



ENTERPRISE PRODUCTS PARTNERS L.P.
ENTERPRISE PRODUCTS HOLDINGS LLC
(General Partner)

ENTERPRISE PRODUCTS OPERATING LLC

May 10, 2024

Return Receipt Requested

New Mexico Environment Department
Air Quality Bureau
525 Camino de los Marquez, Suite 1
Santa Fe, NM 87505-1816

**Re: Title V Permit No P130-R4 Title V Significant Modification
Enterprise Field Services, LLC – South Carlsbad Compressor Station
Eddy County, New Mexico**

Sir or Madam:

Enterprise Products Operating, LLC (Enterprise) is submitting this Title V significant modification application to the current Title V Permit No. P130-R4 for the South Carlsbad Compressor Station. This application is to account for the modifications under NSR Permit No. 0220-M12, issued on May 16, 2023, and under NSR Permit No. 0220-M12R1, issued on October 30, 2023. In addition to that, this application is to update CAM plan requested by NMED (email dated May, 30, 2023 is included in the application).

Enterprise would like to thank you in advance for your review and concurrence with this submission. If you have questions regarding the information presented in this letter and attachments, please do not hesitate to contact me at (713) 381-5766 or via email at jli@eprod.com or Daniel Bissonnette at (713) 381-3669.

Thank you,
Enterprise Field Services, LLC

A handwritten signature in blue ink that reads "Jing Li".

Jing Li
Staff Environmental Engineer

A handwritten signature in black ink that reads "Daniel Bissonnette".

Daniel Bissonnette
Supervisor, Environmental

/sed
Enclosure

Li, Jing

From: Kuhn, Julia, ENV <Julia.Kuhn@env.nm.gov>
Sent: Tuesday, May 30, 2023 12:30 PM
To: Li, Jing
Cc: Owens, Melinda, ENV
Subject: [EXTERNAL] TV Renewal P130R4 - Enterprise Products Operating, LLC - South Carlsbad Compressor Station

[Use caution with links/attachments]

Good morning, Jing Li,

It just came to our attention that the revised CAM Plan for the dehydrator/Condenser/BTEX Buster is not stringent enough, using only dehy parameters and not control device indicators. AQB will issue the TV Renewal permit in a timely manner, however, the current CAM plan in the TV Renewal P130R4 must be revised once you submit your TV modification to incorporate the recently issued NSR permit 0220M12, within the next year.

Let me know if you have any questions.

Regards,

Julia Kuhn M.S.

Permitting - Major Sources

New Mexico Environmental Department

Air Quality Bureau

525 Camino de los Marquez, Suite 1

Santa Fe, NM 87505

505-629-2893

Julia.Kuhn@env.nm.gov

[https://urldefense.com/v3/__http://www.env.nm.gov__;!!AT8jIA!4LBXOZ_k295lf0LHCU1T6bi95aH-fApfTO6i7D3W275-EdTYHyHdkjEWCHLcbfHDcDVWnpQWge1xLczhNg\\$](https://urldefense.com/v3/__http://www.env.nm.gov__;!!AT8jIA!4LBXOZ_k295lf0LHCU1T6bi95aH-fApfTO6i7D3W275-EdTYHyHdkjEWCHLcbfHDcDVWnpQWge1xLczhNg$)



Air Permit Application Compliance History Disclosure Form

Pursuant to Subsection 74-2-7(S) of the New Mexico Air Quality Control Act (“AQCA”), NMSA §§ 74-2-1 to -17, the New Mexico Environment Department (“Department”) may deny any permit application or revoke any permit issued pursuant to the AQCA if, within ten years immediately preceding the date of submission of the permit application, the applicant met any one of the criteria outlined below. In order for the Department to deem an air permit application administratively complete, or issue an air permit for those permits without an administrative completeness determination process, the applicant must complete this Compliance History Disclosure Form as specified in Subsection 74-2-7(P). An existing permit holder (permit issued prior to June 18, 2021) shall provide this Compliance History Disclosure Form to the Department upon request.

Permittee/Applicant Company Name		Expected Application Submittal Date
Enterprise Field Services, LLC		April 19, 2024
Permittee/Company Contact	Phone	Email
Jing Li	(713) 381-5766	JLi@eprod.com
Within the 10 years preceding the expected date of submittal of the application, has the permittee or applicant:		
1	Knowingly misrepresented a material fact in an application for a permit?	<input type="checkbox"/> Yes <input checked="" type="checkbox"/> No
2	Refused to disclose information required by the provisions of the New Mexico Air Quality Control Act?	<input type="checkbox"/> Yes <input checked="" type="checkbox"/> No
3	Been convicted of a felony related to environmental crime in any court of any state or the United States?	<input type="checkbox"/> Yes <input checked="" type="checkbox"/> No
4	Been convicted of a crime defined by state or federal statute as involving or being in restraint of trade, price fixing, bribery, or fraud in any court of any state or the United States?	<input type="checkbox"/> Yes <input checked="" type="checkbox"/> No
5a	Constructed or operated any facility for which a permit was sought, including the current facility, without the required air quality permit(s) under 20.2.70 NMAC, 20.2.72 NMAC, 20.2.74 NMAC, 20.2.79 NMAC, or 20.2.84 NMAC?	<input type="checkbox"/> Yes <input checked="" type="checkbox"/> No
5b	<p>If “No” to question 5a, go to question 6.</p> <p>If “Yes” to question 5a, state whether each facility that was constructed or operated without the required air quality permit met at least one of the following exceptions:</p> <p>a. The unpermitted facility was discovered after acquisition during a timely environmental audit that was authorized by the Department; or</p> <p>b. The operator of the facility estimated that the facility’s emissions would not require an air permit, and the operator applied for an air permit within 30 calendar days of discovering that an air permit was required for the facility.</p>	<input type="checkbox"/> Yes <input type="checkbox"/> No
6	Had any permit revoked or permanently suspended for cause under the environmental laws of any state or the United States?	<input type="checkbox"/> Yes <input checked="" type="checkbox"/> No
7	For each “yes” answer, please provide an explanation and documentation.	

Mail Application To: New Mexico Environment Department Air Quality Bureau Permits Section 525 Camino de los Marquez, Suite 1 Santa Fe, New Mexico, 87505 Phone: (505) 476-4300 Fax: (505) 476-4375 www.env.nm.gov/aqb		For Department use only:
--	---	---------------------------------

Universal Air Quality Permit Application

Use this application for NOI, NSR, or Title V sources.

Use this application for: the initial application, modifications, technical revisions, and renewals. For technical revisions, complete Sections, 1-A, 1-B, 2-E, 3, 9 and any other sections that are relevant to the requested action; coordination with the Air Quality Bureau permit staff prior to submittal is encouraged to clarify submittal requirements and to determine if more or less than these sections of the application are needed. Use this application for streamline permits as well.

This application is submitted as (check all that apply): Request for a No Permit Required Determination (no fee)
 Updating an application currently under NMED review. Include this page and all pages that are being updated (no fee required).
Construction Status: Not Constructed Existing Permitted (or NOI) Facility Existing Non-permitted (or NOI) Facility
Minor Source: NOI 20.2.73 NMAC 20.2.72 NMAC application or revision 20.2.72.300 NMAC Streamline application
Title V Source: Title V (new) Title V renewal TV minor mod. TV significant mod. TV Acid Rain: New Renewal
PSD Major Source: PSD major source (new) Minor Modification to a PSD source a PSD major modification

Acknowledgements:

- I acknowledge that a pre-application meeting is available to me upon request. Title V Operating, Title IV Acid Rain, and NPR applications have no fees.
- \$500 NSR application Filing Fee enclosed **OR** The full permit fee associated with 10 fee points (required w/ streamline applications).
- Check No.: _____ in the amount of _____.
- I acknowledge the required submittal format for the hard copy application is printed double sided 'head-to-toe', 2-hole punched (except the Sect. 2 landscape tables is printed 'head-to-head'), numbered tab separators. Incl. a copy of the check on a separate page.
- I acknowledge there is an annual fee for permits in addition to the permit review fee: www.env.nm.gov/air-quality/permit-fees-2/.
- This facility qualifies for the small business fee reduction per 20.2.75.11.C. NMAC. The full \$500.00 filing fee is included with this application and I understand the fee reduction will be calculated in the balance due invoice. The Small Business Certification Form has been previously submitted or is included with this application. (Small Business Environmental Assistance Program Information: www.env.nm.gov/air-quality/small-biz-eap-2/.)

Citation: Please provide the **low level citation** under which this application is being submitted: **20.2.70.404.C.(1)(a) NMAC** (e.g. application for a new minor source would be 20.2.72.200.A NMAC, one example for a Technical Permit Revision is 20.2.72.219.B.1.b NMAC, a Title V acid rain application would be: 20.2.70.200.C NMAC)

Section 1 – Facility Information

Section 1-A: Company Information		AI # if known: 218	Updating Permit/NOI #: P130-R4
1	Facility Name: South Carlsbad Compressor Station	Plant primary SIC Code (4 digits): 1311	
		Plant NAIC code (6 digits): 211130	
a	Facility Street Address (If no facility street address, provide directions from a prominent landmark): From Loving, NM follow US-285 north 2.5 miles to Roberson Road West. Follow Roberson Road West 1.0 mile to the facility.		
2	Plant Operator Company Name: Enterprise Products Operating, LLC	Phone/Fax: (713) 381-6595 / (713) 381-6811	
a	Plant Operator Address: PO Box 4324, Houston, TX 77210-4324		

b	Plant Operator's New Mexico Corporate ID or Tax ID: 3289188	
3	Plant Owner(s) name(s): Enterprise Field Services, LLC	Phone/Fax: (713) 381-6500 / (713) 381-6811
a	Plant Owner(s) Mailing Address(s): PO Box 4324, Houston, TX 77210-4324	
4	Bill To (Company): Enterprise Field Services, LLC	Phone/Fax: (713) 381-6595 / (713) 381-6811
a	Mailing Address: PO Box 4324, Houston, TX 77210-4324	E-mail: environmental@eprod.com
5	<input checked="" type="checkbox"/> Preparer: Jing Li <input type="checkbox"/> Consultant:	Phone/Fax: (713) 381-5766 / (713) 759-3931
a	Mailing Address: PO Box 4324, Houston, TX 77210-4324	E-mail: jli@eprod.com
6	Plant Operator Contact: Daryl Arredondo	Phone/Fax: (575) 628-6819
a	Address: PO Box 4324, Houston, TX 77210-4324	E-mail: ddarredondo@eprod.com
7	Air Permit Contact: Jing Li	Title: Senior Environmental Engineer
a	E-mail: jli@eprod.com	Phone/Fax: (713) 381-5766 / (713) 759-3931
b	Mailing Address: PO Box 4324, Houston, TX 77210-4324	
c	The designated Air permit Contact will receive all official correspondence (i.e. letters, permits) from the Air Quality Bureau.	

Section 1-B: Current Facility Status

1.a	Has this facility already been constructed? <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No	1.b If yes to question 1.a, is it currently operating in New Mexico? <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No
2	If yes to question 1.a, was the existing facility subject to a Notice of Intent (NOI) (20.2.73 NMAC) before submittal of this application? <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No	If yes to question 1.a, was the existing facility subject to a construction permit (20.2.72 NMAC) before submittal of this application? <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No
3	Is the facility currently shut down? <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No	If yes, give month and year of shut down (MM/YY): N/A
4	Was this facility constructed before 8/31/1972 and continuously operated since 1972? <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No	
5	If Yes to question 3, has this facility been modified (see 20.2.72.7.P NMAC) or the capacity increased since 8/31/1972? <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No <input type="checkbox"/> N/A	
6	Does this facility have a Title V operating permit (20.2.70 NMAC)? <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No	If yes, the permit No. is: P130-R4
7	Has this facility been issued a No Permit Required (NPR)? <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No	If yes, the NPR No. is: N/A
8	Has this facility been issued a Notice of Intent (NOI)? <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No	If yes, the NOI No. is: N/A
9	Does this facility have a construction permit (20.2.72/20.2.74 NMAC)? <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No	If yes, the permit No. is: 0220-M12R1
10	Is this facility registered under a General permit (GCP-1, GCP-2, etc.)? <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No	If yes, the register No. is: N/A

Section 1-C: Facility Input Capacity & Production Rate

1	What is the facility's maximum input capacity, specify units (reference here and list capacities in Section 20, if more room is required)			
a	Current	Hourly: 8.33 MMscf	Daily: 200 MMscf	Annually: 73 Bscf
b	Proposed	Hourly: 12.5 MMscf	Daily: 300 MMscf	Annually: 109.5 MMscf
2	What is the facility's maximum production rate, specify units (reference here and list capacities in Section 20, if more room is required)			
a	Current	Hourly: 8.33 MMscf	Daily: 200 MMscf	Annually: 73 Bscf
b	Proposed	Hourly: 12.5 MMscf	Daily: 300 MMscf	Annually: 109.5 MMscf

Section 1-D: Facility Location Information

1	Latitude (decimal degrees): 32.313828	Longitude (decimal degrees): -104.137132	County: Eddy	Elevation (ft): 3,065
2	UTM Zone: <input type="checkbox"/> 12 or <input checked="" type="checkbox"/> 13		Datum: <input type="checkbox"/> NAD 83 <input checked="" type="checkbox"/> WGS 84	
a	UTM E (in meters, to nearest 10 meters): 581,225 m E		UTM N (in meters, to nearest 10 meters): 3,575,549 m N	
3	Name and zip code of nearest New Mexico town: Loving, NM 88256			
4	Detailed Driving Instructions from nearest NM town (attach a road map if necessary): From Loving, NM follow US-285 north 2.5 miles to Roberson Road West. Follow Roberson Road West 1.0 mile to the facility.			
5	The facility is 2.8 miles northwest of Loving, NM.			
6	Land Status of facility (check one): <input checked="" type="checkbox"/> Private <input type="checkbox"/> Indian/Pueblo <input type="checkbox"/> Government <input type="checkbox"/> BLM <input type="checkbox"/> Forest Service <input type="checkbox"/> Military			
7	List all municipalities, Indian tribes, and counties within a ten (10) mile radius (20.2.72.203.B.2 NMAC) of the property on which the facility is proposed to be constructed or operated: Municipalities: Carlsbad, Loving, Malaga; Indian Tribes: None; Counties: Eddy			
8	20.2.72 NMAC applications only: Will the property on which the facility is proposed to be constructed or operated be closer than 50 km (31 miles) to other states, Bernalillo County, or a Class I area (see www.env.nm.gov/air-quality/modeling-publications/)? <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No (20.2.72.206.A.7 NMAC) If yes, list all with corresponding distances in kilometers: States: Texas – 34.7 km; Class 1 Areas: Carlsbad Caverns National park – 26.1 km			
9	Name nearest Class I area: Carlsbad Caverns National Park			
10	Shortest distance (in km) from facility boundary to the boundary of the nearest Class I area (to the nearest 10 meters): 26.1 km			
11	Distance (meters) from the perimeter of the Area of Operations (AO is defined as the plant site inclusive of all disturbed lands, including mining overburden removal areas) to nearest residence, school or occupied structure: 582.2 m			
12	Method(s) used to delineate the Restricted Area: Fencing, gates, and signage "Restricted Area" is an area to which public entry is effectively precluded. Effective barriers include continuous fencing, continuous walls, or other continuous barriers approved by the Department, such as rugged physical terrain with steep grade that would require special equipment to traverse. If a large property is completely enclosed by fencing, a restricted area within the property may be identified with signage only. Public roads cannot be part of a Restricted Area.			
13	Does the owner/operator intend to operate this source as a portable stationary source as defined in 20.2.72.7.X NMAC? <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No A portable stationary source is not a mobile source, such as an automobile, but a source that can be installed permanently at one location or that can be re-installed at various locations, such as a hot mix asphalt plant that is moved to different job sites.			
14	Will this facility operate in conjunction with other air regulated parties on the same property? <input checked="" type="checkbox"/> No <input type="checkbox"/> Yes If yes, what is the name and permit number (if known) of the other facility?			

Section 1-E: Proposed Operating Schedule (The 1-E.1 & 1-E.2 operating schedules may become conditions in the permit.)

1	Facility maximum operating ($\frac{\text{hours}}{\text{day}}$): 24	($\frac{\text{days}}{\text{week}}$): 7	($\frac{\text{weeks}}{\text{year}}$): 52	($\frac{\text{hours}}{\text{year}}$): 8760
2	Facility's maximum daily operating schedule (if less than 24 $\frac{\text{hours}}{\text{day}}$)? Start: N/A		<input type="checkbox"/> AM <input type="checkbox"/> PM	End: N/A <input type="checkbox"/> AM <input type="checkbox"/> PM
3	Month and year of anticipated start of construction: Upon receipt of permit.			
4	Month and year of anticipated construction completion: N/A			
5	Month and year of anticipated startup of new or modified facility: N/A			
6	Will this facility operate at this site for more than one year? <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No			

Section 1-F: Other Facility Information

1	Are there any current Notice of Violations (NOV), compliance orders, or any other compliance or enforcement issues related to this facility? <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No If yes, specify: N/A		
a	If yes, NOV date or description of issue: N/A	NOV Tracking No: N/A	
b	Is this application in response to any issue listed in 1-F, 1 or 1a above? <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No If Yes, provide the 1c & 1d info below: N/A		
c	Document Title: N/A	Date: N/A	Requirement # (or page # and paragraph #): N/A
d	Provide the required text to be inserted in this permit: N/A		
2	Is air quality dispersion modeling or modeling waiver being submitted with this application? <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No		
3	Does this facility require an "Air Toxics" permit under 20.2.72.400 NMAC & 20.2.72.502, Tables A and/or B? <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No		
4	Will this facility be a source of federal Hazardous Air Pollutants (HAP)? <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No		
a	If Yes, what type of source? <input type="checkbox"/> Major (<input type="checkbox"/> ≥10 tpy of any single HAP OR <input type="checkbox"/> ≥25 tpy of any combination of HAPS) OR <input checked="" type="checkbox"/> Minor (<input checked="" type="checkbox"/> <10 tpy of any single HAP AND <input checked="" type="checkbox"/> <25 tpy of any combination of HAPS)		
5	Is any unit exempt under 20.2.72.202.B.3 NMAC? <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No		
a	If yes, include the name of company providing commercial electric power to the facility: N/A Commercial power is purchased from a commercial utility company, which specifically does not include power generated on site for the sole purpose of the user.		

Section 1-G: Streamline Application (This section applies to 20.2.72.300 NMAC Streamline applications only)

1	<input type="checkbox"/> I have filled out Section 18, "Addendum for Streamline Applications." <input checked="" type="checkbox"/> N/A (This is not a Streamline application.)
---	--

Section 1-H: Current Title V Information - Required for all applications from TV Sources

(Title V-source required information for all applications submitted pursuant to 20.2.72 NMAC (Minor Construction Permits), or 20.2.74/20.2.79 NMAC (Major PSD/NNSR applications), and/or 20.2.70 NMAC (Title V))

1	Responsible Official (R.O.) (20.2.70.300.D.2 NMAC): Graham Bacon	Phone: (713) 381-6595
a	R.O. Title: Executive Vice President-EHS&T	R.O. e-mail: environmental@eprod.com
b	R. O. Address: PO Box 4324, Houston, TX 77210-4324	
2	Alternate Responsible Official (20.2.70.300.D.2 NMAC): Bradley J. Cooley	Phone: (713) 381-6595
a	A. R.O. Title: Senior Director	A. R.O. e-mail: environmental@eprod.com
b	A. R. O. Address: PO Box 4324, Houston, TX 77210-4324	
3	Company's Corporate or Partnership Relationship to any other Air Quality Permittee (List the names of any companies that have operating (20.2.70 NMAC) permits and with whom the applicant for this permit has a corporate or partnership relationship): Enterprise Field Services, LLC and Enterprise Products Operating, LLC	
4	Name of Parent Company ("Parent Company" means the primary name of the organization that owns the company to be permitted wholly or in part.): 1100 Louisiana St., Houston, TX 77002	
a	Address of Parent Company: N/A	
5	Names of Subsidiary Companies ("Subsidiary Companies" means organizations, branches, divisions or subsidiaries, which are owned, wholly or in part, by the company to be permitted.): N/A	
6	Telephone numbers & names of the owners' agents and site contacts familiar with plant operations: Daryl Arredondo (575) 628-6819 / Jing Li (713) 381-5766 / (713) 759-3931	

7	Affected Programs to include Other States, local air pollution control programs (i.e. Bernalillo) and Indian tribes: Will the property on which the facility is proposed to be constructed or operated be closer than 80 km (50 miles) from other states, local pollution control programs, and Indian tribes and pueblos (20.2.70.402.A.2 and 20.2.70.7.B)? If yes, state which ones and provide the distances in kilometers: (~34.7 km)
---	---

Section 1-I – Submittal Requirements

Each 20.2.73 NMAC (NOI), a 20.2.70 NMAC (Title V), a 20.2.72 NMAC (NSR minor source), or 20.2.74 NMAC (PSD) application package shall consist of the following:

Hard Copy Submittal Requirements:

- 1) One hard copy **original signed and notarized application package printed double sided 'head-to-toe' 2-hole punched** as we bind the document on top, not on the side; except Section 2 (landscape tables), which should be **head-to-head**. Please use **numbered tab separators** in the hard copy submittal(s) as this facilitates the review process. For NOI submittals only, hard copies of UA1, Tables 2A, 2D & 2F, Section 3 and the signed Certification Page are required. **Please include a copy of the check on a separate page.**
- 2) If the application is for a minor NSR, PSD, NNSR, or Title V application, include one working hard **copy** for Department use. This **copy** should be printed in book form, 3-hole punched, and **must be double sided**. Note that this is in addition to the head-to-toe 2-hole punched copy required in 1) above. Minor NSR Technical Permit revisions (20.2.72.219.B NMAC) only need to fill out Sections 1-A, 1-B, 3, and should fill out those portions of other Section(s) relevant to the technical permit revision. TV Minor Modifications need only fill out Sections 1-A, 1-B, 1-H, 3, and those portions of other Section(s) relevant to the minor modification. NMED may require additional portions of the application to be submitted, as needed.
- 3) The entire NOI or Permit application package, including the full modeling study, should be submitted electronically. Electronic files for applications for NOIs, any type of General Construction Permit (GCP), or technical revisions to NSRs must be submitted with compact disk (CD) or digital versatile disc (DVD). For these permit application submittals, **two CD** copies are required (in sleeves, not crystal cases, please), with additional CD copies as specified below. NOI applications require only a **single CD** submittal. Electronic files for other New Source Review (construction) permits/permit modifications or Title V permits/permit modifications can be submitted on CD/DVD or sent through AQB's secure file transfer service.

Electronic files sent by (check one):

CD/DVD attached to paper application

Secure electronic transfer. Air Permit Contact Name: [Jing Li](#), Email: jlj@eprod.com, Phone number: [\(713\) 381-5766](tel:7133815766).

a. If the file transfer service is chosen by the applicant, after receipt of the application, the Bureau will email the applicant with instructions for submitting the electronic files through a secure file transfer service. Submission of the electronic files through the file transfer service needs to be completed within 3 business days after the invitation is received, so the applicant should ensure that the files are ready when sending the hard copy of the application. The applicant will not need a password to complete the transfer. **Do not use the file transfer service for NOIs, any type of GCP, or technical revisions to NSR permits.**

- 4) Optionally, the applicant may submit the files with the application on compact disk (CD) or digital versatile disc (DVD) following the instructions above and the instructions in 5 for applications subject to PSD review.
- 5) If **air dispersion modeling** is required by the application type, include the **NMED Modeling Waiver** and/or electronic air dispersion modeling report, input, and output files. The dispersion modeling **summary report only** should be submitted as hard copy(ies) unless otherwise indicated by the Bureau.
- 6) If the applicant submits the electronic files on CD and the application is subject to PSD review under 20.2.74 NMAC (PSD) or NNSR under 20.2.79 NMAC include,
 - a. one additional CD copy for US EPA,
 - b. one additional CD copy for each federal land manager affected (NPS, USFS, FWS, USDI) and,
 - c. one additional CD copy for each affected regulatory agency other than the Air Quality Bureau.

If the application is submitted electronically through the secure file transfer service, these extra CDs do not need to be submitted.

Electronic Submittal Requirements [in addition to the required hard copy(ies)]:

- 1) All required electronic documents shall be submitted as 2 separate CDs or submitted through the AQB secure file transfer service. Submit a single PDF document of the entire application as submitted and the individual documents comprising the application.
- 2) The documents should also be submitted in Microsoft Office compatible file format (Word, Excel, etc.) allowing us to access the text and formulas in the documents (copy & paste). Any documents that cannot be submitted in a Microsoft Office compatible format shall be saved as a PDF file from within the electronic document that created the file. If you are unable to provide Microsoft office compatible electronic files or internally generated PDF files of files (items that were not created electronically: i.e. brochures, maps, graphics, etc.), submit these items in hard copy format. We must be able to review the formulas and inputs that calculated the emissions.
- 3) It is preferred that this application form be submitted as 4 electronic files (**3 MSWord docs**: Universal Application section 1 [UA1], Universal Application section 3-19 [UA3], and Universal Application 4, the modeling report [UA4]) and **1 Excel file** of the tables (Universal Application section 2 [UA2]). Please include as many of the 3-19 Sections as practical in a single MS Word electronic document. Create separate electronic file(s) if a single file becomes too large or if portions must be saved in a file format other than MS Word.
- 4) The **electronic file names** shall be a maximum of 25 characters long (including spaces, if any). The format of the electronic Universal Application shall be in the format: "A-3423-FacilityName". The "A" distinguishes the file as an application submittal, as opposed to other documents the Department itself puts into the database. Thus, all electronic application submittals should begin with "A-". Modifications to existing facilities should use the **core permit number** (i.e. '3423') the Department assigned to the facility as the next 4 digits. Use 'XXXX' for new facility applications. The format of any separate electronic submittals (additional submittals such as non-Word attachments, re-submittals, application updates) and Section document shall be in the format: "A-3423-9-description", where "9" stands for the **section #** (in this case Section 9-Public Notice). Please refrain, as much as possible, from submitting any scanned documents as this file format is extremely large, which uses up too much storage capacity in our database. Please take the time to fill out the **header information** throughout all submittals as this will identify any loose pages, including the Application Date (date submitted) & Revision number (0 for original, 1, 2, etc.; which will help keep track of subsequent partial update(s) to the original submittal. Do not use special symbols (#, @, etc.) in file names. The footer information should not be modified by the applicant.

Table of Contents

Section 1:	General Facility Information
Section 2:	Tables
Section 3:	Application Summary
Section 4:	Process Flow Sheet
Section 5:	Plot Plan Drawn to Scale
Section 6:	All Calculations
Section 7:	Information Used to Determine Emissions
Section 8:	Map(s)
Section 9:	Proof of Public Notice
Section 10:	Written Description of the Routine Operations of the Facility
Section 11:	Source Determination
Section 12:	PSD Applicability Determination for All Sources & Special Requirements for a PSD Application
Section 13:	Discussion Demonstrating Compliance with Each Applicable State & Federal Regulation
Section 14:	Operational Plan to Mitigate Emissions
Section 15:	Alternative Operating Scenarios
Section 16:	Air Dispersion Modeling
Section 17:	Compliance Test History
Section 18:	Addendum for Streamline Applications (streamline applications only)
Section 19:	Requirements for the Title V (20.2.70 NMAC) Program (Title V applications only)
Section 20:	Other Relevant Information
Section 21:	Addendum for Landfill Applications
Section 22:	Certification Page

Table 2-A: Regulated Emission Sources

Unit and stack numbering must correspond throughout the application package. If applying for a NOI under 20.2.73 NMAC, equipment exemptions under 2.72.202 NMAC do not apply.

Unit Number ¹	Source Description	Make	Model #	Serial #	Manufacturer's Rated Capacity ³ (Specify Units)	Requested Permitted Capacity ³ (Specify Units)	Date of Manufacture ²	Controlled by Unit #	Source Classification Code (SCC)	For Each Piece of Equipment, Check One			RICE Ignition Type (CI, SI, 4SLB, 4SRB, 2SLB) ⁴	Replacing Unit No.
							Date of Construction/Reconstruction ²	Emissions vented to Stack #		<input type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed	<input type="checkbox"/> New/Additional		
1	Natural Gas Turbine	Solar Centaur	T-4702	OHD10-C-7915	4700 hp	4328 hp	9/1/2004	N/A	20200201	<input type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed	N/A	N/A	
	3/24/2010						1	<input type="checkbox"/> New/Additional		<input type="checkbox"/> Replacement Unit	<input checked="" type="checkbox"/> To Be Modified			<input type="checkbox"/> To be Replaced
C9101	Compressor	Solar Centaur	T-4702	OHD10-C-7915	4700 hp	4328 hp	Unknown	N/A	20200201	<input type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed	N/A	N/A	
	< 8/23/2011						N/A	<input type="checkbox"/> New/Additional		<input type="checkbox"/> Replacement Unit	<input checked="" type="checkbox"/> To Be Modified			<input type="checkbox"/> To be Replaced
2	Natural Gas Turbine	Solar Centaur	T-4702	OHE12-C-7057	4700 hp	4328 hp	9/1/2004	N/A	20200201	<input checked="" type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed	N/A	N/A	
	8/31/2013						2	<input type="checkbox"/> New/Additional		<input type="checkbox"/> Replacement Unit	<input type="checkbox"/> To Be Modified			<input type="checkbox"/> To be Replaced
C9102	Compressor	Solar Centaur	T-4702	OHE12-C-7057	4700 hp	4328 hp	Unknown	N/A	20200201	<input checked="" type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed	N/A	N/A	
	< 8/23/2011						N/A	<input type="checkbox"/> New/Additional		<input type="checkbox"/> Replacement Unit	<input type="checkbox"/> To Be Modified			<input type="checkbox"/> To be Replaced
5	Natural Gas Turbine	Solar Centaur	T40-4700S	OHL20-C1803	4700 hp	4329 hp	12/18/2000	N/A	20200201	<input checked="" type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed	N/A	N/A	
	< 8/23/2011						N/A	<input type="checkbox"/> New/Additional		<input type="checkbox"/> Replacement Unit	<input type="checkbox"/> To Be Modified			<input type="checkbox"/> To be Replaced
C9103	Compressor	Solar Centaur	T40-4700S	OHL20-C1803	4700 hp	4329 hp	N/A	N/A	20200201	<input checked="" type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed	N/A	N/A	
	N/A						N/A	<input type="checkbox"/> New/Additional		<input type="checkbox"/> Replacement Unit	<input type="checkbox"/> To Be Modified			<input type="checkbox"/> To be Replaced
6	Compressor Engine	Caterpillar	G3608A4	XH701915	2500 hp	2500 hp	TBD	CAT-6	20200254	<input type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed	4SLB	N/A	
	TBD						6	<input checked="" type="checkbox"/> New/Additional		<input type="checkbox"/> Replacement Unit	<input type="checkbox"/> To Be Modified			<input type="checkbox"/> To be Replaced
7	Compressor Engine	Caterpillar	G3608A4	XH701920	2500 hp	2500 hp	TBD	CAT-7	20200254	<input type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed	4SLB	N/A	
	TBD						7	<input checked="" type="checkbox"/> New/Additional		<input type="checkbox"/> Replacement Unit	<input type="checkbox"/> To Be Modified			<input type="checkbox"/> To be Replaced
8	Compressor Engine	Caterpillar	G3608A4	XH701923	2500 hp	2500 hp	TBD	CAT-8	20200254	<input type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed	4SLB	N/A	
	TBD						8	<input checked="" type="checkbox"/> New/Additional		<input type="checkbox"/> Replacement Unit	<input type="checkbox"/> To Be Modified			<input type="checkbox"/> To be Replaced
9	Compressor Engine	Caterpillar	G3608A4	TBD	2500 hp	2500 hp	TBD	CAT-9	20200254	<input type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed	4SLB	N/A	
	TBD						9	<input checked="" type="checkbox"/> New/Additional		<input type="checkbox"/> Replacement Unit	<input type="checkbox"/> To Be Modified			<input type="checkbox"/> To be Replaced
10	Compressor Engine	Caterpillar	G3608A4	TBD	2500 hp	2500 hp	TBD	CAT-10	20200254	<input type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed	4SLB	N/A	
	TBD						10	<input checked="" type="checkbox"/> New/Additional		<input type="checkbox"/> Replacement Unit	<input type="checkbox"/> To Be Modified			<input type="checkbox"/> To be Replaced
3a	Glycol Dehydrator Still Vent	Gas Tech	Unknown	Unknown	200 MMscf/day	200 MMscf/day	1/1/1999	3a	31000302	<input type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed	N/A	N/A	
	Unknown						3b	<input type="checkbox"/> New/Additional		<input type="checkbox"/> Replacement Unit	<input checked="" type="checkbox"/> To Be Modified			<input type="checkbox"/> To be Replaced
3b	Glycol Dehydrator Reboiler	Gas Tech	Unknown	Unknown	3.0 MMBtu/hr	3.0 MMBtu/hr	1/1/1999	3b	31000302	<input type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed	N/A	N/A	
	Unknown						3b	<input type="checkbox"/> New/Additional		<input type="checkbox"/> Replacement Unit	<input checked="" type="checkbox"/> To Be Modified			<input type="checkbox"/> To be Replaced
T-007	Slop Tank	Unknown	Unknown	N/A	400 bbl	400 bbl	2023	N/A	40400315	<input type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed	N/A	N/A	
	Unknown						N/A	<input checked="" type="checkbox"/> New/Additional		<input type="checkbox"/> Replacement Unit	<input type="checkbox"/> To Be Modified			<input type="checkbox"/> To be Replaced
T-008	Stabilized Condensate Tank	Unknown	Unknown	N/A	300 bbl	300 bbl	2013	N/A	40400311	<input checked="" type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed	N/A	N/A	
	Unknown						N/A	<input type="checkbox"/> New/Additional		<input type="checkbox"/> Replacement Unit	<input type="checkbox"/> To Be Modified			<input type="checkbox"/> To be Replaced

Table 2-A: Regulated Emission Sources

Unit and stack numbering must correspond throughout the application package. If applying for a NOI under 20.2.73 NMAC, equipment exemptions under 2.72.202 NMAC do not apply.

Unit Number ¹	Source Description	Make	Model #	Serial #	Manufacturer's Rated Capacity ³ (Specify Units)	Requested Permitted Capacity ³ (Specify Units)	Date of Manufacture ²	Controlled by Unit #	Source Classification Code (SCC)	For Each Piece of Equipment, Check One			RICE Ignition Type (CI, SI, 4SLB, 4SRB, 2SLB) ⁴	Replacing Unit No.
							Date of Construction/Reconstruction ²	Emissions vented to Stack #		<input type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed	<input type="checkbox"/> New/Additional		
T-009	Stabilized Condensate Tank	Unknown	Unknown	N/A	300 bbl	300 bbl	< 8/23/2011	N/A	40400311	<input checked="" type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed	N/A	N/A	
							< 8/23/2011	N/A		<input type="checkbox"/> New/Additional	<input type="checkbox"/> Replacement Unit			<input type="checkbox"/> To Be Modified
T-011	Stabilized Condensate Tank	Unknown	Unknown	N/A	300 bbl	300 bbl	12/1/2006	N/A	40400311	<input checked="" type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed	N/A	N/A	
							Unknown	N/A		<input type="checkbox"/> New/Additional	<input type="checkbox"/> Replacement Unit			<input type="checkbox"/> To Be Modified
T-012	Stabilized Condensate Tank	Unknown	Unknown	N/A	300 bbl	300 bbl	12/1/2006	N/A	40400311	<input checked="" type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed	N/A	N/A	
							Unknown	N/A		<input type="checkbox"/> New/Additional	<input type="checkbox"/> Replacement Unit			<input type="checkbox"/> To Be Modified
ECD	Enclosed Combustion Device	SpiralX	TBD	TBD	6.50 MMscf/yr	6.50 MMscf/yr	TBD	N/A	30600904	<input type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed	N/A	N/A	
							TBD	ECD		<input checked="" type="checkbox"/> New/Additional	<input type="checkbox"/> Replacement Unit			<input type="checkbox"/> To Be Modified
Flare	Process Flare	Unknown	Unknown	N/A	72 Mscf/hr	72 Mscf/hr	Unknown	N/A	31000215	<input type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed	N/A	N/A	
							12/1/2006	Flare		<input checked="" type="checkbox"/> To Be Modified	<input type="checkbox"/> To be Replaced			
VENT (SSM)	Vent for Startup, Shutdown and Blowdown	N/A	N/A	N/A	N/A	N/A	Unknown	N/A	31000299	<input checked="" type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed	N/A	N/A	
							Unknown	N/A		<input type="checkbox"/> New/Additional	<input type="checkbox"/> Replacement Unit			<input type="checkbox"/> To Be Modified
F-001	Fugitives	N/A	N/A	N/A	N/A	N/A	N/A	N/A	31088811	<input type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed	N/A	N/A	
							N/A	N/A		<input checked="" type="checkbox"/> To Be Modified	<input type="checkbox"/> To be Replaced			
Flare (SSM)	SSM Flare	N/A	N/A	N/A	N/A	N/A	N/A	N/A	31000215	<input checked="" type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed	N/A	N/A	
							N/A	N/A		<input type="checkbox"/> New/Additional	<input type="checkbox"/> Replacement Unit			<input type="checkbox"/> To Be Modified
LOAD	Truck Loading Emission	N/A	N/A	N/A	69,350 bbl/yr	69,350 bbl/yr	N/A	N/A	31000199	<input checked="" type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed	N/A	N/A	
							N/A	N/A		<input type="checkbox"/> New/Additional	<input type="checkbox"/> Replacement Unit			<input type="checkbox"/> To Be Modified
Haul	Haul Road Emission	N/A	N/A	N/A	N/A	N/A	N/A	N/A	31088811	<input checked="" type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed	N/A	N/A	
							N/A	N/A		<input type="checkbox"/> New/Additional	<input type="checkbox"/> Replacement Unit			<input type="checkbox"/> To Be Modified
MALF	Malfunction Emissions	N/A	N/A	N/A	N/A	N/A	N/A	N/A	31088811	<input type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed	N/A	N/A	
							N/A	N/A		<input checked="" type="checkbox"/> To Be Modified	<input type="checkbox"/> To be Replaced			

¹ Unit numbers must correspond to unit numbers in the previous permit unless a complete cross reference table of all units in both permits is provided.

² Specify dates required to determine regulatory applicability.

³ To properly account for power conversion efficiencies, generator set rated capacity shall be reported as the rated capacity of the engine in horsepower, not the kilowatt capacity of the generator set.

⁴ "4SLB" means four stroke lean burn engine, "4SRB" means four stroke rich burn engine, "2SLB" means two stroke lean burn engine, "CI" means compression ignition, and "SI" means spark ignition

Table 2-B: Insignificant Activities¹ (20.2.70 NMAC) OR Exempted Equipment (20.2.72 NMAC)

All 20.2.70 NMAC (Title V) applications must list all Insignificant Activities in this table. All 20.2.72 NMAC applications must list Exempted Equipment in this table. If equipment listed on this table is exempt under 20.2.72.202.B.5, include emissions calculations and emissions totals for 202.B.5 "similar functions" units, operations, and activities in Section 6, Calculations. Equipment and activities exempted under 20.2.72.202 NMAC may not necessarily be Insignificant under 20.2.70 NMAC (and vice versa). Unit & stack numbering must be consistent throughout the application package. Per Exemptions Policy 02-012.00 (see http://www.env.nm.gov/aqb/permit/aqb_pol.html), 20.2.72.202.B NMAC Exemptions do not apply, but 20.2.72.202.A NMAC exemptions do apply to NOI facilities under 20.2.73 NMAC. List 20.2.72.301.D.4 NMAC Auxiliary Equipment for Streamline applications in Table 2-A. The List of Insignificant Activities (for TV) can be found online at <https://www.env.nm.gov/wp-content/uploads/sites/2/2017/10/InsignificantListTitleV.pdf>. TV sources may elect to enter both TV Insignificant Activities and Part 72 Exemptions on this form.

Unit Number	Source Description	Manufacturer	Model No.	Max Capacity	List Specific 20.2.72.202 NMAC Exemption (e.g. 20.2.72.202.B.5)	Date of Manufacture /Reconstruction ²	For Each Piece of Equipment, Check One	
			Serial No.	Capacity Units	Insignificant Activity citation (e.g. IA List Item #1.a)	Date of Installation /Construction ²		
T-001	Lube Oil Tank	N/A	N/A	24	20.2.72.202.B(2)(a) NMAC	Unknown	<input checked="" type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed
			N/A	bbl	IA List Item #5	Unknown	<input type="checkbox"/> New/Additional	<input type="checkbox"/> Replacement Unit
T-002	Methanol Tank	N/A	N/A	210	20.2.72.202.B(2)(a) NMAC	Unknown	<input checked="" type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed
			N/A	bbl	IA List Item #5	Unknown	<input type="checkbox"/> New/Additional	<input type="checkbox"/> Replacement Unit
T-003	Triethylene Glycol Tank	N/A	N/A	210	20.2.72.202.B(2)(a) NMAC	Unknown	<input checked="" type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed
			N/A	bbl	IA List Item #5	Unknown	<input type="checkbox"/> New/Additional	<input type="checkbox"/> Replacement Unit
T-004	Used Oil Tank	N/A	N/A	210	20.2.72.202.B(2)(a) NMAC	Unknown	<input checked="" type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed
			N/A	bbl	IA List Item #5	Unknown	<input type="checkbox"/> New/Additional	<input type="checkbox"/> Replacement Unit
T-005	Used Oil Tank	N/A	N/A	210	20.2.72.202.B(2)(a) NMAC	Unknown	<input checked="" type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed
			N/A	bbl	IA List Item #5	Unknown	<input type="checkbox"/> New/Additional	<input type="checkbox"/> Replacement Unit
T-006	Slop Tank	N/A	N/A	TBD	20.2.72.202.B(5) NMAC	N/A	<input checked="" type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed
			N/A	TBD	IA List Item #1.a.	N/A	<input type="checkbox"/> New/Additional	<input type="checkbox"/> Replacement Unit
LOAD_SLOP	Slop Tank	N/A	N/A	TBD	20.2.72.202.B(5) NMAC	N/A	<input type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed
			N/A	TBD	IA List Item #1.a.	N/A	<input checked="" type="checkbox"/> New/Additional	<input type="checkbox"/> Replacement Unit
Unload	Chemical Unloading	N/A	N/A	TBD	20.2.72.202.B(5) NMAC	N/A	<input checked="" type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed
			N/A	TBD	IA List Item #1.a.	N/A	<input type="checkbox"/> New/Additional	<input type="checkbox"/> Replacement Unit
GC-1	Gas Chromatograph	Daniel	700	350	20.2.72.202.B(5) NMAC	Unknown	<input checked="" type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed
			Unknown	cc/min	IA List Item #1.a.	Unknown	<input type="checkbox"/> New/Additional	<input type="checkbox"/> Replacement Unit
GC-2	Gas Chromatograph	ABB	NGC 8206	820	20.2.72.202.B(5) NMAC	Unknown	<input checked="" type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed
			Unknown	cc/min	IA List Item #1.a.	Unknown	<input type="checkbox"/> New/Additional	<input type="checkbox"/> Replacement Unit
Pigging	Pig Receiver and Launcher Emissions	N/A	N/A	280	20.2.72.202.B(5) NMAC	TBD	<input checked="" type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed
			N/A	scf/event	Insignificant Activity #1a	TBD	<input type="checkbox"/> New/Additional	<input type="checkbox"/> Replacement Unit
							<input type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed
							<input type="checkbox"/> New/Additional	<input type="checkbox"/> Replacement Unit
							<input type="checkbox"/> To Be Modified	<input type="checkbox"/> To be Replaced
							<input type="checkbox"/> Existing (unchanged)	<input type="checkbox"/> To be Removed
							<input type="checkbox"/> New/Additional	<input type="checkbox"/> Replacement Unit
							<input type="checkbox"/> To Be Modified	<input type="checkbox"/> To be Replaced

¹ Insignificant activities exempted due to size or production rate are defined in 20.2.70.300.D.6, 20.2.70.7.Q NMAC, and the NMED/AQB List of Insignificant Activities, dated September 15, 2008. Emissions from these insignificant activities do not need to be reported, unless specifically requested.

² Specify date(s) required to determine regulatory applicability.

Table 2-D: Maximum Emissions (under normal operating conditions)

This Table was intentionally left blank because it would be identical to Table 2-E.

Maximum Emissions are the emissions at maximum capacity and prior to (in the absence of) pollution control, emission-reducing process equipment, or any other emission reduction. Calculate the hourly emissions using the worst case hourly emissions for each pollutant. For each pollutant, calculate the annual emissions as if the facility were operating at maximum plant capacity without pollution controls for 8760 hours per year, unless otherwise approved by the Department. List Hazardous Air Pollutants (HAP) & Toxic Air Pollutants (TAPs) in Table 2-I. Unit & stack numbering must be consistent throughout the application package. Fill all cells in this table with the emission numbers or a "-" symbol. A "-" symbol indicates that emissions of this pollutant are not expected. Numbers shall be expressed to at least 2 decimal points (e.g. 0.41, 1.41, or 1.41E-4).

Unit No.	NOx		CO		VOC		SOx		PM ¹		PM10 ¹		PM2.5 ¹		H ₂ S		Lead	
	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
1	27.00	90.82	7.40	11.25	0.77	3.37	0.50	2.21	0.63	2.78	0.63	2.78	0.63	2.78	2.52E-04	1.10E-03	-	-
2	27.00	90.82	7.40	11.25	0.77	3.37	0.50	2.21	0.63	2.78	0.63	2.78	0.63	2.78	2.52E-04	1.10E-03	-	-
5	4.43	19.40	5.89	25.78	1.40	6.15	0.48	2.10	0.27	1.16	0.27	1.16	0.27	1.16	2.39E-04	1.05E-03	-	-
6	1.65	7.24	13.78	60.35	1.49	6.52	0.27	1.17	0.17	0.75	0.17	0.75	0.17	0.75	1.34E-04	5.88E-04	-	-
7	1.65	7.24	13.78	60.35	1.49	6.52	0.27	1.17	0.17	0.75	0.17	0.75	0.17	0.75	1.34E-04	5.88E-04	-	-
8	1.65	7.24	13.78	60.35	1.49	6.52	0.27	1.17	0.17	0.75	0.17	0.75	0.17	0.75	1.34E-04	5.88E-04	-	-
9	1.65	7.24	13.78	60.35	1.49	6.52	0.27	1.17	0.17	0.75	0.17	0.75	0.17	0.75	1.34E-04	5.88E-04	-	-
10	1.65	7.24	13.78	60.35	1.49	6.52	0.27	1.17	0.17	0.75	0.17	0.75	0.17	0.75	1.34E-04	5.88E-04	-	-
3a	-	-	-	-	73.65	322.57	-	-	-	-	-	-	-	-	0.041	0.18	-	-
3b	0.29	1.29	0.25	1.08	0.016	0.071	0.036	0.16	0.022	0.098	0.022	0.098	0.022	0.098	8.93E-04	3.91E-03	-	-
T-007	-	-	-	-	*	0.67	-	-	-	-	-	-	-	-	-	-	-	-
T-008	-	-	-	-	*	18.85	-	-	-	-	-	-	-	-	-	-	-	-
T-009																		
T-011																		
T-012																		
F-001	-	-	-	-	*	44.88	-	-	-	-	-	-	-	-	-	-	-	-
LOAD	-	-	-	-	*	9.82	-	-	-	-	-	-	-	-	-	-	-	-
ECD	0.012	0.052	9.88E-03	0.043	-	-	6.59E-05	2.89E-04	-	-	-	-	-	-	3.50E-05	1.53E-04	-	-
Flare (Process)	7.79	2.82	62.84	22.65	61.88	22.28	0.11	0.46	-	-	-	-	-	-	0.056	0.020	-	-
MALF	15.52	6.00	125.32	10.00	138.01	10.00	0.11	10.00	-	-	-	-	-	-	0.056	2.00	-	-
Totals	90.31	247.41	277.99	383.81	283.93	474.63	3.07	22.99	2.41	10.57	2.41	10.57	2.41	10.57	0.16	2.21	-	-

¹Condensable Particulate Matter: Include condensable particulate matter emissions for PM10 and PM2.5 if the source is a combustion source. Do not include condensable particulate matter for PM unless PM is set equal to PM10 and PM2.5. Particulate matter (PM) is not subject to an ambient air quality standard, but PM is a regulated air pollutant under PSD (20.2.74 NMAC) and Title V (20.2.70 NMAC).

Table 2-E: Requested Allowable Emissions

Unit & stack numbering must be consistent throughout the application package. Fill all cells in this table with the emission numbers or a "-" symbol. A "--" symbol indicates that emissions of this pollutant are not expected. Numbers shall be expressed to at least 2 decimal points (e.g. 0.41, 1.41, or 1.41E⁻⁴).

Unit No.	NOx		CO		VOC		SOx		PM ¹		PM10 ¹		PM2.5 ¹		H ₂ S		Lead	
	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
1	27.00	90.82	7.40	11.25	0.77	3.37	0.50	2.21	0.63	2.78	0.63	2.78	0.63	2.78	2.52E-04	1.10E-03	-	-
2	27.00	90.82	7.40	11.25	0.77	3.37	0.50	2.21	0.63	2.78	0.63	2.78	0.63	2.78	2.52E-04	1.10E-03	-	-
5	4.43	19.40	5.89	25.78	1.40	6.15	0.48	2.10	0.27	1.16	0.27	1.16	0.27	1.16	2.39E-04	1.05E-03	-	-
6	1.65	7.24	3.31	14.48	3.86	16.90	0.27	1.17	0.17	0.75	0.17	0.75	0.17	0.75	1.34E-04	5.88E-04	-	-
7	1.65	7.24	3.31	14.48	3.86	16.90	0.27	1.17	0.17	0.75	0.17	0.75	0.17	0.75	1.34E-04	5.88E-04	-	-
8	1.65	7.24	3.31	14.48	3.86	16.90	0.27	1.17	0.17	0.75	0.17	0.75	0.17	0.75	1.34E-04	5.88E-04	-	-
9	1.65	7.24	3.31	14.48	3.86	16.90	0.27	1.17	0.17	0.75	0.17	0.75	0.17	0.75	1.34E-04	5.88E-04	-	-
10	1.65	7.24	3.31	14.48	3.86	16.90	0.27	1.17	0.17	0.75	0.17	0.75	0.17	0.75	1.34E-04	5.88E-04	-	-
3a	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
3b	0.29	1.29	0.25	1.08	0.016	0.071	0.036	0.16	0.022	0.098	0.022	0.098	0.022	0.098	8.93E-04	3.91E-03	-	-
T-007	-	-	-	-	*	0.67	-	-	-	-	-	-	-	-	-	-	-	-
T-008	-	-	-	-	*	18.85	-	-	-	-	-	-	-	-	-	-	-	-
T-009																		
T-011																		
T-012																		
F-001	-	-	-	-	*	44.88	-	-	-	-	-	-	-	-	-	-	-	-
LOAD	-	-	-	-	*	9.82	-	-	-	-	-	-	-	-	-	-	-	-
ECD	0.15	0.65	0.13	0.55	0.86	3.79	0.07	0.29	5.10E-03	0.02	5.10E-03	0.02	5.10E-03	0.02	7.61E-04	3.33E-03	-	-
Flare (Process)	7.79	2.82	62.84	22.65	61.88	22.28	0.11	0.46	-	-	-	-	-	-	0.056	0.020	-	-
MALF	15.52	6.00	125.32	10.00	138.01	10.00	0.11	10.00	-	-	-	-	-	-	0.056	2.00	-	-
Totals	90.45	248.01	225.75	154.98	223.00	207.75	3.14	23.29	2.42	10.59	2.42	10.59	2.42	10.59	0.12	2.03	-	-

¹Condensable Particulate Matter: Include condensable particulate matter emissions for PM10 and PM2.5 if the source is a combustion source. Do not include condensable particulate matter for PM unless PM is set equal to PM10 and PM2.5. Particulate matter (PM) is not subject to an ambient air quality standard, but it is a regulated air pollutant under PSD (20.2.74 NMAC) and Title V (20.2.70 NMAC).

Table 2-J: Fuel

Specify fuel characteristics and usage. Unit and stack numbering must correspond throughout the application package.

Unit No.	Fuel Type (low sulfur Diesel, ultra low sulfur diesel, Natural Gas, Coal, ...)	Fuel Source: purchased commercial, pipeline quality natural gas, residue gas, raw/field natural gas, process gas (e.g. SRU tail gas) or other	Specify Units				
			Lower Heating Value	Hourly Usage	Annual Usage	% Sulfur	% Ash
1	Natural Gas	Pipeline Quality Natural Gas	1,200 Btu/scf	35.3 Mscf	309 MMscf	5%	Negligible
2	Natural Gas	Pipeline Quality Natural Gas	1,200 Btu/scf	35.3 Mscf	309 MMscf	5%	Negligible
3b	Natural Gas	Pipeline Quality Natural Gas	1,200 Btu/scf	2.5 Mscf	21.9 MMscf	5%	Negligible
5	Natural Gas	Pipeline Quality Natural Gas	1,200 Btu/scf	32.4 Mscf	284 MMscf	5%	Negligible
6	Natural Gas	Pipeline Quality Natural Gas	1,200 Btu/scf	18.78 Mscf	164.51 MMscf	5%	Negligible
7	Natural Gas	Pipeline Quality Natural Gas	1,200 Btu/scf	18.78 Mscf	164.51 MMscf	5%	Negligible
8	Natural Gas	Pipeline Quality Natural Gas	1,200 Btu/scf	18.78 Mscf	164.51 MMscf	5%	Negligible
9	Natural Gas	Pipeline Quality Natural Gas	1,200 Btu/scf	18.78 Mscf	164.51 MMscf	5%	Negligible
10	Natural Gas	Pipeline Quality Natural Gas	1,200 Btu/scf	18.78 Mscf	164.51 MMscf	5%	Negligible
Flare (Process)	Natural Gas	Pipeline Quality Natural Gas	1,200 Btu/scf	0.10 Mscf	0.88 MMscf	5%	Negligible
ECD	Natural Gas	Pipeline Quality Natural Gas	1,200 Btu/scf	0.10 Mscf	0.88 MMscf	5%	Negligible

Table 2-P: Greenhouse Gas Emissions

Applications submitted under 20.2.70, 20.2.72, & 20.2.74 NMAC are required to complete this Table. Power plants, Title V major sources, and PSD major sources must report and calculate all GHG emissions for each unit. Applicants must report potential emission rates in short tons per year (see Section 6.a for assistance). Include GHG emissions during Startup, Shutdown, and Scheduled Maintenance in this table. For minor source facilities that are not power plants, are not Title V, or are not PSD, there are three options for reporting GHGs 1) report GHGs for each individual piece of equipment; 2) report all GHGs from a group of unit types, for example report all combustion source GHGs as a single unit and all venting GHG as a second separate unit; OR 3) check the following box.

By checking this box, the applicant acknowledges the total CO₂e emissions are less than 75,000 tons per year.

		CO ₂ ton/yr	N ₂ O ton/yr	CH ₄ ton/yr	SF ₆ ton/yr	PFC/HFC ton/yr ²									Total GHG Mass Basis ton/yr ⁴	Total CO ₂ e ton/yr ⁵
Unit No.	GWPs¹	1	298	25	22,800	footnote 3										
1	mass GHG	21,685.12	0.041	0.41	-	-									21,685.57	
	CO ₂ e	21,685.12	12.18	10.22	-	-										21,707.51
2	mass GHG	21,685.12	0.041	0.41	-	-									21,685.57	
	CO ₂ e	21,685.12	12.18	10.22	-	-										21,707.51
5	mass GHG	20,596.87	0.039	0.39	-	-									20,597.29	
	CO ₂ e	20,596.87	11.57	9.70	-	-										20,618.14
6	mass GHG	8,775.37	0.017	0.17	-	-									8,775.55	
	CO ₂ e	8,775.37	4.93	4.13	-	-										8,784.43
7	mass GHG	8,775.37	0.017	0.17	-	-									8,775.55	
	CO ₂ e	8,775.37	4.93	4.13	-	-										8,784.43
8	mass GHG	8,775.37	0.017	0.17	-	-									8,775.55	
	CO ₂ e	8,775.37	4.93	4.13	-	-										8,784.43
9	mass GHG	8,775.37	0.017	0.17	-	-									8,775.55	
	CO ₂ e	8,775.37	4.93	4.13	-	-										8,784.43
10	mass GHG	8,775.37	0.017	0.17	-	-									8,775.55	
	CO ₂ e	8,775.37	4.93	4.13	-	-										8,784.43
3a	mass GHG	-	-	-	-	-									-	
	CO ₂ e	-	-	-	-	-									-	
3b	mass GHG	1,537.07	2.90E-03	0.029	-	-									1,537.10	
	CO ₂ e	1,537.07	0.86	0.72	-	-										1,538.65
T-007	mass GHG	0.61	-	1.03	-	-									1.64	
	CO ₂ e	0.61	-	25.75	-	-										26.36
T-008	mass GHG	9.04E-11	-	8.19E-13	-	-									9.13E-11	-
T-009																
T-011	CO ₂ e	9.04E-11	-	2.05E-11	-	-									-	1.11E-10
T-012																
F-001	mass GHG	-	-	-	-	-									-	
	CO ₂ e	-	-	-	-	-									-	
LOAD	mass GHG	-	-	-	-	-									-	
	CO ₂ e	-	-	-	-	-									-	
ECD	mass GHG	61.48	1.16E-04	1.05	-	-									62.53	
	CO ₂ e	61.48	0.035	26.22	-	-										87.73
HAUL	mass GHG	-	-	-	-	-									-	
	CO ₂ e	-	-	-	-	-									-	
Flare (process)	mass GHG	61.48	1.16E-04	1.92	-	-									63.40	
	CO ₂ e	61.48	0.035	47.89	-	-										109.40

Table 2-P: Greenhouse Gas Emissions

Applications submitted under 20.2.70, 20.2.72, & 20.2.74 NMAC are required to complete this Table. Power plants, Title V major sources, and PSD major sources must report and calculate all GHG emissions for each unit. Applicants must report potential emission rates in short tons per year (see Section 6.a for assistance). Include GHG emissions during Startup, Shutdown, and Scheduled Maintenance in this table. For minor source facilities that are not power plants, are not Title V, or are not PSD, there are three options for reporting GHGs 1) report GHGs for each individual piece of equipment; 2) report all GHGs from a group of unit types, for example report all combustion source GHGs as a single unit and all venting GHG as a second separate unit; OR 3) check the following box.

By checking this box, the applicant acknowledges the total CO₂e emissions are less than 75,000 tons per year.

		CO ₂ ton/yr	N ₂ O ton/yr	CH ₄ ton/yr	SF ₆ ton/yr	PFC/HFC ton/yr ²									Total GHG Mass Basis ton/yr ⁴	Total CO ₂ e ton/yr ⁵
Unit No.	GWPs¹	1	298	25	22,800	footnote 3										
Flare (process)	mass GHG	5,146.41	0.011	8.71	-	-									5,155.13	
	CO ₂ e	5,146.41	2.74	217.66	-	-										5,366.81
Flare (SSM)	mass GHG	6,842.42	0.011	5.02	-	-									6,847.46	
	CO ₂ e	6,842.42	3.20	125.54	-	-										6,971.17
Vent (SSM)	mass GHG	4.00	-	70.00	-	-									74.00	
	CO ₂ e	4.00	-	1,750.50	-	-										1,754.50
MALF	mass GHG	-	-	-	-	-									-	
	CO ₂ e	-	-	-	-	-										-
Total	mass GHG	121,497.43	0.23	89.79	-	-									121,587.45	
	CO ₂ e	121,497.43	67.44	2,245.09	-	-										123,809.96

¹ GWP (Global Warming Potential): Applicants must use the most current GWPs codified in Table A-1 of 40 CFR part 98. GWPs are subject to change, therefore, applicants need to check 40 CFR 98 to confirm GWP values.

² For HFCs or PFCs describe the specific HFC or PFC compound and use a separate column for each individual compound.

³ For each new compound, enter the appropriate GWP for each HFC or PFC compound from Table A-1 in 40 CFR 98.

⁴ Green house gas emissions on a mass basis is the ton per year green house gas emission before adjustment with its GWP.

⁵ CO₂e means Carbon Dioxide Equivalent and is calculated by multiplying the TPY mass emissions of the green house gas by its GWP.

Section 3

Application Summary

The **Application Summary** shall include a brief description of the facility and its process, the type of permit application, the applicable regulation (i.e. 20.2.72.200.A.X, or 20.2.73 NMAC) under which the application is being submitted, and any air quality permit numbers associated with this site. If this facility is to be collocated with another facility, provide details of the other facility including permit number(s). In case of a revision or modification to a facility, provide the lowest level regulatory citation (i.e. 20.2.72.219.B.1.d NMAC) under which the revision or modification is being requested. Also describe the proposed changes from the original permit, how the proposed modification will affect the facility's operations and emissions, de-bottlenecking impacts, and changes to the facility's major/minor status (both PSD & Title V).

The **Process Summary** shall include a brief description of the facility and its processes.

Startup, Shutdown, and Maintenance (SSM) routine or predictable emissions: Provide an overview of how SSM emissions are accounted for in this application. Refer to "Guidance for Submittal of Startup, Shutdown, Maintenance Emissions in Permit Applications (http://www.env.nm.gov/aqb/permit/app_form.html) for more detailed instructions on SSM emissions.

Enterprise Field Services, LLC (Enterprise) is submitting this application and accompanying material pursuant to 20.2.70.404.C.(1)(1) NMAC to apply for a significant modification to the existing Title V major source permit for the South Carlsbad Compressor Station (South Carlsbad). The facility is located approximately 2.8 miles northwest of Loving, NM in Eddy County and is currently operating under Title V Permit No. P130-R4. The facility is currently major with respect to Title V and is minor with respect to PSD and will remain so with this modification.

The Title V Significant Modification will reflect the changes incorporated to NSR 0220-M12 and NSR 0220-M12R1 which include:

- Addition of five (5) CAT G3608A4 2500 hp compressor engines (Units 6, 7, 8, 9 & 10);
- Addition of one (1) 400 bbl slop oil storage tank (Unit T-007);
- Addition of slop loading (Unit LOAD_SLOP) (Exempt pursuant to IA List Item #1.a.);
- Addition of one (1) enclosed combustion device (Unit ECD);
- Modification of two (2) Solar Centaur T-4702 natural gas turbines (Units 1 & 2);
- Modification of one (1) 200 MMscf/d glycol dehydrator (Unit 3a);
- Modification of one (1) 72 Mscf/hr process flare (Unit Flare);
- Modification of one (1) 3.0 MMBtu/hr glycol dehydrator reboiler (Unit 3b);
- Modification of facility wide fugitives (Unit F-001); and
- Modification of malfunction emissions (Unit MALF)

The facility is a natural gas compressor station. Gas enters the facility through a separator and is compressed by three gas turbine-driven compressors (Units 1, 2, & 5) and five 4-stroke lean burn compressor engines (Units 6, 7, 8, 9 & 10). After inlet compression, gas is sent to a glycol dehydrator (Unit 3a) and then to a chiller and cold separator, where liquids (primarily water) condense and are removed from the stream. The dry gas stream then goes to a pipeline for transport.

Startup, Shutdown, and Maintenance (SSM) emissions are controlled by the process and SSM flare. This facility is currently permitted to vent VOC emission during SSM events (Unit VENT (SSM)).

Section 4

Process Flow Sheet

A **process flow sheet** and/or block diagram indicating the individual equipment, all emission points and types of control applied to those points. The unit numbering system should be consistent throughout this application.

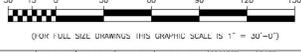
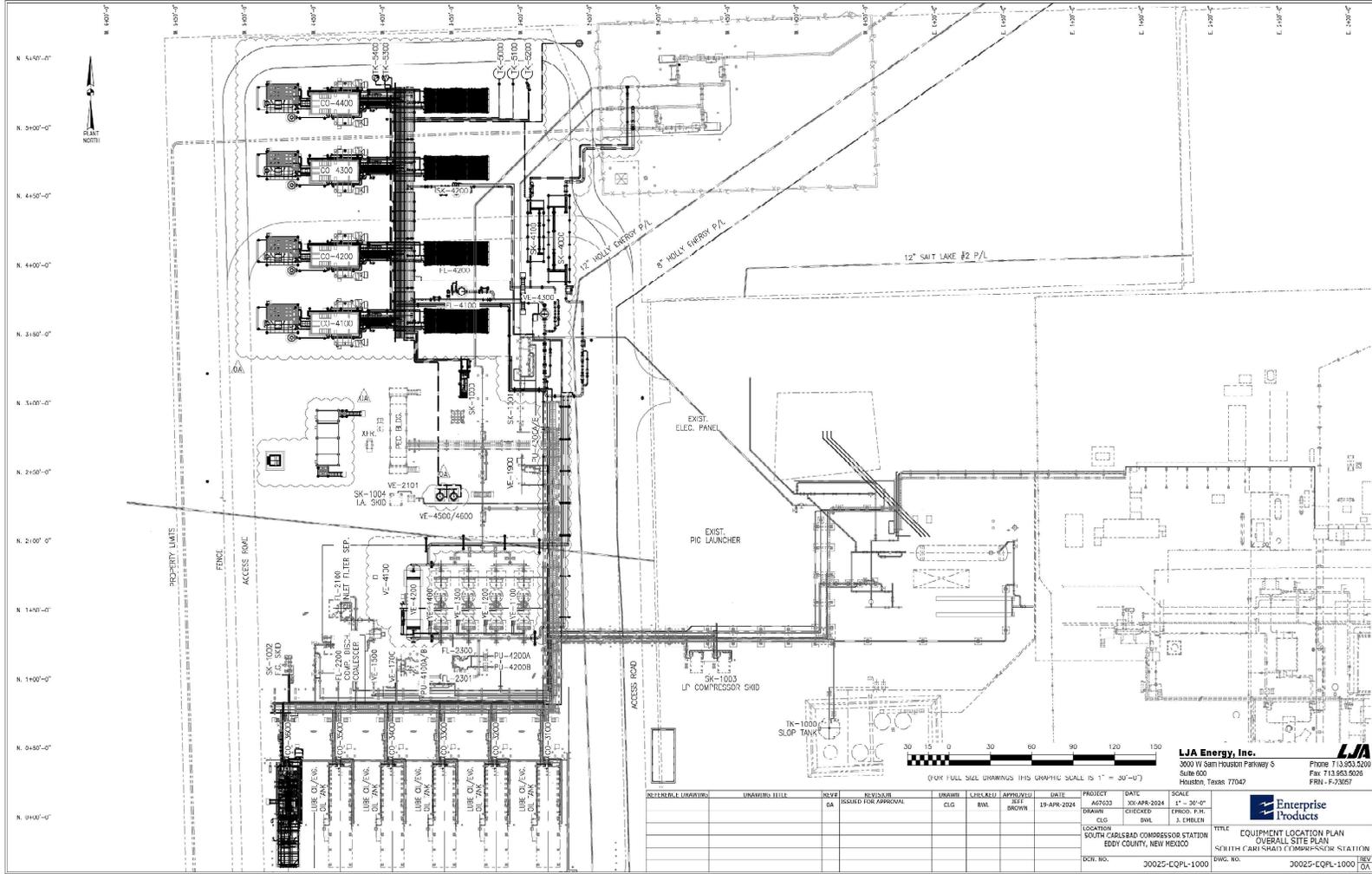
A process flow sheet is attached on the following page.

Section 5

Plot Plan Drawn to Scale

A **plot plan drawn to scale** showing emissions points, roads, structures, tanks, and fences of property owned, leased, or under direct control of the applicant. This plot plan must clearly designate the restricted area as defined in UA1, Section 1-D.12. The unit numbering system should be consistent throughout this application.

A plot plan is attached on the following page.



LJA Energy, Inc.
 3000 W Sam Houston Parkway S
 Suite 600
 Houston, Texas 77042
 Phone 713.653.8200
 Fax 713.653.8026
 FRI - F-2367

REVISION NUMBER	REVISION DATE	ISSUED FOR APPROVAL	DESIGNED BY	CHECKED BY	APPROVED BY	DATE	PROJECT	DWG. NO.	SCALE	TITLE
01	19-APR-2024	CLG	BVA	RTB	BROWN	19-APR-2024	A67033	30025-COPL-1000	1" = 30'-0"	EQUIPMENT LOCATION PLAN OVERALL SITE PLAN



Enterprise Products
 TITLE: EQUIPMENT LOCATION PLAN
 OVERALL SITE PLAN
 SOUTH CARLSBAD COMPRESSOR STATION
 EDDY COUNTY, NEW MEXICO
 DWG. NO.: 30025-COPL-1000

Section 6

All Calculations

Show all calculations used to determine both the hourly and annual controlled and uncontrolled emission rates. All calculations shall be performed keeping a minimum of three significant figures. Document the source of each emission factor used (if an emission rate is carried forward and not revised, then a statement to that effect is required). If identical units are being permitted and will be subject to the same operating conditions, submit calculations for only one unit and a note specifying what other units to which the calculations apply. All formulas and calculations used to calculate emissions must be submitted. The "Calculations" tab in the UA2 has been provided to allow calculations to be linked to the emissions tables. Add additional "Calc" tabs as needed. If the UA2 or other spread sheets are used, all calculation spread sheet(s) shall be submitted electronically in Microsoft Excel compatible format so that formulas and input values can be checked. Format all spread sheets and calculations such that the reviewer can follow the logic and verify the input values. Define all variables. If calculation spread sheets are not used, provide the original formulas with defined variables. Additionally, provide subsequent formulas showing the input values for each variable in the formula. All calculations, including those calculations are imbedded in the Calc tab of the UA2 portion of the application, the printed Calc tab(s), should be submitted under this section.

Tank Flashing Calculations: The information provided to the AQB shall include a discussion of the method used to estimate tank-flashing emissions, relative thresholds (i.e., NOI, permit, or major source (NSPS, PSD or Title V)), accuracy of the model, the input and output from simulation models and software, all calculations, documentation of any assumptions used, descriptions of sampling methods and conditions, copies of any lab sample analysis. If Hysis is used, all relevant input parameters shall be reported, including separator pressure, gas throughput, and all other relevant parameters necessary for flashing calculation.

SSM Calculations: It is the applicant's responsibility to provide an estimate of SSM emissions or to provide justification for not doing so. In this Section, provide emissions calculations for Startup, Shutdown, and Routine Maintenance (SSM) emissions listed in the Section 2 SSM and/or Section 22 GHG Tables and the rationale for why the others are reported as zero (or left blank in the SSM/GHG Tables). Refer to "Guidance for Submittal of Startup, Shutdown, Maintenance Emissions in Permit Applications (http://www.env.nm.gov/aqb/permit/app_form.html) for more detailed instructions on calculating SSM emissions. If SSM emissions are greater than those reported in the Section 2, Requested Allowables Table, modeling may be required to ensure compliance with the standards whether the application is NSR or Title V. Refer to the Modeling Section of this application for more guidance on modeling requirements.

Glycol Dehydrator Calculations: The information provided to the AQB shall include the manufacturer's maximum design recirculation rate for the glycol pump. If GRI-Glycalc is used, the full input summary report shall be included as well as a copy of the gas analysis that was used.

Road Calculations: Calculate fugitive particulate emissions and enter haul road fugitives in Tables 2-A, 2-D and 2-E for:

1. If you transport raw material, process material and/or product into or out of or within the facility and have PER emissions greater than 0.5 tpy.
2. If you transport raw material, process material and/or product into or out of the facility more frequently than one round trip per day.

Significant Figures:

- A. All emissions standards are deemed to have at least two significant figures, but not more than three significant figures.
- B. At least 5 significant figures shall be retained in all intermediate calculations.
- C. In calculating emissions to determine compliance with an emission standard, the following rounding off procedures shall be used:

- (1) If the first digit to be discarded is less than the number 5, the last digit retained shall not be changed;
- (2) If the first digit discarded is greater than the number 5, or if it is the number 5 followed by at least one digit other than the number zero, the last figure retained shall be increased by one unit; **and**
- (3) If the first digit discarded is exactly the number 5, followed only by zeros, the last digit retained shall be rounded upward if it is an odd number, but no adjustment shall be made if it is an even number.
- (4) The final result of the calculation shall be expressed in the units of the standard.

Control Devices: In accordance with 20.2.72.203.A(3) and (8) NMAC, 20.2.70.300.D(5)(b) and (e) NMAC, and 20.2.73.200.B(7) NMAC, the permittee shall report all control devices and list each pollutant controlled by the control device regardless if the applicant takes credit for the reduction in emissions. The applicant can indicate in this section of the application if they chose to not take credit for the reduction in emission rates. For notices of intent submitted under 20.2.73 NMAC, only uncontrolled emission rates can be considered to determine applicability unless the state or federal Acts require the control. This information is necessary to determine if federally enforceable conditions are necessary for the control device, and/or if the control device produces its own regulated pollutants or increases emission rates of other pollutants.

This section contains the following calculations for this facility. Supporting documentation for these calculations can be found in Section 7.

Subsection 1 – Emission calculations for units either added or modified with this application.

Solar Centaur T-4702 turbines (Units 1 & 2)

NO_x and CO emission rates were updated using historical stack test results obtained from 2010 to 2016 stack tests with a safety factor. VOC emission rates are reproduced here from previous applications. SO₂ emissions are based on a conservative fuel sulfur content estimated of 5 gr S/100 scf and 100% conversion of elemental sulfur to SO₂. Particulate emission rates (PM_{2.5}, PM₁₀, and TSP) were updated based on Solar Turbines Inc, Product Information Letter 171, refer to Section 7. Total and individual HAP emissions are calculated using GRI-HAPCalc 3.01. Greenhouse gas emissions are estimated using emission factors from 40 CFR 98 Subpart C Tables C-1 and C-2.

Caterpillar G3608 Engines (Units 6, 7, 8, 9, & 10)

NO_x, CO, and VOC emission rates were calculated using manufacturer specifications. SO₂ emissions are based on a conservative fuel sulfur content estimated of 5 gr S/100 scf and 100% conversion of elemental sulfur to SO₂. Particulate (PM_{2.5}, PM₁₀, and TSP) and HAP emissions were calculated using AP-42 Table 3.2-2. Greenhouse gas emissions are estimated using emission factors from 40 CFR 98 Subpart C Tables C-1 and C-2.

Glycol Dehydrator and Reboiler (Units 3a & 3b)

Glycol dehydrator emissions were calculated using GRI-GLYCalc and an extended gas analysis. VOC and HAP emissions from the regenerator are controlled with a BTEX condenser then sent to the ECD. Flash tank emissions are primarily controlled by the ECD or sent to the reboiler to be used as fuel. The condenser overheads are routed to the ECD where VOC and HAP emissions are combusted and controlled with a 98% efficiency.

Produced Water Slop Tank (Unit T-007)

Working, breathing, and Flash emissions from T-007 are calculated in this application using a BR&E ProMax simulation.

Slop Loading Emissions (Unit LOAD_SLOP) (Exempt pursuant to IA List Item #1.a.)

ProMax was used to perform the loading emissions calculations. Specifically, a RVP11 ProMax simulation was used to determine the stream compositions.

Enclosed Combustion Device (Unit ECD)

Emission calculations account for the possible presence of H₂S in the fuel gas. Emissions of NO_x, CO, and PM are calculated using AP-42 Tables 1.4-1 & 2 emission factors. Pilot H₂S emissions are calculated based on the conservative estimate of 0.25 g H₂S/100 scf and a 98% combustion efficiency of the ECD. Pilot SO₂ emissions are based on a conservative fuel sulfur content estimate of 5 gr S/100 scf and 100% conversion of elemental sulfur to SO₂. SO₂ emissions were calculated based on a destruction rate efficiency (DRE) of 98%, based on the manufacturer specification sheet, and conversion to SO₂. Emissions of VOC, H₂S, and HAPs are calculated based on the GRI-GLYCalc report for the Controlled Regenerator Emissions after the BTEX condenser and the report for the Flash Gas Emissions with a 98% DRE. For the H₂S, it was assumed 98% was combusted and 100% of the combusted H₂S was converted to SO₂.

Flare (Unit Flare)

Emission calculations were updated to account for the possible presence of H₂S. An H₂S composition of 0.5 mol % was assumed. Emissions of NO_x and CO are calculated using the larger of the AP-42 Table 13.5-1 and TNRCC RG-109 emission factors. Pilot H₂S emissions are calculated based on the conservative estimate of 0.25 g H₂S/100 scf and a 98% combustion efficiency of the flare. Pilot SO₂ emissions are based on a conservative fuel sulfur content estimated of 5 gr S/100 scf and 100% conversion of elemental sulfur to SO₂. SO₂ emissions were calculated assuming 98% combustion efficiency and conversion to SO₂.

Emissions of VOCs and HAPs are estimated based on the gas analysis and an assumed 98% combustion efficiency.

During non-routine conditions such as when gas must be released from portions of the facility for maintenance or in the event of an emergency, some VOCs will be directed to the flare. Gas streams 14 and 33 will be directed to the flare in the event of a plant shutdown. Additionally, during an emergency shutdown, pressure vessels or the gas contents of the refrigeration system may be released to the flare; however, the quantity of gas in these vessels or systems is less than the assumed maximum gas volume from streams 14 and 33.

Flare parameters are calculated using a temperature of 1000° C and a 20 m/sec velocity (per NMAQB guidelines), and an effective diameter calculated in accordance with the Modeling Guidelines.

Greenhouse gas emissions were estimated using 40 CFR 98 Subpart W calculation methodology.

Fugitive Emissions (Unit F-001)

Fugitive emission calculations were completed using emission factors from Table 2-4 of EPA Protocol for Equipment Leak Emission Estimates, 1995. Subcomponent counts for each subcomponent are based on estimated average component counts for each piece of equipment.

Subsection 2 – Emission calculations for all other units at this facility not affected by this application.

Solar Centaur 40-4700S (Unit 5)

NO_x, CO, and VOC emission rates were calculated using manufacturer specifications. SO₂ emissions are based on a conservative fuel sulfur content estimated of 5 gr S/100 scf and 100% conversion of elemental sulfur to SO₂. Particulate (PM_{2.5}, PM₁₀, and TSP) and HAP emissions were calculated using AP-42 Table 3.1-2a. Greenhouse gas emissions are estimated using emission factors from 40 CFR 98 Subpart C Tables C-1 and C-2.

Stabilized Condensate Storage Tanks (Units T-008, T-009, T-011, & T-012)

Working and breathing emissions from T-008, T-009, T-011, and T-012 are calculated in this application using a BR&E ProMax simulation.

Exempt Storage Tanks (Units T-001 through T-006)

Methanol storage tanks (T-002) and condensate slop oil tank (T-006) are exempt pursuant to 20.2.72.202.B.(5) NMAC. Emissions from T-002 were conservatively estimated based on 3 anticipated turnovers per year. Emissions from T-006 was calculated with BR&E ProMax using condenser liquid streams from the GRI-GLYCalc process simulation and other relevant calculations. Emission calculations for both units are included in the application for reference. All other storage tanks at South Carlsbad Compressor Station are either exempt because they contain liquids with vapor pressure less than 10mmHg (T-001, T-004, and T-005) or are not a source of regulated pollutants (T-003).

Condensate Loading Emissions (Unit LOAD)

ProMax and GRI-HAPCalc were used to perform the loading emissions calculations. Specifically, a RVP11 ProMax simulation was used to determine the stream compositions.

Unpaved Haul Road Emissions (Unit HAUL)

These emissions were calculated using Equation 2 of AP-42 Section 13.2.2. Haul road emissions at this facility are exempt pursuant to 20.2.72.202.B(5) NMAC. Emission calculations are included in the application for reference.

Vent (Unit VENT)

A RVP11 Promax simulation was used to determine the emissions associated to this unit based on the mole fraction calculated for different components found on the SC Vapor process stream located before the first stage compressor. In addition, to overcome H₂S possible molar fraction changes, it was assumed 0.05% mole instead of zero, as forecasted by the mentioned simulation.

From time to time, the pressurized gas in a portion of the facility's system must be vented in order to relieve the pressure. At South Carlsbad Compressor Station, this is primarily done in order to perform maintenance on the compressors and the compressor turbines (Units 1 and 2). This pressure relief is termed "blow down". Blow down at this facility is and will continue to be directed to various vents, including but not limited to pressure relief valves and blowdown vent stacks, aggregated in this application as unit VENT.

During routine startup, shutdown, or blow down events, gas from the turbines is diverted to unit VENT. A table of the inlet gas composition (based on the combined gas analysis) and the anticipated number of blow down events per year (conservatively estimated) is included in this section. Venting volume and frequency were estimated based on operating history and engineering knowledge. It is assumed that the gas being vented will contain a maximum of 10 ppmv of H₂S.

Maximum hourly venting emissions were calculated assuming 1 hour per event for a worst-case scenario. Annual venting emissions were calculated using the total volume of gas vented annually based on the estimate of predicted annual events with a safety factor of 100% to overcome for components variations. In addition, a molar concentration of 0.05% of H₂S was assumed since the analysis used did not showed any H₂S concentration.

Section 6

Subsection 1 – Emission Calculations for Units either Added or Modified with this Application

For clarity, this Subsection 1 contains emission calculations for units that were either added or modified with this application (i.e. Units 1, 2, 6, 7, 8, 9, 10, 3a, 3b, T-007, LOAD_SLOP, ECD, Flare, F-001, and MALF). For all other emission calculations pertinent to the other units at this facility, please refer to Section 6 Subsection 2.

Maximum Uncontrolled Emissions																
Equipment	NO _x		CO		VOC		SO _x		PM		PM ₁₀		PM _{2.5}		H ₂ S	
	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
1	27.00	90.82	7.40	11.25	0.77	3.37	0.50	2.21	0.63	2.78	0.63	2.78	0.63	2.78	2.52E-04	1.10E-03
2	27.00	90.82	7.40	11.25	0.77	3.37	0.50	2.21	0.63	2.78	0.63	2.78	0.63	2.78	2.52E-04	1.10E-03
5	4.43	19.40	5.89	25.78	1.40	6.15	0.48	2.10	0.27	1.16	0.27	1.16	0.27	1.16	2.39E-04	1.05E-03
6	1.65	7.24	13.78	60.35	1.49	6.52	0.27	1.17	0.17	0.75	0.17	0.75	0.17	0.75	1.34E-04	5.88E-04
7	1.65	7.24	13.78	60.35	1.49	6.52	0.27	1.17	0.17	0.75	0.17	0.75	0.17	0.75	1.34E-04	5.88E-04
8	1.65	7.24	13.78	60.35	1.49	6.52	0.27	1.17	0.17	0.75	0.17	0.75	0.17	0.75	1.34E-04	5.88E-04
9	1.65	7.24	13.78	60.35	1.49	6.52	0.27	1.17	0.17	0.75	0.17	0.75	0.17	0.75	1.34E-04	5.88E-04
10	1.65	7.24	13.78	60.35	1.49	6.52	0.27	1.17	0.17	0.75	0.17	0.75	0.17	0.75	1.34E-04	5.88E-04
3a	-	-	-	-	73.65	322.57	-	-	-	-	-	-	-	-	0.041	0.18
3b	0.29	1.29	0.25	1.08	0.016	0.071	0.036	0.16	0.022	0.10	0.022	0.10	0.022	0.10	8.93E-04	3.91E-03
T-007	-	-	-	-	*	0.67	-	-	-	-	-	-	-	-	-	-
T-008	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
T-009	-	-	-	-	*	18.85	-	-	-	-	-	-	-	-	-	-
T-011	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
T-012	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
F-001	-	-	-	-	*	44.88	-	-	-	-	-	-	-	-	-	-
LOAD	-	-	-	-	*	9.82	-	-	-	-	-	-	-	-	-	-
ECD	0.012	0.052	9.88E-03	0.043	-	-	6.59E-05	2.89E-04	-	-	-	-	-	-	3.50E-05	1.53E-04
Flare (Process)	7.79	2.82	62.84	22.65	61.88	22.28	0.11	0.46	-	-	-	-	-	-	0.056	0.020
Flare (SSM)	7.73	0.20	62.48	1.62	76.13	1.98	-	-	-	-	-	-	-	-	-	-
VENT (SSM)	-	-	-	-	*	26.81	-	-	-	-	-	-	-	-	*	0.10
MALF ¹	15.52	6.00	125.32	10.00	138.01	10.00	0.11	10.00	-	-	-	-	-	-	0.056	2.00
Total	98.04	247.61	340.47	385.43	360.06	503.42	3.07	22.99	2.41	10.57	2.41	10.57	2.41	10.57	0.16	2.31

*** Denotes an hourly emission rate is not appropriate

“-” Indicates emissions of this pollutant are not expected

¹ Flare malfunction hourly emission rates reflect worst case emissions modeled for this unit. These emissions are the maximum allowed for the flare and are not additive with the Process and SSM emissions requested under Unit Flare.

Controlled Emissions																
Equipment	NO _x		CO		VOC		SO _x		PM		PM ₁₀		PM _{2.5}		H ₂ S	
	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
1	27.00	90.82	7.40	11.25	0.77	3.37	0.50	2.21	0.63	2.78	0.63	2.78	0.63	2.78	2.52E-04	1.10E-03
2	27.00	90.82	7.40	11.25	0.77	3.37	0.50	2.21	0.63	2.78	0.63	2.78	0.63	2.78	2.52E-04	1.10E-03
5	4.43	19.40	5.89	25.78	1.40	6.15	0.48	2.10	0.27	1.16	0.27	1.16	0.27	1.16	2.39E-04	1.05E-03
6	1.65	7.24	3.31	14.48	3.86	16.90	0.27	1.17	0.17	0.75	0.17	0.75	0.17	0.75	1.34E-04	5.88E-04
7	1.65	7.24	3.31	14.48	3.86	16.90	0.27	1.17	0.17	0.75	0.17	0.75	0.17	0.75	1.34E-04	5.88E-04
8	1.65	7.24	3.31	14.48	3.86	16.90	0.27	1.17	0.17	0.75	0.17	0.75	0.17	0.75	1.34E-04	5.88E-04
9	1.65	7.24	3.31	14.48	3.86	16.90	0.27	1.17	0.17	0.75	0.17	0.75	0.17	0.75	1.34E-04	5.88E-04
10	1.65	7.24	3.31	14.48	3.86	16.90	0.27	1.17	0.17	0.75	0.17	0.75	0.17	0.75	1.34E-04	5.88E-04
3a	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
3b	0.29	1.29	0.25	1.08	0.016	0.071	0.036	0.16	0.022	0.10	0.022	0.10	0.022	0.10	8.93E-04	3.91E-03
T-007	-	-	-	-	*	-	-	-	-	-	-	-	-	-	-	-
T-008	-	-	-	-	*	0.67	-	-	-	-	-	-	-	-	-	-
T-009	-	-	-	-	*	18.85	-	-	-	-	-	-	-	-	-	-
T-011	-	-	-	-	*	-	-	-	-	-	-	-	-	-	-	-
T-012	-	-	-	-	*	-	-	-	-	-	-	-	-	-	-	-
F-001	-	-	-	-	*	44.88	-	-	-	-	-	-	-	-	-	-
LOAD	-	-	-	-	*	9.82	-	-	-	-	-	-	-	-	-	-
ECD	0.15	0.65	0.13	0.55	0.86	3.79	0.067	0.29	5.10E-03	0.022	5.10E-03	0.022	5.10E-03	0.022	7.61E-04	3.33E-03
Flare (Process)	7.79	2.82	62.84	22.65	61.88	22.28	0.11	0.46	-	-	-	-	-	-	0.056	0.020
Flare (SSM)	7.73	0.20	62.48	1.62	76.13	1.98	-	-	-	-	-	-	-	-	-	-
VENT (SSM)	-	-	-	-	*	26.81	-	-	-	-	-	-	-	-	*	0.10
MALF ¹	15.52	6.00	125.32	10.00	138.01	10.00	0.11	10.00	-	-	-	-	-	-	0.056	2.00
Total	98.18	248.21	288.23	156.60	299.13	236.54	3.14	23.29	2.42	10.59	2.42	10.59	2.42	10.59	0.12	2.13

** Denotes an hourly emission rate is not appropriate

.- Indicates emissions of this pollutant are not expected

¹ Flare malfunction hourly emission rates reflect worst case emissions modeled for this unit. These emissions are the maximum allowed for the flare and are not additive with the Process and SSM emissions requested under Unit Flare.

Controlled HAP and Greenhouse Gas Emissions																	
Equipment	Total HAPs		Formaldehyde		Acetaldehyde		n-Hexane		Benzene		Toluene		Xylenes		Ethylbenzene		CO ₂ e
	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	tpy
1	0.33	1.45	0.13	0.59	0.14	0.60	0.012	0.052	4.27E-03	0.019	3.26E-03	0.014	9.89E-03	0.043	-	-	21707.51
2	0.33	1.45	0.13	0.59	0.14	0.60	0.012	0.052	4.27E-03	0.019	3.26E-03	0.014	9.89E-03	0.043	-	-	21707.51
5	0.04	0.17	0.03	0.13	1.61E-03	7.04E-03	-	-	4.82E-04	2.11E-03	5.23E-03	0.023	2.57E-03	0.011	-	-	20618.14
6	0.38	1.67	0.22	0.97	0.14	0.63	-	-	7.53E-03	0.033	6.98E-03	0.031	3.15E-03	0.014	-	-	8784.43
7	0.38	1.67	0.22	0.97	0.14	0.63	-	-	7.53E-03	0.033	6.98E-03	0.031	3.15E-03	0.014	-	-	8784.43
8	0.38	1.67	0.22	0.97	0.14	0.63	-	-	7.53E-03	0.033	6.98E-03	0.031	3.15E-03	0.014	-	-	8784.43
9	0.38	1.67	0.22	0.97	0.14	0.63	-	-	7.53E-03	0.033	6.98E-03	0.031	3.15E-03	0.014	-	-	8784.43
10	0.38	1.67	0.22	0.97	0.14	0.63	-	-	7.53E-03	0.033	6.98E-03	0.031	3.15E-03	0.014	-	-	8784.43
3a	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
3b	0.022	0.09	1.26E-03	5.50E-03	1.10E-03	4.80E-03	2.10E-03	9.200E-03	1.12E-03	4.90E-03	1.53E-03	6.70E-03	1.99E-03	8.700E-03	3.17E-03	0.014	1538.65
T-007	*	0.10	-	-	-	-	*	7.66E-04	*	0.058	*	0.017	*	1.95E-03	*	5.44E-04	-
T-008	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
T-009	*	0.79	-	-	-	-	*	0.67	*	0.086	*	0.031	*	2.72E-03	*	1.44E-03	-
T-011	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
T-012	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
F-001	*	4.47	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
LOAD	*	0.45	-	-	-	-	*	0.39	*	0.043	*	7.00E-04	*	1.20E-03	*	1.30E-03	-
ECD	0.16	0.70	-	-	-	-	0.018	0.08	0.08	0.37	0.05	0.23	0.05	0.23	-	-	87.73
Flare (Process)	0.79	0.28	-	-	-	-	0.56	0.20	0.075	0.03	0.087	0.031	0.058	0.021	7.50E-03	2.70E-03	5366.81
Flare (SSM)	7.96E-03	2.07E-04	-	-	-	-	7.96E-03	2.07E-04	-	-	-	-	-	-	-	-	6971.17
VENT (SSM)	*	0.69	-	-	-	-	*	0.49	*	0.11	*	0.075	*	0.010	-	5.23E-03	1754.57
MALF	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Total	3.58	18.98	1.40	6.14	0.99	4.35	0.61	1.95	0.21	0.90	0.19	0.59	0.15	0.44	0.011	0.025	123674.27

Unit:	1, 2		
Description:	Solar Centaur T-4702 NG turbines		
Fuel consumption	35.3	Mscf/hr	As permitted
Fuel heat value	1200	Btu/scf	Nominal LHV of fuel gas
Heat rate	42.3	MMbtu/hr	Fuel consumption * fuel heat value / 1000
Annual fuel usage	309.0	MMscf/yr	8760 hrs/yr operation

Uncontrolled Emissions

NO_x	CO	VOC	SO₂¹	PM²	H₂S¹			
				0.015		lb/MMBtu	Solar Turbines Inc Product Information Letter 171 Particulates Emission Rate	
15.8	1.5					lbs/hr	Unit 1: 2010 Stack Test Report Maximum Recordable Rate	
-	-					lbs/hr	Unit 2: 2010 Stack Test Report Maximum Recordable Rate	
15.2	0.8					lbs/hr	Unit 1: 2011 Stack Test Report Maximum Recordable Rate	
15.4	1.0					lbs/hr	Unit 2: 2011 Stack Test Report Maximum Recordable Rate	
16.4	1.2					lbs/hr	Unit 1: 2012 Stack Test Report Maximum Recordable Rate	
15.2	1.0					lbs/hr	Unit 2: 2012 Stack Test Report Maximum Recordable Rate	
17.57	2.14					lbs/hr	Unit 1: 2014 Stack Test Report Maximum Recordable Rate	
18.85	1.87					lbs/hr	Unit 2: 2014 Stack Test Report Maximum Recordable Rate	
15.63	1.87					lbs/hr	Unit 1: 2015 Stack Test Report Maximum Recordable Rate	
16.62	1.27					lbs/hr	Unit 2: 2015 Stack Test Report Maximum Recordable Rate	
7.85	0.90					lbs/hr	Unit 1: 2016 Stack Test Report Maximum Recordable Rate	
9.75	1.21					lbs/hr	Unit 2: 2016 Stack Test Report Maximum Recordable Rate	
18.9	2.1					lbs/hr	Maximum Recordable Rate	
10%	20%						Safety Factor	
20.7	2.6					lbs/hr	Emission Rate with Safety Factor	
27.0	7.4	0.77				lb/hr	As permitted	
27.0	7.4	0.77	0.50	0.63	2.5E-04	lb/hr	Hourly emission rate	
90.8	11.2	3.4	2.2	2.8	1.1E-03	tpy	Annual emission rate (8760 hrs/yr)	
Total HAP³n-Hexane³ HCHO³ Acetaldehyde³ Benzene³ Toluene³ Xylenes³								
0.33	0.012	0.13	0.14	0.0043	0.0033	0.0099	lb/hr	Hourly emission rate
1.4	0.052	0.59	0.60	0.019	0.014	0.043	tpy	Annual emission rate (8760 hrs/yr)

¹ SO₂ emissions based on fuel sulfur content of 5 gr S/100 scf, or 0.00714 lb S/Mscf

$$\text{lb/hr SO}_2 = 5\text{gr S}/100\text{scf} * \text{Fuel consumption (Mscf/hr)} * 1\text{lb}/7000\text{gr} * 1000\text{scf}/\text{Mscf} * 64\text{ lb SO}_2/32\text{ lb S}$$

H₂S emissions based on 0.25 g/100 scf H₂S in fuel

$$\text{lb/hr H}_2\text{S} = 0.25\text{ gr H}_2\text{S}/100\text{ scf} * \text{Fuel consumption (Mscf/hr)} * 1000\text{scf}/\text{Mscf} * 1\text{ lb}/7000\text{ gr} * (1 - \text{Comb. Eff [98\%]})$$

² Assumed TSP = PM₁₀ = PM_{2.5}

³ HAP emissions calculated from GRI-HAPCalc v3.01.

GHG Calculations

CO₂⁴	N₂O⁴	CH₄⁴	CO₂e⁴	
53.06	0.0001	0.001		kg/MMBtu 40 CFR 98 Subpart C Tables C-1 and C-2
1	298	25		GWP 40 CFR 98 Table A-1
21685.1	0.041	0.41		tpy
21685.1	12.2	10.2	21707.5	tpy CO ₂ e

⁴ N₂O, CH₄, and CO₂ tpy Emission Rate= EF* Fuel Usage * Fuel Heat Value * 2.20462 lb/1 kg * 1 ton/2000 lb

$$\text{CO}_2\text{e tpy Emission Rate} = \text{CO}_2\text{ Emission Rate} + \text{N}_2\text{O Emission Rate} * \text{GWP Factor} + \text{CH}_4\text{ Emission Rate} * \text{GWP Factor}$$

Unit(s): 6-10
Description: Five (5) CAT G3608 4-Stroke Lean Burn Compressor Engines

Horespower 2,500 bhp
Fuel Consumption Rate 6,848 Btu/hp-hr
Fuel consumption 18.8 Mscf/hr
Fuel heat value 912 Btu/scf Nominal LHV of fuel gas
Annual fuel usage 164.5 MMscf/yr 8760 hrs/yr operation

Uncontrolled Emissions

NO _x	CO	VOC	SO ₂ ¹	PM ³	H ₂ S ²		
0.300	2.5	0.270	-	0.0100	-	lb/MMBtu	AP-42 Table 3.2-2
1.65	13.78	1.49	0.27	0.17	1.34E-4	g/bhp-hr	Vendor Emission Factors
7.24	60.35	6.52	1.17	0.75	5.88E-4	lb/hr	Hourly emission rate
						tpy	Annual emission rate (8760 hrs/yr)

Total HAP ⁴	n-Hexane ⁴	HCHO ⁴	Acetaldehyde ⁴	Benzene ⁴	Toluene ⁴	Xylenes ⁴		
-	1.11E-03	0.16	-	-	-	-	lb/MMBtu	AP-42 Table 3.2-2
1.04	0.02	0.88	0.14	0.01	0.01	3.15E-3	g/bhp-hr	Vendor Emission Factors
4.57	0.08	3.86	0.63	0.03	0.03	0.01	lb/hr	Hourly emission rate
							tpy	Annual emission rate (8760 hrs/yr)

Controlled Emissions

NO _x	CO	VOC	SO ₂ ¹	PM ³	H ₂ S ²		
0.300	0.6	0.700	-	0.0100	-	lb/MMBtu	AP-42 Table 3.2-2
1.65	3.31	3.86	0.27	0.17	1.34E-4	g/bhp-hr	Vendor Emission Factors
7.24	14.48	16.90	1.17	0.75	5.88E-4	lb/hr	Hourly emission rate
						tpy	Annual emission rate (8760 hrs/yr)

Total HAP ⁴	n-Hexane ⁴	HCHO ⁴	Acetaldehyde ⁴	Benzene ⁴	Toluene ⁴	Xylenes ⁴		
-	1.11E-03	0.04	-	-	-	-	lb/MMBtu	AP-42 Table 3.2-2
0.38	0.02	0.22	0.14	0.01	0.01	3.15E-3	g/bhp-hr	Vendor Emission Factors
1.67	0.08	0.97	0.63	0.03	0.03	0.01	lb/hr	Hourly emission rate
							tpy	Annual emission rate (8760 hrs/yr)

¹ SO₂ emissions based on fuel sulfur content of 5 gr S/100 scf, or 0.00714 lb S/Mscf

lb/hr SO₂ = 5gr S/100scf * Fuel consumption (Mscf/hr) * 1lb/7000gr * 1000scf/Mscf * 64 lb SO₂/32 lb S

² H₂S emissions based on 0.25 g/100 scf H₂S in fuel

lb/hr H₂S = 0.25 gr H₂S/100 scf * Fuel consumption (Mscf/hr) * 1000scf/Mscf * 1 lb/7000 gr * (1 - Comb. Eff [98%])

³ Assumed TSP = PM₁₀ = PM_{2.5}

⁴ HAP emissions calculated using emission factors from AP-42 Table 3.1-3.

GHG Calculations

CO ₂ ⁴	N ₂ O ⁴	CH ₄ ⁴	CO ₂ e ⁴		
53.06	0.0001	0.001		kg/MMBtu	40 CFR 98 Subpart C Tables C-1 and C-2
1	298	25		GWP	40 CFR 98 Table A-1
8,775.37	0.02	0.17	8,775.55	tpy	
8,775.37	4.93	4.13	8,784.43	tpy CO ₂ e	

⁴ N₂O, CH₄, and CO₂ tpy Emission Rate= EF* Fuel Usage * Fuel Heat Value * 2.20462 lb/1 kg * 1 ton/2000 lb

CO₂e tpy Emission Rate = CO₂ Emission Rate + N₂O Emission Rate*GWP Factor +CH₄ Emission Rate*GWP Factor

Unit: 3b
Description: Gas Tech dehydrator reboiler
3b 3 MMBtu/hr Glycol Dehydrator Reboiler

Control Equipment: Controls flash tank vapors from dehy (Unit 3a), along with the ECD (Unit ECD)
Manufacturer: Gas Tech

Reboiler Emissions

Reboiler Fuel Usage

Fuel Consumption	3.0	MMBtu/hr	Input heat rate
Throughput	200	MMscf/d	Throughput
Fuel heat value	1200	Btu/scf	Nominal LHV of fuel gas
Hourly fuel usage	2.50	Mscf/hr	Fuel usage
Annual fuel usage	21.90	MMscf/yr	Annual usage
Operating hours	8760	hr/yr	

Flash Tank Usage

Flow to Reboiler	759	scf/hr	GRI-GLYCalc - flash tank off gas stream (Sent to Fuel Inlet)
	100%		Percentage sent to the reboiler (as fuel)
	0.76	Mscf/hr	Total fuel routed to Reboiler (flash tank off gas not combusted by ECD)

	NO _x	CO	VOC	SO ₂ ¹	H ₂ S ¹	PM		
Reboiler-unit 3b	100	84	5.5			7.6	lb/MMscf	Unit emission rates from AP-42 Table 1.4-1 & 2 (Assuming average NG)
	117.6	98.8	6.5			8.9	lb/MMscf	Adjusted emission factor: EF X (Fuel Heat Value/1,020 Btu/scf)
Total	0.29	0.25	0.016	0.036	8.93E-04	0.022	lb/hr	lb/MMscf * (Mscf/hr / 1000 Mscf/1 MMscf)
	1.29	1.08	0.07	0.16	3.91E-03	0.10	tpy	

	n-Hexane	Benzene	Toluene	Ethylbenzene	Xylenes	HCOH	Acetaldehyde	Total HAPs	
	0.0092	0.0049	0.0067	0.0139	0.0087	0.0055	0.0048	0.0946	tpy
Total	2.10E-03	1.12E-03	1.53E-03	3.17E-03	1.99E-03	1.26E-03	1.10E-03	0.022	lb/hr
	9.20E-03	4.90E-03	6.70E-03	0.014	8.70E-03	5.50E-03	4.80E-03	0.095	tpy

GRI-HAPCalc (Reboiler-3b)

GHG Calculations

CO ₂ ³	N ₂ O ³	CH ₄ ³	CO ₂ e ³		
53.06	0.0001	0.001		kg/MMBtu	40 CFR 98 Subpart C Tables C-1 and C-2
1	298	25		GWP	40 CFR 98 Table A-1
<u>1537.07</u>	<u>0.0029</u>	<u>0.029</u>		tpy	
		19.8			GRI-GLYCalc (flash tank off gas)
		-			GRI-GLYCalc (flash tank off gas, Routed to Fuel)
1537.1	0.86	0.72	1538.7	tpy CO ₂ e	

³ N₂O, CH₄, and CO₂ tpy Emission Rate= EF* Fuel Usage * Fuel Heat Value * 2.20462 lb/1 kg * 1 ton/2000 lb
CO₂e tpy Emission Rate = CO₂ Emission Rate + N₂O Emission Rate*GWP Factor +CH₄ Emission Rate*GWP Factor

Exhaust Parameters

Heat Rate:	3000	MBtu/hr	
Exhaust temp (Tstk):	800	°F	
Site Elevation:	3060	ft MSL	
Ambient pressure (Pstk):	26.73	in. Hg	Calculated based on elevation
F factor:	10610	wscf/MMBtu	40 CFR 60 Appx A Method 19
Exhaust flow:	530.5	scfm	Calculated from F factor and heat rate
Exhaust flow:	1438.6	acfm	scfm * (Pstd/Pstk)*(Tstk/Tstd), Pstd = 29.92 "Hg, Tstd = 520 °R
Stack diameter:	1.33	ft	Engineering estimate
Stack height:	35	ft	Engineering estimate
Exhaust velocity:	17.3	ft/sec	Exhaust flow ÷ stack area

Site Data

Site Elevation	3060	ft MSL	
Standard Pressure	29.92	in Hg	
Pressure at Elevation	26.75	in Hg	Hess, Introduction to Theoretical Meteorology, eqn. 6.8
Standard Temperature	528	R	

Slop Water Tank Emissions

Unit: T-007
Description: Slop Water Tank from 3-Phase Separator and Dehy

Tank Throughput

226 bbl/day	bbl/yr / 365 day/yr
82,381 bbl/yr	Maximum Throughput
3,459,993 gal/yr	bbl/yr * 42 gal/bbl

**Promax Emissions Report
Annual Emissions**

Components	Working Losses (ton/yr)	Breathing Losses (ton/yr)	Flashing Losses (ton/yr)	Total Losses (ton/yr) ¹
Hydrogen Sulfide	--	--	--	--
Nitrogen	4.50E-6	1.44E-6	0.01	0.01
Carbon Dioxide	0.02	0.01	0.58	0.61
Methane	1.16E-3	3.72E-4	1.03	1.03
Ethane	7.96E-4	2.55E-4	0.62	0.62
Propane	6.92E-5	2.22E-5	0.31	0.31
i-Butane	1.66E-6	5.32E-7	0.03	0.03
n-Butane	4.30E-6	1.38E-6	0.09	0.09
2,2-Dimethylpropane	2.39E-9	7.66E-10	1.50E-4	1.50E-4
i-Pentane	1.64E-7	5.25E-8	0.01	0.01
n-Pentane	2.06E-8	6.59E-9	0.01	0.01
2,2-Dimethylbutane	9.32E-11	2.99E-11	4.09E-5	4.09E-5
Cyclopentane	--	--	--	--
2,3-Dimethylbutane	2.41E-9	7.74E-10	5.66E-4	5.66E-4
2-Methylpentane	2.12E-9	6.80E-10	1.01E-3	1.01E-3
3-Methylpentane	5.41E-9	1.73E-9	1.20E-3	1.20E-3
n-Hexane	5.71E-10	1.83E-10	7.66E-4	7.66E-4
Methylcyclopentane	5.26E-9	1.69E-9	9.57E-4	9.57E-4
Benzene	1.84E-5	5.91E-6	0.06	0.06
Cyclohexane	1.33E-8	4.27E-9	1.49E-3	1.49E-3
2-Methylhexane	3.12E-11	9.99E-12	7.40E-5	7.40E-5
3-Methylhexane	--	--	--	--
2,2,4-Trimethylpentane	2.97E-11	9.52E-12	1.12E-4	1.12E-4
n-Heptane	2.48E-11	7.95E-12	1.56E-4	1.56E-4
Methylcyclohexane	6.88E-10	2.20E-10	3.85E-4	3.85E-4
Toluene	1.16E-6	3.71E-7	0.02	0.02
n-Octane	7.42E-14	2.38E-14	3.98E-6	3.98E-6
Ethylbenzene	1.09E-8	3.50E-9	5.44E-4	5.44E-4
m-Xylene	1.15E-9	3.70E-10	1.00E-4	1.00E-4
p-Xylene	--	--	--	--
o-Xylene	3.80E-8	1.22E-8	1.85E-3	1.85E-3
n-Nonane	2.71E-15	8.67E-16	5.59E-7	5.59E-7
n-Decane	6.01E-18	1.93E-18	1.51E-8	1.51E-8
n-Undecane	--	--	--	--
Safety Factor	25%	25%	25%	--
Total VOC	1.19E-4	3.81E-5	0.67	0.67
Total HAP	2.46E-5	7.87E-6	0.10	0.10

Slop Water Loading Emissions

Unit: LOAD_SLOP

Description: Emissions from Truck Loading of Slop Water

Emission Calculations

Loading from T-006

12,000	Throughput (bbl/yr)	Expected condensate throughput
504,000	Throughput (gal/yr)	bbl/d * 42 gal/bbl * 365 d/yr
10.3	tpy VOC	GRI-HAPCalc 3.01
1%	Based on 1% Crude Oil ¹	
0.10	tpy VOC	

Total HAPs	n-Hexane	Benzene	Toluene	e-Benzene	Xylenes		
0.5	0.41	0.05	0.02	0.0007	0.0012	tpy	GRI-HAPCalc3.01
1%	1%	1%	1%	1%	1%	%	Based on 1% Crude Oil ¹
4.71E-03	4.08E-03	4.56E-04	1.51E-04	7.00E-06	1.20E-05	tpy	

¹ Assume slop water contains 1% hydrocarbons per TCEQ guidance.

