

ABBREVIATIONS

English

ac-ft. = acre-foot or acre-feet

b = base (of right triangle)

°C = degrees Celsius

cfs or $ft^3/sec = cubic feet per$

second

 $cfm \text{ or } ft^3/min = cubic \text{ feet per}$

minute

 $cfd \text{ or } ft^3/day = \text{cubic feet per}$

day

D = diameter (circle)

°F = degrees Fahrenheit

fps or ft./sec = feet per second

 $\mathbf{ft.} = \mathbf{feet}$

 ft^2 or sq. ft. = square feet

 ft^3 or cu. ft. = cubic feet

gpd = gallons per day

gpg = grains per gallon

gpm = gallons per minute

gps = gallons per second

 $\mathbf{h} = \text{height}$

hp = horsepower

hr = hour

hrs/day = hours per day

in = inches

 in^2 = square inches

in³ = cubic incheslbs. = pounds

Γ -

mi = miles

min = minute

MG = million gallons

mgd or MGD = million gallons

per day

oz = ounces

ppb = parts per billion

ppm = parts per million

ppt = parts per trillion

psi = pounds per square inch

 $\mathbf{Q} = \text{flow}$

 $\mathbf{r} = \text{radius (circle)}$

sec = second

 $\mathbf{V} = \text{volume}$

 $\mathbf{W} = \text{watts}$

<u>Metric</u>

cm = centimeters

g = gram

Ha = Hectare

kg = kilogram

km = kilometer

kW = kilowatt

L or 1 = liters

 $\mathbf{m} = \text{meter}$

 m^3 = cubic meter

mg = milligram

mg/L or mg/l = milligrams per

liter

mL = ml or milliliter

mm = millimeter

CONVERSION FACTORS

LENGTH

English

1 foot = 12 in.

1 foot = 0.305 m

1 inch = 2.54 cm

1 mile = 5,280 ft.

1 mile = 1.609 km

1 yard = 3 ft.

Metrio

1 centimeter = 0.3937 in.

1 kilometer = 0.6214 mi.

1 meter = 39.37 in.

AREA

<u>Metric</u>

1 Hectare = 2.47 acres

English

1 acre (ac) = $43,560 \text{ ft}^2$

1 acre = 0.405 Hectare (Ha)

 $1 \text{ ft}^2 = 144 \text{ in}^2$

 $1 \text{ in}^2 = 6.45 \text{ cm}^2$

 $1\text{yd}^2 = 9 \text{ ft}^2$



English

1 acre-ft. = 325,828.8 gallons

1 acre-ft. = $43,560 \text{ ft}^3$

1 cfs = 0.646 MGD

1 ft 3 = 7.48 gallons

1 ft 3 = 1,728 in 3

 $1 \text{ gallon} = 231 \text{ in}^3$

1 gallon = 0.1337 ft^3

1 gallon = 0.000001 MG

1 gallon = 3.785 liter

1 gallon = 3,785 mL

 $1yd^3 = 27 \text{ ft}^3$

VOLUME

Metric

1 liter = 1,000 mL

1 liter = 0.2642 gallons

 $1 \text{ m}^3 = 264.2 \text{ gallons}$

 $1 \text{ m}^3 = 35.315 \text{ ft}^3$

FLOW

 $1 \text{ ft}^3/\text{sec} = 646,300 \text{ gpd}$

 $1 \text{ ft}^3/\text{sec} = 0.6463 \text{ MGD}$

 $1 \text{ ft}^3/\text{sec} = 448.8 \text{ gpm}$

1 gpm = 0.00144 MGD

1 MGD = 694.4 gpm

1 MGD = 1.545 cfs

1 MGD = 3.07 acre-ft/day

WEIGHT & MASS

English

1 ft 3 water = 62.4 lbs.

1 gallon water = 8.34 lbs.

1 gpg = 17.118 mg/L

1 lb. = 16 oz

1 lb. = 7,000 grains

1 lb. = 453.6 g

1 lb. = 0.4536 kg

1 ton = 2,000 lbs.

Metric

1 g = 1,000 mg

1 kg = 1,000 g

1 kg = 2.2 lbs.

1 mg/L = 0.0584 gpg

1% = 10,000 mg/L

DOSAGE

1% = 10,000 mg/L

1 gpg = 17.1 ppm

1 ppm = 1 mg/L

1 ppm = 8.34 lbs. per million gal

PRESSURE

1 ft. water = 0.433 psi

1 psi = 2.31 ft. water

POWER

1 hp = 0.746 kW

1 hp = 746 W

1 hp = 550 ft-lb/sec

1 hp = 33,000 ft-lbs/min

1 kW = 1.34 hp

TIME

 $1 \min = 60 \sec$

1 hr. = 60 min

1 day = 24 hrs

1 day = 1,440 min



FORMULAS

For the operator's convenience, both equation formulas and pie wheel formulas are included in this document. When using the pie wheel formula to solve a problem, multiply together the pie wedges below the horizontal line to solve for the quantity above the horizontal line. To solve for one of the pie wedges below the horizontal line, cover the pie wedge for which you are solving and divide the remaining pie wedge(s) below the horizontal line into the quantity above the horizontal line.

