

May 9, 2024

New Mexico Environment Department Air Quality Bureau 525 Camino de los Marquez, Suite 1 Santa Fe, New Mexico, 87505

## RE: New Source Review (NSR) Construction Permit Application Horned Frog Compressor Station, Lea County, New Mexico Delaware G&P, LLC

Dear Air Quality Bureau,

Delaware G&P, LLC (Delaware) submits the enclosed application for issuance of a New Source Review (NSR) Construction Permit to allow for additional compression at the existing Horned Frog Compressor Station.

The facility currently operates under Oil and Gas General Construction Permit (GCP-Oil and Gas) No. 7868M5.

A permit filing fee of \$500 was mailed to the department with the application. Electronic files will be transferred via secure electronic transfer initiated by the assigned permit writer.

Any clarification questions or requests for additional information can be directed to myself via email to <u>jj@resolutecompliance.com</u> or by phone at 903-241-2055 or Mr. Lance Green via email to <u>Lance.Green@enlink.com</u> or by phone at 225-692-6947.

Kind Regards,

Jeff A. Jackson Vice President EHSR

Encl: Initial NSR Permit via the Universal Application Form

Cc: Mr. Lance Green – Lead Environmental Permitting Specialist Ms. Daria Underwood – Lead Environmental Engineer



## **Mail Application To:**

New Mexico Environment Department Air Quality Bureau Permits Section 525 Camino de los Marquez, Suite 1 Santa Fe, New Mexico, 87505

Phone: (505) 476-4300 Fax: (505) 476-4375 www.env.nm.gov/aqb



# **Universal Air Quality Permit Application**

## Use this application for NOI, NSR, or Title V sources.

Use this application for: the initial application, modifications, technical revisions, and renewals. For technical revisions, complete Sections, 1-A, 1-B, 2-E, 3, 9 and any other sections that are relevant to the requested action; coordination with the Air Quality Bureau permit staff prior to submittal is encouraged to clarify submittal requirements and to determine if more or less than these sections of the application are needed. Use this application for streamline permits as well.

 This application is submitted as (check all that apply):
 Request for a No Permit Required Determination (no fee)

 Updating an application currently under NMED review.
 Include this page and all pages that are being updated (no fee required).

 Construction Status:
 Not Constructed
 Existing Permitted (or NOI) Facility
 Existing Non-permitted (or NOI) Facility

 Minor Source:
 NOI 20.2.73 NMAC
 20.2.72 NMAC application or revision
 20.2.72.300 NMAC Streamline application

 Title V Source:
 Title V (new)
 Title V renewal
 TV minor mod.
 TV significant mod.
 TV Acid Rain:
 New
 Renewal

 PSD Major Source:
 PSD major source (new)
 Minor Modification to a PSD source
 a PSD major modification

## Acknowledgements:

I acknowledge that a pre-application meeting is available to me upon request. 🔲 Title V Operating, Title IV Acid Rain, and NPR applications have no fees.

S \$500 NSR application Filing Fee enclosed OR □ The full permit fee associated with 10 fee points (required w/ streamline applications).

Check No.: 1627 in the amount of \$500

I acknowledge the required submittal format for the hard copy application is printed double sided 'head-to-toe', 2-hole punched (except the Sect. 2 landscape tables is printed 'head-to-head'), numbered tab separators. Incl. a copy of the check on a separate page.

I acknowledge there is an annual fee for permits in addition to the permit review fee: <u>www.env.nm.gov/air-quality/permit-fees-</u> <u>2/.</u>

This facility qualifies for the small business fee reduction per 20.2.75.11.C. NMAC. The full \$500.00 filing fee is included with this application and I understand the fee reduction will be calculated in the balance due invoice. The Small Business Certification Form has been previously submitted or is included with this application. (Small Business Environmental Assistance Program Information: <a href="http://www.env.nm.gov/air-quality/small-biz-eap-2/">www.env.nm.gov/air-quality/small-biz-eap-2/</a>.)

**Citation:** Please provide the **low level citation** under which this application is being submitted: **20.2.70.200.A NMAC** (e.g. application for a new minor source would be 20.2.72.200.A NMAC, one example for a Technical Permit Revision is 20.2.72.219.B.1.b NMAC, a Title V acid rain application would be: 20.2.70.200.C NMAC)

## Section 1 – Facility Information

Sec	tion 1-A: Company Information	<mark>AI #</mark> if known: 38473	<mark>Updating</mark> Permit/NOI #: 7868M5						
1	Facility Name: Horned Frog Compressor Station	Plant primary SIC Code (4 digits): 1311							
Ţ		Plant NAIC code (6 digits): 211130							
а	Facility Street Address (If no facility street address, provide directions from a prominent landmark): <sup>3</sup> 23.5 miles W of Jal								
2	Plant Operator Company Name: Delaware G & P, LLC	Phone/Fax: 225-692-6947							
а	Plant Operator Address: 1722 Routh Street, Suite 1300, Dallas, TX 75201								

b	Plant Operator's New Mexico Corporate ID or Tax ID:										
3	Plant Owner(s) name(s): Delaware G & P, LLC Phone/Fax: 225-692-6947										
а	Plant Owner(s) Mailing Address(s): 1722 Routh Street, Suite 1300, Dallas, TX 75201										
4	Bill To (Company): Delaware G & P, LLC	Phone/Fax: 225-692-6947									
а	Mailing Address: 1722 Routh Street, Suite 1300, Dallas, TX 75201	E-mail: Lance.Green@EnLink.com									
5	<ul> <li>Preparer: Resolute Compliance, LLC</li> <li>Consultant: Jeff Jackson</li> </ul>	Phone/Fax: 903-241-2055									
а	Mailing Address: PO Box 970, Royse City, TX 75189	E-mail: jj@resolutecompliance.com									
6	Plant Operator Contact: Zac Luedecke	Phone/Fax: 469-308-7299									
а	Address: P.O. Box 211, Mentone, TX 79754	E-mail: Richard.Luedecke@EnLink.com									
7	Air Permit Contact: Lance Green	Title: Lead Environmental Permitting Specialist									
а	E-mail: Lance.Green@enlink.com	Phone/Fax: 225-692-6947									
b	Mailing Address: 1722 Routh Street, Suite 1300, Dallas, TX 75201										
с	The designated Air permit Contact will receive all official correspondence (i.e. letters, permits) from the Air Quality Bureau.										

## Section 1-B: Current Facility Status

1.a	Has this facility already been constructed? 🛛 Yes 🔲	1.b If yes to question 1.a, is it currently operating in New Mexico?								
2	If yes to question 1.a, was the existing facility subject t Intent (NOI) (20.2.73 NMAC) before submittal of this a Yes X No	If yes to question 1.a, was the existing facility subject to a construction permit (20.2.72 NMAC) before submittal of this application? Yes INO								
3	Is the facility currently shut down? 🔲 Yes 🛛 No	onth and year of shut down (MM/YY):								
4	Was this facility constructed before 8/31/1972 and continuously operated since 1972?   Yes  No									
5	If Yes to question 3, has this facility been modified (see 20.2.72.7.P NMAC) or the capacity increased since 8/31/1972?									
6	Does this facility have a Title V operating permit (20.2. ☐ Yes ⊠ No	70 NMAC)?	If yes, the permit No. is: P-							
7	Has this facility been issued a No Permit Required (NPF	R)?	If yes, the NPR No. is:							
8	Has this facility been issued a Notice of Intent (NOI)?	🗌 Yes 🛛 No	If yes, the NOI No. is:							
9	Does this facility have a construction permit (20.2.72/2 ☐ Yes ⊠ No	? If yes, the permit No. is:								
10	Is this facility registered under a General permit (GCP-: ☑ Yes □ No	If yes, the register No. is: 7868M5								

## Section 1-C: Facility Input Capacity & Production Rate

1	What is the facility's maximum input capacity, specify units (reference here and list capacities in Section 20, if more room is required)										
		Hourly: 12.29 bbl Oil	Daily: 295 bbl Oil	Annually: 107,675 bbl Oil							
а	Current	5.2 MMSCF Natural Gas	125 MMSCF Natural Gas	45,625 MMSCF Natural Gas							
		15.21 bbl Produced Water	365 bbl Produced Water	133,225 bbl Produced Water							
		Hourly: 16.35 bbl Oil	Daily: 392.35 bbl Oil	Annually: 143,208 bbl Oil							
b	Proposed	5.2 MMSCF Natural Gas	125 MMSCF Natural Gas	45,625 MMSCF Natural Gas							
	•	20.22 bbl Produced Water	485.45 bbl Produced Water	177,190 bbl Produced Water							
2	What is the	facility's maximum production rate, s	pecify units (reference here and list capacities i	n Section 20, if more room is required)							
		Hourly: 12.29 bbl Oil	Daily: 295 bbl Oil	Annually: 107675 bbl Oil							
а	Current	5.2 MMSCF Natural Gas	125 MMSCF Natural Gas	45,625 MMSCF Natural Gas							
		15.21 bbl Produced Water	365 bbl Produced Water	133225 bbl Produced Water							
		Hourly: 16.35 bbl Oil	Daily: 392.35 bbl Oil	Annually: 143,208 bbl Oil							
b	Proposed	5.2 MMSCF Natural Gas	125 MMSCF Natural Gas	45,625 MMSCF Natural Gas							
	-	20.22 bbl Produced Water	485.45 bbl Produced Water	177,190 bbl Produced Water							

## Section 1-D: Facility Location Information

1	Latitude (decimal degrees): 32.083086	Longitude	(decimal degrees): -103.5	88061	County: Lea	Elevation (ft): 3325							
2	UTM Zone: 🔲 12 or 🔀 13		Datum: 🔲 NAD 83 🛛 WGS 84										
а	UTM E (in meters, to nearest 10 meters): 633250	)	UTM N (in meters, to neares	t 10 meters)	: 3550517								
3	Name and zip code of nearest New Mexico	o town: Jal 8	8252										
4	Detailed Driving Instructions from nearest NM town (attach a road map if necessary): From Bennett, New Mexico, go west on Anthony Road for 21.91 miles, turn North on an unnamed road 2.44 miles west of the intersection of Anthony Road and Hwy 2. The facility is 1.51 miles on the east side of the unnamed road.												
5	The facility is 23.5 (distance) miles W (dire	ection) of Jal	(nearest town).										
6	Land Status of facility (check one): 🔲 Priv	vate 🔲 Ind	ian/Pueblo 🛛 Governmo	ent 🔲 B	LM 🗌 Forest Se	rvice 🔲 Military							
7	List all municipalities, Indian tribes, and counties within a ten (10) mile radius (20.2.72.203.B.2 NMAC) of the property on which the facility is proposed to be constructed or operated: Lea County, Eddy County, Texas												
8	<b>20.2.72</b> NMAC applications <b>only</b> : Will the property on which the facility is proposed to be constructed or operated be closer than 50 km (31 miles) to other states, Bernalillo County, or a Class I area (see <u>www.env.nm.gov/air-quality/modeling-publications/</u> )? ☐ Yes												
9	Name nearest Class I area: Carlsbad Caver	ns National	Park										
10	Shortest distance (in km) from facility bou	ndary to the	boundary of the nearest	Class I are	a (to the nearest 10 n	neters): 74.5 km							
11	Distance (meters) from the perimeter of t lands, including mining overburden remov	he Area of O /al areas) to	perations (AO is defined a nearest residence, school	as the plar or occupi	it site inclusive of ed structure: > 5 r	all disturbed niles							
12	Method(s) used to delineate the Restricted Area: Continuous Fencing <b>"Restricted Area"</b> is an area to which public entry is effectively precluded. Effective barriers include continuous fencing, continuous walls, or other continuous barriers approved by the Department, such as rugged physical terrain with steep grade that would require special equipment to traverse. If a large property is completely enclosed by fencing, a restricted area within the property may be identified with signage only. Public reads cannot be part of a Destricted Area												
13	Does the owner/operator intend to operate this source as a portable stationary source as defined in 20.2.72.7.X NMAC? Yes No A portable stationary source is not a mobile source, such as an automobile, but a source that can be installed permanently at one location or that can be re-installed at various locations, such as a hot mix asphalt plant that is moved to different job sites												
14	Will this facility operate in conjunction with other air regulated parties on the same property? No Yes												

## Section 1-E: Proposed Operating Schedule (The 1-E.1 & 1-E.2 operating schedules may become conditions in the permit.)

1	Facility <b>maximum</b> operating ( $\frac{hours}{day}$ ): 24	( <mark>days</mark> (week ): 7	( <del>weeks</del> year): 52	( <u>hours</u> ): 8760						
2	Facility's maximum daily operating schedule (if less	than 24 hours day )? Start:	AM PM	End:	₽AM ₽PM					
3	Month and year of anticipated start of construction: Upon Permit Issuance									
4	Month and year of anticipated construction comple	etion: Upon Permit Issuance								
5	Month and year of anticipated startup of new or modified facility: Upon Permit Issuance									
6	Will this facility operate at this site for more than o	ne year? 🛛 Yes 🗌 No								

## Section 1-F: Other Facility Information

1	Are there any current Notice of Violations (NOV), compliance orders, or any other compliance or enforcement issues related									
T	to this facility? 🔲 Yes 🔀 No If yes, specify:									

а	If yes, NOV date or description of issue:		NOV Tracking No:								
b	b Is this application in response to any issue listed in 1-F, 1 or 1a above? Yes No If Yes, provide the 1c & 1d info below:										
С	c     Document Title:     Date:     Requirement # (or page # and paragraph #):										
d	d Provide the required text to be inserted in this permit:										
2	Is air quality dispersion modeling or modeling waiver being submitted with this application? 🛛 Yes 🗌 No										
3	Does this facility require an "Air Toxics" permit under 20.2.72.400 NMAC & 20.2.72.502, Tables A and/or B? 🗌 Yes 🖾 No										
4	Will this facility be a source of federal Hazardous Air Pollutants (HAP)? 🔀 Yes 🔲 No										
а	If Yes, what type of source? Major ( >10 tpy of a OR Minor ( <10 tpy of any	iny single HAP <b>OR</b> single HAP <b>AND</b>	<u>≥</u> 25 <25 t	tpy of any combination of HAPS) py of any combination of HAPS)							
5	Is any unit exempt under 20.2.72.202.B.3 NMAC?  Yes	No									
	If yes, include the name of company providing commercia	l electric power to the	e facility: _								
а	Commercial power is purchased from a commercial utility company, which specifically does not include power generated on site for the sole purpose of the user.										

## Section 1-G: Streamline Application (This section applies to 20.2.72.300 NMAC Streamline applications only)

1	I have filled out Section 18, "Addendum for Streamline Applications."	N/A (This is not a Streamline application.)

## Section 1-H: Current Title V Information - Required for all applications from TV Sources

(Title V-source required information for all applications submitted pursuant to 20.2.72 NMAC (Minor Construction Permits), or 20.2.74/20.2.79 NMAC (Major PSD/NNSR applications), and/or 20.2.70 NMAC (Title V))

1	Responsible Official (R.O.) (20.2.70.300.D.2 NMAC): Michael LeBlanc		Phone: 985-575-8311						
а	R.O. Title: SVP Operations	R.O. e-mail: Michae	el.LeBlanc@EnLink.com						
b	R. O. Address: 5609 Bayou Black Dr, Suite A, Gibson, LA 70356								
2	Alternate Responsible Official       Phone: 432-221-9704         (20.2.70.300.D.2 NMAC): Manish Kumar       Phone: 432-221-9704								
а	A. R.O. Title: Senior Director Operations	A. R.O. e-mail: Mar	nish.Kumar@EnLink.com						
b	A. R. O. Address: 303 West Wall Street, Suite 202, Midland, TX 79701								
3	Company's Corporate or Partnership Relationship to any other Air Quality Permittee (List the names of any companies that have operating (20.2.70 NMAC) permits and with whom the applicant for this permit has a corporate or partnership relationship): N/A								
4	Name of Parent Company ("Parent Company" means the primary name of the organization that owns the company to be permitted wholly or in part.): Delaware G&P, LLC								
а	Address of Parent Company: 1722 Routh Street, Suite 1300, Dallas	, TX 75201							
5	Names of Subsidiary Companies ("Subsidiary Companies" means of owned, wholly or in part, by the company to be permitted.): N/A	rganizations, branch	nes, divisions or subsidiaries, which are						
6	Telephone numbers & names of the owners' agents and site conta Lance Green 225-692-6947	icts familiar with pla	nt operations:						
7	Affected Programs to include Other States, local air pollution control programs (i.e. Bernalillo) and Indian tribes: Will the property on which the facility is proposed to be constructed or operated be closer than 80 km (50 miles) from other states, local pollution control programs, and Indian tribes and pueblos (20.2.70.402.A.2 and 20.2.70.7.B)? If yes, state which ones and provide the distances in kilometers: Texas, 9.2 km								

## Section 1-I – Submittal Requirements

Each 20.2.73 NMAC (NOI), a 20.2.70 NMAC (Title V), a 20.2.72 NMAC (NSR minor source), or 20.2.74 NMAC (PSD) application package shall consist of the following:

## Hard Copy Submittal Requirements:

- One hard copy original signed and notarized application package printed double sided 'head-to-toe' <u>2-hole punched</u> as we bind the document on top, not on the side; except Section 2 (landscape tables), which should be head-to-head. Please use numbered tab separators in the hard copy submittal(s) as this facilitates the review process. For NOI submittals only, hard copies of UA1, Tables 2A, 2D & 2F, Section 3 and the signed Certification Page are required. Please include a copy of the check on a separate page.
- 2) If the application is for a minor NSR, PSD, NNSR, or Title V application, include one working hard **copy** for Department use. This <u>copy</u> should be printed in book form, 3-hole punched, and <u>must be double sided</u>. Note that this is in addition to the head-to-to 2-hole punched copy required in 1) above. Minor NSR Technical Permit revisions (20.2.72.219.B NMAC) only need to fill out Sections 1-A, 1-B, 3, and should fill out those portions of other Section(s) relevant to the technical permit revision. TV Minor Modifications need only fill out Sections 1-A, 1-B, 1-H, 3, and those portions of other Section(s) relevant to the minor modification. NMED may require additional portions of the application to be submitted, as needed.
- 3) The entire NOI or Permit application package, including the full modeling study, should be submitted electronically. Electronic files for applications for NOIs, any type of General Construction Permit (GCP), or technical revisions to NSRs must be submitted with compact disk (CD) or digital versatile disc (DVD). For these permit application submittals, two CD copies are required (in sleeves, not crystal cases, please), with additional CD copies as specified below. NOI applications require only a single CD submittal. Electronic files for other New Source Review (construction) permits/permit modifications or Title V permits/permit modifications can be submitted on CD/DVD or sent through AQB's secure file transfer service.

## Electronic files sent by (check one):

CD/DVD attached to paper application

Secure electronic transfer. Air Permit Contact Name Leslee Kimbrell, Email: LK@resolutecompliance.com Phone number 505-369-6572.

a. If the file transfer service is chosen by the applicant, after receipt of the application, the Bureau will email the applicant with instructions for submitting the electronic files through a secure file transfer service. Submission of the electronic files through the file transfer service needs to be completed within 3 business days after the invitation is received, so the applicant should ensure that the files are ready when sending the hard copy of the application. The applicant will not need a password to complete the transfer. **Do not use the file transfer service for NOIs, any type of GCP, or technical revisions to NSR permits.** 

- 4) Optionally, the applicant may submit the files with the application on compact disk (CD) or digital versatile disc (DVD) following the instructions above and the instructions in 5 for applications subject to PSD review.
- 5) If air dispersion modeling is required by the application type, include the NMED Modeling Waiver and/or electronic air dispersion modeling report, input, and output files. The dispersion modeling <u>summary report only</u> should be submitted as hard copy(ies) unless otherwise indicated by the Bureau.
- 6) If the applicant submits the electronic files on CD and the application is subject to PSD review under 20.2.74 NMAC (PSD) or NNSR under 20.2.79 NMC include,
  - a. one additional CD copy for US EPA,
  - b. one additional CD copy for each federal land manager affected (NPS, USFS, FWS, USDI) and,
  - c. one additional CD copy for each affected regulatory agency other than the Air Quality Bureau.

If the application is submitted electronically through the secure file transfer service, these extra CDs do not need to be submitted.

## Electronic Submittal Requirements [in addition to the required hard copy(ies)]:

1) All required electronic documents shall be submitted as 2 separate CDs or submitted through the AQB secure file transfer service. Submit a single PDF document of the entire application as submitted and the individual documents comprising the application.

- 2) The documents should also be submitted in Microsoft Office compatible file format (Word, Excel, etc.) allowing us to access the text and formulas in the documents (copy & paste). Any documents that cannot be submitted in a Microsoft Office compatible format shall be saved as a PDF file from within the electronic document that created the file. If you are unable to provide Microsoft office compatible electronic files or internally generated PDF files of files (items that were not created electronically: i.e. brochures, maps, graphics, etc.), submit these items in hard copy format. We must be able to review the formulas and inputs that calculated the emissions.
- 3) It is preferred that this application form be submitted as 4 electronic files (3 MSWord docs: Universal Application section 1 [UA1], Universal Application section 3-19 [UA3], and Universal Application 4, the modeling report [UA4]) and 1 Excel file of the tables (Universal Application section 2 [UA2]). Please include as many of the 3-19 Sections as practical in a single MS Word electronic document. Create separate electronic file(s) if a single file becomes too large or if portions must be saved in a file format other than MS Word.
- 4) The electronic file names shall be a maximum of 25 characters long (including spaces, if any). The format of the electronic Universal Application shall be in the format: "A-3423-FacilityName". The "A" distinguishes the file as an application submittal, as opposed to other documents the Department itself puts into the database. Thus, all electronic application submittals should begin with "A-". Modifications to existing facilities should use the core permit number (i.e. '3423') the Department assigned to the facility as the next 4 digits. Use 'XXXX' for new facility applications. The format of any separate electronic submittals (additional submittals such as non-Word attachments, re-submittals, application updates) and Section document shall be in the format: "A-3423-9-description", where "9" stands for the section # (in this case Section 9-Public Notice). Please refrain, as much as possible, from submitting any scanned documents as this file format is extremely large, which uses up too much storage capacity in our database. Please take the time to fill out the header information throughout all submittals as this will identify any loose pages, including the Application Date (date submitted) & Revision number (0 for original, 1, 2, etc.; which will help keep track of subsequent partial update(s) to the original submittal. Do not use special symbols (#, @, etc.) in file names. The footer information should not be modified by the applicant.

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# **Application Summary**

The **Application Summary** shall include a brief description of the facility and its process, the type of permit application, the applicable regulation (i.e. 20.2.72.200.A.X, or 20.2.73 NMAC) under which the application is being submitted, and any air quality permit numbers associated with this site. If this facility is to be collocated with another facility, provide details of the other facility including permit number(s). In case of a revision or modification to a facility, provide the lowest level regulatory citation (i.e. 20.2.72.219.B.1.d NMAC) under which the revision or modification is being requested. Also describe the proposed changes from the original permit, how the proposed modification will affect the facility's operations and emissions, de-bottlenecking impacts, and changes to the facility's major/minor status (both PSD & Title V).

The **<u>Process Summary</u>** shall include a brief description of the facility and its processes.

<u>Startup, Shutdown, and Maintenance (SSM)</u> routine or predictable emissions: Provide an overview of how SSM emissions are accounted for in this application. Refer to "Guidance for Submittal of Startup, Shutdown, Maintenance Emissions in Permit Applications (http://www.env.nm.gov/aqb/permit/app\_form.html) for more detailed instructions on SSM emissions.

Delaware G&P, LLC (Delaware) is submitting an initial New Source Review (NSR) Permit under 20.2.72.200.A NMAC to replace GCP Permit 7868M5 to authorize the addition of two (2) compressor engine options (Source IDs E-9 and E-10) and increase facility throughput at the Horned Frog Compressor Station (Facility), located near Jal in Lea County, New Mexico. The Facility is a natural gas compressor station that receives natural gas from wells located in Lea County through a network of gathering pipelines.

The facility will consist of the following equipment:

- Nine (9) Compressor Engines (Unit IDs E-1, E-2, E-4 through E-10)
- Two (2) generator engines (Unit IDs GEN-4, GEN-5)
- Six (6) 400 bbl condensate tanks (Unit IDs TK-1 through TK-3, TK-5 through TK-7)
- Two (2) 400 bbl produced water tanks (Unit IDs TK-4, TK-8)
- One (1) 750 bbl gunbarrel separator (Unit ID GB-1)
- Two (2) glycol reboilers (Unit IDs H-1, H-2)
- Two (2) TEG dehydrators (Unit IDs DEHY1, DEHY2)
- One (1) enclosed combustor (Unit ID ECD-1)
- One (1) electric vapor recovery unit
- Condensate loading (Unit ID CONDLOAD)
- Produced water loading (Unit ID PWLOAD)
- Facility fugitives (Unit ID FUG)
- Unpaved haul road emissions (Unit ID UR-1)
- Startup, Shutdown, Maintenance emissions (Unit ID SSM)

Site-Specific SSM emissions are estimated for compressor blowdowns, starter vents, dehydrator blowdowns, filter coalescer blowdowns, scrubber blowdowns, pump blowdowns, reboiler maintenance, pipeline maintenance and tank degassing.

This page is intentionally left blank.

# **Process Flow Sheet**

A **process flow sheet** and/or block diagram indicating the individual equipment, all emission points and types of control applied to those points. The unit numbering system should be consistent throughout this application.

A process flow diagram is attached to this section.



# Plot Plan Drawn to Scale

A <u>plot plan drawn to scale</u> showing emissions points, roads, structures, tanks, and fences of property owned, leased, or under direct control of the applicant. This plot plan must clearly designate the restricted area as defined in UA1, Section 1-D.12. The unit numbering system should be consistent throughout this application.

A plot plan is attached to this section.



# **All Calculations**

**Show all calculations** used to determine both the hourly and annual controlled and uncontrolled emission rates. All calculations shall be performed keeping a minimum of three significant figures. Document the source of each emission factor used (if an emission rate is carried forward and not revised, then a statement to that effect is required). If identical units are being permitted and will be subject to the same operating conditions, submit calculations for only one unit and a note specifying what other units to which the calculations apply. All formulas and calculations used to calculate emissions must be submitted. The "Calculations" tab in the UA2 has been provided to allow calculations to be linked to the emissions tables. Add additional "Calc" tabs as needed. If the UA2 or other spread sheets are used, all calculation spread sheet(s) shall be submitted electronically in Microsoft Excel compatible format so that formulas and input values can be checked. Format all spread sheets and calculations such that the reviewer can follow the logic and verify the input values. Define all variables. If calculation spread sheets are not used, provide the original formulas with defined variables. Additionally, provide subsequent formulas showing the input values for each variable in the formula. All calculations, including those calculations are imbedded in the Calc tab of the UA2 portion of the application, the printed Calc tab(s), should be submitted under this section.

**Tank Flashing Calculations**: The information provided to the AQB shall include a discussion of the method used to estimate tank-flashing emissions, relative thresholds (i.e., NOI, permit, or major source (NSPS, PSD or Title V)), accuracy of the model, the input and output from simulation models and software, all calculations, documentation of any assumptions used, descriptions of sampling methods and conditions, copies of any lab sample analysis. If Hysis is used, all relevant input parameters shall be reported, including separator pressure, gas throughput, and all other relevant parameters necessary for flashing calculation.

**SSM Calculations**: It is the applicant's responsibility to provide an estimate of SSM emissions or to provide justification for not doing so. In this Section, provide emissions calculations for Startup, Shutdown, and Routine Maintenance (SSM) emissions listed in the Section 2 SSM and/or Section 22 GHG Tables and the rational for why the others are reported as zero (or left blank in the SSM/GHG Tables). Refer to "Guidance for Submittal of Startup, Shutdown, Maintenance Emissions in Permit Applications (http://www.env.nm.gov/aqb/permit/app\_form.html) for more detailed instructions on calculating SSM emissions. If SSM emissions are greater than those reported in the Section 2, Requested Allowables Table, modeling may be required to ensure compliance with the standards whether the application is NSR or Title V. Refer to the Modeling Section of this application for more guidance on modeling requirements.

**Glycol Dehydrator Calculations**: The information provided to the AQB shall include the manufacturer's maximum design recirculation rate for the glycol pump. If GRI-Glycalc is used, the full input summary report shall be included as well as a copy of the gas analysis that was used.

**Road Calculations:** Calculate fugitive particulate emissions and enter haul road fugitives in Tables 2-A, 2-D and 2-E for:

- 1. If you transport raw material, process material and/or product into or out of or within the facility and have PER emissions greater than 0.5 tpy.
- 2. If you transport raw material, process material and/or product into or out of the facility more frequently than one round trip per day.

## Significant Figures:

A. All emissions standards are deemed to have at least two significant figures, but not more than three significant figures.B. At least 5 significant figures shall be retained in all intermediate calculations.

**C.** In calculating emissions to determine compliance with an emission standard, the following rounding off procedures shall be used:

- (1) If the first digit to be discarded is less than the number 5, the last digit retained shall not be changed;
- (2) If the first digit discarded is greater than the number 5, or if it is the number 5 followed by at least one digit other than the number zero, the last figure retained shall be increased by one unit; and
- (3) If the first digit discarded is exactly the number 5, followed only by zeros, the last digit retained shall be rounded upward if it is an odd number, but no adjustment shall be made if it is an even number.

(4) The final result of the calculation shall be expressed in the units of the standard.

Form-Section 6 last revised: 5/3/16

**Control Devices:** In accordance with 20.2.72.203.A(3) and (8) NMAC, 20.2.70.300.D(5)(b) and (e) NMAC, and 20.2.73.200.B(7) NMAC, the permittee shall report all control devices and list each pollutant controlled by the control device regardless if the applicant takes credit for the reduction in emissions. The applicant can indicate in this section of the application if they chose to not take credit for the reduction in emission rates. For notices of intent submitted under 20.2.73 NMAC, only uncontrolled emission rates can be considered to determine applicability unless the state or federal Acts require the control. This information is necessary to determine if federally enforceable conditions are necessary for the control device, and/or if the control device produces its own regulated pollutants or increases emission rates of other pollutants.

## Caterpillar 3516B Engines (Unit IDs: E-1 and E-2)

NO<sub>X</sub>, CO, and VOC emission rates were calculated using manufacturer specifications. SO<sub>2</sub> emissions are based on a conservative fuel sulfur content estimated of 2 gr S/100 scf and 100% conversion of elemental sulfur to SO<sub>2</sub>. Particulate (PM<sub>2.5</sub>, PM<sub>10</sub>, and PM) and HAP emissions were calculated using AP-42 Table 3.2-2. Greenhouse gas emissions are estimated using emission factors from 40 CFR 98 Subpart C Tables C-1 and C-2.

## Caterpillar 3606 A4 Engine (Unit ID: E-4)

NO<sub>x</sub>, CO, and VOC emission rates were calculated using manufacturer specifications. SO<sub>2</sub> emissions are based on a conservative fuel sulfur content estimated of 2 gr S/100 scf and 100% conversion of elemental sulfur to SO<sub>2</sub>. Particulate (PM<sub>2.5</sub>, PM<sub>10</sub>, and PM) and HAP emissions were calculated using AP-42 Table 3.2-2. Greenhouse gas emissions are estimated using emission factors from 40 CFR 98 Subpart C Tables C-1 and C-2.

## Waukesha P9394GSI S5 Engines (Unit IDs: E-5, E-6, ENG-7, E-8, E-9b)

NO<sub>X</sub>, CO, and VOC emission rates were calculated using manufacturer specifications. SO<sub>2</sub> emissions are based on a conservative fuel sulfur content estimated of 2 gr S/100 scf and 100% conversion of elemental sulfur to SO<sub>2</sub>. Particulate (PM<sub>2.5</sub>, PM<sub>10</sub>, and PM) and HAP emissions were calculated using AP-42 Table 3.2-2. Greenhouse gas emissions are estimated using emission factors from 40 CFR 98 Subpart C Tables C-1 and C-2.

## Caterpillar 3608 A4 Engine (Unit ID: E-9a)

NO<sub>x</sub>, CO, and VOC emission rates were calculated using manufacturer specifications. SO<sub>2</sub> emissions are based on a conservative fuel sulfur content estimated of 2 gr S/100 scf and 100% conversion of elemental sulfur to SO<sub>2</sub>. Particulate (PM<sub>2.5</sub>, PM<sub>10</sub>, and PM) and HAP emissions were calculated using AP-42 Table 3.2-2. Greenhouse gas emissions are estimated using emission factors from 40 CFR 98 Subpart C Tables C-1 and C-2.

## Caterpillar 3612 A4 Engine (Unit ID: E-10a)

NO<sub>x</sub>, CO, and VOC emission rates were calculated using manufacturer specifications. SO<sub>2</sub> emissions are based on a conservative fuel sulfur content estimated of 2 gr S/100 scf and 100% conversion of elemental sulfur to SO<sub>2</sub>. Particulate (PM<sub>2.5</sub>, PM<sub>10</sub>, and PM) and HAP emissions were calculated using AP-42 Table 3.2-2. Greenhouse gas emissions are estimated using emission factors from 40 CFR 98 Subpart C Tables C-1 and C-2.

## Waukesha 12V275GL Engine (Unit ID: E-10b)

NO<sub>x</sub>, CO, and VOC emission rates were calculated using manufacturer specifications. SO<sub>2</sub> emissions are based on a conservative fuel sulfur content estimated of 2 gr S/100 scf and 100% conversion of elemental sulfur to SO<sub>2</sub>. Particulate (PM<sub>2.5</sub>, PM<sub>10</sub>, and PM) and HAP emissions were calculated using AP-42 Table 3.2-2. Greenhouse gas emissions are estimated using emission factors from 40 CFR 98 Subpart C Tables C-1 and C-2.

## Glycol Dehydrators (Unit IDs: DEHY1, DEHY2)

Glycol dehydrator emissions were calculated using BR&E Promax and an extended gas analysis. Flash tank emissions are sent to a VRU with 98% capture efficiency, routed to station suction, during VRU downtime emissions are sent to the ECD for 98% DRE; still column to BTEX, BTEX non-condensable is sent to reboiler stack with glow plug with 98% DRE.

## Gunbarrel Separator (Unit ID: GB-1)

Gunbarrel emissions were estimated using BR&E ProMax. Flash, working and standing emissions are controlled by a VRU with an assumed 98% capture efficiency and 5% downtime. Downtime is sent to ECD with 98% DRE.

## Storage Tanks (Unit IDs: TK-1 through TK-8)

Condensate storage tanks (Unit IDs: TK-1,2,3 and TK-5,6,7) and produced water tanks (Unit IDs: TK-4 and TK-8) emissions were estimated using BR&E ProMax. Flash, working and standing emissions from these tanks are controlled by a VRU with an assumed 98% capture efficiency and 5% downtime. Downtime is sent to ECD with 98% DRE.

## Enclosed Combustor Devices (Unit IDs: ECD-1)

NO<sub>x</sub> and CO emissions were calculated using TNRCC RG-109. VOCs and HAPs emissions were estimated based on the gas analysis and with manufacturer specification of 98% combustion efficiency. Pilot SO<sub>2</sub> emissions are based on a conservative fuel sulfur content estimated of 2 gr S/100 scf and 100% conversion of elemental sulfur to SO<sub>2</sub>. Process emissions were calculated assuming 98% combustion efficiency. Greenhouse gas emissions are estimated using emission factors from 40 CFR Part 98 Subpart C Table C-01 and C-02.

## Fugitive Emissions (Unit ID: FUG)

Fugitive emission calculations were completed using emission factors from Table 2-4 of EPA Protocol for Equipment Leak Emission Estimates, 1995, and weight percent of gas and liquid components from gas and liquid streams generated in a BR&E ProMax simulation. Subcomponent counts for each subcomponent are based on estimated average component counts for each piece of equipment.

## Loading Emissions (Unit ID: CONDLOAD and PWLOAD)

ProMax was used to perform the loading emission for condensate and produced water.

## Reboilers (Unit IDs: H-1 and H-2)

NO<sub>x</sub>, CO, VOCs and PM were estimated using AP-42 Table 1.4-1 & 1.4-2 with adjusted emission factors. HAPs were calculated using adjusted emission rates from AP-42 Table 1.4-3. SO<sub>2</sub> emissions were calculated with a conservative assumption of 2 gr S/100 scf and 100% conversion of elemental sulfur to SO<sub>2</sub>. Greenhouse gas emissions are estimated using emission factors from 40 CFR Part 98 Subpart C Table C-01 and C-02.

## Unpaved Haul Road (Unit ID: UR-1)

PM, PM<sub>10</sub> and PM<sub>2.5</sub> emissions were estimated based on the condensate loadout design basis and using equations 1a & 2 from AP-42 Section 13.2.2. Emissions factors were used from AP-42 Table 13.2.2-2.

#### Allowable Emission Summary New Source Review Permit Horned Frog Compressor Station Delaware G & P, LLC

																												1 metric ton=	1.10231	short to	n
	-				-																								GHG sho	ort tons	
			NOx		CO		VO	C	SO2		PM		PM10		PM2.5		H2S	Acetal	dehyde	Acrol	lein	Benze	ne	Formaldeh	yde	Total H/	APs	CO <sub>2</sub>	N <sub>2</sub> O	CH <sub>4</sub>	CO <sub>2</sub> e
FIN	EPN	Description	lb/hr tp	Y	lb/hr tp	ру	lb/hr t	tpy	lb/hr tpy	It	b/hr tp	y	lb/hr tpy		b/hr tpy	lb/h	r tpy	lb/hr	tpy	lb/hr	tpy	lb/hr tp	Y	lb/hr tpy	·	b/hr tp	iy .	tpy	tpy	tpy	tpy
E-1	E-1	1380 hp Caterpillar Compressor Engine	1.67	7.33	1.89	8.26	1.76	7.73	0.06	0.26	0.11	0.50	0.11	0.50	0.11 0	0.50 -	-	0.095	0.415	0.058	0.255	0.005	0.022	0.26	1.15	0.43	1.87	6398.84	0.01	0.12	6405.4
E-2	E-2	1380 hp Caterpillar Compressor Engine	1.67	7.33	1.89	8.26	1.76	7.73	0.06	0.26	0.11	0.50	0.11	0.50	0.11 0	0.50 -	-	0.095	0.415	0.058	0.255	0.005	0.022	0.26	1.15	0.43	1.87	6398.84	0.01	0.12	6405.4
E-4	E-4	1875 hp Caterpillar Compressor Engine	2.07	9.05	2.07	9.05	1.24	5.43	0.06	0.28	0.12	0.55	0.12	0.55	0.12	0.55 -	-	0.104	0.456	0.064	0.281	0.005	0.024	0.08	0.36	0.26	1.16	7041.03	0.01	0.13	7048.3
E-5	E-5	2500 hp Waukesha Compressor Engine	1.65	7.24	2.20	9.66	1.38	6.04	0.09	0.39	0.34	1.48	0.34	1.48	0.34	1.48 -	-	0.049	0.213	0.046	0.201	0.028	0.121	0.22	0.97	0.36	1.56	9846.93	0.02	0.19	9857.10
E-6	E-6	2500 hp Waukesha Compressor Engine	1.65	7.24	2.20	9.66	1.38	6.04	0.09	0.39	0.34	1.48	0.34	1.48	0.34	1.48 -	-	0.049	0.213	0.046	0.201	0.028	0.121	0.22	0.97	0.36	1.56	9846.93	0.02	0.19	9857.1
E-7	E-7	2500 hp Waukesha Compressor Engine	1.65	7.24	2.20	9.66	1.38	6.04	0.09	0.39	0.34	1.48	0.34	1.48	0.34	1.48 -	-	0.049	0.213	0.046	0.201	0.028	0.121	0.22	0.97	0.36	1.56	9846.93	0.02	0.19	9857.10
E-8	E-8	2500 hp Waukesha Compressor Engine	1.65	7.24	2.20	9.66	1.38	6.04	0.09	0.39	0.34	1.48	0.34	1.48	0.34	1.48 -	-	0.049	0.213	0.046	0.201	0.028	0.121	0.22	0.97	0.36	1.56	9846.93	0.02	0.19	9857.1
E-9*	E-9*	2500 hp Compressor Engine	1.65	7.24	2.20	9.66	1.65	7.24	0.10	0.43	0.34	1.48	0.34	1.48	0.34	1.48 -	-	0.159	0.695	0.098	0.428	0.028	0.121	0.22	0.97	0.50	2.18	10725.16	0.02	0.20	10736.2
E-10*	E-10*	3750 hp Compressor Engine	2.48	10.86	2.48	10.86	2.08	9.13	0.15	0.64	0.28	1.24	0.28	1.24	0.28	1.24 -	-	0.236	1.036	0.145	0.637	0.012	0.055	0.25	1.09	0.66	2.89	15975.49	0.03	0.30	15991.9
GEN-4	GEN-4	536 hp Generator Engine	1.18	5.18	2.36	10.35	0.91	4.01	0.022	0.097	0.08	0.36	0.08	0.36	0.08	0.36 -	-	0.012	0.052	0.011	0.049	0.007	0.030	0.09	0.39	0.12	0.53	2421.77	0.00	0.05	2424.2
GEN-5	GEN-5	536 hp Generator Engine	1.18	5.18	2.36	10.35	0.91	4.01	0.022	0.097	0.08	0.36	0.08	0.36	0.08	0.36 -	-	0.012	0.052	0.011	0.049	0.007	0.030	0.09	0.39	0.12	0.53	2421.77	0.00	0.05	2424.2
TK-1	VRU/ECD	400 bbl Condensate Tank					0.49	1.14		-						-	-	-	-		-				-	-		-	-	0.02	0.5
тк-2	VRU/ECD	400 bbl Condensate Tank					0.49	1.14		-						-	-	-	-		-				-	-		-	-	0.02	0.53
тк-з	VRU/ECD	400 bbl Condensate Tank					0.49	1.14		-						-	-	-	-		-				-	-		-	-	0.02	0.53
ТК-4	VRU/ECD	400 bbl Produced Water Tank					0.001	0.003		-						-	-	-	-		-				-	-		-	-	0.001	0.0
TK-5	VRU/ECD	400 bbl Condensate Tank					0.49	1.14		-						-	-	-	-		-				-	-		-	-	0.02	0.53
ТК-6	VRU/ECD	400 bbl Condensate Tank					0.49	1.14		-						-	-	-	-		-				-			-	-	0.02	0.5
TK-7	VRU/ECD	400 bbl Condensate Tank					0.49	1.14		-						-	-	-	-		-				-	-		-	-	0.02	0.53
TK-8	VRU/ECD	400 bbl Produced Water Tank					0.001	0.003		-						-	-	-	-		-				-	-		-	-	0.0006	0.0
GB-01	VRU/ECD	750 bblGunbarrel Separator					4.03	9.36		-						-	-	-	-		-				-	-		-	-	0.13	3.3
H-1	H-1	0.5 MMBtu/hr Reboiler	0.05	0.20	0.04	0.17	0.00	0.01	0.003	0.011	0.00	0.01	0.00	0.01	0.00	0.01 -	-	-	-		-				-	-		282.39	0.0005	0.005	282.6
H-2	H-2	1 MMBtu/hr Reboiler	0.09	0.39	0.08	0.33	0.00	0.02	0.005	0.023	0.01	0.03	0.01	0.03	0.01 0	0.03 -	-	-	-		-				-	-		564.78	0.0011	0.011	565.36
DEHY1	VRU/ECD	25 MMSCFD Glycol Dehydrator					1.54	4.34		-						-	-	-	-		-	0.040	0.150			0.13	0.57	301.30	-	1.47	338.0
DEHY2	VRU/ECD	100 MSCFD Glycol Dehydrator					1.54	4.30		-						-	-	-	-		-	0.040	0.160			0.13	0.59	290.86	-	1.62	331.2
CONDLOAD	VRU/ECD	Condensate Truck Loading					0.09	0.20		-						-	-	-	-		-				-	-		-	-	0.002	0.0
PWLOAD	VRU/ECD	Produced Water Truck Loading					6.5E-06	1.5E-05		-						-	-	-	-		-				-	-		-	-	0.00005	0.00
VRU	ECD	Enlosed Combustion Device	0.85	0.26	0.43	0.13	0.0002	0.0007	0.0003 0	.0015 -	-					-	-	-	-		-	6.3E-08	2.8E-07		-	-		202681.67	0.38	3.82	202890.99
FUG	FUG	Fugitives					3.50	15.32		-						-	-	-	-		-	0.008	0.036			0.21	0.93	0.58	-	16.28	407.5
UR-1	UR-1	Unpaved Haul Roads									0.63	0.31	0.63	0.31	0.06	0.03 -	-	-	-		-				-	-		-	-	-	
SSM	SSM	Startup, Shutdown, Maintenance					1737.98	18.27		-	-					-	-	-	-	-		5.56	0.06			47.65	0.50	1.10	-	31.00	776.1
		Total	19.51	81.98	24.61	106.05	1767.50	128.10	0.83	3.66	3.13	11.27	3.13	11.27	2.57 10	0.99	0.00 0.0	0 0.91	3.97	0.63	2.76	5.83	1.19	2.13	9.34	52.07	19.86	294,893.30	0.55	56.17	296,462.90

\*Represents worst-case scenario between both engine options.

## Manley Gas Analysis C6+ Speciation Calculator New Source Review Permit Horned Frog Compressor Station Delaware G&P LLC

Component			Sample Mol %	MW	Mol%xMW	Wt%
Water			0.0000%	18.015	0.0000	0.000%
Nitrogen			1.6257%	28.013	0.4554	1.936%
CO2			0.9110%	44.010	0.4009	1.704%
Oxygen			0.0000%	31.999	0.0000	0.000%
H2S			0.0000%	34.081	0.0000	0.000%
Methane			70.5411%	16.043	11.3169	48.103%
Ethane			13.3016%	30.070	3.9998	17.001%
Propane			7.6090%	44.097	3.3553	14.262%
i-Butane (iC4)	Total C4	3.7352%	1.0390%	58.123	0.6039	2.567%
n-Butane (nC4)			2.6962%	58.123	1.5671	6.661%
i-Pentane(iC5)	Total C5	1.3098%	0.6014%	72.150	0.4339	1.844%
n-Pentane(nC5)			0.7084%	72.150	0.5111	2.173%
Hexanes	Total C6+	0.9666%	0.6864%			
Heptanes			0.2802%			
		Sample Sum	100%			
	CE, Normalized	% of Norm. Sample -				
		Adjusted for C6 and	Corrected Mol %	MW	Mol%xMW	Corrected Wt%
	Sample MOL/	C7+ Split				
Benzene	2.055%	3.4372	0.0236%	78.000	0.0184	0.078%
n-Hexane	16.993%	28.4226	0.1951%	86.172	0.1681	0.715%
Hexane (C6)	40.739%	68.1402	0.4677%	86.172	0.4030	1.713%
Toluene	1.771%	4.4040	0.0123%	92.130	0.0114	0.048%
Heptane (C7)	29.283%	72.8197	0.2040%	100.198	0.2044	0.869%
Ethylbenzene	0.060%	0.1492	0.0004%	106.165	0.0004	0.002%
m-Xylene	0.339%	0.8430	0.0024%	106.165	0.0025	0.011%
p-Xylene	0.022%	0.0547	0.0002%	106.165	0.0002	0.001%
o-Xylene	0.082%	0.2039	0.0006%	106.165	0.0006	0.003%
Octane (C8)	5.961%	14.8236	0.0415%	114.224	0.0474	0.202%
Nonane (C9)	1.507%	3.7475	0.0105%	128.250	0.0135	0.057%
Decane	1.148%	2.8548	0.0080%	142.290	0.0114	0.048%
C11	0.040%	0.0995	0.0003%	156.310	0.0004	0.002%
C6+ Sum:	100.00%		0.9666%	Gas MW	23.526	
Totals			100.00%			100.00%
VOCs						31.26%
Max Benzene						0.10%
Total HAP						0.857%

Lower heating value Higher heating value 1335 Btu/scf 1364 Btuscf Specific gravity

0.8096 0.8162

## SCADA Fuel Chromatograph New Source Review Permit Horned Frog Compressor Station Delaware G&P LLC

Component			Sample Mol %	MW	Mol%xMW	Wt%
Water			0.0000%	18.015	0.0000	0.000%
Nitrogen			2.0020%	28.013	0.5608	2.853%
CO2			1.4630%	44.010	0.6439	3.276%
Oxygen			0.0000%	31.999	0.0000	0.000%
H2S			0.0000%	34.081	0.0000	0.000%
Methane			80.6860%	16.043	12.9445	65.859%
Ethane			11.8240%	30.070	3.5555	18.090%
Propane			3.4100%	44.097	1.5037	7.651%
i-Butane (iC4)	Total C4	0.5530%	0.3350%	58.123	0.1947	0.991%
n-Butane (nC4)			0.2180%	58.123	0.1267	0.645%
i-Pentane(iC5)	Total C5	0.0480%	0.0260%	72.150	0.0188	0.095%
n-Pentane(nC5)			0.0220%	72.150	0.0159	0.081%
Hexanes	Total C6+	0.1030%	0.1000%	86.172	0.0862	0.438%
Heptanes			0.0030%	100.198	0.0030	0.015%
Octane (C8)			0.0010%	114.224	0.0011	0.006%
				Gas MW	19.655	
Totals			100%			100.00%
VOCs						9.92%
Max Benzene						0.10%
Total HAP						0.438%

Fuel heating value

1111 Btu/scf

Specific gravity

0.6776

## Manley Liquid Analysis C6+ Speciation Calculator New Source Review Permit Horned Frog Compressor Station Delaware G&P LLC

Component		Sample Mol %	Sample Wt%	
Water		0.00%	0.00%	
Nitrogen		0.00%	0.00%	
CO2		0.00%	0.00%	
Oxygen		0.00%	0.00%	
H2S		0.00%	0.00%	
Methane		0.11%	0.02%	
Ethane		0.27%	0.09%	
Propane		1.72%	0.85%	
i-Butane (iC4)	Total C4	1.41%	0.92%	
n-Butane (nC4)	8.9500%	7.54%	4.91%	
i-Pentane(iC5)	Total C5	7.10%	5.74%	
n-Pentane(nC5)	19.1100%	12.01%	9.71%	
Hexanes	Total C6+	69.84%	77.76%	
		100%	100%	
	C6+ Normalized Sample Mol%	Corrected Mol %	C6+ Normalized Sample Wt%	Corrected Wt%
Benzene	1.54%	1.08%	1.2100%	0.9409%
n-Hexane	11.84%	8.27%	10.2900%	8.0015%
Hexane (C6)	26.93%	18.81%	22.9100%	17.8148%
Toluene	3.06%	2.14%	3.0600%	2.3795%
Heptane (C7)	29.05%	20.29%	28.7800%	22.3793%
Ethylbenzene	0.26%	0.18%	0.2600%	0.2022%
m-Xylene	1.47%	1.03%	1.4700%	1.1431%
p-Xylene	0.37%	0.26%	0.3700%	0.2877%
o-Xylene	0.14%	0.10%	0.1400%	0.1089%
Octane (C8)	14.15%	9.88%	16.3200%	12.6904%
Nonane (C9)	4.87%	3.40%	6.1700%	4.7978%
Decane	6.16%	4.30%	8.7400%	6.7962%
C11	0.16%	0.11%	0.2800%	0.2177%
C6+ Sum:	100.00%	69.84%	100.00%	77.76%
Totals		100.00%		100.00%
VOCs				99.89%
Max Benzene				0.10%

## Worst-Case Emissions for Engine Options New Source Review Permit Horned Frog Compressor Station Delaware G&P, LLC

	Engine 9: Un	controlled																									
		N	Ox	CC	C	VO	С	SO2		Р	M	PN	110		PM2.5		H <sub>2</sub> S	Aceta	ldehyde	Acro	lein	Ber	nzene	Forma	aldehyde	Tota	al HAPs
Unit #	Description	lb/hr	tpy	lb/hr	tpy	lb/hr	ру	lb/hr tpy	y	lb/hr	ton/yr	lb/hr	tpy	lb/hr	tpy	I	lb/hr tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
E-9a	Caterpillar G3608 A4	1.6	5 7.24	12.40	54.32	2.31	10.14	0.10	0.43	0.19	0.83	0.19	0.83	3 0	.19	0.83 -		0.15	0.695	0.098	0.428	0.008	3 0.037	0.60	5 2.90	0.94	4 4.11
E-9b	Waukesha P9394GSI S5	65.9	7 288.96	33.40	146.29	3.31	14.48	0.09	0.39	0.34	1.48	0.34	1.48	3 0	.34	1.48		0.04	9 0.213	0.046	0.201	0.028	3 0.121	. 0.28	8 1.21	0.4	1 1.80
E-9*	Worst Case Emissions	65.9	7 288.96	33.40	146.29	3.31	14.48	0.10	0.43	0.34	1.48	0.34	1.48	3 0	.34	1.48		0.1	5 0.70	0.10	0.43	0.03	8 0.12	2 0.60	6 <b>2.90</b>	0.94	4 4.11

	Engine 9: Co	ontrolled																										
		NOx			СО		VOC		SO2		PM	Р	M10		PM2.5		F	H <sub>2</sub> S	Acetal	dehyde	Acro	olein	Ber	nzene	Form	aldehyde	Tota	l HAPs
Unit #	Description	lb/hr tpy	/	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	ton/yr	lb/hr	tpy	lb/hr	tpy		lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
E-9a	Caterpillar G3608 A4	1.65	7.24	2.2	0 9.66	5 1	.65 7.2	4 0.1	LO 0.43	0.1	.9 0.83	3 0.1	9 0.83	3 0	.19	0.83	-	-	0.159	0.695	0.098	0.428	0.008	3 0.037	0.2	22 0.97	0.50	2.18
E-9b	Waukesha P9394GSI S5	1.65	7.24	2.2	0 9.66	5 1	.38 6.0	4 0.0	0.39	0.3	4 1.48	8 0.3	4 1.48	3 0	.34	1.48	-	-	0.049	0.213	0.046	0.201	0.028	0.121	. 0.2	22 0.97	0.36	1.56
E-9*	Worst Case Emissions	1.65	7.24	2.2	0 9.66	5 1	.65 7.2	4 0.1	LO 0.43	0.3	4 1.48	8 0.3	4 1.48	30	.34	1.48			0.16	0.70	0.10	0.43	0.03	0.12	2 0.2	22 0.97	0.50	2.18

	Engine 9: Green	house Gases	5					_
			<b>CO₂</b> ton/yr	N₂O ton/yr	<b>CH</b> ₄ ton/yr	<b>Total GHG</b> Mass Basis ton/yr	Total CO2e ton/yr	
Unit #	Description	GWPs <sup>1</sup>	1	298	25			
E Op	Catornillar C2609 M	mass GHG	9729.71	0.02	0.18	9729.92		
L-9a	Caterpillar 05000 A4	CO <sub>2</sub> e	9729.71	5.46	4.58		9739.76	
E Ob	Maukocha B0204CSLSE	mass GHG	8932.99	0.0168	0.17	8933.18		E-9b was approved in the GCP issued 4/25/2024
E-90	Waukesha P9594051 55	CO <sub>2</sub> e	8932.99	5.02	4.21		8942.22	
E 0*	Worst Case Emissions	mass GHG	9729.71	0.02	0.18	9729.92		
E-9	worst case emissions	CO <sub>2</sub> e	9729.71	5.46	4.58		9739.76	

	Engine 10: Un	controlled																									
		N	Ox	C	0	VO	2	SO2		PI	Μ	PM	10	F	M2.5		H <sub>2</sub> S	Aceta	dehyde	Acrole	ein	Ben	zene	Forma	aldehyde	Total H	HAPs
Unit #	Description	lb/hr	tpy	lb/hr	tpy	lb/hr t	ру	lb/hr t	ру	lb/hr	ton/yr	lb/hr t	ру	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr t	ру	lb/hr	tpy	lb/hr	tpy	lb/hr t	tpy
E-10a	Caterpillar G3612 A4	2.48	3 10.86	24.39	106.82	6.04	26.43	0.15	0.64	0.28	1.24	0.28	1.24	0.2	.8 1.2	4 -	-	0.236	1.036	0.145	0.637	0.012	0.055	1.5	7 6.88	1.98	8.69
E-10b	Waukesha 12V275GL	2.48	3 10.86	19.84	86.91	4.17	18.25	0.13	0.57	0.25	1.12	0.25	1.12	2 0.2	.5 1.1	2 -	-	0.213	0.934	0.131	0.575	0.011	0.049	0.4	1 1.81	0.79	3.44
E-10*	Worst Case Emissions	2.48	3 10.86	24.39	106.82	6.04	26.43	0.15	0.64	0.28	1.24	0.28	1.24	0.2	8 1.2	4		0.24	1.04	0.15	0.64	0.01	0.05	1.5	7 6.88	1.98	8.69

	Engine 10: Co	ontrolled																										
		NOx		CO		VOC		SO2	2	F	PM	PN	110		PM2.5		H <sub>2</sub>	<sub>2</sub> S	Acetalo	dehyde	Acro	olein	Benz	zene	Forma	aldehyde	Tota	l HAPs
Unit #	Description	lb/hr tpy	,	lb/hr tr	ру	lb/hr tpy		lb/hr t	ру	lb/hr	ton/yr	lb/hr	tpy	lb/hr	tpy		lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
E-10a	Caterpillar G3612 A4	2.48	10.86	2.48	10.86	2.07	9.05	0.15	0.64	0.28	3 1.24	0.28	1.24	1 0.	28	1.24	-	-	0.236	1.036	0.145	0.637	0.012	0.055	0.2	5 1.09	0.66	5 2.89
E-10b	Waukesha 12V275GL	2.48	10.86	1.39	6.08	2.08	9.13	0.13	0.57	0.25	5 1.12	0.25	1.12	2 0.	25	1.12	-	-	0.213	0.934	0.131	0.575	0.011	0.049	0.0	8 0.36	0.45	5 1.99
E-10*	Worst Case Emissions	2.48	10.86	2.48	10.86	2.08	9.13	0.15	0.64	0.28	3 1.24	0.28	1.24	ι O.	28	1.24			0.24	1.04	0.15	0.64	0.01	0.05	0.2	5 1.09	0.66	5 2.89

	Engine 10: Greer	nhouse Gase	S				
			CO2 ton/yr	<b>N₂O</b> ton/yr	<b>CH₄</b> ton/yr	<b>Total GHG</b> Mass Basis ton/yr <sup>4</sup>	Total CO₂e ton/yr <sup>5</sup>
Unit #	Description	GWPs <sup>1</sup>	1	298	25		
E 10a	Catornillar C3612 M	mass GHG	14492.74	0.03	0.27	14493.04	
L-10a		CO₂e	14492.74	8.14	6.83		14507.71
E 10h	Waukasha 12V/27ECI	mass GHG	13074.78	0.02	0.25	13075.05	
E-100	Waukesha 12V275GL	CO <sub>2</sub> e	13074.78	7.34	6.16		13088.29
E 10*		mass GHG	14492.74	0.03	0.27	14493.04	
E-10 <sup>-</sup>		CO <sub>2</sub> e	14492.74	8.14	6.83		14507.71

Unit:	E-1, E-2	
Model: 4SLB	Caterpillar G3516B	
	1380 hp	Mfg. specs
Fuel Consumption:	8210 Btu/hp-hr	Mfg. specs
Fuel Heating Value:	1111.00 Btu/scf	Facility Specific
Daily Fuel Usage:	244748 scf/day	Calculated
Hourly Fuel Usage:	10198 scf/hr	Calculated
Annual Fuel Usage:	89.33 MMscf/yr	Calculated

## Uncontrolled Emissions

	NO <sub>x</sub> <sup>1</sup>	CO1	VOC1	SO22	PM <sup>3</sup>	Formaldehyde <sup>1</sup>	Acetaldehyde <sup>4</sup>	Acrolein <sup>4</sup>	Benzene <sup>4</sup>	E-Benzene <sup>4</sup>	<b>Toluene</b> <sup>4</sup>	Xylene <sup>4</sup>	Total HAP	Units
Emission Factors	0.55	3.11	1.67		0.037	0.43								g/hp-hr
AP-42					0.010		0.00836	0.00514	0.00044	0.0000397	0.000408	0.000184		lb/MMBtu
				0.020										gr/scf
Hourly Totals	1.67	9.46	5.08	0.058	0.11	1.31	0.09	0.058	0.0050	0.00045	0.0046	0.0021	1.47	lb/hr
Annual Totals	7.33	41.44	22.25	0.26	0.50	5.73	0.41	0.26	0.022	0.0020	0.020	0.009	6.45	ton/yr

## **Controlled Emissions**

	NO <sub>x</sub> <sup>1</sup>	CO1	VOC1	<b>SO</b> <sub>2</sub> <sup>2</sup>	PM <sup>3</sup>	Formaldehyde <sup>1</sup>	Acetaldehyde <sup>4</sup>	Acrolein <sup>4</sup>	Benzene <sup>4</sup>	E-Benzene <sup>4</sup>	<b>Toluene</b> <sup>4</sup>	Xylene <sup>4</sup>	Total HAP	Units
Emission Factors	0.55	0.62	0.58		0.037	0.086								g/hp-hr
AP-42					0.010		0.00836	0.00514	0.00044	0.0000397	0.000408	0.000184		lb/MMBtu
				0.020										gr/scf
Percent Reduction	0.0%	80.1%	65.3%			80.0%								
Hourly Totals	1.67	1.89	1.76	0.058	0.11	0.26	0.09	0.058	0.0050	0.00045	0.0046	0.0021	0.43	lb/hr
Annual Totals	7.33	8.26	7.73	0.26	0.50	1.15	0.41	0.26	0.022	0.0020	0.020	0.009	1.87	ton/yr

GHG Calculations						_
	C025	N₂O <sup>5</sup>	CH₄⁵	CO₂e⁵		
	53.06	0.0001	0.001		kg/MMBtu	40 CFR 98 Subpart C Tables C-1 and C-2
	1	298	25		GWP	40 CFR 98 Table A-1
	5804.93	0.01	0.11	5805.06	tpy	
	5804.93	3.26	2.74	5810.93	tpy CO2e	

Converted EF for AECT \*VOC EFs include Formaldehyde

<sup>1</sup> Emissions factors are referenced from the catalyst spec sheet.

 $^2$  SO<sub>2</sub> is calculated based on the default fuel sulfur content from AECT of 0.002 grains total sulfur per scf.

<sup>3</sup> Assumes  $PM_{10} = PM_{2.5}$  (condensable and filterable particulate), referenced from AP-42 Table 3.2-2.

<sup>4</sup> HAPs emissions factors are referenced from AP-42 Table 3.2-2.

HAPs include: Formaldehyde, Acetaldehyde, Acrolein, Benzene, Ethylbenzene, N-Hexane, Toluene, and Xylene HAP emission factors were adjusted using the heat value of gas from site and standard 1020 Btu/scf

 $^5$  N2O, CH4, and CO2 tpy Emission Rate = EF \* Fuel Usage \* Fuel Heat Value \*2.20462 lb/kg \* 1 ton/2000 lb CO<sub>2</sub>e tpy Emission Rate = CO<sub>2</sub> Emission Rate + N<sub>2</sub>O Emission Rate \* GWP Factor + CH<sub>4</sub> Emission Rate \* GWP Factor

Velocity	109.49 ft/s	calculated
Flow Rate	9127 acfm	catalyst spec
Flow rate	152 acfs	calculated
Area	1.39 ft^2	calculated
Stack Diameter	1.33 ft	from previous application
Stack Height	25 ft	client specified
Temperature	993 F	catalyst spec

Unit:	E-4	
Model: 4SLB	Caterpillar G3606 A4	
	1875 hp	Mfg. specs
Fuel Consumption:	6649 Btu/hp-hr	Mfg. specs
Fuel Heating Value:	1111.00 Btu/scf	Facility Specific
Daily Fuel Usage:	269311 scf/day	Calculated
Hourly Fuel Usage:	11221 scf/hr	Calculated
Annual Fuel Usage:	98.30 MMscf/yr	Calculated

### Uncontrolled Emissions

	NO <sub>x</sub> <sup>1</sup>	CO1	VOC1	<b>SO</b> <sub>2</sub> <sup>2</sup>	PM <sup>3</sup>	Formaldehyde <sup>4</sup>	Acetaldehyde <sup>4</sup>	Acrolein <sup>4</sup>	<b>Benzene</b> <sup>4</sup>	E-Benzene <sup>4</sup>	<b>Toluene</b> <sup>4</sup>	Xylene <sup>4</sup>	Total HAP	Units
Emission Factors	0.50	2.20	0.69		0.030	0.16								g/hp-hr
AP-42					0.010	0.0528	0.00836	0.00514	0.00044	0.0000397	0.000408	0.000184		lb/MMBtu
				0.020										gr/scf
Hourly Totals	2.07	9.09	2.85	0.064	0.12	0.66	0.10	0.064	0.0055	0.00049	0.0051	0.0023	0.84	lb/hr
Annual Totals	9.05	39.83	12.49	0.28	0.55	2.88	0.46	0.28	0.024	0.0022	0.022	0.010	3.68	ton/yr

#### Controlled Emissions NO<sub>x</sub><sup>1</sup> CO<sup>1</sup> VOC<sup>1</sup> **SO**<sub>2</sub><sup>2</sup> PM<sup>3</sup> Formaldehyde<sup>1</sup> Acetaldehyde<sup>4</sup> Acrolein<sup>4</sup> E-Benzene<sup>4</sup> Toluene<sup>4</sup> Xylene<sup>4</sup> Total HAP Units Benzene<sup>4</sup> g/hp-hr Emission Factors 0.50 0.50 0.30 0.030 0.020 AP-42 0.010 0.00836 0.00514 0.00044 0.0000397 0.000408 0.000184 lb/MMBtu 0.020 gr/scf Percent Reduction 0.0% 77.3% 56.5% 87.4% Hourly Totals 2.07 2.07 1.24 0.064 0.12 0.08 0.10 0.064 0.0055 0.00049 0.0051 0.0023 0.26 lb/hr Annual Totals 9.05 9.05 5.43 0.28 0.55 0.36 0.46 0.28 0.024 0.0022 0.022 0.010 1.16 ton/yr

GHG Calculations						
	C025	N₂O <sup>5</sup>	CH₄⁵	CO₂e <sup>5</sup>		
	53.06	0.0001	0.001		kg/MMBtu	40 CFR 98 Subpart C Tables C-1 and C-2
	1	298	25		GWP	40 CFR 98 Table A-1
	6387.53	0.01	0.12	6387.66	tpy	
	6387.53	3.59	3.01	6394.12	tpy CO2e	

Notes
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Converted EF for AECT \*VOC EFs include Formaldehyde

<sup>1</sup> Emissions factors are referenced from the catalyst spec sheet.

 $^{2}$  SO<sub>2</sub> is calculated based on the default fuel sulfur content from AECT of 0.002 grains total sulfur per scf.

<sup>3</sup> Assumes  $PM_{10} = PM_{2.5}$  (condensable and filterable particulate), referenced from AP-42 Table 3.2-2.

<sup>4</sup> HAPs emissions factors are referenced from AP-42 Table 3.2-2.

HAPs include: Formaldehyde, Acetaldehyde, Acrolein, Benzene, Ethylbenzene, N-Hexane, Toluene, and Xylene HAP emission factors were adjusted using the heat value of gas from site and standard 1020 Btu/scf

<sup>5</sup> N<sub>2</sub>O, CH<sub>4</sub>, and CO<sub>2</sub> tpy Emission Rate = EF \* Fuel Usage \* Fuel Heat Value \*2.20462 lb/kg \* 1 ton/2000 lb CO<sub>2</sub>e tpy Emission Rate = CO<sub>2</sub> Emission Rate + N<sub>2</sub>O Emission Rate \* GWP Factor + CH<sub>4</sub> Emission Rate \* GWP Factor

rly	lotais		
ual	Totals		

Stack and Exhast Parameters										
Velocity	63.70 ft/s	calculated								
Flow Rate	12008 acfm	catalyst spec								
Flow rate	200 acfs	calculated								
Area	3.14 ft^2	calculated								
Stack Diameter	2 ft	from previous application								
Stack Height	27.25 ft	client specified								
Temperature	809 F	catalyst spec								

E-5, E-6, E-7, E-8, E-9b	
Waukesha P9394GSI S5	
2500 hp	Mfg. specs
6974 Btu/hp-hr	Mfg. specs
1111.00 Btu/scf	Facility Specific
376634 scf/day	Calculated
15693 scf/hr	Calculated
137.47 MMscf/yr	Calculated
	E-5, E-6, E-7, E-8, E-9b Waukesha P9394GSI S5 2500 hp 6974 Btu/hp-hr 1111.00 Btu/scf 376634 scf/day 15693 scf/hr 137.47 MMscf/yr

### Uncontrolled Emissions

	NO <sub>x</sub> <sup>1</sup>	CO1	VOC1	SO <sub>2</sub> <sup>2</sup>	PM <sup>3</sup>	Formaldehyde <sup>1</sup>	Acetaldehyde <sup>4</sup>	Acrolein <sup>4</sup>	Benzene <sup>4</sup>	E-Benzene <sup>4</sup>	Toluene <sup>4</sup>	Xylene <sup>4</sup>	Total HAP	Units
Emission Factors	11.97	6.06	0.60		0.061	0.05								g/hp-hr
AP-42					0.019		0.00279	0.00263	0.00158	0.0000248	0.000558	0.000195		lb/MMBtu
				0.020										gr/scf
Hourly Totals	65.97	33.40	3.307	0.0897	0.338	0.276	0.0486	0.0459	0.02755	0.000432	0.00973	0.00340	0.411	lb/hr
Annual Totals	288.96	146.29	14.484	0.393	1.482	1.207	0.2131	0.2008	0.1207	0.001894	0.0426	0.01489	1.801	ton/yr

### Controlled Emissions

				2	2				4					
	NOx	СО	VOC	SO <sub>2</sub> <sup>2</sup>	PM <sup>3</sup>	Formaldehyde <sup>1</sup>	Acetaldehyde <sup>4</sup>	Acrolein <sup>4</sup>	Benzene <sup>4</sup>	E-Benzene <sup>4</sup>	<b>Toluene</b> <sup>4</sup>	Xylene⁴	Total HAP	Units
Emission Factors	0.30	0.40	0.25		0.061	0.04								g/hp-hr
AP-42					0.019		0.00279	0.00263	0.00158	0.0000248	0.000558	0.000195		lb/MMBtu
				0.020										gr/scf
Percent Reduction	97.49%	93.40%	58.33%			20.00%								
Hourly Totals	1.653	2.205	1.378	0.0897	0.338	0.220	0.0486	0.0459	0.02755	0.000432	0.00973	0.00340	0.356	lb/hr
Annual Totals	7.24	9.66	6.035	0.393	1.482	0.966	0.2131	0.2008	0.1207	0.001894	0.0426	0.01489	1.560	ton/yr

GHG Calculations						_
	C025	N₂O <sup>5</sup>	CH₄⁵	CO₂e <sup>5</sup>		
	53.06	0.0001	0.001		kg/MMBtu	40 CFR 98 Subpart C Tables C-1 and C
	1	298	25		GWP	40 CFR 98 Table A-1
	8932.99	0.01684	0.168	8933.18	tpy	
	8932.99	5.02	4.21	8942.22	tpv CO2e	

Stack and Exhast I	Parameters	
Velocity	55.30 ft/s	calculated
Flow rate	10423 acfm	catalyst spec sheet
Flow rate	173.72 acfs	calculated
Area	3.142 ft^2	calculated
Stack Diameter	2 ft	client specification
Stack Height	24.5 ft	client specification
Temperature	1066 F	catalyst spec sheet

Notes

Converted EF for AECT \*VOC EFs include Formaldehyde <sup>1</sup> Emissions factors are referenced from the catalyst spec sheet.

 $^2$  SO<sub>2</sub> is calculated based on the default fuel sulfur content from AECT of 0.002 grains total sulfur per scf.

<sup>3</sup> Assumes  $PM_{10} = PM_{2.5}$  (condensable and filterable particulate), referenced from AP-42 Table 3.2-2.

<sup>4</sup> HAPs emissions factors are referenced from AP-42 Table 3.2-2.

HAPs include: Formaldehyde, Acetaldehyde, Acrolein, Benzene, Ethylbenzene, N-Hexane, Toluene, and Xylene

HAP emission factors were adjusted using the heat value of gas from site and standard 1020 Btu/scf

<sup>5</sup> N<sub>2</sub>O, CH<sub>4</sub>, and CO<sub>2</sub> tpy Emission Rate = EF \* Fuel Usage \* Fuel Heat Value \*2.20462 lb/kg \* 1 ton/2000 lb

Unit:	E-9a	
Model: 4SLB	Caterpillar G3608 A4	
	2500 hp	Mfg. specs
Fuel Consumption:	7596 Btu/hp-hr	Mfg. specs
Fuel Heating Value:	1111.00 Btu/scf	Facility Specific
Daily Fuel Usage:	410225 scf/day	Calculated
Hourly Fuel Usage:	17093 scf/hr	Calculated
Annual Fuel Usage:	149.73 MMscf/yr	Calculated

### Uncontrolled Emissions

	NO <sub>x</sub> <sup>1</sup>	CO <sup>1</sup>	VOC1	SO <sub>2</sub> <sup>2</sup>	PM <sup>3</sup>	Formaldehyde <sup>1</sup>	Acetaldehyde <sup>4</sup>	Acrolein <sup>4</sup>	Benzene <sup>4</sup>	E-Benzene <sup>4</sup>	Toluene <sup>4</sup>	Xylene <sup>4</sup>	Total HAP	Units
Emission Factors	0.30	2.25	0.42		0.034	0.12								g/hp-hr
AP-42					0.010		0.00836	0.00514	0.00044	0.0000397	0.000408	0.000184		lb/MMBtu
				0.020										gr/scf
Hourly Totals	1.65	12.40	2.31	0.098	0.19	0.66	0.16	0.098	0.0084	0.00075	0.0077	0.0035	0.94	lb/hr
Annual Totals	7.24	54.32	10.14	0.43	0.83	2.90	0.70	0.43	0.037	0.0033	0.034	0.015	4.11	ton/yr

Controlled Emissions														
	NOx1	CO1	VOC1	SO <sub>2</sub> <sup>2</sup>	PM <sup>3</sup>	Formaldehyde <sup>1</sup>	Acetaldehyde <sup>4</sup>	Acrolein <sup>4</sup>	Benzene <sup>4</sup>	E-Benzene <sup>4</sup>	Toluene <sup>4</sup>	Xylene <sup>4</sup>	Total HAP	Units
Emission Factors	0.30	0.40	0.30		0.034	0.040								g/hp-hr
AP-42					0.010		0.00836	0.00514	0.00044	0.0000397	0.000408	0.000184		lb/MMBtu
				0.020										gr/scf
Percent Reduction	0.0%	82.2%	28.6%			66.7%								
Hourly Totals	1.65	2.20	1.65	0.098	0.19	0.22	0.16	0.098	0.0084	0.00075	0.0077	0.0035	0.50	lb/hr
Annual Totals	7.24	9.66	7.24	0.43	0.83	0.97	0.70	0.43	0.037	0.0033	0.034	0.015	2.18	ton/yr

## GHG Calculations

CO2 3	N <sub>2</sub> O <sup>3</sup>	CH₄°	CO <sub>2</sub> e <sup>3</sup>		
53.06	0.0001	0.001		kg/MMBtu	40 CFR 98 Subpart C Tables C-1 and C-2
1	298	25		GWP	40 CFR 98 Table A-1
9729.71	0.02	0.18	9729.92	tpy	
9729.71	5.46	4.58	9739.76	tpy CO2e	

Ν	0	te	es:
	~	~~	

Converted EF for AECT \*VOC EFs include Formaldehyde

<sup>1</sup> Emissions factors are referenced from the catalyst spec sheet.

 $^2$  SO<sub>2</sub> is calculated based on the default fuel sulfur content from AECT of 0.002 grains total sulfur per scf.

<sup>3</sup> Assumes PM<sub>10</sub> = PM<sub>2.5</sub> (condensable and filterable particulate), referenced from AP-42 Table 3.2-2.

<sup>4</sup> HAPs emissions factors are referenced from AP-42 Table 3.2-2.

HAPs include: Formaldehyde, Acetaldehyde, Acrolein, Benzene, Ethylbenzene, N-Hexane, Toluene, and Xylene

HAP emission factors were adjusted using the heat value of gas from site and standard 1020 Btu/scf

 $^5\,$  N2O, CH4, and CO2 tpy Emission Rate = EF \* Fuel Usage \* Fuel Heat Value \*2.20462 lb/kg \* 1 ton/2000 lb

Velocity	85.75 ft/s	calculated	
Flow Rate	16164 acfm	catalyst spec	
Flow rate	269 acfs	calculated	
Area	3.14 ft^2	calculated	
Stack Diameter	2 ft	client specified	
Stack Height	27.25 ft	client specified	
Temperature	812 F	catalyst spec	

Unit:	E-10a	
Model: 4SLB	Caterpillar G3612 A4	
	3750 hp	Mfg. specs
Fuel Consumption:	7543 Btu/hp-hr	Mfg. specs
Fuel Heating Value:	1111.00 Btu/scf	Facility Specific
Daily Fuel Usage:	611044 scf/day	Calculated
Hourly Fuel Usage:	25460 scf/hr	Calculated
Annual Fuel Usage:	223.03 MMscf/yr	Calculated

### Uncontrolled Emissions

	NO <sub>x</sub> <sup>1</sup>	CO1	VOC1	SO <sub>2</sub> <sup>2</sup>	PM <sup>3</sup>	Formaldehyde <sup>1</sup>	Acetaldehyde <sup>4</sup>	Acrolein <sup>4</sup>	Benzene <sup>4</sup>	E-Benzene <sup>4</sup>	Toluene⁴	Xylene⁴	Total HAP	Units
Emission Factors	0.30	2.95	0.73		0.034	0.19								g/hp-hr
AP-42					0.010		0.00836	0.00514	0.00044	0.0000397	0.000408	0.000184		lb/MMBtu
				0.020										gr/scf
Hourly Totals	2.48	24.39	6.04	0.145	0.28	1.57	0.24	0.145	0.0124	0.00112	0.0115	0.0052	1.98	lb/hr
Annual Totals	10.86	106.82	26.43	0.64	1.24	6.88	1.04	0.64	0.055	0.0049	0.051	0.023	8.69	ton/yr

Controlled Emissions														
	NO <sup>1</sup>	CO1	VOC1	SO <sub>2</sub> <sup>2</sup>	PM <sup>3</sup>	Formaldehyde <sup>1</sup>	Acetaldehyde <sup>4</sup>	Acrolein <sup>4</sup>	Benzene <sup>4</sup>	E-Benzene <sup>4</sup>	Toluene <sup>4</sup>	Xylene <sup>4</sup>	Total HAP	Units
Emission Factors	0.30	0.30	0.25		0.034	0.030								g/hp-hr
AP-42					0.010		0.00836	0.00514	0.00044	0.0000397	0.000408	0.000184		lb/MMBtu
				0.020										gr/scf
Percent Reduction	0.0%	89.8%	65.8%			84.2%								
Hourly Totals	2.48	2.48	2.07	0.145	0.28	0.25	0.24	0.145	0.0124	0.00112	0.0115	0.0052	0.66	lb/hr
Annual Totals	10.86	10.86	9.05	0.64	1.24	1.09	1.04	0.64	0.055	0.0049	0.051	0.023	2.89	ton/yr

#### **GHG Calculations** CO,5 N₂0<sup>5</sup> CH₄⁵ CO₂e⁵ 53.06 0.0001 0.001 kg/MMBtu 40 CFR 98 Subpart C Tables C-1 and C-2 40 CFR 98 Table A-1 1 298 25 GWP 14492.74 0.03 0.27 14493.04 tpy 14492.74 14507.71 8.14 6.83 tpy CO2e

Stack and Exhast Pa	rameters		
Velocity	126.98 ft/s	calculated	
Flow Rate	23936 acfm	mfg.data	
Flow rate	399 acfs		
Area	3.14 ft^2	calculated	
Stack Diameter	2 ft	client specified	
Stack Height	28.58 ft	client specified	
Temperature	840 F	client specified	

Notes

Converted EF for AECT \*VOC EFs include Formaldehyde

<sup>1</sup> Emissions factors are referenced from the catalyst spec sheet.

 $^2$  SO<sub>2</sub> is calculated based on the default fuel sulfur content from AECT of 0.002 grains total sulfur per scf.

<sup>3</sup> Assumes PM<sub>10</sub> = PM<sub>2.5</sub> (condensable and filterable particulate), referenced from AP-42 Table 3.2-2.

<sup>4</sup> HAPs emissions factors are referenced from AP-42 Table 3.2-2.

HAPs include: Formaldehyde, Acetaldehyde, Acrolein, Benzene, Ethylbenzene, N-Hexane, Toluene, and Xylene

HAP emission factors were adjusted using the heat value of gas from site and standard 1020 Btu/scf

 $^5\,$  N2O, CH4, and CO2 tpy Emission Rate = EF \* Fuel Usage \* Fuel Heat Value \*2.20462 lb/kg \* 1 ton/2000 lb

Unit:	E-10b	
Model: 4SLB	Waukesha 12V275GL	
	3750 hp	Mfg. specs
Fuel Consumption:	6805 Btu/hp-hr	Mfg. specs
Fuel Heating Value:	1111.00 Btu/scf	Facility Specific
Daily Fuel Usage:	551260 scf/day	Calculated
Hourly Fuel Usage:	22969 scf/hr	Calculated
Annual Fuel Usage:	201.21 MMscf/yr	Calculated

### Uncontrolled Emissions

	NO <sup>1</sup>	CO1	VOC1	SO <sub>2</sub> <sup>2</sup>	PM <sup>3</sup>	Formaldehyde <sup>1</sup>	Acetaldehyde <sup>4</sup>	Acrolein <sup>4</sup>	Benzene <sup>4</sup>	E-Benzene <sup>4</sup>	Toluene⁴	Xylene⁴	Total HAP	Units
Emission Factors	0.30	2.40	0.50		0.031	0.05								g/hp-hr
AP-42					0.010		0.00836	0.00514	0.00044	0.0000397	0.000408	0.000184		lb/MMBtu
				0.020										gr/scf
Hourly Totals	2.48	19.84	4.17	0.131	0.25	0.41	0.21	0.131	0.0112	0.00101	0.0104	0.0047	0.79	lb/hr
Annual Totals	10.86	86.91	18.25	0.57	1.12	1.81	0.93	0.57	0.049	0.0044	0.046	0.021	3.44	ton/yr

Controlled Emissions														
	NO <sub>x</sub> <sup>1</sup>	CO1	VOC1	SO2 <sup>2</sup>	PM <sup>3</sup>	Formaldehyde <sup>1</sup>	Acetaldehyde <sup>4</sup>	Acrolein <sup>4</sup>	Benzene <sup>4</sup>	E-Benzene <sup>4</sup>	<b>Toluene</b> <sup>4</sup>	Xylene <sup>4</sup>	Total HAP	Units
Emission Factors	0.30	0.17	0.25		0.031	0.010								g/hp-hr
AP-42					0.010		0.00836	0.00514	0.00044	0.0000397	0.000408	0.000184		lb/MMBtu
				0.020										gr/scf
Percent Reduction	0.0%	93.0%	50.0%			80.0%								
Hourly Totals	2.48	1.39	2.08	0.131	0.25	0.08	0.21	0.131	0.0112	0.00101	0.0104	0.0047	0.45	lb/hr
Annual Totals	10.86	6.08	9.13	0.57	1.12	0.36	0.93	0.57	0.049	0.0044	0.046	0.021	1.99	ton/yr

kg/MMBtu 40 CFR 98 Subpart C Tables C-1 and C-2 40 CFR 98 Table A-1

#### **GHG Calculations** CO,5 N₂0<sup>5</sup> 53.06 0.0001 1 298 13074.78 0.02

13074.78

Stack and Exhast Pa	ameters	
Velocity	88.02 ft/s	calculated
Flow Rate	25925 acfm	catalyst spec
Flow rate	432 acfs	
Area	4.91 ft^2	calculated
Stack Diameter	2.5 ft	client specified
Stack Height	34.92 ft	client specified
Temperature	836 F	catalyst spec

Notes

Converted EF for AECT \*VOC EFs include Formaldehyde

CH₄⁵

0.001

25

0.25

<sup>1</sup> Emissions factors are referenced from the catalyst spec sheet.

7.34

<sup>2</sup> SO<sub>2</sub> is calculated based on the default fuel sulfur content from AECT of 0.002 grains total sulfur per scf.

CO₂e⁵

13075.05

GWP

tpy

tpy CO2e

<sup>3</sup> Assumes PM<sub>10</sub> = PM<sub>2.5</sub> (condensable and filterable particulate), referenced from AP-42 Table 3.2-2.

6.16 13088.29

<sup>4</sup> HAPs emissions factors are referenced from AP-42 Table 3.2-2.

HAPs include: Formaldehyde, Acetaldehyde, Acrolein, Benzene, Ethylbenzene, N-Hexane, Toluene, and Xylene

HAP emission factors were adjusted using the heat value of gas from site and standard 1020 Btu/scf

 $^{5}$  N<sub>2</sub>O, CH<sub>4</sub>, and CO<sub>2</sub> tpy Emission Rate = EF \* Fuel Usage \* Fuel Heat Value \*2.20462 lb/kg \* 1 ton/2000 lb

Unit:	GEN-4 & GEN-5	
Model: 4SRB	Aggreko GG0400GASCON	
	536 hp	Mfg. specs
Fuel Consumption:	8000 Btu/hp-h	ir assumed, same as previous application
Fuel Heating Value:	1111.00 Btu/scf	Facility Specific
Daily Fuel Usage:	92630 scf/day	Calculated
Hourly Fuel Usage:	3860 scf/hr	Calculated
Annual Fuel Usage:	33.81 MMscf/y	rr Calculated

## Uncontrolled Emissions

	NOx1	CO1	VOC1	SO <sub>2</sub> <sup>2</sup>	PM <sup>3</sup>	Formaldehyde <sup>4</sup>	Acetaldehyde <sup>4</sup>	Acrolein <sup>4</sup>	Benzene <sup>4</sup>	E-Benzene <sup>4</sup>	Toluene <sup>4</sup>	Xylene <sup>4</sup>	Total HAP	Units
Emission Factors	1.00	2.000	0.700		0.070	0.074								g/hp-hr
AP-42					0.019	0.0205	0.00279	0.00263	0.00158	0.0000248	0.000558	0.000195		lb/MMBtu
				0.020										gr/scf
Hourly Totals	1.18	2.36	0.827	0.0221	0.083	0.088	0.0120	0.0113	0.00678	0.000106	0.00239	0.00084	0.121	lb/hr
Annual Totals	5.18	10.35	3.623	0.097	0.365	0.385	0.0524	0.0494	0.0297	0.000466	0.0105	0.00366	0.531	ton/yr

Controlled Emissions														
	NO <sub>x</sub>	со	VOC	SO22	PM <sup>3</sup>	Formaldehyde <sup>4</sup>	Acetaldehyde <sup>4</sup>	Acrolein <sup>4</sup>	Benzene <sup>4</sup>	E-Benzene <sup>4</sup>	Toluene <sup>4</sup>	Xylene <sup>4</sup>	Total HAP	Units
Emission Factors	1.00	2.000	0.774		0.070	0.074								g/hp-hr
AP-42					0.019	0.0205	0.00279	0.00263	0.00158	0.0000248	0.000558	0.000195		lb/MMBtu
				0.020										gr/scf
Percent Reduction	0.00%	0.00%												
Hourly Totals	1.182	2.363	0.915	0.0221	0.083	0.088	0.0120	0.0113	0.00678	0.000106	0.00239	0.00084	0.121	lb/hr
Annual Totals	5.18	10.35	4.006	0.097	0.365	0.385	0.0524	0.0494	0.0297	0.000466	0.0105	0.00366	0.531	ton/yr

#### **GHG** Calculations CO2<sup>5</sup> $N_2O^5$ CH₄⁵ CO₂e<sup>5</sup> 0.0001 0.001 kg/MMBtu 40 CFR 98 Subpart Tables 53.06 298 25 GWP 40 CFR 98 Table A-1 1 2197.00 0.00414 0.041 2197.04 tpy 2197.00 1.23 1.04 2199.27 tpy CO2e

Velocity	205.84 ft/s	calculated	
Flow rate	2425 acfm	client specification	
Flow rate	40.42 acfs		
Area	0.196 ft^2	calculated	
Stack Diameter	0.5 ft	client specification	
Stack Height	15 ft	based on stack calculator	
Temperature	1000 F	from previous permit	

Notes

Converted EF for AECT \*VOC EFs include Formaldehyde

<sup>1</sup> Emissions factors are referenced from the catalyst spec sheet.

 $^2$  SO<sub>2</sub> is calculated based on the default fuel sulfur content from AECT of 0.002 grains total sulfur per scf.

<sup>3</sup> Assumes PM<sub>10</sub> = PM<sub>2.5</sub> (condensable and filterable particulate), referenced from AP-42 Table 3.2-2.

<sup>4</sup> HAPs emissions factors are referenced from AP-42 Table 3.2-2.

HAPs include: Formaldehyde, Acetaldehyde, Acrolein, Benzene, Ethylbenzene, N-Hexane, Toluene, and Xylene HAP emission factors were adjusted using the heat value of gas from site and standard 1020 Btu/scf

 $^5\,$  N2O, CH4, and CO2 tpy Emission Rate = EF \* Fuel Usage \* Fuel Heat Value \*2.20462 lb/kg \* 1 ton/2000 lb

## Heater/Reboiler Calcs New Source Review Permit Horned Frog Compressor Station Delaware G&P, LLC

				Fuel Lower	Annual					Detential t	
EDN	EIN	Description	Rated Duty	Value	Hours	Correction	Pollutant	Emission Factor <sup>a</sup>	Unit	Hourly (lb/br)	Annual Č
EFIN	FIN	Description	(IVIIVIBLU/III)	(Blu/Sll)	(111/ 91)	Factor	Pollutant	Factor	onit	(10/111)	(1/ y1)
HT-1	HT-1	DEHY1 Glycol Reboiler	0.50	1,111	8,760	1.00	NO <sub>x</sub>	100	lb/MMscf	0.05	0.20
							CO	84	lb/MMscf	0.04	0.17
							PM <sup>d</sup>	7.6	lb/MMscf	0.00	0.01
							SO <sub>2</sub> <sup>e</sup>	0.00286	lb S/Mscf	0.0026	0.011
							VOC	5.5	lb/MMscf	0.002	0.011
							CH <sub>2</sub> O	0.075	lb/MMscf	0.00003	0.0001
						GWP				Mass tpy	tpy CO <sub>2</sub> e
						1	CO <sub>2</sub> <sup>5</sup>	53.0600	kg/MMBtu	256.18	256.18
						298	$N_2O^5$	0.0001	kg/MMBtu	0.00048	0.1439
						25	CH4 <sup>5</sup>	0.0010	kg/MMBtu	0.00483	0.1207
							$CO_2e^5$			256.19	256.44
HT-2	HT-2	DEHY2 Glycol Reboiler	1.00	1,111	8,760	1.00	NO <sub>x</sub>	100	lb/MMscf	0.09	0.39
							СО	84	lb/MMscf	0.08	0.33
							PM <sup>d</sup>	7.6	lb/MMscf	0.007	0.03
							SO <sub>2</sub> <sup>e</sup>	0.00286	lb S/Mscf	0.0051	0.023
							VOC	5.5	lb/MMscf	0.005	0.02
							CH <sub>2</sub> O	0.075	lb/MMscf	0.00007	0.0003
						GWP				Mass tpy	tpy CO <sub>2</sub> e
						1	CO <sub>2</sub> <sup>5</sup>	53.0600	kg/MMBtu	512.36	512.36
						298	$N_2O^5$	0.0001	kg/MMBtu	0.00097	0.2878
						25	CH <sub>4</sub> <sup>5</sup>	0.0010	kg/MMBtu	0.00966	0.2414
							$CO_2e^5$			512.37	512.89

<sup>a</sup> Unless otherwise noted, emission factors are from AP-42 Tables 1.4-1, 1.4-2, and 1.4-3 (dated 7/98). GHG emission factors are from 40 cfr 98

<sup>b</sup> Example calculations for hourly PTE CO and SO<sub>2</sub> for EPN H-1 follow:

CO (lb/hr) = (Rated Duty, MMBtu/hr)\*(Correction Factor)/(Fuel Heating Value, Btu/scf)\*(Emission Factor, lb/MMscf)

CO (lb/hr) = (0.50 MMBtu/hr)\*(1.00)/(1,111 Btu/scf)\*(84 lb/MMscf)

= 0.04 lb/hr CO

Sulfur content of 2 gr S/100 scf or 0.00286 lb S/Mscf is conservatively assumed for variance in field gas quality.

SO<sub>2</sub> (lb/hr) = (Rated Duty, MMBtu/hr)/(Fuel Heating Value, Btu/scf)\*(1000scf/Mscf)\*(Sulfur Content, lb S/Mscf gas)\*(64.06 lb SO<sub>2</sub>/32.06 lb S)

SO<sub>2</sub> (lb/hr) = (0.50 MMBtu/hr)/(1,111 Btu/scf)\*(1000scf/Mscf)\*(0.00286 lb S/Mscf gas)\*(64.06 lb SO2/32.06 lb S)

= 0.0026 lb/hr SO<sub>2</sub>

 $^{\rm c}$  An example calculation for annual PTE CO for EPN H-1 follows:

CO (T/yr) = (Hourly PTE, lb/hr)\*(Annual Operating Hours, hr/yr)/(2,000 lb/T)

CO (T/yr) = (0.04 lb/hr)\*(8,760 hr/yr)/(2,000 lb/T)

= 0.17 T/yr CO

<sup>d</sup> All PM is assumed to be less than 2.5 microns in diameter per footnote "c" of AP-42 Table 1.4-2.

<sup>e</sup> A material balance approach was used to estimate the SO<sub>2</sub> emission rates using the maximum sulfur concentration in the natural gas.

### Dehydrator Calcs New Source Review Permit Horned Frog Compressor Station Delaware G&P, LLC

			DEHY1 2	5 MMSCFD			DEHY2 100 MMSCFD					
DEHY1	Regenerate	or Still Vent	Rege	nerator	Flash	n Tank	Regenera	tor Still Vent	Reger	nerator	Flas	sh Tank
25 MMSCFD	Uncon	trolled	Con	trolled	Uncor	ntrolled	Unco	ntrolled	Cont	trolled	Unco	ontrolled
Component	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
Carbon Dioxide	0.979	4.286	62.335	273.026	3.376	14.785	1.134	4.968	60.164	263.520	3.744	16.399
Hydrogen Sulfide	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
Nitrogen	0.002	0.009	622.499	2726.544	0.212	0.927	0.002	0.011	597.882	2618.722	0.236	1.033
Methane	0.493	2.161	0.010	0.043	14.032	61.461	0.559	2.448	0.011	0.049	15.412	67.504
Ethane	1.280	5.606	0.025	0.112	10.999	48.177	1.340	5.871	0.027	0.117	11.661	51.073
Propane	2.660	11.653	0.053	0.231	12.168	53.297	2.622	11.484	0.052	0.227	12.518	54.829
i-Butane	0.636	2.785	0.012	0.054	2.152	9.427	0.598	2.619	0.012	0.051	2.177	9.536
n-Butane	3.072	13.457	0.059	0.260	7.180	31.448	2.933	12.846	0.057	0.250	7.277	31.874
i-Pentane	1.275	5.585	0.023	0.103	1.907	8.354	1.162	5.091	0.022	0.095	1.909	8.360
n-Pentane	2.017	8.835	0.036	0.159	2.539	11.120	1.752	7.672	0.032	0.140	2.475	10.841
Cyclopentane	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
n-Hexane	4.104	17.977	0.062	0.273	2.516	11.020	3.444	15.086	0.054	0.239	2.467	10.807
Cyclohexane	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
n-Heptane	2.254	9.871	0.024	0.103	0.858	3.759	1.841	8.064	0.021	0.091	0.841	3.685
Methylcyclohexane	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
2,2,4-Trimethylpentane	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
Benzene	4.830	21.155	0.063	0.277	0.252	1.102	4.803	21.036	0.064	0.280	0.265	1.162
Toluene	3.831	16.780	0.030	0.132	0.112	0.489	3.757	16.457	0.031	0.138	0.117	0.512
Ethylbenzene	0.136	0.596	0.000	0.002	0.002	0.011	0.135	0.591	0.001	0.002	0.003	0.011
o-Xylene	0.259	1.135	0.001	0.004	0.004	0.016	0.270	1.182	0.001	0.005	0.004	0.017
m-Xylene	0.821	3.597	0.003	0.013	0.015	0.064	0.805	3.526	0.003	0.014	0.015	0.067
p-Xylene	0.065	0.285	0.000	0.001	0.001	0.005	0.064	0.280	0.000	0.001	0.001	0.006
Triethylene Glycol	0.016	0.072	0.000	0.000	0.003	0.015	0.038	0.168	0.000	0.000	0.003	0.012
Ethylene Glycol	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
Water	67.931	297.539	27.910	122.244	0.364	1.593	266.593	1167.675	26.745	117.142	0.950	4.160
Methanol	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
02	0.000	0.000	120.410	527.395	0.000	0.000	0.000	0.000	115.648	506.538	0.000	0.000
SO2	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
Total VOC	25.96	113.71	0.37	1.61	29.71	130.11	24.19	105.93	0.35	1.53	30.07	131.71
Total HAPs	14.05	61.52	0.16	0.70	2.90	12.71	13.28	58.16	0.15	0.68	2.87	12.58
Total GHG	1.47	6.45	62.34	273.07	17.41	76.25	1.69	7.42	60.18	263.57	19.16	83.90

VRU Capture VRU Downtime VRU Uptime ECD DRE

438

98%

98%

5% hrs/yr 95%

Flash Tank Off Gas is routed to the VRU with 98% capture, with 5% downtime routed to th ECD for 98% DRE.