Loading from T-007

4.81E-5	Calculated VOC Emissions (tpy)	Calculated using ProMax
25%	Safety Factor	
6.01E-5	tpy VOC	

Total HAPs	n-Hexane	Benzene	Toluene	e-Benzene	Xylenes		
9.94E-06	2.89E-10	9.33E-06	5.86E-07	5.52E-09	1.98E-08	tpy	Calculated using ProMax
25%	25%	25%	25%	25%	25%	%	Safety Factor
1.24E-05	3.61E-10	1.17E-05	7.32E-07	6.90E-09	2.48E-08	tpy	

Total Emissions

0.10 tpy VOC

Total HAPs	n-Hexane	Benzene	Toluene	e-Benzene	Xylenes	
4.72E-03	4.08E-03	4.68E-04	1.52E-04	7.01E-06	1.20E-05	tpy

Unit: ECD
 Description: BTEX Combustor
 DRE: 98%

Pilot Emissions

MW of fuel gas	16.04	lb/lb-mol	Estimated, nominal for natural gas
Pilot fuel flow	100	scf/hr	Engineering estimate
Fuel heating value	1200	Btu/scf	Estimated, nominal for LHV natural gas
Heat rate	0.12	MMBtu/hr	Btu/scf * scf/hr / 1,000,000
Annual fuel usage	0.88	MMscf/yr	scf/hr * 8760 hrs/yr / 1,000,000

Flash Tank & Still Vent Emissions

Still Vent Flow	362	scf/hr	GRI-GLYCalc Controlled Regenerator Stream
Still Vent Heating Value	2356.59	Btu/scf	Estimated using weighted heat values of components
Flash Tank Flow	759	scf/hr	GRI-GLYCalc Flash Tank Off Gas Stream
Percentage Sent to ECD	50%		Percentage sent to ECD for combustion. Remaining vapors are sent to reboiler as fuel.
Flash Tank Flow to ECD	380	scf/hr	
Flash Tank Heating Value	1447.76	Btu/scf	Estimated using weighted heat values of components
Total Flow	742	scf/hr	BTEX Still Vent + Flash Tank Vapors sent to ECD
Total Heating Value	1891.45	Btu/scf	Weighted average of BTEX Still Vent and Flash Tank streams
Total Heating Rate	1.40	MMBtu/hr	Btu/scf * scf/hr / 1,000,000
Annual fuel usage	6.50	MMscf/yr	scf/hr * 8760 hrs/yr / 1,000,000

Emission Rates

	NO _x	CO	VOC ¹	H ₂ S ²	SO ₂ ³	PM	HAPs ¹	
	100	84				7.6		lb/MMscf AP-42 Tables 1.4-1 & 2
	117.65	98.82				8.94		lb/MMscf Adjusted emission factor (Pilot): EF X (Fuel Heat Value/1,020 Btu/scf)
	185.44	155.77				14.09		lb/MMscf Adjusted emission factor (Still Vent & Flash Tank Vapors): EF X (Fuel Heat Value/1,020 Btu/scf)
Emission Factors			34.59	0.035			7.82	lb/hr Still Vent: GRI-GLYCalc Controlled Regenerator Emissions Stream
			8.65	1.80E-03			0.14	lb/hr Flash Tank: GRI-GLYCalc Flash Tank Off Gas Stream
								lb H ₂ S/hr Pilot Gas: Sweet natural gas fuel, 0.25 gr H ₂ S/100scf
					0.0014			lb SO ₂ /hr Pilot Gas: Sweet natural gas fuel, 5 gr S/100scf
Pilot	0.012	9.88E-03	-	3.50E-05	6.588E-05	-	-	lb/hr 98% combustion H ₂ S; 100% H ₂ S -> SO ₂
	0.052	0.043	-	1.53E-04	2.89E-04	-	-	tpy
Glycol Regenerator Still Vent & Flash Tank	0.138	0.116	0.86	7.26E-04	0.067	5.10E-03	0.16	lb/hr 98% combustion H ₂ S; 100% H ₂ S -> SO ₂
	0.60	0.51	3.79	3.18E-03	0.29	0.022	0.70	tpy
Total (Pilot + Gases)	0.15	0.125	0.86	7.61E-04	0.067	5.10E-03	0.16	lb/hr
	0.65	0.55	3.79	3.33E-03	0.29	0.022	0.70	tpy lb/hr * (8760 hr/yr operation) / 2000 lb/ton

n-Hexane Benzene Toluene Xylenes Total HAPs

0.80	4.16	2.59	0.28	7.82	lb/hr	Still Vent: GRI-GLYCalc Controlled Regenerator Emissions Stream
0.11	0.04	0.03	3.00E-03	0.17	lb/hr	Flash Tank: GRI-GLYCalc Flash Tank Off Gas Stream
0.018	0.08	0.05	0.006	0.16	lb/hr	
0.08	0.37	0.23	0.02	0.70	tpy	

¹ Pilot fuel is purchased natural gas, comprised mainly of methane. VOC and HAP emissions from pilot only are assumed to be negligible.

² Pilot H₂S emissions based on 0.25 g/100 scf H₂S in fuel, 98% combustion.
 0.25 gr H₂S/100 scf * fuel scf/hr * 1 lb/7000 gr = lb/hr H₂S (prior to combustion and conversion to SO₂)

³ SO₂ emissions based on sulfur content of 5 g/100 scf S in fuel and 100% combustion of H₂S to SO₂.
 5 gr S/100 scf * fuel scf/hr * 1 lb/7000 gr * 64 lb SO₂/32 lb S = lb/hr SO₂

GHG Calculations

CO ₂ ⁴	N ₂ O ⁴	CH ₄ ⁴	CO ₂ e ⁴	
53.06	0.0001	0.001		kg/MMBtu 40 CFR 98 Subpart C Tables C-1 and C-2
1	298	25		GWP 40 CFR 98 Table A-1
61.5	0.0001	0.001		tpy
		9.04		tpy Still Vent: GRI-GLYCalc Controlled Regenerator Emissions Stream
		43.34		tpy Flash Tank: GRI-GLYCalc Flash Tank Off Gas Stream
		1.05		tpy Controlled emissions with 98% Combustion Control
61.5	0.03	26.22	87.7	tpy CO ₂ e

⁴ N₂O, CH₄, and CO₂ tpy Emission Rate = EF * Fuel Usage * Fuel Heat Value * 2.20462 lb/1 kg * 1 ton/2000 lb
 CO₂e tpy Emission Rate = CO₂ Emission Rate + N₂O Emission Rate * GWP Factor + CH₄ Emission Rate * GWP Factor

Exhaust Parameters

Heat Rate:	1522.51	MBtu/hr	Design Specification
Exhaust temp (Tstk):	650	°F	Eng Estimate
Site Elevation:	3060	ft MSL	
Ambient pressure (Pstk):	26.73	in. Hg	Calculated based on elevation
F factor:	10610	wscf/MMBtu	40 CFR 60 Appx A Method 19
Exhaust flow:	269.2	scfm	Calculated from F factor and heat rate
Exhaust flow:	643.2	acfm	scfm * (Pstd/Pstk) * (Tstk/Tstd), Pstd = 29.92 "Hg, Tstd = 520 °R
Stack diameter:	4.5	ft	Spec Sheet
Stack height:	11.99	ft	Spec Sheet
Exhaust velocity:	0.67	ft/sec	Exhaust flow ÷ stack area

Site Data

Site Elevation	3060	ft MSL	
Standard Pressure	29.92	in Hg	
Pressure at Elevation	26.75	in Hg	Hess, Introduction to Theoretical Meteorology, eqn. 6.8
Standard Temperature	528	R	

Flare Alternative Operating Scenario

Unit: Flare (Process)
Description: Combustion of vapors from condensate stabilizer - alternative operating scenario

Pilot Emissions

MW of fuel gas	16.04	lb/lb-mol	Estimated, nominal for natural gas
Pilot fuel flow	100	scf/hr	Engineering estimate
Fuel heating value	1200	Btu/scf	Estimated, nominal for LHV natural gas
Heat rate	0.12	MMBtu/hr	Btu/scf * scf/hr / 1,000,000
Annual fuel usage	0.88	MMscf/yr	scf/hr * 8760 hrs/yr / 1,000,000

Pilot Emission Calculations

NOx	CO	VOC ¹	H ₂ S ²	SO ₂ ³	HAPs ¹	
0.0680	0.3100					lb/MMBtu
103%						%
			3.57E-05			lb H ₂ S/hr
				0.0014		lb SO ₂ /hr
			7.1E-07	6.6E-05		lb/hr
0.0166	0.037	-	7.1E-07	0.0015	-	lb/hr
0.0181	0.041	-	7.8E-07	0.0016	-	tpy
0.073	0.163	-	3.1E-06	0.0065	-	tpy

¹ Fuel is purchased natural gas, comprised mainly of methane. VOC and HAP emissions from pilot only are assumed to be negligible.

² H₂S emissions based on 0.25 g/100 scf H₂S in fuel, 98% combustion.
 0.25 gr H₂S/100 scf * fuel scf/hr * 1 lb/7000 gr = lb/hr H₂S (prior to combustion and conversion to SO₂)

³ SO₂ emissions based on sulfur content of 5 g/100 scf S in fuel and 100% combustion of H₂S to SO₂.

5 gr S/100 scf * fuel scf/hr * 1 lb/7000 gr * 64 lb SO₂/32 lb S = lb/hr SO₂

⁴ TCEQ EF factors were removed from calculation; SF used to maintain emissions as currently permitted.

Source: **Armstrong Gas Lab Analysis No. 211306**

Component	MW	vol/mol % Gas Analysis	Dry vol/mol%	MW * dry vol %	Spec. Volume (scf/lb)	Flow (scf/hr)	Loading (lb/hr)	Annual Flow (scf/yr)	Annual Loading (lb/yr)
Water	18.02	0.000%							
Nitrogen	28.01	0.412%	0.414%	0.116	13.547	259	19.102	186,314.1	13,753.2
CO2	44.01	1.020%	1.025%	0.451	8.623	641	74.298	461,284.7	53,494.7
H2S	34.08	0.050%	0.050%	0.017	11.136	31	2.821	22,616.4	2,030.9
Methane	16.04	45.293%	45.527%	7.304	23.65	28455	1203.152	20,487,273.4	866,269.5
Ethane	30.07	15.926%	16.008%	4.814	12.62	10005	792.795	7,203,649.3	570,812.2
Propane	44.10	22.771%	22.889%	10.093	8.606	14305	1662.258	10,299,883.7	1,196,825.9
i-Butane	58.12	4.100%	4.121%	2.395	6.529	2576	394.501	1,854,502.0	284,040.7
n-Butane	58.12	7.034%	7.071%	4.110	6.529	4419	676.846	3,181,769.7	487,328.8
i-Pentane	72.15	1.333%	1.340%	0.967	5.26	838	159.256	603,134.9	114,664.4
n-Pentane	72.15	1.120%	1.126%	0.812	5.26	703	133.745	506,517.5	96,296.1
Cyclopentane	70.14	0.000%	0.000%	0.000	5.411	0	0.000	0.0	0.0
n-Hexane	86.18	0.196%	0.197%	0.170	4.404	123	28.006	88,804.9	20,164.6
Cyclohexane	84.16	0.000%	0.000%	0.000	4.509	0	0.000	0.0	0.0
Other Hexanes	84.16	0.000%	0.000%	0.000	4.509	0	0.000	0.0	0.0
Heptanes	100.20	0.059%	0.059%	0.059	3.787	37	9.794	26,705.8	7,052.0
Methylcyclohexane	98.19	0.000%	0.000%	0.000	3.865	0	0.000	0.0	0.0
2,2,4-Trimethylpentane	114.23	0.000%	0.000%	0.000	3.322	0	0.000	0.0	0.0
Benzene	78.11	0.029%	0.029%	0.023	4.858	18	3.772	13,192.0	2,715.5
Toluene	92.14	0.028%	0.029%	0.026	4.119	18	4.340	12,870.3	3,124.6
Ethylbenzene	106.17	0.002%	0.002%	0.002	3.574	1	0.375	965.3	270.1
Xylenes	106.17	0.016%	0.016%	0.017	3.574	10	2.876	7,400.4	2,070.6
C8+ heavies	114.23	0.095%	0.096%	0.109	3.322	60	18.026	43,115.4	12,978.8
Total		99.5%	100.0%	20.83		62500	5186.0	45,000,000.0	2,227,532.2
Dry total		99.5%							

Note: * Although the RVP 11 gas simulation did not account and H₂S it was determined that a 0.05% wet/mol % will be used to overcome gas composition fluctuations.

Uncontrolled VOC Emissions 36.98%
Uncontrolled HAP Emissions 39.4 lb/hr
3,093.8 lb/hr
2,227,532.2 lb/yr
28,345.4 lb/yr

Gas to Flare
 62,500 scf/hr maximum expected flow of 1.5MMscf/day; assumed 24 hour operation
 45,000,000 scf/yr maximum expected annual flow
 1,828.35 Btu/scf
 114.27 MMBtu/hr
 82,275.84 Mmbtu/yr
 20.83 MW

Pilot Gas to Flare
 100.00 scf/hr
 16.04 MW

Totals all streams
 62,600.00 scf/hr
 20.82 MW
 volume-weighted average

NOx	CO	VOC	H ₂ S	SO ₂	n-Hexane	Benzene	Toluene	Ethylbenzene	Xylenes	HAPs	
0.0680	0.3100										lb/MMBtu
	77%			0.10							%
7.8	62.8	61.9	0.056	0.10	0.56	0.075	0.087	0.008	0.058	0.79	lb/hr
2.8	22.6	22.3	0.020	0.46	0.20	0.027	0.031	0.003	0.021	0.28	lb/hr
											tpy

¹ TCEQ EF factors were removed from calculation; SF used to maintain emissions as currently permitted.

Flare Emission Totals (Pilot + Inlet Gases)

NOx	CO	VOC	H ₂ S	SO ₂	n-Hexane	Benzene	Toluene	Ethylbenzene	Xylenes	HAPs	
7.8	62.8	61.9	5.6E-02	1.1E-01	0.56	0.075	0.087	0.0075	0.058	0.79	lb/hr
2.8	22.6	22.3	2.0E-02	4.6E-01	0.20	0.027	0.031	0.0027	0.021	0.28	tpy

Stack Parameters

1000 °C Exhaust temperature Per NMAQB guidelines
 20 m/sec Exhaust velocity Per NMAQB guidelines
 65 ft Flare height Engineering design

Pilot only
 8,400 cal/sec Heat release (q) MMBtu/hr * 10⁶ * 252 cal/Btu + 3600 sec/hr
 6,785 q_n q_n = q(1-0.048(MW)^{1/2})
 0.08 m Effective stack diameter (D) D = (10⁻⁶q_n)^{1/2}

Pilot and Normal Operation
 114.4 MMBtu/hr Total heat input Sum of fuel and flare gas heating values
 20.82 g/mol Total mean MW Volume weighted average of gas MWs

8,007,440 cal/sec Heat release (q) MMBtu/hr * 10⁶ * 252 cal/Btu + 3600 sec/hr
 6,253,560 q_n q_n = q(1-0.048(MW)^{1/2})
 2.501 m Effective stack diameter (D) D = (10⁻⁶q_n)^{1/2}

Flare GHG Emissions

§98.233(n) Flare stack GHG emissions.

Flared Amine vent gas & Assist Gas

Step 1. Calculate contribution of un-combusted CH₄ emissions

$$E_{a,CH_4} (\text{un-combusted}) = V_a * (1 - \eta) * X_{CH_4} \quad (\text{Equation W-39B})$$

where:

E_{a,CH_4} = contribution of annual un-combusted CH₄ emissions from regenerator in cubic feet under actual conditions.

V_a = volume of gas sent to combustion unit during the year (cf)

η = Fraction of gas combusted by a burning flare (or regenerator), default value from Subpart W = 0.98

For gas sent to an unlit flare, η is zero.

X_{CH_4} = Mole fraction of CH₄ in gas to the flare =

Client Analysis	0.452929	Pilot NG Composition	0.9500
-----------------	----------	----------------------	--------

Step 2. Calculate contribution of un-combusted CO₂ emissions

$$E_{a,CO_2} = V_a * X_{CO_2} \quad (\text{Equation W-20})$$

where:

E_{a,CO_2} = contribution of annual un-combusted CO₂ emissions from regenerator in cubic feet under actual conditions.

V_a = volume of gas sent to combustion unit during the year (cf)

X_{CO_2} = Mole fraction of CO₂ in gas to the flare =

Client Analysis	0.010198	Pilot NG Composition	0.005
-----------------	----------	----------------------	-------

Step 3. Calculate contribution of combusted CO₂ emissions

$$E_{a,CO_2} (\text{combusted}) = \sum (\eta * V_a * Y_j * R_j) \quad (\text{Equation W-21})$$

where:

η = Fraction of gas combusted by a burning flare (or regenerator) = 0.98

For gas sent to an unlit flare, η is zero.

V_a = volume of gas sent to combustion unit during the year (cf)

Y_j = mole fraction of gas hydrocarbon constituents j:

Client Analysis	0.452929	Pilot NG Composition	0.9500
Constituent j, Methane =	0.159257		0.0320
Constituent j, Ethane =	0.227708		0.0020
Constituent j, Propane =	0.111341		0.00060
Constituent j, Butane =	0.028800006		0.015

R_j = number of carbon atoms in the gas hydrocarbon constituent j:

Constituent j, Methane =	1
Constituent j, Ethane =	2
Constituent j, Propane =	3
Constituent j, Butane =	4
Constituent j, Pentanes Plus =	5

Step 4. Calculate GHG volumetric emissions at standard conditions (scf).

$$E_{s,i} = \frac{E_{a,i} * (459.67 + T_s) * P_a}{(459.67 + T_a) * P_s} \quad (\text{Equation W-33})$$

where:

$E_{s,i}$ = GHG i volumetric emissions at standard temperature and pressure (STP) in cubic feet

$E_{a,i}$ = GHG i volumetric emissions at actual conditions (cf)

T_s = Temperature at standard conditions (F) = 60 F

T_a = Temperature at actual conditions (F) = 76 F

P_s = Absolute pressure at standard conditions (psia) = 14.7 psia

P_a = Absolute pressure at actual conditions (psia) = 14.7 psia (Assumption)

Constant = 459.67 (temperature conversion from F to R)

(Based on Annual Avg Max Temperature for Hobbs, NM from Western Regional Climate Center)

Step 5. Calculate annual CH₄ and CO₂ mass emissions (ton).

$$Mass_{s,i} = E_{s,i} * \rho_i * 0.0011023 \quad (\text{Equation W-36})$$

where:

$Mass_{s,i}$ = GHG i (CO₂, CH₄, or N₂O) mass emissions at standard conditions in tons (tpy)

$E_{s,i}$ = GHG i (CO₂, CH₄, or N₂O) volumetric emissions at standard conditions (cf)

ρ_i = Density of GHG i. Use:

CH₄: 0.0192 kg/ft³ (at 60F and 14.7 psia)

CO₂: 0.0526 kg/ft³ (at 60F and 14.7 psia)

Step 6. Calculate annual N₂O emissions from portable or stationary fuel combustion sources under actual conditions (cf) using Equation W-40 .

$$Mass_{N_2O} = 0.0011023 * Fuel * HHV * EF \quad (\text{Equation W-40})$$

where:

$Mass_{N_2O}$ = annual N₂O emissions from combustion of a particular type of fuel (tons).

Fuel = mass or volume of the fuel combusted

HHV = high heat value of the fuel

Pilot Gas = 1.200E-03 MMBtu/scf

Inlet Gas = 1.828E-03 MMBtu/scf

EF = 1.00E-04 kg N₂O/MMBtu

10⁻³ = conversion factor from kg to metric tons.

Step 7. Calculate total annual emission from flare by summing Equations W-40, W-19, W-20, and W-21.

Gas Sent to Flare	Gas Sent to Flare (cf/yr)	CH ₄ Un-Combusted, E_{a,CH_4} (cf)	CO ₂ Un-Combusted, E_{a,CO_2} (cf)	CO ₂ Combusted, E_{a,CO_2} (cf)	CH ₄ Un-Combusted, E_{a,CH_4} (scf)	CO ₂ Un-Combusted, E_{a,CO_2} (scf)	CO ₂ Combusted, E_{a,CO_2} (scf)	CH ₄ Un-Combusted, E_{a,CH_4} (tpy)	CO ₂ Un-Combusted, E_{a,CO_2} (tpy)	CO ₂ Combusted, E_{a,CO_2} (tpy)	N ₂ O Mass Emissions (tpy)	CO ₂ e (tpy)
Inlet Gas	45,000,000	407,636.1	458,910.0	90,137,358.4	395,239.0	444,953.6	87,396,087.5	8.4	25.8	5,067.3	0.0091	5,304.9
Pilot Gas	876,000	16,644.0	4,380.0	943,812.9	16,137.8	4,246.8	915,109.5	0.34	0.25	53.1	0.0001	61.9
							Total	8.7	26.0	5,120.4	0.0092	5,366.8

	CO ₂	CH ₄	N ₂ O
GWP	1	25	298

Flare SSM Emissions

Unit: Flare (SSM)
Description: Flare controlling blowdown and emergency emissions from the facility

Flaring Excess Gas When Plant is Down

Stream 11 26274.78 scf/hr
 2163.24 Btu/scf
 56.84 MMBtu/hr
 37.87 lb/lbmol

Totals all streams 26274.78 scf/hr
 37.87 MW volume-weighted average

	NOx	CO	VOC	H ₂ S	SO ₂	HAPs	PM	Units	
	0.0680	0.3100						lb/MMBtu	AP-42 Tables 13.5-1 & 13.5-2 (02/18)
	0.0641	0.5496						lb/MMBtu	TNRCC RG-109 High Btu ("Other")
				0.0000				% H2S	Max est. concentration from inlet
Stream 11	3.8650	31.2386	-	-	-	-	-	lb/hr	lb/MMBtu * MMBtu/hr
	-	-	38.0652	-	-	0.0040	-	lb/hr	98% destruction of calculated content
	-	-	-	-	-	-	-	lb/hr	Estimated 100% conversion of combusted H ₂ S to SO ₂
	3.87	31.24	38.07	-	-	0.0040	-	lb/hr	Total; Flared gas (upset)
	100%	100%	100%	-	-	100%	100%	%	Safety Factor
	7.7	62.5	76.1	-	-	0.0080	-	lb/hr	
	0.201	1.62	1.98	-	-	2.07E-04	-	tpy	Total; Upset Flared gas
									Assume 52 events of 1 hr duration for upset conditions

Flare SSM Emissions

Unit: Flare (SSM)
Description: Flare controlling blowdown and emergency emissions from the facility

Stack Parameters

1000 °C	Exhaust temperature	Per NMAQB guidelines
20 m/sec	Exhaust velocity	Per NMAQB guidelines
65 ft	Flare height	Engineering design

Upset flare gas

56.8 MMBtu/hr	Total heat input	Sum of fuel and flare gas heating values
37.87 g/mol	Total mean MW	Volume weighted average of gas MWs
3,978,713 cal/sec	Heat release (q)	$\text{MMBtu/hr} * 10^6 * 252 \text{ cal/Btu} \div 3600 \text{ sec/hr}$
2,803,389	q_n	$q_n = q(1-0.048(\text{MW})^{1/2})$
1.674 m	Effective stack diameter (D)	$D = (10^{-6}q_n)^{1/2}$

Combined Normal and SSM Emission Scenario

NOx	CO	VOC	SO ₂	H2S	Units
15.52	125.32	138.0	-	-	lb/hr
3.02	24.27	24.25	-	-	tpy

Pilot, Normal and Upset Combined Flow

171.2 MMBtu/hr	Total heat input	Sum of fuel and flare gas heating values
37.87 g/mol	Total mean MW	Volume weighted average of gas MWs
1.20E+07 cal/sec	Heat release (q)	$\text{MMBtu/hr} * 10^6 * 252 \text{ cal/Btu} \div 3600 \text{ sec/hr}$
8,445,408	q_n	$q_n = q(1-0.048(\text{MW})^{1/2})$
2.9061 m	Effective stack diameter (D)	$D = (10^{-6}q_n)^{1/2}$

Emission unit: F-001

Facility-wide Fugitive Emissions Per Piece of Equipment							
Subcomponent		Emission Factor ¹ (lb/hr/comp)	Control Efficiency	VOC Content ² (wt%)	H ₂ S Content ² (wt%)	HAP Content ² (wt%)	Subcomponent Counts ^{3,6}
Valves	Gas	9.92E-03	0.0%	21.99%	0.00%	0.56%	1089
	Light Oil	5.51E-03	0.0%	100.00%	0.00000%	12.51%	1089
	Heavy Oil	1.85E-05	0.0%	0.00%	0.00000%	0.00%	0
Flanges	Gas	8.60E-04	0.0%	21.99%	0.0000%	0.56%	0
	Light Oil	2.43E-04	0.0%	100.00%	0.000000%	12.51%	0
	Heavy Oil	8.60E-07	0.0%	0.00%	0.000000%	0.00%	0
Connectors	Gas	4.41E-04	0.0%	21.99%	0.00%	0.56%	2673
	Light Oil	4.63E-04	0.0%	100.00%	0.00000%	12.51%	2673
	Heavy Oil	1.65E-05	0.0%	0.00%	0.00000%	0.00%	0
Pumps	Light Oil	2.87E-02	0.0%	100.00%	0.00000%	12.51%	13
	Heavy Oil	2.87E-02	0.0%	0.00%	0.00000%	0.00%	0
Other	Gas	1.94E-02	0.0%	21.99%	0.00%	0.56%	0
	Light Oil	1.65E-02	0.0%	100.00%	0.00000%	12.51%	0
	Heavy Oil	7.06E-05	0.0%	0.00%	0.00000%	0.00%	0
Safety Factor⁶							0.25
Hourly VOC Emission Rate (lb/hr)⁴							10.25
Annual VOC Emission Rate (tpy)⁵							44.88
Hourly H₂S Emission Rate (lb/hr)⁴							0.00
Annual H₂S Emission Rate (tpy)⁵							0.00
Hourly HAP Emission Rate (lb/hr)⁴							1.02
Annual HAP Emission Rate (tpy)⁵							4.47

¹ Emission factors from Table 2-4 of EPA Protocol for Equipment Leak Emission Estimates, 1995.

² Weight percent of gas and liquid components are referenced from flash gas and liquid streams from a ProMax simulation for this facility.

³ Subcomponent counts for each subcomponent are based on estimated average component counts for each piece of equipment.

⁴ Hourly Emissions [lb/hr] = Emissions Factor [lb/hr/component] * Weight Content of Chemical Component [%] * Subcomponent Count.

⁵ Annual Emissions [ton/yr] = Hourly Emissions [lb/hr] * 8760 [hr/yr] * 1/2000 [ton/lb].

⁶ The safety factor of 25% is added to accommodate the addition of the CAT G3608 engines.

Facility Malfunction Emissions

Unit: MALF

Description: Facility-wide malfunction emissions

Emission Calculations

Requested NO _x MALF:	6 tons/yr
Requested CO MALF:	10 tons/yr
Requested VOC MALF:	10 tons/yr
Requested SO _x MALF:	10 tons/yr
Requested H ₂ S MALF:	2 tons/yr
Inlet gas VOC content:	21.99 Mass %
Inlet gas CO ₂ content:	3.28 Mass %
Inlet gas CH ₄ content:	57.05 Mass %

Section 6

Subsection 2 – Emission Calculations for All Other Units at this Facility Not Affected by this Application

For clarity, this Subsection 2 contains emission calculations for all other units that were not affected by this application (i.e. all units except for Units 1, 2, 6, 7, 8, 9, 10, 3a, 3b, T-007, LOAD_SLOP, ECD, Flare , F-001, and MALF). For pertinent calculations relevant to the changes at the facility in this application, please refer to Section 6 Subsection 1.

Unit: 5
 Description: Solar Centaur 40-4700 NG turbines

Fuel consumption 33.5 Mscf/hr
 Fuel heat value 1200 Btu/scf Nominal LHV of fuel gas
 Heat rate 40.2 MMBtu/hr Fuel consumption * fuel heat value / 1000
 Annual fuel usage 293.5 MMscf/yr 8760 hrs/yr operation

Uncontrolled Emissions

NO _x	CO	VOC	SO ₂ ¹	PM ²	H ₂ S ¹		
				0.0066	-	lb/MMBtu	AP-42 Table 3.1-2a
0.100	0.122	0.035				lb/MMBtu	Hourly Emission Factors
0.100	0.122	0.035				lb/MMBtu	Annual emission rate (8760 hrs/yr)
4.03	4.90	1.40	0.48	0.27		lb/hr	
17.64	21.48	6.15	2.10	1.16	-	tpy	
10%	20%						Safety Factor
4.43	5.89	1.40	0.48	0.27	2.39E-04	lb/hr	Emission Rate with Safety Factor
19.40	25.78	6.15	2.10	1.16	1.05E-03	tpy	
Total HAP ³	HCHO ³	Acetaldehyde ³	Benzene ³	Toluene ³	Xylenes ³		
	7.10E-04	4.00E-05	1.20E-05	1.30E-04	6.40E-05	lb/MMBtu	AP-42 Table 3.1-3
0.038	0.029	0.002	4.82E-04	0.0052	0.0026	lb/hr	Hourly emission rate
0.17	0.13	0.0070	0.0021	0.023	0.011	tpy	Annual emission rate (8760 hrs/yr)

¹ SO₂ emissions based on fuel sulfur content of 5 gr S/100 scf, or 0.00714 lb S/Mscf
 lb/hr SO₂ = 5gr S/100scf * Fuel consumption (Mscf/hr) * 1lb/7000gr * 1000scf/Mscf * 64 lb SO₂/32 lb S
 H₂S emissions based on 0.25 g/100 scf H₂S in fuel
 lb/hr H₂S = 0.25 gr H₂S/100 scf * Fuel consumption (Mscf/hr) * 1000scf/Mscf * 1 lb/7000 gr * (1 - Comb. Eff [98%])
² Assumed TSP = PM₁₀ = PM_{2.5}
³ HAP emissions calculated using emission factors from AP-42 Table 3.1-3.

GHG Calculations

CO ₂ ⁴	N ₂ O ⁴	CH ₄ ⁴	CO ₂ e ⁴		
53.06	0.0001	0.001		kg/MMBtu	40 CFR 98 Subpart C Tables C-1 and C-2
1	298	25		GWP	40 CFR 98 Table A-1
20596.9	0.039	0.39		tpy	
20596.866	11.6	9.7	20618.1	tpy CO ₂ e	

⁴ N₂O, CH₄, and CO₂ tpy Emission Rate= EF* Fuel Usage * Fuel Heat Value * 2.20462 lb/1 kg * 1 ton/2000 lb
 CO₂e tpy Emission Rate = CO₂ Emission Rate + N₂O Emission Rate*GWP Factor +CH₄ Emission Rate*GWP Factor

Slop Water Tank Emissions

Unit: T-006
Description: Slop Water Tank from 3-Phase Separator and Dehy

Tank Throughput

33 bbl/day	bbl/yr / 365 day/yr
12,000 bbl/yr	Maximum Throughput
504,000 gal/yr	bbl/yr * 42 gal/bbl

**Promax Emissions Report
Annual Emissions**

Components	Working Losses (ton/yr)	Breathing Losses (ton/yr)	Total Losses (ton/yr) ¹
Hydrogen Sulfide	3.28692E-05	1.89576E-05	5.18268E-05
Nitrogen	1.10618E-05	6.38002E-06	1.74418E-05
Carbon Dioxide	0.002045151	0.001179563	0.003224714
Methane	0.000521325	0.00030068	0.000822004
Ethane	0.00410824	0.002369471	0.006477712
Propane	0.009757611	0.005627806	0.015385417
i-Butane	0.001901042	0.001096446	0.002997489
n-Butane	0.00583467	0.003365208	0.009199879
2,2-Dimethylpropane	0	0	0
i-Pentane	0.001544366	0.00089073	0.002435096
n-Pentane	0.001627716	0.000938803	0.002566519
2,2-Dimethylbutane	0	0	0
Cyclopentane	0	0	0
2,3-Dimethylbutane	0	0	0
2-Methylpentane	0	0	0
3-Methylpentane	0	0	0
n-Hexane	0.000416481	0.00024021	0.00065669
Methylcyclopentane	0	0	0
Benzene	0.002117181	0.001221107	0.003338287
Cyclohexane	0.000822733	0.00047452	0.001297252
2-Methylhexane	0	0	0
3-Methylhexane	0	0	0
2,2,4-Trimethylpentane	0	0	0
n-Heptane	0.000369694	0.000213225	0.000582919
Methylcyclohexane	0.000511008	0.000294729	0.000805737
Toluene	0.00118465	0.00068326	0.00186791
n-Octane	0.000519775	0.000299786	0.000819561
Ethylbenzene	6.81112E-08	3.92839E-08	1.07395E-07
m-Xylene	0.000140878	8.12527E-05	0.00022213
p-Xylene	0	0	0
o-Xylene	0	0	0
n-Nonane	0	0	0
n-Decane	0	0	0
n-Undecane	0	0	0
Safety Factor	100%	100%	100%
Total VOC	0.0535	0.0309	0.0843
Total HAP	7.72E-03	4.45E-03	1.22E-02

¹ Emissions are assumed to be 1% condensate.

Condensate Tank Emissions

Unit: T-008, 009, T-011, T-012
Description: Stabilized condensate tanks
of tanks 4
Tank Throughput* 190 bbl/day

Tanks 4.09d Emissions Report
Annual Emissions

Components	Uncontrolled Emissions per Tank			Uncontrolled Tank Battery
	Working Losses (ton/yr)	Breathing Losses (ton/yr)	Total Losses (ton/yr)	Total Losses (ton/yr)
Hydrogen Sulfide	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Nitrogen	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Carbon Dioxide	1.16E-11	1.10E-11	2.26E-11	9.04E-11
Methane	1.05E-13	1.00E-13	2.05E-13	8.19E-13
Ethane	7.64E-08	7.28E-08	1.49E-07	5.97E-07
Propane	4.13E-04	3.93E-04	8.06E-04	3.22E-03
i-Butane	2.98E-02	2.84E-02	5.83E-02	2.33E-01
n-Butane	7.27E-01	6.93E-01	1.42E+00	5.68E+00
2,2-Dimethylpropane	1.45E-02	1.39E-02	2.84E-02	1.14E-01
i-Pentane	6.38E-01	6.08E-01	1.25E+00	4.99E+00
n-Pentane	5.78E-01	5.51E-01	1.13E+00	4.51E+00
2,2-Dimethylbutane	5.63E-03	5.37E-03	1.10E-02	4.40E-02
Cyclopentane	0.00E+00	0.00E+00	0.00E+00	0.00E+00
2,3-Dimethylbutane	3.99E-02	3.80E-02	7.80E-02	3.12E-01
2-Methylpentane	9.24E-02	8.80E-02	1.80E-01	7.22E-01
3-Methylpentane	4.87E-02	4.65E-02	9.52E-02	3.81E-01
n-Hexane	8.57E-02	8.17E-02	1.67E-01	6.70E-01
Methylcyclopentane	3.96E-02	3.77E-02	7.73E-02	3.09E-01
Benzene	1.10E-02	1.05E-02	2.15E-02	8.58E-02
Cyclohexane	2.72E-02	2.59E-02	5.32E-02	2.13E-01
2-Methylhexane	7.08E-03	6.75E-03	1.38E-02	5.53E-02
3-Methylhexane	7.97E-03	7.59E-03	1.56E-02	6.22E-02
2,2,4-Trimethylpentane	0.00E+00	0.00E+00	0.00E+00	0.00E+00
n-Heptane	3.02E-02	2.88E-02	5.89E-02	2.36E-01
Methylcyclohexane	1.65E-02	1.58E-02	3.23E-02	1.29E-01
Toluene	3.94E-03	3.76E-03	7.70E-03	3.08E-02
n-Octane	7.97E-03	7.60E-03	1.56E-02	6.23E-02
Ethylbenzene	1.84E-04	1.76E-04	3.60E-04	1.44E-03
m-Xylene	1.71E-04	1.63E-04	3.33E-04	1.33E-03
p-Xylene	1.78E-04	1.70E-04	3.48E-04	1.39E-03
o-Xylene	0.00E+00	0.00E+00	0.00E+00	0.00E+00
n-Nonane	7.42E-04	7.07E-04	1.45E-03	5.80E-03
n-Decane	0.00E+00	0.00E+00	0.00E+00	0.00E+00
n-Undecane	0.00E+00	0.00E+00	0.00E+00	0.00E+00
TOTAL VOC	2.41	2.30	4.71	18.85
TOTAL HAPs	0.101	0.096	0.20	0.79

* Facility throughput will be 190 bbl/day. Each tank has the potential to route entire facility throughput through a give tank however actual throughput will likely be much lower.

Venting VOC Emissions

Unit: VENT
Description: Emission rates from venting during startup, shutdown, and blowdown operation

Volume Vented Calculations

	Venting Unit	Volume (Mscf)	Events/yr	Gas Stream	Volume Vented (Mscf/yr)
	1	9	120	Inlet	1080
	2	9	120	Inlet	1080
Totals			240		2160
Total (hrs)			240		

Assumes 1 hour per event

Source: Promax RVP11 Simulation, SC Vapor Stream, from File: ProMax Report South Carlsbad_8

Component	MW	Wet vol/mol %	Dry vol/mol %	MW * dry vol %	Mass Fraction (dry)	Spec. Volume ft ³ /lb	Spec. Volume VOC ft ³ /lb
Water	18.02	0.015%				21.06	
Nitrogen	28.01	2.72%	2.72%	0.762	3.54%	13.547	
CO ₂	44.01	1.61%	1.61%	0.706	3.28%	8.623	
H ₂ S*	34.08	0.05%	0.05%	1.70%	0.08%	11.136	
Methane	16.04	76.6%	76.58%	12.286	57.09%	23.65	
Ethane	30.07	10.1%	10.12%	3.044	14.14%	12.62	
Propane	44.10	5.4%	5.38%	2.375	11.03%	8.606	4.342
i-Butane	58.12	0.67%	0.67%	0.387	1.80%	6.529	0.537
n-Butane	58.12	1.6%	1.56%	0.908	4.22%	6.529	1.260
2,2 Dimethylpropane	72.15	0.010%	0.01%	0.007	0.03%	5.302	0.008
i-Pentane	72.15	0.37%	0.37%	0.264	1.23%	5.26	0.295
n-Pentane	72.15	0.38%	0.38%	0.276	1.28%	5.26	0.308
2,2 Dimethylbutane	86.18	0.0040%	0.00%	0.003	0.02%	5.26	0.004
Cyclopentane	70.14	0.00%	0.00%	0.000	0.00%	5.411	0.000
2,3 Dimethylbutane	86.18	0.035%	0.03%	0.030	0.14%	4.404	0.028
2 Methylpentane	86.18	0.087%	0.09%	0.075	0.35%	4.404	0.070
3 Methylpentane	86.18	0.049%	0.05%	0.043	0.20%	4.404	0.040
n-Hexane	86.18	0.10%	0.10%	0.087	0.40%	4.404	0.081
Methylcyclopentane	84.16	0.053%	0.05%	0.045	0.21%	4.509	0.043
Cyclohexane	84.16	0.048%	0.05%	0.040	0.19%	3.787	0.033
2-Methylhexane	100.20	0.013%	0.01%	0.013	0.06%	3.787	0.010
3-Methylhexane	100.20	0.014%	0.01%	0.015	0.07%	3.787	0.012
n-Heptanes	100.20	0.066%	0.07%	0.066	0.31%	3.787	0.053
Other Heptanes	100.20	0.00%	0.00%	0.000	0.00%	3.787	0.000
Methylcyclohexane	98.19	0.036%	0.04%	0.036	0.17%	3.865	0.029
2,2,4-Trimethylpentane	114.23	0.00%	0.00%	0.000	0.00%	3.322	0.000
Benzene	78.11	0.024%	0.02%	0.018	0.09%	4.858	0.019
Toluene	92.14	0.014%	0.01%	0.013	0.06%	4.119	0.011
Ethylbenzene	106.17	0.00087%	0.00%	0.001	0.00%	3.574	0.001
Xylenes	106.17	0.0017%	0.00%	0.002	0.01%	3.574	0.001
C8+ heavies	114.23	0.0037%	0.00%	0.004	0.02%	3.322	0.003
Total		100.0%	100.0%	21.52	100%		7.188
Dry total		100.0%		(mixture mol. wt)			
NMEHC (VOC)		8.92%					21.87%
Mixture heating value		1241	BTU/scf				

Note: * Although the RVP 11 gas simulation did not account and H₂S it was determined that a 0.05% wet/mol % will be used to overcome gas composition fluctuations.

Venting VOC Emissions

Unit: VENT
Description: Emission rates from venting during startup, shutdown, and blowdown operation

Emission Calculations

Inlet Gas	1.0	Mcf/hr	Engineering estimate	
	VOC	H₂S		
	8.92%	0.0500%	mol%	VOC content from gas analysis; H2S content based on maximum possible estimated inlet concentration
	7.2	11.136	ft ³ /lb	Specific volume from gas analysis, calculated above
	12.4	0.04490	lb/hr	vol. gas * mole fraction / specific volume
	12.4	0.04490	lb/Mcf	lb/hr / Mcf/hr

Total Blowdown Emissions

These calculations estimate the total emission rate per blowdown event, based on duration and volume of gas

Vent

	2160	Mcf/yr total vented		
	100%	Safety Factor		
	4320	with SF		
	9	Max Mcf/event		
	100%	Safety Factor		
	18	with SF		
	VOC	H₂S		
Inlet Gas	12.4	0.04490	lb/Mcf vented	
	223.4	0.808	lb/Max event	Max Mcf/event * lb/Mcf
	223.4	0.808	lb/hr	lb/Max event / 1 hr/event Hourly emission rate shown for informational purposes only
	26.8	0.10	tpy vented	(Mcf/yr * lb/Mcf) / 2000 lb/ton

HAP	VOC content	Specific Volume	lb/Mcf ¹	tpy ²
n-Hexane	0.1004%	4.404	0.2280	0.49
2,2,4-TMP	0.0000%	3.322	0.0000	0.00
Benzene	0.0236%	4.858	0.0486	0.11
Toluene	0.0142%	4.119	0.0345	0.075
Ethylbenzene	0.0009%	3.574	0.0024	0.0052
Xylenes	0.0017%	3.574	0.0048	0.010
Total HAPs				0.69

¹ (Vol. gas * mole fraction / specific volume) / Mcf/hr

² (Mcf/yr * lb/Mcf) / 2000 lb/ton

GHG Calculations

CO₂	CH₄	CO₂e		
4.0	70.0		tpy	Mscf/yr * 1000scf/yr * density * 1.1023tons/MT * 1MT/1000kg*Safety Factor
1	25		GWP	40 CFR 98 Table A-1
4.0	1,750.5	1,754.6	tpy CO ₂ e	

Loading Emissions

Unit: LOAD

Description: Emissions from Truck Loading of Condensate

Emission Calculations

69,350 Throughput (bbl/yr) Expected condensate throughput
2,912,700 Throughput (gal/yr) bbl/d * 42 gal/bbl * 365 d/yr

9.82 tpy VOC GRI-HAPCalc 3.01

Total HAPs	n-Hexane	Benzene	Toluene	e-Benzene	Xylenes		
0.4	0.39	0.04	0.00	0.001	0.0012	tpy	GRI-HAPCalc3.01

Haul Road Emissions

Input Data

Empty vehicle weight ¹	16	tons	
Load weight ²	21.2	tons	
Loaded vehicle ³	37.2	tons	
Mean vehicle weight ⁴	26.6	tons	
Vehicle frequency	1.2	vehicles/day	Throughput (gal/yr) * (1 yr/365 days) * (1 truck/7,560 gal) Maximum
Vehicle frequency	1.2	trips/hour	
Round-trip distance	0.40	mile/trip	
Operating hours	8760	hours/yr	
Surface silt content ⁵	1.8	%	
Annual wet days ⁶	60	days/yr	
Vehicle miles traveled ⁷	0.5	mile/hr	

Emission Factors and Constants

Parameter	PM ₃₀	PM ₁₀	PM _{2.5}
k, lb/VMT ⁸	4.9	1.5	0.15
a, lb/VMT ⁸	0.70	0.90	0.90
b, lb/VMT ⁸	0.45	0.45	0.45
Hourly EF, lb/VMT ⁹	3.47	0.73	0.07
Annual EF, lb/VMT ¹⁰	2.90	0.61	0.06

Uncontrolled Emissions

	PM ₃₀	PM ₁₀	PM _{2.5}
	1.7	0.36	0.036 lb/hr ¹¹
	0.26	0.055	0.0055 ton/yr ¹²

Footnotes

- ¹ Empty vehicle weight includes driver and occupants and full fuel load.
- ² Cargo, transported materials, etc. (lb/gal RVP11 * 7560 gal truck/ 2000lb/ton)
- ³ Loaded vehicle weight = Empty + Load Size
- ⁴ Mean Vehicle weight = (Loaded Weight + Empty Weight) / 2
- ⁵ AP-42 Table 13.2.2-1, Taconite mining and processing mean silt content
A 60% reduction in silt is used based on the use of gravel roads at this facility.
- ⁶ AP-42 Figure 13.2.2-1
- ⁷ VMT/hr = Vehicle Miles Traveled per hour = Trips per hour * Miles per trip
- ⁸ Table 13.2.2-2, Industrial Roads
- ⁹ AP-42 13.2.2, Equation 1a
- ¹⁰ AP-42 13.2.2, Equation 2
- ¹¹ lb/hr = Hourly EF (lb/VMT) * VMT (mile/hr)
- ¹² ton/yr = Annual EF (lb/VMT) * Truck/day * Mile/truck * 365day/yr * 1ton/2000lb

Unit(s): PIGGING
Description: Pig Receiver and Launcher Emissions
Exemption: 20.2.72.202.B(5) NMAC

Inlet Receiver Volume	140.00	scf/event	Estimate based on similar Facility Design
Safety Factor	100%		
Inlet Receiver Volume	280.00	scf/event	Calculated
Annual Events:	24	# of events/yr	Estimate based on similar Facility Design
Duration of Event	0.5	hr/event	Estimate
Number of Receivers:	1		Estimate based on similar Facility Design

Pigging Emissions based on Inlet Analysis								
Composition	MW ²	Wet vol/mol% ¹	Dry vol/mol%	MW*Mol%	Spec. Volume (scf/lb) ²	Mass Flow (lb/hr) ³	Mass Flow (lb/yr ⁴)	Mass Flow (ton/yr) ⁵
Water	18.015	0.015%			21.06			
Nitrogen	28.013	2.72%	2.720%	0.76	13.55	1.12E-02	1.35E-01	6.75E-05
CO2	44.010	1.61%	1.605%	0.71	8.62	1.04E-02	1.25E-01	6.25E-05
H2S*	34.082	0.05%	0.050%	0.02	11.14	2.51E-04	3.02E-03	1.51E-06
Methane	16.043	76.6%	76.581%	12.29	23.65	1.81E-01	2.18E+00	1.09E-03
Ethane	30.070	10.1%	10.122%	3.04	12.62	4.49E-02	5.39E-01	2.70E-04
Propane	44.097	5.4%	5.385%	2.37	8.61	3.50E-02	4.20E-01	2.10E-04
i-Butane	58.123	0.67%	0.666%	0.39	6.53	5.71E-03	6.86E-02	3.43E-05
n-Butane	58.123	1.6%	1.563%	0.91	6.53	1.34E-02	1.61E-01	8.04E-05
2,2 Dimethylpropane	72.150	0.010%	0.010%	0.01	5.30	1.05E-04	1.26E-03	6.32E-07
i-Pentane	72.150	0.37%	0.366%	0.26	5.26	3.89E-03	4.67E-02	2.34E-05
n-Pentane	72.150	0.38%	0.382%	0.28	5.26	4.07E-03	4.88E-02	2.44E-05
2,2 Dimethylbutane	86.180	0.0040%	0.004%	0.003	5.26	4.23E-05	5.07E-04	2.54E-07
Cyclopentane	70.140	0.00%	0.000%	0.000	5.41	0.00E+00	0.00E+00	0.00E+00
2,3 Dimethylbutane	86.180	0.035%	0.035%	0.030	4.40	4.40E-04	5.28E-03	2.64E-06
2 Methylpentane	86.180	0.087%	0.087%	0.075	4.40	1.11E-03	1.33E-02	6.64E-06
3 Methylpentane	86.180	0.049%	0.049%	0.043	4.40	6.28E-04	7.53E-03	3.77E-06
n-Hexane	86.180	0.10%	0.100%	0.087	4.40	1.28E-03	1.53E-02	7.66E-06
Methylcyclopentane	84.160	0.053%	0.053%	0.045	4.51	6.60E-04	7.92E-03	3.96E-06
Cyclohexane	84.160	0.048%	0.048%	0.040	3.79	7.10E-04	8.52E-03	4.26E-06
2-Methylhexane	100.200	0.013%	0.013%	0.013	3.79	1.86E-04	2.23E-03	1.12E-06
3-Methylhexane	100.200	0.014%	0.014%	0.015	3.79	2.14E-04	2.57E-03	1.29E-06
n-Heptanes	100.200	0.066%	0.066%	0.066	3.79	9.78E-04	1.17E-02	5.87E-06
Other Heptanes	100.200	0.00%	0.000%	0.000	3.79	0.00E+00	0.00E+00	0.00E+00
Methylcyclohexane	98.190	0.036%	0.036%	0.036	3.87	5.27E-04	6.32E-03	3.16E-06
2,2,4-Trimethylpentane	114.230	0.00%	0.000%	0.000	3.32	0.00E+00	0.00E+00	0.00E+00
Benzene	78.110	0.024%	0.024%	0.018	4.86	2.72E-04	3.27E-03	1.63E-06
Toluene	92.140	0.014%	0.014%	0.013	4.12	1.93E-04	2.32E-03	1.16E-06
Ethylbenzene	106.170	0.00087%	0.001%	0.001	3.57	1.36E-05	1.63E-04	8.14E-08
Xylenes	106.170	0.0017%	0.002%	0.002	3.57	2.66E-05	3.19E-04	1.60E-07
C8+ heavies	114.230	0.0037%	0.004%	0.004	3.32	6.18E-05	7.41E-04	3.71E-07
Total		100.0%	100.0%	21.52				
Dry Total		100.0%				0.32	3.81	0.0019
VOC Total		0.19		7.75		0.11	1.37	6.87E-04

Notes

- ¹ Source: Promax RVP11 Simulation, SC Vapor Stream, from File: ProMax Report South Carlsbad_8
- ² From "Physical Properties of Hydrocarbons"
- ³ Flow (lb/hr) = Volume (scf/event) / Duration (hr/event) / Sp. Vol. (scf/lb) * Mol%
- ⁴ Flow (tons/yr) = Volume (scf/yr) / Sp. Vol. (scf/lb) * Mol%
- ⁵ Flow (tons/yr) = Flow (lb/yr) / 2000 lb/ton

Section 6.a

Green House Gas Emissions

(Submitting under 20.2.70, 20.2.72 20.2.74 NMAC)

Title V (20.2.70 NMAC), Minor NSR (20.2.72 NMAC), and PSD (20.2.74 NMAC) applicants must estimate and report greenhouse gas (GHG) emissions to verify the emission rates reported in the public notice, determine applicability to 40 CFR 60 Subparts, and to evaluate Prevention of Significant Deterioration (PSD) applicability. GHG emissions that are subject to air permit regulations consist of the sum of an aggregate group of these six greenhouse gases: carbon dioxide (CO₂), nitrous oxide (N₂O), methane (CH₄), hydrofluorocarbons (HFCs), perfluorocarbons (PFCs), and sulfur hexafluoride (SF₆).

Calculating GHG Emissions:

1. Calculate the ton per year (tpy) GHG mass emissions and GHG CO₂e emissions from your facility.
2. GHG mass emissions are the sum of the total annual tons of greenhouse gases without adjusting with the global warming potentials (GWPs). GHG CO₂e emissions are the sum of the mass emissions of each individual GHG multiplied by its GWP found in Table A-1 in 40 CFR 98 Mandatory Greenhouse Gas Reporting.
3. Emissions from routine or predictable start up, shut down, and maintenance must be included.
4. Report GHG mass and GHG CO₂e emissions in Table 2-P of this application. Emissions are reported in **short** tons per year and represent each emission unit's Potential to Emit (PTE).
5. All Title V major sources, PSD major sources, and all power plants, whether major or not, must calculate and report GHG mass and CO₂e emissions for each unit in Table 2-P.
6. For minor source facilities that are not power plants, are not Title V, and are not PSD there are three options for reporting GHGs in Table 2-P: 1) report GHGs for each individual piece of equipment; 2) report all GHGs from a group of unit types, for example report all combustion source GHGs as a single unit and all venting GHGs as a second separate unit; 3) or check the following By checking this box, the applicant acknowledges the total CO₂e emissions are less than 75,000 tons per year.

Sources for Calculating GHG Emissions:

- Manufacturer's Data
- AP-42 Compilation of Air Pollutant Emission Factors at <http://www.epa.gov/ttn/chief/ap42/index.html>
- EPA's Internet emission factor database WebFIRE at <http://cfpub.epa.gov/webfire/>
- 40 CFR 98 Mandatory Green House Gas Reporting except that tons should be reported in short tons rather than in metric tons for the purpose of PSD applicability.
- API Compendium of Greenhouse Gas Emissions Methodologies for the Oil and Natural Gas Industry. August 2009 or most recent version.
- Sources listed on EPA's NSR Resources for Estimating GHG Emissions at <http://www.epa.gov/nsr/clean-air-act-permitting-greenhouse-gases>:

Global Warming Potentials (GWP):

Applicants must use the Global Warming Potentials codified in Table A-1 of the most recent version of 40 CFR 98 Mandatory Greenhouse Gas Reporting. The GWP for a particular GHG is the ratio of heat trapped by one unit mass of the GHG to that of one unit mass of CO₂ over a specified time period.

"Greenhouse gas" for the purpose of air permit regulations is defined as the aggregate group of the following six gases: carbon dioxide, nitrous oxide, methane, hydrofluorocarbons, perfluorocarbons, and sulfur hexafluoride. **(20.2.70.7 NMAC, 20.2.74.7 NMAC)**. You may also find GHGs defined in 40 CFR 86.1818-12(a).

Metric to Short Ton Conversion:

Short tons for GHGs and other regulated pollutants are the standard unit of measure for PSD and title V permitting programs. 40 CFR 98 Mandatory Greenhouse Reporting requires metric tons.

1 metric ton = 1.10231 short tons (per Table A-2 to Subpart A of Part 98 – Units of Measure Conversions)

Section 7

Information Used to Determine Emissions

Information Used to Determine Emissions shall include the following:

- If manufacturer data are used, include specifications for emissions units and control equipment, including control efficiencies specifications and sufficient engineering data for verification of control equipment operation, including design drawings, test reports, and design parameters that affect normal operation.
 - If test data are used, include a copy of the complete test report. If the test data are for an emissions unit other than the one being permitted, the emission units must be identical. Test data may not be used if any difference in operating conditions of the unit being permitted and the unit represented in the test report significantly effect emission rates.
 - If the most current copy of AP-42 is used, reference the section and date located at the bottom of the page. Include a copy of the page containing the emissions factors, and clearly mark the factors used in the calculations.
 - If an older version of AP-42 is used, include a complete copy of the section.
 - If an EPA document or other material is referenced, include a complete copy.
 - Fuel specifications sheet.
 - If computer models are used to estimate emissions, include an input summary (if available) and a detailed report, and a disk containing the input file(s) used to run the model. For tank-flashing emissions, include a discussion of the method used to estimate tank-flashing emissions, relative thresholds (i.e., permit or major source (NSPS, PSD or Title V)), accuracy of the model, the input and output from simulation models and software, all calculations, documentation of any assumptions used, descriptions of sampling methods and conditions, copies of any lab sample analysis.
-

This section contains the following references or actual documentation to support the emissions in the required forms and the calculations in Section 6:

Subsection 1 – Documentation used to support calculations in this permit revision.

- Current version of AP-42 located online at: <http://www.epa.gov/ttn/chief/ap42/index.html>. Specific sections used in this application:
 - Section 1.4 –Natural Gas External Combustion Sources-Natural Gas (Table 1.4-1,2)
 - Section 3.2 – Natural Gas-fired Reciprocating Engines (Table 3.2-2)
- ProMax Output for slop working, breathing, flashing, and loading emissions (for T-007)
- Gas and liquid stream compositions used (for Unit F-001)
- Compressor manufacturer specifications (for Units 6, 7, 8, 9, and 10)
- SpiralX manufacturer specification sheet (for Unit ECD)
- TCEQ TNRCC RG-109 Flare guidance documentation
- Flare manufacturer specifications (for Unit flare)
- Stream 11 properties used (for Unit Flare (SSM))
- GRI-GLYCalc Report (for 3a and ECD)
- 40 CFR 98 Subpart A, Table A-1
- 40 CFR 98 Subpart C, Tables C-1 & C-2

Subsection 2 – Documentation used to support calculations from previous permit application.

- Current version of AP-42 located online at: <http://www.epa.gov/ttn/chief/ap42/index.html>. Specific sections used in this application:
 - Section 3.1- Stationary Natural Gas Turbines (Table 3.1-2a)
 - Section 13.2.2 – Introduction to Fugitive Dust sources – Unpaved Roads
- HAPCalc® 3.01 run results loading
- ProMax Output for slop and condensate working and breathing, and slop loading emissions

- Armstrong Gas Lab Analysis No. 211306
- Turbine manufacturer specifications (for Unit 5)
- Turbine Stack Test Data – Reports (for Units 1 and 2)

Section 7

Subsection 1 – Information Used to Determine Emissions for Units Added or Modified with this Application

For clarity, this Subsection 1 contains information used to determine emissions for units that were either added or modified with this application. (i.e. Units 1, 2, 6, 7, 8, 9, 10, 3a, 3b, T-007, LOAD_SLOP, ECD, Flare , F-001, and MALF). For information pertinent to all other units that were not affected by this application, please refer to Subsection 2.

Table 1.4-1. EMISSION FACTORS FOR NITROGEN OXIDES (NO_x) AND CARBON MONOXIDE (CO)
FROM NATURAL GAS COMBUSTION^a

Combustor Type (MMBtu/hr Heat Input) [SCC]	NO _x ^b		CO	
	Emission Factor (lb/10 ⁶ scf)	Emission Factor Rating	Emission Factor (lb/10 ⁶ scf)	Emission Factor Rating
Large Wall-Fired Boilers (>100) [1-01-006-01, 1-02-006-01, 1-03-006-01]				
Uncontrolled (Pre-NSPS) ^c	280	A	84	B
Uncontrolled (Post-NSPS) ^c	190	A	84	B
Controlled - Low NO _x burners	140	A	84	B
Controlled - Flue gas recirculation	100	D	84	B
Small Boilers (<100) [1-01-006-02, 1-02-006-02, 1-03-006-02, 1-03-006-03]				
Uncontrolled	100	B	84	B
Controlled - Low NO _x burners	50	D	84	B
Controlled - Low NO _x burners/Flue gas recirculation	32	C	84	B
Tangential-Fired Boilers (All Sizes) [1-01-006-04]				
Uncontrolled	170	A	24	C
Controlled - Flue gas recirculation	76	D	98	D
Residential Furnaces (<0.3) [No SCC]				
Uncontrolled	94	B	40	B

^a Reference 11. Units are in pounds of pollutant per million standard cubic feet of natural gas fired. To convert from lb/10⁶ scf to kg/10⁶ m³, multiply by 16. Emission factors are based on an average natural gas higher heating value of 1,020 Btu/scf. To convert from lb/10⁶ scf to lb/MMBtu, divide by 1,020. The emission factors in this table may be converted to other natural gas heating values by multiplying the given emission factor by the ratio of the specified heating value to this average heating value. SCC = Source Classification Code. ND = no data. NA = not applicable.

^b Expressed as NO₂. For large and small wall fired boilers with SNCR control, apply a 24 percent reduction to the appropriate NO_x emission factor. For tangential-fired boilers with SNCR control, apply a 13 percent reduction to the appropriate NO_x emission factor.

^c NSPS=New Source Performance Standard as defined in 40 CFR 60 Subparts D and Db. Post-NSPS units are boilers with greater than 250 MMBtu/hr of heat input that commenced construction modification, or reconstruction after August 17, 1971, and units with heat input capacities between 100 and 250 MMBtu/hr that commenced construction modification, or reconstruction after June 19, 1984.

TABLE 1.4-2. EMISSION FACTORS FOR CRITERIA POLLUTANTS AND GREENHOUSE GASES FROM NATURAL GAS COMBUSTION^a

Pollutant	Emission Factor (lb/10 ⁶ scf)	Emission Factor Rating
CO ₂ ^b	120,000	A
Lead	0.0005	D
N ₂ O (Uncontrolled)	2.2	E
N ₂ O (Controlled-low-NO _x burner)	0.64	E
PM (Total) ^c	7.6	D
PM (Condensable) ^c	5.7	D
PM (Filterable) ^c	1.9	B
SO ₂ ^d	0.6	A
TOC	11	B
Methane	2.3	B
VOC	5.5	C

^a Reference 11. Units are in pounds of pollutant per million standard cubic feet of natural gas fired. Data are for all natural gas combustion sources. To convert from lb/10⁶ scf to kg/10⁶ m³, multiply by 16. To convert from lb/10⁶ scf to lb/MMBtu, divide by 1,020. The emission factors in this table may be converted to other natural gas heating values by multiplying the given emission factor by the ratio of the specified heating value to this average heating value. TOC = Total Organic Compounds.

VOC = Volatile Organic Compounds.

^b Based on approximately 100% conversion of fuel carbon to CO₂. CO₂[lb/10⁶ scf] = (3.67) (CON) (C)(D), where CON = fractional conversion of fuel carbon to CO₂, C = carbon content of fuel by weight (0.76), and D = density of fuel, 4.2x10⁻⁴ lb/10⁶ scf.

^c All PM (total, condensible, and filterable) is assumed to be less than 1.0 micrometer in diameter. Therefore, the PM emission factors presented here may be used to estimate PM₁₀, PM_{2.5} or PM₁ emissions. Total PM is the sum of the filterable PM and condensible PM. Condensible PM is the particulate matter collected using EPA Method 202 (or equivalent). Filterable PM is the particulate matter collected on, or prior to, the filter of an EPA Method 5 (or equivalent) sampling train.

^d Based on 100% conversion of fuel sulfur to SO₂.

Assumes sulfur content is natural gas of 2,000 grains/10⁶ scf. The SO₂ emission factor in this table can be converted to other natural gas sulfur contents by multiplying the SO₂ emission factor by the ratio of the site-specific sulfur content (grains/10⁶ scf) to 2,000 grains/10⁶ scf.

Table 3.2-2. UNCONTROLLED EMISSION FACTORS FOR 4-STROKE LEAN-BURN ENGINES^a
(SCC 2-02-002-54)

Pollutant	Emission Factor (lb/MMBtu) ^b (fuel input)	Emission Factor Rating
Criteria Pollutants and Greenhouse Gases		
NO _x ^c 90 - 105% Load	4.08 E+00	B
NO _x ^c <90% Load	8.47 E-01	B
CO ^c 90 - 105% Load	3.17 E-01	C
CO ^c <90% Load	5.57 E-01	B
CO ₂ ^d	1.10 E+02	A
SO ₂ ^e	5.88 E-04	A
TOC ^f	1.47 E+00	A
Methane ^g	1.25 E+00	C
VOC ^h	1.18 E-01	C
PM10 (filterable) ⁱ	7.71 E-05	D
PM2.5 (filterable) ⁱ	7.71 E-05	D
PM Condensable ^j	9.91 E-03	D
Trace Organic Compounds		
1,1,2,2-Tetrachloroethane ^k	<4.00 E-05	E
1,1,2-Trichloroethane ^k	<3.18 E-05	E
1,1-Dichloroethane	<2.36 E-05	E
1,2,3-Trimethylbenzene	2.30 E-05	D
1,2,4-Trimethylbenzene	1.43 E-05	C
1,2-Dichloroethane	<2.36 E-05	E
1,2-Dichloropropane	<2.69 E-05	E
1,3,5-Trimethylbenzene	3.38 E-05	D
1,3-Butadiene ^k	2.67E-04	D
1,3-Dichloropropene ^k	<2.64 E-05	E
2-Methylnaphthalene ^k	3.32 E-05	C
2,2,4-Trimethylpentane ^k	2.50 E-04	C
Acenaphthene ^k	1.25 E-06	C

Table 3.2-2. UNCONTROLLED EMISSION FACTORS FOR 4-STROKE LEAN-BURN ENGINES
(Continued)

Pollutant	Emission Factor (lb/MMBtu) ^b (fuel input)	Emission Factor Rating
Acenaphthylene ^k	5.53 E-06	C
Acetaldehyde ^{k,l}	8.36 E-03	A
Acrolein ^{k,l}	5.14 E-03	A
Benzene ^k	4.40 E-04	A
Benzo(b)fluoranthene ^k	1.66 E-07	D
Benzo(e)pyrene ^k	4.15 E-07	D
Benzo(g,h,i)perylene ^k	4.14 E-07	D
Biphenyl ^k	2.12 E-04	D
Butane	5.41 E-04	D
Butyr/Isobutyraldehyde	1.01 E-04	C
Carbon Tetrachloride ^k	<3.67 E-05	E
Chlorobenzene ^k	<3.04 E-05	E
Chloroethane	1.87 E-06	D
Chloroform ^k	<2.85 E-05	E
Chrysene ^k	6.93 E-07	C
Cyclopentane	2.27 E-04	C
Ethane	1.05 E-01	C
Ethylbenzene ^k	3.97 E-05	B
Ethylene Dibromide ^k	<4.43 E-05	E
Fluoranthene ^k	1.11 E-06	C
Fluorene ^k	5.67 E-06	C
Formaldehyde ^{k,l}	5.28 E-02	A
Methanol ^k	2.50 E-03	B
Methylcyclohexane	1.23 E-03	C
Methylene Chloride ^k	2.00 E-05	C
n-Hexane ^k	1.11 E-03	C
n-Nonane	1.10 E-04	C

Table 3.2-2. UNCONTROLLED EMISSION FACTORS FOR 4-STROKE LEAN-BURN ENGINES
(Continued)

Pollutant	Emission Factor (lb/MMBtu) ^b (fuel input)	Emission Factor Rating
n-Octane	3.51 E-04	C
n-Pentane	2.60 E-03	C
Naphthalene ^k	7.44 E-05	C
PAH ^k	2.69 E-05	D
Phenanthrene ^k	1.04 E-05	D
Phenol ^k	2.40 E-05	D
Propane	4.19 E-02	C
Pyrene ^k	1.36 E-06	C
Styrene ^k	<2.36 E-05	E
Tetrachloroethane ^k	2.48 E-06	D
Toluene ^k	4.08 E-04	B
Vinyl Chloride ^k	1.49 E-05	C
Xylene ^k	1.84 E-04	B

^a Reference 7. Factors represent uncontrolled levels. For NO_x, CO, and PM₁₀, “uncontrolled” means no combustion or add-on controls; however, the factor may include turbocharged units. For all other pollutants, “uncontrolled” means no oxidation control; the data set may include units with control techniques used for NO_x control, such as PCC and SCR for lean burn engines, and PSC for rich burn engines. Factors are based on large population of engines. Factors are for engines at all loads, except as indicated. SCC = Source Classification Code. TOC = Total Organic Compounds. PM-10 = Particulate Matter ≤ 10 microns (μm) aerodynamic diameter. A “<” sign in front of a factor means that the corresponding emission factor is based on one-half of the method detection limit.

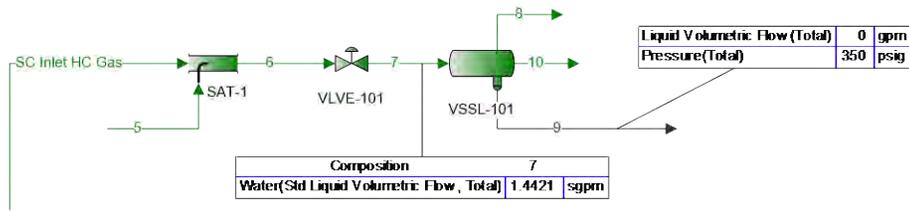
^b Emission factors were calculated in units of (lb/MMBtu) based on procedures in EPA Method 19. To convert from (lb/MMBtu) to (lb/10⁶ scf), multiply by the heat content of the fuel. If the heat content is not available, use 1020 Btu/scf. To convert from (lb/MMBtu) to (lb/hp-hr) use the following equation:

$$\text{lb/hp-hr} = (\text{lb/MMBtu}) (\text{heat input, MMBtu/hr}) (1/\text{operating HP, 1/hp})$$

^c Emission tests with unreported load conditions were not included in the data set.

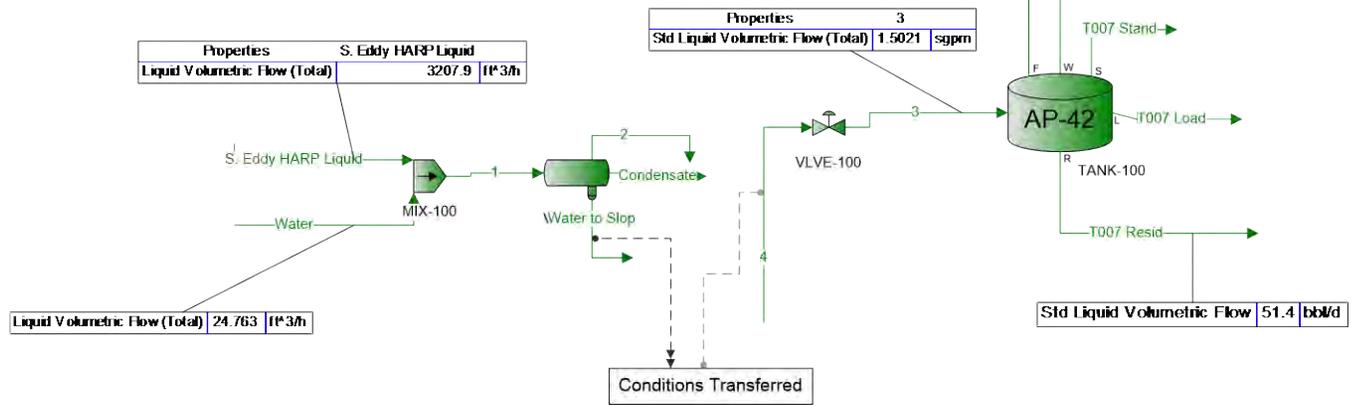
^d Based on 99.5% conversion of the fuel carbon to CO₂. CO₂ [lb/MMBtu] = (3.67)(%CON)(C)(D)(1/h), where %CON = percent conversion of fuel carbon to CO₂, C = carbon content of fuel by weight (0.75), D = density of fuel, 4.1 E+04 lb/10⁶ scf, and

- h = heating value of natural gas (assume 1020 Btu/scf at 60°F).
- ^e Based on 100% conversion of fuel sulfur to SO₂. Assumes sulfur content in natural gas of 2,000 gr/10⁶ scf.
- ^f Emission factor for TOC is based on measured emission levels from 22 source tests.
- ^g Emission factor for methane is determined by subtracting the VOC and ethane emission factors from the TOC emission factor. Measured emission factor for methane compares well with the calculated emission factor, 1.31 lb/MMBtu vs. 1.25 lb/MMBtu, respectively.
- ^h VOC emission factor is based on the sum of the emission factors for all speciated organic compounds less ethane and methane.
- ⁱ Considered $\leq 1 \mu\text{m}$ in aerodynamic diameter. Therefore, for filterable PM emissions, PM10(filterable) = PM2.5(filterable).
- ^j PM Condensable = PM Condensable Inorganic + PM-Condensable Organic
- ^k Hazardous Air Pollutant as defined by Section 112(b) of the Clean Air Act.
- ^l For lean burn engines, aldehyde emissions quantification using CARB 430 may reflect interference with the sampling compounds due to the nitrogen concentration in the stack. The presented emission factor is based on FTIR measurements. Emissions data based on CARB 430 are available in the background report.



Flash Emissions for T007

Per slug catcher vessel:
 Liquid condensate hold up = 3200 ft³
 Water storage = 24.7 ft³
 Vapor Space = 568.6 ft³



Process Streams		T007 Flash	T007 Load	T007 Resid	T007 Stand	T007 Work
Composition		Status: Solved	Solved	Solved	Solved	Solved
Phase: Vapor		From Block: TANK-100	TANK-100	TANK-100	TANK-100	TANK-100
		To Block: --	--	--	--	--
Mass Flow		lb/h	lb/h		lb/h	lb/h
CO2		0.133378	0.00189041		0.00119717	0.00373511
N2		0.00253144	5.20004E-07		3.29312E-07	1.02744E-06
Methane		0.234813	0.000134200		8.49873E-05	0.000265156
Ethane		0.140636	9.19687E-05		5.82427E-05	0.000181714
Propane		0.0718049	8.00178E-06		5.06744E-06	1.58101E-05
i-Butane		0.00714517	1.91629E-07		1.21357E-07	3.78626E-07
n-Butane		0.0203610	4.96324E-07		3.14316E-07	9.80649E-07
2,2-Dimethylpropane		3.41758E-05	2.76260E-10		1.74953E-10	5.45842E-10
i-Pentane		0.00295933	1.89223E-08		1.19833E-08	3.73871E-08
n-Pentane		0.00122503	2.37697E-09		1.50531E-09	4.69648E-09
2,2-Dimethylbutane		9.32821E-06	1.07660E-11		6.81797E-12	2.12717E-11
Cyclopentane		0	0		0	0
2,3-Dimethylbutane		0.000129139	2.78977E-10		1.76673E-10	5.51210E-10
2-Methylpentane		0.000230393	2.45186E-10		1.55274E-10	4.84445E-10
3-Methylpentane		0.000273982	6.25413E-10		3.96067E-10	1.23571E-09
n-Hexane		0.000174999	6.59635E-11		4.17739E-11	1.30332E-10
Methylcyclopentane		0.000218516	6.08282E-10		3.85218E-10	1.20186E-09
Benzene		0.0132306	2.13091E-06		1.34948E-06	4.21031E-06
Cyclohexane		0.000339756	1.53830E-09		9.74191E-10	3.03942E-09
2-Methylhexane		1.68889E-05	3.60261E-12		2.28149E-12	7.11813E-12
3-Methylhexane		0	0		0	0
2,2,4-Trimethylpentane		2.55548E-05	3.43200E-12		2.17345E-12	6.78104E-12
n-Heptane		3.56897E-05	2.86606E-12		1.81504E-12	5.66283E-12
Methylcyclohexane		8.79239E-05	7.94464E-11		5.03125E-11	1.56972E-10
Toluene		0.00376847	1.33734E-07		8.46922E-08	2.64235E-07
n-Octane		9.08574E-07	8.57030E-15		5.42748E-15	1.69334E-14
Ethylbenzene		0.000124212	1.26097E-09		7.98555E-10	2.49145E-09
m-Xylene		2.28563E-05	1.33288E-10		8.44099E-11	2.63354E-10
o-Xylene		0.000421244	4.38913E-09		2.77959E-09	8.67215E-09
n-Nonane		1.27632E-07	3.12644E-16		1.97994E-16	6.17729E-16
n-Decane		3.44277E-09	6.94417E-19		4.39766E-19	1.37205E-18
Undecane		8.55938E-11	6.20916E-21		3.93219E-21	1.22682E-20
Dodecane		2.66972E-11	1.98251E-21		1.25550E-21	3.91709E-21
Water		0.0179314	3.95852E-05		2.50689E-05	7.82135E-05

Process Streams		T007 Flash	T007 Load	T007 Resid	T007 Stand	T007 Work
Properties		Status:	Solved	Solved	Solved	Solved
Phase: Vapor	From Block:	TANK-100	TANK-100	TANK-100	TANK-100	TANK-100
	To Block:	--	--	--	--	--
Property	Units					
Temperature	°F	79.2053	79.2053		79.2053	79.2053
Pressure	psig	-1.81595	-1.81595		-1.81595	-1.81595
Mole Fraction Vapor	%	100	100		100	100
Mole Fraction Light Liquid	%	0	0		0	0
Mole Fraction Heavy Liquid	%	0	0		0	0
Phase Mole Fraction	%	100	13.4249		13.4249	13.4249
Molecular Weight	lb/lbmol	25.2452	38.1519		38.1519	38.1519
Mass Density	lb/ft^3	0.0564449	0.0853451		0.0853451	0.0853451
Molar Flow	lbmol/h	0.0258240	5.68167E-05		3.59814E-05	0.000112260
Mass Flow	lb/h	0.651930	0.00216766		0.00137276	0.00428293
Vapor Volumetric Flow	ft^3/h	11.5499	0.0253988		0.0160848	0.0501836
Liquid Volumetric Flow	gpm	1.43998	0.00316661		0.00200538	0.00625666
Std Vapor Volumetric Flow	MMSCFD	0.000235195	5.17465E-07		3.27704E-07	1.02242E-06
Std Liquid Volumetric Flow	sgpm	0.00315865	6.15482E-06		3.89778E-06	1.21609E-05
Compressibility		0.996134	0.995639		0.995639	0.995639
Specific Gravity		0.871650	1.31729		1.31729	1.31729
API Gravity						
Enthalpy	Btu/h	-1351.68	-7.88170		-4.99139	-15.5729
Mass Enthalpy	Btu/lb	-2073.34	-3636.03		-3636.03	-3636.03
Mass Cp	Btu/(lb*°F)	0.409161	0.237816		0.237816	0.237816
Ideal Gas CpCv Ratio		1.23906	1.28190		1.28190	1.28190
Dynamic Viscosity	cP	0.0111200	0.0143701		0.0143701	0.0143701
Kinematic Viscosity	cSt	12.2987	10.5114		10.5114	10.5114
Thermal Conductivity	Btu/(h*ft*°F)	0.0156055	0.0112447		0.0112447	0.0112447
Surface Tension	lbf/ft					
Net Ideal Gas Heating Value	Btu/ft^3	1052.52	230.930		230.930	230.930
Net Liquid Heating Value	Btu/lb	15713.4	2205.07		2205.07	2205.07
Gross Ideal Gas Heating Value	Btu/ft^3	1158.34	256.574		256.574	256.574
Gross Liquid Heating Value	Btu/lb	17304.5	2460.23		2460.23	2460.23

Inlet Stream for F-001 (Gas)	
Component	Mass Fraction (%)
Hydrogen Sulfide	0
Nitrogen	3.538829845
Carbon Dioxide	3.280317616
Methane	57.05313454
Ethane	14.13458413
Propane	11.02638721
i-Butane	1.798158364
n-Butane	4.216596727
2,2-Dimethylpropane	0.033428867
i-Pentane	1.224412919
n-Pentane	1.279324499
2,2-Dimethylbutane	0.015859292
Cyclopentane	0
2,3-Dimethylbutane	0.138343572
2-Methylpentane	0.347523529
3-Methylpentane	0.19713613
n-Hexane	0.400739155
Methylcyclopentane	0.207266998
Benzene	0.085429758
Cyclohexane	0.187366259
2-Methylhexane	0.058323127
3-Methylhexane	0.067035915
2,2,4-Trimethylpentane	0
n-Heptane	0.305009246
Methylcyclohexane	0.164664219
Toluene	0.060471679
n-Octane	0.147028817
Ethylbenzene	0.004176951
m-Xylene	0.004116063
p-Xylene	0.004145743
o-Xylene	0
n-Nonane	0.02018884

Condensate Stream for F-001 (LL)	
Component	Mass Fraction (%)
Hydrogen Sulfide	0
Nitrogen	0
Carbon Dioxide	1.56E-12
Methane	3.41E-14
Ethane	2.94E-08
Propane	0.000634161
i-Butane	0.128229103
n-Butane	5.031456961
2,2-Dimethylpropane	0.158545918
i-Pentane	14.05103734
n-Pentane	17.18954573
2,2-Dimethylbutane	0.266527577
Cyclopentane	0
2,3-Dimethylbutane	2.563416485
2-Methylpentane	6.596582328
3-Methylpentane	3.881328456
n-Hexane	8.492380503
Methylcyclopentane	4.295514381
Benzene	1.519673324
Cyclohexane	4.138898529
2-Methylhexane	1.565672441
3-Methylhexane	1.873134659
2,2,4-Trimethylpentane	0
n-Heptane	9.463728444
Methylcyclohexane	5.067089098
Toluene	1.749635538
n-Octane	8.41525751
Ethylbenzene	0.244897106
m-Xylene	0.256298415
p-Xylene	0.249932323
o-Xylene	0
n-Nonane	2.800062758



Emission Control Application Data Sheet



Maxim Silencers
6545 N. ELDRIDGE PKWY
HOUSTON TX. 77041
Phone: 713-682-6777
Fax: 713-682-3628

September 26, 2018

Customer: COMPASS	Project: OPP# 2207-270-EPD	Date: 11/11/2022
Customer Contact	Powertherm Contact:	Order/Quote #: 0

Engine Data:

Engine Model: CAT 3608A4	Speed: 1000	RPM
Fuel & Operating Type: Natural Gas Lean Burn	Engine Power: 2500	Hp
	1880	KW
Exhaust Flow Rate: 16069 acfm	Exhaust Temperature: 833	°F
27301 m ³ /hr	445	°C
29528 lbs/hr		

Catalyst Data:

Number of Core layers: 1	Inlet Size: 20	in
Model: MCCOF3-6-2420C3	Outlet Size: 24	in
Grade: Critical	Body Length: 182	in
Body Diameter: 54 in	Estimated Back Pressure of the unit: 6.01	in of WC
Estimated weight: 4180 lbs	15.0	mbar
1897 Kg		
Core Part Number: ERH-1536-1, 15 X 36 SIZE	Qty: 3	Speed through inlet: 5279
Cell Density: 300 cpsi	Back Pressure across Element(s) only: 2.66	ft/min
	6.6	in of WC
		mbar

Emission:

Min. Temp. at Core Face: 752 °F	400 °C	Catalyst Type: Oxidation
Max. Temp. at Core Face: 917 °F	492 °C	O ₂ in Exhaust: vol %
		H ₂ O in Exhaust: vol %

	Pollutant					
	NOx	CO	NMNEHC/VOG	CH ₂ O/CHCO	ORGANIC PM10	
Engine Out / Pre Emission:	0.3	2.5	0.27	0.16	0	g/bhp-hr
	72.19	601.62	64.97	38.50	0.00	mg/Nm3
Post Emission:	0.300	0.600	0.700	0.040	0.000	g/bhp-hr
	72.19	144.39	168.45	9.63	0.00	mg/Nm3
	0.0	76.0	-159.3	75.0	50.0	% Reduction
	1.65	3.31	3.86	0.22		lb/hr
	7.24	14.48	16.90	0.97		tons/year operation
	34.7	69.3	80.9	4.6		8760 hr/year
						ppmv
						ppmvd @ 15% O2

Acoustics:

Frequency Band (Hz):	31.5	63	125	250	500	1000	2000	4000	8000	
Raw Noise SPL (dB) at 3.28 ft.:	0	0	7 dBA							
Estimated Attenuation (dB):	24	35	37	31	28	24	25	29.5	30	No Element
Plus:	24	36	39	33	32	29	31	35.5	35	One Element Layer
Silenced SPL (dB) at 3.28 ft.:	-24	-36	-39	-33	-32	-29	-31	-35.5	-35	-24.8 dBA

Warranty & Notes:

- If Pre-Emission levels are not as noted above, contact Maxim Silencers for a re-quote.
- To achieve Post Emissions levels detailed above, exhaust temperature and Pre-Emission data must be as specified.
- Maximum allowable exhaust temperature at core face is 1350°F.
- If applicable, the engine will require an air/fuel ratio controller to meet above emission levels. For Rich Burn engines λ must be 0.96 - 0.99.
- Catalyst cleaning/regeneration required, if initial backpressure increases by 2" of WC.
- Engine operation to be stable and reproducible.
- QAC is not designed to withstand a backfire, therefore measures should be taken prior to QAC unit to alleviate backfire pressure.
- Maximum lubrication oil consumption rate to be less than 0.0015 lb/bhp/hr.
- Lube oil sulfate ash contents should not exceed 0.5%.
- Phosphorus and/or Zinc should not exceed 5 ppmv in the exhaust stream.
- A high temperature alarm/shutdown to be maintained at downstream of catalyst at 1300°F.
- Fuel not to contain heavy or transition metals such as Pb, Ar, Zn, Cu, Sn, Fe, Ba, Ni, Cr etc.
- Chlorinated or Silicone containing compounds in the exhaust not to exceed 1 ppmv.
- Sulfur compounds in the exhaust gas stream not to exceed 25 ppmv.
- Performance guarantee is voided should the catalyst become masked or de-activated by any contaminant in the exhaust stream.
- Engine to be maintained and operated in accordance within manufacturer's recommended practice.
- Under no condition will Maxim Silencers assume any contingent liabilities.
- Operating manual is available online at www.maximsilencers.com or contact a Maxim sales representative.
- Nomenclature: QAC4-292-8, 4 is grade (Super Critical), 29 is catalyst block size, 2 is no. of catalyst(s) and 8 is flange diameter.
- Organic PM10 are estimate only and not a guarantee because of the variability in fuels and additives which change PM10.
- Maxim Silencers standard one year warranty applies.

Rev level: 86

11/11/2022

GAS COMPRESSION APPLICATION
 ENGINE SPEED (rpm): 1000
 COMPRESSION RATIO: 7.6
 AFTERCOOLER TYPE: SCAC
 AFTERCOOLER - STAGE 2 INLET (°F): 130
 AFTERCOOLER - STAGE 1 INLET (°F): 174
 JACKET WATER OUTLET (°F): 190
 ASPIRATION: TA
 COOLING SYSTEM: JW+1AC, OC+2AC
 CONTROL SYSTEM: ADEM4
 EXHAUST MANIFOLD: DRY
 COMBUSTION: LOW EMISSION
 NOx EMISSION LEVEL (g/bhp-hr NOx): 0.3
 SET POINT TIMING: 18

RATING STRATEGY: STANDARD
 RATING LEVEL: CONTINUOUS
 FUEL SYSTEM: GAV
 WITH AIR FUEL RATIO CONTROL

SITE CONDITIONS:
 FUEL: Nat Gas
 FUEL PRESSURE RANGE(psig): (See note 1) 58.0-70.3
 FUEL METHANE NUMBER: 95.2
 FUEL LHV (Btu/scf): 912
 ALTITUDE(ft): 3000
 INLET AIR TEMPERATURE(°F): 110
 STANDARD RATED POWER: 2500 bhp@1000rpm

RATING	NOTES	LOAD	MAXIMUM RATING	SITE RATING AT MAXIMUM INLET AIR TEMPERATURE		
			100%	100%	75%	50%
ENGINE POWER (WITHOUT FAN)	(2)	bhp	2500	2500	1875	1250
INLET AIR TEMPERATURE		°F	110	110	110	110

ENGINE DATA							
FUEL CONSUMPTION (LHV)		(3)	Btu/bhp-hr	6848	6848	7075	7573
FUEL CONSUMPTION (HHV)		(3)	Btu/bhp-hr	7598	7598	7849	8403
AIR FLOW (@inlet air temp, 14.7 psia)	(WET)	(4)(5)	ft3/min	6636	6636	5029	3419
AIR FLOW	(WET)	(4)(5)	lb/hr	27720	27720	21007	14282
FUEL FLOW (60°F, 14.7 psia)			scfm	313	313	242	173
INLET MANIFOLD PRESSURE		(6)	in Hg(abs)	104.4	104.4	78.9	55.1
EXHAUST TEMPERATURE - ENGINE OUTLET		(7)	°F	833	833	876	941
EXHAUST GAS FLOW (@engine outlet temp, 14.5 psia)	(WET)	(5)(8)	ft3/min	16069	16069	12600	9005
EXHAUST GAS MASS FLOW	(WET)	(5)(8)	lb/hr	28528	28528	21633	14728

EMISSIONS DATA - ENGINE OUT							
NOx (as NO2)		(9)(10)	g/bhp-hr	0.30	0.30	0.30	0.30
CO		(9)(10)	g/bhp-hr	2.50	2.50	2.49	2.50
THC (mol. wt. of 15.84)		(9)(10)	g/bhp-hr	4.41	4.41	4.68	4.75
NMHC (mol. wt. of 15.84)		(9)(10)	g/bhp-hr	0.41	0.41	0.43	0.44
NMNEHC (VOCs) (mol. wt. of 15.84)		(9)(10)(11)	g/bhp-hr	0.27	0.27	0.29	0.30
HCHO (Formaldehyde)		(9)(10)	g/bhp-hr	0.16	0.16	0.17	0.20
CO2		(9)(10)	g/bhp-hr	425	425	441	470
EXHAUST OXYGEN		(9)(12)	% DRY	11.3	11.3	11.1	10.7

HEAT REJECTION							
HEAT REJ. TO JACKET WATER (JW)		(13)	Btu/min	27700	27700	23042	18866
HEAT REJ. TO ATMOSPHERE		(13)	Btu/min	11186	11186	11118	10432
HEAT REJ. TO LUBE OIL (OC)		(13)	Btu/min	12553	12553	11937	10885
HEAT REJ. TO A/C - STAGE 1 (1AC)		(13)(14)	Btu/min	27175	27175	13666	3763
HEAT REJ. TO A/C - STAGE 2 (2AC)		(13)(14)	Btu/min	9026	9026	5673	2840

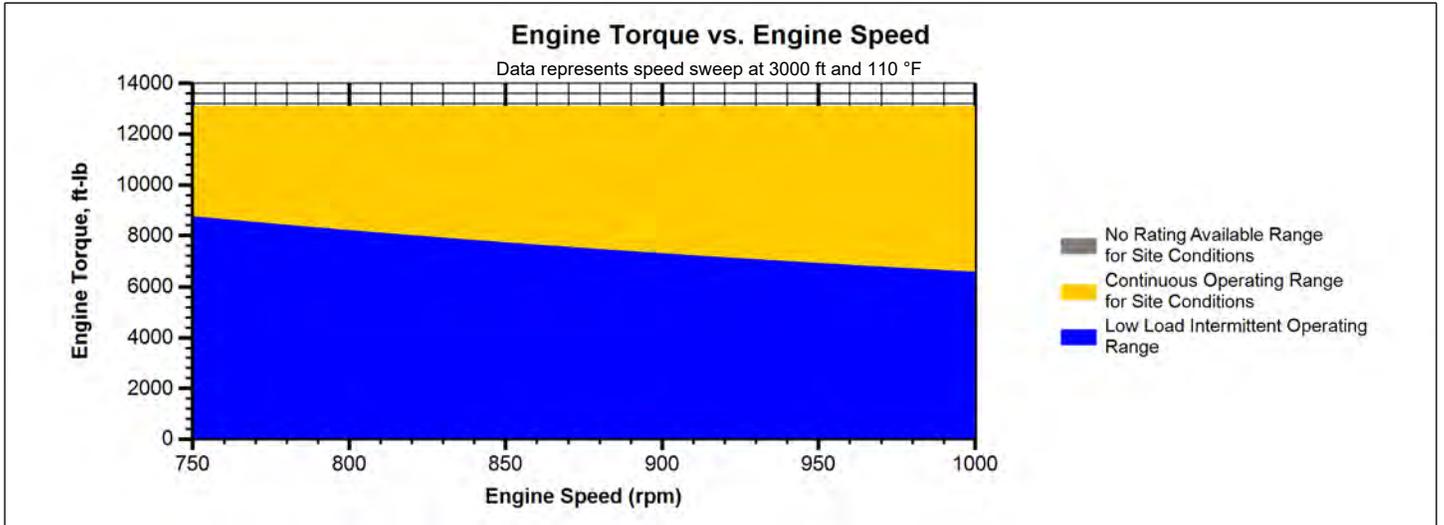
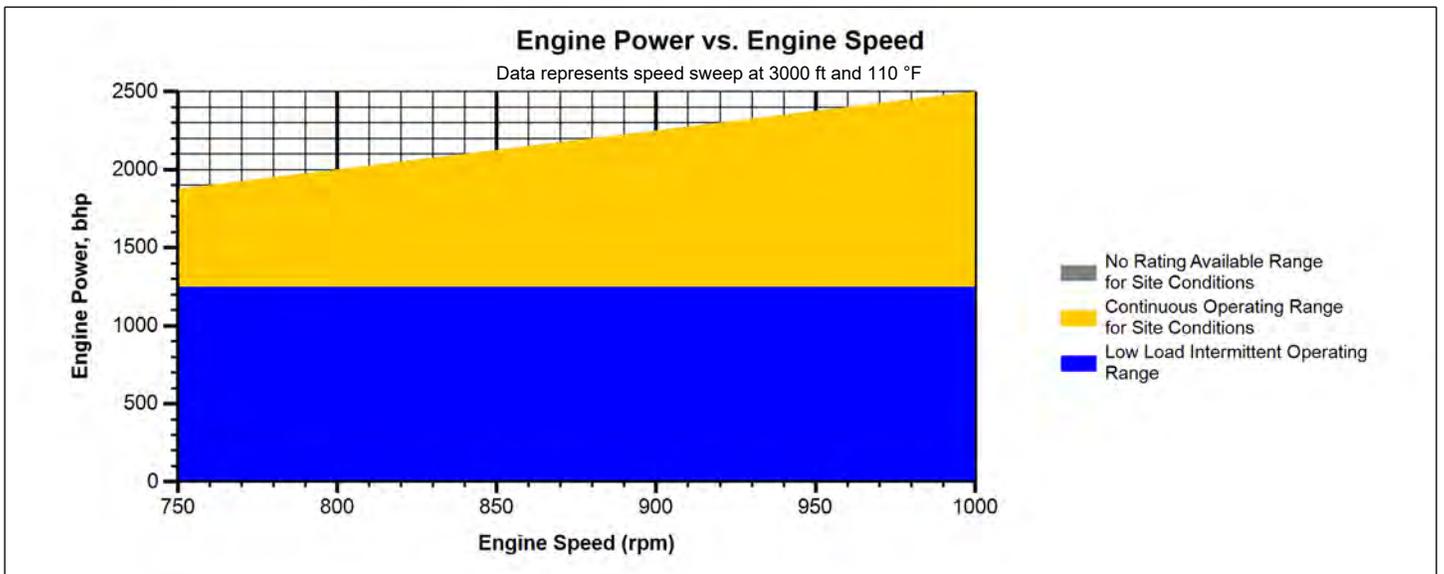
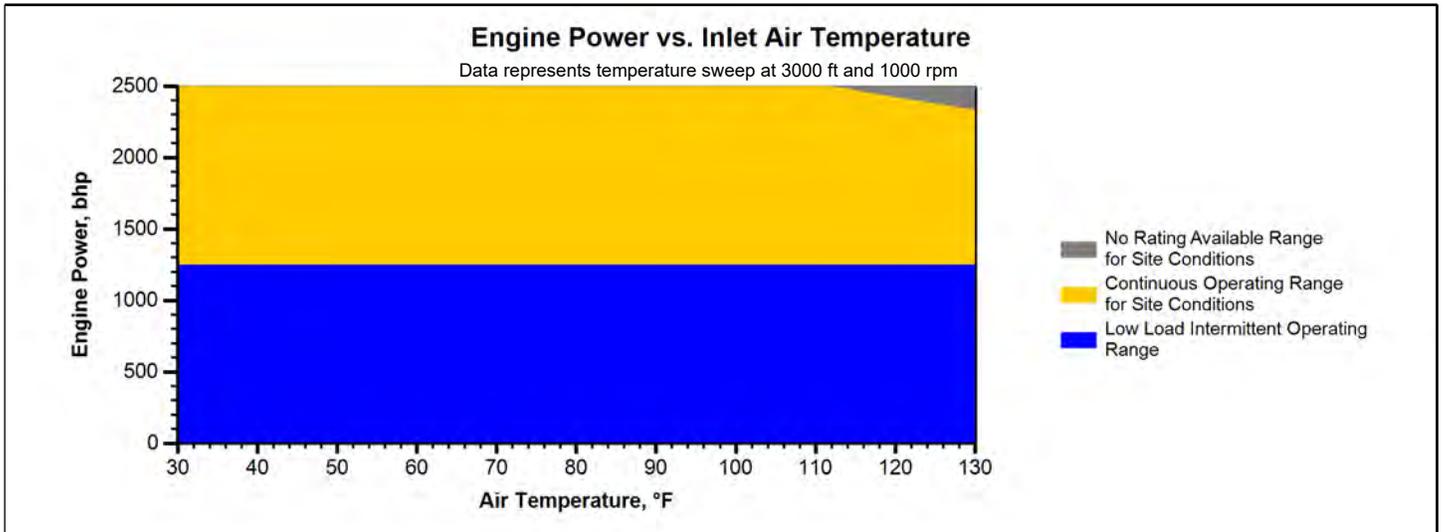
COOLING SYSTEM SIZING CRITERIA				
TOTAL JACKET WATER CIRCUIT (JW+1AC)	(14)(15)	Btu/min	59003	
TOTAL STAGE 2 AFTERCOOLER CIRCUIT (OC+2AC)	(14)(15)	Btu/min	24540	

A cooling system safety factor of 0% has been added to the cooling system sizing criteria.

CONDITIONS AND DEFINITIONS

Engine rating obtained and presented in accordance with ISO 3046/1, adjusted for fuel, site altitude and site inlet air temperature. 100% rating at maximum inlet air temperature is the maximum engine capability for the specified fuel at site altitude and maximum site inlet air temperature. Maximum rating is the maximum capability at the specified aftercooler inlet temperature for the specified fuel at site altitude and reduced inlet air temperature. Refer to product O&M manual for details on additional lower load capability. No overload permitted at rating shown.

For notes information consult page three.



Note:

At site conditions of 3000 ft and 110°F inlet air temp., constant torque can be maintained down to 750 rpm. The minimum speed for loading at these conditions is 750 rpm.

NOTES:

1. Fuel pressure range specified is to the engine gas shutoff valve (GSOV). Additional fuel train components should be considered in pressure and flow calculations.
2. Engine rating is with two engine driven water pumps. Tolerance is $\pm 3\%$ of full load.
3. Fuel consumption tolerance is $\pm 2.5\%$ of full load data.
4. Air flow value is on a 'wet' basis. Flow is a nominal value with a tolerance of $\pm 5\%$.
5. Inlet and Exhaust Restrictions must not exceed A&I limits based on full load flow rates from the standard technical data sheet.
6. Inlet manifold pressure is a nominal value with a tolerance of $\pm 5\%$.
7. Exhaust temperature is a nominal value with a tolerance of $(+)63^{\circ}\text{F}$, $(-)54^{\circ}\text{F}$.
8. Exhaust flow value is on a "wet" basis. Flow is a nominal value with a tolerance of $\pm 6\%$.
9. Emissions data is at engine exhaust flange prior to any after treatment.
10. Values listed are higher than nominal levels to allow for instrumentation, measurement, and engine-to-engine variations. They indicate the maximum values expected under steady state conditions. Fuel methane number cannot vary more than ± 3 . THC, NMHC, and NMNEHC do not include aldehydes. An oxidation catalyst may be required to meet Federal, State or local CO or HC requirements.
11. VOCs - Volatile organic compounds as defined in US EPA 40 CFR 60, subpart JJJJ
12. Exhaust Oxygen level is the result of adjusting the engine to operate at the specified NOx level. Tolerance is ± 0.5 .
13. Heat rejection values are nominal. Tolerances, based on treated water, are $\pm 10\%$ for jacket water circuit, $\pm 50\%$ for radiation, $\pm 20\%$ for lube oil circuit, and $\pm 5\%$ for aftercooler circuit.
14. Aftercooler heat rejection includes an aftercooler heat rejection factor for the site elevation and inlet air temperature specified. Aftercooler heat rejection values at part load are for reference only. Do not use part load data for heat exchanger sizing.
15. Cooling system sizing criteria are maximum circuit heat rejection for the site, with applied tolerances.

Constituent	Abbrev	Mole %	Norm
Water Vapor	H2O	0.0000	0.0000
Methane	CH4	97.1350	97.1350
Ethane	C2H6	1.5540	1.5540
Propane	C3H8	0.0410	0.0410
Isobutane	iso-C4H10	0.0000	0.0000
Norbutane	nor-C4H10	0.0000	0.0000
Isopentane	iso-C5H12	0.0000	0.0000
Norpentane	nor-C5H12	0.0000	0.0000
Hexane	C6H14	0.0000	0.0000
Heptane	C7H16	0.0000	0.0000
Nitrogen	N2	1.2480	1.2480
Carbon Dioxide	CO2	0.0000	0.0000
Hydrogen Sulfide	H2S	0.0000	0.0000
Carbon Monoxide	CO	0.0220	0.0220
Hydrogen	H2	0.0000	0.0000
Oxygen	O2	0.0000	0.0000
Helium	HE	0.0000	0.0000
Neopentane	neo-C5H12	0.0000	0.0000
Octane	C8H18	0.0000	0.0000
Nonane	C9H20	0.0000	0.0000
Ethylene	C2H4	0.0000	0.0000
Propylene	C3H6	0.0000	0.0000
TOTAL (Volume %)		100.0000	100.0000

Fuel Makeup:
Unit of Measure:

Nat Gas
English

Calculated Fuel Properties

Caterpillar Methane Number:	95.2
Lower Heating Value (Btu/scf):	912
Higher Heating Value (Btu/scf):	1012
WOBBE Index (Btu/scf):	1211
THC: Free Inert Ratio:	79.11
Total % Inerts (% N2, CO2, He):	1.25%
RPC (%) (To 905 Btu/scf Fuel):	100%
Compressibility Factor:	0.998
Stoich A/F Ratio (Vol/Vol):	9.52
Stoich A/F Ratio (Mass/Mass):	16.80
Specific Gravity (Relative to Air):	0.567
Fuel Specific Heat Ratio (K):	1.314

CONDITIONS AND DEFINITIONS

Caterpillar Methane Number represents the knock resistance of a gaseous fuel. It should be used with the Caterpillar Fuel Usage Guide for the engine and rating to determine the rating for the fuel specified. A Fuel Usage Guide for each rating is included on page 2 of its standard technical data sheet.

RPC always applies to naturally aspirated (NA) engines, and turbocharged (TA or LE) engines only when they are derated for altitude and ambient site conditions.

Project specific technical data sheets generated by the Caterpillar Gas Engine Rating Pro program take the Caterpillar Methane Number and RPC into account when generating a site rating.

Fuel properties for Btu/scf calculations are at 60F and 14.696 psia.

Caterpillar shall have no liability in law or equity, for damages, consequently or otherwise, arising from use of program and related material or any part thereof.

FUEL LIQUIDS

Field gases, well head gases, and associated gases typically contain liquid water and heavy hydrocarbons entrained in the gas. To prevent detonation and severe damage to the engine, hydrocarbon liquids must not be allowed to enter the engine fuel system. To remove liquids, a liquid separator and coalescing filter are recommended, with an automatic drain and collection tank to prevent contamination of the ground in accordance with local codes and standards.

To avoid water condensation in the engine or fuel lines, limit the relative humidity of water in the fuel to 80% at the minimum fuel operating temperature.

