced water w/trace of hydrocarbons	8.3	N/A*	N/A*	N/A*	N/A*	N/A*
					* N/A: The emi	ssion calculations	do not yield this o	lata.	

Table 2-L: Tank Data

Include appropriate tank-flashing modeling input data. Use an addendum to this table for unlisted data categories. Unit and stack numbering must correspond throughout the application package. Use additional sheets if necessary. See reference Table 2-L2. Note: 1.00 bbl = 10.159 M3 = 42.0 gal

Tank No.	Date Installed	Materials Stored	Seal Type (refer to Table 2- LR below)	Roof Type (refer to Table 2- LR below)	Cap	acity	Diameter (M)	Vapor Space		olor able VI-C)	Paint Condition (from Table VI-	Annual Throughput	Turn- overs
			LK below)	LK below)	(bbl)	(M ³)	, , ,	(M)	Roof	Shell	C)	(gal/yr)	(per year)
T-1		Waste Water	N/A	FX	165.0	26.2	Insignifican	t source					
T-2		Used Oil	N/A	FX	165	26.2	Insignifican	t source					
T-3		Lubrication Oil	N/A	FX	100	15.9	Insignifican	t source					
T-5 - T-17 (each)		Lubrication Oil	N/A	FX	11.9	1.9	Insignifican	t source					
T-18 - T-21 (each)		Glycol	N/A	FX	2.4	0.4	Insignifican	t source					
T-22 - T-25 (each)		Glycol	N/A	FX	1.2	0.2	Insignifican	t source					
T-26		Methanol	N/A	FX	11.9	1.9	Insignifican	t source					
T-27		Solvent	N/A	FX	11.9	1.9	Insignifican	t source					
T-28		Glycol	N/A	FX	11.9	1.9	Insignifican	t source					
T-29		Antifreeze	N/A	FX	11.9	1.9	Insignifican	t source					
T-30 - T-33 (each)		Lubrication Oil	N/A	FX	11.9	1.9	Insignifican	t source					
T-34 - T-35 (each)		Glycol	N/A	FX	2.4	0.4	Insignifican	t source					
T-36 - T-37 (each)		Glycol	N/A	FX	1.2	0.2	Insignifican	t source					
T-38 - T-39 (each)		Produced Water	N/A	FX	300	48	N/A*	N/A*	N/A*	N/A*	N/A*	with T-4	
T40		Produced Water	N/A	FX	500	79	N/A*	N/A*	N/A*	N/A*	N/A*	with T-4	
							* N/A: The	emission calcul	ations do not	yield this data	a.		

Roof Type	Seal Type, V	velded Tank Seal Type	Seal Type, Riv	eted Tank Seal Type	Roof, Shell Color	Paint Condition
FX: Fixed Roof	Mechanical Shoe Seal	Liquid-mounted resilient seal	Vapor-mounted resilient seal	Seal Type	WH: White	Good
IF: Internal Floating Roof	A: Primary only	A: Primary only	A: Primary only	A: Mechanical shoe, primary only	AS: Aluminum (specular)	Poor
EF: External Floating Roof	B: Shoe-mounted secondary	B: Weather shield	B: Weather shield	B: Shoe-mounted secondary	AD: Aluminum (diffuse)	
P: Pressure	C: Rim-mounted secondary	C: Rim-mounted secondary	C: Rim-mounted secondary	C: Rim-mounted secondary	LG: Light Gray	
					MG: Medium Gray	
Note: $1.00 \text{ bbl} = 0.159 \text{ N}$	$A^3 = 42.0 \text{ gal}$				BL: Black	
					OT: Other (specify)	

Table 2-L2: Liquid Storage Tank Data Codes Reference Table

	Materi	al Processed			Material Produced	l	
Description	Chemical Composition	Phase (Gas, Liquid, or Solid)	Quantity (specify units)	Description	Chemical Composition	Phase	Quantity (specify units)
Low pressure natural gas	C1-C6+	Gas	57,380 mmcfy ¹	High pressure natural gas	C1-C6+	Gas	57,380 mmcfy ¹
Produced water	H2O + trace of HC	Liquid	1,302,000 gal/yr	Produced water	H2O + trace of HC	Liquid	1,302,000 gal/yr
¹ The material processed an and pressure, relative humic nominal amount.	d material produced are both a di lity and gas quality, was well as o	rect function of available horsepowe ther factors. The values expressed al	The material processing and pro ove are a nominal quantities (with	duction rates are therefore depende a safety factor), neither an absolute	nt on atmospheric temperatu e maximum, nor an average.	Actual value	gas temperature es will vary from the

Table 2-M: Materials Processed and Produced (Use additional sheets as necessary.)

Table 2-N: CEM Equipment

Enter Continuous Emissions Measurement (CEM) Data in this table. If CEM data will be used as part of a federally enforceable permit condition, or used to satisfy the requirements of a state or federal regulation, include a copy of the CEM's manufacturer specification sheet in the Information Used to Determine Emissions attachment. Unit and stack numbering must correspond throughout the application package. Use additional sheets if necessary.

Stack No.	Pollutant(s)	Manufacturer	Model No.	Serial No.	Sample Frequency	Averaging Time	Range	Sensitivity	Accuracy
N/A									

Table 2-O: Parametric Emissions Measurement Equipment

Unit and stack numbering must correspond throughout the application package. Use additional sheets if necessary.

Unit No.	Parameter/Pollutant Measured	Location of Measurement	Unit of Measure	Acceptable Range	Frequency of Maintenance	Nature of Maintenance	Method of Recording	Averaging Time
N/A								

Table 2-P: Green House Gas Emissions

Applications submitted under 20.2.70, 20.2.72, & 20.2.74 NMAC are required to complete this Table. Power plants, Title V major sources, and PSD major sources must report and calculate all GHG emissions for each unit. Applicants must report potential emission rates in short tons per year (see Section 6.a for assistance). Include GHG emissions during Startup, Shutdown, and Scheduled Maintenance in this table. For minor source facilities that are not power plants, are not Title V, or are not PSD, there are three options for reporting GHGs 1) report GHGs for each individual piece of equipment; 2) report all GHGs from a group of unit types, for example report all combustion source GHGs as a single unit and all venting GHG as a second separate unit; OR 3) check the following box:

□ By checking this box, the applicant acknowledges the total CO2e emissions are less than 75,000 tons per year.

Unit No.		CO ₂ ton/yr	N2O ton/yr	CH ₄ ton/yr	SF ₆ ton/yr	PFC/HFC ton/yr ²					Total GHG Mass Basis ton/yr ⁴	Total CO₂e ton/yr ⁵
Unit No.	GWPs ¹	1	298	25	22,800	footnote 3						
1	mass GHG	6010.45	1.13E-02	0.11							6010.6	-
1	CO ₂ e	6010.45	3.4	2.8							-	6016.7
2	mass GHG	6010.45	1.13E-02	0.11							6010.6	-
2	CO ₂ e	6010.45	3.4	2.8							-	6016.7
3	mass GHG	6010.45	1.13E-02	0.11							6010.6	-
3	CO ₂ e	6010.45	3.4	2.8							-	6016.7
4	mass GHG	6010.45	1.13E-02	0.11							6010.6	-
4	CO ₂ e	6010.45	3.4	2.8							-	6016.7
5	mass GHG	6010.45	1.13E-02	0.11							6010.6	-
5	CO ₂ e	6010.45	3.4	2.8							-	6016.7
6	mass GHG	6010.45	1.13E-02	0.11							6010.6	-
0	CO ₂ e	6010.45	3.4	2.8							-	6016.7
7	mass GHG	6010.45	1.13E-02	0.11							6010.6	-
/	CO ₂ e	6010.45	3.4	2.8							-	6016.7
8	mass GHG	6010.45	1.13E-02	0.11							6010.6	-
0	CO ₂ e	6010.45	3.4	2.8							-	6016.7
13	mass GHG	6010.45	1.13E-02	0.11							6010.6	-
15	CO ₂ e	6010.45	3.4	2.8							-	6016.7
15	mass GHG	6010.45	1.13E-02	0.11							6010.6	-
15	CO ₂ e	6010.45	3.4	2.8							-	6016.7
16	mass GHG	6010.45	1.13E-02	0.11							6010.6	-
10	CO ₂ e	6010.45	3.4	2.8							-	6016.7
18	mass GHG	6010.45	1.13E-02	0.11							6010.6	-
10	CO ₂ e	6010.45	3.4	2.8							-	6016.7
19	mass GHG	6010.45	1.13E-02	0.11							6010.6	-
1)	CO ₂ e	6010.45	3.4	2.8							-	6016.7
20	mass GHG	6010.45	1.13E-02	0.11							6010.6	-
20	CO ₂ e	6010.45	3.4	2.8							-	6016.7

Unit No.		CO ₂ ton/yr	N2O ton/yr	CH ₄ ton/yr	SF ₆ ton/yr	PFC/HFC ton/yr ²					Total GHG Mass Basis ton/yr ⁴	Total CO₂e ton/yr ⁵
Unit No.	GWPs ¹	1	298	25	22,800	footnote 3						
21	mass GHG	6010.45	1.13E-02	0.11							6010.6	-
21	CO ₂ e	6010.45	3.4	2.8							-	6016.7
22	mass GHG	6010.45	1.13E-02	0.11							6010.6	-
	CO ₂ e	6010.45	3.4	2.8							-	6016.7
23	mass GHG	6010.45	1.13E-02	0.11							6010.6	-
25	CO ₂ e	6010.45	3.4	2.8							-	6016.7
SSM	mass GHG	325.35	-	1650.27							1975.6	-
3314	CO ₂ e	325.4	-	41256.7							-	41582.0
9a	mass GHG	70.4	-	148.83							219.3	-
94	CO ₂ e	70.4	-	3720.6							-	3791.1
01	mass GHG	617.6	1.16E-03	1.16E-02							617.6	-
9b	CO ₂ e	617.6	0.3	0.3							-	618.3
10	mass GHG	70.4	-	148.83							219.3	-
10a	CO ₂ e	70.4	-	3720.6							-	3791.1
1.01	mass GHG	617.6	1.16E-03	1.16E-02							617.6	-
10b	CO ₂ e	617.6	0.3	0.3							-	618.3
11	mass GHG	70.65	-	150.98							221.6	-
11a	CO ₂ e	70.6	-	3774.4				1			-	3845.0
	mass GHG	842.6	1.59E-03	1.59E-02							842.6	-
11b	CO ₂ e	842.6	0.5	0.4							-	843.5
10	mass GHG	70.65	-	150.98							221.6	-
12a	CO ₂ e	70.6	-	3774.4							-	3845.0
1.01	mass GHG	842.6	1.59E-03	1.59E-02							842.6	-
12b	CO ₂ e	842.6	0.5	0.4							-	843.5
	mass GHG	70.65	-	150.98							221.6	-
24a	CO ₂ e	70.6	-	3774.4							-	3845.0
	mass GHG	842.6	1.59E-03	1.59E-02							842.6	-
24b	CO ₂ e	842.6	0.5	0.4							-	843.5
	mass GHG	70.65	-	150.98							221.6	-
25a	CO ₂ e	70.6	-	3774.4							-	3845.0
	mass GHG	842.6	1.59E-03	1.59E-02							842.6	-
25b	CO ₂ e	842.6	0.5	0.4							-	843.5
	mass GHG	0	-	0							0.0	-
L-1	CO ₂ e	0	-	0							-	0.0
	mass GHG	8.04	-	38.85							46.9	-

Unit No.		CO ₂ ton/yr	N2O ton/yr	CH ₄ ton/yr	SF ₆ ton/yr	PFC/HFC ton/yr ²					Total GHG Mass Basis ton/yr ⁴	Total CO₂e ton/yr ⁵
Unit No.	GWPs ¹	1	298	25	22,800	footnote 3						
1-1	CO ₂ e	8.0	-	971.2							-	979.3
Recip	mass GHG	210.98	-	1018.96							1229.9	-
Comp Venting	CO ₂ e	211.0	-	25474.1							-	25685.0
Pneum Dev	mass GHG	42.93	-	206.85							249.8	-
Venting	CO ₂ e	42.9	-	5171.1							-	5214.1
Pneum	mass GHG	0.47	-	2.27							2.7	-
Pump Venting	CO ₂ e	0.47	-	56.7							-	57.2
	mass GHG										0.0	-
	CO ₂ e										-	0.0
Total ⁶	mass GHG	107,794.6	0.20	3,820.76							111,616	-
Total	CO ₂ e	107,794.6	59.97	95,518.98							-	203,374

GWP (Global Warming Potential): Applicants must use the most current GWPs codified in Table A-1 of 40 CFR part 98. GWPs are subject to change, therefore, applicants need to check 40 CFR 98 to confirm GWP values.

² For HFCs or PFCs describe the specific HFC or PFC compound and use a separate column for each individual compound.

³ For each new compound, enter the appropriate GWP for each HFC or PFC compound from Table A-1 in 40 CFR 98.

⁴ Green house gas emissions on a **mass basis** is the ton per year green house gas emission before adjustment with its GWP.

⁵ CO₂e means Carbon Dioxide Equivalent and is calculated by multiplying the TPY mass emissions of the green house gas by its GWP.

⁵ The increase in mass GHG and CO2e compared to previous permit applications is based on higher methane and lower VOC content of the updated gas sample. (The gas GHG content fluctuates over time.)

Section 3

Application Summary

The <u>Application Summary</u> shall include a brief description of the facility and its process, the type of permit application, the applicable regulation (i.e. 20.2.72.200.A.X, or 20.2.73 NMAC) under which the application is being submitted, and any air quality permit numbers associated with this site. If this facility is to be collocated with another facility, provide details of the other facility including permit number(s). In case of a revision or modification to a facility, provide the lowest level regulatory citation (i.e. 20.2.72.219.B.1.d NMAC) under which the revision or modification is being requested. Also describe the proposed changes from the original permit, how the proposed modification will affect the facility's operations and emissions, de-bottlenecking impacts, and changes to the facility's major/minor status (both PSD & Title V).

The <u>Process</u> <u>Summary</u> shall include a brief description of the facility and its processes.

<u>Startup, Shutdown, and Maintenance (SSM)</u> routine or predictable emissions: Provide an overview of how SSM emissions are accounted for in this application. Refer to "Guidance for Submittal of Startup, Shutdown, Maintenance Emissions in Permit Applications (http://www.env.nm.gov/aqb/permit/app_form.html) for more detailed instructions on SSM emissions.

Application Summary

The Harvest 32-7 Central Delivery Point (CDP) currently operates under Title V operating permit, P195-R3, issued January 31, 2018 (as modified in P195-R3-M2, August 14, 2020), and construction permit 1032-M9, dated October 11, 2018, as revised through –R5.

A list of the equipment currently approved for use at the facility by the Title V operating permit can be found in Tables 2-A and 2-B of Section 2 of this application.

This Title V renewal application is submitted under section 20.2.70.300.B(2) of the New Mexico Administrative Code (NMAC). The renewal application is due 12 months prior to the expiration of the current Title V Operating Permit on January 31, 2023.

The facility remains a minor source under the 20.2.74 NMAC Prevention of Significant Deterioration (PSD) program.

There are no modifications in this application that would de-bottleneck impacts or change the facility's major/minor status under either the Prevention of Significant Deterioration [PSD] or Title V permitting programs.

Process Description

The 32-7 CDP is a production gathering field compressor station that pressurizes and dehydrates natural gas for transport through natural gas pipelines. The facility is authorized to operate continuously.

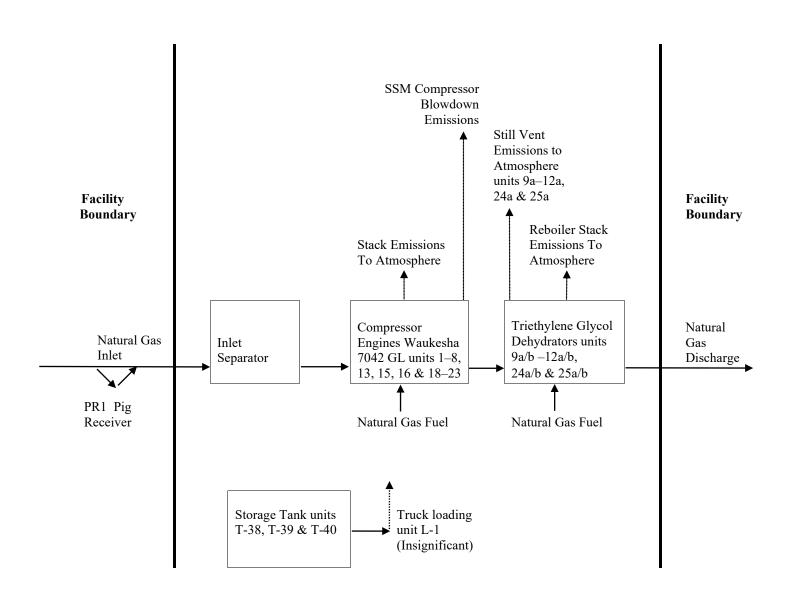
Startup, Shutdown and Maintenance (SSM) Emissions

Except for the emissions from blowdown events (described below), it is concluded there are no SSM emissions in excess of those identified for steady-state operation as seen in Table 2-E of Section 2. Discussions justifying this conclusion are provided in Section 6.

Section 4

Process Flow Sheet

A **process flow sheet** and/or block diagram indicating the individual equipment, all emission points and types of control applied to those points. The unit numbering system should be consistent throughout this application.



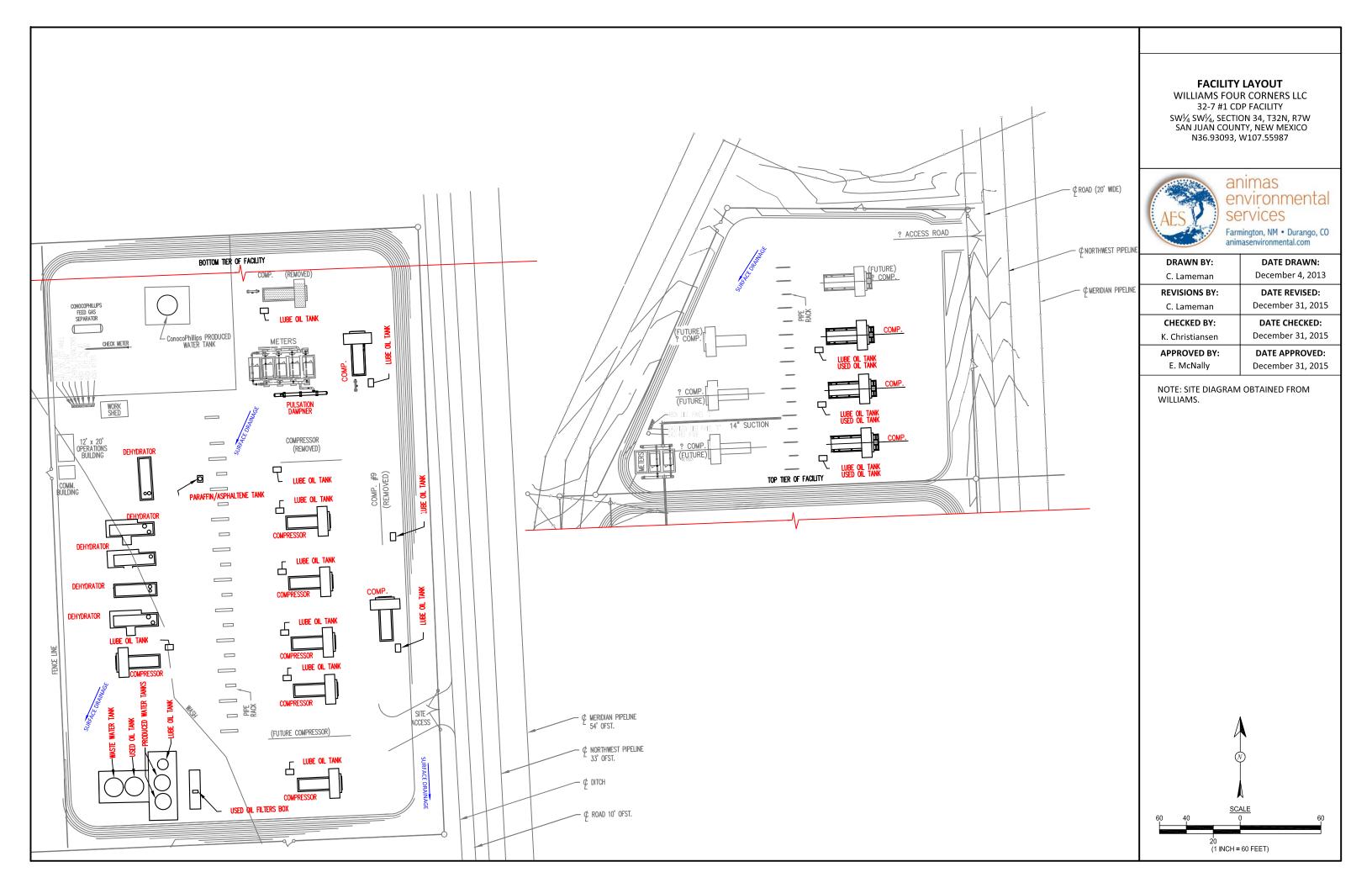
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Section 5

Plot Plan Drawn To Scale

A <u>plot plan drawn to scale</u> showing emissions points, roads, structures, tanks, and fences of property owned, leased, or under direct control of the applicant. This plot plan must clearly designate the restricted area as defined in UA1, Section 1-D.12. The unit numbering system should be consistent throughout this application.

Please see the following page(s).



Section 6

All Calculations

Show all calculations used to determine both the hourly and annual controlled and uncontrolled emission rates. All calculations shall be performed keeping a minimum of three significant figures. Document the source of each emission factor used (if an emission rate is carried forward and not revised, then a statement to that effect is required). If identical units are being permitted and will be subject to the same operating conditions, submit calculations for only one unit and a note specifying what other units to which the calculations apply. All formulas and calculations used to calculate emissions must be submitted. The "Calculations" tab in the UA2 has been provided to allow calculations to be linked to the emissions tables. Add additional "Calc" tabs as needed. If the UA2 or other spread sheets are used, all calculation spread sheet(s) shall be submitted electronically in Microsoft Excel compatible format so that formulas and input values can be checked. Format all spread sheets and calculations such that the reviewer can follow the logic and verify the input values. Define all variables. If calculation spread sheets are not used, provide the original formulas with defined variables. Additionally, provide subsequent formulas showing the input values for each variable in the formula. All calculations, including those calculations are imbedded in the Calc tab of the UA2 portion of the application, the printed Calc tab(s), should be submitted under this section.

Tank Flashing Calculations: The information provided to the AQB shall include a discussion of the method used to estimate tank-flashing emissions, relative thresholds (i.e., NOI, permit, or major source (NSPS, PSD or Title V)), accuracy of the model, the input and output from simulation models and software, all calculations, documentation of any assumptions used, descriptions of sampling methods and conditions, copies of any lab sample analysis. If Hysis is used, all relevant input parameters shall be reported, including separator pressure, gas throughput, and all other relevant parameters necessary for flashing calculation.

SSM Calculations: It is the applicant's responsibility to provide an estimate of SSM emissions or to provide justification for not doing so. In this Section, provide emissions calculations for Startup, Shutdown, and Routine Maintenance (SSM) emissions listed in the Section 2 SSM and/or Section 22 GHG Tables and the rational for why the others are reported as zero (or left blank in the SSM/GHG Tables). Refer to "Guidance for Submittal of Startup, Shutdown, Maintenance Emissions in Permit Applications (http://www.env.nm.gov/aqb/permit/app_form.html) for more detailed instructions on calculating SSM emissions. If SSM emissions are greater than those reported in the Section 2, Requested Allowables Table, modeling may be required to ensure compliance with the standards whether the application is NSR or Title V. Refer to the Modeling Section of this application for more guidance on modeling requirements.

Glycol Dehydrator Calculations: The information provided to the AQB shall include the manufacturer's maximum design recirculation rate for the glycol pump. If GRI-Glycalc is used, the full input summary report shall be included as well as a copy of the gas analysis that was used.

Road Calculations: Calculate fugitive particulate emissions and enter haul road fugitives in Tables 2-A, 2-D and 2-E for:

- 1. If you transport raw material, process material and/or product into or out of or within the facility and have PER emissions greater than 0.5 tpy.
- 2. If you transport raw material, process material and/or product into or out of the facility more frequently than one round trip per day.

Significant Figures:

A. All emissions standards are deemed to have at least two significant figures, but not more than three significant figures.

B. At least 5 significant figures shall be retained in all intermediate calculations.

C. In calculating emissions to determine compliance with an emission standard, the following rounding off procedures shall be used:

- (1) If the first digit to be discarded is less than the number 5, the last digit retained shall not be changed;
- (2) If the first digit discarded is greater than the number 5, or if it is the number 5 followed by at least one digit other than the number zero, the last figure retained shall be increased by one unit; **and**
- (3) If the first digit discarded is exactly the number 5, followed only by zeros, the last digit retained shall be rounded upward if it is an odd number, but no adjustment shall be made if it is an even number.
- (4) The final result of the calculation shall be expressed in the units of the standard.

Control Devices: In accordance with 20.2.72.203.A(3) and (8) NMAC, 20.2.70.300.D(5)(b) and (e) NMAC, and 20.2.73.200.B(7) NMAC, the permittee shall report all control devices and list each pollutant controlled by the control device

regardless if the applicant takes credit for the reduction in emissions. The applicant can indicate in this section of the application if they chose to not take credit for the reduction in emission rates. For notices of intent submitted under 20.2.73 NMAC, only uncontrolled emission rates can be considered to determine applicability unless the state or federal Acts require the control. This information is necessary to determine if federally enforceable conditions are necessary for the control device, and/or if the control device produces its own regulated pollutants or increases emission rates of other pollutants.

Engines

The NO₂, CO, and VOC emissions from the engines were calculated from manufacturer's data. The SO₂ and particulate emissions were calculated using AP-42 emission factors from Table 3.2-2. HAP emissions were calculated using GRI-HAPCalc 3.0. All emissions were calculated assuming each engine operates at full site capacity for 8,760 hours per year.

The engines startup with no load and a rich fuel mixture. As a result, emissions are minimized. Because the engines take only minutes to reach operating temperature, emissions during startup are not expected to exceed the steady-state allowable limits. Similarly, emissions during shutdown do not exceed the steadystate allowable limits, because fuel and air flow cease within seconds of shutdown. Emissions due to scheduled maintenance are negligible as the engines are not in operation during maintenance.

No modifications are being made to the engines or their operation. Permitted criteria pollutant and HAP emissions are carried forward and not revised.

Startup, Shutdown and Maintenance Emissions (SSM)

SSM blowdown emissions from the compressors and piping associated with the facility occur when high pressure gas is used to purge air from the system prior to startup. Also, after shutdowns, high pressure gas is released to atmosphere as a safety precaution.

SSM emissions of VOC and HAP from blowdowns of the compressors and piping associated with the station were calculated from the quantity of gas vented during each event, the composition of the gas, and the number of events. There are three different blowdown volume sizes associated with the compressors at the facility. The total facility SSM emissions are the aggregated sum of the blowdown emissions from each compressor. The quantity of gas vented during each event was determined by Harvest engineering. The composition of the gas was determined from a recent extended gas analysis. For each unit, the annual number of blowdown events were estimated based on historical operations. A safety factor was added because emissions from each blowdown event are dependent on the composition of the gas in the pipeline and because the number of blowdowns in a year may vary. Use of the safety factor is also designed to ensure an adequate emissions limit, which includes emissions from other miscellaneous startup, shutdown and maintenance activities.

The SSM emissions identified in this application are routine or predictable startup/shutdown and scheduled maintenance, and do not include malfunctions or upsets.

Dehydrator Still Vents

VOC and HAP emissions from the dehydrator still vents were calculated using GRI-GLYCalc 4.0. All emissions were calculated assuming each dehydrator operates at full capacity for 8,760 hours per year. To allow for variability in the composition of the inlet gas stream, the dehydrator still vent VOC emission rates identified on the application forms (Table 2-E) are higher than the calculated emission rates in this section.

During startup, the dehydrator reboiler is brought up to temperature before allowing glycol into the absorber. This prevents excess VOC and HAP from collecting in the glycol stream and there are no excess startup emissions above those expected during steady-state operation. During shutdown, the reboiler is shut down in conjunction with the gas flow and glycol circulation. Again, this prevents excess VOC and HAP from collecting in the glycol stream and there are no excess shutdown emissions above those expected during steady-state operation. Emissions due to scheduled maintenance are negligible; either the unit will not be in operation during maintenance or maintenance is limited to tasks for which there are no excess emissions.

No modifications are being made to the dehydrators or their operation. Permitted VOC emissions are carried forward and not revised.

Dehydrator Reboilers

The NO_X and CO emission factors for the reboilers were identified from an Enertek letter dated August 19, 1994. The VOC and SO₂ emission factors were identified from an InFab letter dated July 22, 1998. The particulate and lead emissions were calculated using AP-42 emission factors from Table 1.4-2. HAP emissions were calculated using GRI-HAPCalc 3.0. All emissions were calculated assuming each reboiler operates 8,760 hours per year.

The dehydrator reboilers (uncontrolled) startup with less fuel input than during steady-state operation, so emissions are lower than during steady-state operation. During shutdown, the fuel supply stops quickly, but air flow may not, causing the continued formation of NO_X . Even so, with no fuel, NO_X formation should be less than during steady-state operation. Emissions due to scheduled maintenance are negligible as the units are not in operation.

No modifications are being made to the dehydrator reboilers or their operation. Permitted criteria pollutant and HAP emissions are carried forward and not revised.

Storage Tanks

No changes are being made to the storage tanks or their operation. Emissions from the tanks are carried forward and not revised.

Due to the nature of operations, startup and shutdown emissions from the storage tanks are assumed to be accounted for in the calculations discussed below. Emissions due to maintenance are negligible as the units are not in operation during maintenance.

There are no flash emissions associated with any of the storage tanks.

Regulated Tanks. VOC and HAP emissions from the produced water tanks were calculated using maximum throughputs and emission factors from the Colorado Department of Public Health and Environment (CDPHE) and the Texas Commission on Environmental Quality (TCEQ). The aggregated emissions of VOC exceed 1 tpy; therefore, the aggregated emissions from produced water tank units T-38, T-39, and T-40 are a regulated source under Title V and are included in application Table 2-A, Regulated Emission Sources.

Insignificant Tanks. VOC and HAP emissions from the storage tanks are evaluated using the following assumptions. Where needed, working/breathing losses for the remaining tanks are calculated using TANKS 4.0.9d. The following assumptions were made:

- TANKS 4.0.9d was used to calculate was used to calculate the emissions from the methanol storage tank. As the calculated VOC emission rate is less than 0.5 tpy, the methanol tank is a Title V insignificant source in accordance with Insignificant Activity Item #1, and an NSR exempt source under 20.2.72.202.B(5) NMAC.
- Residual oil #6 was used as an estimate for lubrication (lube) oil and used lube oil. As the vapor pressure of residual oil #6 is less than 0.2 psia, the tanks containing lube oil and used lube oil are Title V insignificant sources in accordance with Insignificant Activity Item #5, and NSR exempt sources under 20.2.72.202.B(2) NMAC.
- Wastewater storage tankage is assumed to contain 99% water and 1% residual oil. As the vapor pressure of residual oil is less than 0.2 psia, the tanks containing wastewater are Title V insignificant sources in accordance with Insignificant Activity Item #5, and NSR exempt sources under 20.2.72.202.B(2) NMAC.
- As the vapor pressure of TEG is less than 0.2 psia, the tanks containing TEG are Title V insignificant sources in accordance with Insignificant Activity Item #5, and NSR exempt sources under 20.2.72.202.B(2) NMAC.
- The anti-freeze is an inhibited ethylene glycol (EG) coolant containing 50 percent EG and 50 percent water. As the vapor pressure of EG is less than 0.2 psia, the tank containing antifreeze is a Title V insignificant source in accordance with Insignificant Activity Item #5, and an NSR exempt source under 20.2.72.202.B(2) NMAC.

• Jet kerosene was used as an estimate for the solvent. As the vapor pressure of jet kerosene is less than 0.2 psia, the storage tank containing solvent is a Title V insignificant source in accordance with Insignificant Activity Item #5, and an NSR exempt source under 20.2.72.202.B(2) NMAC.

Truck Loading (Produced Water)

The VOC emissions from produced water truck loading were calculated using the AP-42 emissions factor identified in Section 5.2-1. The data used to calculate the emission factor was obtained assuming the liquid was pure water.

Due to the nature of the source, it is estimated that SSM emissions from truck loading are accounted for in the calculations.

The produced water truck loading is an exempt source in accordance with 20.2.72.202.B(5) NMAC (VOC emissions are less than 0.5 tons per year) and a Title V insignificant source in accordance with Insignificant Activity Item #1.

Equipment Leak Emissions

VOC and HAP emissions from equipment leaks were calculated using emission factors from Table 2.4 of the 1995 Protocol for Equipment Leak Emission Estimates published by the Environmental Protection Agency (EPA) and the gas stream composition obtained from a recent extended gas analysis. Emissions were calculated assuming the equipment operates 8,760 hours per year.

Due to the nature of the source, it is estimated that SSM emissions from the equipment are accounted for in the calculations.

No modifications are being made to the equipment leak emissions. Permitted VOC emissions are carried forward and not revised.

Pig Receiver

VOC and HAP emissions from the pig receiver was calculated from the quantity of gas vented during each event, the composition of the gas, and the number of events. The quantity of gas vented during each event was determined by Harvest engineering. The composition of the gas was determined from a recent extended gas analysis. The annual number of blowdown events were estimated based on historical operations. A safety factor was added because VOC and HAP emissions from each blowdown event are dependent on the composition of the gas in the pipeline and because the number of blowdowns in a year may vary. Experience indicates there will be a nominal variation in the composition of the gas.

Due to the nature of the source, it is estimated that SSM emissions from the pig receiver is already accounted for in the calculations.

The pig receiver is an existing unit. No modifications are being made to the unit or its operation. As the calculated VOC emission rate is less than 0.5 tpy, the pig receiver is a Title V insignificant source in accordance with Insignificant Activity Item #1, and an NSR exempt source under 20.2.72.202.B(5) NMAC.