Regenerator still vent is routed to a BTEX condenser and remaining gas is controlled by the reboiler glow plug for a total control efficiency of 98%

## Dehydrator Calcs New Source Review Permit Horned Frog Compressor Station Delaware G&P, LLC

-										
					DEHY1 2	5 MMSCFD				
Dehydrator Emissions	Flash Tank Uncontrolled		2% Uncaptured by VRU		5% VRU Downtime routed to ECD		Controlled Fla	sh Tank Emissions	Total Regen and Flash Tank Emissions	
	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
Std Vapor Flow MSCFH	0.7	155	0.0	0143	0.7012	0.3071				
VOCs	29.7061	130.1128	0.5941	2.6023	29.1120	6.3755	0.5822	0.1275	1.54	4.34
Benzene	0.2516	1.1022	0.0050	0.0220	0.2466	0.0540	0.0049	0.0011	0.07	0.30
HAPs	2.9013	12.7077	0.0580	0.2542	2.8433	0.6227	0.0569	0.0125	0.28	0.97
Methane	-	61.4614	-	1.2292	-	3.0116	-	0.0602	-	1.33
Carbon Dioxide	-	14.7848	-	0.2957	-	0.7245	-	0.0145	-	273.34

					DEHY2 1	00 MMSCFD					
Dehydrator Emissions	Flash Tank U	Incontrolled	2% Uncaptured by VRU		5% VRU Downtime routed to ECD		Controlled Fla	sh Tank Emissions	Total Regen and Flash Tank Emissions		
	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	
Std Vapor Flow MSCFH	0.7	756	0.0	0155	0.7601	0.3329					
VOCs	30.0702	131.7073	0.6014	2.6341	29.4688	6.4537	0.5894	0.1291	1.54	4.30	
Benzene	0.2654	1.1624	0.0053	0.0232	0.2601	0.0570	0.0052	0.0011	0.07	0.30	
HAPs	2.8726	12.5819	0.0575	0.2516	2.8151	0.6165	0.0563	0.0123	0.27	0.94	
Methane	-	67.5044	-	1.3501	-	3.3077	-	0.0662	-	1.47	
Carbon Dioxide	-	16.3991	-	0.3280	-	0.8036	-	0.0161	-	263.86	

#### Tank and Loading Losses New Source Review Permit Horned Frog Compressor Station Delaware G&P, LLC

Uncontrolled	Emissions

	Condensa	ite Tanks	Gunb	arrel	PW T	Tanks	Condens	ate Tanks	Gun	barrel	PW	Tanks	Condonsat	aloading	Produced W	ator Loading
	Flash	ning	Flas	hing	Flas	hing	Working/	Breathing	Working	/Breathing	Working	/Breathing	condensati	e Loading	FIGURE W	ater Loading
Component	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
Nitrogen	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
Methane	0.62737	2.74789	0.68748	3.01116	0.00552	0.02417	0.03357	0.14702	0.00402	0.01761	0.00094	0.00412	0.00808	0.03537	0.00029	0.00125
CO2	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
Ethane	1.80307	7.89745	2.20940	9.67717	0.00465	0.02038	0.42602	1.86597	0.05534	0.24239	0.00082	0.00360	0.10250	0.44894	0.00025	0.00109
Propane	8.37378	36.67715	11.59661	50.79317	0.01209	0.05296	1.49826	6.56239	0.21831	0.95620	0.00036	0.00156	0.36047	1.57885	0.00011	0.00047
i-Butane	4.43787	19.43786	6.58805	28.85565	0.00530	0.02322	0.66948	2.93232	0.10444	0.45743	0.00003	0.00015	0.16107	0.70549	0.00001	0.00004
n-Butane	16.90532	74.04531	25.61113	112.17677	0.01736	0.07605	2.51842	11.03067	0.40086	1.75578	0.00011	0.00049	0.60591	2.65389	0.00003	0.00015
i-Pentane	9.00155	39.42678	14.02112	61.41250	0.00829	0.03630	1.16203	5.08969	0.19015	0.83285	0.00001	0.00006	0.27957	1.22454	0.00000	0.00002
n-Pentane	11.69077	51.20555	18.30680	80.18378	0.00628	0.02750	1.46127	6.40038	0.24042	1.05303	0.00000	0.00002	0.35157	1.53988	0.00000	0.00000
i-Hexane	4.14217	18.14272	6.55181	28.69691	0.00254	0.01112	0.49384	2.16300	0.08210	0.35961	0.00000	0.00000	0.11881	0.52040	0.00000	0.00000
Hexane	6.92459	30.32972	10.97752	48.08153	0.00281	0.01229	0.79677	3.48985	0.13275	0.58143	0.00000	0.00000	0.19170	0.83963	0.00000	0.00000
2,2,4-Trimethylpentane	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
Benzene	0.36877	1.61520	0.58320	2.55443	0.00047	0.00204	0.02552	0.11179	0.00428	0.01874	0.00002	0.00007	0.00614	0.02690	0.00001	0.00002
Heptane	2.89080	12.66173	4.59742	20.13672	0.00093	0.00408	0.29244	1.28087	0.04891	0.21423	0.00000	0.00000	0.07036	0.30817	0.00000	0.00000
Toluene	0.26222	1.14854	0.41631	1.82344	0.00029	0.00127	0.01746	0.07650	0.00293	0.01281	0.00000	0.00001	0.00420	0.01840	0.00000	0.00000
Octane	0.53189	2.32968	0.84673	3.70867	0.00008	0.00035	0.04405	0.19293	0.00738	0.03231	0.00000	0.00000	0.01060	0.04642	0.00000	0.00000
Ethylbenzene	0.00859	0.03760	0.01365	0.05977	0.00001	0.00004	0.00055	0.00239	0.00009	0.00040	0.00000	0.00000	0.00013	0.00058	0.00000	0.00000
m-Xylene	0.04419	0.19356	0.07026	0.30772	0.00004	0.00019	0.00273	0.01194	0.00046	0.00200	0.00000	0.00000	0.00066	0.00287	0.00000	0.00000
o-Xylene	0.00386	0.01691	0.00613	0.02687	0.00000	0.00002	0.00021	0.00092	0.00004	0.00015	0.00000	0.00000	0.00005	0.00022	0.00000	0.00000
p-Xylene	0.01155	0.05059	0.01837	0.08044	0.00001	0.00005	0.00074	0.00324	0.00012	0.00054	0.00000	0.00000	0.00018	0.00078	0.00000	0.00000
Nonane	0.06981	0.30579	0.11126	0.48733	0.00001	0.00005	0.00452	0.01980	0.00076	0.00332	0.00000	0.00000	0.00109	0.00476	0.00000	0.00000
Decane	0.03429	0.15019	0.05460	0.23915	0.00000	0.00001	0.00177	0.00774	0.00030	0.00130	0.00000	0.00000	0.00043	0.00186	0.00000	0.00000
Water	0.21565	0.94453	2.18943	9.58971	0.00193	0.00845	0.00002	0.00007	0.19622	0.85946	0.12526	0.54864	0.00000	0.00002	0.03800	0.16642
Undecane	0.00032	0.00141	0.00051	52.93421	0.00000	0.01590	0.00002	3.69663	0.00000	0.61607	0.00000	0.00008	0.00000	0.88938	0.00000	0.00003
Total VOC	65.70	287.78	100.37	439.62	0.06	0.25	8.99	39.38	1.43	6.28	0.0005	0.0024	2.16	9.47	0.000163	0.000715
Total HAP	4.84	21.21	7.66	33.55	0.0034	0.015	0.54	2.37	0.09	0.39	0.00002	0.00009	0.13	0.57	0.000006	0.000026

 VRU Capture
 98%

 VRU Downtime
 5%
 438 hrs/yr

 VRU Uptime
 95%
 ECD DRE
 98%

Number of Condensate Tanks Number of Water Tanks Number of Gunbarrels 6 Condensate Tanks - Vapors routed to VRU at 98% capture and 5% downtime. Vapors routed to ECD during VRU downtime. Uncaptured emissions vented at the tanks.
 2 PW Tanks - Vapors routed to VRU at 98% capture and 5% downtime. Vapors routed to ECD during VRU downtime. Uncaptured emissions vented at the tanks.
 1 Gunbarrel - Vapors routed to VRU at 98% capture and 5% downtime. Vapors routed to ECD during VRU downtime. Uncaptured emissions vented at the tanks.

						VOC Er	nissions							
Storage Tanks	Flashing	Emissions	W/B E	Emissions	Total Uncont	rolled Emissions	2% Uncapt	ured by VRU	5% VRU Dowr E	time routed to CD	Controlled Em	/RU Downtime issions	Total Em	issions
	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
Std Vapor MSCFH					0	.503	0.	010	0.4927	0.2158				
TK-1: Condensate Tank 1	10.95	47.96	1.50	6.56	12.45	54.53	0.25	1.09	12.20	2.67	0.24	0.05	0.49	1.14
TK-2: Condensate Tank 2	10.95	47.96	1.50	6.56	12.45	54.53	0.25	1.09	12.20	2.67	0.24	0.05	0.49	1.14
TK-3: Condensate Tank 3	10.95	47.96	1.50	6.56	12.45	54.53	0.25	1.09	12.20	2.67	0.24	0.05	0.49	1.14
TK-5: Condensate Tank 5	10.95	47.96	1.50	6.56	12.45	54.53	0.25	1.09	12.20	2.67	0.24	0.05	0.49	1.14
TK-6: Condensate Tank 6	10.95	47.96	1.50	6.56	12.45	54.53	0.25	1.09	12.20	2.67	0.24	0.05	0.49	1.14
TK-7: Condensate Tank 7	10.95	47.96	1.50	6.56	12.45	54.53	0.25	1.09	12.20	2.67	0.24	0.05	0.49	1.14
CONDLOAD					2.16	9.47	0.04	0.19	2.12	0.46	0.04	0.01	0.09	0.20
Std Vapor MSCFH					0.	6867	0.	014	0.6730	0.2948				
GB-1: Gunbarrel Tank	100.37	439.62	1.43	6.28	101.81	445.91	2.04	8.92	99.77	21.85	2.00	0.44	4.03	9.36
Std Vapor MSCFH					0.	0041	0.	000	0.0040	0.0017				
TK-4: Produced Water Tank 4	0.028	0.124	0.000	0.001	0.029	0.125	0.001	0.002	0.028	0.006	0.00	0.00	0.00	0.00
TK-8: Produced Water Tank 8	0.028	0.124	0.000	0.001	0.029	0.125	0.001	0.002	0.028	0.006	0.00	0.00	0.00	0.00
PWLOAD					0.000	0.001	0.000	0.000	0.000	0.000	0.00	0.00	0.00	0.00

#### Tank and Loading Losses New Source Review Permit Horned Frog Compressor Station Delaware G&P, LLC

						Total HAP	Emissions							
Storage Tanks	Flashing	Emissions	W/B E	Emissions	Total Uncont	rolled Emissions	2% Uncaptu	red at Tanks	5% VRU Dow E	ntime routed to CD	Controlled V Emis	RU Downtime ssions	Total Em	issions
	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
TK-1: Condensate Tank 1	0.81	3.53	0.09	0.39	0.90	3.93	0.02	0.08	0.88	0.19	0.02	0.00	0.04	0.08
TK-2: Condensate Tank 2	0.81	3.53	0.09	0.39	0.90	3.93	0.02	0.08	0.88	0.19	0.02	0.00	0.04	0.08
TK-3: Condensate Tank 3	0.81	3.53	0.09	0.39	0.90	3.93	0.02	0.08	0.88	0.19	0.02	0.00	0.04	0.08
TK-5: Condensate Tank 5	0.81	3.53	0.09	0.39	0.90	3.93	0.02	0.08	0.88	0.19	0.02	0.00	0.04	0.08
TK-6: Condensate Tank 6	0.81	3.53	0.09	0.39	0.90	3.93	0.02	0.08	0.88	0.19	0.02	0.00	0.04	0.08
TK-7: Condensate Tank 7	0.81	3.53	0.09	0.39	0.90	3.93	0.02	0.08	0.88	0.19	0.02	0.00	0.04	0.08
CONDLOAD					0.13	0.57	0.00	0.01	0.13	0.03	0.00	0.00	0.01	0.01
GB-1: Gunbarrel Tank	7.66	33.55	0.09	0.39	7.75	33.94	0.15	0.68	7.59	1.66	0.15	0.03	0.31	0.71
TK-4: Produced Water Tank 4	0.00	0.01	0.00	0.00	0.00	0.01	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
TK-8: Produced Water Tank 8	0.00	0.01	0.00	0.00	0.00	0.01	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
PWLOAD					0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00

						n-Hexane	Emissions							
Storage Tanks	Flashing	Emissions	W/B E	missions	Total Uncontr	olled Emissions	2% Uncaptu	red at Tanks	5% VRU Down	ntime routed to CD	Controlled VF Emis	RU Downtime sions	Total Em	issions
	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
TK-1: Condensate Tank 1	0.69	3.02	0.08	0.36	0.77	3.38	0.02	0.07	0.76	0.17	0.02	0.00	0.031	0.071
TK-2: Condensate Tank 2	0.69	3.02	0.08	0.36	0.77	3.38	0.02	0.07	0.76	0.17	0.02	0.00	0.031	0.071
TK-3: Condensate Tank 3	0.69	3.02	0.08	0.36	0.77	3.38	0.02	0.07	0.76	0.17	0.02	0.00	0.031	0.071
TK-5: Condensate Tank 5	0.69	3.02	0.08	0.36	0.77	3.38	0.02	0.07	0.76	0.17	0.02	0.00	0.031	0.071
TK-6: Condensate Tank 6	0.69	3.02	0.08	0.36	0.77	3.38	0.02	0.07	0.76	0.17	0.02	0.00	0.031	0.071
TK-7: Condensate Tank 7	0.69	3.02	0.08	0.36	0.77	3.38	0.02	0.07	0.76	0.17	0.02	0.00	0.031	0.071
CONDLOAD					0.12	0.52	0.00	0.01	0.12	0.03	0.00	0.00	0.005	0.011
GB-1: Gunbarrel Tank	6.55	2.55	0.08	0.36	6.63	2.91	0.13	0.06	6.50	0.14	0.13	0.00	0.263	0.061
TK-4: Produced Water Tank 4	0.00	0.01	0.00	0.00	0.00	0.01	0.00	0.00	0.00	0.00	0.00	0.00	0.000	0.000
TK-8: Produced Water Tank 8	0.00	0.01	0.00	0.00	0.00	0.01	0.00	0.00	0.00	0.00	0.00	0.00	0.000	0.000
PWLOAD					0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.000	0.000

						Benzene	Emissions							
	Flaching	Emissions	W//D E	missions	Total Uncentu	collod Emissions	2º/ Uncontu	ured at Tanks	5% VRU Dow	ntime routed to	Controlled V	/RU Downtime	Total Em	lasions
Storage Tanks	Fidshing	ETTISSIOTIS	VV/D E	missions	Total Offcontr	oneu ennissions	2% Uncaptu	ireu at Taliks	F	CD	Emi	ssions	TOLAI EIII	ISSIONS
	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
TK-1: Condensate Tank 1	0.06	0.27	0.00	0.02	0.07	0.29	0.00	0.01	0.06	0.01	0.00	0.00	0.003	0.006
TK-2: Condensate Tank 2	0.06	0.27	0.00	0.02	0.07	0.29	0.00	0.01	0.06	0.01	0.00	0.00	0.003	0.006
TK-3: Condensate Tank 3	0.06	0.27	0.00	0.02	0.07	0.29	0.00	0.01	0.06	0.01	0.00	0.00	0.003	0.006
TK-5: Condensate Tank 5	0.06	0.27	0.00	0.02	0.07	0.29	0.00	0.01	0.06	0.01	0.00	0.00	0.003	0.006
TK-6: Condensate Tank 6	0.06	0.27	0.00	0.02	0.07	0.29	0.00	0.01	0.06	0.01	0.00	0.00	0.003	0.006
TK-7: Condensate Tank 7	0.06	0.27	0.00	0.02	0.07	0.29	0.00	0.01	0.06	0.01	0.00	0.00	0.003	0.006
CONDLOAD					0.01	0.03	0.00	0.00	0.01	0.00	0.00	0.00	0.000	0.001
GB-1: Gunbarrel Tank	0.58	2.55	0.00	0.02	0.59	2.57	0.01	0.05	0.58	0.13	0.01	0.00	0.023	0.054
TK-4: Produced Water Tank 4	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.000	0.000
TK-8: Produced Water Tank 8	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.000	0.000
PWLOAD					0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.000	0.000

						GHG Em	nissions							
	Flashing	Emissions	W/B E	missions	Total Uncontr	olled Emissions	2% Uncaptu	red at Tanks	5% VRU Dow	ntime routed to	Controlled V	/RU Downtime	Total En	nissions
Storage Tanks	CH <sub>4</sub>	CO <sub>2</sub> e	CH <sub>4</sub>	CO <sub>2</sub> e	CH <sub>4</sub>	CO <sub>2</sub> e	CH₄	CO <sub>2</sub> e	CH <sub>4</sub>	CO <sub>2</sub> e	CH <sub>4</sub>	CO <sub>2</sub> e	CH <sub>4</sub>	CO <sub>2</sub> e
	tpy	tpy	tpy	tpy	tpy	tpy	tpy	tpy	tpy	tpy	tpy	tpy	tpy	tpy
TK-1: Condensate Tank 1	0.46	0.00	0.02	0.00	0.48	0.00	0.01	0.00	0.47	0.00	0.01	0.00	0.019	0.000
TK-2: Condensate Tank 2	0.46	0.00	0.02	0.00	0.48	0.00	0.01	0.00	0.47	0.00	0.01	0.00	0.019	0.000
TK-3: Condensate Tank 3	0.46	0.00	0.02	0.00	0.48	0.00	0.01	0.00	0.47	0.00	0.01	0.00	0.019	0.000
TK-5: Condensate Tank 5	0.46	0.00	0.02	0.00	0.48	0.00	0.01	0.00	0.47	0.00	0.01	0.00	0.019	0.000
TK-6: Condensate Tank 6	0.46	0.00	0.02	0.00	0.48	0.00	0.01	0.00	0.47	0.00	0.01	0.00	0.019	0.000
TK-7: Condensate Tank 7	0.46	0.00	0.02	0.00	0.48	0.00	0.01	0.00	0.47	0.00	0.01	0.00	0.019	0.000
CONDLOAD					0.04	0.00	0.00	0.00	0.03	0.00	0.00	0.00	0.001	0.000
GB-1: Gunbarrel Tank	3.01	0.00	0.02	0.00	3.03	0.00	0.06	0.00	2.97	0.00	0.06	0.00	0.120	0.000
TK-4: Produced Water Tank 4	0.01	0.00	0.00	0.00	0.01	0.00	0.00	0.00	0.01	0.00	0.00	0.00	0.001	0.000
TK-8: Produced Water Tank 8	0.01	0.00	0.00	0.00	0.01	0.00	0.00	0.00	0.01	0.00	0.00	0.00	0.001	0.000
PWLOAD					0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.000	0.000

## ECD Pilot Gas Combustion PTE New Source Review Permit Horned Frog Compressor Station Delaware G&P, LLC

			Fuel Gas Flow	Fuel Higher Heating	Annual Operating				Potentia	l to Emit
EPN	FIN	Description	Rate (scf/hr)	Value (Btu/scf)	Hours (hr/yr)	Pollutant	Emission Factors <sup>a</sup>	Units	Hourly <sup>a</sup> (Ib/hr)	Annual <sup>b</sup> (T/yr)
ECD	ECD	Enclosed Combustion Device	30	1,111	8,760	NO <sub>X</sub>	0.1380	lb/MMBtu	0.00460	0.020
						со	0.2755	lb/MMBtu	0.009	0.04
						PM	C			
						SO <sub>2</sub>	0.00286	lb S/Mscf	0.00017	0.0008
						VOC	5.5	lb/MMscf	0.0002	0.001
						Benzene	0.0021	lb/MMscf	0.0000001	0.0000003

<sup>a</sup> Combustor emission factors for CO and NO<sub>x</sub> are based upon the Draft TNRCC Guidance Document for Flares and Vapor Oxidizers (dated 03/21) for non-assisted high-Btu and low-Btu flares. An example calculation for hourly CO emissions for EPN ECD-1 follows:

CO (lb/hr) = (Fuel Flow Rate, scf/hr) \* (Fuel Heating Value, Btu/scf) \* (MM/106) \* (Emission Factor, lb/MMBtu)

CO (lb/hr) = (30 scf/hr) \* (1,111 Btu/scf)\*(MM/10^6) \* (0.2755 lb/MMBtu)

= 0.01 lb/hr CO

Sulfur content of 2 gr S/100 scf or 0.00286 lb S/Mscf is conservatively assumed for variance in field gas quality.

SO<sub>2</sub> (lb/hr) = (Fuel Flow Rate, scf/hr)/1000\*(Sulfur Content, lb S/Mscf gas)\*(64.06 lb SO<sub>2</sub>/32.06 lb S)

SO2 (lb/hr) = (30 scf/hr) / (Mscf/1000scf) \* (0.00286 lb S/Mscf gas) \* (64.06 lb SO2/32.06 lb S)

= 0.00017 lb/hr SO<sub>2</sub>

Emission factors for VOC and benzene are based upon AP-42 Tables 1.4-2 and 1.4-3 (dated 7/98). An example calculation for hourly VOC emissions for EPN FLARE-1 follows:

VOC (lb/hr) = (Fuel Flow Rate, scf/hr) \* (MM/106) \* (Emission Factor, lb/MMscf)

VOC (lb/hr) = (30 scf/hr) \* (MM/10^6) \* (5.5 lb/MMscf)

= 0.0002 lb/hr VOC

<sup>b</sup> An example calculation for annual CO emissions for EPN FLARE-1 follows:

CO (T/yr) = (Hourly Emissions, lb/hr) \* (Annual Operating Hours, hr/yr) \* (1 T/2,000 lb)

CO (T/yr) = (0.01 lb/hr) \* (8,760 hr/yr) \* (1 T/2,000 lb)

= 0.04 T/yr CO

<sup>c</sup> The process flares are smokeless per 40 CFR §60.18 requirements; therefore, PM emissions are negligible.

#### ECD Waste Gas Combustion PTE New Source Review Permit Horned Frog Compressor Station Delaware G&P, LLC

		WG Max hourly	WG Annual	WG Higher Heating	Flare Fe	ed Rate	Annual Operating				Poten	tial to Emit <sup>e</sup>
		Flow Rate <sup>a</sup>	Flow Rate	Value	Hourly	Annual	Hours		Emission		Hourly <sup>b</sup>	Annual <sup>c</sup>
EPN	Description	(Mscf/hr)	(MMscf/yr	(Btu/scf)	(MMBtu/hr)	(MMBtu/yr)	(hr/yr)	Pollutant	Factors <sup>b</sup>	Units	(lb/hr)	(T/yr)
ECD	5% VRU Downtime	2.237	1.15	1,364.00	3.05	1,571.85	8,760	NO <sub>X</sub>	0.1380	lb/MMBtu	0.42	0.11
								со	0.2755	lb/MMBtu	0.84	0.22
								PM	d			
								SO <sub>2</sub>	8.57E-05	lb S/hr	1.61E-04	7.06E-04
							GWP				tpy	tpy CO <sub>2</sub> e
							1	CO25	53.0600	kg/MMBtu	183869.93	183869.93
							298	N <sub>2</sub> O <sup>5</sup>	0.0001	kg/MMBtu	0.35	103.27
							25	CH45	0.0010	kg/MMBtu	3.47	86.63
								CO <sub>2</sub> e <sup>5</sup>			183873.75	184059.83

<sup>a</sup> The WG flow rate, heating value, and feed rates taken from the following sources: TK-1 to TK-8, GB-1 (Flashing, working, and breathing), DEHY1 & DEHY2 (Flash tank), Condensate Loading, Produced Water Loading, Hourly flow rate is the maximum flow rate in an hour during VRU downtime, annual flow rate is base on maximum flow for 5% of the year or 438 hours a year.

<sup>b</sup> Emission factors for CO and NO<sub>x</sub> are based upon the Draft TNRCC Guidance Document for Flares and Vapor Oxidizers (dated 03/21) for non-assisted high or low Btu flares, as appropriate. Thermal oxidizer emission factors for CO, NO<sub>x</sub> and PM are based on AP-42 Table 1.4-2 (dated 7/98) and converted assuming a natural gas heating value of 1,020 Btu/scf. An example calculation for hourly CO emissions for EPN ECD follows:

CO (lb/hr) = (Flare Feed Rate, MMBtu/hr) \* (Emission Factor, lb/MMBtu)

CO (lb/hr) =	(3.05 MMBtu/hr) * (0.2755 lb/MMBtu)	
=	0.84	lb/hr CO
SO <sub>2</sub> emission rates for		
$SO_2$ (lb/hr) =	(Emission Factor, lb/hr S) * (64.06 lb SO <sub>2</sub> /34.08 lb S)	
$SO_2$ (lb/hr) =	(0.0001 lb/hr S) * (64.06 lb SO2 /34.08 lb S)	
=	1.61E-04	lb/hr SO <sub>2</sub>
c An example calculation for an	nual CO emissions for EPN FLARE-1 follows:	
CO (T/yr) =	(Flare Feed Rate, MMBtu/yr) * (Emission Factor, Ib/M	MMBtu) / (2,000 lb/T
CO (T/yr) =	(1,571.85 MMBtu/yr) * (0.2755 lb/MMBtu) / (2,000 l	lb/T)
=	0.22	T/yr CO

<sup>d</sup> The process flares are smokeless per 40 CFR §60.18 requirements; therefore, PM emissions are negligible.

<sup>e</sup> Waste gas emissions of VOC and benzene are represented at the FIN that generates the emissions.

## Enclosed Combustion Device Emission Summary New Source Review Permit Horned Frog Compressor Station Delaware G&P, LLC

				Pilo Potentia	t Gas l to Emit <sup>ª</sup>	Wast Potentia	e Gas l to Emit <sup>b</sup>	To Potentia	tal I to Emit
				Hourly	Annual	Hourly	Annual	Hourly	Annual
EPN	FIN	Description	Pollutant	(lb/hr)	(T/yr)	(lb/hr)	(T/yr)	(lb/hr)	(T/yr)
ECD	ECD Pilot	Enclosed Combustor	СО	0.00	0.02	0.42	0.11	0.43	0.13
	VRU downtime		NO <sub>x</sub>	0.009	0.04	0.84	0.22	0.85	0.26
			PM						
			SO <sub>2</sub>	0.00017	0.0008	0.000	0.00	0.000	0.00
			VOC (Pilot)	0.0002	0.001			0.0002	0.001
			Benzene (Pilot)	0.000001	0.000003			0.0000001	0.000003

<sup>a</sup> The Pilot Gas Potential to Emit emissions are from the Flare Pilot Gas Combustion Potential to Emit worksheet.

<sup>b</sup> The Waste Gas Potential to Emit CO, NO<sub>X</sub>, and SO<sub>2</sub> emissions are from the Flare Waste Gas Combustion Potential to Emit worksheet. Emissions from Periodic Events are not included in the Waste Gas Potential to Emit, but are shown on the Summary of Site-Wide Allowable Emission Rates table. VOC and benzene emissions from the storage tanks, loading, amine units, dehydration unit and blowdown waste gas are reported at their respective emission paths.
#### Fugitive Calculations New Source Review Permit Horned Frog Compressor Station Delaware G&P, LLC

			Annual								Potentia	l To Emit				
		Emission	Operating	Maximum	Maximum	Maximum	Maximum	Maximum	V	oc	Tota	HAP	Ben	zene	Carbon Dioxide	Methane
	Number of	Factors <sup>a</sup>	Hours	VOC	Total HAP	Benzene	Carbon Dioxide	Methane	Hourly <sup>b</sup>	Annual <sup>c</sup>	Hourly <sup>b</sup>	Annual <sup>c</sup>	Hourly <sup>b</sup>	Annual <sup>c</sup>	Annual <sup>c</sup>	Annual <sup>c</sup>
Component	Components	(lb/hr-component)	(hr/yr)	(wt%)	(wt%)	(wt%)	(wt%)	(wt%)	(lb/hr)	(T/yr)	(lb/hr)	(T/yr)	(lb/hr)	(T/yr)	(T/yr)	(T/yr)
Valves																
Gas Stream (Inlet Gas)	394	0.009921	8,760	31.26%	0.86%	0.10%	1.70%	48.10%	1.2217	5.3512	0.03350	0.1467	0.0039	0.0171	0.2918	8.2357
Heavy Liquid	18	0.0000185	8,760	100.00%	0.00%	0.00%	0.00%	0.02%	0.0003	0.0015	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Light Liquid Streams	117	0.005512	8,760	100.00%	13.06%	0.10%	0.00%	0.02%	0.6449	2.8247	0.084248	0.36901	0.0006	0.0028	0.0000	0.0006
Water/Light Liquid Streams	132	0.000216	8,760	100.00%	0.00%	0.00%	0.00%	0.00%	0.0285	0.1249	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Pump Seals																
Light Liquid Streams	2	0.02866	8,760	100.00%	13.06%	0.10%	0.00%	0.02%	0.0573	0.2511	0.0075	0.0328	0.0001	0.0003	0.0000	0.0001
Water/Light Liquid Streams	3	0.000053	8,760	100.00%	0.0000%	0.00%	0.00%	0.00%	0.0002	0.0007	0.000000	0.00000	0.0000	0.0000	0.0000	0.0000
Flanges																
Gas Stream (Inlet Gas)	650	0.00086	8,760	31.26%	0.86%	0.10%	1.70%	48.10%	0.1747	0.7653	0.0048	0.0210	0.0006	0.0024	0.0417	1.1778
Heavy Liquid	8	0.0000086	8,760	100.00%	0.00%	0.00%	0.00%	0.02%	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Light Liquid Streams	324	0.000243	8,760	100.00%	13.06%	0.10%	0.00%	0.02%	0.0787	0.3448	0.0103	0.0450	0.0001	0.0003	0.0000	0.0001
Water/Light Liquid Streams	122	0.0000064	8,760	100.00%	0.00%	0.00%	0.00%	0.00%	0.0008	0.0034	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Open Ended Lines																
Gas Stream (Inlet)	21	0.00441	8,760	31.26%	0.86%	0.10%	1.70%	48.10%	0.0289	0.1268	0.0008	0.0035	0.0001	0.0004	0.0069	0.1951
Heavy Liquid	10	0.000309	8,760	100.00%	0.00%	0.00%	0.00%	0.02%	0.0031	0.0135	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Light Liquid	15	0.003087	8,760	100.00%	13.06%	0.10%	0.00%	0.02%	0.0463	0.2028	0.0060	0.0265	0.0000	0.0002	0.0000	0.0000
Water/Light Liquid Streams	2	0.0000551	8,760	100.00%	0.00%	0.00%	0.00%	0.00%	0.0001	0.0005	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Connectors																
Gas Stream (Inlet Gas)	975	0.000441	8,760	31.26%	0.86%	0.10%	1.70%	48.10%	0.1344	0.5886	0.0037	0.0161	0.0004	0.0019	0.0321	0.9059
Heavy Liquid	12	0.0000165	8,760	100.00%	0.00%	0.00%	0.00%	0.02%	0.0002	0.0009	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Light Liquid Streams	486	0.000463	8,760	100.00%	13.06%	0.10%	0.00%	0.02%	0.2250	0.9856	0.029396	0.12875	0.0002	0.0010	0.0000	0.0002
Water/Light Liquid Streams	183	0.000243	8,760	100.00%	0.00%	0.00%	0.00%	0.00%	0.0445	0.1948	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Other																
Gas Stream (Inlet Gas)	104	0.019401	8,760	31.26%	0.86%	0.10%	1.70%	48.10%	0.6306	2.7622	0.0173	0.0757	0.0020	0.0088	0.1506	4.2512
Heavy Liquid	4	0.0000706	8,760	100.00%	0.00%	0.00%	0.00%	0.02%	0.0003	0.0012	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Light Liquid Streams	7	0.016535	8,760	100.00%	13.06%	0.10%	0.00%	0.02%	0.1157	0.5070	0.015121	0.06623	0.0001	0.0005	0.0000	0.0001
Water/Light Liquid Streams	2	0.030865	8,760	100.00%	0.00%	0.00%	0.00%	0.00%	0.0617	0.2704	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
							Gas Stream (I	nlet Gas) Total:	2.1904	9.5940	0.0601	0.2630	0.0070	0.0307	0.5231	14,7657
							Heavy Liquid	d Stream Total:	0.0039	0.0171	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
							Light Liquid	d Stream Total:	1.1680	5.1159	0.1526	0.6683	0.0012	0.0051	0.0000	0.0010
							Water/Light Liquid	Streams Total:	0.1358	0.5946	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
								TOTALS:	3.50	15.32	0.21	0.93	0.01	0.04	0.52	14.77

<sup>a</sup> Fugitive Emission Factors are per EPA Protocal for Equipment Leak Emission Estimates Table 2-4. The emission factors are for total hydrocarbon.

<sup>b</sup> Hourly VOC emission rates are calculated as follows:

(394 components) \* (0.00992 lb/hr-component) \* (31.26% VOC) \* (100% - 0% reduction credit) = 1.2217 lb/hr

<sup>c</sup> Annual VOC emission rates are calculated as follows:

(394 components) \* (0.00992 lb/hr-component) \* (8,760 hr/yr) \* (31.26% VOC) \* (100% - 0% reduction credit) / (2,000 lb/T) = 5.3512 T/yr

								Но	New Source Re rned Frog Com	view Perr	nit ation										
									Delaware (	G&P, LLC											
			Mean	Rain	Haul Road	Number of H	laul Road	Vehicle Mil	es Traveled	Hou	rly Size-Sp	ecific	Annı	ial Size-Sp	ecific				Emissio	on Rates	
FIN	EPN	% Silt	Vehicle	Days	Distance	Per Hour	Year	(VMT/hour)	(VMT/year)	TSP	PM-10	PM-2.5	TSP	PM-10	PM-2.5	TS	6P	PN	1-10	PM	-2.5
																(lb/hr)	(Tons)	(lb/hr)	(Tons)	(lb/hr)	(Tons)
	HR-1	48	40.0	70	0.30	1	1.204	0.30	361.20	8.28	2.11	0.21	6.69	1.70	0.17	2.48	1.21	0.63	0.31	0.06	0.03

Notes:

1. Calculation method and factors are from AP-42, Section 13.2 (11/2006).

2. The entries for % Silt and Rain Days are the NMED accepted default values.

3. The Haul Road Distance only includes the round-trip distance within the facility boundaries per NMED protocol.

Sample Calculations: (based on PM-10)

#### Emission Factors:

Hourly Size-Specific Emission Factor = k \* [(surface material silt content, %)/12]^a \* [(mean vehicle weight, tons)/3]^b

where k, a, and b are empirical constants from AP-42 Table 13.2.2-2 for industrial roads.

= <u>1.5 lb/VMT \* [(4.8 %) /</u> 12]^0.9 \* [(40.0 tons) / 3]^0.45

= 2.11 Ib/VMT where VMT = vehicle miles traveled

Annual Size-Specific Emission Factor = Hourly Size-Specific Emission Factor \* [ (365 - Rain Days) / 365 ]

where Rain Days = # of days in a year with at least 0.01 inches of precipitation.

= <u>2.11 lbs/VMT \* [ (365 - 70 days / 365 days ]</u>

= 1.70 lb/VMT where VMT = vehicle miles traveled

#### Emissions:

Hourly Emissions = Hourly Size-Specific Emission Factor \* Vehicle Miles Traveled per Hour

= 2.11 lbs/VMT \* 0.30 VMT/hour

Annual Emissions = Annual Size-Specific Emission Factor \* Vehicle Miles Traveled per Year

= <u>1.70 lbs/VMT \* 361.2</u>0 VMT/year

= 0.31 Tons

			Compresso New Sou Horned Frog Delar	r Engine Blowdo rce Review Perm g Compressor Sta ware G&P, LLC	wns lit ation					
Description	Total PTE	E-1	E-2	E-4	E-5	E-6	E-7	E-8	E-9	E-10
Number of Blowdowns per Year		26	26	52	52	52	52	52	52	52
Number of Blowdowns per Hour		1	1	1	1	1	1	1	1	1
Blowdown Volume per Event, scf		2,000	2,000	2,000	2,000	2,000	2,000	2,000	2,000	2,000
Gas Stream Specific Gravity		0.8162	0.8162	0.8162	0.8162	0.8162	0.8162	0.8162	0.8162	0.8162
Air MW, Ib/mole		23.53	23.53	23.53	23.53	23.53	23.53	23.53	23.53	23.53
Gas Stream Density, Ib/scf <sup>a</sup>		0.051	0.051	0.051	0.051	0.051	0.051	0.051	0.051	0.051
Max VOC Bercentare in Gas Stream, wt%		21.26%	21.26%	21.26%	21.26%	21.26%	21.26%	21.26%	21.26%	21.26%
Max VOC Percentage in Gas Stream, wt% Max HAP Percentage in Gas Stream, wt% Max Methane Percentage in Gas Stream, wt%		0.86% 48.10%	0.86% 48.10%	0.86% 48.10%	0.86% 48.10%	0.86% 48.10%	0.86% 48.10%	0.86% 48.10%	0.86% 48.10%	0.86% 48.10%
Max CO <sub>2</sub> Percentage in Gas Stream, wt%		1.70%	1.70%	1.70%	1.70%	1.70%	1.70%	1.70%	1.70%	1.70%
Max Benzene Percentage in Gas Stream, wt%		0.10%	0.10%	0.10%	0.10%	0.10%	0.10%	0.10%	0.10%	0.10%
Hourly VOC Emission Rates (Ib/hr): <sup>b</sup>	63.34	31.67	31.67	31.67	31.67	31.67	31.67	31.67	31.67	31.67
Annual VOC Emission Rates (T/yr): <sup>c</sup>	6.59	0.412	0.412	0.82	0.82	0.82	0.82	0.82	0.82	0.82
Hourly HAP Emission Rates (lb/hr): <sup>b</sup>	1.74	0.8683	0.8683	0.87	0.87	0.87	0.87	0.87	0.87	0.87
Annual HAP Emission Rates (T/yr): <sup>c</sup>	0.18	0.011289	0.011289	0.02	0.02	0.0226	0.02	0.02	0.0226	0.02
Annual Methane Emission Rates (T/yr): <sup>c</sup>	10.14	0.63	0.63	1.27	1.27	1.27	1.27	1.27	1.27	1.27
Annual CO <sub>2</sub> Emission Rates (T/yr): <sup>c</sup>	0.36	0.0224	0.0224	0.04	0.04	0.04	0.04	0.04	0.04	0.04
Hourly Benzene Emission Rates (lb/hr): <sup>b</sup>	0.20	0.101	0.101	0.10	0.10	0.10	0.10	0.10	0.10	0.10
Annual Benzene Emission Rates (T/yr): <sup>c</sup>	0.02	0.00132	0.00132	0.0026	0.0026	0.003	0.0026	0.0026	0.003	0.0026

lb/hr rates assume a max of 2 engines can blowdown simultaneously.

<sup>a</sup> Gas stream density is calculated as follows:

(23.53 lb/mole) / (379 scf/mole) \* (0.8162) = 0.051 lb/scf

<sup>b</sup> Hourly blowdown VOC emission rates are calculated as follows:

(1 blowdown/hr) \* (2,000 scf/blowdown) \* (0.051 lb/scf) \* (31.26% VOC) \* (1 - 0.00) = 31.67 lb/hr

<sup>c</sup> Annual blowdown VOC emission rates are calculated as follows:

(26 blowdowns/yr) \* (2,000 scf/blowdown) \* (0.051 lb/scf) \* (31.26% VOC) / (2,000 lb/T) \* (1 - 0.00) = 0.41 T/yr

			Compresso New Sou Horned Fro Dela	r Engine Starter V Irce Review Perm g Compressor Sta ware G&P, LLC	/ents lit ation					
Description	Total PTE	C-1	C-3	C-5	C-6	C-7	C-8	C-9	C-10	C-11
Number of Starts per Year		156	156	156	156	156	156	156	156	156
Number of Starts per Hour		1	1	1	1	1	1	1	1	1
Starter Vent Volume per Event, scf		900	900	900	900	900	900	900	900	900
Gas Stream Specific Gravity		0.8162	0.8162	0.8162	0.8162	0.8162	0.8162	0.8162	0.8162	0.8162
Air MW, Ib/mole		23.53	23.53	23.53	23.53	23.53	23.53	23.53	23.53	23.53
Gas Stream Density, Ib/scf <sup>a</sup>		0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05
Max VOC Percentage in Gas Stream, wt%		31.26%	31.26%	31.26%	31.26%	31.26%	31.26%	31.26%	31.26%	31.26%
Max HAP Percentage in Gas Stream, wt%		0.86%	0.86%	0.86%	0.86%	0.86%	0.86%	0.86%	0.86%	0.86%
Max Methane Percentage in Gas Stream, wt%		48.10%	48.10%	48.10%	48.10%	48.10%	48.10%	48.10%	48.10%	48.10%
Max CO <sub>2</sub> Percentage in Gas Stream, wt%		1.70%	1.70%	1.70%	1.70%	1.70%	1.70%	1.70%	1.70%	1.70%
Max Benzene Percentage in Gas Stream, wt%		0.10%	0.10%	0.10%	0.10%	0.10%	0.10%	0.10%	0.10%	0.10%
Hourly VOC Emission Rates (Ib/hr): <sup>b</sup>	28.50	14.25	14.25	14.25	14.25	14.25	14.25	14.25	14.25	14.25
Annual VOC Emission Rates (T/yr): <sup>c</sup>	10.00	1.11	1.11	1.11	1.11	1.11	1.11	1.11	1.11	1.11
Hourly HAP Emission Rates (Ib/hr): <sup>b</sup>	0.78	0.39	0.39	0.39	0.39	0.39	0.39	0.39	0.39	0.39
Annual HAP Emission Rates (T/yr): <sup>c</sup>	0.27	0.03	0.03	0.03	0.03	0.03	0.03	0.03	0.03	0.03
Annual Methane Emission Rates (T/yr): <sup>c</sup>	15.40	1.71	1.71	1.71	1.71	1.71	1.71	1.71	1.71	1.71
Annual CO <sub>2</sub> Emission Rates (T/yr): <sup>c</sup>	0.55	0.061	0.061	0.06	0.06	0.06	0.06	0.06	0.06	0.06
Hourly Benzene Emission Rates (Ib/hr): <sup>b</sup>	0.09	0.046	0.046	0.046	0.046	0.046	0.046	0.046	0.046	0.046
Annual Benzene Emission Rates (T/yr): <sup>c</sup>	0.03	0.0036	0.0036	0.0036	0.0036	0.0036	0.0036	0.0036	0.0036	0.0036

lb/hr rates assume a max of 2 engines will start up simultaneously.

<sup>a</sup> Gas stream density is calculated as follows:

(23.53 lb/mole) / (379 scf/mole) \* (0.8162) = 0.05 lb/scf

<sup>b</sup> Hourly starter vent VOC emission rates are calculated as follows:

(1 starts/hr) \* (900 scf/start) \* (0.051 lb/scf) \* (31.26% VOC) = 14.25 lb/hr

<sup>c</sup> Annual starter vent VOC emission rates are calculated as follows:

(156 starts/yr) \* (900 scf/start) \* (0.051 lb/scf) \* (31.26% VOC) / (2,000 lb/T) = 1.11 T/yr

#### Miscellaneous SSM New Source Review Permit Horned Frog Compressor Station Delaware G&P, LLC

Description	Total PTE	DEHYS	Filter Coalescer	Scrubbers	Pumps	Reboiler Maintenance	Pipeline Maintenance	Tank Degassing
Number of Blowdowns per Vear		2	1	c.	Q	2	1	Q
Simultaneous blowdowns per hour		1	1	5	2	1	1	1
Volume of Gas Per Blowdown		18.318.79	900	3,380	16	65	54.874	4.323
Gas Stream Specific Gravity		0.8162	0.8162	0.8162	0.8162	0.8162	0.8162	0.8162
Air MW, lb/mole		23.53	23.53	23.53	23.53	23.53	23.53	70.00
Gas Stream Density. Ib/scf <sup>a</sup>		0.05	0.05	0.05	0.05	0.05	0.05	0.15
Flare Control Efficiency, %		0%	0%	0%	0%	0%	0%	0%
Max VOC Percentage in Gas Stream, wt%		31.26%	31.26%	31.26%	31.26%	31.26%	31.26%	31.26%
Max HAP Percentage in Gas Stream, wt%		0.86%	0.86%	0.86%	0.86%	0.86%	0.86%	0.86%
Max Methane Percentage in Gas Stream, wt%		48.10%	48.10%	48.10%	48.10%	48.10%	48.10%	48.10%
Max CO <sub>2</sub> Percentage in Gas Stream, wt%		1.70%	1.70%	1.70%	1.70%	1.70%	1.70%	1.70%
Max Benzene Percentage in Gas Stream, wt%		0.10%	0.10%	0.10%	0.10%	0.10%	0.10%	0.10%
Hourly VOC Emission Rates (lb/hr): <sup>b</sup>	1646.14	290.09	14.25	267.62	0.51	1.03	868.96	203.68
Annual VOC Emission Rates (T/yr): <sup>c</sup>	1.68	0.29	0.01	0.13	0.00	0.00	0.43	0.81
Hourly HAP Emission Rates (lb/hr): <sup>b</sup>	45.13	7.95	0.39	7.34	0.01	0.03	23.82	5.58
Annual HAP Emission Rates $(T/vr)$ :	0.05	0.01	0.00	0.00	0.00	0.00	0.01	0.02
Annual Methane Emission Rates (T/yr): <sup>c</sup>	2.59	0.45	0.01	0.21	0.00	0.00	0.67	1.25
Annual CO <sub>2</sub> Emission Rates (T/yr): <sup>c</sup>	0.09	0.016	0.00	0.01	0.00	0.00	0.02	0.04
2								
Hourly Benzene Emission Rates (lb/hr): <sup>0</sup>	5.27	0.928	0.046	0.856	0.002	0.003	2.780	0.652
Annual Benzene Emission Rates (T/yr): <sup>c</sup>	0.005	0.0009	0.0000	0.0004	0.0000	0.0000	0.0014	0.0026
	1							

<sup>a</sup> Gas stream density is calculated as follows:

(23.53 lb/mole) / (379 scf/mole) \* (0.8162) = 0.05 lb/scf

<sup>b</sup> Hourly starter vent VOC emission rates are calculated as follows:

(1 starts/hr) \* (18319 scf/start) \* (0.051 lb/scf) \* (31.26% VOC) = 290.09 lb/hr

<sup>c</sup> Annual starter vent VOC emission rates are calculated as follows:

(2 starts/yr) \* (18319 scf/start) \* (0.051 lb/scf) \* (31.26% VOC) / (2,000 lb/T) = 0.29 T/yr

### SSM Summary New Source Review Permit Horned Frog Compressor Station Delaware G&P, LLC

Description	vo	с	Benz	ene	Tota	al HAPs	Methane	Carbon Dioxide
	(lb/hr)	(tpy)	(lb/hr)	(tpy)	(lb/hr)	(tpy)	(tpy)	(tpy)
Compressor Blowdowns	63.34	6.59	0.20	0.02	1.74	0.18	10.14	0.36
Compressor Starter Vents	28.50	10.00	0.09	0.03	0.78	0.27	15.40	0.55
Misc SSM	1646.14	1.68	5.27	5.38E-03	45.13	0.046	2.59	0.0917
TOTAL SSM	1737.98	18.27	5.56	0.06	47.65	0.50	28.13	1.00

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# Section 6.a

# **Green House Gas Emissions**

(Submitting under 20.2.70, 20.2.72 20.2.74 NMAC)

**Title V (20.2.70 NMAC), Minor NSR (20.2.72 NMAC), and PSD (20.2.74 NMAC)** applicants must estimate and report greenhouse gas (GHG) emissions to verify the emission rates reported in the public notice, determine applicability to 40 CFR 60 Subparts, and to evaluate Prevention of Significant Deterioration (PSD) applicability. GHG emissions that are subject to air permit regulations consist of the sum of an aggregate group of these six greenhouse gases: carbon dioxide (CO<sub>2</sub>), nitrous oxide (N<sub>2</sub>O), methane (CH<sub>4</sub>), hydrofluorocarbons (HFCs), perfluorocarbons (PFCs), and sulfur hexafluoride (SF<sub>6</sub>).

# **Calculating GHG Emissions:**

**1.** Calculate the ton per year (tpy) GHG mass emissions and GHG CO<sub>2</sub>e emissions from your facility.

**2.** GHG mass emissions are the sum of the total annual tons of greenhouse gases without adjusting with the global warming potentials (GWPs). GHG CO<sub>2</sub>e emissions are the sum of the mass emissions of each individual GHG multiplied by its GWP found in Table A-1 in 40 CFR 98 <u>Mandatory Greenhouse Gas Reporting</u>.

3. Emissions from routine or predictable start up, shut down, and maintenance must be included.

**4.** Report GHG mass and GHG CO<sub>2</sub>e emissions in Table 2-P of this application. Emissions are reported in <u>short</u> tons per year and represent each emission unit's Potential to Emit (PTE).

**5.** All Title V major sources, PSD major sources, and all power plants, whether major or not, must calculate and report GHG mass and CO2e emissions for each unit in Table 2-P.

**6.** For minor source facilities that are not power plants, are not Title V, and are not PSD there are three options for reporting GHGs in Table 2-P: 1) report GHGs for each individual piece of equipment; 2) report all GHGs from a group of unit types, for example report all combustion source GHGs as a single unit and all venting GHGs as a second separate unit; 3) or check the following I by checking this box, the applicant acknowledges the total CO2e emissions are less than 75,000 tons per year.

# Sources for Calculating GHG Emissions:

- Manufacturer's Data
- AP-42 Compilation of Air Pollutant Emission Factors at http://www.epa.gov/ttn/chief/ap42/index.html
- EPA's Internet emission factor database WebFIRE at http://cfpub.epa.gov/webfire/
- 40 CFR 98 <u>Mandatory Green House Gas Reporting</u> except that tons should be reported in short tons rather than in metric tons for the purpose of PSD applicability.

• API Compendium of Greenhouse Gas Emissions Methodologies for the Oil and Natural Gas Industry. August 2009 or most recent version.

• Sources listed on EPA's NSR Resources for Estimating GHG Emissions at http://www.epa.gov/nsr/clean-air-act-permitting-greenhouse-gases:

## **Global Warming Potentials (GWP):**

Applicants must use the Global Warming Potentials codified in Table A-1 of the most recent version of 40 CFR 98 Mandatory Greenhouse Gas Reporting. The GWP for a particular GHG is the ratio of heat trapped by one unit mass of the GHG to that of one unit mass of CO<sub>2</sub> over a specified time period.

"Greenhouse gas" for the purpose of air permit regulations is defined as the aggregate group of the following six gases: carbon dioxide, nitrous oxide, methane, hydrofluorocarbons, perfluorocarbons, and sulfur hexafluoride. (20.2.70.7 NMAC, 20.2.74.7 NMAC). You may also find GHGs defined in 40 CFR 86.1818-12(a).

## Metric to Short Ton Conversion:

Short tons for GHGs and other regulated pollutants are the standard unit of measure for PSD and title V permitting programs. 40 CFR 98 <u>Mandatory Greenhouse Reporting</u> requires metric tons.

1 metric ton = 1.10231 short tons (per Table A-2 to Subpart A of Part 98 – Units of Measure Conversions)

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# Section 7

# **Information Used to Determine Emissions**

### Information Used to Determine Emissions shall include the following:

- ☑ If manufacturer data are used, include specifications for emissions units <u>and</u> control equipment, including control efficiencies specifications and sufficient engineering data for verification of control equipment operation, including design drawings, test reports, and design parameters that affect normal operation.
- □ If test data are used, include a copy of the complete test report. If the test data are for an emissions unit other than the one being permitted, the emission units must be identical. Test data may not be used if any difference in operating conditions of the unit being permitted and the unit represented in the test report significantly effect emission rates.
- If the most current copy of AP-42 is used, reference the section and date located at the bottom of the page. Include a copy of the page containing the emissions factors, and clearly mark the factors used in the calculations.
- □ If an older version of AP-42 is used, include a complete copy of the section.
- If an EPA document or other material is referenced, include a complete copy.
- I Fuel specifications sheet.
- ☑ If computer models are used to estimate emissions, include an input summary (if available) and a detailed report, and a disk containing the input file(s) used to run the model. For tank-flashing emissions, include a discussion of the method used to estimate tank-flashing emissions, relative thresholds (i.e., permit or major source (NSPS, PSD or Title V)), accuracy of the model, the input and output from simulation models and software, all calculations, documentation of any assumptions used, descriptions of sampling methods and conditions, copies of any lab sample analysis.

Supporting documentation is attached to this section.

ProMax Dehydration Emissic	ons Report		
Case Name:	25 MMSCFD		
File Name:	C:\Users\Admin\Resolute Compliance, I	LC\Environmental Compliance - General\Env\Projects\Env-EnLink-0	254\5.0 Air Permit-
Data	Horned Frog CS NSR\5.2 Modeling\5.2.2	BRE ProMax-Other Simulation\ProMax_Dehydration_Tool.pmx	
Date:			
Description:			
	Dry Gas Flow F	ate 24.71 MMSCED	
	Dry Gas Water Cont	ent 3.20 lb/MMSCF	
	Glycol Circulation F	ate 7.00 sgpm	
	Glycol Circulation R	atio 5.87 gal/lb	
	Annual Operating Ho	urs 8760 hrs	
INPUT SUMMARY:			
reed stream specifications	Fraction of Water Saturaton (%)	100.00	
	Water Content (Ibm/MMSCF)	69.22	
	Temperature (°F)	110.00	
	Pressure (psig)	1100.00	
	Flow Rate (MMSCFD)	25.01	
Lean Glycol Specifications			
	Glycol Circulation Rate (sgpm)	7.00	
Regenerator Specifications			
	Reboiler Temperature (°F)	400.000	
	Overnead vapors	To Control Device	
	is Kenda Coll Present:	163	
Thesh Tauly Constituent			
Flash Tank Specifications	Is Flash Tank Present?	Flash Tank Present	
	Temperature (°F)	160.00	
	Pressure (psig)	45.00	
	Flash Gas	Vent To Atmosphere	
Stripping Gas Specifications			
	Nitrogen (scfm)	Not In Use	
	Dry gas (scfm)	Not In Use	
Kimray Pump Specifications			
	Туре	Gas Injection	
	as Injection Volume Ratio (acfm/gpm)	0.001	
Methanol Specifications			
With the of the official offici		Not Procent in Food	
Methanol Specifications	Is Methanol Present?		

BTEX Condenser Specifications			
Temperature (°F)	120.00		
Pressure (nsig)	-0.30		
BTEX Emissions	To Flare		
	To have		
General Specifications			
Atmospheric Pressure (psia)	14.400		1
Flash Gas Flare Destruction Efficiency (%)	95.000		
Regenerator Flare Destruction Efficiency (%)	98.000		
Feed Composition Data (mol %)			
Carbon Diaxido	0.0115		
Carbon Dioxide	0.9115		
Hydrogen Suffide	0.0000		
Nitrogen	1.6267		
Methane	70.5837		
Ethane	13.3096		
Propane	7.6136		
i-Butane	1.0396		
n-Butane	2.6978		
i-Pentane	0.6018		
n-Pentane	0.0010		
Guelenertere	0.0000		
Cycloperitane	0.0000		
n-Hexane	0.6632		
Cyclohexane	0.0000		
n-Heptane	0.2041		
Methylcyclohexane	0.0000		
2,2,4-Trimethylpentane	0.0000		
Benzene	0.0236		
Toluene	0.0123		
Ethylhonzono	0.0004		
Etityibelizette	0.0004		
o-xyiene	0.0006		
m-Xylene	0.0024		
p-Xylene	0.0002		
Triethylene Glycol	0.0000		
Ethylene Glycol	0.0000		
Water	0.0000		
Methanol	0.000		
02	0.0000		
62	0.0000		
502	0.0000		
SO2	0.0000		
SO2 Total	0.0000 100.00		
SO2 Total	0.0000 100.00		
SO2 Total	0.0000 100.00		
SO2 Total EMISSIONS REPORTS:	0.0000 100.00		
SO2 Total EMISSIONS REPORTS:	0.0000 100.00		
SO2 Total EMISSIONS REPORTS:	0.0000 100.00		
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS	0.0000 100.00		
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component	0.0000 100.00	lbs/dav	tons/yr
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide	0.0000 100.00 lbs/hr 62.33	lbs/day 1496.03	tons/yr 273.03
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide	0.0000 100.00 lbs/hr 62.33	lbs/day 1496.03	tons/yr 273.03
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide	0.0000 100.00 lbs/hr 62.33 0.00	lbs/day 1496.03 0.00	tons/yr 273.03 0.00
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen	0.0000 100.00 lbs/hr 62.33 0.00 622.50	lbs/day 1496.03 0.00 14939.97	tons/yr 273.03 0.00 2726.54
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane	0.0000 100.00 Ibs/hr 62.33 0.00 622.50 0.01	lbs/day 1496.03 0.00 14939.97 0.24	tons/yr 273.03 0.00 2726.54 0.04
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane	0.0000 100.00 Ibs/hr 62.33 0.00 622.50 0.01 0.03	lbs/day 1496.03 0.00 14939.97 0.24 0.61	tons/yr 273.03 0.00 2726.54 0.04 0.11
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane E thane Propane	0.0000 100.00 lbs/hr 62.33 0.00 622.50 0.01 0.03 0.03 0.05	lbs/day 1496.03 0.00 14939.97 0.24 0.61 1.26	tons/yr 273.03 0.00 2726.54 0.04 0.11 0.23
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane	0.0000 100.00 lbs/hr 62.33 0.00 622.50 0.01 0.03 0.05 0.01	lbs/day 1496.03 0.00 14939.97 0.24 0.61 1.26 0.30	tons/yr 273.03 0.00 2726.54 0.04 0.11 0.23 0.05
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane	0.0000 100.00 bs/hr 62.33 0.00 622.50 0.01 0.03 0.05 0.01 0.05 0.01 0.06	lbs/day 1496.03 0.00 14939.97 0.24 0.61 1.26 0.30 1.43	tons/yr 273.03 0.00 2726.54 0.04 0.11 0.23 0.05 0.26
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane	0.0000 100.00 bs/hr 62.33 0.00 622.50 0.01 0.03 0.05 0.01 0.06 0.02	lbs/day 1496.03 0.00 14939.97 0.24 0.61 1.26 0.30 1.43 0.56	tons/yr 273.03 0.00 2726.54 0.04 0.11 0.23 0.05 0.26 0.10
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Pentane n-Pentane	0.0000 100.00 lbs/hr 62.33 0.00 622.50 0.01 0.03 0.05 0.01 0.05 0.01 0.06 0.02 0.04	lbs/day 1496.03 0.00 14939.97 0.24 0.61 1.26 0.30 1.43 0.56 0.87	tons/yr 273.03 0.00 2726.54 0.04 0.11 0.23 0.05 0.26 0.10 0.16
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane Ovclopentane	0.0000 100.00 bs/hr 62.33 0.00 622.50 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.06 0.02 0.02 0.00	lbs/day 1496.03 0.00 14939.97 0.24 0.61 1.26 0.30 1.43 0.56 0.87 0.00	tons/yr 273.03 0.00 2726.54 0.04 0.11 0.23 0.05 0.26 0.10 0.16 0.00
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Pentane n-Pentane Notes Notes No	0.0000 100.00 bs/hr 62.33 0.00 622.50 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.06	lbs/day 1496.03 0.00 14939.97 0.24 0.61 1.26 0.30 1.43 0.56 0.87 0.00 1.50	tons/yr 273.03 0.00 2726.54 0.11 0.23 0.25 0.26 0.10 0.16 0.00
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane E thane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane	0.0000 100.00 bs/hr 62.33 0.00 622.50 0.01 0.03 0.05 0.01 0.06 0.02 0.02 0.04 0.00 0.06 0.02	lbs/day 1496.03 0.00 14939.97 0.24 0.61 1.26 0.30 1.43 0.56 0.87 0.00 1.50 0.00	tons/yr 273.03 0.00 2726.54 0.04 0.11 0.23 0.05 0.26 0.210 0.16 0.00 0.77 0.00
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane	0.0000 100.00 bs/hr 62.33 0.00 622.50 0.01 0.03 0.05 0.01 0.05 0.01 0.06 0.02 0.04 0.00 0.04 0.00 0.06 0.00	lbs/day 1496.03 0.00 14939.97 0.24 0.61 1.26 0.30 1.43 0.56 0.87 0.00 1.50 0.00 0.57	tons/yr 273.03 0.00 2726.54 0.04 0.11 0.23 0.05 0.26 0.10 0.10 0.00 0.27 0.00
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Butane i-Pentane n-Pentane n-Pentane n-Pentane n-Pentane n-Pentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclohexane n-Heptane	0.0000 100.00 bs/hr 62.33 0.00 622.50 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.02 0.04 0.02 0.04 0.00 0.00 0.00 0.00	lbs/day 1496.03 0.00 14939.97 0.24 0.61 1.26 0.30 1.43 0.56 0.87 0.00 1.50 0.00 0.57 0.00	tons/yr 273.03 0.00 2726.54 0.04 0.11 0.23 0.05 0.26 0.10 0.16 0.00 0.27 0.00 0.10
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Butane i-Pentane n-Butane i-Pentane n-Pentane Cyclopentane n-Heptane Cyclohexane NHEPtane	0.0000 100.00 bs/hr 62.33 0.00 622.50 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.02 0.04 0.00 0.02 0.00 0.00 0.02 0.00	lbs/day 1496.03 0.00 14939.97 0.24 0.61 1.26 0.30 1.43 0.56 0.87 0.00 1.50 0.00 0.57 0.00	tons/yr 273.03 0.00 2726.54 0.04 0.11 0.23 0.05 0.26 0.10 0.16 0.00 0.27 0.00 0.10 0.10
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclobexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane	0.0000 100.00 bs/hr 62.33 0.00 622.50 0.01 0.03 0.05 0.01 0.05 0.01 0.06 0.02 0.04 0.00 0.06 0.00 0.00 0.00 0.00 0.00	lbs/day 1496.03 0.00 14939.97 0.24 0.61 1.26 0.30 1.43 0.56 0.87 0.00 1.50 0.00 0.57 0.00 0.57 0.00	tons/yr 273.03 0.00 2726.54 0.04 0.11 0.23 0.05 0.26 0.10 0.16 0.00 0.27 0.00 0.27 0.00 0.10 0.00
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Suffide Nitrogen Methane Ethane Propane i-Butane i-Butane i-Pentane n-Pentane n-Pentane n-Pentane n-Pentane n-Hexane Cyclopentane n-Hexane Cyclobexane n-Hexane 2,2,4-Trimethylpentane Benzene	0.0000 100.00 100.00 62.33 0.00 622.50 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.06 0.02 0.04 0.00 0.00 0.00 0.00 0.00 0.00	Ibs/day 1496.03 0.00 14939.97 0.24 0.61 1.26 0.30 1.43 0.56 0.87 0.00 1.50 0.00 0.57 0.00 0.00 0.57 0.00 0.00 0.57 0.00 0.00 0.00 0.57 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.57 0.00 0.00 0.00 0.57 0.00 0.00 0.00 0.57 0.00 0.00 0.00 0.57 0.00 0.00 0.00 0.57 0.00 0.00 0.57 0.00 0.00 0.57 0.00 0.00 0.00 0.57 0.00 0.00 0.57 0.00 0.00 0.57 0.00 0.00 0.57 0.00 0.00 0.57 0.00 0.00 0.57 0.00 0.00 0.00 0.57 0.00 0.00 0.00 0.00 0.57 0.00 0.00 0.00 0.00 0.57 0.00 0.	tons/yr 273.03 0.00 2726.54 0.04 0.11 0.23 0.25 0.26 0.10 0.16 0.00 0.27 0.00 0.27 0.00 0.10 0.00 0.28
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Pentane n-Butane i-Pentane n-Pentane Cyclopentane n-Heptane N-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene	0.0000 100.00 bs/hr 62.33 0.00 622.50 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.06 0.02 0.04 0.02 0.04 0.00 0.02 0.00 0.00	lbs/day 1496.03 0.00 14939.97 0.24 0.61 1.26 0.30 1.43 0.56 0.87 0.00 1.50 0.00 0.57 0.00 0.57 0.00 1.52 0.72	tons/yr 273.03 0.00 2726.54 0.04 0.11 0.23 0.05 0.10 0.16 0.00 0.27 0.00 0.10 0.10 0.10 0.00 0.10 0.00 0.13
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene	0.0000 100.00 100.00 62.33 0.00 622.50 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.02 0.04 0.02 0.04 0.00 0.02 0.04 0.00 0.00	lbs/day 1496.03 0.00 14939.97 0.24 0.61 1.26 0.30 1.43 0.56 0.87 0.00 1.50 0.00 1.50 0.00 0.57 0.00 1.52 0.72 0.72 0.01	tons/yr 273.03 0.00 2726.54 0.04 0.11 0.23 0.05 0.26 0.10 0.16 0.00 0.27 0.00 0.10 0.10 0.00 0.27 0.00 0.00
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclobexane n-Hexane Nota	0.0000 100.00 100.00 105/hr 62.33 0.00 622.50 0.01 0.03 0.05 0.01 0.06 0.02 0.04 0.00 0.06 0.00 0.01 0.00 0.02 0.01 0.00 0.02 0.01 0.00 0.02 0.01 0.00 0.02 0.01 0.00 0.02 0.01 0.00 0.02 0.00 0.02 0.00 0.02 0.00 0.02 0.00 0.02 0.00 0.00 0.02 0.00 0.00 0.02 0.00 0.00 0.00 0.00 0.02 0.000 0.00	Ibs/day 1496.03 0.00 14939.97 0.24 0.61 1.26 0.30 1.43 0.56 0.87 0.00 1.50 0.00 0.57 0.00 0.00 0.57 0.00 0.00 0.57 0.00 0.00 0.57 0.00 0.00 0.57 0.00 0.00 0.57 0.00 0.01 0.01 0.00 0.01 0.01 0.02 0.02 0.02 0.02 0.02 0.05 0.55 0.55 0.55 0.55 0.55 0.55 0.55 0.55 0.	tons/yr 273.03 0.00 2726.54 0.04 0.11 0.23 0.05 0.26 0.10 0.16 0.00 0.27 0.00 0.10 0.00 0.10 0.00 0.00 0.28 0.13 0.00
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Butane n-Pentane n-Pentane n-Pentane n-Pentane n-Pentane n-Hexane Cyclohexane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene	0.0000 100.00 bs/hr 62.33 0.00 622.50 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.06 0.02 0.04 0.00 0.02 0.04 0.00 0.00 0.00	lbs/day 1496.03 0.00 14939.97 0.24 0.61 1.26 0.30 1.43 0.56 0.87 0.00 1.50 0.00 0.57 0.00 0.57 0.00 1.52 0.72 0.72 0.01 0.02 0.07	tons/yr 273.03 0.00 2726.54 0.01 0.11 0.23 0.05 0.10 0.16 0.00 0.27 0.00 0.10 0.10 0.00 0.10 0.00 0.13 0.00 0.28 0.13 0.00 0.00
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Heptane Cyclopexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene	0.0000 100.00 100.00 62.33 0.00 622.50 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.02 0.04 0.02 0.04 0.00 0.02 0.00 0.00	lbs/day 1496.03 0.00 14939.97 0.24 0.61 1.26 0.30 1.43 0.56 0.87 0.00 1.50 0.00 1.50 0.00 0.57 0.00 0.57 0.00 1.52 0.72 0.72 0.01 0.02 0.07 0.01	tons/yr 273.03 0.00 2726.54 0.04 0.11 0.23 0.05 0.26 0.10 0.16 0.00 0.27 0.00 0.10 0.00 0.10 0.00 0.28 0.13 0.00 0.00 0.00 0.00 0.00
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclohexane n-Hexane Cyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene	0.0000 100.00 100.00 105/hr 62.33 0.00 622.50 0.01 0.03 0.05 0.01 0.06 0.02 0.04 0.00 0.06 0.000 0.00	Ibs/day 1496.03 0.00 14939.97 0.24 0.61 1.26 0.30 1.43 0.56 0.87 0.00 1.50 0.00 1.50 0.00 0.57 0.00 1.52 0.72 0.01 0.02 0.07 0.01 0.02 0.07 0.01 0.00	tons/yr 273.03 0.00 2726.54 0.04 0.11 0.23 0.05 0.26 0.10 0.16 0.00 0.27 0.00 0.10 0.00 0.10 0.00 0.00 0.28 0.13 0.00 0.00 0.00 0.00
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane n-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene p-Xylene Triethylene Glycol Ethylone Circuit	0.0000 100.00 100.00 62.33 0.00 622.50 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.02 0.04 0.00 0.02 0.04 0.00 0.02 0.00 0.02 0.00 0.0	Ibs/day 1496.03 0.00 14939.97 0.24 0.61 1.26 0.30 1.43 0.56 0.87 0.00 1.50 0.00 0.57 0.00 0.00 0.57 0.00 0.57 0.00 0.00 0.57 0.00 0.00 0.57 0.00 0.00 0.00 0.57 0.00 0.00 0.57 0.00 0.00 0.57 0.00 0.00 0.57 0.00 0.00 0.57 0.00 0.00 0.57 0.00 0.00 0.57 0.00 0.00 0.57 0.00 0.00 0.57 0.00 0.00 0.57 0.00 0.00 0.57 0.00 0.00 0.00 0.57 0.00 0.00 0.00 0.57 0.00 0.00 0.00 0.57 0.00 0.	tons/yr 273.03 0.00 2726.54 0.01 0.11 0.23 0.25 0.26 0.10 0.10 0.10 0.10 0.00 0.00 0.00 0.0
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclobexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene Gycol Ethylene Glycol	0.0000 100.00 100.00 100.00 62.33 0.00 622.50 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.03 0.02 0.04 0.00 0.02 0.04 0.00 0.02 0.04 0.00 0.02 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.02 0.00 0.00 0.00 0.00 0.00 0.02 0.00 0	lbs/day 1496.03 0.00 14939.97 0.24 0.61 1.26 0.30 1.43 0.56 0.87 0.00 1.50 0.00 1.50 0.00 0.57 0.00 0.57 0.00 1.52 0.72 0.71 0.01 0.02 0.72 0.01 0.02 0.77 0.72 0.77 0.	tons/yr 273.03 0.00 2726.54 0.04 0.11 0.23 0.05 0.26 0.10 0.16 0.00 0.16 0.00 0.10 0.00 0.0
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Heptane Nethylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Glycol Ethylene Glycol Ethylene Glycol	0.0000 100.00 100.00 100.00 62.33 0.00 622.50 0.01 0.03 0.05 0.01 0.06 0.02 0.04 0.00 0.06 0.00 0.06 0.000 0.00	Ibs/day 1496.03 0.00 14939.97 0.24 0.61 1.26 0.30 1.43 0.56 0.87 0.00 1.50 0.00 0.57 0.00 0.57 0.00 1.52 0.72 0.01 0.02 0.07 0.01 0.02 0.07 0.00 0.00 0.57 0.00 0.58 0.00 0.59 0.00 0.59 0.00 0.59 0.00 0.59 0.00 0.59 0.00 0.59 0.00 0.59 0.00 0.59 0.00 0.59 0.00 0.59 0.00 0.57 0.00 0.00 0.57 0.00 0.00 0.57 0.00 0.00 0.57 0.00 0.	tons/yr 273.03 0.00 2726.54 0.04 0.11 0.23 0.05 0.26 0.10 0.16 0.00 0.27 0.00 0.16 0.00 0.27 0.00 0.10 0.00 0.00 0.00 0.00 0.00 0.0
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Pentane n-Pentane n-Pentane n-Pentane n-Pentane Cyclopentane n-Hexane Cyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Gycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Water Methanol	0.0000 100.00 100.00 62.33 0.00 622.50 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.03 0.02 0.04 0.00 0.02 0.04 0.00 0.02 0.00 0.0	Ibs/day 1496.03 0.00 14939.97 0.24 0.61 1.26 0.30 1.43 0.56 0.87 0.00 1.50 0.00 0.57 0.00 0.57 0.00 0.57 0.00 0.57 0.00 0.57 0.00 0.57 0.00 0.57 0.00 0.57 0.00 0.57 0.00 0.58 0.72 0.72 0.72 0.72 0.01 0.02 0.07 0.01 0.00 659.83 0.00	tons/yr 273.03 0.00 2726.54 0.23 0.25 0.26 0.10 0.16 0.00 0.27 0.00 0.10 0.00 0.00 0.00 0.00 0.00 0.0
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Pentane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclopexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene Dylene Giycol Ethylene Giycol Ethylene Giycol Ethylene Giycol Ethylene Giycol Ethylene Giycol Ethylene Giycol Ethylene Giycol Ethylene Giycol	0.0000 100.00 62.33 0.00 622.50 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.02 0.04 0.00 0.02 0.00 0.00 0.00 0.00	lbs/day 1496.03 0.00 14939.97 0.24 0.61 1.26 0.30 1.43 0.56 0.87 0.00 1.50 1.50 0.00 0.57 0.00 0.57 0.00 0.57 0.00 0.57 0.00 0.57 0.00 0.57 0.00 0.57 0.00 0.57 0.00 0.57 0.00 0.57 0.00 0.57 0.00 0.58 0.00 1.52 0.72 0.72 0.01 0.02 0.72 0.01 0.02 0.07 0.01 0.02 0.07 0.01 0.02 0.07 0.01 0.02 0.00 0.00 0.00 0.57 0.00 0.00 0.00 0.57 0.00 0.00 0.00 0.00 0.00 0.57 0.00 0.	tons/yr 273.03 0.00 2726.54 0.04 0.11 0.23 0.05 0.26 0.10 0.16 0.00 0.27 0.00 0.10 0.00 0.10 0.00 0.00 0.00 0.0
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclohexane n-Hexane Cyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene Gycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol	0.0000 100.00 100.00 100.00 62.33 0.00 622.50 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.06 0.02 0.04 0.00 0.06 0.02 0.04 0.00 0	Ibs/day 1496.03 0.00 14939.97 0.24 0.61 1.26 0.30 1.43 0.56 0.87 0.00 1.50 0.00 1.50 0.00 0.57 0.00 0.57 0.00 1.52 0.72 0.01 0.02 0.07 0.01 0.02 0.07 0.01 0.02 0.07 0.01 0.02 0.07 0.01 0.02 0.07 0.01 0.02 0.07 0.01 0.02 0.07 0.01 0.02 0.07 0.01 0.02 0.07 0.01 0.02 0.07 0.01 0.02 0.07 0.01 0.02 0.07 0.01 0.02 0.07 0.01 0.02 0.07 0.01 0.02 0.07 0.01 0.02 0.07 0.01 0.02 0.07 0.01 0.02 0.07 0.01 0.02 0.01 0.02 0.07 0.01 0.02 0.07 0.01 0.02 0.07 0.01 0.02 0.07 0.01 0.02 0.02 0.01 0.02 0.07 0.01 0.02 0.02 0.01 0.02 0.02 0.01 0.02 0.02 0.00 0.02 0.03 0.00 0.02 0.01 0.02 0.02 0.00 0.02 0.00 0.02 0.00 0.02 0.01 0.00 0.02 0.01 0.00 0.02 0.02 0.00 0.00 0.02 0.01 0.00 0.00 0.02 0.02 0.00 0.00 0.02 0.01 0.00 0.00 0.02 0.01 0.00 0.00 0.02 0.07 0.01 0.00 0.00 0.00 0.02 0.07 0.01 0.00 0.	tons/yr 273.03 0.00 2726.54 0.04 0.11 0.23 0.05 0.26 0.10 0.10 0.10 0.00 0.27 0.00 0.27 0.00 0.27 0.00 0.10 0.00 0.00 0.28 0.13 0.00 0.00 0.00 0.00 0.00 0.00 0.00
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Butane i-Pentane n-Pentane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Gycol Ethylene Glycol Ethylene Glycol Ethylene Glycol SO2 SO2 Total Emissions	0.0000 100.00 100.00 105/hr 62.33 0.00 622.50 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.06 0.02 0.04 0.00 0.02 0.04 0.00 0.02 0.04 0.00 0.02 0.00 0.02 0.000 0.00	Ibs/day 1496.03 0.00 14939.97 0.24 0.61 1.26 0.30 1.43 0.56 0.87 0.00 1.50 0.00 1.50 0.00 0.57 0.00 0.00 1.52 0.72 0.72 0.01 0.02 0.07 0.01 0.00 0.00 1.52 0.72 0.01 0.02 0.07 0.01 0.00 0.00 0.02 0.02 0.00 0.	tons/yr 273.03 0.00 2726.54 0.04 0.11 0.23 0.05 0.26 0.10 0.16 0.00 0.27 0.00 0.10 0.00 0.28 0.13 0.00 0.00 0.28 0.13 0.00 0.00 0.00 0.00 0.00 0.00 0.00
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Pentane n-Pentane n-Pentane n-Pentane Nethyley(oblexane 1,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene p-Xylene Gycol Ethylene Glycol Ethylene Glycol Water Methanol O2 SO2 Total Emissions	0.0000 100.00 100.00 62.33 0.00 622.50 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.03 0.02 0.04 0.00 0.02 0.04 0.00 0.02 0.00 0.02 0.00 0.0	Ibs/day           1496.03           0.00           14939.97           0.24           0.61           1.26           0.30           1.43           0.56           0.87           0.00           1.50           0.00           0.57           0.00           0.57           0.00           0.57           0.00           0.57           0.00           0.57           0.00           0.57           0.00           0.57           0.00           0.57           0.00           0.01           0.02           0.07           0.01           0.00           669.83           0.00           2889.83           0.00           20005.35	tons/yr 273.03 0.00 2726.54 0.04 0.11 0.23 0.05 0.26 0.10 0.16 0.00 0.27 0.00 0.10 0.10 0.10 0.00 0.00 0.00 0.0
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclobexane n-Hexane Cyclobexane n-Heptane Benzene Benzene Toluene Ethyllene Glycol Ethylene Glycol Ethylene Glycol SO2 Total Emissions Total HC Emissions	0.0000 100.00 100.00 100.00 100.00 62.33 0.00 622.50 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.06 0.02 0.04 0.000 0.00	lbs/day 1496.03 0.00 14939.97 0.24 0.61 1.26 0.30 1.43 0.56 0.87 0.00 1.50 0.00 0.57 0.00 0.57 0.00 0.57 0.00 0.57 0.00 1.52 0.72 0.72 0.01 0.02 0.07 0.01 0.02 0.07 0.01 0.00 669.83 0.00 2889.83 0.00 20005.35 9.68	tons/yr 273.03 0.00 2726.54 0.04 0.11 0.23 0.05 0.26 0.10 0.16 0.00 0.27 0.00 0.10 0.00 0.00 0.00 0.00 0.00 0.0
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Suffide Nitrogen Methane Ethane Propane i-Butane n-Bettane n-Pentane n-Pentane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclobexane n-Yelene Sozi Total HC Emissions Total VOC Emissions	0.0000 100.00 100.00 100.00 62.33 0.00 622.50 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.06 0.02 0.04 0.000 0.00	Ibs/day           1496.03           0.00           14939.97           0.24           0.61           1.26           0.30           1.43           0.56           0.87           0.00           1.50           0.00           1.52           0.72           0.01           0.02           0.07           0.01           0.02           0.07           0.01           0.02           0.03           0.04           0.05           0.05           0.06           0.07           0.01           0.02           0.03           0.04           0.05           0.00           289.83           0.00           20005.35           9.68           8.83	tons/yr 273.03 0.00 2726.54 0.04 0.11 0.23 0.05 0.26 0.10 0.16 0.00 0.27 0.00 0.10 0.00 0.27 0.00 0.10 0.00 0.28 0.13 0.00 0.00 0.00 0.00 0.00 0.00 0.00
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Pentane n-Pentane n-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol SO2 Total Etmissions Total HZP Emissions Total HZP Emissions	0.0000 100.00 100.00 62.33 0.00 622.50 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.04 0.06 0.02 0.04 0.00 0.02 0.04 0.00 0.02 0.04 0.00 0.02 0.04 0.00 0.02 0.00 0.02 0.00 0.02 0.00 0.02 0.00 0.02 0.00 0.02 0.00 0.02 0.00 0.02 0.00 0.0	Ibs/day           1496.03           0.00           14939.97           0.24           0.61           1.26           0.30           1.43           0.56           0.87           0.00           1.50           0.00           0.57           0.00           0.57           0.00           0.57           0.00           0.57           0.00           0.57           0.00           0.01           0.02           0.07           0.01           0.00           669.83           0.00           2839.83           0.00           28005.35           9.68           8.83           3.85	tons/yr 273.03 0.00 2726.54 0.04 0.11 0.23 0.05 0.25 0.25 0.20 0.10 0.10 0.10 0.10 0.00 0.27 0.00 0.10 0.10 0.00 0.27 0.00 0.10 0.10 0.00 0.28 0.13 0.00 0.00 0.28 0.13 0.00 0.00 0.28 0.13 0.00 0.00 0.28 0.13 0.00 0.00 0.13 0.00 0.11 0.15 0.27 0.00 0.11 0.11 0.11 0.11 0.11 0.11 0.1
SO2 Total EMISSIONS REPORTS: CONTROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclobexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol Total Emissions Total HC Emissions To	0.0000 100.00 100.00 100.00 100.00 62.33 0.00 622.50 0.01 0.03 0.05 0.01 0.03 0.05 0.01 0.06 0.02 0.04 0.00	lbs/day 1496.03 0.00 14939.97 0.24 0.61 1.26 0.30 1.43 0.56 0.87 0.00 1.50 1.50 1.50 0.00 0.57 0.00 0.00 0.57 0.00 0.00 0.57 0.00 0.00 0.57 0.00 0.00 0.57 0.00 0.00 0.57 0.00 0.00 0.00 0.57 0.00 0.00 0.00 0.57 0.00 0.00 0.00 0.57 0.00 0.00 0.00 0.57 0.00 0.	tons/yr 273.03 0.00 2726.54 0.04 0.11 0.23 0.05 0.26 0.10 0.16 0.00 0.27 0.00 0.10 0.00 0.00 0.00 0.00 0.00 0.0

Component	lbs/hr	lbs/day	tons/vr
Carbon Diovide	0.08	105/08y 23/18	
Hydrogen Sulfida	0.50	20.40	4
Nitrogon	0.00	0.00	0
Methane	0.00 0.49	11 8/	0 2
Fthane	1.28	30 72	5
Pronane	2 66	53.72 63.85	11
i-Rutane	0.64	15.25	211
I-Butdrie	2.04	13.20	12
n-Butane	3.07	/3./4	13
I-Pentane	1.28	30.60	5
n-Pentane	2.02	48.41	8
Cyclopentane	0.00	0.00	C
n-Hexane	4.10	98.51	17
Cyclohexane	0.00	0.00	(
n-Heptane	2.25	54.09	9
Methylcyclohexane	0.00	0.00	(
2,2,4-Trimethylpentane	0.00	0.00	(
Benzene	4.83	115.92	2:
Toluene	3.83	91.94	16
Ethylbenzene	0.14	3.27	(
o-Xylene	0.26	6.22	:
m-Xylene	0.82	19.71	3
p-Xylene	0.07	1.56	
Triethylene Glycol	0.02	0.39	
Ethylene Glycol	0.00	0.00	
Water	67.93	1630 35	29
Methanol	0.00	0.00	25
	0.00	0.00	
02	0.00	0.00	
SU2	0.00	2210.01	10:
	50.00	2519.91	42:
Total UC Emissions		666 DD	13-
	27.75	600.02	12
	25.98	623.46	11.
I OTAL HAP Emissions	14.05	337.12	6
TROLLED FLASH TANK EMISSIONS			
Companyat	lbc/br	lbs/day	tonch
Component Contour Disvite	lbs/hr	lbs/day	tons/yr
Component Carbon Dioxide	lbs/hr 0.00	lbs/day 0.00	tons/yr
Component Carbon Dioxide Hydrogen Sulfide	lbs/hr 0.00 0.00	lbs/day 0.00 0.00	tons/yr
Component Carbon Dioxide Hydrogen Sulfide Nitrogen	lbs/hr 0.00 0.00 0.00 0.00	lbs/day 0.00 0.00 0.00	tons/yr
Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane	lbs/hr 0.00 0.00 0.00 0.00	lbs/day 0.00 0.00 0.00 0.00	tons/yr
Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane	lbs/hr 0.00 0.00 0.00 0.00 0.00	lbs/day 0.00 0.00 0.00 0.00 0.00	tons/yr
Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane	Ibs/hr         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00	lbs/day 0.00 0.00 0.00 0.00 0.00 0.00	tons/yr
Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane	Ibs/hr         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00	lbs/day 0.00 0.00 0.00 0.00 0.00 0.00	tons/yr
Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane	lbs/hr           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00	lbs/day 0.00 0.00 0.00 0.00 0.00 0.00 0.00	tons/yr
Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane	lbs/hr 0.00	lbs/day 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	tons/yr
Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane n-Pentane	Ibs/hr         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00	lbs/day 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	tons/yr
Component Carbon Dioxide Hydrogen Suffide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane	Ibs/hr         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00	lbs/day         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00	tons/yr
Component Carbon Dioxide Hydrogen Suffide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane	Ibs/hr         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00	lbs/day         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00	tons/yr
Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclohexane	Ibs/hr         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00	lbs/day 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	tons/yr
Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclobexane n-Hexane n-Heptane	Ibs/hr         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00	lbs/day         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00	tons/yr
Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane	Ibs/hr         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00	lbs/day         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00	tons/yr
Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane 2,2,4-Trimethylpentane	lbs/hr           0.00	lbs/day           0.00	tons/yr
Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopexane n-Hexane 2,2,4-Trimethylpentane Benzene	Ibs/hr         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00	lbs/day         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00	tons/yr
Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclobexane n-Hexane 2,2,4-Trimethylpentane Benzene Toluene	Ibs/hr         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00	lbs/day         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00	tons/yr
Component Carbon Dioxide Hydrogen Suffide Nitrogen Methane Ethane Propane i-Butane i-Pentane Cyclopentane n-Hexane Cyclohexane n-Hexane Cyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene	Ibs/hr         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00	lbs/day         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00	tons/yr
Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclohexane n-Hexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene	Ibs/hr         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00	lbs/day           0.00	tons/yr
Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopexane n-Hexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene	Ibs/hr         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00	lbs/day         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00	tons/yr
Component Carbon Dioxide Hydrogen Suffide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclobexane n-Hexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene p-Xylene	Ibs/hr         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00	lbs/day         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00	tons/yr
Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Pentane n-Butane i-Pentane Cyclopentane Cyclopentane Cyclopexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene p-Xylene Urclopentane Benzene Triethylbenzene Triethylene Glycol	Ibs/hr         0.00           0.00         0.00	lbs/day         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00	tons/yr
Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Heptane Cyclopexane n-Heptane Qyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol	Ibs/hr         0.00           0.00         0.00	lbs/day         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00	tons/yr
Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol	Ibs/hr         0.00           0.00         0.00	lbs/day         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00	tons/yr
Component Carbon Dioxide Hydrogen Suffide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane Kethylcyclohexane 2,2,4-Trimethylpentane Benzene o-Xylene Toluene Ethylbenzene o-Xylene m-Xylene Divelene Stylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Water	Ibs/hr         0.00           0.00         0.00	lbs/day         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00	tons/yr
Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Heptane Nethylcyclohexane n-Heptane Xethylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol	Ibs/hr         0.00           0.00         0.00	lbs/day         0.00           0.00         0.00	tons/yr
Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Uwter Methanol O2	Ibs/hr         0.00           0.00         0.00	lbs/day           0.00	tons/yr
Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopexane n-Hexane 2,2,4-Trimethylpentane Benzene Z,2,4-Trimethylpentane Ethylbenzene o-Xylene Toluene Ethylbenzene o-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol O2 SO2	Ibs/hr         0.00           0.00         0.00	lbs/day         0.00           0.00         0.00	tons/yr
Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Heytane Cyclopexane n-Heytane Cyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol Uwtar Methanol O2 SO2	Ibs/hr         0.00           0.00         0.00	lbs/day           0.00	tons/yr
Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane 2,2,4-Trimethylpentane Benzene Z,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol O2 502 Total Emissions	Ibs/hr           0.00	Ibs/day           0.00	tons/yr
Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane Cyclopentane NetNy(vclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Total HC Emissions Total HC Emissions	Ibs/hr         0.00           0.00         0.00	Ibs/day         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00	tons/yr
Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane Cyclopentane 2,2,4-Trimethylepentane 2,2,4-Trimethylpentane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol So2 Total HAP Emissions Total HC Emissions Total HC Emissions	Ibs/hr         0.00           0.00         0.00	Ibs/day           0.00	tons/yr