ENGINE SPEED (rpm):	1000	RATING STRATEGY:	STANDARD
COMPRESSION RATIO:	7.6	APPLICATION:	GAS COMPRESSION
AFTERCOOLER TYPE:	SCAC	RATING LEVEL:	CONTINUOUS
AFTERCOOLER - STAGE 2 INLET (°F):	130	FUEL:	NAT GAS
AFTERCOOLER - STAGE 1 INLET (°F):	174	FUEL SYSTEM:	GAV
JACKET WATER OUTLET (°F):	190	FUEL PRESSURE RANGE(psig): (See note 1)	WITH AIR FUEL RATIO CONTROL 58.0-70.3
ASPIRATION:	TA	FUEL METHANE NUMBER:	85
COOLING SYSTEM:	JW+1AC, OC+2AC	FUEL LHV (Btu/scf):	905
CONTROL SYSTEM:	ADEM4	ALTITUDE CAPABILITY AT 100°F INLET AIR TEMP. (ft):	4706
EXHAUST MANIFOLD:	DRY		
COMBUSTION:	LOW EMISSION		
NOx EMISSION LEVEL (g/bhp-hr NOx):	0.3		

RATING	NOTES	LOAD	100%	75%	50%
ENGINE POWER (WITHOUT FAN)	(2)	bhp	2500	1875	1250
ENGINE EFFICIENCY (ISO 3046/1)	(3)	%	38.1	36.8	34.4
ENGINE EFFICIENCY (NOMINAL)	(3)	%	37.2	36.0	33.6

ENGINE DATA						
FUEL CONSUMPTION (ISO 3046/1)	(4)	Btu/bhp-hr	6685	6906	7393	
FUEL CONSUMPTION (NOMINAL)	(4)	Btu/bhp-hr	6848	7075	7574	
AIR FLOW (77°F, 14.7 psia) (WET)	(5)(6)	ft ³ /min	6252	4738	3221	
AIR FLOW (WET)	(5)(6)	lb/hr	27723	21010	14283	
FUEL FLOW (60°F, 14.7 psia)		scfm	315	244	174	
COMPRESSOR OUT PRESSURE		in Hg(abs)	104.9	79.3	55.3	
COMPRESSOR OUT TEMPERATURE		°F	379	307	223	
AFTERCOOLER AIR OUT TEMPERATURE		°F	136	136	136	
INLET MAN. PRESSURE	(7)	in Hg(abs)	104.4	78.9	55.1	
INLET MAN. TEMPERATURE (MEASURED IN PLENUM)	(8)	°F	136	136	136	
TIMING	(9)	°BTDC	18	17	16	
EXHAUST TEMPERATURE - ENGINE OUTLET	(10)	°F	833	876	941	
EXHAUST GAS FLOW (@engine outlet temp, 14.5 psia) (WET)	(6)(11)	ft ³ /min	16088	12616	9016	
EXHAUST GAS MASS FLOW (WET)	(6)(11)	lb/hr	28584	21676	14760	

EMISSIONS DATA - ENGINE OUT					
NOx (as NO ₂)	(12)(13)	g/bhp-hr	0.30	0.30	0.30
CO	(12)(14)	g/bhp-hr	2.50	2.50	2.50
THC (mol. wt. of 15.84)	(12)(14)	g/bhp-hr	4.42	4.69	4.76
NMHC (mol. wt. of 15.84)	(12)(14)	g/bhp-hr	0.41	0.43	0.44
NMNEHC (VOCs) (mol. wt. of 15.84)	(12)(14)(15)	g/bhp-hr	0.28	0.29	0.30
HCHO (Formaldehyde)	(12)(14)	g/bhp-hr	0.16	0.17	0.20
CO ₂	(12)(14)	g/bhp-hr	426	442	471
EXHAUST OXYGEN	(12)(16)	% DRY	11.3	11.1	10.7
LAMBDA	(12)(16)		2.01	1.97	1.87

ENERGY BALANCE DATA					
LHV INPUT	(17)	Btu/min	285298	221058	157762
HEAT REJECTION TO JACKET WATER (JW)	(18)(26)	Btu/min	27698	23042	18866
HEAT REJECTION TO ATMOSPHERE	(19)	Btu/min	10994	10961	10310
HEAT REJECTION TO LUBE OIL (OC)	(20)(27)	Btu/min	12553	11937	10886
HEAT REJECTION TO EXHAUST (LHV TO 77°F)	(21)(22)	Btu/min	97849	78104	56771
HEAT REJECTION TO EXHAUST (LHV TO 350°F)	(21)	Btu/min	61035	50617	38964
HEAT REJECTION TO A/C - STAGE 1 (1AC)	(23)(26)	Btu/min	19561	9599	2375
HEAT REJECTION TO A/C - STAGE 2 (2AC)	(24)(27)	Btu/min	7683	4956	2595
PUMP POWER	(25)	Btu/min	2957	2957	2957

CONDITIONS AND DEFINITIONS

Engine rating obtained and presented in accordance with ISO 3046/1. (Standard reference conditions of 77°F, 29.60 in Hg barometric pressure.) No overload permitted at rating shown. Consult the altitude deration factor chart for applications that exceed the rated altitude or temperature.

Emission levels are at engine exhaust flange prior to any after treatment. Values are based on engine operating at steady state conditions, adjusted to the specified NOx level at 100% load. Tolerances specified are dependent upon fuel quality. Fuel methane number cannot vary more than ±3.

For notes information consult page three.

FUEL USAGE GUIDE

CAT METHANE NUMBER	<10	10	15	20	25	30	35	40	45	50	55	60	65	70	75	80	85	100
SET POINT TIMING	-	16	16	16	16	16	16	16	16	17	17	17	17	18	18	18	18	18
DERATION FACTOR	0	0.50	0.62	0.75	0.87	1	1	1	1	1	1	1	1	1	1	1	1	1
WOBBE INDEX(BTU/scfm)	700		850		1550		1870											
DERATION FACTOR	0.77		1		1		0.9											

ALTITUDE DERATION FACTORS AT RATED SPEED

INLET AIR TEMP °F	130	1	1	0.97	0.93	0.90	0.86	0.83	0.80	0.76	0.73	0.69	0.65	0.61
	120	1	1	1	0.97	0.94	0.90	0.87	0.84	0.80	0.77	0.73	0.69	0.64
	110	1	1	1	1	0.98	0.94	0.91	0.88	0.85	0.81	0.78	0.74	0.68
	100	1	1	1	1	1	0.99	0.96	0.92	0.89	0.85	0.82	0.78	0.75
	90	1	1	1	1	1	1	0.97	0.93	0.90	0.87	0.83	0.80	0.77
	80	1	1	1	1	1	1	0.98	0.94	0.91	0.88	0.85	0.81	0.78
	70	1	1	1	1	1	1	0.99	0.95	0.92	0.89	0.85	0.82	0.78
	60	1	1	1	1	1	1	1	0.96	0.93	0.89	0.86	0.82	0.79
	50	1	1	1	1	1	1	1	0.97	0.93	0.90	0.86	0.82	0.79
		0	1000	2000	3000	4000	5000	6000	7000	8000	9000	10000	11000	12000
	ALTITUDE (FEET ABOVE SEA LEVEL)													

AFTERCOOLER HEAT REJECTION FACTORS (ACHRF)

INLET AIR TEMP °F	130	1.32	1.36	1.41	1.46	1.51	1.56	1.58	1.58	1.58	1.58	1.58	1.58	1.58
	120	1.25	1.30	1.35	1.40	1.44	1.49	1.52	1.52	1.52	1.52	1.52	1.52	1.52
	110	1.19	1.23	1.28	1.33	1.38	1.43	1.45	1.45	1.45	1.45	1.45	1.45	1.45
	100	1.13	1.17	1.22	1.26	1.31	1.36	1.38	1.38	1.38	1.38	1.38	1.38	1.38
	90	1.06	1.11	1.15	1.20	1.24	1.29	1.31	1.31	1.31	1.31	1.31	1.31	1.31
	80	1	1.04	1.08	1.13	1.18	1.22	1.24	1.24	1.24	1.24	1.24	1.24	1.24
	70	1	1	1.02	1.06	1.11	1.15	1.17	1.17	1.17	1.17	1.17	1.17	1.17
	60	1	1	1	1	1.04	1.09	1.11	1.11	1.11	1.11	1.11	1.11	1.11
	50	1	1	1	1	1	1.02	1.04	1.04	1.04	1.04	1.04	1.04	1.04
		0	1000	2000	3000	4000	5000	6000	7000	8000	9000	10000	11000	12000
ALTITUDE (FEET ABOVE SEA LEVEL)														

MINIMUM SPEED CAPABILITY AT THE RATED SPEED'S SITE TORQUE (RPM)

INLET AIR TEMP °F	130	750	750	750	750	750	750	750	750	750	750	750	750	750
	120	750	750	750	750	750	750	750	750	750	750	750	750	750
	110	750	750	750	750	750	750	750	750	750	750	750	750	750
	100	750	750	750	750	750	750	750	750	750	750	750	750	750
	90	750	750	750	750	750	750	750	750	750	750	750	750	750
	80	750	750	750	750	750	750	750	750	750	750	750	750	750
	70	750	750	750	750	750	750	750	750	750	750	750	750	750
	60	750	750	750	750	750	750	750	750	750	750	750	750	750
	50	750	750	750	750	750	750	750	750	750	750	750	750	750
		0	1000	2000	3000	4000	5000	6000	7000	8000	9000	10000	11000	12000
ALTITUDE (FEET ABOVE SEA LEVEL)														

FUEL USAGE GUIDE:

This table shows the derate factor and full load set point timing required for a given fuel. Note that deration and set point timing adjustment may be required as the methane number decreases. Methane number is a scale to measure detonation characteristics of various fuels. The methane number of a fuel is determined by using the Caterpillar methane number calculation.

The Fuel Lower Heating Value (LHV) table shows the derate factor required for a given fuel. To determine the actual power available, use the lowest factor between the Fuel LHV table and the Caterpillar Methane Number table.

ALTITUDE DERATION FACTORS:

This table shows the deration required for various air inlet temperatures and altitudes. Use this information along with the fuel usage guide chart to help determine actual engine power for your site. The derate factors shown do not account for the external cooling system capacity. The derate factors provided assume the external cooling system can maintain the specified cooling water temperatures at site conditions.

ACTUAL ENGINE RATING:

To determine the actual rating of the engine at site conditions, one must consider separately, limitations due to fuel characteristics and air system limitations. The Fuel Usage Guide deration establishes fuel limitations. The Altitude/ Temperature deration factors and RPC(reference the Caterpillar Methane Program) establish air system limitations. RPC comes into play when the Altitude/Temperature deration is less than 1.0 (100%). Under this condition, add the two factors together. When the site conditions do not require an Altitude/Temperature derate (factor is 1.0), it is assumed the turbocharger has sufficient capability to overcome the low fuel relative power, and RPC is ignored. To determine the actual power available, take the lowest rating between 1) and 2).

- 1) Fuel Usage Guide Deration
- 2) $1 - ((1 - \text{Altitude / Temperature Deration}) + (1 - \text{RPC}))$

AFTERCOOLER HEAT REJECTION FACTORS(ACHRF):

To maintain a constant air inlet manifold temperature, as the inlet air temperature goes up, so must the heat rejection. As altitude increases, the turbocharger must work harder to overcome the lower atmospheric pressure. This increases the amount of heat that must be removed from the inlet air by the aftercooler. Use the aftercooler heat rejection factor (ACHRF) to adjust for inlet air temp and altitude conditions. See notes (26) and (27) for application of this factor in calculating the heat exchanger sizing criteria. Failure to properly account for these factors could result in detonation and cause the engine to shutdown or fail.

MINIMUM SPEED CAPABILITY AT THE RATED SPEED'S SITE TORQUE (RPM):

This table shows the minimum allowable engine turndown speed where the engine will maintain the Rated Speed's Torque for the given ambient conditions.

NOTES:

1. Fuel pressure range specified is to the engine gas shutoff valve (GSOV). Additional fuel train components should be considered in pressure and flow calculations.
2. Engine rating is with two engine driven water pumps. Tolerance is $\pm 3\%$ of full load.
3. ISO 3046/1 engine efficiency tolerance is (+)0, (-)5% of full load % efficiency value. Nominal engine efficiency tolerance is $\pm 2.5\%$ of full load % efficiency value.
4. ISO 3046/1 fuel consumption tolerance is (+)5, (-)0% of full load data. Nominal fuel consumption tolerance is $\pm 2.5\%$ of full load data.
5. Air flow value is on a 'wet' basis. Flow is a nominal value with a tolerance of $\pm 5\%$.
6. Inlet and Exhaust Restrictions must not exceed A&I limits based on full load flow rates from the standard technical data sheet.
7. Inlet manifold pressure is a nominal value with a tolerance of $\pm 5\%$.
8. Inlet manifold temperature is a nominal value with a tolerance of $\pm 9^\circ\text{F}$.
9. Timing indicated is for use with the minimum fuel methane number specified. Consult the appropriate fuel usage guide for timing at other methane numbers.
10. Exhaust temperature is a nominal value with a tolerance of (+)63°F, (-)54°F.
11. Exhaust flow value is on a 'wet' basis. Flow is a nominal value with a tolerance of $\pm 6\%$.
12. Emissions data is at engine exhaust flange prior to any after treatment.
13. NOx values are the maximum values expected under steady state conditions.
14. CO, CO₂, THC, NMHC, NMNEHC, and HCHO are the maximum values expected under steady state conditions. THC, NMHC, and NMNEHC do not include aldehydes. An oxidation catalyst may be required to meet Federal, State or local CO or HC requirements.
15. VOCs - Volatile organic compounds as defined in US EPA40 CFR 60, subpart JJJJ
16. Exhaust Oxygen tolerance is ± 0.5 ; Lambda tolerance is ± 0.05 . Lambda and Exhaust Oxygen level are the result of adjusting the engine to operate at the specified NOx level.
17. LHV rate tolerance is $\pm 2.5\%$.
18. Heat rejection to jacket water value displayed includes heat to jacket water alone. Value is based on treated water. Tolerance is $\pm 10\%$ of full load data.
19. Heat rejection to atmosphere based on treated water. Tolerance is $\pm 50\%$ of full load data.
20. Lube oil heat rate based on treated water. Tolerance is $\pm 20\%$ of full load data.
21. Exhaust heat rate based on treated water. Tolerance is $\pm 10\%$ of full load data.
22. Heat rejection to exhaust (LHV to 77°F) value shown includes unburned fuel and is not intended to be used for sizing or recovery calculations.
23. Heat rejection to A/C - Stage 1 based on treated water. Tolerance is $\pm 5\%$ of full load data.
24. Heat rejection to A/C - Stage 2 based on treated water. Tolerance is $\pm 5\%$ of full load data.
25. Pump power includes engine driven jacket water and aftercooler water pumps. Engine brake power includes effects of pump power.
26. Total Jacket Water Circuit heat rejection is calculated as: $(\text{JW} \times 1.1) + (1\text{AC} \times 1.05) + [0.85 \times (1\text{AC} + 2\text{AC}) \times (\text{ACHRF} - 1) \times 1.05]$. Heat exchanger sizing criterion is maximum circuit heat rejection at site conditions, with applied tolerances. A cooling system safety factor may be multiplied by the total circuit heat rejection to provide additional margin.
27. Total Second Stage Aftercooler Circuit heat rejection is calculated as: $(\text{OC} \times 1.2) + (2\text{AC} \times 1.05) + [(1\text{AC} + 2\text{AC}) \times 0.15 \times (\text{ACHRF} - 1) \times 1.05]$. Heat exchanger sizing criterion is maximum circuit heat rejection at site conditions, with applied tolerances. A cooling system safety factor may be multiplied by the total circuit heat rejection to provide additional margin.

FREE FIELD MECHANICAL & EXHAUST NOISE
MECHANICAL: Sound Power (1/3 Octave Frequencies)

Percent Load	Engine Power	Overall	100 Hz	125 Hz	160 Hz	200 Hz	250 Hz	315 Hz	400 Hz	500 Hz	630 Hz	800 Hz
%	bhp	dB(A)	dB(A)	dB(A)	dB(A)	dB(A)	dB(A)	dB(A)	dB(A)	dB(A)	dB(A)	dB(A)
100	2500	126.0	86.3	94.5	99.2	98.8	101.7	105.9	108.0	110.7	108.4	107.3
75	1875	123.1	84.1	92.8	97.4	96.9	101.0	105.5	107.6	110.8	108.0	108.2
50	1250	120.9	86.3	99.0	97.2	97.3	101.3	104.6	108.5	111.8	108.0	107.2

MECHANICAL: Sound Power (1/3 Octave Frequencies)

Percent Load	Engine Power	1 kHz	1.25 kHz	1.6 kHz	2 kHz	2.5 kHz	3.15 kHz	4 kHz	5 kHz	6.3 kHz	8 kHz	10 kHz
%	bhp	dB(A)	dB(A)	dB(A)	dB(A)	dB(A)	dB(A)	dB(A)	dB(A)	dB(A)	dB(A)	dB(A)
100	2500	108.0	109.0	113.2	108.2	108.4	111.8	114.5	124.9	108.8	107.8	111.3
75	1875	107.5	107.6	113.0	107.5	108.0	111.1	116.8	112.2	106.9	115.0	105.5
50	1250	106.9	107.0	112.8	106.9	107.2	110.8	111.5	108.3	107.1	104.8	100.9

EXHAUST: Sound Power (1/3 Octave Frequencies)

Percent Load	Engine Power	Overall	100 Hz	125 Hz	160 Hz	200 Hz	250 Hz	315 Hz	400 Hz	500 Hz	630 Hz	800 Hz
%	bhp	dB(A)	dB(A)	dB(A)	dB(A)	dB(A)	dB(A)	dB(A)	dB(A)	dB(A)	dB(A)	dB(A)
100	2500	138.9	107.1	113.4	117.7	115.0	116.0	120.0	122.0	120.4	122.1	121.7
75	1875	136.7	107.6	108.7	110.6	109.0	110.9	114.2	115.4	113.2	115.3	116.0
50	1250	133.7	104.2	104.2	108.5	106.1	105.8	108.3	112.6	108.2	111.4	112.2

EXHAUST: Sound Power (1/3 Octave Frequencies)

Percent Load	Engine Power	1 kHz	1.25 kHz	1.6 kHz	2 kHz	2.5 kHz	3.15 kHz	4 kHz	5 kHz	6.3 kHz	8 kHz	10 kHz
%	bhp	dB(A)	dB(A)	dB(A)	dB(A)	dB(A)	dB(A)	dB(A)	dB(A)	dB(A)	dB(A)	dB(A)
100	2500	124.8	123.2	123.9	125.9	126.6	130.6	131.3	130.6	129.6	128.0	124.2
75	1875	119.5	119.8	121.2	124.8	126.6	129.0	129.8	128.5	127.4	124.3	119.6
50	1250	116.1	117.3	119.6	122.3	124.4	126.4	127.1	125.5	124.0	119.6	114.0

SOUND PARAMETER DEFINITION:

Sound Power Level Data - DM8702-03

Sound power is defined as the total sound energy emanating from a source irrespective of direction or distance. Sound power level data is presented under two index headings:

Sound power level -- Mechanical
Sound power level -- Exhaust

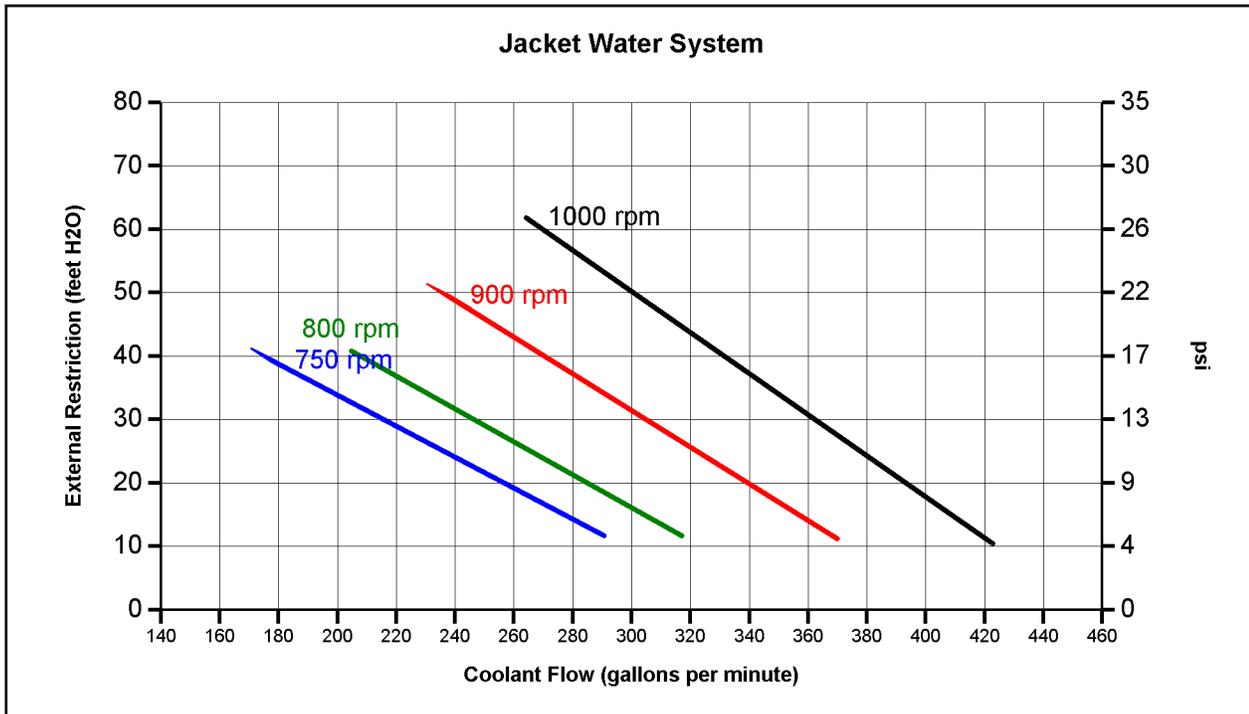
Mechanical: Sound power level data is calculated in accordance with ISO 3747. The data is recorded with the exhaust sound source isolated.

Exhaust: Sound power level data is calculated in accordance with ISO 6798 Annex A. Exhaust data is post-catalyst on gas engine ratings labeled as "Integrated Catalyst".

Measurements made in accordance with ISO 3747 and ISO 6798 for mechanical and exhaust sound level only. Frequency bands outside the displayed ranges are not measured, due to physical test, and environmental conditions that affect the accuracy of the measurement. No cooling system noise is included unless specifically indicated. Sound level data is indicative of noise levels recorded on one engine sample in a survey grade 3 environment.

How an engine is packaged, installed and the site acoustical environment will affect the site specific sound levels. For site specific sound level guarantees, sound data collection needs to be done on-site or under similar conditions.

ENGINE POWER (bhp): 2500
 ENGINE SPEED (rpm): 1000
 EXHAUST MANIFOLD: DRY
 JACKET WATER OUTLET (°F): 190
 COOLING SYSTEM: JW+1AC, OC+2AC
 INLET MANIFOLD AIR TEMP (°F):



Coolant Flow vs. Allowable External Restriction

Engine Speed (rpm) 750 800 900 1000

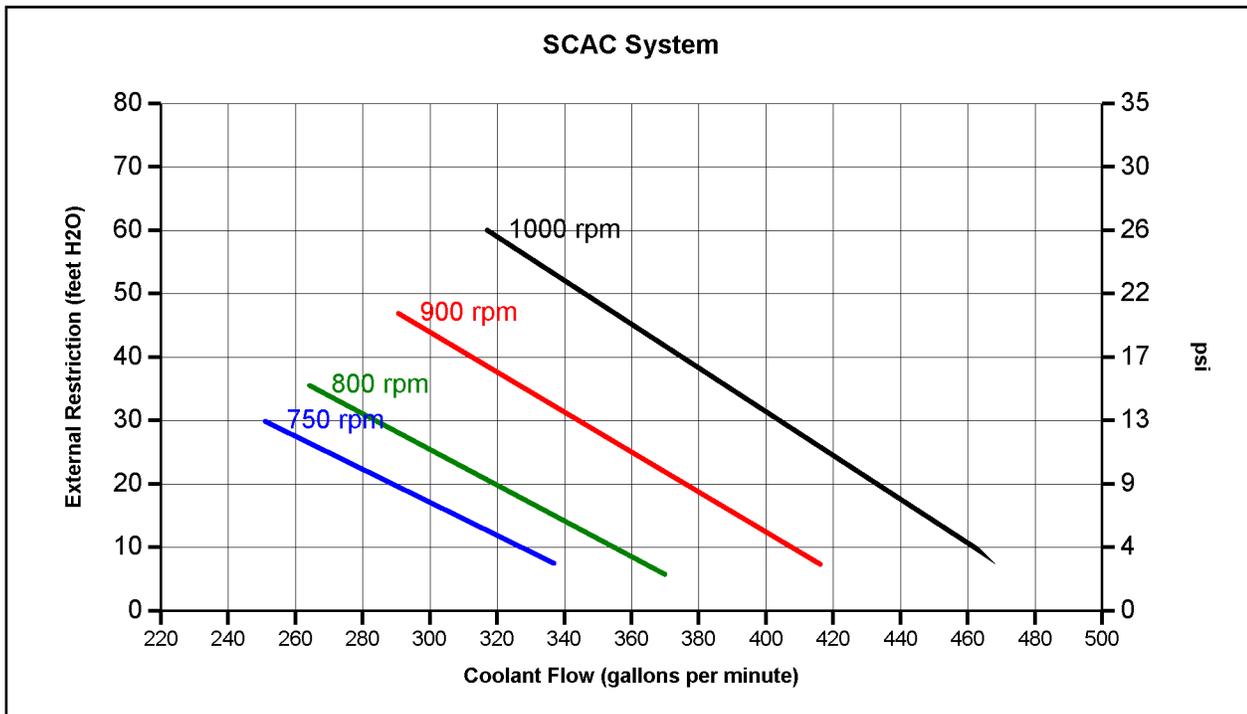
Flow (GPM) Restriction (feet H2O)

Flow (GPM)	750 rpm Restriction (feet H2O)	800 rpm Restriction (feet H2O)	900 rpm Restriction (feet H2O)	1000 rpm Restriction (feet H2O)
180	38.7			
200	33.9			
220	29.0	36.9		
240	24.1	31.7	48.8	
260	19.2	26.5	43.0	
280	14.3	21.3	37.2	56.7
300		16.1	31.4	50.2
320			25.6	43.7
340			19.8	37.2
360			14.1	30.8
380				24.3
400				17.8
420				11.3

Notes:

- 7E8181 JW Pump
- Drive Ratio 2.5:1
- Curves indicate maximum allowable external resistance.
- Do not project curves beyond range shown.
- PSI conversion based on specific gravity of 1.0

ENGINE POWER (bhp):	2500	JACKET WATER OUTLET (°F):	190
ENGINE SPEED (rpm):	1000	COOLING SYSTEM:	JW+1AC, OC+2AC
EXHAUST MANIFOLD:	DRY	INLET MANIFOLD AIR TEMP (°F):	



Coolant Flow vs. Allowable External Restriction

Engine Speed (rpm) **750** **800** **900** **1000**

Flow (GPM)	Restriction (feet H2O)			
260	27.5			
280	22.3	31.1		
300	17.1	25.5	44.0	
320	11.9	19.8	37.7	59.0
340		14.2	31.3	52.1
360		8.5	25.0	45.2
380			18.7	38.3
400			12.4	31.4
420				24.5
440				17.6
460				10.7

Notes:

- 7E8181 SCAC Pump
- Drive Ratio 2.5:1
- Curves indicate maximum allowable external resistance.
- Do not project curves beyond range shown.
- PSI conversion based on specific gravity of 1.0



Table of Contents

1 INTRODUCTION	3
1.1 Competitive Advantage.....	3
1.2 Important Safety Information	4
2 SIZING	5
2.1 30” Combustor	5
2.2 48” Combustor	5
3 CONFIGURATIONS AND ACCESSORIES	6
3.1 Skid Options	6
3.2 Rain/Snow Cap	6
3.3 Body Extension.....	7
3.4 Leg Extension.....	7
3.5 Standard Accessories	7
3.5.1 – Profire™ BMS	7
3.5.2 – Stainless Steel Burner Grid.....	8
4 PERFORMANCE.....	8
5 DIAGRAMS & DRAWINGS.....	9
5.1 Piping and Instrumentation Diagram (P&ID)	10
5.2 General Arrangement of Unit.....	12



1 | INTRODUCTION

SpiralX LLC offers 30" or 48" enclosed combustors as an efficient method of destroying BTEX. They are designed for the destruction of volatile organic compounds (VOCs) at rates greater than 95%, and compliant with regulations governing upstream oil and gas facilities (40 CFR 60, Subpart OOOOa) and gas dehydration facilities (40 CFR 63, Subparts HH and HHH). They can be built on-skid with the condenser as a single unit, or separately on an independent skid. All our combustion units use a Profire™ Burner Management System for the most reliable and efficient means of monitoring the pilot flame, and various accessories allow the combustor to thrive in almost any weather condition. Please look over the many types of units and accessories available within this catalog to see which combustor assembly is right for you. Please call us at 469-480-8802 for any questions you may have.

1.1 | Competitive Advantage

SpiralX has modified product design per customer feedback and includes:

- Stainless steel burner grids for increased product life (2-3 years). Shown to outlast standard carbon steel and ceramic burner grids.
- Lifting supports located at the top of the combustor for easier handling during transport and a top ring bracket for adding optional accessories such as rain/snow caps and body extensions.
- Dual burner grid option for burning exhaust from two different sources.
- Precision laser cutting for more precise and consistent designs.

1.2 | Important Safety Information

Combustors are an explosion and fire hazard and must always be handled and inspected with caution.

Combustors should always be level or at a slight incline from their condenser units to avoid condensate from entering the combustion chamber.

Condensate fluid is extremely flammable. All safety precautions should be used when operating the system.

Positions of components shown within this document may differ slightly from your actual unit.

EXPLOSION HAZARD

Do not attempt to service or open access panel unless proper safety precautions have been taken.



2 | SIZING

SpiralX LLC combustors are made from A36 structural steel and come in 30" or 48" diameter bodies, depending on the amount of BTEX destruction required. These bodies are surrounded by a steel grate to protect objects from coming in direct contact with the combustion section during operation. The two sizes are listed below with their respective dimensions. Note that the on-site dimensions can change depending on the type of skid utilized for the combustor.

2.1 | 30" Combustor



HEIGHT: 106.00"

WEIGHT: 1300 LBS.

DIAMETER: 34.16" with grate. 37.86" max with legs.

2.2 | 48" Combustor

HEIGHT: 143.88"

WEIGHT: 1900 LBS.

DIAMETER: 54" with grate. 63.67" max with legs.

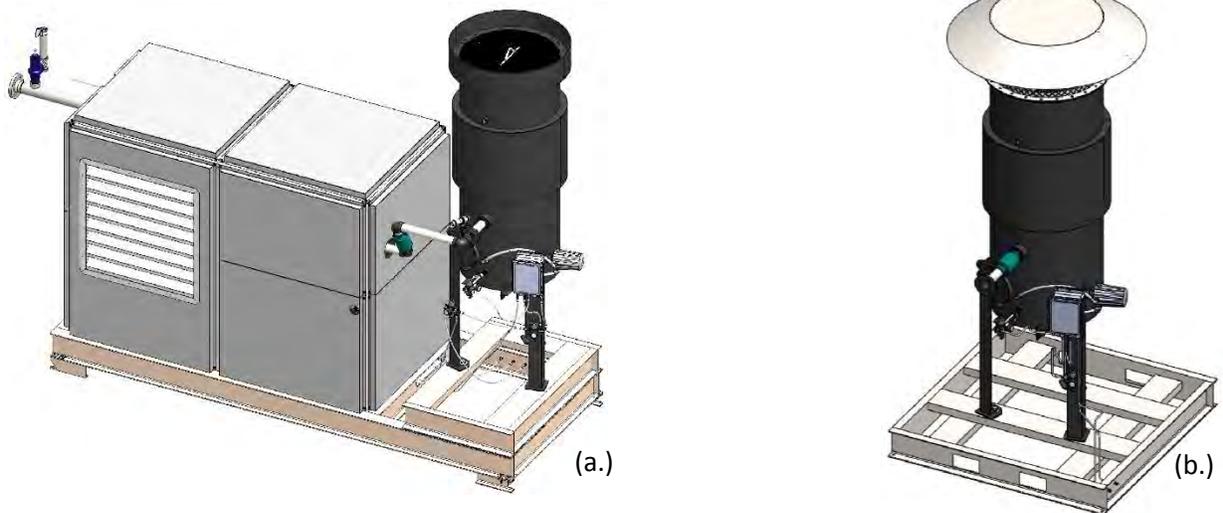


3 | CONFIGURATIONS AND ACCESSORIES

SpiralX combustors are made to suit many environments and regulations within the industry. Here is a list of different designs SpiralX offers.

3.1 | Skid Options

Spatial restrictions can sometimes limit the required footprint of the BTEX system, so SpiralX offers combustor designs that can be attached to or separate from the condenser system.



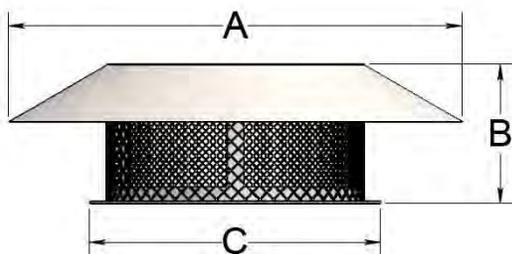
Example of combustor attached to condenser skid (a.) and a standalone combustor skid that can be set close by on site (b.).

3.2 | Rain/Snow Cap

The rain cap can be attached to the top ring bracket to protect the pilot ignition from being extinguished during rainstorms. In the colder regions, the cap can prevent snow from filling up the combustor which can make initial pilot ignition very difficult and time consuming.



Plain Carbon Steel



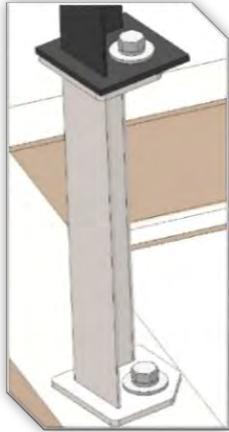
	30"	48"
A	53"	69.75"
B	16.3"	16.3"
C	34"	52"
Weight	66 lbs.	107 lbs.

3.3 | Body Extension

SpiralX offers an extended 120" middle section to the combustor for sites that have safety regulations requiring destroyed gases to be vented at higher altitudes. The tops of these extensions have top ring brackets as well in case a rain cap is also needed.



3.4 | Leg Extension



Leg extensions can raise the combustor exhaust similar to a body extension by lifting the entire combustor, but only to an additional height of 20.75". The main function of the leg extensions is to make the combustor inlet higher than the condenser outlet. This prevents condensate from entering the combustor which can be hazardous.

3.5 | Standard Accessories

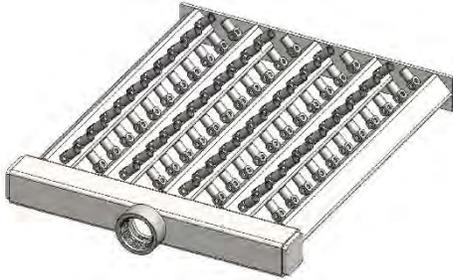
3.5.1 – Profire™ BMS

All SpiralX combustors are fitted with Profire™ Burner Management Systems (BMS). The 2100 model offers advanced pilot monitoring with automatic reignition upon spark detection and self-regulating valve automation based on combustor temperature. All monitored data can optionally be communicated to a central location in real time and remotely controlled via the SCADA and Modbus RS-485 add-ons. This on-board data logging feature can record pilot status and other key operating parameters, allowing for historical data retrieval which can aid in compliance documentation.



For simpler systems that only require flame detection and ignition, a more cost-effective Flare Ignition System (1300F model) is available, designed solely for automatic ignition of flare stacks.

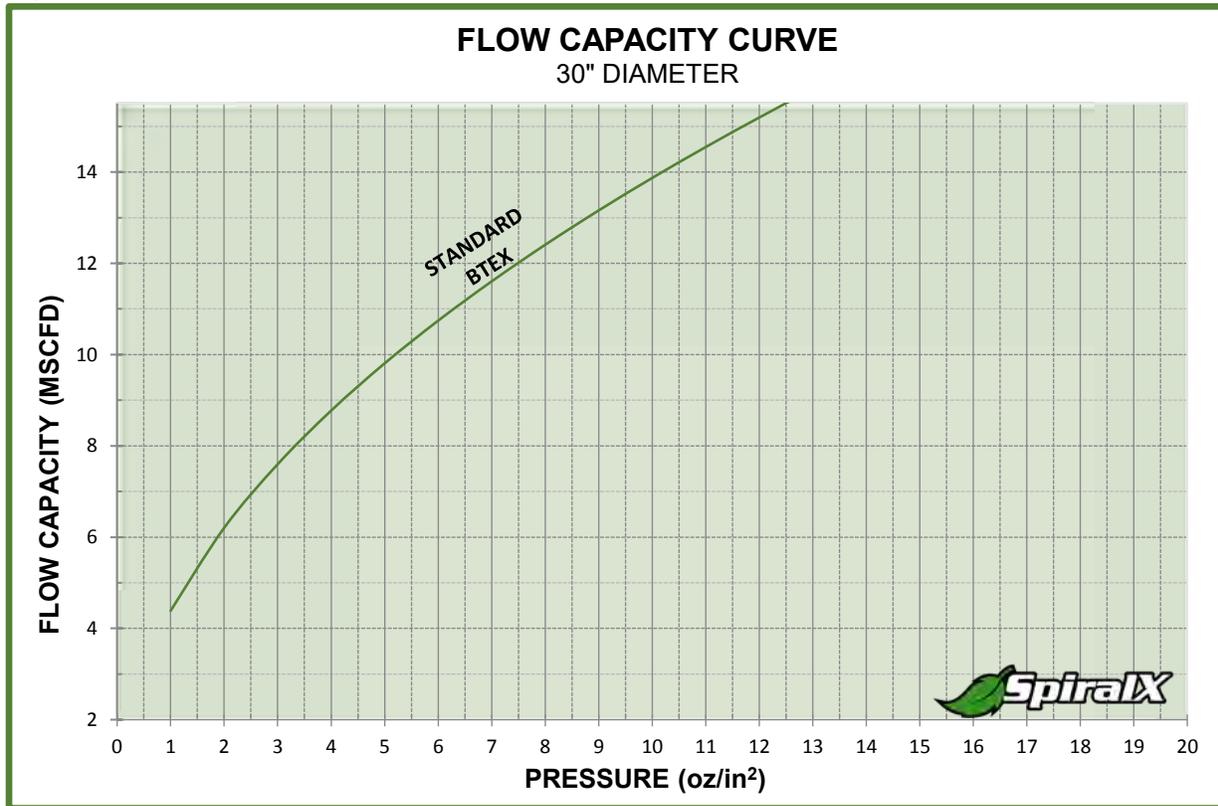
These systems are rated for Class 1, Div. II, but can be wired remotely to the combustor for sites with Div. I environments. Hook ups can be made with stainless steel tubing or JIC hosing.



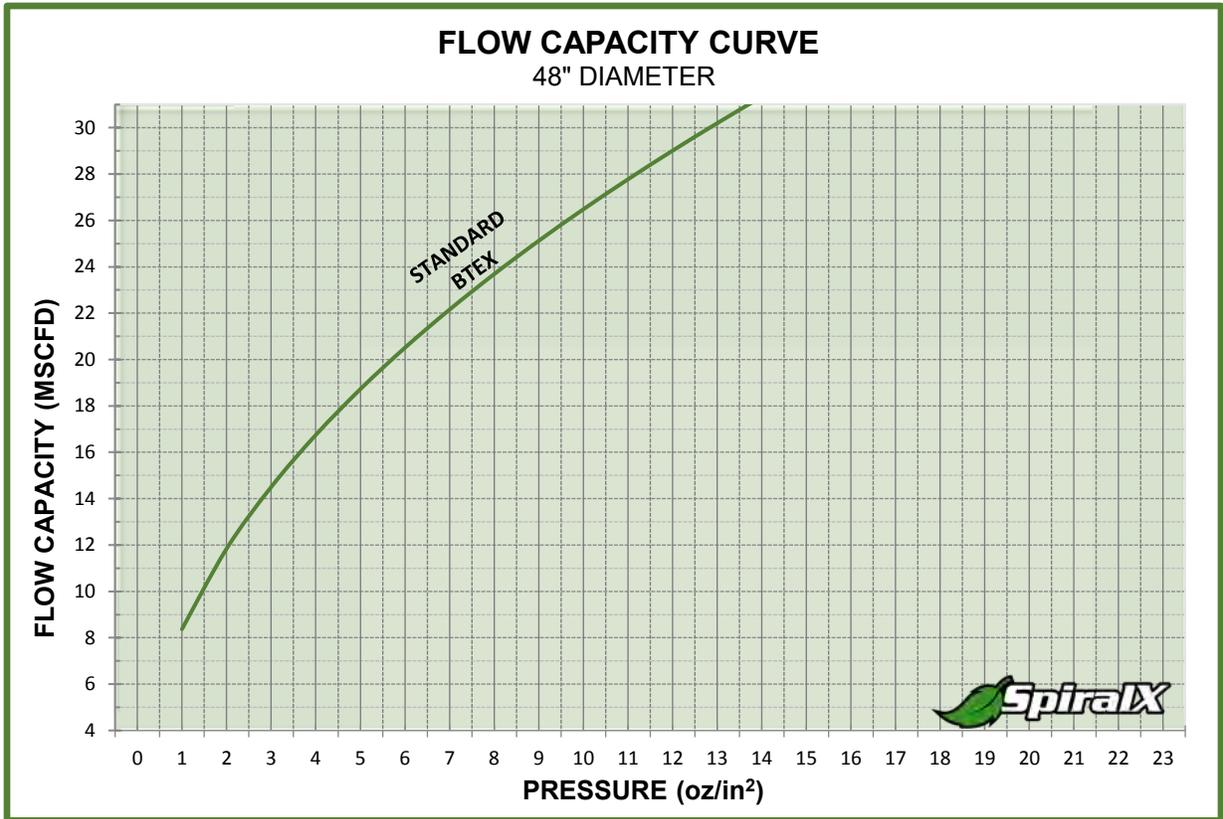
3.5.2 – Stainless Steel Burner Grid

SpiralX burner grids are manufactured in-house with stainless steel for corrosion resistance and durability. A single coupling housing facilitates gas supply hook-up as well.

4 | PERFORMANCE



Flow capacity curve of BTEX for 30" diameter combustor as a function of pressure.

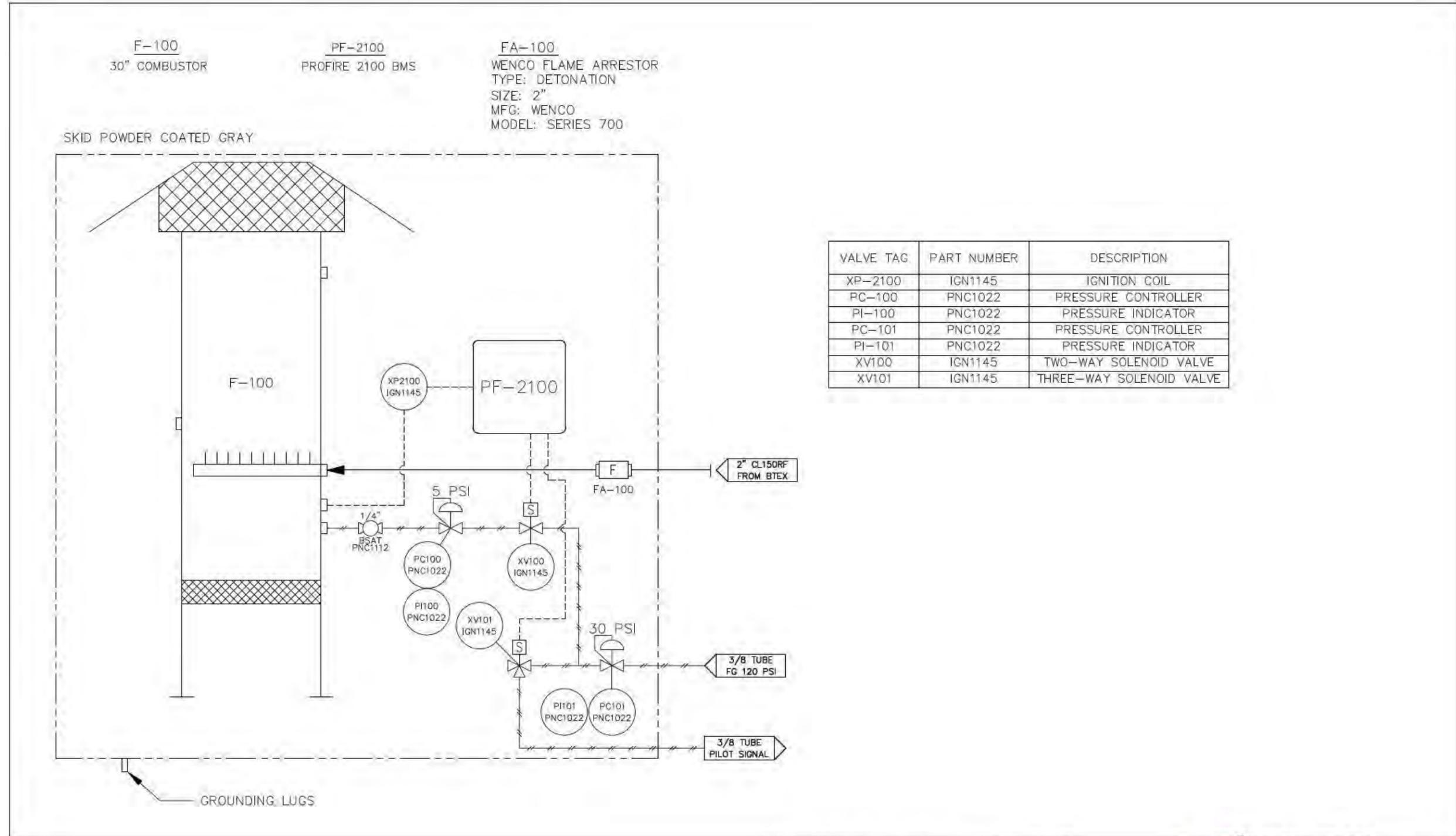


Flow capacity curve of BTEX for 48" diameter combustor as a function of pressure.

5 | DIAGRAMS & DRAWINGS

The following diagrams are typical for stand-alone combustors only. The dimensions and layouts of combustors on skid with condenser systems can vary based on system needs and series model.

<p>MOTOR</p> <p>FAN</p> <p>ACCUMULATOR TANK</p> <p>COMBUSTOR</p> <p>FINNED FORCED HEAT EXCHANGER</p> <p>FINNED AMBIENT HEAT EXCHANGER</p> <p>DIAPHRAGM PUMP</p> <p>CENTRIFUGAL COMPRESSOR</p> <p>HORIZONTAL TANK</p> <p>INSULATED</p> <p>SHELL AND TUBE HEAT EXCHANGER</p>	<h3 style="text-align: center;">VALVE IDENTIFICATION</h3> <p>VALVE FACING VALVE TYPE VALVE SIZE</p> <p>VALVE CLASSIFICATION (FLG OR PRESSURE RATING) VALVE SPECIALTY TYPE (OPTIONAL)</p> <p style="text-align: center;">2" B J E (F)</p> <table border="1" style="width:100%; border-collapse: collapse;"> <thead> <tr> <th>VALVE TYPE</th> <th>VALVE FACING</th> <th>CLASSIFICATION</th> <th>VALVE SPECIALTY</th> </tr> <tr> <th>CODE</th> <th>TYPE</th> <th>CODE</th> <th>TYPE</th> </tr> </thead> <tbody> <tr><td>B</td><td>BALL</td><td>A</td><td>ANSI 150</td></tr> <tr><td>C</td><td>CHECK</td><td>B</td><td>ANSI 300</td></tr> <tr><td>D</td><td>DIAPHRAGM</td><td>C</td><td>ANSI 400</td></tr> <tr><td>G</td><td>GATE</td><td>D</td><td>ANSI 800</td></tr> <tr><td>M</td><td>MULTI-PORT</td><td>E</td><td>ANSI 900</td></tr> <tr><td>N</td><td>NEEDLE</td><td>F</td><td>ANSI 1500</td></tr> <tr><td>R</td><td>CLOSE</td><td>G</td><td>ANSI 2500</td></tr> <tr><td>P</td><td>PLUG</td><td>H</td><td>API 2000</td></tr> <tr><td>Y</td><td>BUTTERFLY</td><td>I</td><td>API 3000</td></tr> <tr><td>X</td><td>CHOKE</td><td>J</td><td>API 5000</td></tr> <tr><td></td><td></td><td>K</td><td>API 10000</td></tr> <tr><td></td><td></td><td>L</td><td>API 15000</td></tr> <tr><td></td><td></td><td>A</td><td>ANSI 150</td></tr> <tr><td></td><td></td><td>B</td><td>ANSI 300</td></tr> <tr><td></td><td></td><td>C</td><td>ANSI 400</td></tr> <tr><td></td><td></td><td>D</td><td>ANSI 800</td></tr> <tr><td></td><td></td><td>E</td><td>ANSI 900</td></tr> <tr><td></td><td></td><td>F</td><td>ANSI 1500</td></tr> <tr><td></td><td></td><td>G</td><td>ANSI 2500</td></tr> <tr><td></td><td></td><td>H</td><td>API 2000</td></tr> <tr><td></td><td></td><td>I</td><td>API 3000</td></tr> <tr><td></td><td></td><td>J</td><td>API 5000</td></tr> <tr><td></td><td></td><td>K</td><td>API 10000</td></tr> <tr><td></td><td></td><td>L</td><td>API 15000</td></tr> <tr><td></td><td></td><td>M</td><td>API 20000</td></tr> <tr><td></td><td></td><td>N</td><td>API 30000</td></tr> <tr><td></td><td></td><td>O</td><td>API 40000</td></tr> <tr><td></td><td></td><td>P</td><td>API 50000</td></tr> <tr><td></td><td></td><td>Q</td><td>API 60000</td></tr> <tr><td></td><td></td><td>R</td><td>API 70000</td></tr> <tr><td></td><td></td><td>S</td><td>API 80000</td></tr> <tr><td></td><td></td><td>T</td><td>API 90000</td></tr> <tr><td></td><td></td><td>U</td><td>API 100000</td></tr> <tr><td></td><td></td><td>V</td><td>API 110000</td></tr> <tr><td></td><td></td><td>W</td><td>API 120000</td></tr> <tr><td></td><td></td><td>X</td><td>API 130000</td></tr> <tr><td></td><td></td><td>Y</td><td>API 140000</td></tr> <tr><td></td><td></td><td>Z</td><td>API 150000</td></tr> </tbody> </table>	VALVE TYPE	VALVE FACING	CLASSIFICATION	VALVE SPECIALTY	CODE	TYPE	CODE	TYPE	B	BALL	A	ANSI 150	C	CHECK	B	ANSI 300	D	DIAPHRAGM	C	ANSI 400	G	GATE	D	ANSI 800	M	MULTI-PORT	E	ANSI 900	N	NEEDLE	F	ANSI 1500	R	CLOSE	G	ANSI 2500	P	PLUG	H	API 2000	Y	BUTTERFLY	I	API 3000	X	CHOKE	J	API 5000			K	API 10000			L	API 15000			A	ANSI 150			B	ANSI 300			C	ANSI 400			D	ANSI 800			E	ANSI 900			F	ANSI 1500			G	ANSI 2500			H	API 2000			I	API 3000			J	API 5000			K	API 10000			L	API 15000			M	API 20000			N	API 30000			O	API 40000			P	API 50000			Q	API 60000			R	API 70000			S	API 80000			T	API 90000			U	API 100000			V	API 110000			W	API 120000			X	API 130000			Y	API 140000			Z	API 150000	<h3 style="text-align: center;">LINE IDENTIFICATION</h3> <p>PIPING CLASSIFICATION PIPE SIZE FLOW MEDIUM MATERIAL CLASSIFICATION</p> <p>OPTIONAL INSULATION AND THICKNESS LINE NUMBER</p> <p style="text-align: center;">4" LH - A1 - 101 - B1" - SR</p> <table border="1" style="width:100%; border-collapse: collapse;"> <thead> <tr> <th>FLOW MEDIUM IDENTIFIER</th> <th>PIPING CLASSIFICATION</th> <th>INSULATION IDENTIFIERS</th> </tr> <tr> <th>CODE</th> <th>CLASS</th> <th>CODE</th> <th>INSULATION TYPE</th> </tr> </thead> <tbody> <tr><td>AD</td><td>ATMOSPHERIC DRAIN</td><td>A</td><td>PERSONNEL PROTECTION</td></tr> <tr><td>AF</td><td>AVIATION FUEL</td><td>B</td><td>HEAT TRACING</td></tr> <tr><td>AV</td><td>ATMOSPHERIC VENT</td><td>C</td><td>FREEZE PROTECTION</td></tr> <tr><td>BW</td><td>BOILER FEED WATER</td><td>D</td><td>HEAT CONSERVATION</td></tr> <tr><td>BP</td><td>BULK PRODUCTION</td><td>E</td><td>COLD CONSERVATION</td></tr> <tr><td>CI</td><td>CHEMICAL INJECTION</td><td>F</td><td>ANTI - SWEAT</td></tr> <tr><td>CW</td><td>COOLING WATER OR JACKET WATER</td><td></td><td></td></tr> <tr><td>DF</td><td>DIESEL FUEL</td><td></td><td></td></tr> <tr><td>DR</td><td>DRAIN</td><td></td><td></td></tr> <tr><td>EX</td><td>EXHAUST</td><td></td><td></td></tr> <tr><td>FG</td><td>FUEL GAS</td><td></td><td></td></tr> <tr><td>FL</td><td>FLARE</td><td></td><td></td></tr> <tr><td>FW</td><td>FIRE WATER</td><td></td><td></td></tr> <tr><td>GH</td><td>GAS, HYDROCARBON</td><td></td><td></td></tr> <tr><td>GL</td><td>GLYCOL</td><td></td><td></td></tr> <tr><td>HF</td><td>HYDRAULIC FLUID</td><td></td><td></td></tr> <tr><td>HM</td><td>HEAT MEDIUM</td><td></td><td></td></tr> <tr><td>HR</td><td>HIGH PRESSURE RELIEF</td><td></td><td></td></tr> <tr><td>IA</td><td>INSTRUMENT AIR</td><td></td><td></td></tr> <tr><td>IG</td><td>INSTRUMENT GAS</td><td></td><td></td></tr> <tr><td>LH</td><td>LIQUID HYDROCARBON</td><td></td><td></td></tr> <tr><td>LO</td><td>LUBE OIL</td><td></td><td></td></tr> <tr><td>LR</td><td>LOW PRESSURE RELIEF</td><td></td><td></td></tr> <tr><td>MD</td><td>MUD OR MUD AND CEMENT</td><td></td><td></td></tr> <tr><td>NI</td><td>NITROGEN</td><td></td><td></td></tr> <tr><td>OX</td><td>OXYGEN</td><td></td><td></td></tr> <tr><td>PW</td><td>PRODUCED WATER</td><td></td><td></td></tr> <tr><td>DW</td><td>POTABLE WATER</td><td></td><td></td></tr> <tr><td>SA</td><td>START AIR</td><td></td><td></td></tr> <tr><td>SC</td><td>STEAM CONDENSATE</td><td></td><td></td></tr> <tr><td>SD</td><td>SANITARY DRAIN</td><td></td><td></td></tr> <tr><td>SG</td><td>START GAS</td><td></td><td></td></tr> <tr><td>ST</td><td>STEAM</td><td></td><td></td></tr> <tr><td>UT</td><td>UTILITY WATER</td><td></td><td></td></tr> <tr><td>WH</td><td>WATER AND HYDROCARBONS</td><td></td><td></td></tr> <tr><td>ZA THRU ZZ</td><td>MISCELLANEOUS FLOW MEDIA</td><td></td><td></td></tr> </tbody> </table>	FLOW MEDIUM IDENTIFIER	PIPING CLASSIFICATION	INSULATION IDENTIFIERS	CODE	CLASS	CODE	INSULATION TYPE	AD	ATMOSPHERIC DRAIN	A	PERSONNEL PROTECTION	AF	AVIATION FUEL	B	HEAT TRACING	AV	ATMOSPHERIC VENT	C	FREEZE PROTECTION	BW	BOILER FEED WATER	D	HEAT CONSERVATION	BP	BULK PRODUCTION	E	COLD CONSERVATION	CI	CHEMICAL INJECTION	F	ANTI - SWEAT	CW	COOLING WATER OR JACKET WATER			DF	DIESEL FUEL			DR	DRAIN			EX	EXHAUST			FG	FUEL GAS			FL	FLARE			FW	FIRE WATER			GH	GAS, HYDROCARBON			GL	GLYCOL			HF	HYDRAULIC FLUID			HM	HEAT MEDIUM			HR	HIGH PRESSURE RELIEF			IA	INSTRUMENT AIR			IG	INSTRUMENT GAS			LH	LIQUID HYDROCARBON			LO	LUBE OIL			LR	LOW PRESSURE RELIEF			MD	MUD OR MUD AND CEMENT			NI	NITROGEN			OX	OXYGEN			PW	PRODUCED WATER			DW	POTABLE WATER			SA	START AIR			SC	STEAM CONDENSATE			SD	SANITARY DRAIN			SG	START GAS			ST	STEAM			UT	UTILITY WATER			WH	WATER AND HYDROCARBONS			ZA THRU ZZ	MISCELLANEOUS FLOW MEDIA			<h3 style="text-align: center;">DISCRETE INSTRUMENT</h3> <p>INSTRUMENT (LOCAL MOUNT) MASTER PANEL NORMALLY INACCESSIBLE DISCRETE INSTRUMENT LOCAL PANEL MOUNTED INSTRUMENT (MOUNTED ON FRONT OF PANEL) LOCAL PANEL MOUNTED INSTRUMENT (MOUNTED ON REAR OF PANEL) LIGHT IN FIELD</p>
VALVE TYPE	VALVE FACING	CLASSIFICATION	VALVE SPECIALTY																																																																																																																																																																																																																																																																																																																							
CODE	TYPE	CODE	TYPE																																																																																																																																																																																																																																																																																																																							
B	BALL	A	ANSI 150																																																																																																																																																																																																																																																																																																																							
C	CHECK	B	ANSI 300																																																																																																																																																																																																																																																																																																																							
D	DIAPHRAGM	C	ANSI 400																																																																																																																																																																																																																																																																																																																							
G	GATE	D	ANSI 800																																																																																																																																																																																																																																																																																																																							
M	MULTI-PORT	E	ANSI 900																																																																																																																																																																																																																																																																																																																							
N	NEEDLE	F	ANSI 1500																																																																																																																																																																																																																																																																																																																							
R	CLOSE	G	ANSI 2500																																																																																																																																																																																																																																																																																																																							
P	PLUG	H	API 2000																																																																																																																																																																																																																																																																																																																							
Y	BUTTERFLY	I	API 3000																																																																																																																																																																																																																																																																																																																							
X	CHOKE	J	API 5000																																																																																																																																																																																																																																																																																																																							
		K	API 10000																																																																																																																																																																																																																																																																																																																							
		L	API 15000																																																																																																																																																																																																																																																																																																																							
		A	ANSI 150																																																																																																																																																																																																																																																																																																																							
		B	ANSI 300																																																																																																																																																																																																																																																																																																																							
		C	ANSI 400																																																																																																																																																																																																																																																																																																																							
		D	ANSI 800																																																																																																																																																																																																																																																																																																																							
		E	ANSI 900																																																																																																																																																																																																																																																																																																																							
		F	ANSI 1500																																																																																																																																																																																																																																																																																																																							
		G	ANSI 2500																																																																																																																																																																																																																																																																																																																							
		H	API 2000																																																																																																																																																																																																																																																																																																																							
		I	API 3000																																																																																																																																																																																																																																																																																																																							
		J	API 5000																																																																																																																																																																																																																																																																																																																							
		K	API 10000																																																																																																																																																																																																																																																																																																																							
		L	API 15000																																																																																																																																																																																																																																																																																																																							
		M	API 20000																																																																																																																																																																																																																																																																																																																							
		N	API 30000																																																																																																																																																																																																																																																																																																																							
		O	API 40000																																																																																																																																																																																																																																																																																																																							
		P	API 50000																																																																																																																																																																																																																																																																																																																							
		Q	API 60000																																																																																																																																																																																																																																																																																																																							
		R	API 70000																																																																																																																																																																																																																																																																																																																							
		S	API 80000																																																																																																																																																																																																																																																																																																																							
		T	API 90000																																																																																																																																																																																																																																																																																																																							
		U	API 100000																																																																																																																																																																																																																																																																																																																							
		V	API 110000																																																																																																																																																																																																																																																																																																																							
		W	API 120000																																																																																																																																																																																																																																																																																																																							
		X	API 130000																																																																																																																																																																																																																																																																																																																							
		Y	API 140000																																																																																																																																																																																																																																																																																																																							
		Z	API 150000																																																																																																																																																																																																																																																																																																																							
FLOW MEDIUM IDENTIFIER	PIPING CLASSIFICATION	INSULATION IDENTIFIERS																																																																																																																																																																																																																																																																																																																								
CODE	CLASS	CODE	INSULATION TYPE																																																																																																																																																																																																																																																																																																																							
AD	ATMOSPHERIC DRAIN	A	PERSONNEL PROTECTION																																																																																																																																																																																																																																																																																																																							
AF	AVIATION FUEL	B	HEAT TRACING																																																																																																																																																																																																																																																																																																																							
AV	ATMOSPHERIC VENT	C	FREEZE PROTECTION																																																																																																																																																																																																																																																																																																																							
BW	BOILER FEED WATER	D	HEAT CONSERVATION																																																																																																																																																																																																																																																																																																																							
BP	BULK PRODUCTION	E	COLD CONSERVATION																																																																																																																																																																																																																																																																																																																							
CI	CHEMICAL INJECTION	F	ANTI - SWEAT																																																																																																																																																																																																																																																																																																																							
CW	COOLING WATER OR JACKET WATER																																																																																																																																																																																																																																																																																																																									
DF	DIESEL FUEL																																																																																																																																																																																																																																																																																																																									
DR	DRAIN																																																																																																																																																																																																																																																																																																																									
EX	EXHAUST																																																																																																																																																																																																																																																																																																																									
FG	FUEL GAS																																																																																																																																																																																																																																																																																																																									
FL	FLARE																																																																																																																																																																																																																																																																																																																									
FW	FIRE WATER																																																																																																																																																																																																																																																																																																																									
GH	GAS, HYDROCARBON																																																																																																																																																																																																																																																																																																																									
GL	GLYCOL																																																																																																																																																																																																																																																																																																																									
HF	HYDRAULIC FLUID																																																																																																																																																																																																																																																																																																																									
HM	HEAT MEDIUM																																																																																																																																																																																																																																																																																																																									
HR	HIGH PRESSURE RELIEF																																																																																																																																																																																																																																																																																																																									
IA	INSTRUMENT AIR																																																																																																																																																																																																																																																																																																																									
IG	INSTRUMENT GAS																																																																																																																																																																																																																																																																																																																									
LH	LIQUID HYDROCARBON																																																																																																																																																																																																																																																																																																																									
LO	LUBE OIL																																																																																																																																																																																																																																																																																																																									
LR	LOW PRESSURE RELIEF																																																																																																																																																																																																																																																																																																																									
MD	MUD OR MUD AND CEMENT																																																																																																																																																																																																																																																																																																																									
NI	NITROGEN																																																																																																																																																																																																																																																																																																																									
OX	OXYGEN																																																																																																																																																																																																																																																																																																																									
PW	PRODUCED WATER																																																																																																																																																																																																																																																																																																																									
DW	POTABLE WATER																																																																																																																																																																																																																																																																																																																									
SA	START AIR																																																																																																																																																																																																																																																																																																																									
SC	STEAM CONDENSATE																																																																																																																																																																																																																																																																																																																									
SD	SANITARY DRAIN																																																																																																																																																																																																																																																																																																																									
SG	START GAS																																																																																																																																																																																																																																																																																																																									
ST	STEAM																																																																																																																																																																																																																																																																																																																									
UT	UTILITY WATER																																																																																																																																																																																																																																																																																																																									
WH	WATER AND HYDROCARBONS																																																																																																																																																																																																																																																																																																																									
ZA THRU ZZ	MISCELLANEOUS FLOW MEDIA																																																																																																																																																																																																																																																																																																																									
<p>CONCENTRIC REDUCER</p> <p>ECCENTRIC REDUCER</p> <p>CAP</p> <p>FLANGED CONNECTION</p> <p>HOSE CONNECTION</p> <p>FLAME ARRESTOR</p> <p>PRESSURE SAFETY VALVE</p> <p>SCREWED UNION CONNECTION</p>	<h3 style="text-align: center;">PLC SYMBOLS</h3> <p>DIGITAL INPUT (TO PROGRAMMABLE CONTROLLER)</p> <p>DIGITAL OUTPUT (FROM PROGRAMMABLE CONTROLLER)</p> <p>ANALOG INPUT (TO PROGRAMMABLE CONTROLLER)</p> <p>ANALOG OUTPUT (FROM PROGRAMMABLE CONTROLLER)</p> <p>ELECTRONIC SAFETY SYSTEM</p> <p>PROCESS CONTROL SYSTEM</p>	<h3 style="text-align: center;">GENERAL ABBREVIATIONS</h3> <table border="1" style="width:100%; border-collapse: collapse;"> <tbody> <tr><td>AI</td><td>ANALOG INPUT</td><td>LAL</td><td>LEVEL ALARM LOW</td><td>PSV</td><td>PRESSURE SAFETY VALVE</td></tr> <tr><td>A/M</td><td>AUTO/MANUAL</td><td>LAH</td><td>LEVEL ALARM HIGH</td><td>PSIG</td><td>POUNDS PER SQUARE INCH GAUGE</td></tr> <tr><td>AO</td><td>ANALOG OUTPUT</td><td>LIC</td><td>LEVEL INDICATING CONTROLLER</td><td>SDV</td><td>SHUT DOWN VALVE</td></tr> <tr><td>AS</td><td>AIR SUPPLY</td><td>LI</td><td>LEVEL INDICATOR</td><td>SV</td><td>SOLENOID VALVE</td></tr> <tr><td>BF</td><td>BLIND FLANGE</td><td>UIS</td><td>LEVEL INDICATING SWITCH</td><td>TC</td><td>TEMPERATURE CONTROLLER</td></tr> <tr><td>BPV</td><td>BACK PRESSURE VALVE</td><td>UIT</td><td>LEVEL INDICATING TRANSMITTER</td><td>PDT</td><td>PRESSURE DIFFERENTIAL TRANSMITTER</td></tr> <tr><td>DI</td><td>DIGITAL INPUT</td><td>LT</td><td>LEVEL TRANSMITTER</td><td>PDC</td><td>PRESSURE DIFFERENTIAL CONTROLLER</td></tr> <tr><td>DO</td><td>DIGITAL OUTPUT</td><td>LC</td><td>LEVEL CONTROLLER</td><td>PDI</td><td>PRESSURE DIFFERENTIAL INDICATOR</td></tr> <tr><td>EI</td><td>POSITION INDICATOR</td><td>LCH</td><td>LEVEL CONTROLLER HIGH</td><td>TI</td><td>TEMPERATURE INDICATOR</td></tr> <tr><td>F</td><td>FLAME ARRESTOR</td><td>LCL</td><td>LEVEL CONTROLLER LOW</td><td>TCV</td><td>TEMPERATURE CONTROL VALVE</td></tr> <tr><td>FC</td><td>FLOW CONTROLLER</td><td>LG</td><td>LEVEL GAUGE</td><td>LVV</td><td>LEVEL GAUGE VALVE</td></tr> <tr><td>FI</td><td>FLOW INDICATOR</td><td>LS</td><td>LEVEL SWITCH</td><td>DDC</td><td>TEMPERATURE DIFFERENTIAL CONTROLLER</td></tr> <tr><td>FCV</td><td>FLOW CONTROL VALVE</td><td>LSHH</td><td>LEVEL SAFETY HIGH HIGH</td><td>DDIC</td><td>TEMPERATURE DIFF INDICATOR CONTROLLER</td></tr> <tr><td>FE</td><td>FLOW ELEMENT</td><td>LSH</td><td>LEVEL SAFETY HIGH</td><td>TE</td><td>TEMPERATURE ELEMENT</td></tr> <tr><td>FI</td><td>FLOW INDICATOR CONTROLLER</td><td>LSL</td><td>LEVEL SAFETY LOW</td><td>TIC</td><td>TEMPERATURE INDICATING CONTROLLER</td></tr> <tr><td>FIT</td><td>FLOW INDICATOR TRANSMITTER</td><td>NC</td><td>NORMALLY CLOSED</td><td>TIT</td><td>TEMPERATURE INDICATING TRANSMITTER</td></tr> <tr><td>FM</td><td>FLOW METER</td><td>NO</td><td>NORMALLY OPEN</td><td>TS</td><td>TEMPERATURE SWITCH</td></tr> <tr><td>FS</td><td>FLOW INDICATOR SWITCH</td><td>C</td><td>COMMON</td><td>TSL</td><td>TEMPERATURE SAFETY LOW</td></tr> <tr><td>FSL</td><td>FLOW SAFETY LOW</td><td>S</td><td>SIGNAL</td><td>TSH</td><td>TEMPERATURE SAFETY HIGH</td></tr> <tr><td>FSH</td><td>FLOW SAFETY HIGH</td><td>PI</td><td>PRESSURE INDICATOR</td><td>WS</td><td>WATER SUPPLY</td></tr> <tr><td>IA</td><td>INSTRUMENT AIR</td><td>PC</td><td>PRESSURE CONTROLLER</td><td>TW</td><td>THERMO WELL</td></tr> <tr><td>IAS</td><td>INSTRUMENT AIR SYSTEM</td><td>PT</td><td>PRESSURE TRANSMITTER</td><td>TR</td><td>TRANSFORMER</td></tr> <tr><td>IS</td><td>INSTRUMENT GAS</td><td>PS</td><td>PRESSURE SWITCH</td><td>VE</td><td>MIST ELIMINATOR</td></tr> <tr><td>IGS</td><td>INSTRUMENT GAS SYSTEM</td><td>PSH</td><td>PRESSURE SAFETY HIGH</td><td>TT</td><td>TEMPERATURE TRANSMITTER</td></tr> <tr><td></td><td></td><td>PSL</td><td>PRESSURE SAFETY LOW</td><td>ELCV</td><td>ELEVATION</td></tr> </tbody> </table>	AI	ANALOG INPUT	LAL	LEVEL ALARM LOW	PSV	PRESSURE SAFETY VALVE	A/M	AUTO/MANUAL	LAH	LEVEL ALARM HIGH	PSIG	POUNDS PER SQUARE INCH GAUGE	AO	ANALOG OUTPUT	LIC	LEVEL INDICATING CONTROLLER	SDV	SHUT DOWN VALVE	AS	AIR SUPPLY	LI	LEVEL INDICATOR	SV	SOLENOID VALVE	BF	BLIND FLANGE	UIS	LEVEL INDICATING SWITCH	TC	TEMPERATURE CONTROLLER	BPV	BACK PRESSURE VALVE	UIT	LEVEL INDICATING TRANSMITTER	PDT	PRESSURE DIFFERENTIAL TRANSMITTER	DI	DIGITAL INPUT	LT	LEVEL TRANSMITTER	PDC	PRESSURE DIFFERENTIAL CONTROLLER	DO	DIGITAL OUTPUT	LC	LEVEL CONTROLLER	PDI	PRESSURE DIFFERENTIAL INDICATOR	EI	POSITION INDICATOR	LCH	LEVEL CONTROLLER HIGH	TI	TEMPERATURE INDICATOR	F	FLAME ARRESTOR	LCL	LEVEL CONTROLLER LOW	TCV	TEMPERATURE CONTROL VALVE	FC	FLOW CONTROLLER	LG	LEVEL GAUGE	LVV	LEVEL GAUGE VALVE	FI	FLOW INDICATOR	LS	LEVEL SWITCH	DDC	TEMPERATURE DIFFERENTIAL CONTROLLER	FCV	FLOW CONTROL VALVE	LSHH	LEVEL SAFETY HIGH HIGH	DDIC	TEMPERATURE DIFF INDICATOR CONTROLLER	FE	FLOW ELEMENT	LSH	LEVEL SAFETY HIGH	TE	TEMPERATURE ELEMENT	FI	FLOW INDICATOR CONTROLLER	LSL	LEVEL SAFETY LOW	TIC	TEMPERATURE INDICATING CONTROLLER	FIT	FLOW INDICATOR TRANSMITTER	NC	NORMALLY CLOSED	TIT	TEMPERATURE INDICATING TRANSMITTER	FM	FLOW METER	NO	NORMALLY OPEN	TS	TEMPERATURE SWITCH	FS	FLOW INDICATOR SWITCH	C	COMMON	TSL	TEMPERATURE SAFETY LOW	FSL	FLOW SAFETY LOW	S	SIGNAL	TSH	TEMPERATURE SAFETY HIGH	FSH	FLOW SAFETY HIGH	PI	PRESSURE INDICATOR	WS	WATER SUPPLY	IA	INSTRUMENT AIR	PC	PRESSURE CONTROLLER	TW	THERMO WELL	IAS	INSTRUMENT AIR SYSTEM	PT	PRESSURE TRANSMITTER	TR	TRANSFORMER	IS	INSTRUMENT GAS	PS	PRESSURE SWITCH	VE	MIST ELIMINATOR	IGS	INSTRUMENT GAS SYSTEM	PSH	PRESSURE SAFETY HIGH	TT	TEMPERATURE TRANSMITTER			PSL	PRESSURE SAFETY LOW	ELCV	ELEVATION																																																																																																																																																																		
AI	ANALOG INPUT	LAL	LEVEL ALARM LOW	PSV	PRESSURE SAFETY VALVE																																																																																																																																																																																																																																																																																																																					
A/M	AUTO/MANUAL	LAH	LEVEL ALARM HIGH	PSIG	POUNDS PER SQUARE INCH GAUGE																																																																																																																																																																																																																																																																																																																					
AO	ANALOG OUTPUT	LIC	LEVEL INDICATING CONTROLLER	SDV	SHUT DOWN VALVE																																																																																																																																																																																																																																																																																																																					
AS	AIR SUPPLY	LI	LEVEL INDICATOR	SV	SOLENOID VALVE																																																																																																																																																																																																																																																																																																																					
BF	BLIND FLANGE	UIS	LEVEL INDICATING SWITCH	TC	TEMPERATURE CONTROLLER																																																																																																																																																																																																																																																																																																																					
BPV	BACK PRESSURE VALVE	UIT	LEVEL INDICATING TRANSMITTER	PDT	PRESSURE DIFFERENTIAL TRANSMITTER																																																																																																																																																																																																																																																																																																																					
DI	DIGITAL INPUT	LT	LEVEL TRANSMITTER	PDC	PRESSURE DIFFERENTIAL CONTROLLER																																																																																																																																																																																																																																																																																																																					
DO	DIGITAL OUTPUT	LC	LEVEL CONTROLLER	PDI	PRESSURE DIFFERENTIAL INDICATOR																																																																																																																																																																																																																																																																																																																					
EI	POSITION INDICATOR	LCH	LEVEL CONTROLLER HIGH	TI	TEMPERATURE INDICATOR																																																																																																																																																																																																																																																																																																																					
F	FLAME ARRESTOR	LCL	LEVEL CONTROLLER LOW	TCV	TEMPERATURE CONTROL VALVE																																																																																																																																																																																																																																																																																																																					
FC	FLOW CONTROLLER	LG	LEVEL GAUGE	LVV	LEVEL GAUGE VALVE																																																																																																																																																																																																																																																																																																																					
FI	FLOW INDICATOR	LS	LEVEL SWITCH	DDC	TEMPERATURE DIFFERENTIAL CONTROLLER																																																																																																																																																																																																																																																																																																																					
FCV	FLOW CONTROL VALVE	LSHH	LEVEL SAFETY HIGH HIGH	DDIC	TEMPERATURE DIFF INDICATOR CONTROLLER																																																																																																																																																																																																																																																																																																																					
FE	FLOW ELEMENT	LSH	LEVEL SAFETY HIGH	TE	TEMPERATURE ELEMENT																																																																																																																																																																																																																																																																																																																					
FI	FLOW INDICATOR CONTROLLER	LSL	LEVEL SAFETY LOW	TIC	TEMPERATURE INDICATING CONTROLLER																																																																																																																																																																																																																																																																																																																					
FIT	FLOW INDICATOR TRANSMITTER	NC	NORMALLY CLOSED	TIT	TEMPERATURE INDICATING TRANSMITTER																																																																																																																																																																																																																																																																																																																					
FM	FLOW METER	NO	NORMALLY OPEN	TS	TEMPERATURE SWITCH																																																																																																																																																																																																																																																																																																																					
FS	FLOW INDICATOR SWITCH	C	COMMON	TSL	TEMPERATURE SAFETY LOW																																																																																																																																																																																																																																																																																																																					
FSL	FLOW SAFETY LOW	S	SIGNAL	TSH	TEMPERATURE SAFETY HIGH																																																																																																																																																																																																																																																																																																																					
FSH	FLOW SAFETY HIGH	PI	PRESSURE INDICATOR	WS	WATER SUPPLY																																																																																																																																																																																																																																																																																																																					
IA	INSTRUMENT AIR	PC	PRESSURE CONTROLLER	TW	THERMO WELL																																																																																																																																																																																																																																																																																																																					
IAS	INSTRUMENT AIR SYSTEM	PT	PRESSURE TRANSMITTER	TR	TRANSFORMER																																																																																																																																																																																																																																																																																																																					
IS	INSTRUMENT GAS	PS	PRESSURE SWITCH	VE	MIST ELIMINATOR																																																																																																																																																																																																																																																																																																																					
IGS	INSTRUMENT GAS SYSTEM	PSH	PRESSURE SAFETY HIGH	TT	TEMPERATURE TRANSMITTER																																																																																																																																																																																																																																																																																																																					
		PSL	PRESSURE SAFETY LOW	ELCV	ELEVATION																																																																																																																																																																																																																																																																																																																					
<p>NOTE: - 1. CONSULT PIPE SPEC FOR PRESSURE RATINGS</p>	<p>THIS DRAWING AND THE INFORMATION HEREIN IS CONFIDENTIAL AND MUST NOT BE REPRODUCED OR USED IN ANY WAY WITHOUT THE WRITTEN PERMISSION OF SPIRAL X LLC</p>	<p>DATE: 2/11/2018</p> <p>REV: A</p> <p>DESCRIPTION: FIRST ISSUE</p>	<p style="text-align: center;">SpiralX</p> <p style="text-align: center;">LEGEND SHEET PIPING AND INSTRUMENTATION DIAGRAM SPIRALX LLC, 2016 GARLAND, TEXAS</p> <p>DRAWN BY: RD 12/11/2018 SCALE: N/A REV: A</p> <p>CHECKED BY: KAK</p> <p>ENGINEERING APPR: MDD NO. LEGEND PAGE</p> <p>PROJECT NO: ****</p>																																																																																																																																																																																																																																																																																																																							



VALVE TAG	PART NUMBER	DESCRIPTION
XP-2100	IGN1145	IGNITION COIL
PC-100	PNC1022	PRESSURE CONTROLLER
PI-100	PNC1022	PRESSURE INDICATOR
PC-101	PNC1022	PRESSURE CONTROLLER
PI-101	PNC1022	PRESSURE INDICATOR
XV100	IGN1145	TWO-WAY SOLENOID VALVE
XV101	IGN1145	THREE-WAY SOLENOID VALVE

P&ID for 30" combustor shown. 48" combustor will be similar.

THIS DRAWING AND THE INFORMATION
 HEREIN IS CONFIDENTIAL AND MUST NOT
 BE REPRODUCED OR USED IN ANY WAY
 WITHOUT THE WRITTEN PERMISSION OF
 SPIRAL X LLC

NOTES:
 1.) VENT TO SAFE LOCATION
 2.) WHEN AT REST (0 PSI), C TO NO IS OPEN, NC IS CLOSED
 3.) WHEN PRESSURIZED, C TO NC IS OPEN, NO IS CLOSED

COPYRIGHT 2019 SPIRALX LLC.



PIPING AND INSTRUMENTATION DIAGRAM
 SPIRALX LLC, 2016
 GARLAND, TEXAS

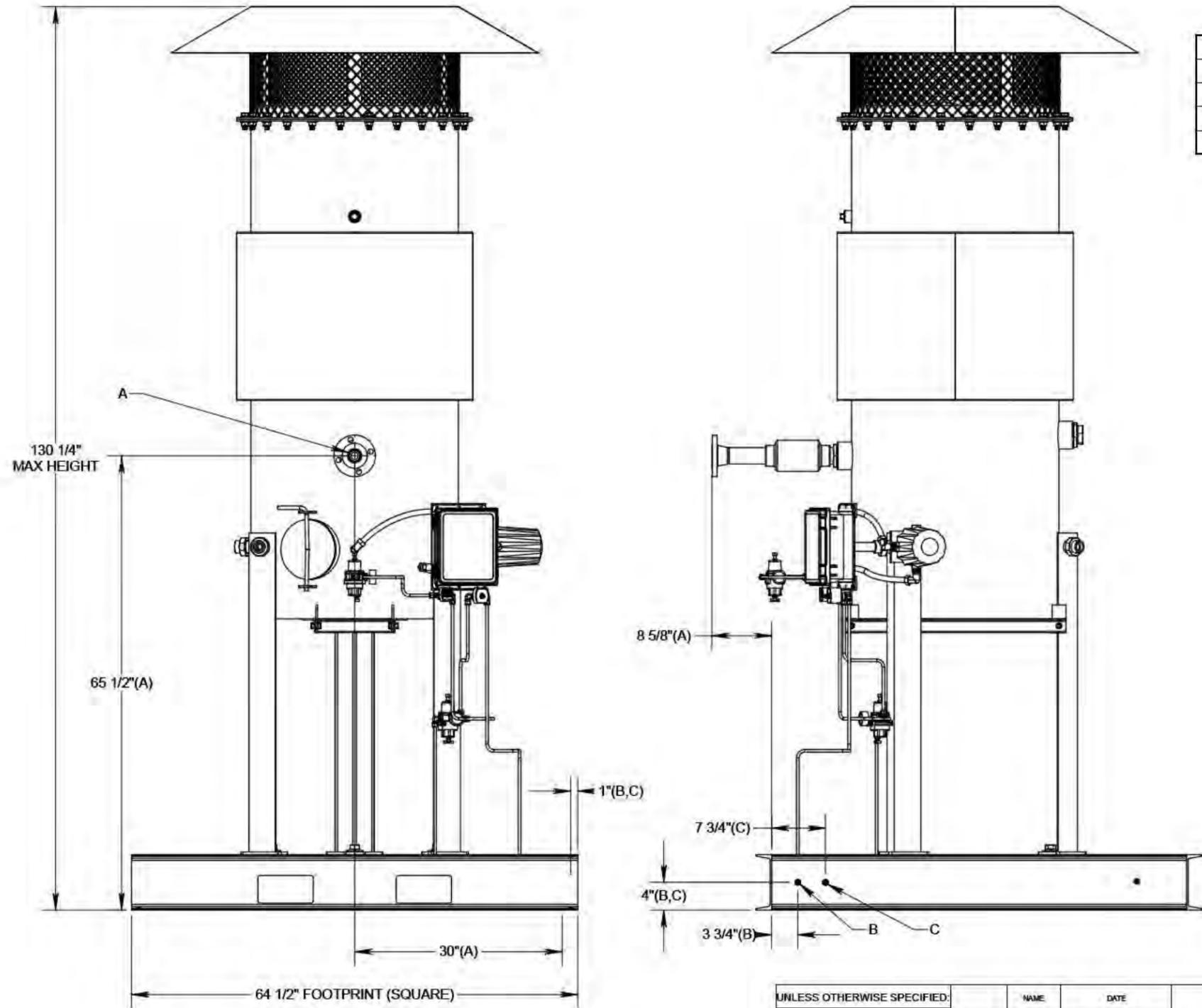
DATE	REV.	DESCRIPTION	DRAWN BY:	RD	2/14/2019	SCALE:	N/A	REV.
2/14/2019	A	FIRST ISSUE	CHECKED BY:	KAK				
			ENGINEERING APPR:	MDD				
			PROJECT NO.:	****				

NO. SK300PFC

A

5.2 | General Arrangement of Unit
 For standalone skid. 30" (with rain cap, no leg or body extension) and 48" (no rain cap, leg or body extension).

END CONNECTIONS				
LABEL	SIZE	TYPE	DESCRIPTION	PRESSURE
A	2"	CL150RF	BTEX INLET	NA
B	3/8"	TUBE FITTING	PILOT SIGNAL	NA
C	3/8"	TUBE FITTING	FUEL GAS	120 PSIG



UNLESS OTHERWISE SPECIFIED:
 DIMENSIONS ARE IN INCHES
 TOLERANCES:
 FRACTIONAL: ±1/16
 ANGULAR: ±1°
 TWO PLACE DECIMAL: ±0.05
 THREE PLACE DECIMAL: ±0.005
 ENCLOSURE: ±3/16
 DEBUR ALL SHARP EDGES
 DO NOT SCALE DRAWING

	NAME	DATE
DRAWN	RD	3/1/2019
CHECKED	KAK	3/5/2019
ENG APPR	MDJ	DATE
Q.C. SIGN		
C.J. SIGN		

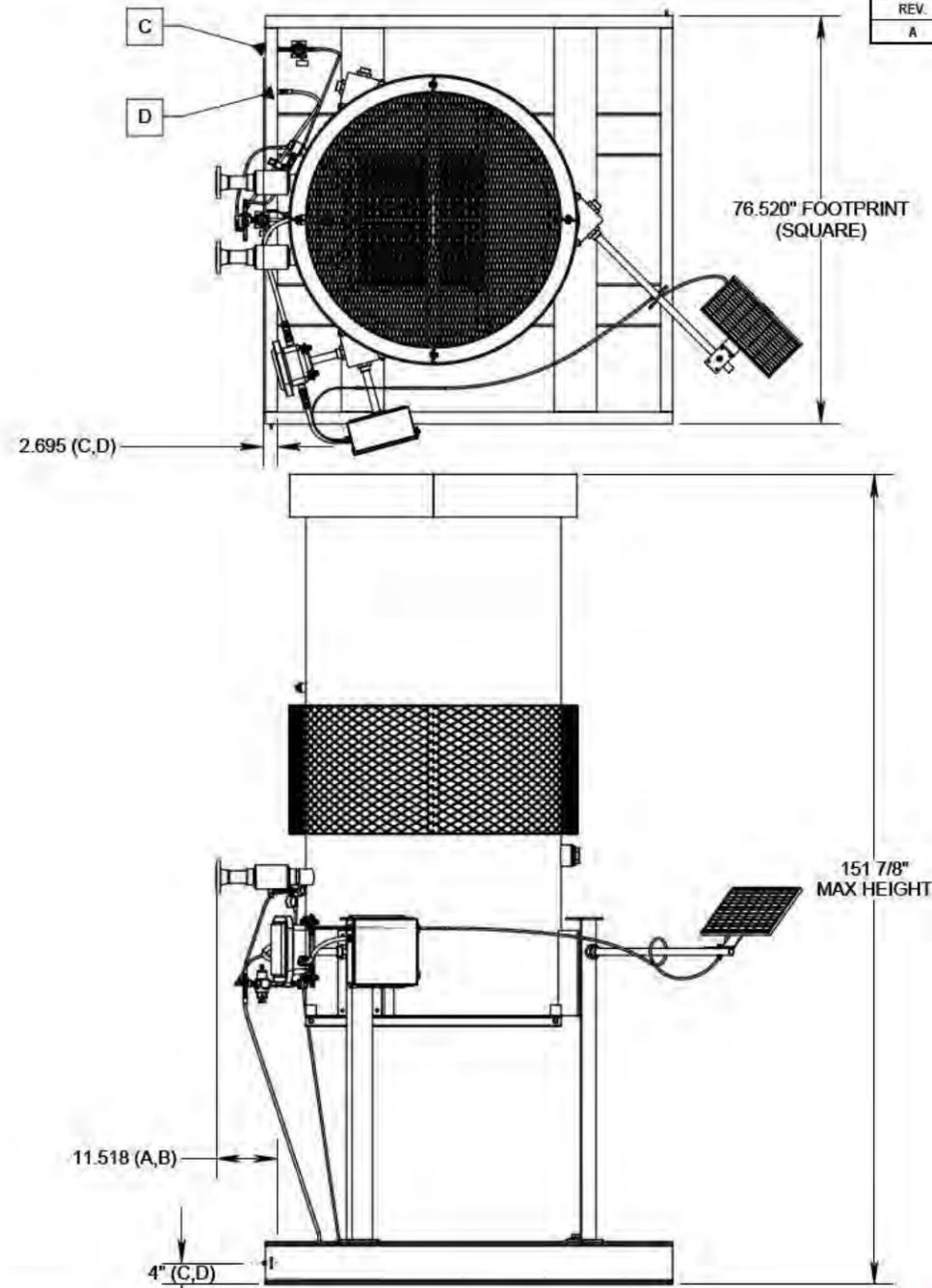
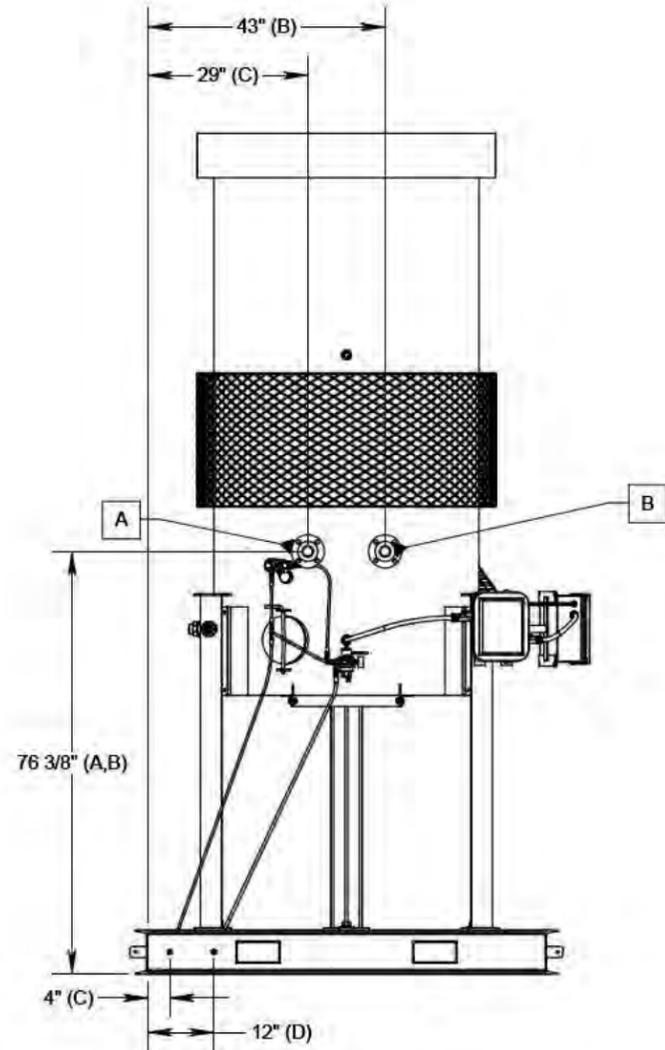


WWW.SPIRALX.LLC.COM
 INFO@SPIRALX.LLC.COM
 1-888-47V-TUBE
 SPIRALX, LLC
 3532 MILLER PARK DR
 GARLAND, TX - 75042

TITLE 30" COMBUSTOR SKID W/ PROFIRE GA			
SIZE B	JOB ID. N/A	DRAWING NO. SK300PFC	REVISION A
SCALE 1:48	MATERIAL	SHEET 1 OF 1	
THIS DRAWING AND THE INFORMATION HEREIN IS CONFIDENTIAL, AND MUST NOT BE REPRODUCED OR USED IN ANY WAY WITHOUT THE WRITTEN PERMISSION OF SPIRALX, LLC.			

CONNECTIONS				
LABEL	SIZE	TYPE	DESCRIPTION	PRESSURE
A	2"	CL150RF	BTEX INLET	N/A
B	2"	CL150RF	BTEX INLET	N/A
C	1/4"	TUBE FITTING	FUEL GAS	N/A
D	3/8"	TUBE FITTING	FLAME OUT SIGNAL	10-250 PSI

REVISIONS			
REV.	DESCRIPTION	DATE	APPROVED
A	FIRST ISSUE	3/4/2019	MDD



PROPRIETARY AND CONFIDENTIAL
 THE INFORMATION CONTAINED IN THIS
 DRAWING IS THE SOLE PROPERTY OF
 SPIRALX, LLC. ANY REPRODUCTION IN
 PART OR AS A WHOLE WITHOUT THE
 WRITTEN PERMISSION OF SPIRALX, LLC
 IS PROHIBITED.

UNLESS OTHERWISE SPECIFIED:
 DIMENSIONS ARE IN INCHES
 TOLERANCES:
 FRACTIONAL: ±1/16
 ANGULAR: ±1°
 TWO PLACE DECIMAL: ±.05
 THREE PLACE DECIMAL: ±.005
 ENCLOSURE: ±3/16
 DEBUR ALL SHARP EDGES
 DO NOT SCALE DRAWING

	NAME	DATE
DRAWN	KAK	3/4/2019
CHECKED	RD	DATE
ENG APPR	MDD	DATE
Q.C. SIGN		
C.I. SIGN		



WWW.SPIRALX.LLC.COM
 INFO@SPIRALX.LLC.COM
 1-288-6INTUBE
 SPIRALX LLC
 3532 MILLER PARK DR
 GARLAND, TX - 75042

TITLE 48" COMBUSTOR SKID GA			
SIZE B	JOB I.D. N/A	DRAWING NO. 48600	REVISION A
SCALE 1:28	MATERIAL	SHEET	1 OF 1

THIS DRAWING AND THE INFORMATION HEREIN IS CONFIDENTIAL, AND MUST NOT BE
 REPRODUCED OR USED IN ANY WAY WITHOUT THE WRITTEN PERMISSION OF SPIRALX, LLC



October 2000
RG-109 (Draft)

Air Permit Technical Guidance
for Chemical Sources:

Flares and Vapor Oxidizers

printed on
recycled paper

Air Permits Division

TEXAS NATURAL RESOURCE CONSERVATION COMMISSION

Waste Stream	Destruction/Removal Efficiency (DRE)												
VOC	98 percent (generic) 99 percent for compounds containing no more than 3 carbons that contain no elements other than carbon and hydrogen in addition to the following compounds: methanol, ethanol, propanol, ethylene oxide and propylene oxide												
H ₂ S	98 percent												
NH ₃	case by case												
CO	case by case												
Air Contaminants	Emission Factors												
thermal NO _x	<table> <tr> <td>steam-assist:</td> <td>high Btu</td> <td>0.0485 lb/MMBtu</td> </tr> <tr> <td></td> <td>low Btu</td> <td>0.068 lb/MMBtu</td> </tr> <tr> <td>other:</td> <td>high Btu</td> <td>0.138 lb/MMBtu</td> </tr> <tr> <td></td> <td>low Btu</td> <td>0.0641 lb/MMBtu</td> </tr> </table>	steam-assist:	high Btu	0.0485 lb/MMBtu		low Btu	0.068 lb/MMBtu	other:	high Btu	0.138 lb/MMBtu		low Btu	0.0641 lb/MMBtu
steam-assist:	high Btu	0.0485 lb/MMBtu											
	low Btu	0.068 lb/MMBtu											
other:	high Btu	0.138 lb/MMBtu											
	low Btu	0.0641 lb/MMBtu											
fuel NO _x	NO _x is 0.5 wt percent of inlet NH ₃ , other fuels case by case												
CO	<table> <tr> <td>steam-assist:</td> <td>high Btu</td> <td>0.3503 lb/MMBtu</td> </tr> <tr> <td></td> <td>low Btu</td> <td>0.3465 lb/MMBtu</td> </tr> <tr> <td>other:</td> <td>high Btu</td> <td>0.2755 lb/MMBtu</td> </tr> <tr> <td></td> <td>low Btu</td> <td>0.5496 lb/MMBtu</td> </tr> </table>	steam-assist:	high Btu	0.3503 lb/MMBtu		low Btu	0.3465 lb/MMBtu	other:	high Btu	0.2755 lb/MMBtu		low Btu	0.5496 lb/MMBtu
steam-assist:	high Btu	0.3503 lb/MMBtu											
	low Btu	0.3465 lb/MMBtu											
other:	high Btu	0.2755 lb/MMBtu											
	low Btu	0.5496 lb/MMBtu											
PM	none, required to be smokeless												
SO ₂	100 percent S in fuel to SO ₂												

*The only exception of this is if inorganics might be emitted from the flare. In the case of landfills, the AP-42 PM factor may be used. In other cases, the emissions should be based on the composition of the waste stream routed to the flare.



- Burners
- Flares
- Incinerators
- Combustion Rentals
- Aftermarket Products and Services

22151 East 91st Street
Broken Arrow, OK 74014 USA
Ph: +1-918-258-8551
Fx: +1-918-251-5519

www.zeeco.com
sales@zeeco.com

April 13, 2016

Enterprise Products
1100 Louisiana St
Houston, TX 77002

Attention: Jing Li

RE: South Carlsbad Flare
Zeeco Ref.: 2016-00271RE-01 Rev 1

Dear Mr. Li,

The hydrocarbon destruction efficiency for the UF-24-38 Flare system proposed in quote number 2016-00271RE-01 Rev 1 will be 99% or higher for C1-C3 compounds and 98% or higher for all other compounds given as long as the flare is operated and maintained within the design operating parameters and accepted industry standard practices for this type of equipment.

Sincerely,

Andrew Grider
Applications Engineer
Zeeco Combustion Rental & Rapid Response Group



Zeeco, Inc.
 22151 E. 91st St.
 Broken Arrow, Oklahoma 74014
 Phone: (918) 258-8551 Fax: (918) 251-5519

DELIVER TO: Jenessa Duncan

DATE: February 10, 2016

COMPANY: Enterprise Products

SENDERS NAME: Andrew Grider / Andrew_Grider@zeeco.com

PHONE: (918) 893-8448

YOUR REFERENCE: Budgetary Low BTU Flare Quote

QUOTE #: 2016-00271RE-01 Rev 1

Design Information (Estimated):

	<u>Design - Upset Condition 1</u>	<u>Fuel Gas- Normal</u>	<u>Fuel Gas- High BTU</u>	<u>Fuel Gas- Low BTU</u>	<u>Design + Fuel Gas Low BTU</u>
Gas MW (lb/mol)	33.27	19.42	20.58	18.76	30.40
Gas LHV (Btu/Scf)	6	1,033	1,086	986	200
Flow Rate (MScfd)	7,690*	1,793*	1,685*	1,901*	9,591*
Available Pressure (psig)	6.97	>6.97	>6.97	>6.97	6.97

Scope of Supply:

1. (1) 38' OAH guy supported flare stack
2. (1) Utility (UF) flare tip w/ Integral Purge Reducing Velocity Seal
3. (1) Shepherd Ring
4. (1) Low Btu Windshield
5. (3) HSLF-Z-HEI Electric Ignition Pilot assembly with Retractable HEI & Type K Thermocouple
6. (1) Nema 4, Skid Mounted Pilot Ignition and Monitoring Panel
7. (1) *Optional Manual Knock Out Drum*

Required Utilities:

Pilot Fuel Gas: 65 Scfh Natural Gas at 15 Psig OR 25 Scfh Propane at 7 psig (per pilot)

Electricity: 120V / 1 Phase / 60 Hz

Shepherd Ring: 3.016 MMBtu/hr

*Enrichment Gas: Flow rates for the 3 different fuel gas compositions are listed in the design information above. For the fuel gas that is being used, the specified flow rate is to be added to the gas being flared as far as possible upstream in the header in order to enrich the combined stream to a minimum required heating value of 200 Btu/SCF

Purge Gas: 435 Scfh of a gas that does not contain oxygen and will not go to its dew point at jobsite conditions

Equipment Description:

- Skid Mounted Guy Supported Flare Stack: The stack is mounted on a carbon steel skid that eliminates the need for a concrete foundation. The skid only needs to be set on firm, flat soil and anchored with the provided guy wires and screw anchors. Design wind speed for this type of installation is 90 mph.
- UF Flare Tip: The UF style flare tip provides high stability flaring while also ensuring reliability of the flame from purge all the way to max flow rates. Components located in the high heat zone will be made of 310SS or equivalent casting material. The flare tip will provide a VOC destruction efficiency of at least 98 wt%. An integral purge reducing velocity seal is also included to reduce the quantity of purge gas to prevent oxygen ingress through the flare tip at low rates.
- Shepherd Ring: A major key to obtaining high destruction efficiency with low Btu gases is to have a consistent ignition source circumferentially around the flare tip to ignite gases exiting the tip. High Btu flares usually have 3 pilots equally spaced around the tip and this is more than adequate. However, with low Btu flares three pilots are insufficient. This is a special concern with flares that are being enriched upstream. Not only do three pilots not provide the coverage required to ensure a cross sectional light off of flames across the tip. But with enriched gases, there is further danger of inadequate mixing of the gases and enrichment gas which can result in pilots being located in areas that do not have sufficient heating value to ignite. Addition of a Shepherd Ring to the flare tip has the same effect as adding an infinite number of pilots. The ring completely surrounds the exit of the tip and is drilled with burner ports that establish a “ring of fire” around the flare tip. The ring itself is lit with pilots but once the Shepherd Ring’s fire has been established, it becomes the primary ignition source for the gases.
- Low BTU Windshield: Since gases have to be burned at very low velocities to ensure stable flames and meet national and state guidelines, the resultant flames are extremely vulnerable to atmospheric wind conditions. Even with only light to moderate wind conditions, flames can become unstable or be blown out. Addition of a Low Btu Windshield reduces the impact of wind on the flames. The addition of the low Btu windshield also helps capture a portion of the heat emitted as the gases are burned. This heat in turn helps produce higher destruction efficiencies by increasing the heat present at the tip exit which in turn promotes more consistent ignition of the gases.
- HSLF-HEI Ignition Pilot: The pilot is proven to stay lit in hurricane force weather conditions. Testing has shown that a stable flame is present even in wind speeds greater than 150 mph in addition to rainfall of over 10 inches per hour. The pilot will be equipped with a Type K thermocouple for continuous monitoring of the pilot status. The pilot also meets API 537 design requirements.
- Retractable Pilot Components: For ease of service, instead of retracting the entire pilot, only the components that need service are made retractable. This ensures that the location of the pilot with relation to the flare tip is maintained, ensuring proper ignition every time. The ignition probe and thermocouple are the only components that can need maintenance. Both components will be retractable so that maintenance can be performed without needing a shutdown of the flare or any special equipment.
- Automatic Ignition/Monitoring Panel: The automatic pilot ignition and monitoring panel will continuously monitor the pilot and attempt to relight if a pilot failure signal is received. The control panel (Nema 4 enclosure) will also be skid mounted.
- Knock Out (KO) Drum - For areas where liquid entrainment is possible in the flare header, we can offer a separate KO drum. The knock out drum will separate any liquids that condense as the flare gas moves through the header. The KO drum vessel comes complete with level gage and manual drain line. As an option, the drum can also be equipped with automatic liquid level monitoring, alarming and draining capabilities.

COMMERCIAL

BUDGETARY PURCHASE PRICING (+/- 15%):

Unit

Guy-Supported 38' Tall Flare as Detailed (UF-24-38) \$100,000

OPTIONAL EQUIPMENT BUDGETARY PURCHASE PRICING (+/- 15%)

4' dia x 8' length Manual KOD \$30,000

Freight: Prepaid and added to our invoice at cost + 15%

Shipping: Ex-works (Point of Manufacture) per Incoterms 2010

Schedule: The flare equipment offered can be readied for shipment within 6-8 weeks ARO.
Please contact Zeeco if your project requires a faster delivery.

Storage: Zeeco will provide space for storage of each unit up to 2 months after notification of readiness to ship free of charge. If you require storage periods longer than 2 months, a fee of 1% of the equipment value will be charged per month until the equipment is moved off site.

Warranty: Length; 18 months from date of shipment or 12 months after startup, whichever condition occurs first. Refer to Zeeco terms and conditions of sale for further clarifications.

Pricing Validity: Pricing quoted is valid for 30 days.

Payment Schedule: Net 60 – 25% Upon Order Placement
75% Upon Notification of Readiness to Ship

Terms and Conditions: This proposal is contingent upon acceptance of Zeeco, Inc Standard Terms and Conditions of Sale (attached).