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Engine Exhaust Emissions Calculations

 Unit Number:
 1, 2, 3, 4, 5, 6, 7, 8, 15, 16, 18, 19, 20, 21, 22 & 23

 Description:
 Waukesha L7042GL

Note: The data on this worksheet applies to each individual emissions unit identified above.

Horsepower Calculations		
6,740 ft above MSL	Elevation	
1,478 hp	Nameplate hp	Mfg. data
1,357 hp	NMAQB Site-rated hp	NMAQB Procedure # 02.002-00 (loss of 3% for every 1,000 ft over 4,000 ft)
1,323 hp	Mfg. Site-rated hp	Mfg. product bulletin Power Derate, S8154-6, April 2001 (loss of 2% for every 1,000 ft over 1,500 ft)
Engine Specifications		
1200 rpm	Engine rpm	Mfg. data
7040 cu in	Engine displacement	Mfg. data
127.17 psi	127.17 psi BMEP Mfg. data (+[(792,000 / (rpm * in^3)])	
Fuel Consumption		
7380 Btu/hp-hr	Brake specific fuel consumption	Mfg. data
10.01 MMBtu/hr	Hourly fuel consumption	Btu/hp-hr x NMAQB site-rated hp / 1,000,000
11,123 scf/hr	Hourly fuel consumption	MMBtu/hr x 1,000,000 / Btu/scf
<mark>8,760</mark> hr/yr	Annual operating time	Harvest
87,694 MMBtu/yr	Annual fuel consumption	MMBtu/hr x hr/yr
97.44 MMscf/yr	Annual fuel consumption	scf/hr x hr/yr / 1,000,000
900 Btu/scf	Field gas heating value	Nominal heat content

Steady-State Emission Rates

	Emission	Uncontrolled E	mission Rates	Control	Controlled E	mission Rates
Pollutants	Factors,	(Units	1 - 6)	Efficiency	(Units 7, 8, 15	i, 16, & 18 - 23)
	g/hp-hr	pph	tpy		pph	tpy
NOX	0.90	2.69	11.79	0%	2.69	11.79
со	2.75	8.22	36.02	93%	0.58	2.52
VOC	1.00	2.99	13.10	79%	0.63	2.75

 NO_x , CO & VOC emissions taken from Waukesha Bulletin 7005 0102 Uncontrolled Emission Rates (pph) = g/hp-hr x NMAQB Site-rated hp / 453.59 g/lb Uncontrolled Emission Rates (tpy) = Uncontrolled Emission Rates (pph) x hr/yr / 2,000 lb/ton Control efficiencies taken based on catalyst manufacturer data sheet. Controlled Emission Rates (pph) = Uncontrolled Emission Rates (pph) x (1 - (% / 100)) Controlled Emission Rates (tpy) = Uncontrolled Emission Rates (tpy) x (1 - (% / 100))

	Emission		
Pollutants	Factors,	Uncontrolled Er	mission Rates,
	lb/MMBtu	pph	tpy
SO2	5.88E-04	5.89E-03	2.58E-02
PM	9.99E-03	1.00E-01	4.38E-01
PM10	9.99E-03	1.00E-01	4.38E-01
PM2.5	9.99E-03	1.00E-01	4.38E-01

Emission factors taken from AP-42, Table 3.2-2

Particulate factors include both filterable and condensible emissions

Uncontrolled Emission Rates (pph) = lb/MMBtu x MMBtu/hr

Uncontrolled Emission Rates (tpy) = Uncontrolled Emission Rates (pph) x hr/yr / 2,000 lb/ton

Exhaust Parameters

701 °F 7550 acfm 1.02 ft 0.82 ft² 153.7 fps 22.00 ft Stack exit temperature Stack flowrate Stack exit diameter Stack exit area Stack exit velocity Stack height Mfg. data Mfg. data Harvest 3.1416 x ((ft / 2) ^2) acfm / ft^2 / 60 sec/min Harvest

Engine Exhaust Emissions Calculations

Unit Number: Description:	<mark>13</mark> Waukesha L7042GL		
	Note: The data on this workshe	eet applies to each individual emissions unit identified	ł above.
Horsepower C	alculations		
6,74	0 ft above MSL	Elevation	
1,47	8 hp	Nameplate hp	Mfg. data
1,35	7 hp	NMAQB Site-rated hp	NMAQB Procedure # 02.002-00 (loss of 3% for every 1,000 ft over 4,000 ft)
1,32	3 hp	Mfg. Site-rated hp	Mfg. product bulletin Power Derate, S8154-6, April 2001 (loss of 2% for every 1,000 ft over 1,500 ft)
Engine Specif	ications		
120	0 rpm	Engine rpm	Mfg. data
704	0 cu in	Engine displacement	Mfg. data
127.1	7 psi	BMEP	Mfg. data (+[(792,000 x NMAQB Site-rated hp) / (rpm * in^3)])
Fuel Consump	otion		
738	0 Btu/hp-hr	Brake specific fuel consumption	Mfg. data
10.0	1 MMBtu/hr	Hourly fuel consumption	Btu/hp-hr x NMAQB site-rated hp / 1,000,000
11,123	3 scf/hr	Hourly fuel consumption	MMBtu/hr x 1,000,000 / Btu/scf
8,76	0 hr/yr	Annual operating time	Harvest
87,694	4 MMBtu/yr	Annual fuel consumption	MMBtu/hr x hr/yr
97.4	4 MMscf/yr	Annual fuel consumption	scf/hr x hr/yr / 1,000,000
90	0 Btu/scf	Field gas heating value	Nominal heat content

Steady-State Emission Rates

Pollutants	Emission Factors,	Uncontrolled E	mission Rates	Control Efficiency		mission Rates it 13)
	g/hp-hr	pph	tpy		pph	tpy
NOX	0.90	2.69	11.79	0%	2.69	11.79
со	2.75	8.22	36.02	90%	0.82	3.60
VOC	1.00	2.99	13.10	80%	0.60	2.62

 NO_x , CO & VOC emissions taken from Waukesha Bulletin 7005 0102 Uncontrolled Emission Rates (pph) = g/hp-hr x NMAQB Site-rated hp / 453.59 g/lb Uncontrolled Emission Rates (tpy) = Uncontrolled Emission Rates (pph) x hr/yr / 2,000 lb/ton Control efficiencies taken based on catalyst manufacturer data sheet. Controlled Emission Rates (pph) = Uncontrolled Emission Rates (pph) x (1 - (% / 100)) Controlled Emission Rates (tpy) = Uncontrolled Emission Rates (tpy) x (1 - (% / 100))

	Emission		
Pollutants	Factors,	Uncontrolled Er	mission Rates,
	lb/MMBtu	pph	tpy
SO2	5.88E-04	5.89E-03	2.58E-02
PM	9.99E-03	1.00E-01	4.38E-01
PM10	9.99E-03	1.00E-01	4.38E-01
PM2.5	9.99E-03	1.00E-01	4.38E-01

Emission factors taken from AP-42, Table 3.2-2

Particulate factors include both filterable and condensible emissions

Uncontrolled Emission Rates (pph) = lb/MMBtu x MMBtu/hr

Uncontrolled Emission Rates (tpy) = Uncontrolled Emission Rates (pph) x hr/yr / 2,000 lb/ton

Exhaust Parameters

701 °F 7550 acfm 1.02 ft 0.82 ft² 153.7 fps 22.00 ft Stack exit temperature Stack flowrate Stack exit diameter Stack exit area Stack exit velocity Stack height Mfg. data Mfg. data Harvest 3.1416 x ((ft / 2) ^2) acfm / ft^2 / 60 sec/min Harvest

<u>GRI-HAPCalc ® 3.01</u> <u>Engines Report</u>

Facility ID: 32-7 CDP Operation Type: COMPRES Facility Name: 32-7 CDP User Name: Cirrus Units of Measure: U.S. STAN : Emissions less than 5.00E-09 tons (or These emissions are indicated on the Emissions between 5.00E-09 and 5.00E	tonnes) per year are considered in report with a "0".	-	000".
Engine Unit			
Unit Name: 4SLB_RICE			
Hours of Operation:	8,760 Yearly		
Rate Power:	1,357 hp		
Fuel Type:	FIELD GAS		
Engine Type:	4-Stroke, Lean Burn		
Emission Factor Set:	EPA > FIELD > LITERATUR	RE	
Additional EF Set:	-NONE-		
	Calculated Emis	ssions (ton/yr)	
Chemical Name	Emissions	Emission Factor	Emission Factor
<u>HAPs</u>			
Formaldehyde	2.2033	0.16830000 g/bhp-hr	GRI Literature
Benzene	0.0681	0.00520000 g/bhp-hr	GRI Literature
Toluene	0.0275	0.00210000 g/bhp-hr	GRI Literature
Xylenes(m,p,o)	0.0183	0.00140000 g/bhp-hr	GRI Literature
Total	2.3172		

Compressor Blowdown Emissions Calculations

Unit Number:	SSM	- Units 1, 2, 4, 5, 6, 7, 8, 13, 15, 16, 18, 22, & 23
Description:	Compressor &	Piping Associated With Station

Throughput

500	events/yr per compressor	events per unit
13	compressors	compressor units
10,995	scf/event	Gas loss per blowdown
71,468,487	scf/yr	Total annual gas loss

Harvest Harvest Harvest events/yr per unit x # of units x scf/event

Emission Rates

		Uncontrolled,	Uncontrolled,
	Emission	Emission	Emission
Pollutants	Factors,	Rates, tpy	Rates, tpy
	lb/scf	per unit	facility-wide
VOC	1.506E-04	0.41	5.38
2,2,4-Trimethylpentane	0.000E+00	0.00E+00	0.00E+00
Benzene	2.059E-07	5.66E-04	7.36E-03
Ethylbenzene	0.000E+00	0.00E+00	0.00E+00
n-Hexane	1.136E-06	3.12E-03	4.06E-02
Toluene	7.286E-07	2.00E-03	2.60E-02
Xylene	5.597E-07	1.54E-03	2.00E-02

Emission factors calculated from gas composition (see table below)

Uncontrolled Emission Rates (tpy) per unit = (lb/scf x events/yr per compressor x scf/event) / 2,000 lb/ton Uncontrolled Emission Rates (tpy) facility-wide = (lb/scf x scf/yr) / 2,000 lb/ton

Gas Composition

	Mole	Molecular	Emission
Components	Percents,	Weights,	Factors,
	%	lb/lb-mole	lb/scf
Carbon dioxide	6.6351	44.01	7.697E-03
Hydrogen sulfide	0.0000	34.07	0.000E+00
Nitrogen	0.0998	28.01	7.368E-05
Methane	92.3408	16.04	3.904E-02
Ethane	0.8094	30.07	6.415E-04
Propane	0.0877	44.09	1.019E-04
Isobutane	0.0082	58.12	1.256E-05
n-Butane	0.0095	58.12	1.455E-05
Isopentane	0.0041	72.15	7.797E-06
n-Pentane	0.0012	72.15	2.282E-06
Cyclopentane	0.0001	70.14	1.849E-07
n-Hexane	0.0005	86.17	1.136E-06
Cyclohexane	0.0002	84.16	4.436E-07
Other hexanes	0.0011	86.18	2.499E-06
Heptanes	0.0004	100.20	1.056E-06
Methylcyclohexane	0.0008	98.19	2.070E-06
2,2,4-Trimethylpentane	0.0000	100.21	0.000E+00
Benzene	0.0001	78.11	2.059E-07
Toluene	0.0003	92.14	7.286E-07
Ethylbenzene	0.0000	106.17	0.000E+00
Xylenes	0.0002	106.17	5.597E-07
C8+ Heavies	0.0009	110.00	2.609E-06
Total	100.0004		
Total VOC			1.506E-04

Gas stream composition obtained from the 32-7 #1 CDP extended gas analysis dated 06/072022. Emission Factors (lb/scf) = (% / 100) x lb/lb-mole / 379.4 scf/lb-mole

Compressor Blowdown Emissions Calculations

Unit Number:	SSM	- Units 19, 20 & 21
Description:	Compressor	& Piping Associated With Station

Throughput

500 events/yr per compressor	events per unit
3 compressors	compressor units
7,257 scf/event	Gas loss per blowdown
10,884,847 scf/yr	Total annual gas loss

Harvest Harvest Harvest events/yr per unit x # of units x scf/event

Emission Rates

		Uncontrolled,	Uncontrolled,
	Emission	Emission	Emission
Pollutants	Factors,	Rates, tpy	Rates, tpy
	lb/scf	per unit	facility-wide
VOC	1.506E-04	0.27	0.82
2,2,4-Trimethylpentane	0.000E+00	0.00E+00	0.00E+00
Benzene	2.059E-07	3.73E-04	1.12E-03
Ethylbenzene	0.000E+00	0.00E+00	0.00E+00
n-Hexane	1.136E-06	2.06E-03	6.18E-03
Toluene	7.286E-07	1.32E-03	3.97E-03
Xylene	5.597E-07	1.02E-03	3.05E-03

Emission factors calculated from gas composition (see table below)

Uncontrolled Emission Rates (tpy) per unit = (lb/scf x events/yr per compressor x scf/event) / 2,000 lb/ton Uncontrolled Emission Rates (tpy) facility-wide = (lb/scf x scf/yr) / 2,000 lb/ton

Gas Composition

	Mole	Molecular	Emission
Components	Percents,	Weights,	Factors,
	%	lb/lb-mole	lb/scf
Carbon dioxide	6.6351	44.01	7.697E-03
Hydrogen sulfide	0.0000	34.07	0.000E+00
Nitrogen	0.0998	28.01	7.368E-05
Methane	92.3408	16.04	3.904E-02
Ethane	0.8094	30.07	6.415E-04
Propane	0.0877	44.09	1.019E-04
Isobutane	0.0082	58.12	1.256E-05
n-Butane	0.0095	58.12	1.455E-05
Isopentane	0.0041	72.15	7.797E-06
n-Pentane	0.0012	72.15	2.282E-06
Cyclopentane	0.0001	70.14	1.849E-07
n-Hexane	0.0005	86.17	1.136E-06
Cyclohexane	0.0002	84.16	4.436E-07
Other hexanes	0.0011	86.18	2.499E-06
Heptanes	0.0004	100.20	1.056E-06
Methylcyclohexane	0.0008	98.19	2.070E-06
2,2,4-Trimethylpentane	0.0000	100.21	0.000E+00
Benzene	0.0001	78.11	2.059E-07
Toluene	0.0003	92.14	7.286E-07
Ethylbenzene	0.0000	106.17	0.000E+00
Xylenes	0.0002	106.17	5.597E-07
C8+ Heavies	0.0009	110.00	2.609E-06
Total	100.0004		
Total VOC			1.506E-04

Gas stream composition obtained from the 32-7 #1 CDP extended gas analysis dated 06/072022. Emission Factors (lb/scf) = (% / 100) x lb/lb-mole / 379.4 scf/lb-mole

Compressor Blowdown Emissions Calculations

Unit Number:	SSM	- Unit 3
Description:	Compress	or & Piping Associated With Station

Throughput

500	events/yr per compressor	events per unit
1	compressors	compressor units
4,368	scf/event	Gas loss per blowdown
2,183,875	scf/yr	Total annual gas loss

Harvest Harvest Harvest events/yr per unit x # of units x scf/event

Emission Rates

		Uncontrolled,	Uncontrolled,
	Emission	Emission	Emission
Pollutants	Factors,	Rates, tpy	Rates, tpy
	lb/scf	per unit	facility-wide
VOC	1.506E-04	0.16	0.16
2,2,4-Trimethylpentane	0.000E+00	0.00E+00	0.00E+00
Benzene	2.059E-07	2.25E-04	2.25E-04
Ethylbenzene	0.000E+00	0.00E+00	0.00E+00
n-Hexane	1.136E-06	1.24E-03	1.24E-03
Toluene	7.286E-07	7.96E-04	7.96E-04
Xylene	5.597E-07	6.11E-04	6.11E-04

Emission factors calculated from gas composition (see table below)

Uncontrolled Emission Rates (tpy) per unit = (lb/scf x events/yr per compressor x scf/event) / 2,000 lb/ton Uncontrolled Emission Rates (tpy) facility-wide = (lb/scf x scf/yr) / 2,000 lb/ton

Gas Composition

	Mole	Molecular	Emission
Components	Percents,	Weights,	Factors,
	%	lb/lb-mole	lb/scf
Carbon dioxide	6.6351	44.01	7.697E-03
Hydrogen sulfide	0.0000	34.07	0.000E+00
Nitrogen	0.0998	28.01	7.368E-05
Methane	92.3408	16.04	3.904E-02
Ethane	0.8094	30.07	6.415E-04
Propane	0.0877	44.09	1.019E-04
Isobutane	0.0082	58.12	1.256E-05
n-Butane	0.0095	58.12	1.455E-05
Isopentane	0.0041	72.15	7.797E-06
n-Pentane	0.0012	72.15	2.282E-06
Cyclopentane	0.0001	70.14	1.849E-07
n-Hexane	0.0005	86.17	1.136E-06
Cyclohexane	0.0002	84.16	4.436E-07
Other hexanes	0.0011	86.18	2.499E-06
Heptanes	0.0004	100.20	1.056E-06
Methylcyclohexane	0.0008	98.19	2.070E-06
2,2,4-Trimethylpentane	0.0000	100.21	0.000E+00
Benzene	0.0001	78.11	2.059E-07
Toluene	0.0003	92.14	7.286E-07
Ethylbenzene	0.0000	106.17	0.000E+00
Xylenes	0.0002	106.17	5.597E-07
C8+ Heavies	0.0009	110.00	2.609E-06
Total	100.0004		
Total VOC			1.506E-04

Gas stream composition obtained from the 32-7 #1 CDP extended gas analysis dated 06/072022. Emission Factors (lb/scf) = (% / 100) x lb/lb-mole / 379.4 scf/lb-mole GRI-GLYCalc VERSION 4.0 - SUMMARY OF INPUT VALUES Case Name: 32-7 EU 9a & 10a PTE (gas 2021-06-22) File Name: C:\Users\user\Documents\Cirrus\Permit applications\New Mexico\Harvest Four Corners\32-7\TITLE V\2021-01 Title V Renewal\Analyses & Info\GLYCalc\32-7 12 mm dehys PTE (gas 2021-06-22).ddf Date: January 05, 2022 DESCRIPTION: _____ Description: 32-7 EU 9 & 10 - 12 mmcfd dehys PTE Title V Renewal Appl 6/22/2021 GAS ext. analysis & avg parameters inc.flash tank temp & pressure Annual Hours of Operation: 8760.0 hours/yr WET GAS: _____ Temperature: 115.00 deg. F Pressure: 928.00 psig Wet Gas Water Content: Saturated Component Conc. (vol %) _____ ____
 Carbon Dioxide
 6.9673

 Nitrogen
 0.0353

 Methane
 92.1867

 Ethane
 0.7106

 Propane
 0.0677
 Isobutane 0.0106 n-Butane 0.0097 Isopentane 0.0031 n-Pentane 0.0020 Cyclopentane 0.0002 n-Hexane 0.0010 Cyclohexane 0.0006 Other Hexanes 0.0020 Heptanes 0.0007 Methylcyclohexane 0.0010
 Toluene
 0.0004

 Xylenes
 0.0003

 C8+ Heavies
 0.0011
 DRY GAS: _____ Flow Rate: 12.0 MMSCF/day Water Content: 7.0 lbs. H2O/MMSCF LEAN GLYCOL: _____ Glycol Type: TEG Water Content: 1.5 wt% H2O Flow Rate: 2.5 gpm

Page: 1

Glycol Pump Type: Gas Injection Gas Injection Pump Volume Ratio: 0.080 acfm gas/gpm glycol

FLASH TANK:

Flash Control: Recycle/recompression Temperature: 99.5 deg. F Pressure: 50.7 psig GRI-GLYCalc VERSION 4.0 - AGGREGATE CALCULATIONS REPORT

DESCRIPTION:

Description: 32-7 EU 9 & 10 - 12 mmcfd dehys PTE Title V Renewal Appl 6/22/2021 GAS ext. analysis & avg parameters inc.flash tank temp & pressure

Annual Hours of Operation: 8760.0 hours/yr

EMISSIONS REPORTS:

UNCONTROLLED REGENERATOR EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane	0.2783	6.680	1.2191
Ethane	0.0184	0.443	0.0808
Propane	0.0070	0.169	0.0308
Isobutane	0.0025	0.061	0.0111
n-Butane	0.0034	0.082	0.0150
Isopentane	0.0016	$\begin{array}{c} 0.037 \\ 0.034 \\ 0.023 \\ 0.044 \\ 0.165 \end{array}$	0.0068
n-Pentane	0.0014		0.0062
Cyclopentane	0.0009		0.0041
n-Hexane	0.0018		0.0080
Cyclohexane	0.0069		0.0302
Other Hexanes	0.0025	0.060	0.0109
Heptanes	0.0035	0.084	0.0153
Methylcyclohexane	0.0155	0.373	0.0680
Toluene	0.0725	1.739	0.3173
Xylenes	0.1047	2.512	0.4584
C8+ Heavies	0.0567	1.360	0.2483
	0.5777	13.865	2.5303
Total Hydrocarbon Emissions	0.5777	$ \begin{array}{r} 13.865 \\ 6.742 \\ 4.294 \\ 4.251 \end{array} $	2.5303
Total VOC Emissions	0.2809		1.2304
Total HAP Emissions	0.1789		0.7837
Total BTEX Emissions	0.1771		0.7757

FLASH GAS EMISSIONS

Note: Flash Gas Emissions are zero with the

Recycle/recompression control option.

Component lbs/hr lbs/day tons	

Page: 1

Methane Ethane Propane Isobutane n-Butane	33.6743 0.5887 0.0922 0.0206 0.0206	14.129	2.5785 0.4039
Isopentane n-Pentane Cyclopentane n-Hexane Cyclohexane	0.0078 0.0055 0.0010 0.0037 0.0036	0.132 0.023	
Other Hexanes Heptanes Methylcyclohexane Toluene Xylenes C8+ Heavies	0.0032 0.0059 0.0025 0.0013	0.077 0.142	0.0140 0.0258 0.0111 0.0058
Total Emissions		826.622	
Total HAP Emissions			0.7866

COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane	0.2783	6.680	1.2191
Ethane	0.0184	0.443	0.0808
Propane	0.0070	0.169	0.0308
Isobutane	0.0025	0.061	0.0111
n-Butane	0.0034	0.082	0.0150
Isopentane	0.0016	$\begin{array}{c} 0.037 \\ 0.034 \\ 0.023 \\ 0.044 \\ 0.165 \end{array}$	0.0068
n-Pentane	0.0014		0.0062
Cyclopentane	0.0009		0.0041
n-Hexane	0.0018		0.0080
Cyclohexane	0.0069		0.0302
Other Hexanes	0.0025	0.060	0.0109
Heptanes	0.0035	0.084	0.0153
Methylcyclohexane	0.0155	0.373	0.0680
Toluene	0.0725	1.739	0.3173
Xylenes	0.1047	2.512	0.4584
C8+ Heavies	0.0567	1.360	0.2483
Total Emissions	0.5777	13.865	2.5303
Total Hydrocarbon Emissions	0.5777	13.865	2.5303
Total VOC Emissions	0.2809	6.742	1.2304
Total HAP Emissions	0.1789	4.294	0.7837
Total BTEX Emissions	0.1771	4.251	0.7757

COMBINED REGENERATOR VENT/FLASH GAS EMISSION CONTROL REPORT:

Component	Uncontrolled tons/yr	Controlled tons/yr	% Reduction
Methane	148.7125	1.2191	99.18

			Page: 3
Ethane	2.6593	0.0808	96.96
Propane	0.4347	0.0308	92.92
Isobutane	0.1014	0.0111	89.03
n-Butane	0.1050	0.0150	85.70
Isopentane	0.0410	0.0068	83.42
n-Pentane	0.0302	0.0062	79.58
Cyclopentane	0.0083	0.0041	50.69
n-Hexane	0.0240	0.0080	66.74
Cyclohexane	0.0459	0.0302	34.19
Other Hexanes	0.0407		73.26
Heptanes	0.0293		47.72
Methylcyclohexane	0.0939	0.0680	27.52
Toluene	0.3284	0.3173	3.38
Xylenes	0.4641	0.4584	1.24
C8+ Heavies	0.2701	0.2483	8.08
	1 5 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2		
Total Emissions	153.3888	2.5303	98.35
Total Hudrogarbon Emigrican	153.3888	2.5303	98.35
Total Hydrocarbon Emissions Total VOC Emissions	2.0170	1.2304	
Total HAP Emissions	0.8165	0.7837	
Total BTEX Emissions	0.7926	0.7757	2.13

EQUIPMENT REPORTS:

ABSORBER

NOTE: Because the Calculated Absorber Stages was below the minimum allowed, GRI-GLYCalc has set the number of Absorber Stages to 1.25 and has calculated a revised Dry Gas Dew Point.

Calculated Absorber Stages: Calculated Dry Gas Dew Point:	1.25 6.61	lbs. H2O/MMSCF
Temperature: Pressure:		deg. F psig
Dry Gas Flow Rate:	12.0000	MMSCF/day
Glycol Losses with Dry Gas: Wet Gas Water Content:	0.2715 Saturated	lb/hr
Calculated Wet Gas Water Content: Calculated Lean Glycol Recirc. Ratio:		lbs. H2O/MMSCF gal/lb H2O

Component	Remaining in Dry Gas	Absorbed in Glycol
Water	6.98%	93.02%
Carbon Dioxide	99.76%	0.24%
Nitrogen	99.98%	0.02%
Methane	99.98%	0.02%
Ethane	99.98%	0.06%
Propane	99.90%	0.10%
Isobutane	99.87%	0.13%
n-Butane	99.83%	0.17%
Isopentane	99.84%	0.16%
n-Pentane	99.79%	0.21%
Cyclopentane	99.12%	0.88%
n-Hexane	99.67%	0.33%

Cyclohexane Other Hexanes Heptanes	98.58% 99.75% 99.43%	Pag 1.42% 0.25% 0.57%	ge: 4
Methylcyclohexane	98.50%	1.50%	
Toluene	84.72%	15.28%	
Xylenes	74.91%	25.09%	
C8+ Heavies	97.66%	2.34%	

FLASH TANK

Flash Contr Flash Temperatu Flash Pressu	ire: 99	/recompression .5 deg. F .7 psig
Component	Left in Glycol	Removed in Flash Gas
Water Carbon Dioxide Nitrogen Methane Ethane	99.90% 11.03% 0.78% 0.82% 3.04%	88.97% 99.22%
Propane	7.08%	92.92%
Isobutane	10.97%	89.03%
n-Butane	14.30%	85.70%
Isopentane	16.80%	83.20%
n-Pentane	20.65%	79.35%
Cyclopentane	49.52%	50.48%
n-Hexane	33.49%	66.51%
Cyclohexane	66.80%	33.20%
Other Hexanes	27.20%	72.80%
Heptanes	52.46%	47.54%
Methylcyclohexane	73.48%	26.52%
Toluene	96.89%	3.11%
Xylenes	98.92%	1.08%
C8+ Heavies	92.84%	7.16%

REGENERATOR

No Stripping Gas used in regenerator.

Component	Remaining in Glycol	Distilled Overhead
Water Carbon Dioxide Nitrogen Methane Ethane	32.40% 0.00% 0.00% 0.00% 0.00%	100.00% 100.00%
Propane	0.00%	100.00%
Isobutane	0.00%	100.00%
n-Butane	0.00%	100.00%
Isopentane	1.54%	98.46%
n-Pentane	1.40%	98.60%
Cyclopentane	0.86%	99.14%
n-Hexane	1.02%	98.98%
Cyclohexane	4.34%	95.66%
Other Hexanes	2.30%	97.70%

Heptanes	0.75%	Page: 99.25%
Methylcyclohexane	4.96%	95.04%
Toluene	8.08%	91.92%
Xylenes	12.99%	87.01%
C8+ Heavies	12.23%	87.77%

5

STREAM REPORTS:

WET GAS STREAM _____ Temperature: 115.00 deg. F Pressure: 942.70 psia Flow Rate: 5.01e+005 scfh Component Conc. Loading (vol%) (lb/hr) ----- ------Water 1.99e-001 4.74e+001 Carbon Dioxide 6.95e+000 4.04e+003 Nitrogen 3.52e-002 1.30e+001 Methane 9.20e+001 1.95e+004 Ethane 7.09e-001 2.82e+002 Propane 6.76e-002 3.94e+001 Isobutane 1.06e-002 8.12e+000 n-Butane 9.68e-003 7.43e+000 Isopentane 3.09e-003 2.95e+000 n-Pentane 2.00e-003 1.90e+000 Cyclopentane 2.00e-004 1.85e-001 n-Hexane 9.98e-004 1.14e+000 Cyclohexane 5.99e-004 6.66e-001 Other Hexanes 2.00e-003 2.27e+000 Heptanes 6.99e-004 9.25e-001 Methylcyclohexane 9.98e-004 1.29e+000 Toluene 3.99e-004 4.86e-001 Xylenes 2.99e-004 4.20e-001 C8+ Heavies 1.10e-003 2.47e+000 ----- -----_____ Total Components 100.00 2.39e+004

DRY GAS STREAM

Temperature: Pressure: Flow Rate:				
	Component	Conc. (vol%)	Loading (lb/hr)	
	Carbon Dioxide Nitrogen Methane	1.39e-002 6.95e+000 3.53e-002 9.22e+001 7.10e-001	4.03e+003 1.30e+001 1.95e+004	
	Isobutane	6.76e-002 1.06e-002 9.69e-003 3.10e-003	8.11e+000 7.42e+000	

n-Pentane 2.00e-003 1.90e+000 Cyclopentane 1.98e-004 1.83e-001 n-Hexane 9.97e-004 1.13e+000 Cyclohexane 5.92e-004 6.56e-001 Other Hexanes 2.00e-003 2.27e+000 Heptanes 6.96e-004 9.19e-001 Methylcyclohexane 9.85e-004 1.27e+000 Toluene 3.39e-004 4.12e-001 Xylenes 2.25e-004 3.15e-001 C8+ Heavies 1.07e-003 2.41e+000 _____ _____ Total Components 100.00 2.39e+004 LEAN GLYCOL STREAM _____ Temperature: 115.00 deg. F Flow Rate: 2.50e+000 gpm Component Conc. Loading (wt%) (lb/hr) _____ ____ TEG 9.85e+001 1.39e+003 Water 1.50e+000 2.11e+001 Carbon Dioxide 7.02e-011 9.89e-010 Nitrogen 2.06e-014 2.89e-013 Methane 9.41e-018 1.32e-016 Ethane 5.82e-009 8.19e-008 Propane 1.12e-010 1.57e-009 Isobutane 2.27e-011 3.19e-010 n-Butane 2.21e-011 3.11e-010 Isopentane 1.72e-006 2.42e-005 n-Pentane 1.41e-006 1.99e-005 Cyclopentane 5.79e-007 8.15e-006 n-Hexane 1.33e-006 1.87e-005 Cyclohexane 2.22e-005 3.12e-004 Other Hexanes 4.16e-006 5.85e-005 Heptanes 1.88e-006 2.65e-005 Methylcyclohexane 5.75e-005 8.10e-004 Toluene 4.53e-004 6.37e-003 Xylenes 1.11e-003 1.56e-002 C8+ Heavies 5.61e-004 7.90e-003 _____ ----- -----Total Components 100.00 1.41e+003 RICH GLYCOL AND PUMP GAS STREAM _____ Temperature: 115.00 deg. F Pressure: 942.70 psia Flow Rate: 2.70e+000 gpm NOTE: Stream has more than one phase. Conc. Loading (wt%) (lb/hr) Component _____ ____ TEG 9.22e+001 1.39e+003 Water 4.34e+000 6.52e+001 Carbon Dioxide 1.07e+000 1.61e+001 Nitrogen 1.53e-003 2.30e-002

Methane 2.26e+000 3.40e+001

Ethane 4.04e-002 6.07e-001

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Propane 6.61e-003 9.93e-002 Isobutane 1.54e-003 2.31e-002 n-Butane 1.60e-003 2.40e-002 Isopentane 6.25e-004 9.39e-003 n-Pentane 4.60e-004 6.91e-003 Cyclopentane 1.27e-004 1.91e-003 n-Hexane 3.66e-004 5.49e-003 Cyclohexane 7.18e-004 1.08e-002 Other Hexanes 6.22e-004 9.35e-003 Heptanes 4.47e-004 6.72e-003 Methylcyclohexane 1.48e-003 2.22e-002 Toluene 5.42e-003 8.14e-002 Xylenes 8.10e-003 1.22e-001 C8+ Heavies 4.63e-003 6.96e-002 Total Components 100.00 1.50e+003

FLASH TANK OFF GAS STREAM

_ _

 Temperature: Pressure: Flow Rate:	99.50 deg. F 65.40 psia 9.31e+002 scfh		
	Component		Loading (lb/hr)
	Carbon Dioxide Nitrogen Methane	1.50e-001 1.33e+001 3.32e-002 8.56e+001 7.98e-001	1.43e+001 2.28e-002 3.37e+001
	Isobutane n-Butane Isopentane	8.53e-002 1.45e-002 1.44e-002 4.41e-003 3.10e-003	2.06e-002 2.06e-002 7.81e-003
	Cyclohexane Other Hexanes	1.73e-003 1.74e-003	3.65e-003 3.58e-003 6.81e-003
		1.12e-003 5.05e-004	2.53e-003 1.31e-003
	Total Components	100.00	4.89e+001

FLASH TANK GLYCOL STREAM

Temperature: 99.50 deg. F Flow Rate: 2.59e+000 gpm Component Conc. Loading (wt%) (lb/hr) TEG 9.54e+001 1.39e+003 Water 4.48e+000 6.52e+001 Carbon Dioxide 1.22e-001 1.78e+000 Nitrogen 1.23e-005 1.78e-004 Methane 1.92e-002 2.78e-001

Ethane	1.27e-003	1.84e-002
Propane	4.84e-004	7.03e-003
Isobutane	1.75e-004	2.54e-003
n-Butane	2.36e-004	3.43e-003
Isopentane	1.09e-004	1.58e-003
	9.82e-005	
Cyclopentane	6.52e-005	9.48e-004
	1.27e-004	
Cyclohexane	4.96e-004	7.21e-003
Other Hexanes	1.75e-004	2.54e-003
Heptanes	2.42e-004	3.52e-003
Methylcyclohexane	1.12e-003	1.63e-002
Toluene	5.42e-003	7.88e-002
Xylenes	8.28e-003	1.20e-001
C8+ Heavies	4.44e-003	6.46e-002
Total Components	100.00	1.45e+003

FLASH GAS EMISSIONS

Control	Method:	Recycle/recompression
Control	Efficiency	100.00

Note: Flash Gas Emissions are zero with the Recycle/recompression control option.