Area Formulas

Circle = $(0.785) \times (D^2)$ Where:

Circle = area of circle

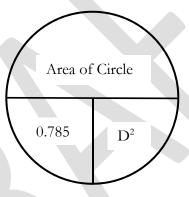
D = diameter of circle

Circle = $(\pi) \times (r^2)$

Where:

Circle = area of circle r = radius of circle

 $\pi = 3.1416$



Cone (lateral area) = $(\pi) \times (r) \times (\sqrt{r^2 + h^2})$

Where:

 $\pi = 3.1416$

r = radius of circle

h = height of cone

Cone (area) = $[(b) \times (h)]/2$

Where:

b = circumference

h = height

Cone (surface area) = $(\pi) \times (r) \times (r + \sqrt{r^2 + h^2})$

Where:

 $\pi = 3.1416$

r = radius of circle

h = height of cone



Sphere (area) = $(\pi) \times (D^2)$ or

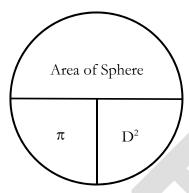
Sphere (area) = $4 \times (\pi) \times (r^2)$ or

Where:

 $\pi = 3.1416$

r = radius of circle

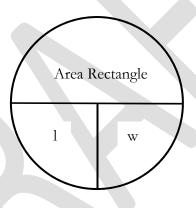
D = diameter of circle



Rectangle = (l) x (w)

Where:

l = length of rectangle w = width of rectangle

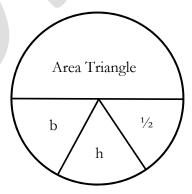


Triangle (area) = $[(b) \times (h)]/2$

Where:

b = base of triangle

h = height of triangle



Circumference = $(\pi) \times (D)$ Where: $\pi = 3.1416$

D = diameter of circle

Circumference = (2) \times (π) \times (τ) Where: π = 3.1416

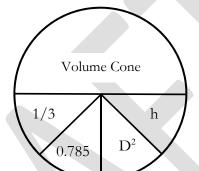
r = radius of circle

Volume Formulas

Cone =
$$(1/3) \times (0.785) \times (D^2) \times (h)$$

Where:

D = diameter of cone h = height of cone



Where:

 $\pi = 3.1416$

.

r = radius of cone h = height of cone

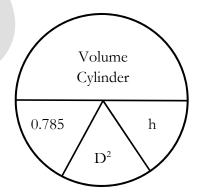
Cylinder = $(0.785) \times (d^2) \times (h)$

Cone = $1/3 \times [(\pi) \times (r^2) \times (h)]$

Where:

D = diameter of cylinder

h = length of cylinder





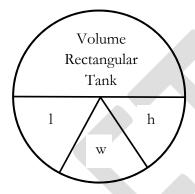
Where: $\pi = 3.1416$ Cylinder = $(\pi) \times (r^2) \times (h)$ r = radius constant of the constant of th

r = radius of cylinder h = length of cylinder

Where: l = length of tank

w = width of tank

h = height of tank



Flow Formulas

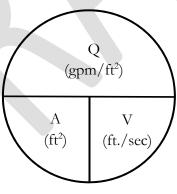
 $Q = (A) \times (V)$

Rectangular Tank = (l) \times (w) \times (h)

 $Q = flow (ft^3/sec)$

 $A = cross-section area (ft^2)$

V = water velocity (ft./sec)



Where: $Q = flow in channel (ft^3/sec)$

w = width (ft.)

d = depth (ft.)

V = velocity (ft./sec)

Where: $Q = flow in full pipe (ft^3/sec)$

D = diameter (ft.)

V = velocity (ft./sec)

 $Q = (w) \times (d) \times (V)$



Where: $Q = \text{flow in partially full pipe (ft}^3/\text{sec})$ $Q = \{1.333 \text{ x (h)}^2 \text{ x} / \sqrt{(D/h) - 0.608} \} \text{ x (V)}$ h = height (ft.)D = diameter (ft.)V = velocity (ft./sec)See also **Appendix A: Flow Through a Partially Full Pipe** (table) Where: V = velocity (ft./sec) $V = (Q) / \{(0.785) \times (D)^2\}$ $Q = flow (ft^3/sec)$ D = diameter (ft.)Where: V = velocity (ft./sec)d = distance (ft.) V = (d)/(T)T = time (sec)Q = avg. daily flow (MGD)Where: $Q = (\sum_{Q \text{ daily}})/(n_{\text{daily}})$ $\sum_{\text{Q daily}} = \text{sum all daily flows (MGD)}$ $n_{daily} = number of daily flows$ Where: Q = avg. daily flow (MGD) $\sum_{Q \text{ monthly}} = \text{sum all monthly avg. daily}$ $Q = (\sum_{Q \text{ monthly}})/(n_{\text{monthly}})$ flows (MGD) $n_{monthly} = number of monthly avg. daily$ flows Where: Q = daily flow (gal/capita/day)Q = (Water used)/(Population)water used or produced = gal/daypopulation = total # people served Where: overflow rate = weir overflow rate Overflow rate = (Q)/(L)(gpd/ft.) Q = flow (gpd)L = weir length (ft.)**Dosage Formulas** Where: dosage = mg/LDosage = <u>Feed rate</u>. feed rate = chemical feed rate (lbs./day) Q = flow rate (MGD)

(Q) x (8.34 lbs./gal)



Where: dosage = mg/Lfeed rate = chemical feed rate (lbs./day) Dosage = $\underline{\text{(Feed rate)}} \times \underline{\text{(Purity)}}$ purity = chemical purity, % expressed as (Q) x (8.34 lbs./gal) decimal Q = flow rate (gal/min.)Where: dosage = mg/LDosage = (Feed rate) \times (1,000 mg/g) feed rate = chemical feed rate (lbs./day) (Q) \times (3.785 L/gal) Q = flow rate (gal/min.)Dose = Demand + ResidualChemical Feed/Feed Rate Formulas (aka pounds) Where: chemical fee = lbs. d = dose (mg/L)Chemical feed = (d) \times (V) \times (8.34 lbs./gal) V = volume (MG)Where: chemical fee = lbs. d = dose (mg/L)Chemical feed = $(d) \times (V) \times (8.34 \text{ lbs./gal})$ V = volume (MG)Chemical purity Chemical purity = %, expressed as decimal Where: feed rate = lbs./dayd = dose (mg/L)Feed rate = (d) \times (Q) \times (8.34 lbs./gal) Q = flow (MGD)Where: feed rate = lbs./dayd = dose (mg/L)Feed rate = $(\underline{d}) \times (\underline{Q}) \times 8.34 \, \text{lbs./gal}$ Q = flow (MGD)Chemical Purity Chemical purity = %, expressed as decimal Feed Rate (lbs./day) [100% purity] 8.34 Flow lbs./gal (MGD) Dose (mg/L)