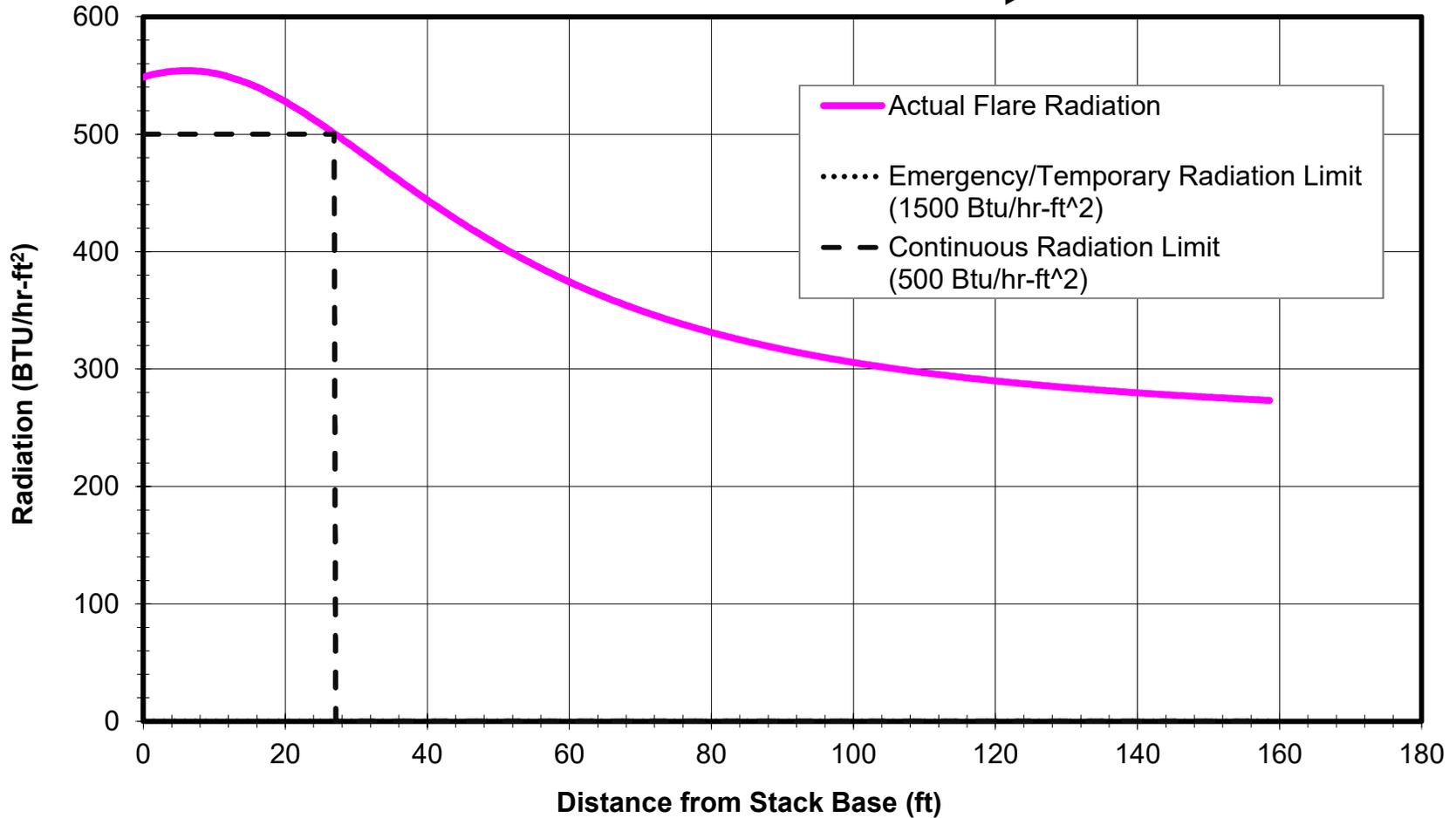
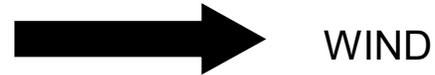
Zeeco Quotation Ref: 2016-00271RE-01 Rev. 0
Radiation At Grade Versus Distance From Stack Base

Stack Height = 38 ft ; Relative Humidity = 85%

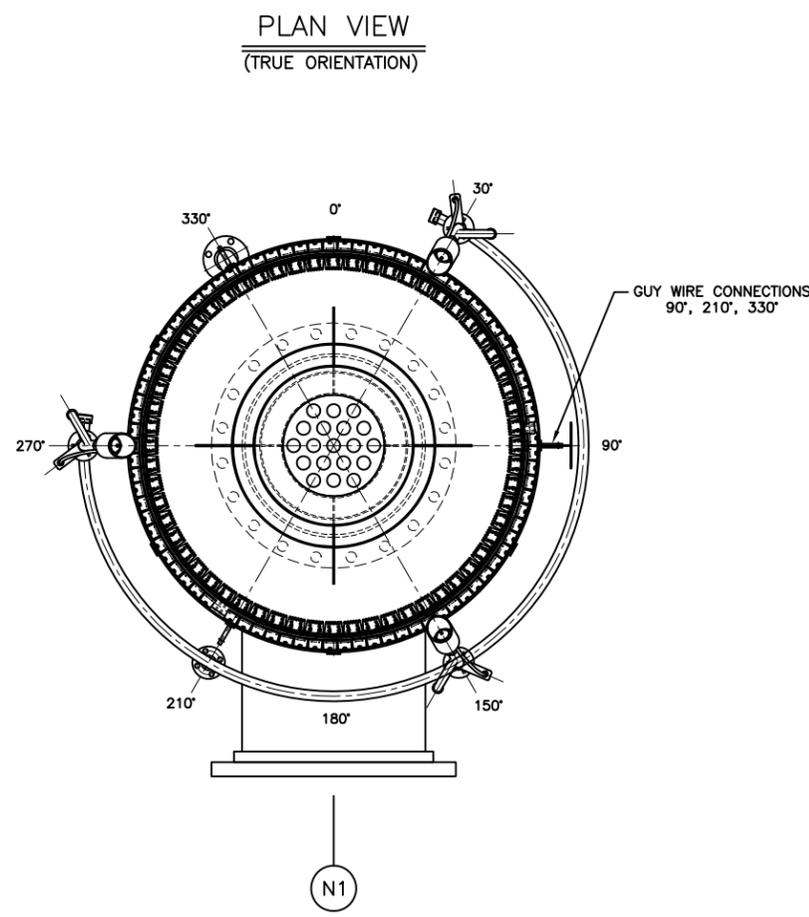
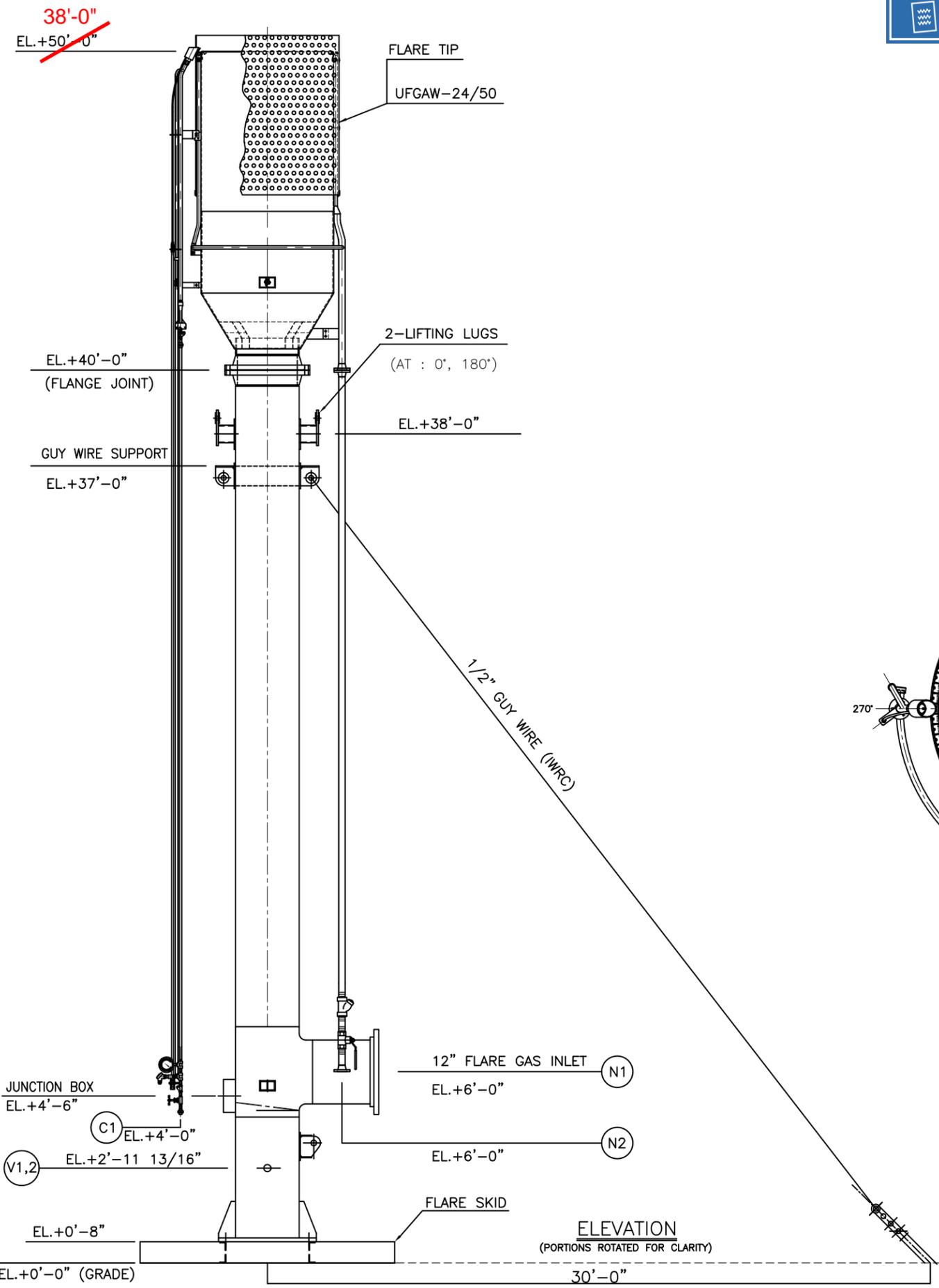
Solar Radiation Included = 250 BTU/hr-ft² ; Wind Speed = 30 ft/s

Flare Tag No. = F-1 ; Operating Case = Upset Condition 1 + Fuel Gas Low BTU (9591 MSCFD)

Max Radiation = 554 BTU/hr-ft² @ 6 ft From Stack Base



DRAFT



MATERIAL SPECIFICATIONS				DESIGN DATA	
STACK RISER	A106-B	FLARE SKID	A36	TYPE	GUY WIRE SUPPORT TYPE
SKIRT	A106-B			DESIGN CODE	ASME STS-1
FLARE TIP	SEE FLARE TIP			WIND LOAD	ASCE 7-05
FLANGE	A105			SEISMIC LOAD	-
STUD BOLT/NUT	A193-B7/A194-2H			FLUID	FLARE GAS
GASKET	C4401			DESIGN PRESS.	N/A psig
BASE BLOCK	A36			DESIGN TEMP.	0° ~ 350° °F
SETTING BOLT	A307-B			M.A.W.P.(NEW & COLD)	- psig
EARTH LUG	304 S.S			OPERATING PRESS.	- psig
NAME PLATE	304 S.S			OPERATING TEMP.	- °F
LIFTING LUG	A36			HYDRO'C TEST PRESS.	- psig
TAILING LUG	-			PNEUM'C TEST PRESS.	- psig
GUY WIRE LUG	A36			P.W.H.T.	(NO)
GUY WIRE	IWRG			RADIOGRAPH	AS PER ITP, (SPOT)
UTILITY LINE	A106-B			JOINT EFFICIENCY	85 %
CONDUIT LINE	C.S (GALV.)			CORROSION ALLOWANCE	N/A
				PAINTING	SEE NOTE 6

NOZZLE AND CONNECTIONS									
MARK	Q'TY	SIZE	SCH.	RATING	FACING	SERVICE	REMARKS	° TO FACE	PIPING SPEC.
N1	1	12"	STD.	ASME #150	WN, RF	FLARE GAS INLET		SEE DWG.	
N2	1	2"	STD.	ASME #150	WN, RF	ASSIST GAS INLET	ORIEN.: 180°	SEE DWG.	
V1,2	2	4"	40	-	-	VENT		SEE DWG.	
C1	1	1"	40	ASME #150	SW, RF	PILOT GAS		SEE DWG.	

- NOTE**
- PILOT MIXER ORIFICE DRILLED: 3/64" DIA
 - PILOT GAS CONSUMPTION: 65 SCFH @ 15 PSIG PER PILOT
 - PILOT ORIFICE DRILLING BASED ON 1000 BTU/SCF (LHV) GAS WITH 0.6 SP. GR.
 - THE FLARE TIP REQUIRES A MINIMUM CONTINUOUS PURGE RATE OF 45 SCFH OF A GAS THAT WILL NOT GO TO DEW POINT AT OPERATING TEMPERATURES TO ENSURE AIR DOES NOT MIGRATE DOWN THE FLARE STACK. IT SHOULD BE NOTED THAT DEPENDING UPON THE TURNDOWN OPERATION OF THE FAN AND THE TYPE OF PURGE GAS USED IT MAY BE NECESSARY TO INCREASE THIS MINIMUM PURGE RATE TO ENSURE PROPER COMBUSTION OF THE PURGE GAS DURING IDLE OPERATION.
 - ALL FLANGE BOLTING TO STRADDLE NORMAL CENTERLINES.
 - ALL EXTERNAL CARBON STEEL SURFACES TO BE PREPARED PER SSPC-SP6. PRIME WITH ONE COAT INORGANIC ZINC (2 1/2 MILS DFT MIN.) PAINT ONE COAT HIGH TEMP ALUMINUM (1 MIL DFT MIN.)
 - THE PILOT THERMOCOUPLE IS FOR ON/OFF INDICATION ONLY, NOT FOR ACCURATE PILOT FLAME MEASUREMENT.
 - FLAME ARRESTOR (IF APPLICABLE) SHALL BE MOUNTED DIRECTLY TO GAS INLET NOZZLE - NO PIPING ALLOWED BETWEEN FLAME ARRESTOR AND FLARE GAS INLET NOZZLE.

Page 5 of 10

NO.	DATE	REVISION DESCRIPTION	BY	CHK.	APP.
1	10OCT15	REVISED PER AS BUILT	JTO	CJM	JTO

ZEECO, INC.
22151 EAST 91st STREET
BROKEN ARROW, OK 74014
PHONE: (918) 258-8551
FAX: (918) 251-5519
www.zeeco.com
sales@zeeco.com

PROPRIETARY DATA IS INCLUDED IN THE INFORMATION DISCLOSED HEREIN AND IS THE PROPERTY OF ZEECO, INC. THIS INFORMATION IS SUBMITTED IN CONFIDENCE AND MUST BE USED IN CONNECTION WITH BIDDING DONE FOR ZEECO, INC. AND ALL RIGHTS OF DESIGN OR INVENTION ARE RESERVED. UNAUTHORIZED DISCLOSURE OR USE IS PROHIBITED BY LAW.

DRAWN SK DATE 01SEP15
CHK MN APP JO
SCALE NTS REV 1
DRAWING NUMBER SD-3224
SHT. 1 OF 2

THE SALE OF EQUIPMENT, PARTS, MATERIALS, SUPPLIES, SOFTWARE AND OTHER GOODS (THE “GOODS”) OR SERVICES (THE “SERVICES”), AS DESCRIBED IN SELLER’S QUOTATION OR PROPOSAL (THE “PROPOSAL”), ARE EXPRESSLY CONDITIONED UPON BUYER’S AGREEMENT TO THESE TERMS & CONDITIONS. ANY ADDITIONAL OR DIFFERENT TERMS PROPOSED BY BUYER ARE EXPRESSLY OBJECTED TO AND WILL NOT BE BINDING UPON SELLER UNLESS AGREED TO IN WRITING BY SELLER. ANY PURCHASE ORDER (THE “ORDER”) ISSUED BY BUYER FOR THE PURCHASE OF GOODS OR SERVICES SHALL CONSTITUTE BUYER’S AGREEMENT TO THESE TERMS & CONDITIONS. UNLESS OTHERWISE SPECIFIED IN THE PROPOSAL OR THE ORDER, ANY PROPOSAL BY SELLER SHALL EXPIRE THIRTY (30) DAYS FROM ITS DATE AND MAY BE MODIFIED OR WITHDRAWN BY SELLER BEFORE RECEIPT OF BUYER’S ACCEPTANCE. THE GOODS AND SERVICES ARE COLLECTIVELY REFERRED TO AS THE “WORK.” UNLESS OTHERWISE STATED, THE SELLER SHALL BE ZEECO, INC., 22151 EAST 91ST STREET, BROKEN ARROW, OKLAHOMA 74014 (USA), AND THE BUYER SHALL BE THE PARTY IDENTIFIED AS SUCH ON THE ORDER.

1. PRICE: Unless otherwise stated in the Proposal, the price of the Order (the “Price”) is fixed and firm and is exclusive of all taxes, duties, fees, charges or assessments of any nature levied by any governmental authority. Additionally, unless otherwise stated in the Proposal, the Price is contingent upon the use of sub-contractors and sub-suppliers listed on Seller’s Approved Manufacturers List (“AML”) as may be amended from time-to-time, and the manufacture of Goods pursuant to Seller’s standard painting procedures. Payment terms shall be as stated in the Proposal and Seller’s acceptance of the Order is subject to credit approval that may include payment by means of an irrevocable documentary letter of credit issued by a first-class U.S. bank acceptable to Seller with funds payable upon delivery of customary presentation documents. The form of the letter of credit shall be negotiated by the parties and submitted to Seller for approval prior to issuance. All costs and fees of the letter of credit shall be to Buyer’s account. Seller shall not be required to obtain any form of payment or performance security in favor of the Buyer, including but not limited to, bank guarantees, standby letters of credit, or surety bonds. Buyer’s breach of agreed payment terms may result in: (a) Seller’s suspension of the Work; (b) Seller’s termination of the Order due to Buyer’s default; (c) Buyer’s liability for Seller’s mobilization and demobilization costs in the event of suspension or termination by Seller, in addition to other damages; (d) Seller’s demand for further assurances of performance by Buyer which may include, without limitation: (i) alteration of payment terms or milestones; (ii) full payment prior to shipment; (iii) additional payment security; (iv) a delay in shipment that may exceed the length of Buyer’s delay in payment.

2. CHANGES: Order changes by Buyer may significantly and disproportionately affect both the Price and completion or delivery date(s) (the “Delivery Schedule”). If Buyer desires to make a modification to the quantity, place, Delivery Schedule, or method of delivery, or the drawings, designs, or specifications of the Work (a “Change”), then Buyer shall so notify Seller in writing and provide sufficient details and descriptions of the proposed Change so that Seller may evaluate the impact of the Change on the Price, Delivery Schedule, or both. Under no circumstances shall Seller be obligated to perform a Change without an agreement concerning modifications to the Price, Delivery Schedule, or both.

3. DELAYS BY BUYER: If Buyer delays delivery for any reason, including but not limited to technical modifications or Changes, suspension, failure to review drawings submitted by Seller within the time specified, or any other cause (whether or not within Buyer’s control), such delays may significantly and disproportionately affect both the Price and Delivery Schedule, which shall then be subject to a reasonable adjustment. The impact of Buyer caused delays on the Delivery Schedule may, in some cases, be more significant or of a longer duration than the actual period of Buyer’s delay. In the event of Buyer’s delay for any reason Seller shall be entitled to invoice Buyer, and Buyer agrees to pay timely, for materials on hand, fabrication completed or in process, and services provided. Unless specified in the Order, or otherwise by written agreement, where the Order requires submission of certain documents (including but not limited to drawings, manuals, or other documents related to the Goods) by Seller to Buyer for approval, then Buyer shall respond to such submission with approval or rejection within fourteen (14) days after Seller’s issuance of such document(s) to Buyer. The failure of Buyer to approve or reject the document(s) by such time shall result in the document(s) being deemed approved and accepted.

4. LIMITED WARRANTY FOR GOODS: Seller warrants the Goods will operate substantially in conformance with Seller’s specifications stated the

Proposal and will be free from defects in material and workmanship for a period of twelve (12) months from the date of initial operation, or eighteen (18) months from the date of shipment, whichever is earlier (the “Warranty Period”) when subjected to normal, proper and intended usage by properly trained personnel. Seller agrees during the Warranty Period, to repair or replace, at Seller’s option, defective Goods so as to cause the Goods to operate in substantial conformance with Seller’s specifications; provided that Buyer shall: (a) promptly notify Seller in writing upon the discovery of any defect and specify details of the warranty claim; (b) provide Seller with all operating data that Seller may reasonably request in order for Seller to evaluate the warranty claim; and (c) after Seller’s review of the warranty claim, return the defective Goods to Seller with costs prepaid by Buyer if required to do so by Seller. Replacement parts may be new or refurbished. Shipment to Buyer of repaired or replaced Goods shall be in accordance with the delivery terms of the Order. Notwithstanding any other provision of this warranty, Seller may at its option, elect to send a service technician to Buyer’s site to inspect, repair or replace (if applicable) warranted Goods, or otherwise to determine whether the Goods should be returned to Seller for repair or replacement. Goods or components thereof that are obtained by Seller from an original manufacturer or third party supplier are not warranted by Seller, but Seller will, to the extent possible, assign to Buyer any warranty rights in such Goods or components that Seller received from the original manufacturer or third party supplier. Consumables such as, but not limited to, bulbs, fuses, thermocouples, gaskets, and similar items are outside the scope of this warranty. Seller’s warranty assumes the Goods are “at grade,” and all responsibility for and costs of removal and/or reinstallation of warranted parts or Goods as well as the cost of and responsibility for gaining access to the warranted parts or Goods, are excluded from this warranty. If the Goods are not placed into service within six (6) months after shipment, in order to validate the warranty, the Goods shall be inspected by Seller at the time of commissioning and refurbished, if necessary, to like new condition at the Buyer’s expense. For any extended time of storage at the jobsite without assembly/installation, the Goods shall be stored and protected in accordance with Seller’s instructions and industry standard long-term storage methods. This warranty shall be void if the Goods have been: (w) exposed to corrosion, erosion, or chemical attack; (x) operated contrary to Seller’s instructions or accepted industry practices; (y) improperly maintained or operated, or subjected to accident, abuse, or vandalism; or (z) operated in conditions other than those stated in Buyer’s written specifications. Additionally, this warranty shall be void if the Buyer is not in compliance with its payment obligations to Seller pursuant to the Order. Seller shall have no obligation to make repairs, replacements or corrections resulting from normal wear and tear to the Goods. If Seller determines that a warranty claim is not valid, then Buyer shall pay or reimburse Seller for all costs of investigating and responding to such claim, including non-warranty parts sold or installed, at Seller’s then prevailing daily service rates and materials rates. ANY INSTALLATION, MAINTENANCE, REPAIR, SERVICE, RELOCATION OR ALTERATION OR OTHER TAMPING WITH THE GOODS, THAT IS PERFORMED BY ANY PERSON OR ENTITY OTHER THAN SELLER WITHOUT SELLER’S PRIOR WRITTEN APPROVAL, OR ANY USE OF REPLACEMENT PARTS NOT SUPPLIED BY SELLER, SHALL IMMEDIATELY VOID AND CANCEL ALL WARRANTIES WITH RESPECT TO THE GOODS. IF THE WARRANTY BECOMES VOID, THE BUYER MAY PURCHASE FROM SELLER, IF AVAILABLE, A SERVICE AGREEMENT OR ONE-TIME SERVICE AT THEN CURRENT RATES. THE OBLIGATIONS CREATED BY THIS WARRANTY TO REPAIR OR REPLACE DEFECTIVE GOODS SHALL BE THE SOLE REMEDY OF BUYER IN THE EVENT OF A WARRANTY CLAIM. SELLER MAKES NO WARRANTY, EITHER EXPRESS OR IMPLIED, OTHER THAN AS STATED HEREIN. SELLER DISCLAIMS ALL IMPLIED WARRANTIES.

5. LIMITED WARRANTY FOR SERVICES: Seller warrants the Services will conform to the specifications stated in the Proposal and will be performed in a workmanlike manner. The warranty on Services shall be for a period of three (3) months following completion of the Services (the “Service Warranty Period”). Seller agrees during the Service Warranty Period, to re-perform any defective Services; provided that Buyer shall promptly notify Seller in writing upon the discovery of any defect and specify details of the warranty claim. THE OBLIGATIONS CREATED BY THIS WARRANTY TO REPERFORM DEFECTIVE SERVICES SHALL BE THE SOLE REMEDY OF BUYER IN THE EVENT OF A WARRANTY CLAIM. SELLER MAKES NO WARRANTY, EITHER EXPRESS OR IMPLIED, OTHER THAN AS STATED HEREIN. SELLER DISCLAIMS ALL IMPLIED WARRANTIES.

6. BACKCHARGES: No backcharges will be paid or allowed by Seller unless Seller is notified in writing of any claim of defect in the Goods or Services and Seller is given a minimum of thirty (30) days within which to begin remediation of such defect. All backcharges must be approved in writing by Seller before

any Services are reperfomed or any Goods are repaired, replaced, or altered in any manner by Buyer or returned to Seller.

7. CANCELLATION FEE: Buyer may cancel the Order for convenience prior to delivery upon written notice to Seller, in which case Seller will cease activity (except that related to the cancellation) and promptly terminate all related subcontracts. In such event, Buyer shall pay the greater of: (a) Seller's total costs incurred in performing the Order up to the date of receipt of notice of cancellation and all costs associated with the cancellation, including but not limited to, costs of canceling related subcontracts and any currency hedge(s) maintained by Seller relative to the Order, plus reasonable overhead and profit; or (b) a cancellation fee of twenty-five percent (25%) of the Price. However, the amount payable to Seller for cancellation will not exceed the Price.

8. TERMINATION FOR DEFAULT: Buyer may declare Seller in default only if: (a) Seller breaches a material provision of the Order; (b) Buyer provides Seller thirty (30) days written notice specifying Seller's alleged breach in detail; and (c) Seller fails to reasonably cure such alleged breach with the thirty (30) day period following Seller's receipt of Buyer's written notice. In the event of Seller's uncured default, Buyer's sole remedy shall be to terminate the Order and recover any payments made to Seller for the Order.

9. INTELLECTUAL PROPERTY INFRINGEMENT & INDEMNITY: Seller warrants the Goods do not infringe any United States patent. Seller shall, subject to the limitations herein, indemnify Buyer for reasonable damages if the Goods are held to constitute infringement of a United States patent. This indemnity shall not apply: (a) to Goods or parts thereof manufactured pursuant to Buyer's design, or to changes in Seller's design requested by Buyer; and (b) if the infringement is a result of Buyer's operation of the Goods. Buyer shall promptly notify Seller in writing of any alleged claim of infringement, permit Seller to control the defense or compromise of any such claim, and render such assistance as Seller may require. Seller shall have no indemnity obligations to Buyer under this Section if the Buyer is not in compliance with its payment obligations to Seller pursuant to the Order.

10. INDEMNITY: Seller shall be responsible for any illness, injury or death, of the employees of the Seller, its subsidiaries, and their officers, directors, employees, agents, and contractors (collectively, the "Seller Group") and for the loss or damage to the property of any member of the Seller Group, arising out of or relating to the performance of this Order and REGARDLESS OF WHETHER CAUSED OR BROUGHT ABOUT BY THE NEGLIGENCE (INCLUDING ACTIVE, PASSIVE, SOLE, JOINT OR CONCURRENT NEGLIGENCE) OF THE BUYER, ITS SUBSIDIARIES AND ITS CUSTOMER OR ULTIMATE RECIPIENT OR USER OF THE GOODS OR SERVICES AND THEIR OFFICERS, DIRECTORS, EMPLOYEES, AGENTS AND CONTRACTORS (COLLECTIVELY, THE "BUYER GROUP") OR ANY OTHER THEORY OF LEGAL LIABILITY, and Seller shall release, defend, protect, indemnify and hold harmless all members of the Buyer Group from and against any loss, cost, claim, suit, judgment, award or damage (including reasonable attorney's fees) on account of such illness, injury or death, loss or damage. In exchange, Buyer shall be responsible for any illness, injury or death, of the employees of any member of the Buyer Group and for the loss or damage to the property of any member of the Buyer Group, arising out of or relating to the performance of this Order and REGARDLESS OF WHETHER CAUSED OR BROUGHT ABOUT BY THE NEGLIGENCE (INCLUDING ACTIVE, PASSIVE, SOLE, JOINT OR CONCURRENT NEGLIGENCE) OF ANY MEMBER OF THE SELLER GROUP OR ANY OTHER THEORY OF LEGAL LIABILITY, and Buyer shall release, defend, protect, indemnify and hold harmless all members of the Seller Group from and against any loss, cost, claim, suit, judgment, award or damage (including reasonable attorney's fees) on account of such illness, injury or death, loss or damage. Seller and Buyer shall each release, defend, protect, indemnify and hold harmless each other, and the applicable members of the Seller Group or Buyer Group, from and against any loss, cost, claim, suit, judgment, award or damage (including reasonable attorney's fees) for illness, injury, death, or damage to property of third parties (not included within the definitions of Seller Group or Buyer Group) but only to the extent caused by the negligent acts or omissions of such party. Seller shall have no indemnity obligations to Buyer under this Section if the Buyer is not in compliance with its payment obligations to Seller pursuant to the Order. Should any of the preceding indemnities be judged unenforceable or be limited by applicable law, then each party's indemnity obligations to the other shall be limited to the extent that liability for any such illness, injury, death or damage to property is caused by the negligent acts or omissions of such party.

11. GOVERNING LAW: To the maximum extent permissible, this Order shall be governed and construed in accordance with the laws of the State of

Oklahoma (U.S.A.), exclusive of any principles of conflicts of laws that would require application of the substantive laws of another jurisdiction. The exclusive venue for all legal actions under this Order shall be the State or Federal Courts sitting in Tulsa, Oklahoma (U.S.A.), and the parties submit to the personal jurisdiction thereof and waive any other venue that may be applicable to such action. This Order excludes the application of the United Nations Convention on Contracts for the International Sale of Goods.

12. FORCE MAJEURE: Except for Buyer's obligations to pay sums to Seller when due, neither party shall be liable for its failure to perform obligations under the Order if such failure results from fire, flood, earthquake, storm, hurricane or other natural disaster, war, invasion, act of foreign enemies, rebellion, terrorist activities, nationalization, government sanction, blockage, embargo, or interruption or failure of electricity, water, telephone or utility service.

13. ASSIGNMENT: Buyer shall not assign the Order without the prior written consent of Seller, and such consent shall not be unreasonably withheld; however, any assignment shall not relieve Buyer of its payment and indemnity obligations to Seller.

14. ENFORCEABILITY: Should a court of competent jurisdiction rule that any provision herein is invalid or unenforceable, such ruling shall not affect the validity or enforceability of any other provision.

15. WAIVER: Seller's failure to enforce any provisions herein shall not constitute a waiver of such rights, or preclude their later enforcement.

16. WAIVER OF CONSEQUENTIAL DAMAGES: SELLER SHALL NOT BE LIABLE FOR PUNITIVE, INDIRECT, INCIDENTAL OR CONSEQUENTIAL DAMAGES, INCLUDING, BUT NOT LIMITED TO, LIABILITY FOR REMOVAL AND REINSTALLATION COSTS, LOSS OF USE, LOSS OF BUSINESS OPPORTUNITY, LOSS OF PROFIT OR REVENUE, LOSS OF PRODUCT OR OUTPUT, OR BUSINESS INTERRUPTION.

17. LIMITATION OF LIABILITY: ANYTHING TO THE CONTRARY CONTAINED IN THIS ORDER NOTWITHSTANDING, SELLER'S CUMULATIVE LIABILITY ARISING OUT OF OR IN ANY MANNER RELATED TO ITS PERFORMANCE SHALL NOT EXCEED, IN THE AGGREGATE, ONE HUNDRED PERCENT (100%) OF THE MONIES RECEIVED BY SELLER UNDER THIS ORDER. THE REMEDIES PROVIDED TO BUYER UNDER THIS ORDER ARE IN LIEU OF ALL OTHER REMEDIES WHICH MAY BE OR BECOME AVAILABLE TO BUYER AT LAW OR IN EQUITY. THE LIMITATIONS SET FORTH HEREIN APPLY WHETHER CLAIMS ARISE PURSUANT TO CONTRACT, TORT, INDEMNITY, STATUTE, EQUITY OR ANY OTHER THEORY OF LAW, INCLUDING, BUT NOT LIMITED TO, THE BREACH OF ANY LEGAL DUTY OR THE FAULT, NEGLIGENCE, PROFESSIONAL LIABILITY OR STRICT LIABILITY OF SELLER. THIS LIMITATION SHALL BE INCLUSIVE OF ALL INSURANCE, BOND, AND LETTER OF CREDIT PROCEEDS, WHICH MAY BE PAID TO THE BUYER BY THE INSURERS, SURETIES OR BANKS OF SELLER. SHOULD THESE REMEDIES BE FOUND INADEQUATE OR TO HAVE FAILED IN THEIR ESSENTIAL PURPOSE FOR ANY REASON WHATSOEVER, THEN THE BUYER AGREES THAT THE SELLER'S RETURN TO THE BUYER OF NO GREATER THAN ONE HUNDRED PERCENT (100%) OF THE MONIES RECEIVED BY SELLER UNDER THIS ORDER SHALL PREVENT THE REMEDIES FROM FAILING THEIR ESSENTIAL PURPOSE AND SHALL BE CONSIDERED BY BUYER AS A FAIR AND ADEQUATE REMEDY.

18. ENTIRE AGREEMENT: This Order contains the entire agreement of the parties and supersedes any and all prior course of dealing, agreements, understandings and communications between Buyer and Seller related to the subject matter of this Order. No amendment or modification of this Order shall be binding unless it is in writing and is signed by an authorized representative of Buyer and Seller.



ATTACHMENT A
START-UP/MAINTENANCE SERVICES, EQUIPMENT DATA/DRAWINGS
AND STANDARD TERMS AND CONDITIONS



I. START-UP/MAINTENANCE SERVICES

RATES	DOMESTIC (Within US)	FOREIGN (Outside US)
Base Rates for Start-Up/Maintenance personnel on all non-holiday (U.S Government recognized) Monday through Friday, inclusive, up to a maximum of ten (10) hours per day.	\$1,600.00 per day	2,300.00 per day
Hours in Excess of ten (10) hours per day Monday through Friday, non-holiday.	\$240.00 per hour	\$345.00 per hour
Saturdays and Sundays - up to a maximum of ten (10) hours per day	\$2,400.00	\$3,450.00
Hours in Excess of ten (10) hours per day Saturday and Sunday, non-holiday	\$368.00 per hour	\$518.00 per hour
Holidays (U.S. Government Recognized) - up to a maximum of ten (10) hours per day	\$3,200.00	\$4,600.00
Hours in Excess of ten (10) hours per day Holidays	\$480.00 per hour	\$690.00 per hour
Air Travel (Class)	Coach	Business
Ground Transportation	Mid-Sized Rental Car	Mid-Sized Rental Car
Engineering Rates	\$375.00 per hour	\$375.00 per hour
Design / Drafting Rates	\$185.00 per hour	\$185.00 per hour

*** The above Domestic and Foreign rates do not include OFFSHORE assistance. Please contact Zeeco if you are interested in obtaining a proposal for OFFSHORE assistance*

Compensable Days

Per diem rates will apply from, and including, the day the start-up/maintenance personnel leaves his basing point up to, and including, his date of return to the basing point.

Expenses

Zeeco shall be reimbursed at actual cost plus 15% for all non-Buyer provided living and travel expenses incurred, which are related to the supply of services rendered.

Engineering / Drafting Charges

Engineering and/or drafting charges will apply for all work performed by Zeeco personnel as required to support Start-Up/Maintenance personnel. These charges will apply at the rate indicated in the chart above.

Independent Contractor

Zeeco personnel shall be considered an independent contractor with respect to services provided hereunder and the start-up/maintenance personnel shall in no respect be considered an employee of the Buyer. Zeeco reserves the right to recall, replace, or return the personnel at Zeeco's sole discretion.

II. EQUIPMENT DATA/DRAWINGS

A. STANDARD QUANTITY

Priced quotation for equipment include three (3) print copies of approval drawings; three (3) print copies and one (1) reproducible copy of the final drawings; and three (3) copies of an operational manual. Additional copies of drawings will be provided at \$30.00 per print and \$45.00 per reproducible. Additional operational manuals will be priced on application, and based on the complexity of the equipment.

Drawings and data provided hereunder are the property of Zeeco, Inc. and may not be used for any purpose other than the repair, operation and maintenance of the equipment depicted.

III. TERMS AND CONDITIONS

- A. All service and data provided under this Attachment are in accordance with Zeeco's Standard Terms and Conditions of Sale.
- B. All rates quoted herein are subject to change without notice.
- C. Zeeco will require a purchase order from the Buyer accepting the terms and condition set forth herein, as well as an estimate of duration and nature of the work to be done.
- D. Prior to dispatch of Zeeco personnel, Buyer may be required to provide a deposit equal to the charges for the anticipated duration of service, or two weeks of service, whichever is greater. This requirement will be enforced at the discretion of Zeeco, Inc.
- E. The transportation modes and carriers and all arrangements therefore, and the choice of lodgings and all arrangements therefore, will be at the sole discretion of Zeeco, Inc.
- F. Where on-site room and board are furnished by the customer, Zeeco, Inc. expects their personnel to be roomed and boarded in a comfortable environment similar to Buyer's personnel or mutually agreed upon accommodations.
- G. It is the Buyer's responsibility to secure all work permits, licenses, and other documents required to allow our personnel to complete their assignment in accordance with local government regulations and labor laws.
- H. All tools, materials, and equipment for use by Zeeco personnel will be furnished by the Buyer, unless other mutually agreed upon arrangements have been made.
- I. The service rates and expenses described herein do not include any taxes of any kind that may be assessed by any governmental department outside the U.S.A. Any such taxes that may be applicable to the service rates and expenses will be for the Buyer's account.

THE SALE OF SERVICES (THE "SERVICES"), AS DESCRIBED IN CONTRACTOR'S QUOTATION OR PROPOSAL (THE "PROPOSAL"), IS EXPRESSLY CONDITIONED UPON BUYER'S AGREEMENT TO THESE TERMS & CONDITIONS. ANY ADDITIONAL OR DIFFERENT TERMS PROPOSED BY BUYER ARE EXPRESSLY OBJECTED TO AND WILL NOT BE BINDING UPON CONTRACTOR UNLESS AGREED TO IN WRITING BY CONTRACTOR. ANY PURCHASE ORDER (THE "ORDER") ISSUED BY BUYER FOR THE PURCHASE OF SERVICES SHALL CONSTITUTE BUYER'S AGREEMENT TO THESE TERMS & CONDITIONS. UNLESS OTHERWISE SPECIFIED IN THE PROPOSAL OR THE ORDER, ANY PROPOSAL BY CONTRACTOR SHALL EXPIRE THIRTY (30) DAYS FROM ITS DATE AND MAY BE MODIFIED OR WITHDRAWN BY CONTRACTOR BEFORE RECEIPT OF BUYER'S ACCEPTANCE. UNLESS OTHERWISE STATED, THE CONTRACTOR SHALL BE ZEECO, INC., 22151 EAST 91ST STREET, BROKEN ARROW, OKLAHOMA 74014 (USA), AND THE BUYER SHALL BE THE PARTY IDENTIFIED AS SUCH ON THE ORDER.

1. PRICE: Unless otherwise stated in the Proposal, the price of the Order (the "Price") is exclusive of all taxes, duties, fees, charges or assessments of any nature levied by any governmental authority. Payment terms shall be as stated in the Proposal and Contractor's acceptance of the Order is subject to credit approval.

2. LIMITED WARRANTY: Contractor warrants the Services will be performed in a workmanlike manner. The warranty on Services shall be for a period of three (3) months following completion of the Services (the "Service Warranty Period"). Contractor agrees during the Service Warranty Period, to re-perform any defective Services; provided that Buyer shall promptly notify Contractor in writing upon the discovery of any defect and specify details of the warranty claim. Contractor warrants all parts manufactured by Contractor and sold in conjunction with the Services (the "Goods") will be free from defects in material and workmanship for a period of twelve (12) months from the date of installation (the "Goods Warranty Period") when subjected to normal, proper and intended usage by properly trained personnel. Contractor agrees during the Goods Warranty Period, to repair or replace any defective Goods; provided that Buyer shall promptly notify Contractor in writing upon the discovery of any defect and specify details of the warranty claim. Goods that are obtained by Contractor from an original manufacturer or third party supplier are not warranted by Contractor, but Contractor will, to the extent possible, assign to Buyer any warranty rights in such Goods that Contractor received from the original manufacturer or third party supplier. Consumables such as, but not limited to, bulbs, fuses, thermocouples, gaskets, and similar items are outside the scope of this warranty. All responsibility for and costs of removal and/or reinstallation of warranted Goods as well as the cost of and responsibility for gaining access to the warranted Goods, are excluded from this warranty. This warranty shall be void if the Goods have been: (a) exposed to corrosion, erosion, or chemical attack; (b) operated contrary to Contractor's instructions or accepted industry practices; (c) improperly maintained or operated, or subjected to accident, abuse, or vandalism; or (d) operated in conditions other than those stated in Buyer's written specifications. Additionally, this warranty shall be void if the Buyer is not in compliance with its payment obligations to Contractor pursuant to the Order. Contractor shall have no obligation to make repairs, replacements or corrections resulting from normal wear and tear to the Goods. If Contractor determines that a warranty claim is not valid, then Buyer shall pay or reimburse Contractor for all costs of investigating and responding to such claim, including non-warranty parts sold or installed, at Contractor's then prevailing time and materials rates. THE OBLIGATIONS CREATED BY THIS WARRANTY TO REPERFORM DEFECTIVE SERVICES, OR REPAIR OR REPLACE DEFECTIVE GOODS, SHALL BE THE SOLE REMEDY OF BUYER IN THE EVENT OF A WARRANTY CLAIM. CONTRACTOR MAKES NO WARRANTY, EITHER EXPRESS OR IMPLIED, OTHER THAN AS STATED HEREIN. CONTRACTOR DISCLAIMS ALL IMPLIED WARRANTIES.

3. BACKCHARGES: No backcharges will be paid or allowed by Contractor unless Contractor is notified in writing of any claim of defect and Contractor is given a minimum of thirty (30) days within which to begin remediation of such defect. All backcharges must be approved in writing by Contractor before any Services are re-performed and charged to Contractor's account or any Goods are repaired, replaced or altered in any manner by Buyer or returned to Contractor.

4. TERMINATION FOR DEFAULT: Buyer may declare Contractor in default only if: (a) Contractor breaches a material provision of the Order; (b) Buyer provides Contractor thirty (30) days written notice specifying Contractor's alleged breach in detail; and (c) Contractor fails to reasonably cure such alleged breach with the thirty (30) day period following Contractor's receipt of Buyer's written notice. In the event of Contractor's uncurd default, Buyer's sole remedy shall be to terminate the Order and recover any payments made to Contractor for the Order.

5. INDEMNITY: Contractor shall be responsible for any illness, injury or death, of the employees of the Contractor, its subsidiaries, and their officers, directors, employees, agents, and contractors (collectively, the "Contractor Group") and for the loss or damage to the property of any member of the Contractor Group, arising out of or relating to the performance of this Order and REGARDLESS OF WHETHER CAUSED OR BROUGHT ABOUT BY THE NEGLIGENCE (INCLUDING ACTIVE, PASSIVE, SOLE, JOINT OR CONCURRENT NEGLIGENCE) OF THE BUYER, ITS SUBSIDIARIES AND ITS CUSTOMER OR ULTIMATE RECIPIENT OR USER OF THE GOODS OR SERVICES AND THEIR OFFICERS, DIRECTORS, EMPLOYEES, AGENTS AND CONTRACTORS (COLLECTIVELY, THE "BUYER GROUP") OR ANY OTHER THEORY OF LEGAL LIABILITY, and Contractor shall release, defend, protect, indemnify and hold harmless all members of the Buyer Group from and against any loss, cost, claim, suit, judgment, award or damage (including reasonable attorney's fees) on account of such illness, injury or death, loss or damage. In exchange, Buyer shall be responsible for any illness, injury or death, of the employees of any member of the Buyer Group and for the loss or damage to the property of any member of the Buyer Group, arising out of or relating to the performance of this Order and REGARDLESS OF WHETHER CAUSED OR BROUGHT ABOUT BY THE

NEGLIGENCE (INCLUDING ACTIVE, PASSIVE, SOLE, JOINT OR CONCURRENT NEGLIGENCE) OF ANY MEMBER OF THE CONTRACTOR GROUP OR ANY OTHER THEORY OF LEGAL LIABILITY, and Buyer shall release, defend, protect, indemnify and hold harmless all members of the Contractor Group from and against any loss, cost, claim, suit, judgment, award or damage (including reasonable attorney's fees) on account of such illness, injury or death, loss or damage. Contractor and Buyer shall each release, defend, protect, indemnify and hold harmless each other, and the applicable members of the Contractor Group or Buyer Group, from and against any loss, cost, claim, suit, judgment, award or damage (including reasonable attorney's fees) for illness, injury, death, or damage to property of third parties (not included within the definitions of Contractor Group or Buyer Group) but only to the extent caused by the negligent acts or omissions of such party. Contractor shall have no indemnity obligations to Buyer under this Section if the Buyer is not in compliance with its payment obligations to Contractor pursuant to the Order. Should any of the preceding indemnities be judged unenforceable or be limited by applicable law, then each party's indemnity obligations to the other shall be limited to the extent that liability for any such illness, injury, death or damage to property is caused by the negligent acts or omissions of such party.

6. INSURANCE: Contractor shall maintain the following insurance coverage and, at Buyer's request, shall provide Buyer with certificates evidencing such coverage: (a) Statutory Workers' Compensation and Employer's Liability Insurance with limits of USD \$1,000,000 per occurrence; (b) Commercial General Liability Insurance with a combined single limit for bodily injury and property damage of USD \$1,000,000 per occurrence and in the aggregate; and (c) Automobile Liability Insurance with a combined single limit for bodily injury and property damage of USD \$1,000,000 per accident.

7. GOVERNING LAW: To the maximum extent permissible, this Order shall be governed and construed in accordance with the laws of the State of Oklahoma (U.S.A.), exclusive of any principles of conflicts of laws that would require application of the substantive laws of another jurisdiction. The exclusive venue for all legal actions under this Order shall be the State or Federal Courts sitting in Tulsa, Oklahoma (U.S.A.), and the parties submit to the personal jurisdiction thereof and waive any other venue that may be applicable to such action.

8. FORCE MAJEURE: Except for Buyer's obligations to pay sums to Contractor when due, neither party shall be liable for its failure to perform obligations under the Order if such failure results from fire, flood, earthquake, storm, hurricane or other natural disaster, war, invasion, act of foreign enemies, rebellion, terrorist activities, nationalization, government sanction, blockage, embargo, or interruption or failure of electricity, water, telephone or utility service.

9. ASSIGNMENT: Buyer shall not assign the Order without the prior written consent of Contractor, and such consent shall not be unreasonably withheld; however, any assignment shall not relieve Buyer of its payment and indemnity obligations to Contractor.

10. ENFORCEABILITY: Should a court of competent jurisdiction rule that any provision herein is invalid or unenforceable, such ruling shall not affect the validity or enforceability of any other provision.

11. WAIVER: Contractor's failure to enforce any provisions herein shall not constitute a waiver of such rights, or preclude their later enforcement.

12. WAIVER OF CONSEQUENTIAL DAMAGES: CONTRACTOR SHALL NOT BE LIABLE FOR PUNITIVE, INDIRECT, INCIDENTAL OR CONSEQUENTIAL DAMAGES, INCLUDING, BUT NOT LIMITED TO, LIABILITY FOR REMOVAL AND REINSTALLATION COSTS, LOSS OF USE, LOSS OF BUSINESS OPPORTUNITY, LOSS OF PROFIT OR REVENUE, LOSS OF PRODUCT OR OUTPUT, OR BUSINESS INTERRUPTION.

13. LIMITATION OF LIABILITY: ANYTHING TO THE CONTRARY CONTAINED IN THIS ORDER NOTWITHSTANDING, CONTRACTOR'S CUMULATIVE LIABILITY ARISING OUT OF OR IN ANY MANNER RELATED TO ITS PERFORMANCE SHALL NOT EXCEED, IN THE AGGREGATE, ONE HUNDRED PERCENT (100%) OF THE MONIES RECEIVED BY CONTRACTOR UNDER THIS ORDER. THE REMEDIES PROVIDED TO BUYER UNDER THIS ORDER ARE IN LIEU OF ALL OTHER REMEDIES WHICH MAY BE OR BECOME AVAILABLE TO BUYER AT LAW OR IN EQUITY. THE LIMITATIONS SET FORTH HEREIN APPLY WHETHER CLAIMS ARISE PURSUANT TO CONTRACT, TORT, INDEMNITY, STATUTE, EQUITY OR ANY OTHER THEORY OF LAW, INCLUDING, BUT NOT LIMITED TO, THE BREACH OF ANY LEGAL DUTY OR THE FAULT, NEGLIGENCE, PROFESSIONAL LIABILITY OR STRICT LIABILITY OF CONTRACTOR. THIS LIMITATION SHALL BE INCLUSIVE OF ALL INSURANCE, BOND, AND LETTER OF CREDIT PROCEEDS, WHICH MAY BE PAID TO THE BUYER BY THE INSURERS, SURETIES OR BANKS OF CONTRACTOR. SHOULD THESE REMEDIES BE FOUND INADEQUATE OR TO HAVE FAILED IN THEIR ESSENTIAL PURPOSE FOR ANY REASON WHATSOEVER, THEN THE BUYER AGREES THAT THE CONTRACTOR'S RETURN TO THE BUYER OF NO GREATER THAN ONE HUNDRED PERCENT (100%) OF THE MONIES RECEIVED BY CONTRACTOR UNDER THIS ORDER SHALL PREVENT THE REMEDIES FROM FAILING THEIR ESSENTIAL PURPOSE AND SHALL BE CONSIDERED BY BUYER AS A FAIR AND ADEQUATE REMEDY.

14. ENTIRE AGREEMENT: This Order contains the entire agreement of the parties and supersedes any and all prior course of dealing, agreements, understandings and communications between Buyer and Contractor related to the subject matter of this Order. No amendment or modification of this Order shall be binding unless it is in writing and is signed by an authorized representative of Buyer and Contractor.

Process Streams		11
Composition		Status: Solved
Phase: Vapor	From Block:	MIX-102
	To Block:	Stab-Off Gas Suction
Mass Flow	lb/h	
Hydrogen Sulfide	0	
Nitrogen	6.05600	
Carbon Dioxide	14.1511	
Methane	302.022	
Ethane	396.811	
Propane	850.564	
i-Butane	240.437	
n-Butane	626.047	
2,2-Dimethylpropane	3.96168	
i-Pentane	76.2225	
n-Pentane	64.1347	
2,2-Dimethylbutane	0.518399	
Cyclopentane	0	
2,3-Dimethylbutane	3.64221	
2-Methylpentane	8.53074	
3-Methylpentane	4.48824	
n-Hexane	7.81511	
Methylcyclopentane	4.07930	
Benzene	1.56366	
Cyclohexane	3.33121	
2-Methylhexane	0.694155	
3-Methylhexane	0.775936	
2,2,4-Trimethylpentane	0	
n-Heptane	3.15518	
Methylcyclohexane	1.66868	
Toluene	0.505030	
n-Octane	0.954325	
Ethylbenzene	0.0252741	
m-Xylene	0.0235965	
p-Xylene	0.0235656	
o-Xylene	0	
n-Nonane	0.0981057	

Process Streams		11
Properties		Status: Solved
Phase: Vapor	From Block:	MIX-102
	To Block:	Stab-Off Gas Suction
Property	Units	
Temperature	°F	94.3754
Pressure	psia	114.696
Mole Fraction Vapor	%	100
Mole Fraction Light Liquid	%	0
Mole Fraction Heavy Liquid	%	0
Molecular Weight	lb/lbmol	37.8745
Mass Density	lb/ft ³	0.802495
Std Vapor Volumetric Flow	MMSCFD	0.630595
Std Liquid Volumetric Flow	sgpm	11.2189
Compressibility		0.910424
Specific Gravity		1.30770
API Gravity		
Mass Cp	Btu/(lb*°F)	0.448998
Ideal Gas CpCv Ratio		1.14048
Dynamic Viscosity	cP	0.00940355
Kinematic Viscosity	cSt	0.731524
Net Ideal Gas Heating Value	Btu/ft ³	1985.94
Net Liquid Heating Value	Btu/lb	19758.4
Gross Ideal Gas Heating Value	Btu/ft ³	2163.24
Gross Liquid Heating Value	Btu/lb	21534.9

GRI-GLYCalc VERSION 4.0 - AGGREGATE CALCULATIONS REPORT

Case Name: Enterprise South Carlsbad

File Name: C:\Users\jzenker\Trinity Consultants, Inc\Enterprise Products - PROJECT\153201.0159 NSR Sig Rev\06
CALCULATIONS\GlyCalc\South Carlsbad GLYCalc VOC_v0.4.ddf

Date: September 04, 2020

DESCRIPTION:

Description: Updated gas analysis for dehy based on South
Carlsbad Max Hourly Rate.pmx - Sweet gas
stream received from Ms. Jing Li (EPCO)

Annual Hours of Operation: 8760.0 hours/yr

EMISSIONS REPORTS:

CONTROLLED REGENERATOR EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Hydrogen Sulfide	0.0345	0.828	0.1511
Methane	2.0630	49.511	9.0357
Ethane	4.0149	96.358	17.5854
Propane	8.3661	200.786	36.6434
Isobutane	2.2448	53.875	9.8322
n-Butane	7.0025	168.059	30.6708
Isopentane	1.8013	43.230	7.8895
n-Pentane	2.4410	58.585	10.6918
n-Hexane	0.7973	19.135	3.4922
Cyclohexane	1.5682	37.636	6.8685
Other Hexanes	1.3772	33.052	6.0320
Heptanes	0.8359	20.062	3.6613
Methylcyclohexane	1.1244	26.985	4.9248
Benzene	4.1552	99.724	18.1996
Toluene	2.5872	62.093	11.3319
Xylenes	0.2782	6.677	1.2185
C8+ Heavies	0.0125	0.300	0.0548
Total Emissions	40.7040	976.897	178.2836
Total Hydrocarbon Emissions	40.6695	976.069	178.1325
Total VOC Emissions	34.5916	830.199	151.5114
Total HAP Emissions	7.8179	187.628	34.2422
Total BTEX Emissions	7.0205	168.493	30.7500

UNCONTROLLED REGENERATOR EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Hydrogen Sulfide	0.0371	0.890	0.1624
Methane	2.0663	49.592	9.0505
Ethane	4.0347	96.832	17.6719
Propane	8.5299	204.717	37.3609
Isobutane	2.3320	55.969	10.2143
n-Butane	7.3974	177.539	32.4008
Isopentane	2.0747	49.793	9.0871
n-Pentane	2.8323	67.976	12.4056
n-Hexane	1.1418	27.403	5.0011
Cyclohexane	2.5465	61.117	11.1538
Other Hexanes	1.8032	43.277	7.8981
Heptanes	1.8748	44.995	8.2115
Methylcyclohexane	2.5316	60.758	11.0883
Benzene	7.2972	175.133	31.9618
Toluene	8.1400	195.361	35.6534
Xylenes	2.5339	60.814	11.0986
C8+ Heavies	5.3119	127.485	23.2660
Total Emissions	62.4854	1499.650	273.6861
Total Hydrocarbon Emissions	62.4483	1498.760	273.5238
Total VOC Emissions	56.3473	1352.336	246.8013
Total HAP Emissions	19.1130	458.711	83.7148
Total BTEX Emissions	17.9712	431.308	78.7138

FLASH TANK OFF GAS

Component	lbs/hr	lbs/day	tons/yr
Hydrogen Sulfide	0.0036	0.087	0.0158
Methane	19.7893	474.943	86.6771
Ethane	11.4918	275.803	50.3340
Propane	8.9269	214.245	39.0996
Isobutane	1.5885	38.123	6.9575
n-Butane	3.7218	89.323	16.3014
Isopentane	0.9009	21.622	3.9460
n-Pentane	0.9619	23.085	4.2130
n-Hexane	0.2122	5.094	0.9297
Cyclohexane	0.1358	3.260	0.5950
Other Hexanes	0.4529	10.870	1.9837
Heptanes	0.1711	4.107	0.7494
Methylcyclohexane	0.1017	2.442	0.4456
Benzene	0.0380	0.912	0.1664
Toluene	0.0270	0.647	0.1181
Xylenes	0.0030	0.073	0.0133

C8+ Heavies	0.0568	1.362	0.2486
-------------	--------	-------	--------

Total Emissions	48.5832	1165.996	212.7943
-----------------	---------	----------	----------

Total Hydrocarbon Emissions	48.5795	1165.909	212.7784
Total VOC Emissions	17.2985	415.163	75.7673
Total HAP Emissions	0.2802	6.725	1.2274
Total BTEX Emissions	0.0680	1.631	0.2977

EQUIPMENT REPORTS:

CONDENSER

Condenser Outlet Temperature: 110.00 deg. F
 Condenser Pressure: 13.10 psia
 Condenser Duty: 7.69e-001 MM BTU/hr
 Hydrocarbon Recovery: 1.70 bbls/day
 Produced Water: 68.54 bbls/day
 VOC Control Efficiency: 38.61 %
 HAP Control Efficiency: 59.10 %
 BTEX Control Efficiency: 60.93 %
 Dissolved Hydrocarbons in Water: 643.60 mg/L

Component	Emitted	Condensed
-----------	---------	-----------

Water	0.17%	99.83%
Carbon Dioxide	97.79%	2.21%
Hydrogen Sulfide	93.07%	6.93%
Nitrogen	99.89%	0.11%
Methane	99.84%	0.16%
Ethane	99.51%	0.49%
Propane	98.08%	1.92%
Isobutane	96.26%	3.74%
n-Butane	94.66%	5.34%
Isopentane	86.82%	13.18%
n-Pentane	86.19%	13.81%
n-Hexane	69.83%	30.17%
Cyclohexane	61.58%	38.42%
Other Hexanes	76.37%	23.63%
Heptanes	44.59%	55.41%
Methylcyclohexane	44.41%	55.59%
Benzene	56.94%	43.06%
Toluene	31.78%	68.22%
Xylenes	10.98%	89.02%
C8+ Heavies	0.24%	99.76%

ABSORBER

Calculated Absorber Stages: 2.05
 Specified Dry Gas Dew Point: 7.00 lbs. H2O/MMSCF
 Temperature: 120.0 deg. F
 Pressure: 750.0 psig
 Dry Gas Flow Rate: 200.0000 MMSCF/day
 Glycol Losses with Dry Gas: 5.8623 lb/hr
 Wet Gas Water Content: Saturated
 Calculated Wet Gas Water Content: 126.81 lbs. H2O/MMSCF
 Calculated Lean Glycol Recirc. Ratio: 1.20 gal/lb H2O

Component	Remaining in Dry Gas	Absorbed in Glycol
Water	5.51%	94.49%
Carbon Dioxide	99.90%	0.10%
Hydrogen Sulfide	99.46%	0.54%
Nitrogen	99.99%	0.01%
Methane	99.99%	0.01%
Ethane	99.98%	0.02%
Propane	99.96%	0.04%
Isobutane	99.95%	0.05%
n-Butane	99.94%	0.06%
Isopentane	99.94%	0.06%
n-Pentane	99.92%	0.08%
n-Hexane	99.88%	0.12%
Cyclohexane	99.50%	0.50%
Other Hexanes	99.91%	0.09%
Heptanes	99.80%	0.20%
Methylcyclohexane	99.47%	0.53%
Benzene	95.72%	4.28%
Toluene	94.23%	5.77%
Xylenes	89.11%	10.89%
C8+ Heavies	99.16%	0.84%

FLASH TANK

Flash Control: Vented to atmosphere
 Flash Temperature: 100.0 deg. F
 Flash Pressure: 73.0 psig

Component	Left in Glycol	Removed in Flash Gas
Water	99.99%	0.01%
Carbon Dioxide	61.37%	38.63%
Hydrogen Sulfide	91.11%	8.89%
Nitrogen	8.57%	91.43%
Methane	9.45%	90.55%

Ethane	25.99%	74.01%
Propane	48.86%	51.14%
Isobutane	59.48%	40.52%
n-Butane	66.53%	33.47%
Isopentane	69.87%	30.13%
n-Pentane	74.77%	25.23%
n-Hexane	84.40%	15.60%
Cyclohexane	95.10%	4.90%
Other Hexanes	80.13%	19.87%
Heptanes	91.68%	8.32%
Methylcyclohexane	96.29%	3.71%
Benzene	99.51%	0.49%
Toluene	99.70%	0.30%
Xylenes	99.90%	0.10%
C8+ Heavies	99.07%	0.93%

REGENERATOR

No Stripping Gas used in regenerator.

Component	Remaining in Glycol	Distilled Overhead
Water	10.11%	89.89%
Carbon Dioxide	0.00%	100.00%
Hydrogen Sulfide	0.00%	100.00%
Nitrogen	0.00%	100.00%
Methane	0.00%	100.00%
Ethane	0.00%	100.00%
Propane	0.00%	100.00%
Isobutane	0.00%	100.00%
n-Butane	0.00%	100.00%
Isopentane	0.72%	99.28%
n-Pentane	0.67%	99.33%
n-Hexane	0.59%	99.41%
Cyclohexane	3.37%	96.63%
Other Hexanes	1.25%	98.75%
Heptanes	0.55%	99.45%
Methylcyclohexane	4.16%	95.84%
Benzene	5.03%	94.97%
Toluene	7.93%	92.07%
Xylenes	12.99%	87.01%
C8+ Heavies	12.18%	87.82%

STREAM REPORTS:

WET GAS STREAM

Temperature: 120.00 deg. F
Pressure: 764.70 psia
Flow Rate: 8.36e+006 scfh

Component	Conc. (vol%)	Loading (lb/hr)
Water	2.67e-001	1.06e+003
Carbon Dioxide	3.18e-001	3.08e+003
Hydrogen Sulfide	9.97e-004	7.49e+000
Nitrogen	1.31e+000	8.08e+003
Methane	8.02e+001	2.83e+005
Ethane	1.04e+001	6.86e+004
Propane	4.63e+000	4.50e+004
Isobutane	6.07e-001	7.77e+003
n-Butane	1.34e+000	1.71e+004
Isopentane	2.98e-001	4.74e+003
n-Pentane	3.03e-001	4.82e+003
n-Hexane	5.98e-002	1.14e+003
Cyclohexane	2.89e-002	5.36e+002
Other Hexanes	1.28e-001	2.42e+003
Heptanes	4.59e-002	1.01e+003
Methylcyclohexane	2.29e-002	4.96e+002
Benzene	9.97e-003	1.72e+002
Toluene	6.98e-003	1.42e+002
Xylenes	9.97e-004	2.33e+001
C8+ Heavies	1.70e-002	6.36e+002
Total Components	100.00	4.50e+005

DRY GAS STREAM

Temperature: 120.00 deg. F
Pressure: 764.70 psia
Flow Rate: 8.33e+006 scfh

Component	Conc. (vol%)	Loading (lb/hr)
Water	1.47e-002	5.83e+001
Carbon Dioxide	3.19e-001	3.08e+003
Hydrogen Sulfide	9.95e-004	7.45e+000
Nitrogen	1.31e+000	8.08e+003
Methane	8.05e+001	2.83e+005
Ethane	1.04e+001	6.86e+004

Propane 4.64e+000 4.49e+004
 Isobutane 6.09e-001 7.77e+003
 n-Butane 1.34e+000 1.71e+004
 Isopentane 2.99e-001 4.74e+003

n-Pentane 3.04e-001 4.81e+003
 n-Hexane 5.99e-002 1.13e+003
 Cyclohexane 2.89e-002 5.33e+002
 Other Hexanes 1.28e-001 2.42e+003
 Heptanes 4.59e-002 1.01e+003

Methylcyclohexane 2.29e-002 4.93e+002
 Benzene 9.57e-003 1.64e+002
 Toluene 6.60e-003 1.34e+002
 Xylenes 8.91e-004 2.08e+001
 C8+ Heavies 1.69e-002 6.31e+002

 Total Components 100.00 4.49e+005

LEAN GLYCOL STREAM

 Temperature: 120.00 deg. F
 Flow Rate: 2.00e+001 gpm

Component	Conc. (wt%)	Loading (lb/hr)

TEG	9.90e+001	1.11e+004
Water	1.00e+000	1.13e+002
Carbon Dioxide	2.61e-012	2.94e-010
Hydrogen Sulfide	3.61e-014	4.07e-012
Nitrogen	5.97e-013	6.72e-011
Methane	6.52e-018	7.34e-016
Ethane	6.51e-008	7.33e-006
Propane	6.31e-009	7.11e-007
Isobutane	1.04e-009	1.18e-007
n-Butane	2.45e-009	2.76e-007
Isopentane	1.33e-004	1.50e-002
n-Pentane	1.69e-004	1.91e-002
n-Hexane	6.04e-005	6.81e-003
Cyclohexane	7.87e-004	8.87e-002
Other Hexanes	2.02e-004	2.28e-002
Heptanes	9.13e-005	1.03e-002
Methylcyclohexane	9.75e-004	1.10e-001
Benzene	3.43e-003	3.86e-001
Toluene	6.23e-003	7.01e-001
Xylenes	3.36e-003	3.78e-001
C8+ Heavies	6.54e-003	7.36e-001

Total Components	100.00	1.13e+004

RICH GLYCOL STREAM

 Temperature: 120.00 deg. F
 Pressure: 764.70 psia
 Flow Rate: 2.22e+001 gpm
 NOTE: Stream has more than one phase.

Component	Conc. (wt%)	Loading (lb/hr)

TEG	9.00e+001	1.11e+004
Water	9.02e+000	1.11e+003
Carbon Dioxide	2.38e-002	2.94e+000
Hydrogen Sulfide	3.29e-004	4.07e-002
Nitrogen	5.40e-003	6.67e-001
Methane	1.77e-001	2.19e+001
Ethane	1.26e-001	1.55e+001
Propane	1.41e-001	1.75e+001
Isobutane	3.17e-002	3.92e+000
n-Butane	9.00e-002	1.11e+001
Isopentane	2.42e-002	2.99e+000
n-Pentane	3.09e-002	3.81e+000
n-Hexane	1.10e-002	1.36e+000
Cyclohexane	2.24e-002	2.77e+000
Other Hexanes	1.84e-002	2.28e+000
Heptanes	1.66e-002	2.06e+000
Methylcyclohexane	2.22e-002	2.74e+000
Benzene	6.25e-002	7.72e+000
Toluene	7.18e-002	8.87e+000
Xylenes	2.36e-002	2.92e+000
C8+ Heavies	4.94e-002	6.11e+000

Total Components	100.00	1.24e+004

FLASH TANK OFF GAS STREAM

 Temperature: 100.00 deg. F
 Pressure: 87.70 psia
 Flow Rate: 7.59e+002 scfh

Component	Conc. (vol%)	Loading (lb/hr)

Water	2.41e-001	8.69e-002
Carbon Dioxide	1.29e+000	1.13e+000
Hydrogen Sulfide	5.31e-003	3.62e-003
Nitrogen	1.09e+000	6.10e-001
Methane	6.16e+001	1.98e+001

Ethane 1.91e+001 1.15e+001
 Propane 1.01e+001 8.93e+000
 Isobutane 1.37e+000 1.59e+000
 n-Butane 3.20e+000 3.72e+000
 Isopentane 6.24e-001 9.01e-001

n-Pentane 6.66e-001 9.62e-001
 n-Hexane 1.23e-001 2.12e-001
 Cyclohexane 8.07e-002 1.36e-001
 Other Hexanes 2.63e-001 4.53e-001
 Heptanes 8.53e-002 1.71e-001

Methylcyclohexane 5.18e-002 1.02e-001
 Benzene 2.43e-002 3.80e-002
 Toluene 1.46e-002 2.70e-002
 Xylenes 1.43e-003 3.03e-003
 C8+ Heavies 1.66e-002 5.68e-002

 Total Components 100.00 5.04e+001

FLASH TANK GLYCOL STREAM

 Temperature: 100.00 deg. F
 Flow Rate: 2.21e+001 gpm

Component	Conc. (wt%)	Loading (lb/hr)

TEG	9.04e+001	1.11e+004
Water	9.05e+000	1.11e+003
Carbon Dioxide	1.46e-002	1.80e+000
Hydrogen Sulfide	3.01e-004	3.71e-002
Nitrogen	4.65e-004	5.72e-002
Methane	1.68e-002	2.07e+000
Ethane	3.28e-002	4.03e+000
Propane	6.93e-002	8.53e+000
Isobutane	1.90e-002	2.33e+000
n-Butane	6.01e-002	7.40e+000
Isopentane	1.70e-002	2.09e+000
n-Pentane	2.32e-002	2.85e+000
n-Hexane	9.33e-003	1.15e+000
Cyclohexane	2.14e-002	2.64e+000
Other Hexanes	1.48e-002	1.83e+000
Heptanes	1.53e-002	1.89e+000
Methylcyclohexane	2.15e-002	2.64e+000
Benzene	6.24e-002	7.68e+000
Toluene	7.19e-002	8.84e+000
Xylenes	2.37e-002	2.91e+000
C8+ Heavies	4.92e-002	6.05e+000

 Total Components 100.00 1.23e+004

REGENERATOR OVERHEADS STREAM

Temperature: 212.00 deg. F
 Pressure: 14.70 psia
 Flow Rate: 2.15e+004 scfh

Component	Conc. (vol%)	Loading (lb/hr)
Water	9.81e+001	1.00e+003
Carbon Dioxide	7.22e-002	1.80e+000
Hydrogen Sulfide	1.92e-003	3.71e-002
Nitrogen	3.60e-003	5.72e-002
Methane	2.27e-001	2.07e+000
Ethane	2.37e-001	4.03e+000
Propane	3.41e-001	8.53e+000
Isobutane	7.08e-002	2.33e+000
n-Butane	2.25e-001	7.40e+000
Isopentane	5.07e-002	2.07e+000
n-Pentane	6.93e-002	2.83e+000
n-Hexane	2.34e-002	1.14e+000
Cyclohexane	5.34e-002	2.55e+000
Other Hexanes	3.69e-002	1.80e+000
Heptanes	3.30e-002	1.87e+000
Methylcyclohexane	4.55e-002	2.53e+000
Benzene	1.65e-001	7.30e+000
Toluene	1.56e-001	8.14e+000
Xylenes	4.21e-002	2.53e+000
C8+ Heavies	5.50e-002	5.31e+000
Total Components	100.00	1.07e+003

CONDENSER VENT GAS STREAM

Temperature: 110.00 deg. F
 Pressure: 13.10 psia
 Flow Rate: 3.62e+002 scfh

Component	Conc. (vol%)	Loading (lb/hr)
Water	9.80e+000	1.68e+000
Carbon Dioxide	4.20e+000	1.76e+000
Hydrogen Sulfide	1.06e-001	3.45e-002
Nitrogen	2.14e-001	5.72e-002
Methane	1.35e+001	2.06e+000
Ethane	1.40e+001	4.01e+000
Propane	1.99e+001	8.37e+000

Isobutane 4.05e+000 2.24e+000
 n-Butane 1.26e+001 7.00e+000
 Isopentane 2.62e+000 1.80e+000

n-Pentane 3.55e+000 2.44e+000
 n-Hexane 9.70e-001 7.97e-001
 Cyclohexane 1.95e+000 1.57e+000
 Other Hexanes 1.68e+000 1.38e+000
 Heptanes 8.74e-001 8.36e-001

Methylcyclohexane 1.20e+000 1.12e+000
 Benzene 5.58e+000 4.16e+000
 Toluene 2.94e+000 2.59e+000
 Xylenes 2.75e-001 2.78e-001
 C8+ Heavies 7.70e-003 1.25e-002

 Total Components 100.00 4.42e+001

CONDENSER PRODUCED WATER STREAM

 Temperature: 110.00 deg. F
 Flow Rate: 2.00e+000 gpm

Component	Conc. (wt%)	Loading (lb/hr)	(ppm)
Water	9.99e+001	1.00e+003	999318.
Carbon Dioxide	3.65e-003	3.65e-002	37.
Hydrogen Sulfide	2.31e-004	2.31e-003	2.
Nitrogen	2.89e-006	2.89e-005	0.
Methane	2.06e-004	2.06e-003	2.
Ethane	4.67e-004	4.68e-003	5.
Propane	9.27e-004	9.27e-003	9.
Isobutane	1.37e-004	1.37e-003	1.
n-Butane	5.74e-004	5.74e-003	6.
Isopentane	1.06e-004	1.06e-003	1.
n-Pentane	1.55e-004	1.55e-003	2.
n-Hexane	4.27e-005	4.27e-004	0.
Cyclohexane	4.90e-004	4.91e-003	5.
Other Hexanes	5.90e-005	5.90e-004	1.
Heptanes	2.51e-005	2.51e-004	0.
Methylcyclohexane	1.69e-004	1.69e-003	2.
Benzene	3.86e-002	3.86e-001	386.
Toluene	2.01e-002	2.01e-001	201.
Xylenes	2.32e-003	2.32e-002	23.
C8+ Heavies	2.31e-007	2.31e-006	0.

Total Components	100.00	1.00e+003	1000000.

CONDENSER RECOVERED OIL STREAM

Temperature: 110.00 deg. F

Flow Rate: 4.97e-002 gpm

Component	Conc. (wt%)	Loading (lb/hr)
Water	3.79e-002	8.02e-003
Carbon Dioxide	1.52e-002	3.22e-003
Hydrogen Sulfide	1.20e-003	2.55e-004
Nitrogen	1.70e-004	3.59e-005
Methane	6.22e-003	1.32e-003
Ethane	7.13e-002	1.51e-002
Propane	7.31e-001	1.55e-001
Isobutane	4.06e-001	8.59e-002
n-Butane	1.84e+000	3.89e-001
Isopentane	1.29e+000	2.72e-001
n-Pentane	1.84e+000	3.90e-001
n-Hexane	1.63e+000	3.44e-001
Cyclohexane	4.60e+000	9.73e-001
Other Hexanes	2.01e+000	4.25e-001
Heptanes	4.91e+000	1.04e+000
Methylcyclohexane	6.65e+000	1.41e+000
Benzene	1.30e+001	2.76e+000
Toluene	2.53e+001	5.35e+000
Xylenes	1.06e+001	2.23e+000
C8+ Heavies	2.51e+001	5.30e+000
Total Components	100.00	2.11e+001

This content is from the eCFR and is authoritative but unofficial.



Displaying title 40, up to date as of 9/05/2023. Title 40 was last amended 9/05/2023.

Title 40 – Protection of Environment
Chapter I – Environmental Protection Agency
Subchapter C – Air Programs
Part 98 – Mandatory Greenhouse Gas Reporting
Subpart A – General Provision

⊙ **Table A-1 to Subpart A of Part 98 – Global Warming Potentials**

[100-Year Time Horizon]

Name	CAS No.	Chemical formula	Global warming potential (100 yr.)
------	---------	------------------	------------------------------------

Chemical-Specific GWPs

Carbon dioxide	124-38-9	CO ₂	1
Methane	74-82-8	CH ₄	^a 25
Nitrous oxide	10024-97-2	N ₂ O	^a 298

Fully Fluorinated GHGs

Sulfur hexafluoride	2551-62-4	SF ₆	^a 22,800
Trifluoromethyl sulphur pentafluoride	373-80-8	SF ₅ CF ₃	17,700
Nitrogen trifluoride	7783-54-2	NF ₃	17,200
PFC-14 (Perfluoromethane)	75-73-0	CF ₄	^a 7,390
PFC-116 (Perfluoroethane)	76-16-4	C ₂ F ₆	^a 12,200
PFC-218 (Perfluoropropane)	76-19-7	C ₃ F ₈	^a 8,830
Perfluorocyclopropane	931-91-9	C-C ₃ F ₆	17,340
PFC-3-1-10 (Perfluorobutane)	355-25-9	C ₄ F ₁₀	^a 8,860
PFC-318 (Perfluorocyclobutane)	115-25-3	C-C ₄ F ₈	^a 10,300
PFC-4-1-12 (Perfluoropentane)	678-26-2	C ₅ F ₁₂	^a 9,160
PFC-5-1-14 (Perfluorohexane, FC-72)	355-42-0	C ₆ F ₁₄	^a 9,300
PFC-6-1-12	335-57-9	C ₇ F ₁₆ ; CF ₃ (CF ₂) ₅ CF ₃	^b 7,820

This content is from the eCFR and is authoritative but unofficial.



Displaying title 40, up to date as of 6/06/2023. Title 40 was last amended 6/06/2023.

Title 40 – Protection of Environment
Chapter I – Environmental Protection Agency
Subchapter C – Air Programs
Part 98 – Mandatory Greenhouse Gas Reporting
Subpart C – General Stationary Fuel Combustion Sources

Table C-1 to Subpart C of Part 98—Default CO₂ Emission Factors and High Heat Values for Various Types of FuelDefault CO₂ Emission Factors and High Heat Values for Various Types of Fuel

Fuel type	Default high heat value	Default CO ₂ emission factor
Coal and coke	mmBtu/short ton	kg CO ₂ /mmBtu
Anthracite	25.09	103.69
Bituminous	24.93	93.28
Subbituminous	17.25	97.17
Lignite	14.21	97.72
Coal Coke	24.80	113.67
Mixed (Commercial sector)	21.39	94.27
Mixed (Industrial coking)	26.28	93.90
Mixed (Industrial sector)	22.35	94.67
Mixed (Electric Power sector)	19.73	95.52
Natural gas	mmBtu/scf	kg CO ₂ /mmBtu
(Weighted U.S. Average)	1.026×10^{-3}	53.06
Petroleum products—liquid	mmBtu/gallon	kg CO ₂ /mmBtu
Distillate Fuel Oil No. 1	0.139	73.25
Distillate Fuel Oil No. 2	0.138	73.96
Distillate Fuel Oil No. 4	0.146	75.04
Residual Fuel Oil No. 5	0.140	72.93
Residual Fuel Oil No. 6	0.150	75.10
Used Oil	0.138	74.00
Kerosene	0.135	75.20
Liquefied petroleum gases (LPG) ¹	0.092	61.71

This content is from the eCFR and is authoritative but unofficial.



Displaying title 40, up to date as of 6/06/2023. Title 40 was last amended 6/06/2023.

Title 40 – Protection of Environment
Chapter I – Environmental Protection Agency
Subchapter C – Air Programs
Part 98 – Mandatory Greenhouse Gas Reporting
Subpart C – General Stationary Fuel Combustion Sources

Table C-2 to Subpart C of Part 98—Default CH₄ and N₂O Emission Factors for Various Types of Fuel

Fuel type	Default CH ₄ emission factor (kg CH ₄ /mmBtu)	Default N ₂ O emission factor (kg N ₂ O/mmBtu)
Coal and Coke (All fuel types in Table C-1)	1.1×10^{-2}	1.6×10^{-3}
Natural Gas	1.0×10^{-3}	1.0×10^{-4}
Petroleum Products (All fuel types in Table C-1)	3.0×10^{-3}	6.0×10^{-4}
Fuel Gas	3.0×10^{-3}	6.0×10^{-4}
Other Fuels—Solid	3.2×10^{-2}	4.2×10^{-3}
Blast Furnace Gas	2.2×10^{-5}	1.0×10^{-4}
Coke Oven Gas	4.8×10^{-4}	1.0×10^{-4}
Biomass Fuels—Solid (All fuel types in Table C-1, except wood and wood residuals)	3.2×10^{-2}	4.2×10^{-3}
Wood and wood residuals	7.2×10^{-3}	3.6×10^{-3}
Biomass Fuels—Gaseous (All fuel types in Table C-1)	3.2×10^{-3}	6.3×10^{-4}
Biomass Fuels—Liquid (All fuel types in Table C-1)	1.1×10^{-3}	1.1×10^{-4}

Note: Those employing this table are assumed to fall under the IPCC definitions of the “Energy Industry” or “Manufacturing Industries and Construction”. In all fuels except for coal the values for these two categories are identical. For coal combustion, those who fall within the IPCC “Energy Industry” category may employ a value of 1g of CH₄/mmBtu.

[78 FR 71952, Nov. 29, 2013, as amended at 81 FR 89252, Dec. 9, 2016]

Section 7

Subsection 2 – Information Used to Determine Emissions for All Other Units Since Acquisition

For clarity, this Subsection 2 contains information used to determine emissions for all other units at this facility that were not affected by this application (i.e. all units except for Units 1, 2, 6, 7, 8, 9, 10, 3a, 3b, T-007, LOAD_SLOP, ECD, Flare , F-001, and MALF). For information pertinent to the units added or modified with this application, please refer to Subsection 1.

Table 3.1-2a. EMISSION FACTORS FOR CRITERIA POLLUTANTS AND GREENHOUSE GASES FROM STATIONARY GAS TURBINES

Emission Factors ^a - Uncontrolled				
Pollutant	Natural Gas-Fired Turbines ^b		Distillate Oil-Fired Turbines ^d	
	(lb/MMBtu) ^c (Fuel Input)	Emission Factor Rating	(lb/MMBtu) ^c (Fuel Input)	Emission Factor Rating
CO ₂ ^f	110	A	157	A
N ₂ O	0.003 ^g	E	ND	NA
Lead	ND	NA	1.4 E-05	C
SO ₂	0.94S ^h	B	1.01S ^h	B
Methane	8.6 E-03	C	ND	NA
VOC	2.1 E-03	D	4.1 E-04 ^j	E
TOC ^k	1.1 E-02	B	4.0 E-03 ^l	C
PM (condensable)	4.7 E-03 ^l	C	7.2 E-03 ^l	C
PM (filterable)	1.9 E-03 ^l	C	4.3 E-03 ^l	C
PM (total)	6.6 E-03 ^l	C	1.2 E-02 ^l	C

^a Factors are derived from units operating at high loads (≥ 80 percent load) only. For information on units operating at other loads, consult the background report for this chapter (Reference 16), available at “www.epa.gov/ttn/chief”. ND = No Data, NA = Not Applicable.

^b SCCs for natural gas-fired turbines include 2-01-002-01, 2-02-002-01 & 03, and 2-03-002-02 & 03.

^c Emission factors based on an average natural gas heating value (HHV) of 1020 Btu/scf at 60°F. To convert from (lb/MMBtu) to (lb/10⁶ scf), multiply by 1020. Similarly, these emission factors can be converted to other natural gas heating values.

^d SCCs for distillate oil-fired turbines are 2-01-001-01, 2-02-001-01, 2-02-001-03, and 2-03-001-02.

^e Emission factors based on an average distillate oil heating value of 139 MMBtu/10³ gallons. To convert from (lb/MMBtu) to (lb/10³ gallons), multiply by 139.

^f Based on 99.5% conversion of fuel carbon to CO₂ for natural gas and 99% conversion of fuel carbon to CO₂ for distillate oil. CO₂ (Natural Gas) [lb/MMBtu] = (0.0036 scf/Btu)(%CON)(C)(D), where %CON = weight percent conversion of fuel carbon to CO₂, C = carbon content of fuel by weight, and D = density of fuel. For natural gas, C is assumed at 75%, and D is assumed at 4.1 E+04 lb/10⁶scf. For distillate oil, CO₂ (Distillate Oil) [lb/MMBtu] = (26.4 gal/MMBtu) (%CON)(C)(D), where C is assumed at 87%, and the D is assumed at 6.9 lb/gallon.

^g Emission factor is carried over from the previous revision to AP-42 (Supplement B, October 1996) and is based on limited source tests on a single turbine with water-steam injection (Reference 5).

^h All sulfur in the fuel is assumed to be converted to SO₂. S = percent sulfur in fuel. Example, if sulfur content in the fuel is 3.4 percent, then S = 3.4. If S is not available, use 3.4 E-03 lb/MMBtu for natural gas turbines, and 3.3 E-02 lb/MMBtu for distillate oil turbines (the equations are more accurate).

^j VOC emissions are assumed equal to the sum of organic emissions.

^k Pollutant referenced as THC in the gathered emission tests. It is assumed as TOC, because it is based on EPA Test Method 25A.

^l Emission factors are based on combustion turbines using water-steam injection.

Table 13.2.2-1. TYPICAL SILT CONTENT VALUES OF SURFACE MATERIAL ON INDUSTRIAL UNPAVED ROADS^a

Industry	Road Use Or Surface Material	Plant Sites	No. Of Samples	Silt Content (%)	
				Range	Mean
Copper smelting	Plant road	1	3	16 - 19	17
Iron and steel production	Plant road	19	135	0.2 - 19	6.0
Sand and gravel processing	Plant road	1	3	4.1 - 6.0	4.8
Stone quarrying and processing	Material storage area	1	1	-	7.1
	Plant road	2	10	2.4 - 16	10
Taconite mining and processing	Haul road to/from pit	4	20	5.0-15	8.3
	Service road	1	8	2.4 - 7.1	4.3
Western surface coal mining	Haul road to/from pit	1	12	3.9 - 9.7	5.8
	Haul road to/from pit	3	21	2.8 - 18	8.4
Construction sites	Plant road	2	2	4.9 - 5.3	5.1
	Scrapper route	3	10	7.2 - 25	17
	Haul road (freshly graded)	2	5	18 - 29	24
Lumber sawmills	Scrapper routes	7	20	0.56-23	8.5
Municipal solid waste landfills	Log yards	2	2	4.8-12	8.4
	Disposal routes	4	20	2.2 - 21	6.4

^aReferences 1,5-15.

The following empirical expressions may be used to estimate the quantity in pounds (lb) of size-specific particulate emissions from an unpaved road, per vehicle mile traveled (VMT):

For vehicles traveling on unpaved surfaces at industrial sites, emissions are estimated from the following equation:

$$E = k (s/12)^a (W/3)^b \quad (1a)$$

and, for vehicles traveling on publicly accessible roads, dominated by light duty vehicles, emissions may be estimated from the following:

$$E = \frac{k (s/12)^a (S/30)^d}{(M/0.5)^c} - C \quad (1b)$$

where k , a , b , c and d are empirical constants (Reference 6) given below and

E = size-specific emission factor (lb/VMT)

s = surface material silt content (%)

W = mean vehicle weight (tons)

M = surface material moisture content (%)

S = mean vehicle speed (mph)

C = emission factor for 1980's vehicle fleet exhaust, brake wear and tire wear.

The source characteristics s , W and M are referred to as correction parameters for adjusting the emission estimates to local conditions. The metric conversion from lb/VMT to grams (g) per vehicle kilometer traveled (VKT) is as follows:

$$1 \text{ lb/VMT} = 281.9 \text{ g/VKT}$$

The constants for Equations 1a and 1b based on the stated aerodynamic particle sizes are shown in Tables 13.2.2-2 and 13.2.2-4. The PM-2.5 particle size multipliers (k -factors) are taken from Reference 27.

Table 13.2.2-2. CONSTANTS FOR EQUATIONS 1a AND 1b

Constant	Industrial Roads (Equation 1a)			Public Roads (Equation 1b)		
	PM-2.5	PM-10	PM-30*	PM-2.5	PM-10	PM-30*
k (lb/VMT)	0.15	1.5	4.9	0.18	1.8	6.0
a	0.9	0.9	0.7	1	1	1
b	0.45	0.45	0.45	-	-	-
c	-	-	-	0.2	0.2	0.3
d	-	-	-	0.5	0.5	0.3
Quality Rating	B	B	B	B	B	B

*Assumed equivalent to total suspended particulate matter (TSP)

“-“ = not used in the emission factor equation

Table 13.2.2-2 also contains the quality ratings for the various size-specific versions of Equation 1a and 1b. The equation retains the assigned quality rating, if applied within the ranges of source conditions, shown in Table 13.2.2-3, that were tested in developing the equation:

Table 13.2.2-3. RANGE OF SOURCE CONDITIONS USED IN DEVELOPING EQUATION 1a AND 1b

Emission Factor	Surface Silt Content, %	Mean Vehicle Weight		Mean Vehicle Speed		Mean No. of Wheels	Surface Moisture Content, %
		Mg	ton	km/hr	mph		
Industrial Roads (Equation 1a)	1.8-25.2	1.8-260	2-290	8-69	5-43	4-17 ^a	0.03-13
Public Roads (Equation 1b)	1.8-35	1.4-2.7	1.5-3	16-88	10-55	4-4.8	0.03-13

^a See discussion in text.

As noted earlier, the models presented as Equations 1a and 1b were developed from tests of traffic on unpaved surfaces. Unpaved roads have a hard, generally nonporous surface that usually dries quickly after a rainfall or watering, because of traffic-enhanced natural evaporation. (Factors influencing how fast a road dries are discussed in Section 13.2.2.3, below.) The quality ratings given above pertain to the mid-range of the measured source conditions for the equation. A higher mean vehicle weight and a higher than normal traffic rate may be justified when performing a worst-case analysis of emissions from unpaved roads.

The emission factors for the exhaust, brake wear and tire wear of a 1980's vehicle fleet (C) was obtained from EPA's MOBILE6.2 model ²³. The emission factor also varies with aerodynamic size range

average uncontrolled conditions (but including natural mitigation) under the simplifying assumption that annual average emissions are inversely proportional to the number of days with measurable (more than 0.254 mm [0.01 inch]) precipitation:

$$E_{\text{ext}} = E [(365 - P)/365] \quad (2)$$

where:

E_{ext} = annual size-specific emission factor extrapolated for natural mitigation, lb/VMT

E = emission factor from Equation 1a or 1b

P = number of days in a year with at least 0.254 mm (0.01 in) of precipitation (see below)

Figure 13.2.2-1 gives the geographical distribution for the mean annual number of “wet” days for the United States.

Equation 2 provides an estimate that accounts for precipitation on an annual average basis for the purpose of inventorying emissions. It should be noted that Equation 2 does not account for differences in the temporal distributions of the rain events, the quantity of rain during any event, or the potential for the rain to evaporate from the road surface. In the event that a finer temporal and spatial resolution is desired for inventories of public unpaved roads, estimates can be based on a more complex set of assumptions. These assumptions include:

1. The moisture content of the road surface material is increased in proportion to the quantity of water added;
2. The moisture content of the road surface material is reduced in proportion to the Class A pan evaporation rate;
3. The moisture content of the road surface material is reduced in proportion to the traffic volume; and
4. The moisture content of the road surface material varies between the extremes observed in the area. The CHIEF Web site (<http://www.epa.gov/ttn/chief/ap42/ch13/related/c13s02-2.html>) has a file which contains a spreadsheet program for calculating emission factors which are temporally and spatially resolved. Information required for use of the spreadsheet program includes monthly Class A pan evaporation values, hourly meteorological data for precipitation, humidity and snow cover, vehicle traffic information, and road surface material information.

It is emphasized that the simple assumption underlying Equation 2 and the more complex set of assumptions underlying the use of the procedure which produces a finer temporal and spatial resolution have not been verified in any rigorous manner. For this reason, the quality ratings for either approach should be downgraded one letter from the rating that would be applied to Equation 1.

13.2.2.3 Controls¹⁸⁻²²

A wide variety of options exist to control emissions from unpaved roads. Options fall into the following three groupings:

1. Vehicle restrictions that limit the speed, weight or number of vehicles on the road;

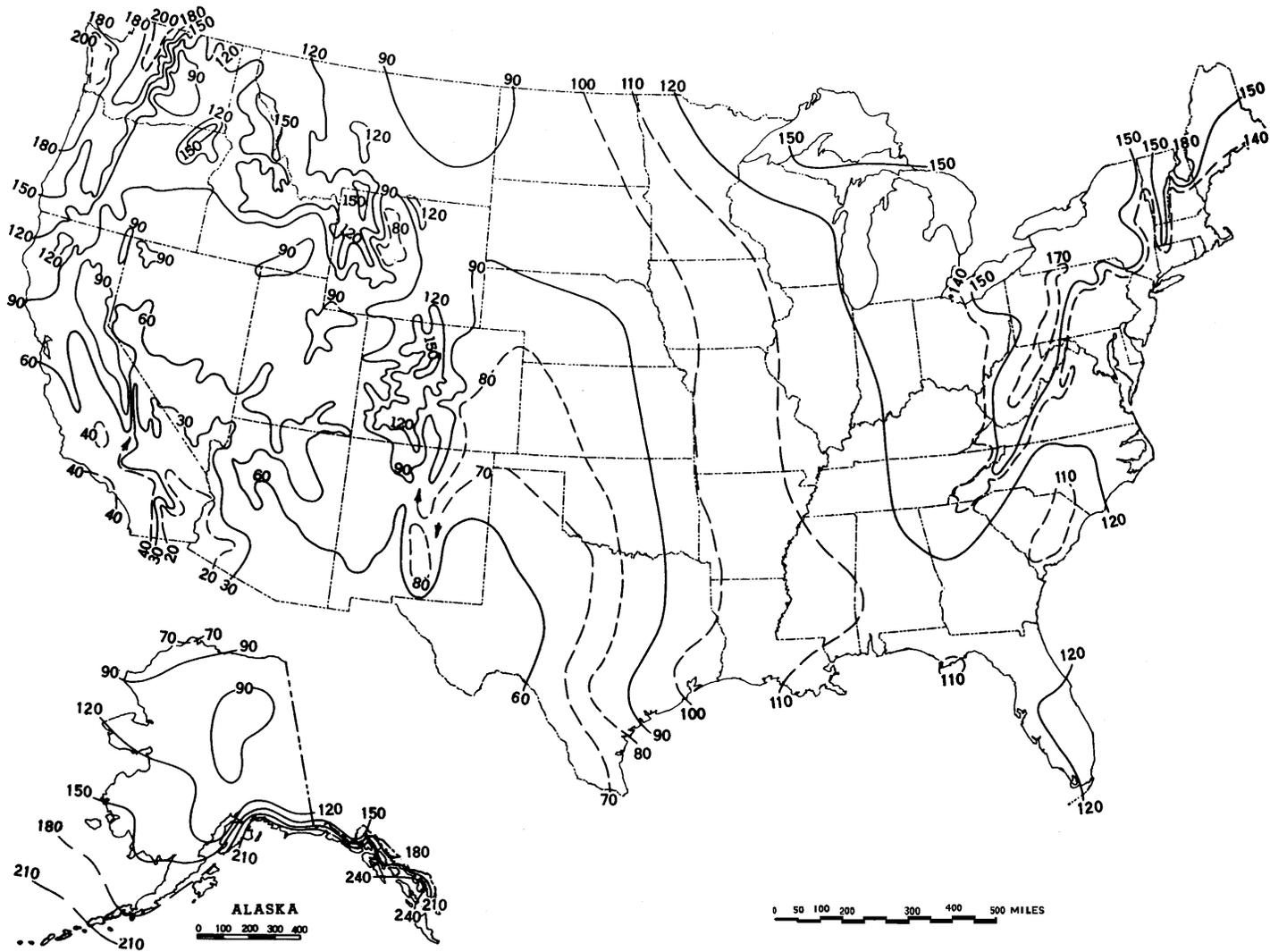


Figure 13.2.2-1. Mean number of days with 0.01 inch or more of precipitation in United States.

Since flares do not lend themselves to conventional emission testing techniques, only a few attempts have been made to characterize flare emissions. Recent EPA tests using propylene as flare gas indicated that efficiencies of 98 percent can be achieved when burning an offgas with at least 11,200 kJ/m³ (300 Btu/ft³). The tests conducted on steam-assisted flares at velocities as low as 39.6 meters per minute (m/min) (130 ft/min) to 1140 m/min (3750 ft/min), and on air-assisted flares at velocities of 180 m/min (617 ft/min) to 3960 m/min (13,087 ft/min) indicated that variations in incoming gas flow rates have no effect on the combustion efficiency. Flare gases with less than 16,770 kJ/m³ (450 Btu/ft³) do not smoke.

Table 13.5-1 presents flare emission factors, and Table 13.5-2 presents emission composition data obtained from the EPA tests.¹ Crude propylene was used as flare gas during the tests. Methane was a major fraction of hydrocarbons in the flare emissions, and acetylene was the dominant intermediate hydrocarbon species. Many other reports on flares indicate that acetylene is always formed as a stable intermediate product. The acetylene formed in the combustion reactions may react further with hydrocarbon radicals to form polyacetylenes followed by polycyclic hydrocarbons.²

In flaring waste gases containing no nitrogen compounds, NO is formed either by the fixation of atmospheric nitrogen (N) with oxygen (O) or by the reaction between the hydrocarbon radicals present in the combustion products and atmospheric nitrogen, by way of the intermediate stages, HCN, CN, and OCN.² Sulfur compounds contained in a flare gas stream are converted to SO₂ when burned. The amount of SO₂ emitted depends directly on the quantity of sulfur in the flared gases.

Table 13.5-1 (English Units). EMISSION FACTORS FOR FLARE OPERATIONS^a

EMISSION FACTOR RATING: B

Component	Emission Factor (lb/10 ⁶ Btu)
Total hydrocarbons ^b	0.14
Carbon monoxide	0.37
Nitrogen oxides	0.068
Soot ^c	0 - 274

^a Reference 1. Based on tests using crude propylene containing 80% propylene and 20% propane.

^b Measured as methane equivalent.

^c Soot in concentration values: nonsmoking flares, 0 micrograms per liter (µg/L); lightly smoking flares, 40 µg/L; average smoking flares, 177 µg/L; and heavily smoking flares, 274 µg/L.

GRI-HAPCalc® 3.01
Truck Loading Report

Facility ID:	SOUTH CARLSBAD	Notes:
Operation Type:	COMPRESSOR STATION	
Facility Name:	SOUTH CARLSBAD	
User Name:		
Units of Measure:	U.S. STANDARD	

Note: Emissions less than 5.00E-09 tons (or tonnes) per year are considered insignificant and are treated as zero. These emissions are indicated on the report with a "0". Emissions between 5.00E-09 and 5.00E-05 tons (or tonnes) per year are represented on the report with "0.0000".

Truck Loading Unit

Unit Name: LOAD

Annual Throughput: 69,350.00 bbl/yr Control Efficiency: 0.00 %
 Ambient Temperature: 74.00 °F
 Loading Factor: 0
 Type of Loading: 0.6 - Submerged loading, dedicated service
 Is Truck Required to Pass Annual Inspection?: NO
 Are Vapors Routed to Control Device?: NO

User Concentration Inputs

<u>Chemical Name</u>	<u>Feed Wt %</u>
Ethane	0.0000
Propane	0.0000
Butane	3.7430
Pentane	32.4470
C6+	63.8100
n-Hexane	8.7170
Benzene	1.5710
Toluene	1.7570
Ethylbenzene	0.2380
Xylenes(m,p,o)	0.5100
2,2,4-Trimethylpentane	0.0000

Calculated Emissions (ton/yr)

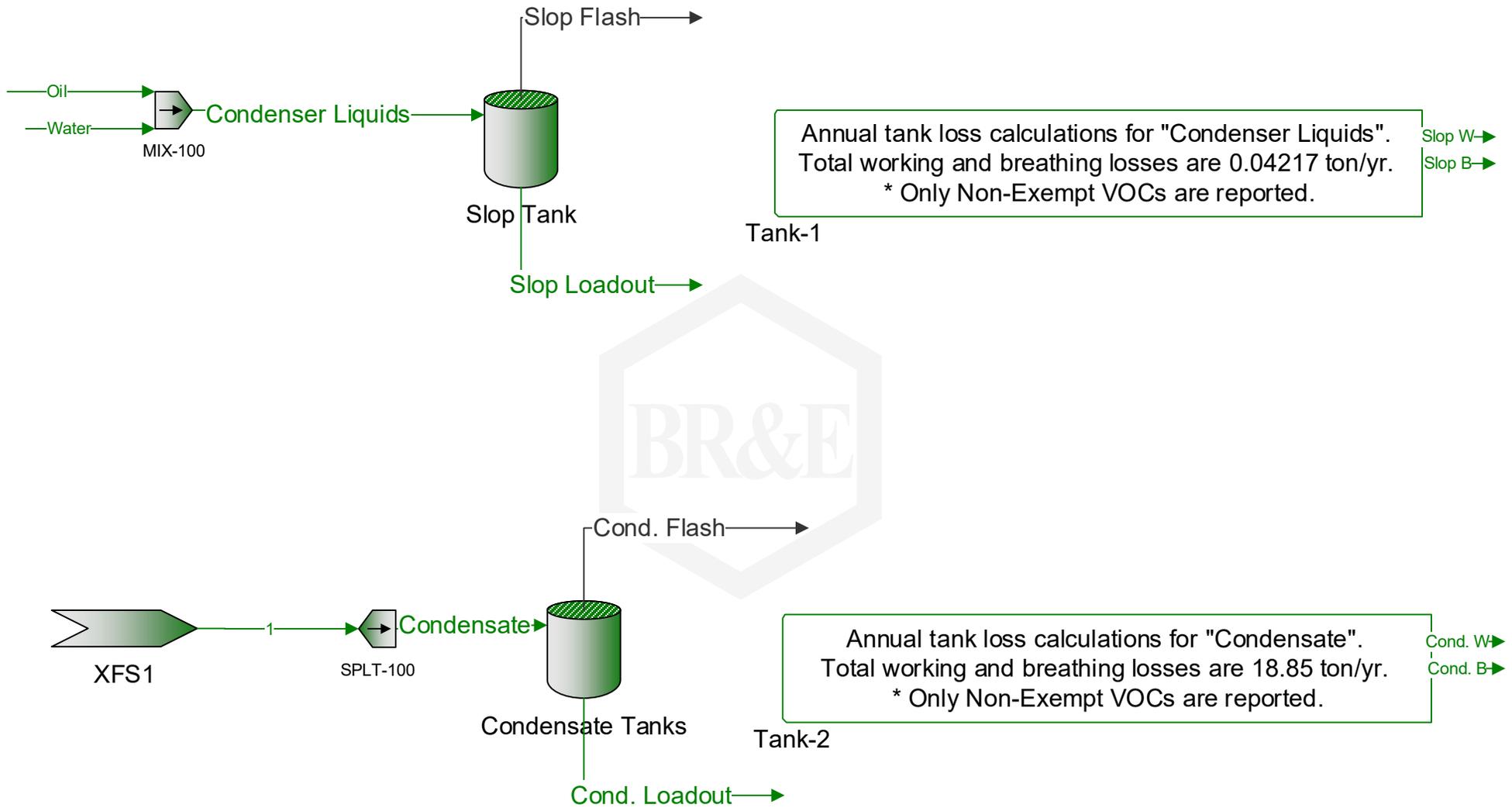
<u>HAPs</u>	<u>Chemical Name</u>	<u>Emissions</u>
	Benzene	0.0433
	Toluene	0.0144
	Ethylbenzene	0.0007
	Xylenes(m,p,o)	0.0012
	n-Hexane	0.3880
Total		0.4476

Criteria Pollutants

NMHC	9.8020
NMEHC	9.8020

Other Pollutants

Butane	2.0418
Pentane	4.9199
C6+	2.8402



Process Streams		Cond. B	Cond. W	Slop B	Slop W
Composition		Status: Solved	Solved	Solved	Solved
Phase: Vapor	From Block:	--	--	--	--
	To Block:	--	--	--	--
Mass Flow		lb/h	lb/h	lb/h	lb/h
Hydrogen Sulfide		0	0	0	0
Nitrogen		0	0	0	0
Carbon Dioxide		4.81714E-12	5.06326E-12	9.90791E-16	3.56382E-15
Methane		8.17987E-14	8.59780E-14	1.68244E-17	6.05164E-17
Ethane		5.61920E-08	5.90630E-08	1.15576E-11	4.15720E-11
Propane		0.000295640	0.000310745	6.08073E-08	2.18720E-07
i-Butane		0.0211533	0.0222341	4.35082E-06	1.56497E-05
n-Butane		0.562185	0.590909	0.000115631	0.000415917
2,2-Dimethylpropane		0.0126659	0.0133130	2.60512E-06	9.37047E-06
i-Pentane		0.593853	0.624194	0.000122144	0.000439345
n-Pentane		0.536838	0.564267	0.000110417	0.000397164
2,2-Dimethylbutane		0.00518274	0.00544754	1.06599E-06	3.83430E-06
Cyclopentane		0	0	0	0
2,3-Dimethylbutane		0.0363321	0.0381884	7.47281E-06	2.68793E-05
2-Methylpentane		0.0838566	0.0881411	1.72477E-05	6.20389E-05
3-Methylpentane		0.0440194	0.0462685	9.05393E-06	3.25665E-05
n-Hexane		0.0766362	0.0805517	1.57626E-05	5.66971E-05
Methylcyclopentane		0.0352034	0.0370020	7.24065E-06	2.60442E-05
Benzene		0.00854433	0.00898088	1.75740E-06	6.32127E-06
Cyclohexane		0.0239256	0.0251480	4.92102E-06	1.77006E-05
2-Methylhexane		0.00606139	0.00637108	1.24671E-06	4.48434E-06
3-Methylhexane		0.00676702	0.00711276	1.39184E-06	5.00638E-06
2,2,4-Trimethylpentane		0	0	0	0
n-Heptane		0.0251696	0.0264556	5.17689E-06	1.86210E-05
Methylcyclohexane		0.0137544	0.0144572	2.82902E-06	1.01758E-05
Toluene		0.00287912	0.00302623	5.92179E-07	2.13004E-06
n-Octane		0.00615584	0.00647036	1.26614E-06	4.55422E-06
Ethylbenzene		0.000131317	0.000138026	2.70093E-08	9.71510E-08
m-Xylene		0.000120060	0.000126194	2.46939E-08	8.88227E-08
p-Xylene		0.000125494	0.000131906	2.58117E-08	9.28432E-08
o-Xylene		0	0	0	0
n-Nonane		0.000544887	0.000572726	1.12073E-07	4.03119E-07

Process Streams		Cond. B	Cond. W	Slop B	Slop W
Properties		Status: Solved	Solved	Solved	Solved
Phase: Vapor	From Block:	--	--	--	--
	To Block:	--	--	--	--
Property	Units				
Temperature	°F	82.6768	82.6768	82.6768	82.6768
Pressure	psia	9.75052	9.75052	0.568983	0.568983
Mole Fraction Vapor	%	100	100	100	100
Mole Fraction Light Liquid	%	0	0	0	0
Mole Fraction Heavy Liquid	%	0	0	0	0
Molecular Weight	lb/lbmol	69.6863	69.6863	19.4093	19.4093
Mass Density	lb/ft^3	0.119713	0.119713	0.00189852	0.00189852
Std Vapor Volumetric Flow	MMSCFD	0.000274772	0.000288811	2.09476E-06	7.53472E-06
Std Liquid Volumetric Flow	sgpm	0.00673106	0.00707497	9.44417E-06	3.39702E-05
Compressibility		0.975200	0.975200	0.999435	0.999435
Specific Gravity		2.40609	2.40609	0.670154	0.670154
API Gravity					
Mass Cp	Btu/(lb*°F)	0.400239	0.400239	0.444343	0.444343
Ideal Gas CpCv Ratio		1.07725	1.07725	1.29931	1.29931
Dynamic Viscosity	cP	0.00719181	0.00719181	0.0100547	0.0100547
Kinematic Viscosity	cSt	3.75039	3.75039	330.622	330.622
Net Ideal Gas Heating Value	Btu/ft^3	3576.44	3576.44	96.4902	96.4902
Net Liquid Heating Value	Btu/lb	19326.7	19326.7	914.987	914.987
Gross Ideal Gas Heating Value	Btu/ft^3	3867.34	3867.34	153.291	153.291
Gross Liquid Heating Value	Btu/lb	20911.4	20911.4	2025.59	2025.59

FESCO, Ltd.
105 Medical Dr. - Ozona, Texas 76943

For: Enterprise Field Services, LLC
 P. O. Box 1508
 Carlsbad, New Mexico 88221

Sample: South Carlsbad Gas Plant
 Inlet to the Plant Gas
 Spot Gas Sample @ 280 psig & 53 °F

Equipment: Normal Operating Conditions as per Customer
 Date Sampled: 01/08/2020 @ 10:59 CST

Job Number: 200013.104

COC No.: 3560

CHROMATOGRAPH EXTENDED ANALYSIS - GPA 2286

COMPONENT	MOL%	GPM
Hydrogen Sulfide*	< 0.001	
Nitrogen	1.313	
Carbon Dioxide	0.319	
Methane	80.464	
Ethane	10.387	2.771
Propane	4.642	1.276
Isobutane	0.609	0.199
n-Butane	1.341	0.422
2-2 Dimethylpropane	0.001	0.000
Isopentane	0.299	0.109
n-Pentane	0.304	0.110
Hexanes	0.163	0.067
Heptanes Plus	<u>0.158</u>	<u>0.062</u>
Totals	100.000	5.016

Computed Real Characteristics Of Heptanes Plus:

Specific Gravity ----- 3.254 (Air=1)
 Molecular Weight ----- 93.94
 Gross Heating Value ----- 4831 BTU/CF

Computed Real Characteristics Of Total Sample:

Specific Gravity ----- 0.708 (Air=1)
 Compressibility (Z) ----- 0.9967
 Molecular Weight ----- 20.44
 Gross Heating Value
 Dry Basis ----- 1217 BTU/CF
 Saturated Basis ----- 1196 BTU/CF

*Hydrogen Sulfide tested on location by: Stain Tube Method (GPA 2377)
 0.016 Gr/100 CF, 0.3 PPMV or <0.0001 Mol%

Detector Tube: Gastec 4LT 0.05 to 4.0 ppm (Meas. Range)

Base Conditions: 14.650 PSI & 60 Deg F

Sampled By: (08)McCollum
 Analyst: JBM
 Processor: BMc
 Cylinder ID: X-0933

Certified: FESCO, Ltd. - Ozona, Texas

Tom Anderson 325-392-3773

CHROMATOGRAPH EXTENDED ANALYSIS - GPA 2286
TOTAL REPORT

COMPONENT	MOL %	GPM	WT %
Hydrogen Sulfide*	< 0.001		< 0.001
Nitrogen	1.313		1.799
Carbon Dioxide	0.319		0.687
Methane	80.464		63.138
Ethane	10.387	2.771	15.277
Propane	4.642	1.276	10.012
Isobutane	0.609	0.199	1.731
n-Butane	1.341	0.422	3.812
2,2 Dimethylpropane	0.001	0.000	0.004
Isopentane	0.299	0.109	1.055
n-Pentane	0.304	0.110	1.073
2,2 Dimethylbutane	0.005	0.002	0.021
Cyclopentane	0.000	0.000	0.000
2,3 Dimethylbutane	0.018	0.007	0.076
2 Methylpentane	0.052	0.022	0.219
3 Methylpentane	0.028	0.011	0.118
n-Hexane	0.060	0.025	0.253
Methylcyclopentane	0.025	0.009	0.103
Benzene	0.010	0.003	0.038
Cyclohexane	0.029	0.010	0.119
2-Methylhexane	0.007	0.003	0.034
3-Methylhexane	0.008	0.004	0.039
2,2,4 Trimethylpentane	0.000	0.000	0.000
Other C7's	0.018	0.008	0.087
n-Heptane	0.013	0.006	0.064
Methylcyclohexane	0.023	0.009	0.110
Toluene	0.007	0.002	0.032
Other C8's	0.012	0.006	0.065
n-Octane	0.003	0.002	0.017
Ethylbenzene	0.000	0.000	0.000
M & P Xylenes	0.001	0.000	0.005
O-Xylene	0.000	0.000	0.000
Other C9's	0.002	0.001	0.012
n-Nonane	0.000	0.000	0.000
Other C10's	0.000	0.000	0.000
n-Decane	0.000	0.000	0.000
Undecanes (11)	<u>0.000</u>	<u>0.000</u>	<u>0.000</u>
Totals	100.000	5.016	100.000

Computed Real Characteristics Of Total Sample:

Specific Gravity -----	0.708	(Air=1)
Compressibility (Z) -----	0.9967	
Molecular Weight -----	20.44	
Gross Heating Value		
Dry Basis -----	1217	BTU/CF
Saturated Basis -----	1196	BTU/CF

Process Streams		SC Vapor
Composition		Status: Solved
Phase: Total	From Block:	V-8201
	To Block:	First Stage Compressor
Mole Fraction	%	
Hydrogen Sulfide	0	
Nitrogen	2.72040	
Carbon Dioxide	1.60514	
Methane	76.5858	
Ethane	10.1231	
Propane	5.38529	
i-Butane	0.666348	
n-Butane	1.56272	
2,2-Dimethylpropane	0.00998088	
i-Pentane	0.365680	
n-Pentane	0.382158	
2,2-Dimethylbutane	0.00396908	
Cyclopentane	0	
2,3-Dimethylbutane	0.0346373	
2-Methylpentane	0.0869974	
3-Methylpentane	0.0493657	
n-Hexane	0.100417	
Methylcyclopentane	0.0531306	
Benzene	0.0236183	
Cyclohexane	0.0480196	
2-Methylhexane	0.0125769	
3-Methylhexane	0.0144867	
2,2,4-Trimethylpentane	0	
n-Heptane	0.0661237	
Methylcyclohexane	0.0363511	
Toluene	0.0142309	
n-Octane	0.0284272	
Ethylbenzene	0.000866152	
m-Xylene	0.000846199	
p-Xylene	0.000852961	
o-Xylene	0	
n-Nonane	0.00366520	
n-Decane	0	
n-Undecane	0	

Customer	
Job ID	
Inquiry Number	
Run By Javier Marquez	Date Run 9-Jul-20

Engine Model CENTAUR 40-4700 CS/MD 80F MATCH	
Fuel Type SD NATURAL GAS	Water Injection NO
Engine Emissions Data REV. 1.2	

NOx EMISSIONS

CO EMISSIONS

UHC EMISSIONS

1	4111 HP	100.0% Load	Elev. 3075 ft	Rel. Humidity 60.0%	Temperature 20.0 Deg. F
	PPMvd at 15% O2		165.00	50.00	50.00
	ton/yr		112.54	20.76	11.89
	lbm/MMBtu (Fuel LHV)		0.661	0.122	0.070
	lbm/(MW-hr)		8.38	1.55	0.89
	(gas turbine shaft pwr) lbm/hr		25.69	4.74	2.71

2	3583 HP	100.0% Load	Elev. 3075 ft	Rel. Humidity 60.0%	Temperature 80.0 Deg. F
	PPMvd at 15% O2		165.00	50.00	50.00
	ton/yr		100.38	18.52	10.61
	lbm/MMBtu (Fuel LHV)		0.652	0.120	0.069
	lbm/(MW-hr)		8.58	1.58	0.91
	(gas turbine shaft pwr) lbm/hr		22.92	4.23	2.42

- Notes
- For short-term emission limits such as lbs/hr., Solar recommends using "worst c conditions specific to the application and the site conditions. Worst case for necessarily the same for another.
 - Solar's typical SoLoNOx warranty, for ppm values, is available for greater than and between 50% and 100% load for gas fuel, and between 65% and 100% load for the Centaur 40). An emission warranty for non-SoLoNOx equipment is available or -20 deg F and between 80% and 100% load.
 - Fuel must meet Solar standard fuel specification ES 9-98. Emissions are based composition, or, San Diego natural gas or equivalent.
 - If needed, Solar can provide Product Information Letters to address turbine ope warranty ranges, as well as non-warranted emissions of SO2, PM10/2.5, VOC, and
 - Solar can provide factory testing in San Diego to ensure the actual unit(s) mee the tolerances quoted. Pricing and schedule impact will be provided upon reque
 - Any emissions warranty is applicable only for steady-state conditions and does shut-down, malfunction, or transient event.