REGENERATOR OVERHEADS STREAM

Temperature: Pressure: Flow Rate:	212.00 deg. F 14.70 psia 9.51e+002 scfh		
	Component		Loading (lb/hr)
	Carbon Dioxide Nitrogen Methane	9.76e+001 1.61e+000 2.54e-004 6.92e-001 2.45e-002	1.78e+000 1.78e-004 2.78e-001
	Isobutane n-Butane Isopentane	6.35e-003 1.74e-003 2.35e-003 8.58e-004 7.78e-004	2.54e-003 3.43e-003 1.55e-003
	Cyclohexane Other Hexanes	8.43e-004 3.27e-003	1.82e-003 6.89e-003 2.48e-003
	Methylcyclohexane Toluene Xylenes C8+ Heavies	3.14e-002 3.93e-002	7.25e-002 1.05e-001
	Total Components	100.00	4.64e+001

Dehydrator Reboiler Exhaust Emissions Calculations

Unit Number:	9b, 10b
Description:	Dehydrator Reboiler (12 mmscfd)

Note: The data on this worksheet applies to each individual emissions unit identified above.

Fuel Consumption

Samption	
1.087 MMBtu/hr	Capacity
1,208 scf/hr	Hourly fuel consumption
8,760 hr/yr	Annual operating time
9,524 MMBtu/yr	Annual fuel consumption
10.58 MMscf/yr	Annual fuel consumption
900 Btu/scf	Field gas heating value

scf/hr x Btu/scf / 1,000,000 Mfg. data (Enertek) Harvest MMBtu/hr x hr/yr scf/hr x hr/yr / 1,000,000 Nominal heat content

Steady-State Emission Rates

	Emission		
Pollutants	Factors,	Uncontrolled E	mission Rates,
	lb/day	pph	tpy
NOX	1.03	4.29E-02	1.88E-01
CO	0.78	3.25E-02	1.42E-01
VOC	0.12	4.79E-03	2.10E-02
SO2	0.02	8.33E-04	3.65E-03

NOX emission factor taken from August 1994 Enertek Letter

CO, TOC and SO2 emission factors taken from July 1998 InFab Letter

50% of TOC emissions are assumed to be VOC emissions, consistent with AP-42, Table 1.4-2 Uncontrolled Emission Rates (pph) = lb/day / 24 hr/day

Uncontrolled Emission Rates (tpy) = Uncontrolled Emission Rates (pph) x hr/yr / 2,000 lb/ton

Pollutants	Emission Factors,	Uncontrolled E	mission Rates,
	lb/MMscf	pph	tpy
PM	7.60	9.18E-03	4.02E-02
PM10	7.60	9.18E-03	4.02E-02
PM2.5	7.60	9.18E-03	4.02E-02

Emission factors taken from AP-42, Table 1.4-2

Uncontrolled Emission Rates (pph) = lb/MMscf x (scf/hr / 1,000,000)

Uncontrolled Emission Rates (tpy) = Uncontrolled Emission Rates (pph) x hr/yr / 2,000 lb/ton

Exhaust Parameters

Exhaust temperature
Stack flowrate
Stack diameter
Stack exit area
Stack velocity
Stack height

Mfg. data (Enertek & InFab) fps x ft^2 x 60 sec/min Mfg. data (InFab) 3.1416 x ((ft / 2) ^2) Mfg. data (Enertek & InFab) Mfg. data (InFab)

GRI-HAPCalc [®] 3.01 External Combustion Devices Report

Facility ID:	32-7 CDP	Notes:
Operation Type:	COMPRESSOR STATION	
Facility Name:	32-7 CDP	
User Name:	Cirrus	
Units of Measure:	U.S. STANDARD	

Note: Emissions less than 5.00E-09 tons (or tonnes) per year are considered insignificant and are treated as zero. These emissions are indicated on the report with a "0". Emissions between 5.00E-09 and 5.00E-05 tons (or tonnes) per year are represented on the report with "0.0000".

External Combustion Devices

Unit Name: 12MM_RBLR

Hours of Operation:	8,760	Yearly
Heat Input:	******	MMBtu/hr
Fuel Type:	NATURAL GA	AS
Device Type:	BOILER	
Emission Factor Set:	EPA > FIELD	> LITERATURE
Additional EF Set:	-NONE-	

Calculated Emissions (ton/yr)

Chemical Name	Emissions	Emission Factor	Emission Factor Set
HAPs_			
3-Methylcholanthrene	0.0000	0.000000018 lb/MMBtu	EPA
7,12-Dimethylbenz(a)anthracene	0.0000	0.000000157 lb/MMBtu	EPA
Formaldehyde	0.0003	0.0000735294 lb/MMBtu	EPA
Methanol	0.0020	0.0004333330 lb/MMBtu	GRI Field
Acetaldehyde	0.0014	0.0002909000 lb/MMBtu	GRI Field
1,3-Butadiene	0.0000	0.0000001830 lb/MMBtu	GRI Field
Benzene	0.0000	0.0000020588 lb/MMBtu	EPA
Toluene	0.0000	0.0000033333 lb/MMBtu	EPA
Ethylbenzene	0.0000	0.000000720 lb/MMBtu	GRI Field
Xylenes(m,p,o)	0.0000	0.0000010610 lb/MMBtu	GRI Field
2,2,4-Trimethylpentane	0.0002	0.0000323000 lb/MMBtu	GRI Field
n-Hexane	0.0083	0.0017647059 lb/MMBtu	EPA
Phenol	0.0000	0.000000950 lb/MMBtu	GRI Field
Naphthalene	0.0000	0.0000005980 lb/MMBtu	EPA
2-Methylnaphthalene	0.0000	0.000000235 lb/MMBtu	EPA
Acenaphthylene	0.0000	0.000000018 lb/MMBtu	EPA
Biphenyl	0.0000	0.0000011500 lb/MMBtu	GRI Field
Acenaphthene	0.0000	0.000000018 lb/MMBtu	EPA
Fluorene	0.0000	0.000000027 lb/MMBtu	EPA
Anthracene	0.0000	0.000000024 lb/MMBtu	EPA
Phenanthrene	0.0000	0.000000167 lb/MMBtu	EPA
Fluoranthene	0.0000	0.000000029 lb/MMBtu	EPA
Pyrene	0.0000	0.000000049 lb/MMBtu	EPA
Benz(a)anthracene	0.0000	0.000000018 lb/MMBtu	EPA
Chrysene	0.0000	0.000000018 lb/MMBtu	EPA

Benzo(a)pyrene	0.0000	0.0000000012 lb/MMBtu	EPA
Benzo(b)fluoranthene	0.0000	0.000000018 lb/MMBtu	EPA
Benzo(k)fluoranthene	0.0000	0.000000018 lb/MMBtu	EPA
Benzo(g,h,i)perylene	0.0000	0.000000012 lb/MMBtu	EPA
Indeno(1,2,3-c,d)pyrene	0.0000	0.000000018 lb/MMBtu	EPA
Dibenz(a,h)anthracene	0.0000	0.000000012 lb/MMBtu	EPA
Lead	0.0000	0.0000004902 lb/MMBtu	EPA
Total	0.0122		
Criteria Pollutants			
VOC	0.0255	0.0053921569 lb/MMBtu	EPA
PM	0.0352	0.0074509804 lb/MMBtu	EPA
PM, Condensible	0.0264	0.0055882353 lb/MMBtu	EPA
PM, Filterable	0.0088	0.0018627451 lb/MMBtu	EPA
СО	0.3896	0.0823529410 lb/MMBtu	EPA
NMHC	0.0403	0.0085294118 lb/MMBtu	EPA
NOx	0.4638	0.0980392157 lb/MMBtu	EPA
SO2	0.0028	0.0005880000 lb/MMBtu	EPA

Other Pollutants

Dichlorobenzene	0.0000	0.0000011765	lb/MMBtu	EPA
Methane	0.0107	0.0022549020	lb/MMBtu	EPA
Acetylene	0.0252	0.0053314000	lb/MMBtu	GRI Field
Ethylene	0.0025	0.0005264000	lb/MMBtu	GRI Field
Ethane	0.0144	0.0030392157	lb/MMBtu	EPA
Propylene	0.0044	0.0009333330	lb/MMBtu	GRI Field
Propane	0.0074	0.0015686275	lb/MMBtu	EPA
Butane	0.0097	0.0020588235	lb/MMBtu	EPA
Cyclopentane	0.0002	0.0000405000	lb/MMBtu	GRI Field
Pentane	0.0121	0.0025490196	lb/MMBtu	EPA
n-Pentane	0.0095	0.0020000000	lb/MMBtu	GRI Field
Cyclohexane	0.0002	0.0000451000	lb/MMBtu	GRI Field
Methylcyclohexane	0.0008	0.0001691000	lb/MMBtu	GRI Field
n-Octane	0.0002	0.0000506000	lb/MMBtu	GRI Field
n-Nonane	0.0000	0.0000050000	lb/MMBtu	GRI Field
CO2	556.5176	117.6470588235	lb/MMBtu	EPA

GRI-GLYCalc VERSION 4.0 - SUMMARY OF INPUT VALUES Case Name: 32-7 EU 11a, 12a, 24a & 25a PTE (gas 2021-06-22) File Name: C:\Users\user\Documents\Cirrus\Permit applications\New Mexico\Harvest Four Corners\32-7\TITLE V\2021-01 Title V Renewal\Analyses & Info\GLYCalc\32-7 20 mm dehys PTE (gas 2021-06-22).ddf Date: January 05, 2022 DESCRIPTION: _____ Description: 32-7 EU 11, 12, 24 & 25 - 20 mmcfd dehys PTE Title V Renewal Appl 6/22/2021 GAS ext. analysis & avg parameters inc.flash tank temp & pressure Annual Hours of Operation: 8760.0 hours/yr WET GAS: _____ Temperature: 115.00 deg. F Pressure: 928.00 psig Wet Gas Water Content: Saturated Component Conc. (vol %) _____ ____
 Carbon Dioxide
 6.9673

 Nitrogen
 0.0353

 Methane
 92.1867

 Ethane
 0.7106

 Propane
 0.0677
 Isobutane 0.0106 n-Butane 0.0097 Isopentane 0.0031 n-Pentane 0.0020 Cyclopentane 0.0002 n-Hexane 0.0010 Cyclohexane 0.0006 Other Hexanes 0.0020 Heptanes 0.0007 Methylcyclohexane 0.0010
 Toluene
 0.0004

 Xylenes
 0.0003

 C8+ Heavies
 0.0011
 DRY GAS: _____ Flow Rate: 20.0 MMSCF/day Water Content: 7.0 lbs. H2O/MMSCF LEAN GLYCOL: _____ Glycol Type: TEG Water Content: 1.5 wt% H2O Flow Rate: 2.5 gpm

Page: 1

Glycol Pump Type: Gas Injection Gas Injection Pump Volume Ratio: 0.080 acfm gas/gpm glycol

FLASH TANK:

Flash Control: Recycle/recompression Temperature: 99.5 deg. F Pressure: 50.7 psig GRI-GLYCalc VERSION 4.0 - AGGREGATE CALCULATIONS REPORT

Case Name: 32-7 EU 11a, 12a, 24a & 25a PTE (gas 2021-06-22)
File Name: C:\Users\user\Documents\Cirrus\Permit applications\New Mexico\Harvest Four
Corners\32-7\TITLE V\2021-01 Title V Renewal\Analyses & Info\GLYCalc\32-7 20 mm dehys PTE
(gas 2021-06-22).ddf
Date: January 05, 2022

DESCRIPTION:

Description: 32-7 EU 11, 12, 24 & 25 - 20 mmcfd dehys PTE Title V Renewal Appl 6/22/2021 GAS ext. analysis & avg parameters inc.flash tank temp & pressure

Annual Hours of Operation: 8760.0 hours/yr

EMISSIONS REPORTS:

UNCONTROLLED REGENERATOR EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane	0.2694	6.465	1.1799
Ethane	0.0169	0.405	0.0739
Propane	0.0069	0.165	0.0301
Isobutane	0.0024	0.058	0.0107
n-Butane	0.0033	0.079	0.0144
Isopentane	0.0015	0.035	0.0064
n-Pentane	0.0013	0.032	0.0058
Cyclopentane	0.0008	0.020	0.0037
n-Hexane	0.0017	0.041	0.0074
Cyclohexane	0.0063	0.151	0.0275
Other Hexanes	0.0023	$0.055 \\ 0.077 \\ 0.341 \\ 1.798 \\ 2.745$	0.0101
Heptanes	0.0032		0.0141
Methylcyclohexane	0.0142		0.0623
Toluene	0.0749		0.3281
Xylenes	0.1144		0.5010
C8+ Heavies	0.0527	1.265	0.2309
Total Emissions	0.5722	13.734	2.5064
Total Hydrocarbon Emissions	0.5722	$ \begin{array}{r} 13.734 \\ 6.863 \\ 4.584 \\ 4.543 \end{array} $	2.5064
Total VOC Emissions	0.2860		1.2526
Total HAP Emissions	0.1910		0.8365
Total BTEX Emissions	0.1893		0.8291

FLASH GAS EMISSIONS

Note: Flash Gas Emissions are zero with the Recycle/recompression control option.

FLASH TANK	OFF GAS			
	Component	lbs/hr	lbs/day	tons/yr

Methane Ethane Propane Isobutane n-Butane	34.1789 0.5915 0.0931 0.0207 0.0207	14.195 2.235	2.5906 0.4078
Isopentane n-Pentane Cyclopentane n-Hexane Cyclohexane	0.0079 0.0055 0.0010 0.0037 0.0037	0.132 0.024	
Toluene Xylenes	0.0069 0.0033 0.0062 0.0028 0.0015	0.149 0.068 0.037	0.0143 0.0271 0.0124 0.0068
C8+ Heavies Total Emissions		0.132	
Total Hydrocarbon Emissions Total VOC Emissions Total HAP Emissions Total BTEX Emissions	34.9529 0.1825 0.0081 0.0044		0.7992

COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane	0.2694	6.465	$\begin{array}{c} 1.1799 \\ 0.0739 \\ 0.0301 \\ 0.0107 \\ 0.0144 \end{array}$
Ethane	0.0169	0.405	
Propane	0.0069	0.165	
Isobutane	0.0024	0.058	
n-Butane	0.0033	0.079	
Isopentane	0.0015	$\begin{array}{c} 0.035 \\ 0.032 \\ 0.020 \\ 0.041 \\ 0.151 \end{array}$	0.0064
n-Pentane	0.0013		0.0058
Cyclopentane	0.0008		0.0037
n-Hexane	0.0017		0.0074
Cyclohexane	0.0063		0.0275
Other Hexanes	0.0023	0.055	0.0101
Heptanes	0.0032	0.077	0.0141
Methylcyclohexane	0.0142	0.341	0.0623
Toluene	0.0749	1.798	0.3281
Xylenes	0.1144	2.745	0.5010
C8+ Heavies	0.0527	1.265	0.2309
Total Emissions	0.5722	$ 13.734 \\ 13.734 \\ 6.863 \\ 4.584 \\ 4.543 $	2.5064
Total Hydrocarbon Emissions	0.5722		2.5064
Total VOC Emissions	0.2860		1.2526
Total HAP Emissions	0.1910		0.8365
Total BTEX Emissions	0.1893		0.8291

COMBINED REGENERATOR VENT/FLASH GAS EMISSION CONTROL REPORT:

Component	Uncontrolled tons/yr	Controlled tons/yr	% Reduction
Methane	150.8836	1.1799	99.22

Ethane Propane Isobutane n-Butane	2.6646 0.4379 0.1015 0.1050	0.0739 0.0301 0.0107 0.0144	Page: 3 97.22 93.13 89.49 86.27
Isopentane	0.0409	0.0064	84.23
n-Pentane	0.0300	0.0058	80.56
Cyclopentane	0.0080	0.0037	53.71
n-Hexane	0.0236	0.0074	68.48
Cyclohexane	0.0438	0.0275	37.22
Other Hexanes	0.0401	0.0101	74.79
Heptanes	0.0284	0.0141	50.36
Methylcyclohexane	0.0894	0.0623	30.33
Toluene	0.3405	0.3281	3.65
Xylenes	0.5078	0.5010	1.34
C8+ Heavies Total Emissions	0.2549 155.5999	0.2309 2.5064	9.42 98.39
Total Hydrocarbon Emissions	155.5999	2.5064	98.39
Total VOC Emissions	2.0518	1.2526	38.95
Total HAP Emissions	0.8719	0.8365	4.05
Total BTEX Emissions	0.8483	0.8291	2.26

EQUIPMENT REPORTS:

ABSORBER

Calculated Absorber Stages:	1.48	
Specified Dry Gas Dew Point:	7.00	lbs. H2O/MMSCF
Temperature:	115.0	deg. F
Pressure:	928.0	psig
Dry Gas Flow Rate:	20.0000	MMSCF/day
Glycol Losses with Dry Gas:	0.4525	lb/hr
Wet Gas Water Content:	Saturated	
Calculated Wet Gas Water Content:	94.49	lbs. H2O/MMSCF
Calculated Lean Glycol Recirc. Ratio:	2.06	gal/lb H2O

Component	Remaining in Dry Gas	Absorbed in Glycol
Water	7.39%	92.61%
Carbon Dioxide	99.85%	0.15%
Nitrogen	99.99%	0.01%
Methane	99.99%	0.01%
Ethane	99.96%	0.04%
Propane	99.94%	0.06%
Isobutane	99.92%	0.08%
n-Butane	99.90%	0.10%
Isopentane	99.90%	0.10%
n-Pentane	99.88%	0.12%
Cyclopentane	99.50%	0.50%
n-Hexane	99.81%	0.19%
Cyclohexane	99.19%	0.81%
Other Hexanes	99.85%	0.15%
Heptanes	99.67%	0.33%
Methylcyclohexane	99.15%	0.85%
Toluene	90.49%	9.51%

			r age
	Xylenes	83.52%	16.48%
C8+	Heavies	98.68%	1.32%

FLASH TANK

Flash Control: Recycle/recompression Flash Temperature: 99.5 deg. F Flash Pressure: 50.7 psig

Flash Pless	ure. 50	./ psig
Component	Left in Glycol	Removed in Flash Gas
Water	99.90%	0.10%
Carbon Dioxide	10.70%	89.30%
Nitrogen	0.72%	99.28%
Methane	0.78%	99.22%
Ethane	2.78%	97.22%
Propane	6.87%	93.13%
Isobutane	10.51%	89.49%
n-Butane	13.73%	86.27%
Isopentane	15.98%	84.02%
n-Pentane	19.66%	80.34%
Cyclopentane	46.52%	53.48%
n-Hexane	31.74%	68.26%
Cyclohexane	63.85%	36.15%
Other Hexanes	25.66%	74.34%
Heptanes	49.84%	50.16%
Methylcyclohexane	70.76%	29.24%
Toluene	96.64%	3.36%
Xylenes	98.84%	1.16%
C8+ Heavies	91.64%	8.36%

REGENERATOR

No Stripping Gas used in regenerator.

Component	Remaining in Glycol	
Water	22.42%	77.58%
Carbon Dioxide	0.00%	100.00%
Nitrogen	0.00%	100.00%
Methane	0.00%	100.00%
Ethane	0.00%	100.00%
Propane Isobutane n-Butane Isopentane n-Pentane	0.00% 0.00% 1.58% 1.43%	100.00% 100.00% 100.00% 98.42% 98.57%
Cyclopentane	0.90%	99.10%
n-Hexane	1.05%	98.95%
Cyclohexane	4.50%	95.50%
Other Hexanes	2.39%	97.61%
Heptanes	0.78%	99.22%
Methylcyclohexane	5.11%	94.89%
Toluene	8.10%	91.90%
Xylenes	13.02%	86.98%
C8+ Heavies	12.33%	87.67%

Page: 4

STREAM REPORTS:

WET GAS STREAM

WET GAS	SIREAM			
Pres	sure:	115.00 deg. F 942.70 psia 8.35e+005 scfh		
		Component	Conc. (vol%)	Loading (lb/hr)
		Carbon Dioxide Nitrogen Methane	1.99e-001 6.95e+000 3.52e-002 9.20e+001 7.09e-001	6.74e+003 2.17e+001 3.25e+004
		Isobutane n-Butane Isopentane	6.76e-002 1.06e-002 9.68e-003 3.09e-003 2.00e-003	1.35e+001 1.24e+001 4.91e+000
		Cyclohexane Other Hexanes	9.98e-004 5.99e-004	1.89e+000 1.11e+000 3.79e+000
		Methylcyclohexane Toluene Xylenes C8+ Heavies	3.99e-004 2.99e-004 1.10e-003	8.10e-001 7.00e-001
		Total Components		3.99e+004
DRY GAS	STREAM			
Pres	sure:	115.00 deg. F 942.70 psia 8.33e+005 scfh		
		Component		Loading (lb/hr)
		Carbon Dioxide Nitrogen Methane	1.47e-002 6.96e+000 3.53e-002 9.22e+001 7.10e-001	6.73e+003 2.17e+001 3.25e+004
		Isobutane n-Butane Isopentane	6.77e-002 1.06e-002 9.69e-003 3.10e-003 2.00e-003	1.35e+001 1.24e+001 4.91e+000
		Cyclopentane n-Hexane Cyclohexane Other Hexanes	9.98e-004 5.95e-004	1.89e+000 1.10e+000

Heptanes 6.98e-004 1.54e+000

	3.62e-004 2.51e-004	7.33e-001 5.84e-001
Total Components	100.00	3.98e+004

LEAN GLYCOL STREAM

_____ Temperature: 115.00 deg. F Flow Rate: 2.50e+000 gpm (wt%) (lb/) Conc. Component _____ ____ TEG 9.85e+001 1.39e+003 Water 1.50e+000 2.11e+001 Carbon Dioxide 6.94e-011 9.77e-010 Nitrogen 1.96e-014 2.76e-013 Methane 9.06e-018 1.28e-016 Ethane 5.55e-009 7.81e-008 Propane 1.10e-010 1.55e-009 Isobutane 2.22e-011 3.12e-010 n-Butane 2.16e-011 3.05e-010 Isopentane 1.68e-006 2.36e-005 n-Pentane 1.38e-006 1.94e-005 Cyclopentane 5.49e-007 7.73e-006 n-Hexane 1.28e-006 1.81e-005 Cyclohexane 2.10e-005 2.96e-004 Other Hexanes 4.01e-006 5.65e-005 Heptanes 1.79e-006 2.52e-005 Methylcyclohexane 5.44e-005 7.65e-004 Toluene 4.69e-004 6.61e-003 Xylenes 1.22e-003 1.71e-002 C8+ Heavies 5.27e-004 7.42e-003 _____ _____ Total Components 100.00 1.41e+003

RICH GLYCOL AND PUMP GAS STREAM

Temperature: 115.00 deg. F Pressure: 942.70 psia Flow Rate: 2.76e+000 gpm NOTE: Stream has more than one phase.

 Component
 Conc. (wt%)
 Loading (lb/hr)

 TEG
 9.05e+001
 1.39e+003

 Water
 6.16e+000
 9.43e+001

 Carbon Dioxide
 1.05e+000
 1.61e+001

 Nitrogen
 1.52e-003
 2.33e-002

 Methane
 2.25e+000
 3.44e+001

 Ethane
 3.97e-002
 6.08e-001

 Propane
 6.53e-003
 1.00e-001

 Isobutane
 1.51e-003
 2.32e-002

 n-Butane
 1.57e-003
 2.40e-002

 Isopentane
 6.11e-004
 9.35e-003

 n-Pentane
 4.48e-004
 6.87e-003

Cyclopentane 1.20e-004 1.84e-003 n-Hexane 3.53e-004 5.40e-003 Cyclohexane 6.73e-004 1.03e-002 Other Hexanes 6.02e-004 9.22e-003 Heptanes 4.25e-004 6.50e-003 Methylcyclohexane 1.38e-003 2.12e-002 Toluene 5.51e-003 8.43e-002 Xylenes 8.69e-003 1.33e-001 C8+ Heavies 4.29e-003 6.56e-002 _____ ____ Total Components 100.00 1.53e+003 FLASH TANK OFF GAS STREAM _____ Temperature: 99.50 deg. F Pressure: 65.40 psia Flow Rate: 9.44e+002 scfh Component Conc. Loading (vol%) (lb/hr) ----- ------Water 2.17e-001 9.71e-002 Carbon Dioxide 1.32e+001 1.44e+001 Nitrogen 3.31e-002 2.31e-002 Methane 8.57e+001 3.42e+001 Ethane 7.91e-001 5.91e-001 Propane 8.49e-002 9.31e-002 Isobutane 1.44e-002 2.07e-002 n-Butane 1.43e-002 2.07e-002 Isopentane 4.38e-003 7.86e-003 n-Pentane 3.07e-003 5.52e-003 Cyclopentane 5.63e-004 9.82e-004 n-Hexane 1.72e-003 3.69e-003 Cyclohexane 1.78e-003 3.72e-003 Other Hexanes 3.20e-003 6.85e-003 Heptanes 1.31e-003 3.26e-003 Methylcyclohexane 2.53e-003 6.19e-003 Toluene 1.24e-003 2.83e-003 Xylenes 5.87e-004 1.55e-003 C8+ Heavies 1.29e-003 5.48e-003 ----- -----_____

FLASH TANK GLYCOL STREAM

Temperature: 99.50 deg. F Flow Rate: 2.65e+000 gpm		
Component		Loading (lb/hr)
Water Carbon Dioxide Nitroger	9.35e+001 6.36e+000 1.16e-001 1.14e-005 e 1.82e-002	9.42e+001 1.73e+000 1.68e-004
Propane Isobutane n-Butane	e 1.14e-003 e 4.64e-004 e 1.64e-004 e 2.22e-004 e 1.01e-004	6.87e-003 2.44e-003 3.29e-003

Total Components 100.00 4.95e+001

n-Pentane 9.11e-005 1.35e-003 Cyclopentane 5.77e-005 8.54e-004 n-Hexane 1.16e-004 1.71e-003 Cyclohexane 4.44e-004 6.58e-003 Other Hexanes 1.60e-004 2.37e-003 Methylcyclohexane 1.01e-003 1.50e-002 Toluene 5.50e-003 8.15e-002 Xylenes 8.88e-003 1.32e-001 C8+ Heavies 4.06e-003 6.01e-002 Total Components 100.00 1.48e+003

FLASH GAS EMISSIONS

Control Method: Recycle/recompression

Control Efficiency: 100.00

Note: Flash Gas Emissions are zero with the Recycle/recompression control option.

REGENERATOR OVERHEADS STREAM

_____ Temperature: 212.00 deg. F Pressure: 14.70 psia Flow Rate: 1.56e+003 scfh Conc. Component Loading (vol%) (lb/hr) _____ Water 9.86e+001 7.31e+001 Carbon Dioxide 9.53e-001 1.73e+000 Nitrogen 1.46e-004 1.68e-004 Methane 4.08e-001 2.69e-001 Ethane 1.36e-002 1.69e-002 Propane 3.78e-003 6.87e-003 Isobutane 1.02e-003 2.44e-003 n-Butane 1.38e-003 3.29e-003 Isopentane 4.95e-004 1.47e-003 n-Pentane 4.48e-004 1.33e-003 Cyclopentane 2.93e-004 8.47e-004 n-Hexane 4.78e-004 1.70e-003 Cyclohexane 1.81e-003 6.28e-003 Other Hexanes 6.51e-004 2.31e-003 Heptanes 7.80e-004 3.22e-003 Methylcyclohexane 3.52e-003 1.42e-002 Toluene 1.98e-002 7.49e-002 Xylenes 2.62e-002 1.14e-001 C8+ Heavies 7.52e-003 5.27e-002 _____ ____ Total Components 100.00 7.54e+001

Dehydrator Reboiler Exhaust Emissions Calculations

Unit Number:	11b, 12b, 24b, 25b
Description:	Dehydrator Reboiler (20 mmscfd)

Note: The data on this worksheet applies to each individual emissions unit identified above.

Fuel Consumption

noumption	
1.483 MMBtu/hr	Capacity
1,648 scf/hr	Hourly fuel consumption
8,760 hr/yr	Annual operating time
12,993 MMBtu/yr	Annual fuel consumption
14.44 MMscf/yr	Annual fuel consumption
900 Btu/scf	Field gas heating value

scf/hr x Btu/scf / 1,000,000 Mfg. data (Enertek) Harvest MMBtu/hr x hr/yr scf/hr x hr/yr / 1,000,000 Nominal heat content

Steady-State Emission Rates

Pollutants	Emission Factors.	Lincontrolled F	mission Rates,
Foliularits	lb/day	pph	tpy
	(12
NOX	1.03	4.29E-02	1.88E-01
CO	1.07	4.46E-02	1.95E-01
VOC	0.16	6.46E-03	2.83E-02
SO2	0.02	8.33E-04	3.65E-03

NOX emission factor taken from August 1994 Enertek Letter

CO, TOC and SO2 emission factors taken from July 1998 InFab Letter

50% of TOC emissions are assumed to be VOC emissions, consistent with AP-42, Table 1.4-2 Uncontrolled Emission Rates (pph) = lb/day / 24 hr/day

Uncontrolled Emission Rates (tpy) = Uncontrolled Emission Rates (pph) x hr/yr / 2,000 lb/ton

Pollutants	Emission Factors,	Uncontrolled Emission Rates,	
	lb/MMscf	pph	tpy
PM	7.60	1.25E-02	5.49E-02
PM10	7.60	1.25E-02	5.49E-02
PM2.5	7.60	1.25E-02	5.49E-02

Emission factors taken from AP-42, Table 1.4-2

Uncontrolled Emission Rates (pph) = lb/MMscf x (scf/hr / 1,000,000)

Uncontrolled Emission Rates (tpy) = Uncontrolled Emission Rates (pph) x hr/yr / 2,000 lb/ton

Exhaust Parameters

600 °F	Exhaust temperature
287.46 cfm	Stack flowrate
1.00 ft	Stack diameter
0.79 ft^2	Stack exit area
6.1 fps	Stack velocity
10.0 ft	Stack height

Mfg. data (Enertek & InFab) fps x ft^2 x 60 sec/min Mfg. data (InFab) 3.1416 x ((ft / 2) ^2) Mfg. data (Enertek & InFab) Mfg. data (InFab)

GRI-HAPCalc [®] 3.01 External Combustion Devices Report

Facility ID:	32-7 CDP	Notes:	
Operation Type:	COMPRESSOR STATION		
Facility Name:	32-7 CDP		
User Name:	Cirrus		
Units of Measure:	U.S. STANDARD		

Note: Emissions less than 5.00E-09 tons (or tonnes) per year are considered insignificant and are treated as zero. These emissions are indicated on the report with a "0". Emissions between 5.00E-09 and 5.00E-05 tons (or tonnes) per year are represented on the report with "0.0000".