Where: feed rate = lbs./dayFeed rate = $(C) \times (V) \times (1,440 \text{ min/day})$. C = concentration (mg/mL)(T) x (1,000 mg/g) x (453.6 g/lb.) V = volume pumped (mL)T = time pumped (min.)Chemical Feed Pump Formulas Where: chemical feed stroke, expressed as % Chemical Feed Stroke = $(Q_d/Q_m) \times 100\%$ Q_d = desired flow $Q_m = maximum flow$ Feed pump rate = $(Q) \times (d) \times (3.785 \text{ L/gal}) \times (1,000,000 \text{ gal/MG})$ (L) x (24 hr./day) x (60 min/hr.) Where: feed pump rate =mL/min Q = flow (MDG)d = dose (mg/L)L = liquid (mg/mL)Power Formulas Where: AC = AC circuit V = volts $AC circuit = V \times A \times PF$ A = ampsPF = power factor $Amps (A) = \underline{V}$ Where: A = ampsV = voltsO = ohms.-.-.-.-.-.-.-. Where: Amps is single phase hp = horsepower $Amps = \underline{(746 \text{ watts/hp}) \times (hp)}.$ $\hat{V} = \text{volts}$ (V) x (Eff) x (Pf) Eff = efficiency (%, as decimal) Pf = power factor...... Where: Amps is three-phase hp = horsepower $Amps = (746 \text{ watts/hp}) \times (hp)$ $\hat{V} = \text{volts}$ (1.732) **x** (V) **x** (Eff) **x** (Pf) Eff = efficiency (%, as decimal)

Pf = power factor



 $Watts = V \times A$

Where: Watts = DC or AC circuit

V = voltsA = amps

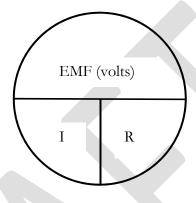
Electromotive Force (EMF) = $I \times R$

Where: (volts)

EMF = electromotive force

I = current (amps)

R = resistance (ohms)



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PUMPS

Pumping Formulas

Pumping Rate = V/T

Where:

pumping rate in gal/min

V = volume (gal.)

T = time (min.)

Where:

pumping rate in gal/min

L = length (ft.)

Pumping Rate = $L \times W \times D \times 7.48 \text{ gal/ft}^3$

Т

W = width (ft.)

D = depth (ft.)

T = time (min.)

Where:

pumping rate in gal/min

d = diameter (ft.) D = depth (ft.)

T = time (min.)

Time to Fill = $\underline{\text{Tank volume}}$

Flow Rate

Pumping Rate = $0.785 \times d^2 \times D \times 7.48 \text{ gal/ft}^3$

Where:

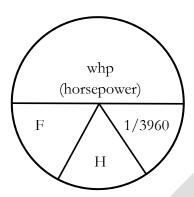
time to fill in min. tank volume in gal.

flow rate in gal/min.



Horsepower, Motor & Pump Efficiency





Where:

whp = water horsepower

F = flow (gpm)

H = head (ft.)

$$bhp = \frac{F \times H}{3,960 \times PE}$$

Where: bhp = brake horsepower

F = flow (gpm)H = head (ft.)

PE = pump efficiency (%, as decimal)

$$bhp = whp/PE$$

Where:

bhp = brake horsepower

whp = water horsepower

PE = pump efficiency (%, as decimal)

$$mhp = \frac{F \times H}{3,960 \times PE \times ME}$$

Where:

mhp = motor horse power

F = flow (gpm)H = head (ft.)

PE = pump efficiency (%, as decimal) ME = motor efficiency (%, as decimal)

$$mhp = bhp/ME$$

Where:

mhp = motor horse power

Bhp = brake horsepower

ME = motor efficiency (%, as decimal)

 $ME = (bhp/mhp) \times 100\%$

 $PE = (whp/bhp) \times 100\%$

Where:

Where:

ME = motor efficiency (%)

bhp = brake horsepower

mhp = motor horse power

PE = pump efficiency (%)

whp = water horsepower

bhp = brake horsepower



Efficiency = $\frac{1}{2}$ hp output . Where: efficiency is % **x** 100% hp supplied Where: overall efficiency is % whp = water horsepowerOverall Efficiency = $(whp/mhp) \times 100\%$ mhp = motor horse power Where: wire to water efficiency is % Wire to water efficiency = whp whp = water horsepower mhp = motor horse powerPower input or mhp power input is hp ************************************* Where: wire to water efficiency is % PE = pump efficiency (%) Wire to water efficiency = (PE \times ME) \times 100% ME = motor efficiency (%) Where: Static Head in ft. Suction Lift in ft. Static Head = Suction lift + Discharge Head Discharge Head in ft. Where: Static Head in ft. Static Head = Discharge Head – Suction Head Discharge Head in ft. Suction Head in ft. Where: Friction Loss is ft. Friction Loss = (0.1) x (Static Head) Static Head is ft. ** use this formula in absence of other data Where: Total Dynamic Head is ft. Static Head is ft. Total Dynamic Head = Static Head + Friction Loss Friction Loss is ft. $Cost = (Motor hp) \times (0.746 kW/hp) \times (Cost,$ Where: Cost is \$/hr. $\frac{\text{W-hr}}{\text{w}}$