Solar Turbines

A Caterpillar Company

PREDICTED ENGINE PERFORMANCE

Customer	
Job ID	
Run By Javier Marquez	Date Run 9-Jul-20
Engine Performance Code REV. 4.20.1.25.13	Engine Performance Data REV. 2.1

Model CENTAUR 40-4700
Package Type CS/MD
Match 80F MATCH
Fuel System GAS
Fuel Type SD NATURAL GAS

DATA FOR MINIMUM PERFORMANCE

Elevation	feet	3075	
Inlet Loss	in H2O	3.5	
Exhaust Loss	in H2O	2.0	
Accessory on GP Shaft	HP	15.5	
		1	2
Engine Inlet Temperature	deg F	20.0	80.0
Relative Humidity	%	60.0	60.0
Driven Equipment Speed	RPM	15500	15500
Specified Load	HP	FULL	FULL
Net Output Power	HP	4111	3583
Fuel Flow	mmBtu/hr	38.90	35.14
Heat Rate	Btu/HP-hr	9462	9809
Therm Eff	%	26.891	25.938
Engine Exhaust Flow	lbm/hr	143144	126652
PT Exit Temperature	deg F	771	850
Exhaust Temperature	deg F	771	850

Fuel Gas Composition (Volume Percent)	Methane (CH4)	92.79
	Ethane (C2H6)	4.16
	Propane (C3H8)	0.84
	N-Butane (C4H10)	0.18
	N-Pentane (C5H12)	0.04
	Hexane (C6H14)	0.04
	Carbon Dioxide (CO2)	0.44
	Hydrogen Sulfide (H2S)	0.0001
	Nitrogen (N2)	1.51

Fuel Gas Properties	LHV (Btu/Scf)	939.2	Specific Gravity	0.5970	Wobbe Index at 60F	1215.6
---------------------	---------------	-------	------------------	--------	--------------------	--------

This performance was calculated with a basic inlet and exhaust system. Special noise silencers, special filters, heat recovery systems or cooling devices will Performance shown is "Expected" performance at the pressure drops stated, not g

Customer Enterprise	
Job ID S.Carlsbad	
Inquiry Number	
Run By Jose Guillen	Date Run 1-Sep-20

Engine Model CENTAUR 40-4700S CS/MD 80F MATCH	
Fuel Type SD NATURAL GAS	Water Injection NO
Engine Emissions Data REV. 0.1	

NOx EMISSIONS

CO EMISSIONS

UHC EMISSIONS

1	4329 HP	100.0% Load	Elev. 3070 ft	Rel. Humidity 60.0%	Temperature 0 Deg. F
----------	----------------	--------------------	----------------------	----------------------------	-----------------------------

PPMvd at 15% O2	25.00	50.00	25.00
ton/yr	17.64	21.48	6.15
lbm/MMBtu (Fuel LHV)	0.100	0.122	0.035
lbm/(MW-hr)	1.25	1.52	0.44
(gas turbine shaft pwr) lbm/hr	4.03	4.90	1.40

2	4056 HP	100.0% Load	Elev. 3070 ft	Rel. Humidity 60.0%	Temperature 40.0 Deg. F
----------	----------------	--------------------	----------------------	----------------------------	--------------------------------

PPMvd at 15% O2	25.00	50.00	25.00
ton/yr	16.54	20.14	5.77
lbm/MMBtu (Fuel LHV)	0.100	0.122	0.035
lbm/(MW-hr)	1.25	1.52	0.44
(gas turbine shaft pwr) lbm/hr	3.78	4.60	1.32

3	3666 HP	100.0% Load	Elev. 3070 ft	Rel. Humidity 60.0%	Temperature 80.0 Deg. F
----------	----------------	--------------------	----------------------	----------------------------	--------------------------------

PPMvd at 15% O2	25.00	50.00	25.00
ton/yr	15.19	18.50	5.30
lbm/MMBtu (Fuel LHV)	0.099	0.120	0.034
lbm/(MW-hr)	1.27	1.54	0.44
(gas turbine shaft pwr) lbm/hr	3.47	4.22	1.21

Notes

- For short-term emission limits such as lbs/hr., Solar recommends using "worst c conditions specific to the application and the site conditions. Worst case for necessarily the same for another.
- Solar's typical SoLoNOx warranty, for ppm values, is available for greater than and between 50% and 100% load for gas fuel, and between 65% and 100% load for the Centaur 40). An emission warranty for non-SoLoNOx equipment is available or -20 deg F and between 80% and 100% load.
- Fuel must meet Solar standard fuel specification ES 9-98. Emissions are based composition, or, San Diego natural gas or equivalent.
- If needed, Solar can provide Product Information Letters to address turbine ope warranty ranges, as well as non-warranted emissions of SO2, PM10/2.5, VOC, and
- Solar can provide factory testing in San Diego to ensure the actual unit(s) mee the tolerances quoted. Pricing and schedule impact will be provided upon reque
- Any emissions warranty is applicable only for steady-state conditions and does shut-down, malfunction, or transient event.

Customer Enterprise	
Job ID S.Carlsbad	
Inquiry Number	
Run By Jose Guillen	Date Run 1-Sep-20

Engine Model CENTAUR 40-4700S CS/MD 80F MATCH	
Fuel Type SD NATURAL GAS	Water Injection NO
Engine Emissions Data REV. 0.1	

NOx EMISSIONS

CO EMISSIONS

UHC EMISSIONS

4	3163 HP	100.0% Load	Elev. 3070 ft	Rel. Humidity 60.0%	Temperature 105.0 Deg. F
PPMvd at 15% O2	25.00	50.00	25.00		
ton/yr	13.55	16.50	4.72		
lbm/MMBtu (Fuel LHV)	0.097	0.118	0.034		
lbm/(MW-hr)	1.31	1.60	0.46		
(gas turbine shaft pwr)					
lbm/hr	3.09	3.77	1.08		

- Notes
1. For short-term emission limits such as lbs/hr., Solar recommends using "worst c conditions specific to the application and the site conditions. Worst case for necessarily the same for another.
 2. Solar's typical SoLoNOx warranty, for ppm values, is available for greater than and between 50% and 100% load for gas fuel, and between 65% and 100% load for the Centaur 40). An emission warranty for non-SoLoNOx equipment is available or -20 deg F and between 80% and 100% load.
 3. Fuel must meet Solar standard fuel specification ES 9-98. Emissions are based composition, or, San Diego natural gas or equivalent.
 4. If needed, Solar can provide Product Information Letters to address turbine ope warranty ranges, as well as non-warranted emissions of SO2, PM10/2.5, VOC, and
 5. Solar can provide factory testing in San Diego to ensure the actual unit(s) mee the tolerances quoted. Pricing and schedule impact will be provided upon reque
 6. Any emissions warranty is applicable only for steady-state conditions and does shut-down, malfunction, or transient event.

Customer Enterprise	
Job ID S.Carlsbad	
Run By Jose Guillen	Date Run 1-Sep-20
Engine Performance Code REV. 4.20.1.25.13	Engine Performance Data REV. 2.2

Model CENTAUR 40-4700S
Package Type CS/MD
Match 80F MATCH
Fuel System GAS
Fuel Type SD NATURAL GAS

DATA FOR NOMINAL PERFORMANCE

Elevation	feet	3070			
Inlet Loss	in H2O	4.0			
Exhaust Loss	in H2O	4.0			
Accessory on GP Shaft	HP	15.5			
		1	2	3	4
Engine Inlet Temperature	deg F	0	40.0	80.0	105.0
Relative Humidity	%	60.0	60.0	60.0	60.0
Driven Equipment Speed	RPM	15500	15500	15500	15042
Specified Load	HP	FULL	FULL	FULL	FULL
Net Output Power	HP	4329	4056	3666	3163
Fuel Flow	mmBtu/hr	40.20	37.80	35.10	31.87
Heat Rate	Btu/HP-hr	9286	9321	9574	10075
Therm Eff	%	27.400	27.299	26.575	25.255
Engine Exhaust Flow	lbm/hr	147450	138006	126500	115569
PT Exit Temperature	deg F	754	800	852	876
Exhaust Temperature	deg F	754	800	852	876

Fuel Gas Composition (Volume Percent)	Methane (CH4)	92.79
	Ethane (C2H6)	4.16
	Propane (C3H8)	0.84
	N-Butane (C4H10)	0.18
	N-Pentane (C5H12)	0.04
	Hexane (C6H14)	0.04
	Carbon Dioxide (CO2)	0.44
	Hydrogen Sulfide (H2S)	0.0001
	Nitrogen (N2)	1.51

Fuel Gas Properties	LHV (Btu/Scf)	939.2	Specific Gravity	0.5970	Wobbe Index at 60F	1215.6
---------------------	----------------------	--------------	-------------------------	---------------	---------------------------	---------------

This performance was calculated with a basic inlet and exhaust system. Special noise silencers, special filters, heat recovery systems or cooling devices will Performance shown is "Expected" performance at the pressure drops stated, not g

Notes 3070 FT

Annual Turbine Emissions TEST REPORT
ON
EXHAUST EMISSIONS
FROM

ONE NATURAL GAS FIRED TURBINE

AT THE
SOUTH CARLSBAD COMPRESSOR STATION
LOVING, NM

PREPARED FOR
ENTERPRISE PRODUCTS OPERATING

MAY 2010

Relient Emissions Testing, Inc
Project Number: 0023

APPENDIX

Summary of Results

Quality Assurance/Quality Control Summary

Example Calculations

Calibration Certifications

Data Logger Files

Summary of Results

Company: Enterprise Products Operating
Location: South Carlsbad Compressor Station
Source: Solar Centaur 40 S/N: 30010096
Engine Rating: 4500hp @ 15000RPM
Technician: RAT

Test Run Number	1	2	3	
Unit	2	2	2	
Date	4/20/2010	4/20/2010	4/20/2010	
Start Time	16:12	16:36	17:02	
Stop Time	16:32	16:56	17:22	
Unit Operational Data				
Engine Speed (rpm)	15000	15000	15000	
Unit Horse Power (Hp)*	4320	4320	4320	
NPT Load (%)	90.0	90.0	90.0	
NGP Load (%)	96.0	96.0	96.0	
Compressor Suction Pressure (psig)	258	258	258	
Compressor Discharge Pressure (psig)	446	446	446	
Compressor Suction Temperature (°F)	69	69	69	
Compressor Discharge Pressure (°F)	408	408	408	
T1 Temperature (°F)	95	95	95	
T5 Temperature (°F)	1155	1155	1155	
Lube Oil Pressure (psig)	46.0	46.0	46.0	
Fuel ΔP (psid)	9.0	9.0	9.0	
PCD (psig)	95.0	95.0	95.0	
Fuel Data				
Calculated Fuel Consumption (SCFH)	34000	34000	34000	
O2 F-Factor (DSCF/MMBtu, HHV basis)	8710	8710	8710	
Fuel Heating Value (Btu/SCF, HHV basis)	1093	1093	1093	
BHp Specific Fuel Rate (Btu/Hp-hr, HHV basis)	8602	8602	8602	
BHp Specific Fuel Rate (Btu/Hp-hr, LHV basis)	7750	7750	7750	
Ambient Conditions				
Pressure Altitude (MSL)	3230	3230	3230	
Atmospheric Pressure ("Hg)	26.62	26.62	26.62	
Dry Bulb Temperature (°F)	63	65	68	
Wet Bulb Temperature (°F)	55	54	52	
Humidity (lb/lb air)	0.0084	0.0073	0.0055	
Measured Exhaust Emissions (Corrected)				Average
O ₂ (% Vol)	16.86	16.88	16.95	16.90
NO _x (ppmv)	73.59	74.50	75.46	74.52
CO (ppmv)	8.30	8.11	8.06	8.2
Exhaust Flow Rate (DSCFH)				
Dry SCFH (dry basis, calc. from Hp/BSFR/HHV)	1.67E+06	1.68E+06	1.71E+06	1689983.01
Calculated Mass Emission Rates (Based on btu Specific Fuel Rate BSFR)				
NO _x (lbs/hr) {Permit Limit = 27}	14.7	14.9	15.4	15.00
CO (lbs/hr) {Permit Limit = 7.4}	1.0	0.9	1.0	0.97

*Based on gas producer speed.

Quality Assurance

Method 7E Non-Dilution Measurement System Performance Test Procedures
Method 7E Calculated Emission Gas Concentration

Project No.: 0023
Technician: RAT

Date: 04/20/10
Client: Enterprise Products Operating
Location: South Carlsbad Compressor Station

Calibration Gas Certified Values	Gas Selection, % of Span							
	Span	Low Gas	Mid Gas	High Gas	Analyzer	Analyzer Serial Number	Low (<20%)	Mid (40%-60%)
O ₂ (% Vol)	20.96	0.00	11.97	20.96	AII GPR-29	001666832	0.0%	57.1%
NO _x (ppmv)	98.18	0.00	50.51	98.18	TECO 42C	03040000000842	0.0%	51.4%
CO (ppmv)	100.60	0.00	50.05	100.60	TECO 48C	48C-67940-359	0.0%	49.8%

Initial Linearity Data

Calibration Error	Analyzer Calibration Response			Absolute Difference			Difference (% of Span)		
	Low	Mid	High	Low	Mid	High	Low	Mid	High
O ₂ (% Vol)	0.20	12.03	20.90	0.20	0.06	0.06	0.95%	0.29%	0.29%
NO _x (ppmv)	0.00	49.50	98.60	0.00	1.01	0.42	0.00%	1.03%	0.43%
CO (ppmv)	0.00	50.50	100.81	0.00	0.45	0.21	0.00%	0.45%	0.21%

Run Number 1 Start: 16:12 End: 16:32

Bias and Drift	Upscale Gas	Cal. Response		Initial Values		Initial System Bias		Final Values		Final System Bias		Drift		Emission Calculation	
		Low	Upscale	Low	Upscale	Low	Upscale	Low	Upscale	Low	Upscale	Low	Upscale	Raw Avg	Run Avg
O ₂ (% Vol)	20.96	0.20	20.90	0.20	20.90	0.00%	0.00%	0.20	20.90	0.00%	0.00%	0.00%	0.00%	16.85	16.86 O ₂ (% Vol)
NO _x (ppmv)	50.51	0.00	49.50	0.00	50.73	0.00%	1.25%	0.00	50.65	0.00%	1.17%	0.00%	-0.08%	73.85	73.59 NO _x (ppmv)
CO (ppmv)	50.05	0.00	50.50	0.00	49.98	0.00%	-0.52%	0.00	49.10	0.00%	-1.39%	0.00%	-0.87%	8.22	8.30 CO (ppmv)

Run Number 2 Start: 16:36 End: 16:56

Bias and Drift	Upscale Gas	Cal. Response		Initial Values		Initial System Bias		Final Values		Final System Bias		Drift		Emission Calculation	
		Low	Upscale	Low	Upscale	Low	Upscale	Low	Upscale	Low	Upscale	Low	Upscale	Raw Avg	Run Avg
O ₂ (% Vol)	20.96	0.20	20.90	0.20	20.90	0.00%	0.00%	0.20	20.90	0.00%	0.00%	0.00%	0.00%	16.87	16.88 O ₂ (% Vol)
NO _x (ppmv)	50.51	0.00	49.50	0.00	50.73	0.00%	1.25%	0.00	50.65	0.00%	1.17%	0.00%	-0.08%	74.77	74.50 NO _x (ppmv)
CO (ppmv)	50.05	0.00	50.50	0.00	49.98	0.00%	-0.52%	0.00	49.10	0.00%	-1.39%	0.00%	-0.87%	8.03	8.11 CO (ppmv)

Run Number 3 Start: 17:02 End: 17:22

Bias and Drift	Upscale Gas	Cal. Response		Initial Values		Initial System Bias		Final Values		Final System Bias		Drift		Emission Calculation	
		Low	Upscale	Low	Upscale	Low	Upscale	Low	Upscale	Low	Upscale	Low	Upscale	Raw Avg	Run Avg
O ₂ (% Vol)	20.96	0.20	20.90	0.20	20.90	0.00%	0.00%	0.20	20.90	0.00%	0.00%	0.00%	0.00%	16.94	16.95 O ₂ (% Vol)
NO _x (ppmv)	50.51	0.00	49.50	0.00	50.73	0.00%	1.25%	0.00	50.65	0.00%	1.17%	0.00%	-0.08%	75.73	75.46 NO _x (ppmv)
CO (ppmv)	50.05	0.00	50.50	0.00	49.98	0.00%	-0.52%	0.00	49.10	0.00%	-1.39%	0.00%	-0.87%	7.98	8.06 CO (ppmv)

Example Calculations

Drift Corrected Emission Concentrations		
<i>Formula</i>		
$C_{GAS} = (C - C_o) \times \frac{C_{MA}}{C_M - C_o} \quad (eq.7e-5)$		
<i>All Calculations Refer to Test Run 1 or an Average of Runs 1-3</i>		
C_{NOx} =	Raw Concentration of NOx	= 73.85 ppmv
C_o =	Avg. of Initial and Final Zero Checks	= 0.00 ppmv
C_M =	Avg. of Initial and Final Span Checks	= 50.69 ppmv
C_{MA} =	Certified Concentration of Span Gas	= 50.51 ppmv
C_{NOx} =	$(73.85 - 0) \quad \times \quad \frac{50.51}{(50.7 - 0)}$	= 73.59 ppmv
C_{CO} =	Raw Concentration of CO	= 8.22 ppmv
C_o =	Avg. of Initial and Final Zero Checks	= 0.00 ppmv
C_M =	Avg. of Initial and Final Span Checks	= 49.54 ppmv
C_{MA} =	Certified Concentration of Span Gas	= 50.05 ppmv
C_{CO} =	$(8.22 + 0) \quad \times \quad \frac{50.05}{(49.5 + 0)}$	= 8.30 ppmv
C_{O2} =	Raw Concentration of O2	= 16.85%
C_o =	Avg. of initial and final zero bias checks	= 0.20%
C_M =	Avg. of initial and final span bias checks	= 20.90%
C_{MA} =	Actual concentration of span gas	= 20.96%
C_{O2} =	$(16.85 - 0.2) \quad \times \quad \frac{20.96}{(20.9 - 0.2)}$	= 16.86%

Example Calculations

Exhaust Calculations				
<i>Measured Data and Constants</i>				
C _{NOx} =	Corrected Concentration of NO _x	=	73.59	ppmv
C _{CO} =	Corrected Concentration of CO	=	8.30	ppmv
Horsepower =	Observed Horsepower	=	4320	Hp
lb / mole =	EPA STP for Ideal Gas	=	385.15	SCF
lbs / hr to tpy =	Mass Conversion Factor	=	4.38	hrs-tons / lbs-yr
C _F =	PPMV Normalization	=	1 x e-6	1 / ppmv
MW _{NOx} =	Molecular Weight of NO _x	=	46	lb / lb-mol
MW _{CO} =	Molecular Weight of CO	=	28	lb / lb-mol
<i>Stack Gas Flow Rate via btu Specific Fuel Rate (BSFR)</i>				
Hp =	Engine Horsepower	=	4320	Hp
FBTU =	btu Specific Fuel Rate	=	8602	Btu/Hp-Hr
FO ₂ =	O ₂ F-Factor	=	8710	DSCF/MMBtu
CO ₂ =	Measured Concentration of O ₂	=	16.86	%
Q _{S M19} =	Hp x FBTU x FO ₂ x 10 ⁶ x		$\frac{20.9}{(20.9 - \%O_2)}$	DSCF/H
Q _{S M19} =	4320.00 x 8602 x 8710 x		5.17 x 1E-06	
Q _{S M19} =	1.67E+06		DSCF/H	
<i>Formulas</i>				
Pounds per Hour (lbs/hr) :				
$Ex \text{ (lb/hr)} = Cx * C_F * Q_s * \{ MW_x / (\text{lb} / \text{mole}) \}$				
Tons per Year (tpy) :				
$Ex \text{ (tpy)} = Ex \text{ (lb/hr)} * \{ 8760 \text{ (hr / yr)} / 2000 \text{ (lb / ton)} \}$				
Grams per Horsepower-hour (g/Hp-hr) :				
$Ex \text{ (g/hp-hr)} = \{ Ex \text{ (lb/hr)} / Hp \} / 454 \text{ (g / lb)} \}$				
<i>Calculated Mass Emission Rates From Method 19 Exhaust Flow Rates</i>				
E_{NOx}				
lbs/hr =	73.59	* 1 x e-6	* 1.67E+06 * $\frac{46}{385.15}$	= 14.72
tpy =	14.72 lb/hr	* 4.38	$\frac{\text{hrs-ton}}{\text{lbs-yr}}$	= 64.46
g/Hp-hr =	$\frac{14.72 \text{ lb/hr}}{4320 \text{ Hp}}$	* $\frac{454 \text{ g}}{1 \text{ lb}}$		= 1.55
E_{CO}				
lbs/hr =	8.30	* 1 x e-6	* 1.67E+06 * $\frac{28}{385.15}$	= 1.01
tpy =	1.01 lb/hr	* 4.38	$\frac{\text{hrs-ton}}{\text{lbs-yr}}$	= 4.43
g/Hp-hr =	$\frac{1.01 \text{ lb/hr}}{4320 \text{ Hp}}$	* $\frac{454 \text{ g}}{1 \text{ lb}}$		= 0.11

CERTIFICATE OF ANALYSIS

Grade of Product: EPA Protocol

Part Number: E03NI74E15A3384	Reference Number: 83-124220680-1
Cylinder Number: CC59336	Cylinder Volume: 149 Cu.Ft.
Laboratory: ASG - Port Allen - LA	Cylinder Pressure: 2015 PSIG
Analysis Date: May 25, 2010	Valve Outlet: 590

Expiration Date: May 25, 2013

Certification performed in accordance with "EPA Traceability Protocol (Sept. 1997)" using the assay procedures listed. Analytical Methodology does not require correction for analytical interferences. This cylinder has a total analytical uncertainty as stated below with a confidence level of 95%. There are no significant impurities which affect the use of this calibration mixture. All concentrations are on a volume/volume basis unless otherwise noted.
 Do Not Use This Cylinder below 150 psig. i.e. 1 Mega Pascal

ANALYTICAL RESULTS				
Component	Requested Concentration	Actual Concentration	Protocol Method	Total Relative Uncertainty
CARBON DIOXIDE	4.900 %	5.110 %	G1	+/- 1% NIST Traceable
OXYGEN	21.00 %	20.96 %	G1	+/- 1% NIST Traceable
NITROGEN	Balance			

CALIBRATION STANDARDS				
Type	Lot ID	Cylinder No	Concentration	Expiration Date
NTRM	06060806	cc206103	22.51% OXYGEN/NITROGEN	May 01, 2016
NTRM	10060118	CC281370	5.207% CARBON DIOXIDE/NITROGEN	Nov 01, 2015

ANALYTICAL EQUIPMENT		
Instrument/Make/Model	Analytical Principle	Last Multipoint Calibration
SCO2GM	NonDispersive Infrared	Apr 29, 2010
HO2GH	PMO2	Apr 29, 2010

Triad Data Available Upon Request

Notes:

Approved for Release

CERTIFICATE OF ANALYSIS

Grade of Product: EPA Protocol

Part Number: E04NI99E15A3530	Reference Number: 83-124198943-4
Cylinder Number: CC265550	Cylinder Volume: 144 Cu.Ft.
Laboratory: ASG - Port Allen - LA	Cylinder Pressure: 2015 PSIG
Analysis Date: Dec 02, 2009	Valve Outlet: 660

Expiration Date: Dec 02, 2011

Certification performed in accordance with "EPA Traceability Protocol (Sept. 1997)" using the assay procedures listed. Analytical Methodology does not require correction for analytical interferences. This cylinder has a total analytical uncertainty as stated below with a confidence level of 95%. There are no significant impurities which affect the use of this calibration mixture. All concentrations are on a volume/volume basis unless otherwise noted.
 Do Not Use This Cylinder below 150 psig i.e. 1 Mega Pascal

ANALYTICAL RESULTS

Component	Requested Concentration	Actual Concentration	Protocol Method	Total Relative Uncertainty
PROPANE	90.00 PPM	90.89 PPM	G1	+/- 1% NIST Traceable
CARBON MONOXIDE	100.0 PPM	100.6 PPM	G1	+/- 1% NIST Traceable
NITRIC OXIDE	100.0 PPM	97.37 PPM	G1	+/- 1% NIST Traceable
NITROGEN	Balance			

Total oxides of nitrogen	98.18 PPM	For Reference Only
--------------------------	-----------	--------------------

CALIBRATION STANDARDS

Type	Lot ID	Cylinder No	Concentration	Expiration Date
NTRM	06060325	CC207559	490PPM NITRIC OXIDE/NITROGEN	Jan 01, 2010
NTRM	08060207	CC255258	51.26PPM CARBON MONOXIDE/NITROGEN	Jan 15, 2012
NTRM	000520	SG9105901BAL	50.5PPM PROPANE/NITROGEN	Apr 03, 2010
NTRM	06060241	CC207849	257.0PPM NITRIC OXIDE/NITROGEN	Jan 01, 2010

ANALYTICAL EQUIPMENT

Instrument/Make/Model	Analytical Principle	Last Multipoint Calibration
FTIR2MCO	FTIR	Nov 11, 2009
FTIR2MNO	FTIR	Nov 04, 2009
FTIR2PROPANE (50-500 ppm)	FTIR	Oct 29, 2009

Triad Data Available Upon Request

Notes:

QA Approval

CERTIFICATE OF ANALYSIS

Grade of Product: EPA Protocol

Part Number: E04NI99E15A3528	Reference Number: 83-124198943-3
Cylinder Number: SG9135772BAL	Cylinder Volume: 144 Cu.Ft.
Laboratory: ASG - Port Allen - LA	Cylinder Pressure: 2015 PSIG
Analysis Date: Dec 02, 2009	Valve Outlet: 660

Expiration Date: Dec 02, 2011

Certification performed in accordance with "EPA Traceability Protocol (Sept. 1997)" using the assay procedures listed. Analytical Methodology does not require correction for analytical interferences. This cylinder has a total analytical uncertainty as stated below with a confidence level of 95%. There are no significant impurities which affect the use of this calibration mixture. All concentrations are on a volume/volume basis unless otherwise noted.
 Do Not Use This Cylinder below 150 psig, i.e. 1 Mega Pascal

ANALYTICAL RESULTS				
Component	Requested Concentration	Actual Concentration	Protocol Method	Total Relative Uncertainty
PROPANE	45.00 PPM	44.07 PPM	G1	+/- 1% NIST Traceable
CARBON MONOXIDE	50.00 PPM	50.05 PPM	G1	+/- 1% NIST Traceable
NITRIC OXIDE	50.00 PPM	50.50 PPM	G1	+/- 1% NIST Traceable
NITROGEN	Balance			

Total oxides of nitrogen	50.51 PPM	For Reference Only
--------------------------	-----------	--------------------

CALIBRATION STANDARDS				
Type	Lot ID	Cylinder No	Concentration	Expiration Date
NTRM	060610	CC206050	49.38PPM NITRIC OXIDE/NITROGEN	Oct 02, 2012
NTRM	08060207	CC255258	51.26PPM CARBON MONOXIDE/NITROGEN	Jan 15, 2012
NTRM	99060203	CC263030	49.62PPM PROPANE/NITROGEN	Jul 08, 2012

ANALYTICAL EQUIPMENT		
Instrument/Make/Model	Analytical Principle	Last Multipoint Calibration
FTIR2MCO	FTIR	Nov 11, 2009
FTIR2LNO	FTIR	Nov 10, 2009
FTIR2PROPANE (10-50 PPM)	FTIR	Oct 29, 2009

Triad Data Available Upon Request

Notes:

QA Approval

Nolan, Shiver

From: Heap, James
Sent: Monday, July 02, 2012 12:55 PM
To: Nolan, Shiver
Cc: Thompson, Roger
Subject: FW: Carlsbad Testing
Attachments: EPCO_SC_Unit_1_Report.pdf; EPCO_SC_Unit_2_Report.pdf

The annual testing for SoCarlsbad has been received. The reports are to be included with the next semi-annual report in October. These are for loading to the portal.

++++
Jim Heap Sr. Field Environmental Scientist
Enterprise Products, LLC
Midland, Texas USA
Office: 432-686-5404
Cell: 432-260-0239
jkheap@eprod.com

From: Ross Thompson [mailto:rthompson@relienteti.com]
Sent: Tuesday, June 26, 2012 4:37 PM
To: Heap, James
Subject: RE: Carlsbad Testing

Attached. I reduced the file size, in case your mail server is booting it due to size.

Thank you,

Ross A. Thompson

Principal Scientist
Relient Emissions Testing, Inc.
806-773-8851 Tel
806-771-2894 Fax



From: Heap, James [mailto:JKHEAP@eprod.com]
Sent: Tuesday, June 26, 2012 1:01 PM
To: 'Ross Thompson'
Subject: RE: Carlsbad Testing

This is the last email I have in my inbox from you.

Can you re-transmit?

Thanks

++++
Jim Heap Sr. Field Environmental Scientist
Enterprise Products, LLC
Midland, Texas USA
Office: 432-686-5404

Cell: 432-260-0239
jkheap@eprod.com

From: Ross Thompson [<mailto:rthompson@relienteti.com>]
Sent: Wednesday, May 23, 2012 12:04 PM
To: Heap, James
Subject: Re: Carlsbad Testing

I'll be there at 08:00 local time.

Ross Thompson
Principal Scientist
Relient Emissions Testing, Inc.
TEL: 806-773-8851
email: rthompson@relienteti.com

Connected by DROID on Verizon Wireless

From: "Heap, James" <JKHEAP@eprod.com>
Sent: Wed May 23 12:01:19 CDT 2012
To: 'Ross Thompson' <rthompson@relienteti.com>
Subject: Carlsbad Testing

Do you have an approximate arrival time for the Carlsbad testing tomorrow?

++++
Jim Heap Sr. Field Environmental Scientist
Enterprise Products, LLC
Midland, Texas USA
Office: 432-686-5404
Cell: 432-260-0239
jkheap@eprod.com

This message (including any attachments) is confidential and intended for a specific individual and purpose. If you are not the intended recipient, please notify the sender immediately and delete this message.

Annual Turbine Emissions TEST REPORT
ON
EXHAUST EMISSIONS
FROM

ONE NATURAL GAS FIRED TURBINE

AT THE
SOUTH CARLSBAD COMPRESSOR STATION
LOVING, NM

PREPARED FOR
SEMINOLE PIPELINE COMPANY

MAY 2012

Relient Emissions Testing, Inc
Project Number: 0181



Mr. Jim Heap
Enterprise Products, LLC
Midland, TX
(432) 686-5404

05/21/2012

Re: Annual emissions testing at the South Carlsbad Compressor Station on unit 1

Mr. Heap,

Exhaust emissions from one compressor turbine was tested at the South Carlsbad compressor station near Loving, New Mexico on. Testing was conducted to demonstrate compliance with emission limits set forth by NMED permit. The engine is identified as follows:

Engine Information	
Unit Number:	Unit 1
Manufacturer:	Solar
Serial Number:	49240
Model:	CENTAUR 40
Mfr. Rated Hp:	4500hp
Mfr. Rated Speed:	15,000

This is a natural gas fired turbine used for compression of natural gas for transportation through the pipeline.

The test matrix consisted of three 60-minute test runs on the turbine in accordance with NMED requirements. For each test, the average emission concentrations of nitrogen oxides (NO_x), oxygen (O₂), and carbon monoxide (CO) were measured using analytical instrumentation. Operational data such as Gas Producer Speed, Turbine Speed, and suction and discharge pressures were recorded during each run from available operational data on the unit.

Results of the tests are presented in tabular format in this report. Included in this table are engine operational data, ambient conditions, emission concentrations, and mass emission rates.

Continuous emission monitors housed in an air-conditioned mobile laboratory were used to measure the exhaust concentrations of NO_x, CO and O₂. This testing utilized the following analytical methods:

EPA Reference Method 3a	O ₂ concentration
EPA Reference Method 7e	NO _x concentration
EPA Reference Method 10	CO concentration
EPA Reference Method 19	Mass emission rates

A computerized data recorder was used to record output from the analyzers. The data logger record provides documentation of the emission measurements and the instrument calibrations. The data logger records are also useful for indicating trends in the data.

Mass emission rates were calculated using EPA Method 19 calculations (combustion stoichiometry). Emission rates in terms of lbs/hr and TPY were calculated using the pollutant concentration (ppmv), the oxygen F-factor (DSCF_{ex}/MMBtu) and the horsepower specific fuel consumption rate (Btu/HP-hr). The O₂ F-Factor used in this test series was 8710 (DSCF_{ex}/MMBtu), the EPA default value for engines burning natural gas.

A summary of the quality assurance procedures associated with the EPA test methods is presented in tabular format in the appendix of this report. Examples of these procedures include daily multipoint calibrations, zero and span checks between each test run, NO₂ to NO converter efficiency check results, sample system bias check results, and analyzer interference test results.

The appendix of this report also includes supporting test documentation, example calculations, and data logger records.

If you have any questions, please feel free to contact me at (806) 773-8851.

Sincerely,



Ross Thompson
Principal Scientist
Relient Emissions Testing, Inc

APPENDIX

Summary of Results

Quality Assurance/Quality Control Summary

Example Calculations

Calibration Certifications

Data Logger Files

Company: Enterprise Products Operating
Location: South Carlsbad Compressor Station
Source: Solar Centaur 40 S/N: 49240
Engine Rating: 4500hp @ 15000RPM
Technician: RAT

Test Run Number	1	2	3	
Unit	1	1	1	
Date	5/24/2012	5/24/2012	5/24/2012	
Start Time	8:48	9:53	11:55	
Stop Time	9:48	10:53	12:55	
Unit Operational Data				
Engine Speed (rpm)	15000	15000	15000	
Unit Horse Power (Hp)*	4307	4307	4307	
NPT Load (%)	91.6	91.6	91.6	
NGP Load (%)	95.7	95.7	95.7	
Compressor Suction Pressure (psig)	385	385	385	
Compressor Discharge Pressure (psig)	634	634	634	
T5 Temperature (°F)	1173	1173	1173	
PCD (psig)	96	96	96	
Fuel Data				
Calculated Fuel Consumption (SCFH)	35440	35440	35440	
O2 F-Factor (DSCF/MMBtu, HHV basis)	8710	8710	8710	
Fuel Heating Value (Btu/SCF, HHV basis)	1093	1093	1093	
BHp Specific Fuel Rate (Btu/Hp-hr, HHV basis)	8995	8995	8995	
BHp Specific Fuel Rate (Btu/Hp-hr, LHV basis)	8103	8103	8103	
Ambient Conditions				
Pressure Altitude (MSL)	3250	3250	3250	
Atmospheric Pressure ("Hg)	26.60	26.60	26.60	
Dry Bulb Temperature (°F)	78	81	85	
Wet Bulb Temperature (°F)	61	63	65	
Humidity (lb/lb air)	0.0087	0.0094	0.0099	
Measured Exhaust Emissions (Corrected)				Average
O ₂ (% Vol)	16.73	16.58	16.52	16.61
NO _x (ppmv)	74.36	84.53	85.65	81.51
CO (ppmv)	10.12	9.21	9.02	9.5
Exhaust Flow Rate (DSCFH)				
Dry SCFH (dry basis, calc. from Hp/BSFR/HHV)	1.69E+06	1.63E+06	1.61E+06	1644398.03
Calculated Mass Emission Rates (Based on btu Specific Fuel Rate BSFR)				
NO _x (lbs/hr) {Permit Limit = 27 lb/hr}	15.0	16.4	16.4	15.93
CO (lbs/hr) {Permit Limit = 7.4 lb/hr}	1.2	1.0	1.0	1.07

* Based on gas producer speed

Quality Assurance

Method 7E Non-Dilution Measurement System Performance Test Procedures
Method 7E Calculated Emission Gas Concentration

Project No.: 0023
Technician: RAT

Date: 05/24/12
Client: Enterprise Products Operating
Location: South Carlsbad Compressor Station

Calibration Gas Certified Values	Gas Selection, % of Span							
	Span	Low Gas	Mid Gas	High Gas	Analyzer	Analyzer Serial Number	Low (<20%)	Mid (40%-60%)
O ₂ (% Vol)	20.90	0.00	11.70	20.90	AII GPR-29	001666832	0.0%	56.0%
NO _x (ppmv)	251.40	0.00	90.00	251.40	TECO 42C	03040000000842	0.0%	35.8%
CO (ppmv)	257.00	0.00	99.00	257.00	TECO 48C	48C-67940-359	0.0%	38.5%

Initial Linearity Data

Calibration Error	Analyzer Calibration Response			Absolute Difference			Difference (% of Span)		
	Low	Mid	High	Low	Mid	High	Low	Mid	High
O ₂ (% Vol)	-0.01	11.70	20.87	0.01	0.00	0.03	0.05%	0.00%	0.14%
NO _x (ppmv)	-0.05	91.00	251.55	0.05	1.00	0.15	0.02%	0.40%	0.06%
CO (ppmv)	0.00	101.20	255.95	0.00	2.20	1.05	0.00%	0.86%	0.41%

Run Number 1 Start: 8:48 End: 9:48

Bias and Drift	Upscale Gas	Cal. Response		Initial Values		Initial System Bias		Final Values		Final System Bias		Drift		Emission Calculation	
		Low	Upscale	Low	Upscale	Low	Upscale	Low	Upscale	Low	Upscale	Low	Upscale	Raw Avg	Run Avg
O ₂ (% Vol)	20.90	-0.01	20.87	-0.01	20.77	0.00%	-0.48%	0.09	20.87	0.48%	0.00%	0.48%	0.48%	16.67	16.73 O ₂ (% Vol)
NO _x (ppmv)	90.00	-0.05	91.00	-0.55	87.45	-0.20%	-1.41%	0.00	86.45	0.02%	-1.81%	0.22%	-0.40%	71.79	74.36 NO _x (ppmv)
CO (ppmv)	99.00	0.00	101.20	-0.50	97.95	-0.19%	-1.26%	0.00	99.45	0.00%	-0.68%	0.19%	0.58%	9.86	10.12 CO (ppmv)

Run Number 2 Start: 9:53 End: 10:53

Bias and Drift	Upscale Gas	Cal. Response		Initial Values		Initial System Bias		Final Values		Final System Bias		Drift		Emission Calculation	
		Low	Upscale	Low	Upscale	Low	Upscale	Low	Upscale	Low	Upscale	Low	Upscale	Raw Avg	Run Avg
O ₂ (% Vol)	20.90	-0.01	20.87	0.09	20.87	0.48%	0.00%	0.00	20.80	0.05%	-0.33%	-0.43%	-0.33%	16.54	16.58 O ₂ (% Vol)
NO _x (ppmv)	90.00	-0.05	91.00	0.00	86.45	0.02%	-1.81%	0.50	90.40	0.22%	-0.24%	0.20%	1.57%	83.07	84.53 NO _x (ppmv)
CO (ppmv)	99.00	0.00	101.20	0.00	99.45	0.00%	-0.68%	0.00	99.35	0.00%	-0.72%	0.00%	-0.04%	9.25	9.21 CO (ppmv)

Run Number 3 Start: 11:55 End: 12:55

Bias and Drift	Upscale Gas	Cal. Response		Initial Values		Initial System Bias		Final Values		Final System Bias		Drift		Emission Calculation	
		Low	Upscale	Low	Upscale	Low	Upscale	Low	Upscale	Low	Upscale	Low	Upscale	Raw Avg	Run Avg
O ₂ (% Vol)	20.90	-0.01	20.87	0.00	20.80	0.05%	-0.33%	-0.01	20.90	0.00%	0.14%	-0.05%	0.48%	16.48	16.52 O ₂ (% Vol)
NO _x (ppmv)	90.00	-0.05	91.00	0.50	90.40	0.22%	-0.24%	0.00	90.21	0.02%	-0.31%	-0.20%	-0.08%	85.95	85.65 NO _x (ppmv)
CO (ppmv)	99.00	0.00	101.20	0.00	99.35	0.00%	-0.72%	0.00	99.45	0.00%	-0.68%	0.00%	0.04%	9.06	9.02 CO (ppmv)

Example Calculations

Drift Corrected Emission Concentrations		
<i>Formula</i>		
$C_{GAS} = (C - C_o) \times \frac{C_{MA}}{C_M - C_o} \quad (eq.7e-5)$		
<i>All Calculations Refer to Test Run 1 or an Average of Runs 1-3</i>		
C_{NOx} =	Raw Concentration of NOx	= 71.79 ppmv
C_o =	Avg. of Initial and Final Zero Checks	= -0.28 ppmv
C_M =	Avg. of Initial and Final Span Checks	= 86.95 ppmv
C_{MA} =	Certified Concentration of Span Gas	= 90.00 ppmv
C_{NOx} =	$(71.79 - -0.28) \times \frac{90}{(87 - -0.3)}$	= 74.36 ppmv
C_{CO} =	Raw Concentration of CO	= 9.86 ppmv
C_o =	Avg. of Initial and Final Zero Checks	= -0.25 ppmv
C_M =	Avg. of Initial and Final Span Checks	= 98.70 ppmv
C_{MA} =	Certified Concentration of Span Gas	= 99.00 ppmv
C_{CO} =	$(9.86 + 0.25) \times \frac{99}{(98.7 + 0.3)}$	= 10.12 ppmv
C_{O2} =	Raw Concentration of O2	= 16.67%
C_o =	Avg. of initial and final zero bias checks	= 0.04%
C_M =	Avg. of initial and final span bias checks	= 20.82%
C_{MA} =	Actual concentration of span gas	= 20.90%
C_{O2} =	$(16.67 - 0.04) \times \frac{20.9}{(20.8 - 0.04)}$	= 16.73%

Example Calculations

Exhaust Calculations			
<i>Measured Data and Constants</i>			
C _{NOx} =	Corrected Concentration of NO _x	=	74.36 ppmv
C _{CO} =	Corrected Concentration of CO	=	10.12 ppmv
Horsepower =	Observed Horsepower	=	4307 Hp
lb / mole =	EPA STP for Ideal Gas	=	385.15 SCF
lbs / hr to tpy =	Mass Conversion Factor	=	4.38 hrs-tons / lbs-yr
C _F =	PPMV Normalization	=	1 x e-6 1 / ppmv
MW _{NOx} =	Molecular Weight of NO _x	=	46 lb / lb-mol
MW _{CO} =	Molecular Weight of CO	=	28 lb / lb-mol
<i>Stack Gas Flow Rate via btu Specific Fuel Rate (BSFR)</i>			
Hp =	Engine Horsepower	=	4307 Hp
F _{BTU} =	btu Specific Fuel Rate	=	8995 Btu/Hp-Hr
F _{O2} =	O ₂ F-Factor	=	8710 DSCF/MMBtu
C _{O2} =	Measured Concentration of O ₂	=	16.73 %
Q _{S M19} =	Hp x F _{BTU} x F _{O2} x 10 ⁶ x	$\frac{20.9}{(20.9 - \%O_2)}$	DSCF/H
Q _{S M19} =	4306.50 x 8995 x 8710 x 5.01 x 1E-06		
Q _{S M19} =	1.69E+06	DSCF/H	
<i>Formulas</i>			
Pounds per Hour (lbs/hr) :			
$Ex \text{ (lb/hr)} = Cx * C_F * Q_s * \{ MW_x / (\text{lb} / \text{mole}) \}$			
Tons per Year (tpy) :			
$Ex \text{ (tpy)} = Ex \text{ (lb/hr)} * \{ 8760 \text{ (hr / yr)} / 2000 \text{ (lb / ton)} \}$			
Grams per Horsepower-hour (g/Hp-hr) :			
$Ex \text{ (g/hp-hr)} = \{ Ex \text{ (lb/hr)} / Hp \} / 454 \text{ (g / lb)} \}$			
Oxygen Correction (Cx @ 15%O₂)			
$(Cx @ 15\% O_2) = (X * (20.9 - 15)) / (20.9 - O_2 \text{ measured})$			
<i>Calculated Mass Emission Rates From Method 19 Exhaust Flow Rates</i>			
E_{NOx}			
lbs/hr =	74.36 * 1 x e-6 * 1.69E+06 * $\frac{46}{385.15}$	=	15.02
tpy =	15.02 lb/hr * 4.38 $\frac{\text{hrs-ton}}{\text{lbs-yr}}$	=	65.78
g/Hp-hr =	$\frac{15.02 \text{ lb/hr}}{4307 \text{ Hp}} * \frac{454 \text{ g}}{1 \text{ lb}}$	=	1.58
E_{CO}			
lbs/hr =	10.12 * 1 x e-6 * 1.69E+06 * $\frac{28}{385.15}$	=	1.24
tpy =	1.24 lb/hr * 4.38 $\frac{\text{hrs-ton}}{\text{lbs-yr}}$	=	5.45
g/Hp-hr =	$\frac{1.24 \text{ lb/hr}}{4307 \text{ Hp}} * \frac{454 \text{ g}}{1 \text{ lb}}$	=	0.13

Project Number	Client	Source	Run Number	Date	Time	O2 (% Vol)	NOX (ppmvd)	CO (ppmvd)
0181	Enterprise Products			5/24/2012	8:52:04 AM	0.18	0.00	0.00
0181	Enterprise Products			5/24/2012	8:53:04 AM	-0.01	0.00	0.00
0181	Enterprise Products			5/24/2012	8:54:04 AM	-0.01	0.00	0.00
0181	Enterprise Products			5/24/2012	8:55:04 AM	-0.01	0.00	0.00
0181	Enterprise Products			5/24/2012	8:56:04 AM	-0.01	-0.05	0.00
0181	Enterprise Products			5/24/2012	8:57:04 AM	-0.01	-0.05	0.00
0181	Enterprise Products			5/24/2012	8:58:04 AM	-0.01	-0.05	0.00
0181	Enterprise Products			5/24/2012	8:59:04 AM	-0.01	0.00	0.00
0181	Enterprise Products			5/24/2012	9:00:04 AM	-0.01	0.00	0.00
0181	Enterprise Products			5/24/2012	9:01:04 AM	-0.01	0.00	-0.05
0181	Enterprise Products			5/24/2012	9:02:04 AM	-0.01	-0.05	0.00
0181	Enterprise Products			5/24/2012	9:03:04 AM	-0.01	-0.05	0.00
0181	Enterprise Products			5/24/2012	9:04:04 AM	-0.01	0.00	0.00
0181	Enterprise Products			5/24/2012	9:05:04 AM	-0.01	0.00	0.00
0181	Enterprise Products			5/24/2012	9:06:04 AM	<u>-0.01</u>	<u>-0.05</u>	<u>0.00</u>
0181	Enterprise Products			5/24/2012	9:07:04 AM	-0.01	-0.05	0.90
0181	Enterprise Products			5/24/2012	9:08:04 AM	21.16	70.00	255.45
0181	Enterprise Products			5/24/2012	9:09:04 AM	<u>20.87</u>	90.50	<u>255.95</u>
0181	Enterprise Products			5/24/2012	9:10:04 AM	12.19	<u>91.00</u>	<u>101.20</u>
0181	Enterprise Products			5/24/2012	9:11:04 AM	11.70	251.44	38.00
0181	Enterprise Products			5/24/2012	9:12:04 AM	<u>11.70</u>	<u>251.55</u>	0.00
0181	Enterprise Products			5/24/2012	9:13:04 AM	11.70	76.95	0.00
0181	Enterprise Products			5/24/2012	9:14:04 AM	11.80	-0.50	-0.05
0181	Enterprise Products			5/24/2012	9:15:04 AM	11.80	-0.50	-0.05
0181	Enterprise Products			5/24/2012	9:16:04 AM	11.80	218.10	0.00
0181	Enterprise Products			5/24/2012	9:17:04 AM	11.90	254.10	0.00
0181	Enterprise Products			5/24/2012	9:18:04 AM	11.90	128.50	0.00
0181	Enterprise Products			5/24/2012	9:19:04 AM	11.90	28.45	0.00
0181	Enterprise Products			5/24/2012	9:20:04 AM	11.90	418.70	0.00
0181	Enterprise Products			5/24/2012	9:21:04 AM	11.90	499.75	-0.05
0181	Enterprise Products			5/24/2012	9:22:04 AM	11.90	300.15	0.00
0181	Enterprise Products			5/24/2012	9:23:04 AM	11.99	104.50	0.00
0181	Enterprise Products			5/24/2012	9:24:04 AM	12.00	89.50	0.00
0181	Enterprise Products			5/24/2012	9:25:04 AM	12.00	89.00	0.00
0181	Enterprise Products			5/24/2012	9:26:04 AM	12.00	19.95	-0.05
0181	Enterprise Products			5/24/2012	9:27:04 AM	12.00	5.95	0.00
0181	Enterprise Products			5/24/2012	9:28:04 AM	12.00	4.95	0.00
0181	Enterprise Products			5/24/2012	9:29:04 AM	12.10	4.95	0.00
0181	Enterprise Products			5/24/2012	9:30:04 AM	12.09	4.95	0.00
0181	Enterprise Products			5/24/2012	9:31:04 AM	12.09	4.95	0.00
0181	Enterprise Products			5/24/2012	9:32:04 AM	12.09	4.90	0.00
0181	Enterprise Products			5/24/2012	9:33:04 AM	12.19	4.45	0.00
0181	Enterprise Products			5/24/2012	9:34:04 AM	12.19	4.45	-0.05
0181	Enterprise Products			5/24/2012	9:35:04 AM	12.19	4.45	0.00
0181	Enterprise Products			5/24/2012	9:36:04 AM	12.19	4.40	0.00
0181	Enterprise Products			5/24/2012	9:37:04 AM	12.19	4.40	0.90
0181	Enterprise Products			5/24/2012	9:38:04 AM	20.68	2.90	0.00
0181	Enterprise Products			5/24/2012	9:39:04 AM	20.68	-0.55	-0.05
0181	Enterprise Products			5/24/2012	9:40:04 AM	20.68	-0.55	-0.55
0181	Enterprise Products			5/24/2012	9:41:04 AM	<u>20.77</u>	<u>-0.55</u>	<u>-0.50</u>
0181	Enterprise Products			5/24/2012	9:42:04 AM	20.68	-0.55	20.25
0181	Enterprise Products			5/24/2012	9:43:04 AM	17.55	1.40	5.90
0181	Enterprise Products			5/24/2012	9:44:04 AM	16.77	67.00	11.30
0181	Enterprise Products			5/24/2012	9:45:04 AM	16.77	71.50	10.80
0181	Enterprise Products			5/24/2012	9:46:04 AM	0.28	71.00	85.10
0181	Enterprise Products			5/24/2012	9:47:04 AM	<u>-0.01</u>	<u>87.45</u>	<u>97.95</u>
0181	Enterprise Products	South Carlsbad #1		5/24/2012	9:47:43 AM	13.46	87.45	62.30
0181	Enterprise Products	South Carlsbad #1		5/24/2012	9:48:13 AM	16.67	81.45	11.85
0181	Enterprise Products	South Carlsbad #1		5/24/2012	9:48:43 AM	16.67	73.00	10.30
0181	Enterprise Products	South Carlsbad #1		5/24/2012	9:48:46 AM	16.67	73.00	10.30
0181	Enterprise Products	South Carlsbad #1	Run 1	5/24/2012	9:49:16 AM	16.67	72.50	9.85
0181	Enterprise Products	South Carlsbad #1	Run 1	5/24/2012	9:49:46 AM	16.67	72.45	9.85
0181	Enterprise Products	South Carlsbad #1	Run 1	5/24/2012	9:50:16 AM	16.67	72.45	10.85
0181	Enterprise Products	South Carlsbad #1	Run 1	5/24/2012	9:50:46 AM	16.67	72.45	10.30
0181	Enterprise Products	South Carlsbad #1	Run 1	5/24/2012	9:51:16 AM	16.67	72.45	10.80
0181	Enterprise Products	South Carlsbad #1	Run 1	5/24/2012	9:51:46 AM	16.67	72.50	10.30
0181	Enterprise Products	South Carlsbad #1	Run 1	5/24/2012	9:52:16 AM	16.67	72.00	10.30
0181	Enterprise Products	South Carlsbad #1	Run 1	5/24/2012	9:52:46 AM	16.67	71.95	10.30
0181	Enterprise Products	South Carlsbad #1	Run 1	5/24/2012	9:53:16 AM	16.67	72.00	9.85

Project Number	Client	Source	Run Number	Date	Time	O2 (% Vol)	NOX (ppmvd)	CO (ppmvd)
0181	Enterprise Products	South Carlsbad #1	Run 3	5/24/2012	12:44:45 PM	16.48	86.00	8.85
0181	Enterprise Products	South Carlsbad #1	Run 3	5/24/2012	12:45:15 PM	16.48	86.00	8.85
0181	Enterprise Products	South Carlsbad #1	Run 3	5/24/2012	12:45:45 PM	16.48	85.50	9.85
0181	Enterprise Products	South Carlsbad #1	Run 3	5/24/2012	12:46:15 PM	16.48	86.00	8.85
0181	Enterprise Products	South Carlsbad #1	Run 3	5/24/2012	12:46:45 PM	16.48	86.00	9.35
0181	Enterprise Products	South Carlsbad #1	Run 3	5/24/2012	12:47:15 PM	16.48	86.00	8.85
0181	Enterprise Products	South Carlsbad #1	Run 3	5/24/2012	12:47:45 PM	16.48	86.00	9.85
0181	Enterprise Products	South Carlsbad #1	Run 3	5/24/2012	12:48:15 PM	16.48	86.50	9.35
0181	Enterprise Products	South Carlsbad #1	Run 3	5/24/2012	12:48:45 PM	16.48	86.50	8.85
0181	Enterprise Products	South Carlsbad #1	Run 3	5/24/2012	12:49:15 PM	16.48	86.50	8.85
0181	Enterprise Products	South Carlsbad #1	Run 3	5/24/2012	12:49:45 PM	16.48	87.00	8.35
0181	Enterprise Products	South Carlsbad #1	Run 3	5/24/2012	12:50:15 PM	16.48	86.50	8.35
0181	Enterprise Products	South Carlsbad #1	Run 3	5/24/2012	12:50:45 PM	16.48	86.50	9.35
0181	Enterprise Products	South Carlsbad #1	Run 3	5/24/2012	12:51:15 PM	16.48	86.50	8.35
0181	Enterprise Products	South Carlsbad #1	Run 3	5/24/2012	12:51:45 PM	16.48	86.50	8.35
0181	Enterprise Products	South Carlsbad #1	Run 3	5/24/2012	12:52:15 PM	16.48	86.50	8.85
0181	Enterprise Products	South Carlsbad #1	Run 3	5/24/2012	12:52:45 PM	16.48	86.50	8.85
0181	Enterprise Products	South Carlsbad #1	Run 3	5/24/2012	12:53:15 PM	16.48	86.50	8.85
0181	Enterprise Products	South Carlsbad #1	Run 3	5/24/2012	12:53:45 PM	16.48	86.00	9.35
0181	Enterprise Products	South Carlsbad #1	Run 3	5/24/2012	12:54:15 PM	16.48	86.50	9.35
0181	Enterprise Products	South Carlsbad #1	Run 3	5/24/2012	12:54:45 PM	16.48	86.00	8.85
Run Averages						16.48	85.95	9.06
0181	Enterprise Products	South Carlsbad #1		5/24/2012	12:55:16 PM	16.48	86.50	8.85
0181	Enterprise Products	South Carlsbad #1		5/24/2012	12:55:46 PM	16.48	86.50	8.85
0181	Enterprise Products	South Carlsbad #1		5/24/2012	12:56:16 PM	-0.01	90.21	99.35
0181	Enterprise Products	South Carlsbad #1		5/24/2012	12:56:46 PM	<u>-0.01</u>	<u>90.21</u>	<u>99.45</u>
0181	Enterprise Products	South Carlsbad #1		5/24/2012	12:57:16 PM	19.99	0.50	5.90
0181	Enterprise Products	South Carlsbad #1		5/24/2012	12:57:46 PM	20.90	0.00	0.00
0181	Enterprise Products	South Carlsbad #1		5/24/2012	12:58:16 PM	<u>20.90</u>	<u>0.00</u>	<u>0.00</u>
0181	Enterprise Products	South Carlsbad #1		5/24/2012	12:58:46 PM	20.48	0.00	0.00
0181	Enterprise Products	South Carlsbad #1		5/24/2012	12:59:16 PM	20.48	0.00	0.00
0181	Enterprise Products	South Carlsbad #1		5/24/2012	12:59:46 PM	20.48	0.00	0.00
0181	Enterprise Products	South Carlsbad #1		5/24/2012	1:00:16 PM	20.48	-0.50	0.00



ANALYTICAL REPORT

Certificate ID: 110711012 Date: 11/7/2011

Customer Name: B&J Welding Supply, TX

Customer Address: 1512 East 50th Street

Lubbock TX 79404

Purchase Order: 17436 Work Order: 127416-03

Lot Number: 1024UA11 Product Name: 3-Component Mixture, EPA Protocol

Size: A31 Pressure: 2220 psig @ 82 Deg F

Content: Ven ID# C12011

Serial #: EB0004610

Analysis Date: 11/2/2011

Shelf Life: 36 months Expiration Date: 11/2/2014

<u>Component</u>	<u>Nominal</u>	<u>Actual</u>	<u>Accuracy</u>	<u>Method</u>
Oxygen	20.9%	20.9%	+/- 1% rel	Paramagnetic
Carbon Dioxide	5.00%	5.10%	+/- 1% rel	FTIR
Nitrogen	Balance	Balance		

<u>REFERENCE STANDARD</u>	<u>Std Type</u>	<u>Std #</u>	<u>Cyl #</u>	<u>Concentration</u>	<u>Exp Date</u>
	GMIS	0318XA11	EB0028214	20.9700	3/18/2013
	GMIS	0625HE10	EB0023062	19.8500	6/28/2012

<u>INSTRUMENTATION</u>	<u>Instrument / ID</u>	<u>Component</u>
	Servomex 5200	O2
	MKS 2031	CO2

Note: * ANALYZED ACCORDING TO EPA TRACEABILITY PROTOCOL FOR ASSAY AND CERTIFICATION OF GASEOUS CALIBRATION STANDARDS - SEPTEMBER 1997:G1
* DO NOT USE STANDARD WHEN PRESSURE IS BELOW 150 PSIG



Issued by: Josh Jones



Global Calibration Gases LLC
 1500 15th Avenue Drive East,
 #109
 Palmetto, FL 34221
 Blending Plant &
 Analytical Laboratory
 Accreditation No: 69191
 PGVP Vendor ID: N12011



**EPA PROTOCOL
 GAS MIXTURE**

Customer: **B&J Specialty Gas** Reference#: **011612 - 2**
 CGA: **660** Certification Date: **1/16/12**
 Customer PO #: Expiration Date: **1/16/14**
 Cylinder #: **EB0034805** Pressure, psig: **2000**

Method: This standard was analyzed according to EPA Traceability Protocol for Assay and Certification of Gaseous Calibration Standards, Procedure G1 (September 1997).

ANALYZED CYLINDER -

Components	Certified Concentration	Analytical Accuracy
NO	90.0 ppm	± 1 %
NOx	> 1 %	± 1 %
Propane	105.0 ppm	± 1 %
Methane	109.0 ppm	± 1 %
Carbon Monoxide	99.0 ppm	± 1 %
Nitrogen	BALANCE	-

REFERENCE STANDARD -

Type/SRM Sample	Cylinder#	Concentration
NO/ SRM 2735	Cal015838	784.4 ppm
NOx/ SRM 2735	Cal015838	787.5 ppm
Propane/ GMIS	EB0026425	310.9 ppm
Methane/ GMIS	EB0019166	94.6 ppm
CO/ GMIS	CC118813	95.5 ppm

INSTRUMENT -

Instrument/Model	Serial #	Last Date Calibrated	Analytical Method
California Analytical Instrument Model 600	Y09003	1/5/12	Chemiluminescence
Agilent	US02002031	1/10/12	Thermal conductivity

These mixtures were prepared gravimetrically using a high load high sensitivity electronic scale. Prior to filling the scale is verified for accuracy throughout the target mass range against applicable NIST traceable weights. We certify that the weights are calibrated to ASTM E617-97 Class 1 tolerances. This calibration is referenced by serial # 7210-1, Certificate # 511635 and NIST Inst # 822/272103-06. This report states accurately the results of the investigation made upon the material submitted to the analytical laboratory. Every effort has been made to determine objectively the information requested. However, in connection with this report, Global Calibration Gases LLC shall have no liability in excess of the established charge for this service. Assayed at Global Calibration Gases LLC, Palmetto, Florida. *Do not use this standard when cylinder pressure is below 150 psig.

Principal Analyst: *Matthew J. [Signature]*
 Date: 1/16/12

Reviewer: *[Signature]*
 Date: 1-16-2012



B&J Welding Supply
Lamesa, Tx



Accreditation No
69191



PGVP Vendor ID
N12012

EPA Protocol
Gas Mixture

Customer: B&J Welding Supply
CGA: 680
Customer PO#: 17784
Cylinder #: EB0032807

Reference#: 011112-1
Certification Date: 01/11/2012
Expiration Date: 01/11/2014
Pressure, psig: 2000

Method: This standard was analyzed according to EPA Traceability Protocol for Assay and Certification of Gaseous Calibration Standards, Procedure G1 (September 1997)

Analyzed Cylinder-

Components	Certified Concentration	Analytical Accuracy
Nitric Oxide	251.4 ppm	+/-1%
NOx	<1%	+/-1%
Carbon Monoxide	257 ppm	+/-1%
Methane	248.6 ppm	+/-1%
Propane	251.6 ppm	+/-1%
Nitrogen	Balance	.

Reference Standard-

Type/SRM Sample	Cylinder #	Concentration
NO/SRM 2735	Cal015838	784.4 ppm
Nox/ SRM 2735	Cal015838	767.5 ppm
CO/ GMIS	EB0019151	1.96%
Propane/ GMIS	CC80938	2984 ppm
Methane/ GMIS	EB0028384	148.3 ppm

Instrument-

Instrument/ Model	Serial Number	Last Date Calibrated	Analytical Method
California Analytical Instrument Model 600	Y06003	01/05/2012	Chemiluminescence
Agilent Quad Series Rosemount 880A	US02002031 F-04300088	01/11/12 01/04/2012	Thermal Conductivity Non-Dispersive Infrared

These mixtures were prepared gravimetrically using a high load high sensitivity electronic scale. Prior to filling the scale is verified for accuracy throughout the target mass range against applicable NIST traceable weights.

We certify that the weights are calibrated to ASTM E817-97 Class 1 tolerances. This calibration is referenced by serial # 7210-1, Certificate # 511635 and NIST Inst # 822/272103-06.

This report states accurately the results of the investigation made upon the material submitted to the analytical laboratory. Every effort has been made to determine objectively the information requested. However, in connection with this report, Global Calibration Gases LLC shall have no liability in excess of the established charge for this service. Assayed at Global Calibration Gases LLC, Palmetto, Florida.

*Do not use this standard when cylinder pressure is below 150 psig.

Produced by:



Global Calibration Gases LLC
1500 15th Avenue Drive, East Suite# 109
Palmetto, Florida 34221
Accreditation No.: 69191
PGVP Vendor ID.: N12012

Principal Analyst: [Signature]
Date: 1-11-12

Principal Reviewer: [Signature]
Date: 1-11-12

Annual Turbine Emissions TEST REPORT
ON
EXHAUST EMISSIONS
FROM

ONE NATURAL GAS FIRED TURBINE

AT THE
SOUTH CARLSBAD COMPRESSOR STATION
LOVING, NM

PREPARED FOR
ENTERPRISE PRODUCTS OPERATING

MAY 2012

Relient Emissions Testing, Inc
Project Number: 0181



Mr. Jim Heap
Enterprise Products, LLC
(432) 686-5404
Midland, TX

May 20, 2012

Re: Annual emissions testing at the South Carlsbad Compressor Station on Unit 2

Mr. Heap,

Exhaust emissions from one compressor turbine was tested at the South Carlsbad compressor station near Loving, New Mexico on. Testing was conducted to demonstrate compliance with emission limits set forth by NMED permit. The engine is identified as follows:

Engine Information	
Unit Number:	Unit 2
Manufacturer:	Solar
Serial Number:	3001096
Model:	CENTAUR 40
Mfr. Rated Hp:	4500hp
Mfr. Rated Speed:	15,000

This is a natural gas fired turbine used for compression of natural gas for transportation through the pipeline.

The test matrix consisted of three 60-minute test runs on the turbine in accordance with NMED requirements. For each test, the average emission concentrations of nitrogen oxides (NO_x), oxygen (O₂), and carbon monoxide (CO) were measured using analytical instrumentation. Operational data such as Gas Producer Speed, Turbine Speed, and suction and discharge pressures were recorded during each run from available operational data on the unit.

Results of the tests are presented in tabular format in this report. Included in this table are engine operational data, ambient conditions, emission concentrations, and mass emission rates.

Continuous emission monitors housed in an air-conditioned mobile laboratory were used to measure the exhaust concentrations of NO_x, CO and O₂. This testing utilized the following analytical methods:

EPA Reference Method 3a	O ₂ concentration
EPA Reference Method 7e	NO _x concentration
EPA Reference Method 10	CO concentration
EPA Reference Method 19	Mass emission rates

A computerized data recorder was used to record output from the analyzers. The data logger record provides documentation of the emission measurements and the instrument calibrations. The data logger records are also useful for indicating trends in the data.

Mass emission rates were calculated using EPA Method 19 calculations (combustion stoichiometry). Emission rates in terms of lbs/hr and TPY were calculated using the pollutant concentration (ppmv), the oxygen F-factor (DSCF_{ex}/MMBtu) and the horsepower specific fuel consumption rate (Btu/Hp-hr). The O₂ F-Factor used in this test series was 8710 (DSCF_{ex}/MMBtu), the EPA default value for engines burning natural gas.

A summary of the quality assurance procedures associated with the EPA test methods is presented in tabular format in the appendix of this report. Examples of these procedures include daily multipoint calibrations, zero and span checks between each test run, NO₂ to NO converter efficiency check results, sample system bias check results, and analyzer interference test results.

The appendix of this report also includes supporting test documentation, example calculations, and data logger records.

If you have any questions, please feel free to contact me at (806) 773-8851.

Sincerely,



Ross Thompson
Principal Scientist
Relient Emissions Testing, Inc

APPENDIX

Summary of Results

Quality Assurance/Quality Control Summary

Example Calculations

Calibration Certifications

Data Logger Files

Summary of Results

Company: Enterprise Products Operating
Location: South Carlsbad Compressor Station
Source: Solar Centaur 40 S/N: 30010096
Engine Rating: 4500hp @ 15000RPM
Technician: RAT

Test Run Number	1	2	3	
Unit	2	2	2	
Date	4/20/2010	4/20/2010	4/20/2010	
Start Time	12:02	13:04	14:07	
Stop Time	12:22	13:24	14:27	
Unit Operational Data				
Engine Speed (rpm)	15000	15000	15000	
Unit Horse Power (Hp)*	4320	4320	4320	
NPT Load (%)	93.0	93.0	93.0	
NGP Load (%)	96.0	96.0	96.0	
Compressor Suction Pressure (psig)	225	225	225	
Compressor Discharge Pressure (psig)	382	382	382	
T5 Temperature (°F)	1190	1190	1190	
PCD (psig)	93.0	93.0	93.0	
Fuel Data				
Calculated Fuel Consumption (SCFH)	34000	34000	34000	
O2 F-Factor (DSCF/MMBtu, HHV basis)	8710	8710	8710	
Fuel Heating Value (Btu/SCF, HHV basis)	1093	1093	1093	
BHp Specific Fuel Rate (Btu/Hp-hr, HHV basis)	8602	8602	8602	
BHp Specific Fuel Rate (Btu/Hp-hr, LHV basis)	7750	7750	7750	
Ambient Conditions				
Pressure Altitude (MSL)	3250	3250	3250	
Atmospheric Pressure ("Hg)	26.60	26.60	26.60	
Dry Bulb Temperature (°F)	87	86	86	
Wet Bulb Temperature (°F)	65	64	64	
Humidity (lb/lb air)	0.0095	0.0090	0.0090	
Measured Exhaust Emissions (Corrected)				Average
O ₂ (% Vol)	16.28	16.32	16.29	16.30
NO _x (ppmv)	86.22	86.64	85.20	86.02
CO (ppmv)	9.60	9.51	9.67	9.6
Exhaust Flow Rate (DSCFH)				
Dry SCFH (dry basis, calc. from Hp/BSFR/HHV)	1.46E+06	1.48E+06	1.47E+06	1469592.84
Calculated Mass Emission Rates (Based on btu Specific Fuel Rate BSFR)				
NO _x (lbs/hr) {Permit Limit = 27}	15.0	15.2	14.9	15.03
CO (lbs/hr) {Permit Limit = 7.4}	1.0	1.0	1.0	1.00

*Based on gas producer speed.

Quality Assurance

Method 7E Non-Dilution Measurement System Performance Test Procedures
Method 7E Calculated Emission Gas Concentration

Project No.: 0023
Technician: RAT

Date: 04/20/10
Client: Enterprise Products Operating
Location: South Carlsbad Compressor Station

Calibration Gas Certified Values	Gas Selection, % of Span							
	Span	Low Gas	Mid Gas	High Gas	Analyzer	Analyzer Serial Number	Low (<20%)	Mid (40%-60%)
O ₂ (% Vol)	20.90	0.00	11.70	20.90	AII GPR-29	001666832	0.0%	56.0%
NOx (ppmv)	251.40	0.00	90.00	251.40	TECO 42C	03040000000842	0.0%	35.8%
CO (ppmv)	257.00	0.00	99.00	257.00	TECO 48C	48C-67940-359	0.0%	38.5%

Initial Linearity Data

Calibration Error	Analyzer Calibration Response			Absolute Difference			Difference (% of Span)		
	Low	Mid	High	Low	Mid	High	Low	Mid	High
O ₂ (% Vol)	-0.01	11.70	20.87	0.01	0.00	0.03	0.05%	0.00%	0.14%
NOx (ppmv)	-0.05	91.00	251.55	0.05	1.00	0.15	0.02%	0.40%	0.06%
CO (ppmv)	0.00	101.20	255.95	0.00	2.20	1.05	0.00%	0.86%	0.41%

Run Number 1 Start: 12:02 End: 12:22

Bias and Drift	Upscale Gas	Cal. Response		Initial Values		Initial System Bias		Final Values		Final System Bias		Drift		Emission Calculation	
		Low	Upscale	Low	Upscale	Low	Upscale	Low	Upscale	Low	Upscale	Low	Upscale	Raw Avg	Run Avg
O ₂ (% Vol)	20.90	-0.01	20.87	-0.01	20.90	0.00%	0.14%	-0.01	20.90	0.00%	0.14%	0.00%	0.00%	16.28	16.28 O ₂ (% Vol)
NOx (ppmv)	90.00	-0.05	91.00	0.00	90.21	0.02%	-0.31%	0.00	90.40	0.02%	-0.24%	0.00%	0.08%	86.51	86.22 NOx (ppmv)
CO (ppmv)	99.00	0.00	101.20	0.00	99.45	0.00%	-0.68%	0.00	99.50	0.00%	-0.66%	0.00%	0.02%	9.65	9.60 CO (ppmv)

Run Number 2 Start: 13:04 End: 13:24

Bias and Drift	Upscale Gas	Cal. Response		Initial Values		Initial System Bias		Final Values		Final System Bias		Drift		Emission Calculation	
		Low	Upscale	Low	Upscale	Low	Upscale	Low	Upscale	Low	Upscale	Low	Upscale	Raw Avg	Run Avg
O ₂ (% Vol)	20.90	-0.01	20.87	-0.01	20.90	0.00%	0.14%	-0.01	20.85	0.00%	-0.10%	0.00%	-0.24%	16.30	16.32 O ₂ (% Vol)
NOx (ppmv)	90.00	-0.05	91.00	0.00	90.40	0.02%	-0.24%	0.00	90.50	0.02%	-0.20%	0.00%	0.04%	87.07	86.64 NOx (ppmv)
CO (ppmv)	99.00	0.00	101.20	0.00	99.50	0.00%	-0.66%	0.00	99.60	0.00%	-0.62%	0.00%	0.04%	9.56	9.51 CO (ppmv)

Run Number 3 Start: 14:07 End: 14:27

Bias and Drift	Upscale Gas	Cal. Response		Initial Values		Initial System Bias		Final Values		Final System Bias		Drift		Emission Calculation	
		Low	Upscale	Low	Upscale	Low	Upscale	Low	Upscale	Low	Upscale	Low	Upscale	Raw Avg	Run Avg
O ₂ (% Vol)	20.90	-0.01	20.87	-0.01	20.85	0.00%	-0.10%	-0.01	20.90	0.00%	0.14%	0.00%	0.24%	16.27	16.29 O ₂ (% Vol)
NOx (ppmv)	90.00	-0.05	91.00	0.00	90.50	0.02%	-0.20%	0.00	90.20	0.02%	-0.32%	0.00%	-0.12%	85.53	85.20 NOx (ppmv)
CO (ppmv)	99.00	0.00	101.20	0.00	99.60	0.00%	-0.62%	-0.50	99.30	-0.19%	-0.74%	-0.19%	-0.12%	9.49	9.67 CO (ppmv)

Example Calculations

Drift Corrected Emission Concentrations		
<i>Formula</i>		
$C_{GAS} = (C - C_0) \times \frac{C_{MA}}{C_M - C_0} \quad (eq.7e-5)$		
<i>All Calculations Refer to Test Run 1 or an Average of Runs 1-3</i>		
C_{NOx} =	Raw Concentration of NOx	= 86.51 ppmv
C_0 =	Avg. of Initial and Final Zero Checks	= 0.00 ppmv
C_M =	Avg. of Initial and Final Span Checks	= 90.31 ppmv
C_{MA} =	Certified Concentration of Span Gas	= 90.00 ppmv
C_{NOx} =	$(86.51 - 0) \times \frac{90}{(90.3 - 0)}$	= 86.22 ppmv
C_{CO} =	Raw Concentration of CO	= 9.65 ppmv
C_0 =	Avg. of Initial and Final Zero Checks	= 0.00 ppmv
C_M =	Avg. of Initial and Final Span Checks	= 99.48 ppmv
C_{MA} =	Certified Concentration of Span Gas	= 99.00 ppmv
C_{CO} =	$(9.65 + 0) \times \frac{99}{(99.5 + 0)}$	= 9.60 ppmv
C_{O2} =	Raw Concentration of O2	= 16.28%
C_0 =	Avg. of initial and final zero bias checks	= -0.01%
C_M =	Avg. of initial and final span bias checks	= 20.90%
C_{MA} =	Actual concentration of span gas	= 20.90%
C_{O2} =	$(16.28 - -0.01) \times \frac{20.9}{(20.9 - 0)}$	= 16.28%

Example Calculations

Exhaust Calculations				
<i>Measured Data and Constants</i>				
C _{NOx} =	Corrected Concentration of NO _x	=	86.22	ppmv
C _{CO} =	Corrected Concentration of CO	=	9.60	ppmv
Horsepower =	Observed Horsepower	=	4320	Hp
lb / mole =	EPA STP for Ideal Gas	=	385.15	SCF
lbs / hr to tpy =	Mass Conversion Factor	=	4.38	hrs-tons / lbs-yr
C _F =	PPMV Normalization	=	1 x e-6	1 / ppmv
MW _{NOx} =	Molecular Weight of NO _x	=	46	lb / lb-mol
MW _{CO} =	Molecular Weight of CO	=	28	lb / lb-mol
<i>Stack Gas Flow Rate via btu Specific Fuel Rate (BSFR)</i>				
Hp =	Engine Horsepower	=	4320	Hp
FBTU =	btu Specific Fuel Rate	=	8602	Btu/Hp-Hr
FO ₂ =	O ₂ F-Factor	=	8710	DSCF/MMBtu
CO ₂ =	Measured Concentration of O ₂	=	16.28	%
Q _{S M19} =	Hp x FBTU x FO ₂ x 10 ⁶ x		$\frac{20.9}{(20.9 - \%O_2)}$	DSCF/H
Q _{S M19} =	4320.00 x 8602 x 8710 x 4.52 x 1E-06			
Q _{S M19} =	1.46E+06		DSCF/H	
<i>Formulas</i>				
Pounds per Hour (lbs/hr) :				
	$Ex \text{ (lb/hr)} = Cx * C_F * Q_s * \{ MW_x / (\text{lb} / \text{mole}) \}$			
Tons per Year (tpy) :				
	$Ex \text{ (tpy)} = Ex \text{ (lb/hr)} * \{ 8760 \text{ (hr / yr)} / 2000 \text{ (lb / ton)} \}$			
Grams per Horsepower-hour (g/Hp-hr) :				
	$Ex \text{ (g/hp-hr)} = \{ Ex \text{ (lb/hr)} / Hp \} / 454 \text{ (g / lb)} \}$			
<i>Calculated Mass Emission Rates From Method 19 Exhaust Flow Rates</i>				
E_{NOx}				
lbs/hr =	86.22	*	$1 \times e-6$	*
		*	1.46E+06	*
			$\frac{46}{385.15}$	= 15.08
tpy =	15.08 lb/hr	*	4.38	$\frac{\text{hrs-ton}}{\text{lbs-yr}}$ = 66.04
g/Hp-hr =	$\frac{15.08 \text{ lb/hr}}{4320 \text{ Hp}}$	*	$\frac{454 \text{ g}}{1 \text{ lb}}$	= 1.58
E_{CO}				
lbs/hr =	9.60	*	$1 \times e-6$	*
		*	1.46E+06	*
			$\frac{28}{385.15}$	= 1.02
tpy =	1.02 lb/hr	*	4.38	$\frac{\text{hrs-ton}}{\text{lbs-yr}}$ = 4.48
g/Hp-hr =	$\frac{1.02 \text{ lb/hr}}{4320 \text{ Hp}}$	*	$\frac{454 \text{ g}}{1 \text{ lb}}$	= 0.11

Project Number	Client	Source	Run Number	Date	Time	O2 (% Vol)	NOX (ppmvd)	CO (ppmvd)
0181	Enterprise Products			5/24/2012	8:52:04 AM	0.18	0.00	0.00
0181	Enterprise Products			5/24/2012	8:53:04 AM	-0.01	0.00	0.00
0181	Enterprise Products			5/24/2012	8:54:04 AM	-0.01	0.00	0.00
0181	Enterprise Products			5/24/2012	8:55:04 AM	-0.01	0.00	0.00
0181	Enterprise Products			5/24/2012	8:56:04 AM	-0.01	-0.05	0.00
0181	Enterprise Products			5/24/2012	8:57:04 AM	-0.01	-0.05	0.00
0181	Enterprise Products			5/24/2012	8:58:04 AM	-0.01	-0.05	0.00
0181	Enterprise Products			5/24/2012	8:59:04 AM	-0.01	0.00	0.00
0181	Enterprise Products			5/24/2012	9:00:04 AM	-0.01	0.00	0.00
0181	Enterprise Products			5/24/2012	9:01:04 AM	-0.01	0.00	-0.05
0181	Enterprise Products			5/24/2012	9:02:04 AM	-0.01	-0.05	0.00
0181	Enterprise Products			5/24/2012	9:03:04 AM	-0.01	-0.05	0.00
0181	Enterprise Products			5/24/2012	9:04:04 AM	-0.01	0.00	0.00
0181	Enterprise Products			5/24/2012	9:05:04 AM	-0.01	0.00	0.00
0181	Enterprise Products			5/24/2012	9:06:04 AM	<u>-0.01</u>	<u>-0.05</u>	<u>0.00</u>
0181	Enterprise Products			5/24/2012	9:07:04 AM	-0.01	-0.05	0.90
0181	Enterprise Products			5/24/2012	9:08:04 AM	21.16	70.00	255.45
0181	Enterprise Products			5/24/2012	9:09:04 AM	<u>20.87</u>	90.50	<u>255.95</u>
0181	Enterprise Products			5/24/2012	9:10:04 AM	12.19	<u>91.00</u>	<u>101.20</u>
0181	Enterprise Products			5/24/2012	9:11:04 AM	11.70	251.44	38.00
0181	Enterprise Products			5/24/2012	9:12:04 AM	<u>11.70</u>	<u>251.55</u>	0.00
0181	Enterprise Products			5/24/2012	9:13:04 AM	11.70	76.95	0.00
0181	Enterprise Products			5/24/2012	9:14:04 AM	11.80	-0.50	-0.05
0181	Enterprise Products			5/24/2012	9:15:04 AM	11.80	-0.50	-0.05
0181	Enterprise Products			5/24/2012	9:16:04 AM	11.80	218.10	0.00
0181	Enterprise Products			5/24/2012	9:17:04 AM	11.90	254.10	0.00
0181	Enterprise Products			5/24/2012	9:18:04 AM	11.90	128.50	0.00
0181	Enterprise Products			5/24/2012	9:19:04 AM	11.90	28.45	0.00
0181	Enterprise Products			5/24/2012	9:20:04 AM	11.90	418.70	0.00
0181	Enterprise Products			5/24/2012	9:21:04 AM	11.90	499.75	-0.05
0181	Enterprise Products			5/24/2012	9:22:04 AM	11.90	300.15	0.00
0181	Enterprise Products			5/24/2012	9:23:04 AM	11.99	104.50	0.00
0181	Enterprise Products			5/24/2012	9:24:04 AM	12.00	89.50	0.00
0181	Enterprise Products			5/24/2012	9:25:04 AM	12.00	89.00	0.00
0181	Enterprise Products			5/24/2012	9:26:04 AM	12.00	19.95	-0.05
0181	Enterprise Products			5/24/2012	9:27:04 AM	12.00	5.95	0.00
0181	Enterprise Products			5/24/2012	9:28:04 AM	12.00	4.95	0.00
0181	Enterprise Products			5/24/2012	9:29:04 AM	12.10	4.95	0.00
0181	Enterprise Products			5/24/2012	9:30:04 AM	12.09	4.95	0.00
0181	Enterprise Products			5/24/2012	9:31:04 AM	12.09	4.95	0.00
0181	Enterprise Products			5/24/2012	9:32:04 AM	12.09	4.90	0.00
0181	Enterprise Products			5/24/2012	9:33:04 AM	12.19	4.45	0.00
0181	Enterprise Products			5/24/2012	9:34:04 AM	12.19	4.45	-0.05
0181	Enterprise Products			5/24/2012	9:35:04 AM	12.19	4.45	0.00
0181	Enterprise Products			5/24/2012	9:36:04 AM	12.19	4.40	0.00
0181	Enterprise Products			5/24/2012	9:37:04 AM	12.19	4.40	0.90
0181	Enterprise Products			5/24/2012	9:38:04 AM	20.68	2.90	0.00
0181	Enterprise Products			5/24/2012	9:39:04 AM	20.68	-0.55	-0.05
0181	Enterprise Products			5/24/2012	9:40:04 AM	20.68	-0.55	-0.55
0181	Enterprise Products			5/24/2012	9:41:04 AM	<u>20.77</u>	<u>-0.55</u>	<u>-0.50</u>
0181	Enterprise Products			5/24/2012	9:42:04 AM	20.68	-0.55	20.25
0181	Enterprise Products			5/24/2012	9:43:04 AM	17.55	1.40	5.90
0181	Enterprise Products			5/24/2012	9:44:04 AM	16.77	67.00	11.30
0181	Enterprise Products			5/24/2012	9:45:04 AM	16.77	71.50	10.80
0181	Enterprise Products			5/24/2012	9:46:04 AM	0.28	71.00	85.10
0181	Enterprise Products			5/24/2012	9:47:04 AM	<u>-0.01</u>	<u>87.45</u>	<u>97.95</u>
0181	Enterprise Products	South Carlsbad #1		5/24/2012	9:47:43 AM	13.46	87.45	62.30
0181	Enterprise Products	South Carlsbad #1		5/24/2012	9:48:13 AM	16.67	81.45	11.85
0181	Enterprise Products	South Carlsbad #1		5/24/2012	9:48:43 AM	16.67	73.00	10.30
0181	Enterprise Products	South Carlsbad #1		5/24/2012	9:48:46 AM	16.67	73.00	10.30
0181	Enterprise Products	South Carlsbad #1		5/24/2012	12:55:46 PM	16.48	86.50	8.85
0181	Enterprise Products	South Carlsbad #1		5/24/2012	12:56:16 PM	-0.01	90.21	99.35
0181	Enterprise Products	South Carlsbad #1		5/24/2012	12:56:46 PM	<u>-0.01</u>	<u>90.21</u>	<u>99.45</u>
0181	Enterprise Products	South Carlsbad #1		5/24/2012	12:57:16 PM	19.99	0.50	5.90
0181	Enterprise Products	South Carlsbad #1		5/24/2012	12:57:46 PM	20.90	0.00	0.00
0181	Enterprise Products	South Carlsbad #1		5/24/2012	12:58:16 PM	<u>20.90</u>	<u>0.00</u>	<u>0.00</u>
0181	Enterprise Products	South Carlsbad #1		5/24/2012	12:58:46 PM	20.48	0.00	0.00
0181	Enterprise Products	South Carlsbad #1		5/24/2012	12:59:16 PM	20.48	0.00	0.00
0181	Enterprise Products	South Carlsbad #1		5/24/2012	12:59:46 PM	20.48	0.00	0.00

Project Number	Client	Source	Run Number	Date	Time	O2 (% Vol)	NOX (ppmvd)	CO (ppmvd)
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	3:50:43 PM	16.28	85.50	9.85
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	3:51:13 PM	16.28	85.00	9.85
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	3:51:43 PM	16.28	85.50	9.85
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	3:52:13 PM	16.28	85.50	9.85
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	3:52:43 PM	16.28	85.50	9.85
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	3:53:13 PM	16.28	85.50	9.35
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	3:53:43 PM	16.28	85.50	9.85
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	3:54:13 PM	16.28	85.00	9.35
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	3:54:43 PM	16.28	85.00	9.35
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	3:55:13 PM	16.28	85.00	9.35
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	3:55:43 PM	16.28	85.00	9.85
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	3:56:13 PM	16.28	85.00	8.85
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	3:56:43 PM	16.28	85.00	8.85
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	3:57:13 PM	16.28	85.00	8.85
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	3:57:43 PM	16.28	85.00	8.85
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	3:58:13 PM	16.28	85.00	9.35
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	3:58:43 PM	16.18	85.00	9.85
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	3:59:13 PM	16.28	85.00	9.35
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	3:59:43 PM	16.28	85.00	9.35
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	4:00:13 PM	16.28	85.00	9.85
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	4:00:43 PM	16.20	85.00	9.85
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	4:01:13 PM	16.18	85.00	9.85
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	4:01:43 PM	16.28	85.00	9.35
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	4:02:13 PM	16.28	85.00	8.85
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	4:02:43 PM	16.28	85.00	9.85
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	4:03:13 PM	16.28	85.00	9.85
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	4:03:43 PM	16.28	85.00	9.85
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	4:04:13 PM	16.18	85.55	9.35
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	4:04:43 PM	16.28	85.00	9.85
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	4:05:13 PM	16.18	85.50	9.85
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	4:05:43 PM	16.18	85.00	9.85
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	4:06:13 PM	16.18	85.00	9.85
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	4:06:43 PM	16.18	85.00	9.85
0181	Enterprise Products	South Carlsbad #2	Run 6	5/24/2012	4:07:13 PM	16.18	85.50	9.85
		Run Averages				16.27	85.53	9.49
0181	Enterprise Products	South Carlsbad #2		5/24/2012	4:07:43 PM	16.18	85.50	9.85
0181	Enterprise Products	South Carlsbad #2		5/24/2012	4:08:13 PM	-0.01	90.20	99.30
0181	Enterprise Products	South Carlsbad #2		5/24/2012	4:08:43 PM	<u>-0.01</u>	<u>90.20</u>	<u>99.30</u>
0181	Enterprise Products	South Carlsbad #2		5/24/2012	4:09:13 PM	-0.01	90.20	99.30
0181	Enterprise Products	South Carlsbad #2		5/24/2012	4:09:43 PM	20.90	0.00	0.00
0181	Enterprise Products	South Carlsbad #2		5/24/2012	4:10:13 PM	<u>20.90</u>	<u>0.00</u>	<u>-0.50</u>
0181	Enterprise Products	South Carlsbad #2		5/24/2012	4:10:43 PM	20.90	0.00	-0.55
0181	Enterprise Products	South Carlsbad #2		5/24/2012	4:11:13 PM	20.90	0.00	-0.55
0181	Enterprise Products	South Carlsbad #2		5/24/2012	4:11:43 PM	20.90	0.00	-0.50
0181	Enterprise Products	South Carlsbad #2		5/24/2012	4:12:13 PM	20.90	0.00	-0.50
0181	Enterprise Products	South Carlsbad #2		5/24/2012	4:12:43 PM	20.90	0.00	-0.50
0181	Enterprise Products	South Carlsbad #2		5/24/2012	4:13:13 PM	20.90	0.00	-0.50



Global Calibration Gases LLC
 1500 15th Avenue Drive East,
 #109
 Palmetto, FL 34221
 Blending Plant &
 Analytical Laboratory
 Accreditation No: 69191
 PGVP Vendor ID: N12011



**EPA PROTOCOL
 GAS MIXTURE**

Customer: **B&J Specialty Gas** Reference#: **011612 - 2**
 CGA: **660** Certification Date: **1/16/12**
 Customer PO #: Expiration Date: **1/16/14**
 Cylinder #: **EB0034805** Pressure, psig: **2000**

Method: This standard was analyzed according to EPA Traceability Protocol for Assay and Certification of Gaseous Calibration Standards, Procedure G1 (September 1997).

ANALYZED CYLINDER -

Components	Certified Concentration	Analytical Accuracy
NO	90.0 ppm	± 1 %
NOx	> 1 %	± 1 %
Propane	105.0 ppm	± 1 %
Methane	109.0 ppm	± 1 %
Carbon Monoxide	99.0 ppm	± 1 %
Nitrogen	BALANCE	-

REFERENCE STANDARD -

Type/SRM Sample	Cylinder#	Concentration
NO/ SRM 2735	Cal015838	784.4 ppm
NOx/ SRM 2735	Cal015838	787.5 ppm
Propane/ GMIS	EB0026425	310.9 ppm
Methane/ GMIS	EB0019166	94.6 ppm
CO/ GMIS	CC118813	95.5 ppm

INSTRUMENT -

Instrument/Model	Serial #	Last Date Calibrated	Analytical Method
California Analytical Instrument Model 600	Y09003	1/5/12	Chemiluminescence
Agilent	US02002031	1/10/12	Thermal conductivity

These mixtures were prepared gravimetrically using a high load high sensitivity electronic scale. Prior to filling the scale is verified for accuracy throughout the target mass range against applicable NIST traceable weights. We certify that the weights are calibrated to ASTM E617-97 Class 1 tolerances. This calibration is referenced by serial # 7210-1, Certificate # 511635 and NIST Inst # 822/272103-06. This report states accurately the results of the investigation made upon the material submitted to the analytical laboratory. Every effort has been made to determine objectively the information requested. However, in connection with this report, Global Calibration Gases LLC shall have no liability in excess of the established charge for this service. Assayed at Global Calibration Gases LLC, Palmetto, Florida. *Do not use this standard when cylinder pressure is below 150 psig.

Principal Analyst: *Matthew J. [Signature]*
 Date: 1/16/12

Reviewer: *[Signature]*
 Date: 1-16-2012



B&J Welding Supply
Lamesa, Tx



Accreditation No
69191



PGVP Vendor ID
N12012

EPA Protocol
Gas Mixture

Customer: B&J Welding Supply
CGA: 680
Customer PO#: 17784
Cylinder #: EB0032807

Reference#: 011112-1
Certification Date: 01/11/2012
Expiration Date: 01/11/2014
Pressure, psig: 2000

Method: This standard was analyzed according to EPA Traceability Protocol for Assay and Certification of Gaseous Calibration Standards, Procedure G1 (September 1997)

Analyzed Cylinder-

Components	Certified Concentration	Analytical Accuracy
Nitric Oxide	251.4 ppm	+/-1%
NOx	<1%	+/-1%
Carbon Monoxide	257 ppm	+/-1%
Methane	248.6 ppm	+/-1%
Propane	251.6 ppm	+/-1%
Nitrogen	Balance	.

Reference Standard-

Type/SRM Sample	Cylinder #	Concentration
NO/SRM 2735	Cal015838	784.4 ppm
Nox/ SRM 2735	Cal015838	767.5 ppm
CO/ GMIS	EB0019151	1.96%
Propane/ GMIS	CC80938	2984 ppm
Methane/ GMIS	EB0028384	148.3 ppm

Instrument-

Instrument/ Model	Serial Number	Last Date Calibrated	Analytical Method
California Analytical Instrument Model 600	Y06003	01/05/2012	Chemiluminescence
Agilent Quad Series Rosemount 880A	US02002031 F-04300088	01/11/12 01/04/2012	Thermal Conductivity Non-Dispersive Infrared

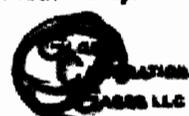
These mixtures were prepared gravimetrically using a high load high sensitivity electronic scale. Prior to filling the scale is verified for accuracy throughout the target mass range against applicable NIST traceable weights.

We certify that the weights are calibrated to ASTM E817-97 Class 1 tolerances. This calibration is referenced by serial # 7210-1, Certificate # 511635 and NIST Inst # 822/272103-06.

This report states accurately the results of the investigation made upon the material submitted to the analytical laboratory. Every effort has been made to determine objectively the information requested. However, in connection with this report, Global Calibration Gases LLC shall have no liability in excess of the established charge for this service. Assayed at Global Calibration Gases LLC, Palmetto, Florida.

*Do not use this standard when cylinder pressure is below 150 psig.

Produced by:



Global Calibration Gases LLC
1500 15th Avenue Drive, East Suite# 109
Palmetto, Florida 34221
Accreditation No.: 69191
PGVP Vendor ID.: N12012

Principal Analyst: [Signature]
Date: 1-11-12

Principal Reviewer: [Signature]
Date: 1-11-12

Nolan, Shiver

From: Heap, James K
Sent: Monday, May 12, 2014 3:08 PM
To: 'stacktest.aqb@state.nm.us'; Nolan, Shiver
Cc: Thompson, Roger A; Babinski, Dina J.; Sage, Sondra, NMENV (Sondra.Sage@state.nm.us); Morris, Allan, NMENV
Subject: Annual Monitoring Report
Attachments: 14-0152-2_EPROD_SCarlsbad_T2_AnnualReport.pdf; 14-0152-1_EPROD_SCarlsbad_T1_AnnualReport.pdf; Test Report T1&T2 Annual monitoring MAY2014.pdf

Pursuant to Section A205 of Permit P130-R2, attached is the submittal form and Periodic Test-report for:
Enterprise Field Services LLC
South Carlsbad Compressor Station
AIRS: 350150044, Operating Permit (Title V): P130-R2

If you have any questions or require further information, please contact me using the info below.

Regards

++++
Jim Heap Sr. Field Environmental Scientist
Enterprise Products, LLC
Midland, Texas USA
Office: 432-686-5404
Cell: 432-260-0239
jkheap@eprod.com



New Mexico Environment Department
 Air Quality Bureau
 1301 Siler Road Building B
 Santa Fe, NM 87507
 Phone (505) 476-4300 Fax (505) 476-4375



Version 1/1/2010

NMED USE ONLY	
DTS	
TEMPO	

UNIVERSAL STACK TEST NOTIFICATION, PROTOCOL AND REPORT FORM

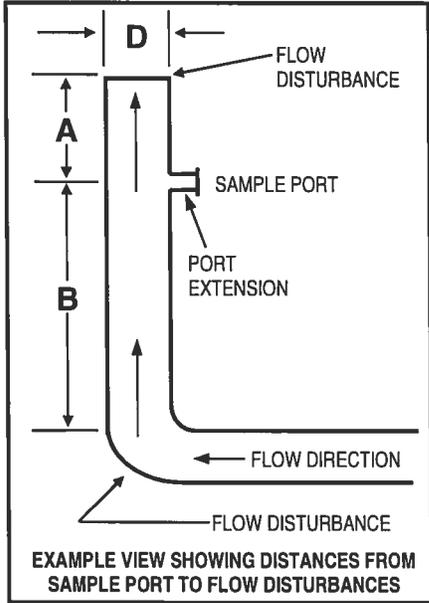
NMED USE ONLY	
Staff	
Admin	

Submit to: Stacktest.aqb@state.nm.us

I. DATABASE HEADER INFORMATION (drop down menus in bold)			
a. AI# 0218	Test Report		Periodic Test (EPA Method)
d. Company Name: Enterprise Field Services LLC		e. Facility Name: South Carlsbad Compressor Station	
f. Emission Unit Numbers: T1, T2		g. Emission Unit Description (boiler, Waukesha 7042, etc) Turbines: GE Solar T4702	
h. Reports - Tracking Number from notification response: CMT		i. Proposed Test Date: 30MAY2014	j. Actual test date: 03JAN14,04JAN14
k. Reason for test (name permit requirement, NSPS, MACT, consent decree, etc. Indicate here is this notification is a revised test date only) Annual Performance Test of existing engines pursuant to Title V Permit A205 A.			

II. GENERAL COMPANY AND FACILITY INFORMATION					
a. Company Address: PO Box 4324			k.. Facility Address: Roberson Road, Eddy County		
b. City: Houston	c. State: TX	d. Zip: 77210^L	l. City: Loving	m. State: NM	n. Zip: 88526
e. Environmental Contact: Jim Heap	f. Title: Sr. Env. Scientist		o. Facility Contact: Dave Kresta	p. Title: Area Mgr. - OPS	
g. Phone Number: 432-686-5404	h. Cell Number: 432-260-0239		q. Phone Number: 432-943-1801	r. Cell Number: 325-277-5728	
i. Email Address: jkheap@eprod.com			s. Email Address: dkresta@eprod.com		
j. Title V Permit Number: P-130-R2			t. NSR Permit Number: 0220-M7		
u. Detailed driving directions from nearest New Mexico town: From Loving: US385N to Roberson Road West Roberson Road west to station.					

III. TESTING FIRM					
a. Company: Nordon Corporation			g. Contact: Shunil Jacob		
b. Address 1: PO Box 1415			h. Title: Operations Manager		
c. Address 2:			i. Office Phone: 512-355-3786	j. Cell Phone: 512-750-9226	
d. City: Round Rock	e. State: TX	f. Zip: 78680	k. Email Address: shunil@nordoncorp.com		

IV. EMISSION UNIT			STACK PARAMETERS	
a. Emission Unit Number: 1 and 2	b. Make & Model Number GE Solar Centaur T-4702		m. Velocity (ft/sec):	
c. Serial Number: 1. OHD10C7915, 2. OHE12C7057	d. Permitted Capacity: 3609 hp		n. Temperature (°C):	
e. Exceptions: Explain if test is late, rescheduled, related to an enforcement action: NA			o. Stack Diameter, D (in.):	
			p. Distance to Stack Bends or Obstructions: Upstream, Distance A (in.): Downstream, Distance B (in.):	
g. Emission Unit Description and brief process name or description: Natural-gas fired turbines and compressors, processing field gas.			 <p style="text-align: center;">EXAMPLE VIEW SHOWING DISTANCES FROM SAMPLE PORT TO FLOW DISTURBANCES</p>	
i. Control Equipment Description as listed in permit (model, ser. # etc. if applicable): NA				
Attach an explanation or drawing to explain any difficult or unusual stack geometry or parameters.				