External Combustion Devices

Unit Name: 20MM_RBLR

Hours of Operation:	8,760	Yearly
Heat Input:	******	MMBtu/hr
Fuel Type:	NATURAL GA	AS
Device Type:	BOILER	
Emission Factor Set:	EPA > FIELD	> LITERATURE
Additional EF Set:	-NONE-	

Calculated Emissions (ton/yr)

Chemical Name	Emissions	Emission Factor	Emission Factor Set
<u>HAPs</u>			
3-Methylcholanthrene	0.0000	0.000000018 lb/MMBtu	EPA
7,12-Dimethylbenz(a)anthracene	0.0000	0.000000157 lb/MMBtu	EPA
Formaldehyde	0.0005	0.0000735294 lb/MMBtu	EPA
Methanol	0.0028	0.0004333330 lb/MMBtu	GRI Field
Acetaldehyde	0.0019	0.0002909000 lb/MMBtu	GRI Field
1,3-Butadiene	0.0000	0.0000001830 lb/MMBtu	GRI Field
Benzene	0.0000	0.0000020588 lb/MMBtu	EPA
Toluene	0.0000	0.0000033333 lb/MMBtu	EPA
Ethylbenzene	0.0000	0.000000720 lb/MMBtu	GRI Field
Xylenes(m,p,o)	0.0000	0.0000010610 lb/MMBtu	GRI Field
2,2,4-Trimethylpentane	0.0002	0.0000323000 lb/MMBtu	GRI Field
n-Hexane	0.0114	0.0017647059 lb/MMBtu	EPA
Phenol	0.0000	0.000000950 lb/MMBtu	GRI Field
Naphthalene	0.0000	0.0000005980 lb/MMBtu	EPA
2-Methylnaphthalene	0.0000	0.000000235 lb/MMBtu	EPA
Acenaphthylene	0.0000	0.000000018 lb/MMBtu	EPA
Biphenyl	0.0000	0.0000011500 lb/MMBtu	GRI Field
Acenaphthene	0.0000	0.000000018 lb/MMBtu	EPA
Fluorene	0.0000	0.000000027 lb/MMBtu	EPA
Anthracene	0.0000	0.000000024 lb/MMBtu	EPA
Phenanthrene	0.0000	0.000000167 lb/MMBtu	EPA
Fluoranthene	0.0000	0.000000029 lb/MMBtu	EPA
Pyrene	0.0000	0.000000049 lb/MMBtu	EPA
Benz(a)anthracene	0.0000	0.000000018 lb/MMBtu	EPA
Chrysene	0.0000	0.000000018 lb/MMBtu	EPA

Benzo(a)pyrene	0.0000	0.0000000012 lb/MMBtu	EPA
Benzo(b)fluoranthene	0.0000	0.000000018 lb/MMBtu	EPA
Benzo(k)fluoranthene	0.0000	0.000000018 lb/MMBtu	EPA
Benzo(g,h,i)perylene	0.0000	0.000000012 lb/MMBtu	EPA
Indeno(1,2,3-c,d)pyrene	0.0000	0.000000018 lb/MMBtu	EPA
Dibenz(a,h)anthracene	0.0000	0.000000012 lb/MMBtu	EPA
Lead	0.0000	0.0000004902 lb/MMBtu	EPA
Total	0.0168		
Criteria Pollutants			
VOC	0.0350	0.0053921569 lb/MMBtu	EPA
PM	0.0483	0.0074509804 lb/MMBtu	EPA
PM, Condensible	0.0362	0.0055882353 lb/MMBtu	EPA
PM, Filterable	0.0121	0.0018627451 lb/MMBtu	EPA
со	0.5338	0.0823529410 lb/MMBtu	EPA
NMHC	0.0553	0.0085294118 lb/MMBtu	EPA
NOx	0.6355	0.0980392157 lb/MMBtu	EPA
SO2	0.0038	0.0005880000 lb/MMBtu	EPA
Other Pollutants			

Dichlorobenzene	0.0000	0.0000011765	lb/MMBtu	EPA
Methane	0.0146	0.0022549020	lb/MMBtu	EPA
Acetylene	0.0346	0.0053314000	lb/MMBtu	GRI Field
Ethylene	0.0034	0.0005264000	lb/MMBtu	GRI Field
Ethane	0.0197	0.0030392157	lb/MMBtu	EPA
Propylene	0.0061	0.0009333330	lb/MMBtu	GRI Field
Propane	0.0102	0.0015686275	lb/MMBtu	EPA
Butane	0.0133	0.0020588235	lb/MMBtu	EPA
Cyclopentane	0.0003	0.0000405000	lb/MMBtu	GRI Field
Pentane	0.0165	0.0025490196	lb/MMBtu	EPA
n-Pentane	0.0130	0.0020000000	lb/MMBtu	GRI Field
Cyclohexane	0.0003	0.0000451000	lb/MMBtu	GRI Field
Methylcyclohexane	0.0011	0.0001691000	lb/MMBtu	GRI Field
n-Octane	0.0003	0.0000506000	lb/MMBtu	GRI Field
n-Nonane	0.0000	0.0000050000	lb/MMBtu	GRI Field
CO2	762.6353	117.6470588235	lb/MMBtu	EPA

TANKS 4.0.9d Emissions Report - Detail Format Tank Indentification and Physical Characteristics

Identification User Identification: City: State: Company:////////////////////////////////////	32-7 Methanol (500 gal) Rio Arriba Co., T-32N, R-07W, Sec 34 NM ₩₩₽æç^•cFour CornersĔŠŠÔ Vertical Fixed Roof Tank 500 gal (11.9 bbl) Methanol tank 6,000 gal throughput (12 turnovers)
Tank Dimensions Shell Height (ft): Diameter (ft): Liquid Height (ft) : Avg. Liquid Height (ft): Volume (gallons): Turnovers: Net Throughput(gal/yr): Is Tank Heated (y/n):	5.00 4.50 4.00 2.00 500.00 12.00 6,000.00 N
Paint Characteristics Shell Color/Shade: Shell Condition Roof Color/Shade: Roof Condition:	White/White Good White/White Good
Roof Characteristics Type: Height (ft) Slope (ft/ft) (Cone Roof)	Cone 0.00 0.06
Breather Vent Settings Vacuum Settings (psig): Pressure Settings (psig)	-0.03 0.03

Meterological Data used in Emissions Calculations: Albuquerque, New Mexico (Avg Atmospheric Pressure = 12.15 psia)

TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

32-7 Methanol (500 gal) - Vertical Fixed Roof Tank Rio Arriba Co., T-32N, R-07W, Sec 34, NM

			aily Liquid S perature (d		Liquid Bulk Temp	Vapo	r Pressure	(psia)	Vapor Mol.	Liquid Mass	Vapor Mass	Mol.	Basis for Vapor Pressure
Mixture/Component	Month	Avg.	Min.	Max.	(deg F)	Avg.	Min.	Max.	Weight.	Fract.	Fract.	Weight	Calculations
Methyl alcohol	All	58.54	51.41	65.66	56.17	1.3769	1.0943	1.7198	32.0400			32.04	Option 2: A=7.897, B=1474.08, C=229.13

TANKS 4.0.9d Emissions Report - Detail Format Detail Calculations (AP-42)

32-7 Methanol (500 gal) - Vertical Fixed Roof Tank Rio Arriba Co., T-32N, R-07W, Sec 34, NM

Annual Emission Calcaulations	
Standing Losses (lb): Vapor Space Volume (cu ft):	12.3406 48.4585
Vapor Density (lb/cu ft):	0.0079
Vapor Space Expansion Factor:	0.1075
Vented Vapor Saturation Factor:	0.8181
Tank Vapor Space Volume: Vapor Space Volume (cu ft):	48.4585
Tank Diameter (ft):	4.5000
Vapor Space Outage (ft):	3.0469
Tank Shell Height (ft):	5.0000
Average Liquid Height (ft):	2.0000
Roof Outage (ft):	0.0469
Roof Outage (Cone Roof)	
Roof Outage (ft):	0.0469
Roof Height (ft):	0.0000
Roof Slope (ft/ft):	0.0625
Shell Radius (ft):	2.2500
Vapor Density Vapor Density (lb/cu ft):	0.0079
Vapor Molecular Weight (lb/lb-mole): Vapor Pressure at Daily Average Liquid	32.0400
Surface Temperature (psia):	1.3769
Daily Avg. Liquid Surface Temp. (deg. R):	518.2062
Daily Average Ambient Temp. (deg. F): Ideal Gas Constant R	56.1542
(psia cuft / (lb-mol-deg R)):	10.731
Liquid Bulk Temperature (deg. R):	515.8442
Tank Paint Solar Absorptance (Shell):	0.1700
Tank Paint Solar Absorptance (Roof):	0.1700
Daily Total Solar Insulation	
Factor (Btu/sqft day):	1,765.3167
Vapor Space Expansion Factor	
Vapor Space Expansion Factor:	0.1075
Daily Vapor Temperature Range (deg. R):	28.5089
Daily Vapor Pressure Range (psia):	0.6255
Breather Vent Press. Setting Range(psia):	0.0600
Vapor Pressure at Daily Average Liquid	1.0700
Surface Temperature (psia): Vapor Pressure at Daily Minimum Liquid	1.3769
Surface Temperature (psia):	1.0943
Vapor Pressure at Daily Maximum Liquid	1.0345
Surface Temperature (psia):	1.7198
Daily Avg. Liquid Surface Temp. (deg R):	518.2062
Daily Min. Liquid Surface Temp. (deg R):	511.0790
Daily Max. Liquid Surface Temp. (deg R):	525.3334
Daily Ambient Temp. Range (deg. R):	27.9250
Vented Vapor Saturation Factor	
Vented Vapor Saturation Factor:	0.8181
Vapor Pressure at Daily Average Liquid:	
Surface Temperature (psia):	1.3769
Vapor Space Outage (ft):	3.0469
Working Losses (Ib):	6.3024
Vapor Molecular Weight (lb/lb-mole):	32.0400
Vapor Pressure at Daily Average Liquid	32.0400
rape. 1. coouro ar Daily Avorago Elquid	

Surface Temperature (psia):	1.3769
Annual Net Throughput (gal/yr.):	6,000.0000
Annual Turnovers:	12.0000
Turnover Factor:	1.0000
Maximum Liquid Volume (gal):	500.0000
Maximum Liquid Height (ft):	4.0000
Tank Diameter (ft):	4.5000
Working Loss Product Factor:	1.0000
Tatal Lagana (Ib):	18 6430
Total Losses (lb):	18.6430

TANKS 4.0.9d Emissions Report - Detail Format Individual Tank Emission Totals

Emissions Report for: Annual

32-7 Methanol (500 gal) - Vertical Fixed Roof Tank Rio Arriba Co., T-32N, R-07W, Sec 34, NM

	Losses(lbs)					
Components	Working Loss	Breathing Loss	Total Emissions			
Methyl alcohol	6.30	12.34	18.64			

Truck Loading Emissions Calculations

Unit Number: L-1 (Insignificant source demonstration) Description: Truck Loading - Produced Water

Emission Factor

True vapor pressure of liquid, P
Molecular weight of vapors, M
Temperature of liquid
Temperature of liquid, T
Emission factor, L

Production Rate

8.40 10^3 gal/hr 1,302.00 10^3 gal/yr

Steady-State Emission Rates

Pollutant	Uncontrolled I	Emission Rates,
	pph	tpy
VOC	0.77	5.99E-02

Uncontrolled Emission Rate (pph) = lb/10^3 gal x 10^3 gal/hr Uncontrolled Emission Rate (tpy) = lb/10^3 gal x 10^3 gal/yr / 2,000 lb/ton

Maximum hourly production rate

Maximum annual production rate

	Wt		
Pollutants	Fraction	Emissio	n Rates,
	of HAP	pph	tpy
Benzene	0.0267	2.07E-02	1.60E-03
Ethylbenzene	0.0027	2.07E-03	1.60E-04
n-Hexane	0.0840	6.49E-02	5.03E-03
Toluene	0.0344	2.66E-02	2.06E-03
m-Xylene	0.0229	1.77E-02	1.37E-03

Wt. Fraction of HAP = CDPHE/TCEQ Produced Water HAP emission factor (lb/bbl) / VOC emission factor (lb/bbl). Emission rate, pph = Wt. Fraction of HAP x VOC Emission rate (pph)

Emission rate, tpy = Wt. Fraction of VOC x VOC Emission rate (tpy)

AP-42, Table 5.2-1 (submerged loading

& dedicated service)

TANKS 4.0 output file for similar fixed roof tank TANKS 4.0 output file for similar fixed roof tank TANKS 4.0 output file for similar fixed roof tank $^\circ\text{F}$ + 459.67

AP-42, Section 5.2, Equation 1

$$L = 12.46 \frac{\text{SPM}}{\text{T}}$$

Harvest Harvest

Equipment Leaks Emissions Calculations

Unit Number: F-1

Description: Valves, Connectors, Seals & Open-Ended Lines

Steady-State Emission Rates

	Number of	Emission	Emission	Uncontro	olled TOC
Equipment	Components,	Factors,	Factors,	Emissio	n Rates,
	# of sources	kg/hr/source	lb/hr/source	pph	tpy
Valves	1368	0.0045	0.0099	13.54	59.32
Connectors	1523	0.0002	0.0004	0.67	2.94
Pump Seals	12	0.0024	0.0053	0.06	0.28
Compressor Seals	92	0.0088	0.0194	1.78	7.80
Pressure Relief Valves	127	0.0088	0.0194	2.46	10.77
Open-Ended Lines	367	0.0020	0.0044	1.61	7.07
Тс	otal			20.13	88.18

Number of components based on the numbers of compressors and dehydrators at the station (see next page) Emission factors taken from the EPA "1995 Protocol for Equipment Leak Emission Estimates"

Emission factors (lb/hr/source) = Emission factors (kg/hr/source) x 2.2 lb/kg

Uncontrolled TOC Emission Rates (pph) = lb/hr/source x # of sources

Uncontrolled TOC Emission Rates (tpy) = Uncontrolled TOC Emission Rates (pph) x 8,760 hr/yr / 2,000 lb/ton

	Mala	Malandar	0	Weight		
Componento	Mole	Molecular	Component	Percent	Lincontrolled F	mission Rates,
Components	Percents,	Weights,	Weights,	of TOC,		· · · · · · · · · · · · · · · · · · ·
O and a second second second	%	lb/lb-mole	lb/lb-mole	%	pph	tpy
Carbon dioxide	6.9673	44.010				
Hydrogen sulfide	0.0000	34.070				
Nitrogen	0.0353	28.013				
Methane	92.1867	16.043	1478.951	98.234		
Ethane	0.7106	30.070	21.368	1.419		
Propane	0.0677	44.097	2.985	0.198	3.99E-02	1.75E-01
Isobutane	0.0106	58.123	0.616	0.041	8.24E-03	3.61E-02
n-Butane	0.0097	58.123	0.564	0.037	7.54E-03	3.30E-02
Isopentane	0.0031	72.150	0.224	0.015	2.99E-03	1.31E-02
n-Pentane	0.0020	72.150	0.144	0.010	1.93E-03	8.45E-03
Cyclopentane	0.0002	70.134	0.014	0.001	1.88E-04	8.22E-04
n-Hexane	0.0010	86.177	0.086	0.006	1.15E-03	5.05E-03
Cyclohexane	0.0006	84.161	0.050	0.003	6.75E-04	2.96E-03
Other hexanes	0.0020	86.177	0.172	0.011	2.30E-03	1.01E-02
Heptanes	0.0007	100.204	0.070	0.005	9.38E-04	4.11E-03
Methylcyclohexane	0.0010	98.188	0.098	0.007	1.31E-03	5.75E-03
2,2,4-Trimethylpentane	0.0000	114.231	0.000	0.000	0.00E+00	0.00E+00
Benzene	0.0000	78.114	0.000	0.000	0.00E+00	0.00E+00
Toluene	0.0004	92.141	0.037	0.002	4.93E-04	2.16E-03
Ethylbenzene	0.0000	106.167	0.000	0.000	0.00E+00	0.00E+00
Xylenes	0.0003	106.167	0.032	0.002	4.26E-04	1.87E-03
C8+ Heavies	0.0011	114.231	0.126	0.008	1.68E-03	7.36E-03
Total	100.0003		1505.538			
Total VOC				0.347	0.070	0.306

Gas stream composition obtained from the 32-7 #1 CDP extended gas analysis dated June 22, 2021.

Component Weights (lb/lb-mole) = (% / 100) * Molecular Weights (lb/lb-mole)

Weight Percent of TOC (%) = 100 x Component Weights (lb/lb-mole) / Total Component Weight (lb/lb-mole)

Uncontrolled Emission Rates (pph) = Total Uncontrolled TOC Emission Rate (pph) x (% / 100)

Uncontrolled Emission Rates (tpy) = Total Uncontrolled TOC Emission Rate (tpy) x (% / 100)

Equipment Leaks Emissions Calculations

Unit Number: F-1 Description: Valves, Connectors, Seals & Lines

Number of Compression Units at the Facility: Number of Dehydrators at the Facility:

17	
6	

			Equipm	ent Count			Instrument Count		
					Pressure				
Process Equipment Description			Pump	Compressor	Relief				
	Valves	Connectors	Seals	Seals	Valves	Open-end	Flow	Level	Pressure
Station inlet, meter run to pulsation dampener	17	14	0	0	1	13	3	0	3
Pulsation dampener	12	8	0	0	0	2	0	4	1
Compressor suction header	7	4	0	0	0	3	0	0	1
Suction header feed to instrument gas header	3	1	0	0	0	1	0	0	0
Compressor discharge header and bypass to station discharge	6	5	0	0	0	3	0	1	1
Compressor discharge header and suction header bypass lines	4	2	0	0	0	2	0	0	1
Fuel gas header	2	2	0	0	1	2	0	0	1
Instrument gas header	2	2	0	0	1	2	0	0	0
Station discharge header	9	5	0	0	1	6	0	0	2
Fuel gas recovery header	2	2	0	0	1	2	0	0	0
Fuel gas feed and filter loop	15	9	0	0	0	1	0	4	1
Instrument gas feed and filter loop	9	11	0	0	0	3	0	0	0
Produced water storage tank	1	0	0	0	0	1	0	1	0
ESD panel	12	0	0	0	0	0	0	0	0
Starting gas header	6	2	0	0	1	3	0	0	0
Hot gas header	2	2	0	0	0	2	0	0	0
Volume bottle lop	12	4	0	24	1	2	0	0	1
Components from Compressors	748	1003	0	68	102	187	0	68	153
Components from dehydrators	36	60	12	0	18	36	0	18	24
Total	905	1136	12	92	127	271	3	96	189
Adjusted Total	1368	1523	12	92	127	367			

The following additions are included in the Adjusted Total:

1 valve is added for each open end line

2 connectors are added for each flow meter

2 valves, 2 connectors and 1 open end line are added for each level gauge

1 connector is added for each pressure gauge

The component count is based on an evaluation of the Sim Mesa Compressor Station (two stage compression)

Pig Receiver Emissions Calculations

Unit Number: PR1 Description: Pig Receiver

Pipe Volume

Outside	Wall	Pipe	Pipe
Diameter,	Thickness,	Length,	Volume,
in	in	ft	ft^3
20	0.375	9	18.190

Pipe Volume

3.1416 x (((Outside Diameter - (2 x Wall Thickness)) / 12 / 2) ^2) x Pipeline Length

Blowdown Volume (Per Event)

Blowdown	Atmospheric	Blowdown	Number of	Purge	Purge	Total
Pressure,	Pressure,	Gas Loss,	Purges,	Pressure,	Gas Loss,	Gas Loss,
psig	psi	scf	#	psig	mscf	scf
120	11.97	163	2	30	104	267.2

Blowdown Gas Loss

Pipe Volume x ((Blowdown Pressure + Atmospheric Pressure) / 14.7)

Purge Gas Loss

Number of Purges x Pipe Volume x ((Purge Pressure + Atmospheric Pressure) / 14.7)

Throughput

26	events/yr	
267	scf/event	
6,946	scf/yr	

Blowdowns per year Gas loss per blowdown Annual gas loss Harvest Four Corners LLC Calculated (see table above) events/yr x scf/event

Emission Rates

		Uncontrolled,
	Emission	Emission
Pollutants	Factors,	Rates,
	lb/scf	tpy
VOC	1.506E-04	5.23E-04
Benzene	2.059E-07	7.15E-07
Ethylbenzene	0.000E+00	0.00E+00
n-Hexane	1.136E-06	3.94E-06
Isooctane	0.000E+00	0.00E+00
Toluene	7.286E-07	2.53E-06
Xylene	5.597E-07	1.94E-06

Emission factors calculated from gas composition (see table below) Uncontrolled Emission Rates (tpy) = scf/yr x lb/scf / 2,000 lb/ton

Gas Composition

	Mole	Molecular	Emission
Components	Percents,	Weights,	Factors,
	%	lb/lb-mole	lb/scf
Carbon dioxide	6.6351	44.01	7.697E-03
Hydrogen sulfide	0.0000	34.07	0.000E+00
Nitrogen	0.0998	28.01	7.368E-05
Methane	92.3408	16.04	3.904E-02
Ethane	0.8094	30.07	6.415E-04
Propane	0.0877	44.09	1.019E-04
Isobutane	0.0082	58.12	1.256E-05
n-Butane	0.0095	58.12	1.455E-05
Isopentane	0.0041	72.15	7.797E-06
n-Pentane	0.0012	72.15	2.282E-06
Cyclopentane	0.0001	70.14	1.849E-07
n-Hexane	0.0005	86.17	1.136E-06
Cyclohexane	0.0002	84.16	4.436E-07
Other hexanes	0.0011	86.18	2.499E-06
Heptanes	0.0004	100.20	1.056E-06
Methylcyclohexane	0.0008	98.19	2.070E-06
Isooctane	0.0000	100.21	0.000E+00
Benzene	0.0001	78.11	2.059E-07
Toluene	0.0003	92.14	7.286E-07
Ethylbenzene	0.0000	106.17	0.000E+00
Xylenes	0.0002	106.17	5.597E-07
C8+ Heavies	0.0009	110.00	2.609E-06
Total	100.0004		
Total VOC			1.506E-04

Gas stream composition obtained from the 32-7 #1 CDP extended gas analysis dated 06/072022. Emission Factors (lb/scf) = (% / 100) x lb/lb-mole / 379.4 scf/lb-mole This page is intentionally left blank.

Section 6.a

Green House Gas Emissions

(Submitting under 20.2.70, 20.2.72 20.2.74 NMAC)

Title V (20.2.70 NMAC), Minor NSR (20.2.72 NMAC), and PSD (20.2.74 NMAC) applicants must estimate and report greenhouse gas (GHG) emissions to verify the emission rates reported in the public notice, determine applicability to 40 CFR 60 Subparts, and to evaluate Prevention of Significant Deterioration (PSD) applicability. GHG emissions that are subject to air permit regulations consist of the sum of an aggregate group of these six greenhouse gases: carbon dioxide (CO₂), nitrous oxide (N₂O), methane (CH₄), hydrofluorocarbons (HFCs), perfluorocarbons (PFCs), and sulfur hexafluoride (SF₆).

Calculating GHG Emissions:

1. Calculate the ton per year (tpy) GHG mass emissions and GHG CO₂e emissions from your facility.

2. GHG mass emissions are the sum of the total annual tons of greenhouse gases without adjusting with the global warming potentials (GWPs). GHG CO₂e emissions are the sum of the mass emissions of each individual GHG multiplied by its GWP found in Table A-1 in 40 CFR 98 <u>Mandatory Greenhouse Gas Reporting</u>.

3. Emissions from routine or predictable start up, shut down, and maintenance must be included.

4. Report GHG mass and GHG CO₂e emissions in Table 2-P of this application. Emissions are reported in <u>short</u> tons per year and represent each emission unit's Potential to Emit (PTE).

5. All Title V major sources, PSD major sources, and all power plants, whether major or not, must calculate and report GHG mass and CO2e emissions for each unit in Table 2-P.

6. For minor source facilities that are not power plants, are not Title V, and are not PSD there are three options for reporting GHGs in Table 2-P: 1) report GHGs for each individual piece of equipment; 2) report all GHGs from a group of unit types, for example report all combustion source GHGs as a single unit and all venting GHGs as a second separate unit; 3) or check the following \Box By checking this box, the applicant acknowledges the total CO2e emissions are less than 75,000 tons per year.

Sources for Calculating GHG Emissions:

- Manufacturer's Data
- AP-42 Compilation of Air Pollutant Emission Factors at http://www.epa.gov/ttn/chief/ap42/index.html
- EPA's Internet emission factor database WebFIRE at http://cfpub.epa.gov/webfire/

• 40 CFR 98 <u>Mandatory Green House Gas Reporting</u> except that tons should be reported in short tons rather than in metric tons for the purpose of PSD applicability.

• API Compendium of Greenhouse Gas Emissions Methodologies for the Oil and Natural Gas Industry. August 2009 or most recent version.

• Sources listed on EPA's NSR Resources for Estimating GHG Emissions at http://www.epa.gov/nsr/clean-air-act-permitting-greenhouse-gases:

Global Warming Potentials (GWP):

Applicants must use the Global Warming Potentials codified in Table A-1 of the most recent version of 40 CFR 98 Mandatory Greenhouse Gas Reporting. The GWP for a particular GHG is the ratio of heat trapped by one unit mass of the GHG to that of one unit mass of CO_2 over a specified time period.

"Greenhouse gas" for the purpose of air permit regulations is defined as the aggregate group of the following six gases: carbon dioxide, nitrous oxide, methane, hydrofluorocarbons, perfluorocarbons, and sulfur hexafluoride. (20.2.70.7 NMAC, 20.2.74.7 NMAC). You may also find GHGs defined in 40 CFR 86.1818-12(a).

Metric to Short Ton Conversion:

Short tons for GHGs and other regulated pollutants are the standard unit of measure for PSD and title V permitting programs. 40 CFR 98 <u>Mandatory Greenhouse Reporting</u> requires metric tons.

1 metric ton = 1.10231 short tons (per Table A-2 to Subpart A of Part 98 – Units of Measure Conversions)

CO₂, CH₄, and N₂O exhaust emissions were calculated using emission factors from 40 Code of Federal Regulations (CFR), Part C, Tables C-1 & C-2 and the combustion source higher heating value (HHV) design heat rates.

CO₂ and CH₄ emissions from SSM blowdown events were calculated from the annual blowdown volumes and gas composition.

The reciprocating and centrifugal compressor CO_2 and CH_4 emissions were calculated using a combination of equations W-26 & W-36 (from Subpart W).

Dehydrator CO₂ and CH₄ emissions were calculated using GRI-GLYCalc.

CO₂ and CH₄ equipment leak emissions were calculated using the TOC emission factors and gas stream composition. CH₄ gas-driven pneumatic device emissions and non-routine emissions were calculated from the facility CH₄ gas stream composition using the emission factors and baseline CH4 content from the API Compendium, Section 5.6.1, Table 5-15. CO₂ gas-driven pneumatic device emissions and non-routine emissions were calculated from the CH₄ emissions and facility CO₂ gas stream composition.

There are no GHG emissions associated with the truck loading operations.

	Facility Total Emissions						
Sources	CO2,	CH4,	N2O,	GHG,	CO2e,		
	tpy	tpy	tpy	tpy	tpy		
Engine & Turbine Exhaust Emissions	102,177.70	1.93E+00	1.93E-01	102,179.82	102283.23		
SSM Emissions	325.35	1,650.27		1,975.62	41582.03		
Reciprocating Compressor Venting Emissions	210.98	1,018.96		1,229.94	25685.04		
Dehydrator Emissions	423.46	901.55		1,325.01	22962.30		
Reboiler Exhaust Emissions	4,605.67	8.68E-02	8.68E-03	4,605.76	4610.42		
Equipment Leak Emissions	8.04	38.85		46.89	979.28		
Natural Gas Pneumatic Device Venting Emissions	42.93	206.85		249.78	5214.07		
Natural Gas Driven Pneumatic Pump Venting Emissions	0.47	2.27		2.74	57.18		
Storage Tank Emissions	0.00	0.00		0.00	0.00		
Total	107,794.60	3,820.76	2.01E-01	111,615.6	203,373.6		

Engine & Turbine Exhaust Emissions

Unit		E	Emission Factor	ſS		Emission Rates	6
Numbers	Description	CO2,	N2O,	CH4,	CO2,	N2O,	CH4,
		kg/MMBtu	kg/MMBtu	kg/MMBtu	tpy	tpy	tpy
1	7042GL engine	53.06	1.00E-04	1.00E-03	6,010.45	1.13E-02	0.11
2	7042GL engine	53.06	1.00E-04	1.00E-03	6,010.45	1.13E-02	0.11
3	7042GL engine	53.06	1.00E-04	1.00E-03	6,010.45	1.13E-02	0.11
4	7042GL engine	53.06	1.00E-04	1.00E-03	6,010.45	1.13E-02	0.11
5	7042GL engine	53.06	1.00E-04	1.00E-03	6,010.45	1.13E-02	0.11
6	7042GL engine	53.06	1.00E-04	1.00E-03	6,010.45	1.13E-02	0.11
7	7042GL engine	53.06	1.00E-04	1.00E-03	6,010.45	1.13E-02	0.11
8	7042GL engine	53.06	1.00E-04	1.00E-03	6,010.45	1.13E-02	0.11
13	7042GL engine	53.06	1.00E-04	1.00E-03	6,010.45	1.13E-02	0.11
15	7042GL engine	53.06	1.00E-04	1.00E-03	6,010.45	1.13E-02	0.11
16	7042GL engine	53.06	1.00E-04	1.00E-03	6,010.45	1.13E-02	0.11
18	7042GL engine	53.06	1.00E-04	1.00E-03	6,010.45	1.13E-02	0.11
19	7042GL engine	53.06	1.00E-04	1.00E-03	6,010.45	1.13E-02	0.11
20	7042GL engine	53.06	1.00E-04	1.00E-03	6,010.45	1.13E-02	0.11
21	7042GL engine	53.06	1.00E-04	1.00E-03	6,010.45	1.13E-02	0.11
22	7042GL engine	53.06	1.00E-04	1.00E-03	6,010.45	1.13E-02	0.11
23	7042GL engine	53.06	1.00E-04	1.00E-03	6,010.45	1.13E-02	0.11
	Total				102,177.70	1.93E-01	1.93

The emissions factors are taken from 40 CFR 98, Subpart C, Tables C-1 & C-2 Emission Rates (tpy) = kg/MMBtu x 2.2 lb/kg x MMBtu/yr / 2,000 lb/ton

				LHV	H	HV
Unit			Operating	Design	Design	Fuel
Numbers	Description	Fuel Types	Times,	Heat Rates,	Heat Rates,	Usages,
			hr/yr	MMBtu/hr	MMBtu/hr	MMBtu/yr
1	7042GL engine	Nat. Gas	8,760	10.58	11.76	102,979
2	7042GL engine	Nat. Gas	8,760	10.58	11.76	102,979
3	7042GL engine	Nat. Gas	8,760	10.58	11.76	102,979
4	7042GL engine	Nat. Gas	8,760	10.58	11.76	102,979
5	7042GL engine	Nat. Gas	8,760	10.58	11.76	102,979
6	7042GL engine	Nat. Gas	8,760	10.58	11.76	102,979
7	7042GL engine	Nat. Gas	8,760	10.58	11.76	102,979
8	7042GL engine	Nat. Gas	8,760	10.58	11.76	102,979
13	7042GL engine	Nat. Gas	8,760	10.58	11.76	102,979
15	7042GL engine	Nat. Gas	8,760	10.58	11.76	102,979
16	7042GL engine	Nat. Gas	8,760	10.58	11.76	102,979
18	7042GL engine	Nat. Gas	8,760	10.58	11.76	102,979
19	7042GL engine	Nat. Gas	8,760	10.58	11.76	102,979
20	7042GL engine	Nat. Gas	8,760	10.58	11.76	102,979
21	7042GL engine	Nat. Gas	8,760	10.58	11.76	102,979
22	7042GL engine	Nat. Gas	8,760	10.58	11.76	102,979
23	7042GL engine	Nat. Gas	8,760	10.58	11.76	102,979

The fuel types and operating times are provided by Williams

The LHV design heat rates are taken from manufacturers data

HHV Design Heat Rates (MMBtu/hr) = LHV Design Heat Rates (MMBtu/hr) / 0.9 LHV/HHV

HHV Fuel Usages (MMBtu/yr) = HHV Design Heat Rates (MMBtu/hr) x hr/yr

SSM Emissions

Unit		Total	CO2 Emission	CH4 Emission	Emission Rates		
Numbers	Description	Gas Losses,	Factors,	Factors,	CO2,	N2O,	CH4,
		scf/yr	lb/scf	lb/scf	tpy	tpy	tpy
SSM (1)	SSM (Eng) (1)	71,468,487	0.0077	0.0390	275.03	-	1,395.04
SSM (2)	SSM (Eng) (2)	10,884,847	0.0077	0.0390	41.89	-	212.47
SSM (3)	SSM (Eng) (3)	2,183,875	0.0077	0.0390	8.40	-	42.63
PR1	Pig Receiver	6,946	0.0077	0.0390	0.03	-	0.14
	Total				325.35	-	1650.27

The annual blowdown volumes are calculated from data provided by Williams

The CO2 and CH4 emission factors are calculated from the facility extended gas analysis Emission Rates (tpy) = scf/yr x lb/scf / 2,000 lb/ton

Reciprocating Compressor Venting Emissions

Unit			Emission Rates	6
Numbers	Description	CO2,	N2O,	CH4,
		tpy	tpy	tpy
NA	Blowdown Valve Leakage	20.15	-	97.33
NA	Rod Packing Emissions	190.83	-	921.63
NA	Isolation Valve Leakage	0.00	-	0.00
	Total	210.98	-	1018.96

Operating or standby mode - includes blowdown valve leakage through blowdown vent stack

Operating mode - includes rod packing emissions

Non-operating depressurized mode - includes isolation valve leakage through open blowdown vents (without blind flanges)

Rod packing gas emissions assume 4 cylinders per compressor

A combination of equations W-26 & W-36 (Subpart W) is used to calculate reciprocating compressor emissions

As the NMED requires CO2 & CH4 emissions rather than CO2e emissions, it is not necessary to include the global warming potential from equation W-36

CO2 Emission Rates (tpy) = # x scf/hr x hr/yr x (CO2 Mole Percent (%) / 100) x CO2 Density (kg/scf) x (2,204.6 lb/tonne / 2,000 lb/ton) / 1,000 kg/tonne

CH4 Emission Rates (tpy) = # x scf/hr x hr/yr x (CH4 Mole Percent (%) / 100) x CH4 Density (kg/scf)

x (2,204.6 lb/tonne / 2,000 lb/ton) / 1,000 kg/tonne

Unit		Number of	Gas	Operating	CO2 Mole	CH4 Mole	CO2	CH4
Numbers	Description	Compressors	Emissions,	Times,	Percents,	Percents,	Density,	Density,
		#	scf/hr	hr/yr	%	%	kg/scf	kg/scf
NA	Blowdown Valve Leakage	17	33.5	8,760	6.97	92.19	0.0526	0.0192
NA	Rod Packing Emissions	17	317.2	8,760	6.97	92.19	0.0526	0.0192
NA	Blowdown Valve Leakage (Stand	17	10.5	0	6.97	92.19	0.0526	0.0192

The number of compressors are provided by Williams

Blowdown valve leakage (33.5 scf/hr) and rod packing emissions occur in operating mode

Blowdown valve leakage (10.5 scf/hr) occurs in standby pressurized mode

Emission factors are the three year rolling average (2012-2014) of all measurements in the Williams Field Services, LLC compressor fleet located at natural gas processing plants

The operating times (the average operating times for all station compressors combined) are provided by Williams

The facility CO2 and CH4 contents are taken from the facility extended gas analysis

The CO2 & CH4 densities (kg/scf) are taken from Subpart W, Paragraph 98.233(v)

Dehydrator Emissions

Unit				Emission Rates	S
Numbers	Description		CO2,	N2O,	CH4,
			tpy	tpy	tpy
9a	Dehydrator (12 mmscfd)		70.43	-	148.83
10a	Dehydrator (12 mmscfd)		70.43	-	148.83
11a	Dehydrator (20 mmscfd)		70.65	-	150.98
12a	Dehydrator (20 mmscfd)		70.65	-	150.98
24a	Dehydrator (20 mmscfd)		70.65	-	150.98
25a	Dehydrator (20 mmscfd)		70.65	-	150.98
		Total	423.46	-	901.55