$DT = (V) \times (24 \text{ hr./day})$ Q	Where:	DT = detention time (hr.) V = volume of tank or basin (gal) Q = flow rate (gal/day)			
DT = (V)/(Q)	Where:	DT = detention time (days) V = volume of tank or basin (gal) Q = flow rate (gal/day)			
Weir Overflow Rate = $(Q)/(L)$	Where:	weir overflow rate = gal/day/ft. Q = flow rate (gal/day) L = total weir length (ft.)			
Weir Overflow Rate = Q (rectangular basin) $[2 \times (1)] + [2 \times (w)]$	Where:	weir overflow rate = gal/day/ft. Q = flow rate (gal/day) l = weir length (ft.) w = weir width (ft.)			
Weir Overflow Rate = Q . (circular basin) (3.14) \times (D)	Where:	weir overflow rate = gal/day/ft. Q = flow rate (gal/day) D = weir diameter (ft.)			
Surface Overflow Rate = $(Q)/(A)$	Where:	surface overflow rate = gal/day/ft ² Q = flow rate (gal/day) A = surface area (ft ²)			
<u>TRICKLING FILTERS</u>					
$HLR = (Q_1 + Q_2)/(A)$	Where:	HLR = hydraulic loading rate (gpd/ft²) Q_1 = primary effluent flow (gpd) Q_2 = recirculated flow (gpd) A = surface area (ft²)			
BOD ₅ of RBC = $(BOD_5)/(A)$	Where:	BOD ₅ of RBC = lbs./day/1,000 ft ² BOD ₅ = lbs./day A = surface area of media (1,000ft ²)			



$BOD_5 = (BOD_5)/(V)$	Where:	$BOD_5 = lbs./day/1,000 \text{ ft}^3$ $BOD_5 = lbs./day$ $V = volume \text{ of media (1,000ft}^3)$
$V = [(0.785) \times (D)^2 \times (d)]/1,000$	Where:	V = volume of media (1,000ft³) D = diameter of trickling filter (ft) d = media depth (ft)
$PE = (Q) \times (BOD_5) \times (8.34 \text{ lbs./gal})$ BOD	Where:	PE = population equivalent Q = flow (MGD) BOD ₅ = mg/L BOD = lbs./day/person
Recirculation Ratio = $(Q_2)/(Q_1)$	Where:	Q_2 = recirculated flow (MGD) Q_1 = primary effluent flow (MGD)
Recirculation Rate, $\% = [(Q_2)/(Q_1)] \times 100\%$	Where:	Q_2 = recirculated flow (MGD) Q_1 = primary effluent flow (MGD)
Reduction in flow, $\% = [(Q_{original} - Q_{reduced})/(Q_{original})]$	original)] X 100%	
	Where:	$Q_{\text{original}} = \text{original flow}$ $Q_{\text{reduced}} = \text{reduced flow}$
Reduction of volatile solids, $\% = \{(In - Out) / \}$		
	Where:	$VS = volatile solids, expressed as % If information (In \mathcal{C} Out) must be in decimal form$
Efficiency, $\% = = [(In - Out)/(In)] \times 100\%$	·-·-·	
BOD removed (lbs./day) = [BOD removed (n		
	Where:	O = flow (MGD)



SS removed (lbs./day) = [SS removed (mg/L)] \times (Q) \times (8.34 lbs./gal) Where: SS = suspended solidsQ = flow (MGD)<u>ACTIVATED SLUDGE</u> Where: $BOD_5 = mg/L$ $DO_I = initial DO (mg/L)$ $BOD_5 = (DO_1 - DO_F) \times 300$ $DO_F = final DO (mg/L)$ V_{sample} $V_{\text{sample}} = \text{sample volume (mL)}$ BOD bottle = 300 mLBOD loading = lbs./day Where: BOD₅ = biological oxygen demand BOD loading = $(BOD_5) \times (Q) \times (8.34 \text{ lbs./gal})$ (mg/L)Q = flow (MGD)Where: COD loading = lbs./dayCOD = chemical oxygen demand (mg/L)COD loading = $(COD) \times (Q) \times (8.34 \text{ lbs./gal})$ Q = flow (MGD)Where: MLSS = mixed liquor suspended solids MLSS (lbs.) = (MLSS, mg/L) x (V) x (8.34 lbs./gal) V = aerator volume (MG). Where: MLVSS = lbs.MLSS = mixed liquor suspended solids (mg/L) V = aerator volume (MG) $MLVSS = (MLSS) \times (V) \times (8.34 \text{ lbs./gal}) \times (VS)$ VS = volatile solids % (expressed as decimal) SVI = sludge volume index (mL/g)Where: $SSV_{wet} = wet settled sludge volume (mL)$ $SVI = (SSV_{wet}) \times (1,000)$

SSM_{dried}

 SSM_{dried} = dried sludge solids mass (mg)



 $SVI = (SSC) \times (1,000,000)$ **MLSS**

 $SVI = (SSV) \times (1,000 \text{ mg/g})$

MLSS

Where:

SVI = sludge volume index (mL/g)SSC = settleable solids concentration %

(expressed as decimal) MLSS = mixed liquor suspended solids

(mg/L)

Where:

SVI = sludge volume index (mL/g)SSV = settled sludge volume (mL/L)

MLSS = mixed liquor suspended solids

(mg/L)

SDI = (100)/(SVI)

Where:

SDI = sludge density index

SVI = sludge volume index (mL/g)

Seeded BOD

Where:

 $BOD_5 = lbs./day$

 $D_1 = DO$ of sample after prep (mg/L) $D_2 = DO$ of sample after 5-day incubation

at 20°C (mg/L)

S = oxygen uptake of seed

(S = 0 if sample not seeded)

 V_S = volume of seed in test bottle (mL) P = decimal volumetric fraction of

sample used. (1/P = dilution factor)

F/M Ratio ('Food to Mass' or 'Food to Microorganism' Ratio)

F/M ratio = (BOD or COD)

MLVSS

 $BOD_5 = (D_1 - D_2) - (S) \times (V_S)$

Where:

BOD = biological oxygen demand

(lbs./day)

COD = chemical oxygen demand

(lbs./day)

MLVSS = mixed liquor volatile suspended

solids (lbs.)