UNCONTROLLED FLASH TANK OFF GAS			
Component	lbs/hr	lbs/day	tons/yr
Carbon Dioxide	3.38	81.01	14.78
Hydrogen Sulfide	0.00	0.00	0.00
Nitrogen	0.21	5.08	0.93
Methane	14.03	336.77	61.46
Ethane	11.00	263.98	48.18
Propane	12.17	292.04	53.30
i-Butane	2.15	51.66	9.43
n-Butane	7.18	1/2.32	31.45
i-Pentane	1.91	45.77	8.35
n-Pentane Guelepentane	2.54	60.93	11.12
cyclopentarie	0.00	0.00	0.00
Cycloboxano	2.32	0.35	11.02
cyclollexalle	0.00	0.00	0.00
Methylcyclobeyane	0.80	20.00	0.00
2.2.4-Trimethylpentane	0.00	0.00	0.00
2,2,4-Timethylpentale Benzene	0.00	6.00	1 10
Toluono	0.23	0.04	1.10
Ethylhonzono	0.11	2.08	0.49
e Yulono	0.00	0.00	0.01
u-Xylene m-Vylene	0.00	0.09	0.02
n-Xylene n Vylene	0.01	0.35	0.00
p-Aylene Triethylene Chucol	0.00	0.05	0.01
Ethylene Glycol	0.00	0.08	0.01
Ethylene Glycol	0.00	0.00 cr o	0.00
Methanol	0.30	8.73	1.39
	0.00	0.00	0.00
SO2	0.00	0.00	0.00
Total Emissions	58 69	1408 61	257.07
	50.05	1100101	257.07
Total HC Emissions	54.74	1313.78	239.77
Total VOC Emissions	29.71	713.03	130.13
Total HAP Emissions	2.90	69.63	12.71
Total GHG Emissions	17.41	417.79	76.25
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS			
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Content Content District	lbs/hr	lbs/day	tons/yr
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Underses Culture	lbs/hr 65.71	lbs/day 1577.04	tons/yr 287.81
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide	lbs/hr 65.71 0.00	lbs/day 1577.04 0.00	tons/yr 287.81 0.00
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Mithoge	lbs/hr 65.71 0.00 622.71	lbs/day 1577.04 0.00 14945.05	tons/yr 287.81 0.00 2727.47
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane	lbs/hr 65.71 0.00 622.71 14.04 11.02	lbs/day 1577.04 0.00 14945.05 337.01 264.59	tons/yr 287.81 0.00 2727.47 61.50 48.29
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Pronzen	lbs/hr 65.71 0.00 622.71 14.04 11.02 13.22	lbs/day 1577.04 0.00 14945.05 337.01 264.59 203.30	tons/yr 287.81 0.00 2727.47 61.50 48.29 52.53
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Buttane	lbs/hr 65.71 0.00 622.71 14.04 11.02 12.22 2.16	lbs/day 1577.04 0.00 14945.05 337.01 264.59 293.30 51.95	tons/yr 287.81 0.00 2727.47 61.50 48.29 53.53 9.48
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane Drbutane	lbs/hr 65.71 0.00 622.71 14.04 11.02 12.22 2.16 7.24	lbs/day 1577.04 0.00 14945.05 337.01 264.59 293.30 51.95 173.74	tons/yr 287.81 0.00 2727.47 61.50 48.29 53.53 9.48 31.71
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Partane	lbs/hr 65.71 0.00 622.71 14.04 11.02 12.22 2.16 7.24 1 93	lbs/day 1577.04 0.00 14945.05 337.01 264.59 293.30 51.95 173.74 46 24	tons/yr 287.81 0.00 2727.47 61.50 48.29 53.53 9.48 31.71 8 46
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane o-Pentane	lbs/hr 65.71 0.00 622.71 14.04 11.02 12.22 2.16 7.24 1.93 2.58	lbs/day 1577.04 0.00 14945.05 337.01 264.59 293.30 51.95 173.74 46.34 61.80	tons/yr 287.81 0.00 2727.47 61.50 48.29 53.53 9.48 31.71 8.46 11 28
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane	lbs/hr 65.71 0.00 622.71 14.04 11.02 12.22 2.16 7.24 1.93 2.58 0.00	lbs/day 1577.04 0.00 14945.05 337.01 264.59 293.30 51.95 173.74 46.34 61.80 0.00	tons/yr 287.81 0.00 2727.47 61.50 48.29 53.53 9.48 31.71 8.46 11.28 0.00
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane D-Hexane	lbs/hr 65.71 0.00 622.71 14.04 11.02 12.22 2.16 7.24 1.93 2.58 0.00 2.58	lbs/day 1577.04 0.00 14945.05 337.01 264.59 293.30 51.95 173.74 46.34 61.80 0.00 61.88	tons/yr 287.81 0.00 2727.47 61.50 48.29 53.53 9.48 31.71 8.46 11.28 0.00 11 29
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclopexane	lbs/hr 65.71 0.00 622.71 14.04 11.02 12.22 2.16 7.24 1.93 2.58 0.00 2.58 0.00	lbs/day 1577.04 0.00 14945.05 337.01 264.59 293.30 51.95 173.74 46.34 61.80 0.00 61.88 0.00	tons/yr 287.81 0.000 2727.47 61.50 48.29 53.53 9.48 31.71 8.46 11.28 0.00 11.29 0.00
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclobexane n-Hentane	lbs/hr         65.71           0.00         622.71           14.04         11.02           12.22         2.16           7.24         1.93           2.58         0.00           0.58         0.00           0.88         0.88	lbs/day           1577.04           0.00           14945.05           337.01           264.59           293.30           51.95           173.74           46.34           61.80           0.00           61.88           0.00           61.88           0.00           21.16	tons/yr 287.81 0.00 2727.47 61.50 48.29 53.53 9.48 31.71 8.46 11.28 0.00 11.29 0.00 3.86
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane	lbs/hr 65.71 0.00 622.71 14.04 11.02 12.22 2.16 7.24 1.93 2.58 0.00 2.58 0.00 0.88 0.00 0.88 0.00	lbs/day 1577.04 0.00 14945.05 337.01 264.59 293.30 51.95 173.74 46.34 61.80 0.00 61.88 0.00 21.16 0.00	tons/yr 287.81 0.00 2727.47 61.50 48.29 53.53 9.48 31.71 8.46 11.28 0.00 11.29 0.00 3.86 0.00
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2.2.4-Trimethylpentane	lbs/hr 65.71 0.00 622.71 14.04 11.02 12.22 2.16 7.24 1.93 2.58 0.00 2.58 0.00 0.88 0.00 0.88 0.00	lbs/day 1577.04 0.00 14945.05 337.01 264.59 293.30 51.95 173.74 46.34 61.80 0.00 61.88 0.00 21.16 0.00 21.16 0.00	tons/yr 287.81 0.00 2727.47 61.50 48.29 53.53 9.48 31.71 8.46 11.28 0.00 11.29 0.00 3.86 0.00 0.00
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene	lbs/hr 65.71 0.00 622.71 14.04 11.02 12.22 2.16 7.24 1.93 2.58 0.00 2.58 0.00 0.88 0.00 0.88 0.00 0.31	lbs/day 1577.04 0.00 14945.05 337.01 264.59 293.30 51.95 173.74 46.34 61.80 0.00 61.88 0.00 21.16 0.00 0.00 0.00 0.00 0.00	tons/yr 287.81 0.00 2727.47 61.50 48.29 53.53 9.48 31.71 8.46 11.28 0.00 11.29 0.00 3.86 0.00 0.3.86 0.00 0.00
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclopexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene	lbs/hr         65.71           0.00         622.71           14.04         11.02           12.22         2.16           7.24         1.93           2.58         0.00           0.258         0.00           0.88         0.00           0.88         0.00           0.31         0.34	lbs/day           1577.04           0.00           14945.05           337.01           264.59           293.30           51.95           173.74           46.34           61.80           0.00           61.88           0.00           21.16           0.00           7.56           3.40	tons/yr 287.81 0.00 2727.47 61.50 48.29 53.53 9.48 31.71 8.46 11.28 0.00 11.29 0.00 3.86 0.00 0.00 0.00 0.00 1.38 0.00
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Butane n-Butane i-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene	lbs/hr         65.71           0.00         622.71           14.04         11.02           12.22         2.16           7.24         1.93           2.58         0.00           0.258         0.00           0.88         0.00           0.31         0.14	lbs/day           1577.04           0.00           14945.05           337.01           264.59           293.30           51.95           173.74           46.34           61.80           0.00           21.16           0.00           7.56           3.40           0.07	tons/yr 287.81 0.00 2727.47 61.50 48.29 53.53 9.48 31.71 8.46 11.28 0.00 11.29 0.00 11.29 0.00 3.86 0.00 0.00 1.38 0.00
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane Sz,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Sylene	lbs/hr           65.71           0.00           622.71           14.04           11.02           12.22           2.16           7.24           1.93           2.58           0.00           0.88           0.00           0.31           0.14           0.00	lbs/day           1577.04           0.00           14945.05           337.01           264.59           293.30           51.95           173.74           46.34           61.80           0.00           21.16           0.00           7.56           3.40           0.07           0.11	tons/yr 287.81 0.00 2727.47 61.50 48.29 53.53 9.48 31.71 8.46 11.28 0.00 11.29 0.00 11.29 0.00 11.29 0.00 11.38 0.00 0.00 0.000 1.388 0.62 0.01 0.01
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Pentane Cyclopentane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene	lbs/hr           65.71           0.00           622.71           14.04           11.02           12.22           2.16           7.24           1.93           2.58           0.00           0.88           0.00           0.88           0.00           0.31           0.14           0.00           0.00           0.00	lbs/day           1577.04           0.00           14945.05           337.01           264.59           293.30           51.95           173.74           46.34           61.80           0.00           21.16           0.00           7.56           3.40           0.011           0.42	tons/yr 287.81 0.000 2727.47 61.50 48.29 53.53 9.48 31.71 8.46 11.28 0.00 11.29 0.00 3.86 0.00 0.00 1.38 0.00 0.00 0.00 0.02 0.02 0.02
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Sylene m-Xylene p-Xylene	lbs/hr           65.71           0.00           622.71           14.04           11.02           12.22           2.16           7.24           1.93           2.58           0.00           2.58           0.00           0.88           0.00           0.31           0.14           0.00           0.02           0.00           0.02           0.00	lbs/day           1577.04           0.00           14945.05           337.01           264.59           293.30           51.95           173.74           46.34           61.80           0.00           61.88           0.00           21.16           0.00           7.56           3.40           0.07           0.11           0.42           0.04	tons/yr 287.81 0.00 2727.47 61.50 48.29 53.53 9.48 31.71 8.46 11.28 0.00 11.29 0.00 11.29 0.00 11.29 0.00 1.386 0.00 0.00 0.00 0.00 0.01 0.02 0.08 0.01
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Butane n-Pentane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol	lbs/hr           65.71           0.00           622.71           14.04           11.02           12.22           2.16           7.24           1.93           2.58           0.00           2.58           0.00           2.58           0.00           0.31           0.14           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00	lbs/day           1577.04           0.00           14945.05           337.01           264.59           293.30           51.95           173.74           46.34           61.80           0.00           61.88           0.00           21.16           0.00           7.56           3.40           0.07           0.11           0.42           0.04           0.08	tons/yr 287.81 0.00 2727.47 61.50 48.29 53.53 9.48 31.71 8.46 11.28 0.00 11.29 0.00 11.29 0.00 11.29 0.00 11.38 0.00 0.00 1.38 0.00 0.00 0.00 0.00 0.01 0.01 0.01
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene p-Sylene Gyclo	lbs/hr           65.71           0.00           622.71           14.04           11.02           12.22           2.16           7.24           1.93           2.58           0.00           2.58           0.00           0.88           0.00           0.31           0.14           0.00           0.02           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00	lbs/day           1577.04           0.00           14945.05           337.01           264.59           293.30           51.95           173.74           46.34           61.80           0.00           61.88           0.00           21.16           0.00           7.56           3.40           0.07           0.11           0.42           0.04           0.08           0.00	tons/yr 287.81 0.00 2727.47 61.50 48.29 53.53 9.48 31.71 8.46 11.28 0.00 11.29 0.00 11.29 0.00 11.29 0.00 11.38 0.00 0.01 0.02 0.01 0.02 0.01 0.01 0.01
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Butane n-Butane i-Pentane Cyclopentane Cyclopentane N-Hexane Cyclopentane N-Heytane N-Heytane Nethylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol	lbs/hr           65.71           0.00           622.71           14.04           11.02           12.22           2.16           7.24           1.93           2.58           0.00           0.88           0.00           0.31           0.14           0.00           0.02           0.00	lbs/day           1577.04           0.00           14945.05           337.01           264.59           293.30           51.95           173.74           46.34           61.80           0.00           61.88           0.00           21.16           0.00           7.56           3.40           0.01           0.42           0.04           0.08           0.00	tons/yr 287.81 0.000 2727.47 61.50 48.29 53.53 9.48 31.71 8.46 11.28 0.00 11.29 0.00 11.29 0.00 11.29 0.00 11.38 0.00 0.000 0.000 0.000 0.001 0.01 0.01
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene	Ibs/hr         65.71           0.00         622.71           14.04         11.02           12.22         2.16           7.24         1.93           2.58         0.00           0.00         0.258           0.00         0.88           0.00         0.031           0.14         0.00           0.00         0.02           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00	lbs/day           1577.04           0.00           14945.05           337.01           264.59           293.30           51.95           173.74           46.34           61.80           0.00           61.88           0.00           21.16           0.00           7.56           3.40           0.07           0.11           0.42           0.04           0.08           0.00           678.56           0.00	tons/yr 287.81 0.00 2727.47 61.50 48.29 53.53 9.48 31.71 8.46 11.28 0.00 11.29 0.00 11.29 0.00 1.386 0.00 0.01 1.38 0.02 0.01 0.02 0.01 0.02 0.01 0.02 0.01 0.02 0.01 0.02 0.01 0.01
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene O-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol	lbs/hr           65.71           0.00           622.71           14.04           11.02           12.22           2.16           7.24           1.93           2.58           0.00           2.58           0.00           2.58           0.00           0.88           0.00           120.41	lbs/day           1577.04           0.00           14945.05           337.01           264.59           293.30           51.95           173.74           46.34           61.80           0.00           61.88           0.00           21.16           0.00           7.56           3.40           0.07           0.11           0.42           0.04           0.08           0.00           678.56           0.00           2889.83	tons/yr 287.81 0.00 2727.47 61.50 48.29 53.53 9.48 31.71 8.46 11.28 0.00 11.29 0.00 11.29 0.00 11.29 0.00 11.28 0.00 0.00 1.386 0.00 0.00 0.00 0.00 1.38 0.02 0.01 0.02 0.01 0.02 0.01 0.02 0.01 0.02 0.01 0.02 0.01 0.02 0.02
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Butane i-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene Jylene Glycol Ethylene Glycol Ethylene Glycol Methanol O2	lbs/hr           65.71           0.00           622.71           14.04           11.02           12.22           2.16           7.24           1.93           2.58           0.00           2.58           0.00           0.88           0.00           0.31           0.14           0.00           120.41           0.00	lbs/day           1577.04           0.00           14945.05           337.01           264.59           293.30           51.95           173.74           46.34           61.80           0.00           61.88           0.00           21.16           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.011           0.42           0.08           0.00           678.56           0.00           2889.83           0.00	tons/yr 287.81 0.00 2727.47 61.50 48.29 53.53 9.48 31.71 8.46 11.28 0.00 11.29 0.00 11.29 0.00 11.29 0.00 11.38 0.00 0.00 1.38 0.02 0.01 0.02 0.01 0.02 0.03 0.01 0.02 0.03 0.01 0.01 0.02 0.03 0.01 0.02 0.03 0.01 0.02 0.03 0.03 0.01 0.00 0.03 0.00 0.00 0.00
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene p-Xylene D-Xylene Gyclo Ethylbenzene O-Xylene D-X	lbs/hr           65.71           0.00           622.71           14.04           11.02           12.22           2.16           7.24           1.93           2.58           0.00           2.58           0.00           0.88           0.00           0.31           0.14           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           120.41           0.00           892.25	lbs/day           1577.04           0.00           14945.05           337.01           264.59           293.30           51.95           173.74           46.34           61.80           0.00           61.88           0.00           21.16           0.00           0.00           7.56           3.40           0.07           0.11           0.42           0.04           0.08           0.00           678.56           0.00           289.83           0.00           289.83           0.00           21413.95	tons/yr 287.81 0.00 2727.47 61.50 48.29 53.53 9.48 31.71 8.46 11.28 0.00 11.29 0.00 11.29 0.00 11.29 0.00 11.38 0.00 0.00 1.386 0.00 0.00 0.01 0.02 0.01 0.01 0.01 0.01
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Pentane Cyclopentane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene M-Xylene Gyclo Ethylene Glycol Water Methanol O2 SO2	lbs/hr           65.71           0.00           622.71           14.04           11.02           12.22           2.16           7.24           1.93           2.58           0.00           0.88           0.00           0.31           0.14           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           28.27           0.00           120.41           0.00           892.25	lbs/day           1577.04           0.00           14945.05           337.01           264.59           293.30           51.95           173.74           46.34           61.80           0.00           21.16           0.00           7.56           3.40           0.01           0.02           7.56           3.40           0.01           0.42           0.04           0.08           0.00           678.56           0.00           289.83           0.00           289.83           0.00           21413.95	tons/yr 287.81 0.00 2727.47 61.50 48.29 53.53 9.48 31.71 8.46 11.28 0.00 11.29 0.00 11.29 0.00 3.86 0.00 0.00 1.38 0.62 0.01 0.02 0.01 0.02 0.01 0.02 0.01 0.02 0.01 0.02 0.01 0.02 0.03 0.01 0.01 0.01 0.01 0.01 0.01 0.01
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane n-Pentane Cyclopentane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Total HC Emissions	lbs/hr           65.71           0.00           622.71           14.04           11.02           12.22           2.16           7.24           1.93           2.58           0.00           2.58           0.00           0.00           0.00           0.01           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           28.27           0.00           120.41           0.00           892.25           55.14	lbs/day           1577.04           0.00           14945.05           337.01           264.59           293.30           51.95           173.74           46.34           61.80           0.00           21.16           0.00           7.56           3.40           0.07           0.11           0.42           0.04           0.08           0.00           678.56           0.00           289.83           0.00           21413.95           1323.47	tons/yr 287.81 0.00 2727.47 61.50 48.29 53.53 9.48 31.71 8.46 11.28 0.00 11.29 0.00 11.29 0.00 11.29 0.00 11.29 0.00 1.386 0.00 0.01 0.02 0.01 0.02 0.01 0.02 0.01 0.01
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Pentane cyclopentane n-Hexane Cyclopentane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Gyclo Ethylene Glycol Ethylene Glycol Ethylene Glycol Triethylene Glycol Total HC Emissions Total HC Emissions	lbs/hr           65.71           0.00           622.71           14.04           11.02           12.22           2.16           7.24           1.93           2.58           0.00           2.58           0.00           2.58           0.00           0.88           0.00           0.31           0.14           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           120.41           0.00           892.25           55.14           30.08	lbs/day           1577.04           0.00           14945.05           337.01           264.59           293.30           51.95           173.74           46.34           61.80           0.00           61.88           0.00           21.16           0.00           7.56           3.40           0.07           0.11           0.42           0.04           0.08           0.00           289.83           0.00           21413.95           1323.47           721.86	tons/yr 287.81 0.00 2727.47 61.50 48.29 53.53 9.48 31.71 8.46 11.28 0.00 11.29 0.00 11.29 0.00 11.29 0.00 11.28 0.00 0.00 1.386 0.00 0.00 0.00 0.00 1.38 0.02 0.01 0.02 0.01 0.02 0.01 0.02 0.03 0.01 0.01 0.02 0.03 0.00 1.23.84 0.00 0.01 0.00 1.23.84 0.00 0.01 0.00 0.00 0.00 0.00 0.00 0.0
COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane i-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene D-Xylene Tritethylene Glycol Ethylene Glycol Ethylene Glycol Total HC Emissions Total HC Emissions Total HC Emissions	lbs/hr           65.71           0.00           622.71           14.04           11.02           12.22           2.16           7.24           1.93           2.58           0.00           2.58           0.00           0.88           0.00           0.31           0.14           0.00           120.41           0.00           892.25           55.14           30.08           3.06	lbs/day           1577.04           0.00           14945.05           337.01           264.59           293.30           51.95           173.74           46.34           61.80           0.00           61.83           0.00           21.16           0.00           0.00           0.01           0.02           0.03           0.04           0.05           3.40           0.07           0.11           0.42           0.04           0.05           0.06           678.56           0.00           289.83           0.00           21413.95           1323.47           721.86           73.48	tons/yr 287.81 0.00 2727.47 61.50 48.29 53.53 9.48 31.71 8.46 11.28 0.00 11.29 0.00 11.29 0.00 11.29 0.00 11.29 0.00 11.38 0.00 0.00 1.38 0.02 0.01 0.02 0.01 0.02 0.03 0.01 0.02 0.01 0.02 0.03 0.01 0.02 0.03 0.01 0.02 0.03 0.00 0.03 0.00 0.03 0.00 0.00

BTEX CONDENSER Component Carbon Dioxidd Hydrogen Sulfidd Nitroger Methann Ethann Propan i-Butanc	Condenser Outlet Temperatuu Condenser Put Hydrocarbon Recove Produced Wate VOC Control Efficienc BTEX Control Efficienc Dissolved Hydrocarbons in Wate Emitted (wt. %) 99. 0.	e: 120.00 y: -0.07 y: 0.65 er: 4.60 y: 29.11 y: 42.97 y: 50.82 er: 851.20	deg. F psia MMBTU/hr bbls/day bbls/day % % % % % % % % Constant (ch of (ch
BTEX CONDENSER Component Carbon Dioxidd Hydrogen Sulfidd Nitroger Methan Ethan Propan i-Butanc	Condenser Outlet Temperatur Condenser Pressur Condenser Duf Hydrocarbon Recover Produced Wate VOC Control Efficienc HAP Control Efficienc BTEX Control Efficienc Dissolved Hydrocarbons in Wate Emitted (wt. %) 99. 0.0. 99.	e: 120.00 e: 14.10 y: -0.07 y: 0.65 er: 4.60 y: 29.11 y: 42.97 y: 50.82 er: 851.20	deg. F psia MMBTU/hr bbls/day bbls/day % % % % % %
BTEX CONDENSER Component Carbon Dioxidi Hydrogen Sulfidi Nitroger Methan Ethan Propan i-Butanc	Condenser Outlet Temperatur Condenser Pressur Condenser Dui Hydrocarbon Recovel Produced Wat VOC Control Efficienc HAP Control Efficienc Dissolved Hydrocarbons in Wate Emitted (wt. %) 99. 0.0. 99.	re: 120.00 re: 14.10 ry: -0.07 ry: 0.65 re: 4.60 ry: 29.11 ry: 42.97 ry: 50.82 re: 851.20	deg. F psia MMBTU/hr bbls/day bbls/day % % % % % % Casternal (ct. 8/)
Component Carbon Dioxid Hydrogen Sulfid Nitroger Methan Ethan Propan i-Butanc	Condenser Portier Terinperatur Condenser Dur Hydrocarbon Recover Produced Wat VOC Control Efficienc HAP Control Efficienc Dissolved Hydrocarbons in Wate Emitted (wt. %) Emitted (wt. %) 99. 99.	e: 120.00 e: 14.10 y: -0.07 y: 0.65 er: 4.60 y: 29.11 y: 42.97 y: 50.82 er: 851.20	ueg.r psia MMBTU/hr bbls/day bbls/day % % % % % % Condensed (ch %)
Component Carbon Dioxid Hydrogen Sulfid Nitroger Methan Ethan Propan i-Butand	Condenser Dui Hydrocarbon Recovel Produced Wat VOC Control Efficienc HAP Control Efficienc BTEX Control Efficienc Dissolved Hydrocarbons in Wate Emitted (wt. %) 99. 0. 0. 99.	y: -0.07 y: 0.65 er: 4.60 y: 29.11 y: 42.97 y: 50.82 er: 851.20	MMBTU/hr bbls/day bbls/day % % % % % mg/L
Component Carbon Dioxid Hydrogen Sulfid Nitroger Methan Ethan Propan i-Butand	Hydrocarbon Recover Produced Watt VOC Control Efficient HAP Control Efficient BTEX Control Efficient Dissolved Hydrocarbons in Watt Emitted (wt. %) Emitted (wt. %) 99. 0.	y: 0.65 er: 4.60 cy: 29.11 cy: 42.97 cy: 50.82 er: 851.20	bbls/day bbls/day % % % mg/L
Component Carbon Dioxid Hydrogen Sulfid Nitroger Methan Ethan Propan i-Butanc i-Butanc	Produced Watk VOC Control Efficient HAP Control Efficient BTEX Control Efficient Dissolved Hydrocarbons in Wate Emitted (wt. %) Emitted (wt. %) 99. 0. 99.	er: 4.60 cy: 29.11 cy: 42.97 cy: 50.82 er: 851.20	bbls/day % % % mg/L
Component Carbon Dioxid Hydrogen Sulfid Nitroger Methan Ethano Propan i-Butano i-Butano	HAP Control Efficient HAP Control Efficient BTEX Control Efficient Dissolved Hydrocarbons in Wate Emitted (wt. %) Emitted (wt. %) 99. 0.	y: 29.11 y: 42.97 y: 50.82 er: 851.20	% % mg/L
Component Carbon Dioxid Hydrogen Sulfid Nitroger Methan Ethano Propan i-Butano i-Butano	BTEX Control Efficient Dissolved Hydrocarbons in Wate Emitted (wt. %) 99. 0.0. 99.	er: 851.20	% mg/L
Component Carbon Dioxid Hydrogen Sulfid Nitroger Methan Ethan Propan i-Butan	Dissolved Hydrocarbons in Wate Emitted (wt. %) 2 99. 2 0. 3 99.	er: 851.20	mg/L
Component Carbon Dioxid Hydrogen Sulfid Nitroger Methan Ethan Propan i-Butan	Emitted (wt. %) 99. 0. 9 99. 9 99. 9 99. 9 99. 9 99. 9 99. 9 99. 9 99. 9 99. 9 99. 9 99. 9		Condensed (with 0())
Hydrogen Sulfid Nitrogen Methan Ethan Propanc i-Butanc	e 0. 99.		Condensed (wt. %)
Nitrogei Methani Ethani Propani i-Butani	99.1	00	0.00
Methan Ethan Propan i-Butan		97	0.03
Ethan Propan i-Butanc	99.	92	0.08
i-Butan	99.	51 27	0.39
	97.	81	2.19
n-Butane	96.	58	3.32
i-Pentan	92.	13	7.87
n-Pentan	90.	00	10.00
Cyclopentan	0.	00 De	0.00
Cyclohexan	0.	00	0.00
n-Heptan	52.	33	47.67
Methylcyclohexan	0.	00	0.00
2,2,4-Trimethylpentane	0.	00	0.00
Benzene	65.	41	34.59
Ethylbenzen		20 53	82 37
o-Xylen	17.	96	82.04
m-Xylen	17.	78	82.22
p-Xylene	18.	13	81.87
Triethylene Glyco	0.	00	100.00
Ethylene Giyco Wate	1.	32	98.68
Methanc	0.	00	0.00
02	. 0.	00	0.00
SOZ	. 0.	00	0.00
ABSORBER			
	Absorber Stage	es: 3.00	
	Dry Gas Dew Poir	nt: 3.20	Ib H2O/MMSCF
	Temperatur	e: 120.00	deg. F
	Dry Gas Flow Rat	e: 1113.40	MMSCFD
	TEG Losses with Dry Ga	is: 0.61	lb/hr
	Wet Gas Water Conter	nt: 69.22	lb H2O/MMSCF
	Lean Glycol Recirc. Rat	o: 5.87	gal/lb H2O
Component Carbon Dioxidi	In Dry Gas (%)	51	Absorbed in Glycol ( %)
Hydrogen Sulfide		-	-
Nitroger	99.	99	0.01
Methane	99.	96	0.04
Ethan	99.	89	0.11
i-Butan	99.	54 83	0.16
n-Butan	99.	76	0.24
i-Pentan	99.	72	0.28
n-Pentan	99.	65	0.35
Cyclopentane		-	-
n-Hexan Cyclobexan	99.	-	0.49
n-Heptan	99.	29	0.71
Methylcyclohexan		-	-
2,2,4-Trimethylpentane	<u>a</u>	-	-
Benzene	88.	35	11.65
	83	55	10.77
Ethylbenzen		35	26.65
Ethylbenzen o-Xvlen	73.		
Ethylbenzen o-Xylen m-Xylen	73.	88	20.12
Ethylbenzen o-Xylen m-Xylen p-Xylen	73. 79. 8	88 05	20.12 18.95
Ethylbenzen o-Xylen m-Xylen p-Xylen Triethylene Glyco	73. 79. 81. 0.	55 88 05 02	20.12 18.95 99.98
Ethylbenzen o-Xylen m-Xylen p-Xylen Triethylene Glyco Ethylene Glyco	73. 79. 81.	88 05 02	20.12 18.95 99.98
Ethylbenzen o-Xylen m-Xylen Triethylene Glyco Ethylene Glyco Wate Methaon	73. 79. 81. 0. 1	55 88 05 02 - 11	20.12 18.95 99.98 - 96.89
Ethylbenzen o-Xylen m-Xylen Triethylene Glyco Ethylene Glyco Wate Methano O	2 73. 79. 81. 0. 1 3.	55 88 05 02 - 11 -	20.12 18.95 99.98 - 96.89 -
Ethylbenzen o-Xylen m-Xylen Jriethylene Glyco Ethylene Glyco Wate Methano SO	2 73. 79. 81. 0. 1 7 3.	55 88 05 02 - 11 - -	20.12 18.95 99.98 - 96.89 - -

FLASH TANK			
	Flash Temperature:	160 deg. F	
	Flash Pressure:	45 psig	
Component	Flashed (wt. %)	Left in Glycol (wt. %)	
Carbon Dioxide	77.53	22.47	
Hydrogen Sulfide	0.00	0.00	
Nitrogen	99.05	0.95	
Methane	96.60	3.40	
Ethane	89.58	10.42	
Propane	82.06	17.94	
i-Butane	77.20	22.80	
n-Butane	70.03	29.97	
i-Pentane	59.93	40.07	
n-Pentane	55.73	44.27	
Cyclopentane	0.00	0.00	
n-Hexane	38.00	62.00	
Cyclohexane	0.00	0.00	
n-Heptane	27.58	72.42	
Methylcyclohexane	0.00	0.00	
2,2,4-Trimethylpentane	0.00	0.00	
Benzene	4.94	95.06	
Toluene	2.79	97.21	
Ethylbenzene	1.72	98.28	
o-Xvlene	1 74	98.76	
m-Yylene	1.24	98.33	
n-Vulene	1 78	98.22	
Triethylene Glycol	1.73	100.00	
Ethylene Glycol	0.00	0.00	
Luiyiene Olycol	0.00	99.65	
\\/>ter	0.55	55.05	
Water	0.00	0.00	
Water Methanol	0.00	0.00	
Water Methanol O2 SO2	0.00 0.00 0.00	0.00 0.00 0.00	
Water Methanol O2 SO2 REGENERATOR	0.00 0.00 0.00 Becovered in Glycol (%)	0.00 0.00 0.00	
Water Methanol O2 SO2 REGENERATOR Component Carbon Dioxide	0.00 0.00 0.00 Recovered in Glycol (%)	0.00 0.00 0.00 Distilled Overhead (%) 100.00	
Water Methanol O2 SO2 REGENERATOR Component Carbon Dioxide Hydrogen Sulfide	0.00 0.00 0.00 Recovered in Glycol (%) 0.00	0.00 0.00 0.00 Distilled Overhead (%) 100.00	
Water Methanol O2 SO2 REGENERATOR Component Carbon Dioxide Hydrogen Sulfide Nitrogen	0.00 0.00 0.00 Recovered in Glycol (%) 0.00	0.00 0.00 0.00 Distilled Overhead (%) 100.00	
Water Methanol O2 SO2 REGENERATOR Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane	0.00 0.00 0.00 Recovered in Glycol (%) 0.00 - 0.00 0.00	0.00 0.00 0.00 Distilled Overhead (%) 100.00 - 100.00	
Water Methanol O2 SO2 REGENERATOR Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethano	0.00 0.00 0.00 Recovered in Glycol (%) - - 0.00 0.00 0.00	0.00 0.00 0.00 Distilled Overhead (%) 100.00 - 100.00 100.00 100.00	
Water Methanol O2 SO2 REGENERATOR Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Ethane	0.00 0.00 0.00 Recovered in Glycol (%) 0.00 - 0.00 0.00 0.00 0.00	0.00 0.00 0.00 Distilled Overhead (%) 100.00 100.00 100.00 100.00	
Water Methanol O2 SO2 REGENERATOR Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i.P.ttop	0.00 0.00 0.00 Recovered in Glycol (%) - - 0.00 0.00 0.00 0.00 0.00	0.00 0.00 0.00 Distilled Overhead (%) 100.00 100.00 100.00 100.00 100.00 100.00	
Water Methanol O2 SO2 REGENERATOR Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane propane	0.00 0.00 0.00 Recovered in Glycol (%) - 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	0.00 0.00 0.00 Distilled Overhead (%) 100.00 - 100.00 100.00 100.00 100.00 100.00 100.00	
Water Methanol O2 SO2 REGENERATOR Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Butane	0.00 0.00 0.00 Recovered in Glycol (%) 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00	0.00 0.00 0.00 Distilled Overhead (%) - 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00	
Water Methanol 02 SO2 REGENERATOR Component Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfide Nitrogen Methane Ethane Fropane i-Butane n-Butane i-Pentane	0.00 0.00 0.00 Recovered in Glycol (%) 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00	0.00 0.00 0.00 Distilled Overhead (%) 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00	
Water Methanol O2 SO2 REGENERATOR Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Curbonotane	0.00 0.00 0.00 Recovered in Glycol (%) 0.00 - 0.00 0.00 0.00 0.00 0.00 0.00 0	0.00 0.00 0.00 Distilled Overhead (%) 100.00 100.	
Water Methanol O2 SO2 REGENERATOR Component Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfid	0.00 0.00 0.00 Recovered in Glycol (%) - 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00	0.00 0.00 0.00 Distilled Overhead (%) 100.00 - 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 - - - - - - - - - - - - -	
Water Methanol O2 SO2 REGENERATOR Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane	0.00 0.00 0.00 Recovered in Glycol (%) - 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00	0.00 0.00 0.00 Distilled Overhead (%) 100.00 - 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 - 100.00 - 100.00 - - - - - - - - - - - - -	
Water Methanol 02 SO2 REGENERATOR Component Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfide Nitrogen Methane Ethane Fropane i-Butane n-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclopentane	0.00 0.00 0.00 Recovered in Glycol (%) 0.00	0.00 0.00 0.00 Distilled Overhead (%) 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00	
Water Methanol O2 SO2 REGENERATOR Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Butane i-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclohexane n-Hexane	0.00 0.00 0.00 Recovered in Glycol (%) 0.00	0.00 0.00 0.00 Distilled Overhead (%) 100.00 - 100.00 100.00 100.00 100.00 100.00 100.00 - 100.00 - 100.00 - 100.00 - 100.00 - - - - - - - - - - - - -	
Water Methanol O2 SO2 REGENERATOR Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Pentane n-Butane i-Pentane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane	0.00 0.00 0.00 Recovered in Glycol (%) - 0.00 0.	0.00 0.00 0.00 Distilled Overhead (%) 100.00 - 100.00 100.00 100.00 100.00 100.00 100.00 - - 100.00 - - - 100.00 - - - - - - - - - - - - -	
Water Methanol O2 SO2 REGENERATOR Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Pentane n-Pentane n-Pentane n-Pentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane	0.00 0.00 0.00 Recovered in Glycol (%) 0.00	0.00 0.00 0.00 Distilled Overhead (%) 100.00 - 100.00 100.00 100.00 100.00 100.00 100.00 100.00 - 100.00 - 100.00 - - - 0.00 - - - - - - - - - - - - -	
Water Methanol 02 SO2 REGENERATOR Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane Nethylcyclohexane 2,2,4-Trimethylpentane Benzene	0.00 0.00 0.00 Recovered in Glycol (%) 0.00	0.00 0.00 0.00 Distilled Overhead (%) - 100.00 100.00 100.00 100.00 100.00 100.00 100.00 - 100.00 - - - - - - - - - - - - -	
Water Methanol O2 SO2 REGENERATOR Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Butane n-Butane i-Pentane n-Pentane n-Pentane Cyclopentane n-Hexane Cyclohexane n-Hexane S2,2,4-Trimethylpentane Benzene Toluene	0.00 0.00 0.00 Recovered in Glycol (%) 0.00	0.00 0.00 0.00 0.00 0.00 0.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 - - 100.00 - - - - - - - - - - - - -	
Water Methanol O2 SO2 REGENERATOR Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Butane i-Butane i-Butane i-Pentane n-Butane i-Pentane n-Pentane Cyclopexane n-Hexane Cyclohexane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene	0.00 0.00 0.00 Recovered in Glycol (%) - 0.00 0.	0.00 0.00 0.00 0.00 Distilled Overhead (%) 100.00 0.00 100.00 0.	
Water Methanol O2 SO2 REGENERATOR Component Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfide Sulfide Hydrogen Sulfide Sulfide Hydrogen Sulfide Sulfide Hydrogen Sulfide Sulfide Hydrogen Sulfide Sulfide Hydrogen Sulfide Sulfide Hydrogen Sulfide Sulfide Hydrogen Sulfide Sulfide Hydrogen Sulfide Sulfide Hydrogen Sulfide Sulfide Sulfide Hydrogen Sulfide Sulfide Sulfide Hydrogen Sulfide Sulfide Sulfide Hydrogen Sulfide Sulfi	0.00 0.00 0.00 Recovered in Glycol (%) - 0.00 0.	0.00 0.00 0.00 0.00 Distilled Overhead (%) - 100.00 100.00 100.00 100.00 100.00 100.00 100.00 - - - - - - - - - - - - -	
Water Methanol 02 SO2 REGENERATOR Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Ethane Propane i-Butane n-Butane n-Butane n-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopexane n-Hexane Cyclopexane n-Hexane Cyclopexane n-Hexane Cyclopexane n-Hexane Cyclopexane n-Hexane Cyclopexane n-Hexane Ethylbenzene o-Xylene m-Xylene	0.00 0.00 0.00 Recovered in Glycol (%) 0.00	0.00 0.00 0.00 0.00 0.00 0.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 - - - - - - - - - - - - -	
Water Methanol O2 SO2 REGENERATOR Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Butane n-Butane i-Pentane n-Pentane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane benzene Toluene Ethylbenzene o-Xylene m-Xylene	0.00 0.00 0.00  Recovered in Glycol (%)  0.00 0	0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 - - - - - - - - - - - - -	
Water Methanol O2 SO2 REGENERATOR Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Butane i-Butane i-Butane i-Butane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclohexane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol	0.00 0.00 0.00 Recovered in Glycol (%) - 0.00 0.33 1.38 4.87 4.40 100.00	0.00 0.00 0.00 0.00 0.00 0.00 10	
Water Methanol 02 SO2 REGENERATOR Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Butane n-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopentane Benzene Toluene Ethylbenzene o-Xylene Triethylene Glycol Ethylene Glycol	0.00 0.00 0.00 Recovered in Glycol (%) 0.00	0.00 0.00 0.00 0.00 0.00 0.00 100.00 0.00	
Water Methanol 02 SO2 REGENERATOR Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Butane n-Butane n-Butane n-Butane n-Hexane Cyclopentane N-Hexane Cyclopentane n-Hexane Cyclohexane n-Hexane Cyclohexane n-Hexane Sulfide Sulfide Nitrogen Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol	0.00 0.00 0.00 Recovered in Glycol (%) 0.00 0.33 1.38 4.66 1.40 1.00 0.00 0.00 0.00 0.00 0.33 1.38 3.58	0.00 0.00 0.00 0.00 0.00 0.00 10	
Water Methanol O2 SO2 REGENERATOR Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Butane n-Butane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclohexane n-Hexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Water	0.00 0.00 0.00 Recovered in Glycol (%) - 0.00 0.33 1.38 4.66 9.10 0.487 4.40 100.00 0.00 0.00 0.33 3.58 -	0.00 0.00 0.00 0.00 0.00 0.00 10	
Water Methanol O2 SO2 REGENERATOR Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Butane i-Butane i-Butane i-Butane i-Butane n-Butane i-Butane i-Butane n-Restane Cyclopentane Cyclopexane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Gyclo Ethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Water Methanol O2	0.00 0.00 0.00 Recovered in Glycol (%) - 0.00 0.33 1.38 4.66 9.10 0.00 0.00 0.33 1.38 3.58 - 3.58 -	0.00 0.00 0.00 0.00 Distilled Overhead (%) 100.00 - - - - - - - - - - - - -	

ET GAS STREAM					
Temperature:	110.00	deg F			
Pressure:	1114.40	psia			
Flow Rate.	24.77	Conc (mo	04)	Mass Flow (lb/b)	
component	Carbon Dioxide	Conc. (mo	0.91	1092.83	
	Hydrogen Sulfide		0.00	0.00	
	Nitrogen		1.64	1246.90	
	Methane		70.89	30926.27	
	Ethane		13.28	10857.42	
	Propane		7.52	9017.17	
	i-Butane		1.01	1601.68	
	n-Butane		2.61	4121.16	
	i-Pentane		0.57	1115.00	
	n-Pentane		0.66	1298.92	
	Cyclopentane		0.00	0.00	
	n-Hexane		0.58	1347.88	
	Cyclohexane		0.00	0.00	
	n-Heptane		0.16	434.54	
	Methylcyclohexane		0.00	0.00	
	2,2,4-Trimethylpentane		0.00	0.00	
	Benzene		0.02	43.73	
	Toluene Ethylhonson		0.01	23.//	
	ctriyibenzene		0.00	0.74	
	u-Ayiene m-Yulono		0.00	1.00	
	n-Xylene		0.00	4.52 0 36	
	Triethylene Glycol		0.00	0.00	
	Ethylene Glycol		0.00	0.00	
	Water		0.15	71.58	
	Methanol		0.00	0.00	
	02		0.00	0.00	
	SO2		0.00	0.00	
	Total Components		100.00	63205.33	
GAS STREAM					
GAS STREAM Temperature:	111.84	deg F			
GAS STREAM Temperature: Pressure:	111.84 1109.40	deg F psia			
GAS STREAM Temperature: Pressure: Flow Rate:	111.84 1109.40 24.71	deg F psia MMSCFD	(0/ <b>)</b>	Mass Flow (Ib /b)	_
GAS STREAM Temperature: Pressure: Flow Rate: Component	111.84 1109.40 24.71	deg F psia MMSCFD Conc. (mo	%)	Mass Flow (lb/h)	
GAS STREAM Temperature: Pressure: Flow Rate: Component	111.84 1109.40 24.71 Carbon Dioxide Hydrogen Sulfide	deg F psia MMSCFD Conc. (mo	%) 0.91 0.00	Mass Flow (lb/h) 1088.53 0.00	
GAS STREAM Temperature: Pressure: Flow Rate: Component	111.84 1109.40 24.71 Carbon Dioxide Hydrogen Sulfide Nitrogen	deg F psia MMSCFD Conc. (mo	%) 0.91 0.00 1.64	Mass Flow (lb/h) 1088.53 0.00 1246.74	
GAS STREAM Temperature: Pressure: Flow Rate: Component	111.84 1109.40 24.71 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane	deg F psia MMSCFD Conc. (mo	%) 0.91 0.00 1.64 71.01	Mass Flow (lb/h) 1088.53 0.00 1246.74 30913.14	
GAS STREAM Temperature: Pressure: Flow Rate: Component	111.84 1109.40 24.71 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane	deg F psia MMSCFD Conc. (mo	%) 0.91 0.00 1.64 71.01 13.29	Mass Flow (lb/h) 1088.53 0.00 1246.74 30913.14 10845.63	
GAS STREAM Temperature: Pressure: Flow Rate: Component	111.84 1109.40 24.71 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane	deg F psia MMSCFD Conc. (mo	%) 0.91 0.00 1.64 71.01 13.29 7.52	Mass Flow (lb/h) 1088.53 0.00 1246.74 30913.14 10845.63 9002.74	
GAS STREAM Temperature: Pressure: Flow Rate: Component	111.84 1109.40 24.71 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane	deg F psia MMSCFD Conc. (mo	%) 0.91 0.00 1.64 71.01 13.29 7.52 1.01	Mass Flow (lb/h) 1088.53 0.00 1246.74 30913.14 10845.63 9002.74 1598.97	
GAS STREAM Temperature: Pressure: Flow Rate: Component	111.84 1109.40 24.71 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane	deg F psia MMSCFD Conc. (mo	%) 0.91 0.00 1.64 71.01 13.29 7.52 1.01 2.61	Mass Flow (lb/h) 1088.53 0.00 1246.74 30913.14 10845.63 9002.74 1598.97 4111.10	
GAS STREAM Temperature: Pressure: Flow Rate: Component	111.84 1109.40 24.71 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane	deg F psia MMSCFD Conc. (mo	%) 0.91 0.00 1.64 71.01 13.29 7.52 1.01 2.61 0.57	Mass Flow (lb/h) 1088.53 0.00 1246.74 30913.14 10845.63 9002.74 1598.97 4111.10 1111.87	
GAS STREAM Temperature: Pressure: Flow Rate: Component	111.84 1109.40 24.71 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane	deg F psia MMSCFD Conc. (mo	%) 0.91 0.00 1.64 71.01 13.29 7.52 1.01 2.61 0.57 0.66	Mass Flow (lb/h) 1088.53 0.00 1246.74 30913.14 10845.63 9002.74 1598.97 4111.10 1111.87 1294.42	
GAS STREAM Temperature: Pressure: Flow Rate: Component	111.84 1109.40 24.71 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane n-Pentane Cyclopentane	deg F psia MMSCFD Conc. (mo	%) 0.91 0.00 1.64 71.01 13.29 7.52 1.01 2.61 0.57 0.66 0.00	Mass Flow (lb/h) 1088.53 0.00 1246.74 30913.14 10845.63 9002.74 1598.97 4111.10 1111.87 1294.42 0.00	
GAS STREAM Temperature: Pressure: Flow Rate: Component	111.84 1109.40 24.71 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane	deg F psia <u>MMSCFD</u> Conc. (mo	%) 0.91 0.00 1.64 71.01 13.29 7.52 1.01 2.61 0.57 0.66 0.00 0.57	Mass Flow (lb/h) 1088.53 0.00 1246.74 30913.14 10845.63 9002.74 1598.97 4111.10 1111.87 1294.42 0.00 1341.32	
GAS STREAM Temperature: Pressure: Flow Rate: Component	111.84 1109.40 24.71 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Butane i-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopentane	deg F psia MMSCFD Conc. (mo	%) 0.91 0.00 1.64 71.01 13.29 7.52 1.01 2.61 0.57 0.66 0.00 0.57 0.00	Mass Flow (lb/h) 1088.53 0.00 1246.74 30913.14 10845.63 9002.74 1598.97 4111.10 1111.87 1294.42 0.00 1341.32 0.00	
GAS STREAM Temperature: Pressure: Flow Rate: Component	111.84 1109.40 24.71 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane Cyclopentane Cyclohexane n-Heptane	deg F psia MMSCFD Conc. (mo	%) 0.91 0.00 1.64 71.01 13.29 7.52 1.01 2.61 0.57 0.66 0.00 0.57 0.00 0.16	Mass Flow (lb/h) 1088.53 0.00 1246.74 30913.14 10845.63 9002.74 1598.97 4111.10 1111.87 1294.42 0.00 1341.32 0.00 431.45	
GAS STREAM Temperature: Pressure: Flow Rate: Component	111.84 1109.40 24.71 Carbon Dioxide Hydrogen Sulfide Nitrogen Ethane Ethane Propane i-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclohexane n-Hetpane	deg F psia MMSCFD Conc. (mo	%) 0.91 0.00 1.64 71.01 13.29 7.52 1.01 2.61 0.57 0.66 0.00 0.57 0.00 0.16 0.00	Mass Flow (lb/h) 1088.53 0.00 1246.74 30913.14 10845.63 9002.74 1598.97 4111.10 1111.87 1294.42 0.00 1341.32 0.00 431.45 0.00	
GAS STREAM Temperature: Pressure: Flow Rate: Component	111.84 1109.40 24.71 Carbon Dioxide Hydrogen Sulfide Nitrogen Ethane Ethane Propane i-Butane n-Butane n-Pentane n-Pentane Cyclopentane n-Hexane Cyclobexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane	deg F psia MMSCFD Conc. (mo	%) 0.91 0.00 1.64 71.01 13.29 7.52 1.01 2.61 0.57 0.66 0.00 0.57 0.06 0.00 0.16 0.00 0.00 0.00	Mass Flow (lb/h) 1088.53 0.00 1246.74 30913.14 10845.63 9002.74 1598.97 4111.10 1111.87 1294.42 0.00 1341.32 0.00 431.45 0.00 0.00	
GAS STREAM Temperature: Pressure: Flow Rate: Component	111.84 1109.40 24.71 Carbon Dioxide Hydrogen Sulfide Nitrogen Ethane Ethane Propane i-Butane n-Butane n-Butane i-Butane n-Pentane Cyclopentane n-Hexane Cyclopexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Eenzene	deg F psia MMSCFD Conc. (mo	%) 0.91 0.00 1.64 71.01 13.29 7.52 1.01 2.61 0.57 0.66 0.00 0.57 0.00 0.16 0.00 0.00 0.02 0.21	Mass Flow (lb/h) 1088.53 0.00 1246.74 30913.14 10845.63 9002.74 1598.97 4111.10 1111.87 1294.42 0.00 1341.32 0.00 431.45 0.00 0.00 38.65 12.02	
GAS STREAM Temperature: Pressure: Flow Rate: Component	111.84 1109.40 24.71 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Butane i-Butane i-Pentane n-Pentane Cyclopentane Cyclopentane Cyclopentane Cyclopentane 2,2,4-Trimethylpentane Benzene Toluene	deg F psia MMSCFD Conc. (mo	%) 0.91 0.00 1.64 71.01 13.29 7.52 1.01 2.61 0.57 0.66 0.00 0.57 0.00 0.16 0.00 0.00 0.00 0.02 0.01 0.02	Mass Flow (lb/h) 1088.53 0.00 1246.74 30913.14 10845.63 9002.74 1598.97 4111.10 1111.87 1294.42 0.00 1341.32 0.00 431.45 0.00 431.45 0.00 38.65 19.83 0.252	
GAS STREAM Temperature: Pressure: Flow Rate: Component	111.84 1109.40 24.71 Carbon Dioxide Hydrogen Sulfide Nitrogen Ethane Ethane n-Butane n-Butane n-Butane n-Pentane Cyclopentane Cyclohexane n-Heytane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene	deg F psia MMSCFD Conc. (mo	%) 0.91 0.00 1.64 71.01 13.29 7.52 1.01 2.61 0.57 0.66 0.00 0.57 0.00 0.16 0.00 0.00 0.02 0.01 0.00 0.02 0.01 0.00 0.02 0.01 0.00 0.02 0.01 0.00 0.02 0.01 0.00 0.02 0.00	Mass Flow (lb/h) 1088.53 0.00 1246.74 30913.14 10845.63 9002.74 1598.97 4111.10 1111.87 1294.42 0.00 1341.32 0.00 431.45 0.00 0.00 38.65 19.83 0.60 0.70	
GAS STREAM Temperature: Pressure: Flow Rate: Component	111.84 1109.40 24.71 Carbon Dioxide Hydrogen Sulfide Nitrogen Ethane Propane i-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopexane n-Hexane Qyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene Toluene Ethylbenzene o-Xylene	deg F psia MMSCFD Conc. (mo	%) 0.91 0.00 1.64 71.01 13.29 7.52 1.01 2.61 0.57 0.66 0.00 0.57 0.00 0.16 0.00	Mass Flow (lb/h) 1088.53 0.00 1246.74 30913.14 10845.63 9002.74 1598.97 4111.10 1111.87 1294.42 0.00 1341.32 0.00 431.45 0.00 0.00 38.65 19.83 0.60 0.79 2.42	
GAS STREAM Temperature: Pressure: Flow Rate: Component	111.84 1109.40 24.71 Carbon Dioxide Hydrogen Sulfide Nitrogen Ethane Propane i-Butane n-Pentane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclohexane Qyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene	deg F psia MMSCFD Conc. (mo	%) 0.91 0.00 1.64 71.01 13.29 7.52 1.01 2.61 0.57 0.66 0.00 0.57 0.66 0.00 0.57 0.00 0.16 0.00	Mass Flow (lb/h) 1088.53 0.00 1246.74 30913.14 10845.63 9002.74 1598.97 4111.10 1111.87 1294.42 0.00 1341.32 0.00 431.45 0.00 0.00 38.65 19.83 0.60 0.79 3.48 0.20	
GAS STREAM  Temperature: Pressure: Flow Rate: Component	111.84 1109.40 24.71 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Butane i-Butane i-Pentane n-Pentane Cyclopentane n-Heytane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene	deg F psia MMSCFD Conc. (mo	%) 0.91 0.00 1.64 71.01 13.29 7.52 1.01 2.61 0.57 0.66 0.00 0.57 0.00 0.16 0.00	Mass Flow (lb/h) 1088.53 0.00 1246.74 30913.14 10845.63 9002.74 1598.97 4111.10 1111.87 1294.42 0.00 1341.32 0.00 431.45 0.00 0.00 38.65 19.83 0.60 0.79 3.48 0.30 0.51	
GAS STREAM  Temperature: Pressure: Flow Rate: Component	111.84 1109.40 24.71 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclopextane n-Hexane Cyclohexane n-Hexane 2,2,4-Trimethylyentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Cyclone Chard	deg F psia MMSCFD Conc. (mo	%) 0.91 0.00 1.64 71.01 13.29 7.52 1.01 2.61 0.57 0.66 0.00 0.57 0.00 0.16 0.00 0.57 0.66 0.00 0.57 0.00 0.00 0.57 0.00	Mass Flow (lb/h) 1088.53 0.00 1246.74 30913.14 10845.63 9002.74 1598.97 4111.10 1111.87 1294.42 0.00 1341.32 0.00 431.45 0.00 38.65 19.83 0.60 0.79 3.48 0.30 0.61 0.20	
GAS STREAM  Temperature: Pressure: Flow Rate: Component	111.84 1109.40 24.71 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Pentane Cyclopextane n-Hexane Cyclohexane n-Hexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol	deg F psia MMSCFD Conc. (mo	%) 0.91 0.00 1.64 71.01 13.29 7.52 1.01 2.61 0.57 0.66 0.00 0.57 0.00 0.16 0.00	Mass Flow (lb/h) 1088.53 0.00 1246.74 30913.14 10845.63 9002.74 1598.97 4111.10 1111.87 1294.42 0.00 1341.32 0.00 431.45 0.00 38.65 19.83 0.60 0.79 3.48 0.30 0.61 0.00 2.20	
GAS STREAM	111.84 1109.40 24.71 Carbon Dioxide Hydrogen Sulfide Nitrogen Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopexane n-Heytane Cyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene Triethylene Glycol Ethylene Glycol	deg F psia MMSCFD Conc. (mo	%) 0.91 0.00 1.64 71.01 13.29 7.52 1.01 2.61 0.57 0.66 0.00 0.57 0.00 0.16 0.00	Mass Flow (lb/h) 1088.53 0.00 1246.74 30913.14 10845.63 9002.74 1598.97 4111.10 1111.87 1294.42 0.00 1341.32 0.00 431.45 0.00 431.45 0.00 0.00 38.65 19.83 0.60 0.79 3.48 0.30 0.61 0.00 3.29 0.00	
GAS STREAM  Temperature: Pressure: Flow Rate: Component	111.84 1109.40 24.71 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Butane i-Pentane n-Pentane Cyclopentane n-Heytane Xylohexane n-Heytane Benzene Toluene Ethylbenzene o-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol	deg F psia MMSCFD Conc. (mo	%) 0.91 0.00 1.64 71.01 13.29 7.52 1.01 2.61 0.57 0.66 0.00 0.57 0.66 0.00 0.57 0.00 0.16 0.00	Mass Flow (lb/h) 1088.53 0.00 1246.74 30913.14 10845.63 9002.74 1598.97 4111.10 1111.87 1294.42 0.00 1341.32 0.00 431.45 0.00 431.45 0.00 0.00 38.65 19.83 0.60 0.79 3.48 0.30 0.61 0.00 3.29 0.00	
'GAS STREAM Temperature: Pressure: Flow Rate: Component	111.84 1109.40 24.71 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Butane i-Pentane n-Butane Cyclopentane n-Heytane Cyclopentane n-Heytane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene cyklpen m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol Xater Methanol OZ	deg F psia MMSCFD Conc. (mo	%) 0.91 0.00 1.64 71.01 13.29 7.52 1.01 2.61 0.57 0.66 0.00 0.57 0.00 0.16 0.00	Mass Flow (lb/h) 1088.53 0.00 1246.74 30913.14 10845.63 9002.74 1598.97 4111.10 1111.87 1294.42 0.00 1341.32 0.00 431.45 0.00 431.45 0.00 0.00 38.65 19.83 0.60 0.79 3.48 0.30 0.61 0.00 3.29 0.00 0.00 0.00 0.00	
GAS STREAM Temperature: Pressure: Flow Rate: Component	111.84 1109.40 24.71 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Pentane n-Pentane n-Pentane Cyclopentane Cyclopentane Cyclopentane Cyclopentane Cyclohexane n-Heytane MethylcyCohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene Triethylene Glycol Ethylene Glycol Water Methanol O2 S02	deg F psia MMSCFD Conc. (mo	%) 0.91 0.00 1.64 71.01 13.29 7.52 1.01 2.61 0.57 0.66 0.00 0.57 0.00 0.57 0.00 0.16 0.00	Mass Flow (lb/h) 1088.53 0.00 1246.74 30913.14 10845.63 9002.74 1598.97 4111.10 1111.87 1294.42 0.00 1341.32 0.00 431.45 0.00 431.45 0.00 0.00 38.65 19.83 0.60 0.79 3.48 0.30 0.61 0.00 3.29 0.00 0.00 0.00	
Y GAS STREAM Temperature: Pressure: Flow Rate: Component	111.84 1109.40 24.71 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane N-Pentane Cyclopentane Cyclopentane N-Heptane N-Heptane Nethylçvçlohexane 2,2,4-Trimethylçohexane Ethylbenzene O-Xylene m-Xylene p-Xylene Triethylene Giycol Ethylene Giycol Ethylene Giycol Ethylene Giycol Ethylene Giycol Store Nethanol O2 SO2	deg F psia MMSCFD Conc. (mo	%) 0.91 0.00 1.64 71.01 13.29 7.52 1.01 2.61 0.57 0.66 0.00 0.57 0.00 0.57 0.00 0.16 0.00	Mass Flow (lb/h) 1088.53 0.00 1246.74 30913.14 10845.63 9002.74 1598.97 4111.10 1111.87 1294.42 0.00 1341.32 0.00 431.45 0.00 431.45 0.00 0.00 38.65 19.83 0.60 0.79 3.48 0.30 0.61 0.00 3.29 0.00	

Temperature: Pressure: Flow Rate:	120.00 de			
Pressure: Flow Rate:		g F		
Flow Rate:	1119.40 ps	ia		
	7.00 sg	pm		
Component		Conc. (wt%)	Mass Flow (lb/h)	_
	Carbon Dioxide	0.00	0.00	
	Hydrogen Sulfide	0.00	0.00	
	Nitrogen	0.00	0.00	
	Methane	0.00	0.00	
	Ethane	0.00	0.00	
	Propane	0.00	0.00	
	i-Butane	0.00	0.00	
	n-Butane	0.00	0.00	
	i-Pentane	0.00	0.00	
	n-Pentane	0.00	0.00	
	Cyclopentane	0.00	0.00	
	n-Hexane	0.00	0.00	
	Cyclohexane	0.00	0.00	
	n-Heptane	0.00	0.00	
	Methylcyclohexane	0.00	0.00	
	2,2,4-Trimethylpentane	0.00	0.00	
	Benzene	0.00	0.02	
	Toluene	0.00	0.05	
	Ethylbenzene	0.00	0.01	
	o-Xylene	0.00	0.03	
	m-Xvlene	0.00	0.04	
	p-Xvlene	0.00	0.00	
	Triethvlene Glycol	99.13	3916.43	
	Ethylene Glycol	0.00	0.00	
	Water	0.87	34 34	
	Methanol	0.00	0.00	
		0.00	0.00	
	502	0.00	0.00	
	502	0.00	0.00	
Temperature: Pressure:	111.57 de 1114.40 psi	g F ia		
Flow Rate:	7.49 sg			
Company		pm		
Component		pm Conc. (wt%)	Mass Flow (lb/h)	
Component	Carbon Dioxide	pm Conc. (wt%) 0.11	Mass Flow (lb/h) 4.35	
Component	Carbon Dioxide Hydrogen Sulfide	pm Conc. (wt%) 0.11 0.00	Mass Flow (lb/h) 4.35 0.00	
Component	Carbon Dioxide Hydrogen Sulfide Nitrogen	pm Conc. (wt%) 0.11 0.00 0.01	Mass Flow (lb/h) 4.35 0.00 0.21	
Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane	pm Conc. (wt%) 0.11 0.00 0.01 0.35	Mass Flow (lb/h) 4.35 0.00 0.21 14.53	
Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane	pm Conc. (wt%) 0.11 0.00 0.01 0.35 0.30	Mass Flow (lb/h) 4.35 0.00 0.21 14.53 12.28	
Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane	pm Conc. (wt%) 0.11 0.00 0.01 0.35 0.30 0.36	Mass Flow (lb/h) 4.35 0.00 0.21 14.53 12.28 14.83	
Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane	pm Conc. (wt%) 0.11 0.00 0.01 0.35 0.30 0.36 0.07	Mass Flow (lb/h) 4.35 0.00 0.21 14.53 12.28 14.83 2.79	
Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane	pm Conc. (wt%) 0.11 0.00 0.01 0.35 0.30 0.36 0.07 0.25	Mass Flow (lb/h) 4.35 0.00 0.21 14.53 12.28 14.83 2.79 10.25	
Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Ethane Propane i-Butane n-Butane i-Pentane	pm Conc. (wt%) 0.11 0.00 0.01 0.35 0.30 0.36 0.07 0.25 0.08	Mass Flow (lb/h) 4.35 0.00 0.21 14.53 12.28 14.83 2.79 10.25 3.18	
Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane	pm Conc. (wt%) 0.11 0.00 0.01 0.35 0.35 0.30 0.36 0.07 0.25 0.08 0.11	Mass Flow (lb/h) 4.35 0.00 0.21 14.53 12.28 14.83 2.79 10.25 3.18 4.56	
Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane	pm Conc. (wt%) 0.11 0.00 0.01 0.35 0.30 0.36 0.07 0.25 0.08 0.11 0.00	Mass Flow (lb/h) 4.35 0.00 0.21 14.53 12.28 14.83 2.79 10.25 3.18 4.56 0.00	
Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane	pm Conc. (wt%) 0.11 0.00 0.01 0.35 0.30 0.36 0.07 0.25 0.08 0.11 0.11 0.00 0.16	Mass Flow (lb/h) 4.35 0.00 0.21 14.53 12.28 14.83 2.79 10.25 3.18 4.56 0.00 6.62	
Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclohexane	pm Conc. (wt%) 0.11 0.00 0.35 0.30 0.36 0.07 0.25 0.08 0.11 0.00 0.16 0.00	Mass Flow (lb/h) 4.35 0.00 0.21 14.53 12.28 14.83 2.79 10.25 3.18 4.56 0.00 6.62 0.00	
Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane Cyclohexane n-Hexane	pm Conc. (wt%) 0.11 0.00 0.01 0.35 0.30 0.36 0.07 0.25 0.08 0.11 0.00 0.16 0.00 0.08	Mass Flow (lb/h) 4.35 0.00 0.21 14.53 12.28 14.83 2.79 10.25 3.18 4.56 0.00 6.62 0.00 3.11	
Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Pentane n-Butane i-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane	pm Conc. (wt%) 0.11 0.00 0.01 0.35 0.30 0.36 0.07 0.25 0.08 0.11 0.00 0.16 0.00 0.08 0.00	Mass Flow (lb/h) 4.35 0.00 0.21 14.53 12.28 14.83 2.79 10.25 3.18 4.56 0.00 6.62 0.00 6.62 0.00 3.11 0.00	
Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Ethane Ethane Propane i-Butane n-Butane i-Pentane Cyclopentane Cyclopentane n-Hexane Cyclohexane n-Heytane Methylcyclohexane 2,2,4-Trimethylpentane	pm Conc. (wt%) 0.11 0.00 0.01 0.35 0.30 0.36 0.07 0.25 0.08 0.11 0.00 0.16 0.00 0.16 0.00 0.08 0.00	Mass Flow (lb/h) 4.35 0.00 0.21 14.53 12.28 14.83 2.79 10.25 3.18 4.56 0.00 6.62 0.00 6.62 0.00 3.11 0.00 0.00	
Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Ethane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene	pm Conc. (wt%) 0.11 0.00 0.01 0.35 0.30 0.36 0.07 0.25 0.08 0.11 0.00 0.16 0.00 0.16 0.00 0.08 0.00 0.08 0.00 0.08 0.00 0.02 0.00 0.02 0.00 0.02 0.00 0.02 0.02 0.00 0.02 0.00 0.02 0.00 0.02 0.00 0.02 0.00 0.02 0.00 0.02 0.00 0.02 0.00 0.02 0.00 0.02 0.00 0.02 0.00 0.02 0.00 0.02 0.000 0.00	Mass Flow (lb/h) 4.35 0.00 0.21 14.53 12.28 14.83 2.79 10.25 3.18 4.56 0.00 6.62 0.00 6.62 0.00 3.11 0.00 0.00 0.00 0.00 0.00 0.00	
Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene	pm Conc. (wt%) 0.11 0.00 0.01 0.35 0.30 0.36 0.07 0.25 0.88 0.11 0.00 0.16 0.00 0.08 0.00 0.08 0.00 0.00 0.00 0.01 0.11 0.10 0.11 0.11 0.00 0.11 0.35 0.30 0.36 0.37 0.36 0.37 0.36 0.37 0.36 0.37 0.36 0.37 0.36 0.37 0.36 0.37 0.36 0.37 0.36 0.37 0.36 0.37 0.36 0.37 0.36 0.07 0.25 0.08 0.11 0.08 0.00 0.11 0.08 0.00 0.11 0.08 0.00 0.11 0.08 0.00 0.11 0.08 0.00 0.11 0.08 0.00 0.11 0.08 0.00 0.11 0.00 0.12 0.00 0.11 0.00 0.12 0.00 0.11 0.00 0.12 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.01 0.00 0.11 0.00 0.01 0.00 0.01 0.00 0.01 0.00 0.01 0.00 0.01 0.00 0.01 0.000 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.12 0.10	Mass Flow (lb/h) 4.35 0.00 0.21 14.53 12.28 14.83 2.79 10.25 3.18 4.56 0.00 6.62 0.00 3.11 0.00 3.11 0.00 0.00 5.10 4.00	
Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Pentane n-Butane i-Pentane Cyclopentane Cyclopexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene	pm Conc. (wt%) 0.11 0.00 0.01 0.35 0.30 0.36 0.07 0.25 0.08 0.11 0.00 0.16 0.00 0.16 0.00 0.08 0.00 0.08 0.00 0.00 0.12 0.10 0.00	Mass Flow (lb/h) 4.35 0.00 0.21 14.53 12.28 14.83 2.79 10.25 3.18 4.56 0.00 6.62 0.00 6.62 0.00 3.11 0.00 0.00 0.00 5.10 4.00 0.15	
Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane Cyclopentane n-Hexane Cyclohexane n-Heytane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene	pm Conc. (wt%) 0.11 0.00 0.01 0.35 0.30 0.36 0.07 0.25 0.08 0.11 0.00 0.16 0.00 0.16 0.00 0.08 0.00 0.00 0.12 0.10 0.00 0.01	Mass Flow (lb/h) 4.35 0.00 0.21 14.53 12.28 14.83 2.79 10.25 3.18 4.56 0.00 6.62 0.00 6.62 0.00 3.11 0.00 0.00 5.10 4.00 0.15 0.29	
Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Heytane Cyclohexane n-Heytane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene	pm Conc. (wt%) 0.11 0.00 0.01 0.35 0.30 0.36 0.07 0.25 0.08 0.11 0.00 0.16 0.00 0.16 0.00 0.08 0.00 0.00 0.00 0.12 0.10 0.00 0.00 0.01 0.00 0.00 0.01 0.00 0.01 0.02 0.01 0.01 0.01 0.00 0.01 0.01 0.00 0.01 0.01 0.00 0.01 0.01 0.00 0.01 0.00 0.01 0.00 0.01 0.00 0.01 0.35 0.30 0.07 0.25 0.08 0.11 0.07 0.25 0.08 0.11 0.00 0.07 0.25 0.00 0.11 0.00 0.07 0.12 0.00 0.00 0.00 0.00 0.11 0.00 0.07 0.25 0.00 0.11 0.00 0.00 0.11 0.00 0.11 0.00 0.01 0.00 0.11 0.00 0.01 0.01 0.00 0.11 0.00 0.00 0.11 0.00 0.00 0.11 0.00 0	Mass Flow (lb/h) 4.35 0.00 0.21 14.53 12.28 14.83 2.79 10.25 3.18 4.56 0.00 6.62 0.00 6.62 0.00 3.11 0.00 6.62 0.00 3.11 0.00 5.10 4.00 0.01 5.10 4.00 0.15 0.29 0.88	
Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene p-Xylene p-Xylene	pm Conc. (wt%) 0.11 0.00 0.01 0.35 0.30 0.36 0.07 0.25 0.08 0.11 0.00 0.16 0.00 0.00 0.00 0.00 0.12 0.10 0.00 0.01 0.00 0.00 0.00 0.00 0.01 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.35 0.30 0.36 0.07 0.25 0.08 0.00 0.01 0.08 0.00 0.01 0.08 0.00 0.00 0.01 0.08 0.00 0.00 0.01 0.08 0.00 0.00 0.01 0.08 0.00 0.00 0.00 0.01 0.05 0.07 0.25 0.08 0.00 0.00 0.00 0.00 0.01 0.00 0.01 0.02 0.00 0	Mass Flow (lb/h) 4.35 0.00 0.21 14.53 12.28 14.83 2.79 10.25 3.18 4.56 0.00 6.62 0.00 3.11 0.00 3.11 0.00 0.00 5.10 4.00 0.15 0.29 0.88 0.07	
Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Ethane Ethane Propane i-Butane n-Butane i-Pentane Cyclopentane n-Hexane Cyclopentane n-Heytane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Giyclo	pm Conc. (wt%) 0.11 0.00 0.01 0.35 0.30 0.36 0.07 0.25 0.08 0.11 0.00 0.16 0.00 0.16 0.00 0.08 0.00 0.08 0.00 0.12 0.10 0.00 0.12 0.10 0.00 0.01 0.00 0.05 0.01 0.07 0.25 0.00 0.11 0.00 0.35 0.07 0.25 0.00 0.11 0.00 0.11 0.30 0.36 0.07 0.25 0.00 0.11 0.07 0.25 0.00 0.11 0.00 0.15 0.07 0.15 0.00 0.11 0.00 0.15 0.07 0.11 0.00 0.15 0.00 0.11 0.00 0.15 0.00 0.11 0.00 0.15 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.00 0.00 0.01 0.00 0	Mass Flow (lb/h) 4.35 0.00 0.21 14.53 12.28 14.83 2.79 10.25 3.18 4.56 0.00 6.62 0.00 6.62 0.00 3.11 0.00 0.00 5.10 4.00 0.15 0.29 0.88 0.07 3915.82	
Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclohexane n-Heytane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Gycol Ethylene Glycol	pm Conc. (wt%) 0.11 0.00 0.01 0.35 0.30 0.36 0.07 0.25 0.08 0.11 0.00 0.16 0.00 0.16 0.00 0.16 0.00 0.12 0.10 0.00 0.00 0.12 0.10 0.00 0.00 0.01 0.00 0.01 0.00 0.11 0.25 0.00 0.11 0.25 0.00 0.11 0.25 0.00 0.11 0.25 0.00 0.11 0.25 0.00 0.11 0.25 0.00 0.11 0.25 0.00 0.11 0.25 0.00 0.11 0.07 0.25 0.08 0.00 0.11 0.00 0.12 0.00 0.00 0.00 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.00 0.12 0.00 0	Mass Flow (lb/h) 4.35 0.00 0.21 14.53 12.28 14.83 2.79 10.25 3.18 4.56 0.00 6.62 0.00 6.62 0.00 3.11 0.00 0.00 5.10 4.00 0.15 0.29 0.88 0.07 3915.82 0.00	
Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Ethane Ethane Propane i-Butane i-Pentane n-Pentane n-Pentane Cyclopentane n-Heytane Cyclohexane n-Heytane Qyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Gycol Ethylene Glycol Water	pm Conc. (wt%) 0.11 0.00 0.01 0.35 0.30 0.36 0.07 0.25 0.88 0.11 0.00 0.16 0.00 0.08 0.00 0.00 0.00 0.12 0.10 0.00 0.12 0.10 0.00 0.12 0.10 0.00 0.25 0.25 0.00 0.25 0.00 0.00 0.00 0.00 0.00 0.00 0.01 0.35 0.30 0.36 0.07 0.25 0.88 0.00 0.00 0.11 0.00 0.11 0.00 0.11 0.35 0.30 0.36 0.07 0.25 0.08 0.08 0.00 0.11 0.00 0.08 0.00 0.00 0.00 0.11 0.00 0.08 0.00 0.00 0.00 0.11 0.00 0.00 0.01 0.00 0.02 0.00 0	Mass Flow (lb/h) 4.35 0.00 0.21 14.53 12.28 14.83 2.79 10.25 3.18 4.56 0.00 6.62 0.00 3.11 0.00 6.62 0.00 3.11 0.00 0.00 5.10 4.00 0.01 5.10 4.00 0.05 0.29 0.88 0.07 3915.82 0.00 102.64	
Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol	pm Conc. (wt%) 0.11 0.00 0.01 0.35 0.30 0.36 0.07 0.25 0.08 0.11 0.00 0.16 0.00 0.00 0.00 0.00 0.12 0.10 0.00 0.12 0.10 0.00 0.12 0.10 0.00 0.01 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.01 0.00 0.01 0.00 0.00 0.01 0.00 0.00 0.01 0.00 0.05 0.07 0.25 0.08 0.00 0	Mass Flow (lb/h) 4.35 0.00 0.21 14.53 12.28 14.83 2.79 10.25 3.18 4.56 0.00 6.62 0.00 6.62 0.00 3.11 0.00 0.00 5.10 4.00 0.15 0.29 0.88 0.07 3915.82 0.00 102.64 0.00	
Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclohexane n-Heytane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol Water Methanol O2	pm Conc. (wt%) 0.11 0.00 0.01 0.35 0.30 0.36 0.07 0.25 0.08 0.11 0.00 0.16 0.00 0.16 0.00 0.08 0.00 0.00 0.10 0.00 0.10 0.00 0.10 0.00 0.10 0.00 0.25 0.00 0.00 0.00 0.00 0.11 0.25 0.00 0.11 0.00 0.36 0.07 0.25 0.00 0.11 0.07 0.25 0.00 0.11 0.00 0.15 0.07 0.25 0.00 0.11 0.00 0.15 0.07 0.11 0.00 0.15 0.07 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0	Mass Flow (lb/h) 4.35 0.00 0.21 14.53 12.28 14.83 2.79 10.25 3.18 4.56 0.00 6.62 0.00 6.62 0.00 3.11 0.00 0.00 5.10 4.00 0.15 0.29 0.88 0.07 3915.82 0.00 102.64 0.00 102.64 0.00	
Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane i-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclohexane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Gyclone Ethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol O2 SO2	pm Conc. (wt%) 0.11 0.00 0.01 0.35 0.30 0.36 0.07 0.25 0.08 0.11 0.00 0.16 0.00 0.16 0.00 0.16 0.00 0.00 0.12 0.10 0.00 0.00 0.00 0.01 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.25 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.11 0.00 0.36 0.07 0.25 0.08 0.00 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.11 0.00 0.15 0.00 0	Mass Flow (lb/h) 4.35 0.00 0.21 14.53 12.28 14.83 2.79 10.25 3.18 4.56 0.00 6.62 0.00 6.62 0.00 3.11 0.00 0.00 5.10 4.00 0.15 0.29 0.88 0.07 3915.82 0.00 102.64 0.00 0.0	
Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Pentane n-Pentane n-Pentane Cyclopentane n-Heytane Cyclohexane n-Heytane Z,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Griethylene Glycol Ethylene Glycol Water Methanol O2 SO2	pm Conc. (wt%) 0.11 0.00 0.01 0.35 0.30 0.36 0.07 0.25 0.08 0.11 0.00 0.16 0.00 0.00 0.00 0.12 0.10 0.00 0.12 0.10 0.00 0.12 0.10 0.00 0.25 0.00 0	Mass Flow (lb/h) 4.35 0.00 0.21 14.53 12.28 14.83 2.79 10.25 3.18 4.56 0.00 6.62 0.00 6.62 0.00 3.11 0.00 0.00 5.10 4.00 0.01 5.10 4.00 0.05 0.29 0.88 0.07 3915.82 0.00 102.64 0.00 0.02 0.00 0.0	

Temperature:	160.00	deg F			
Pressure:	59.40	psia			
Flow Rate:	715.52	scfh			
Component		Conc. (mol%)		Mass Flow (lb/h)	
	Carbon Dioxide		4.07	3.38	
	Hydrogen Sulfide		0.00	0.00	
	Nitrogen		0.40	0.21	
	Methane		46.39	14.03	
	Ethane		19.40	11.00	
	Propane		14.64	12.17	
	i-Butane		1.96	2.15	
	n-Butane		0.55	/.18	
	I-Pentane		1.40	1.91	
	n-Pentane		1.87	2.54	
	Cyclopentane		0.00	0.00	
	п-нехапе		1.55	2.52	
	Cyclonexane		0.00	0.00	
	n-Heptane		0.45	0.86	
	Nietnyicycionexane		0.00	0.00	
	2,2,4-irimetnyipentane		0.00	0.00	
	Benzene		0.17	0.25	
	Thulbass		0.06	0.11	
	Etnyibenzene		0.00	0.00	
	o-xylene		0.00	0.00	
	m-xylene		0.01	0.01	
	p-xylene Triethylong Church		0.00	0.00	
	Ethylong Church		0.00	0.00	
	Ethylene Glycol		1.00	0.00	
	Vvaler		1.07	0.30	
	Methanol		0.00	0.00	
	02		0.00	0.00	
	iotal components		100.00		
SH TANK GLYCOL STREAM Temperature:	160.00	deg F	100.00		
SH TANK GLYCOL STREAM Temperature: Pressure:	160.00 59.40	deg F psia			
SH TANK GLYCOL STREAM Temperature: Pressure: Flow Rate:	160.00 59.40 7.22	deg F psia sgpm			
SH TANK GLYCOL STREAM Temperature: Pressure: Flow Rate: Component	160.00 59.40 7.22	deg F psia sgpm Conc. (wt%)		Mass Flow (lb/h)	
SH TANK GLYCOL STREAM Temperature: Pressure: Flow Rate: Component	160.00 59.40 7.22 Carbon Dioxide	deg F psia sgpm Conc. (wt%)	0.02	Mass Flow (lb/h) 0.98	
SH TANK GLYCOL STREAM Temperature: Pressure: Flow Rate: Component	160.00 59.40 7.22 Carbon Dioxide Hydrogen Sulfide	deg F psia sgpm Conc. (wt%)	0.02	Mass Flow (lb/h) 0.98 0.00	
SH TANK GLYCOL STREAM Temperature: Pressure: Flow Rate: Component	160.00 59.40 7.22 Carbon Dioxide Hydrogen Sulfide Nitrogen	deg F psia sgpm Conc. (wt%)	0.02 0.00 0.00	Mass Flow (lb/h) 0.98 0.00 0.00	
SH TANK GLYCOL STREAM Temperature: Pressure: Flow Rate: Component	160.00 59.40 7.22 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane	deg F psia sgpm Conc. (wt%)	0.02 0.00 0.00 0.00 0.01	Mass Flow (lb/h) 0.98 0.00 0.00 0.49	
SH TANK GLYCOL STREAM Temperature: Pressure: Flow Rate: Component	160.00 59.40 7.22 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane	deg F psia sgpm Conc. (wt%)	0.02 0.00 0.00 0.01 0.03	Mass Flow (lb/h) 0.98 0.00 0.00 0.49 1.28	
SH TANK GLYCOL STREAM Temperature: Pressure: Flow Rate: Component	160.00 59.40 7.22 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane	deg F psia sgpm Conc. (wt%)	0.02 0.00 0.00 0.01 0.03 0.07	Mass Flow (lb/h) 0.98 0.00 0.00 0.49 1.28 2.66	
SH TANK GLYCOL STREAM Temperature: Pressure: Flow Rate: Component	160.00 59.40 7.22 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane	deg F psia sgpm Conc. (wt%)	0.02 0.00 0.00 0.01 0.03 0.07 0.02	Mass Flow (lb/h) 0.98 0.00 0.00 0.49 1.28 2.66 0.64	
SH TANK GLYCOL STREAM Temperature: Pressure: Flow Rate: Component	160.00 59.40 7.22 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane	deg F psia sgpm Conc. (wt%)	0.02 0.00 0.00 0.01 0.03 0.07 0.02 0.08	Mass Flow (lb/h) 0.98 0.00 0.00 0.49 1.28 2.66 0.64 3.07	
SH TANK GLYCOL STREAM Temperature: Pressure: Flow Rate: Component	160.00 59.40 7.22 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Putane	deg F psia sgpm Conc. (wt%)	0.02 0.00 0.00 0.01 0.03 0.07 0.02 0.08 0.03	Mass Flow (lb/h) 0.98 0.00 0.00 0.49 1.28 2.66 0.64 3.07 1.28	
SH TANK GLYCOL STREAM Temperature: Pressure: Flow Rate: Component	160.00 59.40 7.22 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane	deg F psia sgpm Conc. (wt%)	0.02 0.00 0.00 0.01 0.03 0.07 0.02 0.08 0.03 0.05	Mass Flow (lb/h) 0.98 0.00 0.00 0.49 1.28 2.66 0.64 3.07 1.28 2.02	
SH TANK GLYCOL STREAM Temperature: Pressure: Flow Rate: Component	160.00 59.40 7.22 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane n-Pentane Cyclopentane	deg F psia sgpm Conc. (wt%)	0.02 0.00 0.00 0.01 0.03 0.07 0.02 0.08 0.03 0.05 0.00	Mass Flow (lb/h) 0.98 0.00 0.00 0.49 1.28 2.66 0.64 3.07 1.28 2.02 0.00	
SH TANK GLYCOL STREAM Temperature: Pressure: Flow Rate: Component	160.00 59.40 7.22 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Hexane	deg F psia sgpm Conc. (wt%)	0.02 0.00 0.00 0.01 0.03 0.07 0.02 0.08 0.03 0.05 0.00 0.10	Mass Flow (lb/h) 0.98 0.00 0.00 0.49 1.28 2.66 0.64 3.07 1.28 2.02 0.00 4.10	
SH TANK GLYCOL STREAM Temperature: Pressure: Flow Rate: Component	160.00 59.40 7.22 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopentane	deg F psia sgpm Conc. (wt%)	0.02 0.00 0.00 0.01 0.03 0.07 0.02 0.08 0.03 0.05 0.00 0.10 0.00 0.10	Mass Flow (lb/h) 0.98 0.00 0.00 0.49 1.28 2.66 0.64 3.07 1.28 2.02 0.00 4.10 0.00	
SH TANK GLYCOL STREAM Temperature: Pressure: Flow Rate: Component	160.00 59.40 7.22 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane Cyclopentane n-Hexane Cyclohexane n-Heytane	deg F psia sgpm Conc. (wt%)	0.02 0.00 0.00 0.01 0.03 0.07 0.02 0.08 0.03 0.05 0.00 0.10 0.00 0.00 0.00 0.06 0.05	Mass Flow (lb/h) 0.98 0.00 0.00 0.49 1.28 2.66 0.64 3.07 1.28 2.02 0.00 4.10 0.00 2.25 0.00	
SH TANK GLYCOL STREAM Temperature: Pressure: Flow Rate: Component	160.00 59.40 7.22 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Ethane i-Putane n-Butane n-Butane i-Putane n-Butane cyclopentane n-Hexane Cyclopexane N-Hexane Cyclohexane	deg F psia sgpm Conc. (wt%)	0.02 0.00 0.00 0.01 0.03 0.07 0.02 0.08 0.03 0.05 0.00 0.00 0.06 0.00 0.06 0.00	Mass Flow (lb/h) 0.98 0.00 0.00 0.49 1.28 2.66 0.64 3.07 1.28 2.02 0.00 4.10 0.00 4.10 0.00 2.25 0.00 0.00	
SH TANK GLYCOL STREAM Temperature: Pressure: Flow Rate: Component	160.00 59.40 7.22 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane Cyclopentane n-Hexane Cyclohexane 2,2,4-Trimethylpentane	deg F psia sgpm Conc. (wt%)	0.02 0.00 0.00 0.01 0.03 0.07 0.02 0.08 0.03 0.05 0.00 0.10 0.00 0.06 0.00 0.00 0.00	Mass Flow (lb/h)  0.98 0.00 0.00 0.49 1.28 2.66 0.64 3.07 1.28 2.02 0.00 4.10 0.00 2.25 0.00 0.00 0.00 0.00 1.00 0.00 0.00 0.0	
SH TANK GLYCOL STREAM Temperature: Pressure: Flow Rate: Component	160.00 59.40 7.22 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopextane N-Hexane Cyclopextane N-Hexane Cyclopextane N-Hexane Cyclopextane N-Hexane Cyclopextane N-Hexane Cyclopextane N-Hexane Cyclopextane N-Hexane Cyclopextane N-Hexane Cyclopextane N-Hexane Cyclopextane N-Hexane Cyclopextane N-Hexane Cyclopextane N-Hexane Cyclopextane N-Hexane Cyclopextane N-Hexane Cyclopextane N-Hexane Cyclopextane N-Hexane Cyclopextane N-Hexane N-	deg F psia sgpm Conc. (wt%)	0.02 0.00 0.00 0.01 0.03 0.07 0.02 0.08 0.03 0.05 0.00 0.10 0.00 0.00 0.00 0.00 0.00	Mass Flow (lb/h) 0.98 0.00 0.00 0.49 1.28 2.66 0.64 3.07 1.28 2.02 0.00 4.10 0.00 2.25 0.00 0.00 4.10 0.00 2.25 0.00 0.00 0.00 0.98 0.00 0.98 0.00 0.00 0.49 1.28 2.66 0.64 3.07 1.28 2.02 0.00 0.00 0.00 0.49 1.28 2.02 0.00 0.00 0.64 3.07 1.28 2.02 0.00 0.00 0.00 0.64 3.07 1.28 2.02 0.00 0.00 0.00 0.64 3.07 1.28 2.02 0.00 0.00 0.00 0.00 0.64 3.07 1.28 2.02 0.00 0.00 0.00 0.00 0.64 3.07 1.28 2.02 0.00 0.00 4.10 0.00 0.00 0.00 0.00 0.64 3.07 1.28 2.02 0.00	
SH TANK GLYCOL STREAM Temperature: Pressure: Flow Rate: Component	160.00 59.40 7.22 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Heytane Zy2,4-Trimethylpentane Benzene Toluene	deg F psia sgpm Conc. (wt%)	0.02 0.00 0.00 0.01 0.03 0.07 0.02 0.08 0.03 0.05 0.00 0.10 0.00 0.00 0.00 0.00 0.00	Mass Flow (lb/h)  0.98 0.00 0.00 0.49 1.28 2.66 0.64 3.07 1.28 2.02 0.00 4.10 0.00 2.25 0.00 0.00 4.85 3.88 0.64 0.64 0.64 0.64 0.64 0.64 0.64 0.64	
SH TANK GLYCOL STREAM Temperature: Pressure: Flow Rate: Component	160.00 59.40 7.22 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Ethane i-Pentane i-Pentane n-Butane n-Butane n-Butane cyclopentane n-Hexane Qyclopexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene	deg F psia sgpm Conc. (wt%)	0.02 0.00 0.00 0.01 0.03 0.07 0.02 0.08 0.03 0.05 0.00 0.00 0.00 0.00 0.00 0.00	Mass Flow (lb/h) 0.98 0.00 0.00 0.49 1.28 2.66 0.64 3.07 1.28 2.02 0.00 4.10 0.00 4.10 0.00 2.25 0.00 0.00 4.85 3.88 0.14 0.22	
SH TANK GLYCOL STREAM Temperature: Pressure: Flow Rate: Component	160.00 59.40 7.22 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Pentane i-Pentane Cyclopentane n-Hexane Cyclopexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene o-Xylene	deg F psia sgpm Conc. (wt%)	0.02 0.00 0.00 0.01 0.03 0.07 0.02 0.08 0.03 0.05 0.00 0.10 0.00 0.00 0.00 0.00 0.00	Mass Flow (lb/h) 0.98 0.00 0.00 0.49 1.28 2.66 0.64 3.07 1.28 2.02 0.00 4.10 0.00 2.25 0.00 0.00 4.10 0.00 2.25 0.00 0.00 4.85 3.88 0.14 0.29 0.00 0.00 0.98 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.49 1.28 2.66 0.64 3.07 1.28 2.02 0.00 0.00 0.00 0.00 0.49 1.28 2.02 0.00 0.00 0.00 0.49 1.28 2.02 0.00 0.00 0.00 0.00 0.49 1.28 2.02 0.00 0.00 0.00 0.00 0.00 0.49 1.28 2.02 0.00	
SH TANK GLYCOL STREAM Temperature: Pressure: Flow Rate: Component	160.00 59.40 7.22 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopexane n-Heptane n-Heptane thylybenzene Ethylbenzene o-Xylene m-Xylene	deg F psia sgpm Conc. (wt%)	0.02 0.00 0.00 0.01 0.03 0.07 0.02 0.08 0.03 0.07 0.02 0.08 0.03 0.05 0.00 0.10 0.00 0.00 0.00 0.00 0.01 0.00 0.01 0.00 0.01 0.02 0.02	Mass Flow (lb/h) 0.98 0.00 0.00 0.49 1.28 2.66 0.64 3.07 1.28 2.02 0.00 4.10 0.00 4.10 0.00 2.25 0.00 4.10 0.00 4.85 3.88 0.14 0.29 0.86 0.64	
SH TANK GLYCOL STREAM Temperature: Pressure: Flow Rate: Component	160.00 59.40 7.22 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Butane n-Butane cyclopentane Cyclopentane n-Heytane Z,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene	deg F psia sgpm Conc. (wt%)	0.02 0.00 0.00 0.01 0.03 0.07 0.02 0.08 0.03 0.05 0.00 0.10 0.00 0.00 0.12 0.00 0.01 0.00 0.01 0.02 0.00 0.01	Mass Flow (lb/h)  0.98 0.00 0.00 0.49 1.28 2.66 0.64 3.07 1.28 2.02 0.00 4.10 0.00 2.25 0.00 4.10 0.00 2.25 0.00 0.00 4.85 3.88 0.14 0.29 0.86 0.07 2.25 0.00 0.14 0.29 0.86 0.07 2.25 0.20 0.20 0.20 0.20 0.20 0.20 0.20	
SH TANK GLYCOL STREAM Temperature: Pressure: Flow Rate: Component	160.00 59.40 7.22 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Ethane i-Pentane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclopexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene p-Xylene Triethylene Glycol	deg F psia sgpm Conc. (wt%)	0.02 0.00 0.00 0.00 0.01 0.03 0.07 0.02 0.08 0.03 0.05 0.00 0.10 0.00 0.06 0.00 0.00 0.00 0.00	Mass Flow (lb/h) 0.98 0.00 0.00 0.49 1.28 2.66 0.64 3.07 1.28 2.02 0.00 4.10 0.00 2.25 0.00 0.00 4.85 3.88 0.14 0.29 0.86 0.07 3915.81	
SH TANK GLYCOL STREAM Temperature: Pressure: Flow Rate: Component	160.00 59.40 7.22 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Pentane i-Pentane Cyclopentane n-Hexane Cyclohexane Cyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene m-Xylene Triethylene Glycol	deg F psia sgpm Conc. (wt%)	0.02 0.00 0.00 0.01 0.03 0.07 0.02 0.08 0.03 0.05 0.00 0.10 0.00 0.00 0.00 0.00 0.00	Mass Flow (lb/h) 0.98 0.00 0.00 0.49 1.28 2.66 0.64 3.07 1.28 2.02 0.00 4.10 0.00 2.25 0.00 0.00 4.10 0.00 2.45 3.88 0.14 0.29 0.86 0.07 3915.81 0.00 1.0	
SH TANK GLYCOL STREAM Temperature: Pressure: Flow Rate: Component	160.00 59.40 7.22 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Butane n-Butane n-Butane cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopexane n-Heptane n-Heptane n-Heptane thethylencane Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol	deg F psia sgpm Conc. (wt%)	0.02 0.00 0.00 0.01 0.03 0.07 0.02 0.08 0.03 0.07 0.02 0.08 0.03 0.05 0.00 0.10 0.00 0.10 0.00 0.00 0.01 0.00 0.01 0.00 0.01 0.00 0.01 0.02 0.00 0.01 0.02 0.02	Mass Flow (lb/h) 0.98 0.00 0.00 0.49 1.28 2.66 0.64 3.07 1.28 2.02 0.00 4.10 0.00 2.25 0.00 4.10 0.00 4.10 0.00 4.85 3.88 0.14 0.29 0.86 0.07 3915.81 0.00 102.27	
SH TANK GLYCOL STREAM Temperature: Pressure: Flow Rate: Component	160.00 59.40 7.22 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Heptane Cyclopextane n-Heptane Methylcyclohexane 2,2,4-Trimethylepentane Benzene Toluene Ethylbenzene o-Xylene n-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Water	deg F psia sgpm Conc. (wt%)	0.02 0.00 0.00 0.01 0.03 0.07 0.02 0.08 0.03 0.05 0.00 0.10 0.00 0.10 0.00 0.10 0.00 0.12 0.00 0.01 0.02 0.00 0.01 0.02 0.00 0.01 0.02 0.00 0.00	Mass Flow (lb/h) 0.98 0.00 0.00 0.49 1.28 2.66 0.64 3.07 1.28 2.02 0.00 4.10 0.00 2.25 0.00 4.10 0.00 2.25 0.00 4.10 0.00 2.25 0.00 0.00 4.10 0.00 2.25 0.00 0.00 0.00 1.28 2.02 0.00 4.10 0.00 0.00 1.28 2.02 0.00 4.10 0.00 0.00 1.28 2.02 0.00 4.10 0.00 0.00 1.28 2.02 0.00 4.10 0.00 0.00 1.28 2.02 0.00 4.10 0.00 0.00 1.28 2.02 0.00 4.10 0.00 0.00 1.28 2.02 0.00 4.10 0.00 0.00 1.28 1.28 2.02 0.00 4.10 0.00 0.00 0.00 1.25 0.00 0.29 0.86 0.00 0.00 0.00 0.00 0.00 0.29 0.86 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.29 0.86 0.00	
SH TANK GLYCOL STREAM Temperature: Pressure: Flow Rate: Component	160.00 59.40 7.22 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Pentane n-Pentane Cyclopentane n-Hexane Cyclopexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol Uwater Methanol O	deg F psia sgpm Conc. (wt%)	0.02 0.00 0.00 0.00 0.01 0.03 0.07 0.02 0.08 0.03 0.05 0.00 0.10 0.00 0.06 0.00 0.06 0.00 0.01 0.00 0.01 0.00 0.01 0.00 0.00 0.01 0.00 0.01 0.02 0.00 0.01 0.02 0.00 0.01 0.02 0.00 0.02 0.03 0.05 0.00 0.00 0.01 0.02 0.00 0.00 0.01 0.02 0.02	Mass Flow (lb/h) 0.98 0.00 0.00 0.49 1.28 2.66 0.64 3.07 1.28 2.02 0.00 4.10 0.00 4.10 0.00 2.25 0.00 0.00 4.85 3.88 0.14 0.29 0.86 0.07 3915.81 0.00 102.27 0.00 0	
SH TANK GLYCOL STREAM Temperature: Pressure: Flow Rate: Component	160.00 59.40 7.22 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Pentane Cyclopentane n-Pentane Cyclopexane Cyclopexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene m-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol Water Methanol O2 SO2	deg F psia sgpm Conc. (wt%)	0.02 0.00 0.00 0.01 0.03 0.07 0.02 0.08 0.03 0.05 0.00 0.10 0.00 0.00 0.00 0.00 0.00	Mass Flow (lb/h) 0.98 0.00 0.00 0.49 1.28 2.66 0.64 3.07 1.28 2.02 0.00 4.10 0.00 2.25 0.00 0.00 4.85 3.88 0.14 0.29 0.86 0.07 3915.81 0.00 102.27 0.00 0	

Temperature	206 70	deg F		
Pressure:	200.70	neia		
Flow Pate:	1602.13	soft		
Component	1002.15	Conc (mol%)	Mass Flow (lb/b)	
component	Carbon Diovide	0.53	0.98	
	Hydrogen Sulfide	0.00	0.00	
	Nitrogon	0.00	0.00	
	Nitrogen	0.00	0.00	
	Methane	0.73	0.49	
	Ethane	1.01	1.28	
	Propane	1.43	2.66	
	i-Butane	0.26	0.64	
	n-Butane	1.25	3.07	
	i-Pentane	0.42	1.28	
	n-Pentane	0.66	2.02	
	Cyclopentane	0.00	0.00	
	n-Hexane	1.13	4.10	
	Cyclohexane	0.00	0.00	
	n-Hentane	0.53	2 25	
	Mothylcycloboyapo	0.00	2.25	
		0.00	0.00	
	2,2,4-Trimethylpentane	0.00	0.00	
	Benzene	1.46	4.83	
	Toluene	0.98	3.83	
	Ethylbenzene	0.03	0.14	
	o-Xylene	0.06	0.26	
	m-Xylene	0.18	0.82	
	p-Xylene	0.01	0.07	
	Triethylene Glycol	0.00	0.02	
	Ethylene Glycol	0.00	0.00	
	Water	89 32	67 93	
	Methanol	0.00	0.00	
		0.00	0.00	
	02 (O2	0.00	0.00	
Temperature:	120.00	deg F		
X CONDENSER VENT GAS STREAM Temperature: Pressure:	120.00 14.10	deg F psia sefe		
X CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate:	120.00 14.10 157.44	deg F psia scfh	Necco Flow (Ib/b)	
X CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 14.10 157.44	deg F psia scfh Conc. (mol%)	Mass Flow (lb/h)	
X CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 14.10 157.44 Carbon Dioxide	deg F psia scfh Conc. (mol%) 5.33	Mass Flow (lb/h) 0.97	
X CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 14.10 157.44 Carbon Dioxide Hydrogen Sulfide	deg F psia scfh Conc. (mol%) 5.33 0.00	Mass Flow (lb/h) 0.97 0.00	
X CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 14.10 157.44 Carbon Dioxide Hydrogen Sulfide Nitrogen	deg F psia scfh Conc. (mol%) 5.33 0.00 0.02	Mass Flow (lb/h) 0.97 0.00 0.00	
X CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 14.10 157.44 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane	deg F psia scfh Conc. (mol%) 5.33 0.00 0.02 7.41	Mass Flow (lb/h) 0.97 0.00 0.00 0.49	
X CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 14.10 157.44 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane	deg F psia scfh Conc. (mol%) 5.33 0.00 0.02 7.41 10.22	Mass Flow (lb/h) 0.97 0.00 0.00 0.49 1.27	
X CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 14.10 157.44 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane	deg F psia scfh Conc. (mol%) 5.33 0.00 0.02 7.41 10.22 14.39	Mass Flow (lb/h) 0.97 0.00 0.00 0.49 1.27 2.63	
X CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 14.10 157.44 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane	deg F psia scfh Conc. (mol%) 5.33 0.00 0.02 7.41 10.22 14.39 2.58	Mass Flow (lb/h) 0.97 0.00 0.00 0.49 1.27 2.63 0.62	
X CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 14.10 157.44 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane	deg F psia scfh Conc. (mol%) 5.33 0.00 0.02 7.41 10.22 14.39 2.58 12.32	Mass Flow (lb/h) 0.97 0.00 0.00 0.49 1.27 2.63 0.62 2.97	
X CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 14.10 157.44 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane	deg F psia scfh Conc. (mol%) 5.33 0.00 0.02 7.41 10.22 14.39 2.58 12.32 3.92	Mass Flow (lb/h) 0.97 0.00 0.00 0.49 1.27 2.63 0.62 2.97 1.17	
X CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 14.10 157.44 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane n-Pentane	deg F psia scfh Conc. (mol%) 5.33 0.00 0.02 7.41 10.22 14.39 2.58 12.32 3.92 6.06	Mass Flow (lb/h) 0.97 0.00 0.00 0.49 1.27 2.63 0.62 2.97 1.17 1.82	
X CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 14.10 157.44 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Pentane Cvclopentane	deg F psia scfh Conc. (mol%) 5.33 0.00 0.02 7.41 10.22 14.39 2.58 12.32 3.92 6.06	Mass Flow (lb/h) 0.97 0.00 0.49 1.27 2.63 0.62 2.97 1.17 1.82 0.00	
X CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 14.10 157.44 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane	deg F psia scfh Conc. (mol%) 5.33 0.00 0.02 7.41 10.22 14.39 2.58 12.32 3.92 6.06 0.00 8.73	Mass Flow (lb/h) 0.97 0.00 0.00 1.27 2.63 0.62 2.97 1.17 1.82 0.00 3.12	
X CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 14.10 157.44 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclohexane	deg F psia scfh Conc. (mol%) 5.33 0.00 0.02 7.41 10.22 14.39 2.58 12.32 3.92 6.06 0.00 8.73 0.00	Mass Flow (lb/h) 0.97 0.00 0.09 1.27 2.63 0.62 2.97 1.17 1.17 1.82 0.00 3.12 0.00	
X CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 14.10 157.44 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclohexane n-Hextane	deg F psia scfh Conc. (mol%) 5.33 0.00 0.02 7.41 10.22 14.39 2.58 12.32 3.92 6.06 0.00 8.73 0.00	Mass Flow (lb/h) 0.97 0.00 0.00 0.49 1.27 2.63 0.62 2.97 1.17 1.82 0.00 3.12 0.00 1.19	
X CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 14.10 157.44 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane cyclopentane n-Hexane Cyclohexane n-Hexane	deg F psia scfh Conc. (mol%) 5.33 0.00 0.02 7.41 10.22 14.39 2.58 12.32 3.92 6.06 0.00 8.73 0.00 2.84 0.00	Mass Flow (lb/h) 0.97 0.00 0.00 1.27 2.63 0.62 2.97 1.17 1.82 0.00 3.12 0.00 1.18 0.00	
X CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 14.10 157.44 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Butane i-Butane n-Butane Cyclopentane n-Hexane N-Heytane Methylcyclohexane	deg F psia scfh Conc. (mol%) 5.33 0.00 0.02 7.41 10.22 14.39 2.58 12.32 3.92 6.06 0.00 8.73 0.00 2.84 0.00 2.84 0.00	Mass Flow (lb/h) 0.97 0.00 0.00 0.49 1.27 2.63 0.62 2.97 1.17 1.82 0.00 3.12 0.00 1.18 0.00 1.18 0.00	
X CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 14.10 157.44 Carbon Dioxide Hydrogen Sulfide Nitrogen Ethane Propane i-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclohexane 2,2,4-Trimethylpentane	deg F psia scfh Conc. (mol%) 5.33 0.00 0.02 7.41 10.22 14.39 2.58 12.32 3.92 6.06 6.00 0.00 8.73 0.00 2.84 4.00 0.00 2.84 0.00 0.00 0.2	Mass Flow (lb/h) 0.97 0.00 0.00 0.49 1.27 2.63 0.62 2.97 1.17 1.82 0.00 3.12 0.00 3.12 0.00 1.18 0.00 0.10 1.28 0.00 0.2 0.2 0.2 0.2 0.2 0.2 0.	
X CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 14.10 157.44 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Pentane cyclopentane Cyclopentane Methylcyclohexane Methylcyclohexane 2,2,4-Trimethylpentane Benzene	deg F psia scfh Conc. (mol%) 5.33 0.00 0.02 7.41 10.22 7.41 10.22 7.41 10.22 7.41 10.22 7.41 10.22 7.41 10.22 7.41 10.22 8.4 0.00 0.00 8.73 0.00 2.84 0.00 0.00 8.73 0.00 8.73 0.00 0.00 8.73 0.00 8.73 0.00 0.00 7.41 10.22 7.58 12.32 7.58 12.32 7.58 12.32 7.58 12.32 7.58 12.32 7.58 12.32 7.58 12.32 7.58 7.53 7.58 7.53 7.58 7.58 7.58 7.58 7.58 7.58 7.58 7.58	Mass Flow (lb/h) 0.97 0.00 0.00 0.49 1.27 2.63 0.62 2.97 1.17 1.82 0.00 3.12 0.00 1.18 0.00 3.12 0.00 3.12 0.00 1.18 0.00 0.00 0.00 0.00 0.49 0.127 1.17 1.82 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.49 0.127 1.17 1.17 1.82 0.00 0.312 0.00 0.00 0.00 0.312 0.00 0.00 0.00 0.00 0.00 0.312 0.000 0.00	
X CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 14.10 157.44 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Butane n-Butane i-Pentane Cyclopentane Cyclopentane Cyclopentane Athylcyclohexane n-Heytane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene	deg F psia scfh Conc. (mol%) 5.33 0.00 0.02 7.41 10.22 14.39 2.58 12.32 3.92 6.06 0.00 8.73 0.00 2.84 0.00 0.284 0.00 0.284 0.00 0.284 0.00	Mass Flow (lb/h) 0.97 0.00 0.00 0.49 1.27 2.63 0.62 2.97 1.17 1.82 0.00 3.12 0.00 1.18 0.00 3.12 0.00 3.15 1.50	
X CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 14.10 157.44 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane n-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopexane n-Heytane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Benzene Toluene	deg F psia scfh Conc. (mol%) 5.33 0.00 0.02 7.41 10.22 14.39 2.58 12.32 3.92 6.06 0.00 8.73 0.00 2.84 0.00 0.00 9.75 3.93 2.58	Mass Flow (lb/h) 0.97 0.00 0.09 1.27 2.63 0.62 2.97 1.17 1.82 0.00 3.12 0.00 1.18 0.00 3.15 1.50 0.02	
X CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 14.10 157.44 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Butane n-Butane Cyclopentane n-Hexane Cyclopentane n-Hexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene	deg F psia scfh Conc. (mol%) 5.33 0.00 0.02 7.41 10.22 14.39 2.58 12.32 3.92 6.06 6.06 6.00 0.00 8.73 0.00 8.73 0.00 2.84 0.00 0.00 9.75 3.93 0.05 0.01	Mass Flow (lb/h) 0.97 0.00 0.00 0.49 1.27 2.63 0.62 2.97 1.17 1.82 0.00 3.12 0.00 3.12 0.00 3.12 0.00 3.16 1.50 0.02 0.05	
X CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 14.10 157.44 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Butane i-Butane n-Butane Cyclopentane Cyclopentane Cyclopentane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene	deg F psia scfh Conc. (mol%) 5.33 0.00 0.02 7.41 10.22 14.39 2.58 12.32 3.92 6.06 0.00 2.84 0.00 2.84 0.00 0.284 0.00 0.284 0.00 0.284 0.00 0.00 0.284 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	Mass Flow (lb/h) 0.97 0.00 0.00 0.49 1.27 2.63 0.62 2.97 1.17 1.82 0.00 3.12 0.00 1.18 0.00 3.12 0.00 3.16 1.50 0.02 0.05	
x CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 14.10 157.44 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene	deg F psia scfh Conc. (mol%) 5.33 0.00 0.02 7.41 10.22 14.39 2.58 12.32 3.92 6.06 0.00 8.73 0.00 2.84 0.00 0.00 2.84 0.00 0.00 0.00 9.75 3.93 0.05 0.11 0.33	Mass Flow (lb/h) 0.97 0.00 0.00 0.49 1.27 2.63 0.62 2.97 1.17 1.82 0.00 3.12 0.00 1.18 0.00 1.18 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.01 0.00 0.01 0.00 0.01 0.01 0.02 0.05 0.01 0.01 0.00	
X CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 14.10 157.44 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopextane n-Hexane Cyclopextane n-Hexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene p-Xylene	deg F psia scfh Conc. (mol%) 5.33 0.00 0.02 7.41 10.22 14.39 2.58 12.32 3.92 6.06 0.00 8.73 0.00 8.73 0.00 2.84 0.00 0.00 9.75 3.93 3.93 0.05 0.011 0.33 0.03	Mass Flow (lb/h) 0.97 0.00 0.00 0.49 1.27 2.63 0.62 2.97 1.17 1.82 0.00 3.12 0.00 3.12 0.00 3.12 0.00 3.12 0.00 3.12 0.00 3.12 0.00 0.01 1.55 0.01 0.00 0.01	
X CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 14.10 157.44 Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfide Ethane Propane i-Butane n-Butane i-Pentane n-Butane Cyclopentane Cyclopentane Cyclopentane Cyclopentane 2,2,4-Trimethylepentane Benzene Toluene Ethylbenzene m-Xylene p-Xylene Triethylene Glycol	deg F psia scfh Conc. (mol%) 5.33 0.00 0.02 7.41 10.22 14.39 2.58 12.32 3.92 6.06 0.00 2.84 0.00 2.84 0.00 2.84 0.00 9.75 3.93 0.05 0.05 0.01 0.03 0.03 0.00	Mass Flow (lb/h) 0.97 0.00 0.00 1.27 2.63 0.62 2.97 1.17 1.82 0.00 3.12 0.00 1.18 0.00 3.16 1.50 0.00 3.16 1.50 0.02 0.05 0.15 0.01 0.00	
X CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 14.10 157.44 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Butane i-Butane i-Butane i-Pentane Cyclopentane Cyclopentane Cyclopexane n-Hexane Cyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol	deg F psia scfh Conc. (mol%) 5.33 0.00 0.02 7.41 10.22 14.39 2.58 12.32 3.92 6.06 0.00 8.73 0.00 2.84 0.00 0.00 2.84 0.00 0.00 0.00 0.00 0.01 1.99	Mass Flow (lb/h) 0.97 0.00 0.00 0.49 1.27 2.63 0.62 2.97 1.17 1.82 0.00 3.12 0.00 1.18 0.00 0.118 0.00 0.00 0.01 0.05 0.01 0.00 0.00	
X CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 14.10 157.44 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane n-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopexane n-Heyane Methylcyclohexane 2,2,4-Trimethylipentane Benzene Benzene Benzene Toluene Ethylbenzene o-Xylene m-Xylene Triethylene Glycol Ethylene Glycol	deg F psia scfh Conc. (mol%) 5.33 0.00 0.02 7.41 10.22 14.39 2.58 12.32 3.92 6.06 0.00 8.73 0.00 0.00 2.84 0.00 0.00 9.75 3.93 0.05 0.01 0.01 0.03 0.03 0.01 0.03 0.03 0.03	Mass Flow (lb/h) 0.97 0.00 0.00 0.49 1.27 2.63 0.62 2.97 1.82 0.00 3.12 0.00 1.18 0.00 0.118 0.00 0.01 1.18 0.00 0.00	
X CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 14.10 157.44 Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Butane Cyclopentane Cyclopentane Cyclopentane Cyclohexane n-Hexane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol	deg F psia scfh Conc. (mol%) 5.33 0.00 0.02 7.41 10.22 14.39 2.58 12.32 3.92 6.06 0.00 2.84 0.00 2.84 0.00 2.84 0.00 9.75 3.93 0.05 0.01 0.05 0.01 0.03 0.01 0.03 0.00	Mass Flow (lb/h) 0.97 0.00 0.00 0.04 1.27 2.63 0.62 2.97 1.17 1.82 0.00 3.12 0.00 1.18 0.00 3.16 1.50 0.00 3.16 1.50 0.02 0.05 0.15 0.01 0.00 0.00 0.00 0.00 0.00	
EX CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 14.10 157.44 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Butane i-Butane n-Hextane Cyclopentane C	deg F psia scfh Conc. (mol%) 5.33 0.00 0.02 7.41 10.22 14.39 2.58 12.32 3.92 6.06 0.00 8.73 3.92 6.06 0.00 0.873 3.92 6.06 0.00 0.00 0.00 0.00 0.011 0.33 0.03 0.0	Mass Flow (lb/h) 0.97 0.00 0.00 0.04 1.27 2.63 0.62 2.97 1.17 1.82 0.00 3.12 0.00 1.18 0.00 1.18 0.00 0.00 3.16 1.50 0.02 0.05 0.15 0.01 0.00 0.00 0.00 0.00 0.00	
EX CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 14.10 157.44 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane n-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Change Sorg	deg F psia scfh Conc. (mol%) 5.33 0.00 0.02 7.41 10.22 14.39 2.58 12.32 3.92 6.06 0.00 8.73 0.00 2.84 0.00 0.00 0.00 9.75 3.93 0.05 0.11 0.33 0.05 0.11 0.33 0.00 0.00 0.00 0.00 0.00 0.00	Mass Flow (lb/h) 0.97 0.00 0.00 0.49 1.27 2.63 0.62 2.97 1.82 0.00 3.12 0.00 1.18 0.00 1.18 0.00 0.00 1.18 0.00 0.00	