The emission rates are taken from the GRI-GLYCalc output file

Reboiler Exhaust Emissions

Unit		E	Emission Factor	ſS		Emission Rate	S
Numbers	Description	CO2,	N2O,	CH4,	CO2,	N2O,	CH4,
		kg/MMBtu	kg/MMBtu	kg/MMBtu	tpy	tpy	tpy
9b	Reboiler (1208 scfh)	53.06	1.00E-04	1.00E-03	617.63	1.16E-03	1.16E-02
10b	Reboiler (1208 scfh)	53.06	1.00E-04	1.00E-03	617.63	1.16E-03	1.16E-02
11b	Reboiler (1648 scfh)	53.06	1.00E-04	1.00E-03	842.60	1.59E-03	1.59E-02
12b	Reboiler (1648 scfh)	53.06	1.00E-04	1.00E-03	842.60	1.59E-03	1.59E-02
24b	Reboiler (1648 scfh)	53.06	1.00E-04	1.00E-03	842.60	1.59E-03	1.59E-02
25b	Reboiler (1648 scfh)	53.06	1.00E-04	1.00E-03	842.60	1.59E-03	1.59E-02
	Total				4,605.67	8.68E-03	8.68E-02

The emissions factors are taken from 40 CFR 98, Subpart C, Tables C-1 & C-2 Emission Rates (tpy) = kg/MMBtu x 2.2 lb/kg x MMBtu/yr / 2,000 lb/ton

					LHV		H	HV
Unit			Operating	Fuel	Fuel Heat	Fuel	Fuel	Fuel
Numbers	Description	Fuel Types	Times	Usages,	Contents,	Usages,	Usages,	Usages,
			hr/yr	scf/hr	Btu/scf	MMBtu/hr	MMBtu/hr	MMBtu/yr
9b	Reboiler (1208 scfh)	Nat. Gas	8,760	1,208	900	1.09	1.21	10,582
10b	Reboiler (1208 scfh)	Nat. Gas	8,760	1,208	900	1.09	1.21	10,582
11b	Reboiler (1648 scfh)	Nat. Gas	8,760	1,648	900	1.48	1.65	14,436
12b	Reboiler (1648 scfh)	Nat. Gas	8,760	1,648	900	1.48	1.65	14,436
24b	Reboiler (1648 scfh)	Nat. Gas	8,760	1,648	900	1.48	1.65	14,436
25b	Reboiler (1648 scfh)	Nat. Gas	8,760	1,648	900	1.48	1.65	14,436

The fuel types and operating times are provided by Williams

The LHV fuel usages (scf/hr) are taken from manufacturer's data

The LHV fuel heat contents are estimated based on the value typically used by manufacturers

LHV Fuel Usages (MMBtu/hr) = LHV Fuel Usages (scf/hr) x Btu/scf / 1,000,000 Btu/MMBtu

HHV Fuel Usages (MMBtu/hr) = LHV Fuel Usages (MMBtu/hr) / 0.9 LHV/HHV

HHV Fuel Usages (MMBtu/yr) = HHV Fuel Usages (MMBtu/hr) x hr/yr

Equipment Leaks Emissions

Unit				Emission Rates	6
Numbers	Description		CO2,	N2O,	CH4,
			tpy	tpy	tpy
NA	Valves		5.9	-	28.3
NA	Connectors		0.9	-	4.4
NA	Open-Ended Lines		0.4	-	1.9
NA	Pressure Relief Valves		0.9	-	4.2
		Total	8.04	-	38.85

A combination of equations W-31 & W-36 (Subpart W) is used to calculate uncombusted CO2 & CH4 emissions

As the NMED requires CO2 & CH4 emissions rather than CO2e emissions, it is not necessary to include the global warming potential from equation W-36

CO2 Emission Rate (tpy) = # x scf/hr/component x (CO2 Content (mole %) / 100) x hr/yr x CO2 Density (kg/scf) x (2,204.6 lb/tonne / 2,000 lb/ton) / 1,000 kg/tonne

CH4 Emission Rate (tpy) = # x scf/hr/component x (CH4 Content (mole %) / 100) x hr/yr x CH4 Density (kg/scf)

x (2,204.6 lb/tonne / 2,000 lb/ton) / 1,000 kg/tonne

			Emission					
Unit		Number of	Factors,	CO2	CH4	Operating	CO2	CH4
Numbers	Description	Components,	scf/hr	Contents,	Contents,	Times,	Density,	Density,
		#	/component	mole %	mole %	hr/yr	kg/scf	kg/scf
NA	Valves	1368	0.121	6.97	92.19	8,760	0.0526	0.0192
NA	Connectors	1523	0.017	6.97	92.19	8,760	0.0526	0.0192
NA	Open-Ended Lines	367	0.031	6.97	92.19	8,760	0.0526	0.0192
	Pressure Relief Valves	127	0.193	6.97	92.19	8,760	0.0526	0.0192

The number of sources are calculated based on the number of compressors and dehydrators at the station (see criteria pollutant and HAP equipment leaks calculations)

The emission factors are taken from Subpart W, Table W-1A (Western U.S. - Gas Service)

The facility CO2 and CH4 contents are taken from the facility extended gas analysis

The operating times are provided by Williams (default is the entire year)

The CO2 & CH4 densities are taken from Subpart W, Paragraph 98.233(v)

Natural Gas Pneumatic Device Venting Emissions

Unit		Number	Emission	Operating		Emission Rates	Rates	
Numbers	Description	of Devices,	Factors,	Times,	CO2,	N2O,	CH4,	
		#	scf/hr/device	hr/yr	tpy	tpy	tpy	
NA	Continuous High Bleed Pneumatic Devices	2	37.3	8,760	2.64	-	12.72	
NA	Intermittent Bleed Pneumatic Devices	84	13.5	8,760	40.15	-	193.41	
NA	Continuous Low Bleed Pneumatic Devices	3	1.39	8,760	0.15	-	0.71	
	Total				42.93	-	206.85	

The number of devices are provided by Williams

The emission factors are taken from Subpart W, Table W-1A (Western U.S. - Gas Service)

The operating times are provided by Williams Equation W-1 (Subpart W) is used to calculate CO2 & CH4 emissions

Equation vv-1 (Subpart w) is used to calculate CO2 & CH4 emissions

As the NMED requires CO2 & CH4 emissions in addition to CO2e emissions, it is necessary to divide by the global warming potentials CO2 Emission Rates (tpy) = # x scf/hr/device x (CO2 Content (mole %) / 100) x CO2 Conversion Factors (tonne CO2e/scf) x hr/yr

x (2,204.6 lb/tonne / 2,000 lb/ton) / CO2 Global Warming Potentials (tonne CO2e/tonne CO2)

CH4 Emission Rates (tpy) = # x scf/hr/device x (CH4 Contents (mole %) / 100) x CH4 Conversion Factors (tonne CO2e/scf) x hr/yr x (2,204.6 lb/tonne / 2,000 lb/ton) / CH4 Global Warming Potentials (tonne CO2e/tonne CH4)

				CO2	CH4	CO2 Global	CH4 Global
				Conversion	Conversion	Warming	Warming
Unit		CO2	CH4	Factors,	Factors,	Potentials,	Potentials,
Numbers	Description	Contents,	Contents,	tonne CO2e	tonne CO2e	tonne CO2e	tonne CO2e
		mole %	mole %	/scf	/scf	/tonne CO2	/tonne CH4
NA	Continuous High Bleed Pneumatic Devices	6.97	92.19	5.262E-05	4.790E-04	1	25
NA	Continuous Low Bleed Pneumatic Devices	6.97	92.19	5.262E-05	4.790E-04	1	25
NA	Intermittent Bleed Pneumatic Devices	6.97	92.19	5.262E-05	4.790E-04	1	25

The facility CO2 and CH4 contents are taken from the facility extended gas analysis

The conversion factors are taken from Subpart W, Paragraph 98.233(a)

The global warming potentials are taken from 40 CFR Part 98, Table A-1

Natural Gas Driven Pneumatic Pump Venting Emissions

Emission Rates

Unit		Number	Emission	Operating	Emission Rates		
Number	Description	of Pumps,	Factor,	Time,	CO2,	N2O,	CH4,
		#	scf/hr/pump	hr/yr	tpy	tpy	tpy
NA	Pneumatic Pump Venting	1	13.3	8,760	0.47	-	2.27

The number of pumps are provided by Williams

The emission factor is taken from Subpart W, Table W-1A (Western U.S. - Gas Service)

The operating time is provided by Williams (default is the entire year)

Equation W-2 (Subpart W) is used to calculate CO2 & CH4 emissions

As the NMED requires CO2 & CH4 emissions in addition to CO2e emissions, it is necessary to divide by the global warming potentials CO2 Emission Rate (tpy) = $\# x \operatorname{scf/hr/pump} x (CO2 \operatorname{Content} (mole \%) / 100) x \operatorname{CO2} \operatorname{Conversion} \operatorname{Factor} (tonne \operatorname{CO2e/scf}) x \operatorname{hr/yr}$

x (2,204.6 lb/tonne / 2,000 lb/ton) / CO2 Global Warming Potentials (tonne CO2e/tonne CO2)

CH4 Emission Rate (tpy) = # x scf/hr/pump x (CH4 Content (mole %) / 100) x CH4 Conversion Factor (tonne CO2e/scf) x hr/yr x (2,204.6 lb/tonne / 2,000 lb/ton) / CH4 Global Warming Potentials (tonne CO2e/tonne CH4)

				CO2	CH4	CO2 Global	CH4 Global
				Conversion	Conversion	Warming	Warming
Unit		CO2	CH4	Factor,	Factor,	Potential,	Potential,
Number	Description	Content,	Content,	tonne CO2e	tonne CO2e	tonne CO2e	tonne CO2e
		mole %	mole %	/scf	/scf	/tonne CO2	/tonne CH4
NA	Pneumatic Pump Venting	6.97	92.19	5.262E-05	4.790E-04	1	25

The facility CO2 and CH4 contents are taken from the facility extended gas analysis

The conversion factors are taken from Subpart W, Paragraph 98.233(a)

The operating time is provided by Williams (the default is the entire year)

The global warming potentials are taken from 40 CFR Part 98, Table A-1

Storage Tank Emissions

Unit			Emission Rates	6
Number	Description	CO2,	N2O,	CH4,
		tpy	tpy	tpy
	Storage Tanks (all)	0.00	-	0.00
	Storage Tank			
	Storage Tank			
	Storage Tank			
	Tota	0.00	-	0.00

The emission rates are taken from HYSYS output files, as applicable

Gas Stream Composition

				Weight	
	Mole	Molecular	Component	Percent	Emission
Components	Percents,	Weights,	Weights,	of Total,	Factors,
	%	lb/lb-mole	lb/lb-mole	%	lb/scf
Carbon Dioxide	6.9673	44.01	3.07	16.9141	0.0081
Hydrogen Sulfide	0.0000	34.07	0.00	0.0000	0.0000
Nitrogen	0.0353	28.01	0.01	0.0545	0.0000
Methane	92.1867	16.04	14.79	81.5651	0.0390
Ethane	0.7106	30.07	0.21	1.1787	0.0006
Propane	0.0677	44.09	0.03	0.1646	0.0001
IsoButane	0.0106	58.12	0.01	0.0340	0.0000
Normal Butane	0.0097	58.12	0.01	0.0311	0.0000
IsoPentane	0.0031	72.15	0.00	0.0123	0.0000
Normal Pentane	0.0020	72.15	0.00	0.0080	0.0000
Cyclopentane	0.0002	70.14	0.00	0.0008	0.0000
n-Hexane	0.0010	86.17	0.00	0.0048	0.0000
Cyclohexane	0.0006	84.16	0.00	0.0028	0.0000
Other Hexanes	0.0020	86.18	0.00	0.0095	0.0000
Heptanes	0.0007	100.20	0.00	0.0039	0.0000
Methylcyclohexane	0.0010	98.19	0.00	0.0054	0.0000
2,2,4-Trimethylpentane	0.0000	100.21	0.00	0.0000	0.0000
Benzene	0.0000	78.11	0.00	0.0000	0.0000
Toluene	0.0004	92.14	0.00	0.0020	0.0000
Ethylbenzene	0.0000	106.17	0.00	0.0000	0.0000
Xylenes	0.0003	106.17	0.00	0.0018	0.0000
C8+ heavies	0.0011	110.00	0.00	0.0067	0.0000
Total	100.0003		18.13	100.0000	0.0478
VOC			0.05		0.0001

Gas stream composition obtained from the 32-7 #1 CDP extended gas analysis dated June 22, 2021.

Component Weights (lb/lb-mole) = [Mole Percents (%) / 100] x Molecular Weights (lb/lb-mole)

Weight Percent of Total (%) = 100 x Component Weights (lb/lb-mole) / Total Component Weight (lb/lb-mole) Emission Factors (lb/scf) = [Mole Percents (%) / 100] x Molecular Weights (lb/lb-mole) / 379.4 scf/lb-mole

Gas Composition - SSM & PR1

	Mole	Molecular	Emission
Components	Percents,	Weights,	Factors,
	%	lb/lb-mole	lb/scf
Carbon dioxide	6.6351	44.01	7.697E-03
Hydrogen sulfide	0.0000	34.07	0.000E+00
Nitrogen	0.0998	28.01	7.368E-05
Methane	92.3408	16.04	3.904E-02
Ethane	0.8094	30.07	6.415E-04
Propane	0.0877	44.09	1.019E-04
Isobutane	0.0082	58.12	1.256E-05
n-Butane	0.0095	58.12	1.455E-05
Isopentane	0.0041	72.15	7.797E-06
n-Pentane	0.0012	72.15	2.282E-06
Cyclopentane	0.0001	70.14	1.849E-07
n-Hexane	0.0005	86.17	1.136E-06
Cyclohexane	0.0002	84.16	4.436E-07
Other hexanes	0.0011	86.18	2.499E-06
Heptanes	0.0004	100.2	1.056E-06
Methylcyclohexane	0.0008	98.19	2.070E-06
2,2,4-Trimethylpentane	0.0000	100.21	0.000E+00
Benzene	0.0001	78.11	2.059E-07
Toluene	0.0003	92.14	7.286E-07
Ethylbenzene	0.0000	106.17	0.000E+00
Xylenes	0.0002	106.17	5.597E-07
C8+ Heavies	0.0009	110	2.609E-06
Total	100.0004		
Total VOC			1.506E-04

Gas stream composition obtained from the 32-7 #1 CDP extended gas analysis dated 06/072022. Emission Factors (lb/scf) = (% / 100) x lb/lb-mole / 379.4 scf/lb-mole

Section 7

Information Used To Determine Emissions

Information Used to Determine Emissions shall include the following:

- If manufacturer data are used, include specifications for emissions units <u>and</u> control equipment, including control efficiencies specifications and sufficient engineering data for verification of control equipment operation, including design drawings, test reports, and design parameters that affect normal operation.
- □ If test data are used, include a copy of the complete test report. If the test data are for an emissions unit other than the one being permitted, the emission units must be identical. Test data may not be used if any difference in operating conditions of the unit being permitted and the unit represented in the test report significantly effect emission rates.
- ☑ If the most current copy of AP-42 is used, reference the section and date located at the bottom of the page. Include a copy of the page containing the emissions factors, and clearly mark the factors used in the calculations.
- \Box If an older version of AP-42 is used, include a complete copy of the section.
- **X** If an EPA document or other material is referenced, include a complete copy.
- **X** Fuel specifications sheet.
- If computer models are used to estimate emissions, include an input summary (if available) and a detailed report, and a disk containing the input file(s) used to run the model. For tank-flashing emissions, include a discussion of the method used to estimate tank-flashing emissions, relative thresholds (i.e., permit or major source (NSPS, PSD or Title V)), accuracy of the model, the input and output from simulation models and software, all calculations, documentation of any assumptions used, descriptions of sampling methods and conditions, copies of any lab sample analysis.

STANDARD EQUIPMENT

AIR CLEANER - Two, dry type with rain shield and service indicator.

BARRING DEVICE - Manual.

BEARINGS - Heavy duty, replaceable, precision type.

BREATHER - Closed system.

CONNECTING RODS - Drop forged steel, rifle drilled.

CONTROL SYSTEM - Pneumatic. Includes pilot operated valves for air start and prelube. Engine mounted control panel with two push button valves. Pilot operated air start valves omitted when starter is not furnished by Waukesha. Includes engine On/Off push button. One mounted on either side of the engine.

CRANKCASE - Integral crankcase and cylinder frame. Main bearing caps drilled and tapped for temperature sensors. Does not include sensors.

CRANKSHAFT - Counterweighted, forged steel, seven main bearings, and dynamically balanced.

CYLINDERS - Removable wet type cylinder liners, chrome plated on outer diameter. Induction hardened.

CYLINDER HEADS - Twelve interchangeable. Two hard faced intake and two hard faced exhaust valves per cylinder. Hard faced intake and exhaust valve seat inserts. Roller valve lifters and hydraulic push rods. Includes prechamber and related fuel control valves.

ENGINE ROTATION - Counterclockwise when facing flywheel.

ENGINE MONITORING DEVICES - Engine thermocouples. K-type, for jacket water temperature, lube oil temperature, intake manifold temperature, individual cylinder exhaust temperature and a common pre turbine temperatures, one on each bank. Magnetic pickup wired for customer supplied tachometer. Lube oil pressure and intake manifold pressure sensing lines are terminated in a common bulk head.

EXHAUST OUTLET - Single vertical at rear. Flexible stainless steel connection with 8" (203 mm) pipe flange.

FLYWHEEL - Approx. WR² = 155000 lb-in²; with ring gear (208 teeth), machined to accept two drive adapters: 31.88" (810 mm) pilot bore, 30.25" (768 mm) bolt circle, (12) 0.75"-10 tapped holes; or 28.88" (734 mm) pilot bore, 27.25" (692 mm) bolt circle, (12) 0.625"-11 tapped holes and (12) 0.75"-10 tapped holes.

FLYWHEEL HOUSING - No. 00 SAE.

FUEL SYSTEM - Dual natural gas, 4" (102 mm) duplex updraft carburetors. Two Fisher Model 99, 2" (51 mm) gas regulators,

30 - 50 psi (241 - 345 kPa) gas inlet pressure required. Prechamber fuel system and control logic. GOVERNOR - Woodward UG-8 LD hydraulic lever type, with friction type speed control. Mounted on right hand side.

IGNITION - Waukesha Custom Engine Control Ignition Module. Electronic digital ignition system. 24V DC power required.

INTERCOOLER - Air-to-water.

LEVELING BOLTS

LIFTING EYES

LUBRICATION - Full pressure, Gear type pump, Full flow filter, 36 gallon (136 litres) capacity, not mounted. Includes flexible connections. Includes lube oil strainer, mounted on engine. Air/gas motor driven prelube pump. Requires final piping.

MANIFOLDS - Exhaust, (2) water cooled.

OIL COOLER - With thermostatic temperature controller and pressure regulating valve. Not mounted.

OIL PAN - Base type. 90 gallon (340 litres) capacity including filter and cooler.

PAINT - Oilfield orange primer.

PISTONS – Aluminum with floating pin. 10.5:1 compression ratio. Oil cooled.

SHIPPING SKID - Steel for domestic truck or rail.

TURBOCHARGERS - Two, dry type. Wastegate controlled.

VIBRATION DAMPER - Two, viscous type. Guard included with remote mounted radiator or no radiator. WATER CIRCULATING SYSTEM

Auxiliary Circuit - For oil cooler and intercooler. Pump is belt driven from crankshaft pulley. Includes thermostatic valve.

Engine Jacket - Belt driven water circulating pump, cluster type thermostatic temperature regulating valve, full flow bypass type. Flange connections and mating flanges for (2) 4" (102 mm) inlets and (1) 5" (127 mm) outlet.

WAUKESHA CUSTOM ENGINE CONTROL, DETONATION SENSING MODULE (DSM) - Includes individual cylinder sensors, Detonation Sensing Module, filter and cables. Device is compatible with Waukesha CEC Ignition Module only. Sensors are mounted and wired to engine junction box. Detonation Sensing Module and filter are shipped loose. One 11 ft. cable provided for connection between engine junction box and filter. One each 15 ft. cable provided for connection between filter and DSM and Ignition Module and DSM. One 20 ft. cable provided for power and ground for filter. All cables are shipped loose. Packager is responsible for power supply and ground to the DSM. 24V DC power is required. The DSM meets Canadian Standards Association Class 1, Group D, Division 2, hazardous location requirements.



L7042GL

VHP[™] Series Gas Engine 886 - 1547 BHP

Model L7042GL Turbocharged and Intercooled, Twelve Cylinder, Lean Combustion, Four-Cycle Gas Engine

SPECIFICATIONS

Cylinders V 12

Piston Displacement 7040 cu. in. (115 L)

Bore & Stroke 9.375" x 8.5" (238 x 216 mm)

Compression Ratio 10.5:1

Jacket Water System Capacity 107 gal. (405 L) Lube Oil Capacity 90 gal. (340 L)

Starting System 125 - 150 psi air/gas 24/32V electric

Dry Weight 21,000 lb. (9525 kg)

Full Load Exhaust Emissions Nox - 1.50 g/bhp-hr

CO - 2.65 g/bhp-hr HC - 1.00 g/bhp-hr (non-methane)



POWER RATINGS: L7042GL VHP SERIES GAS ENGINES

		Brake Horsepower (kWb Output)						
Model	I.C. Water Inlet Temp. °F (°C) (Tcra)	C.R.	800 rpm	900 rpm	1000 rpm	1100 rpm	1200 rpm	
High Speed Turbo ¹	85° (29°)	10.5:1	928 (692)	1160 (865)	1289 (961)	1418 (1057)	1547 (1154)	
High Speed Turbo ¹	130° (54°)	10.5:1	886 (661)	1108 (826)	1232 (919)	1355 (1010)	1478 (1102)	
Low Speed Turbo ²	85° (29°)	10.5:1	1031 (769)	1160 (865)	1289 (961)			
Low Speed Turbo ²	130° (54°)	10.5:1	985 (735)	1108 (826)	1232 (919)			

¹High speed turbocharger match - 1001-1200 rpm

²Low speed turbocharger match - 700-1000 rpm

Rating Standard: All models: Ratings are based on ISO 3046/1-1995 with mechanical efficiency of 90% and auxiliary water temperature Tcra (clause 10.1) as specified above limited to ± 10° F (± 5° C). Ratings are also valid for SAE J1349, BS5514, DIN6271 and AP17B-11C standard atmospheric conditions.

ISO Standard Power/Continuous Power Rating: The highest load and speed which can be applied 24 hours a day, seven days a week, 365 days per year except for normal maintenance. It is permissible to operate the engine at up to 10% overload, or maximum load indicated by the intermittent rating, whichever is lower, for two hours in each 24 hour period.

All natural gas engine ratings are based on a fuel of 900 Btu/ft3 (35.3 MJ/nm3) SLHV value, with a 91 Waukesha Knock Index®.

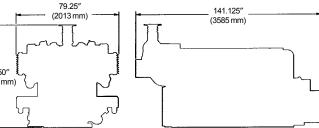
For conditions or fuels other than standard, the Waukesha Engine Sales Engineering Department.

PERFORMANCE: L7042GL VHP SERIES GAS ENGINES

	English	130°	F ICW	85° F	ICW		Metric	54° (CICW	29° (CICW
	RPM	1200	1000	1200	1000		RPM	1200	1000	1200	1000
	Power (Bhp)	1478	1232	1547	1289		Power (kWb)	1103	919	1154	962
<u> </u>	BSFC (Btu/bhp-hr)	7155	6815	7180	6840	×	BSFC (kJ/kW-hr)	10124	9643	10160	9679
NO	NOx (grams/bhp-hr)	0.90	0.90	0.70	0.70	NO	NOx (g/nm³)	0.37	0.37	0.29	0.29
Low NO _x Settings	CO (grams/bhp-hr)	2.75	2.65	2.65	2.55	Low NO _x Settings	CO (g/nm ³)	1.14	1.10	1.10	1.05
	NMHC (grams/bhphr)	1.00	1.00	1.10	1.10		NMHC (g/nm ³)	0.41	0.41	0.45	0.45
u	BSFC (Btu/bhp-hr)	6910	6615	6935	6640	_ uo	BSFC (kJ/kW-hr)	9778	9360	9813	9396
Fuel nptic ngs	NOx (grams/bhp-hr)	1.50	1.60	1.30	1.40	Fuel nptic ngs	NOx (g/nm³)	0.62	0.66	0.54	0.58
Low Fuel Consumption Settings	CO (grams/bhp-hr)	3.00	2.75	2.90	2.65	Low Fuel Consumptio Settings	CO (g/nm³)	1.24	1.14	1.20	1.10
-3	NMHC (grams/bhphr)	0.70	1.00	0.80	1.10	_0	NMHC (g/nm ³)	0.29	0.41	0.33	0.45

NOTES:

- 1) Performance ratings are based on ISO 3046/1-1995 with mechanical efficiency of 90% and Tcra limited to \pm 10° F.
- Fuel consumptions based on ISO 3046/1-1995 with a +5% tolerance for commercial quality natural gas having a 900 Btu/ft³ saturated low heat value.
- Data based on standard conditions of 77° F (25° C) ambient temperature, 29.53 g1.50″ inches Hg (100kPa) barometric pressure, 30% relative humidity (0.3 inches Hg / (2324 mm))
 kPa water vapor pressure).
- Data will vary due to variations in site conditions. For conditions and/or fuels other than standard, consult the Waukesha Engine Sales Engineering Department.





Waukesha

WAUKESHA ENGINE DRESSER, INC. 1000 West St. Paul Avenue Waukesha, WI 53188-4999 Phone: (262) 547-3311 Fax: (262) 549-2795 waukeshaengine.dresser.com Bulletin 7005 0102 WAUKESHA ENGINE DRESSER INDUSTRIAL PRODUCTS, B.V. Farmsumerweg 43, Postbus 330 9900 AH Appingedam, The Netherlands Phone: (31) 596-652222 Fax: (31) 596-628111 Consult your local Waukesha Distributor for system application assistance. The manufacturer reserves the right to change or modify without notice, the design or equipment specifications as herein set forth without incurring any obligation either with respect to equipment previously sold or in the process of construction except where otherwise specifically guaranteed by the manufacturer.

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Waukesha-Pearce Industries, Inc. - Houston, Texas

EMISSIONS CALCULATION FORMULAS

DATE: 03/17/04

	CUSTOMER:	Hanover			MODEL:	Waukesha L	7042 GL		
	ENGI	NE OR CONV	ERTER OUTPU	T DATA			ASSUMED	CALC	CALC
PPM _v	PPM _v	EXH	FUEL BTU	FUEL USED	Mfg BSFC	APPROX	EXH H ₂ 0	SCFH/HP	DSCFM
NOx	co	02 %	Ft/ ³ - HHV	Ft/ ³ - HR	LHV	ENG HP	%		@ H ₂ O %
128.6	48.1	9.8	1,015	11,525	7,155	1,478	10.0	147	3,269
			-						
Oxygen Corre	ection Factor		% (if allowed)	Rich Burn I	Exhaust ~ H _L O %	% is: Fuel Ricl	h=21 Stoke=19	Fuel Lean=17	
				Lean B	lurn Exhaust ~	Ң О % is 13% ∙	- 10% depending	g on AFR	
				EXHAL	JST FLOW - C	ALCULATION	AREA	CALC	
	an Anna ann an Anna an Anna Anna Anna A			EXH FLOW - A	CFM OR	8,165	EITHER / OR	SCFM	
DO NOT PL	JT DATA IN L	.BS/HR ARE	A =====>	EXH FLOW - LE	BS/HR		NOT BOTH	3,632	0
				EXH TEMP		709	۰F		

IMPORTANT: SEE NOTE BELOW

Oxygen Content Indicates Lean Burn Engine - Enter Correct H2O % and Exhaust Flow Data Above

Based on E	xhaust Flow	-	Based on Eng	jine Heat Rate	-	Based on Fue	Consumption			
CARB 1-10	0 METHOD		TCEQ	METHOD		EPA M	ethod 19		Calculate	ed Data
NOx	со		NOx	со		NOx	со		NMHC	CH ₂ O
3.02	0.69		2.99	0.68	1	2.95	0.67		0.68	0.07
lbs/hr	lbs/hr		lbs/hr	lbs/hr		lbs/hr	lbs/hr		lbs/hr	lbs/hr
0.93	0.21	-	0.92	0.21		0.90	0.21		0.21	0.02
g/BHP-Hr	g/BHP-Hr		g/BHP-Hr	g/BHP-Hr		g/BHP-Hr	g/BHP-Hr		g/BHP-Hr	g/BHP-Hr
13.2	3.0		13.1	3.0		12.9	2.9		3.0	0.3
TPY	TPY		TPY	TPY		TPY	TPY		TPY	TPY
		ant the	67.0				Alia in a statistica a			1
WPI Pc	werhouse ®	COMBO	672	Oxidation Co	nverter no	AFK.		in a state of the		

Note: (1) TNRCC method returns g/BHP-Hr without requiring HP. CARB and EPA M-19 return lb/hr. Each Method is calculated separatel (2) g/BHP-Hr = lb/hr / (HP x 0.002205). [0.002205 is reciprocal of 453.6 g/ll

(3) Calculate engine HP using software based on engine data inputs - i.e. intake manif pressure, RPM, CID, etc

and confirm load via compressor or generator loading programs to support data

(4) Assumed heating value of fuel is 1,015 - typical CQNG - unless indicated otherwise above

Note: Any one of the above three methods should return approximately the same values with similar / equal input value: If the output data between the methods is not close, then the input data may be incorrec

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Waukesha-Pearce Industries, Inc.

P.O. Box 35068 - 12320 S. Main - Houston, TX 77235-5068 Phone: 713-723-1050 - Fax: 713-551-0799 - Direct: 713-551-0330

LIMITED WARRANTY STATEMENT - OXIDATION CONVERTER

Waukesha-Pearce Industries, Inc. ("WPI") strictly for the period stated warrants, subject to all terms and conditions herein, that the WPI[®] Powerhouse [®] Catalytic Converter furnished, when operated in accordance with the engine exhaust conditions stated below, will reduce CO & GM by 93.0 %, & NMHC by 79.0 %.

ENGINE EXHAUST CONDITIONS

- * Maximum CO from engine will not exceed 2.8 g/BHP-Hr.
- * Maximum CH2O from engine will not exceed 0.3 g/BHP-Hr.
- * Temperature of exhaust into the catalyst will be 550°F minimum to 1250°F maximum.
- * Engine will have oxygen content in the exhaust in excess of 4%.
- Combustibles content (i.e. unburned fuel) will not produce higher than 1350°F catalyst exit temperature.
- * Pressure drop across catalyst will not change by more than 2"w.c. before cleaning. Such periodic cleaning of particulates is a normal service procedure and not a warranty issue.
- * Engine operation will be stable and reproducible.
- * Maximum lubrication oil consumption rate will be less than 0.0015 lb/BHP-H:
- * Lube oil sulfated ash content will not exceed 0.5%.
- * Lube oil phosphorus will not exceed 10 ppm and zinc will not exceed 5 ppm in the exhaust stream.
- * Customer will maintain a high temperature alarm/shutdown in the catalyst outlet set at a maximum of 1350°F.
- * Fuel will not contain known catalyst deactivators such as lead, mercury, arsenic, antimony, zin copper, tin, iron, barium, nickel, chrome, and/or phosphorous.
- * Chlorinated and Silicon containing compounds will not exceed 1 ppm in the exhaust stream.
- * Sulfur compounds in the exhaust stream will not exceed 25 ppm.
- * User must maintain and operate the engine in accordance with manufacturers' recommendations.

SPECIAL CONDITIONS: Air Fuel Ratio Controller Is NOT Required.

Special Reverse Flow Design - OXMR - for low exhaust temps.

Should the converter not perform as stated above and the equipment has been maintained per the above terms and conditions and the application is as listed below, WPI is obligated to eith repair or replace any part(s) or whole of the converter so that it will perform as stated. The term of original warranty is not extended by any such action. <u>UNDER NO CIRCUMSTANCES</u> WILL WPI ASSUME ANY CONTINGENT LIABILITIES.

Customer / Location:	Hanover	New Mexico
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Engine Model:	Waukesha L 7042 GL	Max HP: 1,478	RPM: 1,200
Powerhouse ®	# 672 COMBO	Calc S.V.=	62,896 hr-1

Dated: 03/17/04 Warranty Term: One (1) Year of Service

THE POWER PEOPLE [®] A PEARCE INDUSTRIES, INC. COMPANY



WAUKESHA-PEARCE INDUSTRIES, INC. - HOUSTON, TEXAS

Houston, Texas (phone) 713-723-1050

QUOTE / PERFORMANCE WORKSHEET

	CUSTOMER:	1	Hanover					
	REQUIRED EMISSIONS:	1	Unspecif	ied				
	EQUIPMENT LOCATION:		New Mexi					
	ADDITIONAL COMMENTS:		Low Nox	-	tings			
	DATE:		03/17/04					
	exmonogygygygygygygygygygygygygygygygygygyg				• • • • • • • • • • • • • • • • • • •			en gezallen nen de koren
			CONDITI		-			
	Engine Make / Model		Waukesha	L		Maximum		
	Engine Horsepower Engine RPM				1,478	Maximum		
	Fuel Type				CQNG		Remired	
	Engine Exhaust Temperature				709	°F (+50°F)	neguzzeu	
	Engine Exhaust Flow				8,165	acfm		
	Converter Flange Size		Specify	on	Order	inches		
	Oxygen in Engine Exhaust				9.80	Percent		~
	Engine Emissions		and an		Manufactu	rers or Site Da	ta	TPY
	NOx				0.90	g/BHP-Hr		13
	со				2.75	g/BHP-Hr		39
	NMHC				1.00	g/BHP-Hr		14
Sumbly a burn	CH20	-			0.290	g/BHP-Hr	-	4
					,		Total	71
Γ	Post Converter Reduction	as 9	6		Equals	Approximately		TPY
	NOx	0.0			0.90	g/BHP-Hr		13
	CO	93.0			0.19	g/BHP-Hr		3
	NMHC	79.0			0.21	g/BHP-Hr		3
	CH20	93.0	1		0.020	g/BHP-Hr		0
Dece		-	100000100000 <u>0</u> 7000007000000000000000000	24000 (Anii Anii			Total	19

NOTE: All HC reductions are temperature dependent. NOTE: Conversion rates are subject to $\pm 3\%$ performance factor. NOTE: Converter Flange Sizes to be determined but will not effect prices.