Where:

BOD = biological oxygen demand

(lbs./day)

F/M ratio = (BOD or COD) (MLSS) x (VS)

COD = chemical oxygen demand

(lbs./day)

MLSS = mixed liquor suspended solids (lbs.)

VS = volatile solids, % (expressed as

decimal)



Where: BOD = biological oxygen demand (mg/L) COD = chemical oxygen demand (mg/L)

Q = flow (MGD)

F/M ratio = (BOD or COD) x (Q) x (8.34 lbs./gal) MLVSS = mixed liquor volatile suspended (MLVSS) x (V) x (8.34 lbs./gal)

solids (mg/L)

V = aerator volume (MG)

Where: BOD = biological oxygen demand (mg/L)

COD = chemical oxygen demand (mg/L)

Q = flow (MGD)

F/M ratio = (BOD or COD) x (Q) x (8.34 lbs./gal)

(MLVSS) x (VS) x (V) x (8.34 lbs./gal)

MLVSS = mixed liquor volatile suspended solids (mg/L)

VS = volatile solids, % (expressed as

decimal)

V = aerator volume (MG)

Where: MLVSS = mixed liquor volatile suspended

solids (lbs.)

MLVSS (desired) = <u>(BOD or COD)</u>

F/M Ratio (desired)

BOD = biological oxygen demand (lbs./day)

COD = chemical oxygen demand

(lbs./day)

Where:

MLSS (desired) = MLVSS (desired)

MLSS = mixed liquor suspended solids (lbs.)

MLVSS = mixed liquor volatile suspended solids (lbs.)

VS = volatile solids, % (expressed as

decimal)

RAS (Return Activated Sludge)

Where:

RAS flow expressed as %

SSV = settled sludge volume (mL)

RAS flow = $\begin{bmatrix} Q_{RAS} \\ Q_{Influent} \end{bmatrix}$ **x** 100%

RAS flow_{final} = (RAS flow %) x Q

Where:

RAS flow expressed as % $Q_{RAS} = RAS \text{ flow (MGD)}$

 $Q_{Influent} = influent flow (MGD)$

Where:

RAS flow_{final} = final RAS flow (gal/day) RAS flow % is expressed as decimal

Q = flow (gpd)



RAS flow = $(Q_{Influent}) \times (MLSS)$ (RSC) - (MLSS)

RSC = (1,000,000)/(SVI)

Where: RAS flow = gal/day

> $Q_{Influent} = aerator influent flow (gpd)$ MLSS = mixed liquor suspended solids

(mg/L)

RSC = return sludge concentration (mg/L)

Where: RSC = return sludge concentration (mg/L)

SVI = sludge volume index (mL/g)

(SVI calculations in 'Activated Sludge' section)

Where: RAS = return activated sludge

MLSS = mixed liquor suspended solids RAS (solids balance) = $\underline{\text{(MLSS)} \times \text{(Q)}}$

Q = flow rate

RAS SS = return activated sludge

suspended solids

MCRT or SRT ('Mean Cell Residence Time' or 'Solids Retention Time')

(RAS SS) - (MLSS)

 $MLSS_{final} = (MLSS_{actual}) \times (V) \times (8.34 lbs./gal)$

(WAS SS) + (SE SS)

Where: $MLSS_{final} = final actual MLSS (lbs.)$

 $MLSS_{actual} = actual MLSS (mg/L)$

V = aerator volume (MG)

Where: MCRT = days

 $MCRT = (SS_{in})/(SS_{leaving})$ SS_{in} = suspended solids in system (lbs.)

SS_{leaving} = suspended solids leaving system

(lbs./day)

Where: MCRT = days

MCRT = SS_{in} = suspended solids in system (lbs.)

WAS SS = waste activated sludge SS

(lbs./day)

SE SS = secondary effluent SS

(lbs./day)

NO CLARIFIER INFO GIVEN:

MCRT =(MLSS) x (V) x (8.34 lbs./gal) $[(WAS SS) \times (Q_{WAS}) \times (8.34 lbs./gal)] + [(SE SS) \times (Q_{Plant}) \times (8.34 lbs./gal)]$

> Where: MCRT = days

> > MLSS = mixed liquor suspended solids (mg/L)

V = aerator volume (MG)

WAS SS =waste activated sludge SS (mg/L)

 $Q_{WAS} = WAS \text{ flow (MGD)}$

SE SS = secondary effluent SS (mg/L)

 $Q_{Plant} = plant flow (MGD)$



FINAL CLARIFIER VOLUME GIVEN BUT NO CLARIFIER CORE SUSPENDED SOLIDS (CCSS):

 $MCRT = \underbrace{(MLSS) \times [(V_{acrator}) + (V_{clarifier})] \times (8.34 \text{ lbs./gal})}_{\text{[(WAS SS)} \times (Q_{WAS}) \times (8.34 \text{ lbs./gal})] + [(SE SS) \times (Q_{Plant}) \times (8.34 \text{ lbs./gal})]}_{\text{[(WAS SS)} \times (Q_{WAS}) \times (8.34 \text{ lbs./gal})]}$