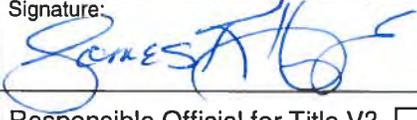
V. POLLUTANTS AND PROPOSED TEST METHODS			
Pollutant or Parameter:	Proposed Test Methods (Deviations from approved methods require supporting documentation and prior authorization)		Deviation to Test Method Requested
<input type="checkbox"/>	Portable Analyzer Methods for NOx, CO, SO₂		<input type="checkbox"/>
<input checked="" type="checkbox"/>	NOx	EPA Method 7E	<input type="checkbox"/>
<input checked="" type="checkbox"/>	CO	EPA Method 10	<input type="checkbox"/>
<input type="checkbox"/>	SO ₂	EPA Method 6	<input type="checkbox"/>
<input type="checkbox"/>	VOCs	(Specify)	<input type="checkbox"/>
<input type="checkbox"/>	HAPs	(Specify)	<input type="checkbox"/>
<input type="checkbox"/>	PM (TSP)	EPA Method 5	<input type="checkbox"/>
<input type="checkbox"/>	PM ₁₀	EPA Method 201	<input type="checkbox"/>
<input type="checkbox"/>	PM _{2.5}	(Specify)	<input type="checkbox"/>
<input type="checkbox"/>	Opacity	EPA Method 9	<input type="checkbox"/>
<input type="checkbox"/>	Visual E.	EPA Method 22	<input type="checkbox"/>
<input type="checkbox"/>	Stack Flow	EPA Methods 1 - 3	<input type="checkbox"/>
<input type="checkbox"/>	Moisture	EPA Method 4	<input type="checkbox"/>
<input checked="" type="checkbox"/>	Other	(Specify) Method 3A (O₂)	<input type="checkbox"/>
<input checked="" type="checkbox"/>	Other	(Specify) Method 19 (Stack Flow)	<input type="checkbox"/>
List Specific VOC's and HAP's:			

VI. PROPOSED TEST RUN AND TEST LOAD INFORMATION			
a. Number of Test Runs: 3	b. Run Duration 00:30:00	c. Required by (regulation or permit number): Title V Permit P130-R2	d. Specific Condition or Section: A205 A.
PLEASE NOTE – Default run duration is 60 minutes, unless otherwise specified by an applicable regulation.			
e. Expected Load:	f. Percent of Permitted Capacity: 90-110%	g. Is this an opacity test? Yes <input type="checkbox"/> No <input checked="" type="checkbox"/>	h. If yes, no. of observation pts.:
i. If expected load during test is less than 90% of capacity, explain:			
NOTE – Failure to test at 90-100% of permitted load will limit unit operation to 110% of tested load until a new initial compliance test is conducted.			
PLANT OR UNIT OPERATING PARAMETERS TO BE MONITORED			
j. List and explain the plant operating parameters that will be monitored and applicable permit conditions or regulatory standards. Stack emissions of NOx and CO			

VII. ADDITIONAL DETAILS (where applicable)		
RATA and INSTRUMENTAL ANALYZER CALIBRATION PROCEDURES		
a. Do any of the methods you are proposing utilize instrumental analyzers (i.e.; EPA Methods 3A, 6C, 7E, 10, 18, 25/25A, 320 etc.)? If yes, briefly describe analyzer calibration procedures and/or calibration standard procedures. Enter the highest pollutant concentration expected and the proposed concentrations of calibration gases.	<input type="checkbox"/> Yes	<input checked="" type="checkbox"/> No
SAMPLING TRAIN LEAK CHECK PROCEDURES		
b. Do any of the methods you are proposing utilize the EPA Method 5 sampling train (i.e.; EPA Methods 1-4, 5, 17, 26/26A, 29, etc.)? If yes, briefly describe sampling train and pitot tube leak check procedures:	<input type="checkbox"/> Yes	<input checked="" type="checkbox"/> No
EPA METHOD 19 IN LIEU OF EPA METHODS 1-4		
c. Are you proposing to utilize EPA Method 19 in lieu of EPA Methods 1-4? If yes, explain why you believe this proposal is justified:	<input checked="" type="checkbox"/> Yes	<input type="checkbox"/> No
Method 19 is being used to avoid specific safety concerns regarding the uninsulated stack (burn hazard).		
PLEASE NOTE – EPA Method 19 may be utilized in lieu of EPA Methods 1-4, subject to the approval of the Department. If you are proposing to utilize EPA Method 19 in lieu of EPA Methods 1-4, you MUST include a recent fuel gas heating value analysis as well as a recent fuel flow meter calibration certificate, preferably conducted on the day of the test, but no earlier than three months prior to the test date. If the analyses have been conducted prior to the test date, you MUST append the certificates to the protocol. If conducted on the day of the test, you MUST append the certificates to the final test report.		

**UNIVERSAL STACK TEST NOTIFICATION,
PROTOCOL AND REPORT FORM**

VIII. ATTACHMENTS (as needed to support proposed test; check all that apply)	
NOTIFICATION/PROTOCOL ATTACHMENTS	
<input type="checkbox"/>	Road Map Indicating Directions from Nearest New Mexico Town to Facility
<input type="checkbox"/>	Schematic of process being tested showing emission points, sampling sites and stack cross-section
<input type="checkbox"/>	Copy of proposed test methods (except for those promulgated test methods found in 40 CFR 51, 60, 61 and 63)
<input type="checkbox"/>	Fuel Heating Value Analysis
<input type="checkbox"/>	Fuel Flow Meter Calibration Certificate
<input type="checkbox"/>	Other:
<input type="checkbox"/>	Other:
TEST REPORT ATTACHMENTS	
<input checked="" type="checkbox"/>	Section 2. Tables of Results
<input type="checkbox"/>	Supporting Documents (Specify)
Retain Report Section 3 - Test Procedures, Data, Calculations, Appendices – 2 years NSR permits, 5 years TV	

IX. CERTIFICATION		
This document has been prepared under my supervision and is accurate and complete to the best of my knowledge. I understand that acceptance of this protocol does not waive the requirements of any permit or regulation. I understand that any procedural errors or omissions are the sole responsibility of the permit holder.		
Signature: 	Print Name and Title: James K. Heap, Senior Environmental Scientist	Date: 12MAY2014
Responsible Official for Title V? <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No (R.O signature not required for routine periodic testing)		

Heap, James K

From: Sage, Sondra, NMENV <Sondra.Sage@state.nm.us>
Sent: Thursday, May 01, 2014 4:11 PM
To: Heap, James K
Cc: Morris, Allan, NMENV; Samaniego, Robert, NMENV
Subject: FW: Test Substitution Request

Mr. Heap,

Following a review of the additional information you provided regarding the previous periodic test, it appears that the test conducted for Initial GG compliance falls within the required timeframe for the Annual Monitoring test. If you wish to reformat the results and use them for the Annual Monitoring Test, please submit a test protocol showing the test as the Annual Monitoring Test, then submit the results in the appropriate format. This will essentially qualify as a case of enforcement discretion, since it will require waiving the 30 day notice for the test, as well as the requirement to report the test in a timely manner. This acceptance of the GG Initial Test results for the Annual Monitoring Test is applicable only to this instance. If, in future, you wish to use the results of a single testing event to comply with two requirements, it will be necessary to submit timely testing notifications and testing results indicating this is the case. It will not be acceptable to request this after the fact in future instances.

Sondra Sage
Compliance Specialist
NMED-Air Quality Bureau
525 Camino de los Marquez, Suite 1
Santa Fe, NM 87505
(505)476-4358

*"Never cruel nor cowardly. Never give up,
never give in." - the Doctor*

From: Morris, Allan, NMENV
Sent: Wednesday, April 30, 2014 10:30 AM
To: Sage, Sondra, NMENV
Cc: Samaniego, Robert, NMENV
Subject: FW: Test Substitution Request

From: Heap, James K [<mailto:JKHEAP@eprod.com>]
Sent: Tuesday, April 29, 2014 6:11 PM
To: Morris, Allan, NMENV; Nolan, Shiver
Cc: Thompson, Roger A; Babinski, Dina J.; Shunil Jacob
Subject: Test Substitution Request

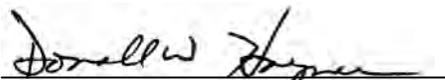
Pursuant to your request during our phone call today, I am providing you detail regarding Enterprise's desire to utilize our January Initial GG test for the permit required Annual Monitoring Test at the South Carlsbad Compressor Station (0218).

Annual Emission Test Report
for one
Solar Centaur T4702 Compressor Turbine
Unit Number T1
located at the
South Carlsbad Compressor Station

Prepared for
Enterprise Field Services, LLC
P. O. Box 4324
Houston, TX 77210

January 2014
Nordon Project No. 14-0152-1

This test report has been reviewed and approved for submittal to the New Mexico Environment Department (NMED) by the following representatives:



Donald W. Haynes
Nordon Corporation

Enterprise Field Services, LLC

 **NORDON** CORPORATION

P. O. Box 1415 Round Rock, Texas 78680
Phone (512) 355-3786 Fax (512) 355-3785

SUMMARY OF RESULTS

Exhaust emission testing was performed on one Solar Centaur T4702 (Unit # T1) compressor turbine for Enterprise Field Services, LLC located at the South Carlsbad Compressor Station, near Loving, Eddy County, New Mexico. The turbine is used for natural gas compression. The testing was performed to demonstrate the continued compliance with the emission limits set forth in the NMED permit. Nordon Corporation of Round Rock, Texas, performed the exhaust emissions testing on January 3, 2014.

Continuous emission instruments housed in a mobile analysis unit were used to determine the concentrations of NO_x , CO, and O_2 in the exhaust stack of the compressor turbine. The following Code of Federal Regulations, Title 40, Part 60 (40CFR60), Appendix A reference methods were used to determine stack gas concentrations: Method 7E for nitrogen oxides (NO_x), Method 10 for carbon monoxide (CO), and Method 3A for oxygen (O_2). Mass emission rates were determined stoichiometrically according to Method 19 data reduction procedures using measured fuel flow rate.

Three thirty-minute test runs were performed on the exhaust of the turbine while firing on natural gas. The results of the testing are presented in a summary of results table. This table includes all the relevant information pertaining to the turbine/compressor operations, exhaust emissions, and ambient conditions. Exhaust concentrations are presented in part per million by volume (ppmv) or percent (%) by volume. The mass emission rates are presented in pound per hour (lb/hr) and ton per year (tpy). Turbine/compressor operational data was collected during each test run.

Summary of Results

NORDON CORPORATION

P.O. Box 1415 Round Rock, Texas 78680
PHONE (512) 355-3786 • FAX (512)355-3785

Plant: South Carlsbad Compressor Station
 Facility Owner:Enterprise Field Services, LLC
 Location: Loving, Eddy County, New Mexico
 Unit Make/Model: Solar Centaur T4702
 Unit Number: T1 , Ser. No.OHD10C7915
 Test Personnel: DWH / KRJ

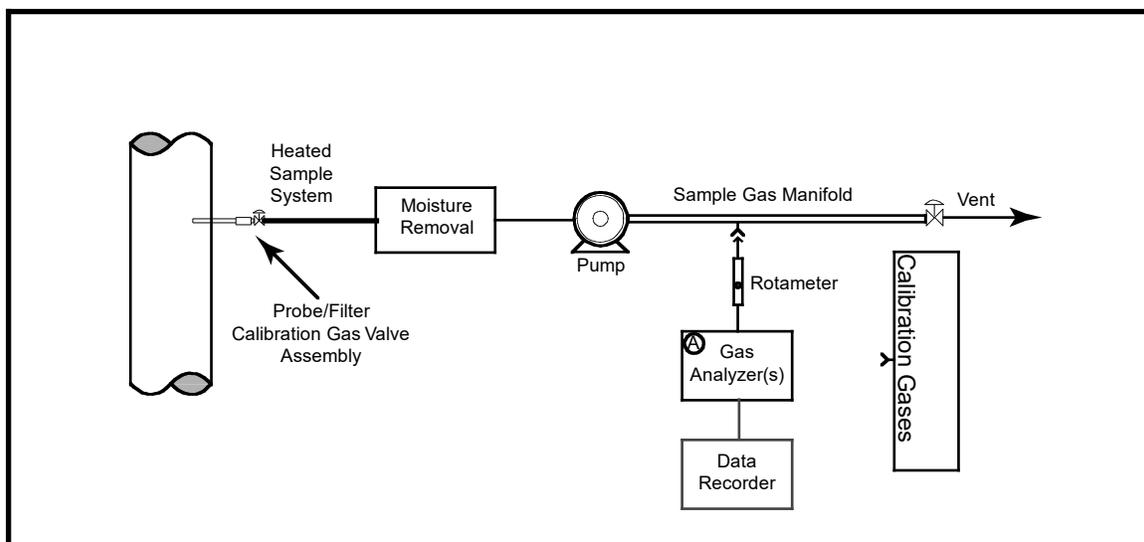
RUN NUMBER	DH-010314.01	DH-010314.02	DH-010314.03	
Date	1/3/14	1/3/14	1/3/14	
Start Time (hr)	9:23	10:12	10:49	
Stop Time (hr)	10:04	10:42	11:19	
TURBINE DATA				
Rated Horsepower (Hp)	3609	3609	3609	
Fuel Pressure (psig)	193	195	207	
Gas Producer Speed (%)	94.8	94.8	94.8	
Power Turbine Speed (%)	92.8	92.3	91.9	
Turbine Compressor Discharge Pressure (psig)	105	104	102	
Exhaust Temperature (°F)	1078	1082	1091	
Horsepower (Hp)	3508	3478	3418	
Heat Rate (MMBtu/hr)	43.0	43.0	42.4	
COMPRESSOR DATA				
Suction Pressure (psig)	293	294	295	
Suction Temperature (°F)	58	62	64	
Discharge Pressure (psig)	529	532	535	
Discharge Temperature (°F)	145	147	148	
Gas Production (MMscfd)	37	38	37	
FUEL & EXHAUST DATA				
O2 F-factor (dscf/MMBtu)	8698	8698	8698	
Fuel Heating Value (HHV Btu/scf)	1098	1098	1098	
Stoichiometric Exhaust Flow (dscfh)	1.94E+06	1.96E+06	1.96E+06	
AMBIENT CONDITIONS				
Temperature (°F): Dry bulb	39	44	47	
Temperature (°F): Wet bulb	32	37	39	
Atmospheric Pressure ("Hg)	26.90	26.88	26.84	
Humidity (lb water/lb air)	0.0026	0.0035	0.0037	
Humidity (% vol)	0.4	0.5	0.6	
MEASURED EXHAUST OUTLET CONCENTRATIONS				AVERAGES
NOx (ppmv)	74.0	74.1	75.0	74.4
CO (ppmv)	15.2	14.0	13.7	14.3
O2 (%)	16.9	16.9	17.0	16.9
EMISSION RATES				
NOx (lb/hr) LIMIT=27.0	17.14	17.36	17.57	17.35
CO (lb/hr) LIMIT=7.4	2.14	2.00	1.95	2.03
NOx (tpy, @8760 hr/yr) LIMIT=118.3	75.06	76.03	76.95	76.01
CO (tpy, @8760 hr/yr) LIMIT=32.5	9.39	8.77	8.55	8.91

PROCEDURES

Continuous emission instruments housed in the mobile analysis unit were used to determine the concentrations of pollutants found in the turbine exhaust stack. The following 40CFR60, Appendix A reference methods were used to determine stack gas concentrations: Method 7E for NO_x , Method 10 for CO, and Method 3A for O_2 . Mass emission rates were determined according to data reduction procedures provided in Method 19.

As depicted in Figure 1, Sample System and Instrumentation, a stainless steel sample probe was located in the centroid of the stack. Sample gas enters the stainless steel probe into a stainless steel 3-way valve. The 3-way valve is used to perform leak checks and sample system bias checks. From the valve, the gas flows through a 3/8" Teflon® heat traced sample line to a stainless steel minimum contact condenser to dry the sample. From the condenser, a 3/8" Teflon sample line brings the exhaust gas to a manifold in the mobile analysis unit via a Teflon-lined diaphragm pump. The manifold partitions the gas through quick-connects so that each instrument can directly sample exhaust gas. Each instrument is equipped with a rotameter to maintain correct sample pressure and flow. The instruments are connected to a computer data acquisition system to document its response during quality assurance activities and testing.

Figure 1: Sample System and Instrumentation



(A) Gas Analyzers - NO_x , CO, O_2

Analyzer Make	Analyzer Model	Detection Principle
<i>NO_x Analyzer:</i> Thermo Environmental	42i-HL	Chemiluminescence
<i>CO Analyzer :</i> Thermo Environmental	48i-HL	Non-dispersive Infra-red
<i>O₂ Analyzer:</i> Thermo Environmental	48i-HL	Paramagnetic Cell

A continuous analyzer is used to determine NO_x concentrations according to EPA Reference Method 7E. This instrument employs a chemiluminescent detection principle. The NO_x concentration and mass emission rates are expressed as NO₂ per the reference method.

A continuous analyzer is used to determine CO concentrations according to EPA Reference Method 10. The instrument employs a nondispersive infrared detector coupled to a gas filter correlation wheel, which eliminates the interferences due to water and carbon dioxide.

A continuous analyzer is used to determine O₂ concentrations according to EPA Reference Method 3A. The instrument is equipped with either an electrochemical or paramagnetic cell.

Data obtained from the continuous emission analyzers were recorded by a National Instruments data acquisition (DAQ) system using Labview software. A copy of the DAQ records can be found in the appendix of this report.

Quality assurance activities meeting the requirements of the EPA reference methods were performed during the turbine testing. Tables documenting quality assurance procedures are located in the appendix of this report.

Exhaust flow rate was determined according to the data reduction procedures provided in EPA Method 19. The O₂ F-Factor used in the emission rate calculation was either calculated based on a recent fuel analysis or the standard 8710 value for natural gas provided by EPA Method 19.

Nordon personnel recorded turbine compressor operating parameters. Ambient conditions were collected using a wet/dry bulb sling psychrometer to measure temperature and a barometer to measure absolute atmospheric pressure.

APPENDIX

Field Data Sheets
Example Calculations
Gas Certifications
Quality Assurance Activities
DAQ Records

C1 86.873
 C2 6.8402
 C3 2.5624
 n-C4 0.5497
 i-C4 0.2817
 n-C5 0.0813
 i-C5 0.0128
 C6 0.0534
 C7+ 0.0813
 N2 1.1928
 CO2 1.4528

Plant: South Carlshad Compressor Station
 Facility Owner: Enterprise
 Unit Owner: Enterprise
 Location: Loving, Eddy County, New Mexico
 Applicable Regulation: 40CFR60, Subpart GG
 Unit Make/Model: Solar Centaur T-4702
 Unit Number: T1
 Test Personnel: DWH/KRJ
 Ser. No. OHD10C7915
 Date: 1/3/14

Run Number	01	02	03	04	05	06	07	08	09	10	11	12
Start Time	10:23	14:20	14:49	12:26	12:03	13:40	14:47	14:24	14:31	15:08	15:45	16:22
Stop Time	9:23	10:12	10:49	11:26	12:03	12:40	13:17	13:54	14:31	15:08	15:45	16:22
Turbine/Compressor Operation												
Load Condition	Max	Max	Max	847	871	865	652	890	874	636	741	677
Fuel Flow (Mscfd)	941	941	926	914	909	906	901	894	891	893	892	898
Fuel Flow (scfh)	72.8	92.3	91.9	91.4	90.9	90.6	90.1	89.4	89.1	89.3	89.2	89.8
Power Turbine Speed (%)	94.8	94.8	94.8	94.7	94.8	94.8	94.8	94.8	94.7	94.8	94.8	94.8
Gas Producer Speed (%)	3609	3609	3609	3609	3609	3609	3609	3609	3609	3609	3609	3609
Horsepower (hp)	105	104	102	102	100	99	98	98	97	98	98	100
Rated Horsepower (hp)	1078	1082	1091	1092	1100	1102	1109	1111	1113	1106	1104	1103
% Load	29.5	29.4	29.5	29.6	30.0	30.4	30.7	31.1	31.3	31.4	31.4	31.3
Turbine Compressor Discharge, PCD (psig)	58.521	53.2	53.5	53.5	52.3	52.1	52.3	52.4	52.6	52.7	52.9	53.1
Turbine Temperature T5 (°F)	58	62	64	64	68	70	72	74	74	76	72	70
Gas Compressor Suction Pressure (psig)	145	147	148	148	151	152	152	153	155	156	151	148
Gas Compressor Discharge Pressure (psig)	193	195	207	191	189	190	195	191	195	191	189	192
Gas Compressor Suction Temperature (°F)	27.37	38	37	38	37	37	37	37	37	38	39	40
Fuel Gas Pressure (MMscfd)	2880	2900	2440	2960	3000	3020	3050	3060	3060	3080	3080	3100
Gas Flow (MMscfd)	26.40	24.86	26.84	26.82	24.78	26.74	26.74	26.72	24.72	26.5	26.3	25.5
Ambient Conditions	3.1	4.1	4.7	4.4	5.5	6.0	6.2	6.7	6.8	6.5	6.3	5.5
Barometric Pressure (absolute in. Hg)	3.2	3.1	3.1	4.0	4.3	4.6	4.7	4.9	4.9	4.8	4.7	4.4
Temperature Dry (°F)												
Temperature Wet (°F)												

C



Certificate of Analysis

Number: 1030-14010388-001A

Houston Laboratories

8820 Interchange Drive

Houston, TX 77054

Phone 713-660-0901

Thor Olsen
Nordon Corporation
PO Box 1415
Round Rock, TX 78680

Jan. 21, 2014

Station Name: South Calrsbad Compressor Stition
Station Location: Loving, NM
Sample Point: Turbine Fuel Gas
Cylinder No: 0298
Analyzed: 01/16/2014 05:34:22 by JD

Sampled By:
Sample Of: Gas Spot
Sample Date: 01/04/2014 10:00
Sample Conditions: 190 psig, @ 65 °F
Method: GPA-2261M

Analytical Data

Components	Mol. %	Wt. %	GPM at 14.65 psia		
Nitrogen	1.204	1.797		GPM TOTAL C2+	2.870
Carbon Dioxide	1.556	3.648		GPM TOTAL C3+	1.036
Methane	86.800	74.184		GPM TOTAL iC5+	0.077
Ethane	6.877	11.016	1.834		
Propane	2.516	5.911	0.691		
Iso-butane	0.292	0.904	0.095		
n-Butane	0.552	1.709	0.173		
Iso-pentane	0.086	0.331	0.031		
n-Pentane	0.072	0.277	0.026		
Hexanes Plus	0.045	0.223	0.020		
	100.000	100.000	2.870		

Physical Properties	Total	C6+
Relative Density Real Gas	0.6496	3.2176
Calculated Molecular Weight	18.77	93.19
Compressibility Factor	0.9973	
GPA 2172-09 Calculation:		
Calculated Gross BTU per ft³ @ 14.65 psia & 60°F		
Real Gas Dry BTU	1097	5113
Water Sat. Gas Base BTU	1078	5024

Comments: H2O Mol% : 1.750 ; Wt% : 1.681
Reran Sample Confirmed GC Analysis

Hydrocarbon Laboratory Manager

Quality Assurance: The above analyses are performed in accordance with ASTM, UOP, GPA guidelines for quality assurance, unless otherwise stated.

Fuel Gas Analysis

Gross Btu/scf 1098 O₂ F-Factor dscf/MMBtu 8698 O₂ F-Factor (wscf/MMBtu) 10660 H₂O F-Factor (scf/MMBtu) 1962 CO₂ F-Factor (scf CO₂/MMBtu) 1058
Btu/lb 22164 Sp. Gr. 0.6516
F_o 1.719 Moisture Factor 18.407 VOC Fraction 0.063

Compound	Mol. Formula	Mol. %
Methane	CH ₄	86.800
Ethane	C ₂ H ₆	6.877
Propane	C ₃ H ₈	2.516
Isobutane	C ₄ H ₁₀	0.292
n-Butane	C ₄ H ₁₀	0.552
Isopentane	C ₅ H ₁₂	0.086
n-Pentane	C ₅ H ₁₂	0.072
NeoPentane	C ₅ H ₁₂	
n-Hexane	C ₆ H ₁₄	0.045
n-Heptane	C ₇ H ₁₆	
n-Octane	C ₈ H ₁₈	
Carbon dioxide	CO ₂	1.556
Nitrogen	N ₂	1.204
Total		100.000

Example Calculations: Method 7E Concentration Correction

Test Run #: DH-010314.01

Component: NOx

Observed Measurements/Data:	Scale, Certified Concentrations
Direct Calibration Results	
0.17 NOx direct zero, Cdiro	94.7 NOx chart scale, CS
95.20 NOx direct span, Cdirn	94.7 NOx actual calibration gas concentration, Cma
System Calibration Results	0 Actual low-level gas concentration, Coa
2.74 NOx, initial zero reading, Csoi	
92.63 NOx initial span reading, Csmi	
2.72 NOx final zero reading, Cof	
91.44 NOx final span reading, Csmf	
Run Results	
72.48 NOx run average, Caverage	

Bias Check Initial Zero (SBoi)

$$SBoi = \frac{(Csoi - Cdiro)}{CS}$$

$$= 2.71 \%$$

Bias Check Initial Span (SBmi)

$$SBmi = \frac{(Csmi - Cdirn)}{CS}$$

$$= -2.72 \%$$

Bias Check Final Zero (SBof)

$$SBof = \frac{(Csof - Cdiro)}{CS}$$

$$= 2.69 \%$$

Bias Check Final Span (SBmf)

$$SBmf = \frac{(Csmf - Cdirn)}{CS}$$

$$= -3.97 \%$$

Drift Check Zero (Do)

$$|SBof - SBoi|$$

$$= 0.03$$

Drift Check Span (Ds)

$$|SBmf - SBmi|$$

$$= 1.26$$

Bias-Average Zero (Coavg)

$$= \left(\frac{Csoi + Csof}{2} \right)$$

$$= 2.730 \text{ (ppmv)}$$

Bias-Average Span (Cmavg)

$$= \left(\frac{Csmi + Csmf}{2} \right)$$

$$= 92.04 \text{ (ppmv)}$$

NOx Concentration Correction

$$= (Caverage - Coavg) \times \left(\frac{Cma}{Cmavg - Coavg} \right)$$

$$74.0 \text{ (ppmv)}$$

Example Calculations: Method 7E Concentration Correction

Test Run #: DH-010314.01

Component: CO

Observed Measurements/Data:		Scale, Certified Concentrations	
Direct Calibration Results			
-0.02	CO direct zero, Cdiro	193	CO chart scale, CS
193.21	CO direct span, Cdirm	193	CO actual calibration gas concentration, Cma
System Calibration Results			
-0.71	CO, initial zero reading, Csoi	0	Actual low-level gas concentration, Coa
192.18	CO initial span reading, Csmi		
-1.00	CO final zero reading, Cof		
191.53	CO final span reading, Csmf		
Run Results			
14.33	CO run average, Caverage		

Bias Check Initial Zero (SBoi)

$$SBoi = \frac{(Csoi - Cdiro)}{CS}$$

$$= -0.35 \%$$

Bias Check Initial Span (SBmi)

$$SBmi = \frac{(Csmi - Cdirm)}{CS}$$

$$= -0.53 \%$$

Bias Check Final Zero (SBof)

$$SBof = \frac{(Csof - Cdiro)}{CS}$$

$$= -0.50 \%$$

Bias Check Final Span (SBmf)

$$SBmf = \frac{(Csmf - Cdirm)}{CS}$$

$$= -0.87 \%$$

Drift Check Zero (Do)

$$|SBof - SBoi|$$

$$= 0.15$$

Drift Check Span (Ds)

$$|SBmf - SBmi|$$

$$= 0.34$$

Bias-Average Zero (Coavg)

$$= \left(\frac{Csoi + Csof}{2} \right)$$

$$= -0.851 \text{ (ppmv)}$$

Bias-Average Span (Cmavg)

$$= \left(\frac{Csmi + Csmf}{2} \right)$$

$$= 191.85 \text{ (ppmv)}$$

CO Concentration Correction

$$= (Caverage - Coavg) \times \left(\frac{Cma}{Cmavg - Coavg} \right)$$

$$= 15.2 \text{ (ppmv)}$$

Example Calculations: Method 7E Concentration Correction

Test Run #: DH-010314.01

Component: O2

Observed Measurements/Data:		Scale, Certified Concentrations	
Direct Calibration Results			
0.05	O2 direct zero, Cdiro	20.92	O2 chart scale, CS
11.02	O2 direct span, Cdirm	10.99	O2 actual calibration gas Concentration, Cma
System Calibration Results			
0.05	O2, initial zero reading, Csoi	0	Actual low-level gas Concentration, Coa
10.98	O2 initial span reading, Csmi		
0.16	O2 final zero reading, Csof		
10.99	O2 final span reading, Csmf		
Run Results			
16.81	O2 run average, Caverage		

Bias Check Initial Zero (SBoi)

$$SBoi = \frac{(Csoi - Cdiro)}{CS}$$

$$= 0.03 \%$$

Bias Check Initial Span (SBmi)

$$SBmi = \frac{(Csmi - Cdirm)}{CS}$$

$$= -0.18 \%$$

Bias Check Final Zero (SBof)

$$SBof = \frac{(Csof - Cdiro)}{CS}$$

$$= 0.55 \%$$

Bias Check Final Span (SBmf)

$$SBmf = \frac{(Csmf - Cdirm)}{CS}$$

$$= -0.16 \%$$

Drift Check Zero (Do)

$$|SBof - SBoi|$$

$$= 0.51$$

Drift Check Span (Ds)

$$|SBmf - SBmi|$$

$$= 0.02$$

Bias-Average Zero (O2avg)

$$= \left(\frac{Csoi + Csof}{2} \right)$$

$$= 0.107 \%$$

Bias-Average Span (Cmavg)

$$= \left(\frac{Csmi + Csmf}{2} \right)$$

$$= 10.99 \%$$

O2 Concentration Correction

$$= (Caverage - Coavg) \times \left(\frac{Cma}{Cmavg - Coavg} \right)$$

$$16.9 \%$$

Example Calculations: Method 19 Exhaust Flow

Test Run #: DH-010314.01

Component: Stack Flow

Observed Measurements/Data:		Standards/Constants/Conversion Factors
39208	Fuel Flow Rate (scfh)	1000000 Btu per MMBtu
8698	Fuel O ₂ F-Factor (dscf/MMBtu)	20.9 O ₂ % in air
1098	Fuel Heating Value (Btu/scf)	
16.9	O ₂ final concentration (%)	

Derivation of Exhaust Flow using Equation 19-1 from Method 19

$$E \left(\frac{lb}{MMBtu} \right) = C_d \left(\frac{lb}{scf} \right) F_d \left(\frac{dscf}{MMBtu} \right) \times \frac{20.9}{(20.9 - \%O_2)} \quad \text{Eq. 19-1}$$

divide each side of equation by Cd to obtain the following

$$\left(\frac{scf}{MMBtu} \right) = F_d \left(\frac{dscf}{MMBtu} \right) \times \frac{20.9}{(20.9 - \%O_2)}$$

multiply each side of equation by heat input (MMBtu/hr)

$$\left(\frac{scf}{hr} \right) = HeatInput \left(\frac{MMBtu}{hr} \right) \times F_d \left(\frac{dscf}{MMBtu} \right) \times \frac{20.9}{(20.9 - \%O_2)}$$

Fuel Gas Heat Rate/Heat Input (MMBtu/hr)

$$= \left(\text{Fuel Flow Rate} \frac{scf}{hr} \right) \times \left(\text{Fuel Heating Value} \frac{Btu}{scf} \right) \times \left(\frac{1MMBtu}{1000000Btu} \right)$$

= 43.04 (MMBtu/hr)

Stack Gas Volumetric Flow Rate, Q (dscfh)

$$= \left(\text{HeatInput} \frac{MMBtu}{hr} \right) \times \left(\text{Fuel O}_2 \text{ F-Factor} \frac{dscf}{MMBtu} \right) \times \left(\frac{20.9}{20.9 - O_2} \right)$$

= 1.94E+06 (dscfh)

Example Calculations: Emissions Calculations

Test Run #: DH-010314.01

Component: NOx

Observed Measurements/Data:	Standards/Constants/Conversion Factors
74.0 NOx final concentration, Cd (ppmv)	528 EPA Standard Temperature, Tstd (°R)
1940680 Average Stack Gas Flow Rate, Q (DSCFH)	29.92 EPA Standard Pressure, Pstd (in. Hg)
16.9 O2 final concentration (%)	385.3 Gas Constant @ EPA STP (SCF/lb-mol)
3508 Horsepower (Hp)	28.317 Liters per Cubic Foot
8698 Fuel O2 Factor (DSCF/MMBtu)	46 NOx molecular wt. (NO2), MW (lb/lb-mol)
	0.001912 Conversion constant (NOx ppm to g/m3)
	8760 hours per year
	2000 pounds per ton
	0.028317 cubic meters per cubic feet

NOx Emissions (ppmv @ 15%O2): Applicable yes

$$= \text{ppmv@15\%O}_2 = Cd \times \left(\frac{20.9-15}{20.9-\text{O}_2 \text{ concentration (\%)}} \right)$$

= 108 ppmv @15% O2

NOx Emission Rate (g/hp-hr): Applicable no

$$= \left(\frac{\text{g}}{\text{HP-hr}} \right) = \frac{Cd \times .001912 \times Q \times \left(\frac{0.028317 \text{ m}^3}{\text{ft}^3} \right)}{HP}$$

= NOT APPLICABLE

NOx Emission Rate (lb/hr): Applicable yes

$$= \left(\frac{\text{ppmv}}{10^6} \right) \times \text{Average Stack Flow, Q} \times \left(\frac{MW}{385.3} \right)$$

= 17.14 (lb/hr)

NOx Emission Rate (tons/year): Applicable yes

$$= \left(\frac{\text{tons}}{\text{yr}} \right) = \frac{\text{lb}}{\text{hr}} \times \frac{8760 \text{ hr}}{\text{year}} \times \frac{\text{ton}}{2000 \text{ lb}}$$

= 75.06 (tons/yr)

NOx Emissions (lb/MMBtu): Applicable no

$$= \left(\frac{\text{lb}}{\text{MMBtu}} \right) = \left(\frac{Cd}{10^6} \right) \times \left(\frac{MW}{385.3} \right) \times \left(\frac{DSCF}{\text{MMBtu}} \right) \times \left(\frac{20.9}{(20.9-\text{O}_2 \text{ concentration (\%)})} \right)$$

= NOT APPLICABLE

Example Calculations: Emissions Calculations

Test Run #: DH-010314.01

Component: CO

Observed Measurements/Data:		Standards/Constants/Conversion Factors	
15.2	CO final concentration, Cd (ppmv)	528	EPA Standard Temperature, Tstd (°R)
1940680	Average Stack Gas Flow Rate, Q (DSCFH)	29.92	EPA Standard Pressure, Pstd (in. Hg)
16.9	O2 final concentration (%)	385.3	Gas Constant @ EPA STP (SCF/lb-mol)
3508	Horsepower (Hp)	28.317	Liters per Cubic Foot
8698	Fuel O2 Factor (DSCF/MMBtu)	28	CO molecular wt., MW (lb/lb-mol)
		0.001164	Conversion constant (CO ppm to g/m3)
		8760	hours per year
		2000	pounds per ton
		0.028317	cubic meters per cubic feet

CO Emissions (ppmv @ 15%O2): *Applicable* no

$$= \text{ppmv@15\%O}_2 = Cd \times \left(\frac{20.9-15}{20.9-\text{O}_2 \text{ concentration (\%)}} \right)$$

= **NOT APPLICABLE**

CO Emission Rate (g/hp-hr): *Applicable* no

$$= \left(\frac{\text{g}}{\text{HP-hr}} \right) = \frac{Cd \times .001164 \times Q \times \left(\frac{0.028317 \text{m}^3}{\text{ft}^3} \right)}{HP}$$

= **NOT APPLICABLE**

CO Emission Rate (lb/hr): *Applicable* yes

$$= \left(\frac{\text{ppmv}}{10^6} \right) \times \text{Average Stack Flow, Q} \times \left(\frac{MW}{385.3} \right)$$

= **2.14 (lb/hr)**

CO Emission Rate (tons/year): *Applicable* yes

$$= \left(\frac{\text{tons}}{\text{yr}} \right) = \frac{\text{lb}}{\text{hr}} \times \frac{8760 \text{ hr}}{\text{year}} \times \frac{\text{ton}}{2000 \text{ lb}}$$

= **9.39 (tons/yr)**

CO Emissions (lb/MMBtu): *Applicable* no

$$= \left(\frac{\text{lb}}{\text{MMBtu}} \right) = \left(\frac{Cd}{10^6} \right) \times \left(\frac{MW}{385.3} \right) \times \left(\frac{DSCF}{\text{MMBtu}} \right) \times \left(\frac{20.9}{(20.9-\text{O}_2 \text{ concentration (\%)})} \right)$$

= **NOT APPLICABLE**

THE LINDE GROUP

Linde

CERTIFICATE OF ANALYSIS

EPA PROTOCOL MIXTURE

PGVP ID#: I12013
 CUSTOMER: UNION CITY
 SALES#: 501210969
 PROD#: 1254051
 P.O.#: 4501210969
 MATERIAL#: 24091202
 CERTIFICATION DATE: 01-May-2013
 EXPIRATION DATE: 02-May-2021

PROCEDURE #: G1
 GAS CODE: APPVD
 CYLINDER #: CC-310704
 CYLINDER PRES: 2000 PSIG
 CYLINDER VALVE: CGA 660
 CYLINDER SIZE: 2A
 CYLINDER MATERIAL: Aluminum
 GAS VOLUME: 4000 Liter
 BLEND TOLERANCE: 5% Relative
 PAGE: 1 of 1

(Using the May 2012 Revision of the EPA Protocol)

CERTIFICATION HISTORY

COMPONENT	DATE OF ASSAY	MEAN CONCENTRATION	CERTIFIED CONCENTRATION	ANALYTICAL ACCURACY
Propane	01-May-2013	30.0 ppm	30.0 ppm	+/- 1%
Nitric Oxide	24-Apr-2013 01-May-2013	47.4 ppm 47.3 ppm	47.3 ppm	+/- 1%
NOx			47.3 ppm	Reference Value Only
Carbon Monoxide	01-May-2013	95.3 ppm	95.3 ppm	+/- 1%

BALANCE Nitrogen

PREVIOUS CERTIFICATION DATES: None

REFERENCE STANDARDS

COMPONENT	SRM/NTRM#	CYLINDER#	CONCENTRATION
Propane	GMIS-1	cc-113884	100.5 ppm
Nitric Oxide	GMIS-1	CC-278874	100.7 ppm
Carbon Monoxide	GMIS-1	cc-88590	96.8 ppm

INSTRUMENTATION

COMPONENT	MAKE/MODEL	SERIAL #	DETECTOR	CALIBRATION DATE(S)
Propane	H. Packard 6890	US00001434	GC - FID	01-May-2013
Nitric Oxide	CAI 400-CLD	6L09004	Cheml	01-Apr-2013
Carbon Monoxide	Horiba VIA-510	570423011	NDIR	19-Apr-2013

THIS STANDARD IS NIST TRACEABLE. IT WAS CERTIFIED ACCORDING TO THE 1997 EPA PROTOCOL PROCEDURES.
 DO NOT USE THIS STANDARD IF THE CYLINDER PRESSURE IS LESS THAN 100 PSIG.

ANALYST: MATTHEW JACKSON

Linde Gas North America LLC

DATE: 01-May-2013



Assay Laboratory: Red Ball TGS
 555 Craig Kennedy Way
 Shreveport, LA 71107
 800-551-8150

CERTIFICATE OF ANALYSIS EPA PROTOCOL GAS

Cylinder Number:	EB0027577	Certification Date:	10/29/2012
Product ID Number:	124749	Expiration Date:	10/22/2016
Cylinder Pressure:	1900 PSIG	MFG Facility:	RBTGS-Shreveport-LA
COA Number:	GC1210170814-0	Lot Number:	GC1210170814
Customer PO. NO.:		Tracking Number:	048358699
Customer:		Previous Certification Dates:	

This calibration standard has been certified per the 1997 EPA Traceability Protocol, Document EPA-600/97/121, using procedure G1 and/or G2. All values so noted are certified to be +/-1% NIST Traceable.

Do Not Use This Cylinder Below 150 psig (1.0 Megapascal).

Certified Concentration(s)

Component	Concentration	Analytical Principle	Accuracy
Nitric Oxide	94.5 PPM	Non Dispersive Infrared Absorptiometry	±0.1% NIST
Total Oxides of Nitrogen	94.7 PPM	Non Dispersive Infrared Absorptiometry	±0.1% NIST
Propane	51 PPM	FTIR	+/- 1% NIST
Carbon Monoxide	193 PPM	Gas Correlation Filter	+/- 1% NIST
Nitrogen	Balance		

Reference Standard(s)

Type	Component	Balance Gas	Concentration	Cylinder Number	Expiration	NIST Reference
GMIS	Nitric Oxide	Nitrogen	98.6 PPM	CC238350	2/14/2013	SRM 1686b
GMIS	Nitric Oxide	Nitrogen	98.6 PPM	CC238350	2/14/2013	SRM 1686b
GMIS	Carbon Monoxide	Nitrogen	398 PPM	EB0005726	1/5/2014	NTRM 021003
SRM	Propane	Nitrogen	49 PPM	CAL018150	8/17/2017	SRM 1667b

Analytical Information

Component	Nitric Oxide			
Analysis Date:	10/22/2012			
Z 0.152	S 16.337	C 15.549	Conc. 93.5 PPM	
S 16.399	C 15.733	Z 0.109	Conc. 94.6 PPM	
C 15.71	Z 0.088	S 16.451	Conc. 94.4 PPM	
Analysis Date:	10/29/2012			
Z 0.295	S 16.912	C 16.321	Conc. 94.9 PPM	
S 16.961	C 16.303	Z 0.281	Conc. 94.8 PPM	
C 16.31	Z 0.325	S 16.9825	Conc. 94.8 PPM	
Component	Carbon Monoxide			
Analysis Date:	10/22/2012			
Z 0.3390	S 41.027	C 19.9610	Conc. 192 PPM	
S 41.0170	C 20.021	Z 0.294	Conc. 193 PPM	
C 20.036	Z 0.3510	S 40.98	Conc. 193 PPM	
Component	Propane			
Analysis Date:	10/26/2012			
Z 0.0110	S 49.01	C 50.7800	Conc. 51 PPM	
S 49.0400	C 50.8	Z 0.004	Conc. 51 PPM	
C 50.8	Z 0.0060	S 49.03	Conc. 51 PPM	

Z= Zero Gas S= Span Gas C= Candidate Gas

Fred Holt

Fred Holt, CHMM
 Quality Control

Red Ball Technical Gas Service
 PGVP Vendor ID # G12012
 Information and Ordering
 800-551-8150
 Fax (318-425-6309)



Assay Laboratory: Red Ball TGS
 555 Craig Kennedy Way
 Shreveport, LA 71107
 800-551-8150

EPA PROTOCOL GAS CERTIFICATE OF ANALYSIS

Cylinder Number:	EB0046618	Certification Date:	07/29/2013
Product ID Number:	124752	Expiration Date:	07/27/2021
Cylinder Pressure:	1900 PSIG	MFG Facility:	RBTGS-Shreveport-LA
COA #	ML130726.170231.3-0	Lot Number:	ML130726.170231.3
Customer PO. NO.:		Tracking Number:	065271430
Customer:		Previous Certification Dates:	

This calibration standard has been certified per the May 2012 EPA Traceability Protocol, Document EPA-600/R-12/531, using procedure G1.

Do Not Use This Cylinder Below 100 psig (0.7 Megapascal).

Certified Concentration(s)			
Component	Concentration	Uncertainty	Analytical Principle
Carbon Dioxide	13.9 %	±0.11 %	NDIR
Oxygen	10.99 %	±0.07 %	MPA
Nitrogen	Balance		

Analytical Measurement Data Available Online.

Reference Standard(s)							
Lot	Expiration	Type	Balance	Component	Concentration	Uncertainty(%)	NIST Reference
GC1106080848	09/07/2013	GMIS	N2	CO2	12.57 %	0.384	3221755
GC0807251121	04/28/2019	GMIS	N2	O2	24.43 %	0.52	71001

Analytical Instrumentation						
Component	Analytical Principle	Make	Model	Serial	MPC Date	
CO2	NDIR	Horiba	VA-3013	H0000P11	07/10/2013	
O2	MPA	Horiba	VA-3013	H0000P11	07/11/2013	

Z= Zero Gas S= Span Gas C= Candidate Gas

Red Ball Technical Gas Service
 PGVP Vendor ID # G12013
 Information and Ordering
 800-551-8150
 Fax (318-425-6309)

Fred Holt
 Fred Holt, CHMM
 Quality Control



Assay Laboratory: Red Ball TGS
 555 Craig Kennedy Way
 Shreveport, LA 71107
 800-551-8150

EPA PROTOCOL GAS CERTIFICATE OF ANALYSIS

Cylinder Number:	EB0039038	Certification Date:	08/02/2013
Product ID Number:	124753	Expiration Date:	07/31/2021
Cylinder Pressure:	1900 PSIG	MFG Facility:	RB TGS-Shreveport-LA
COA #	ML130726.170120.1-0	Lot Number:	ML130726.170120.1
Customer PO. NO.:		Tracking Number:	065155673
Customer:		Previous Certification Dates:	

This calibration standard has been certified per the May 2012 EPA Traceability Protocol, Document EPA-600/R-12/531, using procedure G1.

Do Not Use This Cylinder Below 100 psig (0.7 Megapascal).

Certified Concentration(s)			
Component	Concentration	Uncertainty	Analytical Principle
Carbon Dioxide	6.99 %	±0.03 %	NDIR
Oxygen	20.92 %	±0.08 %	MPA
Nitrogen	Balance		

Analytical Measurement Data Available Online.

Reference Standard(s)							
Lot	Expiration	Type	Balance	Component	Concentration	Uncertainty(%)	NIST Reference
GC1106080848	09/07/2013	GMIS	N2	CO2	12.57 %	0.384	3221755
GC0807251121	04/28/2019	GMIS	N2	O2	24.43 %	0.52	71001

Analytical Instrumentation						
Component	Analytical Principle	Make	Model	Serial	MPC Date	
CO2	NDIR	Horiba	VA-3013	H0000P11	07/31/2013	
O2	MPA	Horiba	VA-3013	H0000P11	07/11/2013	

Z= Zero Gas S= Span Gas C= Candidate Gas

Red Ball Technical Gas Service
 PGVP Vendor ID # G12013
 Information and Ordering
 800-551-8150
 Fax (318-425-6309)

Fred Holt
 Fred Holt, CHMM
 Quality Control



1700 Scepter Rd
Waverly, TN 37185
931-296-3357

Certificate of Analysis - EPA Protocol Mixtures

Customer: NORDON

Protocol:	Reference #:	Lot#:
G1	T176792-1	9302603567
Cylinder Number:	SX49930	
Cylinder Pressure:	1900psig	
Last Analysis Date:	11/19/2012	
Expiration Date:	11/19/2014	

DO NOT USE THIS CYLINDER WHEN THE PRESSURE FALLS BELOW 150 PSIG

REPLICATE RESPONSES

Component: Nitrogen Dioxide	Date: 11/2/2012	Date: 11/19/2012
	45.60	45.20
	45.60	45.26
Certified Conc: 45.38ppm +/- 1% REL	45.40	45.25

BALANCE GAS: Air

REFERENCE STANDARDS:

Component: Nitrogen Dioxide
Reference Standard: SRM
Cylinder #: CAL016152
Concentration: 98.0ppm
Exp Date: 12/31/2015
Lot #: 2660-C-57

CERTIFICATION INSTRUMENTS

Component: Nitrogen Dioxide
Make/Model: HORIBA CLA-510SS
Serial Number: 8H4SOCTJ
Measurement Principle: CHEMI
Last Calibration: 11/2/2012

Notes:

This Certification was performed according to EPA Traceability Protocol for Assay & Certification of Gaseous Calibration Standards September 1997, using procedure G1 and/or G2.

U.S. EPA Vendor ID No.: D52012: PGVP Participation Date: 1/1/2012: PGVP Renewal Date: 12/31/12

Analyst: *Julie Higgins*
Julie Higgins

Date: 11/26/2012

NOx Converter Efficiency and Response Times

Date: January 3, 2014

METHOD 7E NOx CONVERTER EFFICIENCY TEST

Certified NO ₂ Conc. (ppmv)	45.38
Measured NOx Conc. (ppmv)	41.83
Converter Efficiency (%)	92

Criteria: Converter Efficiency should be 90% or greater

METHOD 7E RESPONSE TIMES

	NOx (ppmv)	CO (ppmv)	O ₂ (%)
Low-Level Gas Concentration	0	0	0
Upscale Gas Concentration	94.70	193.00	10.99
95% of Upscale Gas	90.0	183.4	10.4

	NOx	CO	O ₂
Low-Level Gas RT (sec)	88	75	50
Upscale Gas RT (sec)	82	73	37
Longer Analyzer RT Interval (sec)	88	75	50
System Response Time (sec)	88		
*System Response Time (min)	1.5		
†System Purge Time (min)	2.9		

*Longer interval of time to reach 95% of stable stable response for low & upscale level gases.

Criteria: †System Purge Time shall be ≥ 2 times the System Response Time

Analyzer Gas Quality Assurance

Test Run:	DH-010314.01		
Parameter	NOx	CO	O2
CALIBRATION ERROR DATA			
Range/Span Data			
Analyzer Range	100	200	25
Method 7E Span	94.7	193.0	20.9
Certified Calibration Gas Data			
Zero Level Certified Value (ppm or %)	0	0	0
Low Level Certified Value (ppm or %)	0.0	0.0	0.0
Mid Level Certified Value (ppm or %)	47.3	95.3	10.99
High Level Certified Value (ppm or %)	94.7	193.0	20.92
Calibration Error Observations (Direct)			
Zero Level Observed (ppm or %)	n/a	n/a	n/a
Low Level Observed (ppm or %)	0.2	0.0	0.0
Mid Level Observed (ppm or %)	47.6	95.7	11.0
High Level Observed (ppm or %)	95.2	193.2	21.0
Calibration Error Results			
Difference from Zero Level (%)	n/a	n/a	n/a
Difference from Low Level (%)	0.18	0.01	0.22
Difference from Mid Level (%)	0.32	0.22	0.15
Difference from High Level (%)	0.53	0.11	0.37
<i>Allowable Difference (%)</i>	(±2%)	(±2%)	(±2%)
TEST RUN DATA			
Bias Observations			
Low/Zero Level Cal. Gas Certified Value (ppm or %)	0.00	0.00	0.00
Upscale Cal. Gas Certified Value (ppm or %)	94.70	193.00	10.99
Initial Low/Zero Level Observed (ppm or %)	0.17	-0.02	0.05
Initial Upscale Level Observed (ppm or %)	95.20	193.21	11.02
Initial Bias Low/Zero Level Gas (ppm or %)	2.74	-0.71	0.05
Initial Bias Upscale Level Gas (ppm or %)	92.63	192.18	10.98
Final Bias Low/Zero Level Gas (ppm or %)	2.72	-1.00	0.16
Final Bias Upscale Level Gas (ppm or %)	91.44	191.53	10.99
Bias and Drift Results			
Initial Bias Low/Zero Level (%)	2.71	-0.35	0.03
Initial Bias Upscale Level (%)	-2.72	-0.53	-0.18
Final Bias Low/Zero Level (%)	2.69	-0.50	0.55
Final Bias Upscale Level (%)	-3.97	-0.87	-0.16
<i>Allowable Bias (%)</i>	(±5%)	(±5%)	(±5%)
Low/Zero Level Drift Calculation (%)	0.03	0.15	0.51
Upscale Level Drift Calculation (%)	1.26	0.34	0.02
<i>Allowable Drift (%)</i>	(±3%)	(±3%)	(±3%)
Raw Results (ppmv or %)			
	72.48	14.33	16.81
Minimum Detection Limit (MDL)	0.5	1.0	0.1
Corrected Results (ppmv or %)	74.0	15.2	16.9
*Final Results (ppmv or %)	74.0	15.2	16.9

**Final Results which are shown in Italics represent the MDL for that analyte*

Analyzer Gas Quality Assurance

Test Run:	DH-010314.02		
Parameter	NOx	CO	O2
CALIBRATION ERROR DATA			
Range/Span Data			
Analyzer Range	100	200	25
Method 7E Span	94.7	193.0	20.9
Certified Calibration Gas Data			
Zero Level Certified Value (ppm or %)	0	0	0
Low Level Certified Value (ppm or %)	0.0	0.0	0.0
Mid Level Certified Value (ppm or %)	47.3	95.3	10.99
High Level Certified Value (ppm or %)	94.7	193.0	20.92
Calibration Error Observations (Direct)			
Zero Level Observed (ppm or %)	0.0	0.0	0.0
Low Level Observed (ppm or %)	0.2	0.0	0.0
Mid Level Observed (ppm or %)	47.6	95.7	11.0
High Level Observed (ppm or %)	95.2	193.2	21.0
Calibration Error Results			
Difference from Zero Level (%)	n/a	n/a	n/a
Difference from Low Level (%)	0.18	0.01	0.22
Difference from Mid Level (%)	0.32	0.22	0.15
Difference from High Level (%)	0.53	0.11	0.37
<i>Allowable Difference (%)</i>	(±2%)	(±2%)	(±2%)
TEST RUN DATA			
Bias Observations			
Low/Zero Level Cal. Gas Certified Value (ppm or %)	0.00	0.00	0.00
Upscale Cal. Gas Certified Value (ppm or %)	94.70	193.00	10.99
Initial Low/Zero Level Observed (ppm or %)	0.17	-0.02	0.05
Initial Upscale Level Observed (ppm or %)	95.20	193.21	11.02
Initial Bias Low/Zero Level Gas (ppm or %)	2.72	-1.00	0.16
Initial Bias Upscale Level Gas (ppm or %)	91.44	191.53	10.99
Final Bias Low/Zero Level Gas (ppm or %)	1.70	-0.96	0.18
Final Bias Upscale Level Gas (ppm or %)	90.59	191.32	10.99
Bias and Drift Results			
Initial Bias Low/Zero Level (%)	2.69	-0.50	0.55
Initial Bias Upscale Level (%)	-3.97	-0.87	-0.16
Final Bias Low/Zero Level (%)	1.61	-0.48	0.64
Final Bias Upscale Level (%)	-4.86	-0.98	-0.13
<i>Allowable Bias (%)</i>	(±5%)	(±5%)	(±5%)
Low/Zero Level Drift Calculation (%)	1.07	0.02	0.09
Upscale Level Drift Calculation (%)	0.89	0.11	0.02
<i>Allowable Drift (%)</i>	(±3%)	(±3%)	(±3%)
Raw Results (ppmv or %)			
	71.69	13.03	16.82
Minimum Detection Limit (MDL)	0.5	1.0	0.1
Corrected Results (ppmv or %)	74.1	14.0	16.9
*Final Results (ppmv or %)	74.1	14.0	16.9

**Final Results which are shown in Italics represent the MDL for that analyte*

Analyzer Gas Quality Assurance

Test Run:	DH-010314.03		
Parameter	NOx	CO	O2
CALIBRATION ERROR DATA			
Range/Span Data			
Analyzer Range	100	200	25
Method 7E Span	94.7	193.0	20.9
Certified Calibration Gas Data			
Zero Level Certified Value (ppm or %)	0	0	0
Low Level Certified Value (ppm or %)	0.0	0.0	0.0
Mid Level Certified Value (ppm or %)	47.3	95.3	10.99
High Level Certified Value (ppm or %)	94.7	193.0	20.92
Calibration Error Observations (Direct)			
Zero Level Observed (ppm or %)	0.0	0.0	0.0
Low Level Observed (ppm or %)	0.2	0.0	0.0
Mid Level Observed (ppm or %)	47.6	95.7	11.0
High Level Observed (ppm or %)	95.2	193.2	21.0
Calibration Error Results			
Difference from Zero Level (%)	n/a	n/a	n/a
Difference from Low Level (%)	0.18	0.01	0.22
Difference from Mid Level (%)	0.32	0.22	0.15
Difference from High Level (%)	0.53	0.11	0.37
<i>Allowable Difference (%)</i>	(±2%)	(±2%)	(±2%)
TEST RUN DATA			
Bias Observations			
Low/Zero Level Cal. Gas Certified Value (ppm or %)	0.00	0.00	0.00
Upscale Cal. Gas Certified Value (ppm or %)	94.70	193.00	10.99
Initial Low/Zero Level Observed (ppm or %)	0.17	-0.02	0.05
Initial Upscale Level Observed (ppm or %)	95.20	193.21	11.02
Initial Bias Low/Zero Level Gas (ppm or %)	1.70	-0.96	0.18
Initial Bias Upscale Level Gas (ppm or %)	90.59	191.32	10.99
Final Bias Low/Zero Level Gas (ppm or %)	0.19	-4.17	0.01
Final Bias Upscale Level Gas (ppm or %)	91.34	189.89	10.91
Bias and Drift Results			
Initial Bias Low/Zero Level (%)	1.61	-0.48	0.64
Initial Bias Upscale Level (%)	-4.86	-0.98	-0.13
Final Bias Low/Zero Level (%)	0.02	-2.15	-0.16
Final Bias Upscale Level (%)	-4.08	-1.72	-0.55
<i>Allowable Bias (%)</i>	(±5%)	(±5%)	(±5%)
Low/Zero Level Drift Calculation (%)	1.59	1.66	0.80
Upscale Level Drift Calculation (%)	0.78	0.74	0.42
<i>Allowable Drift (%)</i>	(±3%)	(±3%)	(±3%)
Raw Results (ppmv or %)			
	72.28	11.15	16.86
Minimum Detection Limit (MDL)	0.5	1.0	0.1
Corrected Results (ppmv or %)	75.0	13.7	17.0
*Final Results (ppmv or %)	75.0	13.7	17.0

**Final Results which are shown in Italics represent the MDL for that analyte*

DAQ Logs

Company	Plant Name	Unit Make	Unit Model	Unit Number	Status	Date	Time	NOx (ppmvd)	CO (ppmvd)	O2 (%, dry)
Enterprise Products	South Carlsbad CS	Solar	Centaur	Calibration Error	0NOx/0CO/0O2	1/3/14	7:41	0.17	-0.02	0.05
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	7:42	10.35	0.12	13.77
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	7:43	60.42	0.01	20.54
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	7:44	95.27	-0.04	20.97
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	7:45	95.85	-0.03	20.98
Enterprise Products	South Carlsbad CS	Solar	Centaur	Calibration Error	94.7NOx20.92O2	1/3/14	7:46	95.20	-0.05	21.00
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	7:47	55.30	-0.06	11.02
Enterprise Products	South Carlsbad CS	Solar	Centaur	Calibration Error	47.3NOx10.99O2	1/3/14	7:48	47.60	-0.20	11.02
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	7:49	44.34	14.90	0.22
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	7:50	24.23	54.47	0.03
Enterprise Products	South Carlsbad CS	Solar	Centaur	Calibration Error	193CO	1/3/14	7:51	24.25	193.21	0.03
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	7:52	10.00	134.83	0.03
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	7:53	0.57	95.44	0.03
Enterprise Products	South Carlsbad CS	Solar	Centaur	Calibration Error	95.3CO	1/3/14	7:54	0.51	95.73	0.02
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	7:55	0.45	81.22	0.05
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	7:56	2.69	47.66	0.04
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	7:57	3.30	47.74	0.03
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	7:58	38.19	47.68	0.05
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	7:59	41.29	1.88	0.01
Enterprise Products	South Carlsbad CS	Solar	Centaur	CE Test	NO2	1/3/14	8:00	42.18	0.10	0.02
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:01	43.07	0.52	0.03
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:02	43.06	0.48	0.02
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:03	15.10	0.18	0.03
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:04	0.68	0.41	0.03
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:05	0.57	0.16	-0.01
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:06	0.47	0.25	0.02
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:07	0.45	0.06	0.00
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:08	0.45	0.03	0.01
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:09	0.52	0.36	0.01
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:10	0.61	0.36	0.02
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:11	0.85	0.13	0.03
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:12	0.87	-0.14	0.06
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:13	1.38	0.34	0.10
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:14	1.43	0.30	0.14
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:15	1.36	0.51	0.19
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:16	-3.41	-4.24	0.04
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:17	-4.31	-4.96	0.07
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:18	1.10	0.42	0.44
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:19	1.40	0.88	0.57
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:20	1.18	0.76	0.65
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:21	1.45	1.13	0.77
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:22	1.22	0.75	0.89
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:23	0.80	0.43	0.98
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:24	1.27	4.47	6.67
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:25	1.74	25.73	8.18
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:26	1.75	26.08	8.33
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:27	1.67	26.02	8.33
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:28	1.68	25.67	8.38
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:29	0.80	24.64	8.38
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:30	1.79	25.60	8.49
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:31	1.46	25.27	8.57
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:32	1.48	25.16	8.61
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:33	1.49	25.21	8.68
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:34	1.37	24.91	8.71
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:35	1.44	24.83	8.79
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:36	1.47	24.80	8.83
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:37	1.49	24.50	8.92
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:38	1.53	24.59	8.98
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:39	1.67	24.53	9.03
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:40	1.29	23.95	9.11
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:41	1.50	24.19	9.19
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:42	1.67	24.38	9.30
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:43	1.68	24.09	9.40
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:44	1.73	24.08	9.47
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:45	1.79	24.04	9.52
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:46	1.71	23.62	9.64
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:47	1.76	23.54	9.74

DAQ Logs

Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:48	1.78	23.47	9.86	
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:49	1.81	23.06	9.93	
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:50	1.64	22.77	10.00	
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:51	1.69	22.79	10.10	
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:52	1.69	22.63	10.14	
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:53	1.68	22.36	10.22	
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:54	1.58	22.43	10.28	
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:55	1.43	21.99	10.37	
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:56	1.77	21.78	9.54	
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:57	1.14	1.82	0.04	
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:58	0.90	1.12	0.02	
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	8:59	1.47	0.02	10.73	
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	9:00	1.61	-0.52	10.94	
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	9:01	14.47	47.84	0.10	
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	9:02	46.49	95.85	0.02	
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	9:03	39.52	53.59	20.65	
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	9:04	2.02	2.08	20.90	
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	9:05	1.96	1.82	20.92	
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	9:06	2.35	1.77	20.93	
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	9:07	1.55	1.98	20.91	
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	9:08	45.63	188.72	16.54	
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	9:17	4.15	-0.08	11.00	
Enterprise Products	South Carlsbad CS	Solar	Centaur	Bias Check	0NOx/0CO/10.99O2	1/3/14	9:18	2.74	-0.71	10.98	
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	9:19	6.49	20.56	4.10	
Enterprise Products	South Carlsbad CS	Solar	Centaur	Bias Check	94.7NOx/193CO/0O2	1/3/14	9:20	92.63	192.18	0.05	
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	9:21	86.04	152.17	13.07	
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	9:22	68.42	17.67	16.30	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P1	DH-010314.01	1/3/14	9:23	73.69	21.48	16.68	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P1	DH-010314.01	1/3/14	9:24	74.87	21.03	16.76	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P1	DH-010314.01	1/3/14	9:25	74.57	20.79	16.76	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P1	DH-010314.01	1/3/14	9:26	74.35	20.08	16.79	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P2	DH-010314.01	1/3/14	9:27	73.61	16.91	16.79	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P2	DH-010314.01	1/3/14	9:28	71.53	12.47	16.80	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P2	DH-010314.01	1/3/14	9:29	71.55	12.53	16.78	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P3	DH-010314.01	1/3/14	9:30	71.67	11.92	16.83	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P3	DH-010314.01	1/3/14	9:31	70.63	11.73	16.80	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P3	DH-010314.01	1/3/14	9:32	69.26	11.35	16.81	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P4	DH-010314.01	1/3/14	9:33	70.91	11.30	16.78	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P4	DH-010314.01	1/3/14	9:34	72.54	12.14	16.81	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P4	DH-010314.01	1/3/14	9:35	72.63	12.57	16.84	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P5	DH-010314.01	1/3/14	9:36	72.20	12.62	16.84	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P5	DH-010314.01	1/3/14	9:37	72.14	12.24	16.84	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P5	DH-010314.01	1/3/14	9:38	72.31	12.53	16.83	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P6	DH-010314.01	1/3/14	9:39	72.42	12.16	16.82	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P6	DH-010314.01	1/3/14	9:40	74.48	14.44	16.81	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P6	DH-010314.01	1/3/14	9:41	73.29	15.86	16.79	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P6	DH-010314.01	1/3/14	9:42	73.43	16.39	16.82	
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	9:43	70.14	12.09	18.89	
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	9:44	71.29	19.84	16.82	
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	9:45	72.99	29.72	16.82	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P7	DH-010314.01	1/3/14	9:46	71.34	25.55	16.80	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P7	DH-010314.01	1/3/14	9:47	72.35	21.74	16.81	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P7	DH-010314.01	1/3/14	9:48	72.91	18.04	16.86	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P8	DH-010314.01	1/3/14	9:49	72.82	14.70	16.82	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P8	DH-010314.01	1/3/14	9:50	72.16	12.22	16.83	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P8	DH-010314.01	1/3/14	9:51	72.84	12.04	16.83	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P9	DH-010314.01	1/3/14	9:52	72.70	12.01	16.84	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P9	DH-010314.01	1/3/14	9:53	72.17	11.98	16.81	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P9	DH-010314.01	1/3/14	9:54	71.87	11.92	16.82	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P10	DH-010314.01	1/3/14	9:55	72.13	11.81	16.83	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P10	DH-010314.01	1/3/14	9:56	72.34	11.67	16.82	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P10	DH-010314.01	1/3/14	9:57	69.00	8.15	16.60	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P11	DH-010314.01	1/3/14	9:58	70.88	9.84	16.74	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P11	DH-010314.01	1/3/14	9:59	73.33	11.94	16.83	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P11	DH-010314.01	1/3/14	10:00	73.24	11.96	16.85	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P12	DH-010314.01	1/3/14	10:01	73.18	13.23	16.94	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P12	DH-010314.01	1/3/14	10:02	71.83	13.05	16.71	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P12	DH-010314.01	1/3/14	10:03	74.03	16.96	16.85	
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1, P12	DH-010314.01	1/3/14	10:04	73.42	17.59	16.85	
								DH-010314.01 Averages	72.48	14.33	16.81

DAQ Logs

Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	10:05	70.42	22.30	10.94
Enterprise Products	South Carlsbad CS	Solar	Centaur	Bias Check	0NOx/0CO/10.99O2	1/3/14	10:06	2.72	-1.00	10.99
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	10:07	-1.86	4.38	5.33
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	10:08	85.09	183.30	-0.21
Enterprise Products	South Carlsbad CS	Solar	Centaur	Bias Check	94.7NOx/193CO/0O2	1/3/14	10:09	91.44	191.53	0.16
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	10:10	79.65	166.97	5.05
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	10:11	67.55	11.61	16.38
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.02	1/3/14	10:12	71.03	13.91	16.79
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.02	1/3/14	10:13	71.20	14.14	16.82
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.02	1/3/14	10:14	71.43	13.10	16.77
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.02	1/3/14	10:15	72.15	13.91	16.83
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.02	1/3/14	10:16	72.15	14.32	16.85
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.02	1/3/14	10:17	71.94	14.28	16.84
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.02	1/3/14	10:18	69.80	13.20	16.81
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.02	1/3/14	10:19	71.20	13.06	16.81
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.02	1/3/14	10:20	71.94	13.80	16.83
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.02	1/3/14	10:21	71.94	13.74	16.86
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.02	1/3/14	10:22	71.72	13.54	16.81
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.02	1/3/14	10:23	72.01	13.53	16.83
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.02	1/3/14	10:24	71.91	13.39	16.84
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.02	1/3/14	10:25	71.93	13.34	16.83
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.02	1/3/14	10:26	71.83	13.35	16.83
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.02	1/3/14	10:27	71.77	13.25	16.83
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.02	1/3/14	10:28	71.70	13.03	16.82
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.02	1/3/14	10:29	71.96	13.13	16.82
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.02	1/3/14	10:30	71.72	13.07	16.83
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.02	1/3/14	10:31	70.62	12.93	16.82
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.02	1/3/14	10:32	69.81	10.57	16.71
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.02	1/3/14	10:33	72.48	12.90	16.83
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.02	1/3/14	10:34	72.42	12.60	16.84
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.02	1/3/14	10:35	72.19	12.46	16.83
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.02	1/3/14	10:36	72.21	12.67	16.86
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.02	1/3/14	10:37	72.18	12.38	16.85
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.02	1/3/14	10:38	72.19	12.43	16.83
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.02	1/3/14	10:39	72.17	12.52	16.84
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.02	1/3/14	10:40	72.27	12.26	16.86
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.02	1/3/14	10:41	71.75	11.87	16.83
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.02	1/3/14	10:42	70.91	11.17	16.77
DH-010314.02 Averages								71.69	13.03	16.82
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	10:43	36.04	10.05	10.66
Enterprise Products	South Carlsbad CS	Solar	Centaur	Bias Check	0NOx/0CO/10.99O2	1/3/14	10:44	1.70	-0.96	10.99
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	10:45	31.08	84.95	-0.14
Enterprise Products	South Carlsbad CS	Solar	Centaur	Bias Check	94.7NOx/193CO/0O2	1/3/14	10:46	90.59	191.32	0.18
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	10:47	90.76	124.36	16.57
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	10:48	72.21	11.95	16.79
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.03	1/3/14	10:49	72.12	12.12	16.84
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.03	1/3/14	10:50	72.37	11.47	16.83
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.03	1/3/14	10:51	72.38	11.70	16.85
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.03	1/3/14	10:52	72.39	11.50	16.88
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.03	1/3/14	10:53	72.37	11.27	16.86
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.03	1/3/14	10:54	72.33	11.46	16.85
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.03	1/3/14	10:55	72.30	11.44	16.85
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.03	1/3/14	10:56	72.39	11.22	16.88
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.03	1/3/14	10:57	72.36	11.32	16.87
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.03	1/3/14	10:58	72.27	11.11	16.85
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.03	1/3/14	10:59	72.28	11.18	16.86
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.03	1/3/14	11:00	72.37	11.18	16.85
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.03	1/3/14	11:01	72.30	11.16	16.87
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.03	1/3/14	11:02	72.33	11.24	16.85
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.03	1/3/14	11:03	72.28	10.91	16.86
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.03	1/3/14	11:04	72.33	11.13	16.87
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.03	1/3/14	11:05	71.95	10.73	16.85
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.03	1/3/14	11:06	72.29	10.71	16.85
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.03	1/3/14	11:07	72.36	10.84	16.86
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.03	1/3/14	11:08	69.57	8.22	16.70
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.03	1/3/14	11:09	71.66	12.01	16.97
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.03	1/3/14	11:10	71.98	14.94	16.85
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.03	1/3/14	11:11	72.77	11.00	16.87
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.03	1/3/14	11:12	72.64	10.90	16.86
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.03	1/3/14	11:13	72.61	10.49	16.88

DAQ Logs

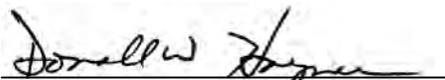
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.03	1/3/14	11:14	72.51	10.79	16.87
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.03	1/3/14	11:15	72.71	11.41	16.86
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.03	1/3/14	11:16	72.76	10.61	16.88
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.03	1/3/14	11:17	72.71	10.57	16.87
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.03	1/3/14	11:18	72.56	10.54	16.88
Enterprise Products	South Carlsbad CS	Solar	Centaur	T1	DH-010314.03	1/3/14	11:19	72.46	10.40	16.86
DH-010314.03 Averages								72.28	11.15	16.86
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	11:20	42.04	9.45	11.03
Enterprise Products	South Carlsbad CS	Solar	Centaur	Bias Check	0NOx/0CO/10.99O2	1/3/14	11:21	0.19	-4.17	10.91
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	11:22	38.35	107.72	0.03
Enterprise Products	South Carlsbad CS	Solar	Centaur	Bias Check	94.7NOx/193CO/0O2	1/3/14	11:23	91.34	189.89	0.01
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	11:24	79.14	101.49	16.20
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	17:01	12.37	-4.16	0.08
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	17:02	38.35	-4.79	0.07
Enterprise Products	South Carlsbad CS	Solar	Centaur	CE Test	NO2	1/3/14	17:03	41.83	-4.42	0.08
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/3/14	17:04	30.41	-4.57	0.08

Annual Emission Test Report
for one
Solar Centaur T4702 Compressor Turbine
Unit Number T2
located at the
South Carlsbad Compressor Station

Prepared for
Enterprise Field Services, LLC
P. O. Box 4324
Houston, TX 77210

January 2014
Nordon Project No. 14-0152-2

This test report has been reviewed and approved for submittal to the New Mexico Environment Department (NMED) by the following representatives:



Donald W. Haynes
Nordon Corporation

Enterprise Field Services, LLC

 **NORDON** CORPORATION

P. O. Box 1415 Round Rock, Texas 78680
Phone (512) 355-3786 Fax (512) 355-3785

SUMMARY OF RESULTS

Exhaust emission testing was performed on one Solar Centaur T4702 (Unit # T2) compressor turbine for Enterprise Field Services, LLC located at the South Carlsbad Compressor Station, near Loving, Eddy County, New Mexico. The turbine is used for natural gas compression. The testing was performed to demonstrate the continued compliance with the emission limits set forth in the NMED permit. Nordon Corporation of Round Rock, Texas, performed the exhaust emissions testing on January 4, 2014.

Continuous emission instruments housed in a mobile analysis unit were used to determine the concentrations of NO_x , CO, and O_2 in the exhaust stack of the compressor turbine. The following Code of Federal Regulations, Title 40, Part 60 (40CFR60), Appendix A reference methods were used to determine stack gas concentrations: Method 7E for nitrogen oxides (NO_x), Method 10 for carbon monoxide (CO), and Method 3A for oxygen (O_2). Mass emission rates were determined stoichiometrically according to Method 19 data reduction procedures using measured fuel flow rate.

Three thirty-minute test runs were performed on the exhaust of the turbine while firing on natural gas. The results of the testing are presented in a summary of results table. This table includes all the relevant information pertaining to the turbine/compressor operations, exhaust emissions, and ambient conditions. Exhaust concentrations are presented in part per million by volume (ppmv) or percent (%) by volume. The mass emission rates are presented in pound per hour (lb/hr) and ton per year (tpy). Turbine/compressor operational data was collected during each test run.

Summary of Results

NORDON CORPORATION

P.O. Box 1415 Round Rock, Texas 78680
PHONE (512) 355-3786 • FAX (512)355-3785

Plant: South Carlsbad Compressor Station
 Facility Owner:Enterprise Field Services, LLC
 Location: Loving, Eddy County, New Mexico
 Unit Make/Model: Solar Centaur T4702
 Unit Number: T2 , Ser. No.OHE12C7057
 Test Personnel: DWH / KRJ

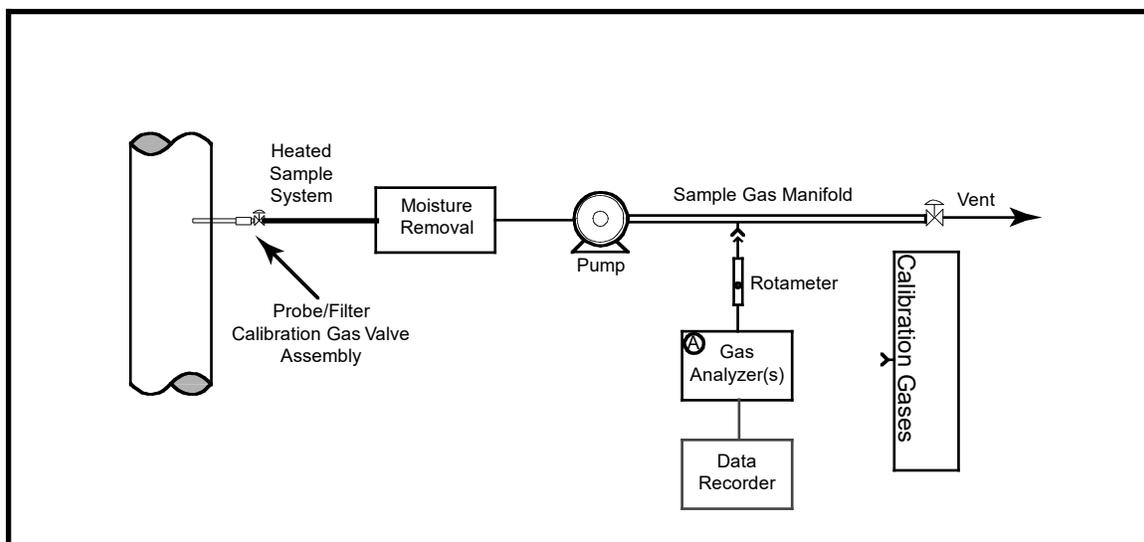
RUN NUMBER	DH-010414.01	DH-010414.02	DH-010414.03	
Date	1/4/14	1/4/14	1/4/14	
Start Time (hr)	8:20	9:10	9:47	
Stop Time (hr)	8:50	9:40	10:17	
TURBINE DATA				
Rated Horsepower (Hp)	3609	3609	3609	
Fuel Pressure (psig)	195	188	192	
Gas Producer Speed (%)	95	95	95	
Power Turbine Speed (%)	86	86	84	
Turbine Compressor Discharge Pressure (psig)	109	107	103	
Exhaust Temperature (°F)	1047	1060	1073	
Horsepower (Hp)	3630	3571	3452	
Heat Rate (MMBtu/hr)	42.9	38.4	39.9	
COMPRESSOR DATA				
Suction Pressure (psig)	330	330	338	
Suction Temperature (°F)	88	93	97	
Discharge Pressure (psig)	560	561	562	
Discharge Temperature (°F)	171	176	177	
Gas Production (MMscfd)	38	34	33	
FUEL & EXHAUST DATA				
O2 F-factor (dscf/MMBtu)	8698	8698	8698	
Fuel Heating Value (HHV Btu/scf)	1098	1098	1098	
Stoichiometric Exhaust Flow (dscfh)	1.97E+06	1.75E+06	1.82E+06	
AMBIENT CONDITIONS				
Temperature (°F): Dry bulb	42	49	64	
Temperature (°F): Wet bulb	36	41	47	
Atmospheric Pressure ("Hg)	26.64	26.64	26.64	
Humidity (lb water/lb air)	0.0036	0.0042	0.0037	
Humidity (% vol)	0.5	0.6	0.5	
MEASURED EXHAUST OUTLET CONCENTRATIONS				AVERAGES
NOx (ppmv)	78.7	80.4	84.1	81.1
CO (ppmv)	13.1	12.3	12.7	12.7
O2 (%)	16.9	16.9	16.9	16.9
EMISSION RATES				
NOx (lb/hr) LIMIT=27.0	18.54	16.85	18.27	17.88
CO (lb/hr) LIMIT=7.4	1.87	1.57	1.68	1.71
NOx (tpy, @8760 hr/yr) LIMIT=118.3	81.19	73.78	80.02	78.33
CO (tpy, @8760 hr/yr) LIMIT=32.5	8.20	6.89	7.35	7.48

PROCEDURES

Continuous emission instruments housed in the mobile analysis unit were used to determine the concentrations of pollutants found in the turbine exhaust stack. The following 40CFR60, Appendix A reference methods were used to determine stack gas concentrations: Method 7E for NO_x , Method 10 for CO, and Method 3A for O_2 . Mass emission rates were determined according to data reduction procedures provided in Method 19.

As depicted in Figure 1, Sample System and Instrumentation, a stainless steel sample probe was located in the centroid of the stack. Sample gas enters the stainless steel probe into a stainless steel 3-way valve. The 3-way valve is used to perform leak checks and sample system bias checks. From the valve, the gas flows through a 3/8" Teflon® heat traced sample line to a stainless steel minimum contact condenser to dry the sample. From the condenser, a 3/8" Teflon sample line brings the exhaust gas to a manifold in the mobile analysis unit via a Teflon-lined diaphragm pump. The manifold partitions the gas through quick-connects so that each instrument can directly sample exhaust gas. Each instrument is equipped with a rotameter to maintain correct sample pressure and flow. The instruments are connected to a computer data acquisition system to document its response during quality assurance activities and testing.

Figure 1: Sample System and Instrumentation



(A) Gas Analyzers - NO_x , CO, O_2

Analyzer Make	Analyzer Model	Detection Principle
<i>NO_x Analyzer:</i> Thermo Environmental	42i-HL	Chemiluminescence
<i>CO Analyzer :</i> Thermo Environmental	48i-HL	Non-dispersive Infra-red
<i>O₂ Analyzer:</i> Thermo Environmental	48i-HL	Paramagnetic Cell

A continuous analyzer is used to determine NO_x concentrations according to EPA Reference Method 7E. This instrument employs a chemiluminescent detection principle. The NO_x concentration and mass emission rates are expressed as NO₂ per the reference method.

A continuous analyzer is used to determine CO concentrations according to EPA Reference Method 10. The instrument employs a nondispersive infrared detector coupled to a gas filter correlation wheel, which eliminates the interferences due to water and carbon dioxide.

A continuous analyzer is used to determine O₂ concentrations according to EPA Reference Method 3A. The instrument is equipped with either an electrochemical or paramagnetic cell.

Data obtained from the continuous emission analyzers were recorded by a National Instruments data acquisition (DAQ) system using Labview software. A copy of the DAQ records can be found in the appendix of this report.

Quality assurance activities meeting the requirements of the EPA reference methods were performed during the turbine testing. Tables documenting quality assurance procedures are located in the appendix of this report.

Exhaust flow rate was determined according to the data reduction procedures provided in EPA Method 19. The O₂ F-Factor used in the emission rate calculation was either calculated based on a recent fuel analysis or the standard 8710 value for natural gas provided by EPA Method 19.

Nordon personnel recorded turbine compressor operating parameters. Ambient conditions were collected using a wet/dry bulb sling psychrometer to measure temperature and a barometer to measure absolute atmospheric pressure.

APPENDIX

Field Data Sheets
Example Calculations
Gas Certifications
Quality Assurance Activities
Run Data Logs

Plant: South Carlisbad Compressor Station
 Facility Owner: Enterprise
 Unit Owner: Enterprise
 Location: Loving, Eddy County, New Mexico
 Applicable Regulation: 40CFR60, Subpart GG
 Unit Make/Model: Solar Centaur T-4702
 Unit Number: T2
 Ser. No. OHE12C7057
 Test Personnel: DWH / KRI

Run Number	01	02	03	04	05	06	07	08	09	10	11	12
Start Time	820	1910	1447	1024	1101	1138	1215	1252	1329	1406	1445	1522
Stop Time												
Turbine/Compressor Operation												
Load Condition												
Fuel Flow (Mscfd)	938	839	873	718	836	778	913	877	635	891	596	618
Fuel Flow (scfh)	86	86	84	84	83	82	80	81	80	80	80	80
Power Turbine Speed (%)	95	95	95	95	95	95	95	95	95	95	95	95
Gas Producer Speed (%)												
Horsepower (hp)												
Rated Horsepower (hp)												
% Load												
Turbine Compressor Discharge, PCD (psig)	109	107	103	103	103	103	102	102	102	102	102	102
Turbine Temperature T5 (°F)	1047	1060	1073	1075	1077	1075	1078	1078	1079	1081	1079	1078
Gas Compressor Suction Pressure (psig)	330	330	338	341	341	356	359	360	361	363	364	364
Gas Compressor Discharge Pressure (psig)	578	561	562	566	567	571	574	576	577	577	577	578
Gas Compressor Suction Temperature (°F)	88	93	97	97	93	91	92	92	92	93	93	93
Gas Compressor Discharge Temperature (°F)	171	176	172	177	171	165	165	165	165	165	165	165
Fuel Gas Pressure (psig)	145	188	192	190	191	190	191	190	191	192	191	194
Gas Production Rate (MMscfd)	38	39	33	33	33	41	40	39	40	40	41	41
Alt. Ft.	3410	3140	3140	3160	3180	3200	3220	3220	3240	3260	3260	3260
Ambient Conditions												
Barometric Pressure (absolute In Hg)	24.44	26.44	26.44	26.44	26.44	26.44	26.44	26.44	26.44	26.44	26.44	26.44
Temperature Dry (°F)	42	49	64	66	68	69	72	72	71	71	70	69
Temperature Wet (°F)	36	41	47	47	48	48	50	47	48	48	48	47



Certificate of Analysis

Number: 1030-14010388-001A

Houston Laboratories

8820 Interchange Drive

Houston, TX 77054

Phone 713-660-0901

Thor Olsen
Nordon Corporation
PO Box 1415
Round Rock, TX 78680

Jan. 21, 2014

Station Name: South Calrsbad Compressor Stition
Station Location: Loving, NM
Sample Point: Turbine Fuel Gas
Cylinder No: 0298
Analyzed: 01/16/2014 05:34:22 by JD

Sampled By:
Sample Of: Gas Spot
Sample Date: 01/04/2014 10:00
Sample Conditions: 190 psig, @ 65 °F
Method: GPA-2261M

Analytical Data

Components	Mol. %	Wt. %	GPM at 14.65 psia		
Nitrogen	1.204	1.797		GPM TOTAL C2+	2.870
Carbon Dioxide	1.556	3.648		GPM TOTAL C3+	1.036
Methane	86.800	74.184		GPM TOTAL iC5+	0.077
Ethane	6.877	11.016	1.834		
Propane	2.516	5.911	0.691		
Iso-butane	0.292	0.904	0.095		
n-Butane	0.552	1.709	0.173		
Iso-pentane	0.086	0.331	0.031		
n-Pentane	0.072	0.277	0.026		
Hexanes Plus	0.045	0.223	0.020		
	100.000	100.000	2.870		

Physical Properties	Total	C6+
Relative Density Real Gas	0.6496	3.2176
Calculated Molecular Weight	18.77	93.19
Compressibility Factor	0.9973	
GPA 2172-09 Calculation:		
Calculated Gross BTU per ft³ @ 14.65 psia & 60°F		
Real Gas Dry BTU	1097	5113
Water Sat. Gas Base BTU	1078	5024

Comments: H2O Mol% : 1.750 ; Wt% : 1.681
Reran Sample Confirmed GC Analysis

Hydrocarbon Laboratory Manager

Quality Assurance: The above analyses are performed in accordance with ASTM, UOP, GPA guidelines for quality assurance, unless otherwise stated.

Fuel Gas Analysis

Gross Btu/scf 1098 O₂ F-Factor dscf/MMBtu 8698 O₂ F-Factor (wscf/MMBtu) 10660 H₂O F-Factor (scf/MMBtu) 1962 CO₂ F-Factor (scf CO₂/MMBtu) 1058
Btu/lb 22164 Sp. Gr. 0.6516
F_o 1.719 Moisture Factor 18.407 VOC Fraction 0.063

Compound	Mol. Formula	Mol. %
Methane	CH ₄	86.800
Ethane	C ₂ H ₆	6.877
Propane	C ₃ H ₈	2.516
Isobutane	C ₄ H ₁₀	0.292
n-Butane	C ₄ H ₁₀	0.552
Isopentane	C ₅ H ₁₂	0.086
n-Pentane	C ₅ H ₁₂	0.072
NeoPentane	C ₅ H ₁₂	
n-Hexane	C ₆ H ₁₄	0.045
n-Heptane	C ₇ H ₁₆	
n-Octane	C ₈ H ₁₈	
Carbon dioxide	CO ₂	1.556
Nitrogen	N ₂	1.204
Total		100.000

Example Calculations: Method 7E Concentration Correction

Test Run #: DH-010414.01

Component: NOx

Observed Measurements/Data:		Scale, Certified Concentrations	
	Direct Calibration Results		
0.42	NOx direct zero, Cdiro	94.7	NOx chart scale, CS
94.68	NOx direct span, Cdirm	94.7	NOx actual calibration gas concentration, Cma
	System Calibration Results	0	Actual low-level gas concentration, Coa
1.66	NOx, initial zero reading, Csoi		
92.45	NOx initial span reading, Csmi		
0.85	NOx final zero reading, Cof		
91.68	NOx final span reading, Csmf		
	Run Results		
76.69	NOx run average, Caverage		

Bias Check Initial Zero (SBoi)

$$SBoi = \frac{(Csoi - Cdiro)}{CS}$$

$$= \mathbf{1.31\%}$$

Bias Check Initial Span (SBmi)

$$SBmi = \frac{(Csmi - Cdirm)}{CS}$$

$$= \mathbf{-2.36\%}$$

Bias Check Final Zero (SBof)

$$SBof = \frac{(Csof - Cdiro)}{CS}$$

$$= \mathbf{0.45\%}$$

Bias Check Final Span (SBmf)

$$SBmf = \frac{(Csmf - Cdirm)}{CS}$$

$$= \mathbf{-3.17\%}$$

Drift Check Zero (Do)

$$= \frac{|SBof - SBoi|}{\mathbf{0.86}}$$

Drift Check Span (Ds)

$$= \frac{|SBmf - SBmi|}{\mathbf{0.81}}$$

Bias-Average Zero (Coavg)

$$= \left(\frac{Csoi + Csof}{2} \right)$$

$$= \mathbf{1.256\text{ (ppmv)}}$$

Bias-Average Span (Cmavg)

$$= \left(\frac{Csmi + Csmf}{2} \right)$$

$$= \mathbf{92.06\text{ (ppmv)}}$$

NOx Concentration Correction

$$= (Caverage - Coavg) \times \left(\frac{Cma}{Cmavg - Coavg} \right)$$

$$\mathbf{78.7\text{ (ppmv)}}$$

Example Calculations: Method 7E Concentration Correction

Test Run #: DH-010414.01

Component: CO

Observed Measurements/Data:		Scale, Certified Concentrations	
Direct Calibration Results			
0.63	CO direct zero, Cdiro	193	CO chart scale, CS
194.59	CO direct span, Cdirm	193	CO actual calibration gas concentration, Cma
System Calibration Results			
-0.63	CO, initial zero reading, Csoi	0	Actual low-level gas concentration, Coa
192.76	CO initial span reading, Csmi		
0.00	CO final zero reading, Cof		
191.43	CO final span reading, Csmf		
Run Results			
12.70	CO run average, Caverage		

Bias Check Initial Zero (SBoi)

$$SBoi = \frac{(Csoi - Cdiro)}{CS}$$

$$= -0.65 \%$$

Bias Check Initial Span (SBmi)

$$SBmi = \frac{(Csmi - Cdirm)}{CS}$$

$$= -0.95 \%$$

Bias Check Final Zero (SBof)

$$SBof = \frac{(Csof - Cdiro)}{CS}$$

$$= -0.32 \%$$

Bias Check Final Span (SBmf)

$$SBmf = \frac{(Csmf - Cdirm)}{CS}$$

$$= -1.63 \%$$

Drift Check Zero (Do)

$$Do = |SBof - SBoi|$$

$$= 0.33$$

Drift Check Span (Ds)

$$Ds = |SBmf - SBmi|$$

$$= 0.69$$

Bias-Average Zero (Coavg)

$$Coavg = \left(\frac{Csoi + Csof}{2} \right)$$

$$= -0.315 \text{ (ppmv)}$$

Bias-Average Span (Cmavg)

$$Cmavg = \left(\frac{Csmi + Csmf}{2} \right)$$

$$= 192.10 \text{ (ppmv)}$$

CO Concentration Correction

$$= (Caverage - Coavg) \times \left(\frac{Cma}{Cmavg - Coavg} \right)$$

$$= 13.1 \text{ (ppmv)}$$

Example Calculations: Method 7E Concentration Correction

Test Run #: DH-010414.01

Component: O2

Observed Measurements/Data:		Scale, Certified Concentrations	
Direct Calibration Results			
0.13	O2 direct zero, Cdiro	20.92	O2 chart scale, CS
21.26	O2 direct span, Cdirn	20.92	O2 actual calibration gas Concentration, Cma
System Calibration Results			
0.25	O2, initial zero reading, Csoi	0	Actual low-level gas Concentration, Coa
21.19	O2 inital span reading, Csmi		
0.28	O2 final zero reading, Csof		
21.21	O2 final span reading, Csmf		
Run Results			
17.22	O2 run average, Caverage		

Bias Check Initial Zero (SBoi)

$$SBoi = \frac{(Csoi - Cdiro)}{CS}$$

$$= 0.57 \%$$

Bias Check Initial Span (SBmi)

$$SBmi = \frac{(Csmi - Cdirn)}{CS}$$

$$= -0.37 \%$$

Bias Check Final Zero (SBof)

$$SBof = \frac{(Csof - Cdiro)}{CS}$$

$$= 0.75 \%$$

Bias Check Final Span (SBmf)

$$SBmf = \frac{(Csmf - Cdirn)}{CS}$$

$$= -0.25 \%$$

Drift Check Zero (Do)

$$|SBof - SBoi|$$

$$= 0.17$$

Drift Check Span (Ds)

$$|SBmf - SBmi|$$

$$= 0.12$$

Bias- Average Zero (O2avg)

$$= \left(\frac{Csoi + Csof}{2} \right)$$

$$= 0.263 \%$$

Bias-Average Span (Cmavg)

$$= \left(\frac{Csmi + Csmf}{2} \right)$$

$$= 21.20 \%$$

O2 Concentration Correction

$$= (Caverage - Coavg) \times \left(\frac{Cma}{Cmavg - Coavg} \right)$$

$$16.9 \%$$

Example Calculations: Method 19 Exhaust Flow

Test Run #: DH-010414.01

Component: Stack Flow

Observed Measurements/Data:		Standards/Constants/Conversion Factors
39083	Fuel Flow Rate (scfh)	1000000 Btu per MMBtu
8698	Fuel O ₂ F-Factor (dscf/MMBtu)	20.9 O ₂ % in air
1098	Fuel Heating Value (Btu/scf)	
16.9	O ₂ final concentration (%)	

Derivation of Exhaust Flow using Equation 19-1 from Method 19

$$E \left(\frac{lb}{MMBtu} \right) = C_d \left(\frac{lb}{scf} \right) F_d \left(\frac{dscf}{MMBtu} \right) \times \frac{20.9}{(20.9 - \%O_2)} \quad \text{Eq. 19-1}$$

divide each side of equation by Cd to obtain the following

$$\left(\frac{scf}{MMBtu} \right) = F_d \left(\frac{dscf}{MMBtu} \right) \times \frac{20.9}{(20.9 - \%O_2)}$$

multiply each side of equation by heat input (MMBtu/hr)

$$\left(\frac{scf}{hr} \right) = HeatInput \left(\frac{MMBtu}{hr} \right) \times F_d \left(\frac{dscf}{MMBtu} \right) \times \frac{20.9}{(20.9 - \%O_2)}$$

Fuel Gas Heat Rate/Heat Input (MMBtu/hr)

$$\begin{aligned}
 &= \left(\text{Fuel Flow Rate} \frac{scf}{hr} \right) \times \left(\text{Fuel Heating Value} \frac{Btu}{scf} \right) \times \left(\frac{1MMBtu}{1000000Btu} \right) \\
 &= \quad \quad \quad \mathbf{42.90 \text{ (MMBtu/hr)}}
 \end{aligned}$$

Stack Gas Volumetric Flow Rate, Q (dscfh)

$$\begin{aligned}
 &= \left(\text{HeatInput} \frac{MMBtu}{hr} \right) \times \left(\text{Fuel O}_2 \text{ F-Factor} \frac{dscf}{MMBtu} \right) \times \left(\frac{20.9}{20.9 - O_2} \right) \\
 &= \quad \quad \quad \mathbf{1.97E+06 \text{ (dscfh)}}
 \end{aligned}$$

Example Calculations: Emissions Calculations

Test Run #: DH-010414.01

Component: NOx

Observed Measurements/Data:		Standards/Constants/Conversion Factors	
78.7	NOx final concentration, Cd (ppmv)	528	EPA Standard Temperature, Tstd (°R)
1973673	Average Stack Gas Flow Rate, Q (DSCFH)	29.92	EPA Standard Pressure, Pstd (in. Hg)
16.9	O2 final concentration (%)	385.3	Gas Constant @ EPA STP (SCF/lb-mol)
3630	Horsepower (Hp)	28.317	Liters per Cubic Foot
8698	Fuel O2 Factor (DSCF/MMBtu)	46	NOx molecular wt. (NO2), MW (lb/lb-mol)
		0.001912	Conversion constant (NOx ppm to g/m3)
		8760	hours per year
		2000	pounds per ton
		0.028317	cubic meters per cubic feet

NOx Emissions (ppmv @ 15%O2): Applicable yes

$$= \text{ppmv@15\%O}_2 = Cd \times \left(\frac{20.9-15}{20.9-\text{O}_2 \text{ concentration (\%)}} \right)$$

$$= \quad \quad \quad \mathbf{117 \text{ ppmv @15\% O}_2}$$

NOx Emission Rate (g/hp-hr): Applicable no

$$= \left(\frac{\text{g}}{\text{HP-hr}} \right) = \frac{Cd \times .001912 \times Q \times \left(\frac{0.028317 \text{m}^3}{\text{ft}^3} \right)}{HP}$$

$$= \quad \quad \quad \mathbf{NOT APPLICABLE}$$

NOx Emission Rate (lb/hr): Applicable yes

$$= \left(\frac{\text{ppmv}}{10^6} \right) \times \text{Average Stack Flow, Q} \times \left(\frac{MW}{385.3} \right)$$

$$= \quad \quad \quad \mathbf{18.54 \text{ (lb/hr)}}$$

NOx Emission Rate (tons/year): Applicable yes

$$= \left(\frac{\text{tons}}{\text{yr}} \right) = \frac{\text{lb}}{\text{hr}} \times \frac{8760 \text{ hr}}{\text{year}} \times \frac{\text{ton}}{2000 \text{ lb}}$$

$$= \quad \quad \quad \mathbf{81.19 \text{ (tons/yr)}}$$

NOx Emissions (lb/MMBtu): Applicable no

$$= \left(\frac{\text{lb}}{\text{MMBtu}} \right) = \left(\frac{Cd}{10^6} \right) \times \left(\frac{MW}{385.3} \right) \times \left(\frac{DSCF}{MMBtu} \right) \times \left(\frac{20.9}{(20.9-\text{O}_2 \text{ concentration (\%)})} \right)$$

$$= \quad \quad \quad \mathbf{NOT APPLICABLE}$$

Example Calculations: Emissions Calculations

Test Run #: DH-010414.01

Component: CO

Observed Measurements/Data:		Standards/Constants/Conversion Factors	
13.1	CO final concentration, Cd (ppmv)	528	EPA Standard Temperature, Tstd (°R)
1973673	Average Stack Gas Flow Rate, Q (DSCFH)	29.92	EPA Standard Pressure, Pstd (in. Hg)
16.9	O2 final concentration (%)	385.3	Gas Constant @ EPA STP (SCF/lb-mol)
3630	Horsepower (Hp)	28.317	Liters per Cubic Foot
8698	Fuel O2 Factor (DSCF/MMBtu)	28	CO molecular wt., MW (lb/lb-mol)
		0.001164	Conversion constant (CO ppm to g/m3)
		8760	hours per year
		2000	pounds per ton
		0.028317	cubic meters per cubic feet

CO Emissions (ppmv @ 15%O2): Applicable no

$$= \text{ppmv@15\%O}_2 = Cd \times \left(\frac{20.9-15}{20.9-\text{O}_2 \text{ concentration (\%)}} \right)$$

= **NOT APPLICABLE**

CO Emission Rate (g/hp-hr): Applicable no

$$= \left(\frac{\text{g}}{\text{HP-hr}} \right) = \frac{Cd \times .001164 \times Q \times \left(\frac{0.028317 \text{m}^3}{\text{ft}^3} \right)}{HP}$$

= **NOT APPLICABLE**

CO Emission Rate (lb/hr): Applicable yes

$$= \left(\frac{\text{ppmv}}{10^6} \right) \times \text{Average Stack Flow, Q} \times \left(\frac{MW}{385.3} \right)$$

= **1.87 (lb/hr)**

CO Emission Rate (tons/year): Applicable yes

$$= \left(\frac{\text{tons}}{\text{yr}} \right) = \frac{\text{lb}}{\text{hr}} \times \frac{8760 \text{ hr}}{\text{year}} \times \frac{\text{ton}}{2000 \text{ lb}}$$

= **8.20 (tons/yr)**

CO Emissions (lb/MMBtu): Applicable no

$$= \left(\frac{\text{lb}}{\text{MMBtu}} \right) = \left(\frac{Cd}{10^6} \right) \times \left(\frac{MW}{385.3} \right) \times \left(\frac{DSCF}{MMBtu} \right) \times \left(\frac{20.9}{(20.9-\text{O}_2 \text{ concentration (\%)})} \right)$$

= **NOT APPLICABLE**

THE LINDE GROUP

Linde

CERTIFICATE OF ANALYSIS

EPA PROTOCOL MIXTURE

PGVP ID#: I12013
 CUSTOMER: UNION CITY
 SALES#: 501210969
 PROD#: 1254051
 P.O.#: 4501210969
 MATERIAL#: 24091202
 CERTIFICATION DATE: 01-May-2013
 EXPIRATION DATE: 02-May-2021

PROCEDURE #: G1
 GAS CODE: APPVD
 CYLINDER #: CC-310704
 CYLINDER PRES: 2000 PSIG
 CYLINDER VALVE: CGA 660
 CYLINDER SIZE: 2A
 CYLINDER MATERIAL: Aluminum
 GAS VOLUME: 4000 Liter
 BLEND TOLERANCE: 5% Relative
 PAGE: 1 of 1

(Using the May 2012 Revision of the EPA Protocol)

CERTIFICATION HISTORY

COMPONENT	DATE OF ASSAY	MEAN CONCENTRATION	CERTIFIED CONCENTRATION	ANALYTICAL ACCURACY
Propane	01-May-2013	30.0 ppm	30.0 ppm	+/- 1%
Nitric Oxide	24-Apr-2013 01-May-2013	47.4 ppm 47.3 ppm	47.3 ppm	+/- 1%
NOx			47.3 ppm	Reference Value Only
Carbon Monoxide	01-May-2013	95.3 ppm	95.3 ppm	+/- 1%

BALANCE Nitrogen

PREVIOUS CERTIFICATION DATES: None

REFERENCE STANDARDS

COMPONENT	SRM/NTRM#	CYLINDER#	CONCENTRATION
Propane	GMIS-1	cc-113884	100.5 ppm
Nitric Oxide	GMIS-1	CC-278874	100.7 ppm
Carbon Monoxide	GMIS-1	cc-88590	96.8 ppm

INSTRUMENTATION

COMPONENT	MAKE/MODEL	SERIAL #	DETECTOR	CALIBRATION DATE(S)
Propane	H. Packard 6890	US00001434	GC - FID	01-May-2013
Nitric Oxide	CAI 400-CLD	6L09004	Cheml	01-Apr-2013
Carbon Monoxide	Horiba VIA-510	570423011	NDIR	19-Apr-2013

THIS STANDARD IS NIST TRACEABLE. IT WAS CERTIFIED ACCORDING TO THE 1997 EPA PROTOCOL PROCEDURES.
 DO NOT USE THIS STANDARD IF THE CYLINDER PRESSURE IS LESS THAN 100 PSIG.

ANALYST: MATTHEW JACKSON

Linde Gas North America LLC

DATE: 01-May-2013



Assay Laboratory: Red Ball TGS
 555 Craig Kennedy Way
 Shreveport, LA 71107
 800-551-8150

CERTIFICATE OF ANALYSIS EPA PROTOCOL GAS

Cylinder Number:	EB0027577	Certification Date:	10/29/2012
Product ID Number:	124749	Expiration Date:	10/22/2016
Cylinder Pressure:	1900 PSIG	MFG Facility:	RBTGS-Shreveport-LA
COA Number:	GC1210170814-0	Lot Number:	GC1210170814
Customer PO. NO.:		Tracking Number:	048358699
Customer:		Previous Certification Dates:	

This calibration standard has been certified per the 1997 EPA Traceability Protocol, Document EPA-600/97/121, using procedure G1 and/or G2. All values so noted are certified to be +/-1% NIST Traceable.

Do Not Use This Cylinder Below 150 psig (1.0 Megapascal).

Certified Concentration(s)

Component	Concentration	Analytical Principle	Accuracy
Nitric Oxide	94.5 PPM	Non Dispersive Infrared Absorptiometry	± 1% NIST
Total Oxides of Nitrogen	94.7 PPM	Non Dispersive Infrared Absorptiometry	± 1% NIST
Propane	51 PPM	FTIR	± 1% NIST
Carbon Monoxide	193 PPM	Gas Correlation Filter	± 1% NIST
Nitrogen	Balance		

Reference Standard(s)

Type	Component	Balance Gas	Concentration	Cylinder Number	Expiration	NIST Reference
GMIS	Nitric Oxide	Nitrogen	98.6 PPM	CC238350	2/14/2013	SRM 1686b
GMIS	Nitric Oxide	Nitrogen	98.6 PPM	CC238350	2/14/2013	SRM 1686b
GMIS	Carbon Monoxide	Nitrogen	398 PPM	EB0005726	1/5/2014	NTRM 021003
SRM	Propane	Nitrogen	49 PPM	CAL018150	8/17/2017	SRM 1667b

Analytical Information

Component	Nitric Oxide		Analysis Date:
Z 0.152	S 16.337	C 15.549	10/22/2012
S 16.399	C 15.733	Z 0.109	Conc. 93.5 PPM
C 15.71	Z 0.088	S 16.451	Conc. 94.6 PPM
			Conc. 94.4 PPM
Component	Carbon Monoxide		Analysis Date:
Z 0.295	S 16.912	C 16.321	10/29/2012
S 16.961	C 16.303	Z 0.281	Conc. 94.9 PPM
C 16.31	Z 0.325	S 16.9825	Conc. 94.8 PPM
			Conc. 94.8 PPM
Component	Propane		Analysis Date:
Z 0.0110	S 49.01	C 50.7800	10/26/2012
S 49.0400	C 50.8	Z 0.004	Conc. 51 PPM
C 50.8	Z 0.0060	S 49.03	Conc. 51 PPM
			Conc. 51 PPM

Z= Zero Gas S= Span Gas C= Candidate Gas

Fred Holt

Fred Holt, CHMM
 Quality Control

Red Ball Technical Gas Service
 PGVP Vendor ID # G12012
 Information and Ordering
 800-551-8150
 Fax (318-425-6309)



Assay Laboratory: Red Ball TGS
 555 Craig Kennedy Way
 Shreveport, LA 71107
 800-551-8150

EPA PROTOCOL GAS CERTIFICATE OF ANALYSIS

Cylinder Number:	EB0046618	Certification Date:	07/29/2013
Product ID Number:	124752	Expiration Date:	07/27/2021
Cylinder Pressure:	1900 PSIG	MFG Facility:	RBTGS-Shreveport-LA
COA #	ML130726.170231.3-0	Lot Number:	ML130726.170231.3
Customer PO. NO.:		Tracking Number:	065271430
Customer:		Previous Certification Dates:	

This calibration standard has been certified per the May 2012 EPA Traceability Protocol, Document EPA-600/R-12/531, using procedure G1.