	QUOTED EQUIPMENT		
Description	Model / Data	Net per System	
WPI Powerhouse [®] COMBO	672	\$17,333	-
		· · · · · · · · · · · · · · · · · · ·	
ADDITIONAL ITEMS:			
Thermocouples >4 - CC / AFR			
Power Supply or DC Required			
Thermocouple Wire (As Req)			
Safety Shutdown - (AFR)			
O2 Sensor Adaptor (>2)			
Crankcase Extractor System	WED Code 1100 Series	Required	
	1		
TOTAL NUMBER OF UNITS: 1	TOTAL COST:	\$17,333	
***** SUBJECT TO THE ATTACHED PI	ERFORMANCE / LIMITED WARRA	ANTY STATEMENT *****	
Special Notes - Assumed Good Fuel	/ Manufacturer Published	l Engine Emissions	
Prox Backpressure "w.c. 6	Calculated S.V. =	62,896 hr-	1
Converter NOx PPMv =- 129	/ CO PPMv =~ 48	/ NMHC PPMv =~ 84	4
	· · ·		

BY:

The Power People [®]

REF:

A Pearce Industries, Inc. Company



295 Chipeta Way P.O. Box 58900 Salt Lake City, UT 84108 801/584-6999

February 26, 1999

Andrew Nowak, Ph.D., P.E. New Mexico Environment Department Air Quality Bureau 2048 Galisteo Street Santa Fe, New Mexico 87505

Subject: 32-7 CDP - PSD Application -1032-M-3

Dear Mr. Nowak:

This letter addresses the issues raised in your incompleteness letter dated February 18, 1999 with regards to the 32-7 Prevention of Significant Deterioration (PSD) permit application PSD-NM-1032-M-3. The following are responses to issues raised in your letter.

The New Mexico Environment Department, Air Quality Bureau (AQB) has requested that a BACT analysis be performed for carbon monoxide (CO) emissions from the proposed Waukesha engines. In a letter dated February 12, 1999, the AQB requested that WFS evaluate CO catalytic converters as BACT for control of CO emissions from the proposed engines. In response to this issue, WFS proposes to install converters on two of the four proposed new engines at the 32-7 CDP.

Using a CO reduction of 90 percent for two of the four proposed engines, the total increase in CO emissions would be reduced from approximately 141.2 tons per year to 78.7 tons per year. Thus, the increase in CO emissions from the proposed modification would be less than the significant emission rate for CO of 100 tons per year. As such, the proposed modification would not be subject to BACT review for CO, and a BACT determination for CO emissions would not be required.

In regard to notification of adjacent landowners of the proposed modification to the 32-7 CDP, the letter to Robert Witten and Frederic Nathan, Trustees, was sent to an incorrect address. This problem was corrected and a copy of the letter has been sent to the appropriate address. A copy of the corrected letter has previously been provided to the AQB.

At the request of the AQB, a simplified flow diagram of the operations at the 32-7 CDP is provided with this letter.

I assume that the information provided in this letter should enable you to complete your review. If any additional information is needed, or you have questions, please feel free to contact me at (801) 584-6999 or Walter Konkel at (805) 963-6777.

Sincerely,

H. Lee Bauerle Senior Enviromental Specialist

attachment

Pollutant	Emission Factor (lb/MMBtu) ^b (fuel input)	Emission Factor Rating
Criteria Pollutants and Greenhou	se Gases	•
NO _x ^c 90 - 105% Load	4.08 E+00	В
NO _x ^c <90% Load	8.47 E-01	В
CO ^c 90 - 105% Load	3.17 E-01	С
CO ^c <90% Load	5.57 E-01	В
$\mathrm{CO_2}^{\mathrm{d}}$	1.10 E+02	А
SO ₂ ^e	5.88 E-04	А
TOC ^f	1.47 E+00	А
Methane ^g	1.25 E+00	С
VOC ^h	1.18 E-01	С
PM10 (filterable) ⁱ	7.71 E-05	D
PM2.5 (filterable) ⁱ	7.71 E-05	D
PM Condensable ^j	9.91 E-03	D
Trace Organic Compounds		
1,1,2,2-Tetrachloroethane ^k	<4.00 E-05	Е
1,1,2-Trichloroethane ^k	<3.18 E-05	Е
1,1-Dichloroethane	<2.36 E-05	Е
1,2,3-Trimethylbenzene	2.30 E-05	D
1,2,4-Trimethylbenzene	1.43 E-05	С
1,2-Dichloroethane	<2.36 E-05	Е
1,2-Dichloropropane	<2.69 E-05	Е
1,3,5-Trimethylbenzene	3.38 E-05	D
1,3-Butadiene ^k	2.67E-04	D
1,3-Dichloropropene ^k	<2.64 E-05	Е
2-Methylnaphthalene ^k	3.32 E-05	С
2,2,4-Trimethylpentane ^k	2.50 E-04	С
Acenaphthene ^k	1.25 E-06	С

Table 3.2-2. UNCONTROLLED EMISSION FACTORS FOR 4-STROKE LEAN-BURN ENGINESa(SCC 2-02-002-54)

Pollutant	Emission Factor (lb/MMBtu) ^b (fuel input)	Emission Factor Rating
Acenaphthylene ^k	5.53 E-06	С
Acetaldehyde ^{k,l}	8.36 E-03	А
Acrolein ^{k,l}	5.14 E-03	А
Benzene ^k	4.40 E-04	А
Benzo(b)fluoranthene ^k	1.66 E-07	D
Benzo(e)pyrene ^k	4.15 E-07	D
Benzo(g,h,i)perylenek	4.14 E-07	D
Biphenyl ^k	2.12 E-04	D
Butane	5.41 E-04	D
Butyr/Isobutyraldehyde	1.01 E-04	С
Carbon Tetrachloride ^k	<3.67 E-05	Е
Chlorobenzene ^k	<3.04 E-05	Е
Chloroethane	1.87 E-06	D
Chloroform ^k	<2.85 E-05	Е
Chrysene ^k	6.93 E-07	С
Cyclopentane	2.27 E-04	С
Ethane	1.05 E-01	С
Ethylbenzene ^k	3.97 E-05	В
Ethylene Dibromide ^k	<4.43 E-05	Е
Fluoranthene ^k	1.11 E-06	С
Fluorene ^k	5.67 E-06	С
Formaldehyde ^{k,1}	5.28 E-02	А
Methanol ^k	2.50 E-03	В
Methylcyclohexane	1.23 E-03	С
Methylene Chloride ^k	2.00 E-05	С
n-Hexane ^k	1.11 E-03	С
n-Nonane	1.10 E-04	С

Table 3.2-2. UNCONTROLLED EMISSION FACTORS FOR 4-STROKE LEAN-BURN ENGINES (Continued)

Pollutant	Emission Factor (lb/MMBtu) ^b (fuel input)	Emission Factor Rating
n-Octane	3.51 E-04	С
n-Pentane	2.60 E-03	С
Naphthalene ^k	7.44 E-05	С
PAH ^k	2.69 E-05	D
Phenanthrene ^k	1.04 E-05	D
Phenol ^k	2.40 E-05	D
Propane	4.19 E-02	С
Pyrene ^k	1.36 E-06	С
Styrene ^k	<2.36 E-05	Е
Tetrachloroethane ^k	2.48 E-06	D
Toluene ^k	4.08 E-04	В
Vinyl Chloride ^k	1.49 E-05	С
Xylene ^k	1.84 E-04	В

Table 3.2-2. UNCONTROLLED EMISSION FACTORS FOR 4-STROKE LEAN-BURN **ENGINES** (Continued)

^a Reference 7. Factors represent uncontrolled levels. For NO_v, CO, and PM10, "uncontrolled" means no combustion or add-on controls; however, the factor may include turbocharged units. For all other pollutants, "uncontrolled" means no oxidation control; the data set may include units with control techniques used for NOx control, such as PCC and SCR for lean burn engines, and PSC for rich burn engines. Factors are based on large population of engines. Factors are for engines at all loads, except as indicated. SCC = Source Classification Code. TOC = Total Organic Compounds. PM-10 = Particulate Matter \leq 10 microns (μ m) aerodynamic diameter. A "<" sign in front of a factor means that the corresponding emission factor is based on one-half of the method detection limit. ^b Emission factors were calculated in units of (lb/MMBtu) based on procedures in EPA Method 19. To convert from (lb/MMBtu) to (lb/ 10^6 scf), multiply by the heat content of the fuel. If the heat content is not available, use 1020 Btu/scf. To convert from

(lb/MMBtu) to (lb/hp-hr) use the following equation:

lb/hp-hr = (lb/MMBtu) (heat input, MMBtu/hr) (1/operating HP, 1/hp)

^c Emission tests with unreported load conditions were not included in the data set.

^d Based on 99.5% conversion of the fuel carbon to CO_2 . CO_2 [lb/MMBtu] = (3.67)(%CON)(C)(D)(1/h), where %CON = percent conversion of fuel carbon to CO_2 , C = carbon content of fuel by weight (0.75), $D = \text{density of fuel}, 4.1 \text{ E}+04 \text{ lb}/10^6 \text{ scf}, \text{ and}$

h = heating value of natural gas (assume 1020 Btu/scf at 60° F).

- ^e Based on 100% conversion of fuel sulfur to SO_2 . Assumes sulfur content in natural gas of $2,000 \text{ gr}/10^6 \text{scf.}$
- Emission factor for TOC is based on measured emission levels from 22 source tests.
- ^g Emission factor for methane is determined by subtracting the VOC and ethane emission factors from the TOC emission factor. Measured emission factor for methane compares well with the calculated emission factor, 1.31 lb/MMBtu vs. 1.25 lb/MMBtu, respectively.
- $^{\rm h}$ VOC emission factor is based on the sum of the emission factors for all speciated organic compounds less ethane and methane.
- Considered $\leq 1 \ \mu m$ in aerodynamic diameter. Therefore, for filterable PM emissions, PM10(filterable) = PM2.5(filterable).
- ^j PM Condensable = PM Condensable Inorganic + PM-Condensable Organic
- Hazardous Air Pollutant as defined by Section 112(b) of the Clean Air Act.
- For lean burn engines, aldehyde emissions quantification using CARB 430 may reflect interference with the sampling compounds due to the nitrogen concentration in the stack. The presented emission factor is based on FTIR measurements. Emissions data based on CARB 430 are available in the background report.

Pollutant	Emission Factor (lb/10 ⁶ scf)	Emission Factor Rating
CO ₂ ^b	120,000	А
Lead	0.0005	D
N ₂ O (Uncontrolled)	2.2	Е
N ₂ O (Controlled-low-NO _X burner)	0.64	Е
PM (Total) ^c	7.6	D
PM (Condensable) ^c	5.7	D
PM (Filterable) ^c	1.9	В
SO_2^{d}	0.6	А
TOC	11	В
Methane	2.3	В
VOC	5.5	С

TABLE 1.4-2. EMISSION FACTORS FOR CRITERIA POLLUTANTS AND GREENHOUSE GASES FROM NATURAL GAS COMBUSTION^a

^a Reference 11. Units are in pounds of pollutant per million standard cubic feet of natural gas fired. Data are for all natural gas combustion sources. To convert from $lb/10^6$ scf to $kg/10^6$ m³, multiply by 16. To convert from $lb/10^6$ scf to 1b/MMBtu, divide by 1,020. The emission factors in this table may be converted to other natural gas heating values by multiplying the given emission factor by the ratio of the specified heating value to this average heating value. TOC = Total Organic Compounds. VOC = Volatile Organic Compounds.

- ^b Based on approximately 100% conversion of fuel carbon to CO_2 . $CO_2[lb/10^6 \text{ scf}] = (3.67)$ (CON) (C)(D), where CON = fractional conversion of fuel carbon to CO_2 , C = carbon content of fuel by weight (0.76), and D = density of fuel, $4.2 \times 10^4 \text{ lb}/10^6 \text{ scf}$.
- ^c All PM (total, condensible, and filterable) is assumed to be less than 1.0 micrometer in diameter. Therefore, the PM emission factors presented here may be used to estimate PM_{10} , $PM_{2.5}$ or PM_1 emissions. Total PM is the sum of the filterable PM and condensible PM. Condensible PM is the particulate matter collected using EPA Method 202 (or equivalent). Filterable PM is the particulate matter collected on, or prior to, the filter of an EPA Method 5 (or equivalent) sampling train.

^d Based on 100% conversion of fuel sulfur to SO_2 . Assumes sulfur content is natural gas of 2,000 grains/10⁶ scf. The SO_2 emission factor in this table can be converted to other natural gas sulfur contents by multiplying the SO_2 emission factor by the ratio of the site-specific sulfur content (grains/10⁶ scf) to 2,000 grains/10⁶ scf.

Extended Gas Analysis

Gas Composition

	Mole	Molecular	Emission
Components	Percents,	Weights,	Factors,
-	%	lb/lb-mole	lb/scf
Carbon dioxide	6.9673	44.01	8.082E-03
Hydrogen sulfide	0.0000	34.07	0.000E+00
Nitrogen	0.0353	28.01	2.606E-05
Methane	92.1867	16.04	3.897E-02
Ethane	0.7106	30.07	5.632E-04
Propane	0.0677	44.09	7.867E-05
Isobutane	0.0106	58.12	1.624E-05
n-Butane	0.0097	58.12	1.486E-05
Isopentane	0.0031	72.15	5.895E-06
n-Pentane	0.0020	72.15	3.803E-06
Cyclopentane	0.0002	70.14	3.697E-07
n-Hexane	0.0010	86.17	2.271E-06
Cyclohexane	0.0006	84.16	1.331E-06
Other hexanes	0.0020	86.18	4.543E-06
Heptanes	0.0007	100.20	1.849E-06
Methylcyclohexane	0.0010	98.19	2.588E-06
2,2,4-Trimethylpentane	0.0000	100.21	0.000E+00
Benzene	0.0000	78.11	0.000E+00
Toluene	0.0004	92.14	9.714E-07
Ethylbenzene	0.0000	106.17	0.000E+00
Xylenes	0.0003	106.17	8.395E-07
C8+ Heavies	0.0011	110.00	3.189E-06
Total	100.0003		
Total VOC			1.374E-04

Gas stream composition obtained from the 32-7 #1 CDP extended gas analysis dated June 22, 2021. Emission Factors (lb/scf) = (% / 100) x lb/lb-mole / 379.4 scf/lb-mole



2030 Afton Place Farmington, NM 87401 (505) 325-6622

Analysis No: HM2021060 Cust No: 33700-10320

		Well/Lease Information		
Customer Name:	HARVEST MIDSTREAM		Source:	Dehy Inlet
Well Name:	32-7 #1 CDP		Well Flowing:	
County/State:	San Juan NM		Pressure:	928 PSIG
Location:			Flow Temp:	117 DEG. F
Lease/PA/CA:			Ambient Temp:	96 DEG. F
Formation:	Mancos/MV		Flow Rate:	52.5 MCF/D
Cust. Stn. No.:	Dehy 42670		Sample Method:	Purge & Fill
			Sample Date:	06/22/2021
			Sample Time:	2.30 PM
			Sampled By:	Daniel Lovato
Heat Trace:			Sampled by (CO)	: Harvest

Heat Trace: Remarks:

Calculated Molecular Weight = 18.1319

Analysis					
Component:	Mole%:	Unormalized %:	**GPM:	*BTU:	*SP Gravity:
Nitrogen	0.0353	0.0346	0.0040	0.00	0.0003
CO2	6.9673	6.8376	1.1910	0.00	0.1059
Methane	92.1867	90.4708	15.6590	931.09	0.5106
Ethane	0.7106	0.6974	0.1900	12.58	0.0074
Propane	0.0677	0.0664	0.0190	1.70	0.0010
Iso-Butane	0.0106	0.0104	0.0030	0.34	0.0002
N-Butane	0.0097	0.0095	0.0030	0.32	0.0002
Neopentane 2,2 dmc3	0.0000	0.0000	0.0000	0.00	0.0000
I-Pentane	0.0031	0.0030	0.0010	0.12	0.0001
N-Pentane	0.0020	0.0020	0.0010	0.08	0.0001
Neohexane	0.0001	N/R	0.0000	0.00	0.0000
2-3-Dimethylbutane	0.0002	N/R	0.0000	0.01	0.0000
Cyclopentane	0.0002	N/R	0.0000	0.01	0.0000
2-Methylpentane	0.0011	N/R	0.0000	0.05	0.0000
3-Methylpentane	0.0005	N/R	0.0000	0.02	0.0000
C6	0.0010	0.0070	0.0000	0.05	0.0000
Methylcyclopentane	0.0001	N/R	0.0000	0.00	0.0000
Benzene	0.0000	N/R	0.0000	0.00	0.0000
Cyclohexane	0.0006	N/R	0.0000	0.03	0.0000
2-Methylhexane	0.0003	N/R	0.0000	0.02	0.0000
3-Methylhexane	0.0000	N/R	0.0000	0.00	0.0000
2-2-4-Trimethylpentane	0.0000	N/R	0.0000	0.00	0.0000
i-heptanes	0.0000	N/R	0.0000	0.00	0.0000
Heptane	0.0004	N/R	0.0000	0.02	0.0000
			0.0000	0.02	

C11 C12P	0.0001 0.0000 0.0000 0.0000	N/R N/R N/R N/R	0.0000 0.0000 0.0000 0.0000	0.01 0.00 0.00 0.00	0.0000 0.0000 0.0000 0.0000
	0.0000 0.0000	N/R N/R	0.0000	0.00	0.0000
	0.0000	N/R			
i-C11			0.0000	0.01	0.0000
C10	0.0004				
i-C10	0.0001	N/R	0.0000	0.01	0.0000
C9	0.0000	N/R	0.0000	0.00	0.0000
i-C9	0.0001	N/R	0.0000	0.01	0.0000
o Xylene (& 2,2,4 tmc7)	0.0001	N/R	0.0000	0.01	0.0000
m, p Xylene	0.0002	N/R	0.0000	0.01	0.0000
Ethylbenzene	0.0000	N/R	0.0000	0.00	0.0000
Octane	0.0003	N/R	0.0000	0.02	0.0000
i-Octanes	0.0000	N/R	0.0000	0.00	0.0000
4-Methylheptane	0.0002	N/R	0.0000	0.01	0.0000
2-Methylheptane	0.0003	N/R	0.0000	0.02	0.0000
Toluene	0.0004	N/R	0.0000	0.02	0.0000
Methylcyclohexane	0.0010	N/R	0.0000	0.05	0.0000

* @ 14.730 PSIA DRY & UNCORRECTED FOR COMPRESSIBILITY

**@ 14.730 PSIA & 60 DEG. F.

COMPRESSIBLITY FACTOR	(1/Z):	1.0022	CYLINDER #:	13
BTU/CU.FT IDEAL:		948.8	CYLINDER PRESSURE:	928 PSIG
BTU/CU.FT (DRY) CORRECTED F	OR (1/Z):	950.9	ANALYSIS DATE:	07/07/2021
BTU/CU.FT (WET) CORRECTED F	OR (1/Z):	934.4	ANALYIS TIME:	02:11:23 AM
DRY BTU @ 15.025:		969.9	ANALYSIS RUN BY:	PATRICIA KING
REAL SPECIFIC GRAVITY:		0.6271		

GPM, BTU, and SPG calculations as shown above are based on current GPA constants. GPA Standard: GPA 2286-14 GC: SRI Instruments 8610 GC Method: C12+BTEX Gas

Description:	32-7 #1 CDP	Company:	HARVEST MIDSTREAM
Field:		WorkOrder:	
Meter Number:	Dehy 42670	GPA Method:	GPA 2286
Analysis Date/Time:	6/9/2022 1:15	:05 Sampled By:	Daniel Lovato
Date Sampled:	6/7/2022	Analyst Initials:	EM
Sample Temperature:	107	Instrument:	SRI 8610
Sample Pressure:	859		

GRI GlyCalc Information

Component	Mol%	Normalized Weight %
Carbon Dioxide	6.6351	16.1662
Hydrogen Sulfide	N/R	0
Nitrogen	0.0998	0.1548
Methane	92.3408	82.0141
Ethane	0.8094	1.3474
Propane	0.0877	0.2141
Iso-Butane	0.0082	0.0264
n-Butane	0.0095	0.0306
Iso-Pentane	0.0041	0.0164
n-Pentane	0.0012	0.0048
Cyclopentane	0.0001	0.0004
n-Hexane	0.0005	0.0025
Cyclohexane	0.0002	0.0009
Other Hexanes	0.0011	0.0061
Heptanes	0.0004	0.0022
Methylcyclohexane	0.0008	0.0043
2 2 4 Trimethylpentane	0	0
Benzene	0.0001	0.0004
Toluene	0.0003	0.0015
Ethylbenzene	0	0
Xylenes	0.0002	0.0012
C8+ Heavies	0.0009	0.0057
Subtotal	100.0004	
Oxygen	N/R	
Subtotal	100.0004	100
Calculated Molecular Weight		18.063

KIMRAY, Inc. "PV" & "SC" SERIES GLYCOL PUMPS 1500 LB. W.P. Okla. City, OK



PUMPS AVAILABLE:

"PV" SERIES GLYCOL PUMPS						
Catalog Number	Model Number		acity / Hr.	Wor Pres	king sure	
		Min.	Max.**	Min.	Max.	
GAA	315 PV	3	13	100	1500	
GAD	1715 PV	8	40	300	1500	
GAB	4015 PV	12	40	300	1500	
GAF	9015 PV	27	90	300	1500	
GAH	21015 PV	66	210	400	1500	
GAJ	45015 PV	166	450	400	1500	

**Maximum output is affected by system pressure drops. See system operation parameter for maximum output curves.

"SC" SERIES GLYCOL PUMPS						
Catalog Number			oacity . / Hr.		king sure	
Number	Number	Min.	Max.**	Min.	Max.	
GAC	2015 SC*	8	20	100	500	
GAG	5015 SC*	12	50	100	500	
GAI	10015 SC*	22	100	100	500	
GAK	20015 SC*	60	200	100	500	

NOTE: To order a Pump with Viton O Rings add 1 to Catalog number. Example: To order GAA with Viton O Rings, specify: GAA1.

MAXIMUM DESIGN PRESSURE FOR P.V. AND S.C. MODELS IS 1500 psig

APPLICATIONS:

Circulating pump for gas glycol dehydrators Circulating pump for gas amine desulphurizers

FEATURES:

Eliminates absorber liquid level controls

No auxiliary power supply required

Low gas consumption

Completely sealed system prevents loss glycol

No springs or toggles, only two moving assemblies

Hydraulic "cushioned" check valves with removable seats of

hardened stainless steel

OPERATION:

Materials for the vital working parts have been selected for greatest wear resistance. These materials include stainless steel, hard chrome plating, satellite, nylon and teflon. Moving "O" Ring seals are compounded specifically for ethylene glycol service. A complete operational check is given each pump after assembly.

"O" Ring sealed check valve darts are standard in all except the model 315 PV. Teflon sealed darts are available. Capsule type ball checks are used in the 315 PV and are available for 1715 PV, 2015 SC and 4015 PV.

*These pumps are designed for operating pressures between 100 and 500 psig maximum design pressure for all models is 1500 psig.

P.1/1

Oil and Gas mailuction Equipment

S. Enerters, Inc. 4101 Ball Marn Street Farmington, NM 87401

505/126-1151 MAR \$05/325-0317 RTEK

VIA FACSDAILE Fax No. (801) 584-7760 Pages 1

August 19, 1994

Mr. Los Bauerla Williams Field Services Salt Lake City, UT

The following table shows the stack emissions at maximum firing conditions for the dahydrators noted

Dehvdrator	NO ₃ #/Day	© ₽/₽₹¥	Fuel SCEH	Total Stack Gates ACEH	Stuck H1. F1	Stack Dis Inclus	Stack Tamp F	Stack Velocity, FPS
J2P10M11109	0.16	0_17	357	10010	121-	8	600	5.1
J2710M749	1.03	0.21	429	12012	19*-1*	10	600	6 .1
J2P12M11109	0.16	0.17	357	10010	13'-5"	¥	600	5. i
JZP12M749	1.03	0_21	«29	12012	19"-1"	10	600	6.1
J2P20M11109	1_03	0.21	429	12012	19-1-	10	600	6.1

Please call me if you need additional information.

Sincerely.

. .

Fronty Heath

FH/ab



Office: (505)632-2200 Fax: (505)632-8070

July 22, 1998

5928 U.S. Highway 64

Farmington, NM 87401

Mr. Bobby Myers Williams Field Services Environmental Affairs 295 Chipeta Way P O Box 58900 Salt Lake City, UT 84158-0900

The table shown below gives the stack emissions for our larger dehydrators:

Unit Description	SO Ib/day	NO _x Ib/ Day	CO Ib/ Day	Fuel SCFH	Total Organic Comp. Lb/d	Stack Ht. Ft.	Stack Dia inches	Temp °F	Stack Velocity
			1	1			1	1	
10 MM LP	01	.27	.43	659	.13	10.	8	600	5.1
10 MM HP	.01	.27	.43	659	.13 1	10.	10	1 600 i	i 6.1
		•			i			1	Í.
12 MM LP	.02	.49	.78	1208	.25	10'	8	600	5.1
								. 1	
12 MM HP	.02	.49	.78	1208	.23 1	10'	10	600	6.1
15 MM	.02	.54	.85	1318	.25	10. 1	8	600 !	5.1
1	1	1	I		1	- 1		I	
20 MM LP	.02	.67	1.07	1648	.31	10, 1	8	600	5.1
20 MM HP	.02	.67	1.07	1648	.31	10' 1	12 1	600 ;	ó.1

If you need any additional information please call me.

Sincerely,

1.Gu

Darby West VP Engineering

1995 Protocol for Equipment Leak Emission Estimates

Emission Standards Division

U.S. ENVIRONMENTAL PROTECTION AGENCY Office of Air and Radiation Office of Air Quality Planning and Standards Research Triangle Park, North Carolina 27711

November 1995

Equipment Type	Service ^a	Emission Factor (kg/hr/source) ^b
Valves	Gas Heavy Oil Light Oil Water/Oil	4.5E-03 8.4E-06 2.5E-03 9.8E-05
Pump seals	Gas Heavy Oil Light Oil Water/Oil	2.4E-03 NA 1.3E-02 2.4E-05
Others ^C	Gas Heavy Oil Light Oil Water/Oil	8.8E-03 3.2E-05 7.5E-03 1.4E-02
Connectors	Gas Heavy Oil Light Oil Water/Oil	2.0E-04 7.5E-06 2.1E-04 1.1E-04
Flanges	Gas Heavy Oil Light Oil Water/Oil	3.9E-04 3.9E-07 1.1E-04 2.9E-06
Open-ended lines	Gas Heavy Oil Light Oil Water/Oil	2.0E-03 1.4E-04 1.4E-03 2.5E-04

TABLE 2-4. OIL AND GAS PRODUCTION OPERATIONS AVERAGE EMISSION FACTORS (kg/hr/source)

^aWater/Oil emission factors apply to water streams in oil service with a water content greater than 50%, from the point of origin to the point where the water content reaches 99%. For water streams with a water content greater than 99%, the emission rate is considered negligible.

^bThese factors are for total organic compound emission rates (including non-VOC's such as methane and ethane) and apply to light crude, heavy crude, gas plant, gas production, and off shore facilities. "NA" indicates that not enough data were available to develop the indicated emission factor.

^CThe "other" equipment type was derived from compressors, diaphrams, drains, dump arms, hatches, instruments, meters, pressure relief valves, polished rods, relief valves, and vents. This "other" equipment type should be applied for any equipment type other than connectors, flanges, open-ended lines, pumps, or valves. loading operation, resulting in high levels of vapor generation and loss. If the turbulence is great enough, liquid droplets will be entrained in the vented vapors.

A second method of loading is submerged loading. Two types are the submerged fill pipe method and the bottom loading method. In the submerged fill pipe method, the fill pipe extends almost to the bottom of the cargo tank. In the bottom loading method, a permanent fill pipe is attached to the cargo tank bottom. During most of submerged loading by both methods, the fill pipe opening is below the liquid surface level. Liquid turbulence is controlled significantly during submerged loading, resulting in much lower vapor generation than encountered during splash loading.

The recent loading history of a cargo carrier is just as important a factor in loading losses as the method of loading. If the carrier has carried a nonvolatile liquid such as fuel oil, or has just been cleaned, it will contain vapor-free air. If it has just carried gasoline and has not been vented, the air in the carrier tank will contain volatile organic vapors, which will be expelled during the loading operation along with newly generated vapors.

Cargo carriers are sometimes designated to transport only one product, and in such cases are practicing "dedicated service". Dedicated gasoline cargo tanks return to a loading terminal containing air fully or partially saturated with vapor from the previous load. Cargo tanks may also be "switch loaded" with various products, so that a nonvolatile product being loaded may expel the vapors remaining from a previous load of a volatile product such as gasoline. These circumstances vary with the type of cargo tank and with the ownership of the carrier, the petroleum liquids being transported, geographic location, and season of the year.

One control measure for vapors displaced during liquid loading is called "vapor balance service", in which the cargo tank retrieves the vapors displaced during product unloading at bulk plants or service stations and transports the vapors back to the loading terminal. Figure 5.2-5 shows a tank truck in vapor balance service filling a service station underground tank and taking on displaced gasoline vapors for return to the terminal. A cargo tank returning to a bulk terminal in vapor balance service normally is saturated with organic vapors, and the presence of these vapors at the start of submerged loading of the tanker truck results in greater loading losses than encountered during nonvapor balance, or "normal", service. Vapor balance service is usually not practiced with marine vessels, although some vessels practice emission control by means of vapor transfer within their own cargo tanks during ballasting operations, discussed below.

Emissions from loading petroleum liquid can be estimated (with a probable error of ± 30 percent)⁴ using the following expression:

$$L_{L} = 12.46 \frac{SPM}{T}$$
(1)

where:

 $L_{\rm L}$ = loading loss, pounds per 1000 gallons (lb/10³ gal) of liquid loaded

- S = a saturation factor (see Table 5.2-1)
- P = true vapor pressure of liquid loaded, pounds per square inch absolute (psia) (see Figure 7.1-5, Figure 7.1-6, and Table 7.1-2)
- M = molecular weight of vapors, pounds per pound-mole (lb/lb-mole) (see Table 7.1-2)
- T = temperature of bulk liquid loaded, ${}^{\circ}\bar{R}$ (${}^{\circ}\bar{F}$ + 460)

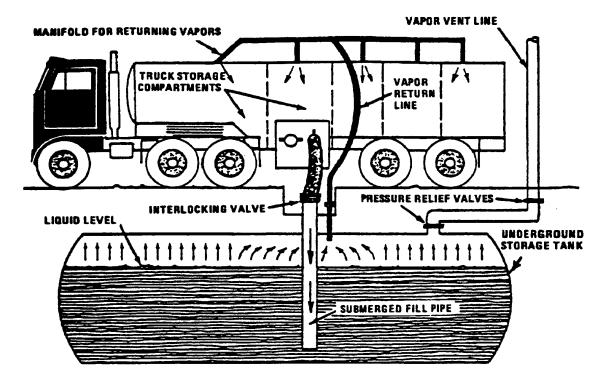


Figure 5.2-5. Tank truck unloading into a service station underground storage tank and practicing "vapor balance" form of emission control.