BTEX CONDENSER RECOVERED OIL STREA	AM			
Temperature:	120.00	deg F		
Pressure:	14.10	psia		
Flow Rate:	0.02	sgpm		
Component		Conc. (mol%)	Mass Flow (lb/h)	
	Carbon Dioxide	0.05	0.00	
	Nitrogen	0.00	0.00	
	Methane	0.00	0.00	
	Fthane	0.18	0.00	
	Propane	0.75	0.03	
	i-Butane	0.28	0.01	
	n-Butane	2.05	0.10	
	i-Pentane	1.63	0.10	
	n-Pentane	3.27	0.20	
	Cyclopentane	0.00	0.00	
	n-Hexane	13.36	0.98	
	Cyclohexane	0.00	0.00	
	n-Heptane	12.56	1.07	
	Nietnylcyclonexane	0.00	0.00	
	2,2,4-Trimetnyipentane	0.00	0.00	
	Toluono	24.47	1.03	
	Ethylhenzono	29.43	2.31	
	0-Xylene	1.25	0.11	
	m-Xylene	7 44	0.67	
	p-Xylene	0.59	0.05	
	Triethylene Glycol	0.00	0.00	
	Ethylene Glycol	0.00	0.00	
	Water	0.33	0.01	
	Methanol	0.00	0.00	
	02	0.00	0.00	
	SO2	0.00	0.00	
BTEX CONDENSER PRODUCED WATER ST Temperature:	<b>TREAM</b> 120.00	deg F		
BTEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Elow Pate:	TREAM 120.00 14.10 0.13	deg F psia sacm		
BTEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.13	deg F psia sgpm	Mass Flow (lh/h)	
BTEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.13 Carbon Dioxide	deg F psia sgpm Conc. (mol%) 0.00	Mass Flow (lb/h) 0.00	
BTEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.13 Carbon Dioxide Hydrogen Sulfide	deg F psia sgpm Conc. (mol%) 0.00 0.00	Mass Flow (lb/h) 0.00 0.00	
BTEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.13 Carbon Dioxide Hydrogen Sulfide Nitrogen	deg F psia sgpm Conc. (mol%) 0.00 0.00 0.00	Mass Flow (lb/h) 0.00 0.00 0.00	
BTEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.13 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane	deg F psia sgpm Conc. (mol%) 0.00 0.00 0.00 0.00	Mass Flow (lb/h) 0.00 0.00 0.00 0.00	
BTEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.13 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane	deg F psia sgpm Conc. (mol%) 0.00 0.00 0.00 0.00 0.00	Mass Flow (lb/h) 0.00 0.00 0.00 0.00 0.00	
BTEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.13 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane	deg F psia sgpm Conc. (mol%) 0.00 0.00 0.00 0.00 0.00 0.00	Mass Flow (lb/h) 0.00 0.00 0.00 0.00 0.00 0.00 0.00	
BTEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.13 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane	deg F psia sgpm Conc. (mol%) 0.00 0.00 0.00 0.00 0.00 0.00 0.00	Mass Flow (lb/h) 0.00 0.00 0.00 0.00 0.00 0.00 0.00	
BTEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.13 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane	deg F psia sgpm Conc. (mol%) 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	Mass Flow (lb/h) 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00	
BTEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.13 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane Postero	deg F psia sgpm Conc. (mol%) 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	Mass Flow (lb/h) 0.00	
BTEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.13 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclonentane	deg F psia sgpm Conc. (mol%) 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	Mass Flow (lb/h) 0.00	
BTEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.13 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Putane n-Pentane Cyclopentane n-Hexane	deg F psia sgpm Conc. (mol%) 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	Mass Flow (lb/h) 0.00	
BTEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.13 Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclohexane	deg F psia sgpm Conc. (mol%) 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	Mass Flow (lb/h) 0.00	
BTEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.13 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Pentane i-Pentane Cyclopentane n-Hexane Cyclohexane n-Hexane	deg F psia sgpm Conc. (mol%) 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	Mass Flow (lb/h) 0.00	
BTEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.13 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopexane n-Heptane Methylcyclohexane	deg F psia sgpm Conc. (mol%) 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	Mass Flow (lb/h) 0.00	
BTEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.13 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Butane i-Butane n-Pentane n-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane	deg F psia sgpm Conc. (mol%) 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	Mass Flow (lb/h) 0.00	
BTEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.13 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Butane Cyclopentane n-Hexane Cyclohexane n-Hexane Methylcyclohexane 2,2,4-Trimethylpentane Benzene	deg F psia sgpm Conc. (mol%) 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	Mass Flow (lb/h) 0.00	
BTEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.13 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane Cyclopentane Cyclopentane Cyclohexane n-Hextane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene	deg F psia sgpm Conc. (mol%) 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	Mass Flow (lb/h) 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	
BTEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.13 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Pentane Cyclopentane n-Pentane Cyclopentane n-Hexane Cyclopexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene	deg F psia sgpm Conc. (mol%) 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	Mass Flow (lb/h) 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	
BTEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.13 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Pentane Cyclopentane n-Pentane Cyclopexane n-Hexane Cyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene	deg F psia sgpm Conc. (mol%) 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	Mass Flow (lb/h) 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	
BTEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.13 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopexane n-Hexane Cyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene	deg F psia sgpm Conc. (mol%) 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	Mass Flow (lb/h) 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	
BTEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.13 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopextane n-Hexane Cyclohexane n-Hexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene Ethylbenzene Toluene Ethylbenzene Toluene Ethylbenzene Toluene Ethylbenzene Cyclopextane N-Xylene p-Xylene p-Xylene	deg F psia sgpm Conc. (mol%) 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	Mass Flow (lb/h) 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	
BTEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	IREAM 120.00 14.10 0.13 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Butane n-Butane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclohexane n-Hexane Cyclohexane n-Hexane Ethylenzene Ethylbenzene Ethylbenzene Ethylbenzene Diuene Ethylbenzene Diuene Ethylbenzene Diuene Ethylbenzene Diuene Ethylbenzene Diuene Ethylbenzene Diuene Ethylbenzene Diuene Ethylbenzene Diuene Ethylbenzene Diuene Ethylbenzene Diuene Ethylbenzene Diuene Ethylbenzene Diuene Ethylbenzene Diuene Ethylbenzene Diuene Ethylbenzene Diuene Ethylbenzene Diuene Ethylbenzene Diuene Diuene Ethylbenzene Diuene	deg F psia sgpm Conc. (mol%) 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	Mass Flow (lb/h) 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	
BTEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.13 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Pentane i-Pentane i-Pentane Cyclopentane n-Pentane Cyclopentane n-Hexane Cyclopexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Gyclop Ethylene Glycol Ethylene Glycol Ethylene Glycol	deg F psia sgpm Conc. (mol%) 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	Mass Flow (lb/h) 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	
BTEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.13 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Pentane Cyclopentane n-Pentane Cyclopentane n-Pentane Cyclopexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol	deg F psia sgpm Conc. (mol%) Conc. (mol%) 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	Mass Flow (lb/h)           0.00           0.01           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00	
BTEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.13 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Pentane Cyclopentane n-Pentane Cyclopexane n-Hexane Cyclopexane n-Hexane Cyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Divene Glycol Ethylene Glycol Ethylene Glycol Water Methanol OZ	deg F psia sgpm Conc. (mol%) Conc. (mol%) 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	Mass Flow (lb/h)  0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	
BTEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.13 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Cyclopexane Nethanol Cyclopexane Nethanol Cyclopexane Nethanol Cyclopexane Nethanol Cyclopexane Nethylene Glycol Cyclopexane Nethanol	deg F psia sgpm Conc. (mol%) Conc. (mol%) Conc. (mol%) 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	Mass Flow (lb/h)  0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	
BTEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	IREAM 120.00 14.10 0.13 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopextane n-Hexane Cyclopextane n-Hexane Cyclohexane n-Hexane Cyclohexane n-Hexane Cyclohexane n-Hexane Cyclohexane n-Hexane Cyclohexane n-Hexane Cyclohexane n-Hexane Cyclohexane n-Hexane Cyclohexane n-Hexane Cyclohexane n-Hexane Cyclohexane n-Hexane Cyclohexane n-Hexane Cyclohexane Nethylcyclohexane Cyclohexane In-Hexane Cyclohexane Nethylcyclohexane Cyclohexane Cyclohexane Nethylcyclohexane Cyclohexane Cyclohexane Nethylcyclohexane Cyclohexane Cyclohexane Nethylcyclohexane Cyclohexane Nethylcyclohexane Cyclohexane Ithylbencel Cyclohexane Ithylbencel Cyclohexane Ithylbencel Cyclohexane Ithylbencel Cyclohexane Ithylbencel Cyclohexane Ithylbencel Cyclohexane Cyclohexane Ithylbencel Cyclohexane Ithylbencel Cyclohexane Ithylbencel Cyclohexane Ithylbencel Cyclohexane Ithylbencel Cyclohexane Ithylbencel Cyclohexane Ithylbencel Cyclohexane Ithylbencel Cyclohexane Ithylbencel Cyclohexane Ithylbencel Cyclohexane Ithylbencel Cyclohexane Ithylbencel Ithylbencel Ithylene Glycol Ithylene Glycol Cyclohexane Ithylene Slycol Ithylene Slycol Ithy	deg F psia sgpm Conc. (mol%) Conc. (mol%) Co	Mass Flow (lb/h)           0.00	

ProMax Dehydration Emissions Report	
Case Name: 100 MMSCED	
C:\Users\Admin\Resolute Complia	ance, LLC\Environmental Compliance - General\Env\Projects\Env-EnLink-0254\5.0 Air Permit-
Horned Frog CS NSR\5.2 Modeling	x\5.2.2 BRE ProMax-Other Simulation\ProMax_Dehydration_Tool.pmx
Date:	
Description:	
Drv Gas	Flow Rate 98.90 MMSCED
Dry Gas Wat	er Content 4.55 lb/MMSCF
Glycol Circu	lation Rate 7.00 sgpm
Glycol Circul Annual Onera	ation Ratio 1.47 gal/lb
Eard Stream Specifications	
Fraction of Water Saturaton (%)	100.00
Water Content (lbm/MMSCF)	69.22
Temperature (°F)	110.00
Pressure (psig)	1100.00
Flow Rate (MMSCFD)	100.00
Lean Glycol Specifications Glycol Circulation Rate (source)	7.00
	7.00
Regenerator Specifications	
Reboiler Temperature (°F)	400.000
Overhead Vapors	To Control Device
Is Reflux Coil Present?	Yes
Flash Tank Specifications	
Is Flash Tank Present?	Flash Tank Present
Pressure (nsiø)	45.00
Flash Gas	Vent To Atmosphere
Stripping Gas Specifications	
Nitrogen (scfm)	Not In Use
Dry gas (scfm)	Not In Use
Kimray Pump Specifications	Castrian
Type Gas Injection Volume Ratio (acfm/gom)	Gas injection 0.001
Methanol Specifications	
Is Methanol Present?	Not Present in Feed
MeOH Feed Mass Fraction (ppm)	0.00
BTEX Condenser Specifications	
Temperature (°F)	120.00
Pressure (psig) BTEX Emissions	-0.30 To Flare
1	

Atmospheric (Psia)	14.400		
Flash Gas Flare Destruction Efficiency (%)	95.000		
Regenerator Flare Destruction Efficiency (%)	98.000		
d Composition Data (mol %)			
Carbon Dioxide	0.9115		
Hydrogen Sulfide	0.0000		
Methane	70 5837		
Ethane	13.3096		
Propane	7.6136		
i-Butane	1.0396		
n-Butane	2.6978		
i-Pentane	0.6018		
n-Pentane	0.7088		
Cyclopentane	0.0000		
n-Hexane	0.6632		
Cyclohexane	0.0000		
n-Heptane	0.2041		
Methylcyclohexane	0.0000		
2,2,4-Trimethylpentane	0.0000		
Benzene	0.0122		
I oluene Ethylkonger	0.0123		
Etnyidenzene	0.0004		
0-Ayiene	0.0000		
n-Xylene	0.0024		
Triethylene Glycol	0.0000		
Ethylene Glycol	0.0000		
Water	0.0000		
Methanol	0.0000		
02	0.0000		
SO2	0.0000		
Total	100.00		
ISSIONS REPORTS:			
SSIONS REPORTS:			
SSIONS REPORTS: ITROLLED REGENERATOR EMISSIONS Component	lbs/hr	lbs/day	tons/yr
SSIONS REPORTS: TROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide	lbs/hr 60.16 0.00	lbs/day 1443.95	tons/yr 263. 0
SSIONS REPORTS: TROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen	lbs/hr 60.16 0.00 597.88	lbs/day 1443.95 0.00 14349 16	tons/yr 263. 0. 2618
SSIONS REPORTS: TROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane	lbs/hr 60.16 0.00 597.88 0.01	lbs/day 1443.95 0.00 14349.16 0.27	tons/yr 263. 0. 2618. 0
SSIONS REPORTS: TROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane	lbs/hr 60.16 0.00 597.88 0.01 0.03	lbs/day 1443.95 0.00 14349.16 0.27 0.64	tons/yr 263. 0. 2618. 0. 0.
SSIONS REPORTS: TROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane	lbs/hr 60.16 0.00 597.88 0.01 0.03 0.05	lbs/day 1443.95 0.00 14349.16 0.27 0.64 1.25	tons/yr 263. 0. 2618. 0. 0. 0. 0.
SSIONS REPORTS: TROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane	lbs/hr 60.16 0.00 597.88 0.01 0.03 0.05 0.01	lbs/day 1443.95 0.00 14349.16 0.27 0.64 1.25 0.28	tons/yr 263. 0. 2618. 0. 0. 0. 0. 0. 0. 0.
SSIONS REPORTS: TROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane	lbs/hr 60.16 0.00 597.88 0.01 0.03 0.05 0.01 0.01 0.06	lbs/day 1443.95 0.00 14349.16 0.27 0.64 1.25 0.28 1.37	tons/yr 263. 0. 2618. 0. 0. 0. 0. 0. 0. 0.
SSIONS REPORTS: TROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane	lbs/hr 60.16 0.00 597.88 0.01 0.03 0.05 0.01 0.01 0.06 0.02	lbs/day 1443.95 0.00 14349.16 0.27 0.64 1.25 0.28 1.37 0.52	tons/yr 2633 0. 2618- 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
SSIONS REPORTS: TROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane	lbs/hr 60.16 0.00 597.88 0.01 0.03 0.05 0.01 0.05 0.01 0.06 0.02 0.03	lbs/day 1443.95 0.00 14349.16 0.27 0.64 1.25 0.28 1.37 0.52 0.77	tons/yr 263. 0. 2618. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
SSIONS REPORTS: TROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Pentane Cyclopentane	lbs/hr 60.16 0.00 597.88 0.01 0.03 0.05 0.01 0.06 0.02 0.03 0.00	lbs/day 1443.95 0.00 14349.16 0.27 0.64 1.25 0.28 1.37 0.52 0.77 0.00	tons/yr 263. 0. 2618. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
SSIONS REPORTS: TROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane	lbs/hr 60.16 0.00 597.88 0.01 0.03 0.05 0.01 0.06 0.02 0.03 0.00 0.05	lbs/day 1443.95 0.00 14349.16 0.27 0.64 1.25 0.28 1.37 0.52 0.77 0.00 1.31	tons/yr 263. 0. 2618. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
SSIONS REPORTS: TROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclopexane	lbs/hr 60.16 0.00 597.88 0.01 0.03 0.05 0.01 0.06 0.02 0.03 0.00 0.03 0.00 0.03 0.00 0.05 0.00 0.05 0.00	lbs/day 1443.95 0.00 14349.16 0.27 0.64 1.25 0.28 1.37 0.52 0.77 0.00 1.31 0.00 1.31 0.00	tons/yr 263. 0. 2618. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
SSIONS REPORTS: TROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane	lbs/hr 60.16 0.00 597.88 0.01 0.03 0.05 0.01 0.06 0.02 0.03 0.00 0.02 0.03 0.00 0.05 0.00 0.05 0.00 0.02	lbs/day 1443.95 0.00 14349.16 0.27 0.64 1.25 0.28 1.37 0.52 0.77 0.00 1.31 0.00 0.50	tons/yr 263. 0. 2618. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
SSIONS REPORTS: TROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane	lbs/hr 60.16 0.00 597.88 0.01 0.03 0.05 0.01 0.06 0.02 0.03 0.00 0.03 0.00 0.05 0.00 0.05 0.00 0.02 0.00 0.02 0.00	lbs/day 1443.95 0.00 14349.16 0.27 0.64 1.25 0.28 1.37 0.52 0.77 0.00 1.31 0.00 0.50 0.00	tons/yr 263. 0. 2618. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
SSIONS REPORTS: TROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Butane i-Butane i-Pentane n-Pentane Cyclopexane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Bennono	lbs/hr 60.16 0.00 597.88 0.01 0.03 0.05 0.01 0.06 0.02 0.03 0.00 0.03 0.00 0.05 0.00 0.02 0.03 0.00 0.02 0.00 0.02 0.00 0.02 0.00 0.00	lbs/day 1443.95 0.00 14349.16 0.27 0.64 1.25 0.28 1.37 0.52 0.77 0.00 1.31 0.00 0.50 0.00 1.53	tons/yr 263. 0. 2618. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
SSIONS REPORTS: TROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Heptane N-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluron	lbs/hr 60.16 0.00 597.88 0.01 0.03 0.05 0.01 0.06 0.02 0.03 0.00 0.05 0.00 0.02 0.03 0.00 0.05 0.00 0.02 0.00 0.02 0.00 0.02 0.00 0.02 0.00 0.02 0.00 0.02 0.00 0.00 0.00 0.00 0.00 0.03	lbs/day 1443.95 0.00 14349.16 0.27 0.64 1.25 0.28 1.37 0.52 0.77 0.00 1.31 0.00 1.31 0.00 0.50 0.00 0.50 0.00 1.53 0.75	tons/yr 263. 0. 2618. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
SSIONS REPORTS: TROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene	lbs/hr           60.16           0.00           597.88           0.01           0.03           0.05           0.01           0.03           0.05           0.01           0.05           0.01           0.02           0.03           0.00           0.02           0.00           0.02           0.00           0.00           0.00           0.00           0.00           0.03           0.03           0.03           0.03           0.04	lbs/day 1443.95 0.00 14349.16 0.27 0.64 1.25 0.28 1.37 0.52 0.77 0.00 1.31 0.00 1.31 0.00 0.50 0.50 0.00 0.00 1.53 0.75 0.01	tons/yr 263. 0. 2618. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
SSIONS REPORTS: TROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclopexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xvlene	lbs/hr 60.16 0.00 597.88 0.01 0.03 0.05 0.01 0.06 0.02 0.03 0.00 0.05 0.00 0.05 0.00 0.05 0.00 0.05 0.00 0.05 0.00 0.05 0.00 0.05 0.00 0.05 0.00 0.05 0.01 0.05 0.02 0.03 0.05 0.00 0.00 0.05 0.000 0.00	lbs/day 1443.95 0.00 14349.16 0.27 0.64 1.25 0.28 1.37 0.52 0.77 0.00 1.31 0.00 0.50 0.00 1.53 0.75 0.01 0.03	tons/yr 263. 0. 2618. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
SSIONS REPORTS: TROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Butane i-Butane i-Pentane n-Butane i-Pentane Cyclopentane n-Hexane Cyclopexane n-Hexane Cyclohexane n-Hextane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene	lbs/hr           60.16           0.00           597.88           0.01           0.03           0.05           0.01           0.03           0.05           0.01           0.06           0.02           0.03           0.00           0.05           0.00           0.02           0.03           0.00           0.00           0.00           0.00           0.01           0.02           0.03           0.00           0.01           0.02           0.03           0.00           0.00           0.00           0.00           0.00           0.00	lbs/day 1443.95 0.00 14349.16 0.27 0.64 1.25 0.28 1.37 0.52 0.77 0.00 1.31 0.00 0.50 0.00 1.53 0.75 0.01 0.03 0.08	tons/yr 263. 0. 2618. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
SSIONS REPORTS: TROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Butane i-Butane i-Pentane n-Butane i-Pentane Cyclopentane n-Hexane Cyclopexane n-Hexane Cyclohexane n-Hexane Cyclohexane n-Hexane Cyclohexane n-Hexane Cyclohexane n-Hexane Serzene Toluene Ethylbenzene o-Xylene m-Xylene	lbs/hr           60.16           0.00           597.88           0.01           0.03           0.05           0.01           0.02           0.03           0.05           0.00           0.05           0.00           0.02           0.03           0.05           0.00           0.02           0.03           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00	lbs/day 1443.95 0.00 14349.16 0.27 0.64 1.25 0.28 1.37 0.52 0.77 0.00 1.31 0.00 0.50 0.00 0.50 0.00 1.53 0.75 0.01 0.03 0.08 0.01	tons/yr 263. 0. 2618. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
SSIONS REPORTS: TROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylenzene o-Xylene m-Xylene p-Xylene	lbs/hr           60.16           0.00           597.88           0.01           0.03           0.05           0.01           0.03           0.05           0.01           0.03           0.05           0.01           0.02           0.03           0.05           0.00           0.02           0.00           0.02           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00	lbs/day 1443.95 0.00 14349.16 0.27 0.64 1.25 0.28 1.37 0.52 0.77 0.00 1.31 0.00 0.50 0.00 1.53 0.75 0.01 0.03 0.08 0.01 0.00	tons/yr 263. 0. 2618. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
SSIONS REPORTS: TROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Butane n-Butane i-Butane n-Butane i-Butane n-Butane Cyclopextane n-Hextane Cyclohexane n-Hextane Cyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylene Glycol Ethylene Glycol	lbs/hr           60.16           0.00           597.88           0.01           0.03           0.05           0.01           0.03           0.05           0.01           0.03           0.05           0.01           0.02           0.03           0.00           0.02           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00	lbs/day 1443.95 0.00 14349.16 0.27 0.64 1.25 0.28 1.37 0.52 0.77 0.00 1.31 0.00 0.50 0.00 1.53 0.75 0.01 0.03 0.08 0.01 0.00 0.00	tons/yr 263. 0. 2618. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
SSIONS REPORTS: TROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Butane n-Butane i-Pentane Cyclopentane n-Hexane Cyclopexane n-Hexane Cyclopexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Givcol Ethylene Givcol Ethylene Givcol Ethylene Givcol Ethylene Givcol Ethylene Givcol	lbs/hr           60.16           0.00           597.88           0.01           0.03           0.05           0.01           0.03           0.05           0.01           0.03           0.05           0.01           0.02           0.03           0.00	lbs/day 1443.95 0.00 14349.16 0.27 0.64 1.25 0.28 1.37 0.52 0.77 0.00 1.31 0.00 1.31 0.00 0.50 0.00 1.53 0.75 0.01 0.03 0.08 0.01 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.01 0.02 0.00 0.00 0.52 0.00 0.00 0.52 0.00 0.55 0.00 0.00 0.55 0.00 0.00 0.55 0.00 0.00 0.55 0.00 0.55 0.00 0.00 0.55 0.00 0.00 0.55 0.00 0.55 0.00 0.00 0.55 0.00 0.00 0.55 0.00 0.00 0.55 0.00 0.00 0.55 0.00 0.00 0.55 0.00 0.00 0.55 0.00 0.00 0.55 0.00 0.00 0.55 0.00 0.00 0.55 0.00 0.00 0.55 0.00 0.00 0.55 0.00 0.00 0.55 0.00 0.00 0.55 0.00 0.00 0.55 0.00 0.00 0.55 0.00 0.00 0.55 0.00 0.00 0.55 0.01 0.03 0.03 0.00 0.	tons/yr 263. 0. 2618. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
SSIONS REPORTS: TROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclopexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol Water Methanol	lbs/hr           60.16           0.00           597.88           0.01           0.03           0.05           0.01           0.03           0.05           0.01           0.06           0.02           0.03           0.00	lbs/day 1443.95 0.00 14349.16 0.27 0.64 1.25 0.28 1.37 0.52 0.77 0.00 1.31 0.00 0.50 0.00 1.53 0.75 0.01 0.03 0.08 0.01 0.00 641.87 0.00	tons/yr 263. 0. 2618. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
SSIONS REPORTS: TROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Butane i-Butane i-Butane i-Pentane Cyclopentane n-Hexane Cyclopexane n-Hexane Cyclohexane n-Hexane Cyclohexane n-Hextane Methyloyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol	lbs/hr           60.16           0.00           597.88           0.01           0.03           0.05           0.01           0.03           0.05           0.01           0.02           0.03           0.00           0.02           0.03           0.00           115.65 <td>lbs/day           1443.95           0.00           14349.16           0.27           0.64           1.25           0.28           1.37           0.52           0.77           0.00           1.31           0.00           0.50           0.00           1.53           0.75           0.01           0.03           0.08           0.01           0.00           641.87           0.00           2775.55</td> <td>tons/yr 263. 0. 2618. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.</td>	lbs/day           1443.95           0.00           14349.16           0.27           0.64           1.25           0.28           1.37           0.52           0.77           0.00           1.31           0.00           0.50           0.00           1.53           0.75           0.01           0.03           0.08           0.01           0.00           641.87           0.00           2775.55	tons/yr 263. 0. 2618. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
SSIONS REPORTS: ITROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Butane i-Pentane Cyclopentane n-Hexane Cyclopexane n-Hexane Cyclohexane n-Hexane Cyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylene cene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol	lbs/hr           60.16           0.00           597.88           0.01           0.03           0.05           0.01           0.03           0.05           0.01           0.03           0.05           0.00           0.05           0.00           0.02           0.03           0.00           0.02           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           26.74           0.00           115.65           0.00	lbs/day           1443.95           0.00           14349.16           0.27           0.64           1.25           0.28           1.37           0.52           0.77           0.00           1.31           0.00           1.33           0.50           0.00           1.53           0.75           0.01           0.03           0.08           0.01           0.00           641.87           0.00           2775.55           0.00	tons/yr 263. 0. 2618. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
ISSIONS REPORTS: ITROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane Cyclopertane n-Hexane Cyclohexane n-Hexane Cyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylene celycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Water Methanol OZ SO2	lbs/hr           60.16           0.00           597.88           0.01           0.03           0.05           0.01           0.03           0.05           0.01           0.06           0.02           0.03           0.05           0.00           0.05           0.00           0.02           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           115.65           0.00           800.83	lbs/day           1443.95           0.00           14349.16           0.27           0.64           1.25           0.28           1.37           0.52           0.77           0.00           1.31           0.00           1.53           0.75           0.01           0.03           0.03           0.04           0.00           0.01           0.02           0.03           0.04           0.05           0.01           0.03           0.04           0.05           0.00           0.01           0.02           0.03           0.04           0.00           2775.55           0.00           19219.85	tons/yr 263. 0. 2618. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
SSIONS REPORTS: TROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Heptane Methylkyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Gycol Ethylene Glycol Ethylene Glycol Ethylene Glycol SOZ Total Emissions	lbs/hr           60.16           0.00           597.88           0.01           0.03           0.05           0.01           0.03           0.05           0.01           0.03           0.05           0.00           0.03           0.00           115.65           0.00           800.83	lbs/day           1443.95           0.00           14349.16           0.27           0.64           1.25           0.28           1.37           0.52           0.77           0.00           1.31           0.00           1.33           0.50           0.00           1.53           0.75           0.01           0.03           0.08           0.01           0.00           2775.55           0.00           19219.85	tons/yr 263. 0. 2618. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
SSIONS REPORTS: TROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclopexane n-Hexane Cyclopexane n-Hexane Cyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene Jylene Triethylene Glycol Ethylene Glycol Uvater Methanol O2 SO2 Total HC Emissions	lbs/hr           60.16           0.00           597.88           0.01           0.03           0.05           0.01           0.03           0.05           0.01           0.03           0.05           0.01           0.06           0.02           0.03           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           115.65           0.00           800.83           0.39           0.37	lbs/day           1443.95           0.00           14349.16           0.27           0.64           1.25           0.28           1.37           0.52           0.77           0.00           1.31           0.00           0.50           0.00           1.53           0.75           0.01           0.03           0.03           0.03           0.00           641.87           0.00           19219.85           9.31	tons/yr 263. 0. 2618. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
ITROLLED REGENERATOR EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Butane i-Pentane Cyclopentane n-Hexane Cyclopexane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2.2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol Total HC Emissions Total HC Emissions	lbs/hr           60.16           0.00           597.88           0.01           0.03           0.05           0.01           0.03           0.05           0.01           0.03           0.05           0.01           0.02           0.03           0.00           0.02           0.03           0.00	lbs/day           1443.95           0.00           14349.16           0.27           0.64           1.25           0.28           1.37           0.52           0.77           0.00           1.31           0.00           0.50           0.00           1.53           0.75           0.01           0.03           0.08           0.01           0.00           641.87           0.00           19219.85           9.31           8.40	tons/yr 263. 0. 2618. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.

Component	lbs/hr	lbs/day	tons/yr
Carbon Dioxide	1.13	27.22	4.
Hydrogen Sulfide	0.00	0.00	0.
Nitrogen	0.00	0.06	0.
Methane	0.56	13.41	2
Fthane	1 34	32 17	<u>د</u>
Pronane	2 62	62 92	J. 11
j-Rutane	0.60	14 35	2
n-Rutane	2 93	70 29	17
i-Deptano	1 16	70.35 27 DO	12
n-Pontano	1.10	27.30	כ ד
Culementane	1.73	42.04	,
cyclopentane n Havana	0.00	0.00	10
II-Hexalle Cueleboxene	3.44	82.00	13
Cyclonexane	0.00	0.00	U
n-Heptane	1.84	44.19	8
Metnyicycionexane	0.00	0.00	0
2,2,4-Trimethylpentane	0.00	0.00	C
Benzene	4.80	115.26	21
Toluene	3.76	90.17	16
Ethylbenzene	0.13	3.24	C
o-Xylene	0.27	6.48	1
m-Xylene	0.81	19.32	3
p-Xylene	0.06	1.53	C
Triethylene Glycol	0.04	0.92	C
Ethylene Glycol	0.00	0.00	0
Water	266.59	6398.22	1167
Methanol	0.00	0.00	C
02	0.00	0.00	C
SO2	0.00	0.00	(
Total Emissions	293.85	7052.47	1287
Total HC Emissions	26.12	626.96	114
Total VOC Emissions	24.22	581.38	106
Total HAP Emissions	13.28	318.67	58
	1.07	40.04	1
ROLLED FLASH TANK EMISSIONS			
ROLLED FLASH TANK EMISSIONS Component	lbs/hr	lbs/day	tons/yr
ROLLED FLASH TANK EMISSIONS Component Carbon Dioxide	lbs/hr 0.00	lbs/day 0.00	tons/yr C
ROLLED FLASH TANK EMISSIONS Component Carbon Dioxide Hydrogen Sulfide	lbs/hr 0.00 0.00	lbs/day 0.00 0.00	tons/yr C
ROLLED FLASH TANK EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen	lbs/hr 0.00 0.00 0.00	lbs/day 0.00 0.00 0.00	tons/yr C C
TROLLED FLASH TANK EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane	lbs/hr 0.00 0.00 0.00 0.00	lbs/day 0.00 0.00 0.00 0.00	tons/yr ( ( ( (
ROLLED FLASH TANK EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane	lbs/hr 0.00 0.00 0.00 0.00 0.00	lbs/day 0.00 0.00 0.00 0.00 0.00	tons/yr ( ( ( ( ( ( (
TROLLED FLASH TANK EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane	lbs/hr 0.00 0.00 0.00 0.00 0.00 0.00 0.00	lbs/day 0.00 0.00 0.00 0.00 0.00 0.00	tons/yr ( ( ( ( ( ( ( ( ( ( ( ())))))))))))))
TROLLED FLASH TANK EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane	lbs/hr 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	lbs/day 0.00 0.00 0.00 0.00 0.00 0.00 0.00	tons/yr ( ( ( ( ( ( ( ( ( ( ( ( ( ( ()))))))))
TROLLED FLASH TANK EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane	lbs/hr 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	lbs/day 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	tons/yr
TROLLED FLASH TANK EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane	lbs/hr 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	lbs/day 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	tons/yr ( ( ( ( ( ( ( ( ( ( ( ( ( ( ( ( ( ( (
TROLLED FLASH TANK EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane	lbs/hr 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00	lbs/day 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	tons/yr ( ( ( ( ( ( ( ( ( ( ( ( ( ( ( ( ( ( (
TROLLED FLASH TANK EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane	lbs/hr 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00	lbs/day 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.	tons/yr ( ( ( ( ( ( ( ( ( ( ( ( ( ( ( ( ( ( (
TROLLED FLASH TANK EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane n-Pentane Cyclopentane n-Hexane	lbs/hr 0.00	lbs/day 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00	tons/yr ( ( ( ( ( ( ( ( ( ( ( ( ( ( ( ( ( ( (
TROLLED FLASH TANK EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane Cyclopentane Cyclopentane Cyclohexane	Ibs/hr         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00	lbs/day 0.00 0.0	tons/yr
TROLLED FLASH TANK EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane n-Hexane n-Hetrane	Ibs/hr           0.00	lbs/day 0.00 0.0	tons/yr
TROLLED FLASH TANK EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclobexane Methylcyclobexane	lbs/hr           0.00	lbs/day 0.00 0.0	tons/yr
IROLLED FLASH TANK EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Pentane n-Butane i-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2.2.4-Trimethylopentane	lbs/hr           0.00	lbs/day 0.00 0.0	tons/yr
ROLLED FLASH TANK EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane Cyclopentane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene	Ibs/hr           0.00	Ibs/day 0.00 0.0	tons/yr
TROLLED FLASH TANK EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluana	Ibs/hr           0.00	lbs/day 0.00 0.0	tons/yr
TROLLED FLASH TANK EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane i-Pentane Cyclopentane Cyclopentane Cyclopentane Cyclopentane Cyclopexane 2,2,4-Trimethylpentane Benzene Toluene Toluene Ethylbenzana	lbs/hr           0.00	lbs/day 0.00 0.0	tons/yr
IROLLED FLASH TANK EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane i-Pentane Cyclopentane n-Hexane Cyclohexane n-Hexane Cyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene Chylone	lbs/hr           0.00	lbs/day 0.00 0.0	tons/yr
IROLLED FLASH TANK EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Pentane Cyclopentane Cyclopentane Cyclopentane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene	Ibs/hr           0.00	lbs/day         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00	tons/yr
TROLLED FLASH TANK EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Heptane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene	Ibs/hr           0.00	lbs/day         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00	tons/yr
TROLLED FLASH TANK EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane Cyclopentane Cyclopentane Cyclopentane Cyclopexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene	Ibs/hr           0.00	lbs/day         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00	tons/yr
TROLLED FLASH TANK EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Butane n-Pentane Cyclohexane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol	lbs/hr           0.00	lbs/day         0.00           0.00         0.00	tons/yr
TROLLED FLASH TANK EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Pentane Cyclopentane Cyclopentane Cyclopentane Cyclopentane Cyclopentane Cyclopexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol	Ibs/hr           0.00	lbs/day           0.00	tons/yr
TROLLED FLASH TANK EMISSIONS  Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane n-Pentane Cyclopentane n-Pentane Cyclopentane Cyclopentane Cyclopexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Tritethylene Glycol Ethylene Glycol	Ibs/hr           0.00	lbs/day         0.00           0.00         0.00	tons/yr
IROLLED FLASH TANK EMISSIONS  Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclopentane Cyclopentane Cyclopentane N-Hexane Cyclopentane Senzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Water Methanol	lbs/hr           0.00	lbs/day         0.00           0.00         0.00	tons/yr
IROLLED FLASH TANK EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Pentane n-Butane i-Pentane n-Pentane Cyclopentane Cyclopentane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol	Ibs/hr           0.00	lbs/day         0.00           0.00         0.00	tons/yr
IROLLED FLASH TANK EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Butane n-Pentane n-Pentane Cyclopentane Cyclopentane Cyclopentane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Glycol Ethylene Glycol Ethylene Glycol	Ibs/hr           0.00	lbs/day           0.00	tons/yr
Triethylene Glycol Ethylene Glycol Total Emissions Erhane Prop	Ibs/hr           0.00	lbs/day         0.00           0.00         0.00	tons/yr
TROLLED FLASH TANK EMISSIONS  Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane n-Pentane Cyclopentane n-Heptane n-Heptane Cyclobexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene mXylene p-Xylene Giycol Ethylene Giycol Ethylene Giycol Ethylene Giycol So2 Total Emissions Total HC Emissions	Ibs/hr           0.00	lbs/day           0.00	tons/yr
IROLLED FLASH TANK EMISSIONS  Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Sog Total Emissions Total HC Emissions Total HC Emissions	Ibs/hr           0.00	lbs/day           0.00	tons/yr
IROLLED FLASH TANK EMISSIONS  Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclokexane 2,2,4-Trimethylpentane Benzene Toluene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene m-Xylene Strighten Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol So2 Total HCE Emissions Tot	Ibs/hr           0.00	lbs/day           0.00	tons/yr c c c c c c c c c c c c c

Component	lbs/hr	lbs/day	tons/vr
Carbon Dioxide	3.74	89.86	16.
Hydrogen Sulfide	0.00	0.00	0.
Nitrogen	0.24	5.66	1
Methane	15 41	369.89	67
Fthane	11 66	279.85	51
Pronane	12.50	300 43	51
i_Rutano	2 12	500.45	<del>ب</del> ر
n_Rutane	7 28	174 65	21
i-Dutatie	1 01	1/4.05	21
n Dentane	1.51	45.81	10
Gulenentane	2.40	35:40	10
cyclopentane	0.00	0.00	10
Cuelebovane	2.47	59.22	10
Cyclonexane	0.00	0.00	L. L
n-Heptane	0.84	20.19	3
Metnyicycionexane	0.00	0.00	C
2,2,4-Trimethylpentane	0.00	0.00	(
Benzene	0.27	6.37	1
Toluene	0.12	2.81	C
Ethylbenzene	0.00	0.06	(
o-Xylene	0.00	0.09	C
m-Xylene	0.02	0.37	C
p-Xylene	0.00	0.03	C
Triethylene Glycol	0.00	0.06	C
Ethylene Glycol	0.00	0.00	C
Water	0.95	22.80	4
Methanol	0.00	0.00	C
02	0.00	0.00	C
SO2	0.00	0.00	
Total Emissions	62.07	1489.80	271
Total HC Emissions	57.15	1371.49	250
Total VOC Emissions	30.07	721.75	131
Total HAP Emissions	2.87	68.94	12
Total GHG Emissions	19.16	459.75	83
MBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component	lbs/hr	lbs/day	tons/yr
IBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide	lbs/hr 63.91	lbs/day 1533.80	tons/yr 279
MBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide	lbs/hr 63.91 0.00	lbs/day 1533.80 0.00	tons/yr 279
ABINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen	lbs/hr 63.91 0.00 598.12	lbs/day 1533.80 0.00 14354.82	tons/yr 275 0 2619
IBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane	lbs/hr 63.91 0.00 598.12 15.42	lbs/day 1533.80 0.00 14354.82 370.15	tons/yr 279 2619 67
IBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane	lbs/hr 63.91 0.00 598.12 15.42 11.69	lbs/day 1533.80 0.00 14354.82 370.15 280.49	tons/yr 279 2619 67 51
IBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane	lbs/hr 63.91 0.00 598.12 15.42 11.69 12.57	lbs/day 1533.80 0.00 14354.82 370.15 280.49 301.68	tons/yr 279 2619 67 51 55
ABINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane	lbs/hr 63.91 0.00 598.12 15.42 11.69 12.57 2.19	lbs/day 1533.80 0.00 14354.82 370.15 280.49 301.68 52.53	tons/yr 279 ( 2619 51 51 55
IBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane	lbs/hr 63.91 0.00 598.12 15.42 11.69 12.57 2.19 7.33	lbs/day 1533.80 0.00 14354.82 370.15 280.49 301.68 52.53 176.02	tons/yr 275 2615 51 51 52 32
IBINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane	lbs/hr 63.91 0.00 598.12 15.42 11.69 12.57 2.19 7.33 1.93	lbs/day 1533.80 0.00 14354.82 370.15 280.49 301.68 52.53 176.02 46.33	tons/yr 279 2619 67 59 9 9 9 33 8
ABINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane	lbs/hr 63.91 0.00 598.12 15.42 11.69 12.57 2.19 7.33 1.93 2.51	lbs/day 1533.80 0.00 14354.82 370.15 280.49 301.68 52.53 176.02 46.33 60.17	tons/yr 275 2615 67 51 55 52 32 8 10
ABINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Butane i-Pentane n-Pentane Cyclopentane	lbs/hr 63.91 0.00 598.12 15.42 11.69 12.57 2.19 7.33 1.93 2.51 0.00	Ibs/day           1533.80           0.00           14354.82           370.15           280.49           301.68           52.53           176.02           46.33           60.17           0.00	tons/yr 275 2619 515 55 55 52 32 8 10 0
ABINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane	lbs/hr 63.91 0.00 598.12 15.42 11.69 12.57 2.19 7.33 1.93 2.51 0.00 2.52	bs/day 1533.80 0.00 14354.82 370.15 280.49 301.68 52.53 176.02 46.33 60.17 0.00 60.52	tons/yr 275 2619 677 55 55 32 8 10 0 0
ABINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane i-Pentane Cyclopentane n-Hexane Cyclopexane	lbs/hr 63.91 0.00 598.12 15.42 11.69 12.57 2.19 7.33 1.93 2.51 0.00 2.52 0.00	lbs/day 1533.80 0.00 14354.82 370.15 280.49 301.68 52.53 176.02 46.33 60.17 0.00 60.52 0.00	tons/yr 275 2615 55 32 32 10 10 11 10 10 11 10 10 10 10 10 10 10
ABINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclobexane n-Hexane	lbs/hr 63.91 0.00 598.12 15.42 11.69 12.57 2.19 7.33 1.93 2.51 0.00 2.52 0.00 0.86	lbs/day 1533.80 0.00 14354.82 370.15 280.49 301.68 52.53 176.02 46.33 60.17 0.00 60.52 0.00 20.70	tons/yr 275 66 55 55 8 10 11 12 12 12 12 12 12 12 12 12 12 12 12
ABINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane	lbs/hr 63.91 0.00 598.12 15.42 11.69 12.57 2.19 7.33 1.93 2.51 0.00 2.52 0.00 0.86 0.00	Ibs/day           1533.80           0.00           14354.82           370.15           280.49           301.68           52.53           176.02           46.33           60.17           0.00           60.52           0.00           20.70           0.00	tons/yr 275 615 55 55 9 32 10 11 11 11 11 11 11 11 11 11 11 11 11
ABINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclopexane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane	Ibs/hr         63.91           0.00         598.12           15.42         11.69           12.57         2.19           7.33         1.93           2.51         0.00           2.52         0.00           0.86         0.00           0.00         0.00	Ibs/day           1533.80           0.00           14354.82           370.15           280.49           301.68           52.53           176.02           46.33           60.17           0.00           60.52           0.00           20.70           0.00           0.00           0.00	tons/yr 275 2619 61 55 55 32 8 10 ( ( 11 11 ( 3 3 2 8 11 ( 12 11 11 ( 3 3 3 11 ( 12 11 11 11 11 11 11 11 11 11 11 11 11
ABINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane Cyclopentane n-Hextane Cyclohexane N-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene	lbs/hr 63.91 0.00 598.12 11.69 12.57 2.19 7.33 1.93 2.51 0.00 2.52 0.00 0.86 0.00 0.86 0.00 0.33	lbs/day 1533.80 0.00 14354.82 370.15 280.49 301.68 52.53 176.02 46.33 60.17 0.00 60.52 0.00 20.70 0.00 7.90	tons/yr 279 66 55 55 33 4 10 ( 11 ( 12 ( 12) 10 ( 12) 10 ( 12) 10 10 10 10 10 10 10 10 10 10 10 10 10
ABINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nittrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene	lbs/hr 63.91 0.00 598.12 15.42 11.69 12.57 2.19 7.33 1.93 2.51 0.00 2.52 0.00 0.86 0.00 0.86 0.00 0.33 0.15	lbs/day 1533.80 0.00 14354.82 370.15 280.49 301.68 52.53 176.02 46.33 60.17 0.00 60.52 0.00 20.70 0.00 7.90 3.56	tons/yr 279 66 55 55 59 30 8 10 ( 0 ( 11 12 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
ABINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzenel	lbs/hr           63.91           0.00           598.12           15.42           11.69           12.57           2.19           7.33           1.93           2.51           0.00           0.86           0.00           0.33           0.15           0.00	Ibs/day           1533.80           0.00           14354.82           370.15           280.49           301.68           52.53           176.02           46.33           60.17           0.00           60.52           0.00           20.70           0.00           7.90           3.56           0.08	tons/yr 275 615 55 55 9 32 10 11 11 11 11 11 11 11 11 11 11 11 11
ABINED REGENERATOR VENT/FLASH GAS EMISSIONS  Component Carbon Dioxide Hydrogen Sulfide Nitrogen Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Yvlene	Ibs/hr           63.91           0.00           598.12           15.42           11.69           12.57           2.19           7.33           1.93           2.51           0.00           2.52           0.00           0.86           0.00           0.33           0.15           0.00	Ibs/day           1533.80           0.00           14354.82           370.15           280.49           301.68           52.53           176.02           46.33           60.17           0.00           60.52           0.00           20.70           0.00           7.90           3.56           0.08           0.12	tons/yr 275 6 55 55 6 33 8 10 11 0 0 0 12 0 0 0 0 0 0 0 0 0 0 0 0
ABINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane Cyclopentane n-Hextane Cyclopentane n-Hextane Cyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Yulene	lbs/hr           63.91           0.00           598.12           15.42           11.69           12.57           2.19           7.33           1.93           2.51           0.00           2.52           0.00           0.86           0.00           0.33           0.15           0.00           0.02	Ibs/day           1533.80           0.00           14354.82           370.15           280.49           301.68           52.53           176.02           46.33           60.17           0.00           60.52           0.00           20.70           0.00           7.90           3.56           0.08           0.12	tons/yr 275 67 51 55 32 32 32 48 10 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
ABINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane Cyclopentane n-Heptane N-Heptane Vethylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene o-Xylene	lbs/hr           63.91           0.00           598.12           15.42           11.69           12.57           2.19           7.33           1.93           2.51           0.00           2.52           0.00           0.86           0.00           0.33           0.15           0.00           0.02	Ibs/day           1533.80           0.00           14354.82           370.15           280.49           301.68           52.53           176.02           46.33           60.17           0.00           60.52           0.00           20.70           0.00           7.90           3.56           0.08           0.12           0.44           0.04	tons/yr 275 67 51 55 9 32 8 10 0 0 11 10 0 0 0 0 0 0 0 0 0 0 0 0
ABINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfide Nittrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Trigethylane Sciercel	Ibs/hr 63.91 0.00 598.12 15.42 11.69 12.57 2.19 7.33 1.93 2.51 0.00 2.52 0.00 0.86 0.00 0.86 0.00 0.00 0.33 0.15 0.00 0.00 0.00 0.00 0.00 0.00	Ibs/day           1533.80           0.00           14354.82           370.15           280.49           301.68           52.53           176.02           46.33           60.17           0.00           20.70           0.00           20.70           0.00           7.90           3.56           0.08           0.12           0.44           0.04	tons/yr 275 67 51 55 62 32 8 10 0 0 11 11 0 0 0 0 0 0 0 0 0 0 0 0
ABINED REGENERATOR VENT/FLASH GAS EMISSIONS  Component  Carbon Dioxide Hydrogen Sulfide Nitrogen Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane Cyclopentane n-Pentane Cyclopentane n-Hexane Cyclopexane n-Hexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene P-Xylene Triethylene Glycol Ethylene Glycol	Ibs/hr           63.91           0.00           598.12           15.42           11.69           12.57           2.19           7.33           1.93           2.51           0.00           2.52           0.00           0.86           0.00           0.33           0.15           0.00           0.02           0.00           0.02           0.00	Ibs/day           1533.80           0.00           14354.82           370.15           280.49           301.68           52.53           176.02           46.33           60.17           0.00           60.52           0.00           20.70           0.00           7.90           3.56           0.08           0.12           0.44           0.04           0.06           0.00	tons/yr 275 67 55 55 55 52 32 8 10 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
Zerbon Dioxide Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane i-Pentane cyclopentane n-Hextane Cyclopentane n-Hextane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene p-Xylene Jylene Gycol Ethylene Glycol Ethylene Glycol Ethylene Glycol	lbs/hr           63.91           0.00           598.12           15.42           11.69           12.57           2.19           7.33           1.93           2.51           0.00           2.52           0.00           0.86           0.00           0.33           0.15           0.00           0.02           0.00	Ibs/day           1533.80           0.00           14354.82           370.15           280.49           301.68           52.53           176.02           46.33           60.17           0.00           60.52           0.00           20.70           0.00           7.90           3.56           0.08           0.12           0.44           0.04           0.06           0.07	tons/yr 275 2615 32 32 32 32 32 32 32 32 32 32 32 32 32
Zerbon Dioxide Component Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane Cyclopentane n-Heptane Cyclohexane n-Heptane Vethylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylene O-Xylene Triethylene Glycol Ethylene Cyclopexane Cyclopexane Cyclopexane Cyclopexane Cyclohexane Cyclohex	lbs/hr           63.91           0.00           598.12           15.42           11.69           12.57           2.19           7.33           1.93           2.51           0.00           2.52           0.00           0.86           0.00           0.33           0.15           0.00           0.02           0.00	Ibs/day           1533.80           0.00           14354.82           370.15           280.49           301.68           52.53           176.02           46.33           60.17           0.00           60.52           0.00           20.70           0.00           7.90           3.56           0.08           0.12           0.44           0.04           0.06           0.00	tons/yr 275 2612 375 375 375 375 375 375 375 375 375 375
Carbon Dioxide           Carbon Dioxide           Hydrogen Sulfide           Hydrogen Sulfide           Nitrogen           Methane           Ethane           Propane           i-Butane           n-Butane           i-Pentane           n-Pentane           Cyclopentane           n-Heptane           n-Heptane           n-Heptane           Nethylcyclohexane           2,2,4-Trimethylpentane           Benzene           Tollene           Ethylene Glycol           Ethylene Glycol           Ethylene Glycol           Water           Methanol	Ibs/hr           63.91           0.00           598.12           15.42           11.69           12.57           2.19           7.33           1.93           2.51           0.00           2.52           0.00           0.86           0.00           0.33           0.15           0.00           11.5 m	Ibs/day           1533.80           0.00           14354.82           370.15           280.49           301.68           52.53           176.02           46.33           60.17           0.00           20.70           0.00           20.70           0.00           20.70           0.00           20.70           0.00           20.70           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.012           0.44           0.04           0.06           0.00           664.67           0.00	tons/yr 275 67 51 55 52 8 8 10 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
Sector           Component           Carbon Dioxide           Hydrogen Sulfide           Hydrogen Sulfide           Nitrogen           Methane           Ethane           Propane           i-Butane           n-Butane           i-Pentane           Cyclopentane           n-Hexane           Cyclopextane           n-Hexa	lbs/hr           63.91           0.00           598.12           15.42           11.69           12.57           2.19           7.33           1.93           2.51           0.00           2.52           0.00           0.86           0.00           0.33           0.15           0.00           15.65	Ibs/day           1533.80           0.00           14354.82           370.15           280.49           301.68           52.53           176.02           46.33           60.17           0.00           60.52           0.00           20.70           0.00           7.90           3.56           0.08           0.12           0.44           0.04           0.06           0.00           664.67           0.00           2775.55	tons/yr 275 2619 555 55 52 32 8 10 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
Subject of the second	Ibs/hr           63.91           0.00           598.12           15.42           11.69           12.57           2.19           7.33           1.93           2.51           0.00           2.52           0.00           0.86           0.00           0.33           0.15           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           115.65           0.00           862.90	Ibs/day           1533.80           0.00           14354.82           370.15           280.49           301.68           52.53           176.02           46.33           60.17           0.00           60.52           0.00           20.70           0.00           7.90           3.56           0.08           0.12           0.44           0.04           0.06           0.00           2775.55           0.00           2775.55           0.00           20709.65	tons/yr 275 2619 372 372 372 3775 3775 3775 3775 3775
Summer Sector           Component           Carbon Dioxide           Hydrogen Sulfide           Nitrogen           Nitrogen           Methane           Ethane           Propane           i-Butane           n-Butane           i-Pentane           Cyclopentane           n-Hexane           Cyclopextane           n-Yelpen           m-Xylene           p-Xylene <td>Ibs/hr           63.91           0.00           598.12           15.42           11.69           12.57           2.19           7.33           1.93           2.51           0.00           2.52           0.00           0.86           0.00           0.33           0.15           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           115.65           0.00           862.90</td> <td>Ibs/day           1533.80           0.00           14354.82           370.15           280.49           301.68           52.53           176.02           46.33           60.17           0.00           20.70           0.00           20.70           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.02           0.03           0.04           0.06           0.00           2070           664.67           0.00           20775.55           0.00           20709.65</td> <td>tons/yr 275 2619 372 372 375 375 3775</td>	Ibs/hr           63.91           0.00           598.12           15.42           11.69           12.57           2.19           7.33           1.93           2.51           0.00           2.52           0.00           0.86           0.00           0.33           0.15           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           115.65           0.00           862.90	Ibs/day           1533.80           0.00           14354.82           370.15           280.49           301.68           52.53           176.02           46.33           60.17           0.00           20.70           0.00           20.70           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.02           0.03           0.04           0.06           0.00           2070           664.67           0.00           20775.55           0.00           20709.65	tons/yr 275 2619 372 372 375 375 3775
ABINED REGENERATOR VENT/FLASH GAS EMISSIONS           Carbon Dioxide           Hydrogen Sulfide           Nikrogen           Nikrogen           Methane           Ethane           Propane           i-Butane           n-Butane           i-Pentane           Cyclopentane           n-Hextane           Cyclopexane           n-Xylene           p-Xylene           n-Xylene           p-Xylene           n-Xylene           p-Xylene           n-Xylene           p-Xylene           n-Xylene           p-Xylene           n-Xylene           p-Xylene           n-Xylene           p-	lbs/hr           63.91           0.00           598.12           15.42           11.69           12.57           2.19           7.33           1.93           2.51           0.00           2.52           0.00           0.86           0.00           0.33           0.15           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           115.65           0.00           862.90           57.53	Ibs/day           1533.80           0.00           14354.82           370.15           280.49           301.68           52.53           176.02           46.33           60.17           0.00           60.52           0.00           20.70           0.00           7.90           3.56           0.08           0.12           0.44           0.04           0.06           0.00           20.70           0.00           7.90           3.56           0.08           0.12           0.44           0.04           0.06           0.00           20705.55           0.00           20709.65           1380.80	tons/yr 275 2615 32 32 32 32 32 32 32 32 32 32 32 32 32
ABINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Hydro	lbs/hr           63.91           0.00           598.12           15.42           11.69           12.57           2.19           7.33           1.93           2.51           0.00           2.52           0.00           0.86           0.00           0.33           0.15           0.00           0.02           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           115.65           0.00           862.90           57.53           30.42	Ibs/day           1533.80           0.00           14354.82           370.15           280.49           301.68           52.53           176.02           46.33           60.17           0.00           60.52           0.00           20.70           0.00           7.90           3.56           0.08           0.12           0.44           0.04           0.06           0.00           2775.55           0.00           20709.65           1380.80           730.15	tons/yr 279 67 2619 67 51 55 52 8 10 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
ABINED REGENERATOR VENT/FLASH GAS EMISSIONS Component Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Ethane Propane i-Butane i-Pentane n-Butane i-Pentane Cyclopexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene O-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol Triethylene Glycol Triethylene Glycol Total Emissions Total HC Emissions	Ibs/hr           63.91           0.00           598.12           15.42           11.69           12.57           2.19           7.33           1.93           2.51           0.00           2.52           0.00           0.86           0.00           0.33           0.15           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           0.00           115.65           0.00           115.65           0.00           862.90           57.53           3.03	Ibs/day           1533.80           0.00           14354.82           370.15           280.49           301.68           52.53           176.02           46.33           60.17           0.00           60.52           0.00           20.70           0.00           20.70           0.00           20.70           0.00           20.70           0.00           20.70           0.00           20.70           0.00           0.00           20.70           0.00           20.70           0.00           212           0.44           0.04           0.05           0.00           2775.55           0.00           20709.65           1380.80           730.15           72.66	tons/yr 275 2619 375 39 32 38 30 00 01 11 00 00 01 11 00 00 00 00 00 00

EQUIPMENT REPORTS:			
BTEX CONDENSER			
BTEX CONDENSER	Condenser Outlet Temperature:	120.00 deg. F	
	Condenser Pressure:	14.10 psia	
	Condenser Duty:	-0.29 MMBTU/hr	
	Hydrocarbon Recovery:	0.55 bbls/day	
	Produced Water:	18.23 bbls/day	
	VOC Control Efficiency:	27.64 %	
	BTEX Control Efficiency:	41.70 %	
	Dissolved Hydrocarbons in Water:	877.02 mg/L	
Component	Emitted (wt. %)	Condensed (wt. %)	
Carbon Dioxide	98.74	1.26	
Hydrogen Sulfide	0.00	0.00	
Nitrogen	99.95	0.05	
Ethane	99.61	0.39	
Propane	99.05	0.95	
i-Butane	98.15	1.85	
n-Butane	97.16	2.84	
i-Pentane	93.21	6.79	
n-Pentane	91.37	8.63	
Cyclopentane	0.00	0.00	
il-Hexane Cyclobeyane	19.05	20.95	
n-Heptane	56.68	43.32	
Methylcyclohexane	0.00	0.00	
2,2,4-Trimethylpentane	0.00	0.00	
Benzene	66.49	33.51	
Toluene	41.84	58.16	
Ethylbenzene	19.51	80.49	
o-Xylene	20.00	80.00	
n-Xylene	20 13	79.87	
Triethylene Glycol	0.00	100.00	
Ethylene Glycol	0.00	0.00	
Water	0.33	99.67	
Methanol	0.00	0.00	
02	0.00	0.00	
	0.00	0.00	
ABSORBER			
	Absorber Stages:	3.00	
	Dry Gas Dew Point:	4.55 lb H2O/MMSCF	
	Temperature:	120.00 deg. F	
	Pressure:		
	TEG Losses with Dry Gas:	2.35 lb/hr	
	Wet Gas Water Content:	69.22 lb H2O/MMSCF	
	Lean Glycol Recirc. Ratio:	1.47 gal/lb H2O	
Component	In Dry Gas (%)	Absorbed in Glycol (%)	
Carbon Dioxide	99.89	0.11	
Hydrogen Sulfide	-	-	
Nitrogen	00.00 100.00	0.00	
Ethane	99.97	0.03	
Propane	99.96	0.04	
i-Butane	99.96	0.04	
n-Butane	99.94	0.06	
i-Pentane			
	99.93	0.07	
n-Pentane	99.93 99.92	0.07	
n-Pentane Cyclopentane	99.93 99.92 - -	0.07 0.08 -	
n-Pentane Cyclopentane n-Hexane Cyclohexane	99.93 99.92 - 99.89	0.07 0.08 -	
n-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane	99.93 99.92 - 99.89 - 99.85	0.07 0.08 - 0.11 - 0.15	
n-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane	99.93 99.92 - 99.85 - 99.85 -	0.07 0.08 - 0.11 - 0.15	
n-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane	99.93 99.92 - 99.85 - 99.85 - -	0.07 0.08 - 0.11 - 0.15 -	
n-Pentane Cyclopentane n-Hexane Scyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene	99.93 99.92 - 99.85 - 99.85 - - 97.10	0.07 0.08 - 0.11 - 0.15 - - 2.90	
n-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene	99.93 99.92 99.89 - 99.85 - 97.10 95.92	0.07 0.08 - 0.11 - 0.15 - - 2.90 4.08	
n-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene	99.93 99.92 - 99.89 - 99.85 - 97.10 95.92 95.33 97.40	0.07 0.08 - 0.11 - 0.15 - - 2.90 4.08 4.67	
n-Pentane Cyclopentane - N-Hexane Cyclohexane - N-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m: Xulene	99.93 99.92 - 99.89 - 99.85 - 97.10 95.92 95.33 93.46 93.46	0.07 0.08 - 0.11 - 0.15 - 2.90 4.08 4.67 6.54 4.77	
n-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene p-Xylene	99.93 99.92 - 99.89 - 99.85 - 97.10 95.92 95.33 93.46 95.23 95.23 95.23	0.07 0.08 - 0.11 - 0.15 - - 2.90 4.08 4.67 6.54 4.77 4.52	
n-Pertane Cyclopertane n-Hexane Cyclohexane Methylcyclohexane 2,2,4-Trimethylpertane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Giycol	99.93 99.92 - 99.89 - 99.85 - 97.10 95.92 95.33 93.46 95.23 95.48 95.23 95.48	0.07 0.08 - 0.11 - 0.15 - - 2.90 4.08 4.67 6.54 4.77 4.52 99.94	
n-Pentane Cyclopentane n-Hexane Cyclohexane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol	99.93 99.92 - 99.89 - 99.85 - 99.85 - 97.10 95.92 95.33 93.46 95.23 95.48 0.0.0	0.07 0.08 - 0.11 - 0.15 - - 2.90 4.08 4.67 6.54 4.77 4.52 99.94	
n-Pentane Cyclopentane n-Hexane Cyclohexane Z,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol	99.93 99.92 - 99.89 - 99.85 - 99.85 - 97.10 95.92 95.33 93.46 95.23 95.48 0.006 - -	0.07 0.08 - 0.11 - 0.15 - 2.90 4.08 4.67 6.54 4.77 4.52 99.94	
n-Pentane Cyclopentane n-Hexane Cyclohexane Cyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Water Methanol	99.93 99.92 - 99.85 - 99.85 - 97.10 95.92 95.33 93.46 95.23 93.46 95.23 95.48 0.06 - -	0.07 0.08 - 0.11 - 0.15 - 2.90 4.08 4.67 6.54 4.77 4.52 99.94 - 94.16	
n-Pentane Cyclopentane n-Hexane Cyclohexane 2,2,4-Trimethylpentane Benzene Ethylibenzene o-Xylene p-Xylene Triethylene Glycol Ethylibene Glycol Uwater Methanol O2	99.93 99.92 - 99.89 - 99.85 - 97.10 95.92 95.33 93.46 95.23 95.48 0.06 - 5.84 -	0.07 0.08 - 0.11 - 0.15 - 2.90 4.08 4.67 6.54 4.77 4.52 99.94 - 94.16 -	

		Flash Temperature:	160 deg. F
		Flash Pressure:	45 psig
Component		Flashed (wt. %)	Left in Glycol (wt. %)
	Carbon Dioxide	76.75	23.25
	Hydrogen Sulfide	0.00	0.00
	Nitrogen	98.99	1.01
	Methane	96.50	3.50
	Ethane	89.69	10.31
	Propane	82.68	17.32
	i-Butane	78.45	21.55
	n-Butane	71.27	28.73
	i-Pentane	62.15	37.85
	n-Pentane	58.56	41.44
	Cyclopentane	0.00	0.00
	n-Hexane	41.74	58.26
	Cyclohexane	0.00	0.00
	n-Heptane	31.37	68.63
	Methylcyclohexane	0.00	0.00
	2,2,4-Trimethylpentane	0.00	0.00
	Benzene	5.24	94.76
	Toluene	3.02	96.98
	Ethylbenzene	1.89	98.11
	o-Xylene	1.37	98.63
	m-Xylene	1.85	98.15
	p-Xylene	1.95	98.05
	Triethylene Glycol	0.00	100.00
	Ethylene Glycol	0.00	0.00
	Water	0.31	99.69
	Methanol	0.00	0.00
	02		
	02	0.00	0.00
	502 S02	0.00	0.00 0.00
RATOR Component	502 502	0.00 0.00 Recovered in Glycol (%)	0.00 0.00 Distilled Overhead (%)
ERATOR Component	SO2 SO2	0.00 0.00 Recovered in Glycol (%) 0.00	0.00 0.00 Distilled Overhead (%) 100.00
Component	Carbon Dioxide Hydrogen Sulfide	0.00 0.00 Recovered in Glycol (%) 0.00	0.00 0.00 Distilled Overhead (%) 100.00
ERATOR Component	Carbon Dioxide Hydrogen Sulfide Nitrogen	0.00 0.00 Recovered in Glycol (%) 0.00 - 0.00	0.00 0.00 Distilled Overhead (%) 100.00 - 100.00
ERATOR Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane	0.00 0.00 Recovered in Glycol (%) 0.00 - 0.00 0.00	0.00 0.00 Distilled Overhead (%) 100.00 - 1000.00 100.00
ERATOR Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane	0.00 0.00 Recovered in Glycol (%) 0.00 - 0.00 0.00 0.00	0.00 0.00 Distilled Overhead (%) 100.00 100.00 100.00 100.00
RATOR Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane	0.00 0.00 Recovered in Glycol (%) 0.00 - 0.00 0.00 0.00 0.00	0.00 0.00 Distilled Overhead (%) 100.00 100.00 100.00 100.00 100.00
RATOR Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane	0.00 0.00 Recovered in Glycol (%) 0.00 - 0.00 0.00 0.00 0.00 0.00	0.00 0.00 Distilled Overhead (%) 100.00 100.00 100.00 100.00 100.00 100.00
ERATOR Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane	0.00 0.00 Recovered in Glycol (%) - 0.00 0.00 0.00 0.00 0.00 0.00 0.00	0.00 0.00 Distilled Overhead (%) 100.00 - 100.00 100.00 100.00 100.00 100.00 100.00
ERATOR Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane	0.00 0.00 Recovered in Glycol (%) 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00	0.00 0.00 Distilled Overhead (%) 100.00 - 100.00 100.00 100.00 100.00 100.00 100.00 100.00
RATOR Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane	0.00 0.00 Recovered in Glycol (%) 0.00 - 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00	0.00 0.00 Distilled Overhead (%) 100.00 - 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00
ERATOR Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane	0.00 0.00 Recovered in Glycol (%) 0.00	0.00 0.00 Distilled Overhead (%) 100.00 - 100.00 100.00 100.00 100.00 100.00 100.00 100.00 - -
ERATOR Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane	0.00 0.00 Recovered in Glycol (%) 0.00	0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.0
ERATOR Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclopexane	0.00 0.00 Recovered in Glycol (%) 0.00	0.00 0.00 0.00 0.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 - - -
ERATOR Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclohexane n-Hentane	0.00 0.00 Recovered in Glycol (%) 0.00	0.00 0.00 0.00 Distilled Overhead (%) 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 - 100.00 - 100.00
ERATOR Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopexane n-Hexane Cyclopexane	0.00 0.00 Recovered in Glycol (%) 0.00	0.00 0.00 0.00 Distilled Overhead (%) 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 - 100.00 - - - - - - - - - - - - -
ERATOR Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2.2.4-Trimethylopentane	0.00 0.00 Recovered in Glycol (%) 0.00	0.00 0.00 0.00 Distilled Overhead (%) 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 - 100.00 - 100.00 - 100.00 - - - - - - - - - - - - -
ERATOR Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene	0.00 0.00 Recovered in Glycol (%) 0.00	0.00 0.00 0.00 0.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 - 100.00 - 100.00 - - - - - - - - - - - - -
ERATOR Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Pentane Cyclopentane n-Hexane Cyclopexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene	0.00 0.00 Recovered in Glycol (%) 0.00	0.00 0.00 0.00 0.00 0.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 - 100.00 - - - - - - - - - - - - -
ERATOR Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopexane n-Hexane Cyclopexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene	0.00 0.00 Recovered in Glycol (%) 0.00	0.00 0.00 0.00 Distilled Overhead (%) 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 - 100.00 - 100.00 - 100.00 - 100.00 - 100.00 - 100.00 - 100.00 - - - - - - - - - - - - -
ERATOR Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xvlene	0.00 0.00 Recovered in Glycol (%) 0.00 0.02 0.12 0.12 0.13 0.14	0.00 0.00 0.00 0.00 0.00 0.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 - - - - - - - - - - - - -
ERATOR Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene	0.00 0.00 Recovered in Glycol (%) 0.00	0.00 0.00 0.00 0.00 0.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 - - - - - - - - - - - - -
ERATOR Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Pentane Cyclopentane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Ethylbenzene O-Xylene m-Xylene n-Xylene	0.00 0.00 Recovered in Glycol (%) 0.00 0.12 0.45	0.00 0.00 0.00 0.00 0.00 0.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 - 100.00 - - - - - - - - - - - - -
ERATOR Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene p-Xylene p-Xylene p-Xylene	0.00 0.00 Recovered in Glycol (%) 0.00	0.00 0.00 0.00 Distilled Overhead (%) 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 - - - - - - - - - - - - -
ERATOR Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclopentane n-Hexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Grifthylene Glycol Ethylane Glycol	0.00 0.00 Recovered in Glycol (%) 0.00 1.00 0.00 0.00 0.00 1.00 0.00 0.00 0.00 0.00 0.00 1.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 1.00 0.02 0.12 0.49 1.14 0.52 0.46 10.00	0.00 0.00 0.00 0.00 0.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 - - - - - - - - - - - - -
ERATOR Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Pentane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Gricthylene Glycol Ethylene Glycol	0.00 0.00 Recovered in Glycol (%) 0.00 0.12 0.46 100.00 0.14 0.14 0.52 0.14 0.52 0.14 0.52 0.14 0.52 0.14 0.52 0.14 0.52 0.14 0.52 0.14 0.52 0.14 0.52 0.14 0.52 0.14 0.52 0.5	0.00 0.00 0.00 0.00 0.00 0.00 100.00 - 100.00 - 100.00 - 100.00 - 100.00 - 100.00 - - - 99.98 99.51 99.54 99.54 0.00 - - - - - - - - - - - - -
ERATOR Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Ethylbenzene o-Xylene Toluene Ethylbenzene o-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol	0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           0.00         0.00           1.00         0.00           0.12         0.49           1.14         0.52           0.46         100.00           11.42         0.42	0.00 0.00 0.00 0.00 0.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 0.00
ERATOR Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopexane n-Hexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol	0.00 0.00 Recovered in Glycol (%) 0.00 0.02 0.12 0.49 1.14 0.52 0.46 10.00 0.49 1.142 0.44 1.142 0.42 1.142 0.44 1.142 0.00 0.00 0.00 0.44 1.142 0.00 0.00 0.00 0.44 1.142 0.44 1.142 0.452 0.452 1.142 0.452 1.142 0.452 1.142 1.142 0.452 1.142 1.	0.00 0.00 0.00 Distilled Overhead (%) 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 100.00 - - - - - - - - - - - - -

VET GAS STREAM           Temperature:         110.00 deg F           Pressure:         1114.40 psia           Flow Rate:         99.05 MMSCFD           Component         Control           Carbon Dioxide         Nitrogen           Hydrogen Sulfide         Nitrogen           Nitrogen         Methane           Ethane         Propane           i-Butane         n-Butane           n-Butane         n-Butane           i-Pentane         Cyclopentane           n-Hexane         Cyclopentane           Cyclopentane         n-Hexane           Cyclopentane         n-Hexane           Cyclopentane         n-Hexane           Cyclopentane         n-Heytane           Display         Benzene           Toluene         Ethylbenzene           o-Xylene         m-Xylene           m-Xylene         p-Xylene           Methanol         O2           SO2         SO2	c. (mol%) 0.91 0.00 1.64 70.89 13.28 7.52 1.01 2.61 0.57 0.66 0.00 0.58 0.00 0.58 0.00 0.16 0.000 0.00	Mass Flow (lb/h) 4370.58 0.00 4986.74 123683.64 43422.17 36062.42 6405.62 16481.80 4459.24 5194.78 0.00 1737.85 0.00 1737.85 0.00 174.87 95.08 2.96 4.23 17.28 1.45 0.00 0.00 286.28 0.00 0.00 0.00	
ET GAS STREAM         Temperature:       110.00 deg F         Pressure:       1114.40 psia         Flow Rate:       90.05 MMSCFD         Component       Como         Hydrogen Sulfide       Nitrogen         Nitrogen       Methane         Ethane       Propane         i-Butane       n-Butane         i-Pentane       Cyclopentane         Cyclopexane       n-Heptane         Cyclopexane       n-Heptane         Cyclopexane       n-Heptane         Cyclopexane       n-Heptane         Cyclopexane       n-Heptane         Cyclopexane       n-Heptane         Cyclopexane       n-Yentane         Cyclopexane       n-Heptane         Cyclopexane       n-Sutane         Dilane       Ethylbenzene         O-Xylene       m-Xylene         m-Xylene       Givol         Ethylene Glycol       Water         Methanol       O2         SO2       SO2	c. (mol%) 0.91 0.00 1.64 70.89 13.28 7.52 1.01 2.61 0.57 0.66 0.00 0.58 0.00 0.16 0.000 0.00	Mass Flow (lb/h) 4370.58 0.00 4986.74 123683.64 43422.17 36062.42 6405.62 16481.80 4459.24 5194.78 0.00 5390.57 0.00 1737.85 0.00 174.87 95.08 2.96 4.23 17.28 1.45 0.00 0.00 0.00 286.28 0.00	
Temperature:       110.00 deg F         Pressure:       1114.40 psia         Flow Rate:       99.05 MMSCFD         Component       Con         Carbon Dioxide       Hydrogen Sulfide         Hydrogen Sulfide       Nitrogen         Methane       Ethane         Propane       i-Butane         i-Butane       n-Pentane         Cyclopentane       n-Pentane         Cyclopentane       n-Hexane         Cyclopentane       n-Heptane         Methylcyclohexane       2,2,4-Trimethylpentane         Benzene       Toluene         Toluene       Ethylbenzene         o-Xylene       m-Xylene         p-Xylene       Striethylene Glycol         Ethylene Glycol       Ethylene Glycol         Water       Methanol         O2       SO2	c. (mol%) 0.91 0.00 1.64 70.89 13.28 7.52 1.01 2.61 0.57 0.66 0.00 0.58 0.00 0.16 0.000 0.00	Mass Flow (lb/h) 4370.58 0.00 4986.74 123683.64 43422.17 36062.42 6405.62 16481.80 4459.24 5194.78 0.00 5390.57 0.00 1737.85 0.00 0.00 174.87 95.08 2.96 4.23 17.28 1.45 0.00 0.00 286.28 0.00 0.00 0.00 0.00	
Pressure: 1114.40 psia Flow Rate: 99.05 MMSCFD Component Carbon Dixide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Butane i-Butane i-Butane i-Butane i-Butane i-Pentane Cyclopentane n-Hexane Cyclopexane n-Hexane Cyclopexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene m-Xylene m-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol Soz Soz Total Components Methanol O2 Soz	c. (mol%) 0.91 0.00 1.64 70.89 13.28 7.52 1.01 2.61 0.57 0.66 0.00 0.58 0.00 0.16 0.000 0.00	Mass Flow (lb/h) 4370.58 0.00 4986.74 123683.64 43422.17 36062.42 6405.62 16481.80 4459.24 5194.78 0.00 5390.57 0.00 1737.85 0.00 174.87 95.08 2.96 4.23 17.28 1.45 0.00 0.00 0.00 286.28 0.00	
Flow Rate:     99.05 MMSCFD       Component     Conv       Carbon Dioxide     Hydrogen Sulfide       Hydrogen Sulfide     Nitrogen       Methane     Ethane       Ethane     Propane       i-Butane     n-Butane       n-Pentane     Cyclopentane       Cyclopexane     N-Heptane       Cyclopexane     N-Heptane       Methylcyclohexane     2,2,4-Trimethylpentane       Benzene     Toluene       Toluene     Benzene       Toluene     Stylene       Triethylene Glycol     Water       Water     Methanol       O2     SO2	<u>c. (mol%)</u> 0.91 0.00 1.64 70.89 13.28 7.52 1.01 2.61 0.57 0.66 0.00 0.58 0.00 0.16 0.00 0.00 0.00 0.00 0.00 0.00	Mass Flow (lb/h) 4370.58 0.00 4986.74 123683.64 43422.17 36062.42 6405.62 16481.80 4459.24 5194.78 0.00 5390.57 0.00 1737.85 0.00 1737.85 0.00 174.87 95.08 2.96 4.23 17.28 1.45 0.00 0.00 286.28 0.00 0	
Component Construction Dioxide Hydrogen Sulfide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Hexana Cyclopentane n-Hexana Cyclopentane structure Benzene Toluene Ethylbenzene Toluene Ethylbenzene o-Xylene m-Xylene m-Xylene m-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol So2	c. (mol%) 0.91 0.00 1.64 70.89 13.28 7.52 1.01 2.61 0.57 0.66 0.00 0.00 0.58 0.00 0.58 0.00 0.16 0.000 0.00	Mass Flow (lb/h) 4370.58 0.00 4986.74 123683.64 43422.17 36062.42 6405.62 16481.80 4459.24 5194.78 0.00 5390.57 0.00 1737.85 0.00 1737.85 0.00 174.87 95.08 2.96 4.23 17.28 1.45 0.00 0.00 286.28 0.00 0.00 0.00 0.00	
Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Pentane n-Pentane Cyclopentane n-Heytane Cyclopentane cyclohexane n-Heytane Methylcyclohexane 2,2,4-Trimethylepentane Bezren Toluene Ethylbenzene o-Xylene Hydrene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Col Soz Total Components	0.91 0.00 1.64 70.89 13.28 7.52 1.01 2.61 0.57 0.66 0.00 0.58 0.00 0.16 0.00 0.00 0.00 0.00 0.00 0.00	4370.58 0.00 4986.74 123683.64 43422.17 36062.42 6405.62 16481.80 4459.24 5194.78 0.00 5390.57 0.00 1737.85 0.00 1737.85 0.00 1737.85 2.96 4.23 17.28 1.45 0.00 0.00 286.28 0.00 0.00	
Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Otlone Ethylbenzene o-Xylene r-Xylene m-Xylene m-Xylene jouene Ethylbenzene o-Xylene r-Xylene Stylene S	0.00 1.64 70.89 13.28 7.52 1.01 2.61 0.57 0.66 0.00 0.58 0.00	0.00 4986.74 123683.64 43422.17 36062.42 6405.62 16481.80 4459.24 5194.78 0.00 5390.57 0.00 1737.85 0.00 1737.85 0.00 0.00 174.87 95.08 2.96 4.23 17.28 1.45 0.00 0.00 0.00 2.86.28 0.00 0.00 0.00 0.00	
Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane Cyclopentane n-Pentane Cyclopentane n-Pentane Cyclopentane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene p-Xylene j-Xylene Stol Ethylene Glycol Ethylene Glycol Stol Stol Stol Stol Stol Stol Stol St	1.64 70.89 13.28 7.52 1.01 2.61 0.57 0.66 0.00 0.58 0.00 0.58 0.00 0.16 0.00 0.00 0.00 0.00 0.00 0.00	4986.74 123683.64 43422.17 36062.42 6405.62 16481.80 4459.24 5194.78 0.00 5390.57 0.00 1737.85 0.00 0.00 174.87 95.08 2.96 4.23 17.28 1.45 0.00 0.00 286.28 0.00 0.00 0.00	
Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Heptane Cyclopexane cyclopexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Soz Soz	70.89         13.28         7.52         1.01         2.61         0.57         0.66         0.00         0.58         0.00         0.16         0.00         0.00         0.00         0.00         0.00         0.00         0.00         0.00         0.00         0.00         0.00         0.00         0.00         0.00         0.00         0.00         0.00         0.00	123683.64 43422.17 36062.42 6405.62 16481.80 4459.24 5194.78 0.00 5390.57 0.00 1737.85 0.00 0.00 174.87 95.08 2.96 4.23 17.28 1.45 0.00 0.00 286.28 0.00 0.00	
thane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Heyane Cyclopexane n-Heyane Cyclopexane 2,2,4-Timethylopechane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Water Methanol O2 SO2 Total Components	13.28 7.52 1.01 2.61 0.57 0.66 0.00 0.58 0.00 0.16 0.00 0.00 0.00 0.00 0.00 0.00	43422.17 36062.42 6405.62 16481.80 4459.24 5194.78 0.00 5390.57 0.00 1737.85 0.00 0.00 174.87 95.08 2.96 4.23 17.28 1.45 0.00 0.00 286.28 0.00 0.00 0.00	
Propane i-Butane i-Butane i-Pentane CPClohexane n-Pentane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene m-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Soz Total Components BESTREM	7.52 1.01 2.61 0.57 0.66 0.00 0.58 0.00 0.16 0.00	30062.42 6405.62 16481.80 4459.24 5194.78 0.00 53390.57 0.00 1737.85 0.00 0.00 174.87 95.08 2.96 4.23 17.28 1.45 0.00 0.00 286.28 0.00 0.00 0.00	
i-Butane i-Pentane i-Pentane n-Pentane Cyclopentane n-Heptane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene m-Xylene Stylene Glycol Ethylene Glycol Ethylene Glycol Kater Methanol 02 502 Total Components	1.01 2.61 0.57 0.66 0.00 0.58 0.00	0443.80         16481.80         4459.24         5194.78         0.00         5390.57         0.00         1737.85         0.00         1737.85         0.00         174.87         95.08         2.96         4.23         17.28         1.45         0.00         286.28         0.00         0.00         0.00         0.00         0.00         0.00         0.00         0.00	
in-Bottane i-Pentane n-Petane Cyclopentane n-Heptane Cyclopexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene 0-Xylene Toluene Ethylbenzene 0-Xylene m-Xylene p-Xylene Nethanol 02 502 Total Components Eds STREAM	2.01 0.57 0.66 0.00 0.58 0.00	4459.24 5194.78 0.00 5390.57 0.00 1737.85 0.00 0.00 174.87 95.08 2.96 4.23 17.28 1.45 0.00 0.00 0.00 286.28 0.00 0.00 0.00 0.00	
An-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene p-Xylene Sthylene Glycol Ethylene Glycol Water Methanol 02 S02 Total Components	0.66 0.66 0.00 0.58 0.00 0.16 0.00	5194.78 0.00 5390.57 0.00 1737.85 0.00 0.00 174.87 95.08 2.96 4.23 17.28 1.45 0.00 0.00 286.28 0.00 0.00 0.00 0.00	
Cyclopentane n-Hexane Cyclopexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Water Methanol O2 SO2 Total Components GAS STREAM	0.00 0.58 0.00 0.16 0.00	0.00 5390.57 0.00 1737.85 0.00 0.00 174.87 95.08 2.96 4.23 17.28 1.45 0.00 0.00 286.28 0.00 0.00 0.00	
n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene Jethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Water Methanol O2 SO2 Total Components	0.58 0.00 0.16 0.00 0.02 0.01 0.00 0.00 0.00 0.00 0.00	5390.57 0.00 1737.85 0.00 0.00 174.87 95.08 2.96 4.23 17.28 1.45 0.00 0.00 286.28 0.00 0.00 0.00 0.00	
Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene D-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol Water Methanol O2 SO2 Total Components GAS STREAM	0.00 0.16 0.00 0.02 0.01 0.00 0.00 0.00 0.00 0.00 0.00 0.15 0.00 0.00 0.00 0.00 0.15 0.00	0.00 1737.85 0.00 0.00 174.87 95.08 2.96 4.23 17.28 1.45 0.00 0.00 286.28 0.00 0.00 0.00 0.00	
n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Ethylene Glycol Water Methanol O2 502 Total Components	0.16 0.00 0.00 0.02 0.01 0.00 0.00 0.00 0.00	1737.85 0.00 0.00 174.87 95.08 2.96 4.23 17.28 1.45 0.00 0.00 286.28 0.00 0.00 0.00 0.00	
Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene D-Xylene M-Xylene S-Xylene M-Xylene Sycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Soz Soz Total Components GAS STREAM Temperature: 111.46 deg F	0.00 0.00 0.02 0.01 0.00 0.00 0.00 0.00	0.00 0.00 174.87 95.08 2.96 4.23 17.28 1.45 0.00 0.00 286.28 0.00 0.00 0.00 0.00	
2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Water Methanol O2 SO2 Total Components GAS STREAM Temperature: 111.46 deg F	0.00 0.02 0.01 0.00 0.00 0.00 0.00 0.00	0.00 174.87 95.08 2.96 4.23 17.28 1.45 0.00 0.00 286.28 0.00 0.00 0.00 0.00	
GAS STREAM Benzene Toluene Ethylbenzene o-Xylene p-Xylene p-Xylene Gas STREAM Temperature: 111.46 deg F	0.02 0.01 0.00 0.00 0.00 0.00 0.00 0.15 0.00 0.00	174.87 95.08 2.96 4.23 17.28 1.45 0.00 0.00 286.28 0.00 0.00 0.00 0.00	
Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Water Methanol O2 SO2 Total Components GAS STREAM Temperature: 111.46 deg F	0.01 0.00 0.00 0.00 0.00 0.00 0.15 0.00 0.00	95.08 2.96 4.23 17.28 1.45 0.00 0.00 286.28 0.00 0.00 0.00 0.00	
Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Water Methanol O2 SO2 Total Components GAS STREAM Temperature: 111.46 deg F	0.00 0.00 0.00 0.00 0.00 0.15 0.00 0.00	2.96 4.23 17.28 1.45 0.00 0.00 286.28 0.00 0.00 0.00 0.00	
o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Water Methanol O2 SO2 Total Components GAS STREAM Temperature: 111.46 deg F	0.00 0.00 0.00 0.00 0.15 0.00 0.00 0.00	4.23 17.28 1.45 0.00 0.00 286.28 0.00 0.00 0.00	
m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Water Methanol O2 SO2 Total Components GAS STREAM Temperature: 111.46 deg F	0.00 0.00 0.00 0.15 0.00 0.00 0.00 100.00	17.28 1.45 0.00 286.28 0.00 0.00 0.00	
P-Xylene Triethylene Glycol Ethylene Glycol Water Methanol O2 SO2 Total Components GAS STREAM Temperature: 111.46 deg F	0.00 0.00 0.15 0.00 0.00 0.00 100.00	1.45 0.00 0.00 286.28 0.00 0.00 0.00	
Triethylene Glycol Ethylene Glycol Water Methanol O2 SO2 Total Components GAS STREAM Temperature: 111.46 deg F	0.00 0.00 0.15 0.00 0.00 0.00 100.00	0.00 0.00 286.28 0.00 0.00 0.00	
Ethylene Glycol Water Methanol O2 SO2 Total Components GAS STREAM Temperature: 111.46 deg F	0.00 0.15 0.00 0.00 0.00 100.00	0.00 286.28 0.00 0.00 0.00	
Water Methanol O2 SO2 Total Components GAS STREAM Temperature: 111.46 deg F	0.15 0.00 0.00 0.00 100.00	286.28 0.00 0.00 0.00	
GAS STREAM Temperature: 111.46 deg F	0.00 0.00 0.00 100.00	0.00 0.00 0.00	
GAS STREAM Temperature: 111.46 deg F	0.00 0.00 100.00	0.00	
GAS STREAM Temperature: 111.46 deg F	100.00	0.00	
GAS STREAM Temperature: 111.46 deg F	100.00		
Pressure: 1109.40 psia			
Flow Rate: 98.90 MMSCFD			
Component Cond	c. (mol%)	Mass Flow (lb/h)	
Carbon Dioxide	0.91	4365.75	
Hydrogen Sulfide	0.00	0.00	
Nitrogen	1.64	4986.55	
Methane	70.99	123669.05	
Ethane	13.29	43409.65	
Propane	/.53	36047.68	
I-Butane	1.01	04U2.91 16471 77	
i-Dentane	2.01	104/1.// AA56 22	
n-Pentane	0.57	5190.61	
Cyclopentane	0.00	0.00	
n-Hexane	0.58	5384.72	
Cvclohexane	0.00	0.00	
n-Heptane	0.16	1735.19	
Methylcyclohexane	0.00	0.00	
2,2,4-Trimethylpentane	0.00	0.00	
Benzene	0.02	169.81	
Toluene	0.01	91.20	
Ethylbenzene	0.00	2.82	
o-Xylene	0.00	3.96	
m-Xylene	0.00	16.46	
p-Xylene	0.00	1.38	
Triethylene Glycol	0.00	2.35	
Ethylene Glycol	0.00	0.00	
	0.01	18.74	
Water	0.01	0.00	
Water Methanol	0.00	0.00	
Water Methanol O2	0.00	0.00	
Water Methanol O2 SO2	0.00 0.00 0.00	0.00 0.00	