Where: MCRT = days

MLSS = mixed liquor suspended solids (mg/L)

 $V_{aerator}$ = aerator volume (MG) $V_{clarifier}$ = final clarifier volume (MG)

WAS SS = waste activated sludge SS (mg/L)

 $Q_{WAS} = WAS \text{ flow (MGD)}$

SE SS = secondary effluent SS (mg/L)

 $Q_{Plant} = plant flow (MGD)$

FINAL CLARIFIER VOLUME & CLARIFIER CORE SUSPENDED SOLIDS (CCSS) GIVEN:

$$\begin{split} \text{MCRT} = & \underline{\text{[(MLSS)} \times \text{($V_{aerator})} \times (8.34 \text{ lbs./gal)]} + \text{[(CCSS)} \times \text{($V_{clarifier})} \times (8.34 \text{ lbs./gal)]}} \\ & \underline{\text{[(WAS SS)} \times \text{($Q_{WAS})} \times (8.34 \text{ lbs./gal)]} + \text{[(SE SS)} \times \text{($Q_{Plant})} \times (8.34 \text{ lbs./gal)]}} \end{split}$$

Where: MCRT = days

MLSS = mixed liquor suspended solids (mg/L)

 $V_{aerator} = aerator volume (MG)$

CCSS = clarifier core suspended solids (mg/L)

 $V_{clarifier}$ = final clarifier volume (MG)

WAS SS = waste activated sludge SS (mg/L)

 $Q_{WAS} = WAS \text{ flow (MGD)}$

SE SS = secondary effluent SS (mg/L)

 $Q_{Plant} = plant flow (MGD)$

 $MCRT = \frac{TSS_{Aeration} + TSS_{Clarifier}}{TSS_{Wasted} + TSS_{Effluent}}.$

Where: MCRT = days

TSS_{Aeration} = aeration tank TSS (lbs.) TSS_{Clarifier} = clarifier TSS (lbs.) TSS_{Wasted} = TSS wasted (lbs./day) TSS_{Effluent} = effluent TSS (lbs./day)

Waste Activated Sludge (WAS)

$$WAS = \left[\begin{array}{c} \underline{\text{(MLSS)} \ \textbf{x} \ (V_{aerator}) \ \textbf{x} \ (8.34 \ lbs./gal)}} \\ MCRT \end{array} \right] - \left[(SE \ SS) \ \textbf{x} \ (Q_{Plant}) \ \textbf{x} \ (8.34 \ lbs./gal) \right]$$

Where: WAS = lbs./day

MLSS = mixed liquor suspended solids (mg/L)

 $V_{aerator} = aerator volume (MG)$

MCRT = days

SE SS = secondary effluent SS (mg/L)

 $Q_{Plant} = plant flow (MGD)$



 $MLSS_{final} = MLSS$ to waste (gal) $MLSS_{initial} = MLSS$ to waste (lbs.) RAS = RAS concentration (mg/L Where: min. to WS = minutes to waste sludge $Min. to WS = \underline{MLSS}$ MLSS = MLSS to waste (gal) WS Pump Capacity WS pump capacity = waste sludge pump capacity (gal/min.) Where: min/hr. to WS = minutes per hour to Min/Hr. to WS = WSwaste sludge 24hrs./day WS = min per day to waste sludge Wastewater Treatment Ponds Where: PL = population loading PL = (Population)/(A)(persons/acre) Population = population served (persons) A = pond area (acres)Where: V = pond volume (ac-ft.) $V = (A) \times (d)$ A = pond area (acres)d = pond depth (ft.)Where: V = pond volume (ac-ft.)L = length (ft.) $V = [(L) \times (W) \times (d)]/(43,560 \text{ ft}^2/\text{ac})$ W = length (ft.)d = pond depth (ft.) $V \text{ (gal)} = [V \text{ (ac-ft.)}] \times (43,560 \text{ ft}^2/\text{ac}) \times (7.48 \text{ gal/ft}^3)$ V = pond volumeWhere: Where: A = pond area (acre)L = length (ft.) $A = [(L) \times (W)]/(43,560 \text{ ft}^2/\text{ac})$ W = length (ft.)



$Q \; (ac\text{-}ft./day) = [Q \; (gal/day)]/[(7.48 \; gal/ft^3) \; \textbf{x}$	(43,560 ft ²)	/ac)]
	Where:	Q = flow
DT = (V)/(Q)	Where:	DT = detention time (days) V = volume (gal) Q = flow (gal/day)
DT = (V)/(Q)	Where:	DT = detention time (days) V = volume (ac-ft.) Q = flow (ac-ft./day)
BOD loading = (BOD ₅) \times (Q) \times (8.34 lbs./gal)	Where:	BOD loading = lbs./day BOD ₅ = biological oxygen demand (MGD) $Q = flow (MGD)$
OLR = (BOD)/(A)	Where:	OLR = organic loading rate (lbs./day/acre) BOD = influent BOD (lbs./day) A = pond areas (acres)
OLR = [(BOD) x (Q) x (8.34 lbs/gal)]/(A)	Where:	OLR = organic loading rate (lbs./day/acre BOD = influent BOD (mg/L) Q = flow (MGD) A = pond areas (acres)
BOD removal efficiency, $\%$ = [(BOD _{removed})/(BOD _{total})] X	100%
	Where:	$\begin{split} &\mathrm{BOD}_{\mathrm{removed}} = \mathrm{BOD} \ \mathrm{removed} \ (\mathrm{mg/L}) \\ &\mathrm{BOD}_{\mathrm{total}} = \mathrm{total} \ \mathrm{BOD} \ (\mathrm{mg/L}) \end{split}$
$HLR = [(Q)/(A)] \times 12 \text{ in/ft.}$	Where:	HLR = hydraulic loading rate (in/day) Q = flow (ac-ft./day) A = pond area (acres)