Table 5.2-1.	SATURATION (S) FACTORS FOR CALCULATING PETROLEUM LIQUID
	LOADING LOSSES

Cargo Carrier	Mode Of Operation	S Factor
Tank trucks and rail tank cars	Submerged loading of a clean cargo tank	0.50
	Submerged loading: dedicated normal service	0.60
	Submerged loading: dedicated vapor balance service	1.00
	Splash loading of a clean cargo tank	1.45
	Splash loading: dedicated normal service	1.45
	Splash loading: dedicated vapor balance service	1.00
Marine vessels ^a	Submerged loading: ships	0.2
	Submerged loading: barges	0.5

^a For products other than gasoline and crude oil. For marine loading of gasoline, use factors from Table 5.2-

2. For marine loading of crude oil, use Equations 2 and 3 and Table 5.2-3.

Table A–1 to Subpart A of Part 98—Global Warming Potentials

[100-Year Time Horizon]

Name	CAS No.	Chemical formula	Global warming potential (100 yr.)
Carbon dioxide	124–38–9	CO ₂	1
Methane	74–82–8	CH ₄	° 25
Nitrous oxide	10024–97–2	N ₂ O	² 298
HFC-23	75–46–7	CHF ₃	° 14,800
HFC-32	75–10–5	CH ₂ F ₂	° 675
HFC-41	593–53–3	CH₃F	^a 92
HFC-125	354–33–6	C ₂ HF ₅	° 3,500
HFC-134	359-35-3	C ₂ H ₂ F ₄	° 1,100
HFC–134a	811–97–2	CH ₂ FCF ₃	° 1,430
HFC-143	430-66-0	$C_2H_3F_3$	° 353
HFC-143a	420-46-2	$C_2H_3F_3$	² 4,470
HFC-152	624–72–6	CH ₂ FCH ₂ F	53
HFC–152a	75–37–6	CH ₃ CHF ₂	° 124
HFC-161	353–36–6	CH ₃ CH ₂ F	12
HFC–227ea	431-89-0	C ₃ HF ₇	° 3,220
HFC–236cb	677–56–5	CH ₂ FCF ₂ CF ₃	1,340
HFC–236ea	431–63–0	CHF ₂ CHFCF ₃	1,370
HFC–236fa	690–39–1	C ₃ H ₂ F ₆	° 9,810
HFC–245ca	679–86–7	C ₃ H ₃ F ₅	° 693
HFC–245fa	460-73-1	CHF ₂ CH ₂ CF ₃	1,030
HFC–365mfc	406–58–6	CH ₃ CF ₂ CH ₂ CF ₃	794
HFC-43-10mee	138495–42–8	CF ₃ CFHCFHCF ₂ CF ₃	² 1,640
Sulfur hexafluoride	2551–62–4	SF ₆	° 22,800
Trifluoromethyl sulphur pentafluoride	373-80-8	SF ₅ CF ₃	17,700
Nitrogen trifluoride	7783–54–2	NF ₃	17,200
PFC–14 (Perfluoromethane)	75–73–0	CF ₄	7,390
PFC–116 (Perfluoroethane)	76–16–4	C ₂ F ₆	^a 12,200
PFC–218 (Perfluoropropane)	76–19–7	C ₃ F ₈	² 8,830

Name	CAS No.	Chemical formula	Global warming potential (100 yr.)
Perfluorocyclopropane	931–91–9	C-C ₃ F ₆	17,340
PFC-3-1-10 (Perfluorobutane)	355-25-9	C ₄ F ₁₀	° 8,860
Perfluorocyclobutane	115-25-3	C-C ₄ F ₈	° 10,300
PFC-4-1-12 (Perfluoropentane)	678–26–2	C ₅ F ₁₂	° 9,160
PFC–5–1–14 (Perfluorohexane)	355-42-0	C ₆ F ₁₄	° 9,300
PFC-9-1-18	306-94-5	C ₁₀ F ₁₈	7,500
HCFE–235da2 (Isoflurane)	26675–46–7	CHF ₂ OCHClCF ₃	350
HFE–43–10pccc (H–Galden 1040x)	E1730133	CHF ₂ OCF ₂ OC ₂ F ₄ OCHF ₂	1,870
HFE-125	3822-68-2	CHF ₂ OCF ₃	14,900
HFE-134	1691–17–4	CHF ₂ OCHF ₂	6,320
HFE–143a	421–14–7	CH ₃ OCF ₃	756
HFE–227ea	2356-62-9	CF ₃ CHFOCF ₃	1,540
HFE–236ca12 (HG–10)	78522–47–1	CHF ₂ OCF ₂ OCHF ₂	2,800
HFE–236ea2 (Desflurane)	57041–67–5	CHF ₂ OCHFCF ₃	989
HFE–236fa	20193–67–3	CF ₃ CH ₂ OCF ₃	487
HFE–245cb2	22410-44-2	CH ₃ OCF ₂ CF ₃	708
HFE–245fa1	84011–15–4	CHF ₂ CH ₂ OCF ₃	286
HFE–245fa2	1885-48-9	CHF ₂ OCH ₂ CF ₃	659
HFE–254cb2	425-88-7	CH ₃ OCF ₂ CHF ₂	359
HFE–263fb2	460-43-5	CF ₃ CH ₂ OCH ₃	11
HFE–329mcc2	67490–36–2	CF ₃ CF ₂ OCF ₂ CHF ₂	919
HFE–338mcf2	156053-88-2	CF ₃ CF ₂ OCH ₂ CF ₃	552
HFE–338pcc13 (HG–01)	188690-78-0	CHF ₂ OCF ₂ CF ₂ OCHF ₂	1,500
HFE–347mcc3	28523-86-6	CH ₃ OCF ₂ CF ₂ CF ₃	575
HFE–347mcf2	E1730135	CF ₃ CF ₂ OCH ₂ CHF ₂	374
HFE-347pcf2	406–78–0	CHF ₂ CF ₂ OCH ₂ CF ₃	580
HFE–356mec3	382-34-3	CH ₃ OCF ₂ CHFCF ₃	101
HFE-356pcc3	160620-20-2	CH ₃ OCF ₂ CF ₂ CHF ₂	110
HFE-356pcf2	E1730137	CHF ₂ CH ₂ OCF ₂ CHF ₂	265
HFE–356pcf3	35042–99–0	CHF ₂ OCH ₂ CF ₂ CHF ₂	502

Name	CAS No.	Chemical formula	Global warming potential (100 yr.)
HFE–365mcf3	378–16–5	CF ₃ CF ₂ CH ₂ OCH ₃	11
HFE-374pc2	512–51–6	CH ₃ CH ₂ OCF ₂ CHF ₂	557
HFE–449sl (HFE–7100) Chemical blend	163702–07–6 163702–08–7	C ₄ F ₉ OCH ₃ (CF ₃) ₂ CFCF ₂ OCH ₃	297
HFE–569sf2 (HFE–7200) Chemical blend	163702–05–4 163702–06–5	C ₄ F ₉ OC ₂ H ₅ (CF ₃) ₂ CFCF ₂ OC ₂ H ₅	59
Sevoflurane	28523-86-6	CH ₂ FOCH(CF ₃) ₂	345
HFE–356mm1	13171–18–1	(CF ₃) ₂ CHOCH ₃	27
HFE–338mmz1	26103–08–2	CHF ₂ OCH(CF ₃) ₂	380
(Octafluorotetramethy- lene)hydroxymethyl group	NA	X-(CF ₂) ₄ CH(OH)-X	73
HFE–347mmy1	22052-84-2	CH ₃ OCF(CF ₃) ₂	343
Bis(trifluoromethyl)-methanol	920-66-1	(CF ₃) ₂ CHOH	195
2,2,3,3,3-pentafluoropropanol	422-05-9	CF ₃ CF ₂ CH ₂ OH	42
PFPMIE	NA	CF ₃ OCF(CF ₃)CF ₂ OCF ₂ O CF ₃	10,300

^a The GWP for this compound is different than the GWP in the version of Table A-1 to subpart A of part 98 published on October 30, 2009.

Table C–1 to Subpart C of Part 98—Default CO₂ Emission Factors and High Heat Values for Various Types of Fuel

Table C–1 to Subpart C—Default CO₂ Emission Factors and High Heat Values for Various Types of Fuel

Fuel type	Default high heat value	Default CO ₂ emission factor	
Coal and coke	mmBtu/short ton	kg CO₂/mmBtu	
Anthracite	25.09	103.69	
Bituminous	24.93	93.28	
Subbituminous	17.25	97.17	
Lignite	14.21	97.72	
Coal Coke	24.80	113.67	
Mixed (Commercial sector)	21.39	94.27	
Mixed (Industrial coking)	26.28	93.90	
Mixed (Industrial sector)	22.35	94.67	
Mixed (Electric Power sector)	19.73	95.52	
Natural gas	mmBtu/scf	kg CO₂/mmBtu	
(Weighted U.S. Average)	1.026×10^{-3}	53.06	
Petroleum products	mmBtu/gallon	kg CO₂/mmBtu	
Distillate Fuel Oil No. 1	0.139	73.25	
Distillate Fuel Oil No. 2	0.138	73.96	
Distillate Fuel Oil No. 4	0.146	75.04	
Residual Fuel Oil No. 5	0.140	72.93	
Residual Fuel Oil No. 6	0.150	75.10	
Used Oil	0.138	74.00	
Kerosene	0.135	75.20	
Liquefied petroleum gases (LPG) ¹	0.092	61.71	
Propane ¹	0.091	62.87	
Propylene ²	0.091	67.77	
Ethane ¹	0.068	59.60	
Ethanol	0.084	68.44	
Ethylene ²	0.058	65.96	
lsobutane ¹	0.099	64.94	
Isobutylene ¹	0.103	68.86	
Butane ¹	0.103	64.77	
Butylene ¹	0.105	68.72	
Naphtha (<401 deg F)	0.125	68.02	
Natural Gasoline	0.110	66.83	

Fuel type	Default high heat value	Default CO ₂ emission factor
Other Oil (>401 deg F)	0.139	76.22
Pentanes Plus	0.110	70.02
Petrochemical Feedstocks	0.125	71.02
Petroleum Coke	0.143	102.41
Special Naphtha	0.125	72.34
Unfinished Oils	0.139	74.54
Heavy Gas Oils	0.148	74.92
Lubricants	0.144	74.27
Motor Gasoline	0.125	70.22
Aviation Gasoline	0.120	69.25
Kerosene-Type Jet Fuel	0.135	72.22
Asphalt and Road Oil	0.158	75.36
Crude Oil	0.138	74.54
Other fuels-solid	mmBtu/short ton	kg CO₂/mmBtu
Municipal Solid Waste	9.95 ³	90.7
Tires	28.00	85.97
Plastics	38.00	75.00
Petroleum Coke	30.00	102.41
Other fuels—gaseous	mmBtu/scf	kg CO₂/mmBtu
Blast Furnace Gas	0.092×10^{-3}	274.32
Coke Oven Gas	0.599×10^{-3}	46.85
Propane Gas	2.516×10^{-3}	61.46
Fuel Gas ⁴	1.388×10^{-3}	59.00
Biomass fuels—solid	mmBtu/short ton	kg CO₂/mmBtu
Wood and Wood Residuals (dry basis)5	17.48	93.80
Agricultural Byproducts	8.25	118.17
Peat	8.00	111.84
Solid Byproducts	10.39	105.51
Biomass fuels—gaseous	mmBtu/scf	kg CO₂/mmBtu
Landfill Gas	0.485×10^{-3}	52.07
Other Biomass Gases	0.655×10^{-3}	52.07
Biomass Fuels—Liquid	mmBtu/gallon	kg CO₂/mmBtu
Ethanol	0.084	68.44
Biodiesel (100%)	0.128	73.84
Rendered Animal Fat	0.125	71.06
Vegetable Oil	0.120	81.55

¹ The HHV for components of LPG determined at 60 °F and saturation pressure with the exception of ethylene.

² Ethylene HHV determined at 41 °F (5 °C) and saturation pressure.

³ Use of this default HHV is allowed only for: (a) Units that combust MSW, do not generate steam, and are allowed to use Tier 1; (b) units that derive no more than 10 percent of their annual heat input from MSW and/or tires; and (c) small batch incinerators that combust no more than 1,000 tons of MSW per year.

⁴ Reporters subject to subpart X of this part that are complying with § 98.243(d) or subpart Y of this part may only use the default HHV and the default CO2 emission factor for fuel gas combustion under the conditions prescribed in § 98.243(d)(2)(i) and (d)(2)(ii) and § 98.252(a)(1) and (a)(2), respectively. Otherwise, reporters subject to subpart X or subpart Y shall use either Tier 3 (Equation C-5) or Tier 4.

⁵ Use the following formula to calculate a wet basis HHV for use in Equation C-1:

$$HHV_w = ((100 - M)/100) * HHV_d$$

where

 HHV_w = wet basis HHV, M = moisture content (percent) and HHV_d = dry basis HHV from Table C-1.

[74 FR 56374, Oct. 30, 2009, as amended at 75 FR 79153, Dec. 17, 2010; 78 FR 71950, Nov. 29, 2013]

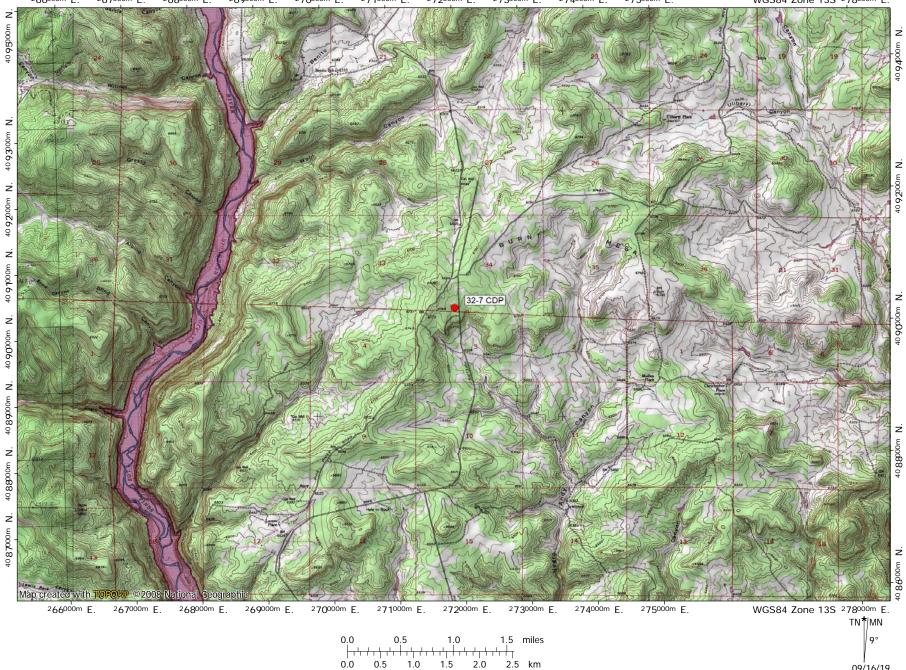
Section 8

Map(s)

<u>A map</u> such as a 7.5 minute topographic quadrangle showing the exact location of the source. The map shall also include the following:

The UTM or Longitudinal coordinate system on both axes	An indicator showing which direction is north
A minimum radius around the plant of 0.8km (0.5 miles)	Access and haul roads
Topographic features of the area	Facility property boundaries
The name of the map	The area which will be restricted to public access
A graphical scale	

Please see the following page(s).



²66^{000m} E. WGS84 Zone 13S 278000m E.

09/16/19

Section 9

Proof of Public Notice

(for NSR applications submitting under 20.2.72 or 20.2.74 NMAC) (This proof is required by: 20.2.72.203.A.14 NMAC "Documentary Proof of applicant's public notice")

□ I have read the AQB "Guidelines for Public Notification for Air Quality Permit Applications" This document provides detailed instructions about public notice requirements for various permitting actions. It also provides public notice examples and certification forms. Material mistakes in the public notice will require a re-notice before issuance of the permit.

Unless otherwise allowed elsewhere in this document, the following items document proof of the applicant's Public Notification. Please include this page in your proof of public notice submittal with checkmarks indicating which documents are being submitted with the application.

New Permit and Significant Permit Revision public notices must include all items in this list.

Technical Revision public notices require only items 1, 5, 9, and 10.

Per the Guidelines for Public Notification document mentioned above, include:

- 1. \Box A copy of the certified letter receipts with post marks (20.2.72.203.B NMAC).
- 2. □ A list of the places where the public notice has been posted in at least four publicly accessible and conspicuous places, including the proposed or existing facility entrance. (e.g: post office, library, grocery, etc.).
- 3. \Box A copy of the property tax record (20.2.72.203.B NMAC).
- 4. \Box A sample of the letters sent to the owners of record.
- 5. \Box A sample of the letters sent to counties, municipalities, and Indian tribes.
- 6. \Box A sample of the public notice posted and a verification of the local postings.
- 7. \Box A table of the noticed citizens, counties, municipalities and tribes and to whom the notices were sent in each group.
- 8. 🗆 A copy of the public service announcement (PSA) sent to a local radio station and documentary proof of submittal.
- 9. A copy of the <u>classified or legal</u> ad including the page header (date and newspaper title) or its affidavit of publication stating the ad date, and a copy of the ad. When appropriate, this ad shall be printed in both English and Spanish.
- 10. □ A copy of the <u>display</u> ad including the page header (date and newspaper title) or its affidavit of publication stating the ad date, and a copy of the ad. When appropriate, this ad shall be printed in both English and Spanish.
- 11. □ A map with a graphic scale showing the facility boundary and the surrounding area in which owners of record were notified by mail. This is necessary for verification that the correct facility boundary was used in determining distance for notifying land owners of record.

Not applicable for Title V applications.

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Section 10

Written Description of the Routine Operations of the Facility

<u>A written description of the routine operations of the facility</u>. Include a description of how each piece of equipment will be operated, how controls will be used, and the fate of both the products and waste generated. For modifications and/or revisions, explain how the changes will affect the existing process. In a separate paragraph describe the major process bottlenecks that limit production. The purpose of this description is to provide sufficient information about plant operations for the permit writer to determine appropriate emission sources.

The 32-7 CDP compresses and dehydrates pipeline quality natural gas. Natural gas is received from independent producers via gathering pipelines. The natural gas stream typically contains produced water, which is separated from the gas stream via an inlet separator. The resulting produced water is stored in above ground fixed roof storage tanks, where it is stored until offsite transport via tank truck.

The natural gas is compressed for pipeline transmission using compressors driven by the natural gas-fired reciprocating internal combustion engines. The natural gas stream is then routed to the triethylene glycol (TEG) dehydrators, which further dehydrate the gas stream. The TEG solution comes into contact with the natural gas and removes the water and some hydrocarbons. The rich TEG solution is regenerated by boiling off the water and hydrocarbons and reclaiming the glycol.

Storage tanks are used to store lube oil and used oil, TEG, produced water, waste water, antifreeze, and solvent. Waste products are hauled off-site as required.

There are no process bottlenecks that limit production.

Other emission sources include: startups, shutdowns and routine maintenance (SSM) from the compressors and piping (Unit SSM), and fugitive emissions from process piping (valves, flanges, seals, etc.).

The facility is authorized to operate continuously.

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Section 11

Source Determination

(Source submitting under 20.2.70, 20.2.72, 20.2.73, and 20.2.74 NMAC)

Sources applying for a construction permit, PSD permit, or operating permit shall evaluate surrounding and/or associated sources (including those sources directly connected to this source for business reasons) and complete this section. Responses to the following questions shall be consistent with the Air Quality Bureau's permitting guidance, <u>Single Source Determination</u> <u>Guidance</u>, which may be found on the Applications Page in the Permitting Section of the Air Quality Bureau website.

Typically, buildings, structures, installations, or facilities that have the same SIC code, that are under common ownership or control, and that are contiguous or adjacent constitute a single stationary source for 20.2.70, 20.2.72, 20.2.73, and 20.2.74 NMAC applicability purposes. Submission of your analysis of these factors in support of the responses below is optional, unless requested by NMED.

A. Identify the emission sources evaluated in this section (list and describe):

32-7 Central Delivery Point (CDP) natural gas compression and dehydration facility

B. Apply the 3 criteria for determining a single source:

<u>SIC</u> <u>Code</u>: Surrounding or associated sources belong to the same 2-digit industrial grouping (2-digit SIC code) as this facility, <u>OR</u> surrounding or associated sources that belong to different 2-digit SIC codes are support facilities for this source.

🗹 Yes 🗆 No

<u>Common</u> <u>Ownership</u> or <u>Control</u>: Surrounding or associated sources are under common ownership or control as this source.

🗹 Yes 🗆 No

Contiguous or Adjacent: Surrounding or associated sources are contiguous or adjacent with this source.

🗹 Yes 🗆 No

C. Make a determination:

- ✓ The source, as described in this application, constitutes the entire source for 20.2.70, 20.2.72, 20.2.73, or 20.2.74 NMAC applicability purposes. If in "A" above you evaluated only the source that is the subject of this application, all "YES" boxes should be checked. If in "A" above you evaluated other sources as well, you must check AT LEAST ONE of the boxes "NO" to conclude that the source, as described in the application, is the entire source for 20.2.70, 20.2.72, 20.2.72, 20.2.73, and 20.2.74 NMAC applicability purposes.
- □ The source, as described in this application, <u>does not</u> constitute the entire source for 20.2.70, 20.2.72, 20.2.73, or 20.2.74 NMAC applicability purposes (A permit may be issued for a portion of a source). The entire source consists of the following facilities or emissions sources (list and describe):

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Section 12.A

PSD Applicability Determination for All Sources

(Submitting under 20.2.72, 20.2.74 NMAC)

<u>A PSD applicability determination for all sources</u>. For sources applying for a significant permit revision, apply the applicable requirements of 20.2.74.AG and 20.2.74.200 NMAC and to determine whether this facility is a major or minor PSD source, and whether this modification is a major or a minor PSD modification. It may be helpful to refer to the procedures for Determining the Net Emissions Change at a Source as specified by Table A-5 (Page A.45) of the <u>EPA New Source Review</u> <u>Workshop Manual</u> to determine if the revision is subject to PSD review.

- A. This facility is:
 - \square a minor PSD source before and after this modification (if so, delete C and D below).
 - \square a major PSD source before this modification. This modification will make this a PSD minor source.
 - \Box an existing PSD Major Source that has never had a major modification requiring a BACT analysis.
 - an existing PSD Major Source that has had a major modification requiring a BACT analysis
 - a new PSD Major Source after this modification.
- B. This facility [is or is not] one of the listed 20.2.74.501 Table I PSD Source Categories. The "project" emissions for this modification are [significant or not significant]. [Discuss why.] The "project" emissions listed below [do or do not] only result from changes described in this permit application, thus no emissions from other [revisions or modifications, past or future] to this facility. Also, specifically discuss whether this project results in "de-bottlenecking", or other associated emissions resulting in higher emissions. The project emissions (before netting) for this project are as follows [see Table 2 in 20.2.74.502 NMAC for a complete list of significance levels]:
 - a. NOx: XX.X TPY
 - b. CO: XX.X TPY
 - c. VOC: XX.X TPY
 - d. SOx: XX.X TPY
 - e. PM: XX.X TPY
 - f. PM10: XX.X TPY
 - g. PM2.5: XX.X TPY
 - h. Fluorides: XX.X TPY
 - i. Lead: XX.X TPY
 - j. Sulfur compounds (listed in Table 2): XX.X TPY
 - k. GHG: XX.X TPY
- C. Netting [is required, and analysis is attached to this document.] OR [is not required (project is not significant)] OR [Applicant is submitting a PSD Major Modification and chooses not to net.]
- D. BACT is [not required for this modification, as this application is a minor modification.] OR [required, as this application is a major modification. List pollutants subject to BACT review and provide a full top down BACT determination.]
- E. If this is an existing PSD major source, or any facility with emissions greater than 250 TPY (or 100 TPY for 20.2.74.501 Table 1 PSD Source Categories), determine whether any permit modifications are related, or could be considered a single project with this action, and provide an explanation for your determination whether a PSD modification is triggered.

Not applicable for Title V applications.

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Section 12.B

Special Requirements for a PSD Application

(Submitting under 20.2.74 NMAC)

<u>**Prior**</u> to Submitting a PSD application, the permittee shall:

- □ Submit the BACT analysis for review prior to submittal of the application. No application will be ruled complete until the final determination regarding BACT is made, as this determination can ultimately affect information to be provided in the application. A pre-application meeting is recommended to discuss the requirements of the BACT analysis.
- □ Submit a modeling protocol prior to submitting the permit application. [Except for GHG]
- □ Submit the monitoring exemption analysis protocol prior to submitting the application. [Except for GHG]

For PSD applications, the permittee shall also include the following:

- Documentation containing an analysis on the impact on visibility. [Except for GHG]
- Documentation containing an analysis on the impact on soil. [Except for GHG]
- Documentation containing an analysis on the impact on vegetation, including state and federal threatened and endangered species. **[Except for GHG]**
- Documentation containing an analysis on the impact on water consumption and quality. [Except for GHG]
- Documentation that the federal land manager of a Class I area within 100 km of the site has been notified and provided a copy of the application, including the BACT and modeling results. The name of any Class I Federal area located within one hundred (100) kilometers of the facility.

Not applicable for Title V applications.

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Section 13

Determination of State & Federal Air Quality Regulations

This section lists each state and federal air quality regulation that may apply to your facility and/or equipment that are stationary sources of regulated air pollutants. Not all state and federal air quality regulations are included in this list. Go to the Code of Federal Regulations (CFR) or to the Air Quality Bureau's regulation page to see the full set of air quality regulations.

Required Information for Specific Equipment:

For regulations that apply to specific source types, in the 'Justification' column **provide any information needed to determine if the regulation does or does not apply**. For example, to determine if emissions standards at 40 CFR 60, Subpart IIII apply to your three identical stationary engines, we need to know the construction date as defined in that regulation; the manufacturer date; the date of reconstruction or modification, if any; if they are or are not fire pump engines; if they are or are not emergency engines as defined in that regulation; their site ratings; and the cylinder displacement.

Required Information for Regulations that Apply to the Entire Facility:

See instructions in the 'Justification' column for the information that is needed to determine if an 'Entire Facility' type of regulation applies (e.g. 20.2.70 or 20.2.73 NMAC).

Regulatory Citations for Regulations That Do Not, but Could Apply:

If there is a state or federal air quality regulation that does not apply, but you have a piece of equipment in a source category for which a regulation has been promulgated, you must **provide the low level regulatory citation showing why your piece of equipment is not subject to or exempt from the regulation. For example** if you have a stationary internal combustion engine that is not subject to 40 CFR 63, Subpart ZZZZ because it is an existing 2 stroke lean burn stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions, your citation would be 40 CFR 63.6590(b)(3)(i). We don't want a discussion of every non-applicable regulation, but if it is possible a regulation could apply, explain why it does not. For example, if your facility is a power plant, you do not need to include a citation to show that 40 CFR 60, Subpart OOO does not apply to your non-existent rock crusher.

Regulatory Citations for Emission Standards:

For each unit that is subject to an emission standard in a source specific regulation, such as 40 CFR 60, Subpart OOO or 40 CFR 63, Subpart HH, include the low level regulatory citation of that emission standard. Emission standards can be numerical emission limits, work practice standards, or other requirements such as maintenance. Here are examples: a glycol dehydrator is subject to the general standards at 63.764C(1)(i) through (iii); an engine is subject to 63.6601, Tables 2a and 2b; a crusher is subject to 60.672(b), Table 3 and all transfer points are subject to 60.672(e)(1)

Federally Enforceable Conditions:

All federal regulations are federally enforceable. All Air Quality Bureau State regulations are federally enforceable except for the following: affirmative defense portions at 20.2.7.6.B, 20.2.7.110(B)(15), 20.2.7.11 through 20.2.7.113, 20.2.7.115, and 20.2.7.116; 20.2.37; 20.2.42; 20.2.43; 20.2.62; 20.2.63; 20.2.86; 20.2.89; and 20.2.90 NMAC. Federally enforceable means that EPA can enforce the regulation as well as the Air Quality Bureau and federally enforceable regulations can count toward determining a facility's potential to emit (PTE) for the Title V, PSD, and nonattainment permit regulations.

INCLUDE ANY OTHER INFORMATION NEEDED TO COMPLETE AN APPLICABILITY DETERMINATION OR THAT IS RELEVENT TO YOUR FACILITY'S NOTICE OF INTENT OR PERMIT.

EPA Applicability Determination Index for 40 CFR 60, 61, 63, etc: <u>http://cfpub.epa.gov/adi/</u>

1

State Regulations

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Applicable state requirements are embodied in the New Mexico SIP, the New Mexico Administrative Code (NMAC), and the terms and conditions of any preconstruction permits issued pursuant to regulations promulgated through rulemaking under Title I of the CAA.

STATE REGU- LATIONS CITATION	Title	Applies? Enter Yes or No	Unit(s) or Facility	JUSTIFICATION:
20.2.1 NMAC	General Provisions	Yes	Facility	This regulation is applicable because it establishes procedures for protecting confidential information, procedures for seeking a variance, NMAQB's authority to require sampling equipment, severability, and the effective date for conformance with the NMACs, and prohibits the violation of other requirements in attempting to comply with the NMACs.
				Although this regulation is applicable, it does not impose any specific requirements.
20.2.3 NMAC	Ambient Air Quality Standards NMAAQS	Yes	Facility	This is a State Implementation Plan (SIP) approved regulation that limits the maximum allowable concentrations of Total Suspended Particulates, Sulfur Compounds, Carbon Monoxide and Nitrogen Dioxide.
20.2.7 NMAC	Excess Emissions	Yes	Facility	This regulation is applicable because it prohibits excess emissions unless proper notification procedures are followed.
20.2.8 NMAC	Emissions Leaving New Mexico	Yes	Facility	This regulation is applicable because it establishes prohibitions on the release of pollutants that cross New Mexico State boundaries.
20.2.14 NMAC	Particulate Emissions from Coal Burning Equipment	No	N/A	This regulation is not applicable because the facility does not burn coal (see 20.2.14.5 NMAC).
20.2.18 NMAC	Oil Burning Equipment - Particulate Matter	No	N/A	This regulation is not applicable because the facility does not burn oil (see 20.2.18.5 NMAC).
20.2.31 NMAC	Coal Burning Equipment – Sulfur Dioxide	No	N/A	This regulation is not applicable because the facility does not burn coal (see 20.2.31.6 NMAC).
20.2.32 NMAC	Coal Burning Equipment – Nitrogen Dioxide,	No	N/A	This regulation is not applicable because the facility does not burn coal (see 20.2.32.6 NMAC).
20.2.33 NMAC	Gas Burning Equipment - Nitrogen Dioxide	No	N/A	This regulation is not applicable because the facility is not equipped with external gas burning equipment which have heat input rates exceeding the trigger level (one million MMBtu/year) established by the regulation (see 20.2.33.108 NMAC).
20.2.34 NMAC	Oil Burning Equipment: NO ₂	No	N/A	This regulation is not applicable because the facility does not burn oil (see 20.2.34.6 NMAC).
20.2.35 NMAC	Natural Gas Processing Plant – Sulfur	No	N/A	This regulation is not applicable because the facility is not a natural gas processing plant (see 20.2.35.6 NMAC).
20.2.38 NMAC	Hydrocarbon Storage Facility	No	N/A	This regulation is not applicable because the facility does not store hydrocarbons containing hydrogen sulfide, nor is there a tank battery storing hydrocarbon liquids with a capacity greater than or equal to 65,000 gallons (see 20.2.38.112 NMAC).
20.2.39 NMAC	Sulfur Recovery Plant - Sulfur	No	N/A	This regulation is not applicable because the facility is not equipped with a sulfur recovery plant (see 20.2.39.6 NMAC).

Table for STATE REGULATIONS:

STATE REGU- LATIONS CITATION	Title	Applies? Enter Yes or No	Unit(s) or Facility	JUSTIFICATION:	
20.2.50 NMAC	Oil and Gas Sector – Ozone Precursor Pollutants	Yes	Engines 1-, 13, 15, 16, & 18-23; Reciprocating compressor seals; F1 Fugitive emissions; Glycol dehydrators 9-12, 24 & 25; Pig receiving: and Pneumatic controllers & pumps	This regulation establishes emission standards for volatile organic compounds (VOC) and oxides of nitrogen (NOx) for oil and gas production processing, compression, and transmission sources. 20.2.50 NMAC subparts: 113 – Engines and Turbines 114 – Compressor Seals 115 – Control Devices and Closed Vent Systems 116 – Equipment Leaks and Fugitive Emissions 117 – Natural Gas Well Liquid Unloading 118 – Glycol Dehydrators 119 – Heaters 120 – Hydrocarbon Liquid Transfers 121 – Pig Launching and Receiving 122 – Pneumatic Controllers and Pumps 123 – Storage Vessels 124 – Well Workovers 125 – Small Business Facilities 126 – Produced Water Management Units 127 – Flowback Vessels and Preproduction Operations This regulation is applicable because the facility is equipped with affecte equipment as defined by the regulation, including engines, reciprocatin compressor seals, equipment leaks and fugitive emissions, glyco dehydrators, and pneumatic controllers & pumps.	
20.2.61.109 NMAC	Smoke & Visible Emissions	Yes	RICE 1-8, 13, 15, 16, and 18-23; Reboilers 9b- 12b, 24b, & 25b	dehydrators, and pneumatic controllers & pumps. This regulation is applicable because the facility is equipped with stationary combustion sources. Emissions from these combustion sources are limited to less than 20% opacity (see 20.2.61.109 NMAC). The regulation is not applicable to Title V insignificant heaters (see 20.2.61.111.D NMAC).	
20.2.70 NMAC	Operating Permits	Yes	Facility	This regulation is applicable because the facility is a major source of NOx, CO, VOC, and HAP emissions (see 20.2.70.200 NMAC).	
20.2.71 NMAC	Operating Permit Fees	Yes	Facility	This regulation is applicable because the facility is subject to 20.2.70 NMAC (see 20.2.71.6 NMAC).	
20.2.72 NMAC	Construction Permits	Yes	Facility	This regulation is applicable because the facility has potential emission rates (PER) greater than 10 pph or 25 tpy for pollutants subject to a state or federal ambient air quality standards (does not include VOCs or HAPs).	
20.2.73 NMAC	NOI & Emissions Inventory Requirements	Yes	Facility	The Notice of Intent portion of this regulation (20.2.73.200.A &.B NMAC) was fulfilled with the construction permit application for the facility submitted under 20.2.72 NMAC. The emissions inventory portion of this regulation is applicable based on the facility is a Title V major source (20.2.73.300.B(1) & (2)).	
20.2.74 NMAC	Permits – Prevention of Significant Deterioration (PSD)	No	N/A	This regulation is not applicable because the facility is not a PSD major source.	
20.2.75 NMAC	Construction Permit Fees	Yes	Facility	This regulation is applicable because it establishes the fee schedule associated with construction permit applications (see 20.2.75.6 NMAC). The facility has a construction permit.	

STATE REGU- LATIONS CITATION	Title	Applies? Enter Yes or No	Unit(s) or Facility	JUSTIFICATION:
20.2.77 NMAC	New Source Performance	No	Potentially applicable to RICE 1, 5, 8, 16, 18, 22 & 23	This regulation is not applicable because there are no installed equipment that are subject to an NSPS. The regulation adopts by reference the federal NSPS codified in 40 CFR 60 (see 20.2.77.6 NMAC). The facility is potentially subject to 40 CFR 60 if affected sources are installed. The applicability or non-applicability of the subpart to units 1, 5, 8, 16, 18, 22 and 23 will be determined upon installation.
20.2.78 NMAC	Emission Standards for HAPS	No	N/A	This regulation is not applicable because it incorporates by reference the NESHAPs codified under 40 CFR 61 (see 20.2.78.6 NMAC). The facility is not subject to 40 CFR 61.
20.2.79 NMAC	Permits – Nonattainment Areas	No	N/A	This regulation is not applicable because the facility is neither located in nor has a significant impact on a nonattainment area (see 20.2.79.6 NMAC).
20.2.80 NMAC	Stack Heights	No	N/A	This regulation is not applicable because it establishes guidelines for the selection of an appropriate stack height for the purpose of atmospheric dispersion modeling (see 20.2.80.6 NMAC); however, it only imposes those requirements when modeling is required as a part of the application. This application does not require modeling.
20.2.82 NMAC	MACT Standards for Source Categories of HAPS	Yes	TEG dehydrators 9a/b-12a/b, 24a/b & 25a/b. Potentially applicable to RICE 1, 5, 8, 16, 18, 22 & 23	This regulation is applicable because it adopts by reference the federal MACT Standards for source categories codified in 40 CFR 63 (see 20.2.82.6 NMAC). The facility TEG dehydrators are subject to 40 CFR 63, subparts A and HH. RICE units 1, 5, 8, 16, 18, 22 & 23 are not installed. The applicability or non- applicability of subpart ZZZZ to units 5, 8, 16, 18, 22 and 23 will be determined upon installation.