Temperature:	120.00 d	eg F	
Pressure:	1119.40 p	sia	
Flow Rate:	7.00 sg	gpm	
Component		Conc. (wt%)	Mass Flow (lb/h)
	Carbon Dioxide	0.00	0.00
	Hydrogen Sulfide	0.00	0.00
	Nitrogen	0.00	0.00
	Methane	0.00	0.00
	Ethane	0.00	0.00
	Propane	0.00	0.00
	i-Butane	0.00	0.00
	n-Butane	0.00	0.00
	i-Pentane	0.00	0.00
	n-Pentane	0.00	0.00
	Cyclopentane	0.00	0.00
	n-Hevane	0.00	0.00
	Curlahavana	0.00	0.00
	Cyclonexane	0.00	0.00
	n-Heptane	0.00	0.00
	Methylcyclohexane	0.00	0.00
	2,2,4-Trimethylpentane	0.00	0.00
	Benzene	0.00	0.00
	Toluene	0.00	0.00
	Ethylbenzene	0.00	0.00
	o-Xylene	0.00	0.00
	m-Xylene	0.00	0.00
	p-Xylene	0.00	0.00
	Triethylene Glycol	99.13	3916.56
	Ethylene Glycol	0.00	0.00
	Water	0.87	34 38
	Mothanol	0.07	0.00
	Methanol 02	0.00	0.00
	02	0.00	0.00
YCOL STREAM	111 ٦٢ ما.	eg F	
YCOL STREAM Temperature: Pressure:	111.25 dı 1114.40 p:	eg F	
YCOL STREAM Temperature: Pressure: Flow Rate:	111.25 d 1114.40 p 7.90 sg	eg F sia gpm	
YCOL STREAM Temperature: Pressure: Flow Rate: Component	111.25 dı 1114.40 p: 7.90 sg	eg F sia gpm Conc. (wt%)	Mass Flow (lb/h)
YCOL STREAM Temperature: Pressure: Flow Rate: Component	111.25 di 1114.40 p: 7.90 sg Carbon Dioxide	eg F sia gpm Conc. (wt%) 0.11	Mass Flow (lb/h) 4.88
LYCOL STREAM Temperature: Pressure: Flow Rate: Component	111.25 di 1114.40 p: 7.90 sg Carbon Dioxide Hydrogen Sulfide	eg F sia gpm Conc. (wt%) 0.11 0.00	Mass Flow (lb/h) 4.88 0.00
LYCOL STREAM Temperature: Pressure: Flow Rate: Component	111.25 di 1114.40 p: 7.90 sg Carbon Dioxide Hydrogen Sulfide Nitrogen	eg F sia gpm Conc. (wt%) 0.11 0.00 0.01	Mass Flow (lb/h) 4.88 0.00 0.24
LYCOL STREAM Temperature: Pressure: Flow Rate: Component	111.25 d 1114.40 p 7.90 sg Carbon Dioxide Hydrogen Sulfide Nitrogen Methane	eg F sia gpm Conc. (wt%) 0.11 0.00 0.01 0.37	Mass Flow (lb/h) 4.88 0.00 0.24 15.97
LYCOL STREAM Temperature: Pressure: Flow Rate: Component	111.25 dr 1114.40 pr 7.90 sg Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Fihane	eg F sia gpm Conc. (wt%) 0.11 0.00 0.01 0.37 0.30	Mass Flow (lb/h) 4.88 0.00 0.24 15.97 13.00
LYCOL STREAM Temperature: Pressure: Flow Rate: Component	111.25 di 1114.40 p 7.90 sg Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane	eg F sia gpm Conc. (wt%) 0.11 0.00 0.01 0.37 0.30 0.35	Mass Flow (lb/h) 4.88 0.00 0.24 15.97 13.00 15.14
LYCOL STREAM Temperature: Pressure: Flow Rate: Component	111.25 di 1114.40 p 7.90 sg Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Ethane Propane i-Butane	eg F sia gpm Conc. (wt%) 0.11 0.00 0.01 0.37 0.30 0.35 0.06	Mass Flow (lb/h) 4.88 0.00 0.24 15.97 13.00 15.14 2.78
LYCOL STREAM Temperature: Pressure: Flow Rate: Component	111.25 di 1114.40 p: 7.90 sg Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane	eg F sia gpm Conc. (wt%) 0.11 0.00 0.01 0.37 0.30 0.35 0.06 0.24	Mass Flow (lb/h) 4.88 0.00 0.24 15.97 13.00 15.14 2.78 10.21
LYCOL STREAM Temperature: Pressure: Flow Rate: Component	111.25 di 1114.40 pr 7.90 sg Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane	eg F sia gpm Conc. (wt%) 0.11 0.00 0.01 0.37 0.30 0.35 0.06 0.24 0.07	Mass Flow (lb/h) 4.88 0.00 0.24 15.97 13.00 15.14 2.78 10.21 3.07
LYCOL STREAM Temperature: Pressure: Flow Rate: Component	111.25 d 1114.40 p 7.90 sg Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Pentane i-Pentane	eg F sia gpm Conc. (wt%) 0.11 0.00 0.01 0.37 0.30 0.35 0.06 0.24 0.07 0.10	Mass Flow (lb/h) 4.88 0.00 0.24 15.97 13.00 15.14 2.78 10.21 3.07 4.22
LYCOL STREAM Temperature: Pressure: Flow Rate: Component	111.25 d 1114.40 p 7.90 sg Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane	eg F sia gpm Conc. (wt%) 0.11 0.00 0.01 0.37 0.30 0.35 0.06 0.24 0.07 0.10 0.22	Mass Flow (lb/h) 4.88 0.00 0.24 15.97 13.00 15.14 2.78 10.21 3.07 4.23 0.00
LYCOL STREAM Temperature: Pressure: Flow Rate: Component	111.25 di 1114.40 p 7.90 s Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane	eg F sia gpm Conc. (wt%) 0.11 0.00 0.01 0.37 0.30 0.35 0.06 0.24 0.07 0.10 0.00 0.00	Mass Flow (lb/h) 4.88 0.00 0.24 15.97 13.00 15.14 2.78 10.21 3.07 4.23 0.00 5.54
LYCOL STREAM Temperature: Pressure: Flow Rate: Component	111.25 di 1114.40 pr 7.90 sg Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Propane i-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane	eg F sia gpm Conc. (wt%) 0.11 0.00 0.01 0.37 0.30 0.35 0.06 0.24 0.07 0.10 0.00 0.00 0.14	Mass Flow (lb/h) 4.88 0.00 0.24 15.97 13.00 15.14 2.78 10.21 3.07 4.23 0.00 5.91
LYCOL STREAM Temperature: Pressure: Flow Rate: Component	111.25 di 1114.40 p 7.90 sg Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopentane	eg F sia gpm Conc. (wt%) 0.11 0.00 0.01 0.37 0.30 0.35 0.06 0.24 0.07 0.10 0.00 0.14 0.00	Mass Flow (lb/h) 4.88 0.00 0.24 15.97 13.00 15.14 2.78 10.21 3.07 4.23 0.00 5.91 0.00
LYCOL STREAM Temperature: Pressure: Flow Rate: Component	111.25 d 1114.40 p 7.90 sg Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Pentane n-Pentane n-Pentane n-Hexane Cyclopextane n-Hexane	eg F sia gpm Conc. (wt%) 0.11 0.00 0.01 0.37 0.30 0.35 0.06 0.24 0.07 0.10 0.00 0.14 0.00 0.06	Mass Flow (lb/h) 4.88 0.00 0.24 15.97 13.00 15.14 2.78 10.21 3.07 4.23 0.00 5.91 0.00 2.68
LYCOL STREAM Temperature: Pressure: Flow Rate: Component	111.25 di 1114.40 pr 7.90 sg Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Pentane cyclopentane n-Hexane n-Hexane n-Hexane h-Heptane	eg F sia gpm Conc. (wt%) 0.11 0.00 0.01 0.37 0.30 0.35 0.06 0.24 0.07 0.10 0.00 0.14 0.00 0.06 0.00	Mass Flow (lb/h) 4.88 0.00 0.24 15.97 13.00 15.14 2.78 10.21 3.07 4.23 0.00 5.91 0.00 2.68 0.00
LYCOL STREAM Temperature: Pressure: Flow Rate: Component	111.25 di 1114.40 pc 7.90 sg Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Propane i-Butane n-Butane n-Butane i-Pentane cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane	eg F sia gpm Conc. (wt%) 0.11 0.00 0.01 0.37 0.30 0.35 0.06 0.24 0.07 0.10 0.00 0.14 0.00 0.14 0.00 0.06 0.00 0.00	Mass Flow (lb/h) 4.88 0.00 0.24 15.97 13.00 15.14 2.78 10.21 3.07 4.23 0.00 5.91 0.00 2.68 0.00 0.00
LYCOL STREAM Temperature: Pressure: Flow Rate: Component	111.25 di 1114.40 p 7.90 s Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclohexane n-Hexane Methylcyclohexane 2,2,4-Trimethylpentane Benzene	eg F sia gpm Conc. (wt%) 0.11 0.00 0.01 0.37 0.30 0.35 0.06 0.24 0.07 0.10 0.00 0.14 0.00 0.14 0.00 0.06 0.00 0.00 0.00 0.00 0.00 0.0	Mass Flow (lb/h) 4.88 0.00 0.24 15.97 13.00 15.14 2.78 10.21 3.07 4.23 0.00 5.91 0.00 2.68 0.00 0.00 2.68 0.00 0.00 5.07
LYCOL STREAM Temperature: Pressure: Flow Rate: Component	111.25 d 1114.40 p 7.90 sg Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Butane n-Pentane n-Pentane n-Pentane n-Pentane n-Pentane 2/2/opentane n-Hexane Cyclopexane n-Hexane Quelopexane 2,2,4-Trimethylpentane Benzene Toluene	eg F sia gpm Conc. (wt%) 0.11 0.00 0.01 0.37 0.30 0.35 0.06 0.24 0.07 0.10 0.00 0.04 0.00 0.00 0.14 0.00 0.00	Mass Flow (lb/h) 4.88 0.00 0.24 15.97 13.00 15.14 2.78 10.21 3.07 4.23 0.00 5.91 0.00 2.68 0.00 0.00 2.68 0.00 0.00 3.88
LYCOL STREAM Temperature: Pressure: Flow Rate: Component	111.25 di 1114.40 pr 7.90 sg Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene	eg F sia gpm Conc. (wt%) 0.11 0.00 0.01 0.37 0.30 0.35 0.06 0.24 0.07 0.10 0.00 0.14 0.00 0.14 0.00 0.00 0.00	Mass Flow (lb/h) 4.88 0.00 0.24 15.97 13.00 15.14 2.78 10.21 3.07 4.23 0.00 5.91 0.00 2.68 0.00 0.00 0.00 5.07 3.88 0.14
LYCOL STREAM Temperature: Pressure: Flow Rate: Component	111.25 di 1114.40 p 7.90 s Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Propane i-Butane i-Butane i-Butane i-Pentane Cyclopentane n-Pentane Cyclopentane n-Hexane Cyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene	eg F sia gpm Conc. (wt%) 0.11 0.00 0.01 0.37 0.30 0.35 0.06 0.24 0.07 0.10 0.00 0.14 0.00 0.01 0.00 0.00 0.00	Mass Flow (lb/h) 4.88 0.00 0.24 15.97 13.00 15.14 2.78 10.21 3.07 4.23 0.00 5.91 0.00 2.68 0.00 0.00 5.07 3.88 0.14 0.28
LYCOL STREAM Temperature: Pressure: Flow Rate: Component	111.25 di 1114.40 p 7.90 sg Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene	eg F sia gpm Conc. (wt%) 0.11 0.00 0.01 0.37 0.30 0.35 0.06 0.24 0.07 0.10 0.00 0.04 0.00 0.00 0.00 0.00 0.00	Mass Flow (lb/h) 4.88 0.00 0.24 15.97 13.00 15.14 2.78 10.21 3.07 4.23 0.00 5.91 0.00 2.68 0.00 0.00 2.68 0.00 0.00 2.68 0.00 0.00 2.68 0.00 0.00 2.68 0.00 0.00 2.68 0.00 0.00 0.02 0.00 0.24 0.00 0.24 0.00 0.24 0.00 0.24 0.00 0.24 0.00 0.24 0.00 0.24 0.00 0.24 0.00 0.24 0.00 0.24 0.00 0.24 0.00 0.24 0.00 0.24 0.00 0.24 0.00 0.24 0.00 0.24 0.00 0.24 0.00 0.24 0.00 0.25 0.00 0.
LYCOL STREAM Temperature: Pressure: Flow Rate: Component	111.25 di 1114.40 pr 7.90 sg Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane n-Pentane n-Pentane Cyclopentane n-Hexane Cyclohexane n-Heytane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene	eg F sia gpm Conc. (wt%) 0.11 0.00 0.01 0.37 0.30 0.35 0.06 0.24 0.07 0.10 0.00 0.14 0.00 0.00 0.00 0.00 0.00	Mass Flow (lb/h) 4.88 0.00 0.24 15.97 13.00 15.14 2.78 10.21 3.07 4.23 0.00 5.91 0.00 2.68 0.00 0.00 2.68 0.00 0.00 5.91 0.00 5.91 0.00 5.91 0.00 5.91 0.00 5.91 0.00 5.91 0.00 5.91 0.00 5.07 3.88 0.14 0.28 0.82 0.02 0.00 0.02 0.00 0.24 0.00 0.24 0.00 0.24 0.00 15.14 2.78 0.00 15.14 2.78 0.00 15.14 2.78 0.00 15.14 2.78 0.00 15.14 2.78 0.00 15.14 2.78 0.00 5.91 0.00 0.00 5.91 0.00 0.00 5.91 0.00 0.
LYCOL STREAM Temperature: Pressure: Flow Rate: Component	111.25 di 1114.40 pr 7.90 sg Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Propane i-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclohexane Cyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene frighthulang Glucal	eg F sia gpm Conc. (wt%) 0.11 0.00 0.01 0.37 0.30 0.35 0.06 0.24 0.07 0.10 0.00 0.14 0.00 0.00 0.14 0.00 0.00	Mass Flow (lb/h) 4.88 0.00 0.24 15.97 13.00 15.14 2.78 10.21 3.07 4.23 0.00 5.91 0.00 2.68 0.00 0.00 5.07 3.88 0.14 0.28 0.14 0.28 0.82 0.07 3.914 22
LYCOL STREAM Temperature: Pressure: Flow Rate: Component	111.25 di 1114.40 pr 7.90 sg Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Propane i-Butane n-Butane i-Pentane Cyclopentane n-Pentane Cyclopentane n-Hexane Cyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol	eg F sia gpm Conc. (wt%) 0.11 0.00 0.01 0.37 0.30 0.35 0.06 0.24 0.07 0.10 0.00 0.14 0.00 0.00 0.00 0.00 0.00	Mass Flow (lb/h) 4.88 0.00 0.24 15.97 13.00 15.14 2.78 10.21 3.07 4.23 0.00 5.91 0.00 2.68 0.00 0.00 5.07 3.88 0.14 0.28 0.28 0.82 0.07 3.914.22 0.00
LYCOL STREAM Temperature: Pressure: Flow Rate: Component	111.25 di 1114.40 p 7.90 s Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Pentane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene Jycene Triethylene Glycol Ethylene Glycol	eg F sia gpm Conc. (wt%) 0.11 0.00 0.01 0.37 0.30 0.35 0.06 0.24 0.07 0.10 0.00 0.00 0.14 0.00 0.00 0.00 0.00	Mass Flow (lb/h) 4.88 0.00 0.24 15.97 13.00 15.14 2.78 10.21 3.07 4.23 0.00 5.91 0.00 2.68 0.00 0.00 2.68 0.00 0.00 5.91 0.00 2.68 0.00 0.00 0.02 0.00 0.00 0.02 0.00 0.02 0.00 0.02 0.02 0.00 0.02 0.02 0.00 0.02 0.02 0.00 0.02 0.02 0.00 0.02 0.00 0.02 0.02 0.02 0.00 0.02 0.02 0.00 0.02 0.02 0.00 0.02 0.02 0.00 0.02 0.02 0.00 0.02 0.02 0.00 0.02 0.02 0.02 0.02 0.02 0.02 0.02 0.02 0.02 0.02 0.02 0.02 0.02 0.02 0.00 0.02 0.
LYCOL STREAM Temperature: Pressure: Flow Rate: Component	111.25 di 1114.40 pr 7.90 sg Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene Triethylene Glycol Ethylene Glycol	eg F sia gpm Conc. (wt%) 0.11 0.00 0.01 0.37 0.30 0.35 0.06 0.24 0.07 0.10 0.00 0.14 0.00 0.00 0.14 0.00 0.00	Mass Flow (lb/h) 4.88 0.00 0.24 15.97 13.00 15.14 2.78 10.21 3.07 4.23 0.00 5.91 0.00 2.68 0.00 0.00 2.68 0.00 0.00 2.68 0.00 0.00 0.00 5.07 3.88 0.14 0.28 0.82 0.07 3.914.22 0.00 301.92 0.00 301.92
LYCOL STREAM  Temperature: Pressure: Flow Rate: Component	111.25 di 1114.40 pr 7.90 sg Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Propane i-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Griethylene Glycol Ethylene Glycol Water Methanol	eg F sia gpm Conc. (wt%) 0.11 0.00 0.01 0.37 0.30 0.35 0.06 0.24 0.07 0.10 0.00 0.04 0.00 0.01 0.00 0.00 0.00	Mass Flow (lb/h) 4.88 0.00 0.24 15.97 13.00 15.14 2.78 10.21 3.07 4.23 0.00 5.91 0.00 5.91 0.00 2.68 0.00 0.00 5.07 3.88 0.14 0.28 0.82 0.07 3914.22 0.00 301.92 0.00 1.51 0.00 0.0
LYCOL STREAM Temperature: Pressure: Flow Rate: Component	111.25 di 1114.40 pr 7.90 sg Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Butane n-Butane i-Pentane Cyclopentane n-Pentane Cyclopentane n-Heytane Cyclopentane n-Heytane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Griethylene Glycol Ethylene Glycol Water Methanol O2	eg F sia gpm Conc. (wt%) 0.11 0.00 0.01 0.37 0.30 0.35 0.06 0.24 0.07 0.10 0.00 0.14 0.00 0.00 0.00 0.00 0.00	Mass Flow (lb/h) 4.88 0.00 0.24 15.97 13.00 15.14 2.78 10.21 3.07 4.23 0.00 5.91 0.00 2.68 0.00 0.00 5.91 0.00 2.68 0.00 0.00 5.07 3.88 0.14 0.28 0.29 0.28 0.28 0.28 0.28 0.28 0.28 0.28 0.28 0.29 0.00 0.29 0.00 0.
LYCOL STREAM Temperature: Pressure: Flow Rate: Component	111.25 di 1114.40 pr 7.90 sg Carbon Dioxide Hydrogen Sulfide Nitrogen Ethane Propane i-Butane n-Butane n-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene Tritethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol O2 SO2	eg F sia gpm Conc. (wt%) 0.11 0.00 0.01 0.37 0.30 0.35 0.06 0.24 0.07 0.10 0.00 0.14 0.00 0.00 0.14 0.00 0.00	Mass Flow (lb/h) 4.88 0.00 0.24 15.97 13.00 15.14 2.78 10.21 3.07 4.23 0.00 5.91 0.00 2.68 0.00 0.00 2.68 0.00 0.00 5.07 3.88 0.14 0.28 0.82 0.07 3914.22 0.00 301.92 0.00 0.00 0.00 0.00

Temperature:	160.00 d	leg F	
Pressure:	59.40 p	sia	
Flow Rate:	775.64 so	cfh	
Component		Conc. (mol%)	Mass Flow (lb/h)
	Carbon Dioxide	4.16	3.74
	Hydrogen Sulfide	0.00	0.00
	Nitrogen	0.41	0.24
	Methane	47.00	15.41
	Ethane	18.97	11.66
	Propane	13.89	12.52
	i-Butane	1.83	2.18
	n-Butane	6.13	7.28
	i-Pentane	1.29	1.91
	n-Pentane	1.68	2.48
	Cyclopentane	0.00	0.00
	n-Hexane	1.40	2.47
	Cyclohexane	0.00	0.00
	n-Hentane	0.00	0.84
	Mothyleycloboyano	0.00	0.84
	2.2.4. Trimesthada antena	0.00	0.00
	2,2,4-Trimetnyipentane	0.00	0.00
	Benzene	0.17	0.27
	Toluene	0.06	0.12
	Ethylbenzene	0.00	0.00
	o-Xylene	0.00	0.00
	m-Xylene	0.01	0.02
	p-Xylene	0.00	0.00
	Triethylene Glycol	0.00	0.00
	Ethylene Glycol	0.00	0.00
	Water	2.58	0.95
	Methanol	0.00	0.00
	02	0.00	0.00
	\$02	0.00	0.00
C GLYCOL STREAM Temperature:	Total Components 160.00 d	100.00	62.07
CITE STREAM Temperature: Pressure:	Total Components 160.00 d 59.40 p	100.00 leg F isia	62.07
GLYCOL STREAM Temperature: Pressure: Flow Rate:	Total Components 160.00 d 59.40 p 7.61 sj	100.00 leg F sia gpm	62.07
C GLYCOL STREAM Temperature: Pressure: Flow Rate: Component	Total Components 160.00 d 59.40 p 7.61 sj	leg F sia gpm Conc. (wt%)	62.07 Mass Flow (lb/h)
Contemporature: Pressure: Flow Rate: Component	Total Components 160.00 d 59.40 p 7.61 s <sub>i</sub> Carbon Dioxide	100.00 leg F sia gpm Conc. (wt%) 0.03	62.07 Mass Flow (lb/h) 1.13
C GLYCOL STREAM Temperature: Pressure: Flow Rate: Component	Total Components 160.00 d 59.40 p 7.61 sg Carbon Dioxide Hydrogen Sulfide	100.00 leg F isia gpm Conc. (wt%) 0.03 0.00	62.07 Mass Flow (lb/h) 1.13 0.00
Component Component Component	Total Components 160.00 d 59.40 p 7.61 sp Carbon Dioxide Hydrogen Sulfide Nitrogen	100.00 leg F isia gpm Conc. (wt%) 0.03 0.00 0.00	62.07 Mass Flow (lb/h) 1.13 0.00 0.00
GLYCOL STREAM Temperature: Pressure: Flow Rate: Component	Total Components 160.00 d 59.40 p 7.61 sj Carbon Dioxide Hydrogen Sulfide Nitrogen Methane	100.00 leg F sia gpm Conc. (wt%) 0.03 0.00 0.00 0.00 0.01	62.07 Mass Flow (lb/h) 1.13 0.00 0.00 0.56
C GLYCOL STREAM Temperature: Pressure: Flow Rate: Component	Total Components 160.00 d 59.40 p 7.61 sj Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane	100.00 leg F sia gpm Conc. (wt%) 0.03 0.00 0.00 0.01 0.03	62.07 Mass Flow (lb/h) 1.13 0.00 0.00 0.56 1.34
Component	Total Components 160.00 d 59.40 p 7.61 s Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane	100.00 leg F isia gpm Conc. (wt%) 0.03 0.00 0.00 0.00 0.01 0.03 0.06	62.07 Mass Flow (lb/h) 1.13 0.00 0.00 0.56 1.34 2.62
Component	Total Components 160.00 d 59.40 p 7.61 sg Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane	100.00 leg F isia gpm Conc. (wt%) 0.03 0.00 0.01 0.03 0.06 0.01	62.07 Mass Flow (lb/h) 1.13 0.00 0.00 0.56 1.34 2.62 0.60
Component	Total Components 160.00 d 59.40 p 7.61 sp Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane	100.00 leg F isia gpm Conc. (wt%) 0.03 0.00 0.00 0.01 0.03 0.06 0.01 0.07	62.07 Mass Flow (lb/h) 1.13 0.00 0.00 0.56 1.34 2.62 0.60 2.93
Component	Total Components 160.00 d 59.40 p 7.61 sp Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane	100.00 leg F sia gpm Conc. (wt%) 0.03 0.00 0.01 0.03 0.06 0.01 0.07 0.03	62.07 Mass Flow (lb/h) 1.13 0.00 0.00 0.56 1.34 2.62 0.60 2.93 1.16
Component	Total Components 160.00 d 59.40 p 7.61 sr Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Propane i-Butane n-Butane i-Pentane n-Pentane	100.00 leg F isia gpm Conc. (wt%) 0.03 0.00 0.01 0.03 0.06 0.01 0.07 0.03 0.04	62.07 Mass Flow (lb/h) 1.13 0.00 0.00 0.56 1.34 2.62 0.60 2.93 1.16 1.75
Component	Total Components 160.00 d 59.40 p 7.61 sg Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cvclopentane	100.00 leg F sia gpm Conc. (wt%) 0.03 0.00 0.01 0.03 0.06 0.01 0.07 0.03 0.04 0.04 0.00	62.07 Mass Flow (lb/h) 1.13 0.00 0.00 0.56 1.34 2.62 0.60 2.93 1.16 1.75 0.00
Component	Total Components	100.00 leg F isia gpm Conc. (wt%) 0.03 0.00 0.00 0.01 0.03 0.06 0.01 0.07 0.03 0.06 0.01 0.07 0.03 0.04 0.00 0.04 0.00 0.09	62.07 Mass Flow (lb/h) 1.13 0.00 0.00 0.56 1.34 2.62 0.60 2.93 1.16 1.75 0.00 3.44
Component	Total Components	100.00  leg F sia gpm Conc. (wt%) 0.03 0.00 0.00 0.01 0.03 0.06 0.01 0.03 0.06 0.01 0.07 0.03 0.04 0.00 0.08 0.08 0.08 0.08 0.08 0.08 0.08 0.08 0.08 0.08 0.	62.07 Mass Flow (lb/h) 1.13 0.00 0.00 0.56 1.34 2.62 0.60 2.93 1.16 1.75 0.00 3.44 0.00 0.00 0.93 1.16 0.75 0.00 0.00 0.00 0.93 0.00 0.56 1.34 2.62 0.60 0.000 0.00
Component	Total Components	100.00 leg F sia gpm Conc. (wt%) 0.03 0.00 0.00 0.01 0.03 0.06 0.01 0.07 0.03 0.06 0.01 0.07 0.03 0.04 0.00 0.04 0.00 0.08 0.00 0.08 0.00 0.06 0.01 0.07 0.03 0.04 0.00 0.08 0.00 0.06 0.00 0.08 0.00 0.06 0.00 0.06 0.00 0.08 0.00 0.06 0.00 0.08 0.00 0.06 0.00 0.08 0.00 0.06 0.00 0.08 0.00 0.06 0.00 0.08 0.00 0.06 0.00 0.08 0.00 0.06 0.00 0.08 0.00 0.06 0.00 0.08 0.00 0.06 0.00 0.08 0.00 0.06 0.00 0.08 0.08 0.00 0.08 0.08 0.08 0.00 0.08 0.08 0.08 0.08 0.08 0.08 0.0	62.07 Mass Flow (lb/h) 1.13 0.00 0.00 0.56 1.34 2.62 0.60 2.93 1.16 1.75 0.00 3.44 0.00 1.84
Component	Total Components 160.00 d 59.40 p 7.61 sy Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane	100.00 leg F sia gpm Conc. (wt%) 0.03 0.00 0.01 0.03 0.06 0.01 0.03 0.06 0.01 0.07 0.03 0.06 0.01 0.07 0.03 0.04 0.00 0.04 0.00 0.08 0.00 0.04 0.04 0.00 0.04 0.04 0.00 0.04 0.00 0.04 0.04 0.00 0.04 0.04 0.0	62.07 Mass Flow (lb/h) 1.13 0.00 0.00 0.56 1.34 2.62 0.60 2.93 1.16 1.75 0.00 3.44 0.00 1.84 0.00
Component	Total Components	100.00 leg F sia gpm Conc. (wt%) 0.03 0.00 0.00 0.00 0.01 0.03 0.06 0.01 0.03 0.06 0.01 0.07 0.03 0.04 0.00 0.08 0.00 0.08 0.00 0.04 0.04 0.00 0.04 0.04 0.04 0.00 0.04 0.04 0.00 0.04 0.04 0.04 0.0	62.07 Mass Flow (lb/h) 1.13 0.00 0.00 0.56 1.34 2.62 0.60 2.93 1.16 1.75 0.00 3.44 0.00 1.84 0.00 1.84 0.00 0.202
Component	Total Components	100.00 leg F sia gpm Conc. (wt%) 0.03 0.00 0.00 0.01 0.03 0.06 0.01 0.03 0.06 0.01 0.07 0.03 0.06 0.01 0.07 0.03 0.04 0.00 0.08 0.00 0.08 0.00 0.04 0.04 0.00 0.04 0.00 0.04 0.04 0.00 0.04 0.04 0.0	62.07 Mass Flow (lb/h) 1.13 0.00 0.00 0.56 1.34 2.62 0.60 2.93 1.16 1.75 0.00 3.44 0.00 1.84 0.00 1.84 0.00 1.84 0.00 1.84 0.00 1.93 1.12 0.00 0.56 1.34 0.00 0.56 1.34 0.00 0.56 1.34 0.00 0.56 1.34 0.00 0.56 1.34 0.00 0.56 1.34 0.00 0.56 1.34 0.00 0.56 1.34 0.00 0.56 1.34 0.00 0.56 1.34 0.00 0.56 1.34 0.00 0.56 1.34 0.00 0.56 1.34 0.00 0.56 1.34 0.00 0.56 1.34 0.00 0.56 1.34 0.00 0.56 1.34 0.00 0.56 1.34 0.00 0.44 0.00 0.00 0.00 0.56 1.34 0.00 0.00 0.56 1.34 0.00 0.56 1.34 0.00 0.00 0.56 1.34 0.00 0.00 0.56 1.34 0.00 0.00 0.56 1.34 0.00 0.00 0.56 1.36 1.56
Component	Total Components	100.00 leg F sia gpm Conc. (wt%) 0.03 0.00 0.00 0.01 0.03 0.06 0.01 0.07 0.03 0.06 0.01 0.07 0.03 0.04 0.00 0.04 0.04 0.00 0.04 0.04 0.00 0.04 0.00 0.04 0.04 0.00 0.04 0.04 0.0	62.07 Mass Flow (lb/h) 1.13 0.00 0.00 0.56 1.34 2.62 0.60 2.93 1.16 1.75 0.00 3.44 0.00 1.84 0.00 1.84 0.00 0.00 1.84 0.00 1.84 0.00 0.00 1.56 1.35 0.00 0.56 1.34 0.60 0.56 1.34 0.60 0.56 1.34 0.60 0.56 1.34 0.60 0.56 1.34 0.60 0.56 1.34 0.60 0.56 1.34 0.60 0.93 1.16 1.75 0.00 0.00 0.00 0.56 1.34 0.60 0.93 1.16 1.75 0.00 0.00 0.00 0.56 1.34 0.00 0.00 0.56 1.34 0.00 0.00 0.56 1.34 0.00 0.00 0.56 1.34 0.00 0.00 0.56 1.34 0.00 0.00 0.00 0.56 1.34 0.00 0.00 0.56 1.34 0.00 0.00 0.56 1.34 0.00 0.00 0.56 1.34 0.00 0.00 0.56 1.34 0.00 0.00 0.56 1.75 0.00 0.00 0.56 1.55 0.00 0.56 1.55 0.00 0.56 1.55 0.00 0.56 1.55 0.00 0.56 1.55 0.00 0.56 1.55 0.00 0.56 1.55 0.00 0.56 1.55 0.00 0.56 1.55 0.00 0.56 1.55 0.00 0.00 0.56 1.55 0.00 0.00 0.56 0.00 0.00 0.56 0.00 0.00 0.56 0.00 0.56 0.00 0.00 0.56 0.00
Component	Total Components	100.00 leg F sia gpm Conc. (wt%) 0.03 0.00 0.00 0.01 0.03 0.06 0.01 0.03 0.06 0.01 0.07 0.03 0.06 0.01 0.07 0.03 0.04 0.00 0.04 0.00 0.08 0.00 0.04 0.04 0.00 0.04 0.04 0.00 0.04 0.04 0.00 0.04 0.04 0.00 0.0	62.07 Mass Flow (lb/h) 1.13 0.00 0.00 0.56 1.34 2.62 0.60 2.93 1.16 1.75 0.00 3.44 0.00 1.84 0.00 1.84 0.00 0.00 1.84 0.00 0.00 1.84 0.00 0.00 1.75 0.00 0.00 0.56 1.35 1.75 0.00 0.00 0.56 1.34 0.00 0.56 1.34 0.00 0.56 1.34 0.60 0.56 1.34 0.60 0.56 1.34 0.00 0.56 1.34 0.00 0.56 1.34 0.00 0.56 1.34 0.00 0.00 0.56 1.34 0.00 0.00 0.56 1.34 0.00 0.00 0.56 1.34 0.00 0.00 0.00 0.56 1.34 0.00 0.00 0.56 1.34 0.00 0.00 0.00 0.00 0.56 1.34 0.00 0.00 0.00 0.00 0.56 1.34 0.00 0.00 0.00 0.00 0.56 1.34 0.00
Component	Total Components	100.00  leg F sia gpm Conc. (wt%) 0.03 0.00 0.00 0.01 0.03 0.06 0.01 0.03 0.06 0.01 0.07 0.03 0.06 0.01 0.07 0.03 0.04 0.00 0.08 0.00 0.04 0.00 0.	62.07 Mass Flow (lb/h) 1.13 0.00 0.00 0.56 1.34 2.62 0.60 2.93 1.16 1.75 0.00 3.44 0.00 3.44 0.00 1.84 0.00 1.84 0.00 0.00 1.84 0.00 0.00 1.84 0.00 0.00 1.13 0.56 0.134 1.34 2.62 0.60 0.34 1.16 1.75 0.00 0.00 0.34 0.00 0.00 0.34 0.00 0.00 0.16 0.175 0.00 0.16 0.175 0.00 0.16 0.175 0.00 0.00 0.34 0.00 0.00 0.16 0.14 0.00 0.16 0.175 0.00 0.00 0.16 0.175 0.00 0.00 0.16 0.175 0.00 0.00 0.16 0.175 0.00 0.00 0.175 0.00 0.00 0.14 0.00 0.00 0.14 0.00 0.00 0.14 0.00 0.00 0.00 0.14 0.00 0.
Component	Total Components	100.00  leg F sia gpm Conc. (wt%) 0.03 0.00 0.00 0.01 0.03 0.06 0.01 0.03 0.06 0.01 0.07 0.03 0.06 0.01 0.07 0.03 0.04 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.01 0.01	62.07 Mass Flow (lb/h) 1.13 0.00 0.00 0.56 1.34 2.62 0.60 2.93 1.16 1.75 0.00 3.44 0.00 1.84 0.00 1.84 0.00 1.84 0.00 0.00 1.84 0.00 0.00 1.84 0.00 0.00 0.14 0.27
Component	Total Components	100.00  leg F sia gpm Conc. (wt%) 0.03 0.00 0.00 0.01 0.03 0.06 0.01 0.07 0.03 0.06 0.01 0.07 0.03 0.04 0.00 0.04 0.00 0.08 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.01 0.02	62.07 Mass Flow (lb/h) 1.13 0.00 0.00 0.56 1.34 2.62 0.60 2.93 1.16 1.75 0.00 3.44 0.00 1.84 0.00 0.00 1.84 0.00 0.00 1.84 0.00 0.00 1.84 0.00 0.00 1.13 0.27 0.81
Component	Total Components	100.00 leg F sia gpm Conc. (wt%) 0.03 0.00 0.00 0.01 0.03 0.06 0.01 0.03 0.06 0.01 0.07 0.03 0.06 0.01 0.07 0.03 0.04 0.00 0.04 0.00 0.08 0.00 0.04 0.00 0.0	62.07 Mass Flow (lb/h) 1.13 0.00 0.00 0.56 1.34 2.62 0.60 2.93 1.16 1.75 0.00 3.44 0.00 1.84 0.00 1.84 0.00 1.84 0.00 0.00 3.44 0.00 0.00 1.84 0.00 0.00 0.00 0.00 0.56 0.134 0.00 0.00 0.56 0.134 0.00 0.00 0.56 0.293 1.16 0.75 0.00 0.00 0.00 0.00 0.56 0.293 1.16 1.75 0.00 0.00 0.00 0.00 0.293 1.16 1.75 0.00 0.00 0.00 0.00 0.00 0.293 1.16 1.75 0.00 0.00 0.00 0.00 0.00 0.00 0.56 0.00 0.00 0.00 0.56 0.00 0.00 0.00 0.56 0.00 0.00 0.00 0.56 0.00 0.00 0.00 0.56 0.00 0.01 0.01 0.00 0.01
Component	Total Components	100.00  leg F sia gpm Conc. (wt%) 0.03 0.00 0.00 0.01 0.03 0.06 0.01 0.03 0.06 0.01 0.07 0.03 0.04 0.00 0.04 0.00 0.08 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.01 0.02 0.00 0.01 0.02 0.00 92.26	62.07 Mass Flow (lb/h) 1.13 0.00 0.00 0.56 1.34 2.62 0.60 2.93 1.16 1.75 0.00 3.44 0.00 1.84 0.00 1.84 0.00 0.00 1.84 0.00 0.00 1.84 0.00 0.00 0.00 0.14 0.27 0.81 0.06 3914.21
Component	Total Components	100.00 leg F sia gpm Conc. (wt%) 0.03 0.00 0.00 0.01 0.03 0.06 0.01 0.03 0.06 0.01 0.07 0.03 0.04 0.00 0.08 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.01 0.02 0.00 0.01 0.02 0.00 92.26 0.00	62.07 Mass Flow (lb/h) 1.13 0.00 0.00 0.56 1.34 2.62 0.60 2.93 1.16 1.75 0.00 3.44 0.00 1.84 0.00 1.84 0.00 0.00 4.80 3.76 0.14 0.27 0.81 0.06 3914.21 0.00
Component	Total Components	100.00  leg F sia gpm Conc. (wt%) 0.03 0.00 0.00 0.01 0.03 0.06 0.01 0.07 0.03 0.06 0.01 0.07 0.03 0.04 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.01 0.02 0.00 92.26 0.00 92.26 0.00 7.09	62.07 Mass Flow (lb/h) 1.13 0.00 0.00 0.56 1.34 2.62 0.60 2.93 1.16 1.75 0.00 3.44 0.00 1.84 0.00 0.00 4.80 3.76 0.14 0.27 0.81 0.06 3914.21 0.00 300.97
Component	Total Components	100.00  leg F sia gpm Conc. (wt%) 0.03 0.00 0.00 0.01 0.03 0.06 0.01 0.03 0.06 0.01 0.07 0.03 0.04 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.01 0.02 0.00 92.26 0.00 7.09 0.00	62.07 Mass Flow (lb/h) 1.13 0.00 0.00 0.56 1.34 2.62 0.60 2.93 1.16 1.75 0.00 3.44 0.00 1.84 0.00 1.84 0.00 1.84 0.00 0.00 0.56 1.34 2.62 0.60 2.93 1.16 1.75 0.00 3.44 0.00 0.00 1.84 0.00 0.00 0.00 1.84 0.00
Component	Total Components	100.00  leg F sia gpm Conc. (wt%) 0.03 0.00 0.00 0.01 0.03 0.06 0.01 0.03 0.06 0.01 0.07 0.03 0.06 0.01 0.07 0.03 0.04 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.01 0.02 0.00 0.01 0.02 0.00 0.00	62.07 Mass Flow (lb/h) 1.13 0.00 0.00 0.56 1.34 2.62 0.60 2.93 1.16 1.75 0.00 3.44 0.00 1.84 0.00 1.84 0.00 1.84 0.00 0.00 1.84 0.00 0.00 1.84 0.00 0.00 0.56 3.93 1.16 1.75 0.00 3.44 0.00 0.56 1.34 2.93 1.16 1.75 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.56 1.34 0.00 0.00 0.56 1.34 0.00 0.00 0.56 1.34 0.00 0.00 0.00 0.56 1.34 0.00
Component	Total Components	100.00  leg F sia gpm Conc. (wt%) 0.03 0.00 0.00 0.01 0.03 0.06 0.01 0.03 0.06 0.01 0.07 0.03 0.06 0.01 0.07 0.03 0.04 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.04 0.00 0.01 0.02 0.00 0.01 0.02 0.00 0.01 0.02 0.00 0.00	62.07 Mass Flow (lb/h) 1.13 0.00 0.00 0.56 1.34 2.62 0.60 2.93 1.16 1.75 0.00 3.44 0.00 1.84 0.00 1.84 0.00 1.84 0.00 0.00 3.44 0.00 0.00 3.44 0.00 0.00 3.44 0.00

Temperature:	209.36 d	leg F	
Pressure:	14.10 n	osia	
Flow Bate:	5782 15 s	cfh	
Component	0,02.10 0	Conc. (mol%)	Mass Flow (lb/h)
	Carbon Dioxide	0.17	1.13
	Hydrogen Sulfide	0.00	0.00
	Nitrogen	0.00	0.00
	Methane	0.23	0.56
	Ethane	0.29	1 34
	Bronano	0.20	2.57
	i Butano	0.35	2.02
		0.07	0.00
	i Dentene	0.33	2.95
	I-Pentane	0.11	1.16
	n-Pentane	0.16	1.75
	Cyclopentane	0.00	0.00
	n-Hexane	0.26	3.44
	Cyclohexane	0.00	0.00
	n-Heptane	0.12	1.84
	Methylcyclohexane	0.00	0.00
	2,2,4-Trimethylpentane	0.00	0.00
	Benzene	0.40	4.80
	Toluene	0.27	3.76
	Ethylbenzene	0.01	0.13
	o-Xylene	0.02	0.27
	m-Xylene	0.05	0.81
	p-Xvlene	0.00	0.06
	Triethvlene Glycol	0.00	0.04
	Ethylene Glycol	0.00	0.00
	Water	97 12	266 59
	Mothanal	0.00	0.00
	wethanol	0.00	0.00
	02	0.00	0.00
	rotal components	100.00	233.83
CONDENSER VENT GAS STREAM Temperature: Procesura:	120.00 d	leg F	295.65
CONDENSER VENT GAS STREAM Temperature: Pressure: Elow Pate:	120.00 d 14.10 p	leg F Isia cfu	295.65
CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 d 14.10 p 156.22 s	leg F sia cfh	295.65 Mass Flow (lh/h)
CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 d 14.10 p 156.22 s	leg F ssia cfh Conc. (mol%)	235.65 Mass Flow (lb/h)
CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 d 14.10 p 156.22 s Carbon Dioxide	leg F ssia cfh Conc. (mol%) 6.18	255.65 Mass Flow (lb/h) 1.12 0.00
CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 d 14.10 p 156.22 s Carbon Dioxide Hydrogen Sulfide	leg F ssia cfh <u>Conc. (mol%)</u> 6.18 0.00 0.02	Mass Flow (lb/h) 1.12 0.00 0.00
CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	Carbon Dioxide Hydrogen Sulfide Nitrogen	ieg F sia cfh <u>Conc. (mol%)</u> 6.18 0.00 0.02 0 c r	Mass Flow (lb/h) 1.12 0.00 0.00 0.00
CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 d 14.10 p 156.22 s Carbon Dioxide Hydrogen Sulfide Nitrogen Methane	leg F sia cfh Conc. (mol%) 6.18 0.00 0.02 8.45 0.02	Mass Flow (lb/h) 1.12 0.00 0.00 0.56 1.22
CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 d 14.10 p 156.22 s Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane	leg F ssia cfh Conc. (mol%) 6.18 0.00 0.02 8.45 10.79	Mass Flow (lb/h) 1.12 0.00 0.00 0.56 1.34 
CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane	leg F osia cfh <u>Conc. (mol%)</u> 6.18 0.00 0.02 8.45 10.79 14.31	Mass Flow (lb/h) 1.12 0.00 0.00 0.56 1.34 2.60
CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Fropane i-Butane	ieg F sia cfh <u>Conc. (mol%)</u> 6.18 0.00 0.02 8.45 10.79 14.31 2.45	Mass Flow (lb/h) 1.12 0.00 0.00 0.56 1.34 2.60 0.59
CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane	leg F sia cfh Conc. (mol%) 6.18 0.00 0.02 8.45 10.79 14.31 2.45 11.91	Mass Flow (lb/h) 1.12 0.00 0.00 0.56 1.34 2.60 0.59 2.85
CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	Carbon Dioxide Hydrogen Sufide Hydrogen Sufide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Putane	lieg F ssia cfh Conc. (mol%) 6.18 0.00 0.02 8.45 10.79 14.31 2.45 11.91 3.65	Mass Flow (lb/h) 1.12 0.00 0.00 0.56 1.34 2.60 0.59 2.85 1.08
CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfide Nitrogen Ethane Propane i-Butane n-Butane n-Pentane n-Pentane	lieg F osia cfh Conc. (mol%) 6.18 0.00 0.02 8.45 10.79 14.31 2.45 11.91 3.65 5.39	Mass Flow (lb/h) 1.12 0.00 0.00 0.56 1.34 2.60 0.59 2.85 1.08 1.60
CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Pentane n-Pentane Cyclopentane	ieg F isia cfh Conc. (mol%) 6.18 0.00 0.02 8.45 10.79 14.31 2.45 11.91 3.65 5.39 0.00	Mass Flow (lb/h) 1.12 0.00 0.00 0.56 1.34 2.60 0.59 2.85 1.08 1.60 0.00
CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Propane i-Butane n-Butane n-Pentane n-Pentane n-Pentane n-Pentane n-Hexane	ieg F isia cfh Conc. (mol%) 6.18 0.00 0.02 8.45 10.79 14.31 2.45 11.91 3.65 5.39 0.00 7.68	Mass Flow (lb/h) 1.12 0.00 0.00 0.56 1.34 2.60 0.59 2.85 1.08 1.60 0.00 2.72
CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane Cyclopentane Cyclohexane	lieg F ssia cfh Conc. (mol%) 6.18 0.00 0.02 8.45 10.79 14.31 2.45 11.91 3.65 5.39 0.00 7.68 0.00	Mass Flow (lb/h) 1.12 0.00 0.00 0.56 1.34 2.60 0.59 2.85 1.08 1.60 0.00 2.72 0.00
CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclohexane	lieg F osia cfh Conc. (mol%) 6.18 0.00 0.02 8.45 10.79 14.31 2.45 11.91 3.65 5.39 0.00 7.68 0.00 2.53	Mass Flow (lb/h) 1.12 0.00 0.00 0.56 1.34 2.60 0.59 2.85 1.08 1.60 0.00 2.72 0.00 1.04
CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Pentane cyclopentane n-Hexane Cyclopexane n-Hexane Cyclopexane Methylcyclohexane	lieg F isia cfh Conc. (mol%) 6.18 0.00 0.02 8.45 10.79 14.31 2.45 11.91 3.65 5.39 0.00 7.68 0.00 2.53 0.00	Mass Flow (lb/h) 1.12 0.00 0.00 0.56 1.34 2.60 0.59 2.85 1.08 1.60 0.00 2.72 0.00 1.04 0.00
CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 d 14.10 p 156.22 s Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane	leg F ssia cfh Conc. (mol%) 6.18 0.00 0.02 8.45 10.79 14.31 2.45 11.91 3.65 5.39 0.00 7.68 0.00 2.53 0.00 0.00	Mass Flow (lb/h) 1.12 0.00 0.00 0.56 1.34 2.60 0.59 2.85 1.08 1.60 0.00 2.72 0.00 1.04 0.00 0.00 0.00 0.00 0.00 0.00 0.59 0.00 0.00 0.59 0.59 0.59 0.59 0.00 0.00 0.59 0.59 0.59 0.59 0.00 0.00 0.59 0.59 0.00 0.00 0.59 0.00 0.00 0.59 0.00 0.00 0.59 0.00 0.00 0.59 0.00 0.00 0.59 0.00 0.00 0.00 0.59 0.00 0.00 0.00 0.59 0.00
CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 d 14.10 p 156.22 s Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Pentane n-Butane i-Pentane Cyclopentane Cyclopexane N-Heytane Methylcyclohexane 2,2,4-Trimethylpentane	lieg F ssia cfh Conc. (mol%) 6.18 0.00 0.02 8.45 10.79 14.31 2.45 11.91 3.65 5.39 0.00 7.68 0.00 2.53 0.00 2.53 0.00 9.93	Mass Flow (lb/h) 1.12 0.00 0.00 0.56 1.34 2.60 0.59 2.85 1.08 1.60 0.00 2.72 0.00 1.04 0.00 1.04 0.00 3.19
CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 d 14.10 p 156.22 s Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene	lieg F cfh Conc. (mol%) 6.18 0.00 0.02 8.45 10.79 14.31 2.45 11.91 3.65 5.39 0.00 7.68 0.00 2.53 0.00 0.02 4.14	Mass Flow (lb/h) 1.12 0.00 0.00 0.56 1.34 2.60 0.59 2.85 1.08 1.60 0.00 2.72 0.00 1.04 0.00 1.04 0.00 3.19 1.57
CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 d 14.10 p 156.22 s Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Pentane n-Pentane Cyclopentane n-Hexane Cyclopexane n-Hexane 2,2,4-Trimethylpentane Benzene Toluene	leg F cfh Conc. (mol%) 6.18 0.00 0.02 8.45 10.79 14.31 2.45 11.91 3.65 5.39 0.00 7.68 0.00 7.68 0.00 7.68 0.00 9.93 4.14 0.06	Mass Flow (lb/h) 1.12 0.00 0.00 0.56 1.34 2.60 0.59 2.85 1.08 1.60 0.00 2.72 0.00 1.04 0.00 1.04 0.00 1.04 0.00 0.00 3.19 1.57 0.03
CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 d 14.10 p 156.22 s Carbon Dioxide Hydrogen Sulfide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane Sz,2,4-Trimethylpentane Benzene Toluene Ethylbenzene Cyclone	lieg F ssia cfh Conc. (mol%) 6.18 0.00 0.02 8.45 10.79 14.31 2.45 11.91 3.65 5.39 0.00 7.68 0.00 2.53 0.00 2.53 0.00 2.53 0.00 9.93 4.14 0.06 0.12	Mass Flow (lb/h) 1.12 0.00 0.00 0.56 1.34 2.60 0.59 2.85 1.08 1.60 0.00 2.72 0.00 1.04 0.00 1.04 0.00 0.00 1.04 0.00 0.00 0.00 0.59 2.85 1.08 1.60 0.00 0.00 0.00 0.59 2.85 1.08 1.60 0.00 0.00 0.00 0.59 2.85 1.08 1.60 0.00 0.00 0.00 0.59 2.85 1.08 1.60 0.00 0.00 0.00 0.00 0.59 2.85 1.08 1.60 0.00 0.00 0.00 0.00 0.59 2.85 1.08 1.60 0.00 0.00 0.00 0.00 0.00 0.59 2.85 1.08 1.60 0.00 0.00 0.00 0.00 0.00 0.00 0.59 2.85 1.08 1.60 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.59 0.00
CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 d 14.10 p 156.22 s Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Pentane n-Butane i-Pentane Cyclopentane Cyclopentane Cyclopentane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene	lieg F ssia cfh Conc. (mol%) 6.18 0.00 0.02 8.45 10.79 14.31 2.45 11.91 3.65 5.39 0.00 7.68 0.00 2.53 0.00 2.53 0.00 0.00 2.53 0.00 0.00 2.53 0.00 0.00 2.53 0.00 0.02 2.53 0.00 0.02 2.53 0.00 0.02 2.53 0.00 0.00 2.53 0.00 0.00 2.53 0.00 0.00 2.53 0.00 0.00 2.53 0.00 0.00 2.53 0.00 0.00 2.53 0.00 0.00 2.53 0.00 0.00 2.53 0.00 0.00 2.53 0.00 0.00 2.53 0.00 0.00 2.53 0.00 0.00 2.53 0.00 0.00 2.53 0.00 0.00 2.53 0.00 0.00 2.53 0.00 0.00 2.53 0.00 0.00 2.53 0.00 0.00 2.53 0.00 0.00 2.53 0.00 0.00 2.53 0.00 0.00 2.53 0.00 0.00 2.53 0.00 0.00 2.53 0.00 0.00 2.53 0.00 0.00 2.53	Mass Flow (lb/h) 1.12 0.00 0.00 0.56 1.34 2.60 0.59 2.85 1.08 1.60 0.00 2.72 0.00 1.04 0.00 1.04 0.00 1.04 0.00 0.00 1.04 0.00 0.00 0.00 1.12 0.00 0.56 1.34 1.57 0.03 0.00 0.15 0.15 0.15 0.00 0.59 0.00 0.00 0.00 0.00 0.00 0.59 0.59 0.00 0.00 0.00 0.59 0.59 0.59 0.59 0.59 0.59 0.59 0.59 0.59 0.00
CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 o 14.10 p 156.22 s Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene	leg F cfh Conc. (mol%) 6.18 0.00 0.02 8.45 10.79 14.31 2.45 11.91 3.65 5.39 0.00 7.68 0.00 2.53 0.00 0.02 8.45 11.91 3.65 5.39 0.00 7.68 0.00 0.02 8.45 11.91 3.65 5.39 0.00 7.68 0.00 0.02 8.45 11.91 3.65 5.39 0.00 0.02 8.45 11.91 3.65 5.39 0.00 0.02 8.45 11.91 3.65 5.39 0.00 0.02 8.45 11.91 3.65 5.39 0.00 0.02 8.45 11.91 3.65 5.39 0.00 0.02 7.68 0.00 0.02 7.68 0.00 0.02 7.68 0.00 0.02 7.68 0.00 0.02 7.68 0.00 0.00 0.02 7.68 0.00 0.00 0.02 7.68 0.00 0.00 0.02 7.68 0.00 0.00 0.02 7.68 0.00 0.00 0.02 7.68 0.00 0.00 0.02 7.68 0.00 0.00 0.02 7.68 0.00	Mass Flow (lb/h) 1.12 0.00 0.00 0.56 1.34 2.60 0.59 2.85 1.08 1.60 0.00 2.72 0.00 1.04 0.00 1.04 0.00 3.19 1.57 0.03 0.05 0.16 0.01
CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 d 14.10 p 156.22 s Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Pentane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene	leg F isia cfh Conc. (mol%) 6.18 0.00 0.02 8.45 10.79 14.31 2.45 11.91 3.65 5.39 0.00 7.68 0.00 7.68 0.00 7.68 0.00 7.68 0.00 9.93 4.14 0.06 0.12 0.36 0.03 0.02	Mass Flow (lb/h) 1.12 0.00 0.00 0.56 1.34 2.60 0.59 2.85 1.08 1.60 0.00 2.72 0.00 1.04 0.00 1.04 0.00 1.04 0.00 0.00 1.04 0.00 0.00 1.04 0.00 0.00 0.00 0.00 0.59 2.85 1.08 1.57 0.03 0.00 0.00 0.16 0.00 0.00 0.00 0.59 2.85 1.08 1.59 2.85 1.08 1.59 2.85 1.08 1.60 0.00 0.00 0.00 0.00 0.00 0.59 2.85 1.08 1.60 0.00 1.04 0.00 0.00 0.00 0.00 0.00 0.59 2.85 1.08 1.60 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.59 2.85 1.08 1.60 0.00 0.00 1.04 0.00
CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 d 14.10 p 156.22 s Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Pentane cyclopentane Cyclopentane Cyclopentane Cyclopentane cyclopentane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol	lieg F ssia cfh Conc. (mol%) 6.18 0.00 0.02 8.45 10.79 14.31 2.45 11.91 3.65 5.39 0.00 2.53 0.00 2.53 0.00 2.53 0.00 2.53 0.00 0.00 0.00 2.53 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	Mass Flow (lb/h) 1.12 0.00 0.00 0.56 1.34 2.60 0.59 2.85 1.08 1.60 0.00 2.72 0.00 1.04 0.00 2.72 0.00 1.04 0.00 0.00 0.00 1.04 0.00 0.00 0.00 0.00 0.00 0.59 2.85 1.08 1.60 0.00 0.00 0.00 0.00 0.59 2.85 1.08 1.60 0.00 0.00 0.00 0.00 0.59 2.85 1.08 1.60 0.00 0.00 0.00 0.00 0.00 0.59 2.85 1.08 1.60 0.00 0.00 0.00 0.00 0.00 0.00 0.59 2.85 1.08 1.60 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.59 2.85 1.08 1.60 0.00
CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 d 14.10 p 156.22 s Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Pentane n-Butane i-Pentane n-Butane i-Pentane Cyclopentane n-Hexane 2,2,4-Trimethylepentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene m-Xylene Triethylene Glycol Ethylene Glycol	lieg F ssia cfh Conc. (mol%) 6.18 0.00 0.02 8.45 10.79 14.31 2.45 11.91 3.65 5.39 0.00 7.68 0.00 2.53 0.00 7.68 0.00 0.00 2.53 0.00 0.00 9.93 4.14 0.06 0.12 0.36 0.03 0.00	Mass Flow (lb/h)
CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 d 14.10 p 156.22 s Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Heytane Cyclopexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene p-Xylene Triethylene Glycol Ethylene Glycol	leg F cfh Conc. (mol%) 6.18 0.00 0.02 8.45 10.79 14.31 2.45 11.91 3.65 5.39 0.00 7.68 0.00 2.53 0.00 0.00 9.93 4.14 0.06 0.12 0.36 0.03 0.00 11.99	Mass Flow (lb/h)
CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 d 14.10 p 156.22 s Carbon Dioxide Hydrogen Sufide Hydrogen Sufide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylpentane Ethylbenzene Toluene Ethylbenzene n-Xylene p-Xylene Triethylene Glycol Ethylene Glycol Water Methanol	leg F ssia cfh Conc. (mol%) 6.18 0.00 0.02 8.45 10.79 14.31 2.45 11.91 3.65 5.39 0.00 7.68 0.00 2.53 0.00 7.68 0.00 2.53 0.00 0.00 0.00 2.53 0.00 0.00 0.00 2.53 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	Mass Flow (lb/h)
CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 of 14.10 p 156.22 s Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Pentane n-Pentane Cyclopentane Cy	lieg F ssia cfh Conc. (mol%) 6.18 0.00 0.02 8.45 10.79 14.31 2.45 11.91 3.65 5.39 0.00 7.68 0.00 2.53 0.00 2.53 0.00 2.53 0.00 2.53 0.00 0.00 0.00 2.53 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	Mass Flow (lb/h) 1.12 0.00 0.00 0.56 1.34 2.60 0.59 2.85 1.08 1.60 0.00 2.72 0.00 1.04 0.00 2.72 0.00 1.04 0.00 0.00 3.19 1.57 0.03 0.05 0.16 0.01 0.01 0.00 0.00 0.89 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.59 0.00 0.00 0.00 0.00 0.00 0.59 0.59 0.59 0.59 0.59 0.00
CONDENSER VENT GAS STREAM Temperature: Pressure: Flow Rate: Component	120.00 o 14.10 p 156.22 s Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Pentane n-Butane i-Pentane n-Butane i-Pentane Cyclopentane Cyclopentane Cyclopentane Cyclopentane n-Hexane n-Hexane 2,2,4-Trimethylpentane Ethylbenzene O-Xylene m-Xylene m-Xylene D-Xylene Methylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Ethylene Glycol Water Methanol O2 SO2	lieg F ssia cfh Conc. (mol%) 6.18 0.00 8.45 10.79 14.31 2.45 11.91 3.65 5.39 0.00 7.68 0.00 2.53 0.00 7.68 0.00 2.53 0.00 0.00 2.53 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	Mass Flow (lb/h)  1.12 0.00 0.00 0.05 1.34 2.60 0.59 2.85 1.08 1.60 0.00 2.72 0.00 1.04 0.00 2.72 0.00 1.04 0.00 0.00 3.19 1.57 0.03 0.05 0.16 0.01 0.00 0.00 0.00 0.00 0.00 0.00

TEX CONDENSER RECOVERED OIL STREA	AM			
Temperature:	120.00	deg F		
Pressure:	14.10	psia		
Flow Rate:	0.02	sgpm		
Component		Conc. (mol%)	Mass Flow (lb/h)	<u>,</u>
	Carbon Dioxide	0.	0.00	)
	Hydrogen Sulfide	0.	0.00	)
	Nitrogen	0.	0.00	)
	Methane	0.	0.00	)
	Ethane	0.	19 0.00	)
	Propane	0.	/3 0.02	2
	i-Butane	0.	26 0.03	<u>l</u>
	n-Butane	1.	92 0.08	3
	i-Pentane	1.	19 0.08	3
	n-Pentane	2.	35 0.15	
	Cyclopentane	0.		)
	n-Hexane	11.	12 0.72	2
	Cyclohexane	0.	0.00	)
	n-Heptane	10.	36 0.80	)
	Methylcyclohexane	0.	0.00	)
	2,2,4-Trimethylpentane	0.	0.00	)
	Benzene	25.	33 1.45	5
	Toluene	31.	17 2.12	2
	Ethylbenzene	1.	39 0.11	L
	o-Xylene	2.	0.21	L
	m-Xylene	8.	26 0.64	1
	p-Xylene	0.	55 0.05	5
	Triethylene Glycol	0.	00 0.00	)
	Ethylene Glycol	0.	0.00	)
	Water	0.	36 0.00	)
	Methanol	0.	0.00	)
	02	0.	0.00	)
	SO2	0.	0.00	)
STEX CONDENSER PRODUCED WATER ST	TREAM 120.00	deg F		
STEX CONDENSER PRODUCED WATER ST Temperature: Pressure:	<b>TREAM</b> 120.00 14.10	deg F psia		
STEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate:	TREAM 120.00 14.10 0.53	deg F psia sgpm		
STEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.53	deg F psia sgpm Conc. (mol%)	Mass Flow (lb/h)	
STEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.53 Carbon Dioxide	deg F psia sgpm Conc. (mol%) 0.	Mass Flow (lb/h) 20 0.02	1
STEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.53 Carbon Dioxide Hydrogen Sulfide	deg F psia sgpm Conc. (mol%) 0. 0.	Mass Flow (lb/h) 00 0.02 00 0.00	L )
STEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.53 Carbon Dioxide Hydrogen Sulfide Nitrogen	deg F psia sgpm Conc. (mol%) 0. 0. 0.	Mass Flow (lb/h) 00 0.02 00 0.00 00 0.00	
STEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.53 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane	deg F psia sgpm Conc. (mol%) 0. 0. 0. 0. 0. 0.	Mass Flow (lb/h) 10 0.02 10 0.00 10 0.00 10 0.00 10 0.00	
STEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.53 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane	deg F psia sgpm Conc. (mol%) 0. 0. 0. 0. 0. 0. 0.	Mass Flow (lb/h) 10 0.00 10 0.00 10 0.00 10 0.00 10 0.00 10 0.00	
STEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.53 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane	deg F psia sgpm Conc. (mol%) 0. 0. 0. 0. 0. 0.	Mass Flow (lb/h) 00 0.00 00 0.00 00 0.00 00 0.00 10 0.00 10 0.00 10 0.00	
STEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.53 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane	deg F psia sgpm Conc. (mol%) 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	Mass Flow (lb/h)           00         0.02           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00	
STEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.53 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane	deg F psia sgpm Conc. (mol%) 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	Mass Flow (lb/h) 10 0.00 10	
STEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.53 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane	deg F psia sgpm Conc. (mol%) 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	Mass Flow (lb/h)           00         0.02           00         0.01           00         0.02           00         0.01           00         0.01           00         0.01           00         0.01           00         0.01           00         0.01           00         0.01           00         0.01           00         0.01           00         0.01           00         0.01           00         0.01	
STEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.53 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane	deg F psia sgpm Conc. (mol%) 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	Mass Flow (lb/h)           00         0.02           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00	
STEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.53 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Butane i-Pentane n-Pentane Cyclopentane	deg F psia sgpm Conc. (mol%) 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	Mass Flow (lb/h)           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00	
STEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.53 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane Cyclopentane n-Hexane	deg F psia sgpm Conc. (mol%) 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	Mass Flow (lb/h)           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00	
STEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.53 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopentane	deg F psia sgpm Conc. (mol%) 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	Mass Flow (lb/h)           00         0.01           00         0.001           00         0.001           00         0.001           00         0.001           00         0.001           00         0.001           00         0.001           00         0.001           00         0.001           00         0.001           00         0.001           00         0.001           00         0.001           00         0.001           00         0.001           00         0.001           00         0.001	
STEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.53 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane Cyclopentane cyclopentane Cyclopexane n-Hexane	deg F psia sgpm Conc. (mol%) 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	Mass Flow (lb/h)           00         0.02           00         0.01           00         0.02           00         0.01	
STEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.53 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclohexane Methylcyclohexane	deg F psia sgpm Conc. (mol%) 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	Mass Flow (lb/h)           00         0.02	
STEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.53 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane i-Pentane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane 2,2,4-Trimethylogane	deg F psia sgpm Conc. (mol%) 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	Mass Flow (lb/h)           00         0.02           00         0.00	
STEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.53 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Butane n-Pentane Cyclopentane n-Hexane Cyclopextane Nethylopext	deg F psia sgpm Conc. (mol%) 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	Mass Flow (lb/h)           10         0.02           10         0.01           10         0.01           10         0.01           10         0.01           10         0.01           10         0.01           10         0.01           10         0.01           10         0.01           10         0.01           10         0.01           10         0.01           10         0.01           10         0.01           10         0.01           10         0.01           10         0.01           10         0.01           10         0.01	
STEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.53 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Butane n-Pentane n-Pentane Cyclopentane n-Hexane Cyclopexane n-Hexane Cyclopexane n-Hexane Qyclopexane n-Hexane Cyclopexane n-Hexane Cyclopexane n-Hexane Cyclopexane Toluene Benzene Toluene	deg F psia sgpm Conc. (mol%) 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	Mass Flow (lb/h)           100         0.01           100         0.001           100         0.001           100         0.001           100         0.001           100         0.001           100         0.001           100         0.001           100         0.001           100         0.001           100         0.001           100         0.001           100         0.001           100         0.001           11         0.116           100         0.001	
STEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.53 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Butane n-Pentane Cyclopentane Cyclopentane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene	deg F psia sgpm Conc. (mol%) 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	Mass Flow (lb/h)           00         0.02           00         0.01           00         0.02           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           00         0.00           01         0.00           02         0.00           03         0.00           04         0.00           05         0.00           06         0.00           07         0.00           08         0.00           09         0.00	
STEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.53 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane i-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclopexane n-Hexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene	deg F psia sgpm Conc. (mol%) 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	Mass Flow (lb/h)           00         0.02           00         0.02           00         0.02           00         0.02           00         0.02           00         0.02           00         0.02           00         0.02           00         0.02           00         0.02           00         0.02           00         0.02           00         0.02           00         0.02           00         0.02           00         0.02           01         0.02           02         0.02           03         0.02           04         0.02           05         0.02           06         0.02           07         0.02           08         0.02	
STEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.53 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Pentane Cyclopentane n-Pentane Cyclopexane n-Hexane Cyclopexane n-Hexane Cyclopexane n-Hexane Cyclopexane n-Hexane Cyclohexane N-Hexane Cyclohexane N-Hexane Cyclohexane N-Hexane Cyclohexane N-Hexane Cyclohexane N-Hexane Cyclohexane N-Hexane Cyclohexane N-Hexane Cyclohexane N-Hexane Cyclohexane N-Hexane Cyclohexane N-Hexane Cyclohexane N-Hexane Cyclohexane N-Hexane Cyclohexane N-Hexane Cyclohexane N-Hexane Cyclohexane N-He	deg F psia sgpm Conc. (mol%) 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	Mass Flow (lb/h)           00         0.02           00         0.00	
STEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.53 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Pentane n-Pentane Cyclopentane n-Pentane Cyclopextane n-Hexane Cyclopextane n-Hexane Cyclopextane n-Hepate Ethylbenzene Ethylbenzene Ethylbenzene Cyclopextane Methylcyclohexane Nethylcyclohexane Cyclopextane Methylcyclohexane Cyclopextane Methylcyclohexane Cyclopextane Methylcyclohexane Cyclopextane Nethylcyclohexane Cyclopextane Nethylcyclohexane Cyclopextane Nethylcyclohexane Cyclopextane Nethylcyclohexane Cyclopextane Methylcyclohexane Cyclopextane Nethylcyclohexane Cyclopextane Nethylcyclohexane Doluene Ethylbenzene Doluene Doluene Ethylbenzene Doluen	deg F psia sgpm Conc. (mol%) 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	Mass Flow (lb/h)           00         0.02           00         0.00           00 <t< td=""><td></td></t<>	
STEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.53 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane i-Pentane n-Pentane Cyclopentane n-Hexane Cyclopentane n-Hexane Cyclohexane n-Heptane Methylcyclohexane n-Heptane Methylcyclohexane n-Heptane Methylcyclohexane n-Heptane Methylcyclohexane n-Heptane Methylcyclohexane n-Kylene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol	deg F psia sgpm Conc. (mol%) 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	Mass Flow (lb/h)           00         0.02           00         0.00           00 <t< td=""><td></td></t<>	
STEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.53 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane Cyclopentane Cyclopentane Cyclopentane Cyclopentane 2,2,4-Trimethylopentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Triethylene Glycol Ethylene Glycol	deg F psia sgpm Conc. (mol%) 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	Mass Flow (lb/h)           00         0.02           00         0.00           00 <t< td=""><td></td></t<>	
STEX CONDENSER PRODUCED WATER ST Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.53 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Pentane Cyclopentane n-Pentane Cyclopentane n-Hexane Cyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene o-Xylene m-Xylene p-Xylene Cyclone Glycol Ethylene Glycol	deg F psia sgpm Conc. (mol%) 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	Mass Flow (lb/h)           10         0.02           10         0.02           10         0.02           10         0.02           10         0.02           10         0.02           10         0.02           10         0.02           10         0.02           10         0.02           10         0.02           10         0.02           10         0.02           10         0.02           10         0.02           11         0.02           10         0.02           11         0.02           10         0.02           10         0.02           10         0.02           10         0.02           10         0.02           10         0.02           10         0.02           10         0.02           10         0.02           10         0.02           10         0.02           10         0.02           10         0.02           10         0.02           10 <t< td=""><td></td></t<>	
STEX CONDENSER PRODUCED WATER ST Femperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.53 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Butane n-Pentane Cyclopexnane n-Hexane Cyclopexnane Toluene n-Xylene p-Xylene Gycol Ethylbenc Glycol Water Methanol	deg F psia sgpm Conc. (mol%) 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	Mass Flow (lb/h)           00         0.02           100         0.01           100         0.02           100         0.01	
STEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.53 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane n-Porpane i-Butane n-Pentane n-Pentane Cyclopextane n-Hexane Cyclopextane n-Hexane Cyclopextane n-Hexane Cyclohexane n-Hexane Cyclohexane n-Heptane 8enzene Toluene Ethylbenzene Ethylbenzene Doluene Ethylbenzene Doluene Ethylbenzene Doluene Ethylbenzene Doluene Ethylbenzene Doluene Ethylbenzene Doluene Ethylbenzene Doluene Ethylbenzene Doluene Ethylbenzene Doluene Ethylbenzene Doluene Ethylbenzene Doluene Ethylbenzene Doluene Do	deg F psia sgpm Conc. (mol%) 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	Mass Flow (lb/h)           00         0.07           00         0.00           00 <t< td=""><td></td></t<>	
STEX CONDENSER PRODUCED WATER ST Temperature: Pressure: Flow Rate: Component	TREAM 120.00 14.10 0.53 Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane i-Butane n-Butane n-Butane n-Butane cyclopentane n-Hexane Cyclopentane n-Hexane Cyclohexane n-Hexane Cyclohexane n-Heptane Methylcyclohexane n-Heptane Methylcyclohexane n-Heptane Benzene Toluene Ethylbenzene o-xylene Triethylene Glycol Ethylene Glycol	deg F psia sgpm Conc. (mol%) 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	Mass Flow (lb/h)           00         0.02           00         0.00           00 <t< td=""><td></td></t<>	

#### Horned Frog CS Tanks

#### Oil TP: 143,208 bbl/y Water TP: 177,190 bbl/y

#### Sample: Horned Frog Condensate



Annual – 2 x 400 bbl Produced Water Tanks

Process Streams		Cond Breathing	Cond F/W/B/L	Cond W&B	Cond Flashing
Composition	Status:	Solved	Solved		Solved
Phase: Total	From Block:		MIX-103		
	To Block:	MIX-103			MIX-103
Mole Fraction		%	%		%
Nitrogen		0*	0		0*
Methane		1.30505*	3.14789		3.47346*
CO2		0*	0		0*
Ethane		8.83674*	5.85311		5.32600*
Propane		21.1921*	17.5163		16.8669*
i-Butane		7.18419*	6.84215		6.78173*
n-Butane		27.0251*	26.0127		25.8339*
i-Pentane		10.0455*	10.9259		11.0814*
n-Pentane		12.6324*	14.1278		14.3920*
i-Hexane		3.57422*	4.16491		4.26927*
Hexane		5.76676*	6.93132		7.13706*
2,2,4-Trimethylpentane		0*	0		0*
Benzene		0.203795*	0.386960		0.419319*
Heptane		1.82027*	2.45100		2.56242*
Toluene		0.118224*	0.232577		0.252779*
Octane		0.240509*	0.387591		0.413576*
Ethylbenzene		0.00320745*	0.00658563		0.00718244*
m-Xylene		0.0160213*	0.0338258		0.0369713*
o-Xylene		0.00123210*	0.00292967		0.00322958*
p-Xylene		0.00434218*	0.00886483		0.00966383*
Nonane		0.0219796*	0.0443889		0.0483479*
		0.00774732*	0.0193553		0.0214061*
			0.903644		1.06319"
Undecane Molar Flow		7.16490E-00	0.000165617		0.000162416
Nitrogon		0*			0*
Methane		0 000524631*	0 0417028		0 0391070*
		0.000324031 0*	0.0417020		0.0091070
Ethane		0 00355238*	0 0775411		0 0599644*
Propane		0.00333230	0.232053		0.00000044
i-Butane		0.00288805*	0.0906438		0.0763541*
n-Butane		0 0108641*	0 344613		0 290858*
i-Pentane		0 00403829*	0 144745		0 124764*
n-Pentane		0.00507823*	0.187163		0.162037*
i-Hexane		0.00143684*	0 0551761		0.0480668*
Hexane		0.00231825*	0.0918251		0.0803547*
2.2.4-Trimethylpentane		0*	0		0*
Benzene		8.19259E-05*	0.00512638		0.00472102*
Heptane		0.000731752*	0.0324704		0.0288498*
Toluene		4.75262E-05*	0.00308114		0.00284598*
Octane		9.66850E-05*	0.00513475		0.00465636*
Ethylbenzene		1.28940E-06*	8.72454E-05		8.08656E-05*
m-Xylene		6.44057E-06*	0.000448119		0.000416252*
o-Xylene		4.95305E-07*	3.88119E-05		3.63612E-05*
p-Xylene		1.74556E-06*	0.000117440		0.000108803*
Nonane		8.83583E-06*	0.000588057		0.000544339*
Decane		3.11443E-06*	0.000256416		0.000241006*
Water		2.25531E-07*	0.0119713		0.0119702*
Undecane		2.88836E-08*	2.19672E-06		2.05381E-06*

Wass Traction	%	%		%
Nitrogen	0	0		0
Methane	0.355221	0.835521		0.917903
CO2	0	0		0
Ethane	4.50830	2.91188		2.63806
Propane	15.8552	12.7792		12.2516
i-Butane	7.08469	6.57963		6.49300
n-Butane	26.6509	25.0147		24.7340
i-Pentane	12.2970	13.0423		13.1701
n-Pentane	15.4638	16.8644		17.1047
i-Hexane	5.22596	5.93821		6.06038
Hexane	8.43173	9.88248		10.1313
2,2,4-Trimethylpentane	0	0		0
Benzene	0.270092	0.500091		0.539541
Heptane	3.09467	4.06336		4.22951
Toluene	0.184819	0.354547		0.383658
Octane	0.466130	0.732513		0.778203
Ethylbenzene	0.00577753	0.0115677		0.0125608
m-Xylene	0.0288589	0.0594150		0.0646560
o-Xylene	0.00221936	0.00514597		0.00564795
p-Xylene	0.00782151	0.0155711		0.0169003
Nonane	0.0478295	0.0941923		0.102145
Decane	0.0187026	0.0455634		0.0501706
Water	0.000171483	0.269343		0.315511
Undecane	0.000190549	0.000428823		0.000469692
Mass Flow	lb/h	lb/h		lb/h
Nitrogen	0*	0	0*	0*
Nillogon	0	0	0	0
Methane	0.00841638*	0.669015	0.033567231*	0.627372*
Methane CO2	0.00841638* 0*	0.669015 0	0.033567231* 0*	0.627372* 0*
Methane CO2 Ethane	0.00841638* 0* 0.106817*	0.669015 0 2.33159	0.033567231* 0* 0.426019635*	0.627372* 0* 1.80307*
Methane CO2 Ethane Propane	0.00841638* 0* 0.106817* 0.375662*	0.669015 0 2.33159 10.2325	0.033567231* 0* 0.426019635* 1.498261984*	0.627372* 0* 1.80307* 8.37378*
Methane CO2 Ethane Propane i-Butane	0.00841638* 0* 0.106817* 0.375662* 0.167860*	0.669015 0 2.33159 10.2325 5.26842	0.033567231* 0* 0.426019635* 1.498261984* 0.669480076*	0.627372* 0* 1.80307* 8.37378* 4.43787*
Methane CO2 Ethane Propane i-Butane n-Butane	0.00841638* 0* 0.106817* 0.375662* 0.167860* 0.631448*	0.669015 0 2.33159 10.2325 5.26842 20.0297	0.033567231* 0* 0.426019635* 1.498261984* 0.669480076* 2.518418397*	0.627372* 0* 1.80307* 8.37378* 4.43787* 16.9053*
Metgen Methane CO2 Ethane Propane i-Butane n-Butane i-Pentane	0.00841638* 0* 0.106817* 0.375662* 0.167860* 0.631448* 0.291358*	0.669015 0 2.33159 10.2325 5.26842 20.0297 10.4432	0.033567231* 0* 0.426019635* 1.498261984* 0.669480076* 2.518418397* 1.162028945*	0.627372* 0* 1.80307* 8.37378* 4.43787* 16.9053* 9.00155*
Metgan Methane CO2 Ethane Propane i-Butane n-Butane i-Pentane n-Pentane	0.00841638* 0* 0.106817* 0.375662* 0.167860* 0.631448* 0.291358* 0.366388*	0.669015 0 2.33159 10.2325 5.26842 20.0297 10.4432 13.5036	0.033567231* 0* 0.426019635* 1.498261984* 0.669480076* 2.518418397* 1.162028945* 1.461273997*	0.627372* 0* 1.80307* 8.37378* 4.43787* 16.9053* 9.00155* 11.6908*
Methane CO2 Ethane Propane i-Butane n-Butane i-Pentane n-Pentane i-Hexane	0.00841638* 0* 0.106817* 0.375662* 0.167860* 0.631448* 0.291358* 0.366388* 0.123820*	0.669015 0 2.33159 10.2325 5.26842 20.0297 10.4432 13.5036 4.75482	0.033567231* 0* 0.426019635* 1.498261984* 0.669480076* 2.518418397* 1.162028945* 1.461273997* 0.49383581*	0.627372* 0* 1.80307* 8.37378* 4.43787* 16.9053* 9.00155* 11.6908* 4.14217*
Methane CO2 Ethane Propane i-Butane n-Butane i-Pentane n-Pentane i-Hexane Hexane	0.00841638* 0* 0.106817* 0.375662* 0.167860* 0.631448* 0.291358* 0.366388* 0.123820* 0.199776*	0.669015 0 2.33159 10.2325 5.26842 20.0297 10.4432 13.5036 4.75482 7.91306	0.033567231* 0* 0.426019635* 1.498261984* 0.669480076* 2.518418397* 1.162028945* 1.461273997* 0.49383581* 0.796770351*	0.627372* 0* 1.80307* 8.37378* 4.43787* 16.9053* 9.00155* 11.6908* 4.14217* 6.92459*
Methane CO2 Ethane Propane i-Butane n-Butane i-Pentane n-Pentane i-Hexane Hexane Hexane	0.00841638* 0* 0.106817* 0.375662* 0.167860* 0.631448* 0.291358* 0.366388* 0.123820* 0.199776* 0*	0.669015 0 2.33159 10.2325 5.26842 20.0297 10.4432 13.5036 4.75482 7.91306 0	0.033567231* 0* 0.426019635* 1.498261984* 0.669480076* 2.518418397* 1.162028945* 1.461273997* 0.49383581* 0.796770351* 0*	0.627372* 0* 1.80307* 8.37378* 4.43787* 16.9053* 9.00155* 11.6908* 4.14217* 6.92459* 0*
Methane CO2 Ethane Propane i-Butane n-Butane i-Pentane n-Pentane i-Hexane Hexane 2,2,4-Trimethylpentane Benzene	0.00841638* 0* 0.106817* 0.375662* 0.167860* 0.631448* 0.291358* 0.366388* 0.123820* 0.199776* 0* 0.00639938*	0.669015 0 2.33159 10.2325 5.26842 20.0297 10.4432 13.5036 4.75482 7.91306 0 0.400431	0.033567231* 0* 0.426019635* 1.498261984* 0.669480076* 2.518418397* 1.162028945* 1.461273997* 0.49383581* 0.796770351* 0* 0* 0.025522804*	0.627372* 0* 1.80307* 8.37378* 4.43787* 16.9053* 9.00155* 11.6908* 4.14217* 6.92459* 0* 0.368768*
Methane CO2 Ethane Propane i-Butane n-Butane i-Pentane i-Pentane i-Hexane Hexane 2,2,4-Trimethylpentane Benzene Heptane	0.00841638* 0* 0.106817* 0.375662* 0.167860* 0.631448* 0.291358* 0.366388* 0.123820* 0.199776* 0* 0.00639938* 0.0733230*	0.669015 0 2.33159 10.2325 5.26842 20.0297 10.4432 13.5036 4.75482 7.91306 0 0.400431 3.25360	0.033567231* 0* 0.426019635* 1.498261984* 0.669480076* 2.518418397* 1.162028945* 1.461273997* 0.49383581* 0.796770351* 0* 0.025522804* 0.292435832*	0.627372* 0* 1.80307* 8.37378* 4.43787* 16.9053* 9.00155* 11.6908* 4.14217* 6.92459* 0* 0.368768* 2.89080*
Methane CO2 Ethane Propane i-Butane n-Butane i-Pentane i-Pentane i-Pentane i-Hexane Hexane 2,2,4-Trimethylpentane Benzene Heptane Toluene	0.00841638* 0* 0.106817* 0.375662* 0.167860* 0.631448* 0.291358* 0.366388* 0.123820* 0.199776* 0* 0.00639938* 0.0733230* 0.00437899*	0.669015 0 2.33159 10.2325 5.26842 20.0297 10.4432 13.5036 4.75482 7.91306 0 0.400431 3.25360 0.283891	0.033567231* 0* 0.426019635* 1.498261984* 0.669480076* 2.518418397* 1.162028945* 1.461273997* 0.49383581* 0.796770351* 0* 0.025522804* 0.292435832* 0.017464831*	0.627372* 0* 1.80307* 8.37378* 4.43787* 16.9053* 9.00155* 11.6908* 4.14217* 6.92459* 0* 0.368768* 2.89080* 0.262225*
Methane CO2 Ethane Propane i-Butane n-Butane i-Pentane i-Pentane i-Hexane 2,2,4-Trimethylpentane Benzene Heptane Toluene Octane	0.00841638* 0* 0.106817* 0.375662* 0.167860* 0.631448* 0.291358* 0.366388* 0.123820* 0.199776* 0* 0.00639938* 0.0733230* 0.00437899* 0.0110442*	0.669015 0 2.33159 10.2325 5.26842 20.0297 10.4432 13.5036 4.75482 7.91306 0 0.400431 3.25360 0.283891 0.586535	0.033567231* 0* 0.426019635* 1.498261984* 0.669480076* 2.518418397* 1.162028945* 1.461273997* 0.49383581* 0.796770351* 0* 0.025522804* 0.292435832* 0.017464831* 0.044047788*	0.627372* 0* 1.80307* 8.37378* 4.43787* 16.9053* 9.00155* 11.6908* 4.14217* 6.92459* 0* 0.368768* 2.89080* 0.262225* 0.531889*
Methane CO2 Ethane Propane i-Butane n-Butane i-Pentane i-Pentane i-Hexane 4exane 2,2,4-Trimethylpentane Benzene Heptane Toluene Octane Ethylbenzene	0.00841638* 0* 0.106817* 0.375662* 0.167860* 0.631448* 0.291358* 0.366388* 0.123820* 0.199776* 0* 0.00639938* 0.0733230* 0.00437899* 0.0110442* 0.000136889* 0.000136889*	0.669015 0 2.33159 10.2325 5.26842 20.0297 10.4432 13.5036 4.75482 7.91306 0 0.400431 3.25360 0.283891 0.586535 0.00926241	0.033567231* 0* 0.426019635* 1.498261984* 0.669480076* 2.518418397* 1.162028945* 1.461273997* 0.49383581* 0.796770351* 0* 0.025522804* 0.292435832* 0.017464831* 0.044047788* 0.00545958*	0.627372* 0* 1.80307* 8.37378* 4.43787* 16.9053* 9.00155* 11.6908* 4.14217* 6.92459* 0* 0.368768* 2.89080* 0.262225* 0.531889* 0.00858510*
Methane CO2 Ethane Propane i-Butane n-Butane i-Pentane n-Pentane i-Pentane i-Hexane 2,2,4-Trimethylpentane Benzene Heptane Toluene Octane Ethylbenzene m-Xylene	0.00841638* 0* 0.106817* 0.375662* 0.167860* 0.631448* 0.291358* 0.366388* 0.123820* 0.199776* 0* 0.00639938* 0.0733230* 0.00437899* 0.0110442* 0.000136889* 0.000683764*	0.669015 0 2.33159 10.2325 5.26842 20.0297 10.4432 13.5036 4.75482 7.91306 0 0.400431 3.25360 0.283891 0.586535 0.00926241 0.0475745	0.033567231* 0* 0.426019635* 1.498261984* 0.669480076* 2.518418397* 1.162028945* 1.461273997* 0.49383581* 0.796770351* 0* 0.025522804* 0.292435832* 0.017464831* 0.044047788* 0.000545958* 0.00272707*	0.627372* 0* 1.80307* 8.37378* 4.43787* 16.9053* 9.00155* 11.6908* 4.14217* 6.92459* 0* 0.368768* 2.89080* 0.262225* 0.531889* 0.00858510* 0.0441914*
Methane Methane CO2 Ethane Propane i-Butane n-Butane i-Pentane n-Pentane i-Pentane i-Hexane 4exane 2,2,4-Trimethylpentane Benzene Heptane Toluene Octane Ethylbenzene m-Xylene o-Xylene	0.00841638* 0* 0.106817* 0.375662* 0.167860* 0.631448* 0.291358* 0.366388* 0.123820* 0.199776* 0* 0.00639938* 0.0733230* 0.00437899* 0.0110442* 0.000136889* 0.000683764* 5.25840E-05*	0.669015 0 2.33159 10.2325 5.26842 20.0297 10.4432 13.5036 4.75482 7.91306 0 0.400431 3.25360 0.283891 0.586535 0.00926241 0.0475745 0.00412046	0.033567231* 0* 0.426019635* 1.498261984* 0.669480076* 2.518418397* 1.162028945* 1.461273997* 0.49383581* 0.796770351* 0* 0.025522804* 0.292435832* 0.017464831* 0.044047788* 0.000545958* 0.00272707* 0.000209722*	0.627372* 0* 1.80307* 8.37378* 4.43787* 16.9053* 9.00155* 11.6908* 4.14217* 6.92459* 0* 0.368768* 2.89080* 0.262225* 0.531889* 0.00858510* 0.0441914* 0.00386028*
Methane Methane CO2 Ethane Propane i-Butane n-Butane i-Pentane n-Pentane i-Pentane i-Hexane 2,2,4-Trimethylpentane Benzene Heptane Toluene Octane Ethylbenzene m-Xylene o-Xylene p-Xylene	0.00841638* 0* 0.106817* 0.375662* 0.167860* 0.631448* 0.291358* 0.366388* 0.123820* 0.199776* 0* 0.00639938* 0.0733230* 0.00437899* 0.0110442* 0.000136889* 0.000136889* 0.000185318* 0.000185318*	0.669015 0 2.33159 10.2325 5.26842 20.0297 10.4432 13.5036 4.75482 7.91306 0 0.400431 3.25360 0.283891 0.586535 0.00926241 0.0475745 0.00412046 0.0124680 0.0376412	0.033567231* 0* 0.426019635* 1.498261984* 0.669480076* 2.518418397* 1.162028945* 1.461273997* 0.49383581* 0.796770351* 0* 0.025522804* 0.292435832* 0.017464831* 0.044047788* 0.000545958* 0.00272707* 0.000209722* 0.000739107*	0.627372* 0* 1.80307* 8.37378* 4.43787* 16.9053* 9.00155* 11.6908* 4.14217* 6.92459* 0* 0.368768* 2.89080* 0.262225* 0.531889* 0.00858510* 0.0441914* 0.00386028* 0.0115511*
Methane Methane CO2 Ethane Propane i-Butane n-Butane n-Pentane n-Pentane i-Pentane i-Hexane 2,2,4-Trimethylpentane Benzene Heptane Toluene Octane Ethylbenzene m-Xylene o-Xylene p-Xylene Nonane	0.00841638* 0* 0.106817* 0.375662* 0.167860* 0.631448* 0.291358* 0.366388* 0.123820* 0.199776* 0* 0.00639938* 0.0733230* 0.00437899* 0.0110442* 0.000136889* 0.000136889* 0.000135318* 0.000113324* 0.000113324*	0.669015 0 2.33159 10.2325 5.26842 20.0297 10.4432 13.5036 4.75482 7.91306 0 0.400431 3.25360 0.283891 0.586535 0.00926241 0.0475745 0.00412046 0.0124680 0.0754213 0.0262213	0.033567231* 0* 0.426019635* 1.498261984* 0.669480076* 2.518418397* 1.162028945* 1.461273997* 0.49383581* 0.796770351* 0* 0.025522804* 0.292435832* 0.017464831* 0.044047788* 0.000545958* 0.00272707* 0.000209722* 0.000739107* 0.004319726*	0.627372* 0* 1.80307* 8.37378* 4.43787* 16.9053* 9.00155* 11.6908* 4.14217* 6.92459* 0* 0.368768* 2.89080* 0.262225* 0.531889* 0.00858510* 0.0441914* 0.00386028* 0.0115511* 0.0698142*
Methane Methane CO2 Ethane Propane i-Butane n-Butane n-Pentane n-Pentane i-Pentane i-Hexane 2,2,4-Trimethylpentane Benzene Heptane Zoluene Octane Ethylbenzene m-Xylene o-Xylene p-Xylene Nonane Decane	0.00841638* 0* 0.106817* 0.375662* 0.167860* 0.631448* 0.291358* 0.366388* 0.123820* 0.199776* 0* 0.00639938* 0.0733230* 0.00437899* 0.0110442* 0.00013689* 0.00013689* 0.00013689* 0.000135318* 0.000143127* 0.000443127*	0.669015 0 2.33159 10.2325 5.26842 20.0297 10.4432 13.5036 4.75482 7.91306 0 0.400431 3.25360 0.283891 0.586535 0.00926241 0.0475745 0.00412046 0.0124680 0.0754213 0.0364833 0.262627	0.033567231* 0* 0.426019635* 1.498261984* 0.669480076* 2.518418397* 1.162028945* 1.461273997* 0.49383581* 0.796770351* 0* 0.025522804* 0.292435832* 0.017464831* 0.044047788* 0.000545958* 0.00272707* 0.00029722* 0.000739107* 0.004519726* 0.001767333* 4.6004555*	0.627372* 0* 1.80307* 8.37378* 4.43787* 16.9053* 9.00155* 11.6908* 4.14217* 6.92459* 0* 0.368768* 2.89080* 0.262225* 0.531889* 0.00858510* 0.0441914* 0.00386028* 0.0115511* 0.0698142* 0.0342908*
Methane Methane CO2 Ethane Propane i-Butane n-Butane n-Pentane i-Pentane n-Pentane i-Hexane 2,2,4-Trimethylpentane Benzene Heptane Toluene Octane Ethylbenzene m-Xylene o-Xylene p-Xylene Nonane Decane Water	0.00841638* 0* 0.106817* 0.375662* 0.167860* 0.631448* 0.291358* 0.366388* 0.123820* 0.199776* 0* 0.00639938* 0.0733230* 0.00437899* 0.0110442* 0.000136889* 0.00013689* 0.000185318* 0.00013324* 0.000143127* 4.06301E-06*	0.669015 0 2.33159 10.2325 5.26842 20.0297 10.4432 13.5036 4.75482 7.91306 0 0.400431 3.25360 0.283891 0.586535 0.00926241 0.0475745 0.00412046 0.0124680 0.0754213 0.0364833 0.215667	0.033567231* 0* 0.426019635* 1.498261984* 0.669480076* 2.518418397* 1.162028945* 1.461273997* 0.49383581* 0.796770351* 0* 0.025522804* 0.292435832* 0.017464831* 0.044047788* 0.002545958* 0.00272707* 0.00029722* 0.000739107* 0.004519726* 0.001767333* 1.62046E-05* 4.90625.05*	0.627372* 0* 1.80307* 8.37378* 4.43787* 16.9053* 9.00155* 11.6908* 4.14217* 6.92459* 0* 0.368768* 2.89080* 0.262225* 0.531889* 0.00858510* 0.0441914* 0.00386028* 0.0115511* 0.0698142* 0.0342908* 0.215647*

Process Streams		Cond Breathing	Cond F/W/B	Cond Flashing
Properties	Status:	Solved	Solved	Solved
Phase: Total	From Block:		MIX-103	
	To Block:	MIX-103		MIX-103
Property	Units			
Temperature	°F	76.2171	94.1767	97.8
Pressure	psia	10.2648	10.2648	12.8800
Mole Fraction Vapor	%	100	100	100
Mole Fraction Light Liquid	%	0	0	0
Mole Fraction Heavy Liquid	%	0	0	0
Phase Mole Fraction	%	100	100	100
Molecular Weight	lb/lbmol	58.9384	60.4412	60.7067
Mass Density	lb/ft^3	0.107322	0.106394	0.133852
Molar Flow	lbmol/h	0.0402001	1.32478	1.12588
Mass Flow	lb/h	2.36933	80.0716	68.3484
Vapor Volumetric Flow	ft^3/h	22.0769	752.597	510.629
Liquid Volumetric Flow	gpm	2.75245	93.8303	63.6628
Std Vapor Volumetric Flow	MMSCFD	0.000366128	0.0120656	0.0102541
Std Liquid Volumetric Flow	sgpm	0.00823923	0.273165	0.232398
Compressibility		0.980218	0.981100	0.976437
Specific Gravity		2.03499	2.08688	2.09605
API Gravity				
Enthalpy	Btu/h	-2213.07	-74258.4	-63308.4
Mass Enthalpy	Btu/lb	-934.048	-927.400	-926.259
Mass Cp	Btu/(lb*°F)	0.401645	0.411625	0.414336
Ideal Gas CpCv Ratio		1.09225	1.08733	1.08645
Dynamic Viscosity	cP	0.00752591	0.00772069	0.00777066
Kinematic Viscosity	cSt	4.37774	4.53022	3.62421
Thermal Conductivity	Btu/(h*ft*°F)	0.00925929	0.00979809	0.00992005
Surface Tension	lbf/ft			
Net Ideal Gas Heating Value	Btu/ft^3	3048.06	3111.72	3122.97
Net Liquid Heating Value	Btu/lb	19466.4	19376.5	19361.0
Gross Ideal Gas Heating Value	e Btu/ft^3	3301.82	3369.81	3381.82
Gross Liquid Heating Value	Btu/lb	21100.7	20997.3	20979.5
	Cond Working	Jondensate to	CP Presthing	
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d Loading	Cond working	Tanks	GB Breatning	GB W&B
Solved	Solved	Solved	Solved	
		Gunbarrel		
MIX-103	MIX-103		MIX-105	
/0	/0	/0	/0	
1 30505*	1 30505*	0 105386	0 701151*	
0*	0*	0.100000	0.701101	
8 83674*	8 83674*	0 267270	5 14917*	
21.1921*	21.1921*	1.71611	13.8514*	
7.18419*	7.18419*	1.40887	5.02721*	
27.0251*	27.0251*	7.53464	19.2960*	
10.0455*	10.0455*	7.09731	7.37357*	
12.6324*	12.6324*	12.0066	9.32292*	
3.57422*	3.57422*	8.26782	2.66559*	
5.76676*	5.76676*	18.8053	4.30974*	
0*	0*	0	0*	
0.203795*	0.203795*	1.07326	0.153215*	
1.82027*	1.82027*	20.2851	1.36567*	
0.118224*	0.118224*	2.13688	0.0888179*	
0.240509*	0.240509*	9.87761	0.180674*	
0.00320745*	0.00320745*	0.179896	0.00241038*	
0.0160213*	0.0160213*	1.02956	0.0120388*	
0.00123210*	0.00123210*	0.0999358	0.000926071*	
0.00434218*	0.00434218*	0.259880	0.00326287*	
0.0219796*	0.0219796*	3.39918	0.0165184*	
0.00774732*	0.00774732*	4.29896	0.00582336*	
0.000561020*	0.000561020*	0.0404807	30.4738*	
7.18496E-05*	7.18496E-05*	0.109973	5.40027E-05*	
Ibmol/h	Ibmol/h	lbmol/h	lbmol/h	
0*	0*	0	0*	
0.000503414*	0.00156777*	0.0453213	7.02729E-06*	
0*	0*	0	0*	
0.00340871*	0.0106157*	0.114940	5.16075E-05*	
0.00817472*	0.0254583*	0.738015	0.000138826*	
0.00277125*	0.00863044*	0.605884	5.03852E-05*	
0.0104248*	0.0324656"	3.24028	0.000193394*	
0.00387497*	0.0120677*	3.05220	7.39015E-05"	
0.00407200	0.0101754	D. 10340	9.34309E-05	
0.00137673	0.00429375	3.00000	2.07 100E-00 4 21042E 05*	
0.00222449	0.00092707	0.00724	4.31943⊑-03 0*	
0 7 86125E_05*	0 000244821*	0 461555	0 1 53560E-06*	
0.000702158*	0.000244021	8 72360	1.35300E-00	
4 56041E-05*	0.000142024*	0.12000	8 90177E-07*	
9 27748E-05*	0.000288926*	4 24787	1 81081F-06*	
1 23725E-06*	3 85314F-06*	0 0773642	2 41580E-08*	
6.18010E-06*	1.92465E-05*	0.442761	1.20659E-07*	
4.75273E-07*	1.48013E-06*	0.0429775	9.28154E-09*	
1.67497E-06*	5.21631E-06*	0.111761	3.27022E-08*	
8.47848E-06*	2.64043E-05*	1.46182	1.65556E-07*	
2.98848E-06*	9.30693E-06*	1.84877	5.83646E-08*	
2.16410E-07*	6.73960E-07*	0.0174087	0.000305424*	
2.77155E-08*	8.63137E-08*	0.0472941	5.41241E-10*	

%	%	%	%	
0	0	0	0	
0.355221	0.355221	0.0188051	0.237912	
0	0	0	0	
4.50830	4.50830	0.0893909	3.27484	
15.8552	15.8552	0.841714	12.9188	
7.08469	7.08469	0.910826	6.18020	
26.6509	26.6509	4.87111	23.7216	
12.2970	12.2970	5.69568	11.2523	
15.4638	15.4638	9.63548	14.2270	
5.22596	5.22596	7.92497	4.85859	
8.43173	8.43173	18.0255	7.85539	
0	0	0	0	
0.270092	0.270092	0.932489	0.253135	
3.09467	3.09467	22.6087	2.89439	
0.184819	0.184819	2.19000	0.173091	
0.466130	0.466130	12.5502	0.436520	
0.00577753	0.00577753	0.212434	0.00541252	
0.0288589	0.0288589	1.21578	0.0270332	
0.00221936	0.00221936	0.118012	0.00207950	
0.00782151	0.00782151	0.306886	0.00732682	
0.0478295	0.0478295	4.84922	0.0448101	
0.0187026	0.0187026	6.80355	0.0175249	
0.000171483	0.000171483	0.00811170	11.6119	
0.000190549	0.000190549	0.191202	0.000178538	
lb/h	lb/h	lb/h	lb/h	
0*	0*	0	0*	0*
0.00807599*	0.0251509*	0.727065	0.000112735*	0.004020392*
0*	0*	0	0*	0*
0.102497*	0.319203*	3.45613	0.00155179*	0.055340371*
0.360469*	1.12260*	32.5432	0.00612160*	0.218310615*
0.161071*	0.501620*	35.2153	0.00292850*	0.104437023*
0.605910*	1.88697*	188.332	0.0112405*	0.400862562*
0.279574*	0.870671*	220.213	0.00533191*	0.190148199*
0.351570*	1.09489*	372.537	0.00674151*	0.240417766*
0.118813*	0.370015*	306.404	0.00230225*	0.082103517*
0.191696*	0.596995*	696.920	0.00372229*	0.132745446*
0* 0.00011057*	*0	0	*0	*0
0.00614057*	0.0191234*	36.0529	0.000119949*	0.004277644*
0.0703576*	0.219113*	874.122	0.00137151*	0.048911237*
0.00420189*	0.0130858*	84.6722	8.20195E-05*	0.002925007*
0.0105975*	0.0330036*	485.228	0.000206846*	0.007376603*
0.000131353*	0.000409069*	8.21337	2.56473E-06*	9.14643E-05*
0.000656110*	0.00204331*	47.0057	1.28097E-05*	0.000456825*
5.04574E-05*	0.000157138*	4.56270	9.85375E-07*	3.51408E-05*
0.000177823*	0.000553789*	11.8652	3.47182E-06*	0.000123813*
0.00108741*	0.00338649*	187.486	2.12333E-05*	0.00075723*
0.000425205*	0.00132421*	263.046	8.30422E-06*	0.000296148*
3.89868E-06*	1.21416E-05*	0.313623	0.00550229*	0.196224607*
4 33216E_06*	1 34915-05*	7 39246	8.46005E-08*	3.01705E-06*