Do Not Use This Cylinder Below 100 psig (0.7 Megapascal).

Certified Concentration(s)

Component	Concentration	Uncertainty	Analytical Principle
Carbon Dioxide	13.9 %	±0.11 %	NDIR
Oxygen	10.99 %	±0.07 %	MPA
Nitrogen	Balance		

Analytical Measurement Data Available Online.

Reference Standard(s)

Lot	Expiration	Type	Balance	Component	Concentration	Uncertainty(%)	NIST Reference
GC1106080848	09/07/2013	GMIS	N2	CO2	12.57 %	0.384	3221755
GC0807251121	04/28/2019	GMIS	N2	O2	24.43 %	0.52	71001

Analytical Instrumentation

Component	Analytical Principle	Make	Model	Serial	MPC Date
CO2	NDIR	Horiba	VA-3013	H0000P11	07/10/2013
O2	MPA	Horiba	VA-3013	H0000P11	07/11/2013

Z= Zero Gas S= Span Gas C= Candidate Gas

Red Ball Technical Gas Service
 PGVP Vendor ID # G12013
 Information and Ordering
 800-551-8150
 Fax (318-425-6309)

Fred Holt
 Fred Holt, CHMM
 Quality Control



Assay Laboratory: Red Ball TGS
 555 Craig Kennedy Way
 Shreveport, LA 71107
 800-551-8150

EPA PROTOCOL GAS CERTIFICATE OF ANALYSIS

Cylinder Number:	EB0039038	Certification Date:	08/02/2013
Product ID Number:	124753	Expiration Date:	07/31/2021
Cylinder Pressure:	1900 PSIG	MFG Facility:	RB TGS-Shreveport-LA
COA #	ML130726.170120.1-0	Lot Number:	ML130726.170120.1
Customer PO. NO.:		Tracking Number:	065155673
Customer:		Previous Certification Dates:	

This calibration standard has been certified per the May 2012 EPA Traceability Protocol, Document EPA-600/R-12/531, using procedure G1.

Do Not Use This Cylinder Below 100 psig (0.7 Megapascal).

Certified Concentration(s)

Component	Concentration	Uncertainty	Analytical Principle
Carbon Dioxide	6.99 %	±0.03 %	NDIR
Oxygen	20.92 %	±0.08 %	MPA
Nitrogen	Balance		

Analytical Measurement Data Available Online.

Reference Standard(s)

Lot	Expiration	Type	Balance	Component	Concentration	Uncertainty(%)	NIST Reference
GC1106080848	09/07/2013	GMIS	N2	CO2	12.57 %	0.384	3221755
GC0807251121	04/28/2019	GMIS	N2	O2	24.43 %	0.52	71001

Analytical Instrumentation

Component	Analytical Principle	Make	Model	Serial	MPC Date
CO2	NDIR	Horiba	VA-3013	H0000P11	07/31/2013
O2	MPA	Horiba	VA-3013	H0000P11	07/11/2013

Z= Zero Gas S= Span Gas C= Candidate Gas

Red Ball Technical Gas Service
 PGVP Vendor ID # G12013
 Information and Ordering
 800-551-8150
 Fax (318-425-6309)

Fred Holt, CHMM
 Quality Control



1700 Scepter Rd
Waverly, TN 37185
931-296-3357

Certificate of Analysis - EPA Protocol Mixtures

Customer: NORDON

		Protocol:	Reference #:	Lot#:
Cylinder Number:	SX49930	G1	T176792-1	9302603567
Cylinder Pressure:	1900psig	DO NOT USE THIS CYLINDER WHEN THE PRESSURE FALLS BELOW 150 PSIG		
Last Analysis Date:	11/19/2012			
Expiration Date:	11/19/2014			

REPLICATE RESPONSES

Component:	Nitrogen Dioxide	Date:	11/2/2012	Date:	11/19/2012
			45.60		45.20
			45.60		45.26
Certified Conc:	45.38ppm +/- 1% REL		45.40		45.25

BALANCE GAS: Air

REFERENCE STANDARDS:

Component: Nitrogen Dioxide
Reference Standard: SRM
Cylinder #: CAL016152
Concentration: 98.0ppm
Exp Date: 12/31/2015
Lot #: 2660-C-57

CERTIFICATION INSTRUMENTS

Component: Nitrogen Dioxide
Make/Model: HORIBA CLA-510SS
Serial Number: 8H4SOCTJ
Measurement Principle: CHEMI
Last Calibration: 11/2/2012

Notes:

This Certification was performed according to EPA Traceability Protocol for Assay & Certification of Gaseous Calibration Standards September 1997, using procedure G1 and/or G2.

U.S. EPA Vendor ID No.: D52012: PGVP Participation Date: 1/1/2012: PGVP Renewal Date: 12/31/12

Analyst: *Julie Higgins*
Julie Higgins

Date: 11/26/2012

NOx Converter Efficiency and Response Times

Date: January 4, 2014

METHOD 7E NOx CONVERTER EFFICIENCY TEST

Certified NO ₂ Conc. (ppmv)	45.38
Measured NOx Conc. (ppmv)	41.03
Converter Efficiency (%)	90

Criteria: Converter Efficiency should be 90% or greater

METHOD 7E RESPONSE TIMES

	NOx (ppmv)	CO (ppmv)	O ₂ (%)
Low-Level Gas Concentration	0	0	0
Upscale Gas Concentration	94.7	193	20.92
95% of Upscale Gas	90.0	183.4	19.9

	NOx	CO	O ₂
Low-Level Gas RT (sec)	70	66	30
Upscale Gas RT (sec)	63	63	33
Longer Analyzer RT Interval (sec)	70	66	33
System Response Time (sec)	70		
*System Response Time (min)	1.2		
†System Purge Time (min)	2.3		

*Longer interval of time to reach 95% of stable stable response for low & upscale level gases.

Criteria: †System Purge Time shall be ≥ 2 times the System Response Time

Analyzer Gas Quality Assurance

Test Run:	DH-010414.01		
Parameter	NOx	CO	O2
CALIBRATION ERROR DATA			
Range/Span Data			
Analyzer Range	100	200	25
Method 7E Span	94.7	193.0	20.9
Certified Calibration Gas Data			
Zero Level Certified Value (ppm or %)	0	0	0
Low Level Certified Value (ppm or %)	0.0	0.0	0.0
Mid Level Certified Value (ppm or %)	47.3	95.3	10.99
High Level Certified Value (ppm or %)	94.7	193.0	20.92
Calibration Error Observations (Direct)			
Zero Level Observed (ppm or %)	n/a	n/a	n/a
Low Level Observed (ppm or %)	0.4	0.6	0.1
Mid Level Observed (ppm or %)	46.9	96.7	11.2
High Level Observed (ppm or %)	94.7	194.6	21.3
Calibration Error Results			
Difference from Zero Level (%)	n/a	n/a	n/a
Difference from Low Level (%)	0.44	0.33	0.60
Difference from Mid Level (%)	0.39	0.71	0.87
Difference from High Level (%)	0.02	0.82	1.64
<i>Allowable Difference (%)</i>	(±2%)	(±2%)	(±2%)
TEST RUN DATA			
Bias Observations			
Low/Zero Level Cal. Gas Certified Value (ppm or %)	0.00	0.00	0.00
Upscale Cal. Gas Certified Value (ppm or %)	94.70	193.00	20.92
Initial Low/Zero Level Observed (ppm or %)	0.42	0.63	0.13
Initial Upscale Level Observed (ppm or %)	94.68	194.59	21.26
Initial Bias Low/Zero Level Gas (ppm or %)	1.66	-0.63	0.25
Initial Bias Upscale Level Gas (ppm or %)	92.45	192.76	21.19
Final Bias Low/Zero Level Gas (ppm or %)	0.85	0.00	0.28
Final Bias Upscale Level Gas (ppm or %)	91.68	191.43	21.21
Bias and Drift Results			
Initial Bias Low/Zero Level (%)	1.31	-0.65	0.57
Initial Bias Upscale Level (%)	-2.36	-0.95	-0.37
Final Bias Low/Zero Level (%)	0.45	-0.32	0.75
Final Bias Upscale Level (%)	-3.17	-1.63	-0.25
<i>Allowable Bias (%)</i>	(±5%)	(±5%)	(±5%)
Low/Zero Level Drift Calculation (%)	0.86	0.33	0.17
Upscale Level Drift Calculation (%)	0.81	0.69	0.12
<i>Allowable Drift (%)</i>	(±3%)	(±3%)	(±3%)
Raw Results (ppmv or %)			
	76.69	12.70	17.22
Minimum Detection Limit (MDL)	0.5	1.0	0.1
Corrected Results (ppmv or %)	78.7	13.1	16.9
*Final Results (ppmv or %)	78.7	13.1	16.9

**Final Results which are shown in Italics represent the MDL for that analyte*

Analyzer Gas Quality Assurance

Test Run:	DH-010414.02		
Parameter	NOx	CO	O2
CALIBRATION ERROR DATA			
Range/Span Data			
Analyzer Range	100	200	25
Method 7E Span	94.7	193.0	20.9
Certified Calibration Gas Data			
Zero Level Certified Value (ppm or %)	0	0	0
Low Level Certified Value (ppm or %)	0.0	0.0	0.0
Mid Level Certified Value (ppm or %)	47.3	95.3	10.99
High Level Certified Value (ppm or %)	94.7	193.0	20.92
Calibration Error Observations (Direct)			
Zero Level Observed (ppm or %)	0.0	0.0	0.0
Low Level Observed (ppm or %)	0.4	0.6	0.1
Mid Level Observed (ppm or %)	46.9	96.7	11.2
High Level Observed (ppm or %)	94.7	194.6	21.3
Calibration Error Results			
Difference from Zero Level (%)	n/a	n/a	n/a
Difference from Low Level (%)	0.44	0.33	0.60
Difference from Mid Level (%)	0.39	0.71	0.87
Difference from High Level (%)	0.02	0.82	1.64
<i>Allowable Difference (%)</i>	(±2%)	(±2%)	(±2%)
TEST RUN DATA			
Bias Observations			
Low/Zero Level Cal. Gas Certified Value (ppm or %)	0.00	0.00	0.00
Upscale Cal. Gas Certified Value (ppm or %)	94.70	193.00	20.92
Initial Low/Zero Level Observed (ppm or %)	0.42	0.63	0.13
Initial Upscale Level Observed (ppm or %)	94.68	194.59	21.26
Initial Bias Low/Zero Level Gas (ppm or %)	0.85	0.00	0.28
Initial Bias Upscale Level Gas (ppm or %)	91.68	191.43	21.21
Final Bias Low/Zero Level Gas (ppm or %)	2.50	-1.50	0.34
Final Bias Upscale Level Gas (ppm or %)	91.54	190.52	21.25
Bias and Drift Results			
Initial Bias Low/Zero Level (%)	0.45	-0.32	0.75
Initial Bias Upscale Level (%)	-3.17	-1.63	-0.25
Final Bias Low/Zero Level (%)	2.20	-1.11	1.00
Final Bias Upscale Level (%)	-3.32	-2.11	-0.05
<i>Allowable Bias (%)</i>	(±5%)	(±5%)	(±5%)
Low/Zero Level Drift Calculation (%)	1.75	0.78	0.26
Upscale Level Drift Calculation (%)	0.15	0.47	0.20
<i>Allowable Drift (%)</i>	(±3%)	(±3%)	(±3%)
Raw Results (ppmv or %)			
	78.07	11.51	17.23
Minimum Detection Limit (MDL)	0.5	1.0	0.1
Corrected Results (ppmv or %)	80.4	12.3	16.9
*Final Results (ppmv or %)	80.4	12.3	16.9

**Final Results which are shown in Italics represent the MDL for that analyte*

Analyzer Gas Quality Assurance

Test Run:	DH-010414.03		
Parameter	NOx	CO	O2
CALIBRATION ERROR DATA			
Range/Span Data			
Analyzer Range	100	200	25
Method 7E Span	94.7	193.0	20.9
Certified Calibration Gas Data			
Zero Level Certified Value (ppm or %)	0	0	0
Low Level Certified Value (ppm or %)	0.0	0.0	0.0
Mid Level Certified Value (ppm or %)	47.3	95.3	10.99
High Level Certified Value (ppm or %)	94.7	193.0	20.92
Calibration Error Observations (Direct)			
Zero Level Observed (ppm or %)	0.0	0.0	0.0
Low Level Observed (ppm or %)	0.4	0.6	0.1
Mid Level Observed (ppm or %)	46.9	96.7	11.2
High Level Observed (ppm or %)	94.7	194.6	21.3
Calibration Error Results			
Difference from Zero Level (%)	n/a	n/a	n/a
Difference from Low Level (%)	0.44	0.33	0.60
Difference from Mid Level (%)	0.39	0.71	0.87
Difference from High Level (%)	0.02	0.82	1.64
<i>Allowable Difference (%)</i>	(±2%)	(±2%)	(±2%)
TEST RUN DATA			
Bias Observations			
Low/Zero Level Cal. Gas Certified Value (ppm or %)	0.00	0.00	0.00
Upscale Cal. Gas Certified Value (ppm or %)	94.70	193.00	20.92
Initial Low/Zero Level Observed (ppm or %)	0.42	0.63	0.13
Initial Upscale Level Observed (ppm or %)	94.68	194.59	21.26
Initial Bias Low/Zero Level Gas (ppm or %)	2.50	-1.50	0.34
Initial Bias Upscale Level Gas (ppm or %)	91.54	190.52	21.25
Final Bias Low/Zero Level Gas (ppm or %)	2.11	-2.63	0.36
Final Bias Upscale Level Gas (ppm or %)	91.12	189.62	21.30
Bias and Drift Results			
Initial Bias Low/Zero Level (%)	2.20	-1.11	1.00
Initial Bias Upscale Level (%)	-3.32	-2.11	-0.05
Final Bias Low/Zero Level (%)	1.79	-1.69	1.13
Final Bias Upscale Level (%)	-3.76	-2.58	0.18
<i>Allowable Bias (%)</i>	(±5%)	(±5%)	(±5%)
Low/Zero Level Drift Calculation (%)	0.41	0.58	0.12
Upscale Level Drift Calculation (%)	0.45	0.47	0.23
<i>Allowable Drift (%)</i>	(±3%)	(±3%)	(±3%)
Raw Results (ppmv or %)			
	81.34	10.56	17.27
Minimum Detection Limit (MDL)	0.5	1.0	0.1
Corrected Results (ppmv or %)	84.1	12.7	16.9
*Final Results (ppmv or %)	84.1	12.7	16.9

**Final Results which are shown in Italics represent the MDL for that analyte*

DAQ Logs

Company	Plant Name	Unit Make	Unit Model	Unit Number	Status	Date	Time	NOx (ppmvd)	CO (ppmvd)	O2 (%, dry)
Enterprise Products	South Carlsbad CS	Solar	Centaur	Calibration Error	0NOx/0CO/0O2	1/4/14	7:21	0.42	0.63	0.13
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	7:22	3.92	0.66	20.19
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	7:23	93.51	0.21	21.24
Enterprise Products	South Carlsbad CS	Solar	Centaur	Calibration Error	94.7NOx/20.92O2	1/4/14	7:24	94.68	0.27	21.26
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	7:25	71.35	-6.37	10.85
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	7:26	39.61	-7.87	10.79
Enterprise Products	South Carlsbad CS	Solar	Centaur	Calibration Error	47.3NOx/10.99O2	1/4/14	7:27	46.93	-1.12	11.17
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	7:28	38.41	116.68	0.17
Enterprise Products	South Carlsbad CS	Solar	Centaur	Calibration Error	193CO	1/4/14	7:29	24.61	194.59	0.15
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	7:30	24.27	169.53	0.16
Enterprise Products	South Carlsbad CS	Solar	Centaur	Calibration Error	95.3CO	1/4/14	7:31	1.07	96.67	0.14
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	7:32	3.55	62.58	0.13
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	7:33	38.71	48.57	0.15
Enterprise Products	South Carlsbad CS	Solar	Centaur	CE Test	NO2	1/4/14	7:34	41.77	44.67	0.17
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	7:35	25.81	1.20	0.14
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	7:36	1.02	1.21	0.14
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	7:37	0.81	0.97	0.14
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	7:38	0.82	1.23	0.15
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	7:39	0.76	1.12	0.14
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	7:40	0.87	0.82	0.15
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	7:41	0.84	1.17	0.13
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	7:42	0.91	1.39	0.16
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	7:43	0.76	0.92	0.14
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	7:44	0.69	0.78	0.15
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	7:45	1.06	0.94	0.19
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	7:46	1.12	0.83	0.28
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	7:47	1.26	1.15	0.52
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	7:48	1.14	1.10	0.74
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	7:49	1.19	1.02	0.93
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	7:50	1.29	0.91	1.21
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	7:51	1.38	1.42	1.39
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	7:52	1.16	1.35	1.53
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	7:53	1.41	1.26	1.78
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	7:54	1.37	1.21	1.94
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	7:55	1.27	1.13	2.16
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	7:56	1.40	1.07	2.39
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	7:57	1.37	1.29	2.66
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	7:58	1.52	1.44	2.89
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	7:59	1.42	1.31	3.07
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	8:00	1.52	1.22	3.31
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	8:01	1.45	1.23	3.51
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	8:02	1.46	1.38	3.72
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	8:03	1.57	1.59	3.97
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	8:04	1.54	1.23	4.19
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	8:05	1.57	1.22	4.41
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	8:06	1.42	1.18	1.45
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	8:07	0.81	0.92	0.19
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	8:08	0.73	0.90	0.18
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	8:09	0.78	0.84	0.18
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	8:10	0.82	0.66	0.18
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	8:11	22.76	13.77	17.03
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	8:12	75.09	27.54	17.19
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	8:13	76.40	20.20	18.18
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	8:14	4.32	0.07	21.20
Enterprise Products	South Carlsbad CS	Solar	Centaur	Bias Check	0NOx/0CO/20.92O2	1/4/14	8:15	1.66	-0.63	21.19
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	8:16	28.78	86.95	0.47
Enterprise Products	South Carlsbad CS	Solar	Centaur	Bias Check	94.7NOx/193CO/0O2	1/4/14	8:17	92.45	192.76	0.25
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	8:18	88.63	101.50	17.01
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	8:19	76.49	16.82	17.18
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P1	DH-010414.01	1/4/14	8:20	76.40	31.71	17.19
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P1	DH-010414.01	1/4/14	8:21	76.70	19.32	17.19
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P1	DH-010414.01	1/4/14	8:22	76.52	16.99	17.20
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P1	DH-010414.01	1/4/14	8:23	76.59	12.25	17.20
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P2	DH-010414.01	1/4/14	8:24	76.64	9.08	17.19
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P2	DH-010414.01	1/4/14	8:25	77.06	21.17	17.18
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P2	DH-010414.01	1/4/14	8:26	77.23	14.08	17.22
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P3	DH-010414.01	1/4/14	8:27	76.98	8.87	17.21

DAQ Logs

Company	Plant Name	Unit Make	Unit Model	Unit Number	Status	Date	Time	NOx (ppmvd)	CO (ppmvd)	O2 (%, dry)
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P3	DH-010414.01	1/4/14	8:28	77.28	13.24	17.20
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P3	DH-010414.01	1/4/14	8:29	76.89	25.32	17.20
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P4	DH-010414.01	1/4/14	8:30	76.32	10.29	17.20
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P4	DH-010414.01	1/4/14	8:31	76.24	14.23	17.20
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P4	DH-010414.01	1/4/14	8:32	76.73	14.74	17.23
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P5	DH-010414.01	1/4/14	8:33	76.75	15.37	17.21
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P5	DH-010414.01	1/4/14	8:34	77.70	12.23	17.21
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P5	DH-010414.01	1/4/14	8:35	77.61	12.50	17.22
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P6	DH-010414.01	1/4/14	8:36	77.56	12.06	17.23
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P6	DH-010414.01	1/4/14	8:37	77.71	12.16	17.23
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P6	DH-010414.01	1/4/14	8:38	77.66	12.70	17.23
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	8:39	77.64	11.35	19.70
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	8:40	4.26	1.07	21.24
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	8:41	3.69	3.05	18.20
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	8:42	77.11	13.11	17.23
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P7	DH-010414.01	1/4/14	8:43	77.46	14.12	17.22
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P7	DH-010414.01	1/4/14	8:44	77.58	14.16	17.22
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P7	DH-010414.01	1/4/14	8:45	77.43	12.11	17.20
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P7	DH-010414.01	1/4/14	8:46	77.61	11.83	17.21
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P8	DH-010414.01	1/4/14	8:47	77.62	4.15	17.22
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P8	DH-010414.01	1/4/14	8:48	77.03	11.53	17.24
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P8	DH-010414.01	1/4/14	8:49	77.02	11.62	17.23
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P9	DH-010414.01	1/4/14	8:50	76.36	8.02	17.20
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P9	DH-010414.01	1/4/14	8:51	75.50	3.66	17.26
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P9	DH-010414.01	1/4/14	8:52	75.09	10.41	17.59
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P10	DH-010414.01	1/4/14	8:53	74.59	6.33	17.22
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P10	DH-010414.01	1/4/14	8:54	73.10	9.95	17.09
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P10	DH-010414.01	1/4/14	8:55	76.57	11.42	17.27
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P11	DH-010414.01	1/4/14	8:56	75.47	9.41	17.20
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P11	DH-010414.01	1/4/14	8:57	75.35	8.14	17.23
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P11	DH-010414.01	1/4/14	8:58	76.93	13.24	17.25
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P12	DH-010414.01	1/4/14	8:59	75.55	9.57	17.26
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P12	DH-010414.01	1/4/14	9:00	77.90	12.98	17.24
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2, P12	DH-010414.01	1/4/14	9:01	77.66	11.54	17.24
DH-010414.01 Averages								76.69	12.70	17.22
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	9:02	70.88	6.28	16.79
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	9:03	12.04	2.26	20.77
Enterprise Products	South Carlsbad CS	Solar	Centaur	Bias Check	0NOx/20.92O2	1/4/14	9:04	0.85	0.00	21.21
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	9:05	23.26	94.71	0.26
Enterprise Products	South Carlsbad CS	Solar	Centaur	Bias Check	94.7NOx/OO2	1/4/14	9:06	91.68	191.43	0.28
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	9:07	88.96	113.37	16.91
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	9:08	77.33	13.19	17.22
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.02	1/4/14	9:09	77.43	13.64	17.21
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.02	1/4/14	9:10	77.51	11.03	17.23
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.02	1/4/14	9:11	77.43	11.77	17.22
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.02	1/4/14	9:12	77.41	12.91	17.22
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.02	1/4/14	9:13	77.71	11.17	17.22
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.02	1/4/14	9:14	77.45	10.93	17.21
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.02	1/4/14	9:15	77.52	10.80	17.24
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.02	1/4/14	9:16	77.58	12.10	17.23
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.02	1/4/14	9:17	77.80	11.00	17.23
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.02	1/4/14	9:18	77.75	11.32	17.24
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.02	1/4/14	9:19	77.70	12.53	17.25
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.02	1/4/14	9:20	77.79	14.40	17.23
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.02	1/4/14	9:21	77.73	11.35	17.24
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.02	1/4/14	9:22	77.88	10.97	17.24
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.02	1/4/14	9:23	77.92	10.77	17.21
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.02	1/4/14	9:24	78.15	10.71	17.23
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.02	1/4/14	9:25	77.92	10.31	17.23
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.02	1/4/14	9:26	78.19	10.32	17.24
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.02	1/4/14	9:27	78.74	10.17	17.24
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.02	1/4/14	9:28	79.05	10.45	17.24
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.02	1/4/14	9:29	78.60	10.36	17.24
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.02	1/4/14	9:30	78.49	10.61	17.25
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.02	1/4/14	9:31	78.74	10.00	17.24
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.02	1/4/14	9:32	78.91	10.30	17.25
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.02	1/4/14	9:33	78.91	11.49	17.25
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.02	1/4/14	9:34	78.51	12.79	17.23

DAQ Logs

Company	Plant Name	Unit Make	Unit Model	Unit Number	Status	Date	Time	NOx (ppmvd)	CO (ppmvd)	O2 (%, dry)
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.02	1/4/14	9:35	78.71	11.39	17.26
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.02	1/4/14	9:36	78.28	10.84	17.21
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.02	1/4/14	9:37	78.48	10.99	17.24
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.02	1/4/14	9:38	78.47	12.85	17.25
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.02	1/4/14	9:39	77.72	14.62	17.24
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.02	1/4/14	9:40	77.63	13.37	17.24
DH-010414.02 Averages								78.07	11.51	17.23
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	9:41	61.99	16.81	21.18
Enterprise Products	South Carlsbad CS	Solar	Centaur	Bias Check	0NOx/20.92O2	1/4/14	9:42	2.50	-1.50	21.25
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	9:43	21.31	58.04	1.49
Enterprise Products	South Carlsbad CS	Solar	Centaur	Bias Check	94.7NOx/0O2	1/4/14	9:44	91.54	190.52	0.34
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	9:45	86.46	73.20	17.17
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	9:46	78.59	12.03	17.24
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.03	1/4/14	9:47	79.11	10.31	17.26
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.03	1/4/14	9:48	79.25	11.30	17.27
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.03	1/4/14	9:49	79.52	9.92	17.26
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.03	1/4/14	9:50	79.99	9.71	17.24
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.03	1/4/14	9:51	80.48	9.48	17.26
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.03	1/4/14	9:52	80.27	9.44	17.24
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.03	1/4/14	9:53	80.31	9.91	17.26
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.03	1/4/14	9:54	80.31	10.72	17.25
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.03	1/4/14	9:55	80.18	9.00	17.25
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.03	1/4/14	9:56	80.76	10.20	17.27
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.03	1/4/14	9:57	81.01	16.00	17.28
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.03	1/4/14	9:58	81.36	11.69	17.26
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.03	1/4/14	9:59	82.09	16.89	17.28
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.03	1/4/14	10:00	82.44	11.24	17.28
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.03	1/4/14	10:01	82.25	10.23	17.26
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.03	1/4/14	10:02	82.07	10.78	17.24
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.03	1/4/14	10:03	82.19	10.41	17.26
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.03	1/4/14	10:04	82.13	9.73	17.27
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.03	1/4/14	10:05	82.25	10.93	17.25
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.03	1/4/14	10:06	82.14	10.30	17.27
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.03	1/4/14	10:07	82.23	9.32	17.27
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.03	1/4/14	10:08	82.22	9.21	17.28
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.03	1/4/14	10:09	81.95	11.52	17.27
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.03	1/4/14	10:10	82.35	9.54	17.29
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.03	1/4/14	10:11	82.21	10.07	17.29
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.03	1/4/14	10:12	82.23	9.75	17.28
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.03	1/4/14	10:13	82.22	9.70	17.28
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.03	1/4/14	10:14	82.17	9.18	17.27
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.03	1/4/14	10:15	82.24	9.96	17.29
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.03	1/4/14	10:16	82.21	9.92	17.28
Enterprise Products	South Carlsbad CS	Solar	Centaur	T2	DH-010414.03	1/4/14	10:17	82.23	9.58	17.29
DH-010414.03 Averages								81.34	10.56	17.27
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	10:18	49.14	12.33	21.26
Enterprise Products	South Carlsbad CS	Solar	Centaur	Bias Check	0NOx/20.92O2	1/4/14	10:19	2.11	-2.63	21.30
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	10:20	38.80	116.05	0.41
Enterprise Products	South Carlsbad CS	Solar	Centaur	Bias Check	94.7NOx/0O2	1/4/14	10:21	91.12	189.62	0.36
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	10:22	86.39	62.81	17.20
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	16:04	40.92	1.54	0.08
Enterprise Products	South Carlsbad CS	Solar	Centaur	RT	NO2	1/4/14	16:05	41.03	1.46	0.09
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	16:06	19.78	1.46	0.08
Enterprise Products	South Carlsbad CS	Solar	Centaur			1/4/14	16:07	-2.28	0.24	0.01



New Mexico Environment Department
 525 Camino de los Marquez, Suite 1
 Santa Fe, NM 87505
 Phone (505) 476-4300 Fax (505) 476-4375



Version 1/1/2010

NMED USE ONLY	
DTS	
TEMPO	

UNIVERSAL STACK TEST NOTIFICATION, PROTOCOL AND REPORT FORM

NMED USE ONLY	
Staff	
Admin	

Submit to: Stacktest.aqb@state.nm.us

I. DATABASE HEADER INFORMATION (drop down menus in bold)			
a. AI# 218	Test Report		Periodic Test (Portable Analyzer)
d. Company Name: Enterprise Field Services LLC		e. Facility Name: South Carlsbad Compressor Station	
f. Emission Unit Numbers: 1, 2		g. Emission Unit Description (boiler, Waukesha 7042, etc) Turbines, Solar Centaur T-4702	
h. Reports - Tracking Number from notification response: CMT		i. Proposed Test Date: Week of 1/19/15	j. Actual test date: 1/20/2015
k. Reason for test (name permit requirement, NSPS, MACT, consent decree, etc. Indicate here is this notification is a revised test date only) Annual performance test of existing turbines pursuant to NSR condition A205C.			

II. GENERAL COMPANY AND FACILITY INFORMATION					
a. Company Address: PO Box 4324			k.. Facility Address: Roberson Road, Eddy County		
b. City: Houston	c. State: TX	d. Zip: 77210[±]	l. City: Loving	m. State: NM	n. Zip: 88526
e. Environmental Contact: Dina Babinski		f. Title: ENV Supervisor		o. Facility Contact: Thomas Green	
g. Phone Number: 210-528-3824		h. Cell Number: 210-232-4880		p. Title: Area Supervisor	
i. Email Address: djbabinski@eprod.com		q. Phone Number: 575-885-7235		r. Cell Number: 575-708-0015	
j. Title V Permit Number: P-130-R2		s. Email Address: tdgreen@eprod.com		t. NSR Permit Number: NSR 220M8-R1	
u. Detailed driving directions from nearest New Mexico town: From Loving, UN285 north to Roberson Road west, Roberson Road west to station.					

III. TESTING FIRM		
a. Company: Compliance Services and Testing		g. Contact: Chris Spencer
b. Address 1: 7108 Washington NE Ste. A		h. Title: Director
c. Address 2: PO Box 94191-87199		i. Office Phone: 505-681-4909
		j. Cell Phone: 505-681-4909

d. City: Albuquerque	e. State: NM	f. Zip: 87109	k. Email Address: cspencer@comptestng.com
--------------------------------	------------------------	-------------------------	---

IV. EMISSION UNIT			STACK PARAMETERS	
a. Emission Unit Number: 1 and 2	b. Make & Model Number Solar Centaur T-4702		m. Velocity (ft/sec):	177
c. Serial Number: See section g.	d. Permitted Capacity: 3609 hp		n. Temperature (°C):	486
e. Exceptions: Explain if test is late, rescheduled, related to an enforcement action:			o. Stack Diameter, D (in.):	NA
			p. Distance to Stack Bends or Obstructions:	
			Upstream, Distance A (in.):	NA
g. Emission Unit Description and brief process name or description: Turbine 1 SN: OHD10C7915 Turbine 2 SN: OHE12C7057 Natural gas-fired turbines for natural gas compression.			Downstream, Distance B (in.):	NA
h. Installation Date:	i. Startup Date:	k. Date Reached Max. Capacity:		
l. Control Equipment Description as listed in permit (model, ser. # etc. if applicable): NA			<p>Attach an explanation or drawing to explain any difficult or unusual stack geometry or parameters.</p>	

V. POLLUTANTS AND PROPOSED TEST METHODS			
Pollutant or Parameter:	Proposed Test Methods (Deviations from approved methods require supporting documentation and prior authorization)		Deviation to Test Method Requested
<input checked="" type="checkbox"/>	Portable Analyzer Methods for NOx, CO, SO₂		<input type="checkbox"/>
<input type="checkbox"/>	NOx	EPA Method 7E	<input type="checkbox"/>
<input type="checkbox"/>	CO	EPA Method 10	<input type="checkbox"/>
<input type="checkbox"/>	SO ₂	EPA Method 6	<input type="checkbox"/>
<input type="checkbox"/>	VOCs	(Specify)	<input type="checkbox"/>
<input type="checkbox"/>	HAPs	(Specify)	<input type="checkbox"/>
<input type="checkbox"/>	PM (TSP)	EPA Method 5	<input type="checkbox"/>
<input type="checkbox"/>	PM ₁₀	EPA Method 201	<input type="checkbox"/>
<input type="checkbox"/>	PM _{2.5}	(Specify)	<input type="checkbox"/>
<input type="checkbox"/>	Opacity	EPA Method 9	<input type="checkbox"/>
<input type="checkbox"/>	Visual E.	EPA Method 22	<input type="checkbox"/>
<input type="checkbox"/>	Stack Flow	EPA Methods 1 - 3	<input type="checkbox"/>
<input type="checkbox"/>	Moisture	EPA Method 4	<input type="checkbox"/>
<input type="checkbox"/>	Other	(Specify)	<input type="checkbox"/>
<input type="checkbox"/>	Other	(Specify)	<input type="checkbox"/>

List Specific VOC's and HAP's:

VI. PROPOSED TEST RUN AND TEST LOAD INFORMATION

a. Number of Test Runs: 3	b. Run Duration 20 min	c. Required by (regulation or permit number): NSR 220 A205C	d. Specific Condition or Section: A205C
-------------------------------------	----------------------------------	---	---

PLEASE NOTE – Default run duration is 60 minutes, unless otherwise specified by an applicable regulation.

e. Expected Load: >90%	f. Percent of Permitted Capacity: >90%	g. Is this an opacity test? Yes <input type="checkbox"/> No <input checked="" type="checkbox"/>	h. If yes, no. of observation pts.:
-------------------------------------	---	--	-------------------------------------

i. If expected load during test is less than 90% of capacity, explain:

NOTE – Failure to test at 90-100% of permitted load will limit unit operation to 110% of tested load until a new initial compliance test is conducted.

PLANT OR UNIT OPERATING PARAMETERS TO BE MONITORED

j. List and explain the plant operating parameters that will be monitored and applicable permit conditions or regulatory standards.

Fuel usage, compressor operating parameters, turbine operating parameters.

VII. ADDITIONAL DETAILS (where applicable)

RATA and INSTRUMENTAL ANALYZER CALIBRATION PROCEDURES

a. Do any of the methods you are proposing utilize instrumental analyzers (i.e.; EPA Methods 3A, 6C, 7E, 10, 18, 25/25A, 320 etc.)? If yes, briefly describe analyzer calibration procedures and/or calibration standard procedures. Enter the highest pollutant concentration expected and the proposed concentrations of calibration gases.	<input checked="" type="checkbox"/> Yes	<input type="checkbox"/> No
---	---	-----------------------------

As described in the methods.

SAMPLING TRAIN LEAK CHECK PROCEDURES

b. Do any of the methods you are proposing utilize the EPA Method 5 sampling train (i.e.; EPA Methods 1-4, 5, 17, 26/26A, 29, etc.)? If yes, briefly describe sampling train and pitot tube leak check procedures:	<input type="checkbox"/> Yes	<input checked="" type="checkbox"/> No
--	------------------------------	--

EPA METHOD 19 IN LIEU OF EPA METHODS 1-4

c. Are you proposing to utilize EPA Method 19 in lieu of EPA Methods 1-4? If yes, explain why you believe this proposal is justified:	<input checked="" type="checkbox"/> Yes	<input type="checkbox"/> No
---	---	-----------------------------

Method 19 with use of a calibrated fuel meter and current fuel gas analysis.

PLEASE NOTE – EPA Method 19 may be utilized in lieu of EPA Methods 1-4, subject to the approval of the Department. If you are proposing to utilize EPA Method 19 in lieu of EPA Methods 1-4, you MUST include a recent fuel gas heating value analysis as well as a recent fuel flow meter calibration certificate, preferably conducted on the day of the test, but no earlier than three months prior to the test date. If the analyses have been conducted prior to the test date, you MUST append the certificates to the protocol. If conducted on the day of the test, you MUST append the certificates to the final test report.

VIII. ATTACHMENTS (as needed to support proposed test; check all that apply)	
NOTIFICATION/PROTOCOL ATTACHMENTS	
<input type="checkbox"/>	Road Map Indicating Directions from Nearest New Mexico Town to Facility
<input type="checkbox"/>	Schematic of process being tested showing emission points, sampling sites and stack cross-section
<input type="checkbox"/>	Copy of proposed test methods (except for those promulgated test methods found in 40 CFR 51, 60, 61 and 63)
<input type="checkbox"/>	Fuel Heating Value Analysis
<input type="checkbox"/>	Fuel Flow Meter Calibration Certificate
<input type="checkbox"/>	Other: _____
<input type="checkbox"/>	Other: _____
TEST REPORT ATTACHMENTS	
<input type="checkbox"/>	Section 2. Tables of Results
<input type="checkbox"/>	Supporting Documents (Specify)
Retain Report Section 3 - Test Procedures, Data, Calculations, Appendices – 2 years NSR permits, 5 years TV	

IX. CERTIFICATION		
<p>This document has been prepared under my supervision and is accurate and complete to the best of my knowledge. I understand that acceptance of this protocol does not waive the requirements of any permit or regulation. I understand that any procedural errors or omissions are the sole responsibility of the permit holder.</p>		
Signature: 	Print Name and Title: Jon E. Fields, Director-Field Compliance	Date: <i>2-18-2014</i>
Responsible Official for Title V? <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No (R.O signature not required for routine periodic testing)		

2015 COMPLIANCE

TEST REPORT

ON

EXHAUST EMISSIONS

FROM TWO

SOLAR CENTAUR T-4702

CENTRIFUGAL INTERNAL COMBUSTION ENGINE

AT THE

SOUTH CARLSBAD COMPRESSOR STATION

NEAR

LOVING, NEW MEXICO

PREPARED FOR

ENTERPRISE FIELD SERVICES

JANUARY 2015

PROJECT NUMBER 1187

STATE OF NEW MEXICO ENVIRONMENT DEPARTMENT
AIR QUALITY BUREAU PERMIT NUMBER 0220-M8-R1

PREPARED BY

COMPLIANCE SERVICES & TESTING



P.O. Box 94191-87199
7108 Washington St. NE
Suite A
Albuquerque, NM 87109
(505) 681-4909 Phone
www.comptesting.com

February 5, 2015

Dina Babinski
Enterprise Field Services
PO Box 4324
Houston, TX 77210

RE: Annual testing at the South Carlsbad Compressor Station.

Mrs. Babinski:

On January 20, 2015 CST performed annual emissions testing at the South Carlsbad Compressor Station to satisfy the requirements of the New Mexico Environment Department Air Quality Bureau Permit Number 0220-M8-R1. The unit is identified as follows:

Engine Information		
Unit Number	1	2
Engine Make	Solar	
Engine Model	Centaur T-4702	
Serial Number	OHD10-C-7915	OHE12-C-7057
Rated Horsepower	3609	
Rated Speed	15000	

The testing followed procedures found in the NMED “SOP for Using Portable Analyzers in Performance Testing.” Mass emission rates were calculated using EPA Method 19 (combustion stoichiometry). The rates in terms of pounds per hour and tons per year were calculated using the oxygen F-factor (DSCF_{ex}/MMBtu), the fuel consumption rate (SCFH), the fuel higher heating value (Btu/SCF), and the pollutant concentration. Fuel consumption was monitored from a fuel meter. Three twenty-minute test runs were performed. The attached data sheet gives a detailed summary of the results of this test. Quality assurance data sheets are also attached. Strip charts are on file, and are available if needed.

Respectfully,



Jeremy Cahn
Compliance Services and Testing

Summary of Results

South Carlsbad Compressor Station, Unit #1

Company: Enterprise Field Services
Location: South Carlsbad Compressor Station
Source: Solar Centaur 40-T4702 SN: OHD10C7915
Engine Site Rating: 3609 Hp @ 15000 RPM
Technician: SR

Test Run Number	1	2	3	
EU Number	1	1	1	
Date	1/20/15	1/20/15	1/20/15	
Start Time	9:51	10:16	10:41	
Stop Time	10:11	10:36	11:01	
Engine/Compressor Operation				
Gas Producer Speed (%)	95.0	95.4	95.4	
Power Turbine Speed (%)	82.0	82.6	82.5	
Engine Horsepower (Hp)	3429	3443	3443	
Engine Compressor Discharge, PCD (psig)	101	102	102	
Fuel Valve Output (%)	58.7	59.3	59.4	
Suction Pressure (psig)	404	404	404	
Discharge Pressure (psig)	689	691	690	
Suction Temperature (°F)	130	132	133	
Discharge Temperature (°F)	167	172	173	
Air Inlet Temperature (T1) (°F)	61	64	65	
Average Exhaust Temperature (T5) (°F)	1104	1121	1126	
Compressor Throughput (MMCFD)	78.9	78.9	78.9	
Fuel Data				
Measured Fuel Consumption (MSCFD)	788.7	788.7	788.7	
Measured Fuel Consumption (SCFH)	32861	32861	32861	
O2 F-Factor (DSCF/MMBtu, HHV basis)	8697	8697	8697	
Fuel Heating Value (Btu/SCF, HHV)	1148	1148	1148	
BHp Specific Fuel Rate (Btu/Hp-hr, HHV basis)	9871	9871	9871	
Ambient Conditions				
Pressure Altitude (MSL)	3010	3010	3010	
Atmospheric Pressure ("Hg)	26.83	26.83	26.83	
Dry Bulb Temperature (°F)	60.3	62.4	63.7	
Wet Bulb Temperature (°F)	47.3	48.2	49.1	
Humidity (lb/lb air)	0.0046	0.0046	0.0048	
Measured Exhaust Emissions (Corrected)				Average
NOx (ppmv)	82.52	83.57	83.12	83.07
CO (ppmv)	16.45	15.56	15.41	15.81
O2 (vol %)	16.52	16.52	16.53	16.52
CO2 (vol %)	2.52	2.54	2.57	2.54
Moisture Content (% - from Method 4)	4.64	4.64	4.64	4.64
Fo (Natural Gas)	1.74	1.73	1.70	1.72
Exhaust Flow Rates (EPA Method 19 - Fuel Based)				
Dry SCFH (dry basis, calc. from Fuel Consumption)	1.57E+06	1.57E+06	1.57E+06	1.57E+06
Calculated Mass Emission Rates (EPA Methods 1-4)				
NOx (lbs/hr) {Permit Limit = 27.0}	15.43	15.63	15.58	15.55
CO (lbs/hr) {Permit Limit = 7.4}	1.87	1.77	1.76	1.80
NOx (tons/yr) {Permit Limit = 118.3}	67.60	68.46	68.24	68.10
CO (tons/yr) {Permit Limit = 32.5}	8.20	7.76	7.70	7.89

Summary of Results

South Carlsbad Compressor Station, Unit #2

Company: Enterprise Field Services
Location: South Carlsbad Compressor Station
Source: Solar Centaur 40-T4702 SN: OHE12C7057
Engine Site Rating: 3609 Hp @ 15000 RPM
Technician: SR

Test Run Number	1	2	3	
EU Number	2	2	2	
Date	1/20/15	1/20/15	1/20/15	
Start Time	8:29	8:54	9:19	
Stop Time	8:49	9:14	9:39	
Engine/Compressor Operation				
Gas Producer Speed (%)	94.8	94.7	94.8	
Power Turbine Speed (%)	84.1	83.7	83.6	
Engine Horsepower (Hp)	3421	3418	3421	
Engine Compressor Discharge, PCD (psig)	105	105	104	
Fuel Valve Output (%)	37.8	37.7	38.1	
Suction Pressure (psig)	237	238	238	
Discharge Pressure (psig)	416	414	413	
Suction Temperature (°F)	49	49	49	
Discharge Temperature (°F)	129	127	127	
Air Inlet Temperature (T1) (°F)	52	53	54	
Average Exhaust Temperature (T5) (°F)	1054	1056	1059	
Compressor Throughput (MMCFD)	80.6	80.6	80.6	
Fuel Data				
Measured Fuel Consumption (MSCFD)	788.7	788.7	788.7	
Measured Fuel Consumption (SCFH)	32861	32861	32861	
O2 F-Factor (DSCF/MMBtu, HHV basis)	8697	8697	8697	
Fuel Heating Value (Btu/SCF, HHV)	1148	1148	1148	
BHp Specific Fuel Rate (Btu/Hp-hr, HHV basis)	9871	9871	9871	
Ambient Conditions				
Pressure Altitude (MSL)	3000	3000	3010	
Atmospheric Pressure ("Hg)	26.84	26.84	26.83	
Dry Bulb Temperature (°F)	47.7	48.7	51.1	
Wet Bulb Temperature (°F)	40.6	41.7	43	
Humidity (lb/lb air)	0.0043	0.0045	0.0046	
Measured Exhaust Emissions (Corrected)				Average
NOx (ppmv)	81.07	83.33	84.59	83.00
CO (ppmv)	10.51	9.99	10.61	10.37
O2 (vol %)	16.71	16.71	16.73	16.72
CO2 (vol %)	2.41	2.41	2.45	2.43
Moisture Content (% - from Method 4)	4.64	4.64	4.64	4.64
Fo (Natural Gas)	1.74	1.74	1.70	1.72
Exhaust Flow Rates (EPA Method 19 - Fuel Based)				
Dry SCFH (dry basis, calc. from Fuel Consumption)	1.64E+06	1.64E+06	1.64E+06	1.64E+06
Calculated Mass Emission Rates (EPA Methods 1-4)				
NOx (lbs/hr) {Permit Limit = 27.0}	15.85	16.29	16.62	16.25
CO (lbs/hr) {Permit Limit = 7.4}	1.25	1.19	1.27	1.24
NOx (tons/yr) {Permit Limit = 118.3}	69.42	71.36	72.79	71.19
CO (tons/yr) {Permit Limit = 32.5}	5.48	5.21	5.56	5.41

Quality Assurance Report - Sample System #1
Converter Efficiency Test, Interference Test, Response Time
and Bias Test, Mass Flow Controller Check, Pre and Post Leak Checks

NOx Converter Efficiency Check							
<i>Method:</i> 7E Section 8.2.4							
<i>Frequency:</i> Before each field test							
<i>Criteria:</i> Equal to or greater than 90% conversion efficiency							
Test Date: 1/19/15		Technician: SR					
NO2 / N2 Balance				Results			
Certified Value				48.9 ppmv			
Observed Value				47.1 ppmv			
Converter Efficiency				96%			
Interference Response Checks							
<i>Method:</i> 7E Section 8.2.7							
<i>Frequency:</i> Prior to initial use in the field or after major alteration or modification							
<i>Criteria:</i> Sum of responses < 2.5 % of calibration span							
Test Date: 1/20/15		Technician: SR					
Interference Test Gases		Analyzer Response (ppmv or % as applicable)					
Type Gas	Conc.	NOx (ppmv)	CO (ppmv)	SO2 (ppmv)	THC (ppmv)	O2 (%)	CO2 (%)
NOx in N2	50 ppm	---	N/A	---	---	0.00	0.01
CO in N2	50 ppm	N/A	---	---	---	0.00	0.01
O2 in N2	10.0%	0.23	-0.21	---	---	---	N/A
CO2 in N2	10.0%	0.23	-0.21	---	---	N/A	---
THC in air	---	---	---	---	---	---	---
Gas Dilution Calibration - 2 Mass Flow Controllers							
<i>Method:</i> 205							
<i>Frequency:</i> Before each field test.							
<i>Criteria:</i> Produce Calibration gases whose measured values are within ± 2% of predicted values.							
Manufacturer: EnviroNics		Cal Gas: NOx		Test Date: 1/19/15			
Model Number: Series 4040		Serial Number: 4456		Technician: SR			
MFC 3				MFC 2			
	Direct Inject	Diluted Conc.	Diluted Conc.	Direct Inject	Diluted Conc.	Diluted Conc.	
Certified Value:	242	2957	2957	242	2957	2957	
Ex. Dilution:	---	242	150	---	750	900	
Injection 1	246	239	147	245	743	896	
Injection 2	248	238	148	244	746	894	
Injection 3	246	237	147	245	742	897	
Average	246.67	238.00	147.33	244.67	743.67	895.67	
% Variation	0.47%	0.42%	0.39%	0.24%	0.28%	0.17%	
% Difference	-1.91%	1.67%	1.79%	-1.10%	0.85%	0.48%	
Sample System Bias & Response Time Check							
<i>Method:</i> 7E Section 8.2.5-6							
<i>Frequency:</i> Before sampling begins							
<i>Criteria:</i> 5% of calibration span							
<i>Criteria:</i> Note the longer of the two times as the response time							
Test Date: 1/20/15		Technician: SR					
Sample System Bias Check							
Introduction Technique	NOx (ppmv)	CO (ppmv)	SO2 (ppmv)	THC (ppmv)	O2 (%)	CO2 (%)	
Direct Zero Input	0	0.0			0.0	0.0	
Bias Input	-1	-0.3			0.0	0.1	
Zero Bias	-0.4%	-0.3%			0.0%	1.0%	
Direct Span Input	49.6	50.1			10.0	10.0	
Bias Input	50.6	50.4			10.0	10.1	
Span Bias	1.1%	0.3%			0.0%	1.0%	
Sample System Response Time							
Parameter	NOx (ppmv)	CO (ppmv)	SO2 (ppmv)	THC (ppmv)	O2 (%)	CO2 (%)	
Upscale Response	35	45			50	55	
Downscale Response	40	50			55	55	
Purge Time	110 seconds						
Sample System Leak Check							
<i>Frequency:</i> Daily or whenever the sample system is moved or disassembled (CST SOP)							
<i>Criteria:</i> Less than one inch decrease in pressure in one minute (CST SOP)							
<u>Test Date</u>							
1/20/15		<u>Vacuum Initial:</u>	0.0 inches	/ minute at	13 inches Hg		
		<u>Vacuum Final:</u>	0.0 inches	/ minute at	13 inches Hg		

Quality Assurance Worksheet

Instrument Calibration and Drift Correction

Company: Enterprise Field Services
Location: South Carlsbad Compressor Station
Source: Solar Centaur 40-T4702 SN: OHD10C7915
Engine Site Rating: 3609 Hp @ 15000 RPM
Test Date: Tuesday, January 20, 15

UNIT NUMBER 1					TEST RUN 1					TEST RUN 2					TEST RUN 3				
GAS LEVELS PER METHOD	CALIBRATION GAS CONCENTRATIONS		INITIAL CALIBRATION & LINEARITY CHECK		Start Run	ZERO and SPAN CALIBRATION CHECK				Start Run	ZERO and SPAN CALIBRATION CHECK				Start Run	ZERO and SPAN CALIBRATION CHECK			
	Certified Concentration	Target (% Span)	Analyzer Response	Calibration Error < 2%	Stop Run	Initial Response	Final Response	Drift < 3%	Bias < 5%	Stop Run	Initial Response	Final Response	Drift < 3%	Bias < 5%	Stop Run	Initial Response	Final Response	Drift < 3%	Bias < 5%
NOx					Avg. ppmv					Avg. ppmv					Avg. ppmv				
Zero	0.0 ppmv	0.0	-0.4 ppmv	-0.4%	82.00	-1.6 ppmv	-0.6 ppmv	1.1%	0.6%	83.00	-0.6 ppmv	-0.7 ppmv	0.1%	0.7%	83.00	-0.7 ppmv	0.8 ppmv	1.6%	0.8%
Mid	50.0 ppmv	52.6	49.6 ppmv	-0.4%	82.52					83.57					83.12				
High	95.0 ppmv	100.0	95.8 ppmv	0.8%	Cal. Span	49.3 ppmv	49.2 ppmv	0.2%	0.8%	Cal. Span	49.2 ppmv	49.6 ppmv	0.8%	0.4%	Cal. Span	49.6 ppmv	50.3 ppmv	1.4%	0.3%
Analyzer Range = 100 ppmv			Span = 95.0		95					95					95				
CO					Avg. ppmv					Avg. ppmv					Avg. ppmv				
Zero	0.0 ppmv	0.0	0 ppmv	0.0%	15.00	-1.5 ppmv	-1.8 ppmv	0.3%	1.9%	14.00	-1.8 ppmv	-1.5 ppmv	0.3%	1.6%	14.00	-1.5 ppmv	-1.5 ppmv	0.0%	1.6%
Mid	50.0 ppmv	52.6	50.1 ppmv	0.1%	16.45					15.56					15.41				
High	95.0 ppmv	100.0	95.6 ppmv	0.6%	Cal. Span	49.3 ppmv	48.6 ppmv	1.4%	1.5%	Cal. Span	48.6 ppmv	48.7 ppmv	0.2%	1.4%	Cal. Span	48.7 ppmv	48.9 ppmv	0.4%	1.2%
Analyzer Range = 100 ppmv			Span = 95.0		95					95					95				
O2					Avg. %					Avg. %					Avg. %				
Zero	0.0%	0.0	0.0%	0.0%	16.52	0.0%	0.0%	0.0%	0.0%	16.52	0.0%	0.0%	0.0%	0.0%	16.53	0.0%	0.0%	0.0%	0.0%
Mid	10.0%	47.6	10.0%	0.0%	16.52					16.52					16.53				
High	21.0%	100.0	21.0%	0.0%	Cal. Span	10.0%	10.0%	0.0%	0.0%	Cal. Span	10.0%	10.0%	0.0%	0.0%	Cal. Span	10.0%	10.0%	0.0%	0.0%
Analyzer Range = 22.0%			Span = 21.0		21					21					21				
CO2					Avg. %					Avg. %					Avg. %				
Zero	0.0%	0.0	0.0%	0.0%	2.79	0.3%	0.3%	0.0%	3.0%	2.81	0.3%	0.3%	0.0%	3.0%	2.83	0.3%	0.3%	0.0%	3.0%
Mid	5.0%	50.0	5.2%	2.0%	2.52					2.54					2.57				
High	10.0%	100.0	10.0%	0.0%	Cal. Span	10.2%	10.2%	0.0%	2.0%	Cal. Span	10.2%	10.2%	0.0%	2.0%	Cal. Span	10.2%	10.1%	1.0%	1.0%
Analyzer Range = 11.0%			Span = 10.0		10					10					10				

Quality Assurance Worksheet

Instrument Calibration and Drift Correction

Company: Enterprise Field Services
Location: South Carlsbad Compressor Station
Source: Solar Centaur 40-T4702 SN: OHE12C7057
Engine Site Rating: 3609 Hp @ 15000 RPM
Test Date: Tuesday, January 20, 15

UNIT NUMBER 2					TEST RUN 1					TEST RUN 2					TEST RUN 3				
GAS LEVELS PER METHOD	CALIBRATION GAS CONCENTRATIONS		INITIAL CALIBRATION & LINEARITY CHECK		Start Run	ZERO and SPAN CALIBRATION CHECK				Start Run	ZERO and SPAN CALIBRATION CHECK				Start Run	ZERO and SPAN CALIBRATION CHECK			
	Certified Concentration	Target (% Span)	Analyzer Response	Calibration Error < 2%	8:29	Initial Response	Final Response	Drift < 3%	Bias < 5%	8:54	Initial Response	Final Response	Drift < 3%	Bias < 5%	9:19	Initial Response	Final Response	Drift < 3%	Bias < 5%
NOx					Avg. ppmv					Avg. ppmv					Avg. ppmv				
Zero	0.0 ppmv	0.0	-0.4 ppmv	-0.4%	82.00	-0.8 ppmv	-0.9 ppmv	0.1%	0.9%	83.00	-0.9 ppmv	-0.6 ppmv	0.3%	0.6%	84.00	-0.6 ppmv	-1.6 ppmv	1.1%	1.7%
Mid	50.0 ppmv	52.6	49.6 ppmv	-0.4%	81.07	50.6 ppmv	49.9 ppmv	1.4%	0.1%	83.33	49.9 ppmv	49.1 ppmv	1.6%	0.9%	84.59	49.1 ppmv	49.3 ppmv	0.4%	0.7%
High	95.0 ppmv	100.0	95.8 ppmv	0.8%	Cal. Span					Cal. Span					Cal. Span				
Analyzer Range = 100 ppmv			Span = 95.0		95					95					95				
CO					Avg. ppmv					Avg. ppmv					Avg. ppmv				
Zero	0.0 ppmv	0.0	0 ppmv	0.0%	10.00	-0.3 ppmv	-1.1 ppmv	0.8%	1.2%	9.00	-1.1 ppmv	-1.3 ppmv	0.2%	1.4%	9.40	-1.3 ppmv	-1.5 ppmv	0.2%	1.6%
Mid	50.0 ppmv	52.6	50.1 ppmv	0.1%	Corr. ppmv					Corr. ppmv					Corr. ppmv				
High	95.0 ppmv	100.0	95.6 ppmv	0.6%	10.51	50.4 ppmv	50.0 ppmv	0.8%	0.0%	9.99	50.0 ppmv	49.7 ppmv	0.6%	0.3%	10.61	49.7 ppmv	49.3 ppmv	0.8%	0.7%
Analyzer Range = 100 ppmv			Span = 95.0		Cal. Span					Cal. Span					Cal. Span				
					95					95					95				
O2					Avg. %					Avg. %					Avg. %				
Zero	0.0%	0.0	0.0%	0.0%	16.71	0.0%	0.0%	0.0%	0.0%	16.71	0.0%	0.0%	0.0%	0.0%	16.73	0.0%	0.0%	0.0%	0.0%
Mid	10.0%	47.6	10.0%	0.0%	Corr. %					Corr. %					Corr. %				
High	21.0%	100.0	21.0%	0.0%	16.71	10.0%	10.0%	0.0%	0.0%	16.71	10.0%	10.0%	0.0%	0.0%	16.73	10.0%	10.0%	0.0%	0.0%
Analyzer Range = 22.0%			Span = 21.0		Cal. Span					Cal. Span					Cal. Span				
					21					21					21				
CO2					Avg. %					Avg. %					Avg. %				
Zero	0.0%	0.0	0.0%	0.0%	2.56	0.1%	0.2%	1.0%	2.0%	2.65	0.2%	0.3%	1.0%	3.0%	2.73	0.3%	0.3%	0.0%	3.0%
Mid	5.0%	50.0	5.2%	2.0%	Corr. %					Corr. %					Corr. %				
High	10.0%	100.0	10.0%	0.0%	2.41	10.1%	10.2%	1.0%	2.0%	2.41	10.2%	10.2%	0.0%	2.0%	2.45	10.2%	10.2%	0.0%	2.0%
Analyzer Range = 11.0%			Span = 10.0		Cal. Span					Cal. Span					Cal. Span				
					10					10					10				

Gas Quality Report - Detail

Prod date: 01/2015 thru 02/2015

Report Date: 01/29/2015 14:58

Request: Meter: 16961

Meter Number: 16961 01

Production month: 01/2015

Sample Type: Hourly Chrom

Gas Quality Source: 1696101

SO CARLSBAD TURB FUEL

Gpa Version: 2145-09

Date/Time	Btu	Gravity	Co2	C1		C2		C3		IC4		NC4		IC5		NC5		NeoC5		Carbon Monoxide
				N2	Methane	Ethane	Propane	Butane	Butane	Pntn	Pntn									
01 07:00	1136.1	0.6631	0.0010	2.8563	83.6352	8.7108	3.5983	0.3324	0.6696	0.0887	0.0739	0.0000	0.0338	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
02 07:00	1131.9	0.6623	0.0000	3.0501	83.5036	8.7941	3.5326	0.3155	0.6255	0.0818	0.0673	0.0000	0.0295	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
03 07:00	1144.6	0.6699	0.0005	2.9842	82.6472	9.2540	3.8378	0.3545	0.7048	0.0964	0.0819	0.0000	0.0387	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
04 07:00	1147.0	0.6710	0.0007	2.9347	82.6754	9.1282	3.9093	0.3730	0.7572	0.1013	0.0839	0.0000	0.0363	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
05 07:00	1137.1	0.6715	0.1691	2.7855	83.1382	8.9093	3.7070	0.3526	0.7133	0.1012	0.0859	0.0000	0.0379	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
06 07:00	1145.9	0.6678	0.0001	2.7198	83.0808	9.1256	3.7825	0.3571	0.7129	0.0977	0.0831	0.0000	0.0404	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
07 07:00	1143.7	0.6680	0.0000	2.8722	82.8418	9.3017	3.7556	0.3455	0.6793	0.0918	0.0759	0.0000	0.0362	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
08 07:00	1145.5	0.6701	0.0000	2.9626	82.5880	9.3120	3.8738	0.3561	0.7034	0.0917	0.0759	0.0000	0.0365	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
09 07:00	1150.8	0.6718	0.0007	2.7886	82.4602	9.4905	3.9595	0.3627	0.7254	0.0950	0.0789	0.0000	0.0385	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
10 07:00	1149.5	0.6724	0.0007	2.9273	82.3088	9.4880	3.9740	0.3640	0.7325	0.0924	0.0766	0.0000	0.0357	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
11 07:00	1149.0	0.6750	0.1284	2.9126	82.0913	9.5789	3.9495	0.3732	0.7553	0.0963	0.0788	0.0000	0.0357	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
12 07:00	1144.4	0.6781	0.4807	3.0357	81.5945	9.6236	3.9708	0.3597	0.7277	0.0938	0.0772	0.0000	0.0363	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
13 07:00	1147.9	0.6768	0.2911	2.9947	81.6992	9.7065	4.0125	0.3615	0.7320	0.0929	0.0757	0.0000	0.0339	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
14 07:00	1148.3	0.6770	0.3226	2.9553	81.6891	9.7146	4.0303	0.3580	0.7251	0.0927	0.0766	0.0000	0.0357	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
15 07:00	1144.8	0.6764	0.3676	3.0413	81.7852	9.5369	3.9848	0.3579	0.7222	0.0938	0.0766	0.0000	0.0337	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
16 07:00	1146.7	0.6761	0.3418	2.9360	81.8389	9.6164	3.9933	0.3578	0.7135	0.0924	0.0757	0.0000	0.0342	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
17 07:00	1147.6	0.6768	0.3276	2.9696	81.6666	9.7419	4.0432	0.3548	0.6993	0.0905	0.0742	0.0000	0.0323	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
18 07:00	1147.0	0.6753	0.3235	2.8677	81.9681	9.5738	4.0126	0.3541	0.6991	0.0917	0.0759	0.0000	0.0335	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
19 07:00	1145.5	0.6751	0.3013	2.9786	81.8912	9.6138	3.9732	0.3507	0.6937	0.0898	0.0743	0.0000	0.0334	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
20 07:00	1145.7	0.6746	0.3163	2.8955	81.9762	9.6418	3.9297	0.3515	0.6939	0.0885	0.0729	0.0000	0.0337	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
21 07:00	1146.7	0.6732	0.2871	2.7472	82.3412	9.4139	3.9329	0.3620	0.7168	0.0908	0.0745	0.0000	0.0336	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
22 07:00	1144.0	0.6735	0.3042	2.9108	82.1824	9.4289	3.9351	0.3518	0.6991	0.0857	0.0706	0.0000	0.0314	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
23 07:00	1143.6	0.6744	0.3243	2.9862	82.0282	9.4913	3.9240	0.3490	0.7001	0.0882	0.0746	0.0000	0.0341	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
24 07:00	1143.9	0.6717	0.2962	2.7363	82.5729	9.2893	3.8392	0.3561	0.7125	0.0889	0.0742	0.0000	0.0344	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
25 07:00	1139.9	0.6721	0.2491	2.9321	82.5773	9.1645	3.8167	0.3529	0.7087	0.0894	0.0743	0.0000	0.0350	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
26 07:00	1140.0	0.6725	0.4310	2.8624	82.4850	9.1263	3.8349	0.3525	0.7065	0.0909	0.0749	0.0000	0.0356	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
27 07:00	1142.3	0.6734	0.3694	2.9020	82.3455	9.1996	3.8931	0.3606	0.7254	0.0942	0.0771	0.0000	0.0331	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
28 07:00	1141.0	0.6745	0.4682	2.9293	82.1582	9.3125	3.8447	0.3595	0.7259	0.0930	0.0760	0.0000	0.0327	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Average:	1144.3	0.6727	0.2180	2.9098	82.3489	9.3675	3.8875	0.3549	0.7100	0.0922	0.0763	0.0000	0.0348	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
AVG GPM:						2.5046	1.0707	0.1161	0.2238	0.0337	0.0277	0.0000	0.0156					TOTAL AVG GPM:	3.9921	

Fuel Gas Analysis

Diluent F Factors, Higher Heating Value Calculation, Predicted Fo, Fuel VOC Content

Company: Enterprise

Sample ID: South Carlsbad Turbine Fuel

Time: N/A

Date: 1/20/15

CALCULATION OF DENSITY AND HEATING VALUE @ 68°F and 29.92 in Hg

Component	% Volume	Molecular Wt.	Density (lb/ft ³)	% volume x Density	weight %	Component Gross Btu/lb	Weight Fract. Btu	Gross Htng. Val. (Btu/SCF)	Volume Fract. Btu
Hydrogen		2.016	0.0052	0.0000	0.0000	61100	0.00	325.0	0.000
Oxygen		32.000	0.0831	0.0000	0.0000	0	0.00	0.0	0.000
Nitrogen	2.8955	28.016	0.0731	0.00212	4.1617	0	0.00	0.0	0.000
CO ₂	0.3163	44.010	0.1149	0.00036	0.7149	0	0.00	0.0	0.000
CO		28.010	0.0727	0.00000	0.0000	4347	0.00	322.0	0.000
Methane	81.9762	16.041	0.0417	0.03414	67.1515	23879	16035.10	1013.0	830.419
Ethane	9.6418	30.067	0.0789	0.00760	14.9562	22320	3338.23	1792.0	172.781
Ethylene		28.051	0.0733	0.00000	0.0000	21644	0.00	1614.0	0.000
Propane	3.9297	44.092	0.1175	0.00462	9.0790	21661	1966.61	2590.0	101.779
propylene		42.077	0.1090	0.00000	0.0000	21041	0.00	2336.0	0.000
Isobutane	0.3515	58.118	0.1554	0.00055	1.0742	21308	228.90	3363.0	11.821
n-butane	0.6939	58.118	0.1554	0.00108	2.1207	21257	450.79	3370.0	23.384
Isobutene		56.102	0.1454	0.00000	0.0000	20840	0.00	3068.0	0.000
Isopentane	0.0885	72.144	0.1870	0.00017	0.3255	21091	68.66	4008.0	3.547
n-pentane	0.0729	72.144	0.1870	0.00014	0.2681	21052	56.45	4016.0	2.928
n-hexane + H ₂ S	0.0337	86.169	0.2234	0.00008	0.1480	20940	31.00	4762.0	1.605
		34.076	0.0895	0.00000	0.0000	7100	0.00	647.0	0.000
Totals	100.00	731.25	1.91	0.0508	100.00	Gross Heating Value			
Total Density:		0.0508	Specific Gravity:		0.665	Btu/lb:	22176	Btu/SCF:	1148

CALCULATION OF F FACTORS

Component	Mol. Wt.	C Factor	H Factor	% volume	Fract. Wt.	Weight Percents				
						Carbon	Hydrogen	Nitrogen	Oxygen	Sulfur
Hydrogen	2.016	0.0000	1.0000	0.0000	0.0000		0.0000			
Oxygen	32.000	0.0000	0.0000	0.0000	0.0000				0.0000	
Nitrogen	28.016	0.0000	0.0000	2.8955	81.1203			4.1632		
CO ₂	44.010	0.2723	0.0000	0.3163	13.9204	0.1945			0.5194	
CO	28.010	0.4259	0.0000	0.0000	0.0000	0.0000			0.0000	
Methane	16.041	0.7500	0.2500	81.9762	1314.9802	50.6153	16.8718			
Ethane	30.067	0.8000	0.2000	9.6418	289.9000	11.9025	2.9756			
Ethylene	28.051	0.8571	0.1429	0.0000	0.0000	0.0000	0.0000			
Propane	44.092	0.8182	0.1818	3.9297	173.2683	7.2756	1.6168			
Propene	42.077	0.8571	0.1429	0.0000	0.0000	0.0000	0.0000			
Isobutane	58.118	0.8276	0.1725	0.3515	20.4285	0.8677	0.1808			
n-butane	58.118	0.8276	0.1725	0.6939	40.3281	1.7129	0.3570			
Isobutene	56.102	0.8571	0.1429	0.0000	0.0000	0.0000	0.0000			
Isopentane	72.144	0.8333	0.1667	0.0885	6.3847	0.2731	0.0546			
n-pentane	72.144	0.8333	0.1667	0.0729	5.2593	0.2249	0.0450			
n-hexane	86.169	0.8372	0.1628	0.0337	2.9039	0.1248	0.0243			
H ₂ S	34.076	0.0000	0.0587	0.0000	0.0000	0.0000	0.0000			0.0000
Totals	731.25	9.80	2.96	100.00	1948.494	73.191	22.126	4.163	0.519	0.000

CALCULATED VALUES

O₂ F Factor (dry)	8697	DSCF of Exhaust/MMBtu of Fuel Burned @ 0% excess air
O₂ F Factor (wet)	10623	SCF of Exhaust/MMBtu of Fuel Burned @ 0% excess air
Moisture F Factor	1926	SCF of Water/MMBtu of Fuel Burned @ 0% excess air
Combust. Moisture	18.13	Volume % water in flue gas @ 0% excess air
CO₂ F Factor	1059	DSCF of CO ₂ /MMBtu of Fuel Burned @ 0% excess air
Carbon Dioxide	12.18	Volume % CO ₂ in flue gas @ 0% O ₂
Predicted Fo Factor	1.72	EPA Method 3b Fo value
Fuel VOC %	29.17%	Non-methane
Fuel VOC %	13.56%	Non-methane, non-ethane

Nolan, Shiver

From: Nolan, Shiver
Sent: Tuesday, February 09, 2016 8:30 AM
To: 'stacktest.aqb@state.nm.us'
Cc: Ferguson, Dina; Polk, Alena (ampolk@eprod.com)
Subject: South Carlsbad Eng 1 & 2 Solar Centaur T-4702
Attachments: 201601 South Carlsbad Annual Test Report.pdf - Adobe Acrobat Pro.pdf

Attached are the two stack test referenced above. Contact Information has been included on the NMED forms.

Shiver Nolan
Sr. Compliance Administrator



New Mexico Environment Department
 525 Camino de los Marquez, Suite 1
 Santa Fe, NM 87505
 Phone (505) 476-4300 Fax (505) 476-4375



Version 1/1/2010

NMED USE ONLY	
DTS	
TEMPO	

UNIVERSAL STACK TEST NOTIFICATION, PROTOCOL AND REPORT FORM

NMED USE ONLY	
Staff	
Admin	

Submit to: Stacktest.aqb@state.nm.us

I. DATABASE HEADER INFORMATION (drop down menus in bold)			
a. AI# 218	Test Report		Periodic Test (Portable Analyzer)
d. Company Name: Enterprise Field Services LLC		e. Facility Name: South Carlsbad Compressor Station	
f. Emission Unit Numbers: 1, 2		g. Emission Unit Description (boiler, Waukesha 7042, etc) Turbines, Solar Centaur T-4702	
h. Reports - Tracking Number from notification response: CMT		i. Proposed Test Date: Week of 1/18/16	j. Actual test date: 1/20/16
k. Reason for test (name permit requirement, NSPS, MACT, consent decree, etc. Indicate here is this notification is a revised test date only) Annual performance test of existing turbines pursuant to NSR condition A205C.			

II. GENERAL COMPANY AND FACILITY INFORMATION					
a. Company Address: PO Box 4324			k.. Facility Address: Roberson Road, Eddy County		
b. City: Houston	c. State: TX	d. Zip: 77210	l. City: Loving	m. State: NM	n. Zip: 88526
e. Environmental Contact: Alena Polk		f. Title: Sr. Env. Engineer		o. Facility Contact: Thomas Green	
g. Phone Number: 575-706-4926		h. Cell Number: 575-706-4926		p. Title: Area Supervisor	
i. Email Address: ampolk@eprod.com		q. Phone Number: 575-885-7235		r. Cell Number: 575-708-0015	
j. Title V Permit Number: P-130-M1R2		s. Email Address: tdgreen@eprod.com		t. NSR Permit Number: NSR 220M9	
u. Detailed driving directions from nearest New Mexico town: From Loving, UN285 north to Roberson Road west, Roberson Road west to station.					

III. TESTING FIRM		
a. Company: Compliance Services and Testing		g. Contact: Chris Spencer
b. Address 1: 7108 Washington NE Ste. A		h. Title: Director
c. Address 2: PO Box 94191-87199		i. Office Phone: 505-681-4909
		j. Cell Phone: 505-681-4909

d. City: Albuquerque	e. State: NM	f. Zip: 87109	k. Email Address: cspencer@comptestesting.com
--------------------------------	------------------------	-------------------------	---

IV. EMISSION UNIT			STACK PARAMETERS	
a. Emission Unit Number: 1 and 2	b. Make & Model Number Solar Centaur T-4702		m. Velocity (ft/sec):	177
c. Serial Number: See section g.	d. Permitted Capacity: 3609 hp		n. Temperature (°C):	486
e. Exceptions: Explain if test is late, rescheduled, related to an enforcement action:			o. Stack Diameter, D (in.):	NA
			p. Distance to Stack Bends or Obstructions:	
			Upstream, Distance A (in.):	NA
g. Emission Unit Description and brief process name or description: Turbine 1 SN: OHD10C795 Turbine 2 SN: OHE12C7057 Natural gas-fired turbines for natural gas compression.			Downstream, Distance B (in.):	NA
h. Installation Date:	i. Startup Date:	k. Date Reached Max. Capacity:		
l. Control Equipment Description as listed in permit (model, ser. # etc. if applicable): NA			<p>Attach an explanation or drawing to explain any difficult or unusual stack geometry or parameters.</p>	

V. POLLUTANTS AND PROPOSED TEST METHODS			
Pollutant or Parameter:	Proposed Test Methods (Deviations from approved methods require supporting documentation and prior authorization)		Deviation to Test Method Requested
<input checked="" type="checkbox"/>	Portable Analyzer Methods for NOx, CO, SO₂		<input type="checkbox"/>
<input type="checkbox"/>	NOx	EPA Method 7E	<input type="checkbox"/>
<input type="checkbox"/>	CO	EPA Method 10	<input type="checkbox"/>
<input type="checkbox"/>	SO ₂	EPA Method 6	<input type="checkbox"/>
<input type="checkbox"/>	VOCs	(Specify)	<input type="checkbox"/>
<input type="checkbox"/>	HAPs	(Specify)	<input type="checkbox"/>
<input type="checkbox"/>	PM (TSP)	EPA Method 5	<input type="checkbox"/>
<input type="checkbox"/>	PM ₁₀	EPA Method 201	<input type="checkbox"/>
<input type="checkbox"/>	PM _{2.5}	(Specify)	<input type="checkbox"/>
<input type="checkbox"/>	Opacity	EPA Method 9	<input type="checkbox"/>
<input type="checkbox"/>	Visual E.	EPA Method 22	<input type="checkbox"/>
<input type="checkbox"/>	Stack Flow	EPA Methods 1 - 3	<input type="checkbox"/>
<input type="checkbox"/>	Moisture	EPA Method 4	<input type="checkbox"/>
<input checked="" type="checkbox"/>	Other	(Specify) EPA Method 19	<input type="checkbox"/>
<input type="checkbox"/>	Other	(Specify)	<input type="checkbox"/>

List Specific VOC's and HAP's:

VI. PROPOSED TEST RUN AND TEST LOAD INFORMATION

a. Number of Test Runs: 3	b. Run Duration 20 min	c. Required by (regulation or permit number): NSR 220 M9	d. Specific Condition or Section: A205C
-------------------------------------	----------------------------------	--	---

PLEASE NOTE – Default run duration is 60 minutes, unless otherwise specified by an applicable regulation.

e. Expected Load: >90%	f. Percent of Permitted Capacity: >90%	g. Is this an opacity test? Yes <input type="checkbox"/> No <input checked="" type="checkbox"/>	h. If yes, no. of observation pts.:
-------------------------------------	---	--	-------------------------------------

i. If expected load during test is less than 90% of capacity, explain:

NOTE – Failure to test at 90-100% of permitted load will limit unit operation to 110% of tested load until a new initial compliance test is conducted.

PLANT OR UNIT OPERATING PARAMETERS TO BE MONITORED

j. List and explain the plant operating parameters that will be monitored and applicable permit conditions or regulatory standards.

Fuel usage, compressor operating parameters, turbine operating parameters.

VII. ADDITIONAL DETAILS (where applicable)

RATA and INSTRUMENTAL ANALYZER CALIBRATION PROCEDURES

a. Do any of the methods you are proposing utilize instrumental analyzers (i.e.; EPA Methods 3A, 6C, 7E, 10, 18, 25/25A, 320 etc.)? If yes, briefly describe analyzer calibration procedures and/or calibration standard procedures. Enter the highest pollutant concentration expected and the proposed concentrations of calibration gases.	<input checked="" type="checkbox"/> Yes	<input type="checkbox"/> No
---	---	-----------------------------

As described in the methods.

SAMPLING TRAIN LEAK CHECK PROCEDURES

b. Do any of the methods you are proposing utilize the EPA Method 5 sampling train (i.e.; EPA Methods 1-4, 5, 17, 26/26A, 29, etc.)? If yes, briefly describe sampling train and pitot tube leak check procedures:	<input type="checkbox"/> Yes	<input checked="" type="checkbox"/> No
--	------------------------------	--

EPA METHOD 19 IN LIEU OF EPA METHODS 1-4

c. Are you proposing to utilize EPA Method 19 in lieu of EPA Methods 1-4? If yes, explain why you believe this proposal is justified:	<input checked="" type="checkbox"/> Yes	<input type="checkbox"/> No
---	---	-----------------------------

Method 19 with use of a calibrated fuel meter and current fuel gas analysis.

PLEASE NOTE – EPA Method 19 may be utilized in lieu of EPA Methods 1-4, subject to the approval of the Department. If you are proposing to utilize EPA Method 19 in lieu of EPA Methods 1-4, you MUST include a recent fuel gas heating value analysis as well as a recent fuel flow meter calibration certificate, preferably conducted on the day of the test, but no earlier than three months prior to the test date. If the analyses have been conducted prior to the test date, you MUST append the certificates to the protocol. If conducted on the day of the test, you MUST append the certificates to the final test report.

VIII. ATTACHMENTS (as needed to support proposed test; check all that apply)

NOTIFICATION/PROTOCOL ATTACHMENTS

- Road Map Indicating Directions from Nearest New Mexico Town to Facility
- Schematic of process being tested showing emission points, sampling sites and stack cross-section
- Copy of proposed test methods (except for those promulgated test methods found in 40 CFR 51, 60, 61 and 63)
- Fuel Heating Value Analysis
- Fuel Flow Meter Calibration Certificate
- Other: _____
- Other: _____

TEST REPORT ATTACHMENTS

- Section 2. Tables of Results**
- Supporting Documents (Specify)**

Retain Report Section 3 - Test Procedures, Data, Calculations, Appendices – 2 years NSR permits, 5 years TV

IX. CERTIFICATION

This document has been prepared under my supervision and is accurate and complete to the best of my knowledge. I understand that acceptance of this protocol does not waive the requirements of any permit or regulation. I understand that any procedural errors or omissions are the sole responsibility of the permit holder.

Signature: 	Print Name and Title: Jon E. Fields - Director, Field Environmental	Date: <i>2-9-2016</i>
--	---	--------------------------

Responsible Official for Title V? Yes No (R.O signature not required for routine periodic testing)

**2016 COMPLIANCE
TEST REPORT**

ON
EXHAUST EMISSIONS

FROM TWO
**SOLAR CENTAUR T-4702
CENTRIFUGAL INTERNAL COMBUSTION ENGINE**

AT THE
SOUTH CARLSBAD COMPRESSOR STATION

NEAR
LOVING, NEW MEXICO

PREPARED FOR
ENTERPRISE FIELD SERVICES

PROJECT NUMBER 1377

STATE OF NEW MEXICO ENVIRONMENT DEPARTMENT
AIR QUALITY BUREAU PERMIT NUMBER 0220-M8-R1

PREPARED BY
COMPLIANCE SERVICES & TESTING



P.O. Box 94191-87199
7108 Washington St. NE
Suite A
Albuquerque, NM 87109
(505) 681-4909 Phone
www.comptesting.com

February 3, 2016

Dina Ferguson
Enterprise Field Services
PO Box 4324
Houston, TX 77210

RE: Annual testing at the South Carlsbad Compressor Station.

Mrs. Ferguson:

On January 20, 2016 CST performed annual emissions testing at the South Carlsbad Compressor Station to satisfy the requirements of the New Mexico Environment Department Air Quality Bureau Permit Number 0220-M8-R1. The unit is identified as follows:

Engine Information		
Unit Number	1	2
Engine Make	Solar	
Engine Model	Centaur T-4702	
Serial Number	OHD10-C-7915	OHE12-C-7057
Rated Horsepower	3609	
Rated Speed	15000	

The testing followed procedures found in the NMED "ASTM D 6522-00 SOP". The mass emission rates were determined using EPA Method 19 (combustion stoichiometry). The rates in terms of pounds per hour and tons per year were calculated using the oxygen F-factor (DSCFex/MMBtu), the fuel consumption rate (SCFH), the fuel higher heating value (Btu/SCF), and the pollutant concentration. Fuel consumption was monitored from a fuel meter. The attached data sheet gives a detailed summary of the results of this test. Quality assurance data sheets are also attached.

Respectfully,



Jeremy Cahn
Compliance Services and Testing

Summary of Results

South Carlsbad Compressor Station, Unit #1

Company: Enterprise Field Services
Location: South Carlsbad Compressor Station
Source: Solar Centaur 40-T4702 SN: OHD10C7915
Engine Site Rating: 3609 Hp @ 15000 RPM
Technician: JC,FC
Sample System #: 1

<i>Test Run Number</i>	<i>1</i>	<i>2</i>	<i>3</i>	
Emissions Unit				
Date	1/20/16	1/20/16	1/20/16	
Start Time	7:53	8:18	8:43	
Stop Time	8:13	8:38	9:03	
Engine/Compressor Operation				
Turbine Load (%)	94.7	95.0	95.2	
Gas Producer Speed (%)	94.7	95.0	95.2	
Power Turbine Speed (%)	82.7	83.0	83.1	
Engine Horsepower (Hp)	3418	3429	3436	
Engine Compressor Discharge, PCD (psig)	104	105	105	
Fuel Valve Output (%)	59.9	61.3	60	
Suction Pressure (psig)	419	423	424	
Discharge Pressure (psig)	659	712	712	
Suction Temperature (°F)	98	98	99	
Discharge Temperature (°F)	123	124	177	
Air Inlet Temperature (T1) (°F)	40.2	39	43.2	
Average Exhaust Temperature (T5) (°F)	1080	1047	1090	
Compressor Throughput (MCFD)	72	72	72	
Fuel Data				
Measured Fuel Consumption (MSCFD)	788	788	788	
Calculated Fuel Consumption (SCFH)	17905	17905	17905	
O2 F-Factor (DSCF/MMBtu, HHV basis)	8696	8696	8696	
Fuel Heating Value (Btu/SCF, HHV)	1155	1155	1155	
BHp Specific Fuel Rate (Btu/Hp-hr, HHV basis)	198790	196897	6017	
Ambient Conditions				
Pressure Altitude (MSL)	3090	3090	3090	
Atmospheric Pressure ("Hg)	26.75	26.75	26.75	
Dry Bulb Temperature (°F)	41.7	42.1	44.8	
Wet Bulb Temperature (°F)	35.8	35.1	38.5	
Humidity (lb/lb air)	0.0035	0.0032	0.0040	
Measured Exhaust Emissions (Corrected)				Average
NOx (ppmv)	67.41	71.88	69.61	69.63
CO (ppmv)	13.62	8.90	8.16	10.23
O2 (vol %)	16.77	16.79	16.79	16.78
CO2 (vol %)	2.46	2.54	2.53	2.51
Fo (Natural Gas)	1.67	1.62	1.62	1.64
Exhaust Flow Rates (EPA Method 19 - Fuel Based)				
Dry SCFH (dry basis, calc. from Fuel Consumption)	910,503	914,424	913,092	912,673
Calculated Mass Emission Rates (EPA Method 19)				
NOx (lbs/hr) {Permit Limit = 27.0}	7.33	7.85	7.59	7.59
CO (lbs/hr) {Permit Limit = 7.4}	0.90	0.59	0.54	0.68
NOx (tons/yr) {Permit Limit = 118.3}	32.11	34.38	33.25	33.25
CO (tons/yr) {Permit Limit = 32.5}	3.95	2.59	2.37	2.97

Summary of Results

South Carlsbad Compressor Station, Unit #2

Company: Enterprise Field Services
Location: South Carlsbad Compressor Station
Source: Solar Centaur 40-T4702 SN: OHE12C7057
Engine Site Rating: 3609 Hp @ 15000 RPM
Technician: JC,FC
Sample System #: 2

<i>Test Run Number</i>	<i>1</i>	<i>2</i>	<i>3</i>	
Emissions Unit	2	2	2	
Date	1/20/16	1/20/16	1/20/16	
Start Time	7:53	8:18	8:43	
Stop Time	8:13	8:38	9:03	
Engine/Compressor Operation				
Turbine Load (%)	94.7	95.2	95.3	
Gas Producer Speed (%)	94.7	95.2	95.3	
Power Turbine Speed (%)	85.2	85.7	86.1	
Engine Horsepower (Hp)	3418	3436	3439	
Engine Compressor Discharge, PCD (psig)	109	110	110.0	
Fuel Valve Output (%)	39.2	39.5	39.6	
Suction Pressure (psig)	237	236	236	
Discharge Pressure (psig)	427	428	427	
Suction Temperature (°F)	41	42	42	
Discharge Temperature (°F)	123	124	125	
Air Inlet Temperature (T1) (°F)	40.2	39	41	
Average Exhaust Temperature (T5) (°F)	1080	1047	1056	
Compressor Throughput (MCFD)	72	72	72	
Fuel Data				
Measured Fuel Consumption (MSCFD)	788	788	788	
Calculated Fuel Consumption (SCFH)	17905	17905	17905	
O2 F-Factor (DSCF/MMBtu, HHV basis)	8696	8696	8696	
Fuel Heating Value (Btu/SCF, HHV)	1155	1155	1155	
BHp Specific Fuel Rate (Btu/Hp-hr, HHV basis)	6049	6017	6011	
Ambient Conditions				
Pressure Altitude (MSL)	3090	3090	3090	
Atmospheric Pressure ("Hg)	26.75	26.75	26.75	
Dry Bulb Temperature (°F)	41.7	42.1	44.8	
Wet Bulb Temperature (°F)	35.8	35.1	38.5	
Humidity (lb/lb air)	0.0035	0.0032	0.0040	
Measured Exhaust Emissions (Corrected)				Average
NOx (ppmv)	71.70	75.09	73.53	73.44
CO (ppmv)	14.67	12.03	9.98	12.23
O2 (vol %)	17.59	17.45	17.30	17.45
CO2 (vol %)	2.00	2.12	2.18	2.10
Fo (Natural Gas)	1.66	1.63	1.65	1.65
Exhaust Flow Rates (EPA Method 19 - Fuel Based)				
Dry SCFH (dry basis, calc. from Fuel Consumption)	1,134,456	1,087,659	1,044,190	1,088,769
Calculated Mass Emission Rates (EPA Method 19)				
NOx (lbs/hr) {Permit Limit = 27.0}	9.71	9.75	9.17	9.55
CO (lbs/hr) {Permit Limit = 7.4}	1.21	0.95	0.76	0.97
NOx (tons/yr) {Permit Limit = 118.3}	42.55	42.72	40.17	41.81
CO (tons/yr) {Permit Limit = 32.5}	5.30	4.17	3.32	4.26

Quality Assurance Report - Sample System #1
Converter Efficiency Test, Interference Test, Response Time
and Bias Test, Mass Flow Controller Check, Pre and Post Leak Checks

NOx Converter Efficiency Check

Method: 7E Section 8.2.4

Frequency: Before each field test

Criteria: Equal to or greater than 90% conversion efficiency

Test Date: 1/20/16 Technician: JC

NO2	Results
Certified Value	48.9 ppmv
Observed Value	49.0 ppmv
Converter Efficiency	100%

Interference Response Checks

Method: 7E Section 8.2.7

Frequency: Prior to initial use in the field or after major alteration or modification

Criteria: Sum of responses < 2.5 % of calibration span

Test Date: 1/20/16 Technician: JC

Interference Test Gases		Analyzer Response (ppmv or % as applicable)					
<i>Type Gas</i>	<i>Conc.</i>	<i>NOx (ppmv)</i>	<i>CO (ppmv)</i>	<i>SO2 (ppmv)</i>	<i>THC (ppmv)</i>	<i>O2 (%)</i>	<i>CO2 (%)</i>
NOx in N2	44.5 ppm	---	N/A	---	---	0.00	-0.03
CO in N2	44.8 ppm	N/A	---	---	---	0.00	-0.03
O2 in N2	9.6%	0.05	-0.24	---	---	---	N/A
CO2 in N2	6.5%	0.05	-0.24	---	---	N/A	---
THC in air	---	---	---	---	---	---	---

Sample System Bias & Response Time Check

Method: 7E Section 8.2.5-6

Frequency: Before sampling begins

Criteria: 5% of calibration span

Criteria: Note the longer of the two times as the response time

Test Date: 1/20/16 Technician: JC

Sample System Bias Check

Introduction Technique	NOx (ppmv)	CO (ppmv)	SO2 (ppmv)	THC (ppmv)	O2 (%)	CO2 (%)
Direct Zero Input	0.0	0.0			0.0	0.0
Bias Input	0.0	0.0			0.0	0.0
Zero Bias	0.0%	0.0%			0.0%	0.0%
Direct Span Input	44.6	44.8			9.6	6.5
Bias Input	43.7	44.8			9.6	6.5
Span Bias	-1.1%	0.0%			0.0%	0.0%

Sample System Response Time

Parameter	NOx (ppmv)	CO (ppmv)	SO2 (ppmv)	THC (ppmv)	O2 (%)	CO2 (%)
Upscale Response	40	35			50	50
Downscale Response	40	35			45	55
Purge Time	110 seconds					

Sample System Leak Check

Frequency: Daily or whenever the sample system is moved or disassembled (CST SOP)

Criteria: Less than one inch decrease in pressure in one minute (CST SOP)

Test Date

1/20/16 Vacuum Initial: 0.0 inches / minute at 14 inches Hg
 Vacuum Final: 0.0 inches / minute at 14 inches Hg

Quality Assurance Worksheet

Instrument Calibration and Drift Correction

Company: Enterprise Field Services

Location: South Carlsbad Compressor Station

Source: Solar Centaur 40-T4702 SN: OHD10C7915

Engine Site Rating: 3609 Hp @ 15000 RPM

Test Date: Wednesday, January 20, 2016

Sample System #: 1

UNIT NUMBER 1					TEST RUN 1					TEST RUN 2					TEST RUN 3				
GAS LEVELS PER METHOD	CALIBRATION GAS CONCENTRATIONS		INITIAL CALIBRATION & LINEARITY CHECK		Start Run	ZERO and SPAN CALIBRATION CHECK				Start Run	ZERO and SPAN CALIBRATION CHECK				Start Run	ZERO and SPAN CALIBRATION CHECK			
	Certified Concentration	Target (% Span)	Analyzer Response	Calibration Error < 2%	7:53	Initial Response	Final Response	Drift < 3%	Bias < 5%	8:18	Initial Response	Final Response	Drift < 3%	Bias < 5%	8:43	Initial Response	Final Response	Drift < 3%	Bias < 5%
NOx					Avg. ppmv	0.0 ppmv	0.0 ppmv	0.0%	0.0%	Avg. ppmv	0.0 ppmv	0.0 ppmv	0.0%	0.0%	Avg. ppmv	0.0 ppmv	1.0 ppmv	1.2%	1.2%
Zero	0.0 ppmv	0.0	0.0 ppmv	0.0%	66.35	43.7 ppmv	43.9 ppmv	0.4%	0.7%	71.15	43.9 ppmv	44.2 ppmv	0.7%	0.4%	69.49	44.2 ppmv	45.0 ppmv	1.8%	0.6%
Mid	44.5 ppmv	52.0	44.6 ppmv	0.1%	Corr. ppmv					Corr. ppmv					Corr. ppmv				
High	85.5 ppmv	100.0	85.7 ppmv	0.2%	Cal. Span					Cal. Span					Cal. Span				
Analyzer Range = 100 ppmv			Span = 85.5		85.5					85.5					85.5				
CO					Avg. ppmv	0.0 ppmv	0.0 ppmv	0.0%	0.0%	Avg. ppmv	0.0 ppmv	0.0 ppmv	0.0%	0.0%	Avg. ppmv	0.0 ppmv	-1.0 ppmv	1.2%	1.2%
Zero	0.0 ppmv	0.0	0.0 ppmv	0.0%	13.52	44.8 ppmv	44.1 ppmv	1.6%	0.8%	8.80	44.1 ppmv	44.5 ppmv	0.9%	0.4%	7.71	44.5 ppmv	44.7 ppmv	0.4%	0.1%
Mid	44.8 ppmv	53.7	44.8 ppmv	0.0%	Corr. ppmv					Corr. ppmv					Corr. ppmv				
High	83.4 ppmv	100.0	83.0 ppmv	-0.5%	Cal. Span					Cal. Span					Cal. Span				
Analyzer Range = 100 ppmv			Span = 83.4		83.4					83.4					83.4				
O2					Avg. %	0.0%	0.0%	0.0%	0.0%	Avg. %	0.0%	0.0%	0.0%	0.0%	Avg. %	0.0%	0.0%	0.0%	0.0%
Zero	0.0%	0.0	0.0%	0.0%	16.77	9.6%	9.6%	0.0%	0.0%	16.79	9.6%	9.6%	0.0%	0.0%	16.79	9.6%	9.6%	0.0%	0.0%
Mid	9.6%	45.5	9.6%	0.0%	Corr. %					Corr. %					Corr. %				
High	21.1%	100.0	21.0%	-0.5%	Cal. Span					Cal. Span					Cal. Span				
Analyzer Range = 22.0%			Span = 21.1		21.1					21.1					21.1				
CO2					Avg. %	0.0%	0.0%	0.0%	0.0%	Avg. %	0.0%	0.0%	0.0%	0.0%	Avg. %	0.0%	0.0%	0.0%	0.0%
Zero	0.0%	0.0	0.0%	0.0%	2.46	6.5%	6.5%	0.0%	0.0%	2.54	6.5%	6.5%	0.0%	0.0%	2.53	6.5%	6.5%	0.0%	0.0%
Mid	4.0%	61.5	4.1%	1.5%	Corr. %					Corr. %					Corr. %				
High	6.5%	100.0	6.5%	0.0%	Cal. Span					Cal. Span					Cal. Span				
Analyzer Range = 7.0%			Span = 6.5		6.5					6.5					6.5				

Quality Assurance Report - Sample System #2
Converter Efficiency Test, Interference Test, Response Time
and Bias Test, Mass Flow Controller Check, Pre and Post Leak Checks

NOx Converter Efficiency Check

Method: 7E Section 8.2.4

Frequency: Before each field test

Criteria: Equal to or greater than 90% conversion efficiency

Test Date: 1/20/16 Technician: JC

NO2	Results
Certified Value	48.9 ppmv
Observed Value	49.4 ppmv
Converter Efficiency	101%

Interference Response Checks

Method: 7E Section 8.2.7

Frequency: Prior to initial use in the field or after major alteration or modification

Criteria: Sum of responses < 2.5 % of calibration span

Test Date: 1/20/16 Technician: JC

Interference Test Gases		Analyzer Response (ppmv or % as applicable)					
Type Gas	Conc.	NOx (ppmv)	CO (ppmv)	SO2 (ppmv)	THC (ppmv)	O2 (%)	CO2 (%)
NOx in N2	44.5 ppm	---	N/A	---	---	0.01	0.02
CO in N2	44.8 ppm	N/A	---	---	---	0.01	0.02
O2 in N2	9.6%	0.37	-0.12	---	---	---	N/A
CO2 in N2	6.5%	0.37	-0.12	---	---	N/A	---
THC in air	---	---	---	---	---	---	---

Sample System Bias & Response Time Check

Method: 7E Section 8.2.5-6

Frequency: Before sampling begins

Criteria: 5% of calibration span

Criteria: Note the longer of the two times as the response time

Test Date: 1/20/16 Technician: JC

Sample System Bias Check

Introduction Technique	NOx (ppmv)	CO (ppmv)	SO2 (ppmv)	THC (ppmv)	O2 (%)	CO2 (%)
Direct Zero Input	0.0	0.0			0.0	0.0
Bias Input	0.0	0.0			0.0	0.0
Zero Bias	0.0%	0.0%			0.0%	0.0%
Direct Span Input	44.1	45.0			9.6	6.5
Bias Input	43.6	43.9			9.6	6.5
Span Bias	-0.6%	-1.3%			0.0%	0.0%

Sample System Response Time

Parameter	NOx (ppmv)	CO (ppmv)	SO2 (ppmv)	THC (ppmv)	O2 (%)	CO2 (%)
Upscale Response	35	40			45	55
Downscale Response	35	40			45	55
Purge Time	110 seconds					

Sample System Leak Check

Frequency: Daily or whenever the sample system is moved or disassembled (CST SOP)

Criteria: Less than one inch decrease in pressure in one minute (CST SOP)

Test Date

1/20/16 Vacuum Initial: 0.0 inches / minute at 16 inches Hg
 Vacuum Final: 0.0 inches / minute at 16 inches Hg

Quality Assurance Worksheet

Instrument Calibration and Drift Correction

Company: Enterprise Field Services

Location: South Carlsbad Compressor Station

Source: Solar Centaur 40-T4702 SN: OHE12C7057

Engine Site Rating: 3609 Hp @ 15000 RPM

Test Date: Wednesday, January 20, 2016

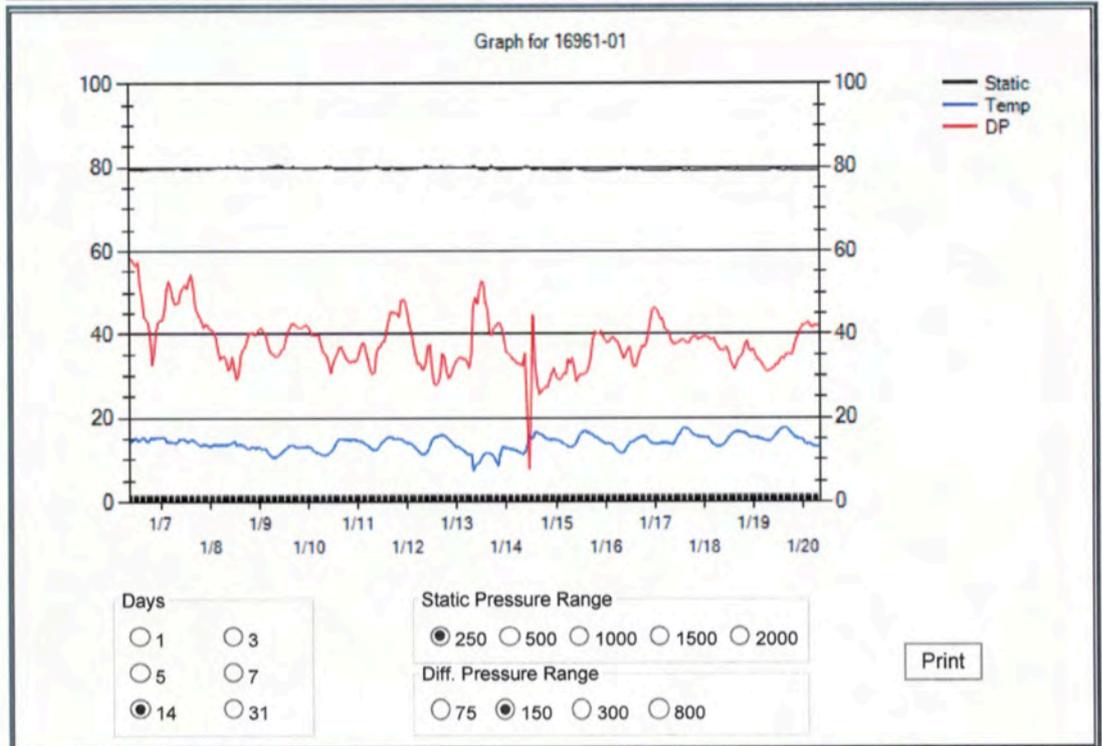
Sample System #: 2

UNIT NUMBER 2					TEST RUN 1					TEST RUN 2					TEST RUN 3				
GAS LEVELS PER METHOD	CALIBRATION GAS CONCENTRATIONS		INITIAL CALIBRATION & LINEARITY CHECK		Start Run	ZERO and SPAN CALIBRATION CHECK				Start Run	ZERO and SPAN CALIBRATION CHECK				Start Run	ZERO and SPAN CALIBRATION CHECK			
	Certified Concentration	Target (% Span)	Analyzer Response	Calibration Error < 2%	Stop Run	Initial Response	Final Response	Drift < 3%	Bias < 5%	Stop Run	Initial Response	Final Response	Drift < 3%	Bias < 5%	Stop Run	Initial Response	Final Response	Drift < 3%	Bias < 5%
NOx					Avg. ppmv					Avg. ppmv					Avg. ppmv				
Zero	0.0 ppmv	0.0	0.0 ppmv	0.0%	70.49	0.0 ppmv	0.0 ppmv	0.0%	0.0%	73.73	0.0 ppmv	1.0 ppmv	1.2%	1.2%	72.22	1.0 ppmv	1.0 ppmv	0.0%	1.2%
Mid	44.5 ppmv	52.0	44.1 ppmv	-0.5%	Corr. ppmv					75.09	43.9 ppmv	43.9 ppmv	0.0%	0.7%	73.53	43.9 ppmv	44.3 ppmv	0.9%	0.2%
High	85.5 ppmv	100.0	84.8 ppmv	-0.8%	Cal. Span	43.6 ppmv	43.9 ppmv	0.7%	0.7%	Cal. Span	43.9 ppmv	43.9 ppmv	0.0%	0.7%	Cal. Span	43.9 ppmv	44.3 ppmv	0.9%	0.2%
Analyzer Range = 100 ppmv			Span = 85.5		85.5					85.5					85.5				
CO					Avg. ppmv					Avg. ppmv					Avg. ppmv				
Zero	0.0 ppmv	0.0	0.0 ppmv	0.0%	14.43	0.0 ppmv	0.0 ppmv	0.0%	0.0%	11.91	0.0 ppmv	0.0 ppmv	0.0%	0.0%	9.57	0.0 ppmv	-1.0 ppmv	1.2%	1.2%
Mid	44.8 ppmv	53.7	45.0 ppmv	0.2%	Corr. ppmv					12.03	44.2 ppmv	44.5 ppmv	0.7%	0.4%	9.98	44.5 ppmv	44.9 ppmv	0.9%	0.1%
High	83.4 ppmv	100.0	83.9 ppmv	0.6%	Cal. Span	43.9 ppmv	44.2 ppmv	0.7%	0.7%	Cal. Span	44.2 ppmv	44.5 ppmv	0.7%	0.4%	Cal. Span	44.5 ppmv	44.9 ppmv	0.9%	0.1%
Analyzer Range = 100 ppmv			Span = 83.4		83.4					83.4					83.4				
O2					Avg. %					Avg. %					Avg. %				
Zero	0.0%	0.0	0.0%	0.0%	17.59	0.0%	0.0%	0.0%	0.0%	17.45	0.0%	0.0%	0.0%	0.0%	17.39	0.0%	0.0%	0.0%	0.0%
Mid	9.6%	45.5	9.6%	0.0%	Corr. %					17.45	9.6%	9.6%	0.0%	0.0%	17.30	9.6%	9.7%	1.0%	0.5%
High	21.1%	100.0	21.1%	0.0%	Cal. Span	9.6%	9.6%	0.0%	0.0%	Cal. Span	9.6%	9.6%	0.0%	0.0%	Cal. Span	9.6%	9.7%	1.0%	0.5%
Analyzer Range = 22.0%			Span = 21.1		21.1					21.1					21.1				
CO2					Avg. %					Avg. %					Avg. %				
Zero	0.0%	0.0	0.0%	0.0%	2.00	0.0%	0.0%	0.0%	0.0%	2.10	0.0%	0.0%	0.0%	0.0%	2.14	0.0%	0.0%	0.0%	0.0%
Mid	4.0%	61.5	4.0%	0.0%	Corr. %					2.12					2.18				
High	6.5%	100.0	6.5%	0.0%	Cal. Span	6.5%	6.5%	0.0%	0.0%	Cal. Span	6.5%	6.4%	1.5%	1.5%	Cal. Span	6.4%	6.4%	0.0%	1.5%
Analyzer Range = 7.0%			Span = 6.5		6.5					6.5					6.5				