Federal Regulations

Federal standards and requirements are embodied in Title 40 (Protection of the Environment), Subchapter C (Air Programs) of the CFR, Parts 50 through 99.

FEDERAL REGULATIONS APPLICABILITY CHECKLIST

FEDERAL REGU- LATIONS CITATION	Title	Applies? Enter Yes or No	Unit(s) or Facility	JUSTIFICATION:	
40 CFR 50	NAAQS	Yes	Facility	This regulation is applicable because it applies to all sources in the state of New Mexico.	
40 CFR 52	Approval and Promulgation of Implementation Plans	No	N/A	40 CFR 52.21 <i>Prevention of Significant Deterioration of Air Quality</i> is not applicable because the facility is not a major Prevention of Significant Deterioration source. The remainder of 40 CFR 52 is not applicable because it addresses approval and promulgation of implementation plans.	
NSPS 40 CFR 60, Subpart A	General Provisions	No	N/A	This regulation is not applicable because none of the other 40 CFR Part 60 subparts are applicable.	
NSPS 40 CFR 60, Subpart K	Standards of Performance for Storage Vessels for Petroleum Liquids for which Construction, Reconstruction, or Modification Commenced After June 11, 1973, and Prior to May 19, 1978	No	N/A	This regulation is not applicable because the petroleum liquids storag tanks at the facility have capacities less than the minimum applicability threshold capacity of 40,000 gallons (see §60.110(a)).	
NSPS 40 CFR 60, Subpart Ka	Standards of Performance for Storage Vessels for Petroleum Liquids for which Construction, Reconstruction, or Modification Commenced After May 18, 1978, and Prior to July 23, 1984	No	N/A	This regulation is not applicable because the storage tanks at the facility have capacities less than the minimum applicability threshold capacity of 40,000 gallons (see §60.110a(a)).	
NSPS 40 CFR 60, Subpart Kb	Standards of Performance for Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels) for Which Construction, Reconstruction, or Modification Commenced After July 23, 1984	No	N/A	This regulation is not applicable because all storage tanks at the facility have capacities less than the minimum applicability threshold capacity of 75 cubic meters (19,812 gallons), or they have a capacity between 75 and 151 cubic meters (40,000 gallons) and store a liquid with a maximum true vapor pressure less than 15.0 kPa (2.2 psi) (see §60.110b(a) & §60.110b(b))).	

FEDERAL REGU- LATIONS CITATION	Title	Applies? Enter Yes or No	Unit(s) or Facility	JUSTIFICATION:
NSPS 40 CFR 60, Subpart KKK	Standards of Performance for Equipment Leaks of VOC from Onshore Gas Plants	No	N/A	This regulation is not applicable because the facility is not an onshore natural gas processing plant as defined by the subpart (see §60.630(a)(1)). Natural gas processing plant (gas plant) means any processing site engaged in the extraction of natural gas liquids from field gas, fractionation of mixed natural gas liquids to natural gas products, or both (see §60.631).
NSPS 40 CFR 60, Subpart LLL	Standards of Performance for Onshore Natural Gas Processing: SO ₂ Emissions	No	N/A	This regulation is not applicable because the facility is not a natural gas processing plant as defined by the subpart. It is not equipped with a sweetening unit (see $60.640(a)$).
NSPS 40 CFR 60, Subpart IIII	Standards of Performance for Stationary Compression Ignition Internal Combustion Engines	No	N/A	This regulation is not applicable because the facility is not equipped with stationary compression ignition (CI) internal combustion engines (ICE) that commenced construction after July 11, 2005 and were manufactured after April 1, 2006 (see §60.4200(a)(2)(i)). For the purpose of this subpart, construction commences on the date the engine is ordered by the owner or operator (see §60.4200(a)).
NSPS 40 CFR 60, Subpart JJJJ	Standards of Performance for Stationary Spark Ignition Internal Combustion Engines	No	Potentially applicable to RICE units 1, 5, 8, 16, 18, 22 & 23	 This regulation is not applicable because the facility is not equipped with spark ignition (SI) internal combustion engines (ICE) constructed, modified, or reconstructed after June 12, 2006. Units 2-4, 6, 7, 13, 15, and 19-21 were constructed prior to the applicability date and have not been modified or reconstructed. The applicability or non-applicability of the subpart to units 1, 5, 8, 16, 18, 22 and 23 will be determined upon installation. See the definitions of construction, modification, and reconstruction referenced in Subpart OOOO, below.
NSPS 40 CFR 60, Subpart OOOO	Standards of Performance for Crude Oil and Natural Gas Production, Transmission, and Distribution for which Construction, Modification or Reconstruction Commenced After August 23, 2011 and On or Before September 18, 2015	No	N/A	This regulation is not applicable because the facility is not equipped with "affected" sources that commenced construction, modification or reconstruction after August 23, 2011 and on or before September 18, 2015: gas wells, centrifugal or reciprocating compressors, pneumatic controllers, and storage vessels (see §60.5365). Note that the facility is not a natural gas processing plant as defined by the subpart (see §60.5430). "Commenced" construction means a continuous program of fabrication, erection or installation (see §60.2). "Modification" means any physical change in or change in the method of operation of an existing facility which increases emissions or results in new emissions (see §60.2). The following, by themselves, are not modifications: routine maintenance, repair or replacement, production increase without capital expenditure, increase in hours of operation, addition of emission controls, or the relocation or change in ownership of an existing facility (see §60.14). "Reconstruction" means the replacement of components of an existing facility such that the fixed capital cost of the new components exceeds 50 % of the fixed capital cost means the capital needed to provide all the depreciable components (see §60.15).

FEDERAL REGU- LATIONS CITATION	Title	Applies? Enter Yes or No	Unit(s) or Facility	JUSTIFICATION:	
NSPS 40 CFR 60, Subpart OOOOa	Standards of Performance for Crude Oil and Natural Gas Facilities for	No	N/A	This regulation is not applicable because the facility is not equipped with "affected" sources that commenced construction, modification or reconstruction after September 18, 2015: gas wells, centrifugal or reciprocating compressors, pneumatic controllers, storage vessels, sweetening units, pneumatic pumps, and equipment leaks (see §60.5365a).	
	which Construction, Modification or			In general, this regulation may apply if existing affected equipment is replaced or new affected equipment is installed.	
	Reconstruction Commenced After September 18, 2015			In particular, this regulation will apply to fugitive emissions components at the facility if any engines and compressors are installed. Fugitive components monitoring is required if a compressor station is modified. For the purpose of fugitive components monitoring as required by this subpart, modification of a compressor station is the addition of a compressor or replacement of a compressor with a larger unit (greater total horsepower) (see §60.5365a(j)).	
				Note that the facility is not a natural gas processing plant as defined by the subpart (see §60.5430a).	
				See the definitions of construction, modification, and reconstruction referenced in Subpart OOOO, above.	
NESHAP 40 CFR 61, Subpart A	General Provisions	No	N/A	This regulation is not applicable because the facility is not subject to any requirements under 40 CFR Part 61 (see §61.01(c)).	
NESHAP 40 CFR 61,	National Emission Standards for	No	N/A	This regulation is not applicable because none of the listed equipment at the facility is in VHAP service.	
Subpart V	Equipment Leaks (Fugitive Emission Sources)			The provisions of this subpart apply to each of the following sources that are <i>intended</i> to operate in volatile hazardous air pollutant (VHAP) service: pumps, compressors, pressure relief devices, sampling connection systems, open-ended valves or lines, valves, connectors, surge control vessels, bottoms receivers, and control devices or systems required by the subpart (see §61.240(a)). "VHAP service" means a piece of equipment either contains or contacts a fluid (liquid or gas) that is at least 10 percent by weight of VHAP. "VHAP" means a substance regulated under this subpart for which a standard for equipment leaks of the substance has been promulgated (see §61.241).	
MACT 40 CFR 63, Subpart A	General Provisions	Yes	TEG dehydrators 9a/b-12a/b, 24a/b & 25a/b	This regulation is applicable because 40 CFR 63 subpart HH applies to the TEG dehydrators (see §63.1(b)).	
MACT 40 CFR 63, Subpart HH	National Emission Standards for Hazardous Air Pollutants For Oil and Natural Gas Production Facilities	Yes	TEG dehydrators 9a/b-12a/b, 24a/b & 25a/b	This regulation is applicable because the facility is equipped with affected equipment subject to 40 CFR 63, subpart HH. As the facility is a production field facility located prior to the point of custody transfer, only HAP emissions from glycol dehydration units and storage vessels (crude oil tanks, condensate tanks, intermediate hydrocarbon liquid tanks, and produced water tanks) are aggregated for a major source determination (see §63.761). As defined under the subpart, the facility is an area source of HAP. The facility is located in an area that is not within an UA plus offset and UC boundary (as defined in §63.761). At a HAP area source, the only affected unit is each dehydration unit (see §63.760(b)(2)). Under §63.764(e)(1)(ii), the owner or operator of an affected area source [TEG dehydrator] with actual average benzene emissions from the process vent to the atmosphere of less than 0.90 megagrams per year (~1 tpy) is exempt from the operational, recordkeeping and notification requirements in §63.764(d), provided that documentation of the exemption determination is maintained as required in §63.774(d)(1).	

FEDERAL REGU- LATIONS CITATION	Title	Applies? Enter Yes or No	Unit(s) or Facility	JUSTIFICATION:	
MACT 40 CFR 63, Subpart HHH	National Emission Standards for Hazardous Air Pollutants From Natural Gas Transmission and Storage Facilities	No	N/A	This regulation is not applicable because the facility is not a natural gas transmission and storage facility as defined by the subpart. A compressor station that transports natural gas prior to the point of custody transfer or to a natural gas processing plant (if present) are not considered a part of the natural gas transmission and storage source category (see §63.1270(a)).	
MACT 40 CFR 63, Subpart ZZZZ	National Emissions Standards for Hazardous Air Pollutants for Stationary Reciprocating Internal Combustion Engines (RICE MACT)	No	Potentially applicable to RICE units 1, 5, 8, 16, 18, 22 & 23	This regulation is potentially applicable if the facility is equipped with affected sources. The station is an major HAP source as defined by the subpart. For production field facilities, HAP emissions from engines, turbines, dehydrators, and storage vessels with the potential for flash emissions are aggregated for the HAP major source determination (see §63.6675). Units 2-4, 6, 7, 13, 15, and 19-21 are 4-stroke, lean burn (4SLB) spark ignition (SI) RICE, each with a site rating of more than 500 hp, and constructed prior to December 19, 2002. Under §63.6590(b)(3)(ii), existing 4SLB stationary RICE with a site rating of more than 500 hp located at a major source of HAP do not have to meet the requirements of the subpart and of subpart A, including initial notification requirements. The applicability or non-applicability of the subpart to units 1, 5, 8, 16, 18, 22 and 23 will be determined upon installation.	
MACT 40 CFR 63, Subpart DDDDD	National Emission Standards for Hazardous Air Pollutants for Major Industrial, Commercial, and Institutional Boilers & Process Heaters	No	N/A	This regulation is not applicable both because the facility is an area HAP source as defined by the subpart (see §63.7480) and is not equipped with boilers and process heaters. Since the facility is a natural gas production facility, only HAP emissions from dehydrators and storage vessels with the potential for flash emissions are aggregated for a major source determination (see §63.7575).	
MACT 40 CFR 63, Subpart JJJJJJ	National Emission Standards for Hazardous Air Pollutants for Industrial, Commercial, and Institutional Boilers at Area Sources	No	N/A	This regulation is not applicable because the facility is not equipped with industrial, commercial, or institutional boilers.	
40 CFR 64	Compliance Assurance Monitoring	No	N/A	This regulation is not applicable because no equipment at the facility requires a control device to achieve compliance with emission limits or standards where pre control emissions equal or exceed the major source threshold (100 tons per year). (see §64.2(a)).	
40 CFR 68	Chemical Accident Prevention	No	N/A	This regulation is not applicable because the facility does not store any of the identified toxic and flammable substances in quantities exceeding the applicability thresholds (see §68.10(a), §68.115(a), and §68.130 Tables 1-4).	
40 CFR 70	State Operating Permit Programs	No	N/A	This regulation is not applicable, as the requirements associated with Title V are delegated to the State of New Mexico and implemented under 20 NMAC 2.70.	
40 CFR 82	Protection of Stratospheric Ozone	No	N/A	This regulation is not applicable because the facility does not produce, transform, destroy, import, or export ozone-depleting substances (see §82.1(b),); does not service motor vehicle air conditioning units (see §82.30(b)); and does not sell, distribute, or offer for sale or distribution any product that contains ozone-depleting substances (see §82.64).	

Operational Plan to Mitigate Emissions

(Submitting under 20.2.70, 20.2.72, 20.2.74 NMAC)

- ✓ Title V Sources (20.2.70 NMAC): By checking this box and certifying this application the permittee certifies that it has developed an <u>Operational Plan to Mitigate Emissions During Startups</u>, <u>Shutdowns</u>, <u>and Emergencies</u> defining the measures to be taken to mitigate source emissions during startups, shutdowns, and emergencies as required by 20.2.70.300.D.5(f) and (g) NMAC. This plan shall be kept on site to be made available to the Department upon request. This plan should not be submitted with this application.
- ✓ NSR (20.2.72 NMAC), PSD (20.2.74 NMAC) & Nonattainment (20.2.79 NMAC) Sources: By checking this box and certifying this application the permittee certifies that it has developed an <u>Operational Plan to Mitigate Source Emissions</u> <u>During Malfunction, Startup, or Shutdown</u> defining the measures to be taken to mitigate source emissions during malfunction, startup, or shutdown as required by 20.2.72.203.A.5 NMAC. This plan shall be kept on site to be made available to the Department upon request. This plan should not be submitted with this application.
- ☑ Title V (20.2.70 NMAC), NSR (20.2.72 NMAC), PSD (20.2.74 NMAC) & Nonattainment (20.2.79 NMAC) Sources: By checking this box and certifying this application the permittee certifies that it has established and implemented a Plan to Minimize Emissions During Routine or Predictable Startup, Shutdown, and Scheduled Maintenance through work practice standards and good air pollution control practices as required by 20.2.7.14.A and B NMAC. This plan shall be kept on site or at the nearest field office to be made available to the Department upon request. This plan should not be submitted with this application.

Alternative Operating Scenarios

(Submitting under 20.2.70, 20.2.72, 20.2.74 NMAC)

Alternative Operating Scenarios: Provide all information required by the department to define alternative operating scenarios. This includes process, material and product changes; facility emissions information; air pollution control equipment requirements; any applicable requirements; monitoring, recordkeeping, and reporting requirements; and compliance certification requirements. Please ensure applicable Tables in this application are clearly marked to show alternative operating scenario.

Construction Scenarios: When a permit is modified authorizing new construction to an existing facility, NMED includes a condition to clearly address which permit condition(s) (from the previous permit and the new permit) govern during the interval between the date of issuance of the modification permit and the completion of construction of the modification(s). There are many possible variables that need to be addressed such as: Is simultaneous operation of the old and new units permitted and, if so for example, for how long and under what restraints? In general, these types of requirements will be addressed in Section A100 of the permit, but additional requirements may be added elsewhere. Look in A100 of our NSR and/or TV permit template for sample language dealing with these requirements. Find these permit templates at: https://www.env.nm.gov/aqb/permit/aqb_pol.html. Compliance with standards must be maintained during construction, which should not usually be a problem unless simultaneous operation of old and new equipment is requested.

In this section, under the bolded title "Construction Scenarios", specify any information necessary to write these conditions, such as: conservative-realistic estimated time for completion of construction of the various units, whether simultaneous operation of old and new units is being requested (and, if so, modeled), whether the old units will be removed or decommissioned, any PSD ramifications, any temporary limits requested during phased construction, whether any increase in emissions is being requested as SSM emissions or will instead be handled as a separate Construction Scenario (with corresponding emission limits and conditions, etc.

Not applicable.

Air Dispersion Modeling

- Minor Source Construction (20.2.72 NMAC) and Prevention of Significant Deterioration (PSD) (20.2.74 NMAC) ambient impact analysis (modeling): Provide an ambient impact analysis as required at 20.2.72.203.A(4) and/or 20.2.74.303 NMAC and as outlined in the Air Quality Bureau's Dispersion Modeling Guidelines found on the Planning Section's modeling website. If air dispersion modeling has been waived for one or more pollutants, attach the AQB Modeling Section modeling waiver approval documentation.
- 2) SSM Modeling: Applicants must conduct dispersion modeling for the total short term emissions during routine or predictable startup, shutdown, or maintenance (SSM) using realistic worst case scenarios following guidance from the Air Quality Bureau's dispersion modeling section. Refer to "Guidance for Submittal of Startup, Shutdown, Maintenance Emissions in Permit Applications (<u>http://www.env.nm.gov/aqb/permit/app_form.html</u>) for more detailed instructions on SSM emissions modeling requirements.
- 3) Title V (20.2.70 NMAC) ambient impact analysis: Title V applications must specify the construction permit and/or Title V Permit number(s) for which air quality dispersion modeling was last approved. Facilities that have only a Title V permit, such as landfills and air curtain incinerators, are subject to the same modeling required for preconstruction permits required by 20.2.72 and 20.2.74 NMAC.

What is the purpose of this application?	Enter an X for each purpose that applies
New PSD major source or PSD major modification (20.2.74 NMAC). See #1 above.	
New Minor Source or significant permit revision under 20.2.72 NMAC (20.2.72.219.D NMAC).	
See #1 above. Note: Neither modeling nor a modeling waiver is required for VOC emissions.	
Reporting existing pollutants that were not previously reported.	
Reporting existing pollutants where the ambient impact is being addressed for the first time.	
Title V application (new, renewal, significant, or minor modification. 20.2.70 NMAC). See #3 above.	Х
Relocation (20.2.72.202.B.4 or 72.202.D.3.c NMAC)	
Minor Source Technical Permit Revision 20.2.72.219.B.1.d.vi NMAC for like-kind unit replacements.	
Other: i.e. SSM modeling. See #2 above.	
This application does not require modeling since this is a No Permit Required (NPR) application.	
This application does not require modeling since this is a Notice of Intent (NOI) application (20.2.73 NMAC).	
This application does not require modeling according to 20.2.70.7.E(11), 20.2.72.203.A(4), 20.2.74.303, 20.2.79.109.D NMAC and in accordance with the Air Quality Bureau's Modeling Guidelines.	

Check each box that applies:

- $\hfill\square$ See attached, approved modeling waiver for all pollutants from the facility.
- $\hfill\square$ See attached, approved modeling waiver for some pollutants from the facility.
- □ Attached in Universal Application Form 4 (UA4) is a **modeling report for all** pollutants from the facility.
- $\hfill\square$ Attached in UA4 is a **modeling report for some** pollutants from the facility.
- \blacksquare No modeling is required.

Modeling was last conducted in the application submitted for construction permit 1032-M4, issued on March 23, 2004.

Compliance Test History

(Submitting under 20.2.70, 20.2.72, 20.2.74 NMAC)

To show compliance with existing NSR permit conditions, you must submit a compliance test history. The table below provides an example.

Unit No.	Test Description	Test Date
2	Compliance test for NOx and CO, in accordance with Operating Permit P195-R3, Condition A201.A	February 25, 2021
3	Compliance test for NOx and CO, in accordance with Operating Permit P195-R3, Condition A201.A	February 25, 2021
4	Compliance test for NOx and CO, in accordance with Operating Permit P195-R3, Condition A201.A	August 24, 2021
6	Compliance test for NOx and CO, in accordance with Operating Permit P195-R3, Condition A201.A	February 25, 2021
7	Compliance test for NOx and CO, in accordance with Operating Permit P195-R3, Condition A201.A & B	November 11, 2021
13	Compliance test for NOx and CO, in accordance with Operating Permit P195-R3, Condition A201.A & B	November 11, 2021
15	Compliance test for NOx and CO, in accordance with Operating Permit P195-R3, Condition A201.A & B	November 11, 2021
19	Compliance test for NOx and CO, in accordance with Operating Permit P195-R3, Condition A201.A & B	November 8, 2021
20	Compliance test for NOx and CO, in accordance with Operating Permit P195-R3, Condition A201.A & B	November 8, 2021
21	Compliance test for NOx and CO, in accordance with Operating Permit P195-R3, Condition A201.A & B	November 8, 2021

Compliance Test History Table

Engine units 1, 5, 8, 16, 18, 22 and 23 are not installed.

Addendum for Streamline Applications

Streamline Applications do not require a complete application. Submit Sections 1-A, 1-B, 1-D, 1-F, 1-G, 2-A, 2-C thru L, Sections 3 thru 8, Section 13, Section 18, Section 22, and Section 23 (Certification). Other sections may be required at the discretion of the Department. 20.2.72.202 NMAC Exemptions do not apply to Streamline sources. 20.2.72.219 NMAC revisions and modifications do not apply to Streamline sources, thus 20.2.72.219 type actions require a complete new application submittal. Please do not print sections of a streamline application that are not required.

Not applicable for Title V applications.

Requirements for Title V Program

Who Must Use this Attachment:

* Any major source as defined in 20.2.70 NMAC.

- * Any source, including an area source, subject to a standard or other requirement promulgated under Section 111 Standards of Performance for New Stationary Sources, or Section 112 Hazardous Air Pollutants, of the 1990 federal Clean Air Act ("federal Act"). Non-major sources subject to Sections 111 or 112 of the federal Act are exempt from the obligation to obtain an 20.2.70 NMAC operating permit until such time that the EPA Administrator completes rulemakings that require such sources to obtain operating permits. In addition, sources that would be required to obtain an operating permit solely because they are subject to regulations or requirements under Section 112(r) of the federal Act are exempt from the requirement to obtain an Operating Permit.
- * Any Acid Rain source as defined under title IV of the federal Act. The Acid Rain program has additional forms. See <u>http://www.env.nm.gov/aqb/index.html</u>. Sources that are subject to both the Title V and Acid Rain regulations are encouraged to submit both applications simultaneously.
- * Any source in a source category designated by the EPA Administrator ("Administrator"), in whole or in part, by regulation, after notice and comment.

19.1 - 40 CFR 64, Compliance Assurance Monitoring (CAM) (20.2.70.300.D.10.e NMAC)

Any source subject to 40CFR, Part 64 (Compliance Assurance Monitoring) must submit all the information required by section 64.7 with the operating permit application. The applicant must prepare a separate section of the application package for this purpose; if the information is already listed elsewhere in the application package, make reference to that location. Facilities not subject to Part 64 are invited to submit periodic monitoring protocols with the application to help the AQB to comply with 20.2.70 NMAC. Sources subject to 40 CFR Part 64, must submit a statement indicating your source's compliance status with any enhanced monitoring and compliance certification requirements of the federal Act.

The facility is not subject to 40 CFR, Part 64, Compliance Assurance Monitoring (CAM); consequently, a monitoring protocol is not required with this application.

19.2 - Compliance Status (20.2.70.300.D.10.a & 10.b NMAC)

Describe the facility's compliance status with each applicable requirement at the time this permit application is submitted. This statement should include descriptions of or references to all methods used for determining compliance. This statement should include descriptions of monitoring, recordkeeping and reporting requirements and test methods used to determine compliance with all applicable requirements. Refer to Section 2, Tables 2-N and 2-O of the Application Form as necessary. (20.2.70.300.D.11 NMAC) For facilities with existing Title V permits, refer to most recent Compliance Certification for existing requirements. Address new requirements such as CAM, here, including steps being taken to achieve compliance.

The facility is in compliance with all applicable requirements, as has been demonstrated by the most recent semi-annual monitoring reports and annual compliance certification. It is assumed that compliance with the Title V operating permit ensures compliance with the construction permit and New Mexico regulations.

Form-Section 19 last revised: 8/15/2011

19.3 - Continued Compliance (20.2.70.300.D.10.c NMAC)

Provide a statement that your facility will continue to be in compliance with requirements for which it is in compliance at the time of permit application. This statement must also include a commitment to comply with other applicable requirements as they come into effect during the permit term. This compliance must occur in a timely manner or be consistent with such schedule expressly required by the applicable requirement.

The facility will continue to be in compliance with applicable requirements for which it is in compliance at the time of this permit application. In addition, Harvest will, in a timely manner or consistent with such schedule expressly required by the applicable requirement, comply with other applicable requirements as they come into effect during the permit term.

19.4 - Schedule for Submission of Compliance (20.2.70.300.D.10.d NMAC)

You must provide a proposed schedule for submission to the department of compliance certifications during the permit term. This certification must be submitted annually unless the applicable requirement or the department specifies a more frequent period. A sample form for these certifications will be attached to the permit.

The submittal of compliance certifications during the five-year term of the operating permit will occur annually.

19.5 - Stratospheric Ozone and Climate Protection

In addition to completing the four (4) questions below, you must submit a statement indicating your source's compliance status with requirements of Title VI, Section 608 (National Recycling and Emissions Reduction Program) and Section 609 (Servicing of Motor Vehicle Air Conditioners).

- 1. Does your facility have any air conditioners or refrigeration equipment that uses CFCs, HCFCs or other ozonedepleting substances? Yes ☑ No
- 2. Does any air conditioner(s) or any piece(s) of refrigeration equipment contain a refrigeration charge greater than 50 lbs? Yes Z No
 (If the answer is yes, describe the type of equipment and how many units are at the facility.)
- 3. Do your facility personnel maintain, service, repair, or dispose of any motor vehicle air conditioners (MVACs) or appliances ("appliance" and "MVAC" as defined at 82. 152)? Yes ☑ No
- Cite and describe which Title VI requirements are applicable to your facility (i.e. 40 CFR Part 82, Subpart A through G). None

The facility does not produce, manufacture, transform, destroy, import, or export any stratospheric ozonedepleting substances (CFCs, HCFCs); does not maintain or service motor vehicle air conditioning units or refrigeration equipment; and does not sell, distribute, or offer for sale any product that may contain stratospheric ozone-depleting substances.

Harvest shall continue to maintain compliance with the conditions stipulated in 40 CFR 82, Subparts A-G of the Stratospheric Ozone Protection Program (Title VI of the Clean Air Act Amendments).

19.6 - Compliance Plan and Schedule

Applications for sources, which are not in compliance with all applicable requirements at the time the permit application is submitted to the department, must include a proposed compliance plan as part of the permit application package. This plan shall include the information requested below:

A. Description of Compliance Status: (20.2.70.300.D.11.a NMAC)

A narrative description of your facility's compliance status with respect to all applicable requirements (as defined in 20.2.70 NMAC) at the time this permit application is submitted to the department.

B. Compliance plan: (20.2.70.300.D.11.B NMAC)

A narrative description of the means by which your facility will achieve compliance with applicable requirements with which it is not in compliance at the time you submit your permit application package.

C. Compliance schedule: (20.2.70.300D.11.c NMAC)

A schedule of remedial measures that you plan to take, including an enforceable sequence of actions with milestones, which will lead to compliance with all applicable requirements for your source. This schedule of compliance must be at least as stringent as that contained in any consent decree or administrative order to which your source is subject. The obligations of any consent decree or administrative order are not in any way diminished by the schedule of compliance.

D. Schedule of Certified Progress Reports: (20.2.70.300.D.11.d NMAC)

A proposed schedule for submission to the department of certified progress reports must also be included in the compliance schedule. The proposed schedule must call for these reports to be submitted at least every six (6) months.

E. Acid Rain Sources: (20.2.70.300.D.11.e NMAC)

If your source is an acid rain source as defined by EPA, the following applies to you. For the portion of your acid rain source subject to the acid rain provisions of title IV of the federal Act, the compliance plan must also include any additional requirements under the acid rain provisions of title IV of the federal Act. Some requirements of title IV regarding the schedule and methods the source will use to achieve compliance with the acid rain emissions limitations may supersede the requirements of title V and 20.2.70 NMAC. You will need to consult with the Air Quality Bureau permitting staff concerning how to properly meet this requirement.

NOTE: The Acid Rain program has additional forms. See <u>http://www.env.nm.gov/aqb/index.html</u>. Sources that are subject to both the Title V and Acid Rain regulations are **encouraged** to submit both applications **simultaneously**.

The facility is in compliance with all applicable requirements; consequently, a compliance plan, a compliance schedule, and a schedule of certified progress reports is not required.

The facility is not equipped with any acid rain sources; consequently, compliance with the acid rain provisions is not required as a part of this permit application.

19.7 - 112(r) Risk Management Plan (RMP)

Any major sources subject to section 112(r) of the Clean Air Act must list all substances that cause the source to be subject to section 112(r) in the application. The permittee must state when the RMP was submitted to and approved by EPA.

The facility is not subject to 40 CFR 68, Chemical Accident Prevention Provisions; consequently, a Risk Management Plan is not required.

Form-Section 19 last revised: 8/15/2011

19.8 - Distance to Other States, Bernalillo, Indian Tribes and Pueblos

Will the property on which the facility is proposed to be constructed or operated be closer than 80 km (50 miles) from other states, local pollution control programs, and Indian tribes and pueblos (20.2.70.402.A.2 and 20.2.70.7.B NMAC)?

(If the answer is yes, state which apply and provide the distances.)

The facility is located within 80 kilometers of the following states, local pollution control programs, Indian tribes and pueblos:

State of Colorado (7.5 km) Jicarilla Apache Tribe (32.4 km) Navajo Nation Tribal land (34.2 km) Southern Ute Tribe (~7.5 km) Ute Mountain Ute Tribe (61.4 km)

19.9 - Responsible Official

Provide the Responsible Official as defined in 20.2.70.7.AD NMAC:

The responsible official is Travis Jones, EH&S Manager.

Other Relevant Information

<u>Other relevant information</u>. Use this attachment to clarify any part in the application that you think needs explaining. Reference the section, table, column, and/or field. Include any additional text, tables, calculations or clarifying information.

Additionally, the applicant may propose specific permit language for AQB consideration. In the case of a revision to an existing permit, the applicant should provide the old language and the new language in track changes format to highlight the proposed changes. If proposing language for a new facility or language for a new unit, submit the proposed operating condition(s), along with the associated monitoring, recordkeeping, and reporting conditions. In either case, please limit the proposed language to the affected portion of the permit.

This section contains the NMAQB *Compliance History Disclosure Form* required for all permit applications submitted on or after October 24, 2022.



Air Permit Application Compliance History Disclosure Form

Pursuant to Subsection 74-2-7(S) of the New Mexico Air Quality Control Act ("AQCA"), NMSA §§ 74-2-1 to -17, the New Mexico Environment Department ("Department") may deny any permit application or revoke any permit issued pursuant to the AQCA if, within ten years immediately preceding the date of submission of the permit application, the applicant met any one of the criteria outlined below. In order for the Department to deem an air permit application administratively complete, or issue an air permit for those permits without an administrative completeness determination process, the applicant must complete this Compliance History Disclosure Form as specified in Subsection 74-2-7(P). An existing permit holder (permit issued prior to June 18, 2021) shall provide this Compliance History Disclosure Form to the Department upon request.

Permittee/Applicant Company Name			Expected Application Submittal Date	
Harve	st Four Corners, LLC	June 6, 2023		
Permi	ttee/Company Contact	Email	Email	
Oakle	y Hayes	505-632-4421	Oakley.Hayes@harvestmidstream.c	om
Withi	n the 10 years preceding the expected date	of submittal of the applicat	ion, has the permittee or applicant:	
1	Knowingly misrepresented a material fact	in an application for a permi	t?	🗆 Yes 🛛 No
2	Refused to disclose information required	by the provisions of the New	Mexico Air Quality Control Act?	🗆 Yes 🖂 No
3	Been convicted of a felony related to envi	ronmental crime in any court	t of any state or the United States?	🗆 Yes 🗵 No
4	Been convicted of a crime defined by stat price fixing, bribery, or fraud in any court			🗆 Yes 🗵 No
5a	Constructed or operated any facility for which a permit was sought, including the current facility, without the required air quality permit(s) under 20.2.70 NMAC, 20.2.72 NMAC, 20.2.74 NMAC, 20.2.79 NMAC, or 20.2.84 NMAC?			
5b	If "No" to question 5a, go to question 6. If "Yes" to question 5a, state whether each facility that was constructed or operated without the required air quality permit met at least one of the following exceptions:			
	a. The unpermitted facility was discovered authorized by the Department; or	nely environmental audit that was		
	b. The operator of the facility estimated the operator applied for an air permit with required for the facility.	-		
6	Had any permit revoked or permanently s or the United States?	uspended for cause under th	e environmental laws of any state	🗆 Yes 🖂 No
7	For each "yes" answer, please provide an	explanation and documentat	ion.	1

Addendum for Landfill Applications

Landfill Applications are not required to complete Sections 1-C Input Capacity and Production Rate, 1-E Operating Schedule, 17 Compliance Test History, and 18 Streamline Applications. Section 12 – PSD Applicability is required only for Landfills with Gas Collection and Control Systems and/or landfills with other non-fugitive stationary sources of air emissions such as engines, turbines, boilers, heaters. All other Sections of the Universal Application Form are required.

EPA Background Information for MSW Landfill Air Quality Regulations: <u>https://www3.epa.gov/airtoxics/landfill/landflpg.html</u>

NM Solid Waste Bureau Website: https://www.env.nm.gov/swb/

Not applicable.

Section 22: Certification

Company Name: <u>Harvest Four Corners, LLC</u>

I, <u>Travis Jones</u>, hereby certify that the information and data submitted in this application are true and as accurate as possible, to the best of my knowledge and professional expertise and experience.

Signed this 17th day of January, 2022, upon my oath or affirmation, before a notary of the State of

17/2022 Date

01-17-2022

EH&S Manager

Title

Travis Jones Printed Name

Scribed and sworn before me on this 17 day of January, 2022.

My authorization as a notary of the State of	Texas	expires on the
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2024 ____ day of __ 's Signature MILLIN.

Notary's Printed Name

Date BRITTANY BURKHALTER Notary Public, State of Texas Comm. Expires 07-23-2024 Notary ID 130640662

*For Title V applications, the signature must be of the Responsible Official as defined in 20.2.70.7.AE NMAC.