Cond Loading	Cond Working	ondensate to Tan	GB Breathing	
Solved	Solved	Solved	Solved	
		Gunbarrel		
MIX-103	MIX-103		MIX-105	
76.2171	76.2171	70	76.1390	
10.2648	10.2648	14.6959	1.46621	
100	100	0	100	
0	C	100	0	
0	C	0	0	
100	100	100	100	
58.9384	58.9384	89.9035	47.2788	
0.107322	0.107322	42.1052	0.0120787	
0.0385743	0.120131	43.0051	0.00100225	
2.27351	7.08034	3866.31	0.0473851	
21.1841	65.9730	91.8250	3.92303	
2.64113	8.22520	11.4483	0.489106	
0.000351320	0.00109411	0.391674	9.12811E-06	
0.00790601	0.0246215	11.4435	0.000155226	
0.980218	0.980218	0.00552039	0.998085	
2.03499	2.03499	0.675100	1.63241	
		76.5330		
-2123.57	-6613.37	-3.64041E+06	-70.5934	
-934.048	-934.048	-941.572	-1489.78	
0.401645	0.401645	0.519999	0.404272	
1.09225	1.09225	1.06095	1.11605	
0.00752591	0.00752591	0.341676	0.00834181	
4.37774	4.37774	0.506592	43.1141	
0.00925929	0.00925929	0.0699816	0.00925756	
		0.00128683		
3048.06	3048.06	4565.83	2159.35	
19466.4	19466.4	19112.4	17068.4	
3301.82	3301.82	4923.09	2354.00	
21100.7	21100.7	20620.7	18631.1	

GB F/W/B	<b>GB</b> Flashing	GB Working	Liquid To GB	PW Breathing	PW W&B
Solved	Solved	Solved	Solved	Solved	
MIX-105			MIX-106		
	MIX-105	MIX-105	Gunbarrel	MIX-101	
%	%	%	%	%	
0	0*	0*	0	0*	
2.38195	2.41581*	0.701151*	0.0108444	0.831929*	
0	0*	0*	0	0*	
4.16207	4.14218*	5.14917*	0.0266181	0.387469*	
14.8063	14.8255*	13.8514*	0.169567	0.114584*	
6.36292	6.38983*	5.02721*	0.139006	0.00821849*	
24.7311	24.8406*	19.2960*	0.743336	0.0272359*	
10.8847	10.9554*	7.37357*	0.699959	0.00253088*	
14.2056	14.3040*	9.32292*	1.18401	0.000677877*	
4.25400	4.28600*	2.66559*	0.815304	0.000115009*	
7.12447	7.18118*	4.30974*	1.85440	4.67500E-05*	
0	0*	0*	0	0*	
0.415612	0.420899*	0.153215*	0.106473	0.00301772*	
2.56239	2.58650*	1.36567*	2.00030	2.63233E-06*	
0.251436	0.254713*	0.0888179*	0.210973	0.000349852*	
0.413188	0.417872*	0.180674*	0.974027	2.45314E-08*	
0.00715051	0.00724602*	0.00241038*	0.0177454	2.63296E-06*	
0.0368068	0.0373059*	0.0120388*	0.101543	7.37336E-06*	
0.00321142	0.00325746*	0.000926071*	0.00985857	1.19650E-06*	
0.00962392	0.00975209*	0.00326287*	0.0256323	2.31759E-06*	
0.0482646	0.0489043*	0.0165184*	0.335191	6.10509E-10*	
0.0213214	0.0216337*	0.00582336*	0.423919	7.00293E-12*	
7.31776	6.85118*	30.4738*	90.1404	98.6238*	
0.000181799	0.000184374*	5.40027E-05*	0.0108444	1.67088E-14*	
Ibmoi/n	n/iomai	Ibmol/n	Ibmoi/n	IDMOI/N	
0.0421044	U <sup>*</sup>	U <sup>*</sup>	0 0472041	U <sup>*</sup> 2.245075.06*	
0.0431044	0.0420000	0.000243362	0.0472941	3.24507E-00	
0.0752190	0.0724775*	0.00170004*	0 116096		
0.0733160	0.0734773	0.00170004	0.110000	1.31130E-00	
0.207939	0.202900	0.00401202	0.739300	4.40952E-07	
0.113145	0.115540	0.00174047	2 2/190	1.06239E 07*	
0.447340	0.440045	0.00070330	3 05262	0.87200E-00*	
0.190972	0.194330	0.00230100	5.05202	9.07209E-09 2.64/16E-09*	
0.207000	0.200707	0.00025001	3 55566	4 48609E-10*	
0.128926	0.0700200	0.000320033	8 08730	1.40005E-10	
0.120320	0.127300	0.00140722	0.007.00	1.02000E-10	
0 00752103	0 00746627*	5 32275E-05*	0 464342	0 1 17711E-08*	
0.0463697	0.0458816*	0.000474439*	8.72362	1.02678E-11*	
0.00455006	0.00451831*	3 08556F-05*	0.920086	1 36465E-09*	
0.00747715	0.00741257*	6.27668E-05*	4.24787	9.56884E-14*	
0.000129398	0.000128536*	8.37372E-07*	0.0773904	1.02703E-11*	
0.000666067	0.000661764*	4.18232E-06*	0.442845	2.87609E-11*	
5.81147E-05		2 017005 07*	0 0429947	4.66711E-12*	
	5.77837E-05°	3.21/20E-0/"	0.0120011		
0.000174157	5.77837E-05 <sup>*</sup> 0.000172991*	3.21720E-07* 1.13353E-06*	0.111786	9.04013E-12*	
0.000174157 0.000873409	5.77837E-05* 0.000172991* 0.000867505*	3.21720E-07* 1.13353E-06* 5.73854E-06*	0.111786 1.46182	9.04013E-12* 2.38138E-15*	
0.000174157 0.000873409 0.000385838	5.77837E-05* 0.000172991* 0.000867505* 0.000383756*	3.21720E-07* 1.13353E-06* 5.73854E-06* 2.02305E-06*	0.111786 1.46182 1.84877	9.04013E-12* 2.38138E-15* 2.73160E-17*	
0.000174157 0.000873409 0.000385838 0.132424	5.77837E-05° 0.000172991* 0.000867505* 0.000383756* 0.121532*	3.21720E-07* 1.13353E-06* 5.73854E-06* 2.02305E-06* 0.0105867*	0.111786 1.46182 1.84877 393.115	9.04013E-12* 2.38138E-15* 2.73160E-17* 0.000384697*	

/0	%	%	%	%	
0	0	0	0	0	
0.645371	0.651900	0.237912	0.00692971	0.737619	
0	0	0	0	0	
2.11366	2.09506	3.27484	0.0318812	0.643919	
11.0268	10.9964	12.9188	0.297835	0.279250	
6.24604	6.24710	6.18020	0.321820	0.0264003	
24.2768	24.2857	23.7216	1.72094	0.0874902	
13.2633	13.2955	11.2523	2.01159	0.0100920	
17.3100	17.3594	14.2270	3.40270	0.00270305	
6.19137	6.21273	4.85859	2.79859	0.000547757	
10.3691	10.4094	7.85539	6.36536	0.000222659	
0	0	0	0	0	
0.548292	0.553021	0.253135	0.331278	0.0130278	
4.33639	4.35949	2.89439	7.98380	1.45778E-05	
0.391269	0.394765	0.173091	0.774294	0.00178156	
0.797128	0.802906	0.436520	4.43183	1.54871E-07	
0.0128211	0.0129398	0.00541252	0.0750421	1.54490E-05	
0.0659958	0.0666201	0.0270332	0.429408	4.32635E-05	
0.00575817	0.00581712	0.00207950	0.0416901	7.02048E-06	
0.0172560	0.0174151	0.00732682	0.108394	1.35986E-05	
0.104547	0.105504	0.0448101	1.71240	4.32754E-09	
0.0512355	0.0517757	0.0175249	2.40253	5.50686E-11	
2.22651	2.07612	11.6119	64.6842	98.1969	
0.000479933	0.000484763	0.000178538	0.0675190	1.44345E-13	
lb/h	lb/h	lb/h	lb/h	lh/h	
	10/11	10/11	10/11	10/11	
0	0*	0*	0	0*	0*
0 0.691500	0* 0.687480*	0* 0.00390766*	0 0.758714	0* 5.20589E-05*	0* 0.000940911*
0 0.691500 0	0* 0.687480* 0*	0* 0.00390766* 0*	0 0.758714 0	0* 5.20589E-05* 0*	0* 0.000940911* 0*
0 0.691500 0 2.26474	0* 0.687480* 0* 2.20940*	0* 0.00390766* 0* 0.0537886*	0 0.758714 0 3.49058	0* 5.20589E-05* 0* 4.54458E-05*	0* 0.000940911* 0* 0.000821387*
0 0.691500 0 2.26474 11.8149	0* 0.687480* 0* 2.20940* 11.5966*	0* 0.00390766* 0* 0.0537886* 0.212189*	0 0.758714 0 3.49058 32.6091	0* 5.20589E-05* 0* 4.54458E-05* 1.97086E-05*	0* 0.000940911* 0* 0.000821387* 0.000356213*
0 0.691500 0 2.26474 11.8149 6.69249	0* 0.687480* 0* 2.20940* 11.5966* 6.58805*	0* 0.00390766* 0* 0.0537886* 0.212189* 0.101509*	0 0.758714 0 3.49058 32.6091 35.2351	0* 5.20589E-05* 0* 4.54458E-05* 1.97086E-05* 1.86325E-06*	0* 0.000940911* 0* 0.000821387* 0.000356213* 3.36764E-05*
0 0.691500 0 2.26474 11.8149 6.69249 26.0120	0* 0.687480* 0* 2.20940* 11.5966* 6.58805* 25.6111*	0* 0.00390766* 0* 0.0537886* 0.212189* 0.101509* 0.389622*	0 0.758714 0 3.49058 32.6091 35.2351 188.420	0* 5.20589E-05* 0* 4.54458E-05* 1.97086E-05* 1.86325E-06* 6.17479E-06*	0* 0.000940911* 0* 0.000821387* 0.000356213* 3.36764E-05* 0.000111603*
0 0.691500 0 2.26474 11.8149 6.69249 26.0120 14.2113	0* 0.687480* 0* 2.20940* 11.5966* 6.58805* 25.6111* 14.0211*	0* 0.00390766* 0* 0.0537886* 0.212189* 0.101509* 0.389622* 0.184816*	0 0.758714 0 3.49058 32.6091 35.2351 188.420 220.243	0* 5.20589E-05* 0* 4.54458E-05* 1.97086E-05* 1.86325E-06* 6.17479E-06* 7.12259E-07*	0* 0.000940911* 0* 0.000821387* 0.000356213* 3.36764E-05* 0.000111603* 1.28734E-05*
0 0.691500 0 2.26474 11.8149 6.69249 26.0120 14.2113 18.5472	0* 0.687480* 0* 2.20940* 11.5966* 6.58805* 25.6111* 14.0211* 18.3068*	0* 0.00390766* 0* 0.0537886* 0.212189* 0.101509* 0.389622* 0.184816* 0.233676*	0 0.758714 0 3.49058 32.6091 35.2351 188.420 220.243 372.552	0* 5.20589E-05* 0* 4.54458E-05* 1.97086E-05* 1.86325E-06* 6.17479E-06* 7.12259E-07* 1.90773E-07*	0* 0.000940911* 0.000821387* 0.000356213* 3.36764E-05* 0.000111603* 1.28734E-05* 3.44803E-06*
0 0.691500 0 2.26474 11.8149 6.69249 26.0120 14.2113 18.5472 6.63391	0* 0.687480* 0* 2.20940* 11.5966* 6.58805* 25.6111* 14.0211* 18.3068* 6.55181*	0* 0.00390766* 0* 0.0537886* 0.212189* 0.101509* 0.389622* 0.184816* 0.233676* 0.0798013*	0 0.758714 0 3.49058 32.6091 35.2351 188.420 220.243 372.552 306.410	0* 5.20589E-05* 0* 4.54458E-05* 1.97086E-05* 1.86325E-06* 6.17479E-06* 7.12259E-07* 1.90773E-07* 3.86590E-08*	0* 0.000940911* 0.000821387* 0.000356213* 3.36764E-05* 0.000111603* 1.28734E-05* 3.44803E-06* 6.98723E-07*
0 0.691500 0 2.26474 11.8149 6.69249 26.0120 14.2113 18.5472 6.63391 11.1103	0* 0.687480* 0* 2.20940* 11.5966* 6.58805* 25.6111* 14.0211* 18.3068* 6.55181* 10.9775*	0* 0.00390766* 0* 0.0537886* 0.212189* 0.101509* 0.389622* 0.184816* 0.233676* 0.0798013* 0.129023*	0 0.758714 0 3.49058 32.6091 35.2351 188.420 220.243 372.552 306.410 696.926	0* 5.20589E-05* 0* 4.54458E-05* 1.97086E-05* 1.86325E-06* 6.17479E-06* 7.12259E-07* 1.90773E-07* 3.86590E-08* 1.57146E-08*	0* 0.000940911* 0.000821387* 0.000356213* 3.36764E-05* 0.000111603* 1.28734E-05* 3.44803E-06* 6.98723E-07* 2.84025E-07*
0 0.691500 0 2.26474 11.8149 6.69249 26.0120 14.2113 18.5472 6.63391 11.1103 0	0* 0.687480* 0* 2.20940* 11.5966* 6.58805* 25.6111* 14.0211* 18.3068* 6.55181* 10.9775* 0*	0* 0.00390766* 0* 0.0537886* 0.212189* 0.101509* 0.389622* 0.184816* 0.233676* 0.0798013* 0.129023* 0*	0 0.758714 0 3.49058 32.6091 35.2351 188.420 220.243 372.552 306.410 696.926 0	0* 5.20589E-05* 0* 4.54458E-05* 1.97086E-05* 1.86325E-06* 6.17479E-06* 7.12259E-07* 1.90773E-07* 3.86590E-08* 1.57146E-08* 0*	0* 0.000940911* 0* 0.000821387* 0.000356213* 3.36764E-05* 0.000111603* 1.28734E-05* 3.44803E-06* 6.98723E-07* 2.84025E-07* 0*
0 0.691500 0 2.26474 11.8149 6.69249 26.0120 14.2113 18.5472 6.63391 11.1103 0 0.587482	0* 0.687480* 0* 2.20940* 11.5966* 6.58805* 25.6111* 14.0211* 18.3068* 6.55181* 10.9775* 0* 0.583204*	0* 0.00390766* 0* 0.0537886* 0.212189* 0.101509* 0.389622* 0.184816* 0.233676* 0.0798013* 0.129023* 0* 0.00415770*	0 0.758714 0 3.49058 32.6091 35.2351 188.420 220.243 372.552 306.410 696.926 0 36.2706	0* 5.20589E-05* 0* 4.54458E-05* 1.97086E-05* 1.86325E-06* 6.17479E-06* 7.12259E-07* 1.90773E-07* 3.86590E-08* 1.57146E-08* 0* 9.19462E-07*	0* 0.000940911* 0* 0.000821387* 0.000356213* 3.36764E-05* 0.000111603* 1.28734E-05* 3.44803E-06* 6.98723E-07* 2.84025E-07* 0* 1.66183E-05*
0 0.691500 0 2.26474 11.8149 6.69249 26.0120 14.2113 18.5472 6.63391 11.1103 0 0.587482 4.64634	0* 0.687480* 0* 2.20940* 11.5966* 6.58805* 25.6111* 14.0211* 18.3068* 6.55181* 10.9775* 0* 0.583204* 4.59742*	0* 0.00390766* 0* 0.0537886* 0.212189* 0.101509* 0.389622* 0.184816* 0.233676* 0.0798013* 0.129023* 0* 0.00415770* 0.0475397*	0 0.758714 0 3.49058 32.6091 35.2351 188.420 220.243 372.552 306.410 696.926 0 36.2706 874.123	0* 5.20589E-05* 0* 4.54458E-05* 1.97086E-05* 1.86325E-06* 6.17479E-06* 7.12259E-07* 1.90773E-07* 3.86590E-08* 1.57146E-08* 0* 9.19462E-07* 1.02885E-09*	0* 0.000940911* 0* 0.000821387* 0.000356213* 3.36764E-05* 0.000111603* 1.28734E-05* 3.44803E-06* 6.98723E-07* 2.84025E-07* 0* 1.66183E-05* 1.85955E-08*
0 0.691500 0 2.26474 11.8149 6.69249 26.0120 14.2113 18.5472 6.63391 11.1103 0 0.587482 4.64634 0.419235	0* 0.687480* 0* 2.20940* 11.5966* 6.58805* 25.6111* 14.0211* 18.3068* 6.55181* 10.9775* 0* 0.583204* 4.59742* 0.416310*	0* 0.00390766* 0* 0.0537886* 0.212189* 0.101509* 0.389622* 0.184816* 0.233676* 0.0798013* 0.129023* 0* 0.00415770* 0.00475397* 0.00284299*	0 0.758714 0 3.49058 32.6091 35.2351 188.420 220.243 372.552 306.410 696.926 0 36.2706 874.123 84.7752	0* 5.20589E-05* 0* 4.54458E-05* 1.97086E-05* 1.86325E-06* 6.17479E-06* 7.12259E-07* 1.90773E-07* 3.86590E-08* 1.57146E-08* 0* 9.19462E-07* 1.02885E-09* 1.25737E-07*	0* 0.000940911* 0* 0.000821387* 0.000356213* 3.36764E-05* 0.000111603* 1.28734E-05* 3.44803E-06* 6.98723E-07* 2.84025E-07* 0* 1.66183E-05* 1.85955E-08* 2.27257E-06*
0 0.691500 0 2.26474 11.8149 6.69249 26.0120 14.2113 18.5472 6.63391 11.1103 0 0.587482 4.64634 0.419235 0.854104	0* 0.687480* 0* 2.20940* 11.5966* 6.58805* 25.6111* 14.0211* 18.3068* 6.55181* 10.9775* 0* 0.583204* 4.59742* 0.416310* 0.846727*	0* 0.00390766* 0* 0.0537886* 0.212189* 0.101509* 0.389622* 0.184816* 0.233676* 0.0798013* 0.129023* 0* 0.00415770* 0.00415770* 0.00284299* 0.00716976*	0 0.758714 0 3.49058 32.6091 35.2351 188.420 220.243 372.552 306.410 696.926 0 36.2706 874.123 84.7752 485.228	0* 5.20589E-05* 0* 4.54458E-05* 1.97086E-05* 1.86325E-06* 6.17479E-06* 7.12259E-07* 1.90773E-07* 3.86590E-08* 1.57146E-08* 0* 9.19462E-07* 1.02885E-09* 1.25737E-07* 1.09303E-11*	0* 0.000940911* 0* 0.000821387* 0.000356213* 3.36764E-05* 0.000111603* 1.28734E-05* 3.44803E-06* 6.98723E-07* 2.84025E-07* 0* 1.66183E-05* 1.85955E-08* 2.27257E-06* 1.97555E-10*
0 0.691500 0 2.26474 11.8149 6.69249 26.0120 14.2113 18.5472 6.63391 11.1103 0 0.587482 4.64634 0.419235 0.854104 0.0137375	0* 0.687480* 0* 2.20940* 11.5966* 6.58805* 25.6111* 14.0211* 18.3068* 6.55181* 10.9775* 0* 0.583204* 4.59742* 0.416310* 0.846727* 0.0136460*	0* 0.00390766* 0* 0.0537886* 0.212189* 0.101509* 0.389622* 0.184816* 0.233676* 0.0798013* 0.129023* 0* 0.00415770* 0.00475397* 0.00284299* 0.00716976* 8.88996E-05*	0 0.758714 0 3.49058 32.6091 35.2351 188.420 220.243 372.552 306.410 696.926 0 36.2706 874.123 84.7752 485.228 8.21615	0* 5.20589E-05* 0* 4.54458E-05* 1.97086E-05* 1.86325E-06* 6.17479E-06* 7.12259E-07* 1.90773E-07* 3.86590E-08* 1.57146E-08* 0* 9.19462E-07* 1.02885E-09* 1.25737E-07* 1.09303E-11* 1.09034E-09*	0* 0.000940911* 0* 0.000821387* 0.000356213* 3.36764E-05* 0.000111603* 1.28734E-05* 3.44803E-06* 6.98723E-07* 2.84025E-07* 1.66183E-05* 1.85955E-08* 2.27257E-06* 1.97555E-10* 1.97068E-08*
0 0.691500 0 2.26474 11.8149 6.69249 26.0120 14.2113 18.5472 6.63391 11.1103 0 0.587482 4.64634 0.419235 0.854104 0.0137375 0.0707130	0* 0.687480* 0* 2.20940* 11.5966* 6.58805* 25.6111* 14.0211* 18.3068* 6.55181* 10.9775* 0* 0.583204* 4.59742* 0.416310* 0.846727* 0.0136460* 0.0702561*	0* 0.00390766* 0* 0.0537886* 0.212189* 0.101509* 0.389622* 0.184816* 0.233676* 0.0798013* 0.129023* 0* 0.00415770* 0.00415770* 0.00284299* 0.00716976* 8.88996E-05* 0.000444015*	0 0.758714 0 3.49058 32.6091 35.2351 188.420 220.243 372.552 306.410 696.926 0 36.2706 874.123 84.7752 485.228 8.21615 47.0146	0* 5.20589E-05* 0* 4.54458E-05* 1.97086E-05* 1.86325E-06* 6.17479E-06* 7.12259E-07* 1.90773E-07* 3.86590E-08* 1.57146E-08* 0* 9.19462E-07* 1.02885E-09* 1.25737E-07* 1.09303E-11* 1.09034E-09* 3.05340E-09*	0* 0.000940911* 0* 0.000821387* 0.000356213* 3.36764E-05* 0.000111603* 1.28734E-05* 3.44803E-06* 6.98723E-07* 2.84025E-07* 1.66183E-05* 1.85955E-08* 2.27257E-06* 1.97555E-10* 1.97068E-08* 5.51872E-08*
0 0.691500 0 2.26474 11.8149 6.69249 26.0120 14.2113 18.5472 6.63391 11.1103 0 0.587482 4.64634 0.419235 0.854104 0.0137375 0.0707130 0.00616974	0* 0.687480* 0* 2.20940* 11.5966* 6.58805* 25.6111* 14.0211* 18.3068* 6.55181* 10.9775* 0* 0.583204* 4.59742* 0.416310* 0.846727* 0.0136460* 0.0702561* 0.00613460*	0* 0.00390766* 0* 0.0537886* 0.212189* 0.101509* 0.389622* 0.184816* 0.233676* 0.0798013* 0.129023* 0* 0.00415770* 0.00415770* 0.00284299* 0.00716976* 8.88996E-05* 0.000444015* 3.41554E-05*	0 0.758714 0 3.49058 32.6091 35.2351 188.420 220.243 372.552 306.410 696.926 0 36.2706 874.123 84.7752 485.228 8.21615 47.0146 4.56453	0* 5.20589E-05* 0* 4.54458E-05* 1.97086E-05* 1.86325E-06* 6.17479E-06* 7.12259E-07* 1.90773E-07* 3.86590E-08* 1.57146E-08* 0* 9.19462E-07* 1.02885E-09* 1.25737E-07* 1.09303E-11* 1.09303E-11* 1.0934E-09* 3.05340E-09* 4.95484E-10*	0* 0.000940911* 0* 0.000821387* 0.000356213* 3.36764E-05* 0.000111603* 1.28734E-05* 3.44803E-06* 6.98723E-07* 2.84025E-07* 1.66183E-05* 1.85955E-08* 2.27257E-06* 1.97555E-10* 1.97068E-08* 5.51872E-08* 8.95537E-09*
0 0.691500 0 2.26474 11.8149 6.69249 26.0120 14.2113 18.5472 6.63391 11.1103 0 0.587482 4.64634 0.419235 0.854104 0.0137375 0.0707130 0.00616974 0.0184894 0.11575	0* 0.687480* 0* 2.20940* 11.5966* 6.58805* 25.6111* 14.0211* 18.3068* 6.55181* 10.9775* 0* 0.583204* 4.59742* 0.416310* 0.846727* 0.0136460* 0.0702561* 0.00613460* 0.0183656*	0* 0.00390766* 0* 0.0537886* 0.212189* 0.101509* 0.389622* 0.184816* 0.233676* 0.0798013* 0.129023* 0* 0.00415770* 0.00284299* 0.00716976* 8.88996E-05* 0.000444015* 3.41554E-05* 0.000120341*	0 0.758714 0 3.49058 32.6091 35.2351 188.420 220.243 372.552 306.410 696.926 0 36.2706 874.123 84.7752 485.228 8.21615 47.0146 4.56453 11.8678	0* 5.20589E-05* 0* 4.54458E-05* 1.97086E-05* 1.86325E-06* 6.17479E-06* 7.12259E-07* 1.90773E-07* 3.86590E-08* 1.57146E-08* 0* 9.19462E-07* 1.02885E-09* 1.25737E-07* 1.09303E-11* 1.09034E-09* 3.05340E-09* 4.95484E-10* 9.59745E-10*	0* 0.000940911* 0* 0.000821387* 0.000356213* 3.36764E-05* 0.000111603* 1.28734E-05* 3.44803E-06* 6.98723E-07* 2.84025E-07* 0* 1.66183E-05* 1.85955E-08* 2.27257E-06* 1.97555E-10* 1.97068E-08* 5.51872E-08* 8.95537E-09* 1.73464E-08*
0 0.691500 0 2.26474 11.8149 6.69249 26.0120 14.2113 18.5472 6.63391 11.1103 0 0.587482 4.64634 0.419235 0.854104 0.0137375 0.0707130 0.00616974 0.0184894 0.112019	0* 0.687480* 0* 2.20940* 11.5966* 6.58805* 25.6111* 14.0211* 18.3068* 6.55181* 10.9775* 0* 0.583204* 4.59742* 0.416310* 0.846727* 0.0136460* 0.0702561* 0.00613460* 0.0183656* 0.111262*	0* 0.00390766* 0* 0.0537886* 0.212189* 0.101509* 0.389622* 0.184816* 0.233676* 0.0798013* 0.129023* 0* 0.00415770* 0.00284299* 0.00716976* 8.88996E-05* 0.000444015* 3.41554E-05* 0.000120341* 0.000735997*	0 0.758714 0 3.49058 32.6091 35.2351 188.420 220.243 372.552 306.410 696.926 0 36.2706 874.123 84.7752 485.228 8.21615 47.0146 4.56453 11.8678 187.486	0* 5.20589E-05* 0* 4.54458E-05* 1.97086E-05* 1.86325E-06* 6.17479E-06* 7.12259E-07* 1.90773E-07* 3.86590E-08* 1.57146E-08* 0* 9.19462E-07* 1.02885E-09* 1.25737E-07* 1.09303E-11* 1.09034E-09* 3.05340E-09* 4.95484E-10* 9.59745E-10* 3.05425E-13*	0* 0.000940911* 0* 0.000821387* 0.000356213* 3.36764E-05* 0.000111603* 1.28734E-05* 3.44803E-06* 6.98723E-07* 2.84025E-07* 0* 1.66183E-05* 1.85955E-08* 2.27257E-06* 1.97555E-10* 1.97068E-08* 5.51872E-08* 8.95537E-09* 1.73464E-08* 5.52024E-12*
0 0.691500 0 2.26474 11.8149 6.69249 26.0120 14.2113 18.5472 6.63391 11.1103 0 0.587482 4.64634 0.419235 0.854104 0.0137375 0.0707130 0.00616974 0.0184894 0.112019 0.0548976	0* 0.687480* 0* 2.20940* 11.5966* 6.58805* 25.6111* 14.0211* 18.3068* 6.55181* 10.9775* 0* 0.583204* 4.59742* 0.416310* 0.846727* 0.0136460* 0.0702561* 0.00613460* 0.0183656* 0.111262* 0.0546015*	0* 0.00390766* 0* 0.0537886* 0.212189* 0.101509* 0.389622* 0.184816* 0.233676* 0.0798013* 0.129023* 0* 0.00415770* 0.00284299* 0.00716976* 8.88996E-05* 0.000444015* 3.41554E-05* 0.000120341* 0.000735997* 0.000287844*	0 0.758714 0 3.49058 32.6091 35.2351 188.420 220.243 372.552 306.410 696.926 0 36.2706 874.123 84.7752 485.228 8.21615 47.0146 4.56453 11.8678 187.486 263.046	0* 5.20589E-05* 0* 4.54458E-05* 1.97086E-05* 1.86325E-06* 6.17479E-06* 7.12259E-07* 1.90773E-07* 3.86590E-08* 1.57146E-08* 0* 9.19462E-07* 1.02885E-09* 1.25737E-07* 1.09303E-11* 1.09034E-09* 3.05340E-09* 4.95484E-10* 9.59745E-10* 3.05425E-13* 3.88657E-15*	0* 0.000940911* 0* 0.000821387* 0.000356213* 3.36764E-05* 0.000111603* 1.28734E-05* 3.44803E-06* 6.98723E-07* 2.84025E-07* 0* 1.66183E-05* 1.85955E-08* 2.27257E-06* 1.97555E-10* 1.97068E-08* 5.51872E-08* 8.95537E-09* 1.73464E-08* 5.52024E-12* 7.02458E-14*
0 0.691500 0 2.26474 11.8149 6.69249 26.0120 14.2113 18.5472 6.63391 11.1103 0 0.587482 4.64634 0.419235 0.854104 0.0137375 0.0707130 0.00616974 0.0184894 0.112019 0.0548976 2.38566	0* 0.687480* 0* 2.20940* 11.5966* 6.58805* 25.6111* 14.0211* 18.3068* 6.55181* 10.9775* 0* 0.583204* 4.59742* 0.416310* 0.846727* 0.0136460* 0.0702561* 0.00613460* 0.0183656* 0.111262* 0.0546015* 2.18943*	0* 0.00390766* 0* 0.0537886* 0.212189* 0.101509* 0.389622* 0.184816* 0.233676* 0.0798013* 0.129023* 0* 0.00415770* 0.00415770* 0.00284299* 0.00716976* 8.88996E-05* 0.000444015* 3.41554E-05* 0.000120341* 0.000735997* 0.000287844* 0.190722*	0 0.758714 0 3.49058 32.6091 35.2351 188.420 220.243 372.552 306.410 696.926 0 36.2706 874.123 84.7752 485.228 8.21615 47.0146 4.56453 11.8678 187.486 263.046 7082.09	0* 5.20589E-05* 0* 4.54458E-05* 1.97086E-05* 1.86325E-06* 6.17479E-06* 7.12259E-07* 1.90773E-07* 3.86590E-08* 1.57146E-08* 0* 9.19462E-07* 1.02885E-09* 1.25737E-07* 1.09303E-11* 1.09034E-09* 3.05340E-09* 4.95484E-10* 9.59745E-10* 3.05425E-13* 3.88657E-15* 0.00693043*	0* 0.000940911* 0* 0.000821387* 0.000356213* 3.36764E-05* 0.000111603* 1.28734E-05* 3.44803E-06* 6.98723E-07* 2.84025E-07* 0* 1.66183E-05* 1.85955E-08* 2.27257E-06* 1.97555E-10* 1.97068E-08* 5.51872E-08* 8.95537E-09* 1.73464E-08* 5.52024E-12* 7.02458E-14* 0.125260491*

GB F/W/B	GB Flashing	GB Working	Liquid To GB	PW Breathing	
Solved	Solved	Solved	Solved	Solved	
MIX-105			MIX-106		
	MIX-105	MIX-105	Gunbarrel	MIX-101	
95.0183	97.8	76.1390	91.9457	76.2171	
1.46621	12.8800	1.46621	34.6959	0.454295	
100	100	100	0	100	
0	0	0	9.86394	0	
0	0	0	90.1361	0	
100	100	100	100	100	
59.2098	59.4502	47.2788	25.1051	18.0936	
0.0146213	0.130953	0.0120787	52.7653	0.00142997	
1.80963	1.77388	0.0347403	436.114	0.000390065	
107.148	105.458	1.64248	10948.7	0.00705769	
7328.21	805.311	135.981	207.498	4.93555	
913.646	100.402	16.9535	25.8699	0.615341	
0.0164814	0.0161559	0.000316401	3.97196	3.55257E-06	
0.358184	0.352648	0.00538049	25.6025	1.45673E-05	
0.997449	0.977393	0.998085	0.00278864	0.999538	
2.04436	2.05266	1.63241	0.846021	0.624725	
			33.4700		
-108478	-105961	-2446.93	-5.17981E+07	-40.1854	
-1012.42	-1004.77	-1489.78	-4730.98	-5693.84	
0.410005	0.414349	0.404272	0.820833	0.445656	
1.08917	1.08841	1.11605	1.22626	1.32691	
0.00781528	0.00787941	0.00834181	0.557748	0.00999099	
33.3687	3.75628	43.1141	0.659886	436.174	
0.00965793	0.00979773	0.00925756	0.226680	0.0119153	
			0.00320989		
2985.07	3001.71	2159.35	450.307	17.8079	
18953.1	18983.3	17068.4	6064.76	-668.818	
3234.98	3252.74	2354.00	530.888	69.1815	
20555.2	20586.0	18631.1	7282.91	408.674	

					Sep	
PW F/W/B/L	PW Flashing	PW Loding	PW to Tanks	PW Working	Condensate	Sep PW
Solved	Solved	Solved	Solved	Solved	Solved	Solved
MIX-101			Gunbarrel			
	MIX-101	MIX-101		MIX-101	MIX-106	MIX-106
%	%	%	%	%	%	%
0	0*	0*	0	0*	0*	0*
3.91422	22.1417*	0.831929*	0.000501856	0.831929*	0.109989*	0*
0	0*	0*	0	0*	0*	0*
1.77165	9.95718*	0.387469*	0.000291482	0.387469*	0.269973*	0*
2.65041	17.6463*	0.114584*	0.000379722	0.114584*	1.71983*	0*
0.856249	5.87118*	0.00821849*	8.65655E-05	0.00821849*	1.40986*	0*
2.80424	19.2264*	0.0272359*	0.000386890	0.0272359*	7.53925*	0*
1.07142	7.39240*	0.00253088*	0.000106362	0.00253088*	7.09929*	0*
0.810666	5.60062*	0.000677877*	5.02083E-05	0.000677877*	12.0088*	0*
0.274296	1.89570*	0.000115009*	1.92975E-05	0.000115009*	8.26917*	0*
0.303258	2.09633*	4.67500E-05*	1.50751E-05	4.67500E-05*	18.8081*	0*
0	0*	0*	0	0*	0*	0*
0.0581073	0.383886*	0.00301772*	0.000709053	0.00301772*	1.07989*	0*
0.0866152	0.598809*	2.63233E-06*	3.68196E-06	2.63233E-06*	20.2880*	0*
0.0295505	0.202232*	0.000349852*	0.000284353	0.000349852*	2.13979*	0 <sup>*</sup>
0.00648622	0.0448431*	2.45314E-08 <sup>*</sup>	2.22514E-07	2.45314E-08*	9.87901*	0^ 0*
0.000832347	0.00573896*	2.03290E-06"	0.00018E-00	2.03290E-00"	0.179982*	0 <sup></sup>
0.00370413	0.0209003	1.37330E-00 1.10650E.06*	2.13933E-03	1.3/330E-00	1.02990	0*
0.000302002	0.00200175	1.19030E-00	4.37 140E-00	1.19030E-00 2.21750E.06*	0.0999900	0*
0.00101913	0.00703214	2.31759E-00 6 10509E-10*	2.20007E-00	2.31759E-00 6 10500E-10*	0.209974	0*
0.000793223	0.000715510*	7.00203E-10	2.09214E-00	7.00203E-10	J.39900 4 20057*	0*
85 3560	6 89493*	08 6238*	00 0071	08 6238*	4.29937	100*
8 58414E-07	5 93475E-06*	1 67088E-14*	2 46079E-11	1 67088E-14*	0 109989*	0*
Ibmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h
0	0*	0*	0	0*	0*	0*
0 000420480	0 000344037*	1 77910F-05*	0 00197284	5 54062E-05*	0 0472941*	0*
0	0*	0*	0	0*	0*	0*
0.000190317	0.000154714*	8.28614E-06*	0.00114584	2.58053E-05*	0.116086*	0*
0.000284717	0.000274189*	2.45041E-06*	0.00149272	7.63125E-06*	0.739508*	0*
9.19814E-05	9.12262E-05*	1.75755E-07*	0.000340297	5.47349E-07*	0.606225*	0*
0.000301242	0.000298739*	5.82449E-07*	0.00152090	1.81391E-06*	3.24180*	0*
0.000115095	0.000114863*	5.41236E-08*	0.000418117	1.68556E-07*	3.05262*	0*
8.70846E-05	8.70224E-05*	1.44966E-08*	0.000197374	4.51464E-08*	5.16366*	0*
2.94659E-05	2.94553E-05*	2.45949E-09*	7.58604E-05	7.65954E-09*	3.55566*	0*
3.25771E-05	3.25728E-05*	9.99764E-10*	5.92617E-05	3.11354E-09*	8.08730*	0*
0	0*	0*	0	0*	0*	0*
6.24210E-06	5.96481E-06*	6.45350E-08*	0.00278735	2.00980E-07*	0.464342*	0*
9.30452E-06	9.30428E-06*	5.62931E-11*	1.44741E-05	1.75312E-10*	8.72362*	0*
3.17442E-06	3.14227E-06*	7.48169E-09*	0.00111782	2.33000E-08*	0.920086*	0*
6.96774E-07	6.96771E-07*	5.24611E-13*	8.74723E-07	1.63378E-12*	4.24787*	0*
8.94137E-08	8.91718E-08*	5.63066E-11*	2.61739E-05	1.75354E-10*	0.0773904*	0*
4.04359E-07	4.03681E-07*	1.57682E-10*	8.41078E-05	4.91064E-10*	0.442845*	0*
3.89821E-08	3.88721E-08*	2.55874E-11*	1.71846E-05	7.96862E-11*	0.0429947*	0*
1.09478E-07	1.09265E-07*	4.95624E-11*	2.46121E-05	1.54351E-10*	0.111786*	0*
8.52109E-08	8.52108E-08*	1.30559E-14*	1.01899E-07	4.06597E-14*	1.46182*	0*
1.11176E-08	1.11176E-08*	1.49760E-16*	1.18046E-08	4.66393E-16*	1.84877*	0*
0.00916925	0.000107133*	0.00210910*	393.098	0.00656832*	*0	393.115*
9.22140E-11	9.22140E-11*	3.5/323E-19*	9.6/359E-11	1.11280E-18*	0.04/2941*	0*

,,,	%	%	%	%	%	%
0	0	0	0	0	0*	0*
2.87202	8.04355	0.737619	0.000446871	0.737619	0.0196221*	0*
0	0	0	0	0	0*	0*
2.43651	6.77988	0.643919	0.000486479	0.643919	0.0902746*	0*
5.34540	17.6204	0.279250	0.000929381	0.279250	0.843346*	0*
2.27621	7.72739	0.0264003	0.000279267	0.0264003	0.911262*	0*
7.45467	25.3050	0.0874902	0.00124814	0.0874902	4.87299*	0*
3.53556	12.0776	0.0100920	0.000425938	0.0100920	5.69599*	0*
2.67511	9.15021	0.00270305	0.000201065	0.00270305	9.63505*	0*
1.08112	3.69929	0.000547757	9.23034E-05	0.000547757	7.92448*	0*
1.19527	4.09081	0.000222659	7.21068E-05	0.000222659	18.0241*	0*
0	0	0	0	0	0*	0*
0.207596	0.679024	0.0130278	0.00307417	0.0130278	0.938043*	0*
0.396955	1.35872	1.45778E-05	2.04780E-05	1.45778E-05	22.6069*	0*
0.124530	0.421945	0.00178156	0.00145423	0.00178156	2.19248*	0*
0.0338873	0.115994	1.54871E-07	1.41080E-06	1.54871E-07	12.5491*	0*
0.00404163	0.0137969	1.54490E-05	3.92346E-05	1.54490E-05	0.212489*	0*
0.0182776	0.0624585	4.32635E-05	0.000126077	4.32635E-05	1.21591*	0*
0.00176205	0.00601438	7.02048E-06	2.57597E-05	7.02048E-06	0.118049*	0*
0.00494857	0.0169058	1.35986E-05	3.68934E-05	1.35986E-05	0.306928*	0*
0.00465308	0.0159273	4.32754E-09	1.84530E-07	4.32754E-09	4.84881*	0*
0.000673488	0.00230532	5.50686E-11	2.37148E-08	5.50686E-11	6.80298*	0*
70.3308	2.81278	98.1969	99.9910	98.1969	0*	100*
6.13691E-06	2.10063E-05	1.44345E-13	2.13496E-10	1.44345E-13	0.191186*	0*
lb/h	lb/h	lb/h	lb/h	lb/h	lb/h	lb/h
<b>lb/h</b>	<b>Ib/h</b> 0*	<b>lb/h</b> 0*	<b>lb/h</b>	<b>lb/h</b> 0*	<b>Ib/h</b>	<b>Ib/h</b> 0*
<b>Ib/h</b> 0 0.00674553	<b>lb/h</b> 0* 0.00551920*	<b>Ib/h</b> 0* 0.000285412*	<b>Ib/h</b> 0 0.0316492	<b>lb/h</b> 0* 0.000888852*	<b>lb/h</b> 0* 0.758714*	<b>lb/h</b> 0* 0*
0 0.00674553 0	<b>Ib/h</b> 0* 0.00551920* 0*	<b>lb/h</b> 0* 0.000285412* 0*	<b>Ib/h</b> 0.0316492 0	lb/h 0* 0.000888852* 0*	<b>lb/h</b> 0* 0.758714* 0*	lb/h 0* 0*
<b>Ib/h</b> 0 0.00674553 0 0.00572266	lb/h 0* 0.00551920* 0* 0.00465211*	<b>Ib/h</b> 0* 0.000285412* 0* 0.000249156*	<b>Ib/h</b> 0.0316492 0 0.0344544	<b>Ib/h</b> 0* 0.000888852* 0* 0.000775941*	<b>Ib/h</b> 0* 0.758714* 0* 3.49058*	lb/h 0* 0* 0*
Ib/h           0           0.00674553           0           0.00572266           0.0125548	lb/h 0* 0.00551920* 0* 0.00465211* 0.0120905*	lb/h           0*           0.000285412*           0*           0.000249156*           0.000108052*	Ib/h           0           0.0316492           0           0.0344544           0.0658226	<b>Ib/h</b> 0.000888852* 0* 0.000775941* 0.000336505*	<b>Ib/h</b> 0* 0.758714* 0* 3.49058* 32.6091*	lb/h 0* 0* 0* 0* 0*
0 0.00674553 0 0.00572266 0.0125548 0.00534616	lb/h           0*           0.00551920*           0*           0.00465211*           0.0120905*           0.00530227*	Ib/h           0*           0.000285412*           0*           0.000249156*           0.000108052*           1.02153E-05*	Ib/h           0           0.0316492           0           0.0344544           0.0658226           0.0197788	Ib/h           0*           0.000888852*           0*           0.000775941*           0.000336505*           3.18131E-05*	lb/h 0* 0.758714* 0* 3.49058* 32.6091* 35.2351*	lb/h 0* 0* 0* 0* 0* 0*
0 0.00674553 0 0.00572266 0.0125548 0.00534616 0.0175088	lb/h           0*           0.00551920*           0*           0.00465211*           0.0120905*           0.00530227*           0.0173634*	Ib/h           0*           0.000285412*           0*           0.000249156*           0.000108052*           1.02153E-05*           3.38532E-05*	Ib/h           0           0.0316492           0           0.0344544           0.0658226           0.0197788           0.0883980	Ib/h           0*           0.000888852*           0*           0.000775941*           0.000336505*           3.18131E-05*           0.000105428*	lb/h 0* 0.758714* 0* 3.49058* 32.6091* 35.2351* 188.420*	lb/h 0* 0* 0* 0* 0* 0* 0*
0 0.00674553 0 0.00572266 0.0125548 0.00534616 0.0175088 0.00830400	lb/h           0*           0.00551920*           0*           0.00465211*           0.0120905*           0.00530227*           0.0173634*           0.00828722*	Ib/h           0*           0.000285412*           0*           0.000249156*           0.000108052*           1.02153E-05*           3.38532E-05*           3.90495E-06*	Ib/h           0           0.0316492           0           0.0344544           0.0658226           0.0197788           0.0883980           0.0301666	Ib/h           0*           0.000888852*           0*           0.000775941*           0.000336505*           3.18131E-05*           0.000105428*           1.21611E-05*	lb/h 0* 0.758714* 0* 3.49058* 32.6091* 35.2351* 188.420* 220.243*	lb/h 0* 0* 0* 0* 0* 0* 0* 0*
0 0.00674553 0 0.00572266 0.0125548 0.00534616 0.0175088 0.00830400 0.00628305	Ib/h           0*           0.00551920*           0*           0.00465211*           0.0120905*           0.00530227*           0.0173634*           0.00828722*           0.00627856*	Ib/h           0*           0.000285412*           0*           0.000249156*           0.000108052*           1.02153E-05*           3.38532E-05*           3.90495E-06*           1.04591E-06*	Ib/h           0           0.0316492           0           0.0344544           0.0658226           0.0197788           0.0883980           0.0301666           0.0142403	Ib/h           0*           0.000888852*           0*           0.000775941*           0.000336505*           3.18131E-05*           0.000105428*           1.21611E-05*           3.25726E-06*	Ib/h           0*           0.758714*           0*           3.49058*           32.6091*           35.2351*           188.420*           220.243*           372.552*	lb/h 0* 0* 0* 0* 0* 0* 0* 0* 0*
0 0.00674553 0 0.00572266 0.0125548 0.00534616 0.0175088 0.00830400 0.00628305 0.00253923	Ib/h           0*           0.00551920*           0*           0.00465211*           0.0120905*           0.00530227*           0.0173634*           0.00828722*           0.00627856*           0.00253832*	Ib/h           0*           0.000285412*           0*           0.000249156*           0.000108052*           1.02153E-05*           3.38532E-05*           3.90495E-06*           1.04591E-06*           2.11948E-07*	Ib/h           0           0.0316492           0           0.0344544           0.0658226           0.0197788           0.0883980           0.0301666           0.0142403           0.00653730	Ib/h           0*           0.000888852*           0*           0.000775941*           0.000336505*           3.18131E-05*           0.000105428*           1.21611E-05*           3.25726E-06*           6.60064E-07*	Ib/h           0*           0.758714*           0*           3.49058*           32.6091*           35.2351*           188.420*           220.243*           372.552*           306.410*	lb/h 0* 0* 0* 0* 0* 0* 0* 0* 0* 0*
Ib/h           0           0.00674553           0           0.00572266           0.0125548           0.00534616           0.0175088           0.00830400           0.00628305           0.00253923           0.00280734	Ib/h           0*           0.00551920*           0*           0.00465211*           0.0120905*           0.00530227*           0.0173634*           0.00828722*           0.00627856*           0.00253832*           0.002580697*	Ib/h           0*           0.000285412*           0*           0.000249156*           0.000108052*           1.02153E-05*           3.38532E-05*           3.90495E-06*           1.04591E-06*           2.11948E-07*           8.61550E-08*	Ib/h           0           0.0316492           0           0.0344544           0.0658226           0.0197788           0.0883980           0.0301666           0.0142403           0.00653730           0.00510689	Ib/h           0*           0.000888852*           0*           0.000775941*           0.00036505*           3.18131E-05*           0.000105428*           1.21611E-05*           3.25726E-06*           6.60064E-07*           2.68310E-07*	Ib/h           0*           0.758714*           0*           3.49058*           32.6091*           35.2351*           188.420*           220.243*           372.552*           306.410*           696.926*	lb/h 0* 0* 0* 0* 0* 0* 0* 0* 0* 0* 0*
Ib/h           0           0.00674553           0           0.00572266           0.0125548           0.00534616           0.0175088           0.00830400           0.00628305           0.00253923           0.00280734           0	Ib/h           0*           0.00551920*           0*           0.00465211*           0.0120905*           0.00530227*           0.0173634*           0.00828722*           0.00627856*           0.00253832*           0.00280697*           0*	Ib/h           0*           0.000285412*           0*           0.000249156*           0.000108052*           1.02153E-05*           3.38532E-05*           3.90495E-06*           1.04591E-06*           2.11948E-07*           8.61550E-08*           0*	Ib/h           0           0.0316492           0           0.0344544           0.0658226           0.0197788           0.0883980           0.0301666           0.0142403           0.00653730           0.00510689           0	Ib/h           0*           0.000888852*           0*           0.000775941*           0.00036505*           3.18131E-05*           0.000105428*           1.21611E-05*           3.25726E-06*           6.60064E-07*           2.68310E-07*           0*	Ib/h           0*           0.758714*           0*           3.49058*           32.6091*           35.2351*           188.420*           220.243*           372.552*           306.410*           696.926*           0*	Ib/h           0*
Ib/h           0           0.00674553           0           0.00572266           0.0125548           0.00534616           0.0175088           0.00830400           0.00628305           0.00253923           0.00280734           0           0.000487582	Ib/h           0*           0.00551920*           0*           0.00465211*           0.0120905*           0.00530227*           0.0173634*           0.00828722*           0.00627856*           0.00253832*           0.00280697*           0*           0.000465922*	Ib/h           0*           0.000285412*           0*           0.000249156*           0.000108052*           1.02153E-05*           3.38532E-05*           3.90495E-06*           1.04591E-06*           2.11948E-07*           8.61550E-08*           0*           5.04094E-06*	Ib/h           0           0.0316492           0           0.0344544           0.0658226           0.0197788           0.0883980           0.0301666           0.0142403           0.00653730           0.00510689           0           0.217725	Ib/h           0*           0.000888852*           0*           0.000775941*           0.00036505*           3.18131E-05*           0.000105428*           1.21611E-05*           3.25726E-06*           6.60064E-07*           2.68310E-07*           0*           1.56989E-05*	Ib/h           0*           0.758714*           0*           3.49058*           32.6091*           35.2351*           188.420*           220.243*           372.552*           306.410*           696.926*           0*           36.2706*	Ib/h           0*
Ib/h           0           0.00674553           0           0.00572266           0.0125548           0.00534616           0.0175088           0.00830400           0.002628305           0.00253923           0.00280734           0           0.000487582           0.000932331	Ib/h           0*           0.00551920*           0*           0.00465211*           0.0120905*           0.00530227*           0.0173634*           0.00828722*           0.00627856*           0.00253832*           0.00280697*           0*           0.000465922*           0.000932307*	Ib/h           0*           0.000285412*           0*           0.000249156*           0.000108052*           1.02153E-05*           3.38532E-05*           3.90495E-06*           1.04591E-06*           2.11948E-07*           8.61550E-08*           0*           5.04094E-06*           5.64068E-09*	Ib/h           0           0.0316492           0           0.0344544           0.0658226           0.0197788           0.0883980           0.0301666           0.0142403           0.00653730           0.00510689           0           0.217725           0.00145034	Ib/h           0*           0.000888852*           0*           0.000775941*           0.000336505*           3.18131E-05*           0.000105428*           1.21611E-05*           3.25726E-06*           6.60064E-07*           2.68310E-07*           0*           1.56989E-05*           1.75666E-08*	Ib/h           0*           0.758714*           0*           3.49058*           32.6091*           35.2351*           188.420*           220.243*           372.552*           306.410*           696.926*           0*           36.2706*           874.123*	Ib/h           0*
Ib/h           0           0.00674553           0           0.00572266           0.0125548           0.00534616           0.0175088           0.00830400           0.00253923           0.00280734           0           0.000487582           0.000932331           0.000292486	Ib/h           0*           0.00551920*           0*           0.00465211*           0.0120905*           0.00530227*           0.0173634*           0.00828722*           0.00627856*           0.00253832*           0.00280697*           0*           0.000465922*           0.000932307*           0.000289524*	Ib/h           0*           0.000285412*           0*           0.000249156*           0.000108052*           1.02153E-05*           3.38532E-05*           3.90495E-06*           1.04591E-06*           2.11948E-07*           8.61550E-08*           0*           5.04094E-06*           5.64068E-09*           6.89351E-07*	Ib/h           0           0.0316492           0           0.0344544           0.0658226           0.0197788           0.0883980           0.0301666           0.0142403           0.00653730           0.00510689           0           0.217725           0.00145034           0.102994	Ib/h           0*           0.000888852*           0*           0.000775941*           0.000336505*           3.18131E-05*           0.000105428*           1.21611E-05*           3.25726E-06*           6.60064E-07*           2.68310E-07*           0*           1.56989E-05*           1.75666E-08*           2.14683E-06*	Ib/h           0*           0.758714*           0*           3.49058*           32.6091*           35.2351*           188.420*           220.243*           372.552*           306.410*           696.926*           0*           36.2706*           874.123*           84.7752*	Ib/h           0*
Ib/h           0           0.00674553           0           0.00572266           0.0125548           0.00534616           0.0175088           0.00830400           0.00253923           0.00280734           0           0.000487582           0.000932331           0.000292486           7.95914E-05	Ib/h           0*           0.00551920*           0*           0.00465211*           0.0120905*           0.00530227*           0.0173634*           0.00828722*           0.00627856*           0.00253832*           0.00280697*           0*           0.000465922*           0.000932307*           0.000289524*           7.95912E-05*	Ib/h           0*           0.000285412*           0*           0.000249156*           0.000108052*           1.02153E-05*           3.38532E-05*           3.90495E-06*           1.04591E-06*           2.11948E-07*           8.61550E-08*           0*           5.04094E-06*           5.64068E-09*           6.89351E-07*           5.99255E-11*	Ib/h           0           0.0316492           0           0.0344544           0.0658226           0.0197788           0.0883980           0.0301666           0.0142403           0.00653730           0.00510689           0           0.217725           0.00145034           0.102994           9.99183E-05	Ib/h           0*           0.000888852*           0*           0.000775941*           0.000336505*           3.18131E-05*           0.000105428*           1.21611E-05*           3.25726E-06*           6.60064E-07*           2.68310E-07*           0*           1.56989E-05*           1.75666E-08*           2.14683E-06*           1.86625E-10*	Ib/h           0*           0.758714*           0*           3.49058*           32.6091*           35.2351*           188.420*           220.243*           372.552*           306.410*           696.926*           0*           36.2706*           874.123*           84.7752*           485.228*	Ib/h           0*
Ib/h           0           0.00674553           0           0.00572266           0.0125548           0.00534616           0.0175088           0.00830400           0.00628305           0.00253923           0.00280734           0           0.000487582           0.000932331           0.000292486           7.95914E-05           9.49261E-06	Ib/h           0*           0.00551920*           0*           0.00465211*           0.0120905*           0.00530227*           0.0173634*           0.00828722*           0.00627856*           0.00253832*           0.002608057*           0.000465922*           0.000465922*           0.000932307*           0.000289524*           7.95912E-05*           9.46692E-06*	Ib/h           0*           0.000285412*           0*           0.000249156*           0.000108052*           1.02153E-05*           3.38532E-05*           3.90495E-06*           1.04591E-06*           2.11948E-07*           8.61550E-08*           0*           5.04094E-06*           5.64068E-09*           6.89351E-07*           5.99255E-11*           5.9779E-09*	Ib/h           0           0.0316492           0           0.0344544           0.0658226           0.0197788           0.0883980           0.0301666           0.0142403           0.00653730           0.00510689           0           0.217725           0.00145034           0.102994           9.99183E-05           0.00277876	Ib/h           0*           0.000888852*           0*           0.000775941*           0.000336505*           3.18131E-05*           0.000105428*           1.21611E-05*           3.25726E-06*           6.60064E-07*           2.68310E-07*           0*           1.56989E-05*           1.75666E-08*           2.14683E-06*           1.86625E-10*           1.86165E-08*	Ib/h           0*           0.758714*           0*           3.49058*           32.6091*           35.2351*           188.420*           220.243*           372.552*           306.410*           696.926*           0*           36.2706*           874.123*           84.7752*           485.228*           8.21615*	Ib/h           0*      0*
Ib/h           0           0.00674553           0           0.00572266           0.0125548           0.00534616           0.0175088           0.00830400           0.00628305           0.00253923           0.00280734           0           0.000487582           0.000932331           0.000292486           7.95914E-05           9.49261E-06           4.29288E-05	Ib/h           0*           0.00551920*           0*           0.00465211*           0.0120905*           0.00530227*           0.0173634*           0.00828722*           0.00627856*           0.00253832*           0.00263832*           0.00280697*           0*           0.000465922*           0.000465922*           0.000289524*           7.95912E-05*           9.46692E-06*           4.28568E-05*	Ib/h           0*           0.000285412*           0*           0.000249156*           0.000108052*           1.02153E-05*           3.38532E-05*           3.90495E-06*           1.04591E-06*           2.11948E-07*           8.61550E-08*           0*           5.04094E-06*           5.64068E-09*           6.89351E-07*           5.99255E-11*           5.97779E-09*           1.67403E-08*	Ib/h           0           0.0316492           0           0.0344544           0.0658226           0.0197788           0.0883980           0.0301666           0.0142403           0.00653730           0.00510689           0           0.217725           0.00145034           0.102994           9.99183E-05           0.00277876           0.00892930	Ib/h           0*           0.000888852*           0*           0.000775941*           0.000336505*           3.18131E-05*           0.000105428*           1.21611E-05*           3.25726E-06*           6.60064E-07*           2.68310E-07*           0*           1.56989E-05*           1.75666E-08*           2.14683E-06*           1.86625E-10*           1.86165E-08*           5.21338E-08*	Ib/h           0*           0.758714*           0*           3.49058*           32.6091*           35.2351*           188.420*           220.243*           372.552*           306.410*           696.926*           0*           36.2706*           874.123*           84.7752*           485.228*           8.21615*           47.0146*	Ib/h           0*      0*
Ib/h           0           0.00674553           0           0.00572266           0.0125548           0.00534616           0.0175088           0.00830400           0.00628305           0.00253923           0.00280734           0           0.000487582           0.000932331           0.000292486           7.95914E-05           9.49261E-06           4.29288E-05           4.13853E-06	Ib/h           0*           0.00551920*           0*           0.00465211*           0.0120905*           0.00530227*           0.0173634*           0.00828722*           0.00627856*           0.00253832*           0.00263832*           0.00280697*           0*           0.000465922*           0.000465922*           0.000289524*           7.95912E-05*           9.46692E-06*           4.28568E-05*           4.12686E-06*	Ib/h           0*           0.000285412*           0*           0.000249156*           0.000108052*           1.02153E-05*           3.38532E-05*           3.90495E-06*           1.04591E-06*           2.11948E-07*           8.61550E-08*           0*           5.04094E-06*           5.64068E-09*           6.89351E-07*           5.99255E-11*           5.97779E-09*           1.67403E-08*           2.71649E-09*	Ib/h           0           0.0316492           0           0.0344544           0.0658226           0.0197788           0.0883980           0.0301666           0.0142403           0.00653730           0.00510689           0           0.217725           0.00145034           0.102994           9.99183E-05           0.00277876           0.00892930           0.00182441	Ib/h           0*           0.000888852*           0*           0.000775941*           0.000336505*           3.18131E-05*           0.000105428*           1.21611E-05*           3.25726E-06*           6.60064E-07*           2.68310E-07*           0*           1.56989E-05*           1.75666E-08*           2.14683E-06*           1.86625E-10*           1.86165E-08*           5.21338E-08*           8.45989E-09*	Ib/h           0*           0.758714*           0*           3.49058*           32.6091*           35.2351*           188.420*           220.243*           372.552*           306.410*           696.926*           0*           36.2706*           874.123*           84.7752*           485.228*           8.21615*           47.0146*           4.56453*	Ib/h           0*      0*           0*
Ib/h           0           0.00674553           0           0.00572266           0.0125548           0.00534616           0.0175088           0.00830400           0.00628305           0.00253923           0.00280734           0           0.000487582           0.000932331           0.000292486           7.95914E-05           9.49261E-06           4.29288E-05           4.13853E-06           1.16228E-05	Ib/h           0*           0.00551920*           0*           0.00465211*           0.0120905*           0.00530227*           0.0173634*           0.00828722*           0.00627856*           0.00253832*           0.00263832*           0.00280697*           0*           0.000465922*           0.000289524*           7.95912E-05*           9.46692E-06*           4.28568E-05*           4.12686E-06*           1.16001E-05*	Ib/h           0*           0.000285412*           0*           0.000249156*           0.000108052*           1.02153E-05*           3.38532E-05*           3.90495E-06*           1.04591E-06*           2.11948E-07*           8.61550E-08*           0*           5.04094E-06*           5.64068E-09*           6.89351E-07*           5.99255E-11*           5.97779E-09*           1.67403E-08*           2.71649E-09*           5.26179E-09*	Ib/h           0           0.0316492           0           0.0344544           0.0658226           0.0197788           0.0883980           0.0301666           0.0142403           0.00653730           0.00510689           0           0.217725           0.00145034           0.102994           9.99183E-05           0.00277876           0.00892930           0.00182441           0.00261294	Ib/h           0*           0.000888852*           0*           0.000775941*           0.000336505*           3.18131E-05*           0.000105428*           1.21611E-05*           3.25726E-06*           6.60064E-07*           2.68310E-07*           0*           1.56989E-05*           1.75666E-08*           2.14683E-06*           1.86625E-10*           1.86165E-08*           5.21338E-08*           8.45989E-09*           1.63867E-08*	Ib/h           0*           0.758714*           0*           3.49058*           32.6091*           35.2351*           188.420*           220.243*           372.552*           306.410*           696.926*           0*           36.2706*           874.123*           84.7752*           485.228*           8.21615*           47.0146*           4.56453*           11.8678*	Ib/h           0*      0*           0*           0*           0*           0*           0*
Ib/h           0           0.00674553           0           0.00572266           0.0125548           0.00534616           0.0175088           0.00830400           0.00628305           0.00253923           0.00280734           0           0.000487582           0.000932331           0.000292486           7.95914E-05           9.49261E-06           4.29288E-05           4.13853E-06           1.16228E-05           1.09287E-05	Ib/h           0*           0.00551920*           0*           0.00465211*           0.0120905*           0.00530227*           0.0173634*           0.00828722*           0.00627856*           0.00253832*           0.002628524*           0.000289524*           7.95912E-05*           9.46692E-06*           4.28568E-05*           4.12686E-06*           1.16001E-05*           1.09287E-05*	Ib/h           0*           0.000285412*           0*           0.000249156*           0.000108052*           1.02153E-05*           3.38532E-05*           3.90495E-06*           1.04591E-06*           2.11948E-07*           8.61550E-08*           0*           5.04094E-06*           5.64068E-09*           6.89351E-07*           5.99255E-11*           5.97779E-09*           1.67403E-08*           2.71649E-09*           5.26179E-09*           1.67449E-12*	Ib/h           0           0.0316492           0           0.0344544           0.0658226           0.0197788           0.0883980           0.0301666           0.0142403           0.00653730           0.00510689           0           0.217725           0.00145034           0.102994           9.99183E-05           0.00277876           0.00892930           0.00182441           0.00261294           1.30691E-05	Ib/h           0*           0.000888852*           0*           0.000775941*           0.000336505*           3.18131E-05*           0.000105428*           1.21611E-05*           3.25726E-06*           6.60064E-07*           2.68310E-07*           0*           1.56989E-05*           1.75666E-08*           2.14683E-06*           1.86165E-08*           5.21338E-08*           8.45989E-09*           1.63867E-08*           5.21482E-12*	Ib/h           0*           0.758714*           0*           3.49058*           32.6091*           35.2351*           188.420*           220.243*           372.552*           306.410*           696.926*           0*           36.2706*           874.123*           84.7752*           485.228*           8.21615*           47.0146*           4.56453*           11.8678*           187.486*	Ib/h           0*      0*           0*           0*           0*           0*           0*           0*           0*
Ib/h           0           0.00674553           0           0.00572266           0.0125548           0.00534616           0.0175088           0.00830400           0.00628305           0.00253923           0.00280734           0           0.000487582           0.000932331           0.000292486           7.95914E-05           9.49261E-06           4.29288E-05           4.13853E-06           1.16228E-05           1.09287E-05           1.58183E-06	Ib/h           0*           0.00551920*           0*           0.00465211*           0.0120905*           0.00530227*           0.0173634*           0.00828722*           0.00627856*           0.00253832*           0.002628524*           0.000289524*           7.95912E-05*           9.46692E-06*           4.28568E-05*           4.12686E-06*           1.6001E-05*           1.09287E-05*           1.58183E-06*	Ib/h           0*           0.000285412*           0*           0.000249156*           0.000108052*           1.02153E-05*           3.38532E-05*           3.90495E-06*           1.04591E-06*           2.11948E-07*           8.61550E-08*           0*           5.04094E-06*           5.64068E-09*           6.89351E-07*           5.99255E-11*           5.97779E-09*           1.67403E-08*           2.71649E-09*           5.26179E-09*           1.67449E-12*           2.13081E-14*	Ib/h           0           0.0316492           0           0.0344544           0.0658226           0.0197788           0.0883980           0.0301666           0.0142403           0.00653730           0.00510689           0           0.217725           0.00145034           0.102994           9.99183E-05           0.00277876           0.00892930           0.00182441           0.00261294           1.30691E-05           1.67958E-06	Ib/h           0*           0.000888852*           0*           0.000775941*           0.000336505*           3.18131E-05*           0.000105428*           1.21611E-05*           3.25726E-06*           6.60064E-07*           2.68310E-07*           0*           1.56989E-05*           1.75666E-08*           2.14683E-06*           1.86165E-08*           5.21338E-08*           8.45989E-09*           1.63867E-08*           5.21482E-12*           6.63592E-14*	Ib/h           0*           0.758714*           0*           3.49058*           32.6091*           35.2351*           188.420*           220.243*           372.552*           306.410*           696.926*           0*           36.2706*           874.123*           84.7752*           485.228*           8.21615*           47.0146*           4.56453*           11.8678*           187.486*           263.046*	Ib/h           0*      0*           0*           0*           0*           0*           0*           0*           0*           0*
Ib/h           0           0.00674553           0           0.00572266           0.0125548           0.00534616           0.0175088           0.00830400           0.00628305           0.00253923           0.00280734           0           0.000487582           0.000932331           0.000292486           7.95914E-05           9.49261E-06           4.29288E-05           4.13853E-06           1.16228E-05           1.09287E-05           1.58183E-06           0.165187	Ib/h           0*           0.00551920*           0*           0.00551920*           0*           0.00551920*           0.00551920*           0.00465211*           0.0173634*           0.00828722*           0.00627856*           0.00253832*           0.00280697*           0*           0.000465922*           0.00032307*           0.000289524*           7.95912E-05*           9.46692E-06*           4.12686E-05*           4.12686E-06*           1.6001E-05*           1.09287E-05*           1.58183E-06*           0.00193003*	Ib/h           0*           0.000285412*           0*           0.000249156*           0.000108052*           1.02153E-05*           3.38532E-05*           3.90495E-06*           1.04591E-06*           2.11948E-07*           8.61550E-08*           0*           0*           0*           0.4591E-06*           2.04094E-06*           5.64068E-09*           6.89351E-07*           5.99255E-11*           5.97779E-09*           1.67403E-08*           2.71649E-09*           5.26179E-09*           1.67449E-12*           2.13081E-14*           0.0379960*	Ib/h           0           0.0316492           0           0.0344544           0.0658226           0.0197788           0.0883980           0.0301666           0.0142403           0.00510689           0           0.217725           0.00145034           0.102994           9.99183E-05           0.00277876           0.00892930           0.00182441           0.00261294           1.30691E-05           1.67958E-06           7081.77	Ib/h           0*           0.000888852*           0*           0.000775941*           0.000336505*           3.18131E-05*           0.000105428*           1.21611E-05*           3.25726E-06*           6.60064E-07*           2.68310E-07*           1.56989E-05*           1.75666E-08*           2.14683E-06*           1.86165E-08*           5.21338E-08*           8.45989E-09*           1.63867E-08*           5.21482E-12*           6.63592E-14*           0.118330*	Ib/h           0*           0.758714*           0*           3.49058*           32.6091*           35.2351*           188.420*           220.243*           372.552*           306.410*           696.926*           0*           36.2706*           874.123*           84.7752*           485.228*           8.21615*           47.0146*           4.56453*           11.8678*           187.486*           263.046*           0*	Ib/h           0*

PW F/W/B	PW Flashing	PW Loding	PW to Tanks	PW Working	Sep Condensate	Sep PW
Solved	Solved	Solved	Solved	Solved	Solved	Solved
MIX-101			Gunbarrel			
	MIX-101	MIX-101		MIX-101	MIX-106	MIX-106
81.6503	97.8	76.2171	70	76.2171	92*	92*
0.454295	12.8800	0.454295	14.6959	0.454295	34.6959*	34.6959*
100	100	100	0	100	0	0
0	0	0	100	0	100	100
0	0	0	0	0	0	0
100	100	100	100	100	100	100
21.8640	44.1605	18.0936	18.0164	18.0936	89.9238	18.0153
0.00171049	0.0962890	0.00142997	62.2807	0.00142997	41.4048	62.0499
0.0107424	0.00155380	0.00213853	393.109	0.00665997	42.9990	393.115
0.234871	0.0686165	0.0386937	7082.41	0.120503	3866.63	7082.09
137.312	0.712610	27.0591	113.718	84.2694	93.3859	114.135
17.1194	0.0888449	3.37360	14.1778	10.5063	11.6429	14.2299
9.78373E-05	1.41514E-05	1.94769E-05	3.58029	6.06565E-05	0.391618	3.58035
0.000603219	0.000260064	7.98653E-05	14.1590	0.000248723	11.4449*	14.1576*
0.999605	0.987389	0.999538	0.000747898	0.999538	0.0127280	0.00170152
0.754907	1.52475	0.624725	0.998589	0.624725	0.663872	0.994887
			10.0005		76.5028	9.99583
-1025.81	-79.1821	-220.316	-4.83553E+07	-686.124	-3.59378E+06	-4.82044E+07
-4367.54	-1153.98	-5693.84	-6827.52	-5693.84	-929.434	-6806.52
0.436350	0.424599	0.445656	0.978677	0.445656	0.534341	0.977228
1.26297	1.11921	1.32691	1.32922	1.32691	1.05884	1.32847
0.0101745	0.00882388	0.00999099	0.995713	0.00999099	0.303184	0.765515
371.338	5.72087	436.174	0.998068	436.174	0.457125	0.770180
0.0116560	0.0119943	0.0119153	0.347035	0.0119153	0.0676796	0.356821
			0.00503205?		0.00117956	0.00486861
339.349	2240.82	17.8079	0.0793467	17.8079	4567.21	0
5101.95	19084.2	-668.818	-1058.01	-668.818	19114.0	-1059.76
411.692	2437.17	69.1815	50.3931	69.1815	4924.55	50.3100
6357.68	20771.8	408.674	1.76705	408.674	20622.2	0

MANLE	Y GAS TE	STING, INC.
P.O. DRAWER 193 OFFICE(432)367-3024	FAX(432)367-116	ODESSA, TEXAS 79760 6 E-MAIL: MANLEYGAST@AOL.COM
CHARGE 23 - 5316 REC. NO 0 TEST NUMBER 61376 SAMPLE TYPE SPOT		DATE SAMPLED 05-24-23 TIME SAMPLED 14:45 DATE RUN 05-25-23
STATION NO PRODUCER ENLINK SAMPLE NAME HORNED FROG RECEIVED FROM ENLINK MIDST LOCATION MIDLAND TEXA	INLET FREAM AS	
FLOWING PRESSURE	0 PSIG	FLOWING TEMPERATURE 0 F
SAMPLED BY: 182		CYLINDER NO NONE
CALCU MOL% HYDROGEN SULFIDE	GPM (REAL) GPM (REAL)	'Z' FACTOR (DRY) = 0.9955 'Z' FACTOR (WET) = 0.9950
CALCULATED SPECIFIC GRAV	ITIES	CALCULATED GROSS HEATING VALUES
IDEAL, DRY 0.8129 IDEAL, WET 0.8096 REAL, DRY 0.8162 REAL, WET 0.8133		BTU/CF - IDEAL, DRY 1358.8 BTU/CF - IDEAL, WET 1335.0 BTU/CF - REAL, DRY 1364.9 BTU/CF - REAL, WET 1341.7
* BASED ON GPA STANDARDS 22 DISTRIBUTION AND REMARKS: T. LEBLANC / B. BROWN / S.	61-20 / 2145-16 / TIRMZI / A. ORTIZ	/ 2172-19 Z / L. GUELKER

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ANALYZED BY: JT

APPROVED : KC

MANLEY GAS TESTING INC. 120 DOCK ROAD - ODESSA, TEXAS-432-367-3024

#### A SAMPLE OF ENLINK-HORNED FROG INLET 5-24-23

	CAPILLARY EXTENDED C-6+ ANALYSIS (NORMALIZED TO 100%)		PAGE NO. 1
COMPONENT	MOL%	WT%	
NEOHEXANE         2, 3DMC4+CYC5         2MPENTANE         3MPENTANE         3MPENTANE         2, 2 DMPENTANE         MCYCLOPENTANE         2, 4 DMPENTANE         2, 2, 3 TMBUTANE         2, 4, 0MPENTANE         2, 2, 3 TMBUTANE         2, 4, 0MPENTANE         2, 2, 3 TMBUTANE         2, 4, 0MPENTANE         2, 2, 3 TMBUTANE         2, 2, 3 TMBUTANE         2, 3, 0MPENTANE         2, 3 DMPENTANE         2, 3 JTMPENTANE         2, 3 JTMPENTANE         2, 3 JTMPENTANE         2, 3 JTMPENTANE         2, 3 DMHEXANE         2, 3 DMHEXANE         3, 4DMHEXANE         3, 4DMHEXANE         3, 4DMHEXANE         2, 3, 5TRIMHEXANE         2, 3, 5TRIMHEXANE         2, 3, 5TRIMHEXANE         2, 2, 4TRIMHEXANE         2, 2, 3TRIMHEXANE         2, 3DIMHEPTANE         3,	0.417 4.109 12.519 6.559 16.993 0.173 7.459 0.398 0.029 2.055 0.070 9.676 2.365 1.247 2.815 6.278 6.601 9.307 0.432 0.000 1.771 0.096 0.004 1.474 0.278 0.095 0.747 0.114 1.322 1.158 0.030 0.030 0.076 0.013 0.020 0.0013 0.020 0.000 0.0013 0.020 0.000 0.000 0.0008 0.221 0.104 0.030 0.030 0.030 0.030 0.030 0.030 0.030 0.022 0.126	0.390 3.346 11.712 6.136 15.903 0.189 6.815 0.433 0.031 1.743 0.076 8.841 2.573 1.357 3.063 6.692 7.181 9.921 0.536 0.000 1.771 0.118 0.926 0.139 1.610 1.436 0.042 0.138 0.028 0.018 0.028 0.001 0.269 0.175	
3EHEPTANE	0.032	0.045	

MANLEY GAS TESTING INC. 120 DOCK ROAD - ODESSA, TEXAS-432-367-3024

### A SAMPLE OF ENLINK-HORNED FROG INLET 5-24-23

			======
	(NORMALIZED TO		
	=======================================	PAGE N	10.2
COMPONENT			
COMPONENT	MOL%	WT%	
4MOCTANE	0 074	0 100	
3MOCTANE	0.044	0.103	
0-XYLENE	. 0.082	0.001	
IC4CYCPENTANE	. 0.036	0.049	
N-NONANE	. 0.328	0.457	
I-DECANE	. 0.031	0.047	
	. 0.030	0.041	
	. 0.027	0.036	
	· U.16/	0.258	
NC4CYCC6	0.529	0.81/	
NC3BENZENE	. 0.208	0.051	
M+P E-TOLUENE	0.129	0.272	
O-E-TOLUENE	. 0.046	0.060	
2,2DMOCTANE	. 0.084	0.130	
IERIBUTYLBENZENE	. 0.007	0.010	
2 6DMOCTANE	0.015	0.019	
	0.045	0.069	
	0.123	0.180	
N DECANE IIIIIIIIII	0.128	0.198	
UNKNOWN C-6'S	0,000	0 000	
UNKNOWN C-7'S	0.000	0.000	
UNKNOWN C-8'S	0.020	0.024	
UNKNOWN C-9'S	0.088	0.122	
UNK CIE'S THRU CIE'S	0.040	0.073	
UNK CID S THRU CID S	0.000	0.000	
UNK CI7 3 THRU C20 5	0.000	0.000	
TOTAL	100 000	100,000	
	=======================================		
	=======================================		
COMPONENT GROUPINGS ( ====================================	PARAFFINS-NAPTHENES	S-AROMATICS)	
	MOL% WT%	* C6+ CHARACTERIZATION	2 <b>2 2 2 2</b> 2 2
TOTAL C-6'S	59 787 54 886		
TOTAL C-7'S	31.054 33.287	SP GRAVITY $-$ 3 1903	
TOTAL C-8'S	6.464 7.935	BTU/FT3(DRY) = 4966 863	
IUTAL C-9'S	1.507 2.059	BTU/FT3(WET) = 4881,316	
IUIAL C-10'S	1.148 1.760	CU.FT./GAL = 24.746	
TOTAL C-11 THRU C-14 $TOTAL C 15 TUDU C 1C$	0.040 $0.073$	GAL/CU.FT. = 0.040411	
TOTAL C-ID INKU C-16		MOL% C6+ AROMATICS = 4.884	
101AL C-17 INKU C-20			
TOTAL	100.000 100 000		

MA	NLEY	GAS	TESTI	NG, INC.	
P.O. DRAW OFFICE(432)367-	ER 193 3024	FAX(432)	367-1166	ODESSA, TEXAS 79760 E-MAIL: MANLEYGAST@	AOL.COM
CHARGE 16 RECORD NO TEST NUMBER 2	2 - 0 - 0 7064	0		DATE SAMPLED	05-10-23 05-19-23
METER NUMBER A SAMPLE OF H RECEIVED FROM E LOCATION F	ORNED FRO NLINK PER T. WORTH	G CONDENS MIAN LLC. TEXAS	ATE		
PRESSURE	20	PSIG	TEMP	ERATURE 92	F
	CALCU	FRACTION ILATED @ 1	AL ANALYSI 4.696 PSIA	S AND 60F	
	MOLE%	LIQUID%	WEIGHT%		
NITROGEN CARBON DIOXIDE.	0.00	0.00	0.00 0.00	TOTAL SP. GRAVITY	0.6979

\*\* CAPILLARY EXTENDED HEXANES+ CALCULATIONS \*\*

0.02

0.09

0.85

0.92

4.91

5.74

9.71

77.76

100.00

SP. GRAVITY C6+ (	9.7290	VAPOR PRESS C6+ 2.797	CF/GAL C6+		23.288
MOLECULAR WT C6+.	99.375		LB/GAL C6+	••	6.078

ANALYSIS BASED ON GPA STANDARDS 2177-13 & 2186-14

0.11

0.27

1.72

1.41

7.54 7.10

12.01

69.84

100.00

0.05

0.18

 $1.17 \\ 1.14$ 

5.86

6.41

10.74

74.45

100.00

DISTRIBUTION / REMARKS :

S. TIRMZI

RUN BY: K.CASWELL

METHANE..... ETHANE..... PROPANE....

ISO-BUTANE....

NOR-BUTANE....

ISO-PENTANE....

NOR-PENTANE....

HEXANES+ .....

APPROVED [1]

TOTAL VAPOR PRESS..

TOTAL MOLECULAR WT..

21.094

89.250

#### MANLEY GAS TESTING INC.

120 DOCK ROAD - ODESSA, TEXAS-432-367-3024

#### A SAMPLE OF HORNED FROG CONDENSATE (5/10/23)

#### 

#### CAPILLARY EXTENDED

#### C-6+ ANALYSIS (NORMALIZED TO 100%)

PAGE NO. 1


COMPONENT	MOL %	LIQ%	WT8
NEQUEVAND	0 18	0 17	0 16
NECHEAANE	1 59	1 25	1 10
	1.JO 7 91	5 02	6 25
ZMPENTANE	1.21	2 02	3 52
SMPENTANE	4.00	11 27	10 20
N-HEXANE	11.04	0 10	10.29
Z,Z DMPENTANE	5 00	4 01	5 09
MCYCLOPENTANE	0.04	4.91	5.00
2,4 DMPENTANE	0.04	0.04	0.04
Z,Z,3 TMBUTANE	1 54	1 00	1 21
BENZENE	1.04	1.00	1.21
3,3 DMPENTANE	7 92	6 24	6 71
CYCLOHEXANE	2 11	2 25	3 1/
ZMHEAANE	3.11	1 17	J.14 1 /1
2,3 DMPENTANE	2.40	2 22	2.05
SMHEXANE	3.03	3.22	1 20
DIMCYCPENTANES(GROUPED)	4.34	4.07 7 3 <i>4</i>	4.49
N-HEPIANE	10 11	7.3 <del>1</del> Q. <i>1</i> 1	Q QQ
2 2DMUEVANE	1 28	1 53	1 47
$2,2DFINEAANE \dots$	0.00	0.00	0 00
Z, J, JIMPENIANE	3.06	2 37	2 83
	0.36	0.42	0 41
	0.00	0.42	0.41
2MUEDENIANE	4 12	4 90	4 73
	0 16	0.19	0.18
3 ADMHEYANE	0.00	0.00	0.00
	1.75	2.06	2.01
TRIMCYCPENTANES (GROUPED)	0.27	0.29	0.31
DIMCYCHEXANES (GROUPED)	2.83	3.02	3.19
N-OCTANE	2.47	2.92	2.84
2.3.5TRIMHEXANE	0.39	0.50	0.50
2.2.4TRIMHEXANE	0.05	0.07	0.07
2.2DIMHEPTANE	0.08	0.10	0.10
2.2.3TRIMHEXANE	0.05	0.07	0.07
2,5DIMHEPTANE	0.00	0.00	0.00
I-NONANE	0.00	0.00	0.00
2.4DIMHEPTANE	0.00	0.00	0.00
E-CYCHEXANE	0.87	0.90	0.98
3,3DIMHEPTANE	0.35	0.45	0.45
2,6DIMHEPTANE	0.13	0.16	0.16
E-BENZENE	0.26	0.23	0.28
2,3DIMHEPTANE	0.00	0.00	0.00
M-XYLENE	1.47	1.31	1.57
P-XYLENE	0.37	0.33	0.39
3,4DIMHEPTANE	0.37	0.47	0.47
SEHEPTANE	0.00	0.00	0.00

#### MANLEY GAS TESTING INC.

120 DOCK ROAD - ODESSA, TEXAS-432-367-3024

#### A SAMPLE OF HORNED FROG CONDENSATE (5/10/23)

#### CAPILLARY EXTENDED

#### C-6+ ANALYSIS

	(NORMALIZE	D TO 1	00%) ========	=====	P/	AGE NO.	2
	0.10		0 1 2		0.10		
4MOCTANE	0.10		0.13		0.12		
3MOCTANE	0.23		0.29		0.29		
O-XYLENE	0.14		0.12		0.13		
IC4CYCPENTANE	0.34		0.40		0.43		
N-NONANE	0.93		1.22		1.21		
<b>I</b> - <b>DECANE</b>	0.16		0.23		0.23		
1E1MCYC6	0.18		0.21		0.23		
IC3BENZENE	0.16		0.17		0.20		
2,3DMOCTANE	0.95		1.33		1.35		
<b>3EOCTANE</b>	2.29		3.20		3.27		
NC4CYCC6	0.00		0.00		0.00		
NC3BENZENE	0.20		0.20		0.24		
M+P E-TOLUENE	0.16		0.16		0.19		
O-E-TOLUENE	0.40		0.40		0.48		
2,2DMOCTANE	1.30		1.87		1.87		
TERTBUTYLBENZENE	0.34		0.39		0.45		
1,3,5TMBENZENE	0.08		0.08		0.10		
3,6DMOCTANE	0.19		0.26		0.27		
IC4BENZENE	0.45		0.52		0.61		
N-DECANE	0.48		0.68		0.69		
UNKNOWN C-6'S	0.00		0.00		0.00		
UNKNOWN C-7'S	0.00		0.00		0.00		
UNKNOWN C-8'S	0.04		0.05		0.05		
UNKNOWN C-9'S	0.67		0.87		0.86		
UNK C10'S THRU C14'S	0.16		0.27		0.28		
UNK C15'S THRU C16'S	0.00		0.00		0.00		
UNK C17'S THRU C20'S	0.00		0.00		0.00		
TOTAL	100.00	•	100.00		100.00		
		=======	==========	=====	=======================================	===========	
COMPONENT GROUPINGS (I	PARAFFINS-NAPI	HENES-	AROMATI	CS)			
	MOL%	LIQ%	=======	==== WT%			
	40 31	35 59	3	<u>4</u> Δ1	- SP GRAV	C6+ =	0 7200
	32 11	31 44	3	1 84	MOL WT	C6+ =	99 375
	16 30	18 27	1	8 56	GAL /LB	C6+ -	16 364
TOTAL C-0 B	4 87	5 95	± 1	6 17		C6+ -	23 289
TOTAL C-7 8	<del>1</del> .07 6 16	0.7J Q /Q		Q 71	LR/CAT	C6+ -	6 070
	0.16	0.40		0.74	DD/ GAD.		0.078
TOTAL C-II INKU C-14	0.10	0.21		0.20		ANTOO	- 9 63
TOTAL C-13 THEO C-10	0.00	0.00		0.00	NUAN TO FLOR	601170	- 0.03
TOTAL C-1/ THEO C-20	0.00	0.00		0.00			
TOTAL	L00.00 1	.00.00	10	0.00	_		

### ICE CATALYST SIZING PROGRAM

rev 2.1.3

Report Date: 7/19/2023



Custome Sales Pe Project Engine I	er Enlink rson KW Horne Name Caterp	Midstream d Frog CS iillar G3516B G3	516B 1380	) BHP @ 14	Housing Element Contact 00 RPM	. MCC Mike	-7140-2 Luckett					
Engine Pov	wer	1380.0	BHP	ACFM		9127.0	CU.	FT/MIN	Exhaust 02		8	%
Exhaust M	ass Flow	14949.0	LBS/HR	ACFH		547620	) CU.	FT/HR	Exhaust CO2		6.4	%
Process Te	emperature	993.0	F	SCFM		3271.5	5 CU.	FT/MIN	Exhaust H2O		11.6	%
Exhaust Pr	ressure	14.5	PSI	SCFH		196288	B CU.	FT/HR	Exhaust N2		74	%
Exhaust De	ensity	0.0273	LBS/FT*	3 Std Te	mp	68.0	)	F	Max Pressure D	)rop	12.0	in wc
Molecular	Weight	29.35	AMU	Std Pr	essure	14.6959	9	PSI	Propane in Fuel		0.00	%
ACS Par OEM Pa Type Geomet X Y	t Name rt Name ry	RN15.440) MCC-7140 NG/Diesel Rectangula 15.440in 24.750in	(24.750X3. -2 (Lean) ar	500-300	Layers Modules Guard B	s/Layer ed	1 3 No		Cell Coun Depth	t	31 3.	00cpsi .500in
(	Open Area	7.145	ft^2		Part Volum	e	0.695	ft^3	Part We	eight	46	lbs
Lin	ear Velocity	1277	ft/min		Total Volum	ne	2.084	ft^3	Total We	eight	138	lbs
Pre	essure Drop	1.4	in wc		Space Veloc	ity	94193	GHSV				
					Inlet Err	nissions						
		g/bhp	p-hr	lb/hr	tons	s/year	pp	mv	ppmvd	рр	mvd%C	02
	NOx	0.5	5	1.67	7.	.33	71.	.40	80.77		40.21	
	CO	3.1	l)	9.47	41	.51	663	.77	750.87		373.85	
		1.24	4	3.78	16	.59	168	.4/	190.58		94.89	
V		1.6	7	5.00	20	./3	253	.52	90.74		48.10	
	00111200	1.01		0.09	Target Fr	missions	200		207.02		140.00	
	min %DI	RE g/bhp	p-hr	lb/hr	tons	s/year	qq	mv	ppmvd	qq	mvd%C	)2
NOx	0.00	0.5	5	1.67	7.	.33	71.	.40	80.77		40.21	
CO	80.08	0.62	2	1.89	8	.27	132	.20	149.55		74.46	
VOC	60.37	0.49	9	1.50	6	.57	66.	.77	75.53		37.60	
H2CO	80.00	0.09	9	0.26	1.	.15	17.	.10	19.35		9.63	
VOC+H2C	65.41	0.58	3	1.76	7.	.72	83.	.87	94.88		47.24	
				Em	issions w	ith Catal	yst					
	%DRE	g/bhp	p-hr	lb/hr	tons	/year	ppi	mv	ppmvd	рр	mvd%C	02
NOx	0.00	<0.5	5	<1.67	<7	.33	<71	.40	<80.77		<40.21	
CO	80.08	<0.6	2	<1.89	<8	.27	<132	2.20	<149.55		<74.46	
VOC	60.37	< 0.4	9	<1.50	<6	.5/	<66	.//	<75.53		<37.60	
	δ0.00 65.41	<0.0	8	<0.20	<	.15	<1/	.10	<19.35		< 9.03	
WILL TIL/	0.4	NU.0	0	\$1.70	5/	.16	~03	.07	N74.00		-41.24	

Safety Value: 2 VOC Molecular Weight: 44.1 02 Reference Value: 15 Uptime (TPY): 100% (8760 hours)

GAS COMPRESSION APPLICATION

#### GAS ENGINE SITE SPECIFIC TECHNICAL DATA

FUEL:



ENGINE SPEED (rpm): COMPRESSION RATIO: AFTERCOOLER TYPE: AFTERCOOLER - STAGE 2 INLET (°F): AFTERCOOLER - STAGE 1 INLET (°F): JACKET WATER OUTLET (°F): ASPIRATION: COOLING SYSTEM: CONTROL SYSTEM: EXHAUST MANIFOLD: COMBUSTION: NOx EMISSION LEVEL (g/bhp-hr NOx): SET POINT TIMING:

1400 8 SCAC 130 201 210 ΤA JW+OC+1AC, 2AC ADEM3 DRY LOW EMISSION 0.5

30

RATING STRATEGY: RATING LEVEL: FUEL SYSTEM:

SITE CONDITIONS:

FUEL LHV (Btu/scf):

ALTITUDE(tt):

FUEL METHANE NUMBER:

FUEL PRESSURE RANGE(psig): (See note 1)

MAXIMUM INLET AIR TEMPERATURE(°F): STANDARD RATED POWER:

STANDARD CONTINUOUS CAT WIDE RANGE WITH AIR FUEL RATIO CONTROL

> Gas Analysis 7.0-40.0 63.9 1058 2600 100

1380 bhp@1400rpm

			MAXIMUM	SITE RA	TING AT N	IAXIMUM
			RATING	INLET A	<b>R TEMPE</b>	RATURE
RATING	NOTES	LOAD	100%	100%	75%	50%
ENGINE POWER (WITHOUT FAN)	(2)	bhp	1380	1380	1035	690
INLET AIR TEMPERATURE		°F	100	100	100	100
		-	-		-	
ENGINE DATA						
FUEL CONSUMPTION (LHV)	(3)	Btu/bhp-hr	7435	7435	7963	8553
FUEL CONSUMPTION (HHV)	(3)	Btu/bhp-hr	8210	8210	8793	9444
AIR FLOW (@inlet air temp, 14.7 psia) (WET)	(4)(5)	ft3/min	3286	3286	2577	1802
AIR FLOW (WET)	(4)(5)	lb/hr	13970	13970	10959	7661
FUEL FLOW (60°F, 14.7 psia)		scfm	162	162	130	93
INLET MANIFOLD PRESSURE	(6)	in Hg(abs)	93.8	93.8	76.1	53.5
EXHAUST TEMPERATURE - ENGINE OUTLET	(7)	°F	988	988	973	983
EXHAUST GAS FLOW (@engine outlet temp, 14.5 psia) (WET)	(8)(5)	ft3/min	9130	9130	7100	5002
EXHAUST GAS MASS FLOW (WET)	(8)(5)	lb/hr	14485	14485	11373	7958
EMISSIONS DATA - ENGINE OUT						
NOx (as NO2)	(9)(10)	g/bhp-hr	0.50	0.50	0.50	0.50
CO	(9)(10)	g/bhp-hr	2.83	2.83	3.03	2.97
THC (mol. wt. of 15.84)	(9)(10)	g/bhp-hr	4.78	4.78	5.12	5.20
NMHC (mol. wt. of 15.84)	(9)(10)	g/bhp-hr	1.76	1.76	1.88	1.91
NMNEHC (VOCs) (mol. wt. of 15.84)	(9)(10)(11)	g/bhp-hr	0.74	0.74	0.79	0.80
HCHO (Formaldehyde)	(9)(10)	g/bhp-hr	0.43	0.43	0.42	0.41
CO2	(9)(10)	g/bhp-hr	491	491	524	570
EXHAUST OXYGEN	(9)(12)	% DRY	9.1	9.1	8.8	8.4
HEAT REJECTION						
HEAT REJ. TO JACKET WATER (JW)	(13)	Btu/min	23277	23277	21905	20584
HEAT REJ. TO ATMOSPHERE	(13)	Btu/min	6110	6110	5092	4074
HEAT REJ. TO LUBE OIL (OC)	(13)	Btu/min	4475	4475	3978	3363
HEAT REJ. TO A/C - STAGE 1 (1AC)	(13)(14)	Btu/min	13221	13221	11024	4008
HEAT REJ. TO A/C - STAGE 2 (2AC)	(13)(14)	Btu/min	5743	5743	5389	3485
	I					
TOTAL JACKET WATER CIRCUIT (JW+OC+1AC)	(14)(15)	Btu/min	44857			
TOTAL AFTERCOOLER CIRCUIT (2AC)	(14)(15)	Btu/min	6030			

A cooling system safety factor of 0% has been added to the cooling system sizing criteria.

CONDITIONS AND DEFINITIONS

Engine ratio obtained and presented in accordance with ISO 3046/1, adjusted for fuel, site altitude and site inlet air temperature. 100% rating at maximum inlet air temperature is the maximum engine capability for the specified fuel at site altitude and maximum site inlet air temperature. Maximum rating is the maximum capability at the specified aftercooler inlet temperature for the specified fuel at site altitude and reduced inlet air temperature. Lowest load point is the lowest continuous duty operating load allowed. No overload permitted at rating shown.

For notes information consult page three

#### Engine Power vs. Inlet Air Temperature

Data represents temperature sweep at 2600 ft and 1400 rpm



Engine Power vs. Engine Speed Data represents speed sweep at 2600 ft and 100 °F



1250

Engine Speed (rpm)

1200



#### Engine Torque vs. Engine Speed

1300

1350

1400

Data represents speed sweep at 2600 ft and 100 °F



Note: At site conditions of 2600 ft and 100°F inlet air temp., constant torque can be maintained down to 1050 rpm. The minimum speed for loading at these conditions is 1050 rpm.

1100

1150

1050

### G3516B

GAS COMPRESSION APPLICATION

#### GAS ENGINE SITE SPECIFIC TECHNICAL DATA



#### NOTES

1. Fuel pressure range specified is to the engine fuel pressure regulator. Additional fuel train components should be considered in pressure and flow calculations.

2. Engine rating is with two engine driven water pumps. Tolerance is  $\pm$  3% of full load.

- 3. Fuel consumption tolerance is  $\pm$  3.0% of full load data.
- 4. Air flow value is on a 'wet' basis. Flow is a nominal value with a tolerance of  $\pm$  5 %.
- 5. Inlet and Exhaust Restrictions must not exceed A&I limits based on full load flow rates from the standard technical data sheet.
- 6. Inlet manifold pressure is a nominal value with a tolerance of  $\pm$  5 %.
- 7. Exhaust temperature is a nominal value with a tolerance of (+)63°F, (-)54°F.
- 8. Exhaust flow value is on a "wet" basis. Flow is a nominal value with a tolerance of  $\pm$  6 %.
- 9. Emissions data is at engine exhaust flange prior to any after treatment.

10. Values listed are higher than nominal levels to allow for instrumentation, measurement, and engine-to-engine variations. They indicate the maximum values expected under steady state conditions. Fuel methane number cannot vary more than ± 3. THC, NMHC, and NMNEHC do not include aldehydes. An oxidation catalyst may be required to meet Federal, State or local CO or HC requirements.

11. VOCs - Volatile organic compounds as defined in US EPA 40 CFR 60, subpart JJJJ

12. Exhaust Oxygen level is the result of adjusting the engine to operate at the specified NOx level. Tolerance is  $\pm 0.5$ .

13. Heat rejection values are nominal. Tolerances, based on treated water, are ± 10% for jacket water circuit, ± 50% for radiation, ± 20% for lube oil circuit, and ± 5% for aftercooler circuit.

14. Aftercooler heat rejection includes an aftercooler heat rejection factor for the site elevation and inlet air temperature specified. Aftercooler heat rejection values at part load are for reference only. Do not use part load data for heat exchanger sizing.

15. Cooling system sizing criteria are maximum circuit heat rejection for the site, with applied tolerances.

Constituent	Abbrev	Mole %	Norm		
Water Vapor	H2O	0.0000	0.0000		
Methane	CH4	77.0700	77.0737	Fuel Makeup:	Gas Analysis
Ethane	C2H6	12.9600	12.9606	Unit of Measure:	English
Propane	C3H8	5.0700	5.0702		5
Isobutane	iso-C4H1O	0.2440	0.2440	Calculated Fuel Properties	
Norbutane	nor-C4H1O	0.5726	0.5726		62.0
Isopentane	iso-C5H12	0.0417	0.0417	Caterpillar Methane Number:	63.9
Norpentane	nor-C5H12	0.0325	0.0325		
Hexane	C6H14	0.0000	0.0000	Lower Heating Value (Btu/scf):	1058
Heptane	C7H16	0.0000	0.0000	Higher Heating Value (Btu/scf):	1169
Nitrogen	N2	3.4399	3.4401	WOBBE Index (Btu/scf):	1266
Carbon Dioxide	CO2	0.5645	0.5645		
Hydrogen Sulfide	H2S	0.0000	0.0000	THC: Free Inert Ratio	23 07
Carbon Monoxide	CO	0.0000	0.0000		20.07
Hydrogen	H2	0.0000	0.0000	Total % mens (% N2, $CO2$ , $He$ ).	4%
Oxygen	O2	0.0000	0.0000	RPC (%) (To 905 Btu/sct Fuel):	100%
Helium	HE	0.0000	0.0000		
Neopentane	neo-C5H12	0.0000	0.0000	Compressibility Factor:	0.997
Octane	C8H18	0.0000	0.0000	Stoich A/F Ratio (Vol/Vol):	10.99
Nonane	C9H20	0.0000	0.0000	Stoich A/F Ratio (Mass/Mass):	15.73
Ethylene	C2H4	0.0000	0.0000	Specific Gravity (Belative to Air):	0.699
Propylene	C3H6	0.0000	0.0000	Evel Specific Heat Patia (K):	1 290
TOTAL (Volume %)		99.9952	99.9999	ruei Specific fiela Rallo (K).	1.209

#### CONDITIONS AND DEFINITIONS

Conditions and Derivitions Caterpillar Methane Number represents the knock resistance of a gaseous fuel. It should be used with the Caterpillar Fuel Usage Guide for the engine and rating to determine the rating for the fuel specified. A Fuel Usage Guide for each rating is included on page 2 of its standard technical data sheet.