Where: Loading is TSS or BOD = lbs./day

Concentration of TSS or BOD = mg/L

Q = flow

Hydraulic loading rate = $\underline{\text{Flow}}$ Where: Hydraulic Loading = gpd/ft²

Flow = gpd $A = area (ft^2)$

Where: Surface Loading/Surface Overflow rate

Surface loading rate or Surface overflow rate = $\underline{\text{Flow}}$

Loading = (Concentration) x (Q) x (8.34 lbs./gal)

Flow = gpd

 $A = area (ft^2)$

LABORATORY FORMULAS

Alkalinity & Hardness

 $P = (A) \times (N) \times (50,000)$

 V_{sample}

 V_{sample}

 V_{sample}

Where: P = phenoltphthalein alkalinity (mg CaCO₃/L)

A = titrant volume used to reach 8.3 pH

(mL)

in gpd/ft²

N = acid normality

 $V_{\text{sample}} = \text{sample volume (mL)}$

Where: $T = \text{total alkalinity (mg CaCO}_3/L)$ $T = (B) \times (N) \times (50,000)$

B = total titrant used (mL)N = acid normality

 $V_{\text{sample}} = \text{sample volume (mL)}$

Where: $Hardness = mg CaCO_3/L$ Hardness = $(B) \times (1,000)$

B = titrant volume (mL)

 $V_{\text{sample}} = \text{sample volume (mL)}$

Only when the titration factor is 1.00 of EDTA

Bacteriological

Average (arithmetic mean) = (sum of all terms)/(number of terms)

Average (geometric mean) = ${}^{n}\sqrt{(X_1)(X_2)(X_3)(X_4)\dots(X_n)}$ The nth root of the product of n numbers



$$BC = \underbrace{(CC) \times (100)}_{V}$$

Where: BC = bacteriological colonies/100 mL CC = number of colonies counted V = sample volume filtered (mL)

Laboratory Solutions Formulas

$$(N_1 \times V_1) + (N_2 \times V_2) = (N_3 \times V_3)$$

Where: $V_1 + V_2 = V_3$ N = normality

 $(\mathbf{N}_1 \times \mathbf{V}_1) = (\mathbf{N}_2 \times \mathbf{V}_2)$

V = volume or flow

 $Milliequivalent = mL \times Normality$

 $\begin{aligned} \text{Molarity} &= \underline{\text{Moles of solute }}. \\ &\quad \text{Liters of solution} \end{aligned}$

Normality = <u>Number of equivalent weights of solute</u> Liters of solution

Number of equivalent weights = <u>Total Weight</u>. Equivalent Weight

Number of Moles = <u>Total Weight</u>.

Molecular Weight

Specific gravity = Specific weight of substance, lbs./gal Specific weight of water, lbs./gal

Oxygen Uptake Rate (OUR)

Where: respiration rate = mg/g/hr.

Respiration Rate = (OUR)/(MLSS) OUR = oxygen uptake rate (mg/L/hr.)

MLSS = mixed liquor suspended solids

(g/L)

OUR mgL/min = $OO_{starting} - OO_{ending}$ x 60 min where: OUR = mg/L/hr. $OO_{starting} = starting DO (mg/L)$



 $DO_{ending} = ending DO (mg/L)$ T = elapsed time (min)Load Index = $(OUR_{fed})/(OUR_{unfed})$ Where: $OUR_{fed} = fed OUR (mg/L/hr.)$ $OUR_{unfed} = unfed OUR (mg/L/hr.)$ Where: SOUR = specific OUR (mg $O_2/hr./g$) OUR = oxygen uptake rate (mg/L/hr.) $SOUR = (OUR) \times (1,000 \text{ mg/g})$ MLSS = mixed liquor volatile suspended **MLVSS** solids (g/L) Solids Where: SS = suspended solids (mg/L)A = final weight of pan, filter & residue (g) $SS = (A - B) \times (1,000,000)$ B = weight of prepared filter & pan (g) V_{sample} $V_{\text{sample}} = \text{sample volume (mL)}$ TS = total solids (mg/L)Where: $TS = (C - D) \times (1,000,000)$ C = weight of dish & dried solids (g) V_{sample} D = weight of dish (g) $V_{\text{sample}} = \text{sample volume (mL)}$ Where: VS = volatile solids (mg/L) $VS = (C - E) \times (1,000,000)$ C = weight of dish & dried solids (g) V_{sample} E = weight of dish & ash (g) $V_{\text{sample}} = \text{sample volume (mL)}$ Where: FS = fixed solids (mg/L) $FS = (C - D) \times (1,000,000)$ E = weight of dish & ash (g)V_{sample} D = weight of dish (g) $V_{\text{sample}} = \text{sample volume (mL)}$ Volatile solids = $\underline{\text{Dry solids}}$ - Fixed solids $\times 100\%$ Volatile solids (as %) Where: Dry solids Dry solids in grams Fixed solids = inorganics (g) Where: VS = volatile solids (mg/L) $% VS = {(VS)/(TS)} \times 100\%$ TS = total solids (mg/L)



$$SC = (W)/(V)$$

Where: SC = solids concentration (mg/L)

> W = weight (mg)V = volume (L)

Temperature Conversions

$$^{\circ}$$
C = ($^{\circ}$ F – 32) **x** (0.566)

°C = degrees Celsius Where:

$$^{\circ}F = (^{\circ}C \times 1.8) + 32$$

Average Formulas

Average (arithmetic mean) = (sum of all terms)/(number of terms)

Average (geometric mean) =
$${}^{n}\sqrt{(X_1)(X_2)(X_3)(X_4)...(X_n)}$$

The nth root of the product of n numbers

FORCE

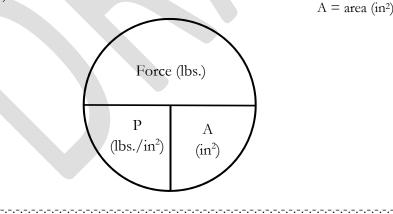
Where:

F = force (lbs.)