Snap-shot	General Information For 16961-01				Measurement
	WellName SO CARLSBAD TURB FUEL				
1/20/2016 8:00:00	PIN 1696101				1/20/2016 8:00:00
Static 198.13	Group Number 5	Local Address 57			Static 198.13
DP 63.18	System GTTAES2	Scada Server AESTX2			DP 63.18
Temp 33.28	DAL / OrgID 661 / EPF	Team C2			Temp 33.28
Volume 1,575.00	Model 827	Load File AESORIF			Volume 65.63
Yest MCF 1,463.88	Business Party 0	Operator Name ENTERPRISE FIELD SERVICES LLC			Flow Time 60.00
Forecast 1,575.17	Pipe: 4.03 Plate: 1.5 B/R: 0.37				
	Meter Type Non WATT Meter				
	S/T/R 12 / 23S / 27E				

M
E
N
U



Fuel Gas Analysis, Gas Fuel O2 F-Factor, Moisture Content, Fuel VOC%, and Heating Value Calculation

Company: Enterprise Field Services

Sample ID: South Carlsbad

Time: N/A

Date: 2/2/16

CALCULATION OF DENSITY AND HEATING VALUE @ 68°F and 29.92 in Hg									
Component	% Volume	Molecular Wt.	Density (lb/ft3)	% volume x Density	weight %	Component Gross Btu/lb	Weight Fract. Btu	Gross Htng. Val. (Btu/SCF)	Volume Fract. Btu
Hydrogen		2.016	0.0052	0.0000	0.0000	61100	0.00	325.0	0.000
Oxygen		32.000	0.0831	0.0000	0.0000	0	0.00	0.0	0.000
Nitrogen	2.9591	28.016	0.0731	0.00216	4.2554	0	0.00	0.0	0.000
CO2	0.0001	44.010	0.1149	0.0000	0.0002	0	0.00	0.0	0.000
CO		28.010	0.0727	0.0000	0.0000	4347	0.00	322.0	0.000
Methane	81.9206	16.041	0.0417	0.03412	67.1414	23879	16032.70	1013.0	829.856
Ethane	9.7466	30.067	0.0789	0.00769	15.1268	22320	3376.30	1792.0	174.659
Ethylene		28.051	0.0733	0.0000	0.0000	21644	0.00	1614.0	0.000
Propane	4.1308	44.092	0.1175	0.00485	9.5487	21661	2068.34	2590.0	106.988
propylene		42.077	0.1090	0.0000	0.0000	21041	0.00	2336.0	0.000
Isobutane	0.3608	58.118	0.1554	0.00056	1.1032	21308	235.08	3363.0	12.134
n-butane	0.7075	58.118	0.1554	0.00110	2.1634	21257	459.87	3370.0	23.843
Isobutene		56.102	0.1454	0.0000	0.0000	20840	0.00	3068.0	0.000
Isopentane	0.0822	72.144	0.1870	0.00015	0.3025	21091	63.80	4008.0	3.295
n-pentane	0.0662	72.144	0.1870	0.00012	0.2436	21052	51.29	4016.0	2.659
n-hexane + H2S	0.0261	86.169	0.2234	0.00006	0.1147	20940	24.02	4762.0	1.243
		34.076	0.0895	0.0000	0.0000	7100	0.00	647.0	0.000
Totals	100.00	731.25	1.91	0.0508	100.00	Gross Heating Value			
Average Density:	0.0508	Specific Gravity:		0.664	Btu/lb:	22311	Btu/SCF:	1155	

CALCULATION OF F FACTORS										
Component	Mol. Wt.	C Factor	H Factor	% volume	Fract. Wt.	Weight Percents				
						Carbon	Hydrogen	Nitrogen	Oxygen	Sulfur
Hydrogen	2.016	0.0000	1.0000	0.0000	0.0000		0.0000			
Oxygen	32.000	0.0000	0.0000	0.0000	0.0000				0.0000	
Nitrogen	28.016	0.0000	0.0000	2.9591	82.9021			4.2575		
CO2	44.010	0.2723	0.0000	0.0001	0.0044	0.0001			0.0002	
CO	28.010	0.4259	0.0000	0.0000	0.0000	0.0000			0.0000	
Methane	16.041	0.7500	0.2500	81.9206	1314.0883	50.6139	16.8713			
Ethane	30.067	0.8000	0.2000	9.7466	293.0510	12.0397	3.0099			
Ethylene	28.051	0.8571	0.1429	0.0000	0.0000	0.0000	0.0000			
Propane	44.092	0.8182	0.1818	4.1308	182.1352	7.6529	1.7007			
Propene	42.077	0.8571	0.1429	0.0000	0.0000	0.0000	0.0000			
Isobutane	58.118	0.8276	0.1725	0.3608	20.9690	0.8912	0.1857			
n-butane	58.118	0.8276	0.1725	0.7075	41.1185	1.7476	0.3642			
Isobutene	56.102	0.8571	0.1429	0.0000	0.0000	0.0000	0.0000			
Isopentane	72.144	0.8333	0.1667	0.0822	5.9302	0.2538	0.0508			
n-pentane	72.144	0.8333	0.1667	0.0662	4.7759	0.2044	0.0409			
n-hexane	86.169	0.8372	0.1628	0.0261	2.2490	0.0967	0.0188			
H2S	34.076	0.0000	0.0587	0.0000	0.0000	0.0000	0.0000			0.0000
Totals	731.25	9.80	2.96	100.00	1947.224	73.500	22.242	4.257	0.000	0.000

CALCULATED VALUES		
O2 F Factor (dry)	8696	DSCF of Exhaust/MMBtu of Fuel Burned @ 0% excess air
O2 F Factor (wet)	10620	SCF of Exhaust/MMBtu of Fuel Burned @ 0% excess air
Moisture F Factor	1924	SCF of Water/MMBtu of Fuel Burned @ 0% excess air
Combust. Moisture	18.12	Volume % water in flue gas @ 0% excess air
CO2 F Factor	1057	DSCF of CO2/MMBtu of Fuel Burned @ 0% excess air
Carbon Dioxide	12.16	Volume % CO2 in flue gas @ 0% O2
Predicted Fo Factor	1.72	EPA Method 3b Fo value
Fuel VOC %	29.63%	Non-methane
Fuel VOC %	13.94%	Non-methane, non-ethane

Example Calculations

Drift Corrected Emission Concentrations		
<i>Formula</i>		
$C_{GAS} = (C - C_0) \times \frac{C_{MA}}{C_M - C_0}$ (eq. 7E-5)		
<i>All Calculations Refer to Test Run 1 Unit #1</i>		
C_{NOx} =	Raw Concentration of NO _x	= 66.35 ppmv
C_0 =	Avg. of Initial and Final Zero Checks	= 0.00 ppmv
C_M =	Avg. of Initial and Final Span Checks	= 43.80 ppmv
C_{MA} =	Certified Concentration of Span Gas	= 44.50 ppmv
C_{NOx} =	$(66.35 - 0.00) \times \frac{44.50}{(43.80 - 0.00)}$	= 67.41 ppmv
C_{CO} =	Raw Concentration of CO	= 13.52 ppmv
C_0 =	Avg. of Initial and Final Zero Checks	= 0.00 ppmv
C_M =	Avg. of Initial and Final Span Checks	= 44.45 ppmv
C_{MA} =	Certified Concentration of Span Gas	= 44.80 ppmv
C_{CO} =	$(13.52 - 0.00) \times \frac{44.80}{(44.45 - 0.00)}$	= 13.62 ppmv
C_{O2} =	Raw Concentration of O ₂	= 16.77%
C_0 =	Avg. of initial and final zero bias checks	= 0.00%
C_M =	Avg. of initial and final span bias checks	= 9.60%
C_{MA} =	Actual concentration of span gas	= 9.60%
C_{O2} =	$(16.77 - 0.00) \times \frac{9.60}{(9.60 - 0.00)}$	= 16.77%
C_{CO2} =	Raw Concentration of CO ₂	= 2.46%
C_0 =	Avg. of initial and final zero bias checks	= 0.00%
C_M =	Avg. of initial and final span bias checks	= 6.50%
C_{MA} =	Actual concentration of span gas	= 6.50%
C_{CO2} =	$(2.46 - 0.00) \times \frac{6.50}{(6.50 - 0.00)}$	= 2.46%
<i>F_o Calculation to Verify O₂ / CO₂ Measurements (Eq. 3b-1)</i>		
C_{O2} =	Corrected Concentration of O ₂	= 16.77%
C_{CO2} =	Corrected Concentration of CO ₂	= 2.46%
Th. Fo =	Theoretical Fo from FGA	= 1.72
Fo =	$\frac{(20.9 - O_2\%)}{CO_2\%}$	
Fo =	$\frac{(20.9 - 16.77)}{2.46}$	= 1.67

Example Calculations

Mass Emission Rates via EPA Method 19					
<i>Measured Data and Constants from Test Run 1 Unit #1</i>					
C _{NOx} =	Corrected Concentration of NO _x	=	67.41	ppmv	
C _{CO} =	Corrected Concentration of CO	=	13.62	ppmv	
Horsepower =	Observed Horsepower	=	3418	Hp	
Q _{S M19} =	Measured Stack Flow Rate	=	910,503	SCF/H Dry	
lb / mole =	EPA STP for Ideal Gas	=	385.15	SCF	
lbs / hr to tpy =	Mass Conversion Factor	=	4.38	hrs-tons / lbs-yr	
C _F =	PPMV Normalization	=	1.00E-06	1 / ppmv	
MW _{NOx} =	Molecular Weight of NO _x	=	46	lb / lb-mol	
MW _{CO} =	Molecular Weight of CO	=	28	lb / lb-mol	
<i>Stack Gas Flow Rate via Method 19 (eq. 19-1)</i>					
Q _F =	Fuel Flow (Measured)	=	17905	SCF/H	
F _{BTU} =	Fuel Higher Heating Value	=	1155	Btu/SCF	
F _{O2} =	O ₂ F-Factor	=	8696	DSCF/MMBtu	
C _{O2} =	Corrected Concentration of O ₂	=	16.77	%	
Q _{S M19} =	$Q_F \times F_{BTU} \times F_{O2} \times 10^6 \times \frac{20.9}{(20.9 - \%O_2)}$				DSCF/H
Q _{S M19} =	17905	x	1155	x	8696
		x	5.06	x	1.00E-06
Q_{S M19} =	910,503		DSCF/H		
<i>Adjust Measured Concentrations to 15% O₂ (Eq. 60.335)</i>					
C_{x @ 15% O₂}	$= C_x (\text{ppmv}) \times \frac{5.9}{(20.9 - O_2\%)}$				
C_{NOx @ 15% O₂}	=	67.41	x	$\frac{5.9}{(20.9 - 16.77)}$	= 96.37 @ 15% O₂
<i>Formulas</i>					
Pounds per Hour (lbs/hr)					
$Ex (\text{lb/hr}) = C_x \times C_F \times Q_S \times \{ MW_x / (\text{lb} / \text{mole}) \}$					
Tons per Year (tpy)					
$Ex (\text{tpy}) = Ex (\text{lb/hr}) \times \{ 8760 (\text{hr} / \text{yr}) / 2000 (\text{lb} / \text{ton}) \}$					
<i>Calculated Mass Emission Rates From Method 19 Exhaust Flow Rate</i>					
E_{NOx}					
lbs/hr =	67.41	x	1.00E-06	x	910,503 x $\frac{46}{385.15}$ = 7.33
tpy =	7.33 lb/hr	x	4.38	$\frac{\text{hrs-ton}}{\text{lbs-yr}}$	= 32.11
E_{CO}					
lbs/hr =	13.62	x	1.00E-06	x	910,503 x $\frac{28}{385.15}$ = 0.90
tpy =	0.90 lb/hr	x	4.38	$\frac{\text{hrs-ton}}{\text{lbs-yr}}$	= 3.95



MATHESON

ask. . .The Gas Professionals™

1700 Scepter Rd
Waverly, TN 37185
931-296-3357

Certificate of Analysis - EPA Protocol Mixtures

Customer: CST

Customer PO#:

Protocol: Reference #: Lot#: 9303606470
G1 T186938-4

Cylinder Number: CC203971

Cylinder Pressure: 1900 PSIG

Last Analysis Date: 8/22/2013

Expiration Date: 8/23/2016

DO NOT USE THIS CYLINDER WHEN THE PRESSURE FALLS BELOW 100 PSIG

REPLICATE RESPONSES

Date: 8/15/2013	Date: 8/22/2013
49.0	48.9
49.0	48.8
48.7	49.1

Component: Nitric Oxide

Certified Conc: 48.9 PPM +/- 0.2 PPM ABS

NOx: 49.9 PPM Reference Only

BALANCE GAS: Nitrogen

REFERENCE STANDARDS:

Component: Nitric Oxide
Reference Standard: NTRM
Cylinder #: ND44693
Concentration: 98.17 PPM
Exp Date: 9/20/2015
NIST Sample #: 121101

CERTIFICATION INSTRUMENTS

Component: Nitric Oxide
Make/Model: Antaris IGS
Serial Number: AKS1000151
Measurement Principle: FTIR
Last Calibration: 8/12/2013

Notes:

The certification was performed according to EPA Traceability Protocol for Assay and Certification of Gaseous Calibration Standards May 2012, using procedure G1 and/or G2. U.S EPA Vendor ID Number: D62013, PGVP Participation Date: 01/01/13, PGVP Renewal Date: 01/01/14

Analyst: Taylor Wallace
Taylor Wallace

Date: 8/22/2013



MATHESON

ask . . The Gas Professionals™

1700 Scepter Rd
Waverly, TN 37185
931-296-3357

Certificate of Analysis - EPA Protocol Mixtures

Customer: CST

Customer PO#:

Part # G2676958

Protocol:

Reference #:

Lot#:

G1

T204960-2

9305612744

Cylinder Number: SX37028

Cylinder Pressure: 1900 psig

Last Analysis Date: 2/18/2015

Expiration Date: 2/19/2018

DO NOT USE THIS CYLINDER WHEN THE PRESSURE FALLS BELOW 100 PSIG

REPLICATE RESPONSES

Component: Carbon Monoxide
Certified Conc: 44.84 ppm +/- 0.06 ppm ABS
Component: Nitric Oxide
Certified Conc: 44.5 ppm +/- 0.2 ppm ABS
NOx: 44.6 ppm Reference Only

Date: 2/9/2015
44.85
44.83
44.84
Date: 2/9/2015 Date: 2/18/2015
44.6 44.6
44.4 44.6
44.4 44.5

BALANCE GAS: Nitrogen

REFERENCE STANDARDS:

Component: Carbon Monoxide
Reference Standard: SRM
Cylinder #: FF10672
Concentration: 24.512 ppm
Exp. Date: 3/28/2021
NIST Sample #: 58-E-11

Component: Nitric Oxide
Reference Standard: SRM
Cylinder #: FF31654
Concentration: 19.06 ppm
Exp. Date: 4/11/2016
NIST Sample #: 50-G-09

CERTIFICATION INSTRUMENTS

Component: Carbon Monoxide
Make/Model: Horiba VIA-510
Serial Number: ETYS79C6
Measurement Principle: NDIR
Last Calibration: 1/27/2015

Component: Nitric Oxide
Make/Model: Horiba CLA-510SS
Serial Number: FDRJ8FDME
Measurement Principle: CHEMI
Last Calibration: 1/19/2015

Notes:

The certification was performed according to EPA Traceability Protocol for Assay and Certification of Gaseous Calibration Standards May 2012, using procedure G1 and/or G2. U.S EPA Vendor ID Number: D62015, PGVP Participation Date: 01/01/15, PGVP Renewal Date: 01/01/16

Analyst:

Roman Khidekel

Date:

2/26/2015



MATHESON

ask. .The Gas Professionals™

1700 Scepter Rd
Waverly, TN 37185
931-296-3357

Certificate of Analysis - EPA Protocol Mixtures

Customer: Matheson Tri-Gas

Customer PO#:

Cylinder Number: SX46823

Cylinder Pressure: 1900 psig

Last Analysis Date: 10/28/2014

Expiration Date: 10/29/2022

Matheson Part Number: G2687072

Protocol:	Reference #:	Lot#:
G1	T201719-3	9304611567

**DO NOT USE THIS CYLINDER WHEN THE
PRESSURE FALLS BELOW 100 PSIG**

Component: Carbon Monoxide

Certified Conc: 83.39 ppm +/- 0.08 ppm ABS

Component: Nitric Oxide

Certified Conc: 85.5 ppm +/- 0.3 ppm ABS

NOx: 86.3 ppm Reference Only

BALANCE GAS: Nitrogen

REPLICATE RESPONSES

Date: 10/21/2014	
83.39	
83.25	
83.53	
Date: 10/21/2014	Date: 10/28/2014
85.4	85.9
85.3	85.7
85.5	86.0

REFERENCE STANDARDS:

Component: Carbon Monoxide
Reference Standard: SRM
Cylinder #: FF18328
Concentration: 49.136 ppm
Exp. Date: 2/24/2021
NIST Sample #: 04-L-64

Component: Nitric Oxide
Reference Standard: NTRM
Cylinder #: ND44704
Concentration: 98.17 ppm
Exp. Date: 9/20/2015
NIST Sample #: 121101

CERTIFICATION INSTRUMENTS

Component: Carbon Monoxide
Make/Model: Antaris IGS
Serial Number: AKS1000151
Measurement Principle: FTIR
Last Calibration: 9/30/2014

Component: Nitric Oxide
Make/Model: Antaris IGS
Serial Number: AKS1000151
Measurement Principle: FTIR
Last Calibration: 10/27/2014

Notes:

The certification was performed according to EPA Traceability Protocol for Assay and Certification of Gaseous Calibration Standards May 2012, using procedure G1 and/or G2. U.S EPA Vendor ID Number: D62014, PGVP Participation Date: 01/01/14, PGVP Renewal Date: 01/01/15

Analyst:

Roman Khidekel

Date: 10/29/2014



MATHESON

ask. . . The Gas Professionals™

1700 Scepter Rd
Waverly, TN 37185
931-296-3357

Certificate of Analysis - EPA Protocol Mixtures

Customer: WHS: 710

Part # G2689319

Cylinder Number: SX35534
Cylinder Pressure: 1900 psig
Last Analysis Date: 10/16/2015
Expiration Date: 10/16/2023

Protocol: G1 *Reference #: T212837-01 Lot#: 9305615921

DO NOT USE THIS CYLINDER WHEN THE PRESSURE FALLS BELOW 100 PSIG

Component: Carbon Dioxide
Certified Conc: 6.46% +/- 0.02% ABS
Component: Oxygen
Certified Conc: 9.56 % +/- 0.02% ABS

REPLICATE RESPONSES
Date: 10/16/2015
6.46
6.46
6.46
Date: 10/16/2015
9.56
9.56
9.56

BALANCE GAS: Nitrogen

REFERENCE STANDARDS:

Component: Carbon Dioxide
Reference Standard: SRM
Cylinder #: FF10608
Concentration: 6.944 %
Exp. Date: 7/14/2018
NIST Sample# 7-H-18

Component: Oxygen
Reference Standard: SRM
Cylinder #: CAL016848
Concentration: 9.918 %
Exp. Date: 6/1/2017
NIST Sample# 72-D-11

CERTIFICATION INSTRUMENTS

Component: Carbon Dioxide
Make/Model: HORIBA VIA 510
Serial Number: 41679080021
Measurement Principle: NDIR
Last Calibration: 10/14/2015

Component: Oxygen
Make/Model: HORIBA MPA 510
Serial Number: U1LSAGS6
Measurement Principle: PARAMAGNETIC
Last Calibration: 10/13/2015

Notes:

The certification was performed according to EPA Traceability Protocol for Assay and Certification of Gaseous Calibration Standards May 2012, using procedure G1 and/or G2. U.S EPA Vendor ID Number: D62015, PGVP Participation Date: 01/01/15, PGVP Renewal Date: 01/01/16
The expanded uncertainty listed for each component was calculated at a coverage factor of k=2 and at a level of confidence of 95%.

Analyst:

Ashley Stokes

Date: 10/19/2015



MATHESON

ask. . .The Gas Professionals™

1700 Scepter Rd
Waverly, TN 37185
931-296-3357

Certificate of Analysis - EPA Protocol Mixtures

Customer: CST

Cylinder Number: SX48140
Cylinder Pressure: 1900psig
Last Analysis Date: 11/13/2013
Expiration Date: 11/14/2021

Protocol: Reference #: Lot#:
G1 T189541-5 9303607405

DO NOT USE THIS CYLINDER WHEN THE PRESSURE FALLS BELOW 100 PSIG

Component: Carbon Dioxide
Certified Conc: 3.97% +/- 0.03% ABS
Component: Oxygen
Certified Conc: 21.1% +/- 0.4% ABS

REPLICATE RESPONSES
Date: 11/13/2013
3.98
3.97
3.97
Date: 11/13/2013
21.1
21.1
21.0

BALANCE GAS: Nitrogen

REFERENCE STANDARDS:

Component: Carbon Dioxide
Reference Standard: PRM
Cylinder #: D249735
Concentration: 19.793%
Exp. Date: 4/4/2018
NIST Sample #: VSL PRIMARY

Component: Oxygen
Reference Standard: SRM
Cylinder #: CAL015730
Concentration: 23.03%
Exp. Date: 1/1/2016
NIST Sample #: 71-D-36

CERTIFICATION INSTRUMENTS

Component: Carbon Dioxide
Make/Model: HORIBA VIA-510
Serial Number: 41679080021
Measurement Principle: NDIR
Last Calibration: 10/30/2013

Component: Oxygen
Make/Model: HORIBA MPA-510
Serial Number: U1LSAGS6
Measurement Principle: PARAMAGNETIC
Last Calibration: 11/13/2013

Notes:

This Certification was performed according to EPA Traceability Protocol for Assay & Certification of Gaseous Calibration Standards May 2012 , using procedure G1 and/or G2.

U.S. EPA Vendor ID No.: D62013 PGVP Participation Date: 01/01/13: PGVP Renewal Date: 1/1/2014

Analyst: La'Shawn Grissom-Brown
La'Shawn Grissom-Brown

Date: 11/13/2013

Data Log Records

Unit #1

Time	Date	NOx PPMV	CO PPMV	O2 %VOL	CO2 %VOL	Event	Time	Date	NOx PPMV	CO PPMV	O2 %VOL	CO2 %VOL	Event	
7:30	1/20/16	0.26	0.13	0.01	0.01	NOx Converter	8:14	1/20/16	0.36	-0.18	0.01	0.01		
7:31	1/20/16	44.55	44.81	0.01	-0.01		Efficiency Test	8:15	1/20/16	43.90	44.07	0.01		-0.03
7:32	1/20/16	85.74	82.99	0.01	-0.01	Initial Linearity	8:16	1/20/16	0.34	-0.24	9.59	6.46		
7:33	1/20/16	-0.11	-0.20	9.56	6.49		8:17	1/20/16	67.69	9.65	16.80	2.55		
7:34	1/20/16	0.44	-0.47	20.97	4.10		8:18	1/20/16	68.60	9.30	16.80	2.55	Start Run 2	
7:35	1/20/16	49.02	-0.57	0.04	0.01	Response Time /	8:19	1/20/16	68.60	9.30	16.79	2.55		
7:36	1/20/16	0.23	-0.12	0.00	-0.03	Bias Check /	8:20	1/20/16	69.77	8.93	16.80	2.55		
7:37	1/20/16	43.67	44.80	0.00	-0.03	Interference Test	8:21	1/20/16	70.88	8.99	16.80	2.55		
7:38	1/20/16	0.05	-0.24	9.57	6.45		8:22	1/20/16	70.31	8.95	16.79	2.55		
7:39	1/20/16	0.34	-0.61	-0.01	0.01		8:23	1/20/16	71.37	8.90	16.79	2.53		
7:40	1/20/16	66.96	13.09	16.80	2.41	Stratification Test	8:24	1/20/16	71.84	8.97	16.79	2.53		
7:41	1/20/16	71.08	12.65	16.80	2.41		Point 1	8:25	1/20/16	71.39	8.60	16.79	2.53	
7:42	1/20/16	70.91	12.61	16.79	2.41		8:26	1/20/16	72.28	8.93	16.79	2.53		
7:43	1/20/16	71.35	12.52	16.78	2.41		8:27	1/20/16	72.21	8.58	16.79	2.53		
7:44	1/20/16	70.57	12.44	16.78	2.43		8:28	1/20/16	71.83	8.98	16.79	2.53		
7:45	1/20/16	70.81	12.64	16.78	2.43	Point 2	8:29	1/20/16	72.31	8.97	16.79	2.53		
7:46	1/20/16	69.75	13.29	16.78	2.43			8:30	1/20/16	71.38	8.56	16.78	2.53	
7:47	1/20/16	69.39	12.85	16.77	2.43		8:31	1/20/16	72.64	8.60	16.79	2.53		
7:48	1/20/16	69.95	12.76	16.77	2.45		8:32	1/20/16	72.26	8.63	16.78	2.53		
7:49	1/20/16	69.31	12.72	16.77	2.45	Point 3	8:33	1/20/16	71.81	8.23	16.79	2.53		
7:50	1/20/16	69.98	13.29	16.76	2.46			8:34	1/20/16	71.91	8.64	16.79	2.53	
7:51	1/20/16	68.65	13.19	16.76	2.45		8:35	1/20/16	71.32	8.94	16.79	2.53		
7:52	1/20/16	68.61	13.78	16.76	2.46		8:36	1/20/16	71.45	8.60	16.79	2.52		
7:53	1/20/16	68.93	13.33	16.76	2.45	Start Run 1	8:37	1/20/16	69.78	8.61	16.79	2.53		
7:54	1/20/16	68.05	13.98	16.77	2.45			8:38	1/20/16	70.24	8.62	16.79	2.52	
7:55	1/20/16	68.44	13.19	16.78	2.45		Run 2 Average		71.15	8.80	16.79	2.54		
7:56	1/20/16	67.22	13.41	16.79	2.45		8:39	1/20/16	0.45	-0.34	0.01	0.01		
7:57	1/20/16	64.52	13.27	16.80	2.45		8:40	1/20/16	44.18	44.45	0.01	-0.03		
7:58	1/20/16	64.48	13.18	16.80	2.45		8:41	1/20/16	0.70	-0.48	9.60	6.50		
7:59	1/20/16	63.99	13.49	16.79	2.46		8:42	1/20/16	69.49	8.26	16.79	2.52		
8:00	1/20/16	64.96	13.06	16.78	2.46		8:43	1/20/16	69.55	8.40	16.79	2.53	Start Run 3	
8:01	1/20/16	66.31	13.33	16.77	2.46		8:44	1/20/16	69.00	8.24	16.79	2.53		
8:02	1/20/16	67.47	13.16	16.77	2.46		8:45	1/20/16	70.87	7.92	16.79	2.53		
8:03	1/20/16	68.35	13.46	16.78	2.45		8:46	1/20/16	69.25	7.90	16.79	2.53		
8:04	1/20/16	66.12	13.31	16.78	2.46		8:47	1/20/16	69.25	7.89	16.79	2.54		
8:05	1/20/16	65.71	12.60	16.78	2.46		8:48	1/20/16	69.55	8.25	16.79	2.54		
8:06	1/20/16	65.72	12.51	16.78	2.46		8:49	1/20/16	69.22	7.94	16.79	2.53		
8:07	1/20/16	66.15	12.44	16.77	2.46		8:50	1/20/16	70.03	7.90	16.79	2.54		
8:08	1/20/16	67.26	14.07	16.77	2.46		8:51	1/20/16	68.83	7.89	16.78	2.54		
8:09	1/20/16	68.57	13.97	16.77	2.46		8:52	1/20/16	69.42	7.92	16.78	2.54		
8:10	1/20/16	66.10	13.88	16.76	2.48		8:53	1/20/16	68.77	7.88	16.78	2.53		
8:11	1/20/16	65.44	13.44	16.77	2.48		8:54	1/20/16	70.00	7.90	16.79	2.54		
8:12	1/20/16	63.77	14.34	16.75	2.52		8:55	1/20/16	69.62	7.54	16.78	2.53		
8:13	1/20/16	65.75	16.42	16.75	2.52		8:56	1/20/16	69.38	7.52	16.78	2.53		
Run 1 Average														
		66.35	13.52	16.77	2.46		8:57	1/20/16	68.86	7.16	16.79	2.54		
							8:58	1/20/16	69.15	7.51	16.78	2.54		
							8:59	1/20/16	69.90	7.17	16.78	2.53		
							9:00	1/20/16	69.39	7.17	16.78	2.54		
							9:01	1/20/16	70.06	7.57	16.78	2.54		
							9:02	1/20/16	69.40	7.15	16.78	2.53		
							9:03	1/20/16	69.72	7.18	16.78	2.53		
							Run 3 Average		69.49	7.71	16.79	2.53		
							9:04	1/20/16	0.73	-0.59	0.01	-0.01		
							9:05	1/20/16	44.96	44.72	0.01	-0.03		
							9:06	1/20/16	0.59	-0.31	9.60	6.53		

Data Log Records

Unit #2

Time	Date	NOx PPMV	CO PPMV	O2 %VOL	CO2 %VOL	Event	Time	Date	NOx PPMV	CO PPMV	O2 %VOL	CO2 %VOL	Event
7:30	1/20/16	0.08	-0.15	0.00	-0.01	NOx Converter	8:14	1/20/16	0.37	-0.45	0.03	-0.03	
7:31	1/20/16	0.21	-0.25	9.62	6.49		Efficiency Test	8:15	1/20/16	0.38	-0.39	9.63	
7:32	1/20/16	0.11	-0.05	21.12	3.99	Initial Linearity	8:16	1/20/16	43.93	44.19	0.01	-0.02	
7:33	1/20/16	44.14	44.95	-0.01	0.01			8:17	1/20/16	74.03	11.19	17.40	
7:34	1/20/16	84.78	83.93	-0.02	0.00	Response Time / Bias Check / Interference Test	8:18	1/20/16	73.80	11.18	17.41	2.10	Start Run 2
7:35	1/20/16	49.35	-0.35	0.01	-0.02			8:19	1/20/16	73.80	11.19	17.42	
7:36	1/20/16	0.32	-0.05	0.00	0.00		8:20	1/20/16	73.75	11.19	17.43	2.09	
7:37	1/20/16	0.37	-0.12	9.59	6.51		8:21	1/20/16	73.67	11.19	17.43	2.11	
7:38	1/20/16	43.63	43.94	0.01	0.02	Stratification Test	8:22	1/20/16	73.57	11.19	17.44	2.09	
7:39	1/20/16	0.02	-0.04	0.00	0.02			8:23	1/20/16	73.36	11.19	17.44	
7:40	1/20/16	71.19	11.95	17.38	1.92	Point 1	8:24	1/20/16	73.69	12.20	17.44	2.09	
7:41	1/20/16	72.71	10.94	17.43	1.96			8:25	1/20/16	73.69	12.19	17.45	
7:42	1/20/16	72.35	10.94	17.46	1.97	Point 2	8:26	1/20/16	73.77	12.20	17.45	2.09	
7:43	1/20/16	72.54	10.94	17.49	1.98			8:27	1/20/16	73.89	12.20	17.45	
7:44	1/20/16	72.15	10.94	17.51	1.97	Point 3	8:28	1/20/16	73.73	12.20	17.45	2.10	
7:45	1/20/16	71.62	11.95	17.52	1.99			8:29	1/20/16	73.85	11.19	17.46	
7:46	1/20/16	69.86	17.94	17.52	1.99	Point 3	8:30	1/20/16	73.71	11.19	17.46	2.10	
7:47	1/20/16	70.53	15.94	17.53	2.01			8:31	1/20/16	73.81	11.19	17.46	
7:48	1/20/16	70.63	15.95	17.53	2.02	Point 3	8:32	1/20/16	73.68	12.20	17.46	2.10	
7:49	1/20/16	70.52	16.94	17.53	2.02			8:33	1/20/16	73.44	12.20	17.45	
7:50	1/20/16	71.00	16.95	17.53	2.05	Point 3	8:34	1/20/16	74.03	12.20	17.46	2.10	
7:51	1/20/16	71.13	16.94	17.53	2.04			8:35	1/20/16	73.66	13.18	17.46	
7:52	1/20/16	71.03	16.96	17.52	2.05	Point 3	8:36	1/20/16	73.72	12.20	17.46	2.10	
7:53	1/20/16	72.01	14.95	17.52	2.04			8:37	1/20/16	73.81	13.18	17.45	
7:54	1/20/16	72.23	12.94	17.53	2.02	Start Run 1	8:38	1/20/16	73.94	13.19	17.45	2.10	
7:55	1/20/16	72.24	13.94	17.54	2.03					Run 2 Average	73.73	11.91	
7:56	1/20/16	72.10	14.95	17.54	2.03	Start Run 1	8:39	1/20/16	0.63	-0.34	0.03	-0.03	
7:57	1/20/16	71.80	14.95	17.54	2.03			8:40	1/20/16	0.48	-0.52	9.62	
7:58	1/20/16	71.86	14.95	17.54	2.03	Start Run 1	8:41	1/20/16	43.86	44.49	0.03	-0.01	
7:59	1/20/16	71.49	14.95	17.53	2.04			8:42	1/20/16	72.68	9.96	17.39	
8:00	1/20/16	71.30	14.96	17.55	2.02	Start Run 1	8:43	1/20/16	72.63	9.96	17.39	2.15	Start Run 3
8:01	1/20/16	71.17	14.95	17.56	2.02			8:44	1/20/16	72.45	9.96	17.39	
8:02	1/20/16	71.06	14.95	17.57	2.01	Start Run 1	8:45	1/20/16	72.26	9.95	17.40	2.15	
8:03	1/20/16	70.39	14.95	17.60	2.00			8:46	1/20/16	72.27	9.96	17.40	
8:04	1/20/16	70.18	12.94	17.62	1.99	Start Run 1	8:47	1/20/16	72.24	9.87	17.40	2.14	
8:05	1/20/16	70.21	11.95	17.63	1.99			8:48	1/20/16	72.36	9.96	17.39	
8:06	1/20/16	70.23	11.95	17.63	1.97	Start Run 1	8:49	1/20/16	72.61	9.96	17.39	2.14	
8:07	1/20/16	70.13	11.95	17.64	1.97			8:50	1/20/16	72.24	9.95	17.40	
8:08	1/20/16	69.49	12.94	17.64	1.96	Start Run 1	8:51	1/20/16	72.21	9.96	17.39	2.15	
8:09	1/20/16	67.93	16.96	17.64	1.98			8:52	1/20/16	72.32	9.96	17.39	
8:10	1/20/16	67.51	18.95	17.64	1.99	Start Run 1	8:53	1/20/16	72.28	9.96	17.39	2.14	
8:11	1/20/16	68.81	14.96	17.63	1.97			8:54	1/20/16	72.31	9.96	17.40	
8:12	1/20/16	68.66	15.95	17.63	1.97	Start Run 1	8:55	1/20/16	72.25	8.95	17.40	2.14	
8:13	1/20/16	69.48	12.94	17.64	1.95			8:56	1/20/16	72.19	9.96	17.39	
	Run 1 Average	70.49	14.43	17.59	2.00		8:57	1/20/16	72.06	8.95	17.39	2.14	
							8:58	1/20/16	71.79	8.95	17.39	2.14	
							8:59	1/20/16	72.34	8.95	17.38	2.14	
							9:00	1/20/16	71.57	8.95	17.39	2.14	
							9:01	1/20/16	72.02	8.95	17.38	2.15	
							9:02	1/20/16	72.03	8.95	17.38	2.14	
							9:03	1/20/16	72.21	8.95	17.38	2.14	
									Run 3 Average	72.22	9.57	17.39	
							9:04	1/20/16	0.87	-0.63	0.04	-0.04	
							9:05	1/20/16	0.29	-0.66	9.66	6.43	
							9:06	1/20/16	44.29	44.94	0.04	-0.04	

Particulate Matter Emission Estimates

Leslie Witherspoon
Solar Turbines Incorporated

PURPOSE

This document summarizes Solar's recommended PM_{10/2.5} emission levels for our combustion turbines. The recommended levels are based on an analysis of emissions tests collected from customer sites.

Particulate Matter Definition

National Ambient Air Quality Standards (NAAQS) for particulate matter were first set in 1971. Total suspended particulate (TSP) was the first indicator used to represent suspended particles in the ambient air. Since July 1, 1987, the Environmental Protection Agency (EPA) has used the indicator PM₁₀, which includes only the particles with aerodynamic diameter smaller than 10 micrometers. PM₁₀ (coarse particles) come from sources such as windblown dust from the desert or agricultural fields and dust kicked up on unpaved roads by vehicle traffic.

The EPA added a PM_{2.5} ambient air standard in 1997. PM_{2.5} includes particles with an aerodynamic diameter less than 2.5 micrometers. PM_{2.5} (fine particles) are generally emitted from activities such as industrial and residential combustion and from vehicle exhaust. Fine particles are also formed in the atmosphere when gases such as sulfur dioxide, nitrogen oxides, and volatile organic compounds, emitted by combustion activities, are transformed by chemical reactions.

Nearly all particulate matter from gas turbine exhaust is less than one micrometer (micron) in diameter. Thus the emission rates of TSP, PM₁₀, and PM_{2.5} from gas turbines are theoretically equivalent although source testing will show variation due to test method detection levels and processes.

TESTING FOR PARTICULATE MATTER

The turbine combustion process has little effect on the particulate matter generated and measured. The largest contributor to particulate matter emissions for gas and liquid fired combustion turbines is measurement technique and error. Other, minor contributing, sources of particulate matter emissions include carbon, ash, fuel-bound sulfur, artifact sulfate formation, compressor/lubricating oils, and inlet air.

Historical customer particulate matter source test data show that there is significant variability from test to test. The source test results support the common industry argument that particulate matter from natural gas fired combustion sources is difficult to measure accurately. The reference test methods for particulate matter were developed primarily for measuring emissions from coal-fired power plants and other major emitters of particulates. Particulate concentrations from gas turbine can be 100 to 10,000 times lower than the "traditional" particulate sources. The test methods were not developed or verified for low emission levels. There are interferences, insignificant at higher exhaust particulate matter concentrations that result in emissions greater than the actual emissions from gas turbines. New methods are being developed to address this problem.

Due to measurement and procedural errors, the measured results, in most cases, may not be representative of actual particulate matter emitted. There are many potential error sources in measuring particulate matter. Most of these have to do with contamination of the samples, material from the sampling apparatus getting into the samples, and general human error in samples and analysis.

Recommended Particulate Matter Emission Factors

When necessary to support the air permitting process Solar recommends the following PM_{10/2.5} emission factors:

- **Natural Gas: 0.015 lb/MMBtu fuel input (HHV)**
- Landfill Gas: 0.03 lb/MMBtu fuel input (HHV)
- Liquid Fuel: 0.06 lb/MMBtu fuel input (HHV). The liquid fuel emission factor assumes fuel sulfur content is <500 ppm and ash content is <0.005% by wt.

The emission levels cited above are only for engine operation with the fuels listed. Other fuels may not yield similar results.

Recent customer source testing has shown that AP-42 (EPA AP-42 "Compilation of Air Pollutant Emission Factors.") emission factors for natural gas are achievable in the field, when the test method recommendations shown below are followed. Historically, Solar did not recommend using AP-42 because while some source test firms have measured below AP-42 levels, others have measured higher. Because particulate matter emissions levels are highly dependent on the test firm and have very little to do with the turbine, Solar does not warrant AP-42 levels but does recognize they are achievable in the field. Customers generally choose a particulate matter emissions factor at or above the AP-42 level that works for their site permitting recognizing that the lower the emissions factor the higher the risk for source testing. Any Solar warranty on particulate matter would be at the recommended levels above, e.g. 0.015 lb/MMBtu (HHV) for natural gas.

Test Method Recommendation

Solar recommends that EPA Methods 201/201A¹ be used to measure the "front half". "Front half" represents filterable particulate matter.

EPA Method 202² (with nitrogen purge and field blanks) should be used to measure the "back half". "Back half" measurements represent the condensable portion of particulate matter.

EPA Method 5³, which measures the front and back halves may be substituted (e.g. where exhaust temperatures do not allow the use of Method 202).

Testing should include three test runs of 4 hours each.

Solar recommends using the aforementioned test methods until more representative test methods are developed and made commercially available.

References

¹ EPA Method 201, Determination of PM₁₀ Emissions, Exhaust Gas Recycle Procedure. EPA Method 201A, Determination of PM₁₀ Emissions, Constant Sampling Rate Procedure, 40 CFR 60, Part 60, Appendix A.

² EPA Method 202, Determination of Condensable Particulate Emissions from Stationary Sources, 40 CFR 60, Part 60, Appendix A.

³ EPA Method 5, Determination of Particulate Emissions from Stationary Sources, 40 CFR 60, Part 60, Appendix

Solar Turbines Incorporated
9330 Sky Park Court
San Diego, CA 92123-5398

Cat and Caterpillar are registered trademarks of Caterpillar Inc. *Solar*, *Saturn*, *Centaur*, *Taurus*, *Mercury*, *Mars*, *Titan*, *SoLoNOx*, *Turbotronic*, *InSight System*, and *InSight Connect*, are trademarks of Solar Turbines Incorporated. All other trademarks are the intellectual property of their respective companies.

© 2014 Solar Turbines Incorporated. All rights reserved. Specifications are subject to change without notice.

Ms. Jennifer Courser
Enterprise Products Operating
2162 Commerce Dr.
Midland, TX 79707
(432) 681-2600

05/15/2010

Re: Annual emissions testing at the South Carlsbad Compressor Station on Unit 1

Ms. Courser,

Exhaust emissions from one compressor turbine was tested at the South Carlsbad compressor station near Loving, New Mexico on. Testing was conducted to demonstrate compliance with emission limits set forth by NMED permit. The engine is identified as follows:

Engine Information	
Unit Number:	Unit 1
Manufacturer:	Solar
Serial Number:	4920
Model:	CENTAUR 40
Mfr. Rated Hp:	4500hp
Mfr. Rated Speed:	15,000

This is a natural gas fired turbine used for compression of natural gas for transportation through the pipeline.

The test matrix consisted of three 20-minute test runs on the turbine in accordance with NMED requirements. For each test, the average emission concentrations of nitrogen oxides (NO_x), oxygen (O₂), and carbon monoxide (CO) were measured using analytical instrumentation. Operational data such as Gas Producer Speed, Turbine Speed, and suction and discharge pressures were recorded during each run from available operational data on the unit.

Results of the tests are presented in tabular format in this report. Included in this table are engine operational data, ambient conditions, emission concentrations, and mass emission rates.

Continuous emission monitors housed in an air-conditioned mobile laboratory were used to measure the exhaust concentrations of NO_x, CO and O₂. This testing utilized the following analytical methods:

EPA Reference Method 3a	O ₂ concentration
EPA Reference Method 7e	NO _x concentration
EPA Reference Method 10	CO concentration
EPA Reference Method 19	Mass emission rates

A computerized data recorder was used to record output from the analyzers. The data logger record provides documentation of the emission measurements and the instrument calibrations. The data logger records are also useful for indicating trends in the data.

Mass emission rates were calculated using EPA Method 19 calculations (combustion stoichiometry). Emission rates in terms of lbs/hr and TPY were calculated using the pollutant concentration (ppmv), the oxygen F-factor (DSCF_{ex}/MMBtu) and the horsepower specific fuel consumption rate (Btu/Hp-hr). The O₂ F-Factor used in this test series was 8710 (DSCF_{ex}/MMBtu), the EPA default value for engines burning natural gas. The horsepower specific fuel rate used in the test was 9080 Btu/Hp-hr.

A summary of the quality assurance procedures associated with the EPA test methods is presented in tabular format in the appendix of this report. Examples of these procedures include daily multipoint calibrations, zero and span checks between each test run, NO₂ to NO converter efficiency check results, sample system bias check results, and analyzer interference test results.

The appendix of this report also includes supporting test documentation, example calculations, and data logger records.

If you have any questions, please feel free to contact me at (806) 773-8851.

Sincerely,



Ross Thompson
Principal Scientist
Relient Emissions Testing, Inc

Solar Turbines

A Caterpillar Company

Solar Turbines Incorporated

9330 Sky Park Court
San Diego, CA 92123
Tel: (858) 694-1616

Submitted Electronically

September 4, 2019

Attn: Jing Li
Enterprise Products

Subject: Centaur 40 Routine Maintenance Overhaul
South Carlsbad (NM)

The Centaur 40 turbine package (S/N 3020123) at the above facility recently underwent a routine maintenance overhaul utilizing Solar Turbine's engine exchange program.

The overhaul engine core that Solar Turbines provided to Enterprise was a like-for-like replacement with the same guarantees on performance and emissions as the core that was replaced.

Per 40 CFR 60, Subpart KKKK rule language, an overhaul does not trigger the definition of "modification" because it is a like-for-like exchange with the same performance and emissions specifications as the original equipment. In addition, an overhaul is not "reconstruction" as the cost of a routine overhaul is well less than 50% of the cost of a new comparable unit.

This turbine package "commenced construction" in 1973. Routine overhaul exchange of turbine components does not signify a new affected facility per the NSPS provisions in 40 CFR 60.

Because routine overhaul exchange of components on an existing facility does not trigger the definitions of "new", "modification" or "reconstruction" there are no federal NSPS ramifications. Solar recommends a review of the State-issued operating permit for any facility specific requirements associated with the overhaul which typically may include agency notification and/or emissions testing.

Please call me at 858.505.8554 if you have any questions.

Sincerely,

Anthony Pocengal
Solar Turbines Incorporated

cc: Joey Guillen, Solar Turbines

Solar Turbines

A Caterpillar Company

Solar Turbines Incorporated

9330 Sky Park Court
San Diego, CA 92123
Tel: (858) 694-1616

Submitted Electronically

October 3, 2019

Attn: Alena Miro
Enterprise Products

Subject: Centaur 40 – Routine Maintenance Overhaul
South Carlsbad Unit 2 (NM)

The Centaur 40 turbine (S/N CC79419) at the above facility underwent a routine maintenance overhaul utilizing Solar Turbine's engine exchange program in September 2018.

The overhauled turbine core (gas producer and power turbine) that Solar Turbines provided Enterprise is a like-kind replacement with the same guarantees on performance and emissions as the core that was replaced.

Per 40 CFR 60, Subparts GG and KKKK rule language, an overhaul does not trigger the definition of "modification" because it is a like-for-like exchange with the same performance and emissions specifications as the original equipment. In addition, the engine exchange is not "reconstruction" as the cost of a routine overhaul is well less than 50% of the cost of a new comparable unit.

The overhauled engine is not "new" as per the NSPS General Provisions in 40 CFR 60, Subpart A, this turbine "commenced construction" in 1979. Routine overhaul exchange of turbine components does not signify a new affected facility per either of the Subpart GG or KKKK definitions.

Because routine overhaul exchange of components on an existing facility does not trigger the definitions of "new", "modification" or "reconstruction", there are no NSPS ramifications due to this activity.

Please call me at 858.505.8554 if you have any questions.

Sincerely,

Anthony Pocengal
Solar Turbines Incorporated

cc: Joey Guillen, Solar Turbines Incorporated

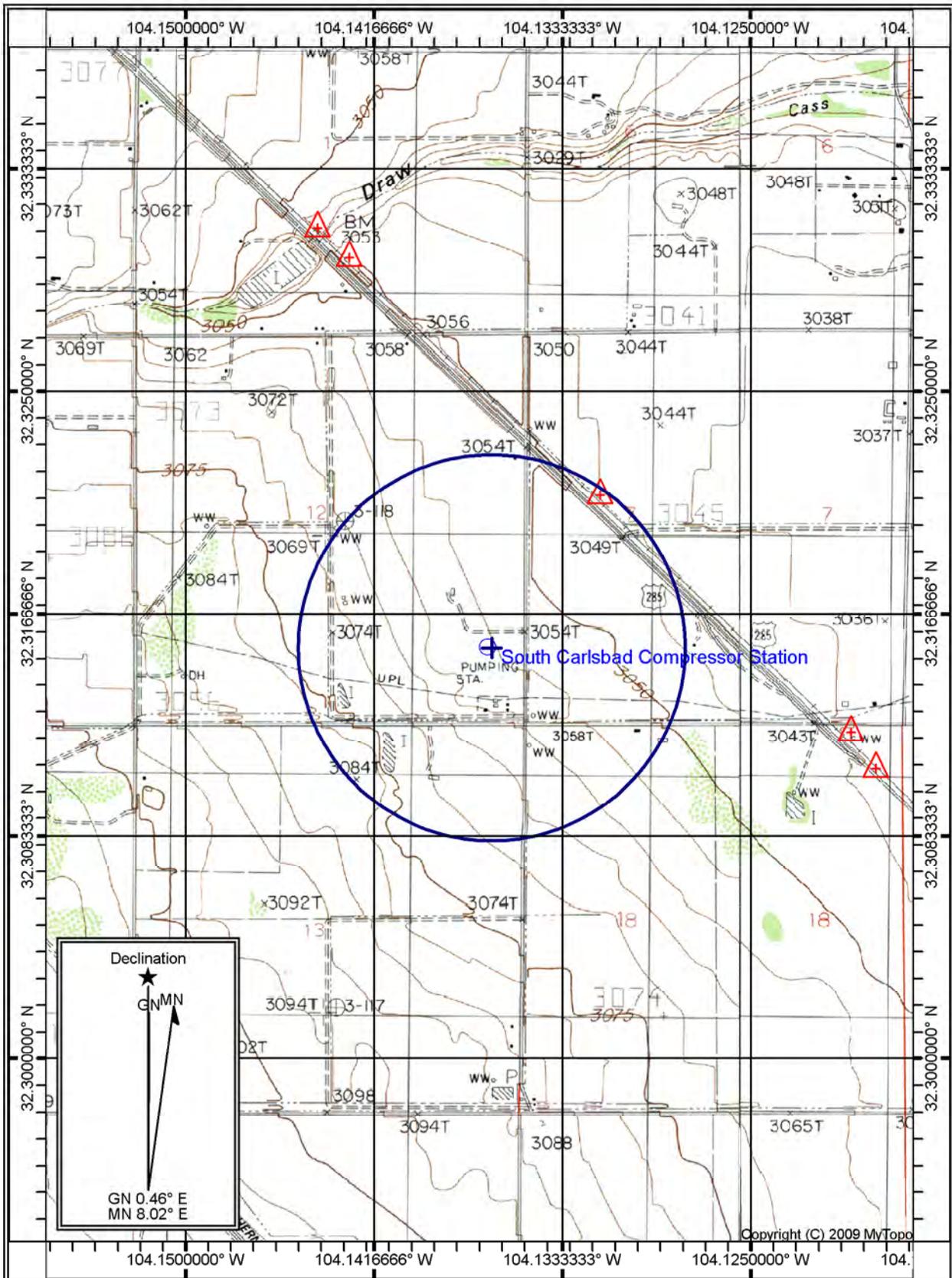
Section 8

Map(s)

A map such as a 7.5 minute topographic quadrangle showing the exact location of the source. The map shall also include the following:

The UTM or Longitudinal coordinate system on both axes	An indicator showing which direction is north
A minimum radius around the plant of 0.8km (0.5 miles)	Access and haul roads
Topographic features of the area	Facility property boundaries
The name of the map	The area which will be restricted to public access
A graphical scale	

A topographic map is attached on the following page.



Map Name: OTIS
 Print Date: 07/15/20
 Scale: 1 inch = 2,000 ft.
 Map Center: 032.3155315° N 104.1370278° W

Horizontal Datum: WGS84

Section 10

Written Description of the Routine Operations of the Facility

A written description of the routine operations of the facility. Include a description of how each piece of equipment will be operated, how controls will be used, and the fate of both the products and waste generated. For modifications and/or revisions, explain how the changes will affect the existing process. In a separate paragraph describe the major process bottlenecks that limit production. The purpose of this description is to provide sufficient information about plant operations for the permit writer to determine appropriate emission sources.

The facility is a natural gas compressor station or transport of natural gas. Gas enters the facility through a separator and is compressed by three gas turbine-driven compressors (Units 1, 2, & 5) and five 4-stroke lean burn compressor engines (Units 6, 7, 8, 9, & 10). The gas is then routed through a dehydrator, Unit 3, where water is removed. The water from the dehydrator regenerator, which contains some hydrocarbons, is routed through a condenser to recover salable hydrocarbons, which are routed to T-006. The non-condensable gas from the condenser is routed to ECD-1 with a 100% capture efficiency and a 98% DRE. The gas stream from the flash tank is sent to the reboiler as fuel. When the reboiler does not call for fuel, the flash gas is sent to ECD-1 with a 100% capture efficiency and a 98% DRE. After inlet compression, gas is sent directly to a chiller and cold separator, where liquids (primarily water) condense and are removed from the stream. The dry gas stream then goes to a pipeline for transport.

Liquids from the inlet separator are routed to a 3-phase separator, where water, hydrocarbon liquids, and gas are separated. The gas stream from the 3-phase separator is used as turbine fuel (along with makeup fuel if needed from the discharge residue gas stream and/or the gas stream from the condensate stabilizer). The water goes to tanks for storage. The hydrocarbon liquids from the 3-phase separator and from the cold separator go to the condensate stabilizer where the water and hydrocarbons are further separated. Liquid hydrocarbons and water are stored in separate tanks, and hydrocarbon gases are added to the turbine fuel stream.

In the event of an emergency, the gas streams from the 3-phase separator and from the condensate stabilizer may be routed to the flare. During non-routine conditions such as when gas must be released from portions of the facility for maintenance or in the event of an emergency, some VOCs will be directed to the flare. Gas from the 3-phase separator and stabilizer overheads will be directed to the flare in the event of a plant shutdown. Additionally, during an emergency shutdown, pressure vessels or the gas contents of the refrigeration system may be released to the flare; however, the quantity of gas in these vessels or systems is less than the assumed maximum gas volume from the 3-phase separator and stabilizer overheads.

Section 11

Source Determination

Source submitting under 20.2.70, 20.2.72, 20.2.73, and 20.2.74 NMAC

Sources applying for a construction permit, PSD permit, or operating permit shall evaluate surrounding and/or associated sources (including those sources directly connected to this source for business reasons) and complete this section. Responses to the following questions shall be consistent with the Air Quality Bureau's permitting guidance, Single Source Determination Guidance, which may be found on the Applications Page in the Permitting Section of the Air Quality Bureau website.

Typically, buildings, structures, installations, or facilities that have the same SIC code, that are under common ownership or control, and that are contiguous or adjacent constitute a single stationary source for 20.2.70, 20.2.72, 20.2.73, and 20.2.74 NMAC applicability purposes. Submission of your analysis of these factors in support of the responses below is optional, unless requested by NMED.

A. Identify the emission sources evaluated in this section (list and describe):

All sources listed in Table2-A of this application.

B. Apply the 3 criteria for determining a single source:

SIC Code: Surrounding or associated sources belong to the same 2-digit industrial grouping (2-digit SIC code) as this facility, OR surrounding or associated sources that belong to different 2-digit SIC codes are support facilities for this source.

Yes No

Common Ownership or Control: Surrounding or associated sources are under common ownership or control as this source.

Yes No

Contiguous or Adjacent: Surrounding or associated sources are contiguous or adjacent with this source.

Yes No

C. Make a determination:

- The source, as described in this application, constitutes the entire source for 20.2.70, 20.2.72, 20.2.73, or 20.2.74 NMAC applicability purposes. If in "A" above you evaluated only the source that is the subject of this application, all "YES" boxes should be checked. If in "A" above you evaluated other sources as well, you must check **AT LEAST ONE** of the boxes "NO" to conclude that the source, as described in the application, is the entire source for 20.2.70, 20.2.72, 20.2.73, and 20.2.74 NMAC applicability purposes.
- The source, as described in this application, **does not** constitute the entire source for 20.2.70, 20.2.72, 20.2.73, or 20.2.74 NMAC applicability purposes (A permit may be issued for a portion of a source). The entire source consists of the following facilities or emissions sources (list and describe):

Section 12

Section 12.A

PSD Applicability Determination for All Sources

(Submitting under 20.2.72, 20.2.74 NMAC)

A PSD applicability determination for all sources. For sources applying for a significant permit revision, apply the applicable requirements of 20.2.74.AG and 20.2.74.200 NMAC and to determine whether this facility is a major or minor PSD source, and whether this modification is a major or a minor PSD modification. It may be helpful to refer to the procedures for Determining the Net Emissions Change at a Source as specified by Table A-5 (Page A.45) of the EPA New Source Review Workshop Manual to determine if the revision is subject to PSD review.

A. This facility is:

- a minor PSD source before and after this modification (if so, delete C and D below).
- a major PSD source before this modification. This modification will make this a PSD minor source.
- an existing PSD Major Source that has never had a major modification requiring a BACT analysis.
- an existing PSD Major Source that has had a major modification requiring a BACT analysis
- a new PSD Major Source after this modification.

B. This facility is a minor source. With this permit application emissions for this facility will be less than 250 tpy for all regulated pollutants making this a PSD minor source.

Section 13

Determination of State & Federal Air Quality Regulations

This section lists each state and federal air quality regulation that may apply to your facility and/or equipment that are stationary sources of regulated air pollutants.

Not all state and federal air quality regulations are included in this list. Go to the Code of Federal Regulations (CFR) or to the Air Quality Bureau's regulation page to see the full set of air quality regulations.

Required Information for Specific Equipment:

For regulations that apply to specific source types, in the 'Justification' column **provide any information needed to determine if the regulation does or does not apply**. For example, to determine if emissions standards at 40 CFR 60, Subpart IIII apply to your three identical stationary engines, we need to know the construction date as defined in that regulation; the manufacturer date; the date of reconstruction or modification, if any; if they are or are not fire pump engines; if they are or are not emergency engines as defined in that regulation; their site ratings; and the cylinder displacement.

Required Information for Regulations that Apply to the Entire Facility:

See instructions in the 'Justification' column for the information that is needed to determine if an 'Entire Facility' type of regulation applies (e.g. 20.2.70 or 20.2.73 NMAC).

Regulatory Citations for Regulations That Do Not, but Could Apply:

If there is a state or federal air quality regulation that does not apply, but you have a piece of equipment in a source category for which a regulation has been promulgated, you must **provide the low level regulatory citation showing why your piece of equipment is not subject to or exempt from the regulation**. For example if you have a stationary internal combustion engine that is not subject to 40 CFR 63, Subpart ZZZZ because it is an existing 2 stroke lean burn stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions, your citation would be 40 CFR 63.6590(b)(3)(i). **We don't want a discussion of every non-applicable regulation, but if it is possible a regulation could apply, explain why it does not**. For example, if your facility is a power plant, you do not need to include a citation to show that 40 CFR 60, Subpart OOO does not apply to your non-existent rock crusher.

Regulatory Citations for Emission Standards:

For each unit that is subject to an emission standard in a source specific regulation, such as 40 CFR 60, Subpart OOO or 40 CFR 63, Subpart HH, include the low level regulatory citation of that emission standard. Emission standards can be numerical emission limits, work practice standards, or other requirements such as maintenance. **Here are examples:** a glycol dehydrator is subject to the general standards at 63.764C(1)(i) through (iii); an engine is subject to 63.6601, Tables 2a and 2b; a crusher is subject to 60.672(b), Table 3 and all transfer points are subject to 60.672(e)(1)

Federally Enforceable Conditions:

All federal regulations are federally enforceable. All Air Quality Bureau State regulations are federally enforceable except for the following: affirmative defense portions at 20.2.7.6.B, 20.2.7.110(B)(15), 20.2.7.11 through 20.2.7.113, 20.2.7.115, and 20.2.7.116; 20.2.37; 20.2.42; 20.2.43; 20.2.62; 20.2.63; 20.2.86; 20.2.89; and 20.2.90 NMAC. Federally enforceable means that EPA can enforce the regulation as well as the Air Quality Bureau and federally enforceable regulations can count toward determining a facility's potential to emit (PTE) for the Title V, PSD, and nonattainment permit regulations.

INCLUDE ANY OTHER INFORMATION NEEDED TO COMPLETE AN APPLICABILITY DETERMINATION OR THAT IS RELEVANT TO YOUR FACILITY'S NOTICE OF INTENT OR PERMIT.

EPA Applicability Determination Index for 40 CFR 60, 61, 63, etc: <http://cfpub.epa.gov/adi/>

Table for State Regulations:

State Regulation Citation	Title	Applies? Enter Yes or No	Unit(s) or Facility	Justification: (You may delete instructions or statements that do not apply in the justification column to shorten the document.)
20.2.1 NMAC	General Provisions	Yes	Facility	General Provisions apply to Notice of Intent, Construction, and Title V permit applications.
20.2.3 NMAC	Ambient Air Quality Standards NMAAQS	Yes	Facility	20.2.3 NMAC is a SIP approved regulation that limits the maximum allowable concentration of Total Suspended Particulates, Sulfur Compounds, Carbon Monoxide and Nitrogen Dioxide. The facility meets maximum allowable concentrations of TSP, SO ₂ , H ₂ S, NO _x , and CO under this regulation.
20.2.7 NMAC	Excess Emissions	Yes	Facility	This regulation establishes requirements for the facility if operations at the facility result in any excess emissions. The owner or operator will operate the source at the facility having an excess emission, to the extent practicable, including associated air pollution control equipment, in a manner consistent with good air pollution control practices for minimizing emissions. The facility will also notify the NMED of any excess emission per 20.2.7.110 NMAC.
20.2.23 NMAC	Fugitive Dust Control	No	N/A	This regulation does not apply as the facility has no need of fugitive dust control measures as the facility does not generate enough particulate matter.
20.2.33 NMAC	Gas Burning Equipment - Nitrogen Dioxide	No	N/A	This facility does not have gas burning equipment (external combustion emission sources, such as gas fired boilers and heaters) having a heat input of greater than 1,000,000 million British Thermal Units per year per unit. The facility is not subject to this regulation and does not have emission sources that meet the applicability requirements under 20.2.33.108 NMAC.
20.2.34 NMAC	Oil Burning Equipment: NO ₂	No	N/A	This facility does not have oil burning equipment (external combustion emission sources, such as oil fired boilers and heaters) having a heat input of greater than 1,000,000 million British Thermal Units per year per unit. The facility is not subject to this regulation and does not have emission sources that meet the applicability requirements under 20.2.34.108 NMAC.
20.2.35 NMAC	Natural Gas Processing Plant – Sulfur	Yes	Facility	This regulation establishes sulfur emission standards for natural gas processing plants. This facility is a new natural gas processing plant as defined in 20.2.35.7.B NMAC. The facility does not meet the minimum sulfur emission requirement of an average of 5 tpy [20.2.35.110.A NMAC]. This facility is subject to the stack height, recordkeeping, and reporting requirements of this regulation [20.2.35.111-112 NMAC].
20.2.37 and 20.2.36 NMAC	Petroleum Processing Facilities and Petroleum Refineries	N/A	N/A	These regulations were repealed by the Environmental Improvement Board. If you had equipment subject to 20.2.37 NMAC before the repeal, your combustion emission sources are now subject to 20.2.61 NMAC.
20.2.38 NMAC	Hydrocarbon Storage Facility	No	N/A	This facility is not a petroleum production facility as defined in 20.2.38.7.D NMAC. Natural gas enters this facility via pipeline and inlet separator. Condensate stored at this facility comes from the pipeline, not a well. Accordingly, the tanks at this facility do not meet the definition of a tank battery as defined in 20.2.38.7.E.
20.2.39 NMAC	Sulfur Recovery Plant - Sulfur	No	N/A	This regulation establishes sulfur emission standards for sulfur recovery plants that are not part of petroleum or natural gas processing facilities. This regulation does not apply to the facility because this facility does not have a sulfur recovery plant.
20.2.50 NMAC	Oil and Gas Sector – Ozone Precursor Pollutants	Yes	1, 2, 3b, 5, 6, 7, 8, 9, 10, ECD, Flare	This regulation establishes emission standards for volatile organic compounds (VOC) and oxides of nitrogen (NO _x) for oil and gas production, processing, compression, and transmission sources. 20.2.50 NMAC subparts below: Check the box for the subparts that are applicable: <input checked="" type="checkbox"/> 113 – Engines and Turbines – Enterprise will comply with the requirements of this subpart. <input checked="" type="checkbox"/> 114 – Compressor Seals – Reciprocating compressors located at boosting stations are subject to the requirements of this subpart. <input checked="" type="checkbox"/> 115 – Control Devices and Closed Vent Systems – Enterprise will comply with the requirements of this subpart.

<u>State Regulation Citation</u>	Title	Applies? Enter Yes or No	Unit(s) or Facility	Justification: (You may delete instructions or statements that do not apply in the justification column to shorten the document.)
				<input checked="" type="checkbox"/> 116 – Equipment Leaks and Fugitive Emissions – Enterprise will comply with the requirements of this subpart. <input type="checkbox"/> 117 – Natural Gas Well Liquid Unloading – N/A – This facility does not contain natural gas wells; therefore, they are not subject to the requirements of this subpart. <input type="checkbox"/> 118 – Glycol Dehydrators – N/A – The glycol dehydrator has a PTE of less than 2 tpy and will therefore not be subject to this subpart. <input type="checkbox"/> 119 – Heaters – N/A – The firing rates of the heaters are less than 20 MMBtu/hr; therefore, they are not subject to this subpart. <input checked="" type="checkbox"/> 120 – Hydrocarbon Liquid Transfers – This facility trucks out more than 13 times a year and is therefore subject to this subpart. <input type="checkbox"/> 121 – Pig Launching and Receiving – N/A – Pig launching and receiving operations at this facility are below 1 tpy and will therefore not be subject to this subpart. <input checked="" type="checkbox"/> 122 – Pneumatic Controllers and Pumps – Any natural-gas driven controllers or pumps at the facility will comply with the applicable requirements of this rule. <input type="checkbox"/> 123 – Storage Vessels – N/A – The permitted PTE for the storage tanks is less than the applicability thresholds; therefore, the requirements of this subpart do not apply. <input type="checkbox"/> 124 – Well Workovers – N/A – There are no oil or natural gas wells located at this facility; therefore, this subpart does not apply. <input type="checkbox"/> 125 – Small Business Facilities – N/A – This facility does not qualify as a small business facility; therefore, this subpart does not apply. <input type="checkbox"/> 126 – Produced Water Management Unit – N/A – There are no produced water management units located at this facility; therefore, this subpart does not apply. <input type="checkbox"/> 127 – Flowback Vessels and Preproduction Operations – N/A – There are no wells located at this facility; therefore, this subpart does not apply.
20.2.61.109 NMAC	Smoke & Visible Emissions	Yes	1, 2, 3b, 5, 6, 7, 8, 9, 10 ECD, Flare	This regulation establishes controls on smoke and visible emissions from certain sources, including stationary combustion equipment. This regulation is applicable to the following stationary combustion units: 1, 2, 3b, 5, 6, 7, 8, 9, 10, ECD, and Flare.
20.2.70 NMAC	Operating Permits	Yes	Facility	This regulation establishes requirements for obtaining an operating permit. This facility is a major source with respect to Title V and is permitted under P-130-R4. The facility will comply with all operating permit conditions as applicable.
20.2.71 NMAC	Operating Permit Fees	Yes	Facility	This regulation establishes a schedule of operating permit emission fees. The facility is subject to 20.2.70 NMAC and is therefore subject to requirements of this regulation.
20.2.72 NMAC	Construction Permits	Yes	Facility	This regulation establishes the requirements for obtaining a construction permit. This facility is subject to the requirements of this subpart and complies with NSR Permit 0220-M12R1.
20.2.73 NMAC	NOI & Emissions Inventory Requirements	Yes	Facility	This regulation establishes emission inventory requirements. The facility meets the applicability requirements of 20.2.73.300 NMAC. The facility will meet all applicable reporting requirements under 20.2.73.300.B.1 NMAC.
20.2.74 NMAC	Permits – Prevention of Significant Deterioration (PSD)	No	Facility	This regulation establishes requirements for obtaining a prevention of significant deterioration permit. This facility is not a major source with respect to PSD and is therefore not subject to 20.2.74 NMAC.
20.2.75 NMAC	Construction Permit Fees	Yes	Facility	This regulation establishes a schedule of operating permit emission fees. This facility is subject to 20.2.72 NMAC and in turn subject to 20.2.75 NMAC. The facility is exempt from annual fees under this part (20.2.75.11.E NMAC) as it is subject to fees pursuant to 20.2.71 NMAC.

<u>State Regulation Citation</u>	Title	Applies? Enter Yes or No	Unit(s) or Facility	Justification: (You may delete instructions or statements that do not apply in the justification column to shorten the document.)
20.2.77 NMAC	New Source Performance	Yes	F-001, 2, 5, 6, 7, 8, 9, 10	This regulation establishes state authority to implement new source performance standards (NSPS) for stationary sources, as amended through January 15, 2017. F-001 applies as it is subject to NSPS OOOOa and units 2 and 5 are subject to NSPS GG. Units 6, 7, 8, 9, & 10 will be subject to JJJJ and OOOOb when the rule is promulgated.
20.2.78 NMAC	Emission Standards for HAPS	No	N/A	This regulation establishes state authority to implement emission standards for hazardous air pollutants subject to 40 CFR Part 61. This facility does not emit hazardous air pollutants which are subject to the requirements of 40 CFR Part 61 and is therefore not subject to this regulation.
20.2.79 NMAC	Permits – Nonattainment Areas	No	Facility	This regulation establishes the requirements for obtaining a nonattainment area permit. The facility is not located in a non-attainment area and therefore is not subject to this regulation.
20.2.80 NMAC	Stack Heights	No	N/A	This regulation establishes requirements for the evaluation of stack heights and other dispersion techniques. This regulation does not apply, as all stacks at the facility will follow good engineering practice.
20.2.82 NMAC	MACT Standards for source categories of HAPS	Yes	3a, 6, 7, 8, 9, 10	The glycol dehydrator at this facility is Subject to the requirements of 40 CFR 63 Subpart HH. Also, the engines 6, 7, 8, 9, & 10 are subject to Subpart ZZZZ. Therefore, this regulation applies.

Table for Applicable Federal Regulations:

<u>Federal Regulation Citation</u>	Title	Applies? Enter Yes or No	Unit(s) or Facility	Justification:
40 CFR 50	NAAQS	Yes	Facility	This regulation defines national ambient air quality standards. The facility meets all applicable national ambient air quality standards for NO _x , CO, SO ₂ , H ₂ S, PM ₁₀ , and PM _{2.5} under this regulation.
NSPS 40 CFR 60, Subpart A	General Provisions	Yes	2, 5, 6, 7, 8, 9, 10, F-001	This regulation defines general provisions for relevant standards that have been set under this part. The facility is subject to this regulation because the following subparts apply: - Units 1, 2 & 5 are subject to NSPS GG. - Unit F-001 is subject to the leak detection requirements of NSPS OOOOa. - Units 6, 7, 8, 9, & 10 is subject to JJJJ and will be subject to NSPS OOOOb.
NSPS 40 CFR60.40a, Subpart Da	Subpart Da, Performance Standards for Electric Utility Steam Generating Units	No	N/A	This regulation establishes standards of performance for fossil-fuel-fired steam generators. This regulation does not apply as the facility does not have any fossil-fuel-fired steam generating units with a heat input rate of 250 MMBtu/hr [60.40(a)(1)].
NSPS 40 CFR60.40b Subpart Db	Electric Utility Steam Generating Units	No	N/A	This regulation establishes standards of performance for electric utility steam generating units. This regulation does not apply because the facility does not operate any electric utility steam generating units.

Federal Regulation Citation	Title	Applies? Enter Yes or No	Unit(s) or Facility	Justification:
40 CFR 60.40c, Subpart Dc	Standards of Performance for Small Industrial-Commercial-Institutional Steam Generating Units	No	N/A	This regulation does not apply as the facility does not have any steam generating units.
NSPS 40 CFR 60, Subpart Ka	Standards of Performance for Storage Vessels for Petroleum Liquids for which Construction, Reconstruction, or Modification Commenced After May 18, 1978, and Prior to July 23, 1984	No	N/A	This regulation establishes performance standards for storage vessels for petroleum liquids for which construction, reconstruction, or modification commenced after May 18, 1978, and prior to July 23, 1984. The tanks at the facility, which are regulated emission sources, are 300 bbl (12,600 gallons) and 210 bbl (8,820 gallons). The capacities of the tanks at the facility are less than 40,000 gallons and are not subject to this regulation. [40 CFR Part 60.110a(a)]
NSPS 40 CFR 60, Subpart Kb	Standards of Performance for Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels) for Which Construction, Reconstruction, or Modification Commenced After July 23, 1984	No	N/A	This regulation establishes performance standards for volatile organic liquid storage vessels (including petroleum liquid storage vessels) for which construction, reconstruction, or modification commenced after July 23, 1984. This facility does not have any storage vessels with a capacity greater than or equal to 75 cubic meters that were constructed, reconstructed or modified after July 23, 1984. This regulation is not applicable.
NSPS 40 CFR 60.330 Subpart GG	Stationary Gas Turbines	Yes	1, 2 & 5	This regulation establishes standards of performance for stationary gas turbines with a heat input of 10 MMBtu/hr or greater. Units 1, 2 & 5 each have heat inputs of 35.3 MMBtu/hour and commenced construction after October 3, 1977. Accordingly, these units are subject to this regulation. [60.330(b)]
NSPS 40 CFR 60, Subpart KKK	Leaks of VOC from Onshore Gas Plants	No	N/A	This regulation defines standards of performance for equipment leaks of VOC emissions from onshore natural gas processing plants for which construction, reconstruction, or modification commenced after January 20, 1984, and on or before August 23, 2011. The facility is not subject to this regulation because the operations performed at this site are no longer consistent to those carried out at an onshore natural gas processing plant. The removal of the dew point plant ensured that the facility is no longer subject to this regulation.
NSPS 40 CFR Part 60 Subpart LLL	Standards of Performance for Onshore Natural Gas Processing: SO₂ Emissions	No	N/A	This regulation establishes standards of performance for SO ₂ emissions from onshore natural gas processing for which construction, reconstruction, or modification of the amine sweetening unit commenced after January 20, 1984 and on or before August 23, 2011. This regulation is not applicable as the amine sweetening unit (Unit 4a) commenced construction after August 23, 2011.
NSPS 40 CFR Part 60 Subpart OOOO	Standards of Performance for Crude Oil and Natural Gas Production, Transmission, and Distribution for which	No	N/A	This regulation establishes standards of performance for crude oil and natural gas production, transmission, and distribution. Because the dew point plant is being removed this change the facility to be a compressor station; therefore, this regulation does not apply. Facility fugitive emissions are not subject to the leak detection requirements of this regulation. Compressors associated with units 1, 2, 5, and unit EC-1 were manufactured prior to August 23, 2011. Relocation does not constitute a modification; therefore, compressors associated with units 1,2,5 and unit EC-1 are not subject to this regulation. Unit T- 006 is an existing exempt

Federal Regulation Citation	Title	Applies? Enter Yes or No	Unit(s) or Facility	Justification:
	construction, modification or reconstruction commenced after August 23, 2011 and before September 18, 2015			tank. This unit was constructed prior to 8/23/2011 and is not subject to this regulation T-008 through T-012 are also constructed prior to 8/23/2011 and are not subject to this regulation.
NSPS 40 CFR Part 60 Subpart OOOOa	Standards of Performance for Crude Oil and Natural Gas Facilities for which Construction, Modification or Reconstruction Commenced After September 18, 2015	Yes	F-001	This regulation establishes standards of performance for crude oil and natural gas production, transmission, and distribution. As this facility is a compressor station, fugitive emissions (F-001) are subject to the leak detection requirements of this regulation. Compressors associated with units 1, 2, 5, and unit EC-1 were manufactured prior to August 23, 2011 and prior to September 18, 2015. Relocation does not constitute a modification; therefore, compressors associated with units 1, 2, 5, and EC-a are not subject to this regulation. Unit T-006 is an existing exempt tank. This unit was constructed prior to 8/23/2011 and is not subject to this regulation. Facility wide LDAR monitoring will be conducted by using optical gas imaging for the compressor station. T-008 through T-012 are also constructed prior to 8/23/2011 and prior to 9/18/2015 and are not subject to this regulation.
NSPS 40 CFR Part 60 Subpart OOOOb	Standards of Performance for Crude Oil and Natural Gas Facilities for which Construction, Modification or Reconstruction Commenced After November 15, 2021	Yes	6, 7, 8, 9 & 10	This regulation establishes standards of performance for crude oil and natural gas production, transmission, and distribution. As this facility is a compressor station, compressor engines will be subject to the requirements of this regulation. As this rule is not yet finalized, if approved, these units would be subject and will comply with all applicable requirements.
NSPS 40 CFR 60 Subpart IIII	Standards of performance for Stationary Compression Ignition Internal Combustion Engines	No	N/A	This regulation establishes standards of performance for stationary compression ignition internal combustion engines. This rule applies to IC engines (diesel engines) that commenced construction after July 11, 2005. This regulation does not apply, as there are no stationary compression ignition internal combustion engines at this facility.
NSPS 40 CFR Part 60 Subpart JJJJ	Standards of Performance for Stationary Spark Ignition Internal Combustion Engines	Yes	6, 7, 8, 9 & 10	This regulation establishes standards of performance for stationary spark ignition combustion engines. The site has a unit that is a portable non-road engine that will be at the facility for less than 12 months. In accordance with 40 CFR 60.4230(f), this unit is not subject to the requirements of this subpart. Units 6, 7, 8, 9, & 10 are subject to this regulation.
NSPS 40 CFR 60 Subpart TTTT	Standards of Performance for Greenhouse Gas Emissions for Electric Generating Units	No	N/A	This facility does not generate electricity; therefore, this regulation does not apply.
NSPS 40 CFR 60 Subpart UUUU	Emissions Guidelines for Greenhouse Gas Emissions and Compliance Times for Electric Utility Generating Units	No	N/A	This facility does not generate electricity; therefore, this regulation does not apply.

Federal Regulation Citation	Title	Applies? Enter Yes or No	Unit(s) or Facility	Justification:
NSPS 40 CFR 60, Subparts WWW, XXX, Cc, and Cf	Standards of performance for Municipal Solid Waste (MSW) Landfills	No	N/A	This facility is not a landfill; therefore, this regulation does not apply.
NESHAP 40 CFR 61 Subpart A	General Provisions	No	N/A	NSPS 40 CFR 61 does not apply to the facility because the facility does not emit or have the triggering substances on site and/or the facility is not involved in the triggering activity. The facility is not subject to this regulation. None of the subparts of Part 61 apply to the facility.
NESHAP 40 CFR 61 Subpart E	National Emission Standards for Mercury	No	N/A	The provisions of this subpart are applicable to those stationary sources which process mercury ore to recover mercury, use mercury chlor-alkali cells to produce chlorine gas and alkali metal hydroxide, and incinerate or dry wastewater treatment plant sludge. This facility does not process mercury ore, use mercury chlor-alkali cells, or incinerate or dry wastewater treatment plant sludge. Therefore, this facility is not subject to this regulation.
NESHAP 40 CFR 61 Subpart V	National Emission Standards for Equipment Leaks (Fugitive Emission Sources)	No	N/A	This regulation establishes national emission standards for equipment leaks (fugitive emission sources). The facility does not have equipment that operates in volatile hazardous air pollutant (VHAP) service [40 CFR Part 61.240]. The regulated activities subject to this regulation do not take place at this facility. The facility is not subject to this regulation.
MACT 40 CFR 63, Subpart A	General Provisions	Yes	3a, 6, 7, 8, 9, 10	This regulation defines general provisions for relevant standards that have been set under this part. The regulation applies to the glycol dehydrator and the engines 6, 7, 8, 9, & 10 that are subject to MACT ZZZZ and comply by following the requirements of NSPS JJJJ.
MACT 40 CFR 63.760 Subpart HH	Oil and Natural Gas Production Facilities	Yes	3a	This regulation establishes national emission standards for hazardous air pollutants from oil and natural gas production facilities. This facility is an Area Source of HAPs, therefore Unit 3 (200 MMscf/day Glycol Dehydrator) is subject to this regulation per 40 CFR 63.760(d)(2).
MACT 40 CFR 63 Subpart HHH	National Emission Standards for Hazardous Air Pollutants From Natural Gas Transmission and Storage Facilities	No	N/A	This regulation establishes national emission standards for hazardous air pollutants from boilers and heaters at major sources for HAPs. This facility is an area source for HAPs therefore this regulation does not apply. [63.1270(a)]. Additionally, this facility is not a natural gas transmission or storage facility, as defined by this regulation.
MACT 40 CFR 63 Subpart DDDDD	National Emission Standards for Hazardous Air Pollutants for Major Industrial, Commercial, and Institutional Boilers & Process Heaters	No	N/A	The facility does not have any heaters or boilers on site; therefore, this regulation does not apply.
MACT 40 CFR 63 Subpart UUUUU	National Emission Standards for Hazardous Air Pollutants Coal & Oil Fire Electric Utility Steam Generating Unit	No	N/A	This subpart establishes national emission limitations and work practice standards for hazardous air pollutants (HAP) emitted from coal- and oil-fired electric utility steam generating units (EGUs) as defined in §63.10042 of this subpart. This subpart also establishes requirements to demonstrate initial and continuous compliance with the emission limitations. This facility does not contain the affected units and is therefore not subject to this regulation.

Federal Regulation Citation	Title	Applies? Enter Yes or No	Unit(s) or Facility	Justification:
MACT 40 CFR 63 Subpart ZZZZ	National Emissions Standards for Hazardous Air Pollutants for Stationary Reciprocating Internal Combustion Engines (RICE MACT)	Yes	6, 7, 8, 9, 10	This regulation defines national emissions standards for HAPs from stationary reciprocating Internal Combustion Engines. Unit GEN-1 is a portable non-road engine that will be at the facility for less than 12 months. In accordance with 40 CFR 63.6585(a), this unit is not subject to the requirements of this regulation. The engines 6, 7, 8, 9, & 10 are subject to MACT ZZZZ and comply by following the requirements of NSPS JJJJ.
40 CFR 64	Compliance Assurance Monitoring	Yes	3a	The dehydrator (unit 3a) has uncontrolled VOC emission greater than 100 tpy. Unit 3a emissions are controlled by ECD. Thus, Unit 3a is subject to this regulation.
40 CFR 68	Chemical Accident Prevention	No	N/A	Enterprise has more than a threshold quantity of a regulated substance in a process, as determined under §68.115, and is therefore subject to this regulation. Enterprise complies by maintaining a Risk Management Plan.
Title IV – Acid Rain 40 CFR 72	Acid Rain	No	N/A	This part establishes the acid rain program. This facility is not an acid rain source. This regulation does not apply.
Title IV – Acid Rain 40 CFR 73	Sulfur Dioxide Allowance Emissions	No	N/A	This regulation establishes sulfur dioxide allowance emissions for certain types of facilities. This facility is not an acid rain source. This regulation does not apply.
Title IV-Acid Rain 40 CFR 75	Continuous Emissions Monitoring	No	N/A	This facility does not produce commercial electricity for sale; therefore, this regulation does not apply.
Title IV – Acid Rain 40 CFR 76	Acid Rain Nitrogen Oxides Emission Reduction Program	No	N/A	This regulation establishes an acid rain nitrogen oxides emission reduction program. This regulation applies to each coal-fired utility unit that is subject to an acid rain emissions limitation or reduction requirement for SO ₂ . This part does not apply because the facility does not operate any coal-fired units [40 CFR Part 76.1].
Title VI – 40 CFR 82	Protection of Stratospheric Ozone	No	N/A	Enterprise owns appliances containing CFCs and is therefore subject to this requirement. However, this requirement imposes no obligations on the facility beyond those imposed on any individual or corporate owner of such appliances, and is mentioned here only in the interest of being thorough. Enterprise uses only certified technicians for the maintenance, service, repair, and disposal of appliances and maintains the appropriate records for this requirement.

Section 14

Operational Plan to Mitigate Emissions

(Submitting under 20.2.70, 20.2.72, 20.2.74 NMAC)

- Title V Sources** (20.2.70 NMAC): By checking this box and certifying this application the permittee certifies that it has developed an **Operational Plan to Mitigate Emissions During Startups, Shutdowns, and Emergencies** defining the measures to be taken to mitigate source emissions during startups, shutdowns, and emergencies as required by 20.2.70.300.D.5(f) and (g) NMAC. This plan shall be kept on site to be made available to the Department upon request. This plan should not be submitted with this application.
- NSR** (20.2.72 NMAC), **PSD** (20.2.74 NMAC) **& Nonattainment** (20.2.79 NMAC) **Sources:** By checking this box and certifying this application the permittee certifies that it has developed an **Operational Plan to Mitigate Source Emissions During Malfunction, Startup, or Shutdown** defining the measures to be taken to mitigate source emissions during malfunction, startup, or shutdown as required by 20.2.72.203.A.5 NMAC. This plan shall be kept on site to be made available to the Department upon request. This plan should not be submitted with this application.
- Title V** (20.2.70 NMAC), **NSR** (20.2.72 NMAC), **PSD** (20.2.74 NMAC) **& Nonattainment** (20.2.79 NMAC) **Sources:** By checking this box and certifying this application the permittee certifies that it has established and implemented a Plan to Minimize Emissions During Routine or Predictable Startup, Shutdown, and Scheduled Maintenance through work practice standards and good air pollution control practices as required by 20.2.7.14.A and B NMAC. This plan shall be kept on site or at the nearest field office to be made available to the Department upon request. This plan should not be submitted with this application.
-

Startup and shutdown procedures are either based on manufacturer's recommendations or based on Enterprise's experience with specific equipment. These procedures are designed to proactively address the potential for malfunction to the greatest extent possible. These procedures dictate a sequence of operations that are designed to minimize emissions from the facility during events that result in shutdown and subsequent startup.

Equipment located at this facility is equipped with various safety devices and features that aid in the prevention of excess emissions in the event of an operational emergency. If an operational emergency does occur and excess emissions occur, Enterprise will submit the required Excess Emissions Report as per 20.2.7 NMAC. Corrective action to eliminate the excess emissions and prevent recurrence in the future will be undertaken as quickly as safety allows.

Section 15

Alternative Operating Scenarios

(Submitting under 20.2.70, 20.2.72, 20.2.74 NMAC)

Alternative Operating Scenarios: Provide all information required by the department to define alternative operating scenarios. This includes process, material and product changes; facility emissions information; air pollution control equipment requirements; any applicable requirements; monitoring, recordkeeping, and reporting requirements; and compliance certification requirements. Please ensure applicable Tables in this application are clearly marked to show alternative operating scenario.

Construction Scenarios: When a permit is modified authorizing new construction to an existing facility, NMED includes a condition to clearly address which permit condition(s) (from the previous permit and the new permit) govern during the interval between the date of issuance of the modification permit and the completion of construction of the modification(s). There are many possible variables that need to be addressed such as: Is simultaneous operation of the old and new units permitted and, if so for example, for how long and under what restraints? In general, these types of requirements will be addressed in Section A100 of the permit, but additional requirements may be added elsewhere. Look in A100 of our NSR and/or TV permit template for sample language dealing with these requirements. Find these permit templates at: www.env.nm.gov/air-quality/permitting-section-procedures-and-guidance/. Compliance with standards must be maintained during construction, which should not usually be a problem unless simultaneous operation of old and new equipment is requested.

In this section, under the bolded title "Construction Scenarios", specify any information necessary to write these conditions, such as: conservative-realistic estimated time for completion of construction of the various units, whether simultaneous operation of old and new units is being requested (and, if so, modeled), whether the old units will be removed or decommissioned, any PSD ramifications, any temporary limits requested during phased construction, whether any increase in emissions is being requested as SSM emissions or will instead be handled as a separate Construction Scenario (with corresponding emission limits and conditions, etc.

There are no alternative operating scenarios.

Section 17

Compliance Test History

(Submitting under 20.2.70, 20.2.72, 20.2.74 NMAC)

To show compliance with existing NSR permits conditions, you must submit a compliance test history. The table below provides an example.

Compliance Test History Table

Unit No.	Test Description	Test Date
1, 2	Tested for NO _x and CO as required by Title V Permit P118-R2	May 2008
1, 2	Tested for NO _x and CO as required by Title V Permit P118-R2	July 2009
1, 2	Tested for NO _x and CO as required by Title V Permit P118-R2	May 2010
1, 2	Tested for NO _x and CO as required by Title V Permit P118-R2	June 2011
1, 2	Tested for NO _x and CO as required by Title V Permit P118-R2	May 2012
1, 2	Tested for NO _x and CO as required by Title V Permit P118-R2	April 2013
1, 2	Tested for NO _x and CO as required by Title V Permit P118-R2	January 2014
1, 2	Tested for NO _x and CO as required by Title V Permit P118-R2	January 2018
2	Tested for NO _x and CO as required by Title V Permit P118-R2	April 2018
1	Tested for NO _x and CO as required by Title V Permit P118-R2	May 2018
1, 2	Tested for NO _x and CO as required by Title V Permit P118-R2	February 2019
1, 2	Tested for NO _x and CO as required by Title V Permit P118-R2	June 2019
1, 2	Tested for NO _x and CO as required by Title V Permit P118-R2	August 2019
1, 2	Tested for NO _x and CO as required by Title V Permit P118-R2	November 2019
1, 2	Tested for NO _x and CO as required by Title V Permit P118-R2	March 202
1, 2	Tested for NO _x and CO as required by Title V Permit P118-R2	May 2020
5	Tested for NO _x and CO as required by Title V Permit P118-R2	May 2021
5	Tested for NO _x and CO as required by Title V Permit P118-R2	July 2021
1, 2, 5	Tested for NO _x and CO as required by Title V Permit P118-R2	March 2022
1, 2, 5	Tested for NO _x and CO as required by Title V Permit P118-R2	June 2022
1, 2, 5	Tested for NO _x and CO as required by Title V Permit P118-R2	December 2022

Section 19

Requirements for Title V Program

Who Must Use this Attachment:

- * Any major source as defined in 20.2.70 NMAC.
 - * Any source, including an area source, subject to a standard or other requirement promulgated under Section 111 - Standards of Performance for New Stationary Sources, or Section 112 Hazardous Air Pollutants, of the 1990 federal Clean Air Act ("federal Act"). Non-major sources subject to Sections 111 or 112 of the federal Act are exempt from the obligation to obtain a 20.2.70 NMAC operating permit until such time that the EPA Administrator completes rulemakings that require such sources to obtain operating permits. In addition, sources that would be required to obtain an operating permit solely because they are subject to regulations or requirements under Section 112(r) of the federal Act are exempt from the requirement to obtain an Operating Permit.
 - * Any Acid Rain source as defined under title IV of the federal Act. The Acid Rain program has additional forms. See www.env.nm.gov/air-quality/air-quality-title-v-operating-permits-guidance-page/. Sources that are subject to both the Title V and Acid Rain regulations are encouraged to submit both applications simultaneously.
 - * Any source in a source category designated by the EPA Administrator ("Administrator"), in whole or in part, by regulation, after notice and comment.
-

19.1 - 40 CFR 64, Compliance Assurance Monitoring (CAM) (20.2.70.300.D.10.e NMAC)

Any source subject to 40CFR, Part 64 (Compliance Assurance Monitoring) must submit all the information required by section 64.7 with the operating permit application. The applicant must prepare a separate section of the application package for this purpose; if the information is already listed elsewhere in the application package, make reference to that location. Facilities not subject to Part 64 are invited to submit periodic monitoring protocols with the application to help the AQB to comply with 20.2.70 NMAC. Sources subject to 40 CFR Part 64, must submit a statement indicating your source's compliance status with any enhanced monitoring and compliance certification requirements of the federal Act.

This facility has a CAM Plan for the Glycol Dehydrator at the facility. A modified CAM Plan for the Glycol Dehydrator is attached following Section 19.

19.2 - Compliance Status (20.2.70.300.D.10.a & 10.b NMAC)

Describe the facility's compliance status with each applicable requirement at the time this permit application is submitted. This statement should include descriptions of or references to all methods used for determining compliance. This statement should include descriptions of monitoring, recordkeeping and reporting requirements and test methods used to determine compliance with all applicable requirements. Refer to Section 2, Tables 2-N and 2-O of the Application Form as necessary. (20.2.70.300.D.11 NMAC) For facilities with existing Title V permits, refer to most recent Compliance Certification for existing requirements. Address new requirements such as CAM, here, including steps being taken to achieve compliance.

Enterprise believes that the South Carlsbad Compressor Station complies with each applicable state and federal regulation identified in Section 13 (Determination of State & Federal Air Quality Regulations). In the event that Enterprise discovers new information affecting the compliance status of the facility, Enterprise will make appropriate notifications and/or take corrective actions to maintain the required compliance.

19.3 - Continued Compliance (20.2.70.300.D.10.c NMAC)

Provide a statement that your facility will continue to be in compliance with requirements for which it is in compliance at the time of permit application. This statement must also include a commitment to comply with other applicable requirements as they come into effect during the permit term. This compliance must occur in a timely manner or be consistent with such schedule expressly required by the applicable requirement.

As described in Section 19.2 Enterprise states that South Carlsbad Compressor Station will continue to be operated in compliance with applicable requirements for which it is in compliance as of the date of submittal of this application.

In addition, Enterprise will meet additional applicable requirements that become effective during the permit term in a timely manner or on such a time schedule as expressly required by the applicable requirement. In the event that Enterprise should discover new information affecting the compliance status of the South Carlsbad Compressor Station, Enterprise will make appropriate notifications and/or take corrective actions as appropriate.

19.4 - Schedule for Submission of Compliance (20.2.70.300.D.10.d NMAC)

You must provide a proposed schedule for submission to the department of compliance certifications during the permit term. This certification must be submitted annually unless the applicable requirement or the department specifies a more frequent period. A sample form for these certifications will be attached to the permit.

Compliance certification will be submitted annually as required by NMAC 20.2.70.300.D.10.d.

19.5 - Stratospheric Ozone and Climate Protection

In addition to completing the four (4) questions below, you must submit a statement indicating your source's compliance status with requirements of Title VI, Section 608 (National Recycling and Emissions Reduction Program) and Section 609 (Servicing of Motor Vehicle Air Conditioners).

1. Does your facility have any air conditioners or refrigeration equipment that uses CFCs, HCFCs or other ozone-depleting substances? Yes No
 2. Does any air conditioner(s) or any piece(s) of refrigeration equipment contain a refrigeration charge greater than 50 lbs? Yes No
(If the answer is yes, describe the type of equipment and how many units are at the facility.)
 3. Do your facility personnel maintain, service, repair, or dispose of any motor vehicle air conditioners (MVACs) or appliances ("appliance" and "MVAC" as defined at 82. 152)? Yes No
 4. Cite and describe which Title VI requirements are applicable to your facility (i.e. 40 CFR Part 82, Subpart A through G.)
-

Enterprise does not service, maintain, repair, or dispose of appliances that use Class I or Class II chemicals (chlorofluorocarbons, halon, carbon tetrachloride, methyl chloroform or hydrochlorofluorocarbon) and that motor vehicle air conditioners are not serviced at the Red Raider Compressor Station. Therefore, the requirements of Title VI, Sections 608 and 609 of the Clean Air Act are not applicable to the Red Raider Compressor Station.

19.6 - Compliance Plan and Schedule

Applications for sources, which are not in compliance with all applicable requirements at the time the permit application is submitted to the department, must include a proposed compliance plan as part of the permit application package. This plan shall include the information requested below:

A. Description of Compliance Status: (20.2.70.300.D.11.a NMAC)

A narrative description of your facility's compliance status with respect to all applicable requirements (as defined in 20.2.70 NMAC) at the time this permit application is submitted to the department.

B. Compliance plan: (20.2.70.300.D.11.B NMAC)

A narrative description of the means by which your facility will achieve compliance with applicable requirements with which it is not in compliance at the time you submit your permit application package.

C. Compliance schedule: (20.2.70.300D.11.c NMAC)

A schedule of remedial measures that you plan to take, including an enforceable sequence of actions with milestones, which will lead to compliance with all applicable requirements for your source. This schedule of compliance must be at least as stringent as that contained in any consent decree or administrative order to which your source is subject. The obligations of any consent decree or administrative order are not in any way diminished by the schedule of compliance.

D. Schedule of Certified Progress Reports: (20.2.70.300.D.11.d NMAC)

A proposed schedule for submission to the department of certified progress reports must also be included in the compliance schedule. The proposed schedule must call for these reports to be submitted at least every six (6) months.

E. Acid Rain Sources: (20.2.70.300.D.11.e NMAC)

If your source is an acid rain source as defined by EPA, the following applies to you. For the portion of your acid rain source subject to the acid rain provisions of title IV of the federal Act, the compliance plan must also include any additional requirements under the acid rain provisions of title IV of the federal Act. Some requirements of title IV regarding the schedule and methods the source will use to achieve compliance with the acid rain emissions limitations may supersede the requirements of title V and 20.2.70 NMAC. You will need to consult with the Air Quality Bureau permitting staff concerning how to properly meet this requirement.

NOTE: The Acid Rain program has additional forms. See www.env.nm.gov/air-quality/air-quality-title-v-operating-permits-guidance-page/. Sources that are subject to both the Title V and Acid Rain regulations are **encouraged** to submit both applications **simultaneously**.

Based on information and belief formed after reasonable inquiry and as described in Section 19.2, and with this filing, Enterprise states that South Carlsbad Compressor Station is in compliance with applicable requirements. No compliance plan, compliance schedule, or compliance reports are required. In addition, based on information and belief formed after reasonable inquiry Enterprise states that South Carlsbad Compressor Station is not an acid rain source as defined at 40 CFR 72.6.

19.7 - 112(r) Risk Management Plan (RMP)

Any major sources subject to section 112(r) of the Clean Air Act must list all substances that cause the source to be subject to section 112(r) in the application. The permittee must state when the RMP was submitted to and approved by EPA.

Any major sources subject to section 112(r) of the Clean Air Act must list all substances that cause the source to be subject to section 112(r) in the application. The permittee must state when the RMP was submitted to and approved by EPA.

19.8 - Distance to Other States, Bernalillo, Indian Tribes and Pueblos

Will the property on which the facility is proposed to be constructed or operated be closer than 80 km (50 miles) from other states, local pollution control programs, and Indian tribes and pueblos (20.2.70.402.A.2 and 20.2.70.7.B NMAC)?

(If the answer is yes, state which apply and provide the distances.)

Texas – 34.7 km; No Tribes or pueblos or local pollution control programs within 80 km.

19.9 - Responsible Official

Provide the Responsible Official as defined in 20.2.70.7.AD NMAC:

Responsible Official: Graham Bacon

R.O. Title: Executive Vice President-EHS&T

R.O. Address: PO Box 4324, Houston TX 77210-4324

Phone: (713) 381-6595

R.O. email: environmental@eprod.com

Enterprise Products Operating LLC – South Carlsbad Compressor Station

COMPLIANCE ASSURANCE MONITORING PLAN FOR GLYCOL DEHYDRATOR

I. Background

A. Emissions Unit

Description: Glycol Dehydrator (Still Vent & Flash Tank)

Identification: 3a

Facility: South Carlsbad Compressor Station

B. Applicable Regulation, Emission Limit, and Pre-CAM Monitoring Requirements

Regulation: Operation and reporting requirements created in NSR Permit 0220-M12 et seq; 40 CFR 60 Subpart HH.

Emission limits: Uncontrolled – VOC: 322.57 tpy

HAPs: 84.9 tpy

Controlled – VOC: 0.00 tpy

HAPs: 0.00 tpy

C. Control Technology, Capture System, Bypass, PER

Controls: Enclosed Combustion Device

Capture System: Enclosed Combustion Device

Potential pre-control device emissions: 322.57 tpy VOC, 84.9 tpy HAP, 0.18 tpy H₂S.
Under 40 CFR §64.2(a) this is a CAM affected unit.

Potential post-control device emissions: 0.0 tpy VOC, 0.0 tpy HAP, 0.0 tpy H₂S. The ECD will control the flash tank and BTEX still vent vapors of the glycol dehydrator (Unit 3a). The ECD will be used as a primary controller for the dehydrator flash tank. When gas is not sent to the ECD, it will be used as fuel for the reboiler. The ECD destruction removal efficiency (DRE) is 98%.

II. Monitoring Approach

The key elements of the monitoring approach are presented in the attached table.

III. Response to Excursion

Per 40 CFR §64.1, excursion is defined as “a departure from an indicator range established for monitoring under this part, consistent with any averaging period specified for averaging the results of the monitoring.” Excursions of the enclosed combustion device will trigger an inspection, corrective action, and reporting.

Monitoring Approach: South Carlsbad Compressor Station (ECD-1)

	Indicator No. 1	Indicator No. 2
I. Indicator	Proper equipment operation	Glycol pump recirculation rate
Measurement Approach	Semi-annual inspections shall demonstrate compliance with allowable emission limits.	Monitoring the circulation rate shall demonstrate compliance with allowable emission limits.
II. Indicator Range	All equipment is operating in accordance with site-specific operation and maintenance plan or there is a deficiency.	The glycol pump circulation rate shall not exceed 50 gallons per minute.
III. Performance Criteria	Compliance with allowable emissions is assumed if the glycol dehydrator, control equipment, reboiler, and all associated equipment are operating in accordance with the site-specific operation and maintenance plan.	Compliance with allowable emission limits is assumed if the glycol pump is operated according to and within the limits of the emissions calculations included in the permit application.
A. Data Representativeness		
B. QA/QC Practices and Criteria	Dehydrator still vent (regenerator) shall be routed via hard piping to a condenser that meets heat dissipation of 7.66E-1 MMBtu/hr. Non-condensable gases from the condenser and flash gases shall be routed via hard piping to the enclosed combustion device (unit ECD). Inspection of the glycol dehydrator, control equipment, and the reboiler.	The permittee shall operate and maintain the glycol pump and associated equipment in accordance with the manufacturer recommended procedure or site-specific operation and maintenance plan. Inspection of the pump rate setting.
C. Monitoring Frequency	Inspection shall be performed semi-annually.	Inspection shall be performed quarterly.
D. Data Collection Procedures	Records shall be kept of the person conducting the inspection, the results of all equipment inspections, and any maintenance or repairs needed to bring the equipment into compliance.	Records shall be kept of the circulation rate, name of the person monitoring the circulation rate, the date and time of the readings, and records of any required adjustments, calibration, or any maintenance or repairs. Deficiencies identified, resultant repairs or maintenance performed, and dates of actions taken shall be recorded.
E. Averaging Period	Not applicable	Not applicable

Monitoring Approach (Continued)

	Indicator No. 3	Indicator No. 4
I. Indicator	Glycol dehydrator gas flow rate	Dehydrator inlet gas analysis
Measurement Approach	Monitoring the flow rate of gas to the glycol dehydrator shall demonstrate compliance with allowable emission limits.	Perform an extended analysis on the dehydrator inlet gas and complete emissions calculations to comply with allowable emission limits.
II. Indicator Range	The flow rate of gas to the glycol dehydrator shall not exceed 200 MMscf/day.	A GRI-GLYCalc analysis shall be performed and emissions compared with allowable emission limits.
III. Performance Criteria	Compliance with allowable emission limits is assumed if the flow rate of gas to the glycol dehydrator is within the limits of the emissions calculations included in the permit application.	Compliance with allowable emission limits will be determined based on the extended gas analysis and GRI-GLYCalc analysis.
A. Data Representativeness		
B. QA/QC Practices and Criteria	A gas flow meter equipped with a chart recorder or data logger shall be installed to monitor gas flow to the dehydrator. The flow meter shall be operated, calibrated, and maintained as specified by the manufacturer or equivalent site-specific operation and maintenance plan and as necessary to ensure correct and accurate readings.	Comparison of calculated actual emission rate and allowable emission limits.
C. Monitoring Frequency	Total flow rate shall be recorded daily.	Extended gas analysis shall be conducted annually.
D. Data Collection Procedures	Records shall be kept for flow meter certifications, calibrations, breakdowns, reasons for breakdown, and corrective actions.	Records shall be maintained of laboratory sample documentation; all parameters used in the emission calculation; detailed calculation results; actual controlled emission rates; and the most current emission factors for NO _x and CO.
E. Averaging Period	Not applicable	Not applicable.

Monitoring Approach (Continued)

	Indicator No. 5	Indicator No. 6
I. Indicator	Condenser temperature indicator	ECD adequate combustion
Measurement Approach	A deviation from expected operating conditions shall be monitored by an alarm if the condenser temperature goes outside of ideal conditions.	Adequate combustion shall be monitored by a thermocouple with alarm that signals non-combustion of gas.
II. Indicator Range	No alarm or alarm.	No alarm or alarm.
III. Performance Criteria	Compliance with allowable emission limits is assumed if the condenser is operating according to manufacturer recommendations.	Compliance with allowable emission limits is assumed if the ECD is operating according to manufacturer recommendations.
A. Data Representativeness		
B. QA/QC Practices and Criteria	Proper operation of the condenser is achieved by maintaining the alarm system.	Proper operation of the flare is achieved by maintaining the non-combustion thermocouple with an alarm system. Operators will record the date and result of each such maintenance activity, as well as repairs or replacements made.
C. Monitoring Frequency	The alarm will be tested annually.	The thermocouple and alarm system will be tested twice a year by turning off the thermocouples and recording the time required for the alarm to respond.
D. Data Collection Procedures	Records shall be maintained of annual testing.	Records shall be maintained of ECD shutdown for any reason, including failure to deliver fuel, and of inspection and maintenance to the flare.
E. Averaging Period	Annually	Semi-Annually

Section 20

Other Relevant Information

Other relevant information. Use this attachment to clarify any part in the application that you think needs explaining. Reference the section, table, column, and/or field. Include any additional text, tables, calculations or clarifying information.

Additionally, the applicant may propose specific permit language for AQB consideration. In the case of a revision to an existing permit, the applicant should provide the old language and the new language in track changes format to highlight the proposed changes. If proposing language for a new facility or language for a new unit, submit the proposed operating condition(s), along with the associated monitoring, recordkeeping, and reporting conditions. In either case, please limit the proposed language to the affected portion of the permit.

No other relevant information is being submitted as part of this application.

Section 22: Certification

Company Name: Enterprise Field Services, LLC

I, Bradley J. Cooley, hereby certify that the information and data submitted in this application are true and as accurate as possible, to the best of my knowledge and professional expertise and experience.

Signed this ___ day of _____, _____, upon my oath or affirmation, before a notary of the State of _____.

_____.

*Signature

Date

Bradley J. Cooley
Printed Name

Senior Director
Title

Scribed and sworn before me on this ___ day of _____, _____.

My authorization as a notary of the State of _____ expires on the

_____ day of _____, _____.

Notary's Signature

Date

Notary's Printed Name

*For Title V applications, the signature must be of the Responsible Official as defined in 20.2.70.7.AE NMAC.