RPC always applies to naturally aspirated (NA) engines, and turbocharged (TA or LE) engines only when they are derated for altitude and ambient site conditions.

Project specific technical data sheets generated by the Caterpillar Gas Engine Rating Pro program take the Caterpillar Methane Number and RPC into account when generating a site rating.

Fuel properties for Btu/scf calculations are at 60F and 14.696 psia.

Caterpillar shall have no liability in law or equity, for damages, consequently or otherwise, arising from use of program and related material or any part thereof.

FUEL LIQUIDS Field gases, well head gases, and associated gases typically contain liquid water and heavy hydrocarbons entrained in the gas. To prevent detonation and severe damage to the engine, hydrocarbon liquids must not be allowed to enter the engine fuel system. To remove liquids, a liquid separator and coalescing filter are recommended, with an automatic drain and collection tank to prevent contamination of the ground in accordance with local codes and standards.

To avoid water condensation in the engine or fuel lines, limit the relative humidity of water in the fuel to 80% at the minimum fuel operating temperature.

### ICE CATALYST SIZING PROGRAM

rev 2.1.3

Report Date: 9/29/2023



Customer Sales Persc Project Engine Nar	Enlink Mic on KW Horned Fr me Caterpilla	lstream <sup>.</sup> og CS r G3606 A4 0	).5 Caterpi	llar G3606 /	Housing Element Contact A4 0.5	t MC Lai	CC-7 nce	'140-2 Green					
Engine Power		1875.0	BHP	ACFM		12008	8.0	CU. F	T/MIN	Exhaust 02		8	%
Exhaust Mass	Flow	22520.0	LBS/HR	R ACFH		7204	80	CU. F	T/HR	Exhaust CO2		6.4	%
Process Temp	erature	809.0	F	SCFM		4928	8.3	CU. F	T/MIN	Exhaust H20		11.6	%
Exhaust Press	ure	14.5	PSI	SCFH		2957	00	CU. F	T/HR	Exhaust N2		74	%
Exhaust Densit	ty	0.0313	LBS/FT^	3 Std Te	mp	68	8.0		F	Max Pressure D	rop	12.0	in wc
Molecular Weig	ght	29.35	AMU	Std Pro	essure	14.69	59	P	SI	Propane in Fuel		0.00	%
ACS Part N OEM Part N Type Geometry X Y	ame Name	RN15.440X MCC-7140- NG/Diesel Rectangula 15.440in 24.750in	24.750X3. 2 (Lean) Ir	0X3.500-300 Layers 1 Modules/Layer 4 Guard Bed No				Cell Coun Depth	t	3( 3.	00cpsi 500in		
Oper	n Area	9.526	ft^2		Part Volum	e	(	0.695	ft^3	Part We	ight	46	lbs
Linear	Velocity	1260	ft/min		Total Volum	ne	2	2.779 ft^3		Total Weight		183	lbs
Pressu	ire Drop	1.3	in wc		Space Veloc	ity	1	06423	GHSV				
					Inlet En	nissions							
		g/bhp	-hr	lb/hr	tons	s/year		ppm	v	ppmvd	рр	mvd%C	2
N	Ox	0.50	)	2.07	9	.06		58.5	4	66.23	32.97		
C	0	2.20	)	9.09	39	9.86		423.08		478.60		238.29	
V0C+	H2CO	0.69		2.85	12	2.50		95.1	5	107.64		53.59	
		4			larget Ei	mission	S						_
NO	min %DRE	g/bhp	hr	lb/hr	tons	s/year		ppm	עו געו	ppmvd	pp	mvd%C	02
NUX	0.00	0.50		2.07	9	.06		58.5	4	66.23		32.97	
	//.Z/ 56.52	0.50		2.07	9	.00		90.1	7	108.77		22.06	
VUCTHZCU	J0.JZ	0.30	J	T.24	issions M	.44 /ith Cata	alve	42.3 st	1	47.95		23.00	
	%DRF	a/bhp	-hr	lb/hr	tons	s/vear	arys	non	าง	ppmyd	pp	mvd%C	)2
NOx	0.00	<0.5	0	<2.07	<9	9.06		<58.5	54	<66.23	99	<32.97	_
CO	77.27	< 0.5	0	<2.07	<9	9.06		<96.1	6	<108.77		<54.16	
VOC+H2CO	56.52	< 0.3	0	<1.24	<5	5.44		<42.3	37	<47.93	<23.86		

Safety Value: 2 VOC Molecular Weight: 44.1 02 Reference Value: 15 Uptime (TPY): 100% (8760 hours)

# G3606 with ADEM<sup>™</sup> A4 Gas Engine

### 1398-1499 bkW (1875-2010 bhp) @ 1000 rpm 0.5 g/bhp-hr NOx (NTE)



Shown with optional equipment

### **FEATURES AND BENEFITS**

#### **Engine Design**

- Industry-leading power with ambient-based rating capability
- ADEM A4 engine control system provides complete engine control, monitoring, and protection while maintaining emissions.
- Widest fuel tolerance in the industry for application flexibility
- Proven reliability and durability with the lowest owning and operating costs
- Factory-installed thermostats

#### Emissions

Meets U.S. EPA Spark Ignited Stationary NSPS Emissions for 2010 with the use of an oxidation catalyst

#### Lean Burn Engine Technology

Lean-burn engines operate with large amounts of excess air. The excess air absorbs heat during combustion reducing the combustion temperature and pressure, greatly reducing levels of NOx. Leanburn design also provides longer component life and excellent fuel consumption.

#### **Ease of Operation**

Side covers on block allow for inspection of internal components

#### **Advanced Digital Engine Management**

ADEM A4 engine management system integrates speed control, air/fuel ratio control, and ignition/detonation controls into a complete engine management system. ADEM A4 has improved: user interface, display system, shutdown controls, and system diagnostics.

#### **Full Range of Attachments**

Large variety of factory-installed attachments reduces packaging time.

#### Testing

Every engine is full-load tested to ensure proper engine performance.

#### Cat<sup>®</sup> Engine Specifications In-Line 6, 4-Stroke-Cycle

**Bore** 300 mm (11.8 in)

**Stroke** 300 mm (11.8 in)

Displacement 127.2 L (7762 cu. in)

Aspiration Turbocharged-Aftercooled

Digital Engine Management Governor and Protection Electronic (ADEM™ A4)

**Combustion** Low Emission (Lean Burn)

#### **Cooling System Capacity**

Total	420 L (111	Gal)
JW	340 L (90	Gal
SCAC	80 L (21	Gal)

Lube Oil System (refill) 708 L (187 gal)

**Oil Change Interval** 5000 hours

Rotation (from flywheel end) Counterclockwise

Flywheel Teeth 255

#### Gas Engine Rating Pro (GERP)

GERP is a PC-based program designed to provide site performance capabilities for Cat natural gas engines for the gas compression industry. GERP provides engine data for your site's altitude, ambient temperature, fuel, engine coolant heat rejection, performance data, installation drawings, spec sheets, and pump curves.

#### **Product Support Offered Through Global Cat Dealer Network**

- More than 2,200 dealer outlets
- Cat factory-trained dealer technicians service every aspect of your Oil & Gas Engine
- Caterpillar parts and labor warranty
- Preventive maintenance agreements available for repair-beforefailure options
- S•0•S program matches your oil and coolant samples against Caterpillar set standards to determine:
  - Internal engine component condition
  - Presence of unwanted fluids
  - Presence of combustion by-products
  - Site-specific oil change interval

#### **Over 80 Years of Engine Manufacturing Experience**

Over 60 years of natural gas engine production. Ownership of these manufacturing processes enables Caterpillar to produce high quality, dependable products.

- Cast engine blocks, heads, cylinder liners, and flywheel housings
- Machine critical components
- Assemble complete engine

#### Web Site

For all your Oil & Gas power requirements, visit www.cat.com



#### Air Inlet System

- Air cleaner standard duty
- Inlet air adapter

#### **Control System**

- ADEM A4 control system provides electronic governing integrated with air/fuel ratio control and individual cylinder ignition timing control
- Electrical system and instrumentation certified for Class I, Division 2, Group D hazardous location. Includes entire ADEM A4 system and optional control panel

#### **Cooling System**

- Compressor oil cooler connections
- Jacket water pump
- Jacket water thermostats and housing
- Aftercooler/oil cooler pump
- Aftercooler/oil cooler thermostats and housing
- Two-stage aftercooler
- Jacket water heater connections
- Standard ANSI connections

#### **Exhaust System**

- Dry exhaust manifolds
- Single vertical outlet adapter
- Form fitted soft wrap insulation

#### **Flywheels & Flywheel Housings**

SAE standard rotation

## **OPTIONAL EQUIPMENT**

#### **Air Inlet System**

· Heavy-duty air cleaner with precleaners

#### **Charging System**

35 Amp & 65 Amp charging alternators - CSA Approved

#### **Exhaust System**

- Flexible bellows adapters
- Exhaust expander
- Weld flanges

#### **Fuel System**

- Fuel filter
- Gas pressure regulator
- Flexible connection

#### Instrumentation

- LCD display panel
- Color HMI display
- Remote data monitoring and speed control
- Compatible with Cat Electronic Technician (ET) and Data View
- Modbus and Ethernet capable

#### **Fuel System**

Gas admission valves — electronically controlled fuel supply pressure

#### **Ignition System**

• A4 control system — senses individual cylinder detonation and controls individual cylinder timing

#### Lube System

- Crankcase breather —top mounted
- Oil cooler
- Oil filter
- Oil pan drain valve front and rear

#### **Mounting System**

• Engine mounting feet (four total)

#### **Protection System**

- Electronic shutoff system with purge cycle
- Crankcase explosion relief valves
- Gas shutoff valve

#### **Starting System**

• Air starting system

#### General

- Paint, Caterpillar yellow
- Single vibration damper with guard

#### Lube System

- Air or electric motor-driven prelube
- Duplex oil filter
- RH service
- Lube oil makeup system

#### **Mounting System**

- Mounting plates (set of four)
- Extra mounting feet (set of two)
- Extra mounting plates (set of two)

#### **Power Take-offs**

Front stub shafts

#### **Starting System**

Air pressure reducing valve

#### General

- Engine barring device
- Damper guard

### **BUILT FOR IT.**



## G3606 with ADEM A4 Gas Engine

Performance Number		EM0555-07	EM0556-06	EM0557-06
Rating	°C (°F)	54 (130)	43 (110)	32 (90)
Engine Power	bkW (bhp)	1398 ( <mark>1875</mark> )	1454 (1950)	1499 (2010)
Engine Speed	rpm	1000	1000	1000
Max Altitude @ Rated Torque and 38°C (100°F)	m (ft)	2519.3 (8274)	2358 (7744)	2198 (7219)
Speed Turndown @ Max Altitude, Rated Torque, and 38°C (100°F)	%	25	25	25
Aftercooler Temperature				
Stage 1 (JW)	°C (°F)	88 (190)	88 (190)	88 (190)
Stage 2 (SCAC)	°C (°F)	54 (130)	43 (110)	32 (90)
Emissions (NTE)*				
NOx	g/bkW-hr (g/bhp-hr)	0.67 (0.5)	0.67 (0.5)	0.67 (0.5)
СО	g/bkW-hr (g/bhp-hr)	2.95 (2.2)	2.95 (2.2)	2.95 (2.2)
CO <sub>2</sub>	g/bkW-hr (g/bhp-hr)	582 (434)	579 (432)	577 (430)
VOC**	g/bkW-hr (g/bhp-hr)	0.38 (0.29)	0.36 (0.27)	0.34 (0.26)
Fuel Consumption ***	MJ/bkW-hr (Btu/bhp- hr)	9.4 <mark>(6649)</mark>	9.39 (6638)	9.38 (6629)
Heat Balance				
Heat Rejection to Jacket Water	bkW (Btu/min)	387 (21987)	395 (22436)	401 (22785)
Heat Rejection to Oil Cooler	bkW (Btu/min)	206 (11709)	214 (12154)	220 (12514)
Heat Rejection to Aftercooler				
Stage 1 (JW)	bkW (Btu/min)	228 (12970)	239 (13591)	248 (14097)
Stage 2 (SCAC)	bkW (Btu/min)	115 (6550)	148 (8423)	176 (9997)
Heat Rejection to Exhaust LHV To 25°C (77°F)	bkW (Btu/min)	1259 (71578)	1288 (73268)	1312 (74619)
Heat Rejection to Atmosphere	bkW (Btu/min)	98 (5575)	96 (5465)	93 (5305)
Exhaust System				
Exhaust Gas Flow Rate	m <sup>3</sup> /min (scfm)	334.76 (11822)	343.28 (12123)	350.11 (12364)
Exhaust Stack Temperature	°C (°F)	446 (835)	446 (835)	446 (836)
Intake System				
Air Inlet Flow Rate	m <sup>3</sup> /min (scfm)	129.86 (4586)	133.06 (4699)	135.61 (4789)
Gas Pressure	kPag (psig)	400 - 485 (58 - 70)	400 - 485 (58 - 70)	400 - 485 (58 - 70)

All technical data is based on 100% load and speed

\* listed as not to exceed

\*\* Volatile organic compounds as defined in U.S. EPA 40 CFR 60, subpart JJJJ

\*\*\* ISO 3046/1



### **TECHNICAL DATA G3606 with ADEM A4 Gas Engine**





Note: General confi guration not to be used for installation

Dimensions		
Length	4356.8 mm	171.53 in
Width	2188.7 mm	86.17 in
Height	2922.0 mm	115.04 in
Weight	16,670 kg	36,883 lb

#### **Rating Definitions and Conditions**

Engine performance is obtained in accordance with SAE J1995, ISO3046/1, BS5514/1, and DIN6271/1 standards.

Conditions: Power for gas engines is based on fuel having an LHV of 33.74 kJ/L (905 Btu/cu ft) at 101 kPa (29.91 in Hg) and 15°C (59°F). Fuel rate is based on a cubic meter at 100 kPa (29.61 in Hg) and 15.6°C (60.1°F). Air flow is based on a cubic foot at 100 kPa (29.61 in Hg) and 25°C (77°F). Exhaust flow is based on a cubic foot at 100 kPa (29.61 in Hg) and stack temperature.

To find your nearest dealer, please visit: www.cat.com

Subject to change without notice. LEHW0234-01

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### **BUILT FOR IT**



### ICE CATALYST SIZING PROGRAM

rev 2.1.3

Report Date: 5/18/2023



	Customer Sales Perso Project Engine Nar	Enlink Mic n KW Horned Fr me Waukesha	dstream rog CS a VHP - P9394GSI S5 2500 BHI			Housing Elemen Contact 1200 RPM	9 t 36 Mi	ike L	3-Way ₋uckett						
	Engine Power		2500.0	BHP	ACF	М	1042	3.0	CU. FT/MIN		Exhaust 02		0.2	%	
	Exhaust Mass	Flow	15368.0	LBS/H	R ACF	Н	6253	380	CU.	FT/HR	Exhaust CO2	Exhaust CO2		%	
	Process Tempe	erature	1066.0	F	SCF	М	355	7.3	CU. I	FT/MIN	Exhaust H2O		18.7	%	
	Exhaust Pressu	lre	14.5	PSI	SCF	Н	2134	435	CU.	FT/HR	Exhaust N2		71.2	%	
	Exhaust Densit	y	0.0246	LBS/FT	^3 Std	Temp	6	8.0		F	Max Pressure D	rop	27.0	in wc	
	Molecular Weig	ght	27.75	AMU	Std	Pressure	14.69	959	I	PSI	Propane in Fuel		0.00	%	
	Type Geometry Diameter		Stoichiome Round 36.500in	tric	ic Layers Modules Guard B		s/Layer Bed		2 1 No		Cell Count Depth		300cpsi 3.500in		
	Open	Area	7.266	ft^2		Part Volum	ie		2.119	ft^3	Part We	ight	118	lbs	
	Linear	Velocity	1434	ft/min		Total Volun	ne		4.239 ft^3		Total We	eight	235	lbs	
	Pressu	re Drop	3.1	in wc		Space Veloc	city	y 50354 GHSV							
						Inlet En	nissions	5							
			g/bhp	-hr	lb/hr	p/hr tons/yea		r ppmv		ppmvd	рр	mvd%C	2		
	NC	Эх	11.9	7	65.97	28	9.16	2588.95		.95	3183.18	3183.18		911.69	
	C	0	6.06		33.40	3.40 146.39			2152.77		2646.90		/58.09		
	H2		0.05	0.05 0		0.28 1.21			16.57		20.37		5.83		
	VUC+	HZCU	0.60	<b>)</b>	3.31	Target C	4.49 maiocian		140.	00	172.95		49.53		
		min %DDE	g/bbp	br	lb/br	top	rhission shioar	15	nnr		nnmvd	20	mvd%C	n	
	ΝΟχ	97 49	0.30	)	1 65	7	25		64 8	39	79.78	ρp	22.85	2	
	CO	93.40	0.40	)	2.20	g	.66		142.	10	174.71		50.04		
	H2CO	20.00	0.04	ļ	0.22	C	.97		13.2	25	16.30		4.67		
	VOC+H2CO	58.33	0.25	5	1.38	1.38 6.			60.6	54	74.55		21.35		
					Ε	missions v	vith Cat	aly	st						
Ī		%DRE	g/bhp	-hr	lb/hr	tons	s/year		ppr	nv	ppmvd	рр	mvd%C	2	
	NOx	97.49	<0.30	0	<1.65	<7	7.25		<64.	89	<79.78		<22.85		
	CO	93.40	<0.40	0	<2.20	<9	9.66		<142	.10	<174.71		<50.04		
	H2CO	20.00	< 0.04	4	<0.22	<(	).97		<13.	25	<16.30		<4.67		
	VOC+H2CO	58.33	< 0.2	5	<1.38	<6	5.04		<60.64		<74.55	<21.35			

Safety Value: 2 VOC Molecular Weight: 44.1 02 Reference Value: 15 Uptime (TPY): 100% (8760 hours)



### VHP Series Five P9394GSI S5

With ESM2 and emPact Emission Control System

CHILL IN

1,875 - 2,500 hp (1,400 - 1,865 kWb)

#### Technical Data

Cylinders	V16
Piston displacement	9,388 cu. in. (154 L)
Compression ratio	9.7:1
Bore & stroke	9.375" x 8.5" (238 x 216)
Jacket water system capacity	148 gal. (560 L)
Lube oil capacity	239 gal. (904 L)
Starting system	Single air/gas starter: 90-150 psi Single air/gas starter: 50-90 psi Dual air/gas starters: 90-150 psi Dual air/gas starters: 50-90 psi 2 electric starters, 24V each

#### Dimensions I x w x h inch (mm)

170 (4,318) x 78 (1,981) x 113 (2,870)

#### Weights Ib (kg)

34,000 (15,422)



The Series Five family of Waukesha\* VHP\* engines gets more powerful with the addition of the 2500 hp P9394GSI S5. The P9394GSI S5 has the same features and benefits as the 1900 hp L7044GSI S5 and 1500 hp L7042GSI S5, creating a family of engines with common controls, operation, and service parts.

Series Five rich-burn engines combine the most advanced technology available with the history and experience of the VHP platform, resulting in a 16-cylinder engine with more power, better fuel flexibility, lower fuel consumption and lifecycle costs, and longer service intervals. Although Series Five engines are capable of higher power levels than previous versions, the stresses on the components have not increased. This is made possible by enhanced rich-burn combustion through the Miller Cycle, an improved cylinder head design that reduces

temperatures in key regions, and an optimized piston design. The Miller Cycle moves work from the

piston to the turbocharger, reducing combustion and exhaust temperatures and making Series Five engines the most fuel efficient VHP engines ever.

The improved cylinder head design reduces key internal temperatures by

up to 40%, increasing reliability and extending the life of the head.

The Series Five piston design has been optimized to reduce unburned hydrocarbons, which improves emissions and fuel consumption while lowering the temperature of the piston itself, improving fuel flexibility even at a higher power rating.

Improvements to the ignition system allow for 4,000-hour spark plug intervals with low-cost, non-precious metal plugs. Matching 4,000 oil change intervals reduce operating costs and trips to site. Series Five engines come standard with ESM\*2, Waukesha's next-generation engine controller. ESM2 uses a 12" full color customer interface panel, allowing users to see all engine parameters, trend data, view manuals, and walk through troubleshooting steps, eliminating the need for a laptop computer.

Waukesha's emPact Emission Control System is the option of choice for reducing emissions. emPact optimizes the interaction between the Series Five engine, AFR2 air/fuel ratio control, and the Waukesha-supplied 3-way (NSCR) catalyst to maintain emissions compliance even as engine speed, load, fuel, and environmental conditions change.





### **Performance Data**

Intercoo	ler Water Temperature 130°F (54°C)	1200 RPM	1000 RPM
	Power bhp (kWb)	2,500 (1,864)	2,085 (1,555)
	BSFC (LHV) Btu/bhp-hr (kJ/kWh)	<mark>6,974</mark> (9,867)	6,982 (9,878)
	Fuel Consumption Btu/hr x 1000 (kW)	17,435 (5,110)	14,557 (4,267)
s r	NOx g/bhp-hr (mg/Nm <sup>3</sup> @ 5% $O_2$ )	12.02 (5,155)	11.52 (4,934)
e-0	CO g/bhp-hr (mg/Nm <sup>3</sup> @ 5% O <sub>2</sub> )	6.08 (2,606)	6.52 (2,791)
nigr	NMHC g/bhp-hr (mg/Nm <sup>3</sup> @ 5% $0_2$ )	0.17 (74)	0.15 (63)
	THC g/bhp-hr (mg/Nm <sup>3</sup> @ 5% O <sub>2</sub> )	0.50 (214)	0.51 (219)
	Heat to Jacket Water Btu/hr x 1000 (kW)	4,810 (1,410)	4,222 (1,237)
00	Heat to Lube Oil Btu/hr x 1000 (kW)	683 (200)	493 (145)
Heat alan	Heat to Intercooler Btu/hr x 1000 (kW)	670 (196)	455 (133)
ă	Heat to Radiation Btu/hr x 1000 (kW)	627 (184)	595 (174)
	Total Exhaust Heat Btu/hr x 1000 (kW)	4,635 (1,358)	3,776 (1,107)
at st	Induction Air Flow scfm (Nm³/hr)	3,267 (4,921)	2,726 (4,106)
ntak: chau yster	Exhaust Flow Ib/hr (kg/hr)	15,190 (6,890)	12,676 (5,750)
μ Ω Ω	Exhaust Temperature °F (°C)	1,093 (589)	1,067 (575)

All data according to full load and subject to technical development and modification.

emPact catalyst-out emissions valid from 100% - 75% load and 1200 rpm to 900 rpm and assume proper engine/catalyst maintenance and manual adjustment as necessary.

Consult your local Waukesha representative for system application assistance. The manufacturer reserves the right to change or modify without notice, the design or equipment specifications as herein set forth without incurring any obligation either with respect to equipment previously sold or in the process of construction except where otherwise specifically guaranteed by the manufacturer.

INNIO\* is a leading solutions provider of gas engines, power equipment, a digital platform and related services for power generation and gas compression at or near the point of use. With our Jenbacher\* and Waukesha\* product brands, INNIO pushes beyond the possible and looks boldly toward tomorrow. Our diverse portfolio of reliable, economical and sustainable industrial gas engines generates 200 kW to 10 MW of power for numerous industries globally. We can provide life cycle support to the more than 48,000 delivered gas engines worldwide. And, backed by our service network in more than 100 countries, INNIO connects with you locally for rapid response to your service needs. Headquartered in Jenbach, Austria, the business also has primary operations in Welland, Ontario, Canada, and Waukesha, Wisconsin, US.

Find your local support online: www.innio.com/en/company/providers IWK-119055-EN

\*Indicates a trademark

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### ICE CATALYST SIZING PROGRAM

rev 2.1.3

Report Date: 5/8/2023



CustomerEnlink MidstreamHousingSales PersonKWElementProjectG3608A4ContactEngine NameCaterpillar G3608 G3608 - 2500bhp - 1000RPM							C-714 Ice Gr	0-2 een					
Engine Power		2500.0	BHP ACFM			16164	.0	CU. FT/MIN		Exhaust 02		10.4	%
Exhaust Mass	Flow	29271.0	LBS/HR	ACFH		9698	40	CU. F	T/HR	Exhaust CO2		6.5	%
Process Temp	erature	812.0	F	SCFM		6618	.4	CU. F	T/MIN	Exhaust H2O		10.6	%
Exhaust Press	ure	14.5	PSI	SCFH		3971	03	CU. F	T/HR	Exhaust N2		72.6	%
Exhaust Densi	ty	0.0302	LBS/FT^3	Std Te	mp	68	.0		F	Max Pressure	Drop	12.0	in wc
Molecular Wei	ght	28.41	AMU	Std Pr	essure	14.69	59	Ρ	SI	Propane in Fue	el .	2.93	%
ACS Part N OEM Part I Type Geometry X Y	ame Name	RN15.440X MCC-7140- NG/Diesel Rectangula 15.440in 24.750in	24.750X3.50 2 (Lean) r	0-300	Layers Modules Guard B	s/Layer sed	1 2 1	1 4 No		Cell Cour Depth	nt	31 3.	00cpsi 500in
Oper	n Area	9.526	ft^2 Part Volume		e	0.69	0.695 ft^3		Part Weight		46	lbs	
Linear	Velocity	1697	ft/min		Total Volum	ne	2.77	2.779 ft^3		Total W	/eight	183	lbs
Pressu	ure Drop	1.6	in wc		Space Veloc	ity	1429	918	GHSV				
					Inlet En	nissions							
		g/bhp-hr		lb/hr tons		;/year ppmv		١V	ppmvd	рр	mvd%C	)2	
N	Ox	0.30	0.30		1.67 7.		.31 35.15		5	39.30		24.93	
C	0	2.25		12.50		4.79	433.04		)4	484.13		307.14	
H2	200	0.12		0.67		.92	21.54		4	24.08		15.28	
VOC+	H2CO	0.42		2.33	1(	).23		58.2	1	65.08		41.29	
					Target E	mission	5						
	min %DRE	g/bhp	-hr	b/hr	tons	s/year		ppm	۱V	ppmvd	рр	mvd%C	2
NOx	0.00	<0.30	)	<1.67	<7	7.31		<35.1	5	<39.30		<24.93	
CO	82.22	<0.40	)	<2.22	<0	9.74		<76.9	9	<86.07		<54.60	
H2CO	66.67	< 0.04	1	<0.22	<(	).97		<7.1	8	<8.03		<5.09	
VOC+H2CO	28.57	<0.30	)	<1.67	<7	7.31		<38.9	96	<43.56		<27.64	
				Em	issions w	ith Cata	alyst						
	%DRE	g/bhp	-hr	b/hr	tons	s/year		ppm	١V	ppmvd	рр	mvd%C	)2
NOx	0.00	< 0.3		<1.67	<7	7.31		<35.1	5	<39.30		<24.93	
CO	82.22	<0.4	)	<2.22	<0	9.74		<76.9	9	<86.07		<54.60	
H2CO	66.67	< 0.04	4	<0.22	<(	).97		<7.1	8	<8.03		< 5.09	
VOC+H2CO	28.57	< 0.30	)	<1.67	<7	7.31		<38.9	16	<43.56		<27.64	

Safety Value: 2 VOC Molecular Weight: 44.1 02 Reference Value: 15 Uptime (TPY): 100% (8760 hours)

### G3608

#### GAS ENGINE SITE SPECIFIC TECHNICAL DATA Cat 3608 A4 2,500-hp



GAS COMPRESSION APPLICATION ENGINE SPEED (rpm): COMPRESSION RATIO: AFTERCOOLER TYPE: AFTERCOOLER - STAGE 2 INLET (°F): AFTERCOOLER - STAGE 1 INLET (°F): JACKET WATER OUTLET (°F): ASPIRATION: COOLING SYSTEM: CONTROL SYSTEM: EXHAUST MANIFOLD: COMBUSTION: NOX EMISSION LEVEL (g/bhp-hr NOX): SET POINT TIMING:	1000 7.6 SCAC 130 174 190 TA JW+1AC, OC+2AC ADEM4 DRY LOW EMISSION 0.3 18	RATING STRATEGY: RATING LEVEL: FUEL SYSTEM: <b>SITE CONDITIONS:</b> FUEL: FUEL PRESSURE RANGE(psig): (See FUEL METHANE NUMBER: FUEL LHV (Btu/scf): ALTITUDE(ft): INLET AIR TEMPERATURE(°F): STANDARD RATED POWER:	e note 1)	STANDARD CONTINUOUS GAV WITH AIR FUEL RATIO CONTROL Nat Gas 58.0-70.3 84.7 905 500 77 2500 bhp@1000rpm
			MAXIMUM	SILE RATING AT MAXIMUM

				RATING	INLET A	IR TEMPE	RATURE
RATING		NOTES	LOAD	100%	100%	75%	50%
ENGINE POWER	(WITHOUT FAN)	(2)	bhp	2500	2500	1875	1250
INLET AIR TEMPERATURE			°F	77	77	77	77
ENGINE DATA							
FUEL CONSUMPTION (LHV)		(3)	Btu/bhp-hr	6848	6848	7075	7574
FUEL CONSUMPTION (HHV)		(3)	Btu/bhp-hr	7596	7596	7848	8401
AIR FLOW (@inlet air temp, 14.7 psia)	(WET)	(4)(5)	ft3/min	6252	6252	4738	3221
AIR FLOW	(WET)	(4)(5)	lb/hr	27723	27723	21010	14283
FUEL FLOW (60°F, 14.7 psia)			scfm	315	315	244	174
INLET MANIFOLD PRESSURE		(6)	in Hg(abs)	104.4	104.4	78.9	55.1
EXHAUST TEMPERATURE - ENGINE OUTLET		(7)	°F	833	833	876	941
EXHAUST GAS FLOW (@engine outlet temp, 14.5 psia)	(WET)	(5)(8)	ft3/min	16088	16088	12616	9016
EXHAUST GAS MASS FLOW	(WET)	(5)(8)	lb/hr	28584	28584	21676	14760
EMISSIONS DATA - ENGINE OUT							
		(9)(10)	a/bhp-hr	0.30	0.30	0.30	0.30
		(9)(10)	a/bhp-hr	2.50	2.50	2.50	2.50
THC (mol. wt. of 15.84)		(9)(10)	a/bhp-hr	4.42	4.42	4.69	4.76
NMHC (mol. wt. of 15.84)		(9)(10)	a/bhp-hr	0.41	0.41	0.43	0.44
NMNEHC (VOCs) (mol. wt. of 15.84)		(9)(10)(11)	g/bhp-hr	0.28	0.28	0.29	0.30
HCHO (Formaldehyde)		(9)(10)	g/bhp-hr	0.16	0.16	0.17	0.20
CO2		(9)(10)	g/bhp-hr	426	426	442	471
EXHAUST OXYGEN		(9)(12)	% DRY	11.3	11.3	11.1	10.7
HEAT REJECTION							
HEAT REJ. TO JACKET WATER (JW)		(13)	Btu/min	27698	27698	23042	18866
HEAT REJ. TO ATMOSPHERE		(13)	Btu/min	10994	10994	10961	10310
HEAT REJ. TO LUBE OIL (OC)		(13)	Btu/min	12553	12553	11937	10886
HEAT REJ. TO A/C - STAGE 1 (1AC)		(13)(14)	Btu/min	19561	19561	9599	2375
HEAT REJ. TO A/C - STAGE 2 (2AC)		(13)(14)	Btu/min	7683	7683	4956	2595
COOLING SYSTEM SIZING CRITERIA							
TOTAL JACKET WATER CIRCUIT (JW+1AC)		(14)(15)	Btu/min	51006	]		
TOTAL STAGE 2 AFTERCOOLER CIRCUIT (OC+2AC)		(14)(15)	Btu/min	23131			
A cooling system safety factor of 0% has been added to the cooling	system sizing criteria.	,	•	•	1		

#### CONDITIONS AND DEFINITIONS

Engine rating obtained and presented in accordance with ISO 3046/1, adjusted for fuel, site altitude and site inlet air temperature. 100% rating at maximum inlet air temperature is the maximum engine capability for the specified fuel at site altitude and maximum site inlet air temperature. Maximum rating is the maximum capability at the specified fuel at site altitude and reduced inlet air temperature. Refer to product O&M manual for details on additional lower load capability. No overload permitted at rating shown.

For notes information consult page three.

#### GAS ENGINE SITE SPECIFIC TECHNICAL DATA Cat 3608 A4 2,500-hp



#### Note:

At site conditions of 500 ft and 77°F inlet air temp., constant torque can be maintained down to 750 rpm. The minimum speed for loading at these conditions is 750 rpm.

**CATERPILLAR®** 

### G3608

#### GAS ENGINE SITE SPECIFIC TECHNICAL DATA Cat 3608 A4 2,500-hp



#### NOTES:

1. Fuel pressure range specified is to the engine gas shutoff valve (GSOV). Additional fuel train components should be considered in pressure and flow calculations.

2. Engine rating is with two engine driven water pumps. Tolerance is  $\pm$  3% of full load.

3. Fuel consumption tolerance is ± 2.5% of full load data.

4. Air flow value is on a 'wet' basis. Flow is a nominal value with a tolerance of  $\pm 5$  %.

5. Inlet and Exhaust Restrictions must not exceed A&I limits based on full load flow rates from the standard technical data sheet.

6. Inlet manifold pressure is a nominal value with a tolerance of  $\pm$  5 %.

7. Exhaust temperature is a nominal value with a tolerance of (+)63°F, (-)54°F.

8. Exhaust flow value is on a "wet" basis. Flow is a nominal value with a tolerance of ± 6 %.

9. Emissions data is at engine exhaust flange prior to any after treatment.

10. Values listed are higher than nominal levels to allow for instrumentation, measurement, and engine-to-engine variations. They indicate the maximum values expected under steady state conditions. Fuel methane number cannot vary more than ± 3. THC, NMHC, and NMNEHC do not include aldehydes. An oxidation catalyst may be required to meet Federal, State or local CO or HC requirements.

11. VOCs - Volatile organic compounds as defined in US EPA 40 CFR 60, subpart JJJJ

12. Exhaust Oxygen level is the result of adjusting the engine to operate at the specified NOx level. Tolerance is  $\pm 0.5$ .

13. Heat rejection values are nominal. Tolerances, based on treated water, are ± 10% for jacket water circuit, ± 50% for radiation, ± 20% for lube oil circuit, and ± 5% for aftercooler circuit.

14. Aftercooler heat rejection includes an aftercooler heat rejection factor for the site elevation and inlet air temperature specified. Aftercooler heat rejection values at part load are for reference only. Do not use part load data for heat exchanger sizing.

15. Cooling system sizing criteria are maximum circuit heat rejection for the site, with applied tolerances.

#### GAS ENGINE SITE SPECIFIC TECHNICAL DATA Cat 3608 A4 2,500-hp



Constituent	Abbrev	Mole %	Norm		
Water Vapor	H2O	0.0000	0.0000	Fuel Makeup:	Nat Ga
Methane	CH4	92.2700	92.2700	Unit of Measure:	Englis
Ethane	C2H6	2.5000	2.5000		
Propane	C3H8	0.5000	0.5000	Calculated Fuel Properties	
Isobutane	iso-C4H10	0.0000	0.0000	Caterpillar Methane Number:	84.
Norbutane	nor-C4H10	0.2000	0.2000		
Isopentane	iso-C5H12	0.0000	0.0000	Lower Heating Value (Btu/scf):	905
Norpentane	nor-C5H12	0.1000	0.1000	Higher Heating Value (Btu/scf):	1004
Hexane	C6H14	0.0500	0.0500	WOBBE Index (Btu/scf):	1168
Heptane	C7H16	0.0000	0.0000		
Nitrogen	N2	3.4800	3.4800	THC: Free Inert Ratio:	21.83
Carbon Dioxide	CO2	0.9000	0.9000	Total % Inerts (% N2, CO2, He):	4.38%
Hydrogen Sulfide	H2S	0.0000	0.0000	RPC (%) (To 905 Btu/scf Fuel):	100%
Carbon Monoxide	CO	0.0000	0.0000		
Hydrogen	H2	0.0000	0.0000	Compressibility Factor:	0.998
Oxygen	O2	0.0000	0.0000	Stoich A/F Ratio (Vol/Vol):	9.45
Helium	HE	0.0000	0.0000	Stoich A/F Ratio (Mass/Mass):	15.75
Neopentane	neo-C5H12	0.0000	0.0000	Specific Gravity (Relative to Air):	0.600
Octane	C8H18	0.0000	0.0000		
Nonane	C9H20	0.0000	0.0000	Fuel Specific Heat Ratio (K):	1.313
Ethylene	C2H4	0.0000	0.0000		1.010
Propylene	C3H6	0.0000	0.0000		
TOTAL (Volume %)		100.0000	100.0000		

#### CONDITIONS AND DEFINITIONS

Caterpillar Methane Number represents the knock resistance of a gaseous fuel. It should be used with the Caterpillar Fuel Usage Guide for the engine and rating to determine the rating for the fuel specified. A Fuel Usage Guide for each rating is included on page 2 of its standard technical data sheet.

RPC always applies to naturally aspirated (NA) engines, and turbocharged (TA or LE) engines only when they are derated for altitude and ambient site conditions.

Project specific technical data sheets generated by the Caterpillar Gas Engine Rating Pro program take the Caterpillar Methane Number and RPC into account when generating a site rating.

Fuel properties for Btu/scf calculations are at 60F and 14.696 psia.

Caterpillar shall have no liability in law or equity, for damages, consequently or otherwise, arising from use of program and related material or any part thereof.

#### FUEL LIQUIDS

Field gases, well head gases, and associated gases typically contain liquid water and heavy hydrocarbons entrained in the gas. To prevent detonation and severe damage to the engine, hydrocarbon liquids must not be allowed to enter the engine fuel system. To remove liquids, a liquid separator and coalescing filter are recommended, with an automatic drain and collection tank to prevent contamination of the ground in accordance with local codes and standards.

To avoid water condensation in the engine or fuel lines, limit the relative humidity of water in the fuel to 80% at the minimum fuel operating temperature.



#### ICE Catalyst Sizing Program

ENGINE INPUT (Manufacturer, Model, Type) - Caterpillar G3612 A4 Caterpillar G3612 A4 3750 BHP @ 1000 RPM - EXPERT MODE

	lbs/hr	"scfm"	"scfh"	"acfm"	"acfh"	Estimate	ed Exhaust Gas Con	nposition
lb/hr(Estimated):	44,538	9,728	583,700	23797	1,427,820	N2	74.5	vol%
Brake Horse Power:	3750					02	10	vol%
			Maximum Pres	essure Drop (in)		H2O	10	vol%
Molecular weight:	28.50		0.031	Exhaust De	nsity (lbs/ft3)	CO2	6	vol%
			mol% propan	e in fuel gas:	<5			
Inlet Temperature		Enter permitted gra	ims per brake horse	power hour (g/bhp	-hr)			
Process Temperature (F):	812	NOx**		CO**		VOC(NMNE)**		H2CO**
		0.3		0.3		0.25		0.03
Catalyst Type		Catalyst Module De	etails					
		Module	Shape		Module/Layer	6	Layers	1
CO/DOC Catalyst		Squ	iare				cpsi	300
		Guard Bed - No		X&Y (inch)	15.44	24.75	Depth	3.5
				Part Nu	umber MCC-7140-2			
Open area for gas flow (ft2):	14.29							
Linear Velocity(ft/min):	1,665	Calculated Sp	bace Velocity:	140,050		Safety Value	2	
Foil thickness (inches):	0.002							
Pressure Drop		Inlet Pollutants					10/ 0.01	
		NO	g/bnp-nr	Ib/hr	tons/year	ppmv	ppmvd%O2^	
		NOX	0.30	2.48	10.86	35.01	21.06	
200	0.77	00	2.95	24.39	106.82	00.00	340.14	
300	2.11	000	0.73	0.04	20.43	00.00	00.45	
		H2CO	0.19	1.57	0.00	34.00	20.45	
Target Conversions		Required Output P	ollutants					
		Required Output I	g/bhp-hr	lb/hr	tons/vear	vmqq	ppmyd%O2*	
NOx	0.0%	NOx	0.3	2.48	10.86	35.01	21.06	
CO	89.8%	CO	0.3	2.48	10.86	57.51	34.59	
VOC(NMNE)	65.8%	VOC	0.25	2.07	9.05	30.43	18.30	
H2CO	84.2%	H2CO	0.03	0.25	1.09	5.37	3.23	
Conversions Catalyst Design		Output Pollutants w	vith Catalyst Sizing					
			g/bhp-hr	lb/hr	tons/year	ppmv	ppmvd%O2*	
NOx	0.0%	NOx	0.3	2.48	10.86	35.01	21.06	
со	89.8%	со	0.3	2.48	10.86	57.51	34.59	
VOC(NMNE)	65.8%	VOC	0.25	2.07	9.05	30.43	18.30	
H2CO	84.2%	H2CO	0.03	0.25	1.09	5.37	3.23	

Notes:

Customer: Enlink Midstream Sales Person: KW

Housing:

Date: 4/10/2019 Element: MCC-7140-2 

 Project:
 G3612A4

 Contact:
 Travis Burke

 Description:
 Element, Catalyst, Oxidation, 15.44 x 24.75

### G3612

#### GAS ENGINE SITE SPECIFIC TECHNICAL DATA 3,750-hp Cat 3612 A4



GAS COMPRESSION APPLICATION			
ENGINE SPEED (rpm):	1000	RATING STRATEGY:	STANDARD
COMPRESSION RATIO:	7.6	RATING LEVEL:	CONTINUOUS
AFTERCOOLER TYPE:	SCAC	FUEL SYSTEM:	GAV
AFTERCOOLER - STAGE 2 INLET (°F):	130 174	SITE CONDITIONS:	WITH AIR FUEL RATIO CONTROL
JACKET WATER OUTLET (°E)	190	FUEL:	Nat Gas
ASPIRATION.	TA	FUEL PRESSURE RANGE(psig): (See note 1)	58.0-70.3
COOLING SYSTEM	JW+1AC OC+2AC	FUEL METHANE NUMBER:	84.7
CONTROL SYSTEM:	ADEM4	FUEL LHV (Btu/scf):	905
EXHAUST MANIFOLD:	DRY	ALTITUDE(ft):	500
COMBUSTION:	LOW EMISSION	INLET AIR TEMPERATURE(°F):	77
NOx EMISSION LEVEL (g/bhp-hr NOx):	0.3	STANDARD RATED POWER:	3750 bhp@1000rpm
SET POINT TIMING:	18		
		MAXIMUN	1 SITE RATING AT MAXIMUM

				RATING	INLET A	IR TEMPE	RATURE
RATING		NOTES	LOAD	100%	100%	75%	50%
ENGINE POWER	(WITHOUT FAN)	(2)	bhp	3750	3750	2813	1875
INLET AIR TEMPERATURE			°F	77	77	77	77
ENGINE DATA							
FUEL CONSUMPTION (LHV)		(3)	Btu/bhp-hr	6800	6800	7003	7465
FUEL CONSUMPTION (HHV)		(3)	Btu/bhp-hr	7543	7543	7768	8280
AIR FLOW (@inlet air temp, 14.7 psia)	(WET)	(4)(5)	ft3/min	9251	9251	7013	4802
AIR FLOW	(WET)	(4)(5)	lb/hr	41017	41017	31095	21293
FUEL FLOW (60°F, 14.7 psia)			scfm	470	470	363	258
INLET MANIFOLD PRESSURE		(6)	in Hg(abs)	99.2	99.2	75.7	53.1
EXHAUST TEMPERATURE - ENGINE OUTLET		(7)	°F	840	840	894	957
EXHAUST GAS FLOW (@engine outlet temp, 14.5 psia)	(WET)	(5)(8)	ft3/min	23936	23936	18904	13581
EXHAUST GAS MASS FLOW	(WET)	(5)(8)	lb/hr	42304	42304	32089	21999
EMISSIONS DATA - ENGINE OUT							
NOx (as NO2)		(9)(10)	g/bhp-hr	0.30	0.30	0.30	0.30
co`´		(9)(10)	g/bhp-hr	2.50	2.50	2.50	2.50
THC (mol. wt. of 15.84)		(9)(10)	g/bhp-hr	4.49	4.49	4.65	4.67
NMHC (mol. wt. of 15.84)		(9)(10)	g/bhp-hr	0.42	0.42	0.43	0.43
NMNEHC (VOCs) (mol. wt. of 15.84)		(9)(10)(11)	g/bhp-hr	0.28	0.28	0.29	0.29
HCHO (Formaldehyde)		(9)(10)	g/bhp-hr	0.19	0.19	0.19	0.21
CO2		(9)(10)	g/bhp-hr	423	423	438	468
EXHAUST OXYGEN		(9)(12)	% DRY	11.5	11.5	11.3	10.9
HEAT REJECTION							
HEAT REJ. TO JACKET WATER (JW)		(13)	Btu/min	40888	40888	32639	27887
HEAT REJ. TO ATMOSPHERE		(13)	Btu/min	17674	17674	16883	13955
HEAT REJ. TO LUBE OIL (OC)		(13)	Btu/min	18701	18701	17070	15164
HEAT REJ. TO A/C - STAGE 1 (1AC)		(13)(14)	Btu/min	30425	30425	14447	2708
HEAT REJ. TO A/C - STAGE 2 (2AC)		(13)(14)	Btu/min	7352	7352	5372	3527
COOLING SYSTEM SIZING CRITERIA							
TOTAL JACKET WATER CIRCUIT (JW+1AC)		(14)(15)	Btu/min	76923	]		
TOTAL STAGE 2 AFTERCOOLER CIRCUIT (OC+2AC)		(14)(15)	Btu/min	30160			
A cooling system safety factor of 0% has been added to the cooling	system sizing criteria.	•			]		

#### CONDITIONS AND DEFINITIONS

Engine rating obtained and presented in accordance with ISO 3046/1, adjusted for fuel, site altitude and site inlet air temperature. 100% rating at maximum inlet air temperature is the maximum engine capability for the specified fuel at site altitude and maximum site inlet air temperature. Maximum rating is the maximum capability at the specified fuel at site altitude and reduced inlet air temperature. Refer to product O&M manual for details on additional lower load capability. No overload permitted at rating shown.

For notes information consult page three.









#### Note:

At site conditions of 500 ft and 77°F inlet air temp., constant torque can be maintained down to 750 rpm. The minimum speed for loading at these conditions is 750 rpm.
# G3612

#### GAS ENGINE SITE SPECIFIC TECHNICAL DATA 3,750-hp Cat 3612 A4



#### NOTES:

1. Fuel pressure range specified is to the engine gas shutoff valve (GSOV). Additional fuel train components should be considered in pressure and flow calculations.

2. Engine rating is with two engine driven water pumps. Tolerance is  $\pm$  3% of full load.

3. Fuel consumption tolerance is ± 2.5% of full load data.

4. Air flow value is on a 'wet' basis. Flow is a nominal value with a tolerance of  $\pm$  5 %.

5. Inlet and Exhaust Restrictions must not exceed A&I limits based on full load flow rates from the standard technical data sheet.

6. Inlet manifold pressure is a nominal value with a tolerance of  $\pm$  5 %.

7. Exhaust temperature is a nominal value with a tolerance of (+)63°F, (-)54°F.

8. Exhaust flow value is on a "wet" basis. Flow is a nominal value with a tolerance of ± 6 %.

9. Emissions data is at engine exhaust flange prior to any after treatment.

10. Values listed are higher than nominal levels to allow for instrumentation, measurement, and engine-to-engine variations. They indicate the maximum values expected under steady state conditions. Fuel methane number cannot vary more than ± 3. THC, NMHC, and NMNEHC do not include aldehydes. An oxidation catalyst may be required to meet Federal, State or local CO or HC requirements.

11. VOCs - Volatile organic compounds as defined in US EPA 40 CFR 60, subpart JJJJ

12. Exhaust Oxygen level is the result of adjusting the engine to operate at the specified NOx level. Tolerance is  $\pm 0.5$ .

13. Heat rejection values are nominal. Tolerances, based on treated water, are ± 10% for jacket water circuit, ± 50% for radiation, ± 20% for lube oil circuit, and ± 5% for aftercooler circuit.

14. Aftercooler heat rejection includes an aftercooler heat rejection factor for the site elevation and inlet air temperature specified. Aftercooler heat rejection values at part load are for reference only. Do not use part load data for heat exchanger sizing.

15. Cooling system sizing criteria are maximum circuit heat rejection for the site, with applied tolerances.

#### GAS ENGINE SITE SPECIFIC TECHNICAL DATA 3,750-hp Cat 3612 A4



Constituent	Abbrev	Mole %	Norm		
Water Vapor	H2O	0.0000	0.0000	Fuel Makeup:	Nat Gas
Methane	CH4	92.2700	92.2700	Unit of Measure:	English
Ethane	C2H6	2.5000	2.5000		
Propane	C3H8	0.5000	0.5000	Calculated Fuel Properties	
Isobutane	iso-C4H10	0.0000	0.0000	Caterpillar Methane Number:	84.7
Norbutane	nor-C4H10	0.2000	0.2000		
Isopentane	iso-C5H12	0.0000	0.0000	Lower Heating Value (Btu/scf):	905
Norpentane	nor-C5H12	0.1000	0.1000	Higher Heating Value (Btu/scf):	1004
Hexane	C6H14	0.0500	0.0500	WOBBE Index (Btu/scf):	1168
Heptane	C7H16	0.0000	0.0000		
Nitrogen	N2	3.4800	3.4800	THC: Free Inert Ratio:	21.83
Carbon Dioxide	CO2	0.9000	0.9000	Total % Inerts (% N2, CO2, He):	4.38%
Hydrogen Sulfide	H2S	0.0000	0.0000	RPC (%) (To 905 Btu/scf Fuel):	100%
Carbon Monoxide	CO	0.0000	0.0000		
Hydrogen	H2	0.0000	0.0000	Compressibility Factor:	0.998
Oxygen	O2	0.0000	0.0000	Stoich A/F Ratio (Vol/Vol):	9.45
Helium	HE	0.0000	0.0000	Stoich A/F Ratio (Mass/Mass):	15.75
Neopentane	neo-C5H12	0.0000	0.0000	Specific Gravity (Relative to Air):	0.600
Octane	C8H18	0.0000	0.0000		
Nonane	C9H20	0.0000	0.0000	Fuel Specific Heat Ratio (K)	1 313
Ethylene	C2H4	0.0000	0.0000		1.010
Propylene	C3H6	0.0000	0.0000		
TOTAL (Volume %)	_	100.0000	100.0000		

#### CONDITIONS AND DEFINITIONS

Caterpillar Methane Number represents the knock resistance of a gaseous fuel. It should be used with the Caterpillar Fuel Usage Guide for the engine and rating to determine the rating for the fuel specified. A Fuel Usage Guide for each rating is included on page 2 of its standard technical data sheet.

RPC always applies to naturally aspirated (NA) engines, and turbocharged (TA or LE) engines only when they are derated for altitude and ambient site conditions.

Project specific technical data sheets generated by the Caterpillar Gas Engine Rating Pro program take the Caterpillar Methane Number and RPC into account when generating a site rating.

Fuel properties for Btu/scf calculations are at 60F and 14.696 psia.

Caterpillar shall have no liability in law or equity, for damages, consequently or otherwise, arising from use of program and related material or any part thereof.

#### FUEL LIQUIDS

Field gases, well head gases, and associated gases typically contain liquid water and heavy hydrocarbons entrained in the gas. To prevent detonation and severe damage to the engine, hydrocarbon liquids must not be allowed to enter the engine fuel system. To remove liquids, a liquid separator and coalescing filter are recommended, with an automatic drain and collection tank to prevent contamination of the ground in accordance with local codes and standards.

To avoid water condensation in the engine or fuel lines, limit the relative humidity of water in the fuel to 80% at the minimum fuel operating temperature.



Emission Control Application Data Sheet



Maxim Silencers 10635 Brighton Lane Stafford, Texas 77477 832 554-0980 832 554-0990 Phone: Fax:

Customer: AG EQUIPMENT

Customer Contact	

Project: ENLINK Powertherm Contact:

Order/Quote #:	0

Date: 4/26/2019

#### Engine Data:

						)
Engine Model:	WAUK 12V27	5GL+	Speed:	1000	RPM	
Fuel & Operating Type:	Natural Gas L	₋ean Burn	Engine Power:	3750 2704	Hp KW	
Exhaust Flow Rate:	<mark>25925</mark> 44047 47529	<mark>acfm</mark> m³/hr Ibs/hr	Exhaust Temperature:	<mark>836</mark> 447	°F ℃	)

#### Catalyst Data:

(	Number of Core layers:	1							
	Model:	MCC3-G8-342	8-C3			Inlet Size:	28	in	
	Grade:	Critical				Outlet Size:	34	in	
	Body Diameter:	68	in			Body Length:	303	in	
	Estimated weight:	6598 2994	lbs Kg			Estimated Back Pressure of the unit:	4.88 12.1	in of WC mbar	
	Core Part Number:	MCC-7140-2 (	15.44 X 24.75 ) SIZE	Qty	6	Speed through inlet:	4235	ft/min	
	Cell Density	300	cpsi			Back Pressure across Element(s) only	2.72 <b>6.8</b>	in of WC mbar	/

#### Emission:

Min. Temp. at Core Face:	752	°F	400	°C				Catalyst Type:	Oxidation
Max. Temp. at Core Face:	763	°F	406	°C				O₂ in Exhaus	t vol %
					Pollutant			H <sub>2</sub> O in Exhaus	t vol %
		NOx		CO	NMNEHC/VOC	CH <sub>2</sub> O/CHCO	ORGANIC PM10	]	
Engine Out / Pre Emission:		0.3		2.4	0.504	0.05	0	g/bhp-hr	
-		67.28		538.22	113.03	11.21	0.00	mg/Nm3	
Post Emission:		0.300		0.168	0.252	0.010	0.000	g/bhp-hr	
		67.28		37.68	56.51	2.24	0.00	mg/Nm3	
		0.0		93.0	50.0	80.0	50.0	% Reduction	
		2.48		1.39	2.08	0.08		lb/hr	
		10.86		6.08	9.13	0.36		tons/year operation	8760 hr/year
		32.3		18.1	27.1	1.1		ppmv	·
<b>`</b>								ppmvd @ 15% O2	

#### Acoustics:

Frequency Band (Hz):	31.5	63	125	250	500	1000	2000	4000	8000	
Raw Noise SPL (dB) at 3.28 ft.:	0	0	0	0	0	0	0	0	0	7 dBA
Estimated Attenuation (dB):	24	35	37	31	28	24	25	29.5	30	No Element
Plus:	24	36	39	33	32	29	31	35.5	35	One Element Layer
Silenced SPL (dB) at 3.28 ft.:	-24	-36	-39	-33	-32	-29	-31	-35.5	-35	-24.8 dBA
										_

#### Warranty & Notes:

/	<ul> <li>If Pre-Emission levels are not as noted above, contact Maxim Silencers for a re-quote.</li> </ul>		
/	<ul> <li>To achieve Post Emissions levels detailed above, exhaust temperature and Pre-Emission data must be as specified.</li> </ul>		1
	<ul> <li>Maximum allowable exhaust temperature at core face is 1350°F.</li> </ul>		
	<ul> <li>If applicable, the engine will require an air/fuel ratio controller to meet above emission levels. For Rich Burn engines λ must be 0.96 - 0.99.</li> </ul>		
	<ul> <li>Catalyst cleaning/regeneration required, if initial backpressure increases by 2" of WC.</li> </ul>		
	Engine operation to be stable and reproducible.		
	<ul> <li>QAC is not designed to withstand a backfire, therefore measures should be taken prior to QAC unit to alleviate backfire pressure.</li> </ul>		
	<ul> <li>Maximum lubrication oil consumption rate to be less than 0.0015 lb/bhp/hr.</li> </ul>		
	Lube oil sulfate ash contents should not exceed 0.5%.		
	<ul> <li>Phosphorus and/or Zinc should not exceed 5 ppmv in the exhaust stream.</li> </ul>		
	<ul> <li>A high temperature alarm/shutdown to be maintained at downstream of catalyst at 1300°F.</li> </ul>		
	<ul> <li>Fuel not to contain heavy or transition metals such as Pb, Ar, Zn, Cu, Sn, Fe, Ba, Ni, Cr etc.</li> </ul>		
	<ul> <li>Chlorinated or Silicone containing compounds in the exhaust not to exceed 1 ppmv.</li> </ul>		
	<ul> <li>Sulfur compounds in the exhaust gas stream not to exceed 25 ppmv.</li> </ul>		
	<ul> <li>Performance guarantee is voided should the catalyst become masked or de-activated by any contaminant in the exhaust stream.</li> </ul>		
	<ul> <li>Engine to be maintained and operated in accordance within manufacturer's recommended practice.</li> </ul>		
	Under no condition will Maxim Silencers assume any contingent liabilities.		
	<ul> <li>Operating manual is available online at www.maximsilencers.com or contact a Maxim sales representative.</li> </ul>		
	<ul> <li>Nomenclature: QAC4-292-8, 4 is grade (Super Critical), 29 is catalyst block size, 2 is no. of catalyst(s) and 8 is flange diameter.</li> </ul>		
	<ul> <li>Organic PM10 are estimate only and not a guarantee because of the variability in fuels and additives which change PM10.</li> </ul>		
$\backslash$	Maxim Silencers standard one year warranty applies.		
		Rev level: 86	
	<ul> <li>Organic PM10 are estimate only and not a guarantee because of the variability in fuels and additives which change PM10.</li> <li>Maxim Silencers standard one year warranty applies.</li> </ul>	Rev level: 86	/



# 275GL Series 12V 275GL+ Fuel Flex Gas Engine with ESM\*2

Constant Torque Ratings 3,750 bhp (2,796 kWb) @ 1,000 rpm

## **Technical Data**

Cylinders	12V
Piston displacement	13,048 cu. in. (214 L)
Compression ratio	8:1
Bore & stroke	10.83" x 11.81" (275 x 300 mm)
Jacket water system capacity	100 gal. (379 L)
Lube oil capacity	220 gal. (883 L)
Fuel pressure range	50 – 60 psi (3.4 – 4.1 bar)
Starting system	150 psi (10.3 bar)

#### Dimensions I x w x h inch (mm)

188.8 (4,796) x 91.3 (2,320) x 126.4 (3,211)

Weights Ib (kg)

54,000 (24,493)



Image is representative of engine model.

INNIO's Waukesha 275GL+ represents the most advanced generation of high-horsepower engines designed for optimum performance in gas compression and other mechanical drive applications. A unique combination of robust construction and innovative technology, the 275GL+ lean-burn engine delivers the fuel flexibility, reliability, power output, and emissions demanded by the oil and gas industry. The 275GL+ features Waukesha's ESM2 control, which integrates engine functionality into a single, closed-loop system with direct NOx measurement.

Key components such as the oil filters, oil cooler, pre-lube pump, and jacket water and auxiliary thermostats have been mounted on the engine, simplifying the packaging process and skid layout.





# **Technical Features**

Feature	Description	Advantages
Excellent fuel efficiency	Optimized to achieve excellent fuel efficiency while running on a wide variety of field gases and load profiles.	Minimize fuel costs and maximize profits across the entire range of speed and load combinations.
Single, closed-loop engine control system	<ul> <li>Waukesha's proven ESM2 control integrates the following into a single, closed-loop system:</li> <li>Air/Fuel Ratio Control</li> <li>Wastegate Control</li> <li>Turbocharger Bypass Control</li> <li>Ignition Timing</li> <li>Knock Detection</li> <li>Fault Monitoring</li> </ul>	Directly measures NOx emissions and automatically adjusts operating parameters to maintain desired NOx setting.
Wide range of fuel flexibility	Operation on a broad range of fuels with full power from 850-1,550 BTU/ft³ and capability up to 2,300 BTU/ft³.	More power on more fuels means more profits without the additional costs associated with fuel treatment skids.
High reliability with long maintenance intervals	Achieves up to 36,000 hours before top-end overhaul and 72,000 hours before bottom end.	With low lifecycle costs and the ability to run up to 5 years continuously before overhaul, the 275GL+ is the best choice for the most remote, rugged, and demanding applications.

## **Performance Data**

Interco	oler Water Temperature 130°F (54°C)	1000	1000 RPM			
		0.3 NOx	0.5 NOx			
	Power bhp (kWb)	3,750	(2,796)			
	BSFC (LHV) Btu/bhp-hr (kJ/kWh)	6,805 (10,225)	6,665 (10,014) 50			
	WKI* (before derate)	50				
	Altitude (before derate) ft (m)	4,900 (1,493)	5,700 (1,737)			
	NOx g/bhp-hr (mg/Nm <sup>3</sup> @ 5% O <sub>2</sub> )	0.3 (121)	0.5 (202)			
suc	CO g/bhp-hr (mg/Nm³ @ 5% O₂)	1.99 (806)	1.57 (636)			
Emissio	NMHC g/bhp-hr (mg/Nm³ @ 5% 0 <sub>2</sub> )	0.32 (131)	0.80 (326)			
	THC g/bhp-hr (mg/Nm <sup>3</sup> @ 5% O <sub>2</sub> )	5.14 (2,080)	4.37 (1,780)			
	Methane g/bhp-hr (mg/Nm³ @ 5% O,)	4.27 (1,730)	3.56 (1,445)			

All information provided is subject to change without notice. All technical and performance data to be released via SAA - please contact Application Engineering.

Consult your local Waukesha representative for system application assistance. The manufacturer reserves the right to change or modify without notice, the design or equipment specifications as herein set forth without incurring any obligation either with respect to equipment previously sold or in the process of construction except where otherwise specifically guaranteed by the manufacturer.

INNIO\* is a leading solutions provider of gas engines, power equipment, a digital platform and related services for power generation and gas compression at or near the point of use. With our Jenbacher\* and Waukesha\* product brands, INNIO pushes beyond the possible and looks boldly toward tomorrow. Our diverse portfolio of reliable, economical and sustainable industrial gas engines generates 200 kW to 10 MW of power for numerous industries globally. We can provide life cycle support to the more than 48,000 delivered gas engines worldwide. And, backed by our service network in more than 100 countries, INNIO connects with you locally for rapid response to your service needs. Headquartered in Jenbach, Austria, the business also has primary operations in Welland, Ontario, Canada, and Waukesha, Wisconsin, US.

Find your local support online: www.innio.com/en/company/providers IWK-119017-EN

\*Indicates a trademark

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# **EQUIPMENT DATA SHEET**

## Generator Gas

Model

# 400kW Rich Burn Gas data sheet

Document No: G08000870 Revision: B Created By: C. McGregor Approved By: A. Blackford Approval Date: 15/09/2022 Page: 1 of 4

		000,000,000,000,000		
Model reference		GG0400GASCON		
Model size and rating		400 kVA		
Bill of Material reference number		611039 B		
Manufacturer				
Model Reference			NHC20 H	24SE - EPA CGT
Performance Data				
Maximum Ambient Before Derate (LTA)			41.0°C (1	05.8°F) COP
Electrical (ISO 8528-1) *				
Continuous Power (COP)	kW (kVA)		359.0	(448.75)
LPG Continuous Power (COP)	kW (kVA)		255.0	(318.75)
Prime Power (PRP)	kW (kVA)		394.0	(492.5)
Single Step Load Application			44%	
Max Parasitic Load			17kW	
Gas Energy Input - LHV (ISO 3046-1) **				
100% KW PRP			1296kW	
100% KW COP			1181kW	
Aller				
Alternator				
Class F Temp Rise (105°C) Three Phase	kW (kVA)		540.0	(675)
Ends Out			12	
Make & Type			HCI534 E	13 or S5L1S-E4
AVR			MX341	
Regulation			/- 1	
Number of Bearings			1	

#### **Circuit Breaker**

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# **EQUIPMENT DATA SHEET**

Document No: G08000870

Generator Gas 400kW Rich Burn Gas da	ta sheet	Document No: G08000870 Revision: B Created By: C. McGregor Approved By: A. Blackford Approval Date: 15/09/2022 Page: 2 of 4
Make & Model		Schneider NS100N
Number of Poles		3
Rating	Amp (Amp)	1000.0 (1000)
Trip Unit Type		Micrologic 6.0
Overload Protection Range		400-1000 Amps (Adjustable by selector)
Short Circuit Protection Range		1500-10000 Amps (Adjustable b selector)
Load Terminals		
Туре		Busbar M12
Engine		
Make & Type		Waukesha VGF H24SE-EPA
Cylinders & Form		8 In-Line
Aspiration		Turbocharged Intercooled
Governor Make & Type		Electronic
Steady State Frequency		/- 1% ( /-0.6Hz)
Battery Voltage		24V
Generator Gas Supply Pressures		
Allowable Gas Supply Pressure (Natura Gas)	l	10 - 100 psi
Allowable Gas Supply Pressure (LPG)		30 - 300 psi
Engine Gas Supply Pressures		
Allowable Gas Supply Pressure (Natura Gas)	ıl	1.5 - 5 psi
Exhaust Emissions		
Specific Load		75% - 100%
Stationary Part 1048 HC NOx g/kW-h	r	0.8 g/kW-hr
Stationary Part 1048 CO g/kW-hr		20.6 g/kW-hr

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# **EQUIPMENT DATA SHEET**

Generator Gas 400kW Rich Burn Gas da	ta sheet	Document No: Revision: B Created By: C. Approved By: / Approval Date: Page: 3 of 4	G08000870 McGregor A. Blackford 15/09/2022
Stationary Part 1048 NMHC NOx g/kW-hr		0.8 g	/kW-hr
Mobile Part 1048 HC NOx g/kW-hr		1.3 g	/kW-hr
Mobile Part 1048 CO g/kW-hr		11.1	g/kW-hr
Mobile Part 1048 NMHC NOx g/kW-h	r	1.3 g	/kW-hr
Part 60 Subpart JJJJ Table 1 NOx g/Hp-hr		1.0 g	/HP-hr
Part 60 Subpart JJJJ Table 1 VOC g/Hp-hr		0.7 g	/HP-hr
Part 60 Subpart JJJJ Table 1 CO g/Hp-hr		2.0 g	/HP-hr
Fuel		LPG/ (CNG	Propane or Natural Gas 6/LNG)
Exhaust Silencer			
Make & Type		DCL GR 0 D304	International 2-DC18-8 CRIT CATALYTIC SILENCER (PN: -01-1Y18-32)
Certificate Number		JDR	SB24.0VGF-002
Permissible Back Pressure		28 (1	.1) mm (in) Hg
Current back pressure		17 (0	.67) mm (in) Hg
Noise			
Sound Pressure at 1m/3ft		81.4	dBA
Sound Pressure at 7m/21ft		71.7	dBA
Gas Supply			
Minimum Methane Index		33.0	
Other Capacities and Dimensions			
Lube Oil Capacity - Total	L (US gal)	338.0	) (89.232)
Lube Oil Capacity Sump	L (US gal)	212.8	3 (56.179)
Lube Oil Capacity Additional Oil Top Up	L (US gal)	125.0	) (33)
Coolant Capacity	L (US gal)	300.0	) (79.2)

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# **EQUIPMENT DATA SHEET**

### Generator Gas

## 400kW Rich Burn Gas data sheet

Document No: G08000870 Revision: B Created By: C. McGregor Approved By: A. Blackford Approval Date: 15/09/2022 Page: 4 of 4

#### **Physical Characteristics**

Length	6.06 m	19.88 ft
Width	2.44 m	8 ft
Height	2.62 m	8.6 ft
Gross Weight	13870 kg	30578.11 lbs
Net Weight	13430 kg	29608.08 lbs
Gross Fuel	0 lit	0 US gal
Net Fuel	0 lit	0 US gal

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Cimarron's product and service offering has greatly expanded following the recent acquisitions of HY-BON and Aereon and their associated brands of products:

## **Products and Services**

Emissions Control	Oil and Gas Processing	Services
<ul> <li>Vapor Recovery Units:</li> <li>Compression-base: Screw, Vane Compressors, Plunger Lift Pumps</li> <li>Activated Carbon-based Vapor Recovery Systems</li> <li>Enclosed Combustion:</li> <li>Quad O Combustors (98% DRE), Thermal Oxidizers, Vapor Combustion Units (99.9% DRE), CEB™ (99.99% DRE, low NOx)</li> <li>Smokeless Flares:</li> <li>High Efficiency Assisted (air, steam,</li> </ul>	<ul> <li>Production and processing:</li> <li>Modular Production Packages</li> <li>Separator</li> <li>Gas Filtration</li> <li>Glycol Dehydration</li> <li>Gas Production Units</li> <li>Oil and Gas Heaters</li> <li>Heater Treaters</li> <li>Vapor Recovery Towers</li> <li>BTEX Eliminators</li> <li>Plunger Lift Pumps</li> <li>API Tanks</li> </ul>	<ul> <li>Field Services:</li> <li>Startup &amp; Maintenance</li> <li>Spare parts</li> <li>Lease/Rentals</li> <li>LDAR Detection</li> </ul> Automation: <ul> <li>Burner Management Systems</li> <li>Emissions Control Real-time Monitoring</li> <li>DRE optimization (DRE-Max<sup>™</sup>)</li> </ul>
	CREATING A CLEANER ENVIRONMENT**	CONTROL *** OF DRE MAX.

## **Segments and Applications**

Oil & Gas Focus Areas	Expanded Focus Areas for Combustion Applications
<ul> <li>Upstream:</li> <li>Wellhead Oil and Gas Handling Production equipment to include separator packages, heater treaters, gas production units (GPUs), Line Heaters, Tanks, Tank Vapor Combustors, Flares, Mechanical Vapor Recovery</li> </ul>	<ul> <li>Biogas</li> <li>Agricultural</li> <li>Landfill</li> <li>Wastewater Treatment</li> </ul>
<ul> <li>Midstream:</li> <li>Gas Processing applications to include gas dehydration, gas filtration, gas line heaters, flares combustion, BTEX Eliminators</li> </ul>	<ul><li>Coal Mines</li><li>Industrial</li><li>Aerospace</li></ul>
<ul> <li>Downstream:</li> <li>Loading Terminal Vapor Combustors, Carbon Vapor Recovery, Refinery spec Flares &amp; Combustors</li> </ul>	

Pollutant	Emission Factor (lb/MMBtu) <sup>b</sup> (fuel input)	Emission Factor Rating
Criteria Pollutants and Greenhou	se Gases	
NO <sub>x</sub> <sup>c</sup> 90 - 105% Load	4.08 E+00	В
NO <sub>x</sub> <sup>c</sup> <90% Load	8.47 E-01	В
CO <sup>c</sup> 90 - 105% Load	3.17 E-01	С
CO <sup>c</sup> <90% Load	5.57 E-01	В
CO <sub>2</sub> <sup>d</sup>	1.10 E+02	А
SO <sub>2</sub> <sup>e</sup>	5.88 E-04	А
TOC <sup>f</sup>	1.47 E+00	А
Methane <sup>g</sup>	1.25 E+00	С
VOC <sup>h</sup>	1.18 E-01	С
PM10 (filterable) <sup>i</sup>	7.71 E-05	D
PM2.5 (filterable) <sup>i</sup>	7.71 E-05	D
PM Condensable <sup>j</sup>	9.91 E-03	D
Trace Organic Compounds	·	
1,1,2,2-Tetrachloroethane <sup>k</sup>	<4.00 E-05	Е
1,1,2-Trichloroethane <sup>k</sup>	<3.18 E-05	E
1,1-Dichloroethane	<2.36 E-05	Е
1,2,3-Trimethylbenzene	2.30 E-05	D
1,2,4-Trimethylbenzene	1.43 E-05	С
1,2-Dichloroethane	<2.36 E-05	Е
1,2-Dichloropropane	<2.69 E-05	Е
1,3,5-Trimethylbenzene	3.38 E-05	D
1,3-Butadiene <sup>k</sup>	2.67E-04	D
1,3-Dichloropropene <sup>k</sup>	<2.64 E-05	Е
2-Methylnaphthalene <sup>k</sup>	3.32 E-05	С
2,2,4-Trimethylpentane <sup>k</sup>	2.50 E-04	С
Acenaphthenek	1.25 E-06	С

# Table 3.2-2. UNCONTROLLED EMISSION FACTORS FOR 4-STROKE LEAN-BURN ENGINESa(SCC 2-02-002-54)

Pollutant	Emission Factor (lb/MMBtu) <sup>b</sup> (fuel input)	Emission Factor Rating
Acenaphthylene <sup>k</sup>	5.53 E-06	C
Acetaldehyde <sup>k,l</sup>	8.36 E-03	A
Acrolein <sup>k,l</sup>	5.14 E-03	A
Benzene <sup>k</sup>	4.40 E-04	A
Benzo(b)fluoranthene <sup>k</sup>	1.66 E-07	D
Benzo(e)pyrene <sup>k</sup>	4.15 E-07	D
Benzo(g,h,i)pervlene <sup>k</sup>	4.14 E-07	D
Biphenyl <sup>k</sup>	2.12 E-04	D
Butane	5.41 E-04	D
Butyr/Isobutyraldehyde	1.01 E-04	С
Carbon Tetrachloride <sup>k</sup>	<3.67 E-05	Е
Chlorobenzene <sup>k</sup>	<3.04 E-05	Е
Chloroethane	1.87 E-06	D
Chloroform <sup>k</sup>	<2.85 E-05	Е
Chrysene <sup>k</sup>	6.93 E-07	С
Cyclopentane	2.27 E-04	С
Ethane	1.05 E-01	С
Ethylbenzene <sup>k</sup>	3.97 E-05	В
Ethylene Dibromide <sup>k</sup>	<4.43 E-05	Е
Fluoranthene <sup>k</sup>	1.11 E-06	С
Fluorene <sup>k</sup>	5.67 E-06	С
Formaldehyde <sup>k,l</sup>	5.28 E-02	А
Methanol <sup>k</sup>	2.50 E-03	В
Methylcyclohexane	1.23 E-03	С
Methylene Chloride <sup>k</sup>	2.00 E-05	С
n-Hexane <sup>k</sup>	1.11 E-03	С
n-Nonane	1.10 E-04	С

# Table 3.2-2. UNCONTROLLED EMISSION FACTORS FOR 4-STROKE LEAN-BURN ENGINES (Continued)

Pollutant	Emission Factor (lb/MMBtu) <sup>b</sup> (fuel input)	Emission Factor Rating
n-Octane	3.51 E-04	С
n-Pentane	2.60 E-03	С
Naphthalene <sup>k</sup>	7.44 E-05	С
PAH <sup>k</sup>	2.69 E-05	D
Phenanthrene <sup>k</sup>	1.04 E-05	D
Phenol <sup>k</sup>	2.40 E-05	D
Propane	4.19 E-02	С
Pyrene <sup>k</sup>	1.36 E-06	С
Styrene <sup>k</sup>	<2.36 E-05	Е
Tetrachloroethane <sup>k</sup>	2.48 E-06	D
Toluenek	4.08 E-04	В
Vinyl Chloride <sup>k</sup>	1.49 E-05	С
Xylene <sup>k</sup>	1.84 E-04	В

#### Table 3.2-2. UNCONTROLLED EMISSION FACTORS FOR 4-STROKE LEAN-BURN ENGINES (Continued)

<sup>a</sup> Reference 7. Factors represent uncontrolled levels. For NO<sub>x</sub>, CO, and PM10, "uncontrolled" means no combustion or add-on controls; however, the factor may include turbocharged units. For all other pollutants, "uncontrolled" means no oxidation control; the data set may include units with control techniques used for NOx control, such as PCC and SCR for lean burn engines, and PSC for rich burn engines. Factors are based on large population of engines. Factors are for engines at all loads, except as indicated. SCC = Source Classification Code. TOC = Total Organic Compounds. PM-10 = Particulate Matter ≤ 10 microns (µm) aerodynamic diameter. A "<" sign in front of a factor means that the corresponding emission factor is based on one-half of the method detection limit.</li>
<sup>b</sup> Emission factors were calculated in units of (lb/MMBtu) based on procedures in EPA Method 19. To convert from (lb/MMBtu) to (lb/10<sup>6</sup> scf), multiply by the heat content of the fuel. If the heat content is not available, use 1020 Btu/scf. To convert from

(lb/MMBtu) to (lb/hp-hr) use the following equation:

lb/hp-hr = (lb/MMBtu) (heat input, MMBtu/hr) (1/operating HP, 1/hp)

(3.67)(% CON)(C)(D)(1/h), where  $\% \text{CON} = \text{percent conversion of fuel carbon to CO}_2$ , C = carbon content of fuel by weight (0.75), D = density of fuel, 4.1 E+04 lb/10<sup>6</sup> scf, and

<sup>&</sup>lt;sup>c</sup> Emission tests with unreported load conditions were not included in the data set.

<sup>&</sup>lt;sup>d</sup> Based on 99.5% conversion of the fuel carbon to  $CO_2$ .  $CO_2$  [lb/MMBtu] =

h = heating value of natural gas (assume 1020 Btu/scf at  $60^{\circ}$ F).

- Based on 100% conversion of fuel sulfur to SO<sub>2</sub>. Assumes sulfur content in natural gas of  $2,000 \text{ gr}/10^6 \text{scf.}$
- Emission factor for TOC is based on measured emission levels from 22 source tests.
- <sup>g</sup> Emission factor for methane is determined by subtracting the VOC and ethane emission factors from the TOC emission factor. Measured emission factor for methane compares well with the calculated emission factor, 1.31 lb/MMBtu vs. 1.25 lb/MMBtu, respectively.
- $^{\rm h}$  VOC emission factor is based on the sum of the emission factors for all speciated organic compounds less ethane and methane.
- Considered  $\leq 1 \ \mu m$  in aerodynamic diameter. Therefore, for filterable PM emissions, PM10(filterable) = PM2.5(filterable).
- <sup>j</sup> PM Condensable = PM Condensable Inorganic + PM-Condensable Organic
- Hazardous Air Pollutant as defined by Section 112(b) of the Clean Air Act.
- For lean burn engines, aldehyde emissions quantification using CARB 430 may reflect interference with the sampling compounds due to the nitrogen concentration in the stack. The presented emission factor is based on FTIR measurements. Emissions data based on CARB 430 are available in the background report.

#### Table 3.2-3. UNCONTROLLED EMISSION FACTORS FOR 4-STROKE RICH-BURN ENGINES<sup>a</sup> (SCC 2-02-002-53)

	Emission Factor (lb/MMBtu) <sup>b</sup>	Emission Factor	
Pollutant	(fuel input)	Rating	
Criteria Pollutants and Greenhous	se Gases		
$NO_{x}^{c}$ 90 - 105% Load	2.21 E+00	А	
NO <sub>x</sub> <sup>c</sup> <90% Load	2.27 E+00	С	
CO <sup>c</sup> 90 - 105% Load	3.72 E+00	А	
CO <sup>c</sup> <90% Load	3.51 E+00	С	
CO <sub>2</sub> <sup>d</sup>	1.10 E+02	А	
SO <sub>2</sub> <sup>e</sup>	5.88 E-04	А	
TOC <sup>f</sup>	3.58 E-01	С	
Methane <sup>g</sup>	2.30 E-01	С	
VOC <sup>h</sup>	2.96 E-02	С	
PM10 (filterable) <sup>i,j</sup>	9.50 E-03	Е	
PM2.5 (filterable) <sup>j</sup>	9.50 E-03	E	
PM Condensable <sup>k</sup>	9.91 E-03	Е	
Trace Organic Compounds			
1,1,2,2-Tetrachloroethane <sup>1</sup>	2.53 E-05	С	
1,1,2-Trichloroethane <sup>1</sup>	<1.53 E-05	Е	
1,1-Dichloroethane	<1.13 E-05	E	
1,2-Dichloroethane	<1.13 E-05	E	
1,2-Dichloropropane	<1.30 E-05	E	
1,3-Butadiene <sup>l</sup>	6.63 E-04	D	
1,3-Dichloropropene <sup>1</sup>	<1.27 E-05	Е	
Acetaldehyde <sup>l,m</sup>	2.79 E-03	С	
Acrolein <sup>1,m</sup>	2.63 E-03	С	
Benzene <sup>1</sup>	1.58 E-03	В	
Butyr/isobutyraldehyde	4.86 E-05	D	
Carbon Tetrachloride <sup>1</sup>	<1.77 E-05	Е	

Pollutant	Emission Factor (lb/MMBtu) <sup>b</sup> (fuel input)	Emission Factor Rating
Chlorobenzene <sup>l</sup>	<1.29 E-05	Е
Chloroform <sup>1</sup>	<1.37 E-05	E
Ethane <sup>n</sup>	7.04 E-02	С
Ethylbenzenel	<2.48 E-05	E
Ethylene Dibromide <sup>1</sup>	<2.13 E-05	Ε
Formaldehyde <sup>l,m</sup>	2.05 E-02	А
Methanol <sup>1</sup>	3.06 E-03	D
Methylene Chloride <sup>1</sup>	4.12 E-05	С
Naphthalene <sup>l</sup>	<9.71 E-05	Е
PAH <sup>1</sup>	1.41 E-04	D
Styrene <sup>1</sup>	<1.19 E-05	Ε
Toluene	5.58 E-04	А
Vinyl Chloride <sup>1</sup>	<7.18 E-06	Е
Xylene	1.95 E-04	А

#### Table 3.2-3. UNCONTROLLED EMISSION FACTORS FOR 4-STROKE RICH-BURN ENGINES (Concluded)

<sup>a</sup> Reference 7. Factors represent uncontrolled levels. For NO<sub>x</sub>, CO, and PM-10, "uncontrolled" means no combustion or add-on controls; however, the factor may include turbocharged units. For all other pollutants, "uncontrolled" means no oxidation control; the data set may include units with control techniques used for NOx control, such as PCC and SCR for lean burn engines, and PSC for rich burn engines. Factors are based on large population of engines. Factors are for engines at all loads, except as indicated. SCC = Source Classification Code. TOC = Total Organic Compounds. PM10 = Particulate Matter  $\leq$  10 microns ( $\mu$ m) aerodynamic diameter. A "<" sign in front of a factor means that the corresponding emission factor is based on one-half of the method detection limit.

<sup>b</sup> Emission factors were calculated in units of (lb/MMBtu) based on procedures in EPA Method 19. To convert from (lb/MMBtu) to (lb/ $10^6$  scf), multiply by the heat content of the fuel. If the heat content is not available, use 1020 Btu/scf. To convert from (lb/MMBtu) to (lb/hp-hr) use the following equation:

lb/hp-hr = db/MMBtu, heat input, MMBtu/hr, d/operating HP, 1/hp

<sup>c</sup> Emission tests with unreported load conditions were not included in the data set. <sup>d</sup> Based on 99.5% conversion of the fuel carbon to  $CO_2$ .  $CO_2$  [lb/MMBtu] =

(3.67)(%CON)(C)(D)(1/h), where %CON = percent conversion of fuel carbon to CO<sub>2</sub>,

Pollutant	Emission Factor (lb/10 <sup>6</sup> scf)	Emission Factor Rating
CO <sub>2</sub> <sup>b</sup>	120,000	А
Lead	0.0005	D
N <sub>2</sub> O (Uncontrolled)	2.2	Е
N <sub>2</sub> O (Controlled-low-NO <sub>X</sub> burner)	0.64	Е
PM (Total) <sup>c</sup>	7.6	D
PM (Condensable) <sup>c</sup>	5.7	D
PM (Filterable) <sup>c</sup>	1.9	В
$\mathrm{SO}_2^{\mathrm{d}}$	0.6	А
TOC	11	В
Methane	2.3	В
VOC	5.5	С

# TABLE 1.4-2. EMISSION FACTORS FOR CRITERIA POLLUTANTS AND GREENHOUSE GASESFROM NATURAL GAS COMBUSTION<sup>a</sup>

<sup>a</sup> Reference 11. Units are in pounds of pollutant per million standard cubic feet of natural gas fired. Data are for all natural gas combustion sources. To convert from  $lb/10^6$  scf to  $kg/10^6$  m<sup>3</sup>, multiply by 16. To convert from  $lb/10^6$  scf to 1b/MMBtu, divide by 1,020. The emission factors in this table may be converted to other natural gas heating values by multiplying the given emission factor by the ratio of the specified heating value to this average heating value. TOC = Total Organic Compounds. VOC = Volatile Organic Compounds.

- <sup>b</sup> Based on approximately 100% conversion of fuel carbon to  $CO_2$ .  $CO_2[lb/10^6 \text{ scf}] = (3.67)$  (CON) (C)(D), where CON = fractional conversion of fuel carbon to  $CO_2$ , C = carbon content of fuel by weight (0.76), and D = density of fuel,  $4.2 \times 10^4 \text{ lb}/10^6 \text{ scf}$ .
- <sup>c</sup> All PM (total, condensible, and filterable) is assumed to be less than 1.0 micrometer in diameter. Therefore, the PM emission factors presented here may be used to estimate  $PM_{10}$ ,  $PM_{2.5}$  or  $PM_1$  emissions. Total PM is the sum of the filterable PM and condensible PM. Condensible PM is the particulate matter collected using EPA Method 202 (or equivalent). Filterable PM is the particulate matter collected on, or prior to, the filter of an EPA Method 5 (or equivalent) sampling train.

<sup>d</sup> Based on 100% conversion of fuel sulfur to  $SO_2$ . Assumes sulfur content is natural gas of 2,000 grains/10<sup>6</sup> scf. The  $SO_2$  emission factor in this table can be converted to other natural gas sulfur contents by multiplying the  $SO_2$  emission factor by the ratio of the site-specific sulfur content (grains/10<sup>6</sup> scf) to 2,000 grains/10<sup>6</sup> scf.

Waste Stream⁵	Destruction/Removal Efficiency (DRE)
VOC	98 percent (generic)
	99 percent for compounds containing no more than 3 carbons that contain no elements other than carbon and hydrogen in addition to the following compounds: methanol, ethanol, propanol, ethylene oxide and propylene oxide.
H <sub>2</sub> S	98 percent
NH <sub>3</sub>	case-by-case
СО	case-by-case

Air Contaminants	Emission Factors	Btu	lb/MMBtu
Thermal NO <sub>x</sub>	Steam-assist	High Btu	0.0485 lb/MMBtu
		Low Btu	0.068 lb/MMBtu
	Other	High Btu	0.138 lb/MMBtu
		Low Btu	0.0641 lb/MMBtu

Air Contaminants	Emission Factors
Fuel NO <sub>x</sub>	$NO_x$ is 0.5 wt percent of inlet $NH_3$ in the sample calculations. The actual conversion of ammonia and other fuels to Fuel $NO_x$ are subject to case-by-case review.

Air Contaminants	Emission Factors	Btu	lb/MMBtu
СО	Steam-assist	High Btu	0.3503 lb/MMBtu
		Low Btu	0.3465 lb/MMBtu
	Other	High Btu	0.2755 lb/MMBtu
		Low Btu	0.5496 lb/MMBtu

Air Contaminants	Emission Factors
PM	None, required to be smokeless
SO <sub>2</sub>	100 percent S in fuel to SO <sub>2</sub>

<sup>&</sup>lt;sup>5</sup>The only exception of this is if inorganics might be emitted from the flare. In the case of landfills, the AP-42 PM factor may be used. In other cases, the emissions should be based on the composition of the waste stream routed to the flare.

# Table 1.4-1. EMISSION FACTORS FOR NITROGEN OXIDES (NOx) AND CARBON MONOXIDE (CO)FROM NATURAL GAS COMBUSTIONa

	Ν	O <sub>x</sub> <sup>b</sup>		СО
Combustor Type (MMBtu/hr Heat Input) [SCC]	Emission Factor (lb/10 <sup>6</sup> scf)	Emission Factor Rating	Emission Factor (lb/10 <sup>6</sup> scf)	Emission Factor Rating
Large Wall-Fired Boilers				
[1-01-006-01, 1-02-006-01, 1-03-006-01]				
Uncontrolled (Pre-NSPS) <sup>c</sup>	280	А	84	В
Uncontrolled (Post-NSPS) <sup>c</sup>	190	А	84	В
Controlled - Low NO <sub>x</sub> burners	140	А	84	В
Controlled - Flue gas recirculation	100	D	84	В
Small Boilers (<100) [1-01-006-02, 1-02-006-02, 1-03-006-02, 1-03-006-03]				
Uncontrolled	100	В	84	В
Controlled - Low NO <sub>x</sub> burners	50	D	84	В
Controlled - Low NO <sub>x</sub> burners/Flue gas recirculation	32	С	84	В
Tangential-Fired Boilers (All Sizes) [1-01-006-04]				
Uncontrolled	170	А	24	С
Controlled - Flue gas recirculation	76	D	98	D
Residential Furnaces (<0.3) [No SCC]				
Uncontrolled	94	В	40	В

<sup>a</sup> Reference 11. Units are in pounds of pollutant per million standard cubic feet of natural gas fired. To convert from  $lb/10^{6}$  scf to  $kg/10^{6}$  m<sup>3</sup>, multiply by 16. Emission factors are based on an average natural gas higher heating value of 1,020 Btu/scf. To convert from  $1b/10^{6}$  scf to lb/MMBtu, divide by 1,020. The emission factors in this table may be converted to other natural gas heating values by multiplying the given emission factor by the ratio of the specified heating value to this average heating value. SCC = Source Classification Code. ND = no data. NA = not applicable. <sup>b</sup> Expressed as NO<sub>2</sub>. For large and small wall fired boilers with SNCR control, apply a 24 percent reduction to the appropriate NO x emission factor. For

<sup>b</sup> Expressed as NO<sub>2</sub>. For large and small wall fired boilers with SNCR control, apply a 24 percent reduction to the appropriate NO x emission factor. For tangential-fired boilers with SNCR control, apply a 13 percent reduction to the appropriate NO x emission factor.
 <sup>c</sup> NSPS=New Source Performance Standard as defined in 40 CFR 60 Subparts D and Db. Post-NSPS units are boilers with greater than 250 MMBtu/hr of

<sup>c</sup> NSPS=New Source Performance Standard as defined in 40 CFR 60 Subparts D and Db. Post-NSPS units are boilers with greater than 250 MMBtu/hr of heat input that commenced construction modification, or reconstruction after August 17, 1971, and units with heat input capacities between 100 and 250 MMBtu/hr that commenced construction modification, or reconstruction after June 19, 1984.

6-1



Figure 5.2-5. Tank truck unloading into a service station underground storage tank and practicing "vapor balance" form of emission control.

Table 5.2-1.	SATURATION (S) FACTORS FOR CALCULATING PETROLEUM LIQUID
	LOADING LOSSES

Cargo Carrier	ier Mode Of Operation	
Tank trucks and rail tank cars	Submerged loading of a clean cargo tank	0.50
	Submerged loading: dedicated normal service	0.60
	Submerged loading: dedicated vapor balance service	1.00
	Splash loading of a clean cargo tank	1.45
	Splash loading: dedicated normal service	1.45
	Splash loading: dedicated vapor balance service	1.00
Marine vessels <sup>a</sup>	Submerged loading: ships	0.2
	Submerged loading: barges	0.5

<sup>a</sup> For products other than gasoline and crude oil. For marine loading of gasoline, use factors from Table 5.2-

2. For marine loading of crude oil, use Equations 2 and 3 and Table 5.2-3.

Equipment Type	Service <sup>a</sup>	Emission Factor (kg/hr/source) <sup>b</sup>
Valves	Gas Heavy Oil Light Oil Water/Oil	4.5E-03 8.4E-06 2.5E-03 9.8E-05
Pump seals	Gas Heavy Oil Light Oil Water/Oil	2.4E-03 NA 1.3E-02 2.4E-05
Others <sup>C</sup>	Gas Heavy Oil Light Oil Water/Oil	8.8E-03 3.2E-05 7.5E-03 1.4E-02
Connectors	Gas Heavy Oil Light Oil Water/Oil	2.0E-04 7.5E-06 2.1E-04 1.1E-04
Flanges	Gas Heavy Oil Light Oil Water/Oil	3.9E-04 3.9E-07 1.1E-04 2.9E-06
Open-ended lines	Gas Heavy Oil Light Oil Water/Oil	2.0E-03 1.4E-04 1.4E-03 2.5E-04

TABLE 2-4. OIL AND GAS PRODUCTION OPERATIONS AVERAGE EMISSION FACTORS (kg/hr/source)

<sup>a</sup>Water/Oil emission factors apply to water streams in oil service with a water content greater than 50%, from the point of origin to the point where the water content reaches 99%. For water streams with a water content greater than 99%, the emission rate is considered negligible.

<sup>b</sup>These factors are for total organic compound emission rates (including non-VOC's such as methane and ethane) and apply to light crude, heavy crude, gas plant, gas production, and off shore facilities. "NA" indicates that not enough data were available to develop the indicated emission factor.

<sup>C</sup>The "other" equipment type was derived from compressors, diaphrams, drains, dump arms, hatches, instruments, meters, pressure relief valves, polished rods, relief valves, and vents. This "other" equipment type should be applied for any equipment type other than connectors, flanges, open-ended lines, pumps, or valves.

#### **Environmental Protection Agency**

Pt. 98, Subpt. W, Table W-1A

and outer diameter greater than or equal to 2.375 inch.

*Tubing systems* means piping equal to or less than one half inch diameter as per nominal pipe size.

*Turbine meter* means a flow meter in which a gas or liquid flow rate through the calibrated tube spins a turbine from which the spin rate is detected and calibrated to measure the fluid flow rate.

Vented emissions means intentional or designed releases of  $CH_4$  or  $CO_2$  containing natural gas or hydrocarbon gas (not including stationary combustion flue gas), including process designed flow to the atmosphere through seals or vent pipes, equipment blowdown for maintenance, and direct venting of gas

Pneumatic Pumps<sup>3</sup>

used to power equipment (such as pneumatic devices).

Vertical well means a well bore that is primarily vertical but has some unintentional deviation or one or more intentional deviations to enter one or more subsurface targets that are offset horizontally from the surface location, intercepting the targets either vertically or at an angle.

Well testing venting and flaring means venting and/or flaring of natural gas at the time the production rate of a well is determined for regulatory, commercial, or technical purposes. If well testing is conducted immediately after well completion or workover, then it is considered part of well completion or workover.

10.3

#### [75 FR 74488, Nov. 30, 2010, as amended at 76 FR 80590, Dec. 23, 2011]

# TABLE W–1A OF SUBPART W–DEFAULT WHOLE GAS EMISSION FACTORS FOR ONSHORE PETROLEUM AND NATURAL GAS PRODUCTION

Onshore petroleum and natural gas production	Emission factor (scf/hour/ component)
Eastern U.S. Population Emission Factors—All Components, Gas Service <sup>1</sup>	·
Valve Connector Open-ended Line Pressure Relief Valve Low Continuous Bleed Pneumatic Device Vents <sup>2</sup> High Continuous Bleed Pneumatic Device Vents <sup>2</sup> Intermittent Bleed Pneumatic Device Vents <sup>2</sup> Pneumatic Pumps <sup>3</sup>	0.640 0.083 1.46 0.97 1.39 37.3 13.5 10.3
Population Emission Factors—All Components, Light Crude Service 4	
Valve Flange Connector Open-ended Line Pump Other <sup>5</sup>	0.04 0.002 0.005 0.04 0.01 0.23
Population Emission Factors—All Components, Heavy Crude Service 6	
Valve Flange Connector (other) Open-ended Line Other <sup>5</sup>	0.0004 0.0007 0.0002 0.004 0.002
Western U.S. Population Emission Factors—All Components, Gas Service	
Valve Connector Open-ended Line Pressure Relief Valve Low Continuous Bleed Pneumatic Device Vents <sup>2</sup> High Continuous Bleed Pneumatic Device Vents <sup>2</sup> Intermittent Bleed Pneumatic Device Vents <sup>2</sup>	2.903 0.396 0.748 4.631 1.77 47.4 17.1

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Onshore petroleum and natural gas production	Emission factor (scf/hour/ component)
Population Emission Factors—All Components, Light Crude Service 4	
Valve	0.04
Flange	0.002
Connector	0.005
Open-ended Line	0.04
Pump	0.01
Other <sup>5</sup>	0.23
Population Emission Factors—All Components, Heavy Crude Service 6	

alve lange	0.0004 0.0007 0.0002 0.004 0.002
	0.002

<sup>1</sup> For multi-phase flow that includes gas, use the gas service emissions factors.
 <sup>2</sup> Emission Factor is in units of "scf/hour/device."
 <sup>3</sup> Emission Factor is in units of "scf/hour/pump."
 <sup>4</sup> Hydrocarbon liquids greater than or equal to 20°API are considered "light crude."
 <sup>5</sup> "Others" category includes instruments, loading arms, pressure relief valves, stuffing boxes, compressor seals, dump lever arms, and vents.
 <sup>6</sup> Hydrocarbon liquids less than 20°API are considered "heavy crude."

#### [76 FR 80591, Dec. 23, 2011]

#### TABLE W-1B TO SUBPART W OF PART 98-DEFAULT AVERAGE COMPONENT COUNTS FOR MAJOR **ONSHORE NATURAL GAS PRODUCTION EQUIPMENT**

Major equipment	Valves	Connectors	Open-ended lines	Pressure relief valves
Ea	stern U.S.			
Wellheads	8	38	0.5	0
Separators	1	6	0	0
Meters/piping	12	45	0	0
Compressors	12	57	0	0
In-line heaters	14	65	2	1
Dehydrators	24	90	2	2
We	estern U.S.			
Wellheads	11	36	1	0
Separators	34	106	6	2
Meters/piping	14	51	1	1
Compressors	73	179	3	4
In-line heaters	14	65	2	1
Dehydrators	24	90	2	2

#### TABLE W-1C TO SUBPART W OF PART 98-DEFAULT AVERAGE COMPONENT COUNTS FOR MAJOR **CRUDE OIL PRODUCTION EQUIPMENT**

Major equipment	Valves	Flanges Connectors		Open-ended lines	Other compo- nents
	Ea	stern U.S.			
Wellhead	5	10	4	0	1
Separator	6	12	10	0	0
Heater-treater	8	12	20	0	0
Header	5	10	4	0	0
	We	estern U.S.			
Wellhead	5	10	4	0	1
Separator	6	12	10	0	0
Heater-treater	8	12	20	0	0
Header	5	10	4	0	0

#### **Environmental Protection Agency**

TABLE W–1D OF SUBPART W OF PART 98— DESIGNATION OF EASTERN AND WESTERN U.S.