 $F = (P) \times (A)$

 $P = pressure (psi or lbs./in^2)$

 $A = area (in^2)$



Coagulation/Flocculation Formulas

 $DT = (V) \times (1,440 \text{ min/day}) \times (60 \text{ sec/min})$

Where:

DT = detention time (sec)

V = volume (gal)

Q = flow rate(gal/day)



$$DT = \underbrace{(V) \times (1,440 \text{ min/day})}{Q} \qquad Where: \qquad DT = \text{detention time (min)} \\ V = \text{volume (gal)} \\ Q = \text{flow rate (gal/day)}$$

$$Filter Formulas$$

$$Backwash rise rate = \underbrace{Backwash \text{ rate} \times 12 \text{ in/ft.}}_{7.48 \text{ gal/ft}} \text{ Where:} \qquad backwash rinse rate = in/min.}_{backwash \text{ rate } \text{egpm/ft}^2}$$

$$V = (R) \times (T) \times (A) \qquad Where: \qquad V = \text{backwash water volume (gal)}_{R} = \text{backwash time (min)}_{A} = \text{filter area (ft}^2)$$

$$Yield = \underbrace{\begin{bmatrix} Backwash \text{ water } \\ Water \text{ Filtered} \end{bmatrix}}_{X \text{ 100\%}} \times 100\% \qquad Where: \qquad yield = \text{backwash water yield, \%}_{backwash \text{ water } \text{gal water filtered}} = \text{gal water filtered} = \text{gal}$$

$$Flow/Backwash \text{ rate} = (Q)/(A) \qquad Where: \qquad flow/backwash \text{ rate} = \text{gpm/ft}^2$$

$$Q = \text{flow (gpm)}_{A} = \text{filter area (ft}^2)$$

$$Filtration \text{ Rate} = (V)/(T) \qquad Where: \qquad \text{filtration rate} = \text{gpm}_{A} \times 100\% = \text{filtratio$$

Where:

Filter Production Rate = $(R) \times (A)$

 $A = filter area (ft^2)$

filter production rate = gal/min

 $R = filtration rate (gpm/ft^2)$



Yield = (Loading) x (Recovery).
(Filter operation) x (A)

Where:

yield = lbs./hr./ ft²

loading = solids loading (lbs./day) recovery = %, expressed as a decimal

filter operation = hr./day

 $A = area (ft^2)$

......

SEDIMENTATION

Where:

DT = detention time, hr.

Vol = volume of tank (gal) Q = flow rate (cal/day)

Q = flow rate (gal/day)

Weir Overflow rate = F/L

 $DT = (Vol \times 24 hr./day)/Q$

Where:

overflow rate = gal/day/ft.

F = flow (gal/day)

L = total weir length (ft.)

Weir Length (Rectangular Basin)

Weir length = $(2 \times L) + (2 \times W)$

Weir Length (Circular Basin)

Weir length = $3.14 \times D$

Where:

weir length = ft.

L = length (ft.)

W = width (ft.)

D = diameter (ft.)

Weir Overflow rate (Rectangular Basin)

Overflow rate = $F/[(2 \times L) + (2 \times W)]$

Weir Overflow rate (Circular Basin) Overflow rate = F/(3.14 × D) Where:

overflow rate = gal/day/ft.

F = flow (gal/day)

L = length (ft.) W = width (ft.)

D = diameter (ft.)

......

Surface Overflow rate = F/A

Where:

overflow rate = $gal/day/ft^2$

F = flow (gal/day)

 $A = surface area (ft^2)$

Solids Loading rate = Solids Applied/A

Where:

loading rate = $lbs./day/ft^2$

solids applied = lbs./day $A = surface area (ft^2)$

Solids Loading rate (Rectangular Basin)

 $Loading \ rate = Solids \ Applied/(L \ \textbf{x} \ W)$

Solids Loading rate (Circular Basin)
Loading rate = Solids Applied/(0.785 x D)

Where:

loading rate is lbs./day/ft2

solids applied is lbs./day L = length (ft.)

W = width (ft.)

D = diameter (ft.)



BOD removed (lbs./day) = BOD removed x F x 8.34 lbs.	Where: ./gal	BOD removed is mg/L F = Flow (MGD)
SS Removed (lbs./day) = SS Removed × F × 8.34 lbs./gal	Where:	SS removed is mg/L F = Flow (MGD)
Efficiency = [(In – Out)/In] x 100%		
-	WET WELL	
Cycle time (min) = $\frac{SV}{PC - Inflow}$.	Where:	SV = storage volume (gal) PC = pump capacity (gpm) Inflow = wet well inflow (gpm)
***********		,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,
COLL	ECTION SYSTE	<u>M</u>
Slope, $\% = \begin{bmatrix} \underline{\text{Drop or rise}} \\ \text{Distance} \end{bmatrix} x 100\%$	OR	Slope, $\% = \left[\frac{\text{Rise}}{\text{Run}}\right] \times 100\%$
*************		vonnennenne
Velocity = F/A	Where:	Velocity is ft./sec F = flow (ft ³ /sec) A = area (ft ²)
$Velocity = \frac{Distance}{Time}$	Where:	Velocity is ft./sec D = distance (ft.) T = time (sec)