Eastern U.S.	Western U.S.
Connecticut	Alabama Alaska Arizona Arkansas California Colorado Hawaii Idaho Iowa Kansas Louisiana Minnesota Missoiri

#### Pt. 98, Subpt. W, Table W--

TABLE W-1D OF SUBPART W OF PART 98-DESIGNATION OF EASTERN AND WESTERN U.S.-Continued

Eastern U.S.	Western U.S.		
North Carolina Ohio Pennsylvania Rhode Island South Carolina Tennessee Vermont Virginia West Virginia Wisconsin	Montana Nebraska Nevada New Mexico North Dakota Oklahoma Oregon South Dakota Texas Utah Washington Wyoming		

# TABLE W–2 OF SUBPART W—DEFAULT TOTAL HYDROCARBON EMISSION FACTORS FOR ONSHORE NATURAL GAS PROCESSING

Onshore natural gas processing plants	Emission factor (scf/hour/ component)
Leaker Emission Factors—Compressor Components, Gas Service	
Valve <sup>1</sup>	14.84
Connector	5.59
Open-Ended Line	17.27
Pressure Relief Valve	39.66
Meter	19.33

Leaker Emission Factors-Non-Compressor Components, Gas Service

Valve 1	6.42
Connector	5.71
Open-Ended Line	11.27
Pressure Relief Valve	2.01
Meter	2.93

<sup>1</sup> Valves include control valves, block valves and regulator valves.

[76 FR 80592, Dec. 23, 2011]

# TABLE W–3 of Subpart W—Default Total Hydrocarbon Emission Factors for Onshore Natural Gas Transmission Compression

Onshore natural gas transmission compression	Emission factor (scf/hour/ component)
Leaker Emission Factors—Compressor Components, Gas Service	
Valve 1	14.84
Connector	5.59
Open-Ended Line	17.27
Pressure Relief Valve	39.66
Meter	19.33
Leaker Emission Factors—Non-Compressor Components, Gas Service	6.42
Connector	5.71
Open-Ended Line	11.27
Pressure Relief Valve	2.01
Meter	2.93
Population Emission Factors—Gas Service	
Low Continuous Bleed Pneumatic Device Vents <sup>2</sup>	1.37
High Continuous Bleed Pneumatic Device Vents <sup>2</sup>	18.20

The following empirical expressions may be used to estimate the quantity in pounds (lb) of size-specific particulate emissions from an unpaved road, per vehicle mile traveled (VMT):

For vehicles traveling on unpaved surfaces at industrial sites, emissions are estimated from the following equation:

$$E = k (s/12)^{a} (W/3)^{b}$$
(1a)

and, for vehicles traveling on publicly accessible roads, dominated by light duty vehicles, emissions may be estimated from the following:

$$E = \frac{k (s/12)^{a} (S/30)^{d}}{(M/0.5)^{c}} - C$$
(1b)

where k, a, b, c and d are empirical constants (Reference 6) given below and

- E = size-specific emission factor (lb/VMT)
- s = surface material silt content (%)
- W = mean vehicle weight (tons)
- M = surface material moisture content (%)
- S = mean vehicle speed (mph)
- C = emission factor for 1980's vehicle fleet exhaust, brake wear and tire wear.

The source characteristics s, W and M are referred to as correction parameters for adjusting the emission estimates to local conditions. The metric conversion from lb/VMT to grams (g) per vehicle kilometer traveled (VKT) is as follows:

$$1 \text{ lb/VMT} = 281.9 \text{ g/VKT}$$

The constants for Equations 1a and 1b based on the stated aerodynamic particle sizes are shown in Tables 13.2.2-2 and 13.2.2-4. The PM-2.5 particle size multipliers (k-factors) are taken from Reference 27.

	Industrial Roads (Equation 1a)			Public Roads (Equation 1b)		
Constant	PM-2.5	<b>PM-10</b>	PM-30*	PM-2.5	<b>PM-</b> 10	PM-30*
k (lb/VMT)	0.15	1.5	4.9	0.18	1.8	6.0
a	0.9	0.9	0.7	1	1	1
b	0.45	0.45	0.45	-	-	-
с	-	-	-	0.2	0.2	0.3
d	-	-	-	0.5	0.5	0.3
Quality Rating	В	В	В	В	В	В

Table 13.2.2-2. CONSTANTS FOR EQUATIONS 1a AND 1b

\*Assumed equivalent to total suspended particulate matter (TSP)

"-" = not used in the emission factor equation

Table 13.2.2-2 also contains the quality ratings for the various size-specific versions of Equation 1a and 1b. The equation retains the assigned quality rating, if applied within the ranges of source conditions, shown in Table 13.2.2-3, that were tested in developing the equation:

Table 13.2.2-3.RANGE OF SOURCE CONDITIONS USED IN DEVELOPING EQUATION 1a AND<br/>1b

		Mean Vehicle Weight		Mean Vehicle Speed		Mean	Surface Moisture
Emission Factor	Surface Silt Content, %	Mg	ton	km/hr	mph	No. of Wheels	Content, %
Industrial Roads (Equation 1a)	1.8-25.2	1.8-260	2-290	8-69	5-43	4-17ª	0.03-13
Public Roads (Equation 1b)	1.8-35	1.4-2.7	1.5-3	16-88	10-55	4-4.8	0.03-13

<sup>a</sup> See discussion in text.

As noted earlier, the models presented as Equations 1a and 1b were developed from tests of traffic on unpaved surfaces. Unpaved roads have a hard, generally nonporous surface that usually dries quickly after a rainfall or watering, because of traffic-enhanced natural evaporation. (Factors influencing how fast a road dries are discussed in Section 13.2.2.3, below.) The quality ratings given above pertain to the mid-range of the measured source conditions for the equation. A higher mean vehicle weight and a higher than normal traffic rate may be justified when performing a worst-case analysis of emissions from unpaved roads.

The emission factors for the exhaust, brake wear and tire wear of a 1980's vehicle fleet (C) was obtained from EPA's MOBILE6.2 model <sup>23</sup>. The emission factor also varies with aerodynamic size range

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# **Section 8**

# Map(s)

<u>A map</u> such as a 7.5 minute topographic quadrangle showing the exact location of the source. The map shall also include the following:

The UTM or Longitudinal coordinate system on both axes	An indicator showing which direction is north
A minimum radius around the plant of 0.8km (0.5 miles)	Access and haul roads
Topographic features of the area	Facility property boundaries
The name of the map	The area which will be restricted to public access
A graphical scale	

A topographical map is attached to this section.





# **Section 9**

# **Proof of Public Notice**

(for NSR applications submitting under 20.2.72 or 20.2.74 NMAC) (This proof is required by: 20.2.72.203.A.14 NMAC "Documentary Proof of applicant's public notice")

I have read the AQB "Guidelines for Public Notification for Air Quality Permit Applications" This document provides detailed instructions about public notice requirements for various permitting actions. It also provides public notice examples and certification forms. Material mistakes in the public notice will require a re-notice before issuance of the permit.

Unless otherwise allowed elsewhere in this document, the following items document proof of the applicant's Public Notification. Please include this page in your proof of public notice submittal with checkmarks indicating which documents are being submitted with the application.

New Permit and Significant Permit Revision public notices must include all items in this list.

Technical Revision public notices require only items 1, 5, 9, and 10.

Per the Guidelines for Public Notification document mentioned above, include:

- 1. 🛛 A copy of the certified letter receipts with post marks (20.2.72.203.B NMAC)
- 2. A list of the places where the public notice has been posted in at least four publicly accessible and conspicuous places, including the proposed or existing facility entrance. (e.g: post office, library, grocery, etc.)
- 3. A copy of the property tax record (20.2.72.203.B NMAC).
- 4. 🛛 A sample of the letters sent to the owners of record.
- 5. 🛛 A sample of the letters sent to counties, municipalities, and Indian tribes.
- 6. 🛛 A sample of the public notice posted and a verification of the local postings.
- 7. 🛛 A table of the noticed citizens, counties, municipalities and tribes and to whom the notices were sent in each group.
- 8. X A copy of the public service announcement (PSA) sent to a local radio station and documentary proof of submittal.
- 9. A copy of the <u>classified or legal</u> ad including the page header (date and newspaper title) or its affidavit of publication stating the ad date, and a copy of the ad. When appropriate, this ad shall be printed in both English and Spanish.
- 10. A copy of the <u>display</u> ad including the page header (date and newspaper title) or its affidavit of publication stating the ad date, and a copy of the ad. When appropriate, this ad shall be printed in both English and Spanish.
- 11. A map with a graphic scale showing the facility boundary and the surrounding area in which owners of record were notified by mail. This is necessary for verification that the correct facility boundary was used in determining distance for notifying land owners of record.

# Sample of Posted Notice and Proof of Posting Horned Frog Compressor Station Delaware G&P, LLC

Facility entrance

Woolworth Community Library – 100 E Utah Ave, Jal, NM 88252

Jal City Hall – 710 W Wyoming Ave, Jal, NM 88525

Post Office 111 S 4<sup>th</sup> St., Jal, NM 88252

# NOTICE

**Delaware G&P, LLC** announces its application to the New Mexico Environment Department for an air quality permit for the **modification** of its **oil and gas** facility. The expected date of application submittal to the Air Quality Bureau is **May 2024.** 

The exact location for the proposed facility, known as **Horned Frog Compressor Station**, is located at latitude **32.083086** dec deg North and longitude **-103.588061** dec deg West. The approximate location of this facility is **23.5** miles **West** of **Jal** in **Lea** County.

The proposed **modification** consists of nine compressor engines, two generator engines, six condensate tanks, two produced water tanks, one gunbarrel separator, two glycol reboilers, two TEG dehydrators, condensate loadout, produced water loadout, one combustor, haul road fugitives, facility piping fugitives, and startup, shutdown, maintenance emissions.

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PM <sub>2.5</sub>	3.0 pph	11.0 tpy
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Nitrogen Oxides (NO <sub>x</sub> )	20.0 pph	82.0 tpy
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Volatile Organic Compounds (VOC)	1768.0 pph	128.5 tpy
Total sum of all Hazardous Air Pollutants (HAPs)	60.5 pph	20.0 tpy
Green House Gas Emissions as Total CO2e	n/a	296,463.0 tpy

The standard and maximum operating schedules of the facility will be from 12:00 a.m. to 11:59 p.m. 7 days a week and a maximum of 52 weeks per year.

# The owner and/or operator of the Facility is: **Delaware G&P, LLC; 1722 Routh Street, Suite 1300, Dallas, TX 75201**

If you have any comments about the construction or operation of this facility, and you want your comments to be made as part of the permit review process, you must submit your comments in writing to this address: Permit Programs Manager; New Mexico Environment Department; Air Quality Bureau; 525 Camino de los Marquez, Suite 1; Santa Fe, New Mexico; 87505-1816. Other comments and questions may be submitted verbally. (505) 476-4300; 1 800 224-7009.

With your comments, please refer to the company name and facility name, or send a copy of this notice along with your comments. This information is necessary since the Department may have not yet received the permit application. Please include a legible return mailing address. Once the Department

has completed its preliminary review of the application and its air quality impacts, the Department's notice will be published in the legal section of a newspaper circulated near the facility location.

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#### **Notice of Non-Discrimination**

NMED does not discriminate on the basis of race, color, national origin, disability, age or sex in the administration of its programs or activities, as required by applicable laws and regulations. NMED is responsible for coordination of compliance efforts and receipt of inquiries concerning non-discrimination requirements implemented by 40 C.F.R. Part 7, including Title VI of the Civil Rights Act of 1964, as amended; Section 504 of the Rehabilitation Act of 1973; the Age Discrimination Act of 1975, Title IX of the Education Amendments of 1972, and Section 13 of the Federal Water Pollution Control Act Amendments of 1972. If you have any questions about this notice or any of NMED's non-discrimination programs, policies or procedures, or if you believe that you have been discriminated against with respect to a NMED program or activity, you may contact: Non-Discrimination Coordinator, NMED, 1190 St. Francis Dr., Suite N4050, P.O. Box 5469, Santa Fe, NM 87502, (505) 827-2855,

nd.coordinator@env.nm.gov. You may also visit our website at https://www.env.nm.gov/non-employeediscrimination-complaint-page/ to learn how and where to file a complaint of discrimination.





# **General Posting of Notices – Certification**

I, \_\_\_\_\_Breanne Halfmann\_, the undersigned, certify that on DATE, posted a true and correct copy of the attached Public Notice in the following publicly accessible and conspicuous places in the City of Jal in Lea County, State of New Mexico on the following dates:

- 1. Facility entrance -5/6/2024
- 2. Woolworth Community Library 100 E Utah Ave, Jal, NM 88252 5/6/2024
- 3. Jal City Hall 710 W Wyoming Ave, Jal, NM 88525 5/6/2024
- 4. Post Office 111 S 4<sup>th</sup> St., Jal, NM 88252 5/6/2024

Signed this Unday of May ..., 2029, Bream Halfmann Signature

Date

Breanne Halfmann

Printed Name
# Table of Notified Owners, Counties, Municipalities, Indian Tribes Horned Frog Compressor Station Delaware G&P, LLC

Owners within ½ mile of the Property Boundary	
Occidental Permian Ltd – Oil and Gas	5 Greenway Plaza, Suite 110
	Houston, TX 77046-0521
USA- Dinwiddie Cattle Co -agricultural	1893 Cross Y Rd
	Roswell, NM 88202
Basin Properties Ranches, LLC	P.O. Box 5677
	Abilene, TX 79608
Intrepid Potash – NM LLC	101 17 <sup>th</sup> Street, Suite 1050
	Denver, CO 80202
BLM	301 Dinosaur Trail
	Santa Fe, NM 87508
State Land Office	310 Old Santa Fe Trail
	Santa Fe, NM 87508
Municipalities within 10 miles of the Property Boundary	
Lea County Clerk's Office	PO Box 1507
	Lovington, NM 88260
Eddy County Clerk's Office	101 W Greene Street
	Carlsbad, NM 88220

## Sample of Letter Sent to Owners, Counties, Municipalities, Indian Tribes

### <u>CERTIFIED MAIL XXXX XXXX XXXX XXXX</u> <u>RETURN RECEIPT REQUESTED (certified mail is required, **return receipt is optional**)</u>

To Whom it May Concern,

**Delaware G&P, LLC** announces its application to the New Mexico Environment Department for an air quality permit for the **modification** of its **oil and gas** facility. The expected date of application submittal to the Air Quality Bureau is **May 2024.** 

The exact location for the proposed facility, known as **Horned Frog Compressor Station**, is located at latitude **32.083086** dec deg North and longitude **-103.588061** dec deg West. The approximate location of this facility is **23.5** miles **West** of **Jal** in **Lea** County.

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Sincerely,

Daria Underwood

303 W Wall Street, Suite 202 Midland, TX 79701

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1710 5270 0217	Certified Mail Fee  Certified Mail Fee  Certified Mail Fee  Certified Mail Fee  Certified Mail Reservices & Fees (check box, add fee as accreate)  Certified Mail Restricted Delivery  Certified Mail Restricted Delivery  Adult Signature Required  Certified Mail Restricted Delivery  Cerified Mail Restricted Delivery  Ce	UIISH III Postmark Here OTT/AIH//ZDC224	7150 0752 0217	Certified Mail Fee \$4440 S Extra Services & Fees (check box, add fee \$200, 5 Return Receipt (hardcopy) Certified Mail Restricted Delivery Certified Mail Restricted Delivery Adult Signature Required Adult Signature Restricted Delivery Postage S Total Postage and Fees S	05596679224
9289	Sent To Din widdie (attle Co Street and Apt. No. pr PO Box No 1893 (D555) Rd City, States 21P+48 Coswell, NM 8821 PS Form 3800, January 2023 PSN 7530-02-000-9047	2 See Reverse for Instructions	9589 [	Sent To Occidental Permian Ltd Street and Apt. No., or PO Box No. 5 Greenway Plaza, Suite City, State, 219-19 Houston, Tx 77046-C PS Form 3800, January 2023 PSN 7530-02-000-9047	2  10 252   See Reverse for Instructions



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Sections	0	0.13	0.25	12	0.5 mi
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Esri Community Maps Contributors, Texas Parks & Wildlife, CONANP, Esri, TomTom, Garmin, SafeGraph, GeoTechnologies, Inc, METI/NASA, USGS, EPA, NPS, US Census Bureau, USDA, USPWS

### **Parcel Details**

OWNER NUMBER:	51702	UPC CODE:	4194150233331
PARCEL NUMBER:	4000517020001		

Owner Information		
Owner:	INTREPID POTASH-NEW MEXICO LLC	
Mailing Address:	707 17TH ST	
Property Address:		

Subdivision Information		
Name:		
Unit:		
Block:		
Lot:		

### Legal Information

#### 320.00 AC BEING W2E2, SW4

Other Information			
Taxable Value:	\$16974	Deed Book:	2150
Exempt Value:	\$0	Deed Page:	23
Net Value:	\$16974	District:	190
Livestock Value:	\$0	Section:	33
Manufactured Home Value:	\$0	Township:	25
Personal Property:	\$0	Range:	33
Land Value:	\$50922	Date Filed:	20190501
Improvement Value:	\$0	Most Current Tax:	391
Full Value:	\$50922	Year Recorded:	

# Square Foot and Year Built listed only to be used for comparative purposes, NOT to be used for commerce.

Building Information			
Year Built:		Number of Stories:	
Basement SQFT:		First Floor SQFT:	
Second Floor SQFT:			

#### Lea County, New Mexico Disclaimer Information deeded reliable but not guaranteed. Copyright © 2023 MAP TO BE USED FOR TAX PURPOSES ONLY. NOT TO BE USED FOR CONVEYANCE.



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Sections	0	0.13	0.25	<sup>1</sup>	0.5 mi
Parcels	Г 0	0.2	0.4		0.8 km

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### **Parcel Details**

OWNER NUMBER:	51831	UPC CODE:	4193151265265
PARCEL NUMBER:	4000518310001		

Owner Information		
Owner:	BASIN PROPERTIES RANCHES LLC	
Mailing Address:	PO BOX 5677	
Property Address:		

Subdivision Information			
Name:			
Unit:			
Block:			
Lot:			

### Legal Information

#### 640.00 AC ALL

Other Information							
Taxable Value:	\$6898	Deed Book:	2140				
Exempt Value:	\$0	Deed Page:	578				
Net Value:	\$6898	District:	190				
Livestock Value:	\$7257	Section:	05				
Manufactured Home Value:	\$0	Township:	26				
Personal Property:	\$0	Range:	33				
Land Value:	\$8436	Date Filed:	20181011				
Improvement Value:	\$5001	Most Current Tax:	431				
Full Value:	\$20694	Year Recorded:					

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General information about air quality and the permitting process, and links to the regulations can be found at the Air Quality Bureau's website: www.env.nm.gov/air-quality/permitting-section-home-page/. The regulation dealing with public participation in the permit review process is 20.2.72.206 NMAC.

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# Affidavit of Publication

STATE OF NEW MEXICO COUNTY OF LEA

I, Daniel Russell, Publisher of the Hobbs News-Sun, a newspaper published at Hobbs, New Mexico, solemnly swear that the clipping attached hereto was published in the regular and entire issue of said newspaper, and not a supplement thereof for a period of 1 issue(s).

> Beginning with the issue dated May 05, 2024 and ending with the issue dated May 05, 2024.

has

Publisher

Sworn and subscribed to before me this 5th day of May 2024.

Business Manager

My commission expires January 29, 2007 NEW MEXICO (Seal) STATE OF NEW MEXICO NOTARY PUBLIC GUSSIE RUTH BLACK COMMISSION # 1087526 COMMISSION EXPIRES 01/29/2027

This newspaper is duly qualified to publish legal notices or advertisements within the meaning of Section 3, Chapter 167, Laws of 1937 and payment of fees for said publicatior has been made.

## NOTICE OF AIR QUALITY PERMIT APPLICA

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67116752

00290064

JEFF JACKSON RESOLUTE COMPLIANCE, LLC **PO BOX 970** ROYSE CITY, TX 75189

### Leslee Kimbrell

From:	Leslee Kimbrell
Sent:	Tuesday, May 7, 2024 11:16 AM
То:	aaron@1radiosquare.com
Cc:	Lance Green; Daria Underwood; Jeff Jackson; Kayla Curtis
Subject:	Public Service Announcement

To Whom It May Concern,

Delaware G&P, LLC (EnLink) requests a public service announcement on KZOR Radio, for its intention to modify a compressor station in Lea County. The State of New Mexico requires that any company that desires to construct or modify an oil and gas facility must have a public service announcement. EnLink has written out the following to be aired as soon as practical:

"Delaware G&P, LLC is an oil and gas gathering company planning to modify and operate the Horned Frog Compressor Station in Lea County. The location for the proposed facility will be at latitude 32 degrees, 4 minutes, 59.1 seconds and longitude -103 degrees, 35 minutes, 17.02 seconds. The approximate location of this facility is 23.5 miles Southwest of Jal in Lea County. More information about this facility can be found at the Woolworth Community Library, Jal City Hall, and the Post Office on 111 S 4<sup>th</sup> St. in Jal. For any comments about the construction or operation of the proposed facility, the New Mexico Air Quality Bureau can be contacted by phone at (505) 476-4300 or by mail at 525 Camino de los Marquez, Suite 1, Santa Fe, New Mexico 87505-1816."

Please respond to this email and provide an electronic version of the affidavit immediately after airing this announcement. You can also reply to this email with the invoice.

Thank you,

Leslee Kimbrell Senior Environmental Specialist



Email: <u>lk@resolutecompliance.com</u>

# Submittal of Public Service Announcement – Certification

I, <u>Jeff Jackson</u>, the undersigned, certify that on **May 7, 2024**, submitted a public service announcement to **KZOR FM Station** that serves the town of **Jal**, **Lea** County, New Mexico, in which the source is or is proposed to be located and that **KZOR RESPONDED THAT IT WOULD AIR THE ANNOUNCEMENT.** 

Signed this \_\_\_\_ day of \_\_\_\_\_, \_\_\_\_,

Signature

Date

Jeff Jackson	
Printed Name	

<u>Consultant to Delaware G&P LLC</u> Title {APPLICANT OR RELATIONSHIP TO APPLICANT}

## Written Description of the Routine Operations of the Facility

<u>A written description of the routine operations of the facility</u>. Include a description of how each piece of equipment will be operated, how controls will be used, and the fate of both the products and waste generated. For modifications and/or revisions, explain how the changes will affect the existing process. In a separate paragraph describe the major process bottlenecks that limit production. The purpose of this description is to provide sufficient information about plant operations for the permit writer to determine appropriate emission sources.

The Facility receives natural gas from natural gas wells located in Lea County and adjacent countries through a network of gathering pipelines. The inlet natural gas enters the Facility and is routed to an inlet separator where liquids are separated. The condensate and produced water are routed to one (1) 750 bbl gunbarrel separator (Source ID GB-1). Condensate is then routed to six (6) 400 bbl condensate tanks (Source IDs TK-1, TK-2, TK-3, TK-5, TK-6, TK-7). Produced water is transferred to the two (2) 400 bbl produced water tanks (Source IDs TK-4, TK-8). The condensate and produced water tank emissions are 98% captured by a vapor recovery unit (VRU) which is routed to an enclosed combustor device (ECD) during 5% VRU downtime. Uncaptured emissions are vented from the tanks. Liquids collected in the tanks are periodically transported off-site via truck (Source IDs CONDLOAD and PWLOAD). Emissions from truck loading are routed back to VRU and routed to the ECD during VRU downtime. From the inlet separator, gas is routed to nine (9) compressor engines (Source IDs E-1, E-2, E-4, E-5, E-6, E-7, E-8, E-9, E-10).

The following engine options for Unit E-9 and E-10 are being requested. The worst-case emissions per pollutant are represented in all emission tables.

Unit #	Description HP			
E-9a	Caterpillar G3608 A4	2500		
E-9b	Waukesha P9394GSI S5	2500		
E-10a	Caterpillar G3612 A4	3750		
E-10b	Waukesha 12V275GL	3750		

The compressed gas is routed to two (2) glycol dehydration units (Source IDs DEHY1, DEHY2), which remove water from the gas through contact with glycol. The rich glycol (water saturated) is routed to the reboilers (Source ID H-1, H-2), which heats the glycol and vaporizes water from the stream. The lean glycol is then recycled back to the dehydration units. The dehydration units are equipped with a flash tank and condenser. Flash gas is captured 98% by the VRU with 5% routed to the ECD with a 98% DRE. Uncaptured emissions are vented from the Dehys. Emissions from the regenerator still vent are controlled by a BTEX condenser and remaining gas is controlled by the reboiler glow plug for a total control efficiency of 98%. The dry gas is transported off-site via pipeline.

Two (2) natural gas-fired generator engines (Source IDs GEN-4, GEN-5) supply electricity to the Facility. Additional sources of emissions include fugitive components (Source ID FUG), unpaved road dust (Source ID UR-01), and start-up, shutdown, maintenance operations (Source ID SSM).

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## **Source Determination**

Source submitting under 20.2.70, 20.2.72, 20.2.73, and 20.2.74 NMAC

Sources applying for a construction permit, PSD permit, or operating permit shall evaluate surrounding and/or associated sources (including those sources directly connected to this source for business reasons) and complete this section. Responses to the following questions shall be consistent with the Air Quality Bureau's permitting guidance, <u>Single Source Determination Guidance</u>, which may be found on the Applications Page in the Permitting Section of the Air Quality Bureau website.

Typically, buildings, structures, installations, or facilities that have the same SIC code, that are under common ownership or control, and that are contiguous or adjacent constitute a single stationary source for 20.2.70, 20.2.72, 20.2.73, and 20.2.74 NMAC applicability purposes. Submission of your analysis of these factors in support of the responses below is optional, unless requested by NMED.

#### A. Identify the emission sources evaluated in this section (list and describe):

All sources listed in Table 2-A of this application.

### B. Apply the 3 criteria for determining a single source:

<u>SIC Code</u>: Surrounding or associated sources belong to the same 2-digit industrial grouping (2-digit SIC code) as this facility OR surrounding or associated sources that belong to different 2-digit SIC codes are support facilities for this source.

🛛 Yes 🛛 🗆 No

<u>Common</u> <u>Ownership</u> or <u>Control</u>: Surrounding or associated sources are under common ownership or control as this source.

<u>Contiguous</u> or <u>Adjacent</u>: Surrounding or associated sources are contiguous or adjacent with this source.

□ Yes 🛛 🖾 No

### C. Make a determination:

- ☑ The source, as described in this application, constitutes the entire source for 20.2.70, 20.2.72, 20.2.73, or 20.2.74 NMAC applicability purposes. If in "A" above you evaluated only the source that is the subject of this application, all "YES" boxes should be checked. If in "A" above you evaluated other sources as well, you must check AT LEAST ONE of the boxes "NO" to conclude that the source, as described in the application, is the entire source for 20.2.70, 20.2.72, 20.2.73, and 20.2.74 NMAC applicability purposes.
- The source, as described in this application, <u>does not</u> constitute the entire source for 20.2.70, 20.2.72, 20.2.73, or 20.2.74 NMAC applicability purposes (A permit may be issued for a portion of a source). The entire source consists of the following facilities or emissions sources (list and describe):

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Section 12.A

## **PSD Applicability Determination for All Sources**

(Submitting under 20.2.72, 20.2.74 NMAC)

<u>A PSD applicability determination for all sources</u>. For sources applying for a significant permit revision, apply the applicable requirements of 20.2.74.AG and 20.2.74.200 NMAC and to determine whether this facility is a major or minor PSD source, and whether this modification is a major or a minor PSD modification. It may be helpful to refer to the procedures for Determining the Net Emissions Change at a Source as specified by Table A-5 (Page A.45) of the <u>EPA New Source Review Workshop Manual</u> to determine if the revision is subject to PSD review.

- A. This facility is:
  - □ a minor PSD source before and after this modification (if so, delete C and D below).
  - □ a major PSD source before this modification. This modification will make this a PSD minor source.
  - □ an existing PSD Major Source that has never had a major modification requiring a BACT analysis.
  - □ an existing PSD Major Source that has had a major modification requiring a BACT analysis
  - **a new PSD Major Source after this modification.**

N/A – This application is being submitted under 20.2.70.300.A.(2) NMAC.

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# **Determination of State & Federal Air Quality Regulations**

# This section lists each state and federal air quality regulation that may apply to your facility and/or equipment that are stationary sources of regulated air pollutants.

Not all state and federal air quality regulations are included in this list. Go to the Code of Federal Regulations (CFR) or to the Air Quality Bureau's regulation page to see the full set of air quality regulations.

#### **Required Information for Specific Equipment:**

For regulations that apply to specific source types, in the 'Justification' column **provide any information needed to determine if the regulation does or does not apply**. **For example**, to determine if emissions standards at 40 CFR 60, Subpart IIII apply to your three identical stationary engines, we need to know the construction date as defined in that regulation; the manufacturer date; the date of reconstruction or modification, if any; if they are or are not fire pump engines; if they are or are not emergency engines as defined in that regulation; their site ratings; and the cylinder displacement.

#### Required Information for Regulations that Apply to the Entire Facility:

See instructions in the 'Justification' column for the information that is needed to determine if an 'Entire Facility' type of regulation applies (e.g. 20.2.70 or 20.2.73 NMAC).

#### Regulatory Citations for Regulations That Do Not, but Could Apply:

If there is a state or federal air quality regulation that does not apply, but you have a piece of equipment in a source category for which a regulation has been promulgated, you must **provide the low level regulatory citation showing why your piece of equipment is not subject to or exempt from the regulation. For example** if you have a stationary internal combustion engine that is not subject to 40 CFR 63, Subpart ZZZZ because it is an existing 2 stroke lean burn stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions, your citation would be 40 CFR 63.6590(b)(3)(i). **We don't want a discussion of every non-applicable regulation, but if it is possible a regulation could apply, explain why it does not. For example,** if your facility is a power plant, you do not need to include a citation to show that 40 CFR 60, Subpart OOO does not apply to your non-existent rock crusher.

#### **Regulatory Citations for Emission Standards:**

For each unit that is subject to an emission standard in a source specific regulation, such as 40 CFR 60, Subpart OOO or 40 CFR 63, Subpart HH, include the low level regulatory citation of that emission standard. Emission standards can be numerical emission limits, work practice standards, or other requirements such as maintenance. Here are examples: a glycol dehydrator is subject to the general standards at 63.764C(1)(i) through (iii); an engine is subject to 63.6601, Tables 2a and 2b; a crusher is subject to 60.672(b), Table 3 and all transfer points are subject to 60.672(e)(1)

#### Federally Enforceable Conditions:

All federal regulations are federally enforceable. All Air Quality Bureau State regulations are federally enforceable except for the following: affirmative defense portions at 20.2.7.6.B, 20.2.7.110(B)(15), 20.2.7.11 through 20.2.7.113, 20.2.7.115, and 20.2.7.116; 20.2.37; 20.2.42; 20.2.43; 20.2.62; 20.2.63; 20.2.86; 20.2.89; and 20.2.90 NMAC. Federally enforceable means that EPA can enforce the regulation as well as the Air Quality Bureau and federally enforceable regulations can count toward determining a facility's potential to emit (PTE) for the Title V, PSD, and nonattainment permit regulations.

INCLUDE ANY OTHER INFORMATION NEEDED TO COMPLETE AN APPLICABILITY DETERMINATION OR THAT IS RELEVENT TO YOUR FACILITY'S NOTICE OF INTENT OR PERMIT.

EPA Applicability Determination Index for 40 CFR 60, 61, 63, etc: <u>http://cfpub.epa.gov/adi/</u>

### Example of a Table for State Regulations:

<u>State</u>		Applies?	Unit(s)	Justification:
Regulation	Title	Enter Yes	or Facility	(You may delete instructions or statements that do not apply in
		01110	Tacinty	the justification column to shorten the document.)
20.2.1 NMAC	General Provisions	Yes	Facility	General Provisions apply to Notice of Intent, Construction, and Title V permit applications.
20.2.3 NMAC	Ambient Air Quality Standards	Yes	Facility	20.2.3 NMAC is a State Implementation Plan (SIP) approved regulation that limits the maximum allowable concentration of, Sulfur Compounds, Carbon Monoxide and Nitrogen Dioxide.
	NMAAQS			The TSP NM ambient air quality standard was repealed by the EIB effective November 30, 2018.
20.2.7 NMAC	Excess Emissions	Yes	Facility	This regulation establishes requirements for the facility if operations at the facility result in any excess emissions. The owner or operator will operate the source at the facility having an excess emission, to the extent practicable, including associated air pollution control equipment, in a manner consistent with good air pollution control practices for minimizing emissions. The facility will also notify the NMED of any excess emission per 20.2.7.110 NMAC.
20.2.23 NMAC	Fugitive Dust Control	No	N/A	This regulation does not apply because this application is not for a Notice of Intent.
20.2.33 NMAC	Gas Burning Equipment - Nitrogen Dioxide	No	N/A	This facility does not have gas burning equipment having a heat input of greater than 1,000,000 million British Thermal Units per year per unit; therefore, this regulation does not apply.
20.2.34 NMAC	Oil Burning Equipment: NO <sub>2</sub>	No	N/A	This facility does not have oil burning equipment having a heat input of greater than 1,000,000 million British Thermal Units per year per unit; therefore, this unit does not apply.
20.2.35 NMAC	Natural Gas Processing Plant – Sulfur	No	N/A	This facility does not meet the definition of a natural gas processing plant; therefore, this regulation does not apply.
20.2.37 and 20.2.36 NMAC	Petroleum Processing Facilities and Petroleum Refineries	N/A	N/A	These regulations were repealed by the Environmental Improvement Board. If you had equipment subject to 20.2.37 NMAC before the repeal, your combustion emission sources are now subject to 20.2.61 NMAC.
20.2.38 NMAC	Hydrocarbon Storage Facility	Yes	TK-1 thru TK-8	The storage vessels have a capacity greater than 20,000 gallons; therefore, this regulation is subject.
20.2.39 NMAC	Sulfur Recovery Plant - Sulfur	No	N/A	This facility does not meet the definition of a sulfur recovery plant; therefore, this regulation does not apply.
				This regulation establishes emission standards for volatile organic compounds (VOC) and oxides of nitrogen (NOx) for oil and gas production, processing, compression, and transmission sources. 20.2.50 NMAC subparts below:
			E-1, E-2, E-4 thru E-10	Include the construction status of applicable units as "New", "Existing", "Relocation of Existing", or "Reconstructed" as defined by this Part in your justification:
20.2.50	Oil and Gas Sector – Ozone Precursor	Yes	VRU,	Check the box for the subparts that are applicable: $\boxtimes$ 113 – Engines and Turbines: E-1, E-2, E-4-E-10 are existing, and existing
NMAC Pollutants	FUG,	relocated. GEN-4 and GEN-5 are existing less than 1000 hp $\square$ 114 – Compressor Seals: Reciprocating compressors for E 1 E 2 E 4 E 10		
	DEHY1,	$\boxtimes$ 114 Compressor search reciprocating compressors for E-1, E-2, E-4-E-10		
			DEHY2	⊠116 – Equipment Leaks and Fugitive Emissions: FUG
				□ 117 – Natural Gas Well Liquid Unloading
		98% by the ECD		
		119 – Heaters: H-1 & H-2 are <20 MMBTU/Hr		
				🗆 120 – Hydrocarbon Liquid Transfers

<u>State</u> <u>Regulation</u> Citation	Title	Applies? Enter Yes or No	Unit(s) or Facility	Justification: (You may delete instructions or statements that do not apply in the justification column to shorten the document.)
				<ul> <li>121 – Pig Launching and Receiving</li> <li>122 – Pneumatic Controllers and Pumps</li> <li>123 – Storage Vessels: TK-1 thru TK-8 are existing with a PTE &lt;3tpy</li> <li>124 – Well Workovers</li> <li>125 – Small Business Facilities</li> <li>126 – Produced Water Management Unit</li> <li>127 – Flowback Vessels and Preproduction Operations</li> </ul>
20.2.61.109 NMAC	Smoke & Visible Emissions	Yes	E-1, E-2, E-4 thru E-10 GEN-4, GEN-5, H-1, H-2 ECD-1	This regulation that limits opacity to 20% applies to Stationary Combustion Equipment, such as engines, boilers, heaters, and flares unless your equipment is subject to another state regulation that limits particulate matter such as 20.2.19 NMAC (see 20.2.61.109 NMAC). If equipment at your facility was subject to the repealed regulation 20.2.37 NMAC it is now subject to 20.2.61 NMAC.
20.2.70 NMAC	Operating Permits	Yes	Facility	The facility has the potential to emit more than 100 tpy of carbon monoxide and VOCs; therefore, this regulation is subject.
20.2.71 NMAC	Operating Permit Fees	Yes	Facility	This facility is subject to 20.2.70 NMAC; therefore, this regulation is subject.
20.2.72 NMAC	Construction Permits	Yes	Facility	This facility is subject to 20.2.72 NMAC.
20.2.73 NMAC	NOI & Emissions Inventory Requirements	Yes	Facility	This regulation establishes emission inventory requirements. The facility meets the applicability requirements of 20.2.73.300 NMAC. The facility will meet all applicable reporting requirements under 20.2.73.300.B.1 NMAC.
20.2.74 NMAC	Permits – Prevention of Significant Deterioration (PSD)	No	Facility	This facility is not a PSD source; therefore, this regulation does not apply.
20.2.75 NMAC	Construction Permit Fees	Yes	Facility	This facility is subject to 20.2.72 NMAC; therefore, this regulation applies.
20.2.77 NMAC	New Source Performance	Yes	FUG, E-1, E-2, E-4 through E-10	This regulation establishes state authority to implement new source performance standards (NSPS) for stationary sources, as amended through January 15, 2017. FUG are subject to NSPS OOOOa, and Units E-1, E-2, E-4 through E-10 are subject to NSPS JJJJ.
20.2.78 NMAC	Emission Standards for HAPS	No	N/A	This regulation establishes state authority to implement emission standards for hazardous air pollutants subject to 40 CFR Part 61. This facility does not emit hazardous air pollutants which are subject to the requirements of 40 CFR Part 61 and is therefore not subject to this regulation
20.2.79 NMAC	Permits – Nonattainment Areas	No	Facility	This regulation establishes the requirements for obtaining a nonattainment area permit. The facility is not located in a non-attainment area and therefore is not subject to this regulation.

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<u>State</u> <u>Regulation</u> Citation	Title	Applies? Enter Yes or No	Unit(s) or Facility	Justification: (You may delete instructions or statements that do not apply in the justification column to shorten the document.)
20.2.80 NMAC	Stack Heights	No	N/A	This regulation establishes requirements for the evaluation of stack heights and other dispersion techniques. This regulation does not apply, as all stacks at the facility will follow good engineering practice.
20.2.82 NMAC	MACT Standards for source categories of HAPS	Yes	DEHY1, DEHY2 E-1, E-2, E-4 through E-10, GEN-4, GEN-5	This regulation applies to all sources emitting hazardous air pollutants, which are subject to the requirements of 40 CFR Part 63.

### Example of a Table for Applicable Federal Regulations (Note: This is not an exhaustive list):

Federal Regulation Citation	Title	Applies? Enter Yes or No	Unit(s) or Facility	Justification:
40 CFR 50	NAAQS	Yes	Facility	This regulation defines national ambient air quality standards. The facility meets all applicable national ambient air quality standards for NOx, CO, SO2, H2S, PM10, and PM2.5 under this regulation.
NSPS 40 CFR 60, Subpart A	General Provisions	Yes	E-1, E-2, E-4 through E-10, GEN-4, GEN-5 FUG	<ul> <li>This regulation defines general provisions for relevant standards that have been set under this part. The facility is subject to this regulation because the following subparts apply:</li> <li>Units E-1, E-2, E-4 through E-10, GEN-4, GEN-5 are subject to NSPS JJJJ.</li> <li>Unit FUG is subject to NSPS OOOOa</li> <li>Units E-4 through E-10, FUG, TK-1 through TK-8 are potentially subject to OOOOb.</li> </ul>
NSPS 40 CFR60.40a, Subpart Da	Subpart Da, Performance Standards for Electric Utility Steam Generating Units	No	N/A	There are no electric utility steam generating units located at this facility; therefore, the facility is not subject to this regulation.
NSPS 40 CFR60.40b Subpart Db	Electric Utility Steam Generating Units	No	N/A	There are no electric utility steam generating units located at this facility; therefore, the facility is not subject to this regulation.
40 CFR 60.40c, Subpart Dc	Standards of Performance for Small Industrial- Commercial- Institutional Steam Generating Units	No	N/A	There are no small industrial commercial institutional steam generating units located at this facility; therefore, the facility is not subject to this regulation.

Federal Regulation Citation	Title	Applies? Enter Yes or No	Unit(s) or Facility	Justification:
NSPS 40 CFR 60, Subpart Ka	Standards of Performance for Storage Vessels for Petroleum Liquids for which Construction, Reconstruction, or Modification Commenced After May 18, 1978, and Prior to July 23, 1984	Yes	TK-1 thru TK- 8	Tanks TK-1 through TK-8 have a storage capacity greater than 151,416 liters (40,000 gallons) that are used to store petroleum liquids for which construction commenced after May 18, 1978.
NSPS 40 CFR 60, Subpart Kb	Standards of Performance for Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels) for Which Construction, Reconstruction, or Modification Commenced After July 23, 1984	No	TK-1 thru TK-8	TK-1 through TK-8 were constructed after July 23, 1984 but are not subject because they store "Petroleum (other than crude oil) or condensate stored, processed, and/or treated prior to custody transfer" and are less than 420,000-gal capacity (10,000-bbl) per §60.110b(d)(4).
NSPS 40 CFR 60.330 Subpart GG	Stationary Gas Turbines	No	N/A	There are no turbines located at this facility; therefore, this regulation does not apply.
NSPS 40 CFR 60, Subpart KKK	Leaks of VOC from Onshore Gas Plants	No	N/A	This is not a natural gas processing plant; therefore, this regulation does not apply.
NSPS 40 CFR Part 60 Subpart LLL	Standards of Performance for Onshore Natural Gas Processing: SO <sub>2</sub> Emissions	No	N/A	This is not a natural gas processing plant; therefore, this regulation does not apply.
NSPS 40 CFR 60 Subpart IIII	Standards of performance for Stationary Compression Ignition Internal Combustion Engines	No	N/A	This facility does not have any compression internal combustion engines. Thus, it is not subject to this regulation.
NSPS 40 CFR Part 60 Subpart JJJJ	Standards of Performance for Stationary Spark Ignition Internal Combustion Engines	Yes	E-1, E-2, E-4 through E-10, GEN-4, GEN-5	E-1, E-2, E-4 through E-10, GEN-4, GEN-5 are manufactured after June 12, 2006, and have maximum engine power greater than 500 HP, therefore are subject to this subpart.
NSPS 40 CFR Part 60 Subpart 0000	Standards of Performance for Crude Oil and Natural Gas Production, Transmission, and Distribution for	No	N/A	The facility was constructed after September 18, 2015.

Federal Regulation Citation	Title	Applies? Enter Yes or No	Unit(s) or Facility	Justification:
	which construction, modification or reconstruction commenced after August 23, 2011 and before September 18, 2015			
NSPS 40 CFR Part 60 Subpart OOOOa	Standards of Performance for Crude Oil and Natural Gas Facilities for which Construction, Modification or Reconstruction Commenced After September 18, 2015	Yes	E-1, E-2, E-4 through E-10, FUG	Standards apply to storage vessels constructed, modified or reconstructed after September 18, 2015, with VOC emissions equal to or greater than 6 tons per year (TPY). Storage tank TK-1 through TK-8 VOC emissions are less than 6 TPY. Therefore; the storage tanks are not subject to the requirements of this rule. Reciprocating compressors for E-1, E-2, E-4 through E-10 manufactured after September 18, 2015 will comply with this rule accordingly. Pneumatic controllers installed at the Station after September 18, 2015 will operate at a natural gas bleed rate less than 6 standard cubic feet per hour (SCFH). Delaware G&P will prepare a fugitive monitoring plan and will conduct fugitive monitoring as required by this rule. Additionally, the VRU will comply with 60.5411a.
NSPS 40 CFR Part 60 Subpart OOOOb	Standards of Performance for Crude Oil and Natural Gas Facilities for which Construction, Modification or Reconstruction Commenced After November 15, 2021	Yes	E-4 through E-10, FUG, TK-1 through TK-8	The facility is a natural gas compressor station constructed or modified after November 15, 2021, therefore the compressors associated with E-4 through E- 10, fugitives, and TK-1 through TK-8 are potentially affected sources under this subpart and will comply with all applicable requirements.
NSPS 40 CFR 60 Subpart TTTT	Standards of Performance for Greenhouse Gas Emissions for Electric Generating Units	No	N/A	This facility does not have any steam generating units and is therefore not subject to this regulation.
NSPS 40 CFR 60 Subpart UUUU	Emissions Guidelines for Greenhouse Gas Emissions and Compliance Times for Electric Utility Generating Units	No	N/A	This facility does not operate any sources that are applicable to this subpart.
NSPS 40 CFR 60, Subparts WWW, XXX, Cc, and Cf	Standards of performance for Municipal Solid Waste (MSW) Landfills	No	N/A	This facility is not a municipal solid waste landfill and is therefore not subject to this regulation.
NESHAP 40 CFR 61 Subpart A	General Provisions	No	N/A	This facility is not subject to any subparts of 40 CFR 61.
NESHAP 40 CFR 61 Subpart E	National Emission Standards for <b>Mercury</b>	No	N/A	The provisions of this subpart are applicable to those stationary sources which process mercury ore to recover mercury, use mercury chlor-alkali cells to produce chlorine gas and alkali metal hydroxide, and incinerate or dry wastewater treatment plant sludge

<u>Federal</u> <u>Regulation</u> Citation	Title	Applies? Enter Yes or No	Unit(s) or Facility	Justification:
NESHAP 40 CFR 61 Subpart V	National Emission Standards for <b>Equipment Leaks</b> (Fugitive Emission Sources)	No	N/A	Not applicable as the facility equipment does not operate in VHAP service. VHAP service is a piece of equipment, which contains or encounters a fluid that is at least 10% weight of VHAP. VHAP is a substance regulated under this subpart for which a standard for equipment leaks of VHAPs has been promulgated
MACT 40 CFR 63, Subpart A	General Provisions	Yes	E-1, E-2, E-4 through E-10, GEN-4, GEN-5	Applies if any other Subpart in 40 CFR 63 applies.
MACT 40 CFR 63.760 Subpart HH	Oil and Natural Gas Production Facilities	Yes	DEHY1, DEHY2	The dehydrators (Unit DEHY1, DEHY2) are located at an area source of HAPS and have the potential to emit less than 1 tpy (0.90 megagram per year) of benzene. Therefore, it is subject to the operating and recordkeeping requirements of §63.764(e)(1)(ii).
MACT 40 CFR 63 Subpart HHH		No	N/A	This facility is not a natural gas transmission or storage facility; therefore, this subpart does not apply.
MACT 40 CFR 63 Subpart DDDDD	National Emission Standards for Hazardous Air Pollutants for Major Industrial, Commercial, and Institutional Boilers & Process Heaters	No	N/A	RBL-1 is a process heater that is located at a facility that is not a major source of HAPs; therefore, this subpart will apply.
MACT 40 CFR 63 Subpart UUUUU	National Emission Standards for Hazardous Air Pollutants Coal & Oil Fire Electric Utility Steam Generating Unit	No	N/A	This facility does not contain a coal or oil fire electric utility steam generating units; therefore, this regulation does not apply.
MACT 40 CFR 63 Subpart ZZZZ	National Emissions Standards for Hazardous Air Pollutants for Stationary Reciprocating Internal Combustion Engines (RICE MACT)	Yes	E-1, E-2, E-4 through E-10, GEN-4, GEN-5	E-1, E-2, E-4 through E-10, GEN-4, GEN-5 are stationary internal combustion engines that are operated at an area source of HAPs; therefore, these engines are subject to this subpart.
40 CFR 64	Compliance Assurance Monitoring	No	N/A	This facility is submitting an application pursuant of 20.2.72.200A.(1) NMAC for an NSR permit. Thus, this regulation does not apply.
40 CFR 68	Chemical Accident Prevention	No	Facility	The facility does not have a threshold quantity of a regulated substance in a process, as determined under §68.115; therefore, this regulation is not subject.
Title IV – Acid Rain 40 CFR 72	Acid Rain	No	N/A	This facility is not an acid rain source; therefore, this regulation is not subject.

<u>Federal</u> <u>Regulation</u> Citation	Title	Applies? Enter Yes or No	Unit(s) or Facility	Justification:
Title IV – Acid Rain 40 CFR 73	Sulfur Dioxide Allowance Emissions	No	N/A	This facility is not an acid rain source; therefore, this regulation is not subject.
Title IV-Acid Rain 40 CFR 75	Continuous Emissions Monitoring	No	N/A	This facility does not generate commercial electric power or electric power for sale and is therefore not subject to this regulation.
Title IV – Acid Rain 40 CFR 76	Acid Rain Nitrogen Oxides Emission Reduction Program	No	N/A	This facility is not an acid rain source; therefore, this regulation is not subject.
Title VI – 40 CFR 82	Protection of Stratospheric Ozone	No	N/A	This facility will have appliances containing CFCs. The owner will use only certified technicians for the maintenance, service, repair and disposal of appliances to comply with this regulation.

# **Operational Plan to Mitigate Emissions**

(Submitting under 20.2.70, 20.2.72, 20.2.74 NMAC)

□ Title V Sources (20.2.70 NMAC): By checking this box and certifying this application the permittee certifies that it has developed an <u>Operational Plan to Mitigate Emissions During Startups</u>, <u>Shutdowns</u>, <u>and Emergencies</u> defining the measures to be taken to mitigate source emissions during startups, shutdowns, and emergencies as required by 20.2.70.300.D.5(f) and (g) NMAC. This plan shall be kept on site to be made available to the Department upon request. This plan should not be submitted with this application.

- NSR (20.2.72 NMAC), PSD (20.2.74 NMAC) & Nonattainment (20.2.79 NMAC) Sources: By checking this box and certifying this application the permittee certifies that it has developed an <u>Operational Plan to Mitigate Source Emissions During</u> <u>Malfunction, Startup, or Shutdown</u> defining the measures to be taken to mitigate source emissions during malfunction, startup, or shutdown as required by 20.2.72.203.A.5 NMAC. This plan shall be kept on site to be made available to the Department upon request. This plan should not be submitted with this application.
- ☑ Title V (20.2.70 NMAC), NSR (20.2.72 NMAC), PSD (20.2.74 NMAC) & Nonattainment (20.2.79 NMAC) Sources: By checking this box and certifying this application the permittee certifies that it has established and implemented a Plan to Minimize Emissions During Routine or Predictable Startup, Shutdown, and Scheduled Maintenance through work practice standards and good air pollution control practices as required by 20.2.7.14.A and B NMAC. This plan shall be kept on site or at the nearest field office to be made available to the Department upon request. This plan should not be submitted with this application.

Startup and shutdown procedures are either based on manufacturer's recommendations or based on Delaware G&P's experience with specific equipment. These procedures are designed to proactively address the potential for malfunction to minimize emissions from the facility during events that result in shutdown and subsequent startup.

Equipment located at this facility is equipped with various safety devices and features that aid in the prevention of excess emissions in the event of an operational emergency. If an operational emergency does occur and excess emissions occur, Delaware G&P will submit the required Excess Emissions Report as per 20.2.7 NMAC. Corrective action to eliminate the excess emissions and prevent recurrence in the future will be undertaken as quickly as safety allows.

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# **Alternative Operating Scenarios**

(Submitting under 20.2.70, 20.2.72, 20.2.74 NMAC)

**Alternative Operating Scenarios:** Provide all information required by the department to define alternative operating scenarios. This includes process, material and product changes; facility emissions information; air pollution control equipment requirements; any applicable requirements; monitoring, recordkeeping, and reporting requirements; and compliance certification requirements. Please ensure applicable Tables in this application are clearly marked to show alternative operating scenario.

**Construction Scenarios**: When a permit is modified authorizing new construction to an existing facility, NMED includes a condition to clearly address which permit condition(s) (from the previous permit and the new permit) govern during the interval between the date of issuance of the modification permit and the completion of construction of the modification(s). There are many possible variables that need to be addressed such as: Is simultaneous operation of the old and new units permitted and, if so for example, for how long and under what restraints? In general, these types of requirements will be addressed in Section A100 of the permit, but additional requirements may be added elsewhere. Look in A100 of our NSR and/or TV permit template for sample language dealing with these requirements. Find these permit templates at: <a href="https://www.env.nm.gov/air-quality/permitting-section-procedures-and-guidance/">www.env.nm.gov/air-quality/permitting-section-procedures-and-guidance/</a>. Compliance with standards must be maintained during construction, which should not usually be a problem unless simultaneous operation of old and new equipment is requested.

In this section, under the bolded title "Construction Scenarios", specify any information necessary to write these conditions, such as: conservative-realistic estimated time for completion of construction of the various units, whether simultaneous operation of old and new units is being requested (and, if so, modeled), whether the old units will be removed or decommissioned, any PSD ramifications, any temporary limits requested during phased construction, whether any increase in emissions is being requested as SSM emissions or will instead be handled as a separate Construction Scenario (with corresponding emission limits and conditions, etc.

There are no alternative operating scenarios.

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# Air Dispersion Modeling

- Minor Source Construction (20.2.72 NMAC) and Prevention of Significant Deterioration (PSD) (20.2.74 NMAC) ambient impact analysis (modeling): Provide an ambient impact analysis as required at 20.2.72.203.A(4) and/or 20.2.74.303 NMAC and as outlined in the Air Quality Bureau's Dispersion Modeling Guidelines found on the Planning Section's modeling website. If air dispersion modeling has been waived for one or more pollutants, attach the AQB Modeling Section modeling waiver approval documentation.
- 2) SSM Modeling: Applicants must conduct dispersion modeling for the total short term emissions during routine or predictable startup, shutdown, or maintenance (SSM) using realistic worst case scenarios following guidance from the Air Quality Bureau's dispersion modeling section. Refer to "Guidance for Submittal of Startup, Shutdown, Maintenance Emissions in Permit Applications (<u>http://www.env.nm.gov/aqb/permit/app\_form.html</u>) for more detailed instructions on SSM emissions modeling requirements.
- 3) Title V (20.2.70 NMAC) ambient impact analysis: Title V applications must specify the construction permit and/or Title V Permit number(s) for which air quality dispersion modeling was last approved. Facilities that have only a Title V permit, such as landfills and air curtain incinerators, are subject to the same modeling required for preconstruction permits required by 20.2.72 and 20.2.74 NMAC.

What is the purpose of this application?	Enter an X for each purpose that applies
New PSD major source or PSD major modification (20.2.74 NMAC). See #1 above.	
New Minor Source or significant permit revision under 20.2.72 NMAC (20.2.72.219.D NMAC).	Х
See #1 above. Note: Neither modeling nor a modeling waiver is required for VOC emissions.	
Reporting existing pollutants that were not previously reported.	
Reporting existing pollutants where the ambient impact is being addressed for the first time.	
Title V application (new, renewal, significant, or minor modification. 20.2.70 NMAC). See #3	
above.	
Relocation (20.2.72.202.B.4 or 72.202.D.3.c NMAC)	
Minor Source Technical Permit Revision 20.2.72.219.B.1.d.vi NMAC for like-kind unit replacements.	
Other: i.e. SSM modeling. See #2 above.	
This application does not require modeling since this is a No Permit Required (NPR) application.	
This application does not require modeling since this is a Notice of Intent (NOI) application	
(20.2.73 NMAC).	
This application does not require modeling according to 20.2.70.7.E(11), 20.2.72.203.A(4),	
Guidelines.	

#### Check each box that applies:

- □ See attached, approved modeling **waiver for all** pollutants from the facility.
- See attached, approved modeling **waiver for some** pollutants from the facility.
- Attached in Universal Application Form 4 (UA4) is a **modeling report for all** pollutants from the facility.
- Attached in UA4 is a **modeling report for some** pollutants from the facility.
- □ No modeling is required.
Air Dispersion Modeling Summary for Permit No. 7868

### **Facility Identification:**

Project: Horned Frog Compressor Station Company: Delaware G&P, LLC Permit number: 7868M5 TEMPO ID: 38473

### **Location Information:**

The facility is located 23 miles West of Jal, in Lea County. UTM Coordinates: 633,250.70 m East, 3,550,517.38 m North, zone 13, Datum: NAD83 (32.083086, -103.588061) Elevation = 3,281 feet Air Quality Control Region (AQCR): 155 Airshed: Pr

### **Project Description:**

<u>Brief:</u> Delaware G&P, LLC has applied to the New Mexico Air Quality Bureau for a New Source Review air quality permit for the authorization of the Horned Frog Compressor Station facility (the facility). The facility is a compressor station.

Delaware G&P, LLC seeks to authorize a facility throughput of 120 MMSCFD of natural gas, the operation of two (2) CAT G3516B compressor engines (E-1, E-2), one (1) CAT G3606 A4 (E-4) compressor engine, five (5) Waukesha P9394GSI S5 compressor engines, one (1) CAT G3612 A4 compressor engine, two (2) Aggreko GG0400GASCON glycol reboilers, and one (1) Enclosed Combustion Unit (ECD-1).

The following types of emission sources are included in the project: CAT G3516B, CAT G3606 A4, Waukesha P9394GSI S5, CAT G3612A4, Waukesha 12V275GL, Aggreko GG0400GASCON, and Enclosed Combustion Unit. The emission units used in the modeling are described in the tables below.

For this permit, modeling was required for the following pollutants: Carbon Monoxide (CO), Nitrogen Dioxide (NO<sub>2</sub>), Particulate Matter 10 micrometers or less in aerodynamic diameter (PM<sub>10</sub>), Particulate Matter (2.5 microns or less) (PM<sub>2.5</sub>), and Sulfur Dioxide (SO<sub>2</sub>).

### Table 1. Table of Total Facility Emissions

NO <sub>2</sub> Rate (lbs/hr)	CO Rate (lbs/hr)	SO <sub>2</sub> Rate (lbs/hr)	PM <sub>10</sub> Rate (lbs/hr)	PM <sub>2.5</sub> Rate (lbs/hr)
19.51	24.61	0.83	3.13	2.57

### Table 2. Table of Point Sources

Stack Number	Description	Stack Height (ft)	Diameter (ft)	Velocity (ft/s)	Temperature (°F)	NO <sub>2</sub> Rate (Ibs/hr)	CO Rate (Ibs/hr)	SO <sub>2</sub> Rate (Ibs/hr)	PM <sub>10</sub> Rate (lbs/hr)	PM <sub>2.5</sub> Rate (Ibs/hr)
E-1	1380 hp Caterpillar Compressor Engine	25.00	1.33	109.49	993	1.67	9.46	0.06	0.11	0.11
E-2	1380 hp Caterpillar Compressor Engine	25.00	1.33	109.49	993	1.67	9.46	0.06	0.11	0.11
E-4	1875 hp Caterpillar Compressor Engine	27.25	2.00	63.70	809	2.07	9.09	006	0.12	0.12
E-5	2500 hp Waukesha Compressor Engine	24.50	2.00	55.30	1,066	65.97	33.40	0.09	0.34	0.34
E-6	2500 hp Waukesha Compressor Engine	24.50	2.00	55.30	1,066	65.97	33.40	0.09	0.34	0.34
E-7	2500 hp Waukesha Compressor Engine	24.50	2.00	55.30	1,066	65.97	33.40	0.09	0.34	0.34
E-8	2500 hp Waukesha Compressor Engine	24.50	2.00	55.30	1,066	65.97	33.40	0.09	0.34	0.34
E-9*	2500 hp Compressor Engine	24.50	2.00	55.30	1,066	65.97	33.40	0.09	0.34	0.34
E-10*	3750 hp Compressor Engine	34.92	2.50	88.02	836	2.48	19.84	0.13	0.25	0.25
GEN-4	536 hp Generator Engine	15.00	0.50	205.84	1,000	1.18	2.36	0.02	0.08	0.08
GEN-5	536 hp Generator Engine	15.00	0.50	205.84	1,000	1.18	2.36	0.02	0.08	0.08

H-1	0.5 MMBtu/hr Reboiler	11.20	0.50	12.69	500	0.05	0.04	0.003	0.00	0.00
H-2	1 MMBtu/hr Reboiler	20.00	1.00	6.34	500	0.09	0.08	0.005	0.01	0.01
ECD-1	Enclosed Combustion Device	25.00	4	7.3	800	0.85	0.43	0.0003		

\*Represents worst-case scenario between both engine options.

### **Modeling Assumptions:**

The facility operates continuously all year long, 8760 hours per year.

### Permit Conditions:

The facility has no additional permit conditions derived from these modeling analyses.

### **Conclusion:**

This modeling analysis demonstrates that operation of the facility described in this report neither causes nor contributes to any exceedances of applicable air quality standards. The standards relevant at this facility are NAAQS for CO, NO<sub>2</sub>, PM10, PM2.5, and SO<sub>2</sub>.

<u>Action</u>: The permit can be issued based on this modeling analysis. Modeling report submitted by Resolute Compliance, LLC (dated 5/9/2024).

The air quality analysis demonstrates compliance with applicable regulatory requirements. Model(s) Used: AERMOD VIEW Version 12.0.0 was used to run the modeling analysis.

**Note:** Complete modeling input and output files can be made available and are located in the Modeling Archives in the folder, "7868M5\_Delaware G&P, LLC\_Horned Frog Compressor Station".

### **Modeling Parameters:**

The AERMOD regulatory default parameters were included in assumptions made by the model.

Building downwash produced by buildings at the facility was considered. The following buildings were included in the modeling.

Building Name	Height (m)	Diagonal Length (m)
ТК-1	6.096	3.658
ТК-2	6.096	3.658
ТК-3	6.096	3.658

### Table 3. Table of Buildings

ТК-4	6.096	3.658
ТК-5	6.096	3.658
ТК-6	6.096	3.658
ТК-7	6.096	3.658
ТК-8	6.096	3.658
ТК-9	6.096	3.658
GB-1	7.315	4.755

### **Complex Terrain Data:**

Elevations of receptors, facility sources, and surrounding sources were obtained from USGS GeoTIFF files using AERMAP.

Elevated terrain was used to model the facility.

**<u>Receptor Grid</u>**: The following grids were used to determine the maximum concentration for each pollutant.

### Table 4. Table of Receptors

Grid Type	Description	Shape	Spacing	Radius or Length
Cartesian	Intermediate	Square	1 kilometer	45 kilometers
Cartesian	Intermediate	Square	250 meters	4 kilometers
Cartesian	Fine	Square	100 meters	500 meters
Cartesian	Very fine	Square	50 meters	500 meters

Receptors outside of the radii of impact were discarded for the surrounding source runs.

### Meteorological Data: HOBBS 2017\_2021

<u>Adjacent Sources</u>: The Division 's Modeling Guidance was used to select surrounding sources for NO<sub>2</sub>, CO, SO<sub>2</sub>, PM<sub>10</sub>, and PM<sub>2.5</sub> which were used in the AERMOD modeling analysis. The closest the facility is to another source is 1.12 km from Redhills Unit 16H.

### **PSD Increment Information:**

The facility is a minor source (for PSD purposes) located in AQCR 155. The minor source baseline dates here are 3/16/1988 for NO<sub>2</sub>, 7/28/1978 for SO<sub>2</sub>, 2/20/1979 for PM10, and 11/13/2013 for PM2.5.

The facility is 75 km (via Google Earth) from the Class I area Carlsbad Caverns National Park.

### **Results Discussions:**

### CO Analysis:

The 1-hour CO concentration was below the significance level. No cumulative analysis is

required. The maximum source alone 1-hour CO concentration was  $175.509 \,\mu$ g/m<sup>3</sup>, which occurred 141 m southeast from the center of the facility. This was 8.78% of the NAAQS SIL.

The 8-hour CO concentration was below the significance level. No cumulative analysis is required. The maximum source alone 8-hour CO concentration was 89.55  $\mu$ g/m<sup>3</sup>, which occurred 139 m northeast from the center of the facility. This was 17.91% of the NAAQS SIL.

### NO<sub>2</sub> Analysis:

The conversion of 100% NOX to NO2 was utilized for the analysis.

Compliance with 1-hour NO<sub>2</sub> NAAQS automatically demonstrates compliance with air quality standards of other periods. The 1-hour NOx concentration is above the significance level. The maximum source alone 1-hour NOx concentration was 112.534  $\mu$ g/m<sup>3</sup>, which occurred 143 m west from the center of the facility. A background concentration of 65.8  $\mu$ g/m<sup>3</sup> was added from the monitor 5ZS (ID: 350250008), at 2320 N. Jefferson St., Hobbs NM. A cumulative concentration of 178.33  $\mu$ g/m<sup>3</sup> was 94.01% of the NAAQS<sup>1</sup>.

The maximum source alone 24-hr NO<sub>2</sub> concentration was 32.37  $\mu$ g/m<sup>3</sup>, which occurred 114 m northwest from the center of the facility. This was above the NAAQS SIL of 5  $\mu$ g/m<sup>3</sup> and is significant.

The maximum source alone annual NO<sub>2</sub> concentration was 5.39  $\mu$ g/m<sup>3</sup>, which occurred 114 m northwest from the center of the facility. A background concentration of 9.3  $\mu$ g/m<sup>3</sup> was added from the monitor 5ZS (ID: 350250008), at 2320 N. Jefferson St., Hobbs NM. A cumulative concentration of 14.69  $\mu$ g/m<sup>3</sup> was 14.69% of the NAAQS<sup>1</sup>.

### PM<sub>10</sub> Analysis:

The 24-hour PM10 concentration is above the significance level. A cumulative analysis is required. The maximum source alone annual PM10 concentration was 3.447  $\mu$ g/m<sup>3</sup>, which occurred 141 m southeast from the center of the facility. Surrounding source concentrations were included in the modeling analysis but did not impact the maximum concentration result. A background concentration of 37.3  $\mu$ g/m<sup>3</sup> was added from the monitor 5ZS (ID: 350250008), at 2320 N. Jefferson St., Hobbs NM. A cumulative concentration of 40.74  $\mu$ g/m<sup>3</sup> was 27.16% of the NAAQS<sup>1</sup>.

The annual PM10 concentration was above the significance level. A cumulative analysis is required. The maximum source alone annual PM10 concentration was 0.086  $\mu$ g/m<sup>3</sup>, which occurred 99 m north from the center of the facility. Surrounding source concentrations were included in the modeling analysis but did not impact the maximum concentration result. A background concentration of 24.0  $\mu$ g/m<sup>3</sup> was added from the monitor 5ZS (ID: 350250008), at 2320 N. Jefferson St., Hobbs NM. A cumulative concentration of 24.086  $\mu$ g/m<sup>3</sup> was above the NAAQS SIL of 1  $\mu$ g/m<sup>3</sup> and is significant.

### PM<sub>2.5</sub> Analysis:

The PM2.5 analysis was represented as PM10 as a worst-case scenario.

The maximum total 24-hour PM2.5 concentration was 3.44  $\mu$ g/m<sup>3</sup>, which occurred 141 m southeast the center of the facility. Surrounding source concentrations were included in the modeling analysis but did not impact the maximum concentration result. A background concentration of 16.5  $\mu$ g/m<sup>3</sup> was added from the monitor 5ZS (ID: 350250008), at 2320 N. Jefferson St., Hobbs NM. A cumulative concentration of 19.94  $\mu$ g/m<sup>3</sup> was 56.97% of the NAAQS<sup>1</sup>.

The maximum total annual PM2.5 concentration was 0.086  $\mu$ g/m<sup>3</sup>, which occurred 999 m north from the center of the facility. Surrounding source concentrations were included in the modeling analysis but did not impact the maximum concentration result. A background concentration of 7.1  $\mu$ g/m<sup>3</sup> was added from the monitor 5ZS (ID: 350250008), at 2320 N. Jefferson St., Hobbs NM. A cumulative concentration of 7.186  $\mu$ g/m<sup>3</sup> was 59.88% of the NAAQS<sup>1</sup>.

### SO<sub>2</sub> Analysis:

Compliance with 1-hour SO<sub>2</sub> NAAQS automatically demonstrates compliance with air quality standards of other periods. The 1-hour SO<sub>2</sub> concentration was below the significance level. No cumulative analysis is required. The maximum source alone 1-hour SO<sub>2</sub> concentration was 3.750  $\mu$ g/m<sup>3</sup>, which occurred 143 m west from the center of the facility. This was 48.08% of the NAAQS SIL.

The 3-hour SO<sub>2</sub> concentration was below the significance level. No cumulative analysis is required. The maximum source alone 3-hour SO<sub>2</sub> concentration was 2.754  $\mu$ g/m<sup>3</sup>, which occurred 137 m east from the center of the facility. This was 11.00% of the NAAQS SIL.

The annual SO<sub>2</sub> concentration was below the significance level. No cumulative analysis is required. The maximum source alone annual SO<sub>2</sub> concentration was 0.205  $\mu$ g/m<sup>3</sup>, which occurred 141 m northwest from the center of the facility. This was 20.60% of the NAAQS SIL.

Pollutant	Period	Modeled Facility Concentration (µg/m³)	Modeled Concentration with Surrounding Sources (µg/m³)	Secondary Formation (µg/m³)	Background Concentration (µg/m <sup>3</sup> )	Cumulative Concentration (µg/m <sup>3</sup> )	Standard	Value of Standard (µg/m³)	Percent of Standard	UTM East (m)	UTM North (m)	Elevation (ft)
NO <sub>2</sub>	1-hour	112.53	-	-	65.8	178.33	NAAQS <sup>1</sup>	188	94.86	633103.9	3550522.2	3380.217
NO <sub>2</sub>	24-hour	32.37	-	-	-	32.37	NAAQS SIL	5	647.40	633103.9	3550522.2	3380.217
NO <sub>2</sub>	Annual	5.39	-	-	9.3	14.69	NAAQS <sup>1</sup>	100	14.69	633176.9	3550623.5	3380.446
со	1-hour	175.5	-	-	-	175.5	NAAQS SIL	2000	8.78	633304.6	3550380.1	3372.080
со	8-hour	89.55	-	-	-	89.55	NAAQS SIL	500	17.91	633388.9	3550498.8	3371.457
SO <sub>2</sub>	1-hour	3.75	-	-	_	3.75	NAAQS SIL	7.8	48.08	633103.9	3550522.2	3380.217
SO <sub>2</sub>	3-hour	2.75	-	-	-	2.75	NAAQS SIL	25	11.00	633388.7	3550498.8	3371.457
SO <sub>2</sub>	Annual	0.206	-	-	-	0.206	NAAQS SIL	1	20.60	633176.9	3550623.5	3380.446
PM <sub>10</sub>	24-hour	3.44	3.44	-	37.3	40.74	NAAQS <sup>1</sup>	150	27.16	633304.6	3550380.5	3372.080
PM <sub>10</sub>	Annual	0.086	0.086	-	24	24.086	NAAQS SIL	1	2408.60	633251.0	3551517.0	3392.913
PM <sub>2.5</sub>	24-hour	3.44	3.44	-	16.5	19.94	NAAQS <sup>1</sup>	35	56.97	633304.6	3550380.5	3372.080
PM <sub>2.5</sub>	Annual	0.086	0.086	-	7.1	7.186	NAAQS <sup>1</sup>	12	59.88	633251.0	3551517.0	3392.913

# **Universal Application 4**

# Air Dispersion Modeling Report

Refer to and complete Section 16 of the Universal Application form (UA3) to assist your determination as to whether modeling is required. If, after filling out Section 16, you are still unsure if modeling is required, e-mail the completed Section 16 to the AQB Modeling Manager for assistance in making this determination. If modeling is required, a modeling protocol would be submitted and approved prior to an application submittal. The protocol should be emailed to the modeling manager. A protocol is recommended but optional for minor sources and is required for new PSD sources or PSD major modifications. Fill out and submit this portion of the Universal Application form (UA4), the "Air Dispersion Modeling Report", only if air dispersion modeling is required for this application submittal. This serves as your modeling report submittal and should contain all the information needed to describe the modeling. No other modeling report or modeling protocol should be submitted with this permit application.

16-	16-A: Identification					
1	Name of facility:	Horned Frog Compressor Station				
2	Name of company:	Delaware G&P, LLC				
3	Current Permit number:	GCP No. 7867M5				
4	Name of applicant's modeler:	Jeff Jackson, Resolute Compliance, LLC				
5	Phone number of modeler:	972-842-4304				
6	E-mail of modeler:	jj@resolutecompliance.com				

16	16-B: Brief						
1	Was a modeling protocol submitted and approved?	Yes⊠	No□				
2	Why is the modeling being done?	Adding New Equipment					
3	Additional compression added which will increase emissions beyond GCP limits; existing equipment emissions changes to accommodate increase drive need for modeling site emissions to determine NAAQS compliance in this initial NSR application.						
4	What geodetic datum was used in the modeling? NAD83						
5	How long will the facility be at this location? Permanent Facility						
6	Is the facility a major source with respect to Prevention of Significant Deterioration (PSD)?	Yes	No⊠				

7	Identify the Air Quality Control Region (AQCR) in which the fac	155						
	List the PSD baseline dates for this region (minor or major, as appropriate).							
Q	NO2	March 16, 1988						
0	SO2	July 28, 1978						
	PM10	February 20, 1979						
	PM2.5 November 13, 2013							
	Provide the name and distance to Class I areas within 50 km of the facility (300 km for PSD permits).							
9	There are no Class 1 areas within 50 km of the Horned Frog Compressor Station							
10	Is the facility located in a non-attainment area? If so describe b	pelow	Yes□	No⊠				
Describe any special modeling requirements, such as streamline permit requirements.								
	N/A							

16	16-C: Modeling History of Facility							
	Describe the modeling history of the facility, including the air permit numbers, the pollutants modeled, the National Ambient Air Quality Standards (NAAQS), New Mexico AAQS (NMAAQS), and PSD increments modeled. (Do not include modeling waivers).							
	Pollutant	Latest permit and modification number that modeled the pollutant facility-wide.	Date of Permit	Comments				
	СО	7864M5	4/25/2024	GCP-O&G Permit modeling				
	NO <sub>2</sub>	7864M5		GCP-O&G Permit modeling				
1	SO <sub>2</sub>	7864M5	4/25/2024	GCP-O&G Permit modeling				
	H <sub>2</sub> S	N/A	N/A	N/A				
	PM2.5	7864M5	4/25/2024	GCP-O&G Permit modeling				
	PM10	7864M5	4/25/2024	GCP-O&G Permit modeling				
	Lead	N/A	N/A	Facility has no permitted lead emissions				
	Ozone (PSD only)	N/A	N/A	Not a PSD Permit				
	NM Toxic Air Pollutants (20.2.72.402 NMAC)	N/A	N/A	Facility does not require TAL modeling.				

16-D: Modeling performed for this application										
	For each pollutant, Choose the most co analysis were also p	For each pollutant, indicate the modeling performed and submitted with this application. Choose the most complicated modeling applicable for that pollutant, i.e., culpability analysis assumes ROI and cumulative analysis were also performed.								
1	Pollutant	ROI	Cumulative analysis	Culpability analysis	Waiver approved	Pollutant not emitted or not changed.				
	CO	$\boxtimes$								

	NO <sub>2</sub>	$\boxtimes$	$\boxtimes$		
	SO <sub>2</sub>	$\boxtimes$			
	H <sub>2</sub> S				$\boxtimes$
	PM2.5	$\boxtimes$	$\boxtimes$		
	PM10	$\boxtimes$	$\boxtimes$		
	Lead				$\boxtimes$
	Ozone				$\boxtimes$
	State air toxic(s) (20.2.72.402 NMAC)				

16-	16-E: New Mexico toxic air pollutants modeling									
1	List any New Mexico toxic air pollutants (NMTAPs) from Tables A and B in 20.2.72.502 NMAC that are modeled for this application. N/A The facility does not emit any toxic air pollutants listed in Tables A and B in 20.2.72.502 NMAC.									
	List any NMTAPs that are emitted but not modeled because stack height correction factor. Add additional rows to the table below, if required.									
2	Pollutant	Emission Rate (pounds/hour)	Emission Rate Screening Level (pounds/hour)	Stack Height (meters)	Correction Factor	Emission Rate/ Correction Factor				
	N/A N/A N/A		N/A	N/A	N/A	N/A				

16-	16-F: Modeling options									
	Was the latest version of AERMOD used with regulatory default options? If not explain below.	Yes⊠	No□							
1	<ul> <li>Delaware G&amp;P ran the model in Regulatory Default mode with the following options:</li> <li>the use of stack-tip downwash;</li> </ul>									
<ul> <li>incorporating the effects of simple terrain; and</li> <li>including the calms and missing data processing routines.</li> </ul>										
	To estimate NO2 concentrations, the Ambient Ratio Method 2 (ARM2) was used. As indicated in AERMOD									
	User's Guide Section 3.3.6.3, 0.5 was used for the minimum ambient ratio and 0.9 for the maxim	num ambient rat	10							

16-	16-G: Surrounding source modeling								
1	Date of surroundi	ng source retrieval	Surrounding sources were downloaded from NMED February 23, 2024 for $NO_X$ , $SO_2$ , $PM_{2.5}$ , $PM_{10}$ and were used in cumulative modeling.						
	If the surrounding sources modeled table below to de	If the surrounding source inventory provided by the Air Quality Bureau was believed to be inaccurate, describe how the sources modeled differ from the inventory provided. If changes to the surrounding source inventory were made, use the table below to describe them. Add rows as needed.							
2	AQB Source ID	Description of Corrections							
	N/A	N/A							

16-	16-H: Building and structure downwash										
1	How many buil	dings are pre	sent at the faci	lity?	The follov • I	ollowing structures were included in the modeling scenario: N/A					
2	How many abo at the facility?	ve ground sto	orage tanks are	present	• 5	Six (6) Condensate Ta Fwo (2) Condensate t One (1) Gunbarrel ser	nks anks parator				
3	Was building d	ownwash mo	deled for all bu	uildings and	gs and tanks? If not explain why below.				No□		
4	Building comm	ents			N/A						
16-	I: Recepto	ors and n	nodeled p	propert	y boun	dary					
1	continuous walls, or other continuous barriers approved by the Department, such as rugged physical terrain with a steep grade that would require special equipment to traverse. If a large property is completely enclosed by fencing, a restricted area within the property may be identified with signage only. Public roads cannot be part of a Restricted Area. A Restricted Area is required in order to exclude receptors from the facility property. If the facility does not have a Restricted Area, then receptors shall be placed within the property boundaries of the facility. Describe the fence or other physical barrier at the facility that defines the restricted area.										
	The facility has	installed a pe	erimeter fence	to restrict a	iccess to th	e site.					
2	Receptors mus Are there publi	t be placed al ic roads passi	ong publicly ac ng through the	cessible roa restricted a	ads in the ro area?	estricted area.		Yes□	No⊠		
3	Are restricted a	area boundar	y coordinates in	ncluded in t	he modelir	ng files?		Yes⊠	No□		
	Describe the re	eceptor grids a	and their spaci	ng. The tabl	e below ma	ay be used, adding ro	ws as nee	eded.			
	Grid Type	Shape	Spacing	Start dista restricted center of	ance from area or facility	End distance from restricted area or center of facility	Comme	ents			
	Cartesian	Square	50 meters	0 meters		500 meters					
	Cartesian	Square	100 meters	500 mete	rs	1 km					
	Cartesian	Square	250 meters	1 km		5 km					
4	Cartesian	Square	1 km	5 km		50+ km					
	Cartesian	Circle	50, 100, 250, 500, & 1000 meters	0 meters emissions centroid)	(from						
	Cartesian	Circle	50 meters	0 meters emissions centroid)	(from						
Cartesian Circle 50, 100 meters Centroid											

	Cartesian	Circle	50 meters	0 meters (from emissions centroid)						
Describe receptor spacing along the fence line.										
5	Fence line receptors were placed every 50m.									
	Describe the PSD Class I area receptors.									
6	The closest Class I area is Carlsbad Caverns National Park, but is 75 km from the facility, so no receptors are analyzed there for this study.									

\_\_\_\_\_

16	-J: Mod	eling S	Scenari	os								
1	Identify, define, and describe all modeling scenarios. Examples of modeling scenarios include using different production rates, times of day, times of year, simultaneous or alternate operation of old and new equipment during transition periods, etc. Alternative operating scenarios should correspond to all parts of the Universal Application and should be fully described in Section 15 of the Universal Application (UA3).											
The facility operates 24 hrs per day, 7 days per week and 52 weeks per year. This represents maximum operational (8,760).										ional hours		
2	Which sce	nario prod	uces the h	ighest con	centratior	is? Why?						
2	N/A	N/A										
3	Were emission factor sets used to limit emission rates or hours of operation? (This question pertains to the "SEASON", "MONTH", "HROFDY" and related factor sets, not to the factors used for calculating the maximum emission rate.)											
4	If so, descr (Modify or Sources:	ribe factors duplicate	s for each g table as ne	group of so ecessary. It	ources. Lis t's ok to p	t the sourd ut the tabl	es in each e below se	group befe ection 16-K	ore the facto if it makes fo	r table fo prmattin	or that g g easier	group. .)
	Hour of Day	Factor	Hour of Day	Factor								
	1		13									
	2		14									
	3		15				_					
	4		16									
-	5		17				-					
5	6		18				-					
	/		19									
	8		20									
	9 10		21									
	10		22									
	12		24									
	If hourly, v	variable em	hission rate	es were use	ed that we	ere not des	cribed abo	ove, descril	be them belo	w.	1	I
	,,						-	•				

	N/A		
6	Were different emission rates used for short-term and annual modeling? If so describe below.	Yes□	No⊠

16-	K: NO <sub>2</sub> N	Modeling								
	Which types Check all the	s of NO2 modeling were used? at apply.								
		ARM2								
1	$\boxtimes$	100% NO <sub>x</sub> to NO <sub>2</sub> conversion								
		PVMRM								
		Other:								
	Describe the NO <sub>2</sub> modeling.									
2	The Ambien indicated in maximum a	It Ratio Method 2 (ARM2) technique was used for both the SIL/ROI and NAAQS/increment analyses. As AERMOD User's Guide Section 3.3.6.3, 0.5 was used for the minimum ambient ratio and 0.9 for the mbient ratio.								
3	Were defau describe an	lt NO <sub>2</sub> /NO <sub>x</sub> ratios (0.5 minimum, 0.9 maximum or equilibrium) used? If not d justify the ratios used below.	Yes⊠	No□						
	N/A									
4	Describe the	Describe the design value used for each averaging period modeled.								
	1-hour: High Annual One	ו first high Year Annual Average:								

# **16-L: Ozone Analysis**1NMED has performed a generic analysis that demonstrates sources that are minor with respect to PSD do not cause or<br/>contribute to any violations of ozone NAAQS. The analysis follows.1The basis of the ozone SIL is documented in *Guidance on Significant Impact Levels for Ozone and Fine Particles in the*<br/>*Prevention of Significant Deterioration Permitting Program*, EPA, April 17, 2018 and associated documents. NMED<br/>accepts this SIL basis and incorporates it into this permit record by reference. Complete documentation of the ozone<br/>concentration analysis using MERPS is included in the New Mexico Air Quality Bureau Air Dispersion Modeling Guidelines.2The MERP values presented in Table 10 and Table 11 of the NM AQB Modeling Guidelines that produce the highest<br/>concentrations indicate that facilities emitting no more than 250 tons/year of NOx and no more than 250 tons/year of VOCs<br/>will cause less formation of O3 than the O3 significance level.2 $[O_3]_{8-hourr} = \left(\frac{250 \frac{ton}{yr}}{340_{MERP_NOX}} + \frac{250 \frac{ton}{yr}}{4679_{MERP_VOC}}\right) \times 1.96 \,\mu\text{g/m}^3.$

	Sources that produce ozone concentrations below the ozone SIL do not cause or contribute to air contaminant levels exceeding the ozone NAAQS.								
3	Does the facility emit at least 250 tons per year of NOx or at least 250 tons per year of VOCs? Sources that emit at least 250 tons per year of NOx or at least 250 tons per year of VOCs are covered by the analysis above and require an individual analysis.YesNo								
	For new PSD Major Sources or PSD major modifications, if MERPs were used to account for ozone fill out the information below. If another method was used describe below.								
5	NO <sub>x</sub> (ton/yr)	MERP <sub>NOX</sub>	VOCs (ton/yr)	MERPvoc		[O3]8-hour			
	N/A	N/A	N/A	N/A		N/A	N/A		

16-	16-M: Particulate Matter Modeling										
	Select the pollutants for which plume depletion modeling was used.										
1		PM2.5									
		PM10									
	⊠ None										
_	Describe the	e particle size dist	ributions used.	Include the source of inform	nation.						
N/A											
3	Does the fac tons per yea NO <sub>x</sub> or at lea significant a formation of	ility emit at least ir of SO <sub>2</sub> ? Sources ast 40 tons per ye mounts of precurs f PM2.5.	40 tons per yea that emit at lea ar of SO <sub>2</sub> are co sors and must a	Yes⊠	No□						
4	Was second Horned Frog secondary fo	ary PM modeled f compressor Stat prmation analysis	or PM2.5? ion is not a PSD required.	) major source – no PM2.5	Yes No 🛛						
	If MERPs we below.	re used to accour	nt for secondary	y PM2.5 fill out the informa	tion below. If another method was us	ed describe					
	Pollutant		NO <sub>X</sub>	SO <sub>2</sub>	[PM2.5] <sub>24-hour</sub>						
5	MERPannual		81.98	3.66							
	MERP <sub>24-hour</sub>				[PM2.5] <sub>annual</sub>						
	Emission rat	e (ton/yr)									
				·							

16-	16-N: Setback Distances							
1	Portable sources or sources that need flexibility in their site configuration requires that setback distances be determined between the emission sources and the restricted area boundary (e.g. fence line) for both the initial location and future locations. Describe the setback distances for the initial location.							
	N/A							

Describe the requested, modeled, setback distances for future locations, if this permit is for a portable stationary source.
 Include a haul road in the relocation modeling.
 N/A

16-	16-O: PSD Increment and Source IDs							
1	The unit numbers in t modeling files. Do the numbers if they do no	h the ones in the ween unit	Yes		No□			
	Unit Number in UA-2			Unit Numb	er in Modeling Files			
						-		
2	The emission rates in these match? If not, e	the Tables 2-E and 2 xplain why below.	-F should match the	e ones in the	modeling files. Do	Yes		No□
3	Have the minor NSR e been modeled? N/A	exempt sources or Ti	tle V Insignificant Ac	ctivities" (Tab	ble 2-B) sources	Yes□		No⊠
	Which units consume	increment for which	n pollutants?					
4	Unit ID	NO <sub>2</sub>	SO <sub>2</sub>	PM10		PM2.5		
5	PSD increment description for sources. (for unusual cases, i.e., baseline unit expanded emissions after baseline date).       The facility is located in AQCR 155 which has triggered the Minor Source Baseline Date for NO2 (March 16, 1988), SO2 (July 28, 1978), PM10 (February 20, 1979), and PM2.5 (November 13, 2013).							riggered the 6, 1988), SO2 J PM2.5
6	Are all the actual insta This is necessary to ve increment consumpti	allation dates include erify the accuracy of on status is determin	ed in Table 2A of the PSD increment mod ned for the missing i	e application leling. If not p installation d	form, as required? please explain how ates below.	Yes		No□

16-P: Flare Modeling								
1	For each flare or flaring scena	rio, complete the following						
	Flare ID (and scenario)	Average Molecular Weight	Gross Heat Release (cal/s)	Effective Flare Diameter (m)				
	N/A	N/A						

16-	16-Q: Volume and Related Sources							
1	Were the dimensions of volume sources different from standard dimensions in the Air Quality Bureau (AQB) Modeling Guidelines?	Yes	No□					
	installation dates below.							
	N/A							
	Describe the determination of sigma-Y and sigma-Z for fugitive sources.							

2	N/A
3	Describe how the volume sources are related to unit numbers. Or say they are the same.
	N/A
	Describe any open pits.
4	N/A
5	Describe emission units included in each open pit.
5	N/A

16-	16-R: Background Concentrations								
	Were NMED used below. that was use	Were NMED provided background concentrations used? Identify the background station       used below. If non-NMED provided background concentrations were used describe the data       Yes       No         that was used.       No       No       No       No							
	CO: N/A								
	NO <sub>2</sub> : Outside	Carlsbad (350151005)							
	PM2.5: Hobb	s-Jefferson (350450019)							
1	PM10: Hobbs-Jefferson (350250008)								
	SO <sub>2</sub> : N/A								
	Other:								
	<ul> <li>Consistent with NMED modeling guidance, the 1-hour NO<sub>2</sub> and SO<sub>2</sub> NAAQS modeling did include background concentrations and also included nearby sources. PM<sub>10</sub> NAAQS included a 24-hour background concentration along with nearby sources. The concentration was 100.7 µg/m<sub>3</sub>. The only other pollutant and standards that require an additional monitored background concentration is the PM<sub>2.5</sub> NAAQS. The background concentration was 16.5 µg/m<sub>3</sub> for the 24-hour average and 7.1 µg/m<sub>3</sub> for the annual average.</li> </ul>								
2	Were background concentrations refined to monthly or hourly values? If so describe below. Yes No								

16-S: Meteorological Data							
	Was NMED provided meteorological data used? If so select the station used.						
1	Hobbs	Yes⊠	No□				
2	If NMED provided meteorological data was not used describe the data set(s) used below. Discu handled, how stability class was determined, and how the data were processed.	uss how missing	data were				
	N/A						

16-T: Terrain								
1	Was complex terrain used in the modeling? If not, describe why below.	Yes□	No⊠					

2	What was the source of the terrain data?
2	

NED GEOTIFF

# 16-U: Modeling Files

Describe the modeling files:

	File name (or folder and file name)	Pollutant(s)	Purpose (ROI/SIA, cumulative, culpability analysis, other)
1	HF 1-hr NOX R2	NO2	SIA
	HF Annual NOx	NO2	CIA
	HF 1-hr CO	СО	SIA
1	HF 8-hr CO	СО	SIA
	HF 1-hr SO2	SO2	SIA
	HF 3-hr SO2	SO2	SIA
	HF Annual SO2	SO2	SIA
	HF 24-hr PM10	PM10	CIA
	HF Annual PM10	PM10	CIA
	HF 24-hr PM2	PM2.5	CIA
	HF Annual PM2	PM 2.5	CIA

16-	V: PSD New or Major Modification Applications				
1	A new PSD major source or a major modification to an existing PSD major source requires additional analysis. Was preconstruction monitoring done (see 20.2.74.306 NMAC and PSD Preapplication Guidance on the AQB website)?	Yes□	No⊠		
2	If not, did AQB approve an exemption from preconstruction monitoring?	Yes□	No□		
3	Describe how preconstruction monitoring has been addressed or attach the approved preconstruction monitoring or monitoring exemption.				
	N/A				
Д	Describe the additional impacts analysis required at 20.2.74.304 NMAC.				
	N/A				
5	If required, have ozone and secondary PM2.5 ambient impacts analyses been completed? If so describe below.	Yes□	No⊠		
	N/A				

16-W: Modeling Results												
1	If a req sign des	ambie uired nificai scribe	ent standards are I for the source to nce levels for the below.	e exceeded be o show that th e specific pollu	cause of surroun he contribution f utant. Was culpal	ding sources, a c rom this source i pility analysis per	ulpability ar s less than t formed? If s	ialysis is he Y io	es□	No⊠		
2	lde bel	Identify the maximum concentrations from the modeling analysis. Rows may be modified, added and removed from the table below as necessary.										
Pollutant, Time	Modele Facility	d '	Modeled Concentratio n with	Secondary PM	Background Concentratio	Cumulative	Value of	Percent	Location			
Period and Standard	dand Concentratio dard n (μg/m3)		Surrounding Sources (μg/m3)	ng (μg/m3) n ( ;	n (μg/m3)	n (µg/m3)	Standard (µg/m3)	of Standard	UTM E (m)	UTM N (m)	Elevation (ft)	
NO <sub>2</sub> 1-hr NAAQS <sup>1</sup>	112.53		-	-	65.8	178.33	188	94.86	633103.9	3550522.2	3380.217	
NO <sub>2</sub> 24-hr SIL	32.37		-	-	-	32.37	5	647.40	633103.9 3550522.2 33		3380.217	
NO <sub>2</sub> Annual NAAQS <sup>1</sup>	5.39		-	-	9.3	14.69	100	14.69	633176.9	3550623.5	3380.446	
CO 1-hr SIL	175.5		-	-	-	175.5	2000	8.78	633304.6	3550380.1	3372.080	
CO 8-hr SIL	89.55		-	-	-	89.55	500	17.91	633388.9	3550498.8	3371.457	
SO <sub>2</sub> 1-hr SIL	3.75		-	-	-	3.75	7.8	48.08	633103.9	3550522.2	3380.217	
SO <sub>2</sub> 3-hr SIL	2.75		-	-	-	2.75	25	11.00	633388.7	3550498.8	3371.457	
SO <sub>2</sub> Annual SIL	0.206		-	-	-	0.206	1	20.60	633176.9	3550623.5	3380.446	
PM <sub>10</sub> 24-hr NAAQS <sup>1</sup>	3.44		3.44	-	37.3	40.74	150	27.16	633304.6	3550380.5	3372.080	
PM <sub>10</sub> Annual SIL	0.086		0.086	-	24	24.086	1	2408.60	633251.0	3551517.0	3392.913	
PM <sub>2.5</sub> 24-hr NAAQS <sup>1</sup>	3.44		3.44	-	16.5	19.94	35	56.97	633304.6	3550380.5	3372.080	
PM <sub>2.5</sub> Annual NAAQS <sup>1</sup>	0.086		0.086	-	7.1	7.186	12	59.88	633251.0	3551517.0	3392.913	

16-X: Summary/conclusions				
	A statement that modeling requirements have been satisfied and that the permit can be issued.			
1	The results of the modeling reflect demonstrates the operation of the facility described in this application neither causes or contributes to any exceedances of applicable National Ambient Air Quality Standards. The permit can be issued based on this modeling set.			

# Section 17

# **Compliance Test History**

(Submitting under 20.2.70, 20.2.72, 20.2.74 NMAC)

To show compliance with existing NSR permits conditions, you must submit a compliance test history. The table below provides an example.

Unit No.	Test Description	Test Date
E-1, E-2	Tested in accordance with NSPS JJJJ	1/8/2019
E-1, E-2	Tested in accordance with NSPS JJJJ	1/8/2020
E-1, E-2	Tested in accordance with NSPS JJJJ	1/6/2022
E-4	Tested in accordance with NSPS JJJJ	9/16/2022
E-1, E-2	Tested in accordance with NSPS JJJJ	1/5/2023
E-4	Tested in accordance with NSPS JJJJ	9/14/2023
E-5, E-6	Tested in accordance with NSPS JJJJ	12/19/2023
E-7, E-8	Tested in accordance with NSPS JJJJ	12/20/2023

### **Compliance Test History Table**



### Air Permit Application Compliance History Disclosure Form

Pursuant to Subsection 74-2-7(S) of the New Mexico Air Quality Control Act ("AQCA"), NMSA §§ 74-2-1 to -17, the New Mexico Environment Department ("Department") may deny any permit application or revoke any permit issued pursuant to the AQCA if, within ten years immediately preceding the date of submission of the permit application, the applicant met any one of the criteria outlined below. In order for the Department to deem an air permit application administratively complete, or issue an air permit for those permits without an administrative completeness determination process, the applicant must complete this Compliance History Disclosure Form as specified in Subsection 74-2-7(P). An existing permit holder (permit issued prior to June 18, 2021) shall provide this Compliance History Disclosure Form to the Department upon request.

Permittee/Applicant Company Name			Expected Application Submittal Date			
Delaware G&P, LLC			May 2024			
Permittee/Company Contact		Phone	Email			
Lance Green		225-692-6947	Lance.Green@enlink.com			
Within the 10 years preceding the expected date of submittal of the application, has the permittee or applicant:						
1	Knowingly misrepresented a material fact in an application for a permit?			🗆 Yes 🖂 No		
2	Refused to disclose information required by the provisions of the New Mexico Air Quality Control Act?					
3	Been convicted of a felony related to environmental crime in any court of any state or the United States?					
4	Been convicted of a crime defined by state or federal statute as involving or being in restraint of trade, price fixing, bribery, or fraud in any court of any state or the United States?					
5a	Constructed or operated any facility for which a permit was sought, including the current facility, without the required air quality permit(s) under 20.2.70 NMAC, 20.2.72 NMAC, 20.2.74 NMAC, 20.2.79 NMAC, or 20.2.84 NMAC?					
5b	<ul> <li>If "No" to question 5a, go to question 6.</li> <li>If "Yes" to question 5a, state whether each facility that was constructed or operated without the required air quality permit met at least one of the following exceptions:</li> <li>a. The unpermitted facility was discovered after acquisition during a timely environmental audit that was authorized by the Department; or</li> <li>b. The operator of the facility estimated that the facility's emissions would not require an air permit, and the operator applied for an air permit within 30 calendar days of discovering that an air permit was required for the facility.</li> </ul>					
6	Had any permit revoked or permanently s or the United States?	suspended for cause under th	e environmental laws of any state	🗆 Yes 🔟 No		
7	For each "yes" answer, please provide an	explanation and documentat	ion.			

# Section 22: Certification

Company Name: Delaware G&P, LLC

I, <u>Manish Kumar</u>, hereby certify that the information and data submitted in this application are true and as accurate as possible, to the best of my knowledge and professional expertise and experience.

Signed this <u>May</u> <u>J024</u>, upon my oath or affirmation, before a notary of the State of Texas furnin i'm kumpr Date ONS. DIRECTOR \*Signature Scribed and sworn before me on this Thay of May, 2024. <u>22</u><sup>nd</sup> day of Janvary, 2028. Leanne B. Halfmann Irv's Signature 202-Date **BREANNE B. HALFMANN** Veanne B. Notary Public, State of Texas Comm. Expires 01-22-2028 Notary's Printed Name Notary ID 132324830

\*For Title V applications, the signature must be of the Responsible Official as defined in 20.2.70.7.AE NMAC.